

*September, 2000*

**COMPLIANCE REPORT**

**COMPLIANCE TEST PROGRAM  
for  
PARTICULATE EMISSIONS  
from  
FLASH DRYER #3**

Submitted For:  
**OMYA, INC.**  
61 Main Street  
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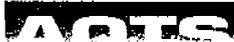
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Submitted To:  
**AGENCY OF NATURAL RESOURCES  
DEPARTMENT OF ENVIRONMENTAL CONSERVATION  
AIR POLLUTION CONTROL DIVISION**  
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Project Number: 001266

October 27, 2000

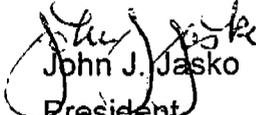


## FOREWORD

Air Quality Technical Services, Inc., an environmental consulting company specializing in air resource management and air quality assessment, has been contracted by OMYA, Inc. to conduct a source emission compliance program at the non-metallic mineral processing facility it owns and operates in Florence, Vermont.

This report presents program results, test and analytical data, sampling and analytical methods, and other relevant data.

To the best of my knowledge the data contained herein are correct and reliable.

  
John J. Jasko  
President

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## 1.0 INTRODUCTION

The State of Vermont Agency of Natural Resources Department of Environmental Conservation, Air Pollution Control Division (APCD), issued OMYA, Inc. (OMYA) an Amended Air Pollution Control Permit to Construct and Operate (#AOP-98-015a) on October 26, 1999, for a third flash dryer (Flash Dryer #3) at the Verpol facility it owns and operates in Florence, Vermont.

Condition (11) of the Permit states that at no time shall OMYA cause to be emitted from any fabric filter dust collector any stack visible emissions (VE) that exhibit greater than 7% opacity.

Condition (12) of the Permit limits the emission of particulate matter (PM) concentration from each fabric filter to 0.01 grains per dry standard cubic foot (gr/dscf) of undiluted exhaust gas, and further limits the time based emission rate of PM from Flash Dryer #3 to 0.86 pounds per hour (lbs/hr).

Condition (32) of the Permit requires that OMYA conduct PM and VE testing on Flash Dryer #3 to demonstrate compliance with the aforementioned standards and furnish the Agency with a written report of the results within 180 days after achieving normal operation.

The particulate emission portion of the compliance program was originally initiated and two test runs were completed on August 10, 2000. Test run 1-1 was interrupted on several occasions due to process upsets and was ultimately declared void due to the inability to demonstrate that the sample train met the post test leak check requirement. Test run 1-2 was completed without interruption and was deemed valid. On August 11 another run, test run 1-3, was started but was terminated after approximately 30 minutes due to a major process malfunction. The field portion of the compliance test program was rescheduled for September 27 and two runs, test runs 1-4 and 1-5, were completed. An attempt was made to complete an additional test run on September 28 but was aborted due to another major process malfunction.

The visible emission portion of the compliance program was not performed in conjunction with the particulate emission compliance evaluation. At the start of the initial program on August 10, the decision was made to place emphasis on completing particulate emission testing because of the uncertain operation of the process.

The major on-site representatives that participated in the field portion of the particulate emission compliance program, rescheduled for September 27, and their respective affiliations were:

OMYA, Inc.

Neal Jordan - Environmental Engineer

Jim Prior - Engineer

State of Vermont Agency of Natural Resources, Air Pollution Control Division

Dave Manning - Environmental Technician

Air Quality Technical Services, Inc.

John Jasko - Project Director

Roland Tremble - Environmental Technician

## 2.0 SUMMARY OF RESULTS

Particulate matter was measured as a non-filterable sample fraction collected by a filter media and preceding section of sample train. This fraction includes particulates greater than or equal to the particle cut point size of the filter media (0.3  $\mu$ ).

### 2.1 FLASH DRYER #3

#### 2.1.1 Particulate Matter

The concentrations of PM for the two test runs conducted September 27 were 0.0031, and 0.0026 gr/dscf, respectively, with an average of 0.0029 gr/dscf. The corresponding emission rates of PM were 0.31 and 0.29 lbs/hr with an average of 0.30 lbs/hr.

A summary of the PM test determinations for Flash Dryer #3 is presented in Table 2-1.

**TEST DATA SUMMARY****FLASH DRYER #3**

<b>PARTICULATE MATTER</b>			
<b>Test Run</b>	1-4	1-5	Average
Date	09/27/2000	09/27/2000	----
Clock Time (24 hour)	13:08-14:48	16:15-17:58	----
Test Duration (minutes)	96	96	----
Sample Volume (dscf)	75.265	81.754	----
<b>Test Measurements</b>			
Isokinetics (%)	96.4	95.1	----
Moisture Content (%)	17.2	15.1	16.1
Temperature (°F)	287.0	282.2	284.6
Gas Composition - CO <sub>2</sub> (%)	2.0	2.0	2.0
O <sub>2</sub> (%)	18.5	18.5	18.5
CO (%)	0	0	0
N <sub>2</sub> (%)	79.5	79.5	79.5
Gas Velocity (fps)	68.8	73.9	71.3
Gas Volumetric Flow (dscfm)	11721	12909	12315
(acfm)	20264	21767	21016
<b>Emission Determinations</b>			
<b>Particulate:</b>			
Concentration (gr/dscf)	0.0031	0.0026	0.0028
Emission Rate (lbs/hr)	0.31	0.29	0.30

Table 2-1

### 3.0 COMPLIANCE PROCEDURES

The procedures used in the source emission compliance/evaluation programs were conducted in accordance with standard methods described in 40 CFR 60 (revised July 1, 1999), **Standards of Performance for New Stationary Sources, Appendix A - Test Methods.**

The test methods used for the determination of compliance are referenced as follows:

- Method 1 - Sample Velocity Traverses for Stationary Sources;
- Method 2 - Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube);
- Method 3 - Gas Analysis for Determination of Dry Molecular Weight;
- Method 4 - Determination of Moisture Content in Stack Gas
- Method 5 - Determination of Particulate Emissions form Stationary Sources.

### 3.1 SAMPLING LOCATION

The sampling ports were positioned according to Method 1 - Sample and Velocity Traverses for Stationary Sources (40 CFR 60, App. A, pp. 577 - 584).

#### 3.1.1 Flash Dryer #3

Two sample ports were located 90° opposed on the stack approximately 132 inches from the top of a silencer located in the stack and approximately 30 inches from the discharge of the stack. At the sample port location the stack had an inside diameter of 30.5 inches. These dimensions placed the sample ports approximately 4.3 diameters downstream and 1.0 diameters upstream from respective flow disturbances.

In accordance with Method 1 a minimum of twenty-four sample points were required for a particulate traverse. Twelve traverse points positioned at 2.1, 6.7, 11.8, 17.7, 25.0, 35.6, 64.4, 75.0, 82.3, 88.2, 93.3 and 97.9 percent of the diameter ( 1.0, 2.0, 3.6, 5.4, 7.6, 10.9, 19.6, 22.9, 25.1, 26.9, 28.5, and 29.5 inches from the inner stack wall) were sampled through each port.

## 3.2 PARTICULATE

Sample collection and analysis was performed according to procedures outlined in Method 5 - Determination of Particulate Emissions from Stationary Sources (40 CFR 60, App. A, pp. 740 - 764).

