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**Title: Test Report For Air Pollution Source Testing At Macasphalt,  
Melbourne, Florida,  
Ramcon Environmental Corporation, Memphis, TN,  
December 2-4, 1992.**

Test Report for Air Pollution Source Testing

at

**MACASPHALT  
MELBOURNE, FLORIDA**

and

**NATIONAL ASPHALT PAVEMENT ASSOCIATION  
5100 FORBES BLVD., NAPA BUILDING  
LANHAM, MARYLAND**

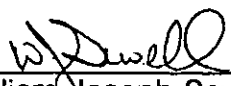
submitted by:

**RAMCON ENVIRONMENTAL CORPORATION  
6707 FLETCHER CREEK COVE  
MEMPHIS, TENNESSEE 38133**

December 2-4, 1992

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Mr. Tom Brumagin  
National Asphalt Pavement  
Association

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William Joseph Sewell, II  
Vice President

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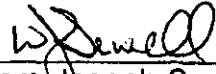
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## I. INTRODUCTION

On January 2, 3 and 4, 1993, personnel from RAMCON Environmental Corporation conducted source emissions determinations at Macasphalt located in Melbourne, Florida. The testing was conducted according to the National Asphalt Pavement Association (NAPA) guidelines entitled, "Protocol for Air Pollution Source Testing".

The scope of work involved testing this facility for filterable and condensible particulate matter, formaldehyde, and polynuclear aromatic hydrocarbons. These compounds were sampled according to specified isokinetic testing procedures. Reference Method 202 was employed for the particulate matter including condensibles. Method 0011/8315 issued in SW-846 was utilized for the formaldehyde extraction, collection, and analysis. The polynuclear aromatic hydrocarbons were sampled using Modified Method 5.

In addition, "real-time" continuous emission monitor (CEM) instrumentation was utilized to conduct on-site analysis for oxygen, carbon dioxide, total volatile organics, sulfur dioxide, carbon monoxide, and NOx. Reference Methods 3A, 6C, 7E, 10, and 25A were employed for the analysis of oxygen and carbon dioxide, sulfur dioxide, nitrogen oxides, carbon monoxide, and total hydrocarbons respectively. These testing procedures utilize a sampling system to continuously extract sample gas from the source. This sample stream is routed to individual CEM's for analysis of the various targeted pollutants and diluent gases. The test results are based on the average value of one minute averages generated by the CEM instrument data acquisition during the test periods.

Methane, benzene, toluene, ethyl benzene, and xylene compounds were analyzed on a semi-continuous basis by employing a gas chromatograph to the sampling location. Reference Method 18 was used for these determinations. The gas stream is continuously sampled during the testing period(s). Periodically, a sample of the extracted gas stream is injected into the gas chromatograph for analysis. The test results are based on the average value of the injections performed during each test period.

Additionally stack gas moisture, velocity, and volumetric flow rate were determined to provide data enabling conversion of flue gas concentrations to emission data. These determinations were conducted in conjunction with each of the isokinetic testing procedures.

Where possible, the testing was conducted simultaneously. This provides correlations of the various stack effluents relationships with one another. Three (3) test runs were conducted for each isokinetic testing procedure. Eleven test runs were conducted utilizing the CEM instrumental procedures for SO<sub>2</sub>, CO, THC, NO<sub>x</sub>, CO<sub>2</sub>, and O<sub>2</sub>. Nine (9) test periods were conducted for the semi-continuous GC procedure.

The purpose of the testing project was to provide air emissions information for developing a database of information using various types of hot mix asphalt plants.

Mr. Thomas E. Brumagin representing the National Asphalt Pavement Association was present during the testing procedure(s) conducted by RAMCON Environmental Corporation.

## II. TEST RESULTS

The test results are summarized in Tables I through III. Each summary table represents the test results for particulate, formaldehyde, and PAH's respectively. The gaseous pollutants of interest, THC, SO<sub>2</sub>, CO<sub>2</sub>, CO, NO<sub>x</sub>, O<sub>2</sub>, CH<sub>4</sub>, and BTEX, test results are listed in each summary table. The test results for these gaseous compounds listed on each summary table were correlated to the isokinetic tests according to date and times. This provides a direct comparison of the test data for a specific targeted pollutant to other operational and emission data.

The summary tables provide the test results in concentration values of milligrams per dry standard cubic meter (mg/dscm) and parts per million (ppm), volume basis. The emission values of all targeted compounds are listed in pounds per hour (lb/hr).

TABLE I - Summary of Results

Test Performed: Run No.: Date: Time: Production Rate: Amount of RAP:	Part. 1	Part. 2	Part. 3	Part. Average	Part. 1	Part. 2	Part. 3	Part. Average	Part. 1	Part. 2	Part. 3	Part. Average
	12-02-02 1418-1521 154	12-03-92 1459-1618 153	12-04-92 0826-1058 146	Average	12-02-02 1418-1521 154	12-03-92 1459-1618 153	12-04-92 0826-1058 146	Average	12-02-02 1418-1521 154	12-03-92 1459-1618 153	12-04-92 0826-1058 146	Average
	tph	tph	tph	%	tph	tph	tph	%	tph	tph	tph	%
Volumetric Flow Rate (acfm)	44975	43624	42933	43844	44975	43624	42933	43844	44975	43624	42933	43844
Volumetric Flow Rate (dscfm)	25452	26549	25721	25907	25452	26549	25721	25907	25452	26549	25721	25907
Stack Temperature (°F)	272	264	264	267	272	264	264	267	272	264	264	267
Percent Moisture	21.78	16.83	18.07	18.89	21.78	16.83	18.07	18.89	21.78	16.83	18.07	18.89
% CO <sub>2</sub>	5.5	4.2	4.8	4.8	5.5	4.2	4.8	4.8	5.5	4.2	4.8	4.8
% O <sub>2</sub>	14.4	15.1	15.1	14.9	14.4	15.1	15.1	14.9	14.4	15.1	15.1	14.9
% CO	0.007	0.005	0.007	0.006	0.007	0.005	0.007	0.006	0.007	0.005	0.007	0.006
% Excess Air	213.3	243.3	249.6	235.4	213.3	243.3	249.6	235.4	213.3	243.3	249.6	235.4
	mg/m <sup>3</sup>				ppm				lbs/hr			
CO	80.3	61.2	80.9	74.1	68.9	52.5	69.4	63.6	7.63	6.07	7.77	7.16
SO <sub>2</sub>	398.4	353.9	317.1	356.5	149.5	132.8	119.0	133.87	37.88	35.10	30.47	34.48
NO <sub>x</sub>	254.3	243.6	267.6	255.2	132.9	127.3	139.8	133.3	24.18	24.16	25.71	24.68
Total Hydrocarbon (as CH <sub>4</sub> )	66.4	50.4	64.4	60.4	99.5	75.5	96.7	90.6	6.32	5.00	6.20	5.84
Methane	6.60	0.37	6.02	4.33	9.88	0.57	9.02	6.49	0.63	0.04	0.58	0.42
Benzene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Toluene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Ethyl Benzene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Xylene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Particulate Matter	130.9	122.2	162.8	138.6	N/A	N/A	N/A	N/A	12.46	12.13	15.65	13.41
Condensable Particulate	89.2	40.8	79.6	69.9	N/A	N/A	N/A	N/A	8.49	4.05	7.65	6.73

TABLE II - Summary of Results

Test Performed: Run No.: Date: Time: Production Rate: Amount of RAP:	Form. 1	Form. 2	Form. 3	Form. Average	Form. 1	Form. 2	Form. 3	Form. Average	Form. 1	Form. 2	Form. 3	Form. Average
	12-04-92 1149-1304 134	12-04-92 1303-1404 151	12-04-92 1448-1602 150	tph %	12-04-92 1149-1304 134	12-04-92 1303-1404 151	12-04-92 1448-1602 150	tph %	12-04-92 1149-1304 134	12-04-92 1303-1404 151	12-04-92 1448-1602 150	tph %
Volumetric Flow Rate (acfm)	41638	47542	44796	44658	41638	47542	44796	44658	41638	47542	44796	44658
Volumetric Flow Rate (dscfm)	24469	27036	25632	25712	24469	27036	25632	25712	24469	27036	25632	25712
Stack Temperature (°F)	268	284	264	272	268	284	264	272	268	284	264	272
Percent Moisture	19.19	20.08	21.75	20.34	19.19	20.08	21.75	20.34	19.19	20.08	21.75	20.34
% CO <sub>2</sub>	4.8	4.8	4.7	4.8	4.8	4.8	4.7	4.8	4.8	4.8	4.7	4.8
% O <sub>2</sub>	15.0	15.0	15.3	15.1	15.0	15.0	15.3	15.1	15.0	15.0	15.3	15.1
% CO	.014	.014	.017	.015	.014	.014	.017	.015	.014	.014	.017	.015
% Excess Air	242.8	242.8	262.6	249.4	242.8	242.8	262.6	249.4	242.8	242.8	262.6	249.4
	mg/m <sup>3</sup>				ppm <sub>v</sub>				lbs/hr			
CO	161.2	161.2	201.4	174.6	138.4	138.4	172.9	149.9	14.74	16.29	19.29	16.77
SO <sub>2</sub>	389.4	389.4	346.2	375.0	146.1	146.1	129.9	140.7	35.59	39.33	33.15	36.02
NO <sub>x</sub>	245.2	245.2	212.8	234.4	128.1	128.1	111.2	122.5	22.41	24.76	20.38	22.52
Total Hydrocarbon (as CH <sub>4</sub> )	79.7	80.5	95.6	85.3	119.4	120.7	143.3	127.8	7.28	8.13	9.16	8.19
Methane	4.18	14.02	15.01	11.1	6.27	21.02	22.50	16.60	0.38	1.42	1.44	1.08
Benzene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Toluene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Ethyl Benzene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Xylene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Formaldehyde	0.046	3.210	0.459	1.238	0.04	2.6	0.3	1.0	0.004	0.32	0.04	0.121



TABLE III-A — Summary of Results

Test Performed: Run No.: Date: Time: Production Rate: Amount of RAP:	PAH 1 12-03-92 1025-1222 142	PAH 2 12-03-92 1255-1639 153	PAH 3 12-04-92 0811-1126 149	PAH Average tph %	PAH 1 12-03-92 1025-1222 142	PAH 2 12-03-92 1255-1639 153	PAH 3 12-04-92 0811-1126 149	PAH Average tph %	PAH 1 12-03-92 1025-1222 142	PAH 2 12-03-92 1255-1639 153	PAH 3 12-04-92 0811-1126 149	PAH Average tph %
	mg/m <sup>3</sup>				ppm <sub>v</sub>				lbs/hr			
Volumetric Flow Rate (acfm)	48903	47642	46984	47843	48903	47642	46984	47843	48903	47642	46984	47843
Volumetric Flow Rate (dscfm)	28197	28131	27299	27875	28197	28131	27299	27875	28197	28131	27299	27875
Stack Temperature (°F)	280	266	266	270	280	266	266	270	280	266	266	270
Percent Moisture	19.46	19.08	20.32	19.62	19.46	19.08	20.32	19.62	19.46	19.08	20.32	19.62
% CO <sub>2</sub>	4.6	4.5	4.8	4.6	4.6	4.5	4.8	4.6	4.6	4.5	4.8	4.6
% O <sub>2</sub>	14.4	14.9	15.1	14.8	14.4	14.9	15.1	14.8	14.4	14.9	15.1	14.8
% CO	0.004	0.005	0.007	0.005	0.004	0.005	0.007	0.005	0.004	0.005	0.007	0.005
% Excess Air	206.1	233.5	249.6	229.7	206.1	233.5	249.6	229.7	206.1	233.5	249.6	229.7
	mg/m <sup>3</sup>				ppm <sub>v</sub>				lbs/hr			
CO	51.6	58.4	80.9	63.6	44.3	50.1	69.4	54.6	5.44	6.13	8.25	6.60
SO <sub>2</sub>	399.8	363.0	317.1	359.9	150.0	136.2	119.0	135.0	42.11	38.15	32.34	37.53
NO <sub>x</sub>	274.8	249.9	267.6	264.1	143.6	130.6	139.8	138.0	29.0	26.27	27.29	27.52
Total Hydrocarbon (as CH <sub>4</sub> )	67.0	52.2	66.3	61.8	100.6	78.2	99.4	92.7	7.06	5.49	6.76	6.43
Methane	BDL	0.38	6.19	2.19	BDL	0.58	9.27	3.28	BDL	0.04	0.63	0.22
Benzene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Toluene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Ethyl Benzene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Xylene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL

TABLE III-B - Summary of Results

Test Performed: Run No.: Date: Time: Production Rate: Amount of RAP:	PAH 1	PAH 2	PAH 3	PAH Average	PAH 1	PAH 2	PAH 3	PAH Average	PAH 1	PAH 2	PAH 3	PAH Average	PAH 1	PAH 2	PAH 3	PAH Average
	12-02-92 1025-1222 142	12-03-92 1255-1639 153	12-04-92 0811-1126 149	Average tph %	12-02-92 1025-1222 142	12-03-92 1255-1639 153	12-04-92 0811-1126 149	Average tph %	12-02-92 1025-1222 142	12-03-92 1255-1639 153	12-04-92 0811-1126 149	Average tph %	12-02-92 1025-1222 142	12-03-92 1255-1639 153	12-04-92 0811-1126 149	Average tph %
PAH's	mg/m <sup>3</sup>				ppm				lbs/hr							
Naphthalene	0.0564	0.0489	0.0843	0.0632	0.0106	0.0092	0.0158	0.0119	0.0060	0.0052	0.0086	0.0066	0.0060	0.0052	0.0086	0.0066
2-Methylnaphthalene	0.0815	0.0711	0.1002	0.0843	0.0138	0.0120	0.0170	0.0143	0.0086	0.0075	0.0103	0.0088	0.0086	0.0075	0.0103	0.0088
2-Chloronaphthalene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Acenaphthylene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Fluorene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Phenanthrene	BDL	0.0691	0.0380	0.0357	BDL	0.0093	0.0051	0.0048	BDL	0.0073	0.0039	0.0037	BDL	0.0073	0.0039	0.0037
Anthracene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Fluoranthene	0.0144	0.0698	0.0203	0.0348	0.0017	0.0083	0.0024	0.0041	0.0015	0.0074	0.0021	0.0037	0.0015	0.0074	0.0021	0.0037
Pyrene	0.0187	0.1937	0.0233	0.0786	0.0022	0.0231	0.0028	0.0094	0.0020	0.0204	0.0024	0.0083	0.0020	0.0204	0.0024	0.0083
Benzo(a)anthracene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Chrysene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Benzo(b)fluoranthene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Benzo(k)fluoranthene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Benzo(e)pyrene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Benzo(a)pyrene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Perylene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Indeno(1,2,3-cd)pyrene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Dibenz(a,h)anthracene	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL	BDL
Benzo(g,h,i)perylene	0.0054	BDL	BDL	0.0018	0.0005	BDL	BDL	0.0002	0.0006	BDL	BDL	0.0002	0.0006	BDL	BDL	0.0002
Total PAH's	0.1764	0.4526	0.2661	0.2966	0.0288	0.0619	0.0431	0.0445	0.0187	0.0478	0.0273	0.0311	0.0187	0.0478	0.0273	0.0311

### III. SAMPLING & ANALYTICAL PROCEDURES

The following is a description of each of the test methods that were conducted during the performance test(s). In this description, a discussion of the pertinent segments including preparation, sampling, and analysis is addressed. This section will provide information supporting the validity of the samples.

#### A. Determination of Carbon Dioxide and Oxygen Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 3A:

The collection and analysis of carbon dioxide and oxygen content at the test location was performed by US EPA Reference Method 3A. This procedure utilizes continuous emissions monitors that provide the data results from the source on a "real-time" or instantaneous basis.

All of the CEM instrumental procedures that were conducted at the outlet testing location were extracted and analyzed with similar testing strategies. Because of this similarity, a detailed description of the calibration and operation procedures of the CEM procedures is provided in the discussion of Method 3A and is referred to in the other sections concerning the additional procedures.

##### 1. Calibration.

The calibration of the instruments is performed using certified gas standards composed of a known concentration of carbon dioxide and oxygen in zero grade nitrogen. These gas standards are prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis certificate for each of the certified gas mixtures used during the testing is included in the test report.

The oxygen instrument utilizes a paramagnetic detector and the carbon dioxide instrument utilizes a nondispersive infrared detector. The minimum detection limit for both gas analyzers is 0.1 %. The fullscale limitations of the oxygen and carbon dioxide analyzers is 25 and 20 % respectively.

Immediately prior to each compliance test series, a complete calibration of the instrument is performed. Each instrument has zero grade nitrogen injected into it and the zero potentiometer is adjusted, if necessary, until the proper voltage output from the analyzer is achieved.

Then a high range pollutant gas mixture, that has been prepared in the specified range percentage of the span or fullscale, is injected. After the system stabilizes, the span or fullscale potentiometer is adjusted until the voltage output from analyzer corresponds to the certification of analysis for the respective calibration gas.

When this procedure is complete and the system has responded properly to a zero and fullscale reading, a mid and/or low range certified calibration gas is injected into the system. No adjustments are made to the system except to achieve proper flow rate through the analyzer. The analyzer, after reaching a stable value, must correspond to the certified value of the calibration gas within a specified percentage of the fullscale.

This mid range calibration gas serves two purposes of quality control and quality assurance. The first is to show that the instrument analyzes and outputs data on a linear scale. The second purpose is to validate that the zero and fullscale values of the instrument are properly set.

Prior to sampling, a single calibration gas was injected into the probe inlet. This calibration gas is usually a mixture of oxygen and carbon dioxide in a balance of zero nitrogen. The system is not adjusted except to achieve proper flow through the analyzers. The calibration standard is allowed to traverse the sampling system. The response of the analyzer during this bias check must agree with the initial analyzer

response of this standard within the specified tolerances set forth in the test method. This system bias check serves to demonstrate that the sample train is leak free and causes no interference to the integrity of the sample.

## 2. Sampling.

After calibration, the system is purged with zero grade nitrogen to remove any pollutants that were injected as calibration gas. Once the system indicates that the pollutant gases have been removed, the calibration valve assembly is positioned to allow stack gas to flow through the instrument.

The sample gas is filtered at the stack position to remove any particulate matter. This prevents instruments from being contaminated and ensures reliable data acquisition.

All samples injected to the instruments are removed from the stack and delivered to the instruments via a heated probe and sample line. This prevents any condensation of water vapor and/or pollutant in the gas stream. Once the sample gas exits the sample line, the stream is separated in a sample gas manifold. The split stream enables analysis of the CEM instrumentation on both wet and dry basis as necessary.

The portion of the sample gas dedicated to the dry basis analyzers is directed into a gas conditioning system where the moisture content of the stream is removed. The sample gas that exits the gas conditioning system is then routed to the instruments for analysis on a dry basis.

To demonstrate that the instrument did not exhibit any deviation from the calibrated values set at the beginning of a test period, a sample of certified calibration gas is injected into the sampling system at the conclusion of each test run. The sample system must respond within specified tolerance limits according to the initial system bias check.

This post-test calibration serves two purposes: (1) it demonstrates that excessive calibration drift of the instrument(s) did not occur during the test period and, (2) that the system was not contaminated with any foreign material from the source to alter any results during the test period.

