

11.1 Hot Mix Asphalt Plants

11.1.1 General^{1-3,23, 392-394}

Hot mix asphalt (HMA) paving materials are a mixture of size-graded, high quality aggregate (which can include reclaimed asphalt pavement [RAP]), and liquid asphalt cement, which is heated and mixed in measured quantities to produce HMA. Aggregate and RAP (if used) constitute over 92 percent by weight of the total mixture. Aside from the amount and grade of asphalt cement used, mix characteristics are determined by the relative amounts and types of aggregate and RAP used. A certain percentage of fine aggregate (less than 74 micrometers [μm] in physical diameter) is required for the production of good quality HMA.

Hot mix asphalt paving materials can be manufactured by: (1) batch mix plants, (2) continuous mix (mix outside dryer drum) plants, (3) parallel flow drum mix plants, and (4) counterflow drum mix plants. This order of listing generally reflects the chronological order of development and use within the HMA industry.

In 1996, approximately 500 million tons of HMA were produced at the 3,600 (estimated) active asphalt plants in the United States. Of these 3,600 plants, approximately 2,300 are batch plants, 1,000 are parallel flow drum mix plants, and 300 are counterflow drum mix plants. The total 1996 HMA production from batch and drum mix plants is estimated at about 240 million tons and 260 million tons, respectively. About 85 percent of plants being manufactured today are of the counterflow drum mix design, while batch plants and parallel flow drum mix plants account for 10 percent and 5 percent respectively. Continuous mix plants represent a very small fraction of the plants in use (≤ 0.5 percent) and, therefore, are not discussed further.

An HMA plant can be constructed as a permanent plant, a skid-mounted (easily relocated) plant, or a portable plant. All plants can have RAP processing capabilities. Virtually all plants being manufactured today have RAP processing capability. Most plants have the capability to use either gaseous fuels (natural gas) or fuel oil. However, based upon Department of Energy and limited State inventory information, between 70 and 90 percent of the HMA is produced using natural gas as the fuel to dry and heat the aggregate.

11.1.1.1 Batch Mix Plants –

Figure 11.1-1 shows the batch mix HMA production process. Raw aggregate normally is stockpiled near the production unit. The bulk aggregate moisture content typically stabilizes between 3 to 5 percent by weight.

Processing begins as the aggregate is hauled from the storage piles and is placed in the appropriate hoppers of the cold feed unit. The material is metered from the hoppers onto a conveyer belt and is transported into a rotary dryer (typically gas- or oil-fired). Dryers are equipped with flights designed to shower the aggregate inside the drum to promote drying efficiency.

As the hot aggregate leaves the dryer, it drops into a bucket elevator and is transferred to a set of vibrating screens, where it is classified into as many as four different grades (sizes) and is dropped into individual “hot” bins according to size. At newer facilities, RAP also may be transferred to a separate heated storage bin. To control aggregate size distribution in the final batch mix, the operator opens various hot bins over a weigh hopper until the desired mix and weight are obtained. Concurrent with the

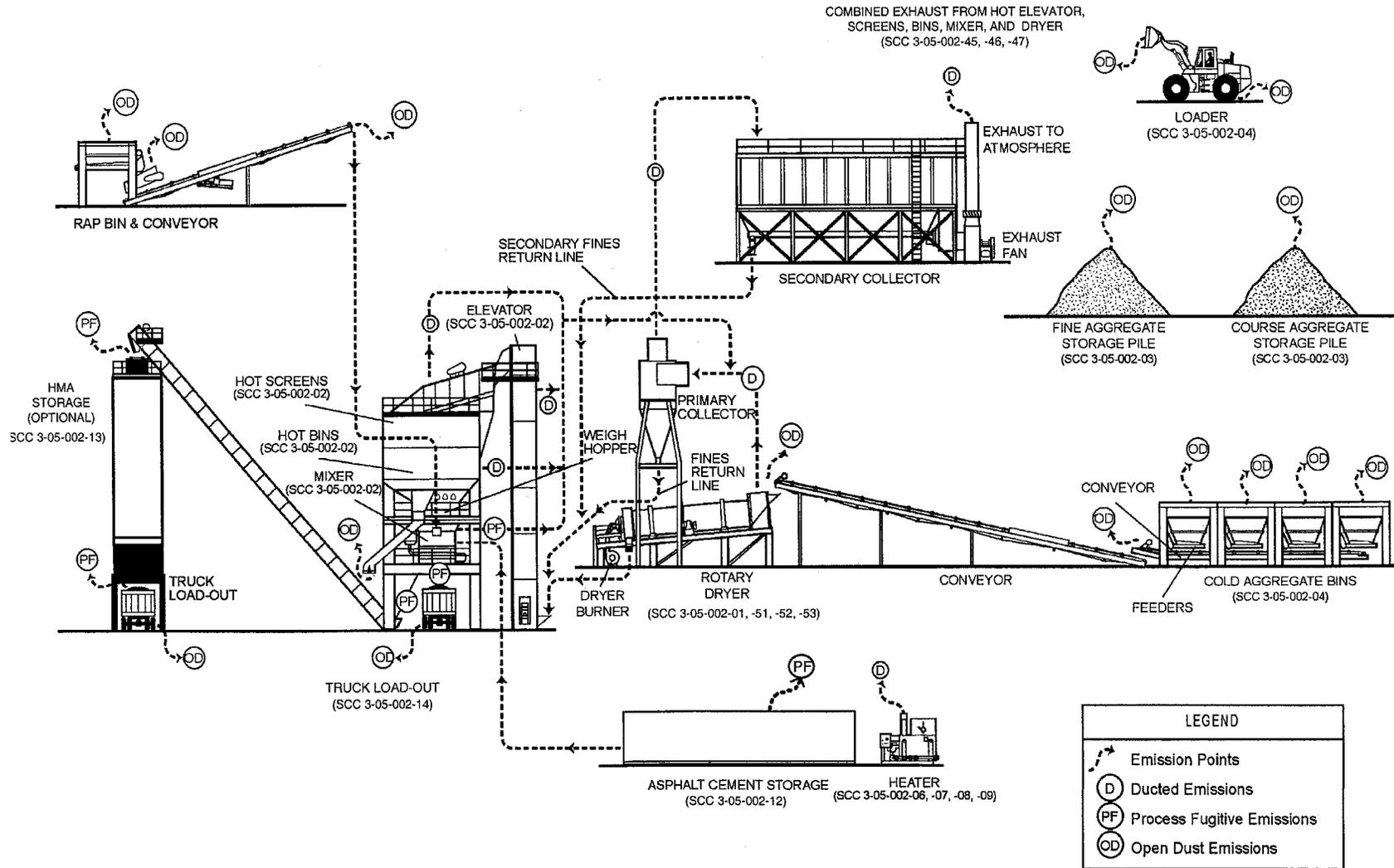


Figure 11.1-1. General process flow diagram for batch mix asphalt plants (source classification codes in parentheses).³

aggregate being weighed, liquid asphalt cement is pumped from a heated storage tank to an asphalt bucket, where it is weighed to achieve the desired aggregate-to-asphalt cement ratio in the final mix.

The aggregate from the weigh hopper is dropped into the mixer (pug mill) and dry-mixed for 6 to 10 seconds. The liquid asphalt is then dropped into the pug mill where it is mixed for an additional period of time. At older plants, RAP typically is conveyed directly to the pug mill from storage hoppers and combined with the hot aggregate. Total mixing time usually is less than 60 seconds. Then the hot mix is conveyed to a hot storage silo or is dropped directly into a truck and hauled to the job site.

11.1.1.2 Parallel Flow Drum Mix Plants –

Figure 11.1-2 shows the parallel flow drum mix process. This process is a continuous mixing type process, using proportioning cold feed controls for the process materials. The major difference between this process and the batch process is that the dryer is used not only to dry the material but also to mix the heated and dried aggregates with the liquid asphalt cement. Aggregate, which has been proportioned by size gradations, is introduced to the drum at the burner end. As the drum rotates, the aggregates, as well as the combustion products, move toward the other end of the drum in parallel. Liquid asphalt cement flow is controlled by a variable flow pump electronically linked to the new (virgin) aggregate and RAP weigh scales. The asphalt cement is introduced in the mixing zone midway down the drum in a lower temperature zone, along with any RAP and particulate matter (PM) from collectors.

The mixture is discharged at the end of the drum and is conveyed to either a surge bin or HMA storage silos, where it is loaded into transport trucks. The exhaust gases also exit the end of the drum and pass on to the collection system.

Parallel flow drum mixers have an advantage, in that mixing in the discharge end of the drum captures a substantial portion of the aggregate dust, therefore lowering the load on the downstream PM collection equipment. For this reason, most parallel flow drum mixers are followed only by primary collection equipment (usually a baghouse or venturi scrubber). However, because the mixing of aggregate and liquid asphalt cement occurs in the hot combustion product flow, organic emissions (gaseous and liquid aerosol) may be greater than in other asphalt mixing processes. Because data are not available to distinguish significant emissions differences between the two process designs, this effect on emissions cannot be verified.

11.1.1.3 Counterflow Drum Mix Plants –

Figure 11.1-3 shows a counterflow drum mix plant. In this type of plant, the material flow in the drum is opposite or counterflow to the direction of exhaust gases. In addition, the liquid asphalt cement mixing zone is located behind the burner flame zone so as to remove the materials from direct contact with hot exhaust gases.

Liquid asphalt cement flow is controlled by a variable flow pump which is electronically linked to the virgin aggregate and RAP weigh scales. It is injected into the mixing zone along with any RAP and particulate matter from primary and secondary collectors.

Because the liquid asphalt cement, virgin aggregate, and RAP are mixed in a zone removed from the exhaust gas stream, counterflow drum mix plants will likely have organic emissions (gaseous and liquid aerosol) that are lower than parallel flow drum mix plants. However, the available data are insufficient to discern any differences in emissions that result from differences in the two processes. A counterflow drum mix plant can normally process RAP at ratios up to 50 percent with little or no observed effect upon emissions.