A total of two test runs were conducted for the purpose of determining compliance. Each test run had a sample duration of 96 minutes and collected a volume close to or in excess of the 60 dscf required by 40 CFR Part 60, Subpart OOO for PM concentration determination (§ 60.675 Test Methods and Procedures). A sampling rate, +/- 10 percent of the isokinetic rate, was maintained over the course of each test run.

### 3.2.1 Sampling Apparatus

#### 3.2.1.1 Particulate

The PM sample train consisted of:

- a) a stainless steel nozzle sized to maintain isokinetic sampling;
- b) a borosilicate glass-lined probe heated to a temperature of 250 °F, +/- 25 °F;
- c) an encased glass fiber filter heated to a temperature of 250 °F, +/- 25 °F;
- d) a sample/moisture condensing unit with four 500 ml glass impingers immersed in an ice water bath:
  - 1 modified Greenburg-Smith type containing a volume of H<sub>2</sub>O tared to a known weight,
  - 1 Greenburg-Smith type containing a volume of H<sub>2</sub>O tared to a known weight,
  - 1 modified Greenburg-Smith type empty tared to a known weight; and,
  - 1 modified Greenburg-Smith type containing silica gel tared to a known weight;
- e) an umbilical; and,
- f) a metering console with: main valve and by-pass valve for flow adjustment, leak-free pump, calibrated dry gas meter with inlet and outlet temperature gauges, calibrated orifice, and inclined manometer.

The typical sampling apparatus is depicted in Figure 3-1.

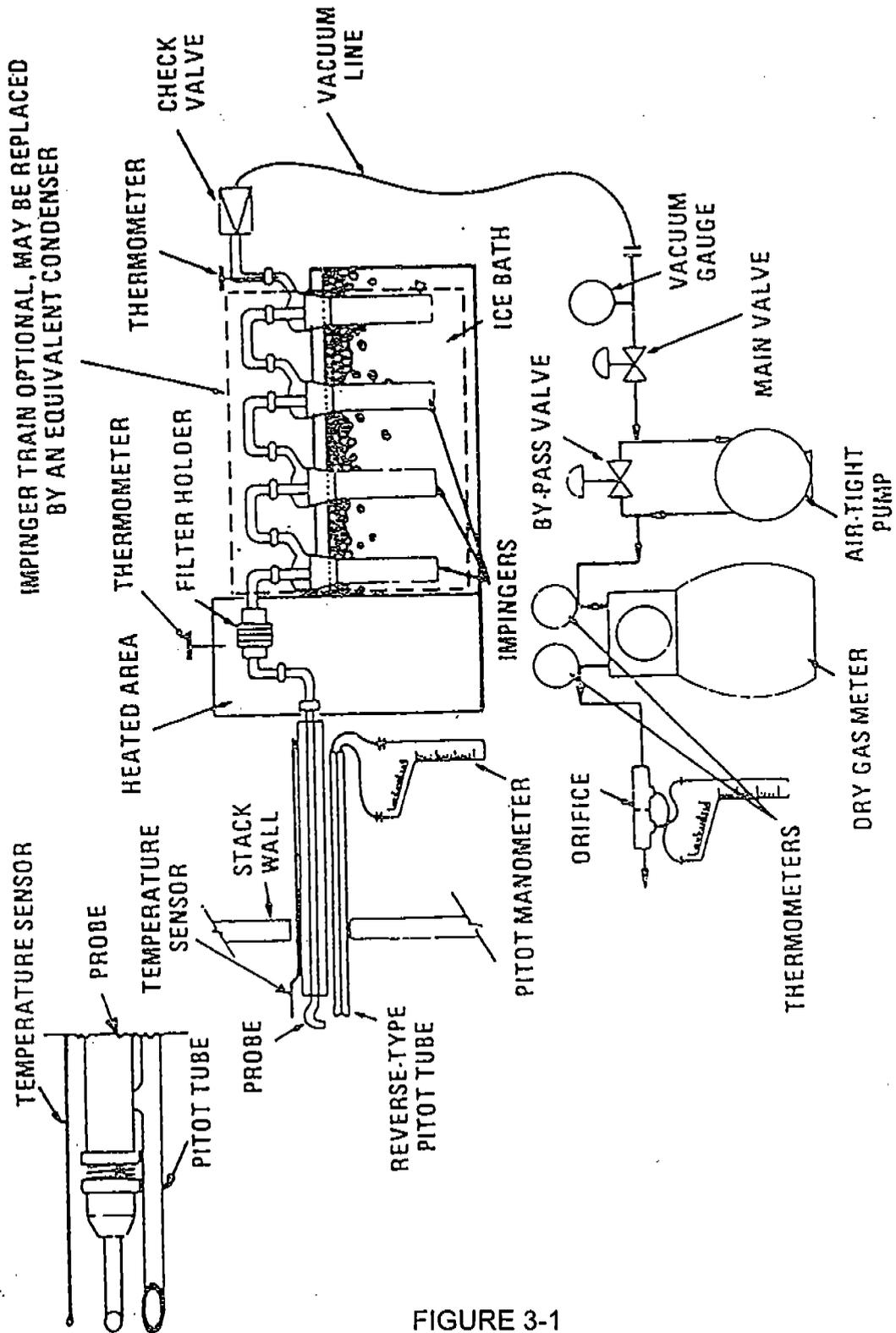


FIGURE 3-1

### 3.2.2 Sample Recovery

#### 3.2.2.1 Field

The samples were handled or recovered in the field using the procedures outlined below:

Filter - The filter holder was removed from the sample box, sealed, labeled for identification, and secured for transport.

Front half - The nozzle and probe were internally brushed and rinsed with acetone to remove any particulate matter which may have been deposited during a test run. The rinse was collected in a glass jar, sealed with a Teflon lined cap, labeled for identification noting the volume of the contents, and secured for transport.

Impinger catch - The first three impingers were weighed to determine the net weight gain attributable to condensed moisture which was recorded.

Silica gel - The silica gel impinger was weighed to determine the net weight gain attributable to condensed moisture which was recorded.

#### 3.2.2.2 Laboratory

The samples were recovered in the laboratory using the procedures outlined below:

Filter - The filter was removed from the filter holder and placed in the original container.

Front half - The front half of the filter holder was internally brushed and rinsed with acetone, and the filter support frit gasket was scraped off under an acetone rinse to recover any adhering filter media; this rinse was combined with the front half acetone rinse collected in the field.

### 3.2.3 Sample Analysis

#### 3.2.3.1 Particulate

Prior to use in the program, glass fiber filters were marked with an identifying number, desiccated for a minimum of 24 hours, weighed, re-desiccated for a minimum of 6 hours, re-weighed to establish a final constant weight (<0.5 mg difference), and,

sealed in individual plastic petri dish containers that were labeled with the identifying number and tare weight of the filter.

After use in the program, the filters were placed in a dessicator, desiccated for a minimum of 24 hours, weighed, re-dessicated for a minimum of 6 hours, re-weighed to establish a final constant weight (<0.5 mg difference).

