

Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources*. AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

AP42 Section: 13.2.6

Background Chapter 4

Reference: 6

**Title: Summary of Source Test Results, Poly Engineering, Richmond, CA,
Bay Area Air Quality Management District, San Francisco,
CA,**

November 19, 1990.

DISTRIBUTION: Firm Permit Services Enforcement Technical Services Source Inventory Planning Requester DAPCO	BAY AREA AIR QUALITY MANAGEMENT DISTRICT 939 Ellis Street San Francisco, California 94109 (415) 771-6000 SUMMARY OF SOURCE TEST RESULTS	Report No. <u>91077</u> Test Date: <u>11/2/90</u> Test Times: Run A: <u>0935-1109</u> (56 min) Run B: <u>1121-1309</u> (48 min) Run C: <u>1320-1419</u> (48 min)
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SOURCE INFORMATION		BAAQMD REPRESENTATIVES
Firm Name and Address POLY ENGINEERING 701 Erlandson Street Richmond, CA 94804	Firm Representative and Title Mr. Dan Lynch General Manager Phone No. (415)233-1420	Source Test Engineers C. McClure/H. Doi/K. Kunaniec
Permit Conditions None	Source: S-1 Sandblast Booth Plant No. 2503 Operates 8 hr/day & 260 days/yr	Permit Services Division / Enforcement Division N. Yee Test Requested by: D. Nelson

Operating Parameters:
 Pneumatic blast room operated intermittently during testing utilizing an average of 1740 lb/hr of abrasive to blast 700 lb/hr of parts. Abrasive is C.A.R.B. certified 30/40 mesh garnet conveyed by 60 to 70 psi air.

Applicable Regulations: 6-310, 6-311	VN Recommended: NO
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Source Test Results and Comments:

<u>METHOD: TEST</u>	<u>RUN A</u>	<u>RUN B</u>	<u>RUN C</u>	<u>AVERAGE</u>	<u>LIMIT</u>
ST-17 Stack Volume Flowrate, SDCFM				2520	
Stack Gas Temperature °F	70	75	80	75	
Water Content, Volume %				1.0*	
ST-15 Particulate, gr/SDCF	.040	.066	.058	.055	.15
Particulate, lb/hr	.9	1.4	1.2	1.2	4.7
Isokinetic Ratio, Act/Theo.	1.01	1.00	0.98		

* Determined Psychrometrically

NO COMMERCIAL USE OF THESE RESULTS IS AUTHORIZED

Source Test Team Leader <i>C. J. McClure</i> C. McClure	Date 11/16/90	Senior Source Test Engineer <i>K. Kunaniec</i> K. Kunaniec	Date 11/19/90	Approved by Source Test Manager <i>G. Karels</i> G. Karels	Date 11/19/90
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ISOTHERMICS-

PDLI ENGINEERING #2503

S-1 11/2/90

$D_n = 4.5 \text{ mm} = .45 \text{ cm}$

$$R_I = \frac{(T_s)(V_m)(100)}{(60)(100 - \%H_2O)(A_n)(V_s)(TIME)(T_m)}$$

$$A_n = 0.0002691 \pi (D_{ncm})^2 \text{ ft}^2$$

$$A_n = 0.0002691 \pi (.45 \text{ cm})^2 \text{ ft}^2$$

$$A_n = 0.0001712 \text{ ft}^2$$

$$A_n = 1.712 \times 10^{-4} \text{ ft}^2$$

RUNA) $T_s = 529.6^\circ R$ $V_m = 25.996 \text{ ft}^3$ $V_s = 46.34 \text{ FPS}$ $TIME = 56 \text{ MIN}$ $T_m = 577.1^\circ R$
 $\%H_2O = 1\%$ $100 - \%H_2O = 99$

$$R_{IA} = \frac{(529.6)(25.996)(100)}{(60)(99)(1.712 \times 10^{-4})(46.34)(56)(577.1)} = 1.009$$

$$R_{IA} = 1.01$$

RUNB) $T_s = 535.25^\circ R$ $V_m = 22.95 \text{ ft}^3$ $V_s = 48.21 \text{ FPS}$ $TIME = 4 \text{ MIN}$ $T_m = 523.4^\circ R$
 $100 - \%H_2O = 99$