### 3. Data Acquisition.

The CEM monitors utilized in the testing project output a voltage signal corresponding to the pollutant concentration determined by the detector. This signal is relayed to a computerized datalogger system. This system retrieves the output signal from each monitor every 10 seconds. This data is then averaged on a per minute basis and stored on the hard drive of the computer. Additionally, a strip chart recorder is employed to record the data. This device records the instrument output on a one minute, instantaneous basis.

The data listing for all of the analyzers, for each testing period, is provided in another section. This listing provides the data results as recorded by the computerized datalogger system.

#### B. Determination of Nitrogen Oxides Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 7E:

The calibration, sampling, and data acquisition procedures are similar to that of Method 3A. Listed below are any deviations or differences that were incurred specifically in this testing procedure.

The calibration of the instruments is performed using certified gas standards composed of a known concentration of nitrogen oxide in zero grade nitrogen. These gas standards are prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis certificate for each of the certified gas mixtures used during the testing is included in the test report.

The instrument utilizes an chemiluminescent detector. The detection limitation of the analyzer is 0.1 ppm. Multiple fullscale ranges are available for operation. A 250, 1000, 2500, and 10,000 ppm fullscale may be selected according to the concentrations of NOx present in the gas steam. The analyzers were calibrated using standards that were the appropriate percentage of fullscale according to Method 7E.

The pre-test calibration, system bias, and post-test calibration procedures are identical to those discussed in Reference Method 3A.

C. Determination of Carbon Monoxide Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 10:

1. Calibration.

The calibration of the instruments is performed using certified gas standards composed of a known concentration of carbon monoxide in zero grade nitrogen. These gas standards are prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis certificate for each of the certified gas mixtures used during the testing is included in the test report.

The instrument utilizes a Luft-type nondispersive infrared detector. Immediately prior to each compliance test series, a complete calibration of the instrument is performed. Each instrument has zero grade nitrogen injected into it and the zero potentiometer is adjusted, if necessary, until the proper voltage output from the analyzer is achieved.

Then a high range pollutant gas mixture, that has been prepared in the specified range percentage of the span or fullscale, is injected. After the system stabilizes, the span or fullscale potentiometer is adjusted until the voltage output from analyzer corresponds to the certification of analysis for the respective calibration gas.

When this procedure is complete and the system has responded properly to a zero and fullscale reading, a mid and low range certified calibration gas is injected into the system. No adjustments are made to the system except to achieve proper flow rate through the analyzer. The analyzer, after reaching a stable value, must correspond to the certified value of the calibration gas within a specified percentage of the fullscale. This mid and low range calibration gas serves two purposes of quality control and quality assurance. The first is to show that the instrument analyzes and outputs data on a linear scale. The second purpose is to validate that the zero and fullscale values of the instrument are properly set.

## 2. Sampling.

After calibration of the instrument(s) has been completed, a sample bias check is performed. This involves injecting calibration gas into the sample probe inlet and allowing the calibration gas to traverse through the sample train to the analyzer(s) where it is analyzed. This analysis will correspond to the pre-test calibration analysis value of the standard within the tolerances set forth in the reference method.

Once the system indicates that the calibration gases have been removed, the calibration valve assembly is positioned to allow stack gas to flow through the instrument. The sample gas is filtered at the stack position to remove any particulate matter. This prevents instruments from being contaminated and ensures reliable data acquisition.

All samples injected to the instruments are removed from the stack and delivered to the instruments via a heated probe and sample line. This prevents any condensation of water vapor and/or pollutant in the gas stream.



To demonstrate that the instrument did not exhibit any deviation from the calibrated values set at the beginning of a test period, a sample of certified calibration gas is injected into the sampling system at the conclusion of each test run. The sample system must respond within specified tolerance limits according to the initial system bias check.

This post-test calibration serves two purposes: (1) it demonstrates that excessive calibration drift of the instrument(s) did not occur during the test period and, (2) that the system was not contaminated with any foreign material from the source to alter any results during the test period.

D. Determination of Total Gaseous Organic Emissions From Stationary Sources (Instrumental Analyzer Procedure) - US EPA Method 25A:

1. Calibration.

The calibration of the instruments is performed using certified gas standards composed of a known concentration of methane in zero grade nitrogen. These gas standards are prepared using partial pressure/volumetric and gravimetric methods.

The prepared gas mixture is analyzed and the certification tolerance is not greater than 2% of the pollutant component. A copy of the analysis certificate for each of the certified gas mixtures used during the testing is included in the test report.

The instrument utilizes an flame ionization detector. Immediately prior to each compliance test series, a complete calibration of the instrument is performed. Each instrument has zero grade nitrogen injected into it and the zero potentiometer is adjusted, if necessary, until the proper voltage output from the analyzer is achieved.

Then a high range pollutant gas mixture, that has been prepared in the specified range percentage of the span or fullscale, is injected. After the system stabilizes, the span or

fullscale potentiometer is adjusted until the voltage output from analyzer corresponds to the certification of analysis for the respective calibration gas.

When this procedure is complete and the system has responded properly to a zero and fullscale reading, a mid and low range certified calibration gas is injected into the system. No adjustments are made to the system except to achieve proper flow rate through the analyzer. The analyzer, after reaching a stable value, must correspond to the certified value of the calibration gas within a specified percentage of the fullscale. This mid and low range calibration gas serves two purposes of quality control and quality assurance. The first is to show that the instrument analyzes and outputs data on a linear scale. The second purpose is to validate that the zero and fullscale values of the instrument are properly set.

## 2. Sampling.

After calibration, the system is purged with zero grade nitrogen to remove any pollutants that were injected as calibration gas. Once the system indicates that the pollutant gases have been removed, the calibration valve assembly is positioned to allow stack gas to flow through the instrument.

The sample gas is filtered at the stack position to remove any particulate matter. This prevents instruments from being contaminated and ensures reliable data acquisition. All samples injected to the instruments are removed from the stack and delivered to the instruments via a heated probe and sample line. This prevents any condensation of water vapor and/or pollutant in the gas stream. The data obtained from the THC analyzer is therefore on a "wet basis". The data listing must be corrected to a "dry basis" for use in emission determinations, e.g. lb/hr. This correction is conducted utilizing the moisture percentage of the flue gas stream as determined during the test run.

To demonstrate that the instrument did not exhibit any deviation from the calibrated values set at the beginning of a test period, a sample of certified calibration gas is injected into

the sampling system at the conclusion of each test run. The sample system must respond within specified tolerance limits according to the initial system bias check.

This post-test calibration serves two purposes: (1) it demonstrates that excessive calibration drift of the instrument(s) did not occur during the test period and, (2) that the system was not contaminated with any foreign material from the source to alter any results during the test period.

E. Total Particulate - US EPA Reference Methods 5:

1. Preparation.

All glassware utilized in each sampling train was thoroughly cleaned and dried prior to each test series. A glass fiber filter was used that had been labeled, desiccated for a minimum of 24 hours and pre-weighed.

The impinger system configuration was assembled using the procedure outlined in Method 5. One hundred ml of deionized water was placed in the first two impingers. The third impinger was initially empty and the fourth impinger contained a pre-weighed amount of silica gel for complete moisture removal.

A stainless steel probe liner and nozzle system was utilized for the total particulate determinations. The probe housed a set of calibrated S-type pitot tubes and a calibrated thermocouple for monitoring stack temperature.

2. Sampling.

The probe and sample box were heated to an approximate temperature of 250 F. These temperatures were monitored throughout the testing. An ice bath was prepared to submerge the impinger system. The temperature of the last impinger was monitored

throughout the testing to ensure adequate condensation of the water vapor in the flue gases.

A leak check was performed prior to each test run. The sample train system was subjected to a vacuum that did not exceed 0.02 cfm leakage rate. The vacuum that was established during the pre-test leak check was not exceeded during the test period(s).

When a test run had been completed, a post-test leak check was conducted prior to dismantling of the sampling train. Once this had been successfully achieved, the sample train was dismantled for sample recovery.

The probe and connecting glassware were washed with acetone. The contents of the impingers were volumetrically measured for moisture gain and transferred to a labeled sample container. The glass fiber filter was carefully transferred to its sample container.

### 3. Analysis.

The glass fiber filter was desiccated for 24 hours prior to any weighing. The acetone probe wash was transferred to a tared beaker and evaporated to dryness. The resultant residue was also desiccated prior to gravimetric analysis.

The first weighing was performed after this initial period of drying. The weights were recorded to 0.0001 g. After a minimum of 6 additional hours of desiccating, a second weighing was conducted. The weights must agree within 0.0005 g or further desiccation must be conducted until the weights stabilize.

Sample field blanks of acetone were collected, contained, labeled and analyzed in conjunction with the samples. The blank weight was deducted from the acetone probe wash residue weight determinations.

F. EPA Draft Method 202, "Determination of Filterable and Condensable Particulate Matter"

The testing procedure was conducted according to Reference Method 5 for particulate matter determination. This testing procedure was covered in a previous section. The filterable portion of the particulate matter was determined via this procedure. The condensable fraction of the sample was determined by analyzing the back half impinger catch with a methylene chloride extraction.

This extraction procedure will yield fractions of inorganic and organic condensable matter. The concentrations and emission values of both filterable particulate and condensable particulate matter have been summarized in the test results section.

G. Polynuclear Aromatic Hydrocarbons - Method SW846 8270 "Semivolatile Organic Compounds by Gas Chromatography/Mass Spectrometry (GC/MS): Capillary Column Technique"

1. Preparation.

All glassware utilized in each sampling train was thoroughly cleaned with hot soapy water and dried prior to each test series. All residue silicon grease was removed from glassware upstream of the absorbent module. A glass fiber filter was used that has been properly labeled.

The absorbent traps was packed by the analytical laboratory that conducted the final analysis.

The impinger system was assembled using 100 ml of D.I. water in impingers 1 and 2. The third impinger was initially empty and the fourth impinger contained silica gel.

In assembling the sample train, teflon tape was placed on the ball joints to ensure adequate sealing upstream of the absorbent module. All connections downstream of the module were sealed with silicon grease.

A glass probe liner and nozzle system was utilized for the collection train. The probe housed a set of calibrated S-type pitot tubes and a calibrated thermocouple for monitoring stack temperature.

## 2. Sampling.

The probe and sample box was heated to an approximate temperature of 250 F. These temperatures were monitored throughout the testing.

The probe was connected to the heated filter system with connecting glassware. This filter system was connected to the condenser by a teflon line. The condenser and absorbent module are directly connected via ground glass ball and socket.

An ice bath was prepared to submerge the impinger system into. The temperature of the last impinger was monitored throughout the testing to ensure adequate condensation of the water vapor in the flue gases.

The condenser cooling fluid was recirculated through the system by a peristaltic pump. This pump is to be started prior to the start up of the sampling system to ensure that the temperature of the absorbent material in the module does not exceed its thermal decomposition temperature. The temperature of gas entering the module was monitored to ensure that the temperature did not exceed the recommended limitation for efficient capture.

A leak check was performed prior to each test run. The entire sample train system was subjected to a vacuum that did not exceed 0.02 cfm leakage rate. The vacuum that was established during the pre-test leak check was not exceeded during the test period.

Three sample runs were conducted to constitute a complete test. The sample time was be a *minimum of one hour*.

When a test run had been completed, a post-test leak check was conducted prior to any dismantling of the sampling train. Once this had been successfully achieved, the sample train was dismantled for sample recovery.

### 3. Sample Analysis.

Method 8270 is used to determine the concentration of semivolatile organic compounds in extracts prepared from all types of solid waste matrices. Each compound present in the sample is separated by gas chromatography and quantified by mass spectrometry.

The detection limitation of this type of sample has been determined to be 1.0 microgram. If the samples are separated for further analysis, the detection limit will be 2.0 micrograms.

#### H. EPA Draft Method 0011, "Determination of Formaldehyde"

This sampling procedure is similar to the operational procedures found in Reference Method 5. *Described in this section are the differences set forth from Method 5 to ensure that the integrity of the formaldehyde sample is maintained.*

Prior to any sampling, all glassware shall be rinsed with methylene chloride to remove any contamination that may be initially on the glassware such as stopcock grease. This includes the rinsing of the glass probe liner material required for the collection of the sample.

In collecting the sample, a minimum of 45 cubic feet must be pulled isokinetically such that the extracted sample is transferred through the DNPH absorption solution. All

samples should be placed into glass amber sample containers to avoid the alteration of the sample by sunlight.

The analysis of the formaldehyde samples shall be conducted according to the procedures outlined in Method 8315. This analysis procedure provides guidance in the evaluation of formaldehyde samples by High Performance Liquid Chromatography (HPLC).

I. Determination of Gaseous Organic Emissions From Stationary Sources By Gas Chromatography - US EPA Method 18:

This procedure utilizes the technology of gas chromatography to separate, identify, and quantitate various volatile organic compounds that co-exist in a flue gas stream. In this testing project, methane and the BTEX compounds were targeted.

The gas chromatograph was first conditioned in the laboratory where ideal conditions exist for this initial calibration. This consists of conditioning the column, if necessary, and creating calibration curves based on actual data from the GC with known concentration standards. As required by EPA, three (3) standards of known concentration were used in creating the calibration curves. The concentrations of the standards bracketed the expected concentration of pollutant at the source level.

A field calibration check was performed prior to introducing any sample into the gas chromatograph. This is performed by injecting one of the known standards into the GC and comparing the result to the calibration curve. It must agree within 5 % of the previously determined response.

Analysis of the samples follow a successful field calibration. Collecting the sample consisted of extracting the sample from the stack via a heated sample line. The sample was introduced directly into the sample loop, where it was injected to the instrument for analysis. This type of sampling is termed "semi-continuous".

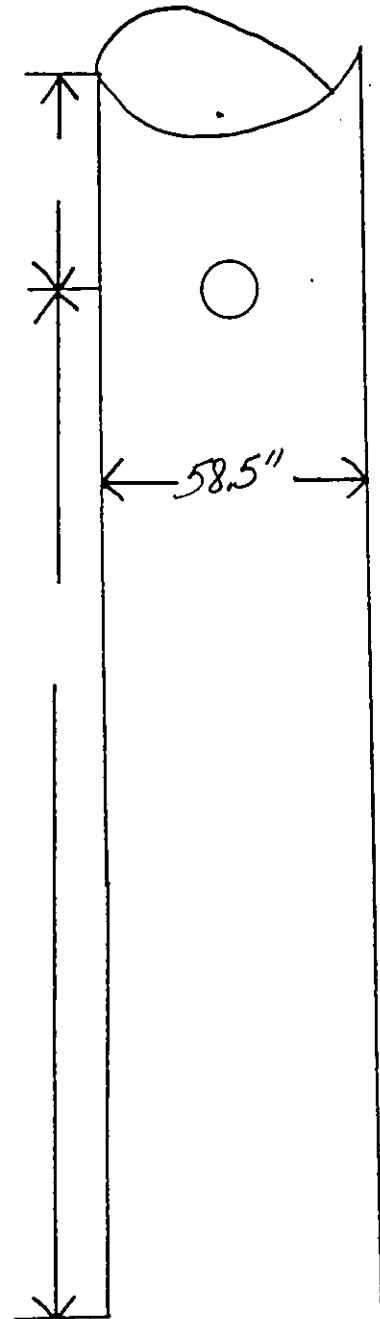


#### IV. SOURCE INFORMATION

The emissions test was conducted on a round stack with a diameter of 58.5". Two (2) sample ports are positioned at 90° apart in the same test plane. The sample port location is positioned such that the minimum requirements for sampling in a non-turbulent zone are met. Twenty-four (24) points were sampled, twelve (12) through each traverse for 2.5 minutes each for a total testing time of sixty (60) minutes.

<u>Points on a Diameter</u>	<u>Probe Mark</u>
1	*8.7"
2	11.4"
3	14.4"
4	17.8"
5	22.1"
6	28.2"
7	45.2"
8	51.3"
9	55.6"
10	59.0"
11	62.0"
12	65.0"

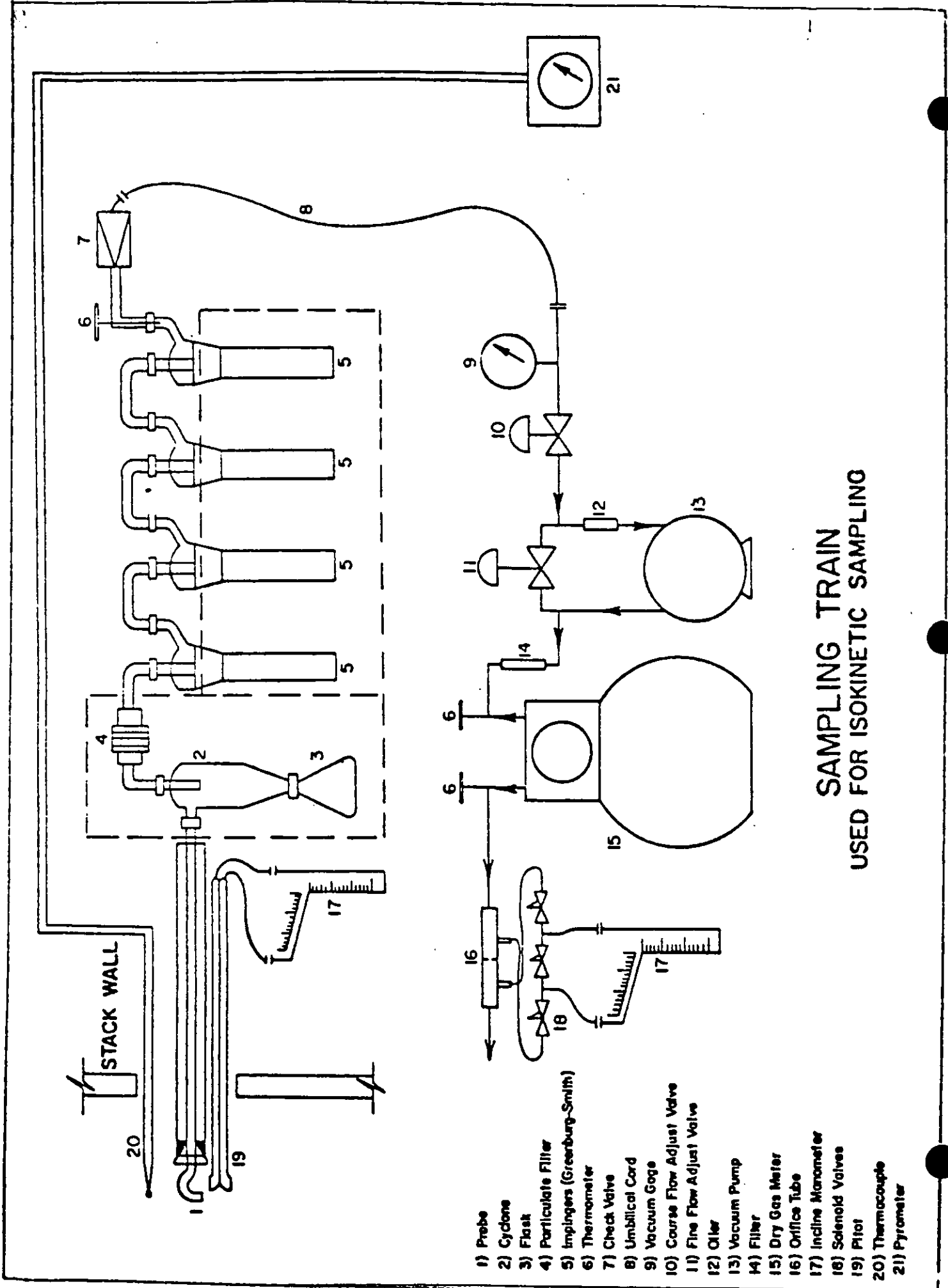
\*Measurements include a  
7.5" standoff.