The front half acetone washes were transferred to tared beakers, evaporated, desiccated for a minimum of 24 hours, weighed, re-dessicated for a minimum of 6 hours, re-weighed to establish a final constant weight (<0.5 mg difference).

### 3.3 GAS VELOCITY/VOLUMETRIC FLOW

Measurements of stack gas velocity and volumetric flow were performed according to procedures outlined in Method 2 - Determination of Stack Gas Velocity and Volumetric Flow Rate (40 CFR 60, App. A, pp. 586 - 603).

#### 3.3.1 Measurement Apparatus

The apparatus used to measure stack differential pressure and temperature profiles consisted of:

- a) a Type S (Stausscheibe) pitot tube with an assigned design coefficient of 0.84 connected to an inclined manometer; and,
- b) Type-K thermocouple probe connected to a digital pyrometer.

### 3.4 GAS COMPOSITION

Carbon dioxide (CO<sub>2</sub>) and oxygen (O<sub>2</sub>) sample collection and analyses was performed according to procedures outlined in using EPA Test Method 3 - Gas Analysis for the Determination of Dry Molecular Weight (40 CFR 60, App. A, pp. 726 - 729).

A single-point grab sample was taken and analyzed with Fyrite analyzers to measure the CO<sub>2</sub> and O<sub>2</sub> concentrations. The balance of the gas composition was considered N<sub>2</sub>. The results were used to determine the dry molecular weight of the effluent stream.

#### 4.0 QUALITY ASSURANCE/QUALITY CONTROL

Air Quality Technical Services, Inc. maintains a QA/QC program to ensure sampling techniques and analytical procedures are valid and data generated from test programs are accurate.

##### 4.1 CHAIN OF CUSTODY

AQTS utilizes chain-of-custody procedures. While in the field, samples collected during each test run are sealed in appropriate sample vessels, labeled and identified by field number, and placed in secure containers. Storage containers are the responsibility of the project director or assigned personnel. Upon return to AQTS facilities, samples are logged in and assigned sample identification numbers. Samples are safely and properly stored until processed and/or shipped to an outside laboratory.

##### 4.2 EQUIPMENT CALIBRATIONS

Dry gas meters and orifices undergo semi-annual calibration according to procedures outlined in Method 5, Section 5 - Calibration (§5.3 Metering System, §5.3.1 Calibration Prior to Use). After completion of compliance programs, dry gas meter calibrations are rechecked for accuracy according to procedures outlined in Method 5, Section 5 - Calibration (§5.3 Metering System, §5.3.2 Calibration After Use).

Prior to use in compliance programs, probe nozzles are calibrated according to procedures outlined in Method 5, Section 5 - Calibration (§5.1 Probe Nozzle).

Thermometers and barometers are calibrated according to Method 6, §5.2 and §5.4.

Prior to field use, pitot tube assemblies are checked for conformity with the design specifications listed in Method 2 (4. Calibration, §4.1 Type S Pitot Tube, §4.1.1 Type S Pitot Tube Assemblies).

Thermocouple probes undergo annual calibration according to procedures outlined in the Quality Assurance Handbook, Section 3.1 - Method 2 (§3.1.2 Calibration of Apparatus).

### 4.3 EQUIPMENT LEAK CHECKS

#### 4.3.1 Particulate Sample Trains

Sample trains are leak checked according to procedures outlined in Method 5, Section 4 - Procedure (§4.1 Sampling, §4.1.4 Leak-Check Procedures). Before the start of each test run, the inlet of the probe nozzle is plugged and a vacuum of approximately 15" Hg is drawn and held. The metering dial is timed for a period of one minute and any movement during that period is noted. At the end of each test run, the same procedure is followed using the highest vacuum attained during the run. In each instance, the maximum acceptable leakage rate is 0.02 cfm.

#### 4.3.2 Pitot Tubes

Pitot tubes are leak checked according to procedures outlined in Method 2 (§3. Procedure, §3.1). The pitot tubes are subjected to leak checks prior to and after a test run. The impact opening of a pitot is blown through until a minimum pressure of 3" H<sub>2</sub>O registers on an inclined manometer. The impact opening is then closed off and a pressure reading observed. The reading must remain stable for a period of 15 seconds to be accepted. The same procedure is used to check the static pressure side of the pitot by applying suction to the static opening.

### 4.4 METHOD BLANKS

Method blanks (filters, absorbing solution, rinses, and digestion media) are handled and processed like actual samples. The blanks are weighed, evaporated, digested, and analyzed accordingly. Blanks reported greater than analytical detection levels are subtracted from sample results.

### 4.5 DATA REDUCTION AND HANDLING

Data are generally reported in English units, however, metric units are reported as requested by clients or regulatory agencies. The flow of data conforms to standard chain-of-custody procedures. Raw data generated from AQTS emission evaluation and compliance test programs are reduced using Lotus 1-2-3 or data acquisition systems. Calculations generally follow equations found in 40 CFR 60, Appendix A, Test Methods

or other air pollution and engineering references. Spreadsheet equations and calculations are frequently verified using scientific calculators. Isokinetic tests are manually recorded on data sheets and/or Lotus spreadsheets. Isokinetic sample rates are adjusted using a spreadsheet and/or slide rule nomograph.

**APPENDIX A**

## METHOD 5 PARTICULATE EQUATION FORMAT

Volume of dry gas sampled at standard conditions, 68 °F, 29.92 "Hg -  $V_{m_{std}}$  (scf):

$$V_{m_{std}} = 17.65 (V_m) (Y) \sqrt{\frac{P_b + \frac{A_H}{13.6}}{T_m + 460}}$$

Stack gas moisture condensed at standard conditions -  $V_{w_{std}}$  (scf):

$$V_{w_{std}} = 0.04707 (V_{lc})$$

Decimal fraction stack gas proportion of water by volume -  $B_{wo}$

$$B_{wo} = \frac{V_{w_{std}}}{V_{w_{std}} + V_{m_{std}}}$$

Stack gas dry molecular weight -  $MW_d$  (lb/lb-mole):

$$MW_d = 0.44 (\%CO_2) + 0.32 (\%O_2) + 0.28 (\%N_2 + \%CO)$$

Stack gas molecular weight -  $MW_s$  (lb/lb-mole):

$$MW_s = MW_d (1 - B_{wo}) + 18 (B_{wo})$$

Pressure of stack -  $P_s$  (in. Hg):

$$P_s = P_b + (P_{st}/13.6)$$

Stack gas velocity at stack conditions -  $V_s$  (fps):

$$V_s = 85.49 (C_p) (\sqrt{\Delta P})_{avg} \sqrt{\frac{T_s + 460}{(P_s) (MW_s)}}$$

Stack gas volumetric flow rate at standard conditions -  $Q_{s_s}$  (scfm):

$$Q_{s_s} = 60 (V_s) (A_s) \left(\frac{528}{T_s + 460}\right) \left(\frac{P_s}{29.92}\right)$$

Stack gas volumetric flow rate at actual conditions -  $Q_{s_a}$  (acfm):

$$Q_{s_a} = 60 (V_s) (A_s)$$

Stack gas volumetric flow at dry standard conditions -  $Q_{s_d}$  (dscfm):

$$Q_{s_d} = (60) (1 - B_{wo}) (V_s) (A_s) \left(\frac{528}{T_s + 460}\right) \left(\frac{P_s}{29.92}\right)$$

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Concentration of particulate matter in stack gas, dry basis, standard conditions - Cs  
(gr/dscf)

$$Cs = 15.432 \left( \frac{Mp}{Vm_{std}} \right)$$

Emission rate of particulate matter, dry basis, standard conditions - ER (lbs/hr)

$$ER = 0.00857 (Qsd) (Cs)$$

Isokinetic variation - Iso (%)

$$Iso = \frac{17.33 (Ts + 460) [0.04707 (Vlc) + Vm_{std}]}{\theta (Vs) (Ps) (Dn^2)}$$

Where:

As = Cross section area of stack (ft<sup>2</sup>)

Cp = Pitot tube coefficient

Dn = Diameter of nozzle (in.)

