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AP42 Section: 11.1

Reference Number: 72

Title: Results Of The June 21, 1993 NSPS Particulate And Opacity Compliance Tests On The T. A. Schifsky & Sons Stationary Asphalt Plant Located In North St. Paul, Minnesota, Interpoll Laboratories, Inc., Circle Pines, MN,

July 22, 1993.

AP-42 Section	11.1
Reference	
Report Sect.	4
Reference	72

Interpoll Laboratories, Inc.
 4500 Ball Road N.E.
 Circle Pines, Minnesota 55014-1819

TEL: (612) 786-6020
 FAX: (612) 786-7854



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**RESULTS OF THE JUNE 21, 1993 NSPS
 PARTICULATE AND OPACITY COMPLIANCE TESTS
 CONDUCTED ON THE STATIONARY
 ASPHALT PLANT LOCATED IN
 NORTH ST. PAUL, MINNESOTA**

Submitted to:

T.A. SCHIFSKY & SONS
 2370 East Highway 36
 North St. Paul, Minnesota 55109

Attention:

Tom Schifsky, Jr.

Approved by:

Daniel Despen
 Manager
 Stationary Source Testing Department

Report Number 3-9190
 July 22, 1993
 SP/slp

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ABBREVIATIONS

ACFM	actual cubic feet per minute
cc (ml)	cubic centimeter (milliliter)
DSCFM	dry standard cubic foot of dry gas per minute
DSML	dry standard milliliter
DEG-F (°F)	degrees Fahrenheit
DIA.	diameter
FP	finished product for plant
FT/SEC	feet per second
g	gram
GPM	gallons per minute
GR/ACF	grains per actual cubic foot
GR/DSCF	grains per dry standard cubic foot
g/dscm	grams per dry standard cubic meter
HP	horsepower
HRS	hours
IN.	inches
IN.HG.	inches of mercury
IN.WC.	inches of water
LB	pound
LB/DSCF	pounds per dry standard cubic foot
LB/HR	pounds per hour
LB/10 ⁶ BTU	pounds per million British Thermal Units heat input
LB/MMBTU	pounds per million British Thermal Units heat input
LTPD	long tons per day
MW	megawatt
mg/Nm ³	milligrams per dry standard cubic meter
ug/Nm ³	micrograms per dry standard cubic meter
microns (um)	micrometer
MIN.	minutes
ng	nanograms
ohm-cm	ohm-centimeter
PM	particulate matter
PPH	pounds per hour
PPM	parts per million
ppmC	parts per million carbon
ppm,d	parts per million, dry
ppm,w	parts per million, wet
ppt	parts per trillion
PSI	pounds per square inch
SQ.FT.	square feet
TPD	tons per day
ug	micrograms
v/v	percent by volume
w/w	percent by weight
<	≤ (when following a number)

Standard conditions are defined as 68°F (20°C) and 29.92 IN. of mercury pressure.

1 INTRODUCTION

On June 21, 1993 Interpoll Laboratories Personnel conducted a NSPS Particulate and Visible Emission Compliance Test on the T.A. Schifsky and Sons Stationary Asphalt Plant located in North St. Paul, Minnesota. Duane Van Hoever, Jeff Bergstrom, and Rick Eidem performed the on-site portion of the test. *Coordination between testing activities and plant operation* was provided by Tom Schifsky Jr. of T.A. Schifsky and Sons. The test was not witnessed by a member of the Minnesota Pollution Control Agency.

The unit tested is a Stansteel Model 628 ^{Batch plant #} stationary batch asphalt plant which has a rated capacity of 140 TPH with 5% moisture. The particulate emissions are controlled by a Stansteel Model 384 Baghouse. ✓ The unit was tested processing 100% virgin aggregate. The plant was fired with natural gas and operated under normal conditions.

Particulate evaluations were performed in accordance with EPA Methods 1 - 5, and 9, CFR Title 40, Part 60, Appendix A (revised July 1, 1992). A preliminary determination of the gas linear velocity profile was made before the first particulate determination to allow selection of the appropriate nozzle diameter required for isokinetic sample withdrawal. An Interpoll Labs sampling train which meets or exceeds specifications in the above-cited reference was used to extract particulate samples by means of a heated glass-lined probe. Wet catch samples were collected in the back half of the Method 5 sampling train and analyzed as per Minnesota Rules part 7005.0500.

An integrated flue gas sample was extracted simultaneously with each particulate sample using a specially designed gas sampling system. Integrated flue gas samples were collected in 44-liter Tedlar bags housed in a protective aluminum container. After sampling was complete, the bags were returned to the laboratory for Orsat analysis. Prior to sampling, the Tedlar bags are leak checked at 15 IN.HG. vacuum with an in-line

rotameter. Bags with any detectable inleakage are discarded.

Testing was conducted from 2 test ports oriented at 90 degrees on the stack. The test ports are located 5 diameters downstream and 1 diameters upstream of the nearest flow disturbances. A 24-point traverse was used to collect representative particulate samples. Each traverse point was sampled 2.5 minutes to give a total sampling time of 60 minutes per run. Visible emissions determinations were performed by Rick Eidem, an EPA-certified observer.

The important results of the test are summarized in Section 2. Detailed results are presented in Section 3. Field data and all other supporting information are presented in the appendices.

2 SUMMARY AND DISCUSSION

The results of the particulate emission test are summarized in Tables 1 - 2. The results are summarized in the table below.

Process	Concentration (GR/DSCF)	Emission Rate (LB/HR)
Virgin (Dry + Organic Wet Catch)	0.0125	1.65
Virgin (Dry Catch Only)	0.00796	1.05

Opacity averaged 0 percent.

No difficulties were encountered in the field or in the laboratory evaluation of the samples. On the basis of these facts and a complete review of the data and results, it is our opinion that the results reported herein are accurate and closely reflect the actual values which existed at the time the test was performed.

Table 1. Summary of the Results of the June 21, 1993 NSPS Particulate Emission Compliance Test on the TA Schiffsky & Sons Stationary Asphalt Plant Located in St. Paul, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	06-21-93	06-21-93	06-21-93
Time runs were done (HRS)	930/1032	1159/1255	1356/1457
Process rate (TON/HR)			
recycle	0.0	0.0	0.0
aggregate	143.0	148.0	147.0
asphalt	7.5	7.7	7.5
total	150.5	155.7	154.5
Volumetric flow (ACFM)	31428	31742	31014
actual	15720	15396	14992
standard			
Gas temperature (DEG-F)	245	251	258
Moisture content (%V/V)	31.00	32.50	32.12
Gas composition (%V/V, dry)			
carbon dioxide	4.40	4.50	4.60
oxygen	13.40	13.30	13.10
nitrogen	82.20	82.20	82.30
Isokinetic variation (%)	105.7	100.7	99.0
Part. emission rate (LB/HR)	1.92	1.61	1.41
Particulate concentration (GR/ACF)			
actual	.00713	.00592	.00531
standard (GR/DSCF)	.0143	.0122	.0110

Note: Dry + Organic Wet Catch

* Federal regulations restrict particulate emissions from portable asphalt plants to .04 GR/DSCF, CFR Title 40, Part 60, Subpart I.

Table 2. Summary of the Results of the June 21, 1993 NSPS Particulate Emission Compliance Test on the TA Schiffsky & Sons Stationary Asphalt Plant Located in St. Paul, Minnesota.

ITEM	Run 1	Run 2	Run 3
Date of test	06-21-93	06-21-93	06-21-93
Time runs were done (HRS)	930/1032	1159/1255	1356/1457
Process rate (TON/HR)			
recycle	0.0	0.0	0.0
aggregate	143.0	148.0	147.0
asphalt	7.5	7.7	7.5
total	150.5	155.7	154.5
Volumetric flow (ACFM)	31428	31742	31014
actual			
standard (DSCFM)	15720	15396	14992
Gas temperature (DEG-F)	245	251	258
Moisture content (%V/V)	31.00	32.50	32.12
Gas composition (%V/V, dry)			
carbon dioxide	4.40	4.50	4.60
oxygen	13.40	13.30	13.10
nitrogen	82.20	82.20	82.30
Isokinetic variation (%)	105.7	100.7	99.0
Part. emission rate (LB/HR)	1.03	1.06	1.05
Particulate concentration (GR/ACF)			
actual	.00382	.00390	.00396
standard (GR/DSCF)	.00765	.00804	.00819

Note: Dry Catch Only

* Federal regulations restrict particulate emissions from portable asphalt plants to .04 GR/DSCF, CFR Title 40, Part 60, Subpart I.

3 RESULTS

The results of all field and laboratory evaluations are presented in this section. Gas composition (Orsat and moisture) are presented first followed by the computer printout of the particulate and opacity results. Preliminary measurements including test port locations are given in the appendices.

The results have been calculated on a personal computer using programs written in Extended BASIC specifically for source testing calculations. EPA-published equations have been used as the basis of the calculation techniques in these programs. The particulate emission rate has been calculated using the product of the concentration times flow method.

3.1 Results of Orsat & Moisture Determinations

Test No. 1
 Asphalt Plant Stack

Results of Orsat & Moisture Analyses-----Methods 3 & 4(%v/v)

Date of run	Run 1 06-21-93	Run 2 06-21-93	Run 3 06-21-93
-------------	-------------------	-------------------	-------------------

Dry basis (orsat)

carbon dioxide.....	4.40	4.50	4.60 ✓
oxygen.....	13.40	13.30	13.10 ✓
nitrogen.....	82.20	82.20	82.30 ✓

Wet basis (orsat)

carbon dioxide.....	3.04	3.04	3.12
oxygen.....	9.25	8.98	8.89
nitrogen.....	56.72	55.48	55.87
water vapor.....	31.00	32.50	32.12
Dry molecular weight.....	29.24	29.25	29.26
Wet molecular weight.....	25.76	25.59	25.64
Specific gravity.....	0.890	0.884	0.886
Water mass flow.....(LB/HR)	19810	20797	19895

FO	1.705	1.689	1.696
----	-------	-------	-------

3.2 Results of Particulate Loading Determinations

Test No. 1
 Asphalt Plant Stack

Results of Particulate Loading Determinations-----Method 5

	Run 1	Run 2	Run 3
Date of run	06-21-93	06-21-93	06-21-93 ✓
Time run start/end.....(HRS)	930/1032	1159/1255	1356/1457
Static pressure.....(IN.WC)	-0.78	-0.78	-0.78 ✓
Cross sectional area (SQ.FT)	7.77	7.77	7.77 ✓
Pitot tube coefficient.....	.840	.840	.840 ✓
Water in sample gas			
condenser.....(ML)	0.0	0.0	0.0
impingers.....(GRAMS)	381.0	381.0	363.0 ✓
desiccant.....(GRAMS)	19.0	19.0	13.0 ✓
total.....(GRAMS)	400.0	400.0	376.0
Total particulate material..			
.....collected(grams)	0.0388	0.0310	0.0267
Gas meter coefficient.....	0.9979	0.9979	0.9979
Barometric pressure..(IN.HG)	29.01	29.01	29.01 ✓
Avg. orif.pres.drop..(IN.WC)	1.70	1.49	1.38
Avg. gas meter temp..(DEF-F)	92.2	98.2	103.4 ✓
Volume through gas meter....			
at meter conditions...(CF)	45.20	42.65	41.20 ✓
standard conditions.(DSCF)	41.98	39.17	37.47
Total sampling time....(MIN)	60.00	60.00	60.00 ✓
Nozzle diameter.....(IN)	.245	.245	.245 ✓
Avg.stack gas temp ..(DEG-F)	245	251	258 ✓
Volumetric flow rate.....			
actual.....(ACFM)	31428	31742	31014
dry standard.....(DSCFM)	15720	15396	14992
Isokinetic variation.....(%)	105.7	100.7	99.0
Particulate concentration...			
actual.....(GR/ACF)	0.00713	0.00592	0.00531
dry standard.....(GR/DSCF)	0.01426	0.01221	0.01099
Particle mass rate...(LB/HR)	1.922	1.612	1.413