## EQUIPMENT USED

Equipment used to conduct the particulate emissions test was:

- A. A Lear Siegler PM-100 stack sampler with appropriate auxiliary equipment and glassware (with train set up according to the schematic on the next page).
- B. An Airguide Instruments Model 211-B (uncorrected) aneroid barometer for checking the barometric pressure.
- C. Weston dial thermometers to check meter temperatures or an Analogic Model 2572 Digital Thermocouple to check stack temperatures.
- D. A Hays 621 Analyzer to measure the oxygen, carbon dioxide and carbon monoxide content of the stack gases or, for non-combustion sources, a Bacharach Instrument Company Fyrite for gas analysis.
- E. Schleicher and Schuell Type 1-HV filters with a porosity of .03 microns.
- F. Reagent- or ACS-grade acetone with a residue of  $\leq .001$ .



## SAMPLING TRAIN USED FOR ISOKINETIC SAMPLING

- 1) Probe
- 2) Cyclone
- 3) Flask
- 4) Particulate Filter
- 5) Impingers (Greenburg-Smith)
- 6) Thermomater
- 7) Check Valve
- 8) Umbilical Cord
- 9) Vacuum Gage
- 10) Course Flow Adjust Valve
- 11) Fine Flow Adjust Valve
- 12) Orler
- 13) Vacuum Pump
- 14) Filter
- 15) Dry Gas Meter
- 16) Orifice Tube
- 17) Incline Manometer
- 18) Solenoid Valves
- 19) Pilot
- 20) Thermocouple
- 21) Pyrometer

## HEATED TOTAL HYDROCARBON ANALYZER MODEL VE7

The J.U.M. Engineering Model VE7 is a high accuracy Total Hydrocarbon Analyzer for the measurement and analysis of organic vapors.

The VE7 utilizes a Hydrogen Flame Ionization Detector (FID) in a thermostatically controlled oven to prevent the loss of high molecular weight hydrocarbons.

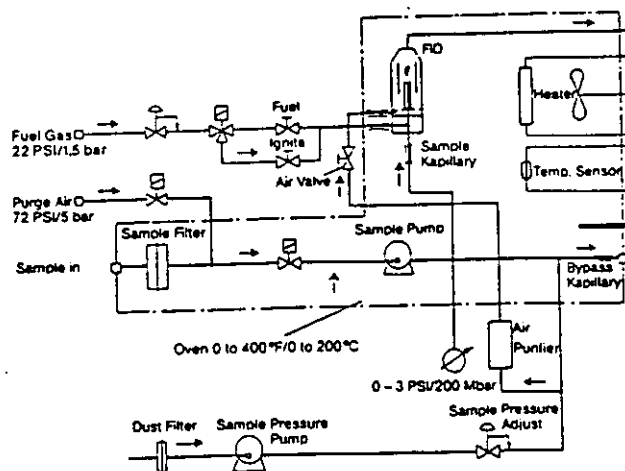
### Options

Digital display with BCD output/without BCD output Remote range control and range I.D. Recorder output of oven temperature

- All heated components
- Integrated heated sample pump
- Permanent heated stainless steel 2 micron sample filter
- Built in burner air supply - no extra bottles needed
- Automatic fuel enrichment for ignition
- 19 inch relay rack mount
- 1% precision full scale
- Response time - 90% full scale within 1 second

### STANDARD SPECIFICATIONS:

<b>Analysis Method:</b>	Flame Ionization Detector (FID)
<b>Sensitivity:</b>	Max. 1 ppm CH
<b>Response Time:</b>	90% of full scale in less than one second
<b>Zero Drift:</b>	1% of full scale per 24 hours
<b>Span Drift:</b>	1% of full scale per 24 hours
<b>Linearity:</b>	Within 1%
<b>Oxygen Synergism:</b>	Less than 1% of selected range
<b>Ranges:</b>	Any three of the following: 0 - 10, 100, 1000, 10,000, 100,000 ppm
<b>Outputs:</b>	0 - 10 Volts D.C.
<b>Display:</b>	Analog Meter in ppm Hydrocarbon or in % LEL
<b>Zero/Span Adjust:</b>	Manual on front panel
<b>Fuel Consumption:</b>	Hydrogen 20 cc/min at 22 psig (1.5 Bar) Hydrogen/Helium 40/60 mix: 80 cc/min.
<b>Air Consumption:</b>	None Integral Air generator
<b>Zero &amp; Span Gas:</b>	3 psig (200 m Bar)
<b>Sample Pump:</b>	All Stainless Steel, heated, 3 liters per minute at operating temperature
<b>Sample Pressure:</b>	By Integral Pump 3 psig (200 m Bar)
<b>Sample Filter:</b>	Permanent all stainless steel 2 micron back-purged for cleaning
<b>Analysis Temperature:</b>	Adjustable 200 to 400°F (93 to 204°C)
<b>Power Requirements:</b>	110 Volts, 60 Hertz AC 800 Watts (others on request)
<b>Ambient Temperature:</b>	32°F to 110°F (0 to 43°C)
<b>Dimensions:</b>	Width 483 mm (19 inches), Depth 460 mm (18-1/8 inches), Height 221 mm (8-3/4 inches)
<b>Weight:</b>	38.6 lbs (17.5 kg)
<b>Shipping Weight:</b>	53 lbs (24 kg)

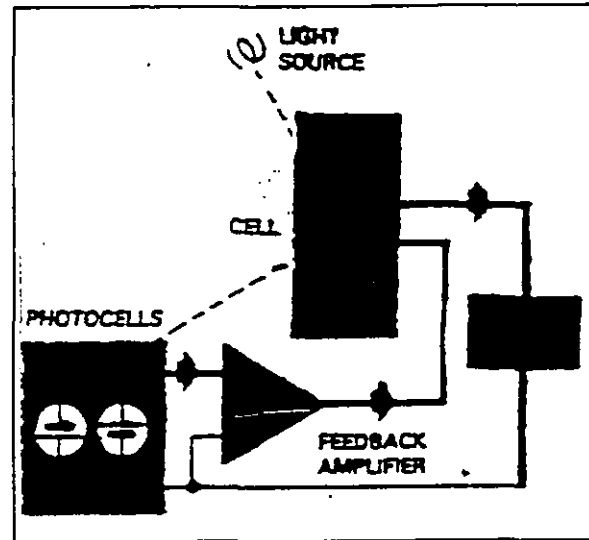


## PRINCIPLES OF OPERATION

**SERVOMEX  
1400 SERIES  
GAS ANALYZERS**

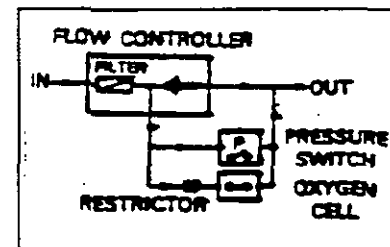
**SPECIFICATION****OXYGEN**

Principle	Magneto-dynamic
Linearity	$\pm 0.2\% \text{ O}_2$
Repeatability	$\pm 0.2\% \text{ O}_2$
Zero Drift (Per Week)	$< 0.2\% \text{ O}_2$
Signal Output	0-1V non-isolated for 0-100% $\text{O}_2$
Alarms	Flow alarm. 4 sets of changeover relay contacts rated at 3A/120V AC, 1A/240V AC or 1A/28V DC
Display	3½ digit LCD reading 0 to 100% $\text{O}_2$
Response Time	Less than 15 seconds to 90%
Operating Ambient Temperature	32 - 104°F (0-40°C)
Relative Humidity	0 - 85%, non-condensing
Sample Pressure	0.2 to 0.6 barg
Sample Contact Materials	Stainless steel, pyrex, glass, brass, platinum, epoxy resin, viton, polypropylene and glass fibre
AC Supply	110 to 120V AC, or 220 to 240V AC, $\pm 10\%$ , 48 to 62Hz, 15VA maximum
Dimensions	19" Rack - 4U case Bench top - 7.1" (180mm) hi gh, 10.1" (256mm) wide, 15.4" (390mm) deep  22 lbs (10kg) approximately

**PARAMAGNETIC OXYGEN**

The oxygen analyzer measures the paramagnetic susceptibility of the sample gas by means of a magneto-dynamic type measuring cell.

Oxygen is virtually unique in being a paramagnetic gas, this means that it is attracted into a magnetic field. In the Servomex measuring cell, the oxygen concentration is detected by means of a dumb-bell mounted on a torque suspension in a strong, non-linear magnetic field. The higher the concentration of oxygen, the greater the dumb-bell is deflected from its rest position. This deflection is detected by an optical system and twin photocells connected to an amplifier. Around the dumb-bell is a coil of wire. A current is passed through this coil to return the dumb-bell to its original position. The current is measured and is proportional to the oxygen concentration.



Gas Flow Diagram

**Advantages**

- Not cross sensitive to most common gases
- Long lifetime
- Rugged Design
- No routine cell maintenance

## 8610 GAS CHROMATOGRAPH

### Miniature Lab GC

At a fraction of the cost, the SRI 8610 Gas Chromatograph provides the capabilities and sophistication of vastly larger and more expensive instruments in a small, lightweight and attractive package. More of a miniature laboratory GC than a true portable, the 8610 is the perfect size and weight for easy field use without sacrificing big GC features. In the lab or in the field, the 8610 Gas Chromatograph gives you up to five detectors plus a built-in purge and trap in a simple to operate, easy to trouble-shoot, and unbelievably low cost package. And, the Peaksimple Data System, provided free with every 8610 GC turns your IBM PC into a powerful chromatography integrator which also controls the 8610's temperature program and purge and trap.

### Multi-Level Temperature Programming

Temperature programming is a standard feature on every 8610 GC. Up to 15 ramp/plateau segments permit maximum flexibility. Because the temperature program is controlled by the data system, an unlimited number of different temperature programs may be permanently stored on disk and activated with a few keystrokes. The 8610's temperature program can be controlled either by the Peaksimple Data System (included free with every GC) or by any other data system or integrator which has the ability to close relay contacts at specified times during the run.

### Ultra Low Mass Column Oven

The SRI 8610's large easily accessible column oven is designed to fit all standard packed and capillary columns with diameters up to eight inches. The ultra-low mass design allows rapid heat-up and cool-down from ambient to 250 degrees centigrade. Interchangeable screw-in heater elements allow power consumption to be reduced for low temperature battery powered applications, or easy heater replacement in the event of a failure. Squirrel-cage type oven fan insures uniform heat distribution and stability to within .1 degree.

### Low Cost GC • Free Data System/Integrator

### Field Portable • Built-In Purge and Trap

### Temperature Programmable • Multiple Detectors

#### Digital Gas Flow Controllers

The carrier gas flow rate is regulated by a unique Digital Flow Controller. Precise and reproducible even at capillary flow rates below 1 cc/per minute, the carrier gas flow controller is standard equipment on every SRI 8610 GC (except low-cost student model). Digital dial allows flow rates to be adjusted without having to measure actual flows with a bubblemeter. A column head pressure gauge is provided to alert the operator to leaks or blockages in the column. The same flow controller is optionally available for hydrogen and air combustion gas flows (recommended for NPD operation). In addition, inlet pressure regulators are supplied for each gas to isolate the GC from fluctuations in gas supply pressure.

#### Direct Cool On Column Injection

The zero-dead volume on-column injector is designed for state of the art, cool on-column injections using both packed and wide-bore capillary (.53 mm). A special wide-bore adapter positions the .53 mm column so the syringe smoothly deposits the sample in the bore of the column itself. This provides a totally inert, metal and glass free sample path. Peaks are exceptionally sharp and well resolved.

#### Detectors

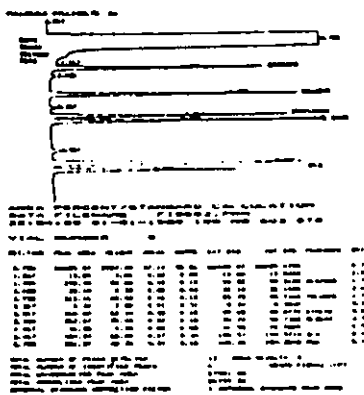
Thermal Conductivity (TCD)  
Flame Ionization (FID)  
Nitrogen-Phosphorus (NPD)  
Thermionic Ionization (TID)

Photo-Ionization (PID)  
Electron Capture (ECD)  
Hall Detector (HALL or ELCD)  
Flame Photometric (FPD)

Up to 3 detectors may be mounted simultaneously and plumbed in series so that one injection passes through each detector and into the next. Common series configurations include:

(PID-FID), (TCD-FID), (PID-ECD),  
(PID-HALL) and (PID-ECD-FID).

D:\DONNA\8610GAS.DJB



100 NG.  
602 STD.  
Data  
plotted  
using  
Peaksimple  
Data  
System.

## FUJI 730 NDIR SINGLE GAS ANALYZER

This unique Mass Flow Sensor used in the Fuji 730 Single Gas Analyzer provides significant advantages over other sensors used for this purpose. The design of the Mass Flow Detector minimizes the adverse effects of vibration which is often present in harsh environments. In addition the Mass Flow Sensor System virtually eliminates interference making the Fuji 730 a powerful analytical tool for monitoring burner and boiler efficiency heat treatment fermentation well logging and many other applications which require exceptional accuracy stability high sensitivity and reliability.

### PRINCIPLE OF OPERATION

The Fuji 730 Series Analyzers use the infrared adsorption characteristic of gases to measure the concentration of gas samples. An efficient single beam design which incorporates a unique mass flow sensor system insures accurate and interference free analysis for a wide variety of applications.

A single beam of infrared energy is chopped and passed through a sample cell containing the flowing as sample. Due to the adsorption characteristic, the amount of energy in the beam is reduced by the concentration of the measured gas in the sample. The attenuated infrared beam is passed serially through the two cavities of the mass flow sensor which contain a high concentration of the gas species the analyzer is intended to measure. The two cavity sensor performs two functions in the analyzing process, it first eliminates interference caused by other gases and water vapor by detecting and subtracting the interference component from the detector output, and secondly, produces an output signal which represents an accurate duplication of the relative infrared energy adsorption. This resultant signal is electronically processed and linearized to provide an electrical signal which drives meters and other output devices.

### STANDARD GASES:

Carbon Monoxide (CO)  
Carbon Dioxide (CO<sub>2</sub>)  
Methane (CH<sub>4</sub>)

### STANDARD RANGES:

0-500/1000 ppm  
0-1000/2000 ppm  
0-2000/5000 ppm  
0-2500/5000 ppm

0-0.5/1.0%  
0-1/2%  
0-2/5%  
0-5/10%  
1-10/20%

### PURGE GAS FITTING

Standard Equipment

### INTERNAL SPAN CHECK FEATURE

Calibration check without the use of span gases.  
Conserves gas and reduces operating costs.

### SPECIFICATIONS

<b>Repeatability:</b>	±0.5% of full scale (low range) ±1.0% of full scale (high range)
<b>Zero Drift*:</b>	±1% of full scale per 24 hours
<b>Span Drift*:</b>	±1% of full scale per 24 hours
<b>Linearity:</b>	±2% of full scale (within linearizer)
<b>Noise Level:</b>	0.5% of full scale
<b>Speed of Response:</b>	90% indication
<b>Electrical:</b>	2, 3 or 5 seconds (field selectable)
<b>Pneumatic:</b>	Less than 15 seconds (depending on cell length)
<b>Warm-Up:</b>	Two hours (to ±2% full scale)
<b>Internal Span Check:</b>	Manually activated from front panel
<b>Outputs:</b>	0 to 1V DC, linear & 4-20mA DC, linear
<b>Ambient Temperature Range:</b>	23 to 113°F (-5 to 45°C)
<b>Ambient Humidity:</b>	To 90% R.H. (non-condensing)
<b>Sample Gas Temperature:</b>	32 to 122°F (0 to 50°C)
<b>Sample Gas Flow Rate:</b>	2 ± 1 scfh (1.0 ± .05 slpm)
<b>Purge Gas Rate (where necessary):</b>	2 scfh (1 slpm) when required
<b>Power Requirements:</b>	115V AC ± 10%, 60 Hz, 30VA
<b>Gas Connections:</b>	All 1/4" compression-type tube fittings
<b>Size and Weight:</b>	7.9 (H) x 9.8 (W) x 21.3 (D) inches (200 x 250 x 541 mm) 24.2 pounds (11 kg)

\*constant conditions

# FUJI 760 NDIR GAS ANALYZER

- Unique Mass Flow Sensor System Eliminates Interference
- Wide Dynamic Range Permits Ultra-Sensitive and High Concentration Gas Analysis
- Designed for Continuous Operation and Low Maintenance
- Measures:
  - Carbon Monoxide (CO)
  - Carbon Dioxide (CO<sub>2</sub>)
  - Sulfur Dioxide (SO<sub>2</sub>)
  - Nitric Oxide (NO)
  - Methane (CH<sub>4</sub>)
- Insensitive to Vibration

This instrument is designed for stack monitoring and process control applications. It's remarkable accuracy and fast response makes it an ideal instrument for CEMS, boiler control equipment, research labs and many other monitoring applications. For usage requiring ultra sensitive measurement, the Fuji 760 delivers superior performance. Using the Non-Dispersive Infrared (NDIR) Mass Flow Detector, low concentration measurements are accurate and reliable. The Fuji 760 incorporates an Interference Compensating Detector which minimizes the effects of other gases, particularly when operating in ranges of high sensitivity.

### FEATURES OF THE FUJI-760

The Fuji 760 Analyze uses infrared adsorption techniques to measure gas concentrations, however, many innovative patented features make this instrument far superior to conventional Non Dispersive Infrared Analyzers. Among its unique features are an optical chopper design which virtually eliminates the effects of vibration and resultant optical noise; a mass flow sensor system which reduces the effects of interfering gases to insignificant levels, thus permitting gas analysis at low concentration ranges; and a dual beam optical system derived from a single infrared source which enhances long term stability.

### PRINCIPAL OF OPERATION

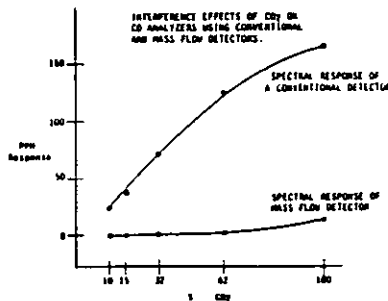
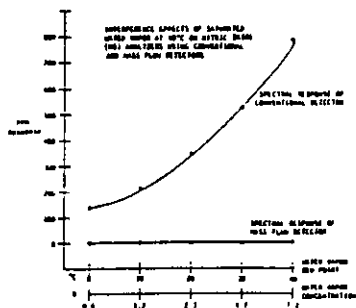
A single beam of infrared energy is modulated and split into two parallel beams by a distribution cell. One beam is passed through a reference cell containing a non-absorbing gas, and the other beam is passed through a cell containing the sample gas being measured. The beam passing through the sample cell is attenuated by the amount of gas concentration in the sample and compared against the unattenuated reference beam by the mass flow detector system. One set of detectors sense the amount of sample gas as compared against the reference, the second set of detectors measure and cancel interferences in the sample. The outputs of the detectors are electronically processed and conditioned into useable signals for indicators and other output devices.