ΔH = Pressure differential across orifice (in. H<sub>2</sub>O)

Mp = Mass of particulate in grams

Pb = Barometric pressure (in. Hg)

Pst = Static pressure of stack (in. H<sub>2</sub>O)

Pstd = Standard pressure, 29.92 (in. H<sub>2</sub>O)

ΔP = Stack differential pressure (in. H<sub>2</sub>O)

Tm = Average temperature of dry gas meter (°F)

Ts = Average stack temperature (°F)

Tstd = Standard temperature, 68 (°F)

Vlc = Volume of liquid condensate (ml)

Vm = Volume of dry gas sample metered (ft<sup>3</sup>)

Y = Dry gas meter correction factor

θ = Sample duration (min.)

0.00857 = Conversion factor, gr to lbs and min. to hr.

0.04707 = Conversion factor, ml to ft<sup>3</sup>

0.264 = ratio of O<sub>2</sub> to N<sub>2</sub> in air, v/v

15.432 = Conversion factor, g/ft<sup>3</sup> to gr/ft<sup>3</sup>

17.65 = Conversion factor, standard temperature and pressure

17.33 = Isokinetic constant from factoring

18 = Molecular weight of water

85.49 = Pitot tube constant

000002

**APPENDIX B**

## FIELD DATA TEST RESULTS

CLIENT: OMYA, INC.  
FACILITY: FLORENCE, VT  
PROJECT: 001266  
UNIT: FLASH DRYER 3  
TEST DATE: September 27, 2000  
TEST RUN: 1-4

### TEST DATA SUMMARY

#### INPUT VALUES

Pitot Coefficient - Cp:	0.84	Average Delta P ("H2O):	1.002
Nozzle Diameter - Dn (in):	0.25	Average Delta H ("H2O):	2.043
Dry Gas Meter Cal. (Y):	1.004	Stack Temperature - Ts (°F):	287
Stack Area (ft²):	4.909	Meter Temperature - Tm (°F):	103
Barometric Press. - Pb ("Hg):	29.61	Average Square Root of Delta P:	0.993
Static Press. - Pst ("Hg):	-0.51	Mass of Particulate Collected - Mp - (g.):	0.0152
Sample Duration (min.):	96		
Volume of Gas Metered - Vm (ft³):	80.86		
Volume of Water Condensed - Vlc (g.):	332		
Oxygen - O2 (%):	18.5		
Carbon Dioxide - CO2 (%):	2		
Carbon Monoxide - CO (%):	0		
Nitrogen - N2 (%):	79.5		

#### OUTPUT VALUES

Dry Gas Volume (Standard) - Vmstd (dscf):	75.265
Volume of Water (Standard) - Vwstd (scf):	15.627
Stack Gas Water Proportion by Volume - Bwo:	0.172
Molecular Weight of Dry Stack Gas - MWd (lb/lb-mole):	29.06
Molecular Weight of Stack Gas - MWs (lb/lb-mole):	27.16
Pressure of Stack - Ps ("Hg.):	29.57
Velocity of Stack Gas - Vs (fps):	68.8
Dry Standard Volumetric Flow of Stack Gas - Qdscfm:	11721
Actual Volumetric Flow of Stack Gas - Qacfm:	20264
Test Isokinetic Sample Rate (%):	96.4
Particulate Concentration of Stack Gas - Cs (gr/dscf):	0.0031
Particulate Emission Rate - ER (lbs/hr):	0.31

000003

## FIELD DATA TEST RESULTS

CLIENT: OMYA, INC.  
 FACILITY: FLORENCE, VT  
 PROJECT: 001266  
 UNIT: FLASH DRYER 3  
 TEST DATE: September 27, 2000  
 TEST RUN: 1-5

### TEST DATA SUMMARY

#### INPUT VALUES

Pitot Coefficient - Cp:	0.84	Average Delta P (" H2O):	1.176
Nozzle Diameter - Dn (in):	0.25	Average Delta H ("H2O):	2.488
Dry Gas Meter Cal. (Y):	1.004	Stack Temperature - Ts (°F):	282.2
Stack Area (ft²):	4.909	Meter Temperature - Tm (°F):	97
Barometric Press. - Pb ("Hg):	29.42	Average Square Root of Delta P:	1.072
Static Press. - Pst ("Hg):	-0.51	Mass of Particulate Collected - Mp - (g.):	0.0137
Sample Duration (min.):	96		
Volume of Gas Metered - Vm (ft³):	87.457		
Volume of Water Condensed - Vlc (g.):	309.7		
Oxygen - O2 (%):	18.5		
Carbon Dioxide - CO2 (%):	2		
Carbon Monoxide - CO (%):	0		
Nitrogen - N2 (%):	79.5		

#### OUTPUT VALUES

Dry Gas Volume (Standard) - Vmstd (dscf):	81.754
Volume of Water (Standard) - Vwstd (scf):	14.578
Stack Gas Water Proportion by Volume - Bwo:	0.151
Molecular Weight of Dry Stack Gas - MWd (lb/lb-mole):	29.06
Molecular Weight of Stack Gas - MWs (lb/lb-mole):	27.39
Pressure of Stack - Ps ("Hg):	29.38
Velocity of Stack Gas - Vs (fps):	73.9
Dry Standard Volumetric Flow of Stack Gas - Qdscfm:	12909
Actual Volumetric Flow of Stack Gas - Qacfm:	21767
Test Isokinetic Sample Rate (%):	95.1
Particulate Concentration of Stack Gas - Cs (gr/dscf):	0.0026
Particulate Emission Rate - ER (lbs/hr):	0.29

000004

**APPENDIX C**

OMYA, INC., FLORENCE, VT

PROJECT: 001266

FLASH DRYER #3

PARTICULATE CONCENTRATION AND EMISSION DATA

SAMPLE ID	TEST RUN	GROSS SAMPLE MASS (g)	NET SAMPLE MASS (g)	AIR VOLUME SAMPLED (dscf)	EMISSION CONCENTRATIONS			VOLUMETRIC AIR FLOW (dscfm)	EMISSION RATE (lbs/hr)
					(gr/dscf)	(mg/dscm)	(lbs/dscf)		
C823/C824	1-4	0.0169	0.0152	75.265	0.0031	7.13	4.45E-007	11721	0.31
C825/C826	1-5	0.0154	0.0137	81.754	0.0026	5.92	3.69E-007	12909	0.29
C828	BLANK	0.0017							
VERAGES					0.0029	6.53	4.07E-007	12315	0.30