3.3 Results of Opacity Observations

Test No. 1
Asphalt Plant Stack

Results of Opacity Observations ----- EPA Method 9

PERCENT OPACITY	OPTICAL DENSITY	RELATIVE FREQUENCY (%)
0	0.0000	100.00
5	0.0223	0.00
10	0.0458	0.00
15	0.0706	0.00
20	0.0969	0.00
25	0.1249	0.00
30	0.1549	0.00
35	0.1871	0.00
40	0.2219	0.00
45	0.2596	0.00
50	0.3010	0.00
55	0.3468	0.00
60	0.3979	0.00
65	0.4559	0.00
70	0.5229	0.00
75	0.6021	0.00
80	0.6690	0.00
85	0.8239	0.00
90	1.0000	0.00
95	1.3010	0.00
99	2.0000	0.00
Avg Opac 0.00	Avg OD 0.0000	Time average

Observer: Richard J. Eidem
Cert. Date: 03-30-93
Date of Observation: 06-21-93
Time of Observation: 0930-1030

4 RESULTS OF AGGREGATE ANALYSES

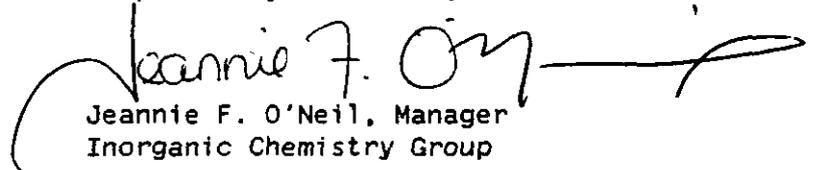
INTERPOLL LABORATORIES, INC.
(612)786-6020

T.A. Schifsky & Sons
Laboratory Log No. 9190

Results of Moisture Analysis¹

<u>Log No.</u>	<u>Test/Run</u>	<u>Sample Type</u>	<u>% Moisture</u>
9190-16	Test 1 Run 1	Virgin Aggregate	5.53
9190-17	Test 1 Run 2	Virgin Aggregate	5.28
9190-18	Test 1 Run 3	Virgin Aggregate	4.63

Respectfully submitted,


Jeannie F. O'Neil, Manager
Inorganic Chemistry Group

JFO/cg

¹Analysis by ASTM Method D3173

APPENDIX A

PRELIMINARY VOLUMETRIC FLOW RATE DETERMINATION

Test No. 1
 Asphalt Plant Stack

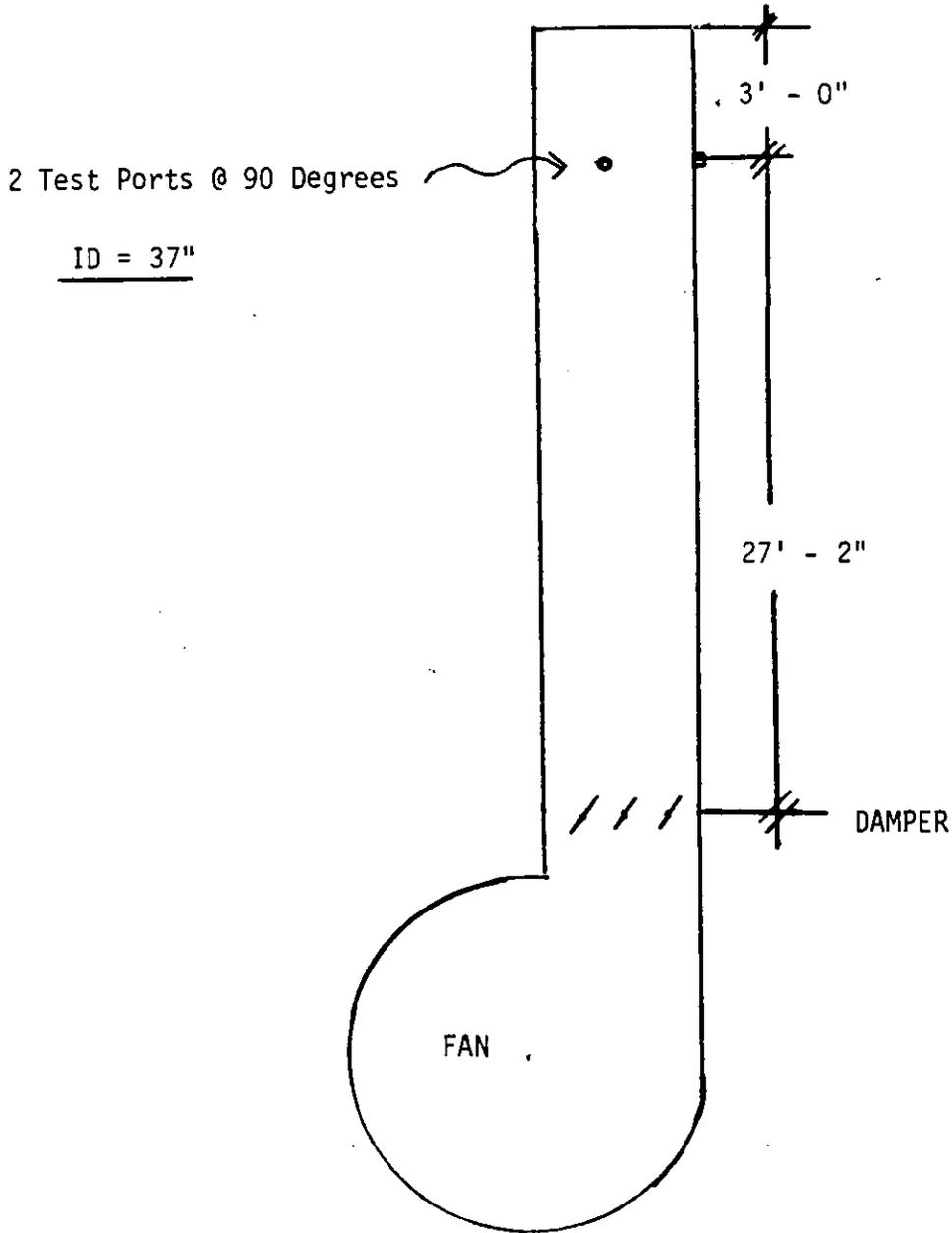
Results of Volumetric Flow Rate Determination-----Method 2

Date of Determination.....	06-21-93
Time of Determination.....(HRS)	800
Barometric pressure.....(IN.HG)	29.01
Pitot tube coefficient.....	.84
Number of sampling ports.....	2
Total number of points.....	24
Shape of duct.....	Round
Stack diameter.....(IN)	37.75
Duct area.....(SQ.FT)	7.77
Direction of flow.....	UP
Static pressure.....(IN.WC)	-.78
Avg. gas temp.....(DEG-F)	250
Moisture content.....(% V/V)	31.00
Avg. linear velocity.....(FT/SEC)	68.8
Gas density.....(LB/ACF)	.04813
Molecular weight.....(LB/LBMOLE)	29.24
Mass flow of gas.....(LB/HR)	92676
Volumetric flow rate.....	
actual.....(ACFM)	32091
dry standard.....(DSCFM)	15935

APPENDIX B

LOCATION OF TEST PORTS

T.A. SCHIFSKY AND SONS
ASPHALT PLANT STACK



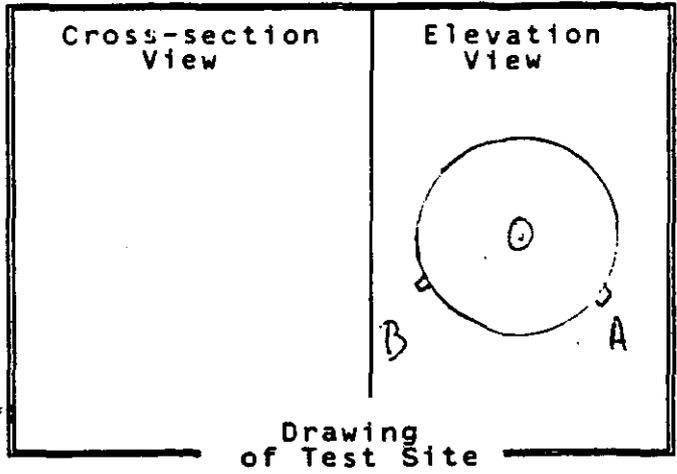
PS 7-22-93

APPENDIX C

FIELD DATA SHEETS

INTERPOLL LABORATORIES - EPA METHOD 2 FIELD DATA SHEET

Job T.A. Schifsky
 Source Asphalt Plant Stack
 Test 1 Run 1 Date 6/21/93
 Stack dimen. 37.75 IN.
 Dry bulb °F Wet bulb °F
 Manometer: Reg. Exp. Elec.
 Barometric pressure 29.01 in Hg
 Static pressure -78 in WC
 Operators D. VanHoever & J. Bergstrom
 Pitot No. V23-4 C_p.84



Traverse Point No.	Fraction of Diameter	Distance from Stack Wall (in)	Distance from End of Port (in)	Velocity Pressure (in WC)	Temperature of gas (°F)
		Port length: <u>1.75</u> in.		Time start: <u>0800</u> hrs	
A 1	.021	.79	2.54	.63	
2	.067	2.52	4.28	.82	
3	.118	4.45	6.20	.90	
4	.177	6.68	8.43	1.0	
5	.250	9.43	11.18	1.05	
6	.356	13.44	15.18	1.05	250
7	.644	24.31	26.06	1.0	
8	.750	28.31	30.06	1.05	
9	.823	31.07	32.82	1.05	
10	.882	33.30	35.05	1.0	
11	.933	35.22	36.97	.96	
12	.979	36.96	38.70	.92	
B 1				.65	
2				.70	
3				.73	
4				.83	
5				.92	
6				.98	
7				1.20	
8				1.20	
9				1.20	
10				1.20	
11				1.20	
12				1.10	

Temp. meas. device & S/N: PDT #18 & PDTM1 Time end: hrs

R or nothing = reg. manometer; S = expanded; E = electronic S-3921

INTERFOLL LABORATORIES EPA METHOD 5/17 SAMPLE LOG SHEET

Job T.A. Shifsky Date 6/21/93 Test 1 Run 1
 Source Asphalt Plant Stack No. of traverse points 24
 Method 5 Filter holder: glass Filter type: glass fiber

Sample Train Leak Checks:

Pretest: (0.02 cfm at 15 in. Hg. (vac)
 Posttest: 0 cfm at 6 in. Hg. (vac)

Particulate Catch Data:

No. of filters used: _____ Recovery solvent(s)
 _____ acetone _____
 _____ other(s) _____
 No. of probe wash bottles: _____
 Sample recovered by: DW

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		200	
Impinger No. 2	581		381
Impinger No. 3			
Condenser			
Desiccant	1337	1315	19
Total			400

Integrated Gas Sampling Data:

Bag Pump No. 23B Box No. 12 Bag No. 1
 Bag Material: 5-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 14 in. Hg.
 Time start: 0935 (HRS) Time end: 1032 (HRS)
 Sampling rate: 400 cc/min Operator: DW
 S/N of O₂ Analyzer used to monitor train outlet: 3

CF-023

INTERFOLL LABORATORIES EPA METHOD 5/17 SAMPLE LOG SHEET

Job T.A. Shifsky Date 1/21/93 Test 1 Run 2
 Source Asphalt Plant Stack No. of traverse points 27
 Method 5 Filter holder: glass Filter type: glass fiber

Sample Train Leak Check:

Pretest: (0.02 cfm at 15 in. Hg. (vac)
 Posttest: 0 cfm at 9 in. Hg. (vac)

Particulate Catch Data:

No.s of filters used: 5423 Recovery solvent(s)
 acetone _____
 other(s) _____
 No. of probe wash bottles: 1
 Sample recovered by: JAH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1		5700	
Impinger No. 2	581		381
Impinger No. 3			
Condenser			
Desiccant	1429	1410	19
Total			400

Integrated Gas Sampling Data:

Bag Pump No. 23B Box No. 12 Bag No. 2
 Bag Material: 5-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 14 in. Hg.
 Time start: 1159 (HRS) Time end: 1255 (HRS)
 Sampling rate: 400 cc/min Operator: JAH
 S/N of O₂ Analyzer used to monitor train outlet: 3

CF-023

INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Job T.A. Schifsky Operator Dick J.B. Pitot No. 123-1 Cp 8
 Source Asphalt Plant Stack Water Box No. 6 KHF 7.79 IN MC 1 inHg H₂O 22 X
 Date 6/21/83 1981 7 Room 2 Cooperator code 19079 Nozzle No. 7-4 Nozzle Dia. 2.5 IN.