### DETECTABLE GAS RANGES

#### Standard Configuration

Component	Minimum Range
Carbon Monoxide (CO)	0 to 100 ppm
Carbon Dioxide (CO <sub>2</sub> )	0 to 50 ppm
Nitric Oxide (NO)	0 to 100 ppm
Sulfur Dioxide (SO <sub>2</sub> )	0 to 100 ppm
Total Hydrocarbons	0 to 500 ppm

Other Gases can be measured.



### Specifications

#### (Standard Configuration)

- Repeatability:** ±0.5% of full scale
- Zero Drift:** ±2 % of full scale per week
- Span Drift:** ±2% of full scale per week
- Linearity:** ±2% of full scale
- Speed of Response:** 90% indication within 5 seconds (Electronic Response)
- Range Selection:** Either of two ranges selected by front panel switch or external contact closure.
- Warm-Up:** Four hours minimum
- Outputs:** 0 to 1V DC, linear and 4-20mA DC, linear
- Ambient Temperature Range:** 23 to 113°F (-5 to 45°C)
- Ambient Humidity:** To 90% R.H. (non-condensing)
- Sample Gas Temperature:** 32 to 122°F (0 to 50°C)
- Sample Gas Flow Rate:** 1.0 ±0.5 scfh (0.50±0.25 slpm) for standard configuration
- Materials in Contact with Sample:** 304 Stainless steel, neoprene rubber, silicone rubber, CaF<sub>2</sub>/ sapphire, Teflon®
- Power Requirements:** 115V AC ± 10%, 50/60 Hz (switch selectable)  
110 VA max. (200VA max with converter)  
220V AC available
- Gas Connections:** All 1/4" compression-type tube fittings
- Size and Weight:**  
8.66 (H) x 17.44 (W) x 16.78 (D) inches  
(220 x 443 x 350 mm)  
37.4 pounds (17 kg)



## MODEL 10 FOR CONTINUOUS SOURCE GAS MONITORING

## CHEMILUMINESCENT NO/NO<sub>x</sub> ANALYZER

Thermo Electron's Model 10 NO/NO<sub>x</sub> Analyzer is based on the chemiluminescent reaction between nitric oxide (NO) and ozone (O<sub>3</sub>) according to the reaction:  $\text{NO} + \text{O}_3 \rightarrow \text{NO}_2 + \text{O}_2 + h\nu$

Light emission results when the electronically excited NO<sub>2</sub> molecules revert to their ground state.

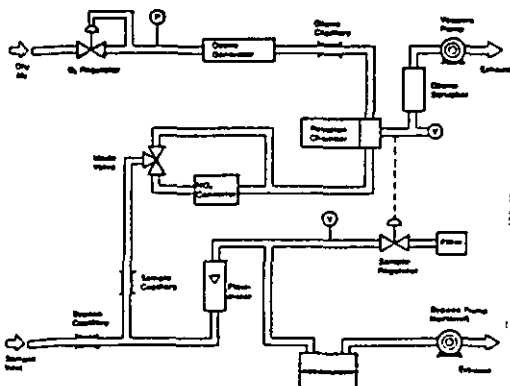
A front panel mode switch provides for either a direct readout of the NO concentration in the sample being analyzed ("NO" mode) or the total NO<sub>x</sub> concentration ("NO<sub>x</sub>" mode). When the Model 10 is placed in the "NO<sub>x</sub>" mode, the sample stream passes through a NO<sub>x</sub>-to-NO converter prior to entering the reaction chamber for subsequent analysis.

### Key Features

- Selective detection of NO or NO<sub>x</sub>
- Eight ranges, from 2.5 to 10,000 ppm FS
- Continuous monitoring with rapid response
- Linear on all ranges
- Field proven reliability
- Insensitive to changes in sample flow

As illustrated in the diagram, sample gas enters the Model 10, flows through the bypass capillary, and divides. Most of the sample flows through the flowmeter, accumulator, bypass pump, and exhausts. Only a small amount of sample flows through the sample capillary for analysis. The bypass pump in conjunction with the sample regulator maintain a constant pressure differential across the sample capillary, thus maintaining constant sample flow for analysis. This plumbing network makes the analyzer insensitive to pressure fluctuation in the sample inlet.

From the sample capillary, the sample to be analyzed is either directed through the NO<sub>x</sub> to NO converter or around it, depending on the choice of the operator. In the reaction chamber the sample reacts with ozone to produce the light emission and is exhausted. The ozone is produced internally from dry air entering through the oxygen regulator and ozonator. The light emission is sensed by the photomultiplier tube and amplified.



### Model 10 Specifications\*

Ranges	0-2.5 ppm	0-250 ppm
	0-10 ppm	0-1000 ppm
	0-25 ppm	0-2500 ppm
	0-100 ppm	0-10,000 ppm
Minimum Detectable Concentration	.05 ppm	
Noise	Less than 1% of FS	
Reproducibility	1% of FS	
Operating Temperature Extremes	0-40°C	
Response Time (0-90%)	~1.5 second NO mode ~1.7 second NO <sub>x</sub> mode	
Zero Stability	±1 ppm in 24 hours	
Span Stability	±1% in 24 hours	
Linearity	±1% from 0.05 to 10,000 ppm**	
Power Requirements	1000 watts, 115 ± 10 volts, 60 Hz standard. Also available in 115V 50 Hz, and 210 ± 15 volts, 50 Hz versions	
Physical Dimensions	19" wide x 17" high x 20" deep	
Instrument Weight	75 lbs. (including pump)	
Outputs	Two standard outputs supplied: 1) 0-10V; 2) Field selectable from 0-10V, 5V, 1V, 100mV or 10mV. (ma options available.)	

\*Specifications are typical and subject to change without notice.

\*\*With O<sub>2</sub> Feed; With dry air, linearity to 2000 ppm.

## **VI. CALCULATIONS**

### **A. Particulate — Condensibles**

SUMMARY OF TEST DATA

	12-02-92	12-03-92	12-04-92
	RUN #1	RUN #2	RUN #3

SAMPLING TRAIN DATA

	start	14:18	14:59	08:26
	finish	15:21	16:18	10:58
1. Sampling time, minutes	$\Theta$	60.0	60.0	60.0
2. Sampling nozzle diameter, in.	$D_n$	.3000	.3000	.3000
3. Sampling nozzle cross-sect. area, ft <sup>2</sup>	$A_n$	.000490	.000490	.000490
4. Isokinetic variation	I	100.1	90.9	100.3
5. Sample gas volume - meter cond., cf.	$V_m$	42.036	39.562	41.821
6. Average meter temperature, °R	$T_m$	548	545	537
7. Avg. oriface pressure drop, in. H <sub>2</sub> O	dH	1.38	1.26	1.39
8. Total particulate collected, mg.	$M_n$	149.10	131.80	188.30

VELOCITY TRAVERSE DATA

9. Stack area, ft <sup>2</sup>	A	18.60	18.60	18.60
10. Absolute stack gas pressure, in. Hg.	$P_s$	30.01	30.02	30.00
11. Barometric pressure, in. Hg.	$P_{bar}$	30.01	30.02	30.00
12. Avg. absolute stack temperature, R°	$T_s$	732	724	724
13. Average $-\sqrt{\text{vel. head}}$ , ( $C_p = .84$ )	$-\sqrt{dP}$	0.59	0.58	0.57
14. Average stack gas velocity, ft./sec.	$V_s$	40.30	39.09	38.47

STACK MOISTURE CONTENT

15. Total water collected by train, ml.	$V_{ic}$	239.10	164.90	189.70
16. Moisture in stack gas, %	$B_{ws}$	21.78	16.83	18.07

EMISSIONS DATA

17. Stack gas flow rate, dscf/hr.(000's)	$Q_{sd}$	1527	1592	1543
18. Stack gas flow rate, cfm	acfm	44975	43624	42933
19. Particulate concentration, gr/dscf	$C_s$	0.0571	0.0533	0.0710
20. Particulate concentration, lb/hr	E	12.46	12.13	15.65
21. Particulate concentration, lb/mBtu	E'	0.00000	0.00000	0.00000

ORSAT DATA

22. Percent CO <sub>2</sub> by volume	CO <sub>2</sub>	5.50	4.20	4.80
23. Percent O <sub>2</sub> by volume	O <sub>2</sub>	14.40	15.10	15.10
24. Percent CO by volume	CO	.00	.00	.00
25. Percent N <sub>2</sub> by volume	N <sub>2</sub>	80.10	80.70	80.10

$$V_{m(std)} = V_m \left[ \frac{T_{(std)}}{T_m} \right] \left[ \frac{P_{bar} + \frac{dH}{13.6}}{P_{(std)}} \right] = 17.64 \frac{^{\circ}R}{in.Hg} Y V_m \left[ \frac{P_{bar} + \frac{dH}{13.6}}{T_m} \right]$$

Where:

$V_{m(std)}$  = Dry Gas Volume through meter at standard conditions, cu. ft.

$V_m$  = Dry Gas Volume measured by meter, cu. ft.

$P_{bar}$  = Barometric pressure at oriface meter, in. Hg.

$P_{std}$  = Standard absolute pressure, (29.92 in. Hg.).

$T_m$  = Absolute temperature at meter  $^{\circ}R$ .

$T_{std}$  = Standard absolute temperature ( 528 $^{\circ}R$ ).

$dH$  = Average pressure drop across oriface meter, in. H<sub>2</sub>O.

$Y$  = Dry gas meter calibration factor.

13.6 = Inches water per inches Hg.

RUN 1:

$$V_{m(std)} = (17.64)(.987)(42.036) \left[ \frac{(30.01) + \frac{1.38}{13.6}}{548} \right] = 40.215 \text{ dscf}$$

RUN 2:

$$V_{m(std)} = (17.64)(.987)(39.562) \left[ \frac{(30.02) + \frac{1.26}{13.6}}{545} \right] = 38.058 \text{ dscf}$$

RUN 3:

$$V_{m(std)} = (17.64)(.987)(41.821) \left[ \frac{(30.00) + \frac{1.39}{13.6}}{537} \right] = 40.816 \text{ dscf}$$

Total Contaminants by Weight: GRAIN LOADING

Particulate concentration  $C'_s$  gr./dscf.

$$C'_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

$C'_s$  = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, gr./dscf.

$M_n$  = Total amount of particulate matter collected, mg.

$V_{m(\text{std})}$  = Dry gas volume through meter at standard conditions, cu. ft.

Run 1:

$$C'_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{149.10}{40.215} \right] = 0.0571 \text{ gr./dscf.}$$

Run 2:

$$C'_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{131.80}{38.058} \right] = 0.0533 \text{ gr./dscf.}$$

Run 3:

$$C'_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{188.30}{40.816} \right] = 0.0710 \text{ gr./dscf.}$$

**Particulate  
CONVERSION TO mg/m<sup>3</sup>**

$$C, \text{mg/m}^3 = (C, \text{gr/dscf}) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right)$$

Where:

- C,mg/m<sup>3</sup> = Concentration as milligrams per cubic meter
- C,gr/dscf = Concentration as grains per cubic foot
- 35.31 = Conversion of ft<sup>3</sup> to m<sup>3</sup>
- 0.0154 = Conversion from grains to milligrams

Run #1:

$$C, \text{mg/m}^3 = (0.0571) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 130.9$$

Run #2:

$$C, \text{mg/m}^3 = (0.0533) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 122.2$$

Run #3:

$$C, \text{mg/m}^3 = (0.0710) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 162.8$$

**TOTAL CONTAMINANTS BY WEIGHT: GRAIN LOADING**

Condensable Particulate Concentration:  $C_s'$  gr/dscf

$$C_s' = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

$C_s'$  = Concentration of condensibles in stack gas, dry basis, corrected to standard conditions, gr/dscf.

$M_n$  = Total amount of condensible matter collected, mg.

$V_{m(\text{std})}$  = Dry gas volume through meter at standard conditions, cu. ft.

Run #1:

$$C_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{101.7}{40.215} \right] = 0.0389 \text{ gr/dscf}$$

Run #2:

$$C_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{44.0}{38.058} \right] = 0.0178 \text{ gr/dscf}$$

Run #3:

$$C_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{92.1}{40.816} \right] = 0.0347 \text{ gr/dscf}$$

**NAME:** MACASPHALT  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**Condensible Particulate  
 CONVERSION TO mg/m<sup>3</sup>**

$$C, \text{mg/m}^3 = (C, \text{gr/dscf}) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right)$$

Where:

C, mg/m<sup>3</sup> = Concentration as milligrams per cubic meter  
 C, gr/dscf = Concentration as grains per cubic foot  
 35.31 = Conversion of ft<sup>3</sup> to m<sup>3</sup>  
 0.0154 = Conversion from grains to milligrams

Run #1:

$$C, \text{mg/m}^3 = (0.0389) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 89.2$$

Run #2:

$$C, \text{mg/m}^3 = (0.0178) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 40.8$$

Run #3:

$$C, \text{mg/m}^3 = (0.0347) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 79.6$$



$$M_d = 0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%CO + \%N_2)$$

Where:

$M_d$  = Dry molecular weight, lb./lb.-mole.

$\%CO_2$  = Percent carbon dioxide by volume (dry basis).

$\%O_2$  = Percent oxygen by volume (dry basis).

$\%N_2$  = Percent nitrogen by volume (dry basis).

$\%CO$  = Percent carbon monoxide by volume (dry basis).

0.264 = Ratio of  $O_2$  to  $N_2$  in air, v/v.

0.28 = Molecular weight of  $N_2$  or  $CO$ , divided by 100.

0.32 = Molecular weight of  $O_2$  divided by 100.

0.44 = Molecular weight of  $CO_2$  divided by 100.

Run 1:

$$M_d = 0.44( 5.50\%) + 0.32(14.40\%) + 0.28( .00\% + 80.10\%) = 29.46 \frac{lb}{lb-mole}$$

Run 2:

$$M_d = 0.44( 4.20\%) + 0.32(15.10\%) + 0.28( .00\% + 80.70\%) = 29.28 \frac{lb}{lb-mole}$$

Run 3:

$$M_d = 0.44( 4.80\%) + 0.32(15.10\%) + 0.28( .00\% + 80.10\%) = 29.37 \frac{lb}{lb-mole}$$

Water Vapor Condensed

$$V_{wc_{std}} = \left[ V_f - V_i \right] \left[ \frac{p_w R T_{(std)}}{M_w P_{(std)}} \right] = 0.04707 \left[ V_f - V_i \right]$$

$$V_{wsg_{std}} = \left[ W_f - W_i \right] \left[ \frac{R T_{(std)}}{M_w P_{(std)}} \right] = 0.04715 \left[ W_f - W_i \right]$$

Where:

0.04707 = Conversion factor, ft.<sup>3</sup>/ml.

0.04715 = Conversion factor, ft.<sup>3</sup>/g.

$V_{wc_{std}}$  = Volume of water vapor condensed (standard conditions), scf.

$V_{wsg_{std}}$  = Volume of water vapor collected in silica gel (standard conditions), ml.

$V_f - V_i$  = Final volume of impinger contents less initial volume, ml.

$W_f - W_i$  = Final weight of silica gel less initial weight, g.

$p_w$  = Density of water, 0.002201 lb/ml.

R = Ideal gas constant, 21.85 in.Hg. (cu.ft./lb.-mole)(<sup>o</sup>R).

$M_w$  = Molecular weight of water vapor, 18.0 lb/lb-mole.

$T_{std}$  = Absolute temperature at standard conditions, 528<sup>o</sup>R.

$P_{std}$  = Absolute pressure at standard conditions, 29.92 inches Hg.

Run 1:

$$\begin{aligned} V_{wc(std)} &= (0.04707) ( 232.0 ) = 10.9 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) ( 7.1 ) = 0.3 \text{ cu.ft} \end{aligned}$$

Run 2:

$$\begin{aligned} V_{wc(std)} &= (0.04707) ( 160.0 ) = 7.5 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) ( 4.9 ) = 0.2 \text{ cu.ft} \end{aligned}$$

Run 3:

$$\begin{aligned} V_{wc(std)} &= (0.04707) ( 182.0 ) = 8.6 \text{ cu.ft} \\ V_{wsg(std)} &= (0.04715) ( 7.7 ) = 0.4 \text{ cu.ft} \end{aligned}$$

Moisture Content of Stack Gases

$$B_{ws} = \frac{V_{wc_{std}} + V_{wsg_{std}}}{V_{wc_{std}} + V_{wsg_{std}} + V_{m_{std}}} \times 100$$

Where:

$B_{ws}$  = Proportion of water vapor, by volume, in the gas stream.

$V_m$  = Dry gas volume measured by dry gas meter, (dcf).

$V_{wc_{std}}$  = Volume of water vapor condensed corrected to standard conditions (scf).

$V_{wsg_{std}}$  = Volume of water vapor collected in silica gel corrected to standard conditions (scf).

Run 1:

$$B_{ws} = \frac{10.9 + 0.3}{10.9 + 0.3 + 40.215} \times 100 = 21.78 \%$$

Run 2:

$$B_{ws} = \frac{7.5 + 0.2}{7.5 + 0.2 + 38.058} \times 100 = 16.83 \%$$

Run 3:

$$B_{ws} = \frac{8.6 + 0.4}{8.6 + 0.4 + 40.816} \times 100 = 18.07 \%$$

Molecular Weight of Stack Gases

$$M_s = M_d ( 1 - B_{ws} ) + 18 ( B_{ws} )$$

Where:

$M_s$  = Molecular weight of stack gas, wet basis, (lb./lb.-mole).

$M_d$  = Molecular weight of stack gas, dry basis, (lb./lb.-mole).

Run 1:

$$M_s = 29.46 ( 1 - 21.78 ) + 18 ( 21.78 ) = 26.96 \text{ (lb./lb.-mole)}$$

Run 2:

$$M_s = 29.28 ( 1 - 16.83 ) + 18 ( 16.83 ) = 27.38 \text{ (lb./lb.-mole)}$$

Run 3:

$$M_s = 29.37 ( 1 - 18.07 ) + 18 ( 18.07 ) = 27.32 \text{ (lb./lb.-mole)}$$

Stack Gas Velocity

$$V_s = K_p C_p \left[ \sqrt{dP} \right]_{\text{avg.}} \sqrt{\frac{T_{s(\text{avg.})}}{P_s M_s}}$$

Where:

- $V_s$  = Average velocity of gas stream in stack, ft./sec.
- $K_p$  = 85.49 ft/sec  $\left[ \frac{(\text{g/g-mole}) - (\text{mm Hg})}{(^{\circ}\text{K})(\text{mm H}_2\text{O})} \right]^{1/2}$
- $C_p$  = Pitot tube coefficient, (dimensionless).
- $dP$  = Velocity head of stack gas, in.  $\text{H}_2\text{O}$ .
- $P_{\text{bar}}$  = Barometric pressure at measurement site, (in. Hg).
- $P_g$  = Stack static pressure, (in. Hg).
- $P_s$  = Absolute stack gas pressure, (in. Hg) =  $P_{\text{bar}} + P_g$
- $P_{\text{std}}$  = Standard absolute pressure, ( 29.92 in. Hg ).
- $t_s$  = Stack temperature, ( $^{\circ}\text{f}$ ).
- $T_s$  = Absolute stack temperature, ( $^{\circ}\text{R}$ ). =  $460 + t_s$ .
- $M_s$  = Molecular weight of stack gas, wet basis, (lb/lb-mole).