000005

**APPENDIX D**

# ISOKINETIC STACK CALCULATOR

(Revised 06/03/96)

## INPUT PARAMETERS

PITOT COEFFICIENT (Cp):	0.84
METER TEMPERATURE (°F):	115
STACK TEMPERATURE (°F):	305
AVERAGE DELTA P ("H2O):	1
MAXIMUM DELTA P ("H2O):	1.3
ESTIMATED MOISTURE (%):	20
METER BOX NUMBER:	1286-340
DELTA H @:	1.699

## NOZZLE DIAMETER (Dn) DATA

CALCULATED DIAMETER (in.):	0.2331
SELECTED SIZE (in.):	0.25

## CALCULATED PARAMETERS

K FACTOR =	2.0715
ISOKINETIC DELTA H ("H2O) =	2.07
MAX DELTA H ("H2O) =	2.69

## SAMPLING PARAMETERS

MIMIMUM SAMPLE VOLUME REQUIRED (dscf):	60
SAMPLE TIME REQUIRED (min):	82
SAMPLE RATE > 0.75 CFM	0.83
MAX SAMPLE RATE > 0.75 cfm:	0.94

PROJECT NUMBER:	001266
TEST RUN NUMBER:	1-4

000006

**METHOD 5**

CLIENT: OMYA, INC.  
 FACILITY: FLORENCE, VT  
 PROJECT: 001266  
 UNIT: FLASH DRYER 3  
 TEST DATE: September 27, 2000  
 TEST RUN: 1-4

Barometric Press. - Pb ("Hg): 29.61  
 Static Press. - Pst ("H2O): -0.51  
 Stack Press. - Ps ("Hg.): 29.57  
 Pitot Coefficient - Cp: 0.84  
 Nozzle Number: B-4  
 Nozzle Diameter - Dn (in): 0.250  
 Meter Box Number: 1286-340  
 Dry Gas Meter Cal. (Y): 1.004  
 Stack area (ft²): 4.909  
 Filter Number(s): 110-787

Impinger Volume (ml)	
Initial	Final
1>	585.7
2>	575.4
3>	480.9
Silica Gel (g)	
Initial	Final
4>	743.6
Total Volume>	
	332.0

Gas Composition	
O2	18.5
CO2	2
CO	0
N2	79.5

Vacuum Leak Check	
Leak Rate (cf.)	Vacuum ("Hg.)
Pre-test: 0.017	16
Post-test: 0.008	10

Pitot Leak Checks	
Pre-test:	Positive OK
	Negative OK
Post-test:	Positive OK
	Negative OK

Run Clock Time (24-Hr.): 01:08-14:48  
 Sample Duration (min.): 96  
 Number of Sample Points: 24

SAMPLE POINT	CLOCK TIME (24 Hr)	GAS METER READING (cf)	DELTA P (In. H2O)	DESRED DELTA H (In. H2O)	ACTUAL DELTA H (In. H2O)	STACK	TEMPERATURES (°F)		SQUARE ROOT DELTA P	PERCENT ISO
							INLET	OUTLET		
N1	01:08 PM	7.614	0.75	1.55	1.55	280	102	82	0.866	101.8
2	01:12 PM	10.57	0.78	1.62	1.62	285	117	83	0.883	97.9
3	01:16 PM	13.5	0.84	1.74	1.74	285	114	85	0.917	100.5
4	01:20 PM	16.62	1.2	2.49	2.49	296	119	86	1.095	100.1
5	01:24 PM	20.32	1.4	2.9	2.9	305	123	87	1.183	98.7
6	01:28 PM	24.25	1.5	3.11	3.11	287	124	88	1.225	99.3
7	01:32 PM	28.4	1.1	2.28	2.28	287	122	89	1.049	99.4
8	01:36 PM	31.96	0.88	1.82	1.82	285	119	89	0.938	99
9	01:40 PM	35.13	0.9	1.86	1.86	283	119	89	0.949	99
10	01:44 PM	38.34	0.72	1.49	1.49	278	117	89	0.849	98.3
11	01:48 PM	41.2	0.52	1.08	1.08	276	115	89	0.721	99.1
12	01:52 PM	43.65	0.54	1.12	1.12	275	116	89	0.735	101.8
END	01:56 PM	46.219								
B1	02:00 PM	46.219	1.2	2.49	2.49	291	112	87	1.095	97.1
2	02:04 PM	49.8	1.1	2.28	2.28	290	120	87	1.049	100
3	02:08 PM	53.36	1.1	2.28	2.28	292	122	87	1.049	99.1
4	02:12 PM	56.89	1.1	2.28	2.49	285	122	88	1.049	99.4
5	02:16 PM	60.45	1.2	2.49	2.49	295	122	88	1.095	101.3
6	02:20 PM	64.21	1.2	2.49	2.49	293	121	88	1.095	100.7
7	02:24 PM	67.95	1.2	2.49	2.49	293	121	88	1.095	100.9
8	02:28 PM	71.7	1.2	2.49	2.28	286	121	89	1.095	100.3
9	02:32 PM	75.45	1.1	2.28	1.91	290	121	89	1.049	100.7
10	02:36 PM	79.05	0.92	1.91	1.76	286	119	90	0.959	99.5
11	02:40 PM	82.31	0.85	1.76	1.55	284	116	90	0.922	100.1
12	02:44 PM	85.46	0.74	1.53	1.46	280	115	90	0.86	102.5
END	02:48 PM	88.474								

000007

# ISOKINETIC STACK CALCULATOR

(Revised 06/03/96)

## INPUT PARAMETERS

PITOT COEFFICIENT (Cp):	0.84
METER TEMPERATURE (°F):	100
STACK TEMPERATURE (°F):	300
AVERAGE DELTA P ("H2O):	1
MAXIMUM DELTA P ("H2O):	1.3
ESTIMATED MOISTURE (%):	18
METER BOX NUMBER:	1286-340
DELTA H @:	1.699

## NOZZLE DIAMETER (Dn) DATA

CALCULATED DIAMETER (in.):	0.2334
SELECTED SIZE (in.):	0.25

## CALCULATED PARAMETERS

K FACTOR =	2.1161
ISOKINETIC DELTA H ("H2O) =	2.12
MAX DELTA H ("H2O) =	2.75

## SAMPLING PARAMETERS

MIMIMUM SAMPLE VOLUME REQUIRED (dscf):	60
SAMPLE TIME REQUIRED (min):	81
SAMPLE RATE > 0.75 CFM	0.84
MAX SAMPLE RATE > 0.75 cfm:	0.95

PROJECT NUMBER:	001266
TEST RUN NUMBER:	1-5

000008

APPENDIX E

**METHOD 5**

CLIENT: OMYA, INC.  
 FACILITY: FLORENCE, VT  
 PROJECT: 001266  
 UNIT: FLASH DRYER 3  
 TEST DATE: September 27, 2000  
 TEST RUN: 1-5