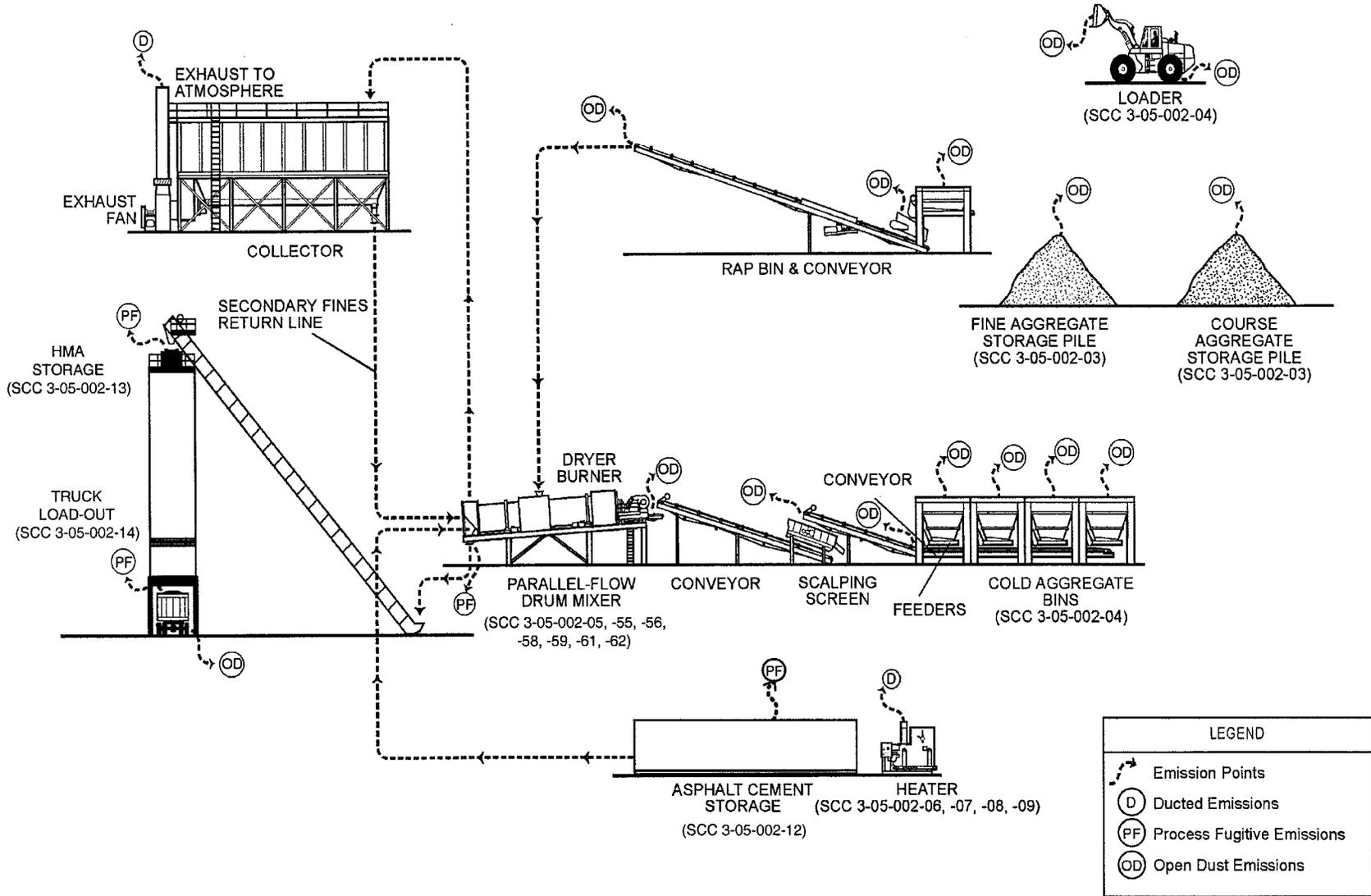


Figure 11.1-2. General process flow diagram for parallel-flow drum mix asphalt plants (source classification codes in parentheses).³

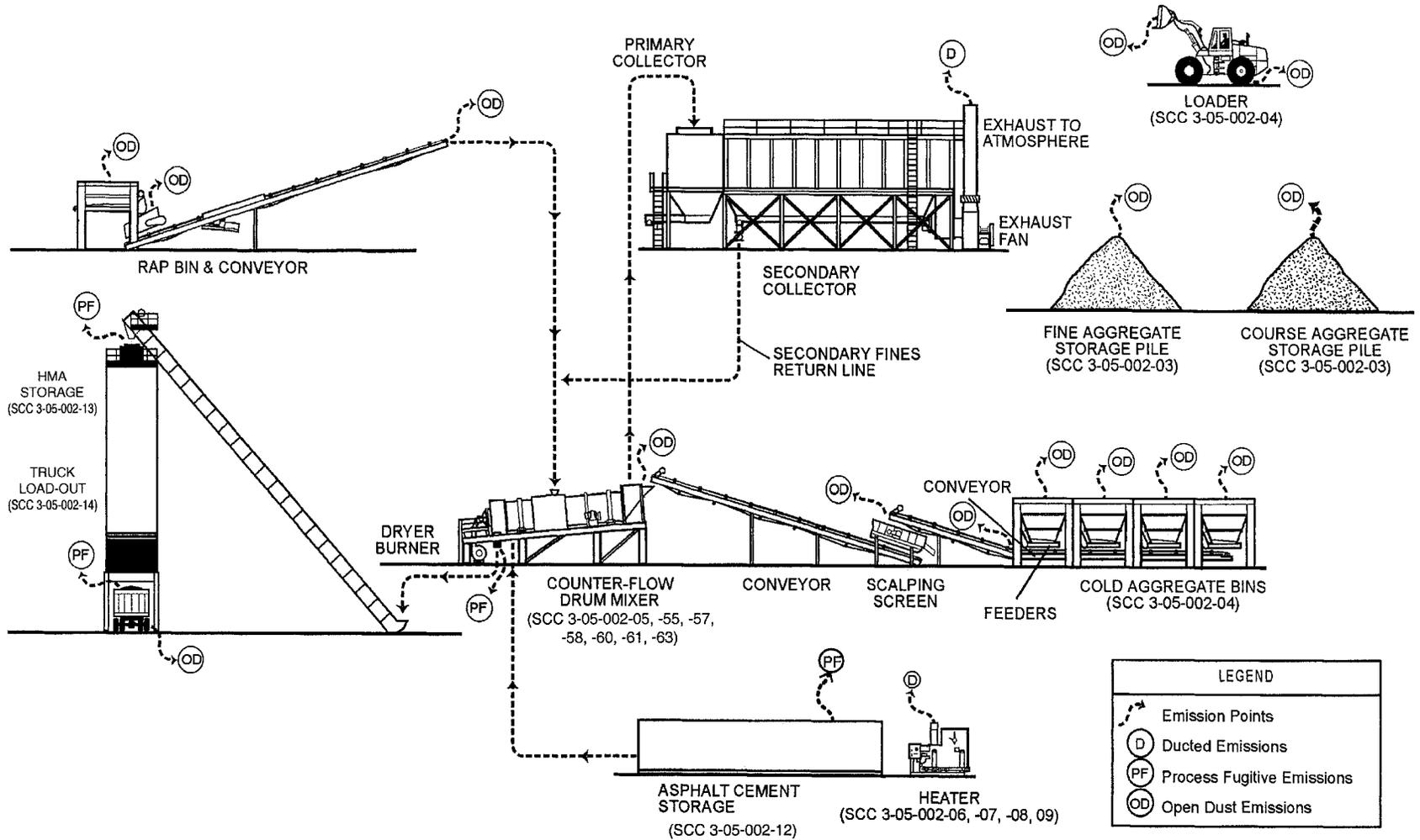


Figure 11.1-3. General process flow diagram for counter-flow drum mix asphalt plants (source classification codes in parentheses).³

11.1.1.4 Recycle Processes³⁹³ –

In recent years, the use of RAP has been initiated in the HMA industry. Reclaimed asphalt pavement significantly reduces the amount of virgin rock and asphalt cement needed to produce HMA.

In the reclamation process, old asphalt pavement is removed from the road base. This material is then transported to the plant, and is crushed and screened to the appropriate size for further processing. The paving material is then heated and mixed with new aggregate (if applicable), and the proper amount of new asphalt cement is added to produce HMA that meets the required quality specifications.

11.1.2 Emissions And Controls^{2-3,23}

Emissions from HMA plants may be divided into ducted production emissions, pre-production fugitive dust emissions, and other production-related fugitive emissions. Pre-production fugitive dust sources associated with HMA plants include vehicular traffic generating fugitive dust on paved and unpaved roads, aggregate material handling, and other aggregate processing operations. Fugitive dust may range from 0.1 μm to more than 300 μm in aerodynamic diameter. On average, 5 percent of cold aggregate feed is less than 74 μm (minus 200 mesh). Fugitive dust that may escape collection before primary control generally consists of PM with 50 to 70 percent of the total mass less than 74 μm . Uncontrolled PM emission factors for various types of fugitive sources in HMA plants are addressed in Sections 11.19.2, “Crushed Stone Processing”, 13.2.1, “Paved Roads”, 13.2.2, “Unpaved Roads”, 13.2.3, “Heavy Construction Operations”, and 13.2.4, “Aggregate Handling and Storage Piles.” Production-related fugitive emissions and emissions from ducted production operations are discussed below. Emission points discussed below refer to Figure 11.1-1 for batch mix asphalt plants and to Figures 11.1-2 and 11.1-3 for drum mix plants.

11.1.2.1 Batch Mix Plants –

As with most facilities in the mineral products industry, batch mix HMA plants have two major categories of emissions: ducted sources (those vented to the atmosphere through some type of stack, vent, or pipe), and fugitive sources (those not confined to ducts and vents but emitted directly from the source to the ambient air). Ducted emissions are usually collected and transported by an industrial ventilation system having one or more fans or air movers, eventually to be emitted to the atmosphere through some type of stack. Fugitive emissions result from process and open sources and consist of a combination of gaseous pollutants and PM.

The most significant ducted source of emissions of most pollutants from batch mix HMA plants is the rotary drum dryer. The dryer emissions consist of water (as steam evaporated from the aggregate); PM; products of combustion (carbon dioxide [CO_2], nitrogen oxides [NO_x], and sulfur oxides [SO_x]); carbon monoxide (CO); and small amounts of organic compounds of various species (including volatile organic compounds [VOC], methane [CH_4], and hazardous air pollutants [HAP]). The CO and organic compound emissions result from incomplete combustion of the fuel. It is estimated that between 70 and 90 percent of the energy used at HMA plants is from the combustion of natural gas.

Other potential process sources include the hot-side conveying, classifying, and mixing equipment, which are vented either to the primary dust collector (along with the dryer gas) or to a separate dust collection system. The vents and enclosures that collect emissions from these sources are commonly called “fugitive air” or “scavenger” systems. The scavenger system may or may not have its own separate air mover device, depending on the particular facility. The emissions captured and transported by the scavenger system are mostly aggregate dust, but they may also contain gaseous organic compounds and a fine aerosol of condensed organic particles. This organic aerosol is created by the condensation of vapor into particles during cooling of organic vapors volatilized from the asphalt cement in the mixer (pug mill).

The amount of organic aerosol produced depends to a large extent on the temperature of the asphalt cement and aggregate entering the pug mill. Organic vapor and its associated aerosol also are emitted directly to the atmosphere as process fugitives during truck load-out, from the bed of the truck itself during transport to the job site, and from the asphalt storage tank. Both the low molecular weight organic compounds and the higher weight organic aerosol contain small amounts of HAP. The ducted emissions from the heated asphalt storage tanks include gaseous and aerosol organic compounds and combustion products from the tank heater.

The choice of applicable emission controls for PM emissions from the dryer and vent line includes dry mechanical collectors, scrubbers, and fabric filters. Attempts to apply electrostatic precipitators have met with little success. Practically all plants use primary dust collection equipment such as large diameter cyclones, skimmers, or settling chambers. These chambers often are used as classifiers to return collected material to the hot elevator and to combine it with the drier aggregate. To capture remaining PM, the primary collector effluent is ducted to a secondary collection device. Most plants use either a fabric filter or a venturi scrubber for secondary emissions control. As with any combustion process, the design, operation, and maintenance of the burner provides opportunities to minimize emissions of NO_x , CO, and organic compounds.