Run 1:

$$V = (85.49) ( .84 ) ( 0.59 ) \sqrt{\frac{732}{(30.01)(26.96)}} = 40.30 \text{ ft/sec.}$$

Run 2:

$$V = (85.49) ( .84 ) ( 0.58 ) \sqrt{\frac{724}{(30.02)(27.38)}} = 39.09 \text{ ft/sec.}$$

Run 3:

$$V = (85.49) ( .84 ) ( 0.57 ) \sqrt{\frac{724}{(30.00)(27.32)}} = 38.47 \text{ ft/sec.}$$

Stack Gas Flow Rate

$$Q_{sd} = 3600 \left[ 1 - B_{wc} \right] V_s A \left[ \frac{T_{std}}{T_{stk}} \right] \left[ \frac{P_s}{P_{std}} \right]$$

Where:

- $Q_{sd}$  = Dry volumetric stack gas flow rate corrected to standard conditions, (dscf/hr).
- $A$  = Cross sectional area of stack, (ft.<sup>2</sup>).
- 3600 = Conversion factor, (sec./hr.).
- $t_s$  = Stack temperature, (°f).
- $T_s$  = Absolute stack temperature, (°R).
- $T_{std}$  = Standard absolute temperature, (528°R).
- $P_{bar}$  = Barometric pressure at measurement site, (in.Hg.).
- $P_g$  = Stack static pressure, (in.Hg.).
- $P_s$  = Absolute stack gas pressure, (in.Hg.); =  $P_{bar} + P_g$
- $P_{std}$  = Standard absolute pressure, (29.92 in.Hg.).

Run 1:

$$Q_{sd} = 3600(1 - .2178)(40.30)(18.60) \left[ \frac{528}{732} \right] \left[ \frac{30.01}{29.92} \right] = 1527093.2 \frac{dscf}{hr}$$

Run 2:

$$Q_{sd} = 3600(1 - .1683)(39.09)(18.60) \left[ \frac{528}{724} \right] \left[ \frac{30.02}{29.92} \right] = 1592913.8 \frac{dscf}{hr}$$

Run 3:

$$Q_{sd} = 3600(1 - .1807)(38.47)(18.60) \left[ \frac{528}{724} \right] \left[ \frac{30.00}{29.92} \right] = 1543247.6 \frac{dscf}{hr}$$

Emissions Rate from Stack

$$E = \frac{(C_s) (Q_{sd})}{7000 \text{ gr./lb.}} = \text{lb. / hr.}$$

Where:

E = Emissions rate, lb/hr.

C<sub>s</sub> = Concentration of particulate matter in stack gas, dry basis, corrected to standard conditions, gr/dscf.

Q<sub>sd</sub> = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run 1:

$$E = \frac{(0.0571) (1527093.2)}{7000} = 12.46 \text{ lb. / hr.}$$

Run 2:

$$E = \frac{(0.0533) (1592913.8)}{7000} = 12.13 \text{ lb. / hr.}$$

Run 3:

$$E = \frac{(0.0710) (1543247.6)}{7000} = 15.65 \text{ lb. / hr.}$$

NAME: MACASPHALT  
 LOCATION: MELBOURNE, FLORIDA

DATE: December 2-4, 1992

**Condensible Particulate  
 EMISSIONS RATE FROM STACK**

$$E = \left[ \frac{(C_s) (Q_{sd})}{7,000 \text{ gr/lb}} \right] = 0.0000 \text{ lb/hr}$$

Where:

E = Emissions rate, lbs/hr.

$C_s$  = Concentration of condensibles in stack gas, dry basis, corrected to standard conditions, gr/dscf.

$Q_{sd}$  = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run #1:

$$E = \frac{(0.0389) (1527093.2)}{7,000} = 8.49$$

Run #2:

$$E = \frac{(0.0178) (1592913.8)}{7,000} = 4.05$$

Run #3:

$$E = \frac{(0.0347) (1543247.6)}{7,000} = 7.65$$



$$I = 100 T_s \left[ \frac{0.002669 V_{ic} + \frac{(V_m / T_m) (P_{bar} + dH / 13.6)}{\theta V_s P_s A_n}}{60} \right]$$

Where:

- I = Percent isokinetic sampling.
- 100 = Conversion to percent.
- T<sub>s</sub> = Absolute average stack gas temperature, °R.
- 0.002669 = Conversion factor, Hg - ft<sup>3</sup>/ml - °R.
- V<sub>ic</sub> = Ttl vol of liquid collected in impingers and silica gel, ml.
- T<sub>m</sub> = Absolute average dry gas meter temperature, °R.
- P<sub>bar</sub> = Barometric pressure at sampling site, (in. Hg).
- dH = Av pressure differential across the oriface meter, (in.H<sub>2</sub>O).
- 13.6 = Specific gravity of mercury.
- 60 = Conversion seconds to minutes.
- θ = Total sampling time, minutes.
- V<sub>s</sub> = Stack gas velocity, ft./sec.
- P<sub>s</sub> = Absolute stack gas pressure, in. Hg.
- A<sub>n</sub> = Cross sectional area of nozzle, ft<sup>2</sup>.

Run 1:

$$I = (100)(732) \left[ \frac{(0.002669)(239.10) + \frac{42.036}{548} \left[ 30.01 + \frac{1.38}{13.6} \right]}{60 (60.0) (40.30) (30.01) (.000490)} \right] = 100.1\%$$

Run 2:

$$I = (100)(724) \left[ \frac{(0.002669)(164.90) + \frac{39.562}{545} \left[ 30.02 + \frac{1.26}{13.6} \right]}{60 (60.0) (39.09) (30.02) (.000490)} \right] = 90.9\%$$

Run 3:

$$I = (100)(724) \left[ \frac{(0.002669)(189.70) + \frac{41.821}{537} \left[ 30.00 + \frac{1.39}{13.6} \right]}{60 (60.0) (38.47) (30.00) (.000490)} \right] = 100.3\%$$

## **VI. CALCULATIONS**

### **B. Formaldehyde**

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**SUMMARY OF TEST DATA**

		Run #1 12-04-92	Run #2 12-04-92	Run #3 12-04-92
<b>SAMPLING TRAIN DATA</b>				
	Start	11:49	13:03	14:48
	Finish	13:04	14:04	16:02
1. Sampling time, minutes	$\theta$	72.0	60.0	72.0
2. Sampling nozzle diameter, in.	$D_n$	.3000	.3200	.3000
3. Sampling nozzle cross-sect. area, ft <sup>2</sup>	$A_n$	.000490	.000576	.000490
4. Isokinetic variation	I	100.8	91.9	99.9
5. Sample gas volume - meter cond., cf.	$V_m$	49.675	50.155	52.085
6. Average meter temperature, °R	$T_m$	557	567	562
7. Avg. orifice pressure drop, in. H <sub>2</sub> O	$\Delta H$	1.29	2.68	1.46
8. Total formaldehyde collected, mg.	$M_n$	.063	4.30	.600
<b>VELOCITY TRAVERSE DATA</b>				
9. Stack area, ft. <sup>2</sup>	A	18.60	18.60	18.60
10. Absolute stack gas pressure, in. Hg.	$P_s$	30.00	30.00	30.00
11. Barometric pressure, in. Hg.	$P_{bar}$	30.00	30.00	30.00
12. Avg. absolute stack temperature, R°	$T_s$	728	744	724
13. Average $\sqrt{vel.}$ head, ( $C_p = .84$ )	$\sqrt{dp}$	0.55	0.62	0.59
14. Average stack gas velocity, ft./sec.	$V_s$	37.31	42.60	40.14
<b>STACK MOISTURE CONTENT</b>				
15. Total water collected by train, ml.	$V_{ic}$	236.90	246.30	285.40
16. Moisture in stack gas, %	$B_{ws}$	19.19	20.08	21.75
<b>EMISSION DATA</b>				
17. Stack gas flow rate, dscf/hr.	$Q_{std}$	1468	1622	1537
18. Stack gas flow rate, cfm	acfm	41638	47542	44796
19. Formaldehyde concentration, gr/dscf	$C_s$	0.00002	0.00140	0.00020
20. Formaldehyde concentration, lb/hr	E	0.004	0.320	0.040
<b>ORSAT DATA</b>				
21. Percent CO <sub>2</sub> by volume	CO <sub>2</sub>	4.80	4.80	4.70
22. Percent O <sub>2</sub> by volume	O <sub>2</sub>	15.00	15.00	15.30
23. Percent CO by volume	CO	.00	.00	.00
24. Percent N <sub>2</sub> by volume	N <sub>2</sub>	80.20	80.20	80.00

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**MOISTURE DETERMINATION  
 DRY GAS VOLUME**

$$V_{m(std)} = V_m \left[ \frac{T_{(std)}}{T_m} \right] \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{P_{std}} \right] - 17.64 \frac{^{\circ}R}{\epsilon. Hg} Y V_m \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right]$$

Where:

- $V_{m(std)}$  = Dry gas volume through meter at standard conditions, ft<sup>3</sup>.  
 $V_m$  = Dry gas volume measured by meter, ft<sup>3</sup>.  
 $P_{bar}$  = Barometric pressure at orifice meter, in. Hg.  
 $P_{std}$  = Standard absolute pressure, (29.92 in. Hg.).  
 $T_m$  = Absolute temperature at meter, °R.  
 $T_{std}$  = Standard absolute temperature, (528°R).  
 $\Delta H$  = Avg. pressure drop across orifice meter, in. H<sub>2</sub>O.  
 $Y$  = Dry gas meter calibration factor.  
 13.6 = Inches of water per Hg.

Run #1:

$$V_{m(std)} = (17.64)(.987)(49.675) \left[ \frac{30.00 + \frac{1.29}{13.6}}{557} \right] = 46.729 \text{ dscf}$$

Run #2:

$$V_{m(std)} = (17.64)(.980)(50.155) \left[ \frac{30.00 + \frac{2.68}{13.6}}{567} \right] = 46.176 \text{ dscf}$$

Run #3:

$$V_{m(std)} = (17.64)(.987)(52.085) \left[ \frac{30.00 + \frac{1.46}{13.6}}{562} \right] = 48.581 \text{ dscf}$$

TOTAL CONTAMINANTS BY WEIGHT: GRAIN LOADING

Formaldehyde Concentration:  $C_s'$  gr/dscf

$$C_s' = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

$C_s'$  = Concentration of formaldehyde in stack gas, dry basis, corrected to standard conditions, gr/dscf.

$M_n$  = Total amount of formaldehyde collected, mg.

$V_{m(\text{std})}$  = Dry gas volume through meter at standard conditions, cu. ft.

Run #1:

$$C_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{0.063}{46.729} \right] = 0.00002 \text{ gr/dscf}$$

Run #2:

$$C_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{4.200}{46.176} \right] = 0.00140 \text{ gr/dscf}$$

Run #3:

$$C_s = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{0.600}{48.581} \right] = 0.00020 \text{ gr/dscf}$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**Formaldehyde  
 CONVERSION TO mg/m<sup>3</sup>**

$$C, \text{mg/m}^3 = (C, \text{gr/dscf}) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right)$$

Where:

C,mg/m<sup>3</sup> = Concentration as milligrams per cubic meter  
 C,gr/dscf = Concentration as grains per cubic foot  
 35.31 = Conversion of ft<sup>3</sup> to m<sup>3</sup>  
 0.0154 = Conversion from grains to milligrams

Run #1:

$$C, \text{mg/m}^3 = (0.00002) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 0.046$$

Run #2:

$$C, \text{mg/m}^3 = (0.00140) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 3.210$$

Run #3:

$$C, \text{mg/m}^3 = (0.00020) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 0.459$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**Emissions of Formaldehyde: PPM (PARTS PER MILLION)**

$$E = \frac{C_s}{1,000 \text{ mg}} \times \frac{\text{g}}{30.03 \text{ g}} \times \frac{\text{MOL}}{\text{MOL}} \times \frac{22.4 \text{ l}}{\text{MOL}} \times \frac{293^\circ\text{K}}{273^\circ\text{K}} \times \frac{\text{ft}^3}{28.317} \times 1,000,000$$

Where:

- $C_s$  = Concentration of formaldehyde in mg/dscf.  
 1000 mg/g = Conversion to grams.  
 30.03 g/MOL = Molar conversion for formaldehyde.  
 22.4 l/MOL = Volumetric molar conversion @ 273°K.  
 293°K/273°K = Temperature correction to standard conditions.  
 28.317/ft<sup>3</sup> = Conversion to liters.  
 1,000,000 = Conversion to parts per million.

Run #1:

$$\frac{0.063 \text{ mg}}{46.729 \text{ dscf}} \times \frac{\text{g}}{1,000 \text{ mg}} \times \frac{\text{MOL}}{30.03 \text{ g}} \times \frac{22.4 \text{ l}}{\text{MOL}} \times \frac{293^\circ\text{K}}{273^\circ\text{K}} \times \frac{\text{ft}^3}{28.317} \times 1,000,000 = 0.04 \text{ ppm}$$

Run #2:

$$\frac{4.20 \text{ mg}}{46.176 \text{ dscf}} \times \frac{\text{g}}{1,000 \text{ mg}} \times \frac{\text{MOL}}{30.03 \text{ g}} \times \frac{22.4 \text{ l}}{\text{MOL}} \times \frac{293^\circ\text{K}}{273^\circ\text{K}} \times \frac{\text{ft}^3}{28.317} \times 1,000,000 = 2.60 \text{ ppm}$$

Run #3:

$$\frac{0.60 \text{ mg}}{48.581 \text{ dscf}} \times \frac{\text{g}}{1,000 \text{ mg}} \times \frac{\text{MOL}}{30.03 \text{ g}} \times \frac{22.4 \text{ l}}{\text{MOL}} \times \frac{293^\circ\text{K}}{273^\circ\text{K}} \times \frac{\text{ft}^3}{28.317} \times 1,000,000 = 0.30 \text{ ppm}$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

### DRY MOLECULAR WEIGHT

$$M_d = 0.44 (\% \text{CO}_2) + 0.32 (\% \text{O}_2) + 0.28 (\% \text{CO} + \% \text{N}_2)$$

Where:

- $M_d$  = Dry molecular weight, lb/lb-mole.
- $\% \text{CO}_2$  = Percent carbon dioxide by volume, dry basis.
- $\% \text{O}_2$  = Percent oxygen by volume, dry basis.
- $\% \text{N}_2$  = Percent nitrogen by volume, dry basis.
- $\% \text{CO}$  = Percent carbon monoxide by volume, dry basis.
- 0.264 = Ratio of  $\text{O}_2$  to  $\text{N}_2$  in air, v/v.
- 0.28 = Molecular weight of  $\text{N}_2$  or  $\text{CO}$ , divided by 100.
- 0.32 = Molecular weight of  $\text{O}_2$  divided by 100.
- 0.44 = Molecular weight of  $\text{CO}_2$  divided by 100.

Run #1:

$$M_d = 0.44 (4.80\%) + 0.32 (15.00\%) + 0.28 (0.00\% + 80.20\%) = 29.37 \frac{\text{lb}}{\text{lb-mole}}$$

Run #2:

$$M_d = 0.44 (4.80\%) + 0.32 (15.00\%) + 0.28 (0.00\% + 80.20\%) = 29.37 \frac{\text{lb}}{\text{lb-mole}}$$

Run #3:

$$M_d = 0.44 (4.70\%) + 0.32 (15.30\%) + 0.28 (0.00\% + 29.36\%) = 29.36 \frac{\text{lb}}{\text{lb-mole}}$$



**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

### WATER VAPOR CONDENSED

$$V_{wc_{std}} = [V_f - V_i] \left[ \frac{P_w R T_{(std)}}{M_w P_{(std)}} \right] - 0.04707 [V_f - V_i]$$

$$V_{wsg_{std}} = [W_f - W_i] \left[ \frac{R T_{(std)}}{M_w P_{(std)}} \right] - 0.04715 [W_f - W_i]$$

Where:

- 0.04707 = Conversion factor, ft<sup>3</sup>/ml.  
 0.04715 = Conversion factor, ft<sup>3</sup>/g.  
 V<sub>wc<sub>std</sub></sub> = Volume of water vapor condensed (std. cond.), ml.  
 V<sub>wsg<sub>std</sub></sub> = Volume of water vapor collected in silica gel (standard conditions), ml.  
 V<sub>f</sub> - V<sub>i</sub> = Final volume of impinger contents less initial volume, ml.  
 W<sub>f</sub> - W<sub>i</sub> = Final weight of silica gel less initial weight, g.  
 P<sub>w</sub> = Density of water, 0.002201 lb/ml.  
 R = Ideal gas constant, 21.85 in.Hg. (cu.ft./lb-mole)(°R).  
 M<sub>w</sub> = Molecular weight of water vapor, 18.0 lb/lb-mole.  
 T<sub>std</sub> = Absolute temperature at standard conditions, 528°R.  
 P<sub>std</sub> = Absolute pressure at standard conditions, 29.92 inches Hg.

Run 1:

$$V_{wc_{std}} = (0.04707) (230.0) - 10.8 \text{ cu.ft.}$$

$$V_{wsg_{std}} = (0.04715) (6.9) - 0.3 \text{ cu.ft.}$$

Run 2:

$$V_{wc_{std}} = (0.04707) (240.0) - 11.3 \text{ cu.ft.}$$

$$V_{wsg_{std}} = (0.04715) (6.3) - 0.3 \text{ cu.ft.}$$

Run 3:

$$V_{wc_{std}} = (0.04707) (280.0) - 13.2 \text{ cu.ft.}$$

$$V_{wsg_{std}} = (0.04715) (5.4) - 0.3 \text{ cu.ft.}$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

### MOISTURE CONTENT OF STACK GASES

$$B_{ws} = \left[ \frac{V_{WC_{std}} + V_{Wsg_{std}}}{V_{WC_{std}} + V_{Wsg_{std}} + V_{mstd}} \right] \times 100$$

Where:

$B_{ws}$  = Proportion of water vapor, by volume, in the gas stream.

$V_m$  = Dry gas volume measured by dry gas meter, dcf.

$V_{WC_{std}}$  = Volume of water vapor condensed, corrected to standard conditions, scf.

$V_{Wsg_{std}}$  = Volume of water vapor collected in silica gel corrected to std. cond., scf.

Run 1:

$$B_{ws} = \left[ \frac{10.8 + 0.3}{10.8 + 0.3 + 46.729} \right] \times 100 = 19.19\%$$

Run 2:

$$B_{ws} = \left[ \frac{11.3 + 0.3}{11.3 + 0.3 + 46.176} \right] \times 100 = 20.08\%$$

Run 3:

$$B_{ws} = \left[ \frac{13.2 + 0.3}{13.2 + 0.3 + 48.581} \right] \times 100 = 21.75\%$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

### MOLECULAR WEIGHT OF STACK GASES

$$M_s = M_d (1 - B_{ws}) + 18 (B_{ws})$$

Where:

$M_s$  = Molecular weight of stack gas, wet basis (lb./lb.-mole).

$M_d$  = Molecular weight of stack gas, dry basis (lb./lb.-mole).