$$R_{IB} = \frac{(535.25)(22.95)(100)}{(60)(99)(1.712 \times 10^{-4})(48.21)(4)(523.4)} = 0.997$$

$$R_{IB} = 1.00$$

RUNC) $T_s = 540.9^\circ R$ $V_m = 22.44 \text{ ft}^3$ $V_s = 47.39 \text{ FPS}$ $TIME = 4 \text{ MIN}$ $T_m = 537^\circ R$
 $100 - \%H_2O = 99$

$$R_{IC} = \frac{(540.9)(22.44)(100)}{(60)(99)(1.712 \times 10^{-4})(47.39)(4)(537)} = 0.977$$

$$R_{IC} = 0.98$$

GRAIN LOADING:

$$G_{gr}/SDCF = 15.43 \cdot \frac{W_p}{V_0}$$

$$G_A = \frac{15.43(0.0694)}{26.84} = \underline{0.0399}$$

$$\underline{G_A = 0.0409 \text{ gr}/SDCF}$$

$$G_B = \frac{15.43(0.1004)}{23.41} = \underline{0.0662}$$

$$\underline{G_B = 0.066 \text{ gr}/SDCF}$$

$$G_C = \frac{15.43(0.0833)}{22.31} = \underline{0.0576}$$

$$\underline{G_C = 0.058 \text{ gr}/SDCF}$$

MASS EMISSIONS:

$$M = \frac{G \cdot Q}{116.67} \text{ Lb}/\text{HR}$$

$$M_A = \frac{(0.0399)(2521)}{116.67} = \underline{0.9 \text{ Lb}/\text{HR}}$$

$$M_B = \frac{(0.0662)(2521)}{116.67} = \underline{1.4 \text{ Lb}/\text{HR}}$$

$$M_C = \frac{(0.0576)(2521)}{116.67} = \underline{1.2 \text{ Lb}/\text{HR}}$$

PDLT ~~to~~ ENGINEERING #2503
S-1 11/2/90

$$W_{PA} = 0.0694 \text{ g}$$

$$W_{PB} = 0.1004 \text{ g}$$

$$W_{PC} = 0.0833 \text{ g}$$

$$V_{DA} = 26.84 \text{ SDCF}$$

$$V_{DB} = 23.41 \text{ SDCF}$$

$$V_{DC} = 22.31 \text{ SDCF}$$

$$G_{AVG} = 0.055 \text{ gr}/\text{SDCF}$$

$$Q = 2521 \text{ SDCF}/\text{HR}$$

$$M_{AVG} = 1.2 \text{ Lb}/\text{HR}$$

SOURCE TEST LAB DATA SHEET

PLANT: POLY ENGINEERING
 SOURCE OPERATION: SANDBLASTING CABINETS
 SOURCE TEST NO.: _____
 FILTER MEDIA: 110MM FLAT GLASS FIBRE

PAGE 1 OF 1
 INITIAL CM
 TEST DATE 11/2/90

Drying Procedure: 105°C 24 hours before
 and after test, desiccated

WINDER DATA

RUN NO.	FILTER NO.	TARE WEIGHT (g)		FINAL WEIGHT (g)		SAMPLE WEIGHT (g)
		<small>9/6/90 Am</small>	<small>9/2/90 Am</small>	<small>11/6/90 Am</small>	<small>11/8/90 Am</small>	
A	443	.7154	.7155	.7339	.7341	0.0184 ✓
B	444	.7067	.7069	.7307	.7308	0.0238 ✓
C	445	.7137	.7137	.7347	.7349	0.0210 ✓

PROBE & NOZZLE RINSE DATA (total all runs)

RUN NO.	FILTER NO.	JAR SAMPLE FINAL WEIGHT (g)	FILTER SAMPLE FINAL WEIGHT (g)	SAMPLE WEIGHT (g)
A	443	0.0510	0.0184	0.0694 ✓
B	444	0.0766	0.0238	0.1004 ✓
C	445	0.0623	0.0210	0.0833 ✓

PROBE & NOZZLE RINSE DATA (each run)