11.1.2.2 Parallel Flow Drum Mix Plants –

The most significant ducted source of emissions from parallel-flow drum mix plants is the rotary drum dryer. Emissions from the drum consist of water (as steam evaporated from the aggregate); PM; products of combustion; CO; and small amounts of organic compounds of various species (including VOC, CH_4 , and HAP). The organic compound and CO emissions result from incomplete combustion of the fuel and from heating and mixing of the liquid asphalt cement inside the drum. Although it has been suggested that the processing of RAP materials at these type plants may increase organic compound emissions because of an increase in mixing zone temperature during processing, the data supporting this hypothesis are very weak. Specifically, although the data show a relationship only between RAP content and condensible organic particulate emissions, 89 percent of the variations in the data were the result of other unknown process variables.

Once the organic compounds cool after discharge from the process stack, some condense to form a fine organic aerosol or “blue smoke” plume. A number of process modifications or restrictions have been introduced to reduce blue smoke, including installation of flame shields, rearrangement of flights inside the drum, adjustments of the asphalt injection point, and other design changes.

11.1.2.3 Counterflow Drum Mix Plants –

The most significant ducted source of emissions from counterflow drum mix plants is the rotary drum dryer. Emissions from the drum consist of water (as steam evaporated from the aggregate); PM; products of combustion; CO; and small amounts of organic compounds of various species (including VOC, CH_4 , and HAP). The CO and organic compound emissions result primarily from incomplete combustion of the fuel, and can also be released from the heated asphalt. Liquid asphalt cement, aggregate, and sometimes RAP, are mixed in a zone not in contact with the hot exhaust gas stream. As a result, kiln stack emissions of organic compounds from counterflow drum mix plants may be lower than parallel flow drum mix plants. However, variations in the emissions due to other unknown process variables are more significant. As a result, the emission factors for parallel flow and counterflow drum mix plants are the same.

11.1.2.4 Parallel and Counterflow Drum Mix Plants –

Process fugitive emissions associated with batch plant hot screens, elevators, and the mixer (pug mill) are not present in the drum mix processes. However, there are fugitive PM and VOC emissions from transport and handling of the HMA from the drum mixer to the storage silo and also from the load-out operations to the delivery trucks. Since the drum process is continuous, these plants have surge bins or storage silos. The fugitive dust sources associated with drum mix plants are similar to those of batch mix plants with regard to truck traffic and to aggregate material feed and handling operations.

Table 11.1-1 presents emission factors for filterable PM and PM-10, condensable PM, and total PM for batch mix HMA plants. Particle size data for batch mix HMA plants, based on the control technology used, are shown in Table 11.1-2. Table 11.1-3 presents filterable PM and PM-10, condensable PM, and total PM emission factors for drum mix HMA plants. Particle size data for drum mix HMA plants, based on the control technology used, are shown in Table 11.1-4. Tables 11.1-5 and -6 present emission factors for CO, CO₂, NO_x, sulfur dioxide (SO₂), total organic compounds (TOC), formaldehyde, CH₄, and VOC from batch mix plants. Tables 11.1-7 and -8 present emission factors for CO, CO₂, NO_x, SO₂, TOC, CH₄, VOC, and hydrochloric acid (HCl) from drum mix plants. The emission factors for CO, NO_x, and organic compounds represent normal plant operations without scrutiny of the burner design, operation, and maintenance. Information provided in Reference 390 indicates that attention to burner design, periodic evaluation of burner operation, and appropriate maintenance can reduce these emissions. Table 11.1-9 presents organic pollutant emission factors for batch mix plants. Table 11.1-10 presents organic pollutant emission factors for drum mix plants. Tables 11.1-11 and -12 present metals emission factors for batch and drum mix plants, respectively. Table 11.1-13 presents organic pollutant emission factors for hot (asphalt) oil heaters.

11.1.2.5 Fugitive Emissions from Production Operations –

Emission factors for HMA load-out and silo filling operations can be estimated using the data in Tables 11.1-14, -15, and -16. Table 11.1-14 presents predictive emission factor equations for HMA load-out and silo filling operations. Separate equations are presented for total PM, extractable organic PM (as measured by EPA Method 315), TOC, and CO. For example, to estimate total PM emissions from drum mix or batch mix plant load-out operations using an asphalt loss-on-heating of 0.41 percent and temperature of 290°F, the following calculation is made:

$$\begin{aligned} \text{EF} &= 0.000181 + 0.00141(-V)e^{((0.0251)(290 + 460) - 20.43)} \\ &= 0.000181 + 0.00141(-(-0.41))e^{((0.0251)(290 + 460) - 20.43)} \\ &= 0.000181 + 0.00141(0.41)e^{-1.605} \\ &= 0.000181 + 0.00141(0.41)(0.2009) \\ &= 0.000181 + 0.000116 \\ &= 0.00030 \text{ lb total PM/ton of asphalt loaded} \end{aligned}$$

Tables 11.1-15 and -16 present speciation profiles for organic particulate-based and volatile particulate-based compounds, respectively. The speciation profile shown in Table 11.1-15 can be applied to the extractable organic PM emission factors estimated by the equations in Table 11.1-14 to estimate emission factors for specific organic PM compounds. The speciation profile presented in Table 11.1-16 can be applied to the TOC emission factors estimated by the equations in Table 11.1-14 to estimate emission factors for specific volatile organic compounds. The derivations of the predictive emission factor equations and the speciation profiles can be found in Reference 1.

For example, to estimate TOC emissions from drum mix plant load-out operations using an asphalt loss-on-heating of 0.41 percent and temperature of 290°F, the following calculation is made:

$$\begin{aligned}
 EF &= 0.0172(-V)e^{((0.0251)(290 + 460) - 20.43)} \\
 &= 0.0172(-(-0.41))e^{((0.0251)(290 + 460) - 20.43)} \\
 &= 0.0172(0.41)e^{-1.605} \\
 &= 0.0172(0.41)(0.2009) \\
 &= 0.0014 \text{ lb TOC/ton of asphalt loaded}
 \end{aligned}$$

To estimate the benzene emissions from the same operation, use the TOC emission factor calculated above and apply the benzene fraction for load-out emissions from Table 11.1-16:

$$\begin{aligned}
 EF &= 0.0014 (0.00052) \\
 &= 7.3 \times 10^{-7} \text{ lb benzene/ton of asphalt loaded}
 \end{aligned}$$

Emissions from asphalt storage tanks can be estimated using the procedures described in AP-42 Section 7.1, Organic Liquid Storage Tanks, and the TANKS software. Site-specific data should be used for storage tank specifications and operating parameters, such as temperature. If site-specific data for Antoine's constants for an average asphalt binder used by the facility are unavailable, the following values for an average liquid asphalt binder can be used:

$$\begin{aligned}
 A &= 75,350.06 \\
 B &= 9.00346
 \end{aligned}$$

These values should be inserted into the Antoine's equation in the following form:

$$\log_{10} P = \frac{-0.05223A}{T} + B$$

where:

$$\begin{aligned}
 P &= \text{vapor pressure, mm Hg} \\
 T &= \text{absolute temperature, Kelvin}
 \end{aligned}$$

The assumed average liquid molecular weight associated with these Antoine's constants is 1,000 atomic mass units and the average vapor molecular weight is 105. Emission factors estimated using these default values should be assigned a rating of E. Carbon monoxide emissions can be estimated by multiplying the THC emissions calculated by the TANKS program by 0.097 (the ratio of silo filling CO emissions to silo filling TOC emissions).

Vapors from the HMA loaded into transport trucks continue following load-out operations. The TOC emissions for the 8-minute period immediately following load-out (yard emissions) can be estimated using an emission factor of 0.00055 kg/Mg (0.0011 lb/ton) of asphalt loaded. This factor is assigned a rating of E. The derivation of this emission factor is described in Reference 1. Carbon monoxide emissions can be estimated by multiplying the TOC emissions by 0.32 (the ratio of truck load-out CO emissions to truck load-out THC emissions).

Table 11.1-1. PARTICULATE MATTER EMISSION FACTORS FOR BATCH MIX HOT MIX ASPHALT PLANTS^a

Process	Filterable PM				Condensable PM ^b				Total PM			
	PM ^c	EMISSION FACTOR RATING	PM-10 ^d	EMISSION FACTOR RATING	Inorganic	EMISSION FACTOR RATING	Organic	EMISSION FACTOR RATING	PM ^e	EMISSION FACTOR RATING	PM-10 ^f	EMISSION FACTOR RATING
Dryer, hot screens, mixer ^g (SCC 3-05-002-45, -46, -47)												
Uncontrolled	32 ^h	E	4.5	E	0.013 ^j	E	0.0041 ^j	E	32	E	4.5	E
Venturi or wet scrubber	0.12 ^k	C	ND	NA	0.013 ^m	B	0.0041 ⁿ	B	0.14	C	ND	NA
Fabric filter	0.025 ^p	A	0.0098	C	0.013 ^m	A	0.0041 ⁿ	A	0.042	B	0.027	C

^a Factors are lb/ton of product. SCC = Source Classification Code. ND = no data. NA = not applicable. To convert from lb/ton to kg/Mg, multiply by 0.5.

^b Condensable PM is that PM collected using an EPA Method 202, Method 5 (analysis of "back-half" or impingers), or equivalent sampling train.

^c Filterable PM is that PM collected on or before the filter of an EPA Method 5 (or equivalent) sampling train.

^d Particle size data from Reference 23 were used in conjunction with the filterable PM emission factors shown.

^e Total PM is the sum of filterable PM, condensable inorganic PM, and condensable organic PM.

^f Total PM-10 is the sum of filterable PM-10, condensable inorganic PM, and condensable organic PM.

^g Batch mix dryer fired with natural gas, propane, fuel oil, waste oil, and coal. The data indicate that fuel type does not significantly effect PM emissions.

^h Reference 5.

^j Although no data are available for uncontrolled condensable PM, values are assumed to be equal to the controlled value measured.

^k Reference 1, Table 4-19. Average of data from 16 facilities. Range: 0.047 to 0.40 lb/ton. Median: 0.049 lb/ton. Standard deviation: 0.11 lb/ton.

^m Reference 1, Table 4-19. Average of data from 35 facilities. Range: 0.00073 to 0.12 lb/ton. Median: 0.0042 lb/ton. Standard deviation: 0.024 lb/ton.

ⁿ Reference 1, Table 4-19. Average of data from 24 facilities. Range: 0.000012 to 0.018 lb/ton. Median: 0.0026 lb/ton. Standard deviation: 0.0042 lb/ton.

^p Reference 1, Table 4-19. Average of data from 89 facilities. Range: 0.0023 to 0.18 lb/ton. Median: 0.012 lb/ton. Standard deviation: 0.033 lb/ton.