Run #1:

$$M_s = 29.37 (1 - 19.19) + 18 (19.19) = 27.19 \text{ (lb./lb.-mole)}$$

Run #2:

$$M_s = 29.37 (1 - 20.08) + 18 (20.08) = 27.09 \text{ (lb./lb.-mole)}$$

Run #1:

$$M_s = 29.36 (1 - 21.75) + 18 (21.75) = 26.89 \text{ (lb./lb.-mole)}$$

### STACK GAS VELOCITY

$$V_s = K_p C_p [\sqrt{\Delta P}]_{avg} \sqrt{\frac{T_s(avg)}{P_s M_s}}$$

Where:

- $V_s$  = Average velocity of gas stream in stack, ft/sec.
- $K_p$  = 85.49 ft/sec [(g/g·mole) - (mm Hg)/(°K)(mm H<sub>2</sub>O)]<sup>1/2</sup>
- $C_p$  = Pitot tube coefficient, dimensionless.
- $\Delta P$  = Velocity head of stack gas, in. H<sub>2</sub>O.
- $P_{bar}$  = Barometric pressure at measurement site, in. Hg.
- $P_g$  = Stack static pressure, in. Hg.
- $P_s$  = Absolute stack gas pressure, in. Hg. =  $P_{bar} + P_g$
- $P_{std}$  = Standard absolute pressure, 29.92 in. Hg.
- $t_s$  = Stack temperature, °F.
- $T_s$  = Absolute stack temperature, °R. = 460 +  $t_s$ .
- $M_s$  = Molecular weight of stack gas, wet basis, lb/lb·mole.

Run #1:

$$V = (85.49) (.84) (0.55) \sqrt{\frac{728}{(30.00)(27.19)}} = 37.31 \text{ ft/sec}$$

Run #2:

$$V = (85.49) (.84) (0.62) \sqrt{\frac{744}{(30.00)(27.09)}} = 42.60 \text{ ft/sec}$$

Run #3:

$$V = (85.49) (.84) (0.59) \sqrt{\frac{724}{(30.00)(26.89)}} = 40.14 \text{ ft/sec}$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

### STACK GAS FLOW RATE

$$Q_{sd} = 3600 [1 - B_{wc}] V_s A \left[ \frac{T_{std}}{T_{stk}} \right] \left[ \frac{P_s}{P_{std}} \right]$$

Where:

- $Q_{sd}$  = Dry volumetric stack gas flow rate corrected to standard conditions (dscf/hr).  
 $A$  = Cross sectional area of stack (ft<sup>2</sup>).  
 $3600$  = Conversion factor (sec/hr).  
 $T_{stk}$  = Absolute stack temperature (°R).  
 $T_{std}$  = Standard absolute temperature (528°R).  
 $P_{bar}$  = Barometric pressure at measurement site (in. Hg.).  
 $P_g$  = Stack static pressure (in. Hg.).  
 $P_s$  = Absolute stack gas pressure (in. Hg.) =  $P_{bar} + P_g$   
 $P_{std}$  = Standard absolute pressure (29.92 in. Hg.).

Run #1:

$$Q_{sd} = 3600 (1 - .1919) (37.31) (18.60) \left[ \frac{528}{728} \right] \left[ \frac{30.00}{29.92} \right] = 1468141.8 \frac{\text{dscf}}{\text{hr}}$$

Run #2:

$$Q_{sd} = 3600 (1 - .2008) (42.60) (18.60) \left[ \frac{528}{744} \right] \left[ \frac{30.00}{29.92} \right] = 1622188.0 \frac{\text{dscf}}{\text{hr}}$$

Run #3:

$$Q_{sd} = 3600 (1 - .2175) (40.14) (18.60) \left[ \frac{528}{724} \right] \left[ \frac{30.00}{29.92} \right] = 1537914.5 \frac{\text{dscf}}{\text{hr}}$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**Formaldehyde  
 EMISSIONS RATE FROM STACK**

$$E = \left[ \frac{(C_s) (Q_{sd})}{7,000 \text{ gr/lb}} \right] = 0.0000 \text{ lb/hr}$$

Where:

- E = Emissions rate, lbs/hr.  
 C<sub>s</sub> = Concentration of formaldehyde in stack gas, dry basis, corrected to standard conditions, gr/dscf.  
 Q<sub>sd</sub> = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run #1:

$$E = \frac{(0.00002) (1468141.8)}{7,000} = 0.004$$

Run #2:

$$E = \frac{(0.00140) (1622188.0)}{7,000} = 0.320$$

Run #3:

$$E = \frac{(0.00020) (1537914.5)}{7,000} = 0.040$$

**NAME:** MACASPHALT (Formaldehyde)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

### ISOKINETIC VARIATION

$$I = 100 T_s \left[ \frac{(0.002669) (V_{ic} + (V_m/T_m) (P_{bar} + \Delta H/13.6))}{60 \theta V_s P_s A_n} \right]$$

Where:

- I = Percent isokinetic sampling.
- 100 = Conversion to percent.
- $T_s$  = Absolute average stack gas temperature, °R.
- 0.002669 = Conversion factor, Hg - ft<sup>3</sup>/ml - °R.
- $V_{ic}$  = Total volume of liquid collected in impingers and silica gel, ml.
- $T_m$  = Absolute average dry gas meter temperature, °R.
- $P_{bar}$  = Barometric pressure at sampling site, in. Hg.
- $\Delta H$  = Average pressure differential across the orifice meter, in. H<sub>2</sub>O.
- 13.6 = Specific gravity of mercury.
- 60 = Conversion seconds to minutes.
- $\theta$  = Total sampling time, minutes.
- $V_s$  = Stack gas velocity, ft/sec.
- $P_s$  = Absolute stack gas pressure, in. Hg.
- $A_n$  = Cross sectional area of nozzle, ft<sup>2</sup>.

Run #1:

$$I = (100) (728) \left[ \frac{(0.002669) (236.90) + \frac{49.675}{557} \left[ 30.00 + \frac{1.29}{13.6} \right]}{60 (72.0) (37.31) (30.00) (.000490)} \right] = 100.8\%$$

Run #2:

$$I = (100) (744) \left[ \frac{(0.002669) (246.30) + \frac{50.155}{567} \left[ 30.00 + \frac{2.68}{13.6} \right]}{60 (60.0) (42.60) (30.00) (.000576)} \right] = 91.9\%$$

Run #3:

$$I = (100) (724) \left[ \frac{(0.002669) (285.40) + \frac{52.085}{562} \left[ 30.00 + \frac{1.46}{13.6} \right]}{60 (72.0) (40.14) (30.00) (.000490)} \right] = 99.9\%$$

**VI. CALCULATIONS**

**C. PAH**



NAME: MACASPHALT (PAH)  
 LOCATION: MELBOURNE, FLORIDA

DATE: December 2-4, 1992

### SUMMARY OF TEST DATA

		Run #1 12-03-92	Run #2 12-03-92	Run #3 12-04-92
<b>SAMPLING TRAIN DATA</b>				
	Start	10:25	12:55	08:11
	Finish	12:22	16:39	11:26
1. Sampling time, minutes	$\theta$	90.0	90.0	90.0
2. Sampling nozzle diameter, in.	$D_n$	.3250	.3100	.3250
3. Sampling nozzle cross-sect. area, ft <sup>2</sup>	$A_n$	.000576	.000525	.000576
4. Isokinetic variation	I	93.8	92.8	87.1
5. Sample gas volume - meter cond., cf.	$V_m$	79.821	71.546	70.457
6. Average meter temperature, °R	$T_m$	566	564	555
7. Avg. orifice pressure drop, in. H <sub>2</sub> O	$\Delta H$	2.70	2.12	2.64
8. Total PAH collected, mg.	$M_n$	.00	.00	.00
<b>VELOCITY TRAVERSE DATA</b>				
9. Stack area, ft. <sup>2</sup>	A	18.60	18.60	18.60
10. Absolute stack gas pressure, in. Hg.	$P_s$	30.02	30.02	30.00
11. Barometric pressure, in. Hg.	$P_{bar}$	30.02	30.02	30.00
12. Avg. absolute stack temperature, R°	$T_s$	740	726	726
13. Average vel. head, ( $C_p = .84$ )	$\sqrt{dp}$	0.64	0.63	0.62
14. Average stack gas velocity, ft./sec.	$V_s$	43.82	42.69	42.10
<b>STACK MOISTURE CONTENT</b>				
15. Total water collected by train, ml.	$V_{ic}$	378.30	331.40	358.80
16. Moisture in stack gas, %	$B_{ws}$	19.46	19.08	20.32
<b>EMISSION DATA</b>				
17. Stack gas flow rate, dscf/hr.	$Q_{sd}$	1691	1687	1637
18. Stack gas flow rate, cfm	acfm	48903	47642	46984
19. PAH concentration, gr/dscf	$C_s$	0.00010	0.00020	0.00009
20. PAH concentration, lb/hr	E	0.024	0.048	0.021
<b>ORSAT DATA</b>				
21. Percent CO <sub>2</sub> by volume	CO <sub>2</sub>	4.60	4.50	4.80
22. Percent O <sub>2</sub> by volume	O <sub>2</sub>	14.40	14.90	15.10
23. Percent CO by volume	CO	.00	.00	.00
24. Percent N <sub>2</sub> by volume	N <sub>2</sub>	81.00	80.60	80.10

**NAME:** MACASPHALT (PAH)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**MOISTURE DETERMINATION  
 DRY GAS VOLUME**

$V_{m(std)} =$

$$V_m \left[ \frac{T_{(std)}}{T_m} \right] \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{P_{std}} \right] - 17.64 \frac{^{\circ}R}{\epsilon. Hg} Y V_m \left[ \frac{P_{bar} + \frac{\Delta H}{13.6}}{T_m} \right]$$

Where:

- $V_{m(std)}$  = Dry gas volume through meter at standard conditions, ft<sup>3</sup>.  
 $V_m$  = Dry gas volume measured by meter, ft<sup>3</sup>.  
 $P_{bar}$  = Barometric pressure at orifice meter, in. Hg.  
 $P_{std}$  = Standard absolute pressure, (29.92 in. Hg.).  
 $T_m$  = Absolute temperature at meter, °R.  
 $T_{std}$  = Standard absolute temperature, (528°R).  
 $\Delta H$  = Avg. pressure drop across orifice meter, in. H<sub>2</sub>O.  
 $Y$  = Dry gas meter calibration factor.  
 13.6 = Inches of water per Hg.

Run #1:

$$V_{m(std)} = (17.64)(.980)(79.821) \left[ \frac{30.02 + \frac{2.70}{13.6}}{566} \right] = 73.671 \text{ dscf}$$

Run #2:

$$V_{m(std)} = (17.64)(.980)(71.546) \left[ \frac{30.02 + \frac{2.12}{13.6}}{564} \right] = 66.175 \text{ dscf}$$

Run #3:

$$V_{m(std)} = (17.64)(.980)(70.457) \left[ \frac{30.00 + \frac{2.64}{13.6}}{555} \right] = 66.264 \text{ dscf}$$

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**TOTAL CONTAMINANTS BY WEIGHT: GRAIN LOADING**

PAH Concentration:  $C_s'$  gr/dscf

$$C_s' = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{M_n}{V_{m(\text{std})}} \right]$$

Where:

$C_s'$  = Concentration of PAH in stack gas, dry basis, corrected to standard conditions, gr/dscf.

$M_n$  = Total amount of PAH's collected, mg.

$V_{m(\text{std})}$  = Dry gas volume through meter at standard conditions, cu. ft.

Run #1:

$$C_s' = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{0.499}{73.671} \right] = 0.00010 \text{ gr/dscf}$$

Run #2:

$$C_s' = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{0.848}{66.175} \right] = 0.00020 \text{ gr/dscf}$$

Run #3:

$$C_s' = \left[ 0.0154 \frac{\text{gr}}{\text{mg}} \right] \left[ \frac{0.368}{66.264} \right] = 0.00009 \text{ gr/dscf}$$

**NAME:** MACASPHALT (PAH)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**PAH  
 CONVERSION TO mg/m<sup>3</sup>**

$$C, \text{mg/m}^3 = (C, \text{gr/dscf}) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right)$$

Where:

- C, mg/m<sup>3</sup> = Concentration as milligrams per cubic meter  
 C, gr/dscf = Concentration as grains per cubic foot  
 35.31 = Conversion of ft<sup>3</sup> to m<sup>3</sup>  
 0.0154 = Conversion from grains to milligrams

Run #1:

$$C, \text{mg/m}^3 = (0.00010) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 0.229$$

Run #2:

$$C, \text{mg/m}^3 = (0.00020) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 0.459$$

Run #3:

$$C, \text{mg/m}^3 = (0.00009) \left( \frac{35.31 \text{ ft}^3}{\text{m}^3} \right) \left( \frac{\text{mg}}{0.0154 \text{ gr}} \right) = 0.206$$

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### DRY MOLECULAR WEIGHT

$$M_d = 0.44 (\%CO_2) + 0.32 (\%O_2) + 0.28 (\%CO + \%N_2)$$

Where:

- $M_d$  = Dry molecular weight, lb/lb-mole.
- $\%CO_2$  = Percent carbon dioxide by volume, dry basis.
- $\%O_2$  = Percent oxygen by volume, dry basis.
- $\%N_2$  = Percent nitrogen by volume, dry basis.
- $\%CO$  = Percent carbon monoxide by volume, dry basis.
- 0.264 = Ratio of  $O_2$  to  $N_2$  in air, v/v.
- 0.28 = Molecular weight of  $N_2$  or  $CO$ , divided by 100.
- 0.32 = Molecular weight of  $O_2$  divided by 100.
- 0.44 = Molecular weight of  $CO_2$  divided by 100.

Run #1:

$$M_d = 0.44 (4.60\%) + 0.32 (14.40\%) + 0.28 (0.00\% + 81.00\%) = 29.31 \frac{\text{lb}}{\text{lb-mole}}$$

Run #2:

$$M_d = 0.44 (4.50\%) + 0.32 (14.90\%) + 0.28 (0.00\% + 80.60\%) = 29.32 \frac{\text{lb}}{\text{lb-mole}}$$

Run #3:

$$M_d = 0.44 (4.80\%) + 0.32 (15.10\%) + 0.28 (0.00\% + 80.10\%) = 29.37 \frac{\text{lb}}{\text{lb-mole}}$$

**NAME:** MACASPHALT (PAH)  
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**DATE:** December 2-4, 1992

### WATER VAPOR CONDENSED

$$V_{WC_{std}} = [V_f - V_i] \left[ \frac{P_w R T_{(std)}}{M_w P_{(std)}} \right] = 0.04707 [V_f - V_i]$$

$$V_{WSG_{std}} = [W_f - W_i] \left[ \frac{R T_{(std)}}{M_w P_{(std)}} \right] = 0.04715 [W_f - W_i]$$

Where:

- 0.04707 = Conversion factor, ft<sup>3</sup>/ml.  
 0.04715 = Conversion factor, ft<sup>3</sup>/g.  
 $V_{WC_{std}}$  = Volume of water vapor condensed (std. cond.), ml.  
 $V_{WSG_{std}}$  = Volume of water vapor collected in silica gel (standard conditions), ml.  
 $V_f - V_i$  = Final volume of impinger contents less initial volume, ml.  
 $W_f - W_i$  = Final weight of silica gel less initial weight, g.  
 $P_w$  = Density of water, 0.002201 lb/ml.  
 $R$  = Ideal gas constant, 21.85 in.Hg. (cu.ft./lb-mole)(°R).  
 $M_w$  = Molecular weight of water vapor, 18.0 lb/lb-mole.  
 $T_{std}$  = Absolute temperature at standard conditions, 528°R.  
 $P_{std}$  = Absolute pressure at standard conditions, 29.92 inches Hg.

Run 1:

$$\begin{aligned} V_{WC_{std}} &= (0.04707) (370.0) = 17.4 \text{ cu.ft} \\ V_{WSG_{std}} &= (0.04715) (8.3) = 0.4 \text{ cu.ft} \end{aligned}$$

Run 2:

$$\begin{aligned} V_{WC_{std}} &= (0.04707) (325.0) = 15.3 \text{ cu.ft} \\ V_{WSG_{std}} &= (0.04715) (6.4) = 0.3 \text{ cu.ft} \end{aligned}$$

Run 3:

$$\begin{aligned} V_{WC_{std}} &= (0.04707) (353.0) = 16.6 \text{ cu.ft} \\ V_{WSG_{std}} &= (0.04715) (5.8) = 0.3 \text{ cu.ft} \end{aligned}$$

**NAME:** MACASPHALT (PAH)  
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**DATE:** December 2-4, 1992

### MOISTURE CONTENT OF STACK GASES

$$B_{ws} = \left[ \frac{V_{wc_{std}} + V_{wsg_{std}}}{V_{wc_{std}} + V_{wsg_{std}} + V_{mstd}} \right] \times 100$$

Where:

$B_{ws}$  = Proportion of water vapor, by volume, in the gas stream.

$V_m$  = Dry gas volume measured by dry gas meter, dcf.

$V_{wc_{std}}$  = Volume of water vapor condensed, corrected to standard conditions, scf.

$V_{wsg_{std}}$  = Volume of water vapor collected in silica gel corrected to std. cond., scf.

Run 1:

$$B_{ws} = \left[ \frac{17.4 + 0.4}{17.4 + 0.4 + 73.671} \right] \times 100 = 19.46\%$$

Run 2:

$$B_{ws} = \left[ \frac{15.3 + 0.3}{15.3 + 0.3 + 66.175} \right] \times 100 = 19.08\%$$

Run 3:

$$B_{ws} = \left[ \frac{16.6 + 0.3}{16.6 + 0.3 + 66.264} \right] \times 100 = 20.32\%$$

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### MOLECULAR WEIGHT OF STACK GASES

$$M_s = M_d (1 - B_{ws}) + 18 (B_{ws})$$

Where:

$M_s$  = Molecular weight of stack gas, wet basis (lb./lb.-mole).

$M_d$  = Molecular weight of stack gas, dry basis (lb./lb.-mole).

Run #1:

$$M_s = 29.31 (1 - 19.46) + 18 (19.46) = 27.11 \text{ (lb./lb.-mole)}$$

Run #2:

$$M_s = 29.32 (1 - 19.08) + 18 (19.08) = 27.16 \text{ (lb./lb.-mole)}$$

Run #1:

$$M_s = 29.37 (1 - 20.32) + 18 (20.32) = 27.06 \text{ (lb./lb.-mole)}$$



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### STACK GAS VELOCITY

$$V_s = K_p C_p [\sqrt{\Delta P}]_{\text{avg}} \sqrt{\frac{T_s(\text{avg})}{P_s M_s}}$$

Where:

- $V_s$  = Average velocity of gas stream in stack, ft/sec.  
 $K_p$  = 85.49 ft/sec [(g/g·mole) - (mm Hg)/(°K)(mm H<sub>2</sub>O)]<sup>1/2</sup>  
 $C_p$  = Pitot tube coefficient, dimensionless.  
 $\Delta P$  = Velocity head of stack gas, in. H<sub>2</sub>O.  
 $P_{\text{bar}}$  = Barometric pressure at measurement site, in. Hg.  
 $P_g$  = Stack static pressure, in. Hg.  
 $P_s$  = Absolute stack gas pressure, in. Hg. =  $P_{\text{bar}} + P_g$   
 $P_{\text{std}}$  = Standard absolute pressure, 29.92 in. Hg.  
 $t_s$  = Stack temperature, °F.  
 $T_s$  = Absolute stack temperature, °R. = 460 +  $t_s$ .  
 $M_s$  = Molecular weight of stack gas, wet basis, lb/lb·mole.