Traverse Point No.	Sampling Time (min)	Sample Volume (cf)	Velocity Head (inHC)	Drifts Meter (inHC)	Des. Vol. (cf)	VAC. inHg	Stack	Probe	Dyan	Temperature (°F)			Gas/Out	Oxygen (xv/v)
										Temp	Impq.	Gas/In		
12	11.4	279.55	1.05	1.68	1.43	7	230	251	247	53	88	88	11.4	
11	2.5	281.44	1.10	1.76	3.36	1.2	225				94	90	12.1	
10	5	283.30	1.10	1.76	5.29	1.3	231	254	252	53	96	91	12.2	
9	7.5	285.23	1.10	1.75	7.22	1.7	237				98	91	12.1	
8	10	287.20	1.10	1.74	9.14	6	241	253	253	53	99	92	12.0	
7	12.5	289.14	1.10	1.74	1.07	6	241				100	93	12.0	
6	15	291.03	1.10	1.74	2.84	5	249	254	250	52	100	93	12.0	
5	17.5	293.80	1.0	1.57	4.67	5	251				100	93	11.8	
4	20	294.60	1.0	1.28	6.33	5	252	254	251	53	101	94	11.9	
3	22.5	296.30	1.0	1.18	7.92	5	251				101	94	11.8	
2	25	297.90	1.0	1.08	9.40	5	251	254	252	52	102	95	11.8	
1	27.5	299.43	1.0	1.08	0.94	5	251				102	95	11.8	
	30	300.94	1.0	1.04	2.85	7	251	257	252	53	103	96	11.6	
12	32.5	302.90	1.08	1.70	4.86	7	251				103	96	11.7	
11	35	304.91	1.20	1.89	6.87	7	258	253	254	51	104	96	11.8	
10	37.5	306.87	1.20	1.87	8.87	7	257				104	97	12.0	
9	40	308.90	1.20	1.87	0.88	7	260	251	253	51	105	97	12.0	
8	42.5	310.75	1.20	1.87	2.80	7	262				105	98	11.9	
7	45	312.81	1.10	1.71	4.50	6	262	252	253	51	105	98	12.1	
6	47.5	314.55	1.0	1.34	6.14	5	262				106	98	11.8	
5	50	316.23	1.0	1.25	7.72	5	262	254	254	54	106	98	11.7	
4	52.5	317.73	1.0	1.15	9.25	5	262				106	98	11.7	
3	55	319.24	1.0	1.09	0.73	5	262	253	254	54	106	98	11.7	
2	57.5	320.74	1.0	1.01	2.17	5	263				106	99	11.6	
1	60	322.90	1.0	1.0							106	99		
	1255													
V = 4265													AVG. = 98.2	
Q = 60														

150
10

INTERFOLL LABORATORIES EPA METHOD 5/17 SAMPLE LOG SHEET

Job T.A. Shifsky Date 6/21/97 Test 1 Run 3
 Source Asphalt Plant Stack No. of traverse points 24
 Method 5 Filter holder: _____ Filter type: glass fiber

Sample Train Leak Check:

Pretest: (0.02 cfm at 15 in. Hg. (vac)
 Posttest: 0 cfm at 14 in. Hg. (vac)

Particulate Catch Data:

No.s of filters used: 5424 Recovery solvent(s) _____
 acetone _____
 other(s) _____
 No. of probe wash bottles: _____
 Sample recovered by: DWH

Condensate Data:

Item	Weight (g)		
	Final	Tare	Difference
Impinger No. 1			
Impinger No. 2	<u>503</u>	<u>2200</u>	<u>363</u>
Impinger No. 3			
Condenser			
Desiccant	<u>1347</u>	<u>1334</u>	<u>13</u>
Total			<u>376</u>

Integrated Gas Sampling Data:

Bag Pump No. 23B Box No. 12 Bag No. 3
 Bag Material: 5-layer Aluminized Tedlar Size: 44 L
 Pretest leak check: 0 cc/min at 14 in. Hg.
 Time start: 1400 (HRS) Time end: 1457 (HRS)
 Sampling rate: 400 cc/min Operator: DWH
 S/N of O₂ Analyzer used to monitor train outlet: 3

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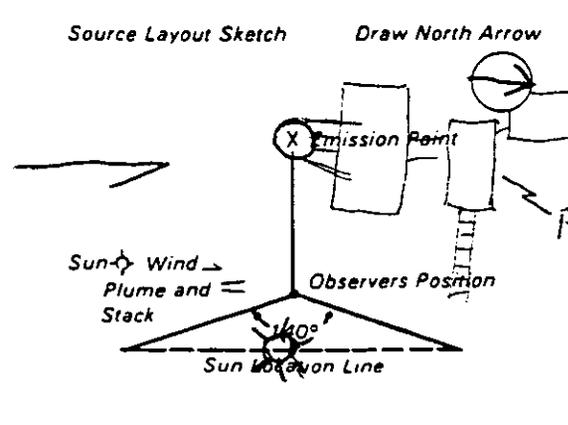
INTERPOL LABORATORIES EPA METHOD 5 FIELD DATA SHEET

Job: T.A. Schifsky
 Source: Asphalt Plant
 Date: 6/27/93
 Operator: D.K.H. or J.P.B.
 Meter Box No: 3370
 Counter Code: 179
 Pitot No. 103-4
 Bar. Press. 29.1
 Nozzle Dia. 2.52 IN.
 Cp 1.84
 InHg H2O

Traverse Point No.	Sampling Time (min)	Sample Volume (cfs)	Velocity Head (inH ₂ O)	Drifted Water (inH ₂ O)	Des. Vol. (cft)	VAC. inHg	Temperature (°F)				Oxygen (xv/v)		
							Stack	Probe	Duct	Imp.		Gas In	Gas Out
9	13.56	322.50	1.10	1.74	4.43	4	230	253	250	57	95	95	12.1
11	2.5	324.52	1.10	1.22	6.34	4	233	257	254	54	96	95	12.7
10	5	326.40	1.20	1.88	8.34	7	239	257	254	54	98	95	12.7
9	7.5	328.35	1.25	1.95	0.38	7	236	260	257	54	100	96	12.3
8	10	330.35	1.05	1.79	2.34	7	242	260	257	54	102	97	12.2
7	15	334.24	1.05	1.78	4.29	7	247	261	258	52	103	98	12.1
6	17.5	336.20	1.94	1.44	6.06	7	253	261	258	52	104	98	12.0
5	20	337.83	1.84	1.29	7.72	6	256	257	257	53	105	99	11.9
4	22.5	339.36	7.7	1.18	9.32	6	258	257	257	53	105	99	11.9
3	25	340.85	7.3	1.11	0.87	5	259	257	256	53	106	100	11.8
2	27.5	342.25	6.0	9.2	2.28	5	259	257	256	53	106	100	11.5
1	30	343.70	1.60	9.2	3.69	5	259	255	257	54	106	100	11.0
A 12	32.5	345.46	9.2	1.41	5.44	7	259	255	257	54	108	101	11.8
11	35	347.24	9.7	1.47	7.23	7	266	256	257	54	108	102	11.8
10	37.5	349.72	1.05	1.60	9.09	7	266	256	257	54	109	102	11.7
9	40	351.09	1.10	1.67	1.00	7	266	258	260	55	110	103	11.6
8	42.5	352.85	9.8	1.48	2.77	7	271	258	260	55	110	103	11.7
7	45	354.58	9.3	1.41	4.55	7	268	257	261	56	110	104	11.8
6	47.5	356.20	8.1	1.23	6.19	6	268	257	261	56	111	104	11.8
5	50	357.86	9.0	1.37	7.92	6	267	257	263	56	111	104	12.0
4	52.5	359.51	7.7	1.17	9.52	6	267	257	263	56	111	105	11.8
3	55	361.60	6.7	1.02	1.02	6	267	256	263	56	112	105	11.7
2	57.5	362.36	5.6	8.5	2.51	6	267	256	263	56	112	106	11.8
1	60	363.70	5.2	7.9	3.71	6	267	256	263	56	112	106	11.8
Average		41.20		1.38									103.4

Interpoll Laboratories
(612)786-6020

Visible Emissions Form

SOURCE NAME				OBSERVATION DATE				START TIME				STOP TIME			
T.H. Schifsky & Sons Inc.				6-21-93				0930				1032			
ADDRESS				SEC		MIN		SEC		MIN		SEC		MIN	
2370 E. Hwy. 36				0	15	30	45	0	15	30	45	0	15	30	45
CITY				STATE				ZIP				1			
North St. Paul				MN								0 0 0 0			
PHONE				SOURCE ID NUMBER				2				0 0 0 0			
PROCESS EQUIPMENT				OPERATING MODE				3				0 0 0 0			
Asphalt Plant				100%				31				0 0 0 0			
CONTROL EQUIPMENT				OPERATING MODE				32				0 0 0 0			
Baghouse				100%				33				0 0 0 0			
DESCRIBE EMISSION POINT				5				35				0 0 0 0			
START ground metal stack STOP ✓				6				36				0 0 0 0			
HEIGHT ABOVE GROUND LEVEL				HEIGHT RELATIVE TO OBSERVER				7				0 0 0 0			
START 39' STOP ✓				START 39' STOP ✓				37				0 0 0 0			
DISTANCE FROM OBSERVER				DIRECTION FROM OBSERVER				8				0 0 0 0			
START 117' STOP ✓				START W STOP ✓				38				0 0 0 0			
DESCRIBE EMISSIONS				9				39				0 0 0 0			
START lifting STOP ✓				10				40				0 0 0 0			
EMISSION COLOR				PLUME TYPE				11				0 0 0 0			
START clear STOP ✓				CONTINUOUS <input checked="" type="checkbox"/>				41				0 0 0 0			
WATER DROPLETS PRESENT:				IF WATER DROPLET PLUME:				12				0 0 0 0			
NO <input type="checkbox"/> YES <input checked="" type="checkbox"/>				ATTACHED <input type="checkbox"/> DETACHED <input checked="" type="checkbox"/>				42				0 0 0 0			
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED				13				43				0 0 0 0			
START 2' above stack STOP ✓				14				44				0 0 0 0			
DESCRIBE BACKGROUND				15				45				0 0 0 0			
START SKY STOP ✓				16				46				0 0 0 0			
BACKGROUND COLOR				SKY CONDITIONS				17				0 0 0 0			
START blue STOP ✓				START clear STOP ✓				47				0 0 0 0			
WIND SPEED				WIND DIRECTION				18				0 0 0 0			
START 5-10 STOP ✓				START S STOP ✓				48				0 0 0 0			
AMBIENT TEMP.				WET BULB TEMP.		RH. percent		19				0 0 0 0			
START 73° STOP 74°				67°		72%		49				0 0 0 0			
Source Layout Sketch				20				50				0 0 0 0			
Draw North Arrow				21				51				0 0 0 0			
				22				52				0 0 0 0			
* AVERAGE OPACITY FOR HIGHEST PERIOD				23				53				0 0 0 0			
NUMBER OF READINGS ABOVE % WERE				24				54				0 0 0 0			
RANGE OF OPACITY READINGS				25				55				0 0 0 0			
MINIMUM				26				56				0 0 0 0			
MAXIMUM				27				57				0 0 0 0			
OBSERVER'S NAME (PRINT)				28				58				0 0 0 0			
RICHARD J. EIDEM				29				59				0 0 0 0			
OBSERVER'S SIGNATURE				30				60				0 0 0 0			
DATE				AVERAGE OPACITY FOR HIGHEST PERIOD				NUMBER OF READINGS ABOVE % WERE							
6-21-93															
ORGANIZATION				OBSERVER'S SIGNATURE				DATE							
Interpoll Inc.				Richard J. Eidem				6-21-93							
CERTIFIED BY				ORGANIZATION				DATE							
ETA Inc.				Interpoll Inc.				3-30-93							
VERIFIED BY				DATE				DATE							

VISIBLE EMISSIONS EVALUATOR

This is to certify that

Richard Tidem

met the specifications of Federal Reference Method 9 and qualified as a visible emissions evaluator. Maximum deviation on white and black smoke did not exceed 7.5% opacity and no single error exceeding 15% opacity was incurred during the certification test conducted by Eastern Technical Associates of Raleigh, North Carolina. This certificate is valid for six months from date of issue.