Table 11.1-2. SUMMARY OF PARTICLE SIZE DISTRIBUTION FOR BATCH MIX DRYERS, HOT SCREENS, AND MIXERS^a

EMISSION FACTOR RATING: E

Particle Size, μm ^b	Cumulative Mass Less Than or Equal to Stated Size (%) ^c		Emission Factors, lb/ton	
	Uncontrolled ^d	Fabric Filter	Uncontrolled ^d	Fabric Filter
1.0	ND	30 ^e	ND	0.0075 ^e
2.5	0.83	33 ^e	0.27	0.0083 ^e
5.0	3.5	36 ^e	1.1	0.0090 ^e
10.0	14	39 ^f	4.5	0.0098 ^f
15.0	23	47 ^e	7.4	0.012 ^e

- ^a Emission factor units are lb/ton of HMA provided. Rounded to two significant figures. SCC 3-05-002-45, -46, -47. ND = no data available. To convert from lb/ton to kg/Mg, multiply by 0.5.
- ^b Aerodynamic diameter.
- ^c Applies only to the mass of filterable PM.
- ^d References 23, Table 3-36. The emission factors are calculated using the particle size data from this reference in conjunction with the filterable PM emission factor shown in Table 11.1-1.
- ^e References 23, Page J-61. The emission factors are calculated using the particle size data from this reference in conjunction with the filterable PM emission factor shown in Table 11.1-1.
- ^f References 23-24. The emission factors are calculated using the particle size data from these references in conjunction with the filterable PM emission factor shown in Table 11.1-1.

Table 11.1-3. PARTICULATE MATTER EMISSION FACTORS FOR DRUM MIX HOT MIX ASPHALT PLANTS^a

Process	Filterable PM				Condensable PM ^b				Total PM			
	PM ^c	EMISSION FACTOR RATING	PM-10 ^d	EMISSION FACTOR RATING	Inorganic	EMISSION FACTOR RATING	Organic	EMISSION FACTOR RATING	PM ^e	EMISSION FACTOR RATING	PM-10 ^f	EMISSION FACTOR RATING
Dryer ^g (SCC 3-05-002-05,-55 to -63)												
Uncontrolled	28 ^h	D	6.4	D	0.0074 ^j	E	0.058 ^k	E	28	D	6.5	D
Venturi or wet scrubber	0.026 ^m	A	ND	NA	0.0074 ⁿ	A	0.012 ^p	A	0.045	A	ND	NA
Fabric filter	0.014 ^q	A	0.0039	C	0.0074 ⁿ	A	0.012 ^p	A	0.033	A	0.023	C

^a Factors are lb/ton of product. SCC = Source Classification Code. ND = no data. NA = not applicable. To convert from lb/ton to kg/Mg, multiply by 0.5.

^b Condensable PM is that PM collected using an EPA Method 202, Method 5 (analysis of “back-half” or impingers), or equivalent sampling train.

^c Filterable PM is that PM collected on or before the filter of an EPA Method 5 (or equivalent) sampling train.

^d Particle size data from Reference 23 were used in conjunction with the filterable PM emission factors shown.

^e Total PM is the sum of filterable PM, condensable inorganic PM, and condensable organic PM.

^f Total PM-10 is the sum of filterable PM-10, condensable inorganic PM, and condensable organic PM.

^g Drum mix dryer fired with natural gas, propane, fuel oil, and waste oil. The data indicate that fuel type does not significantly effect PM emissions.

^h References 31, 36-38, 340.

^j Because no data are available for uncontrolled condensable inorganic PM, the emission factor is assumed to be equal to the maximum controlled condensable inorganic PM emission factor.

^k References 36-37.

^m Reference 1, Table 4-14. Average of data from 36 facilities. Range: 0.0036 to 0.097 lb/ton. Median: 0.020 lb/ton. Standard deviation: 0.022 lb/ton.

ⁿ Reference 1, Table 4-14. Average of data from 30 facilities. Range: 0.0012 to 0.027 lb/ton. Median: 0.0051 lb/ton. Standard deviation: 0.0063 lb/ton.

^p Reference 1, Table 4-14. Average of data from 41 facilities. Range: 0.00035 to 0.074 lb/ton. Median: 0.0046 lb/ton. Standard deviation: 0.016 lb/ton.

^q Reference 1, Table 4-14. Average of data from 155 facilities. Range: 0.00089 to 0.14 lb/ton. Median: 0.010 lb/ton. Standard deviation: 0.017 lb/ton.

Table 11.1-4. SUMMARY OF PARTICLE SIZE DISTRIBUTION FOR DRUM MIX DRYERS^a

EMISSION FACTOR RATING: E

Particle Size, μm ^b	Cumulative Mass Less Than or Equal to Stated Size (%) ^c		Emission Factors, lb/ton	
	Uncontrolled ^d	Fabric Filter	Uncontrolled ^d	Fabric Filter
1.0	ND	15 ^e	ND	0.0021 ^e
2.5	5.5	21 ^f	1.5	0.0029 ^f
10.0	23	30 ^g	6.4	0.0042 ^g
15.0	27	35 ^d	7.6	0.0049 ^d

^a Emission factor units are lb/ton of HMA produced. Rounded to two significant figures. SCC 3-05-002-05, and 3-05-002-55 to -63. ND = no data available. To convert from lb/ton to kg/Mg, multiply by 0.5.

^b Aerodynamic diameter.

^c Applies only to the mass of filterable PM.

^d Reference 23, Table 3-35. The emission factors are calculated using the particle size data from this reference in conjunction with the filterable PM emission factor shown in Table 11.1-3.

^e References 214, 229. The emission factors are calculated using the particle size data from these references in conjunction with the filterable PM emission factor shown in Table 11.1-3.

^f References 23, 214, 229. The emission factors are calculated using the particle size data from these references in conjunction with the filterable PM emission factor shown in Table 11.1-3.

^g Reference 23, 25, 229. The emission factors are calculated using the particle size data from these references in conjunction with the filterable PM emission factor shown in Table 11.1-3. EMISSION FACTOR RATING: D.

Table 11.1-5. EMISSION FACTORS FOR CO, CO₂, NO_x, AND SO₂ FROM BATCH MIX HOT MIX ASPHALT PLANTS^a

Process	CO ^b	EMISSION FACTOR RATING	CO ₂ ^c	EMISSION FACTOR RATING	NO _x	EMISSION FACTOR RATING	SO ₂ ^c	EMISSION FACTOR RATING
Natural gas-fired dryer, hot screens, and mixer (SCC 3-05-002-45)	0.40	C	37 ^d	A	0.025 ^e	D	0.0046 ^f	E
No. 2 fuel oil-fired dryer, hot screens, and mixer (SCC 3-05-002-46)	0.40	C	37 ^d	A	0.12 ^g	E	0.088 ^h	E
Waste oil-fired dryer, hot screens, and mixer (SCC 3-05-002-47)	0.40	C	37 ^d	A	0.12 ^g	E	0.088 ^h	E
Coal-fired dryer, hot screens, and mixer ^j (SCC 3-05-002-98)	ND	NA	37 ^d	A	ND	NA	0.043 ^k	E

- ^a Emission factor units are lb per ton of HMA produced. SCC = Source Classification Code. ND = no data available. NA = not applicable. To convert from lb/ton to kg/Mg, multiply by 0.5.
- ^b References 24, 34, 46-47, 49, 161, 204, 215-217, 282, 370, 378, 381. The CO emission factors represent normal plant operations without scrutiny of the burner design, operation, and maintenance. Information is available that indicates that attention to burner design, periodic evaluation of burner operation, and appropriate maintenance can reduce CO emissions. Data for dryers firing natural gas, No. 2 fuel oil, and No. 6 fuel oil were combined to develop a single emission factor because the magnitude of emissions was similar for dryers fired with these fuels.
- ^c Emissions of CO₂ and SO₂ can also be estimated based on fuel usage and the fuel combustion emission factors (for the appropriate fuel) presented in AP-42 Chapter 1. The CO₂ emission factors are an average of all available data, regardless of the dryer fuel (emissions were similar from dryers firing any of the various fuels). Based on data for drum mix facilities, 50 percent of the fuel-bound sulfur, up to a maximum (as SO₂) of 0.1 lb/ton of product, is expected to be retained in the product, with the remainder emitted as SO₂.
- ^d Reference 1, Table 4-20. Average of data from 115 facilities. Range: 6.9 to 160 lb/ton. Median: 32 lb/ton. Standard deviation: 22 lb/ton.
- ^e References 24, 34, 46-47.
- ^f References 46-47.
- ^g References 49, 226.
- ^h References 49, 226, 228, 385.
- ^j Dryer fired with coal and supplemental natural gas or fuel oil.
- ^k Reference 126.

Table 11.1-6. EMISSION FACTORS FOR TOC, METHANE, AND VOC FROM BATCH MIX HOT MIX ASPHALT PLANTS^a

Process	TOC ^b	EMISSION FACTOR RATING	CH ₄ ^c	EMISSION FACTOR RATING	VOC ^d	EMISSION FACTOR RATING
Natural gas-fired dryer, hot screens, and mixer (SCC 3-05-002-45)	0.015 ^e	D	0.0074	D	0.0082	D
No. 2 fuel oil-fired dryer, hot screens, and mixer (SCC 3-05-002-46)	0.015 ^e	D	0.0074	D	0.0082	D
No. 6 fuel oil-fired dryer, hot screens, and mixer (SCC 3-05-002-47)	0.043 ^f	E	0.0074	D	0.036	E

^a Emission factor units are lb per ton of HMA produced. SCC = Source Classification Code. ND = no data available. NA = not applicable. To convert from lb/ton to kg/Mg, multiply by 0.5.

^b TOC equals total hydrocarbons as propane, as measured with an EPA Method 25A or equivalent sampling train plus formaldehyde.

^c References 24, 46-47, 49. Factor includes data from natural gas- and No. 6 fuel oil-fired dryers. Methane measured with an EPA Method 18 or equivalent sampling train.

^d The VOC emission factors are equal to the TOC factors minus the methane emission factors; differences in values reported are due to rounding.

^e References 24, 46-47, 155.

^f Reference 49.

Table 11.1-7. EMISSION FACTORS FOR CO, CO₂, NO_x, AND SO₂ FROM DRUM MIX HOT MIX ASPHALT PLANTS^a

Process	CO ^b	EMISSION FACTOR RATING	CO ₂ ^c	EMISSION FACTOR RATING	NO _x	EMISSION FACTOR RATING	SO ₂ ^c	EMISSION FACTOR RATING
Natural gas-fired dryer (SCC 3-05-002-55,-56,-57)	0.13	B	33 ^d	A	0.026 ^e	D	0.0034 ^f	D
No. 2 fuel oil-fired dryer (SCC 3-05-002-58,-59,-60)	0.13	B	33 ^d	A	0.055 ^g	C	0.011 ^h	E
Waste oil-fired dryer (SCC 3-05-002-61,-62,-63)	0.13	B	33 ^d	A	0.055 ^g	C	0.058 ^j	B
Coal-fired dryer ^k (SCC 3-05-002-98)	ND	NA	33 ^d	A	ND	NA	0.19 ^m	E

^a Emission factor units are lb per ton of HMA produced. SCC = Source Classification Code. ND = no data available. NA = not applicable. To convert from lb/ton to kg/Mg, multiply by 0.5.

^b References 25, 44, 48, 50, 149, 154, 197, 214, 229, 254, 339-342, 344, 346, 347, 390. The CO emission factors represent normal plant operations without scrutiny of the burner design, operation, and maintenance. Information is available that indicates that attention to burner design, periodic evaluation of burner operation, and appropriate maintenance can reduce CO emissions. Data for dryers firing natural gas, No. 2 fuel oil, and No. 6 fuel oil were combined to develop a single emission factor because the magnitude of emissions was similar for dryers fired with these fuels.