RUN NO.	PROBE/NOZZLE NOS.	JAR TARE WEIGHT (g)		JAR FINAL WEIGHT (g)		JAR SAMPLE WEIGHT (g)
		<small>10/30/90 Am</small>	<small>7/23/88 Am</small>	<small>11/7/90 Am</small>	<small>11/9/90 Am</small>	
A	11	54.5158	54.5157	54.5668	54.5669	0.0510 ✓
B	23	54.9315	54.9312	55.0081	55.0083	0.0766 ✓
C	24	56.2977	56.2980	56.3603	56.3604	0.0623 ✓

IMPINGER DATA

SOLUTION	NO.	A TARE WEIGHT	B FILLED WEIGHT	C FINAL WEIGHT	C-A SAMPLE WEIGHT	C-B COMPONENTS WEIGHT

OK
 CM
 11/13/90



SANDS/MARLE 30-TO-GARNET 1-17-57
 WELSH-CARACTS HANDRAINS - 2-2-57
 Source Operation SAND AND ASBESTOS
 Plant ADY ENGINEERING
 Sample Type ASBESTOS
 Process Cycle BREATHABLE
 Duct Size 11.24 x 11
 Duct Pressure -1.30" H₂O
 ASSUMED H₂O 1.90

A. Swim Nozzle Diameter
 0.85 Pilot Tube
 AMBIENT Gas Collector No.
 30.15 Barometric Pressure
 0.002 Leak Rate @ 15" Hg
 TIME EACH POINT
 # OF POINTS
 TIME EACH RUN

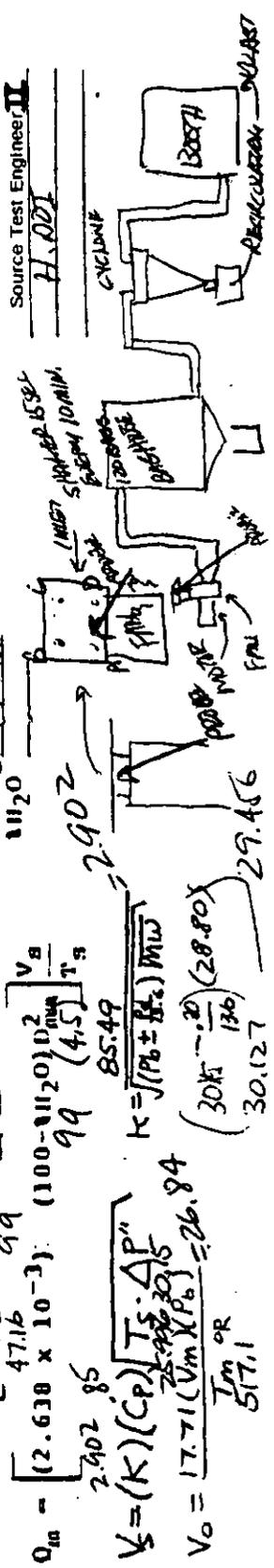
Source Test No. IEA
 Run No. 4240
 Date: 4/2/60

18.64 SEC IN BUCKET

Sampling Train: PROBE → FILTER #43 → IMPH P-1 IMPH P-2 → PUMP# D684 → METER# 103970A → EXH.

Traverse Point	Dist. From Inches	INITIAL TRAVERSE		Traverse Point	h H ₂ O	Vg FPS	0935 Time	Rate CFM	Temp OF	METER			Sat'd Gas Temp OF	Tg Duct Temp OF	REMARKS
		Duct Temp OF	ΔP H ₂ O							Volume Ft ³	Vac "Hg	CFM			
A	.65	STOPPED	STOPPED	A1	.65	4570	7.8	4577	56	35.1364	6	32	68	27.5	
B	.50	STOPPED	STOPPED	B2	.65	457	4.18	4577	56	57.72.71	6	35	68	27.5	
C	.75 TO .90	STOPPED	STOPPED	B1	.45	388	21.27	3806	56	62.0.40	4	35	69	22.8	
D	.75	STOPPED	STOPPED	B2	.38	34.9	29.30	3476	56	62.85	4	34	69	20.9	
				C1	.90	53.88	35.45	5376	56	62.0.68	7	34	70	32.2	
				L2	.90	53.88	42.54	5376	59	72.94.49	7	35	70	32.3	
				O2	.75	49.23	41.63	4903	59	73.92.93	6	36	71	29.4	
				D2	.75	49.23	56	4897	59	77.7.36	6	37	72	29.4	
ΔP = 1.70										57.1.26					
Ts = 52.2										57.1.26					