Run #1:

$$V = (85.49) (.84) (0.64) \sqrt{\frac{740}{(30.02)(27.11)}} = 43.82 \text{ ft/sec}$$

Run #2:

$$V = (85.49) (.84) (0.63) \sqrt{\frac{726}{(30.02)(27.16)}} = 42.69 \text{ ft/sec}$$

Run #3:

$$V = (85.49) (.84) (0.62) \sqrt{\frac{726}{(30.00)(27.06)}} = 42.10 \text{ ft/sec}$$

STACK GAS FLOW RATE

$$Q_{sd} = 3600 [1 - B_{wc}] V_s A \left[ \frac{T_{std}}{T_{stk}} \right] \left[ \frac{P_s}{P_{std}} \right]$$

Where:

- $Q_{sd}$  = Dry volumetric stack gas flow rate corrected to standard conditions (dscf/hr).
- $A$  = Cross sectional area of stack (ft<sup>2</sup>).
- 3600 = Conversion factor (sec/hr).
- $T_{stk}$  = Absolute stack temperature (°R).
- $T_{std}$  = Standard absolute temperature (528°R).
- $P_{bar}$  = Barometric pressure at measurement site (in. Hg.).
- $P_g$  = Stack static pressure (in. Hg.).
- $P_s$  = Absolute stack gas pressure (in. Hg.) =  $P_{bar} + P_g$
- $P_{std}$  = Standard absolute pressure (29.92 in. Hg.).

Run #1:

$$Q_{sd} = 3600 (1 - .1946) (43.82) (18.60) \left[ \frac{528}{740} \right] \left[ \frac{30.02}{29.92} \right] = 1691806.7 \frac{\text{dscf}}{\text{hr}}$$

Run #2:

$$Q_{sd} = 3600 (1 - .1908) (42.69) (18.60) \left[ \frac{528}{726} \right] \left[ \frac{30.02}{29.92} \right] = 1687889.0 \frac{\text{dscf}}{\text{hr}}$$

Run #3:

$$Q_{sd} = 3600 (1 - .2032) (42.10) (18.60) \left[ \frac{528}{726} \right] \left[ \frac{30.00}{29.92} \right] = 1638962.0 \frac{\text{dscf}}{\text{hr}}$$

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### EMISSIONS RATE FROM STACK

$$E = \left[ \frac{(C_s) (Q_{sd})}{7,000 \text{ gr/lb}} \right] = 0.0000 \text{ lb/hr}$$

Where:

E = Emissions rate, lbs/hr.

$C_s$  = Concentration of PAH's in stack gas, dry basis, corrected to standard conditions, gr/dscf.

$Q_{sd}$  = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.

Run #1:

$$E = \left[ \frac{(0.00010) (1691806.7)}{7,000} \right] = 0.024 \text{ lbs/hr}$$

Run #2:

$$E = \left[ \frac{(0.00020) (1687889.0)}{7,000} \right] = 0.048 \text{ lbs/hr}$$

Run #3:

$$E = \left[ \frac{(0.00009) (1637962.0)}{7,000} \right] = 0.021 \text{ lbs/hr}$$

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**DATE:** December 2-4, 1992

### ISOKINETIC VARIATION

$$I = 100 T_s \left[ \frac{(0.002669) (V_{ic} + (V_m/T_m) (P_{bar} + \Delta H/13.6))}{60 \theta V_s P_s A_n} \right]$$

Where:

- I = Percent isokinetic sampling.
- 100 = Conversion to percent.
- $T_s$  = Absolute average stack gas temperature, °R.
- 0.002669 = Conversion factor, Hg - ft<sup>3</sup>/ml - °R.
- $V_{ic}$  = Total volume of liquid collected in impingers and silica gel, ml.
- $T_m$  = Absolute average dry gas meter temperature, °R.
- $P_{bar}$  = Barometric pressure at sampling site, in. Hg.
- $\Delta H$  = Average pressure differential across the orifice meter, in. H<sub>2</sub>O.
- 13.6 = Specific gravity of mercury.
- 60 = Conversion seconds to minutes.
- $\theta$  = Total sampling time, minutes.
- $V_s$  = Stack gas velocity, ft/sec.
- $P_s$  = Absolute stack gas pressure, in. Hg.
- $A_n$  = Cross sectional area of nozzle, ft<sup>2</sup>.

Run #1:

$$I = (100) (740) \left[ \frac{(0.002669) (378.30) + \frac{79.821}{566} \left[ 30.02 + \frac{2.70}{13.6} \right]}{60 (90.0) (43.82) (30.02) (.000576)} \right] = 93.8\%$$

Run #2:

$$I = (100) (726) \left[ \frac{(0.002669) (331.40) + \frac{71.546}{564} \left[ 30.02 + \frac{2.12}{13.6} \right]}{60 (90.0) (42.69) (30.02) (.000524)} \right] = 92.8\%$$

Run #3:

$$I = (100) (726) \left[ \frac{(0.002669) (358.80) + \frac{70.457}{555} \left[ 30.00 + \frac{2.64}{13.6} \right]}{60 (90.0) (42.10) (30.00) (.000576)} \right] = 87.1\%$$

## VI. CALCULATIONS

### D. SO<sub>2</sub>, THC, CO, NO<sub>x</sub> and CH<sub>4</sub>

NAME: MACASPHALT (Gaseous Compounds)

LOCATION: MELBOURNE, FLORIDA

DATE: December 2-4, 1992

**CO**  
**GASEOUS CONCENTRATION CONVERSION TO mg/m<sup>3</sup>**

Example Calculation

$$\text{ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 28.01 \text{ g} & 1,000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = \frac{\text{mg}}{\text{m}^3}$$

Where:

- ppm = Parts per million, dry basis
- $1 \times 10^{-6}$  = Conversion from parts per million
- 28.317 = Conversion of liters to  $\text{ft}^3$
- 35,3145 = Conversion of  $\text{ft}^3$  to  $\text{m}^3$
- $273/293^\circ\text{K}$  = Temperature correction to standard conditions
- 22.4  $\ell$  = Volumetric molar conversion @  $273^\circ\text{K}$
- 28.01 g/mole = Molecular weight of pollutant
- 1,000 mg/g = Conversion to milligrams

Run #1:

$$138.4 \text{ ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 28.01 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = 161.2 \frac{\text{mg}}{\text{m}^3}$$

Run #2:

$$138.4 \text{ ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 28.01 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = 161.2 \frac{\text{mg}}{\text{m}^3}$$

Run #3:

$$172.9 \text{ ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 28.01 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = 201.4 \frac{\text{mg}}{\text{m}^3}$$

**NAME:** MACASPHALT (Gaseous Compounds)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**SO<sub>2</sub>**  
**GASEOUS CONCENTRATION CONVERSION TO mg/m<sup>3</sup>**

Example Calculation

$$\text{ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 64.07 \text{ g} & 1,000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = \frac{\text{mg}}{\text{m}^3}$$

Where:

- ppm = Parts per million, dry basis
- $1 \times 10^{-6}$  = Conversion from parts per million
- 28.317 = Conversion of liters to ft<sup>3</sup>
- 35,3145 = Conversion of ft<sup>3</sup> to m<sup>3</sup>
- 273/293°K = Temperature correction to standard conditions
- 22.4ℓ = Volumetric molar conversion @ 273°K
- 64.07 g/mole = Molecular weight of pollutant
- 1,000 mg/g = Conversion to milligrams

Run #1:

$$146.1 \text{ ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 64.07 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = 389.4 \frac{\text{mg}}{\text{m}^3}$$

Run #2:

$$146.1 \text{ ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 64.07 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = 389.4 \frac{\text{mg}}{\text{m}^3}$$

Run #3:

$$129.9 \text{ ppm} \left| \begin{array}{c|c|c|c|c|c|c|c} 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 64.07 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \end{array} \right| = 346.2 \frac{\text{mg}}{\text{m}^3}$$

**NAME:** MACASPHALT (Gaseous Compounds)  
**LOCATION:** MELBOURNE, FLORIDA

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**NO<sub>x</sub>**  
**GASEOUS CONCENTRATION CONVERSION TO mg/m<sup>3</sup>**

Example Calculation

ppm	1	28.317 ℓ	35.3145 ft <sup>3</sup>	273°K	mole	46.01 g	1,000 mg	= $\frac{\text{mg}}{\text{m}^3}$
	1x10 <sup>-6</sup>	ft <sup>3</sup>	m <sup>3</sup>	293°K	22.4 ℓ	mole	g	

Where:

- ppm = Parts per million, dry basis
- 1x10<sup>-6</sup> = Conversion form parts per million
- 28.317 = Conversion of liters to ft<sup>3</sup>
- 35,3145 = Conversion of ft<sup>3</sup> to m<sup>3</sup>
- 273/293°K = Temperature correction to standard conditions
- 22.4ℓ = Volumetric molar conversion @ 273°K
- 46.01 g/mole = Molecular weight of pollutant
- 1,000 mg/g = Conversion to milligrams

Run #1:

128.1 ppm	1	28.317 ℓ	35.3145 ft <sup>3</sup>	273°K	mole	46.01 g	1000 mg	= 245.2 $\frac{\text{mg}}{\text{m}^3}$
	1x10 <sup>-6</sup>	ft <sup>3</sup>	m <sup>3</sup>	293°K	22.4 ℓ	mole	g	

Run #2:

128.1 ppm	1	28.317 ℓ	35.3145 ft <sup>3</sup>	273°K	mole	46.01 g	1000 mg	= 245.2 $\frac{\text{mg}}{\text{m}^3}$
	1x10 <sup>-6</sup>	ft <sup>3</sup>	m <sup>3</sup>	293°K	22.4 ℓ	mole	g	

Run #3:

111.2 ppm	1	28.317 ℓ	35.3145 ft <sup>3</sup>	273°K	mole	46.01 g	1000 mg	= 212.8 $\frac{\text{mg}}{\text{m}^3}$
	1x10 <sup>-6</sup>	ft <sup>3</sup>	m <sup>3</sup>	293°K	22.4 ℓ	mole	g	



**NAME:** MACASPHALT (Gaseous Compounds)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

72

**TOTAL HYDROCARBON EMISSIONS** - Convert ppm (wet) to ppm (dry)

$$\text{ppm}_d = \text{ppm}_w \left( \frac{100}{100 - B_{ws}} \right)$$

Where:

$\text{ppm}_d$  = Parts per million, dry basis, as carbon.

$\text{ppm}_w$  = Parts per million, wet basis, as carbon.

$B_{ws}$  = Proportion of water vapor, by volume, in the gas stream.

Run #1 =

$$(96.5) \left( \frac{100}{100 - 19.19} \right) = 119.4 \text{ ppm}_d$$

Run #2 =

$$(96.5) \left( \frac{100}{100 - 20.08} \right) = 120.7 \text{ ppm}_d$$

Run #3 =

$$(112.1) \left( \frac{100}{100 - 21.75} \right) = 143.3 \text{ ppm}_d$$

**NAME:** MACASPHALT (Gaseous Compounds)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**THC**  
**GASEOUS CONCENTRATION CONVERSION TO mg/m<sup>3</sup>**

Example Calculation

$$\text{ppm} \left| \begin{array}{|c|c|c|c|c|c|c|c|} \hline 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 16.04 \text{ g} & 1,000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \\ \hline \end{array} \right| = \frac{\text{mg}}{\text{m}^3}$$

Where:

- ppm = Parts per million, dry basis
- $1 \times 10^{-6}$  = Conversion from parts per million
- 28.317 = Conversion of liters to ft<sup>3</sup>
- 35,3145 = Conversion of ft<sup>3</sup> to m<sup>3</sup>
- 273/293°K = Temperature correction to standard conditions
- 22.4ℓ = Volumetric molar conversion @ 273°K
- 16.04 g/mole = Molecular weight of pollutant (CH<sub>4</sub>)
- 1,000 mg/g = Conversion to milligrams

Run #1:

$$119.4 \text{ ppm} \left| \begin{array}{|c|c|c|c|c|c|c|c|} \hline 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 16.04 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \\ \hline \end{array} \right| = 79.7 \frac{\text{mg}}{\text{m}^3}$$

Run #2:

$$120.7 \text{ ppm} \left| \begin{array}{|c|c|c|c|c|c|c|c|} \hline 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 16.04 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \\ \hline \end{array} \right| = 80.5 \frac{\text{mg}}{\text{m}^3}$$

Run #3:

$$143.3 \text{ ppm} \left| \begin{array}{|c|c|c|c|c|c|c|c|} \hline 1 & 28.317 \ell & 35.3145 \text{ ft}^3 & 273^\circ\text{K} & \text{mole} & 16.04 \text{ g} & 1000 \text{ mg} & \\ \hline 1 \times 10^{-6} & \text{ft}^3 & \text{m}^3 & 293^\circ\text{K} & 22.4 \ell & \text{mole} & \text{g} & \\ \hline \end{array} \right| = 95.6 \frac{\text{mg}}{\text{m}^3}$$

**NAME:** MACASPHALT (Gaseous Compounds)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**TOTAL CARBON MONOXIDE EMISSIONS: POUNDS PER HOUR**

$$E = (2.59 \times 10^{-9})(M_d)(\text{ppm}_d)(Q_{sd})(K)$$

Where:

$E$  = CO emissions rate, lbs/hr.

$2.59 \times 10^{-9}$  = Conversion factor, lbs/dscf.

$M_d$  = Dry molecular weight (CO = 28.01).

$Q_{sd}$  = Dry volumetric stack gas flow rate  
corrected to standard conditions, dscf/hr.

$\text{ppm}_d$  = Parts per million, dry basis.

$K$  = Constant (typically 1).

Run #1:

$$E = (2.59 \times 10^{-9}) (28.01) (138.4) (1,468,141.8) = 14.74 \text{ lbs/hr}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (28.01) (138.4) (1,622,188.0) = 16.29 \text{ lbs/hr}$$

Run #3:

$$E = (2.59 \times 10^{-9}) (28.01) (172.9) (1,537,914.5) = 19.29 \text{ lbs/hr}$$

**TOTAL SULFUR DIOXIDE EMISSIONS: POUNDS PER HOUR**

$$E = (2.59 \times 10^{-9})(M_d)(\text{ppm}_d)(Q_{sd})(K)$$

Where:

- E = SO<sub>2</sub> emissions rate, lbs/hr.
- $2.59 \times 10^{-9}$  = Conversion factor, lbs/dscf.
- M<sub>d</sub> = Dry molecular weight (SO<sub>2</sub> = 64.07).
- Q<sub>sd</sub> = Dry volumetric stack gas flow rate corrected to standard conditions, dscf/hr.
- ppm<sub>d</sub> = Parts per million, dry basis.
- K = Constant (typically 1).

Run #1:

$$E = (2.59 \times 10^{-9}) (64.07) (146.1) 1,468,141.8 = 35.59 \text{ lbs/hr}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (64.07) (146.1) 1,622,188.0 = 39.33 \text{ lbs/hr}$$

Run #3:

$$E = (2.59 \times 10^{-9}) (64.07) (129.9) 1,537,914.5 = 33.15 \text{ lbs/hr}$$

**NAME:** MACASPHALT (Gaseous Compounds)  
**LOCATION:** MELBOURNE, FLORIDA

**DATE:** December 2-4, 1992

**TOTAL NO<sub>x</sub> EMISSIONS: POUNDS PER HOUR**

$$E = (2.59 \times 10^{-9})(M_d)(\text{ppm}_d)(Q_{sd})(K)$$

Where:

$E$  = NO<sub>x</sub> as NO<sub>2</sub> emissions rate, lbs/hr.

$2.59 \times 10^{-9}$  = Conversion factor, lbs/dscf.

$M_d$  = Dry molecular weight (NO<sub>2</sub> = 46.01).

$Q_{sd}$  = Dry volumetric stack gas flow rate  
corrected to standard conditions, dscf/hr.

$\text{ppm}_d$  = Parts per million, dry basis.

$K$  = Constant (typically 1).

Run #1:

$$E = (2.59 \times 10^{-9}) (46.01) (128.1) (1,468,141.8) = 22.41 \text{ lbs/hr}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (46.01) (128.1) (1,622,180.0) = 24.76 \text{ lbs/hr}$$

Run #3:

$$E = (2.59 \times 10^{-9}) (46.01) (111.2) (1,537,914.5) = 20.38 \text{ lbs/hr}$$

**TOTAL HYDROCARBON EMISSIONS: POUNDS PER HOUR**

$$E = (2.59 \times 10^{-9})(M_d)(\text{ppm}_d)(Q_{sd})(K)$$

Where:

E = THC as CH<sub>4</sub> emissions rate, lbs/hr.

$2.59 \times 10^{-9}$  = Conversion factor, lbs/dscf.

$M_d$  = Dry molecular weight (CH<sub>4</sub> = 16.04).

$Q_{sd}$  = Dry volumetric stack gas flow rate  
corrected to standard conditions, dscf/hr.

$\text{ppm}_d$  = Parts per million, dry basis.

K = Constant (typically 1).

Run #1:

$$E = (2.59 \times 10^{-9}) (16.04) (119.4) (1,468,141.8) = 7.28 \text{ lbs/hr}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (16.04) (120.7) (1,622,180.0) = 8.13 \text{ lbs/hr}$$

Run #3:

$$E = (2.59 \times 10^{-9}) (16.04) (143.3) (1,537,914.5) = 9.16 \text{ lbs/hr}$$

**TOTAL METHANE EMISSIONS: POUNDS PER HOUR**

$$E = (2.59 \times 10^{-9})(M_d)(\text{ppm}_d)(Q_{sd})(K)$$

Where:

$E$  =  $\text{CH}_4$  emissions rate, lbs/hr.

$2.59 \times 10^{-9}$  = Conversion factor, lbs/dscf.

$M_d$  = Dry molecular weight ( $\text{CH}_4 = 16.04$ ).

$Q_{sd}$  = Dry volumetric stack gas flow rate  
corrected to standard conditions, dscf/hr.

$\text{ppm}_d$  = Parts per million, dry basis.

$K$  = Constant (typically 1).