^c Emissions of CO₂ and SO₂ can also be estimated based on fuel usage and the fuel combustion emission factors (for the appropriate fuel) presented in AP-42 Chapter 1. The CO₂ emission factors are an average of all available data, regardless of the dryer fuel (emissions were similar from dryers firing any of the various fuels). Fifty percent of the fuel-bound sulfur, up to a maximum (as SO₂) of 0.1 lb/ton of product, is expected to be retained in the product, with the remainder emitted as SO₂.

^d Reference 1, Table 4-15. Average of data from 180 facilities. Range: 2.6 to 96 lb/ton. Median: 31 lb/ton. Standard deviation: 13 lb/ton.

^e References 44-45, 48, 209, 341, 342.

^f References 44-45, 48.

^g References 25, 50, 153, 214, 229, 344, 346, 347, 352-354.

^h References 50, 119, 255, 340

^j References 25, 299, 300, 339, 345, 351, 371-377, 379, 380, 386-388.

^k Dryer fired with coal and supplemental natural gas or fuel oil.

^m References 88, 108, 189-190.

Table 11.1-8. EMISSION FACTORS FOR TOC, METHANE, VOC, AND HCl FROM DRUM MIX HOT MIX ASPHALT PLANTS^a

Process	TOC ^b	EMISSION FACTOR RATING	CH ₄ ^c	EMISSION FACTOR RATING	VOC ^d	EMISSION FACTOR RATING	HCl ^e	EMISSION FACTOR RATING
Natural gas-fired dryer (SCC 3-05-002-55, -56,-57)	0.044 ^f	B	0.012	C	0.032	C	ND	NA
No. 2 fuel oil-fired dryer (SCC 3-05-002-58, -59,-60)	0.044 ^f	B	0.012	C	0.032	C	ND	NA
Waste oil-fired dryer (SCC 3-05-002-61, -62,-63)	0.044 ^f	E	0.012	C	0.032	E	0.00021	D

- ^a Emission factor units are lb per ton of HMA produced. SCC = Source Classification Code. ND = no data available. NA = not applicable. To convert from lb/ton to kg/Mg, multiply by 0.5.
- ^b TOC equals total hydrocarbons as propane as measured with an EPA Method 25A or equivalent sampling train plus formaldehyde.
- ^c References 25, 44-45, 48, 50, 339-340, 355. Factor includes data from natural gas-, No. 2 fuel oil, and waste oil-fired dryers. Methane measured with an EPA Method 18 or equivalent sampling train.
- ^d The VOC emission factors are equal to the TOC factors minus the sum of the methane emission factors and the emission factors for compounds with negligible photochemical reactivity shown in Table 11.1-10; differences in values reported are due to rounding.
- ^e References 348, 374, 376, 379, 380.
- ^f References 25, 44-45, 48, 50, 149, 153-154, 209-212, 214, 241, 242, 339-340, 355.

Table 11.1-9. EMISSION FACTORS FOR ORGANIC POLLUTANT EMISSIONS FROM BATCH MIX HOT MIX ASPHALT PLANTS^a

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. Nos.	
	CASRN	Name				
Natural gas- or No. 2 fuel oil-fired dryer, hot screens, and mixer with fabric filter (SCC 3-05-002-45,-46)	Non-PAH Hazardous Air Pollutants ^b					
	75-07-0	Acetaldehyde	0.00032	E	24,34	
	71-43-2	Benzene	0.00028	D	24,34,46, 382	
	100-41-4	Ethylbenzene	0.0022	D	24,46,47,49	
	50-00-0	Formaldehyde	0.00074	D	24,34,46,47,49,226,382	
	106-51-4	Quinone	0.00027	E	24	
	108-88-3	Toluene	0.0010	D	24,34,46,47	
	1330-20-7	Xylene	0.0027	D	24,46,47,49	
		Total non-PAH HAPs	0.0075			
		PAH HAPs				
	91-57-6	2-Methylnaphthalene ^c	7.1x10 ⁻⁵	D	24,47,49	
	83-32-9	Acenaphthene ^c	9.0x10 ⁻⁷	D	34,46,226	
	208-96-8	Acenaphthylene ^c	5.8x10 ⁻⁷	D	34,46,226	
	120-12-7	Anthracene ^c	2.1x10 ⁻⁷	D	34,46,226	
	56-55-3	Benzo(a)anthracene ^c	4.6x10 ⁻⁹	E	46,226	
	50-32-8	Benzo(a)pyrene ^c	3.1x10 ⁻¹⁰	E	226	
	205-99-2	Benzo(b)fluoranthene ^c	9.4x10 ⁻⁹	D	34,46,226	
	191-24-2	Benzo(g,h,i)perylene ^c	5.0x10 ⁻¹⁰	E	226	
	207-08-9	Benzo(k)fluoranthene ^c	1.3x10 ⁻⁸	E	34,226	
	218-01-9	Chrysene ^c	3.8x10 ⁻⁹	E	46,226	
	53-70-3	Dibenz(a,h)anthracene ^c	9.5x10 ⁻¹¹	E	226	
	206-44-0	Fluoranthene ^c	1.6x10 ⁻⁷	D	34,46,47,226	
	86-73-7	Fluorene ^c	1.6x10 ⁻⁶	D	34,46,47,226	
	193-39-5	Indeno(1,2,3-cd)pyrene ^c	3.0x10 ⁻¹⁰	E	226	
	91-20-3	Naphthalene	3.6x10 ⁻⁵	D	34,46,47,49,226	
	85-01-8	Phenanthrene ^c	2.6x10 ⁻⁶	D	34,46,47,226	
	129-00-0	Pyrene ^c	6.2x10 ⁻⁸	D	34,46,226	
		Total PAH HAPs	0.00011			
		Total HAPs		0.0076		
		Non-HAP organic compounds				
	100-52-7	Benzaldehyde	0.00013	E	24	
	78-84-2	Butyraldehyde/ isobutyraldehyde	3.0x10 ⁻⁵	E	24	
4170-30-3	Crotonaldehyde	2.9x10 ⁻⁵	E	24		
66-25-1	Hexanal	2.4x10 ⁻⁵	E	24		
	Total non-HAPs	0.00019				

Table 11.1-9 (cont.)

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. Nos.
	CASRN	Name			
Waste oil-, drain oil-, or No. 6 fuel oil-fired dryer, hot screens, and mixer with fabric filter (SCC 3-05-002-47)	Non-PAH Hazardous Air Pollutants ^b				
	75-07-0	Acetaldehyde	0.00032	E	24,34
	71-43-2	Benzene	0.00028	D	24,34,46, 382
	100-41-4	Ethylbenzene	0.0022	D	24,46,47,49
	50-00-0	Formaldehyde	0.00074	D	24,34,46,47,49,226, 382
	106-51-4	Quinone	0.00027	E	24
	108-88-3	Toluene	0.0010	D	24,34,46,47
	1330-20-7	Xylene	0.0027	D	24,46,47,49
		Total non-PAH HAPs	0.0075		
	PAH HAPs ^b				
	91-57-6	2-Methylnaphthalene ^c	7.1×10^{-5}	D	24,47,49
	83-32-9	Acenaphthene ^c	9.0×10^{-7}	D	34,46,226
	208-96-8	Acenaphthylene ^c	5.8×10^{-7}	D	34,46,226
	120-12-7	Anthracene ^c	2.1×10^{-7}	D	34,46,226
	56-55-3	Benzo(a)anthracene ^c	4.6×10^{-9}	E	46,226
	50-32-8	Benzo(a)pyrene ^c	3.1×10^{-10}	E	226
	205-99-2	Benzo(b)fluoranthene ^c	9.4×10^{-9}	D	34,46,226
	191-24-2	Benzo(g,h,i)perylene ^c	5.0×10^{-10}	E	226
	207-08-9	Benzo(k)fluoranthene ^c	1.3×10^{-8}	E	34,226
	218-01-9	Chrysene ^c	3.8×10^{-9}	E	46,226
	53-70-3	Dibenz(a,h)anthracene ^c	9.5×10^{-11}	E	226
	206-44-0	Fluoranthene ^c	2.4×10^{-5}	E	49
	86-73-7	Fluorene ^c	1.6×10^{-6}	D	34,46,47,226
	193-39-5	Indeno(1,2,3-cd)pyrene ^c	3.0×10^{-10}	E	226
	91-20-3	Naphthalene	3.6×10^{-5}	D	34,46,47,49, 226
	85-01-8	Phenanthrene ^c	3.7×10^{-5}	E	49
	129-00-0	Pyrene ^c	5.5×10^{-5}	E	49
		Total PAH HAPs	0.00023		
	Total HAPs		0.0077		
	Non-HAP organic compounds				
	100-52-7	Benzaldehyde	0.00013	E	24
	78-84-2	Butyraldehyde/ isobutyraldehyde	3.0×10^{-5}	E	24
	4170-30-3	Crotonaldehyde	2.9×10^{-5}	E	24
66-25-1	Hexanal	2.4×10^{-5}	E	24	
	Total non-HAPs	0.00019			

^a Emission factor units are lb/ton of hot mix asphalt produced. Factors represent uncontrolled emissions, unless noted. CASRN = Chemical Abstracts Service Registry Number. SCC = Source Classification Code. To convert from lb/ton to kg/Mg, multiply by 0.5.

^b Hazardous air pollutants (HAP) as defined in the 1990 Clean Air Act Amendments (CAAA).

^c Compound is classified as polycyclic organic matter, as defined in the 1990 CAAA.

Table 11.1-10. EMISSION FACTORS FOR ORGANIC POLLUTANT EMISSIONS FROM DRUM MIX HOT MIX ASPHALT PLANTS^a

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. No.	
	CASRN	Name				
Natural gas-fired dryer with fabric filter ^b (SCC 3-05-002-55, -56,-57)	Non-PAH hazardous air pollutants ^c					
	71-43-2	Benzene ^d	0.00039	A	25,44,45,50, 341, 342, 344-351, 373, 376, 377, 383, 384	
	100-41-4	Ethylbenzene	0.00024	D	25,44,45	
	50-00-0	Formaldehyde ^e	0.0031	A	25,35,44,45,50, 339-344, 347-349, 371-373, 384, 388	
	110-54-3	Hexane	0.00092	E	339-340	
	540-84-1	Isooctane (2,2,4-trimethylpentane)	4.0x10 ⁻⁵	E	339-340	
	71-55-6	Methyl chloroform ^f	4.8x10 ⁻⁵	E	35	
	108-88-3	Toluene	0.00015	D	35,44,45	
	1330-20-7	Xylene	0.00020	D	25,44,45	
		Total non-PAH HAPs	0.0051			
		PAH HAPs				
		91-57-6	2-Methylnaphthalene ^g	7.4x10 ⁻⁵	D	44,45,48
		83-32-9	Acenaphthene ^g	1.4x10 ⁻⁶	E	48
		208-96-8	Acenaphthylene ^g	8.6x10 ⁻⁶	D	35,45,48
		120-12-7	Anthracene ^g	2.2x10 ⁻⁷	E	35,48
		56-55-3	Benzo(a)anthracene ^g	2.1x10 ⁻⁷	E	48
		50-32-8	Benzo(a)pyrene ^g	9.8x10 ⁻⁹	E	48
		205-99-2	Benzo(b)fluoranthene ^g	1.0x10 ⁻⁷	E	35,48
		192-97-2	Benzo(e)pyrene ^g	1.1x10 ⁻⁷	E	48
		191-24-2	Benzo(g,h,i)perylene ^g	4.0x10 ⁻⁸	E	48
		207-08-9	Benzo(k)fluoranthene ^g	4.1x10 ⁻⁸	E	35,48
		218-01-9	Chrysene ^g	1.8x10 ⁻⁷	E	35,48
		206-44-0	Fluoranthene ^g	6.1x10 ⁻⁷	D	35,45,48
		86-73-7	Fluorene ^g	3.8x10 ⁻⁶	D	35,45,48,163
		193-39-5	Indeno(1,2,3-cd)pyrene ^g	7.0x10 ⁻⁹	E	48
		91-20-3	Naphthalene ^g	9.0x10 ⁻⁵	D	35,44,45,48,163
		198-55-0	Perylene ^g	8.8x10 ⁻⁹	E	48
		85-01-8	Phenanthrene ^g	7.6x10 ⁻⁶	D	35,44,45,48,163
		129-00-0	Pyrene ^g	5.4x10 ⁻⁷	D	45,48
			Total PAH HAPs	0.00019		

Table 11.1-10 (cont.)