Q_m = 13.7 [$\frac{52.2}{T_s + 460} \left(\frac{V_g (100 - 11120)}{47.16} \right) = 4.58 \text{ g/sec Condensate (g)}$]
 1120 EQUATION = 11.36 9066PTS 34 PALS BUA STATION THIS RUN
 B-STATION



Source Test Team
 CHUCK McCLURE
 Source Test Engineer
 H. OOI

Q_m = (2.638 x 10⁻³) (100 - 11120) $\frac{V_g}{99} (4.5) T_s$
 $\frac{2.902 \cdot 85}{85.49} = 2.902$
 $K = \sqrt{\frac{P_0 - P_2}{P_0}} \frac{V_g}{T_s}$
 $V_0 = 17.71 (V_m \times P_0) = 26.84$
 $\frac{T_m \text{ OR } 57.1}{30.127} = 29.466$

Source Operation SAND BUST BODY
 Plant FRY FABRICATING
 Sample Type FABRIC WASTE
 Process Cycle FABRIC
 Duct Size 11.75 X 11
 Duct Pressure 30" H2O
 ASSUMED H2O 1.90

Source Test No. B

Run No. 1112190

Date: 7/5 + 7 40#

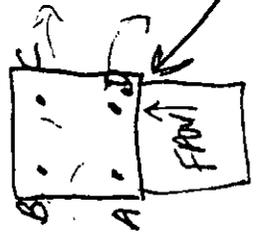
4.5" Nozzle Diameter
 PDS Pitot Tube
 AMB/FM Gas Collector No.
 3015 Barometric Pressure
 0.0022 Leak Rate @ 15" Hg
 TIME EACH POINT
 # OF POINTS
 TIME EACH RUN

Sampling Train: PROBE → FILTER # 444 → IMP # P-3 IMP # P-4 → PUMP # D684 → METER # 10370 → EXH.

Traverse Point	Dist. From inches	INITIAL TRAVERSE		Traverse Point	h H2O	Vg FPS	Time	Rate CFM	Temp OF	METER			Sat'd Gas Temp OF	Tg Duct Temp OF	REMARKS
		Duct Temp OF	ΔP							Volume Ft ³	Vac "Hg	Ratio Vm/Point			
A1				A1	.70	47.9	1121.0	6.4741	60	379.02	8	35	70	28.4	
A2				A2	.70	47.65		12.4728	60	384.72	8	36	73	28.4	
B1				B1	.5	40.2		6.18.4003	62	371.18	7	33	71	24.0	
B2				B2	.65	46.8		12.24.4539	62	388.90	8	36	77	27.2	
C1				C1	.90	54.23		19.30.5341	64	353.10	9	37	77	32.0	
C2				C2	.90	54.23		24.36.5341	65	368.30	9	38	77	32.0	
D1				D1	.70	47.8		37.42.4706	66	393.14	8	38	78	28.2	
D2				D2	.70	47.92		40.148.4701	68	401.97	8	39	79	28.2	
									63.4	22.95	8.125	34.5	75.25		
									523A				835.25		

B-STATION

Source Test Team
 CHUCK MCCLURE
 Source Test Engineer



Condensate V0 (9) SKF
 1120

$$D_n = 13.7 \left[\frac{T_a + 460}{V_s (100 - \%H_2O)} \right]^{1/2}$$

$$Q_m = \left[(2.638 \times 10^{-3}) (100 - \%H_2O) D_n^2 \frac{V_s}{T_s} \right]$$

$$V_s = (K) (CP) \sqrt{T_s \cdot \Delta P}$$

$$V_0 = \frac{17.71 (V_m \times P_b)}{T_m \text{ or } T_s}$$

$$K = \frac{85.49}{\sqrt{(P_b \pm \Delta P) P_m}}$$

WB = 55°F
 DB = 68°F
 1% H2O

1139



BAY AREA AIR QUALITY MANAGEMENT DISTRICT
 939 Ellis Street, San Francisco, Calif. 94109 - 771-6000
 Source Test Data Sheet

Source Operation SPIN AIRS (600)H
 Plant PROT FAN/HEATING
 Sample Type PRECIPITATE
 Process Cycle CONTINUOUS
 Duct Size 11.75" x 11
 Duct Pressure - .30" H₂O
 ASSUMED H₂O 10%

Source Test No. C
 Run No. 11/21/90
 Date: 11/21/90

4.0" Nozzle Diameter
 O.P.S. Pitot Tube
 AMBIENT Gas Collector No.
 30.15 Barometric Pressure
 O.D.S. 21 Leak Rate @ 15" Hg
 TIME EACH POINT
 # OF POINTS
 TIME EACH RUN

21 + 20

Sampling Train: PROBE → FILTER #445 → IMPH #5 IMPH #6 → PUMPH #688A → METER #103970A → EXH.