[Signature]
President

[Signature]

David B. Savage, Jr.
Program Manager

238303

Certificate Number

Microscopists

March 31, 1993
Date of Issue

APPENDIX D

INTERPOLL LABORATORIES ANALYTICAL DATA

EPA Method 3 Data Reporting Sheet
Orsat Analysis

Job T.A. Schifsko Source Asphalt Plant
 Team Leader Bob Test Site Stack
 Date Submitted 2-21-93 Date of Test 2-21-93
 Test No. 1 No. of Runs Completed 3
 Date of Analysis 2-22-93 Technician C. Helms

Test/Run	Sample Log Number and Type	No. of An.	Buret Readings (ml)			Conc. CO ₂ %v/v Dry	Conc. O ₂ %v/v Dry	F _o
			Zero Pt.	After CO ₂	After O ₂			
1/1	9190-07 <input checked="" type="checkbox"/> B <input type="checkbox"/> F	1	0.00	4.40	17.80	4.40	13.40	1.70
		2	0.00	4.40	17.80	4.40	13.40	1.70
		Avg	██			4.40	13.40	████
1/2	-11 <input checked="" type="checkbox"/> B <input type="checkbox"/> F	1	0.00	4.50	17.80	4.50	13.30	1.69
		2	0.00	4.50	17.80	4.50	13.30	1.69
		Avg	██			4.50	13.30	████
1/3	-15 <input checked="" type="checkbox"/> B <input type="checkbox"/> F	1	0.00	4.60	17.70	4.60	13.10	1.70
		2	0.00	4.60	17.70	4.60	13.10	1.70
		Avg	██			4.60	13.10	████
	<input type="checkbox"/> B <input type="checkbox"/> F	1						
		2						
		Avg	██					████
	<input type="checkbox"/> B <input type="checkbox"/> F	1						
		2						
		Avg	██					████
	<input type="checkbox"/> B <input type="checkbox"/> F	1						
		2						
		Avg	██					████
	<input type="checkbox"/> B <input type="checkbox"/> F	1						
		2						
		Avg	██					████
	<input type="checkbox"/> B <input type="checkbox"/> F	1						
		2						
		Avg	██					████

- Ambient Air QA Check
- Orsat Analyzer System Leak Check
- F_o Within EPA M-3 Guidelines for fuel type.

Where $F_o = \frac{20.9 - O_2}{CO_2}$

EPA Method 3 Guidelines
Fuel Type F_o Range

Coal:	
Anthracite/Lignite	1.016-1.130
Bituminous	1.083-1.230
Oil:	
Distillate	1.260-1.413
Residual	1.210-1.370
Gas:	
Natural	1.600-1.836
Propane	1.434-1.586
Butane	1.405-1.553
Wood/Wood Bark	1.000-1.130

F=Flask (250 cc all glass)
B=Tedlar Bag (5-layer)

Interpoll Laboratories
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EPA Method 5 Data Reporting Sheet
Impinger Catch/Minnesota Protocol

Job TA Schiffsky Source Asphalt Plant
 Team Leader DOH Test Site Stack
 Date Submitted 6-22-93 Date of Test 6-21-93
 Test No. 1 No. of Runs Completed 3
 Date of Analysis 7-6-93 Technician C. Helgeson

0	Test <u>1</u> Run <u>0</u> Field Blank Log Number <u>9190-03</u> Comments _____	Dish No. <u>61A</u> Dish Tare Wt. <u>51.4732</u> g Dish+Sample Wt. <u>51.4737</u> g Sample Wt. <u>0.0005</u> g
1	Test <u>1</u> Run <u>1</u> Log Number <u>-06</u> Comments _____	Dish No. <u>102</u> Dish Tare Wt. <u>44.3251</u> g Dish+Sample Wt. <u>44.3436</u> g Sample Wt. <u>0.0185</u> g
2	Test <u>1</u> Run <u>2</u> Log Number <u>-10</u> Comments _____	Dish No. <u>105</u> Dish Tare Wt. <u>47.8643</u> g Dish+Sample Wt. <u>47.8754</u> g Sample Wt. <u>0.0111</u> g
3	Test <u>1</u> Run <u>3</u> Log Number <u>-14</u> Comments _____	Dish No. <u>206</u> Dish Tare Wt. <u>47.8189</u> g Dish+Sample Wt. <u>47.8262</u> g Sample Wt. <u>0.0073</u> g
4	Test _____ Run _____ Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

Blank Solvent Wt. 0.0005g

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	<u>0.0080</u>	<u>0.0106</u>	<u>0.0068</u> D-2		
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LSC-03.GR

Interpoll Laboratories
(612) 786-6020

EPA Method 5 Data Reporting Sheet
Probe/Cyclone Wash

Job T. A. Schiffs Ky Source Asphalt Plant
 Team Leader DUH Test Site Stack
 Date Submitted 6-22-93 Date of Test 6-21-93
 Test No. 1 No. of Runs Completed 3
 Date of Analysis 7-6-93 Technician C. Helgeson
 Transport Leakage None ml Solvent Acetone

0	Test <u>1</u> Run <u>0</u> Field Blank Log Number <u>9190-01</u> Vol. of Solvent <u>110</u> ml *Solvent Residue <u>3.6</u> ug/ml	Dish No. <u>405</u> Dish Tare Wt. <u>48.4903</u> g Dish+Sample Wt. <u>48.4907</u> g Sample Wt. <u>0.0004</u> g
1	Test <u>1</u> Run <u>1</u> Vol. of Solvent <u>155</u> ml Log Number <u>-04</u> Comments _____	Dish No. <u>513</u> Dish Tare Wt. <u>77.4132</u> g Dish+Sample Wt. <u>77.4281</u> g Sample Wt. <u>0.0149</u> g
2	Test <u>1</u> Run <u>2</u> Vol. of Solvent <u>115</u> ml Log Number <u>-08</u> Comments _____	Dish No. <u>515</u> Dish Tare Wt. <u>50.0146</u> g Dish+Sample Wt. <u>50.0303</u> g Sample Wt. <u>0.0157</u> g
3	Test <u>1</u> Run <u>3</u> Vol. of Solvent <u>115</u> ml Log Number <u>-12</u> Comments _____	Dish No. <u>517</u> Dish Tare Wt. <u>48.5960</u> g Dish+Sample Wt. <u>48.6100</u> g Sample Wt. <u>0.0140</u> g
4	Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Vol. of Solvent _____ ml Log Number _____ Comments _____	Dish No. _____ Dish Tare Wt. _____ g Dish+Sample Wt. _____ g Sample Wt. _____ g

*Solvent Residue 3.6 ug/ml = [(Sample Wt. 0.0004g) (10⁶)] / Vol. of Sol. 110 ml
 EPA-MS Acetone Residue Blank Spec. (7.8 ug/ml)

Results:

Field Blk. Run 1 Run 2 Run 3 Run 4 Run 5

	<u>0.0143</u>	<u>0.0153</u>	<u>0.0136</u>	<u>D-3</u>	
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LSC-01YR

Interpoll Laboratories
(612) 786-6020

EPA Method 5 Data Reporting Sheet
Filter Gravimetrics

Job TA Schifsky Source Asphalt Plant
 Team Leader DUH Test Site Steck
 Date Submitted 6-22-93 Date of Test 6-21-93
 Test No. 1 No. of Runs Completed 3
 Date of Analysis 7-6-93 Technician C. Hejeren

0	Test <u>1</u> Run <u>0</u> Field Blank Log Number <u>9190-02</u> Comments _____	Filter No. <u>5426</u> Filter Type <u>4"6F</u> Filter Tare Wt. <u>.9176</u> g Filter+Sample Wt. <u>.9178</u> g Sample Wt. <u>0.0002</u> g
1	Test <u>1</u> Run <u>1</u> Log Number <u>-05</u> Comments _____	Filter No. <u>5421</u> Filter Type <u>4"6F</u> Filter Tare Wt. <u>.9244</u> g Filter+Sample Wt. <u>.9309</u> g Sample Wt. <u>0.0065</u> g
2	Test <u>1</u> Run <u>2</u> Log Number <u>-09</u> Comments _____	Filter No. <u>5423</u> Filter Type <u>4"6F</u> Filter Tare Wt. <u>.9227</u> g Filter+Sample Wt. <u>.9278</u> g Sample Wt. <u>0.0051</u> g
3	Test <u>1</u> Run <u>3</u> Log Number <u>-13</u> Comments _____	Filter No. <u>5424</u> Filter Type <u>4"6F</u> Filter Tare Wt. <u>.9129</u> g Filter+Sample Wt. <u>.9192</u> g Sample Wt. <u>0.0063</u> g
4	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g
5	Test _____ Run _____ Log Number _____ Comments _____	Filter No. _____ Filter Type _____ Filter Tare Wt. _____ g Filter+Sample Wt. _____ g Sample Wt. _____ g

Results:

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0065	0.0051	0.0063		

Field Blk.	Run 1	Run 2	Run 3	Run 4	Run 5
	0.0388	0.0310	0.0267		

Interpoll Laboratories
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Sample Deposition

Job T.A. Schiffsky Source Asphalt Plant
 Field Engineer DWT Test Site Stack
 Date Submitted 6/21/93 Date of Test 6/21/93
 Test No. 1 No. of Runs Completed 3

No.	Sample Type	Analysis	Comments
4	Probe Wash: <input checked="" type="checkbox"/> Acetone <input type="checkbox"/> MeCl ₂ <input type="checkbox"/> DI Water <input type="checkbox"/> _____	<input checked="" type="checkbox"/> As per EPA M-5 <input type="checkbox"/> As per EPA M-29 <input type="checkbox"/> As per EPA M-201A <input type="checkbox"/> Other _____	
4	Filter: <input checked="" type="checkbox"/> 4" Glass <input type="checkbox"/> SS Thimble <input type="checkbox"/> 2.5" Glass <input type="checkbox"/> Pallflex	<input checked="" type="checkbox"/> As per EPA M-5 <input type="checkbox"/> As per EPA M-29 <input type="checkbox"/> As per EPA M-201A <input type="checkbox"/> As per EPA M-17 <input type="checkbox"/> Other _____	
4	Impingers: <input checked="" type="checkbox"/> DI Water <input type="checkbox"/> 3% H ₂ O ₂ <input type="checkbox"/> 1N NaOH <input type="checkbox"/> KOH (Cr VI) <input type="checkbox"/> H ₂ SO ₄ (HCl) <input type="checkbox"/> 2,4-DNPH <input type="checkbox"/> _____ <input type="checkbox"/> _____	<input checked="" type="checkbox"/> MN Protocol <input type="checkbox"/> WI Protocol <input type="checkbox"/> As per EPA M-202 <input type="checkbox"/> As per EPA M-6,8 <input type="checkbox"/> Acid Gases <input type="checkbox"/> Formaldehyde <input type="checkbox"/> As per EPA M-29 <input type="checkbox"/> As per EPA M-26 <input type="checkbox"/> Other _____	
3	Integrated Gas Sample <input checked="" type="checkbox"/> Tedlar Bag <input type="checkbox"/> _____	<input checked="" type="checkbox"/> As per EPA M-3 <input type="checkbox"/> As per EPA M-10 <input type="checkbox"/> Other _____	
	Oxides of Nitrogen (NO _x)	<input type="checkbox"/> As per EPA M-7A <input type="checkbox"/> Other _____	
3	<input type="checkbox"/> Fuel Sample <input checked="" type="checkbox"/> Aggregate	<input type="checkbox"/> Attached Form S-0163	
	Particle Size	<input type="checkbox"/> X-Ray Sedigraph <input type="checkbox"/> Cascade Impactor <input type="checkbox"/> Other _____	
	Misc Samples <input type="checkbox"/> _____ <input type="checkbox"/> _____	<input type="checkbox"/> As per EPA M-6 <input type="checkbox"/> As per EPA M-7A <input type="checkbox"/> Other _____	

Type of Source: _____

Fuel Type:
Coal: Bituminous Anthracite Lignite
Wood: Wood Waste Dust Bark
Oil: Waste Oil No. 2 No. 6
 Natural Gas RDF Other _____

APPENDIX E

ASPHALT PLANT INFORMATION

Interpoll Laboratories
(612)786-6020

MPCA Exhibit C for Process Emissions

JOB 93-16
SOURCE T. A. Schitsky & Sons Inc
DATE 6/21/93

C. Equipment & Operating Data

1. Process Equip. No./Ident. STANDSTEEL / 628
2. Process Equip. Description BATCH PLANT
3. Process equipment operating under normal operating conditions:
No Yes X

D. Instrument Data on Process Equipment

1. Include copy of production records or instrumentation which indicates rate of production or operation of the equipment, i.e. units per hour, lbs. per hour, pressure, air flow, etc.