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. No.
	CASRN	Name			
Natural gas-fired dryer with fabric filter ^b (SCC 3-05-002-55, -56,-57) (cont.)	Total HAPs		0.0053		
	Non-HAP organic compounds				
	106-97-8	Butane	0.00067	E	339
	74-85-1	Ethylene	0.0070	E	339-340
	142-82-5	Heptane	0.0094	E	339-340
	763-29-1	2-Methyl-1-pentene	0.0040	E	339,340
	513-35-9	2-Methyl-2-butene	0.00058	E	339,340
	96-14-0	3-Methylpentane	0.00019	D	339,340
	109-67-1	1-Pentene	0.0022	E	339-340
	109-66-0	n-Pentane	0.00021	E	339-340
	Total non-HAP organics	0.024			
No. 2 fuel oil-fired dryer with fabric filter (SCC 3-05-002-58, -59,-60)	Non-PAH HAPs ^c				
	71-43-2	Benzene ^d	0.00039	A	25,44,45,50, 341, 342, 344-351, 373, 376, 377, 383, 384
	100-41-4	Ethylbenzene	0.00024	D	25,44,45
	50-00-0	Formaldehyde ^e	0.0031	A	25,35,44,45,50, 339-344, 347-349, 371-373, 384, 388
	110-54-3	Hexane	0.00092	E	339-340
	540-84-1	Isooctane (2,2,4-trimethylpentane)	4.0x10 ⁻⁵	E	339-340
	71-55-6	Methyl chloroform ^f	4.8x10 ⁻⁵	E	35
	108-88-3	Toluene	0.0029	E	25, 50, 339-340
	1330-20-7	Xylene	0.00020	D	25,44,45
		Total non-PAH HAPs	0.0078		
	PAH HAPs				
	91-57-6	2-Methylnaphthalene ^g	0.00017	E	50
	83-32-9	Acenaphthene ^g	1.4x10 ⁻⁶	E	48
	208-96-8	Acenaphthylene ^g	2.2x10 ⁻⁵	E	50
	120-12-7	Anthracene ^g	3.1x10 ⁻⁶	E	50,162
56-55-3	Benzo(a)anthracene ^g	2.1x10 ⁻⁷	E	48	
50-32-8	Benzo(a)pyrene ^g	9.8x10 ⁻⁹	E	48	
205-99-2	Benzo(b)fluoranthene ^g	1.0x10 ⁻⁷	E	35,48	
192-97-2	Benzo(e)pyrene ^g	1.1x10 ⁻⁷	E	48	

Table 11.1-10 (cont.)

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. No.	
	CASRN	Name				
No. 2 fuel oil-fired dryer with fabric filter (SCC 3-05-002-58, -59,-60) (cont.)	191-24-2	Benzo(g,h,i)perylene ^g	4.0x10 ⁻⁸	E	48	
	207-08-9	Benzo(k)fluoranthene ^g	4.1x10 ⁻⁸	E	35,48	
	218-01-9	Chrysene ^g	1.8x10 ⁻⁷	E	35,48	
	206-44-0	Fluoranthene ^g	6.1x10 ⁻⁷	D	35,45,48	
	86-73-7	Fluorene ^g	1.1x10 ⁻⁵	E	50,164	
	193-39-5	Indeno(1,2,3-cd)pyrene ^g	7.0x10 ⁻⁹	E	48	
	91-20-3	Naphthalene ^g	0.00065	D	25,50,162,164	
	198-55-0	Perylene ^g	8.8x10 ⁻⁹	E	48	
	85-01-8	Phenanthrene ^g	2.3x10 ⁻⁵	D	50,162,164	
	129-00-0	Pyrene ^g	3.0x10 ⁻⁶	E	50	
		Total PAH HAPs	0.00088			
		Total HAPs	0.0087			
		Non-HAP organic compounds				
		106-97-8	Butane	0.00067	E	339
		74-85-1	Ethylene	0.0070	E	339-340
		142-82-5	Heptane	0.0094	E	339-340
		763-29-1	2-Methyl-1-pentene	0.0040	E	339,340
		513-35-9	2-Methyl-2-butene	0.00058	E	339,340
		96-14-0	3-Methylpentane	0.00019	D	339,340
		109-67-1	1-Pentene	0.0022	E	339-340
	109-66-0	n-Pentane	0.00021	E	339-340	
		Total non-HAP organics	0.024			
Fuel oil- or waste oil-fired dryer with fabric filter (SCC 3-05-002-58, -59,-60,-61,-62,-63)	Dioxins					
	1746-01-6	2,3,7,8-TCDD ^g	2.1x10 ⁻¹³	E	339	
		Total TCDD ^g	9.3x10 ⁻¹³	E	339	
	40321-76-4	1,2,3,7,8-PeCDD ^g	3.1x10 ⁻¹³	E	339	
		Total PeCDD ^g	2.2x10 ⁻¹¹	E	339-340	
	39227-28-6	1,2,3,4,7,8-HxCDD ^g	4.2x10 ⁻¹³	E	339	
	57653-85-7	1,2,3,6,7,8-HxCDD ^g	1.3x10 ⁻¹²	E	339	
	19408-24-3	1,2,3,7,8,9-HxCDD ^g	9.8x10 ⁻¹³	E	339	
		Total HxCDD ^g	1.2x10 ⁻¹¹	E	339-340	
	35822-46-9	1,2,3,4,6,7,8-HpCDD ^g	4.8x10 ⁻¹²	E	339	
	Total HpCDD ^g	1.9x10 ⁻¹¹	E	339-340		

Table 11.1-10 (cont.)

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. No.	
	CASRN	Name				
Fuel oil- or waste oil-fired dryer with fabric filter (SCC 3-05-002-58, -59,-60,-61,-62, -63) (cont.)	3268-87-9	Octa CDD ^g	2.5x10 ⁻¹¹	E	339	
		Total PCDD ^g	7.9x10 ⁻¹¹	E	339-340	
	Furans					
	51207-31-9	2,3,7,8-TCDF ^g	9.7x10 ⁻¹³	E	339	
		Total TCDF ^g	3.7x10 ⁻¹²	E	339-340	
		1,2,3,7,8-PeCDF ^g	4.3x10 ⁻¹²	E	339-340	
		2,3,4,7,8-PeCDF ^g	8.4x10 ⁻¹³	E	339	
		Total PeCDF ^g	8.4x10 ⁻¹¹	E	339-340	
		1,2,3,4,7,8-HxCDF ^g	4.0x10 ⁻¹²	E	339	
		1,2,3,6,7,8-HxCDF ^g	1.2x10 ⁻¹²	E	339	
		2,3,4,6,7,8-HxCDF ^g	1.9x10 ⁻¹²	E	339	
		1,2,3,7,8,9-HxCDF ^g	8.4x10 ⁻¹²	E	340	
		Total HxCDF ^g	1.3x10 ⁻¹¹	E	339-340	
		1,2,3,4,6,7,8-HpCDF ^g	6.5x10 ⁻¹²	E	339	
	1,2,3,4,7,8,9-HpCDF ^g	2.7x10 ⁻¹²	E	339		
	Total HpCDF ^g	1.0x10 ⁻¹¹	E	339-340		
	39001-02-0	Octa CDF ^g	4.8x10 ⁻¹²	E	339	
Total PCDF ^g		4.0x10 ⁻¹¹	E	339-340		
Total PCDD/PCDF ^g		1.2x10 ⁻¹⁰	E	339-340		
Fuel oil- or waste oil-fired dryer (uncontrolled) (SCC 3-05-002-58, -59,-60,-61,-62, -63)	Hazardous air pollutants ^c					
	Dioxins					
	35822-46-9	Total HxCDD ^g	5.4x10 ⁻¹²	E	340	
		1,2,3,4,6,7,8-HpCDD ^g	3.4x10 ⁻¹¹	E	340	
		Total HpCDD ^g	7.1x10 ⁻¹¹	E	340	
	3268-87-9	Octa CDD ^g	2.7x10 ⁻⁹	E	340	
		Total PCDD ^g	2.8x10 ⁻⁹	E	340	
	Furans					
		Total TCDF ^g	3.3x10 ⁻¹¹	E	340	
		Total PeCDF ^g	7.4x10 ⁻¹¹	E	340	
		1,2,3,4,7,8-HxCDF ^g	5.4x10 ⁻¹²	E	340	
2,3,4,6,7,8-HxCDF ^g		1.6x10 ⁻¹²	E	340		
Total HxCDF ^g		8.1x10 ⁻¹²	E	340		

Table 11.1-10 (cont.)

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. No.
	CASRN	Name			
Fuel oil- or waste oil-fired dryer (uncontrolled) (SCC 3-05-002-58, -59,-60,-61,-62, -63) (cont.)		1,2,3,4,6,7,8-HpCDF ^g	1.1x10 ⁻¹¹	E	340
		Total HpCDF ^g	3.8x10 ⁻¹¹	E	340
		Total PCDF ^g	1.5x10 ⁻¹⁰	E	340
		Total PCDD/PCDF ^g	3.0x10 ⁻⁹	E	340
Waste oil-fired dryer with fabric filter (SCC 3-05-002-61, -62,-63)	Non-PAH HAPs ^c				
	75-07-0	Acetaldehyde	0.0013	E	25
	107-02-8	Acrolein	2.6x10 ⁻⁵	E	25
	71-43-2	Benzene ^d	0.00039	A	25,44,45,50,341,342, 344-351, 373, 376, 377, 383, 384
	100-41-4	Ethylbenzene	0.00024	D	25,44,45
	50-00-0	Formaldehyde ^e	0.0031	A	25,35,44,45,50,339-344,347-349,371-373, 384, 388
	110-54-3	Hexane	0.00092	E	339-340
	540-84-1	Isooctane (2,2,4-trimethylpentane)	4.0x10 ⁻⁵	E	339-340
	78-93-3	Methyl Ethyl Ketone	2.0x10 ⁻⁵	E	25
	123-38-6	Propionaldehyde	0.00013	E	25
	106-51-4	Quinone	0.00016	E	25
	71-55-6	Methyl chloroform ^f	4.8x10 ⁻⁵	E	35
	108-88-3	Toluene	0.0029	E	25, 50, 339-340
	1330-20-7	Xylene	0.00020	D	25,44,45
		Total non-PAH HAPs	0.0095		
	PAH HAPs				
	91-57-6	2-Methylnaphthalene ^g	0.00017	E	50
	83-32-9	Acenaphthene ^g	1.4x10 ⁻⁶	E	48
	208-96-8	Acenaphthylene ^g	2.2x10 ⁻⁵	E	50
	120-12-7	Anthracene ^g	3.1x10 ⁻⁶	E	50,162
56-55-3	Benzo(a)anthracene ^g	2.1x10 ⁻⁷	E	48	
50-32-8	Benzo(a)pyrene ^g	9.8x10 ⁻⁹	E	48	
205-99-2	Benzo(b)fluoranthene ^g	1.0x10 ⁻⁷	E	35,48	
192-97-2	Benzo(e)pyrene ^g	1.1x10 ⁻⁷	E	48	
191-24-2	Benzo(g,h,i)perylene ^g	4.0x10 ⁻⁸	E	48	

Table 11.1-10 (cont.)