Traverse Point	Dist. From inches	INITIAL TRAVERSE		Traverse Point	h H ₂ O	V _g FPS	Time	Rate CFM	Temp OF	METER		Vac "Hg	Sat'd Gas Temp OF	T _a Duct Temp OF	REMARKS
		Duct Temp OF	ΔP H ₂ O							Volume Ft. ³	Temp OF				
				A-1	.65	16.19	6	4.539	70	4.96	402.24	5.5	37	77	27.2
				A-2	.70	17.0	12	4.683	74	10.40	402.24	6	37	81	28.1
				B-1	.50	10.5	18	3.946	76	10.21	402.24	5	37	81	23.8
				B-2	.46	38.4	20	3.763	78	12.50	402.24	4	37	81	22.6
				C-1	.85	52.90	30	5.171	79	15.60	402.24	6	38	81	31.02
				C-2	.87	53.5	36	5.227	79	18.8	402.24	7	40	82	31.4
				D-1	.75	49.74	42	4.953	80	21.77	402.24	6	40	82	29.1
				D-2	.75	49.74	1419.48	4.953	80	24.68	402.24	6	41	82	29.1
									77	22.44	402.24	5.7	38	80.9	
									537					540A	

ALL READS BLASTED THIS RUN SAMPLING

$$Q_n = 13.7 \left[\frac{T_a + 460}{V_g (100 - \%H_2O)} \right]^{1/2}$$

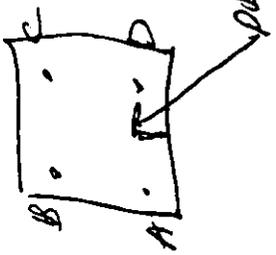
$$Q_n = \left[(2.638 \times 10^{-3}) \frac{V_g}{(100 - \%H_2O) D^2} \right] T_g$$

$$V_g = (K)(C_p) \sqrt{T_s \cdot \Delta P} \quad K = \frac{85.49}{\sqrt{(P_b \pm \Delta P) P_{std}}}$$

$$V_0 = \frac{17.71 (V_m)(P_b)}{T_m \text{ OR } P_{std}}$$

B-STATION

Source Test Team
 CHUCK MCCLURE
 Source Test Engineer II
 H. ADZ



POOR

PROCESS DATA

PD2 - ENGINEERING

11/2/90

S-1 #2583

GARNET

804.1g

859.4g

952.4g

967.1g

509.3g

SAMPLE TIME = 18.6 SEC

4092.3g

453.6 gm / 1Lb.

$$4092.3g \cdot \frac{1Lb}{453.6g} = \frac{9.02Lb}{18.6SEC} = 0.4850 Lb/SEC$$

$$0.4850 \frac{Lb}{SEC} \times \frac{60SEC}{MIN} \times \frac{60MIN}{HR} = \underline{\underline{1746 \frac{Lb}{HR} \text{ SAND IN.}}}$$

PARTS IN:

1 RAIL = 17.5 LBS RUN A) 34 RAIS at 17.5 Lb/RAIL = 595 LBS

RUN B) 15 RAIS at 17.5 Lb/RAIL = 262.5 Lb + 115 LBS MISCATS
= 377.5 LBS

RUN C) 41 RAIS at 17.5 Lb/RAIL = 717.5 LBS

AVERAGE 595.0 LBS 3 | 1690 LBS
377.5 LBS 563.33 Lb/RUN x $\frac{1RUN}{0.8HR}$ = 704.2 Lb/HR AVERAGE
717.5 LBS

~~1690 LBS~~ / ~~0.8 HRS~~ = ~~2112.5 LBS/HR~~
48 MIN

PD2 - ENGINEERING

SO: 1746 Lb/HR SAND IN

11/2/80 5-1 #2503

+ 704.2 Lb/HR PARTS PROCESSED

2450 Lb/HR > PROCESS

$$E_{MAX} = 4.10 (P_{TON/HR})^{0.67}$$

$$2450 \text{ Lb/HR} \cdot \frac{1 \text{ TON}}{2000 \text{ Lb}} = 1.22 \text{ TON/HR}$$

$$\underline{\underline{E_{MAX} \text{ Lb/HR}}} = 4.10 (1.22)^{0.67} = \underline{\underline{4.7 \text{ Lb/HR}}}$$