Barometric Press. - Pb ("Hg): 29.42  
 Static Press. - Pst ("H2O): -0.51  
 Stack Press. - Ps ("Hg.): 29.38  
 Pitot Coefficient - Cp: 0.84  
 Nozzle Number: B-4  
 Nozzle Diameter - Dn (in): 0.250  
 Meter Box Number: 1286-340  
 Dry Gas Meter Cal. (Y): 1.004  
 Stack area (ft<sup>2</sup>): 4.909  
 Filter Number(s): 110-788

Run Clock Time (24-Hr.): 16:15-17:58  
 Sample Duration (min.): 96  
 Number of Sample Points: 24

Impinger Volume (ml)	
Initial	Final
1> 576.5	813
2> 586.5	631.3
3> 516.2	523.7
Silica Gel (g)	
Initial	Final
4> 675.9	696.8
Total Volume>	309.7

Gas Composition	
O2	18.5
CO2	2
CO	0
N2	79.5

Vacuum Leak Check		
	Leak Rate (cf)	Vacuum ("Hg.)
Pre-test:	0.006	15
Post-test:	0.003	10

Pitot-Leak Checks	
Pre-test:	OK
Negative	OK
Post-test:	OK
Negative	OK

SAMPLE POINT	CLOCK TIME (24 Hr)	GAS METER READING (cf)	DELTA P (In. H2O)	DESIRED DELTA H (In. H2O)	ACTUAL DELTA H (In. H2O)	STACK TEMPERATURES (°F)	DRY GAS METER		SQUARE ROOT DELTA P	PERCENT ISO
							INLET	OUTLET		
E1	04:15 PM	89.928	1.2	2.54	2.54	280	84	73	1.095	101.1
2	04:19 PM	93.63	1.8	3.81	3.81	291	99	74	1.342	98.6
3	04:23 PM	98.07	1.8	3.81	3.81	281	105	76	1.342	98.1
4	04:27 PM	102.55	1.8	3.81	3.81	290	108	78	1.342	97.5
5	04:31 PM	107	1.5	3.17	3.17	282	109	80	1.225	98.2
6	04:35 PM	111.13	1.3	2.75	2.75	283	110	82	1.14	99.9
7	04:39 PM	115.05	1.1	2.33	2.33	285	110	83	1.049	99.1
8	04:43 PM	118.63	0.98	2.07	2.07	289	111	84	0.99	97.7
9	04:47 PM	121.96	0.92	1.95	1.95	294	111	85	0.959	98.6
10	04:51 PM	125.21	0.88	1.86	1.86	283	111	85	0.938	97.3
11	04:55 PM	128.37	0.74	1.57	1.57	280	110	86	0.86	96.1
12	04:59 PM	131.24	0.62	1.31	1.31	276	109	86	0.787	98.2
END	05:03 PM	133.93								
B1	05:10 PM	133.93	1.2	2.54	2.54	279	108	85	1.095	104.3
2	05:14 PM	137.88	1.5	3.17	3.17	284	115	86	1.2	100.8
3	05:18 PM	142.16	1.5	3.17	3.17	282	115	87		96.6
4	05:22 PM	146.27	1.5	3.17	3.17	280	114	88		96.3
5	05:26 PM	150.37	1.2	2.54	2.54	286	113	89		98.7
6	05:30 PM	154.12	1.3	2.75	2.75	279	113	89		97.7
7	05:34 PM	158	1	2.12	2.12	278	112	89		97.7
8	05:38 PM	161.43	1	2.12	2.12	280	112			97.7
9	05:43 PM	164.79	1	2.12	2.12	282	112			97.7
10	05:46 PM	168.28	0.94	1.99	1.99	279	112			97.7
11	05:50 PM	171.53	0.82	1.74	1.74	276				97.7
12	05:54 PM	174.64	0.62	1.31	1.31	273				97.7
END	05:58 PM	177.385								97.7

000009

**APPENDIX E**

## FILTER TARE WEIGHT LOG

CLIENT:	OMYA, Inc.
PROJECT:	001266
FILTER TYPE:	GFF
SIZE:	110 mm

Filter Number	Date/Time	Weight (g)			
110 786					
110 787	08/21/00 08:00	0.5780	08/23/00 09:00	0.5779	
110 788	08/21/00 08:00	0.5816	08/23/00 09:00	0.5817	
110 789	08/21/00 08:00	0.5768	08/23/00 09:00	0.5769	
110 790	08/21/00 08:00	0.5838	08/23/00 09:00	0.5838	
110 791	08/21/00 08:00	0.5822	08/23/00 09:00	0.5822	
110 792	08/21/00 08:00	0.5853	08/23/00 09:00	0.5853	
110 793	08/21/00 08:00	0.5823	08/23/00 09:00	0.5824	
110 794	08/21/00 08:00	0.5836	08/23/00 09:00	0.5836	
110 795	08/21/00 08:00	0.5863	08/23/00 09:00	0.5862	
110 796	08/21/00 08:00	0.5883	08/23/00 09:00	0.5884	
110 797	08/21/00 08:00	0.5835	08/23/00 09:00	0.5836	
110 798	08/21/00 08:00	0.5836	08/23/00 09:00	0.5836	
110 799	08/21/00 08:00	0.5832	08/23/00 09:00	0.5832	
110 800					
110 801					
110 802					
110 803					
110 804					
110 805					

000010



## BEAKER TARE WEIGHT LOG SHEET

Client: OMYA, Inc.  
 Facility: Florence, VT  
 Project: 001266 - FD#3

Beaker Number	Date/Time				
	Tare Weight (g.)				
25/3	10/03/00 - 07:00	10/07/00 - 14:30	10/08/00 - 12:50		
	105.7073	105.7066	105.7065		
25/7	10/03/00 - 07:00	10/07/00 - 14:30	10/08/00 - 12:50		
	99.9606	99.9596	99.9594		
25/15	10/03/00 - 07:00	10/07/00 - 14:30	10/08/00 - 12:50	10/09/00 - 08:45	
	106.1155	106.1140	106.1130	106.1128	

## SAMPLE WEIGHT LOG SHEET

Client: OMYA, Inc.  
 Facility: Florence, VT  
 Project: 001266 - FD#3

Sample Number	Identification	Date/Time			
	Tare Weight (g.)	Gross Weight (g.)			
C823	GFF 110-787	10/03/00 - 07:00	10/19/00 - 06:30	10/19/00 - 17:45	10/20/00 - 07:00
	0.5779	0.6038	0.5795	0.5788	0.5789
C824	Beaker 25/3	10/20/00 - 07:00	10/20/00 - 19:00	10/21/00 - 08:30	
	105.7065	105.7236	105.7222	105.7224	
C825	GFF 110-788	10/03/00 - 07:00	10/19/00 - 06:30	10/19/00 - 17:45	10/20/00 - 07:00
	0.5817	0.5833	0.5818	0.5807	0.5807
C826	Beaker 25/7	10/20/00 - 07:00	10/20/00 - 19:00	10/21/00 - 08:30	
	99.9594	99.9771	99.9758	99.9758	
C827	GFF 10-793	10/03/00 - 07:00			
	0.5824	0.5823			
C828	Beaker 25/15	10/20/00 - 07:00	10/20/00 - 19:00	10/21/00 - 08:30	
	106.1128	106.1153	106.1143	106.1145	