Process	Pollutant		Emission Factor, lb/ton	Emission Factor Rating	Ref. No.	
	CASRN	Name				
Waste oil-fired dryer with fabric filter (SCC 3-05-002-61, -62, -63) (cont.)	207-08-9	Benzo(k)fluoranthene ^g	4.1x10 ⁻⁸	E	35,48	
	218-01-9	Chrysene ^g	1.8x10 ⁻⁷	E	35,48	
	206-44-0	Fluoranthene ^g	6.1x10 ⁻⁷	D	35,45,48	
	86-73-7	Fluorene ^g	1.1x10 ⁻⁵	E	50,164	
	193-39-5	Indeno(1,2,3-cd)pyrene ^g	7.0x10 ⁻⁹	E	48	
	91-20-3	Naphthalene ^g	0.00065	D	25,50,162,164	
	198-55-0	Perylene ^g	8.8x10 ⁻⁹	E	48	
	85-01-8	Phenanthrene ^g	2.3x10 ⁻⁵	D	50,162,164	
	129-00-0	Pyrene ^g	3.0x10 ⁻⁶	E	50	
		Total PAH HAPs	0.00088			
		Total HAPs	0.010			
		Non-HAP organic compounds				
		67-64-1	Acetone ^f	0.00083	E	25
		100-52-7	Benzaldehyde	0.00011	E	25
		106-97-8	Butane	0.00067	E	339
		78-84-2	Butyraldehyde	0.00016	E	25
		4170-30-3	Crotonaldehyde	8.6x10 ⁻⁵	E	25
		74-85-1	Ethylene	0.0070	E	339, 340
		142-82-5	Heptane	0.0094	E	339, 340
		66-25-1	Hexanal	0.00011	E	25
	590-86-3	Isovaleraldehyde	3.2x10 ⁻⁵	E	25	
	763-29-1	2-Methyl-1-pentene	0.0040	E	339, 340	
	513-35-9	2-Methyl-2-butene	0.00058	E	339, 340	
	96-14-0	3-Methylpentane	0.00019	D	339, 340	
	109-67-1	1-Pentene	0.0022	E	339, 340	
	109-66-0	n-Pentane	0.00021	E	339, 340	
	110-62-3	Valeraldehyde	6.7x10 ⁻⁵	E	25	
		Total non-HAP organics	0.026			

^a Emission factor units are lb/ton of hot mix asphalt produced. Table includes data from both parallel flow and counterflow drum mix dryers. Organic compound emissions from counterflow systems are expected to be less than from parallel flow systems, but the available data are insufficient to quantify accurately the difference in these emissions. CASRN = Chemical Abstracts Service Registry Number. SCC = Source Classification Code. To convert from lb/ton to kg/Mg, multiply by 0.5.

Table 11.1-10 (cont.)

- b Tests included dryers that were processing reclaimed asphalt pavement. Because of limited data, the effect of RAP processing on emissions could not be determined.
- c Hazardous air pollutants (HAP) as defined in the 1990 Clean Air Act Amendments (CAAA).
- d Based on data from 19 tests. Range: 0.000063 to 0.0012 lb/ton; median: 0.00030; Standard deviation: 0.00031.
- e Based on data from 21 tests. Range: 0.0030 to 0.014 lb/ton; median: 0.0020; Standard deviation: 0.0036.
- f Compound has negligible photochemical reactivity.
- g Compound is classified as polycyclic organic matter, as defined in the 1990 CAAA. Total PCDD is the sum of the total tetra through octa dioxins; total PCDF is sum of the total tetra through octa furans; and total PCDD/PCDF is the sum of total PCDD and total PCDF.

Table 11.1-11. EMISSION FACTORS FOR METAL EMISSIONS FROM BATCH MIX HOT MIX ASPHALT PLANTS^a

Process	Pollutant	Emission Factor, lb/ton	Emission Factor Rating	Reference Numbers
Dryer, hot screens, and mixer ^b (SCC 3-05-002-45,-46,-47)	Arsenic ^c	4.6x10 ⁻⁷	D	34, 40, 226
	Barium	1.5x10 ⁻⁶	E	24
	Beryllium ^c	1.5x10 ⁻⁷	E	34, 226
	Cadmium ^c	6.1x10 ⁻⁷	D	24, 34, 226
	Chromium ^c	5.7x10 ⁻⁷	D	24, 34, 226
	Hexavalent chromium ^c	4.8x10 ⁻⁸	E	34, 226
	Copper	2.8x10 ⁻⁶	D	24, 34, 226
	Lead ^c	8.9x10 ⁻⁷	D	24, 34, 226
	Manganese ^c	6.9x10 ⁻⁶	D	24, 34, 226
	Mercury ^c	4.1x10 ⁻⁷	E	34, 226
	Nickel ^c	3.0x10 ⁻⁶	D	24, 34, 226
	Selenium ^c	4.9x10 ⁻⁷	E	34, 226
	Zinc	6.8x10 ⁻⁶	D	24, 34, 226

^a Emission factor units are lb/ton of HMA produced. Emissions controlled by a fabric filter.

SCC = Source Classification Code. To convert from lb/ton to kg/Mg, multiply by 0.5.

^b Natural gas-, propane-, No. 2 fuel oil-, or waste oil-/drain oil-/No. 6 fuel oil-fired dryer. For waste oil-/drain oil-/No. 6 fuel oil-fired dryer, use a lead emission factor of 1.0x10⁻⁵ lb/ton (References 177 and 321, Emission factor rating: E) in lieu of the emission factor shown.

^c Arsenic, beryllium, cadmium, chromium, hexavalent chromium, lead, manganese, mercury, nickel, and selenium are HAPs as defined in the 1990 CAAA.

Table 11.1-12. EMISSION FACTORS FOR METAL EMISSIONS
FROM DRUM MIX HOT MIX ASPHALT PLANTS^a

Process	Pollutant	Emission Factor, lb/ton	Emission Factor Rating	Reference Numbers
Fuel oil-fired dryer, uncontrolled (SCC 3-05-002-58, -59,-60)	Arsenic ^b	1.3x10 ⁻⁶	E	340
	Barium	0.00025	E	340
	Beryllium ^b	0.0	E	340
	Cadmium ^b	4.2x10 ⁻⁶	E	340
	Chromium ^b	2.4x10 ⁻⁵	E	340
	Cobalt ^b	1.5x10 ⁻⁵	E	340
	Copper	0.00017	E	340
	Lead ^b	0.00054	E	340
	Manganese ^b	0.00065	E	340
	Nickel ^b	0.0013	E	340
	Phosphorus ^b	0.0012	E	340
	Selenium ^b	2.4x10 ⁻⁶	E	340
	Thallium	2.2x10 ⁻⁶	E	340
Zinc	0.00018	E	340	
Natural gas- or propane-fired dryer, with fabric filter (SCC 3-05-002-55, -56,-57))	Antimony	1.8x10 ⁻⁷	E	339
	Arsenic ^b	5.6x10 ⁻⁷	D	25, 35, 339-340
	Barium	5.8x10 ⁻⁶	E	25, 339-340
	Beryllium ^b	0.0	E	339-340
	Cadmium ^b	4.1x10 ⁻⁷	D	25, 35, 162, 301, 339-340
	Chromium ^b	5.5x10 ⁻⁶	C	25, 162-164, 301, 339-340
	Cobalt ^b	2.6x10 ⁻⁸	E	339-340
	Copper	3.1x10 ⁻⁶	D	25, 162-164, 339-340
	Hexavalent chromium ^b	4.5x10 ⁻⁷	E	163
	Lead ^b	6.2x10 ⁻⁷	E	35
	Manganese ^b	7.7x10 ⁻⁶	D	25, 162-164, 339-340
	Mercury ^b	2.4x10 ⁻⁷	E	35, 163
	Nickel ^b	6.3x10 ⁻⁵	D	25, 163-164, 339-340
	Phosphorus ^b	2.8x10 ⁻⁵	E	25, 339-340
	Silver	4.8x10 ⁻⁷	E	25, 339-340
Selenium ^b	3.5x10 ⁻⁷	E	339-340	
Thallium	4.1x10 ⁻⁹	E	339-340	
Zinc	6.1x10 ⁻⁵	C	25, 35, 162-164, 339-340	

Table 11.1-12 (cont.)

Process	Pollutant	Emission Factor, lb/ton	Emission Factor Rating	Reference Numbers
No. 2 fuel oil-fired dryer or waste oil/drain oil/No. 6 fuel oil-fired dryer, with fabric filter (SCC 3-05-002-58, -59,-60,-61,-62,-63)	Antimony	1.8x10 ⁻⁷	E	339
	Arsenic ^b	5.6x10 ⁻⁷	D	25, 35, 339-340
	Barium	5.8x10 ⁻⁶	E	25, 339-340
	Beryllium ^b	0.0	E	339-340
	Cadmium ^b	4.1x10 ⁻⁷	D	25, 35, 162, 301, 339-340
	Chromium ^b	5.5x10 ⁻⁶	C	25, 162-164, 301, 339-340
	Cobalt ^b	2.6x10 ⁻⁸	E	339-340
	Copper	3.1x10 ⁻⁶	D	25, 162-164, 339-340
	Hexavalent chromium ^b	4.5x10 ⁻⁷	E	163
	Lead ^b	1.5x10 ⁻⁵	C	25, 162, 164, 178-179, 183, 301, 315, 339-340
	Manganese ^b	7.7x10 ⁻⁶	D	25, 162-164, 339-340
	Mercury ^b	2.6x10 ⁻⁶	D	162, 164, 339-340
	Nickel ^b	6.3x10 ⁻⁵	D	25, 163-164, 339-340
	Phosphorus ^b	2.8x10 ⁻⁵	E	25, 339-340
	Silver	4.8x10 ⁻⁷	E	25, 339-340
	Selenium ^b	3.5x10 ⁻⁷	E	339-340
Thallium	4.1x10 ⁻⁹	E	339-340	
Zinc	6.1x10 ⁻⁵	C	25, 35, 162-164, 339-340	

^a Emission factor units are lb/ton of HMA produced. SCC = Source Classification Code. To convert from lb/ton to kg/Mg, multiply by 0.5. Emission factors apply to facilities processing virgin aggregate or a combination of virgin aggregate and RAP.