SOURCE TEST LAB DATA SHEET

PLANT: POLY ENGINEERING
 SOURCE OPERATION: SAND BLASTING BAGHOUSE
 SOURCE TEST NO.: _____
 FILTER MEDIA: H₂O IMPINGERS

PAGE 1 OF 1
 INITIAL CM
 TEST DATE 11/2/80

Drying Procedure: 105 °C 24 hours before and after test, desiccated

FILTER DATA

RUN NO.	FILTER NO.	TARE WEIGHT (g)	FINAL WEIGHT (g)	SAMPLE WEIGHT (g)

PROBE & NOZZLE RINSE DATA (total all runs)

RUN NO.	FILTER NO.	JAR SAMPLE FINAL WEIGHT (g)	FILTER SAMPLE FINAL WEIGHT (g)	SAMPLE WEIGHT (g)

PROBE & NOZZLE RINSE DATA (each run)

RUN NO.	PROBE/NOZZLE NOS.	JAR TARE WEIGHT (g)	JAR FINAL WEIGHT (g)	JAR SAMPLE WEIGHT (g)

IMPINGER DATA

SOLUTION	NO.	A TARE WEIGHT	B FILLED WEIGHT	C FINAL WEIGHT	C-A SAMPLE WEIGHT	C-B CONDENSATE WEIGHT
H ₂ O	P-1	482.0	582.1	581.8	99.8	<0.3> <-0.5>
	P-2	491.7	592.1	591.4	100.2	<0.2>
	P-3	486.3	586.5	583.9	97.6	<2.6> <-3.0>
	P-4	480.4	580.9	580.5	100.1	<0.4>
	P-5	495.1	595.3	593.6	98.5	<1.7> <-1.9>
	P-6	501.0	601.4	601.2	100.2	<0.2>

EMISSION TEST REPORT REVIEW SUMMARY

Source Category: Abrasive Blasting

Filename: refX.xls
 Ref. No.: X/6
 Date: 19-Jun-97
 Reviewer: BLS

Facility: Poly Engineering
 Location: Richmond, CA
 Source: Abrasive blasting w/FF
 Test date: 02-Nov-90

Emission Data/Mass Flux Rates/Emission Factors

Test ID	Parameter	Units	Values reported			
			Run 1	Run 2	Run 3	AVERAGE
1	Stack temperature	Deg F	69.6	75.25	80.9	75.3
	Pressure	in. Hg				#DIV/0!
	Moisture (assumed 1%)	%	1.0	1.0	1.0	1.0
	Oxygen	%	ND	ND	ND	0.0
	Gas volume sampled	dscf	26.00	22.95	22.44	23.80
	Vol. flow, actual	acfm	ND	ND	ND	0
	Vol. flow, standard*	dscfm	2,520	2,520	2,520	2,520
	Isokinetic variation	%	100.0	99.7	97.7	99.1
	Process rate (specify units)	1740 lb/hr	1740	1740	1740	1740
Indicate basis for process rate (feed or production): garnet (abrasive) used						
Pollutant mass:						
	Filterable PM	grams	0.0694	0.1004	0.0833	0.0844
Pollutant concentrations:						AVERAGE
	Filterable PM	gr/dscf	0.0412	0.0675	0.0573	0.0553
Pollutant mass flux rates:						AVERAGE
	Filterable PM	lb/hr	8.90E-01	1.46E+00	1.24E+00	1.20E+00
Emission factors (ENGLISH UNITS):						AVERAGE
	Filterable PM	lb/unit	5.11E-04	8.38E-04	7.11E-04	6.87E-04

*DSCFM BASED ON A STANDARD TEMPERATURE OF 68 DEGREES FAHRENHEIT