E. Air Pollution Control Equipment

1. Type/model control equipment STANDSTEEL / 384
2. Air pressure drop across the control equipment 3.0 to 4.0
3. Air flow through the control equipment 31,434 ACFM AT 275°
4. Was the control equipment operating normally? YES
5. Data of last major maintenance/cleaning of control equipment
NONE

F. Plant Manager's Certification

I certify that the information submitted herein is accurate and correct and that no information requested was withheld from MPCA, Division of Air Quality.

By Thomas J. Schifky, Position VICE PRES.

Interpoll Laboratories
(612)786-6020

Asphalt Plant Information Sheet

Manufacturer and Model No.
of the Plant Stansteel / 628

Owner and Operator of the Plant

Location of Plant at time of
Test (State, County and Address) 2370 E. Hwy 36
North St. Paul, MN. Ramsey co.

Estimated Total Time of the
Plant at this Site (from when to when) 1959 to present

Type of Pollution Control Equipment (wet scrubber, mechanical collector,
etc.) Stansteel Baghouse

Model No. of Pollution Control Equipment model 384

If wet scrubber, provide the following information:

Percent recycle of scrubber water N/A %

Flow of water to scrubber N/A GPM

Manufacturer recommended pressure drop
across venturi 3.0 to 4.0 IN.WC.

Rated Capacity of Asphalt Plant 140 TONS/HR
at an aggregate moisture content of 5 %

Type of Fuel Used to Fire Plant:

- Natural Gas
- No. 2 Fuel Oil
- No. 5 Fuel Oil
- Propane

Normal Production Rate of Plant 140 TONS/HR
at an aggregate moisture content of 5 %

NOTE: Attach drawings of plant and pollution control equipment.

Name of Individual Supplying Information Steve Schiff

Date 6/21/93

S-0150R(2)

APPENDIX F

ASPHALT PLANT OPERATING DATA

TEST 1

MPCA

Asphalt Plant

Records of Operating Conditions During Compliance Tests

Plant Manufacturer and Model STANSTEEL 628 Plant type BATCH

Date of first installation _____

Test date 6/21/93 Location 2370 E Hwy 36 Time: start 9:30 AM stop 10:30 AM

Fuel burned NAT. GAS Dust collector Venturi scrubber, Other wet scrubber
41.0 CUBIC FT. Cyclone/multiclone Baghouse

Number of burners 1 Burner(s) rating 50 MMBTUH = 100% setting

If wet scrubbing, percent water recycle N/A %

Time	Burner setting %	Aggregate TPH	Recycle TPH	Asphalt TPH	Mix Temperature °F	Pressure drop across dust collector(s) in H ₂ O	Water Flow rate through wet collectors gpm
9:30	100%	0	-	0	300°	3.25	
9:45	100%	37	-	1.46	295°	3.25	
10:00	100%	36.6 73.6	-	1.92 3.88	302°	3.25	
10:15	100%	37.8 111.4	-	2.0 5.88	300°	3.25	
10:30	100%	32 143.4	-	1.64 7.54	300°	3.25	

Moisture content in the aggregates

1434 | 410 | .29

	Run No. 1	Run No. 2	Run No. 3	Average	Average Measured or calculated* fuel usage: .29
Virgin					
Recycle					

Responsible Signature and Date: *Randy Blongquist* 6/21/93

* if calculated, applicant should attach a schedule showing the bases, assumptions, sources of colligative data, and the computation.

Include fuel analysis as required

CES:prw9.4

TEST 2

MPCA

Asphalt Plant

Records of Operating Conditions During Compliance Tests

Plant Manufacturer and Model STAN STEEL 628 Plant type BATCH

Date of first installation _____

Test date 6/21/93 Location 2370 E Hwy 36 Time: start 11:55 stop 12:55

Fuel burned NAT. GAS Dist collector Venturi scrubber, Other wet scrubber
38.0 cubic ft Cyclone/multiclone Baghouse

Number of burners 1 Burner(s) rating 50 MMBTUH = 100% setting

If wet scrubbing, percent water recycle N/A %

Time	Burner setting %	Aggregate TPH		Recycle TPH	Asphalt TPH		Mix Temperature °F	Pressure drop across dust collector(s) in H ₂ O	Water Flow rate through wet collector gpm
11:55	100%	0		-	0		300°	3.25	
12:10	100%	43		-	2.28		300°	3.25	
12:25	100%	36	79	-	1.87	4.1	295°	3.25	
12:40	100%	37	116	-	1.95	6.05	300°	3.25	
12:55	100%	31.5	147.5	-	1.61	7.66	300°	3.25	

Moisture content in the aggregates

1475/38.0

	Run No. 1	Run No. 2	Run No. 3	Average	Average Measured or calculated* fuel usage:
Virgin					.26
Recycle					cf/ton produc
					gal/ton produc

Responsible Signature and Date: Randy Blomquist 6/21/93

* if calculated, applicant should attach a schedule showing the bases, assumptions, sources of colligative data, and the computation.

Include fuel analysis as required

CES:pmw9.4

TEST # 3

MPCA

Asphalt Plant

Records of Operating Conditions During Compliance Tests

Plant Manufacturer and Model STANSTEEL 628 Plant type BATCH
 Date of first installation _____
 Test date 6/21/93 Location 2370 E Hwy 36 Time: start 2:00 pm stop 3:00 pm
 Fuel burned NAT GAS Dust collector Venturi scrubber, Other wet scrubber
41.0 cubic ft Cyclone/multiclone Baghouse
 Number of burners 1 Burner(s) rating 50 MMBTUH = 100% setting
 If wet scrubbing, percent water recycle _____ %

Time	Burner setting %	Aggregate TPH	Recycle TPH	Asphalt TPH	Mix Temperature °F	Pressure drop across dust collector(s) in H ₂ O	Water Flow rate through wet collector: gpm
2:00	100%	0	-	0	305	3.25	
2:15	100%	39	-	1.96	302	3.25	
2:30	100%	36 75	-	1.87 3.85	300	3.25	
2:45	100%	33 108	-	1.69 5.54	300	3.25	
3:00	100%	38.5 146.5	-	1.96 7.5	300	3.25	

Moisture content in the aggregates					146.5/41.0 = .28
	Run No. 1	Run No. 2	Run No. 3	Average	Average Measured or calculated* fuel usage:
Virgin					.28 cf/ton product gal/ton produc
Recycle					

Responsible Signature and Date: *Sandy Blount* 6/21/93

* if calculated, applicant should attach a schedule showing the bases, assumptions, sources of colligative data, and the computation.
 Include fuel analysis as required
 CES:pmw9.4

TEST 1

THE METAL DOCTOR



Steel & Aluminum Welding

770-6285

Tons

lbs Asp.

9:30 162

2247800

9:45 199 (37)

2251724
2000 | 3924 | 1.96

10:00 236.2 (36.6)

2255565
2000 | 3841 | 1.92

10:15 274.8 (37.8)

2259567
2000 | 4002 | 2.00

10:30 306 (32)

2262856
2000 | 3289 | 1.64

TEST 2

THE METAL DOCTOR



Steel & Aluminum Welding

770-6285

TOTAL TONS

11:55 316 START 2263844

12:20 359
(43) tons 2268 400
2000 | 4556 | 2.28

12:25 395
(36) ton 2272038
2000 | 3638 | 1.82

12:40 432
(37) 2275932
2000 | 3894 | 1.95

12:55 463.5
31.5
2279156
/ 3224 | 1.61

- Truck Bodies
- Hoists
- Fuel & Hyd. Tanks
- Ladder Racks
- Truck Frames
- Custom Trailers
- Hitches
- Aluminum Floors
- Custom Trailers
- Aluminum Floors

1/27 FS



THE METAL DOCTOR

Steel & Aluminum Welding
770-6285

2:00	499	2282794
2:15	538 (39)	2286707
2:30	574 (36)	2000/3913 (1.96)
2:45	607 (33)	2290481
3:00	645.5 (38.5)	2000/3774 (1.89)
		2293859
		2000/3378 (1.69)
		2297773
		/3914 (1.96)

- Truck Bodies
- Fuel & Hyd. Tanks
- Ladder Racks
- Truck Frames
- Custom Trailers
- Hitches
- Aluminum Floors

"Where the Quality is Built In"

APPENDIX G

PROCEDURES

Particulate Loadings and Emission Rates

The particulate emission rates were determined per EPA Methods 1-5, CFR title 40, Part 60, Appendix A (revised July 1, 1987). In this procedure, a preliminary velocity profile of the gases in the flue is obtained by means of a temperature and velocity traverse. On the basis of these values, sampling nozzles of appropriate diameter are selected to allow isokinetic sampling, a necessary prerequisite for obtaining a representative sample.

The sampling train consists of a heated glass-lined sampling probe equipped with a Type S pitot and a thermocouple. The probe is attached to a sampling module which houses the all-glass in line filter holder in a temperature controlled oven. In addition, the sampling module also houses the impinger case and a Drierite drying column. The sampling module is connected by means of an umbilical cord to the control module which houses the dry test gasmeter, the calibrated orifice, a leakless pump, two inclined manometers, and all controls required for operating the sampling train.

Particulate samples were collected as follows: The sample gas was drawn in through the sampling probe isokinetically and passed through a 4-inch diameter Gelman Type A/E glass fiber filter. The particulates were removed at this point and collected on the filter. The gases then passed through an ice-cooled impinger train and a desiccant-packed drying column which quantitatively absorb all moisture from the sample gas stream after which the sample gas passes through the pump and the dry test gasmeter which integrates the sample gas flow throughout the course of the test. A calibrated orifice attached to the outlet of the gasmeter provides instantaneous flow rate data.

A representative particulate sample was acquired by sampling for equal periods of time at the centroid of a number of equal area regions in the duct. The sampling rate is adjusted at each site such that an isokinetic sampling condition prevails. Nomographs are used to aid in the rapid determination of the sampling rate.

After sampling is complete, the filter is removed and placed in a clean container. The nozzle and inlet side of the filter holder are quantitatively washed with acetone and the washings are stored in a second container. A brush is often used in the cleaning step to help dislodge deposits. The samples are returned to the laboratory where they are logged in and analyzed. The volume of the acetone rinse ("probe wash") is noted and then the rinse is quantitatively transferred to a tared 120 cc porcelain evaporating dish and the acetone evaporated off at 97-105 OF. This temperature is used to prevent condensation of atmospheric moisture due to the cooling effect induced by the evaporation of acetone. The acetone-free sample is then transferred to an oven and dried at 105 OC for 30 minutes, cooled in a desiccator over Drierite, and then weighed to the nearest .01 mg. The filter sample is quantitatively transferred to a 6-inch watch glass and dried in an oven at 105 OC for two hours. The filter and watch glass are then cooled in a desiccator and the filter weighed to the nearest .01 mg. All weighings are performed in a balance room where the relative humidity is hydrostatted to less than 50% relative humidity. Microscopic examination of the samples is performed if any unusual characteristics are observed. The weight of the acetone rinse is corrected for the acetone blank. The Drierite column is weighed on-site and the water collected by Drierite is added to the condensate so that the total amount of absorbed water may be ascertained.