^b Arsenic, beryllium, cadmium, chromium, hexavalent chromium, cobalt, lead, manganese, mercury, nickel, and selenium compounds are HAPs as defined in the 1990 CAAA. Elemental phosphorus also is a listed HAP, but the phosphorus measured by Method 29 is not elemental phosphorus.

Table 11.1-13. EMISSION FACTORS FOR ORGANIC POLLUTANT EMISSIONS FROM HOT MIX ASPHALT HOT OIL HEATERS^a

EMISSION FACTOR RATING: E

Process	Pollutant		Emission factor, lb/gal	
	CASRN	Name		
Hot oil heater fired with No. 2 fuel oil (SCC 3-05-002-08)	50-00-0	Formaldehyde	0.027	
	83-32-9	Acenaphthene ^b	5.3x10 ⁻⁷	
	208-96-8	Acenaphthylene ^b	2.0x10 ⁻⁷	
	120-12-7	Anthracene ^b	1.8x10 ⁻⁷	
	205-99-2	Benzo(b)fluoranthene ^b	1.0x10 ⁻⁷	
	206-44-0	Fluoranthene ^b	4.4x10 ⁻⁸	
	86-73-7	Fluorene ^b	3.2x10 ⁻⁸	
	91-20-3	Naphthalene ^b	1.7x10 ⁻⁵	
	85-01-8	Phenanthrene ^b	4.9x10 ⁻⁶	
	129-00-0	Pyrene ^b	3.2x10 ⁻⁸	
	Dioxins			
	19408-74-3	1,2,3,7,8,9-HxCDD ^b	7.6x10 ⁻¹³	
	39227-28-6	1,2,3,4,7,8-HxCDD ^b	6.9x10 ⁻¹³	
		HxCDD ^b	6.2x10 ⁻¹²	
	35822-46-9	1,2,3,4,6,7,8-HpCDD ^b	1.5x10 ⁻¹¹	
		HpCDD ^b	2.0x10 ⁻¹¹	
	3268-87-9	OCDD ^b	1.6x10 ⁻¹⁰	
		Total PCDD	2.0x10 ⁻¹⁰	
	Furans			
			TCDF ^b	3.3x10 ⁻¹²
			PeCDF ^b	4.8x10 ⁻¹³
			HxCDF ^b	2.0x10 ⁻¹²
			HpCDF ^b	9.7x10 ⁻¹²
		67562-39-4	1,2,3,4,6,7,8-HpCDF ^b	3.5x10 ⁻¹²
		39001-02-0	OCDF ^b	1.2x10 ⁻¹¹
			Total PCDF	3.1x10 ⁻¹¹
		Total PCDD/PCDF	2.3x10 ⁻¹⁰	

^a Reference 35. Emission factor units are lb/gal of fuel consumed. To convert from lb/gal to kilograms per liter (kg/L), multiply by 0.12. CASRN = Chemical Abstracts Service Registry Number. SCC = Source Classification Code.

^b Compound is classified as polycyclic organic matter, as defined in the 1990 Clean Air Act Amendments (CAAA). Total PCDD is the sum of the total tetra through octa dioxins; total PCDF is sum of the total tetra through octa furans; and total PCDD/PCDF is the sum of total PCDD and total PCDF.

Table 11.1-14. PREDICTIVE EMISSION FACTOR EQUATIONS
FOR LOAD-OUT AND SILO FILLING OPERATIONS^a

EMISSION FACTOR RATING: C

Source	Pollutant	Equation
Drum mix or batch mix plant load-out (SCC 3-05-002-14)	Total PM ^b	$EF = 0.000181 + 0.00141(-V)e^{((0.0251)(T + 460) - 20.43)}$
	Organic PM ^c	$EF = 0.00141(-V)e^{((0.0251)(T + 460) - 20.43)}$
	TOC ^d	$EF = 0.0172(-V)e^{((0.0251)(T + 460) - 20.43)}$
	CO	$EF = 0.00558(-V)e^{((0.0251)(T + 460) - 20.43)}$
Silo filling (SCC 3-05-002-13)	Total PM ^b	$EF = 0.000332 + 0.00105(-V)e^{((0.0251)(T + 460) - 20.43)}$
	Organic PM ^c	$EF = 0.00105(-V)e^{((0.0251)(T + 460) - 20.43)}$
	TOC ^d	$EF = 0.0504(-V)e^{((0.0251)(T + 460) - 20.43)}$
	CO	$EF = 0.00488(-V)e^{((0.0251)(T + 460) - 20.43)}$

^a Emission factor units are lb/ton of HMA produced. SCC = Source Classification Code. To convert from lb/ton to kg/Mg, multiply by 0.5. EF = emission factor; V = asphalt volatility, as determined by ASTM Method D2872-88 “Effects of Heat and Air on a Moving Film of Asphalt (Rolling Thin Film Oven Test - RTFOT),” where a 0.5 percent loss-on-heating is expressed as “-0.5.” Regional- or site-specific data for asphalt volatility should be used, whenever possible; otherwise, a default value of -0.5 should be used for V in these equations. T = HMA mix temperature in °F. Site-specific temperature data should be used, whenever possible; otherwise a default temperature of 325°F can be used. Reference 1, Tables 4-27 through 4-31, 4-34 through 4-36, and 4-38 through 4-41.

^b Total PM, as measured by EPA Method 315 (EPA Method 5 plus the extractable organic particulate from the impingers). Total PM is assumed to be predominantly PM-2.5 since emissions consist of condensed vapors.

^c Extractable organic PM, as measured by EPA Method 315 (methylene chloride extract of EPA Method 5 particulate plus methylene chloride extract of impinger particulate).

^d TOC as propane, as measured with an EPA Method 25A sampling train or equivalent sampling train.

Table 11.1-15. SPECIATION PROFILES FOR LOAD-OUT, SILO FILLING, AND ASPHALT STORAGE EMISSIONS—ORGANIC PARTICULATE-BASED COMPOUNDS

EMISSION FACTOR RATING: C

Pollutant	CASRN ^a	Speciation Profile for Load-out and Yard Emissions ^b	Speciation Profile for Silo Filling and Asphalt Storage Tank Emissions
		Compound/Organic PM ^c	Compound/Organic PM ^c
<u>PAH HAPs</u>			
Acenaphthene	83-32-9	0.26%	0.47%
Acenaphthylene	208-96-8	0.028%	0.014%
Anthracene	120-1207	0.070%	0.13%
Benzo(a)anthracene	56-55-3	0.019%	0.056%
Benzo(b)fluoranthene	205-99-2	0.0076%	ND ^d
Benzo(k)fluoranthene	207-08-9	0.0022%	ND ^d
Benzo(g,h,i)perylene	191-24-2	0.0019%	ND ^d
Benzo(a)pyrene	50-32-8	0.0023%	ND ^d
Benzo(e)pyrene	192-97-2	0.0078%	0.0095%
Chrysene	218-01-9	0.103%	0.21%
Dibenz(a,h)anthracene	53-70-3	0.00037%	ND ^d
Fluoranthene	206-44-0	0.050%	0.15%
Fluorene	86-73-7	0.77%	1.01%
Indeno(1,2,3-cd)pyrene	193-39-5	0.00047%	ND ^d
2-Methylnaphthalene	91-57-6	2.38%	5.27%
Naphthalene	91-20-3	1.25%	1.82%
Perylene	198-55-0	0.022%	0.030%
Phenanthrene	85-01-8	0.81%	1.80%
Pyrene	129-00-0	0.15%	0.44%
Total PAH HAPs		5.93%	11.40%
<u>Other semi-volatile HAPs</u>			
Phenol		1.18%	ND ^d

^a Chemical Abstract Service Registry Number.

^b Emissions from loaded trucks during the period between load-out and the time the truck departs the plant.

^c Emission factor for compound is determined by multiplying the percentage presented for the compound by the emission factor for extractable organic particulate (organic PM) as determined from Table 11.1-14.

^d ND = Measured data below detection limits.

Table 11.1-16. SPECIATION PROFILES FOR LOAD-OUT, SILO FILLING, AND ASPHALT STORAGE EMISSIONS—ORGANIC VOLATILE-BASED COMPOUNDS

EMISSION FACTOR RATING: C

Pollutant	CASRN	Speciation Profile for Load-Out and Yard Emissions	Speciation Profile for Silo Filling and Asphalt Storage Tank Emissions
		Compound/TOC ^a	Compound/TOC (%) ^a
VOC ^b		94% ^b	100%
<u>Non-VOC/non-HAPs</u>			
Methane	74-82-8	6.5%	0.26%
Acetone	67-64-1	0.046%	0.055%
Ethylene	74-85-1	0.71%	1.1%
Total non-VOC/non-HAPS		7.3%	1.4%
<u>Volatile organic HAPS</u>			
Benzene	71-43-2	0.052%	0.032%
Bromomethane	74-83-9	0.0096%	0.0049%
2-Butanone	78-93-3	0.049%	0.039%
Carbon Disulfide	75-15-0	0.013%	0.016%
Chloroethane	75-00-3	0.00021%	0.0040%
Chloromethane	74-87-3	0.015%	0.023%
Cumene	92-82-8	0.11%	ND ^c
Ethylbenzene	100-41-4	0.28%	0.038%
Formaldehyde	50-00-0	0.088%	0.69%
n-Hexane	100-54-3	0.15%	0.10%
Isooctane	540-84-1	0.0018%	0.00031%
Methylene Chloride	75-09-2	0.0% ^d	0.00027%
MTBE	596899	0.0% ^d	ND ^c
Styrene	100-42-5	0.0073%	0.0054%
Tetrachloroethene	127-18-4	0.0077%	ND ^c
Toluene	100-88-3	0.21%	0.062%
1,1,1-Trichloroethane	71-55-6	0.0% ^d	ND ^c
Trichloroethene	79-01-6	0.0% ^d	ND ^c
Trichlorofluoromethane	75-69-4	0.0013%	ND ^c
m-/p-Xylene	1330-20-7	0.41%	0.2%
o-Xylene	95-47-6	0.08%	0.057%
Total volatile organic HAPs		1.5%	1.3%

^a Emission factor for compound is determined by multiplying the percentage presented for the compound by the emission factor for total organic compounds (TOC) as determined from Table 11.1-14.

Table 11.1-16 (cont.)

- ^b The VOC percentages are equal to 100 percent of TOC minus the methane, acetone, methylene chloride, and 1,1,1-trichloroethane percentages.
- ^c ND = Measured data below detection limits. Additional compounds that were not detected are: acrylonitrile, allyl chloride, bromodichloromethane, bromoform, 1,3-butadiene, carbon tetrachloride, chlorobenzene, chloroform, dibromochloromethane, 1,2-dibromoethane, 1,1-dichloroethane, 1,2-dichloroethane, 1,1-dichloroethene, cis-1,2-dichloroethene, trans-1,2-dichloroethene, 1,2-dichloropropane, cis-1,3-dichloropropene, trans-1,3-dichloropropene, 1,2-epoxybutane, ethyl acrylate, 2-hexanone, iodomethane, methyl methacrylate, 1,1,2,2-tetrachloroethane, 1,1,2-trichloroethane, vinyl acetate, vinyl bromide, and vinyl chloride
- ^d Values presented as 0.0% had background concentrations higher than the capture efficiency-corrected measured concentration.

REFERENCES FOR SECTION 11.1

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