**PARTICULATE LAB ANALYSIS  
SUMMARY SHEET**

Client: OMYA, Inc. Project Number: 001266 Test/Run: 1-4

**Sample Identification**

Number	Description
C823	GFF 110-787
C824	Front half acetone wash - 225 ml A/P
C828	Acetone blank - 225 ml A/P

**Acetone Blank Background Data**

Manufacturer: Anachemia Lot/Batch: 990413 Density: 0.7857 g/ml  
 $C_a$  = Acetone blank residue concentration (mg/mg)  
 $m_a$  = Mass of acetone residue after evaporation (mg)  
 $V_a$  = Volume of acetone blank (ml)  
 $\rho_a$  = Density of acetone (mg/ml)

$$C_a = m_a / (V_a \rho_a) = ( 1.7 ) / ( 225 ) ( 0.0007857 ) = \underline{9.616} \text{ mg/mg}$$

**Front Half Acetone Wash Data**

$W_a$  = Weight of acetone residue in wash (mg)  
 $V_{aw}$  = Volume of acetone wash (ml)

$$W_a = C_a V_a \rho_a = ( 9.616 ) ( 225 ) ( 0.0007857 ) = \underline{1.7} \text{ mg}$$

**Acetone Wash Data**

Beaker Number: 25/3

Gross Weight (g): 105.7224  
Tare Weight (g): 105.7065  
Blank Weight (g): 0.0017  
Net Weight (g): 0.0142

**Filter Data**

Filter Number: 110-787

Gross Weight (g): 0.5789  
Tare Weight (g): 0.5779  
Net Weight (g): 0.0010

**Particulate Weight Summary**

Weight of particulate in front half wash (g): 0.0142  
Weight of particulate on filter (g): 0.0010  
Total weight of particulate catch (g): 0.0152

000014

**PARTICULATE LAB ANALYSIS  
SUMMARY SHEET**

Client: OMYA, Inc. Project Number: 001266 Test/Run: 1-5

**Sample Identification**

Number	Description
C825	GFF 110-788
C826	Front half acetone wash - 225 ml A/P
C828	Acetone blank - 225 ml A/P

**Acetone Blank Background Data**

Manufacturer: Anachemia Lot/Batch: 990413 Density: 0.7857 g/ml

$C_a$  = Acetone blank residue concentration (mg/mg)  
 $m_a$  = Mass of acetone residue after evaporation (mg)  
 $V_a$  = Volume of acetone blank (ml)  
 $\rho_a$  = Density of acetone (mg/ml)

$$C_a = m_a / (V_a \rho_a) = ( 1.7 ) / ( 225 ) ( 0.0007857 ) = \underline{9.616} \text{ mg/mg}$$

**Front Half Acetone Wash Data**

$W_a$  = Weight of acetone residue in wash (mg)  
 $V_{aw}$  = Volume of acetone wash (ml)

$$W_a = C_a V_a \rho_a = ( 9.616 ) ( 225 ) ( 0.0007857 ) = \underline{1.7} \text{ mg}$$

**Acetone Wash Data**

Beaker Number: <u>25/7</u>	Gross Weight (g):	99.9758
	Tare Weight (g):	99.9594
	Blank Weight (g):	0.0017
	Net Weight (g):	0.0147

**Filter Data**

Filter Number: <u>110-788</u>	Gross Weight (g):	0.5807
	Tare Weight (g):	0.5817
	Net Weight (g):	-0.0010

**Particulate Weight Summary**

Weight of particulate in front half wash (g):	0.0147
Weight of particulate on filter (g):	-0.0010
Total weight of particulate catch (g):	0.0137

**000015**

**APPENDIX F**

REQUIREMENTS FOR ASSIGNING A BASELINE COEFFICIENT VALUE  
OF 0.84 TO AN "S" TYPE PITOT TUBE

PITOT # 36-1    DATE 8/9/00    OBSERVATIONS BY (S)

- 1.) All construction criteria for an isolated "S" type pitot are within given tolerances prescribed in Federal Register, Vol. 42, No. 160. Thursday, August 18, 1977.

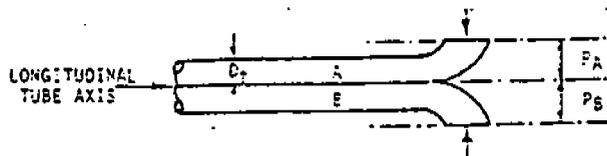
REQUIRED MEASUREMENTS

- a. External tubing diameter,  $D_t$ , 0.23 in.  $< D_t < 0.38$  in.  
 b. Base to plane opening Distance,  $P_A$  and  $P_B$ , 0.40 in.  $< P_A=P_B < 0.60$  in.

$D_t = 0.375$

$P_A = 0.50$

$P_B = 0.50$



- 2.) All assembly criteria to prevent aerodynamic interference for a sampling arrangement of an "S" type pitot, nozzle and thermocouple, are within given tolerances prescribed in Federal Register, Vol. 42, No. 160. Thursday, August 18, 1977.

REQUIRED MEASUREMENTS

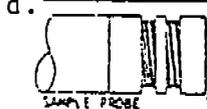
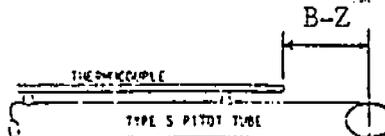
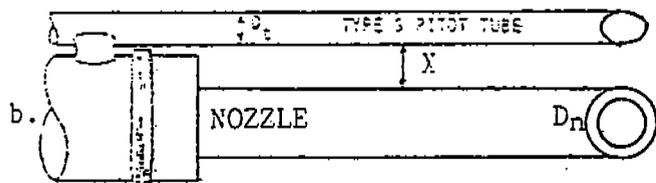
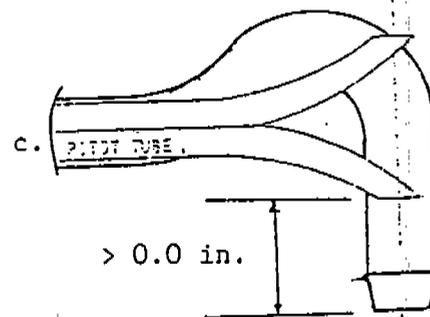
- a. External tubing diameter. See 1.a. above  
 b. Pitot / nozzle separation,  $X$ ,  $X \geq 0.75$  in. for nozzle diameter,  $D_n = 0.50$  in.  
 c. Plane of impact side of pitot in relation to plane of nozzle opening.  
 d. Thermocouple placement,  $Z$ ,  $A-Z \geq 0.75$  in.,  $A-W \geq 3.0$  in.,  $B-Z \geq 2.0$  in.  
 e. Pitot / probe sheath distance,  $Y$ ,  $Y \geq 3.0$  in.

$D_n = 0.25$

$X = 0.75$

$Z = 1.00$

$Y = 3.5$



OR



e.