Integrated flue gas samples for Orsat analysis were collected simultaneously from the stack and from the breeching at the inlet to the wet scrubber. The samples were collected in 15-liter gas sampling bags at a constant flow rate throughout each particulate run. The bags were then returned to the laboratory and analyzed by Orsat analysis. Standard commercially prepared solutions were used in the Orsat analyzer (sat. KOH for carbon dioxide and reduced methylene blue for oxygen).

Interpoll Laboratories
(612)786-6020

Condensable Organic Compounds Analysis

(State of Minnesota - MPCA Exhibit C)

Method II-8672-MN

Equipment: Separatory funnel - 500 cc with Teflon stopcock
Powder funnel - 75 mm ID with a 17 mm stem
Evaporating dish(es) - 200 cc or 250 cc beaker

Reagents: Diethyl ether - reagent grade
Chloroform - reagent grade
Sodium sulfate - (ACS) granular anhydrous
Toluene - (if 3% hydrogen peroxide is used to collect the samples)
Glass wool (Pyrex microfiber)

PREPARATION

1. Place 1 kg of granular anhydrous sodium sulfate in a shallow tray and heat to 200 °C for at least four hours. Store in a tightly sealed glass container.
2. Place a plug of clean glass wool in the stem of the powder funnel. The plug must be of sufficient size so that it is held snugly in place by its own pressure. Add a one-inch layer of dry sodium sulfate.

SAMPLING

An all-glass impinger assembly is used in the back half of the EPA Method 5 sampling train when an organic wet catch is to be collected. The impinger assembly consists of a modified impinger, a Greenburg Smith impinger followed by another modified impinger. The third impinger should have a temperature measuring device at the outlet upstream of a final impinger or desiccant column to monitor the temperature of the outlet gas stream. Prior to the start of the test, each of the first two impingers should be charged with 100 g of Class I water. The Method 5 train should be operated as provided for in EPA Method 5. Ice should be added to the impinger bath to keep the temperature of the gas at the outlet at or less than 68 °F. After the post test leak check, the impinger train is removed and impinger contents poured into a tared all-glass sample bottle and closed with a Teflon-lined cap. The sample bottle is then weighed and the total condensate calculated by subtraction of the bottle tare weight and the weight of initial water added to the impingers (200 g). A label is affixed and the sample is returned to the laboratory for analysis. The sample should be stored at 4 °C if the analysis is not conducted within 48 hours.

ANALYSIS

I. Organics

Caution! Work in vented hood!!!

A. Organic Blank Determination

1. Pour 125 mL of ethyl ether and 125 mL of chloroform into a tared beaker.
2. Evaporate solvent in hood at 70 °F or less until no solvent remains.
3. Desiccate the sample in dish for two hours.
4. Weigh the sample to nearest 0.1 mg, record and report on Form LSC-036.

B. Organic Sample Determination

1. Test for peroxide in sample ether using KI strips. (If KI strip shows positive, contact your supervisor before proceeding.)
2. Transfer the sample solution quantitatively to a 500 mL separatory funnel. Use the first of three 25 mL chloroform aliquots to rinse the sample container.
3. Extract with three 25 mL portions of chloroform. (Shake and vent to release pressure about 4 to 5 times each.) Allow the phases to separate. (Bottom layer is chloroform.) Draw off the bottom layer, transferring the solvent with a funnel containing a plug of sodium sulfate into a tared beaker. (Do not draw off any of the aqueous layer.)

4. After the three chloroform extractions, use two 25 mL portions of chloroform to rinse the sodium sulfate, collecting the rinses in the same tared beaker as the extracts.
5. Next extract the sample three times with 25 mL aliquots of ethyl ether. (Shake and vent to release pressure about 4 to 5 times each.) Allow the phases to separate. (Top layer is ethyl ether.) Draw off the bottom layer (aqueous) into another separatory funnel taking less than 1 mL of the ethyl ether layer with. Decant the ethyl ether, passing it through sodium sulfate and collecting the ethyl ether in the same tared dish as the chloroform.
6. After the three ethyl ether extractions, take two 25 mL portions of ethyl ether and rinse the sodium sulfate collecting the rinses in the same tared beaker as the extracts.
7. Evaporate the solvents (chloroform and ethyl ether) in the tared beaker in the hood at 70 °F or less until no solvent remains. (Use no heat and have no sources of ignition in the hood when doing this procedure.) Do not evaporate so quickly as to allow evaporative cooling to lower the temperature of the container below the dew point of water, otherwise, water will be condensed out in the container.
8. Desiccate to constant weight (two hours). Record and report the final weight to the nearest 0.1 mg on Form LSC-036.

II. Inorganics

If inorganic residue information is required, the following procedure should be conducted:

A. Inorganic Blank Determination

1. Vent the remaining aqueous phase from the organic extraction in the hood to remove residual organic solvents (usually overnight).
2. Decant the impinger catch into a tared evaporating dish.
3. Evaporate all of the water in the sample in an oven at 100 °C. Take care not to boil to prevent bumping and loss of sample.
4. Cool the dried sample in the desiccator and desiccate until a constant weight is obtained.
5. Report the results to the nearest 0.1 mg on Form LSC-036.

B. Inorganic Sample Determination

Follow steps 1-5 in Section A above.

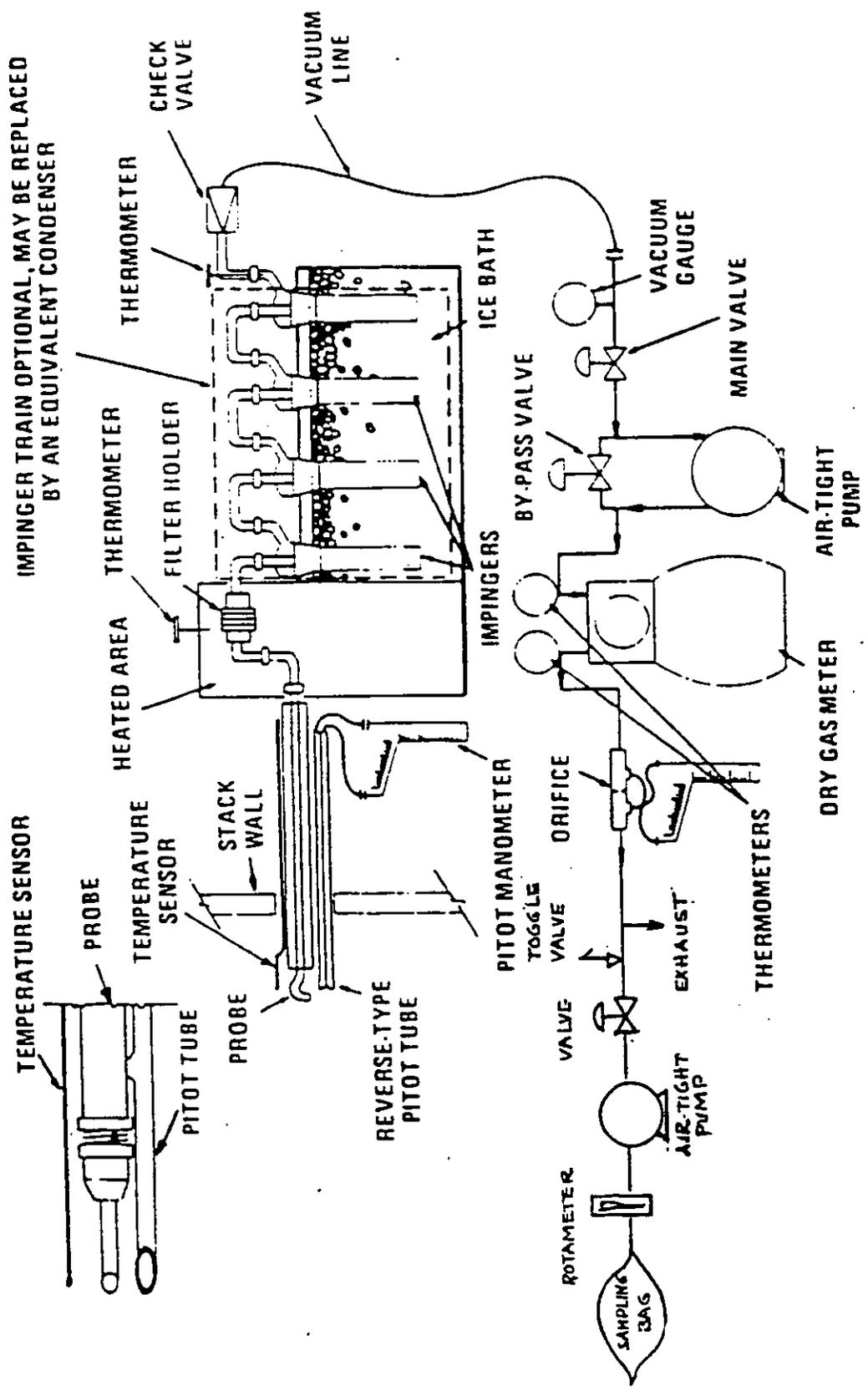
NOTES

1. For the organics determination, in the rare event that the impinger catch resulted from a Modified Method 6 determination (SO_2), whereby the solution contains dilute hydrogen peroxide ($\geq 3\%$), do not use ether as an extraction solvent. Substitute toluene for ethyl ether in Section I. (Ether in the presence of peroxide forms explosive hydroperoxide.)
2. In the organics determination, more than three extractions may be required to extract all of the organics. Additional extractions should be performed if the aqueous phase is still cloudy.
3. Special state requirements:
 - Michigan - Total sample evaporated in tared evaporating dish on steam bath.
 - Iowa - Organics and inorganics separately, as required.
 - Wisconsin - Use Method II-8672-WI.
 - Rest of states - Organics only.

REFERENCES

Proposed Standards of Performance for New Stationary Sources, Federal Register 36(159) Part II, August 1, 1979.

Minnesota Pollution Control Agency, Exhibit C.



IMPINGER TRAIN OPTIONAL, MAY BE REPLACED BY AN EQUIVALENT CONDENSER

Particulate sampling train.

APPENDIX H

CALCULATION EQUATIONS

CALCULATION EQUATIONS

METHOD 2

$$\bar{V}_s = 35.48 C_p (\sqrt{\Delta p})_{avg} \sqrt{\frac{T_{s(avg)}}{P_s M_s}}$$

$$Q_{s,d} = 60(1 - B_{ws}) \bar{V}_s A \left(\frac{528}{T_{s(avg)}}\right) \left(\frac{P_s}{29.92}\right)$$

$$Q_a = 60 \bar{V}_s A$$

$$\dot{m}_g = \frac{4.995 Q_{s,d} G_d}{1 - B_{ws}}$$

$$RH^* = 100 (vp_{twb} + 0.0003641 P_s (T_{db} - T_{wb}))/vp_{tdb}$$

$$B_{ws}^* = RH(vp_{tdb})/P_s$$

$$= \frac{4.585 \times 10^{-2} P_s M_s}{T_s (avg)}$$

*Alternate equations for calculating moisture content from wet bulb and dry bulb data.

SYMBOLS

- A = Cross sectional area of stack, SQ. FT.
- A_n = Cross sectional area of nozzle, SQ. FT.
- B_{ws} = Water vapor in gas stream, proportion by volume
- C_p = Pitot tube coefficient, dimensionless
- C_a = Concentration of particulate matter in stack gas, wet basis, GR/ACF
- C_s = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, GR/DSCF
- EA = Excess air, percent by volume
- γ = Dry test meter correction factor, dimensionless
- G_d = Specific gravity (relative to air), dimensionless
- I = Isokinetic variation, percent by volume
- M_d = Molecular weight of stack gas, dry basis, g/g - mole.
- \dot{m}_g = Mass flow of wet flue gas, LB/HR
- \dot{m}_p = Particulate mass flow, LB/HR
- M_s = Molecular weight of stack gas, wet basis, g/g, mole.
- M_p = Total amount of particulate matter collected, g
- P_{bar} = Atmospheric pressure, IN. HG. (uncompensated)
- P_g = Stack static gas pressure, IN. WC.

- P_s = Absolute pressure of stack gas, IN.HG.
- P_{std} = Standard absolute pressure, 29.92 IN. HG.
- A_a = Actual volumetric stack gas flow rate, ACFM
- $Q_{s,d}$ = Dry volumetric stack gas flow rate corrected to standard conditions, DSCFM
- RH = Relative humidity, %
- T_{db} = Dry bulb temperature of stack gas, °F
- T_{wb} = Wet bulb temperature of stack gas, °F
- $T_{m(avg)}$ = Absolute average dry gas meter temperature, °R
- $T_s(avg)$ = Absolute average stack temperature, °F
- T_{std} = Standard absolute temperature, 528 °F (68 °F)
- θ = Total sampling time, min.
- V_{lc} = Total volume of liquid collected in impingers and silica gel, ml
- V_m = Volume of gas sample as measured by dry gas meter, CF
- $V_m(std)$ = Volume of gas sample measured by the dry gas meter corrected to standard conditions, DSCF
- $V_w(std)$ = Volume of water vapor in the gas sample corrected to standard conditions, SCF
- \bar{V}_s = Average actual stack gas velocity, FT/SEC
- v_{Ptdb} = Vapor pressure at T_{db} , IN. HG.

$v_{p_{twb}}$ = Vapor pressure at T_{wb} , IN. HG

$\overline{\Delta H}$ = Average pressure differential across the orifice meter, IN. WC.

ΔP = Velocity pressure of stack gas, IN. WC.

γ = Dry test meter correction coefficient, dimensionless

ρ = Actual gas density, LB/ACF

CALCULATION EQUATIONS

METHOD 3

$$\%EA = \frac{100(\%O_2 -) - .5\% CO}{0.264\% N_2 - \%O_2 + 0.5\% CO}$$

$$M_d = 0.44(\%CO_2) + 0.32 (\%O_2) + 0.28 (\%N_2 + \%CO)$$

$$M_s = M_d (I - B_{ws}) + 0.18 B_{ws}$$

$$B_{ws} = \frac{V_{w(std)}}{V_{w(std)} + V_{m(std)}}$$

CALCULATION EQUATIONS

METHOD 5

$$V_{m(\text{std})} = 17.65 V_m \gamma \left(\frac{P_{\text{bar}} + \overline{\Delta H}/13.6}{T_{m(\text{avg})}} \right)$$

$$V_{w(\text{std})} = 0.0472 V_{I_s}$$

$$B_{ws} = \frac{V_{w(\text{std})}}{V_{w(\text{std})} + V_{m(\text{std})}}$$

$$I = 0.0944 \left(\frac{T_{s(\text{avg})} V_{m(\text{std})}}{P_s V_s A_n \theta (1 - B_{ws})} \right)$$

$$C_s = \frac{15.43 M_p}{V_{m(\text{std})}}$$

$$C_a = \frac{272.3 M_p P_s}{T_{s(\text{avg})} (V_{w(\text{std})} + V_{m(\text{std})})}$$

$$(\dot{m}_p)_1 = 8.5714 \times 10^{-3} C_s Q_{s,d}$$

$$(\dot{m}_p)_2 = \frac{1.3228 \times 10^{-1} M_p A}{0 A_n}$$

$$\dot{m}_p = \frac{(\dot{m}_p)_1 + (\dot{m}_p)_2}{2}$$

SYMBOLS

- A = Cross sectional area of stack, SQ. FT.
- A_n = Cross sectional area of nozzle, SQ. FT.
- B_{ws} = Water vapor in gas stream, proportion by volume
- C_p = Pitot tube coefficient, dimensionless
- C_a = Concentration of particulate matter in stack gas, wet basis, GR/ACF
- C_s = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, GR/DSCF
- EA = Excess air, percent by volume
- γ = Dry test meter correction factor, dimensionless
- G_d = Specific gravity (relative to air), dimensionless
- I = Isokinetic variation, percent by volume
- M_d = Molecular weight of stack gas, dry basis, g/g - mole.
- \dot{m}_g = Mass flow of wet flue gas, LB/HR
- \dot{m}_p = Particulate mass flow, LB/HR
- M_s = Molecular weight of stack gas, wet basis, g/g, mole.
- M_p = Total amount of particulate matter collected, g
- P_{bar} = Atmospheric pressure, IN. HG. (uncompensated)
- P_g = Stack static gas pressure, IN. WC.

- P_s = Absolute pressure of stack gas, IN.HG.
- P_{std} = Standard absolute pressure, 29.92 IN. HG.
- A_a = Actual volumetric stack gas flow rate, ACFM
- $Q_{s,d}$ = Dry volumetric stack gas flow rate corrected to standard conditions, DSCFM
- RH = Relative humidity, %
- T_{db} = Dry bulb temperature of stack gas, °F
- T_{wb} = Wet bulb temperature of stack gas, °F
- $T_{m(avg)}$ = Absolute average dry gas meter temperature, °R
- $T_s(avg)$ = Absolute average stack temperature, °F
- T_{std} = Standard absolute temperature, 528 °F (68 °F)
- θ = Total sampling time, min.
- V_{lc} = Total volume of liquid collected in impingers and silica gel, ml
- V_m = Volume of gas sample as measured by dry gas meter, CF
- $V_m(std)$ = Volume of gas sample measured by the dry gas meter corrected to standard conditions, DSCF
- $V_w(std)$ = Volume of water vapor in the gas sample corrected to standard conditions, SCF
- \bar{V}_s = Average actual stack gas velocity, FT/SEC
- $v_{p_{tdb}}$ = Vapor pressure at T_{db} , IN. HG.

$v_{p_{twb}}$ = Vapor pressure at T_{wb} , IN. HG

$\overline{\Delta H}$ = Average pressure differential across the orifice meter, IN. WC.

ΔP = Velocity pressure of stack gas, IN. WC.

γ = Dry test meter correction coefficient, dimensionless

ρ = Actual gas density, LB/ACF

APPENDIX I

SAMPLING TRAIN CALIBRATION DATA

INTERPOLL LABORATORIES
EPA Method 5 Gas Metering System
Quality Control Check Data Sheet

Job T.A. Schiffsky
 Operator J.H.

Date 6/17/93
 Module No. 6

Instructions: Operate the control module at a flow rate equal to ΔH for 10 minutes before attaching the umbilical. Record the following data:

Bar press 28.70 in. Hg. $\tau =$.9979 $\Delta H =$ 1.79 in. W.C.

Time (min)	Volume (CF)	Meter Temp. (°F)	
		Inlet	Outlet
	(226.20)		
2.5	228.09	73	71
5.0	230.02	74	71
7.5	231.85	76	73
10	233.74	77	73
	$V_m = 7.54$	Avg(t_m) = 73.56 °F	

Calculate Y_{cn} as follows:

$$Y_{cn} = \frac{1.786}{\tau V_m} \left[\frac{(t_m + 460)}{P_b} \right]^{0.5}$$

$$Y_{cn} = \frac{1.786}{(.9979)(7.54)} \left[\frac{(73.50) + 460}{(28.70)} \right]^{0.5}$$

$$Y_{cn} = \underline{1.02}$$

If Y_{cn} is not within the range of 0.97 to 1.03, the volume metering system should be investigated before beginning.

CFR Title 40, Part 60, Appendix A, Method 5, Section 4.4.1

Interpoll Laboratories, Inc.
(612) 786-6020

Meter Box Calibration and Usage Status

Date of Report: June 22, 1993

Meter Box No. : 6 (Rockwell Dry Test Meter Serial No. 712852)

Date of Last Calibration: May 7, 1993

Calibration Technician: D. Brennan

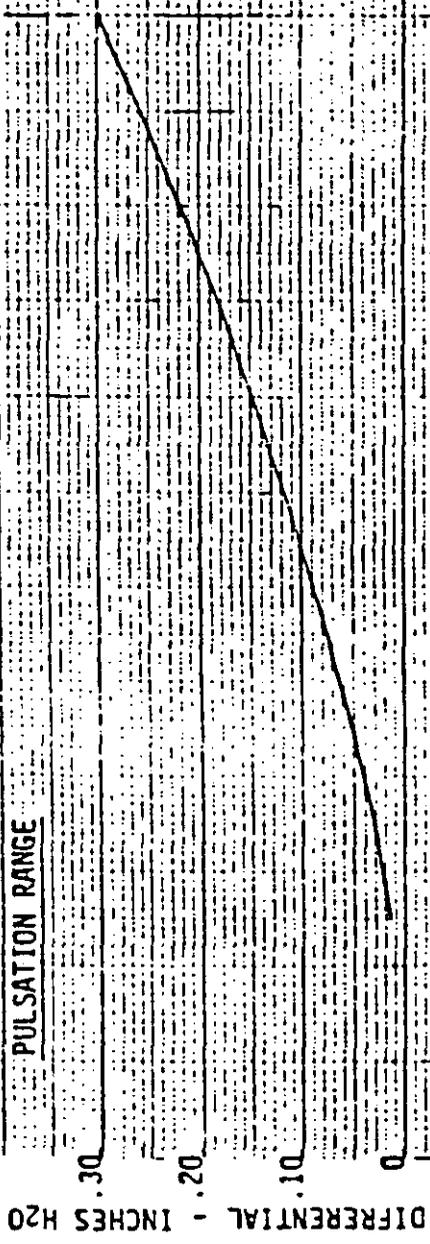
Wet Test Meter No.: American Meter AL-20

Date of Use	Report No.	Initial Meter Reading	Final Meter Reading	Volume/Job (cu. ft.)	Total Volume* (cu. ft.)
May 13, 1993	3-8767	207.50	435.80	228.30	228.30
May 19, 1993	3-8844	436.00	588.20	152.20	380.50
May 25, 1993	3-8918	591.70	846.45	254.75	635.25
June 4, 1993	3-8985	846.90	1008.07	161.17	796.42
June 15, 1993	3-9131	1009.40	1225.33	215.93	1012.35
June 21, 1993	3-9190	1226.20	1363.70	137.50	1149.85

* Total volume through meter since last calibration.

DIFFERENTIAL PRESSURE AND PROOF CALIBRATION CURVES

WET TEST METER

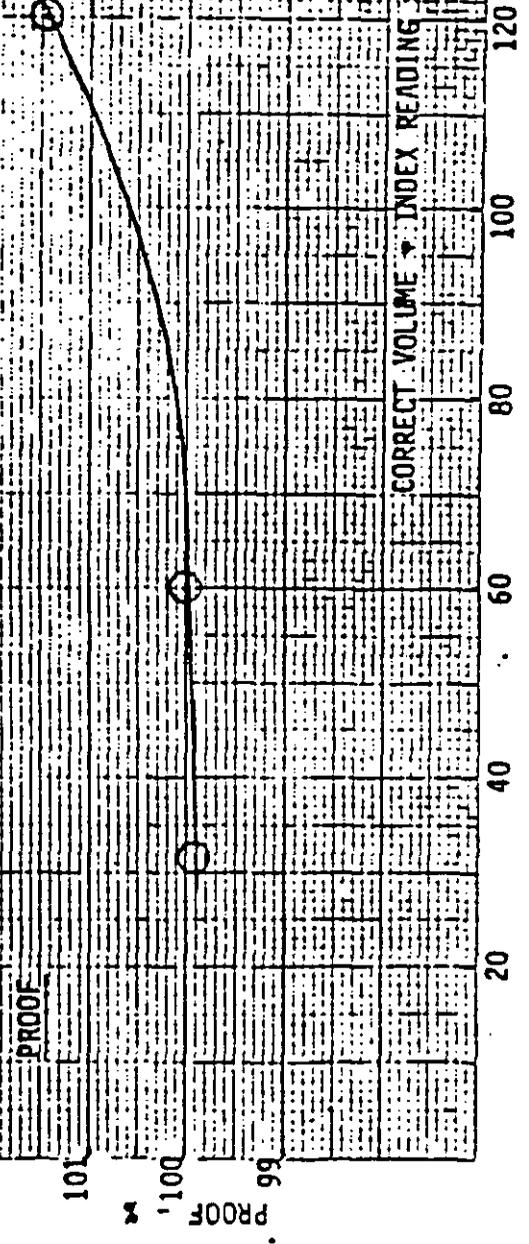


PULSATION RANGE

Calibrated with a 10 Ft. American Bell Prover, Serial No. 3157. Traceable to the Bureau of Standards. Reference No. 5249068, PI-TAPE.