## Stack Temperature Sensor Calibration

Date: 01/12/2000

Barometric Pressure: 29.82

Ambient Temperature: 61°F

Calibrated by: John Jasko

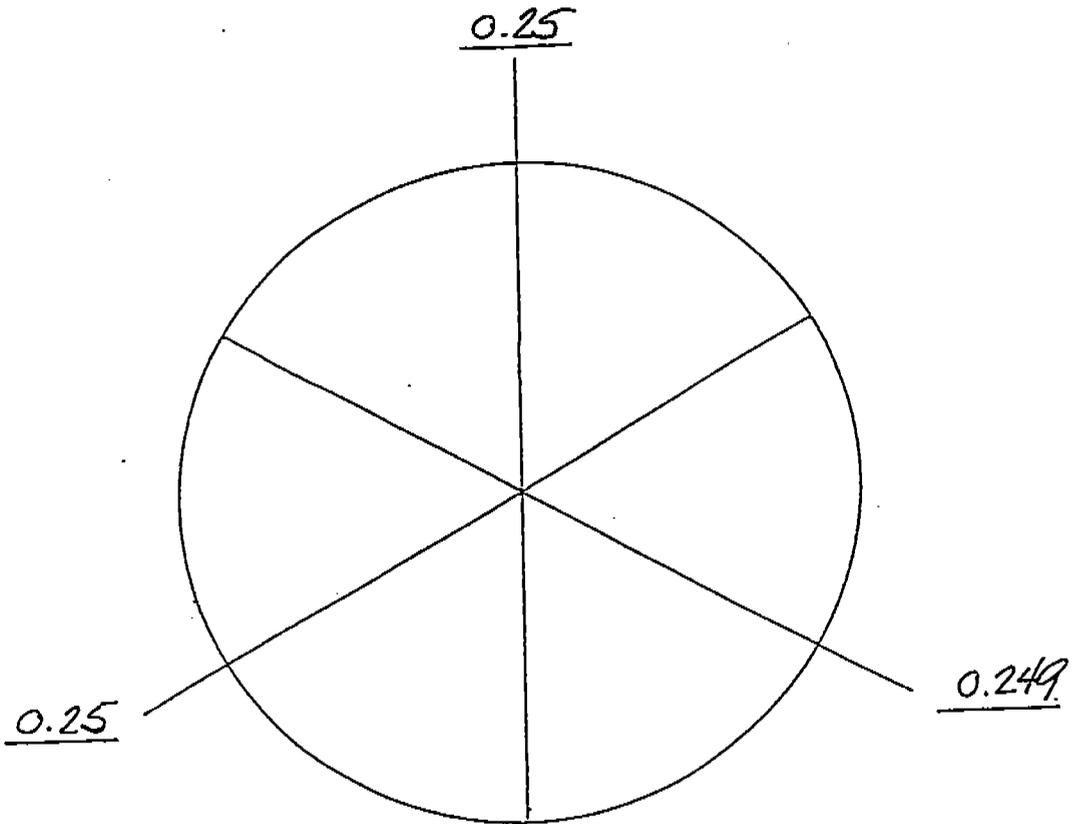
Thermocouple Id # : TC-36-1		Reference Thermometer Temperature (°F)	Thermocouple Potentiometer Temperature (°F)	Temperature Difference (%)
Reference Point	Source			
1	Ice Water	33	33	0.00
2	Warm Water	116	117	-0.17
3	Hot Oil	389	392	-0.35
4	Hot Oil	242	244	-0.28
Thermocouple Id # : TC-36-2		Reference Thermometer Temperature (°F)	Thermocouple Potentiometer Temperature (°F)	Temperature Difference (%)
Reference Point	Source			
1	Ice Water	33	33	0.00
2	Warm Water	116	116	0.00
3	Hot Oil	391	389	0.24
4	Hot Oil	245	243	0.28

000017

NOZZLE CALIBRATION DATA FORM

Date: 8/9/2000

Calibrated by: (A)



Nozzle Identification Number	Nozzle Diameter <sup>a</sup>			$\Delta D^b$ mm (in.)	$D_{avg}^c$
	$D_1$ mm (in.)	$D_2$ mm (in.)	$D_3$ mm (in.)		
B-4	0.250	0.250	0.249	0.001	0.250

Where:  
a = nozzle diameters    b = maximum difference    c = average diameter

000018

**METER BOX CALIBRATION  
(ANNUAL)**

DATE: 04-Jan-00  
CALIBRATED BY: John Jasko

METER BOX NUMBER: 1286-340  
NEXT CAL DUE: 05-Jul-00

BAROMETRIC PRESSURE (in. Hg)	ORIFICE MANOMETER SETTING (in. H <sub>2</sub> O)	WET TEST METER VOLUME (cf)	DRY GAS METER VOLUME		WET TEST METER (°F)	TEMPERATURES			TIME (min)	Y <sub>i</sub>	DELTA H@	
			INITIAL (cf)	FINAL (cf)		WET TEST METER (°F)	DRY GAS METER INLET (°F)	DRY GAS METER OUTLET (°F)				AVERAGE (°F)
29.45	0.5	5	60.587	65.780	60.5	95	67	82.8	12.23	1.003	1.607	
29.45	1.0	5	66.822	72.037	60.5	95	74	85.0	8.81	1.001	1.661	
29.45	1.5	10	72.764	83.263	60.5	100	75	90.3	14.70	1.003	1.718	
29.45	2.0	10	84.585	95.141	60.5	109	81	94.5	12.86	1.004	1.740	
29.45	3.0	10	97.002	107.568	60.5	111	83	97.3	10.49	1.006	1.728	
29.45	4.0	10	109.248	119.825	60.5	114	85	99.3	9.13	1.006	1.739	
										AVERAGE	1.004	1.699

TOLERANCES FROM AVERAGE FOR Y<sub>i</sub> AND DELTA H@ ARE <0.02 AND 0.20, RESPECTIVELY

Y <sub>i</sub>	Y <sub>i</sub> DIFF	DELTA H@	DELTA H@ DIFF
1.003	-0.001	1.607	-0.092
1.001	-0.003	1.661	-0.038
1.003	-0.001	1.718	0.019
1.004	0.000	1.740	0.041
1.006	0.002	1.728	0.029
1.006	0.002	1.739	0.040

000013

**METER BOX CALIBRATION  
(POST-TEST)**

PROJECT: 001266  
 DATE: 25-Oct-00  
 CALIBRATED BY: Roland Tremble

METER BOX NUMBER: 1286-340  
 PRETEST CAL Y: 1.004

BAROMETRIC PRESSURE (in. Hg)	ORIFICE MANOMETER SETTING (in. H <sub>2</sub> O)	MAXIMUM VACUUM (in. H <sub>2</sub> O)	WET TEST METER VOLUME (cf)	DRY GAS METER VOLUME (cf)		WET TEST METER (°F)	TEMPERATURES (°F)			TIME (min)	Yr
				INITIAL	FINAL		INLET	OUTLET	AVERAGE		
30.06	2.20	4.0	10	306.253	316.512	59.5	79	65	77.5	12.17	1.003
30.06	2.20	4.0	10	316.512	326.881	59.5	96	70	83.8	12.13	1.004
30.06	2.20	4.0	10	326.881	337.301	59.5	90	75	85.3	12.20	1.002
										AVERAGE	1.003

ACCEPTABLE VARIATION IN CALIBRATION  
 (Must be less than 5% of Pretest Meter Calibration)

Difference from Pretest Calibration = -0.1 % >>>> ACCEPTABLE

000020