AL-20 American Wet Test Meter
Serial No. p-717

Stainless Steel w/Removable Back
Calibrated w/Saturated Air
Water Temp. 74° F.
Air Temp. 74° F.
Inlet Pressure 2" H₂O Constant
Calibration Rate: 60 CFH/HR.
Capacity Rate: 120 CFH/HR.
Restricted Outlet for Rate Deviation



CORRECT VOLUME + INDEX READING x PROOF + 100

FLOW RATE - CUBIC FEET OF AIR PER HOUR

DAVID BANKS

November, 1991

Interpoll Laboratories, Inc.
(612) 786-6020

**Nozzle Calibration
Data Sheet**

Date of Calibration: 6-21-93

Nozzle Number 7-4

Technician: Duane Van Hoever

The nozzle is rotated in 60 degree increments and the diameter at each point is measured to the nearest 0.001 inch. The observed readings and average are shown below.

Position	Diameter (inches)
1	.245
2	.245
3	.246
Average:	.245

Interpoll Laboratories, Inc.

Temperature Measurement Device
Calibration Sheet

Unit under test:

Vendor Beckman Industrial
 Model HD 110 T Serial Number POT #18
 Range -1999 °F Thermocouple Type K
 Date of Calibration 4/7/93 Technician D. VAN HOEVER

Method of Calibration:

- Comparison against ASTM mercury in glass thermometer using a thermostatted and insulated aluminum block designed to provide uniform temperature. The temperature is adjusted by adjusting the voltage on the block heater cartridge.
- Omega Model CL-300 Type K Thermocouple Simulator which provides 22 precise temperature equivalent millivolt signals. The CL-300 is cold junction compensated. Calibration accuracy is $\pm 0.1\%$ of span (2100 °F) ± 1 degree (for negative temperatures add ± 2 degrees. The CL-300 simulates exactly the millivoltage of a Type K thermocouple at the indicated temperature.

Desired Temp (°F) Nominal	Temperature of Standard or Simulated Temp (°F)	Response of Unit Under Test (°F)	Deviation	
			Δt (°F)	(%)
0		0	0	0
100		96	4	.71
200		199	1	.15
300		298	2	.26
400		395	5	.58
500		495	5	.52
600		597	3	.28
700		698	2	.25
800		803	3	.24
900		906	6	.38
1000		1011	11	.75
1100		1114	14	.89
1200		1220	20	1.20
1300		1321	21	1.19
1400		1426	26	1.39
1500		1524	24	1.22
1600		1625	25	1.21
1700		1721	21	.97
1800		1819	19	.84
1900		1912	12	.51
2000				
2100				
		Averages:		.68

OF = off scale response by unit under test (°F)
 $\% \text{ dev} = 100 \Delta t / (460 + t)$

- Unit in tolerance
- Unit was not in tolerance: recalibrated - See new calibration sheet.

S-Type Pitot Tube Inspection Sheet

Pitot No. 23-4

Pitot tube dimensions:

- 1. External tubing diameter (D_t) 1.314 IN.
- 2. Base to Side A opening plane (P_A) 1.460 IN.
- 3. Base to Side B opening plane (P_B) 1.460 IN.

Alignment:

- 4. $\alpha_1 < 10^\circ$ 0
- 5. $\alpha_2 < 10^\circ$ 0
- 6. $B_1 < 5^\circ$ 1
- 7. $B_2 < 5^\circ$ 1
- 8. $Z < .125"$.03
- 9. $W < .0625"$.03

Distance from Pitot to Probe Components:

- 10. Pitot to 0.500 IN. nozzle 1.755 IN.
- 11. Pitot to probe sheath 3.00 IN.
- 12. Pitot to thermocouple (parallel to probe) 3.00 IN.
- 13. Pitot to thermocouple (perpendicular to probe) 1.760 IN.

- Meets all EPA design criteria thus $C_p = 0.84$
- Does not meet EPA design criteria - thus calibrate in wind tunnel
 $C_p =$ _____

Date of Inspection:

Inspected by:

4-7-93

[Signature]

INTERPOLL LABORATORIES
 (612)786-6020
 Stack Sampling Department - QA
 Aneroid Barometer Calibration Sheet

Date 4/7/93
 Technician D Van Hoever
 Mercury Column Barometer No. _____
 Aneroid Barometer No. 861216

Actual Mercury Barometer Read	Ambient Temp.	Temperature Correction Factor	Adjusted Mercury Barometer Read	Initial Aneroid Barometer Read	Difference (P _{ba} -P _{bm})
29.11	72	.110	29.00	28.94	.06

Has this barometer shown any consistent problems with calibration? Yes/No. If yes, explain. NO

Has problem been alleviated? Yes/No. How? _____

***Note**

Aneroid barometers will be calibrated periodically against a mercury column barometer. The aneroid barometer to be calibrated should be placed in close proximity to the mercury barometer and left to equilibrate for 20-30 minutes before calibrating. Aneroid barometer will be calibrated to the adjusted mercury barometer readings.

APPENDIX J

MPCA TEST PLAN AND PROTOCOL

Minnesota Pollution Control Agency
Division of Air Quality
Stack Testing Protocol

The following is a summary of the testing requirements for the facility owned by T.A. Schifsky and Sons:

I. Test Methods

- A. EPA Method 1 for the location of sampling ports and points. Location of the sampling ports must be approved before the test.

Check for cyclonic flow must be done whenever there is a cyclonic type of device directly upstream of the sampling location. Correction of cyclonic flow by straightening vanes must also be verified by checking the cyclonic flow before the test.

If the location does not meet the minimum requirements in Method 1, the testing firm must conduct the flow pattern evaluation and testing according to the alternative procedures in part 2.5 of EPA Method 1 (Three-dimensional directional probe).

- B. EPA Method 2 for velocity and volumetric flow rate. Three determinations: one measurement concurrently with each test run for pollutant.
- C. EPA Method 3 for gas analysis. Three determinations: one measurement on an integrated sample taken concurrently with each test run for pollutant.
- D. EPA Method 4 for the determination of moisture in the flue gases. Three determinations: one measurement concurrently with each test for pollutant.
- E. EPA Method 5 as amended in Exhibit C and Minn. Rules 7005.0500 for the determination of particulate matter emissions. Three one-hour determinations are required. The sampling time for each run must be at least 60 minutes and the sampling rate must be at least 0.9 dscm/hr (0.53 dscf/min). Report the results as dry catch only, and wet and dry catch separately.
- F. EPA Method 9 for the determination of visible emissions as amended in Minn. Rules part 7005.1860. One hour of opacity readings are required.

AQD File No.: 104

NOTE: The protocol, testplan, and information required in Exhibit C shall be submitted as part of the performance test report. Please note the new Asphalt Plant Operating Conditions During Stack Testing Sheet.

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JUN 16 1993

INTERPOLL LABORATORIES

TEST PLAN

I. GENERAL INFORMATION

Permittee: Schifsky, T.A. and Sons

Permittee's contact person and telephone number: Tom Schifsky 777-1313

Permittee's mailing address: 2370 Highway 36 North St. Paul, Mn. 55109

DAQ File No.: 104

MPCA permitting engineer: Jerry Liefert

Applicable regulations for each source tested (be specific): Mn. Rules pts. 7005.1860, 7005.2030, 7005.2040 for PM and opacity.

Reason for testing:

Is this test for initial compliance demonstration: Yes

Drawings showing location of sampling ports included: To be submitted

Location of the plant at the time of the test: North St. Paul

Date when test plan was discussed and agreed upon with the permittee, or Pre-test meeting needed: Pre-test meeting to be scheduled by Permittee.

II. NOTIFICATION REQUIREMENTS:

The permittee must contact the Agency at least two weeks before the scheduled test to have a pre-test meeting and obtain all necessary approvals, unless prior agreement is reached.

It is very important to allow at least two weeks before the test to review the testing requirements in order to avoid last minute cancellations due to inadequate testing conditions.

Among the potential problems that may need to be solved before the test are:

1. Unsuitable location of sampling ports. The stack may need to be extended and/or straightening vanes be installed.
2. Permittee must schedule the test at a time when the plant can be operated at 100% of rated capacity, and at maximum recycle rate if applicable. If the plant is tested at less than 100% of capacity, the Permittee will be required to limit production to the tested rate.
3. Permittee must be ready to burn specified fuel.
4. Permittee may have to install pressure drop taps and gauges.
5. ~~Permittee may have to install sampling taps on the line feeding fuel to the burner.~~

III. TEST PLAN

The following is the test plan developed for the Standard Steel Corp. plant.

- A. Emission point(s) to be tested: Exhaust stack for fabric filter
- B. Parameters to be tested at each emission point: PM and opacity for Emission Point 1.

C. ~~Fuel sampling and analysis (Fuel oils and used oil)~~

~~This is part of the compliance demonstration requirements. Please note that the test report will not be accepted without complete submittal of fuel analysis results of samples taken at the time of the test.~~

- 1. Sampling. One tap sample per particulate test run must be taken. The sample must be taken as close as possible to the burner, (somewhere in feeding line) to be representative of the fuel burned at the time of the test. The sample may be taken in a pint-size clean container, and according to the procedures in Exhibit D. Mix the three samples taken into a composite.
- 2. Analysis. The composite must be analyzed as specified in Exhibit D.

D. Moisture content in the virgin aggregate

- 1. Take two samples the virgin aggregate per test run of particulates. Sample must be taken as close as possible to the feeding conveyor and during the corresponding run. Mix the two samples of virgin aggregate, this will give one composite sample per test run.
- 2. Perform one analysis of moisture content in each composite sample as per ASTM or other recognized methodologies. A total of three analysis shall be performed, one per test run for particulates.

E. Operating Conditions during the Test

- 1. Operation must be at 100% of design capacity at the existing aggregate moisture content - no deliberate reduction of feed rate or fan speed during testing, except for nominal damper adjustment for proper combustion. - The test report must include copies of the manufacturer's specifications that define the design capacity of the plant as a function of the moisture content of the aggregate. If circumstances cause operation of the plant to be less than 100% during the test, the Permittee will be required to limit production to the tested rate.
- 2. Must burn 100% of the highest emitting fuel to be listed in and allowed by the permit: No. 2 fuel oil
- 3. If normal operation of the plant will be with recycling of collected PM from the baghouse into the dryer, the test must be conducted under the same conditions.

F. Operating Data to Be Recorded during the Test

Operating data must be recorded during the test in its entirety i.e., particulates and visible emission observations. Operating data must be recorded every fifteen minutes. Please use the attached data sheet or equivalent.

Note: No test report will be accepted without a complete data sheet included.

1. During testing the following measurements must be made:

- a) Pressure drop across the baghouse.
- b) Virgin aggregate input (ton per hour) as well as asphalt input (ton per hour). Provide the manufacturer's rating of the asphalt plant at different moisture contents in the aggregate.
- c) Moisture content of the aggregate.

2. Please provide the following data:

- a) Average fuel consumption rate (calculated or measured) and type
- b) Cleaning cycles of the baghouse
- c) Operating data sheet enclosed

G. Testing schedules and testing firm: Test shall be conducted by June 30, 1993 by a firm acceptable to the MPCA

H. Permitting engineer to witness the test: No