Run #1:

$$E = (2.59 \times 10^{-9}) (16.04) (6.27) (1,468,141.8) = 0.38 \text{ lbs/hr}$$

Run #2:

$$E = (2.59 \times 10^{-9}) (16.04) (21.02) (1,622,180.0) = 1.42 \text{ lbs/hr}$$

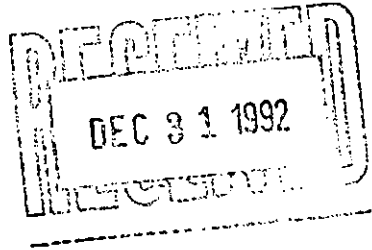
Run #3:

$$E = (2.59 \times 10^{-9}) (16.04) (22.50) (1,537,914.5) = 1.44 \text{ lbs/hr}$$

## **VII. LABORATORY ANALYSIS RESULTS**

### **A. Formaldehyde Analysis Results**





8600 Kanis Road  
Little Rock, AR 72204-2322  
(501) 224-5060

Ramcon Environmental Corporation (C-488)  
6707 Fletcher Creek Cove  
Memphis, TN 38134

December 28, 1992

ATTN: Mr. Joe Sewell

Control No. 11643

Sample Description: Six (6) impinger solutions received on 12/17/92  
Plant: Mac Asphalt - NAPA; P.O. Nos. 080102, 080103

Results:

<u>Sample Identification</u>	<u>Volume, ml</u>	<u>Formaldehyde, mg</u>
Run 1, 12/9/92	530	8.8
Run 2, 12/9/92	700	8.8
Run 3, 12/9/92	685	5.8
Run 1, 12/4/92	495	0.063
Run 2, 12/4/92	495	4.2
Run 3, 12/4/92	575	0.60

Method: 40 CFR Part 266, Appendix IX Section 3.6 Method 0011A

AMERICAN INTERPLEX CORPORATION

By Steven Lovell  
Steven Lovell  
Technical Director

SL/td

**VII. LABORATORY ANALYSIS RESULTS**

**B. PAH Analysis Results**

Triangle Laboratories of RTP, Inc.  
801 Capitola Dr.  
Durham, NC 27713  
(919) 544-5729

Sample File : GL505  
Response File : GL500  
Date Analyzed : 01/03/93  
Date Reported : 01/05/93  
Project Number: 22680

Sample ID: RUN#1  
TLI ID: 62.51.1A-I  
Dilution Factor: 4.00

Quantitation Results Method 8270

Analyte	Area	RF	SCAN	ISID	Amt. (ug)	Code	Quan	FLAG
1,4-Dichlorobenzene-d4	3692		420	1		I		
Naphthalene-d8	16898		599	2		I		
2-Methylnaphthalene	12192	0.679	705	2	170.01	D	40.0	
Naphthalene	12447	1.001	602	2	117.74	D	40.0	
Acenaphthene-d10	7882		857	3		I		
Acenaphthene	0	0.957	0	3	0.42	ND	40.0	
Fluorene	0	1.180	0	3	0.34	ND	40.0	
2-Chloronaphthalene	0	0.971	0	3	0.42	ND	40.0	
Acenaphthylene	0	1.680	0	3	0.24	ND	40.0	
Phenanthrene-d10	12369		1076	4		I		
Phenanthrene	0	0.921	0	4	0.28	ND	40.0	
Anthracene	0	0.944	0	4	0.27	ND	40.0	
Fluoranthene	2581	1.115	1256	4	29.95	E	40.0	
Chrysene-d12	15209		1471	5		I		
Chrysene	0	0.995	0	5	0.21	ND	40.0	
Pyrene	4322	1.167	1288	5	38.97	E	40.0	
Benzo(a)anthracene	0	0.978	0	5	0.22	ND	40.0	
Perylene-d12	13417		1741	6		I		
Benzo(b)fluoranthene	0	1.380	0	6	0.17	ND	40.0	
Benzo(k)fluoranthene	0	1.785	0	6	0.13	ND	40.0	
Benzo(e)pyrene	0	1.423	0	6	0.17	ND	40.0	
Benzo(a)pyrene	0	1.321	0	6	0.18	ND	40.0	
Perylene	0	0.688	0	6	0.35	ND	40.0	
Indeno(1,2,3-cd)pyrene	0	0.876	0	6	0.27	ND	40.0	
Dibenz(a,h)anthracene	0	0.875	0	6	0.27	ND	40.0	
Benzo(g,h,i)perylene	1004	1.068	2016	6	11.22	E	40.0	

Surrogate Summary	Area	RF	SCAN	ISID	Amount (ug)	Code	%REC
Anthracene-d10	4253	0.508	1084	4	108.32	D	108.3
Pyrene-d10	6179	1.066	1286	5	60.98	D	61.0

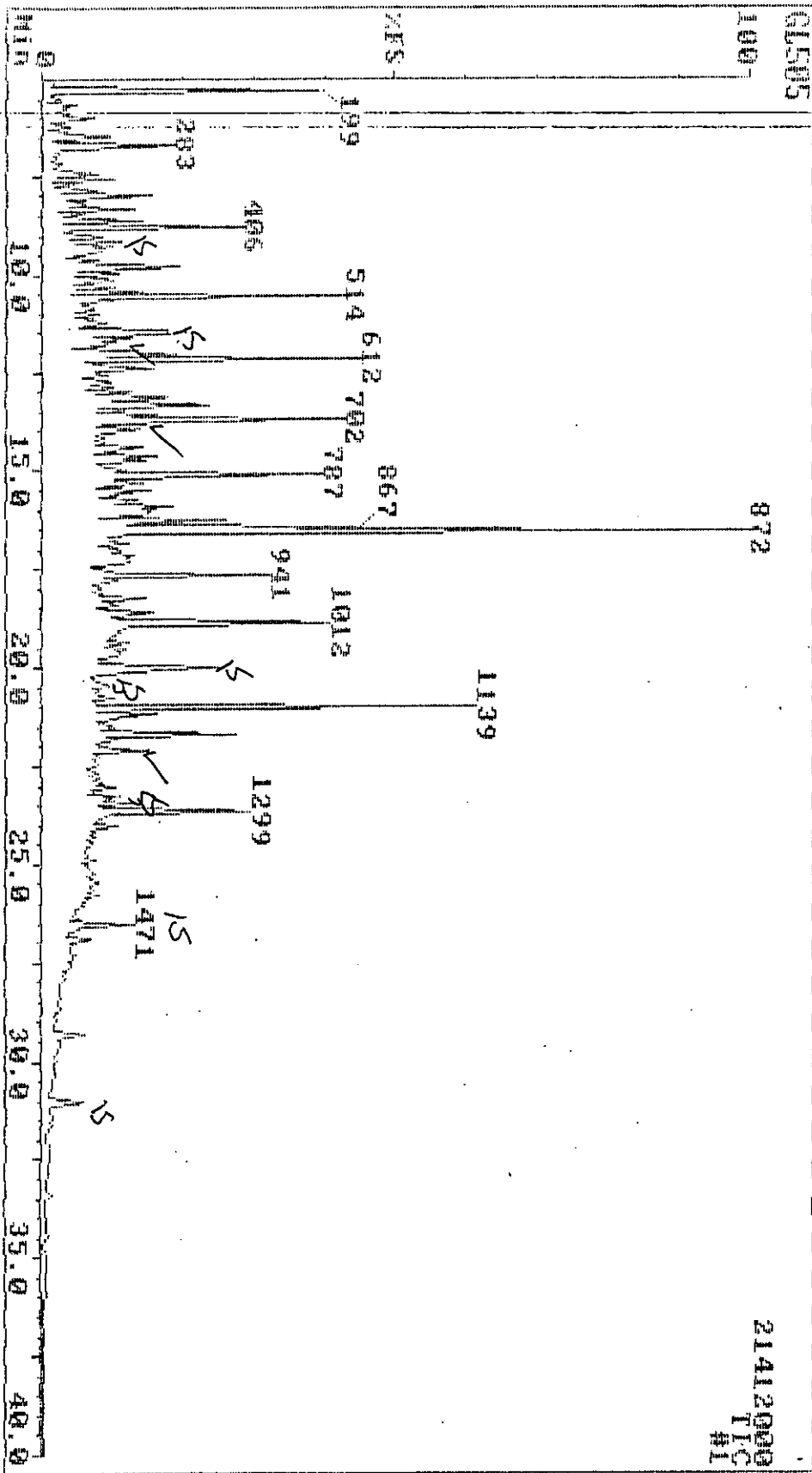
Reviewed by J. Lyon Date 1/5/93  
ND -Not Detected; D- Detected; E- Estimated; I- Internal Standard

Orgrep v2.5

03-Jan-93 23:51  
Sample: HUH #1 (1:4 DIL.)

Triangle Laboratories of RTP, Inc.  
22680

(919) 544-5729  
Instrument G



21412000  
TIC  
#1

AT-5-43

No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	93	52	97	0	369290	bb	420	152 1,4-Dichlorobenzene-d4
2	90	54	90	0	1689900	vv	599	136 Naphthalene-d8
3	75	33	87	0	788270	vv	857	164 Acenaphthene-d10
4	88	46	94	0	1236900	vv	1076	188 Phenanthrene-d10
5	92	61	97	-1	1520900	vv	1471	240 Chrysene-d12
6	100	66	94	0	1341700	bv	1741	264 Perylene-d12
7	0	0	0	0	0		0	112 2-Fluorophenol
8	0	0	0	0	0		0	132 2-Chlorophenol-d4
9	0	0	0	0	0		0	99 Phenol-d5
10	0	0	0	0	0		0	152 1,2-Dichlorobenzene-d4
11	0	0	0	0	0		0	82 Nitrobenzene-d5
12	0	0	0	0	0		0	185 1,3,5-Trichlorobenzene-d3
13	0	0	0	0	0		0	240 1,4-Dibromobenzene-d4
14	0	0	0	0	0		0	172 2-Fluorobiphenyl
15	0	0	0	0	0		0	330 2,4,6-Tribromophenol
16	68	26	83	-1	425390	vv	1084	188 Anthracene-d10
17	81	38	92	0	617930	vv	1286	212 Pyrene-d10
18	0	0	0	0	0		0	244 Terphenyl-d14
19	84	38	97	0	1244800	vv	602	128 Naphthalene
20	88	54	87	0	1219200	vb	705	142 2-Methylnaphthalene
21	0	0	0	0	0		0	162 2-Chloronaphthalene
22	0	0	0	0	0		0	152 Acenaphthylene
23	0	0	0	0	0		0	154 Acenaphthene
24	0	0	0	0	0		0	166 Fluorene
25	0	0	0	0	0		0	266 Pentachlorophenol
26	0	0	0	0	0		0	178 Phenanthrene
27	0	0	0	0	0		0	178 Anthracene
28	66	24	89	-1	258180	vb	1256	202 Fluoranthene
29	73	30	87	-1	432270	vv	1288	202 Pyrene
30	0	0	0	0	0		0	228 Benzo(a)anthracene
31	0	0	0	0	0		0	228 Chrysene
32	0	0	0	0	0		0	252 Benzo(b)fluoranthene
33	0	0	0	0	0		0	252 Benzo(k)fluoranthene
34	0	0	0	0	0		0	252 Benzo(e)pyrene
35	0	0	0	0	0		0	252 Benzo(a)pyrene
36	0	0	0	0	0		0	252 Perylene
37	0	0	0	0	0		0	276 Indeno(1,2,3-cd)pyrene
38	0	0	0	0	0		0	278 Dibenz(a,h)anthracene
39	42	21	83	-4	100470	bb	2016	276 Benzo(g,h,i)perylene

*GL*  
1-5-93

03-Jan-93 23:51

Triangle Laboratories of RTP, Inc.

(919) 544-5729

Sample: RUN #1 (1:4 DIL.)

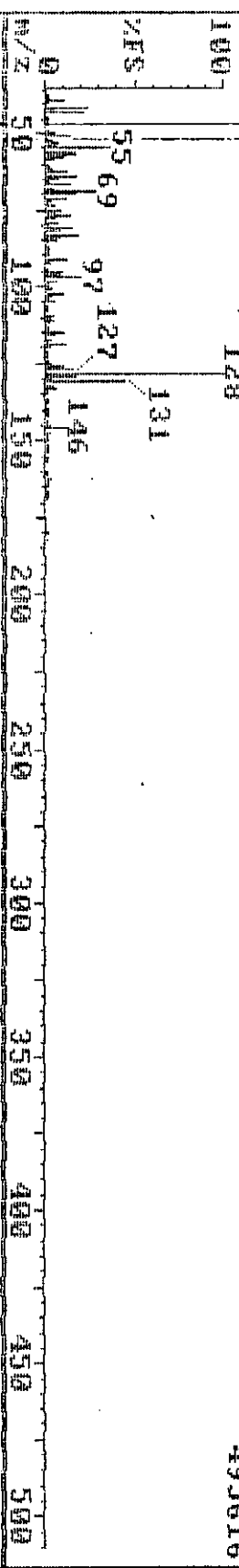
22600

Instrument G

GL505 602 (12.034)

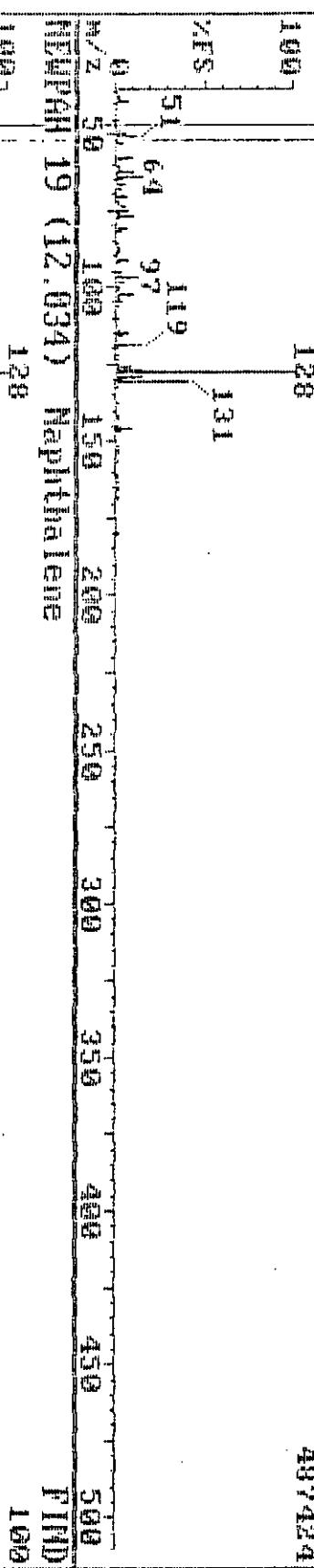
128

495616



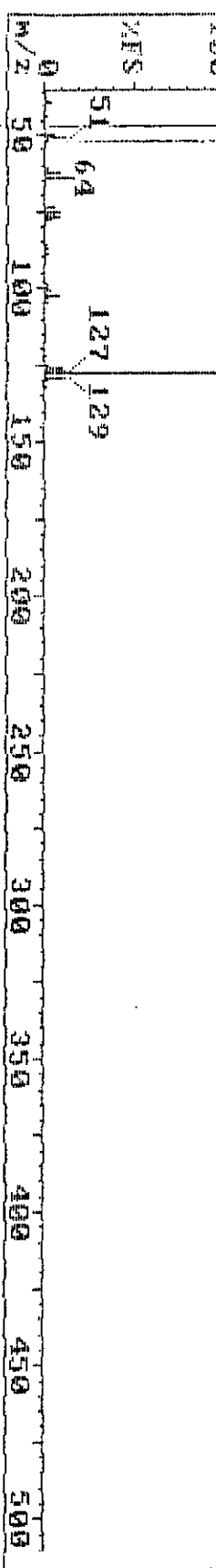
GL505 602 (12.034) REFINE

497434



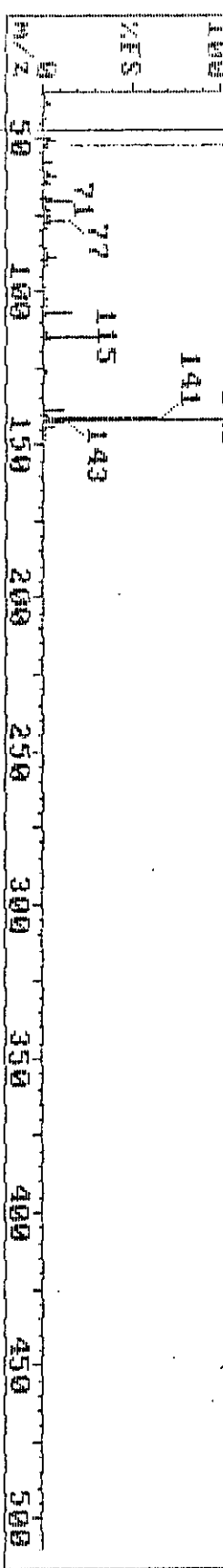
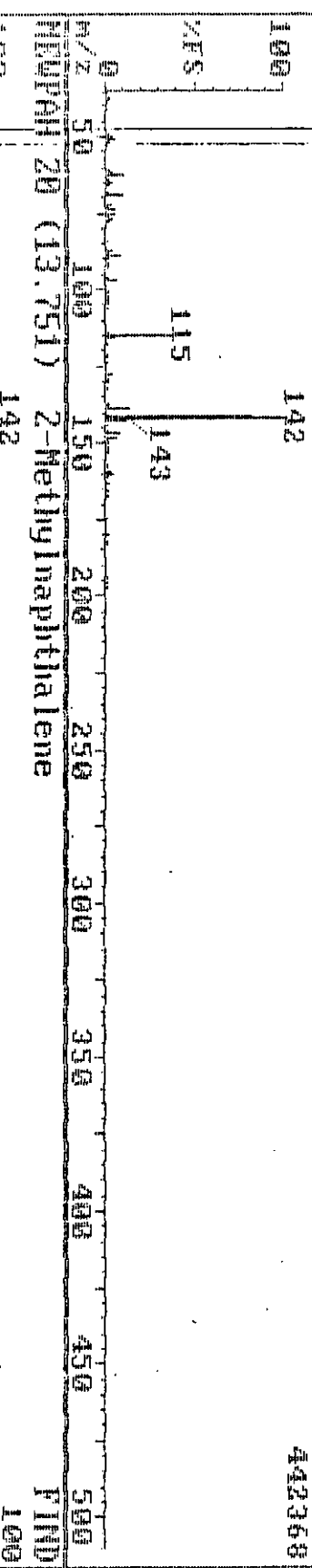
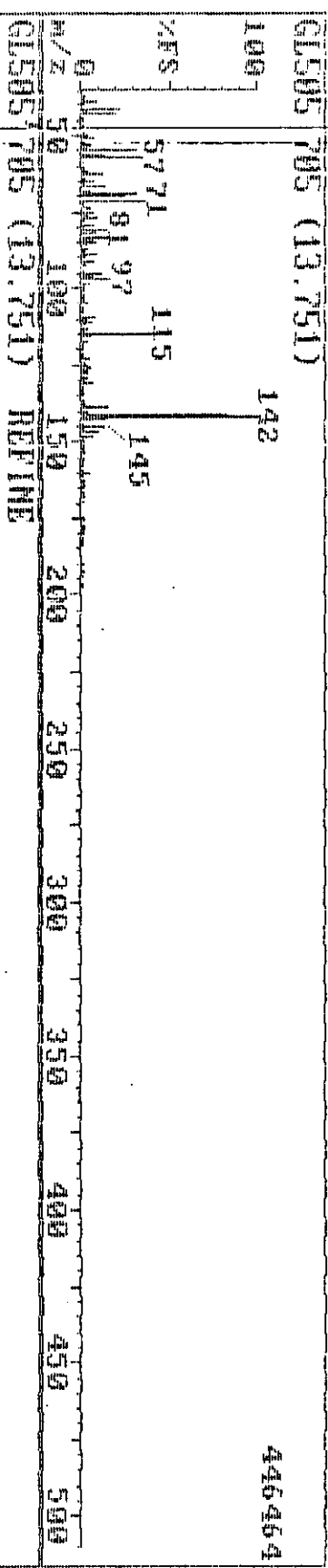
HEURAN 19 (12.034) Naphthalene

FIND 100



M/Z 0 50 100 150 200 250 300 350 400 450 500

03-Jan-93 23:51 Triangle Laboratories of RTP, Inc. (919) 544-5729  
 Sample: MM H1 (1:4 DIL.) 22688 Instrument G



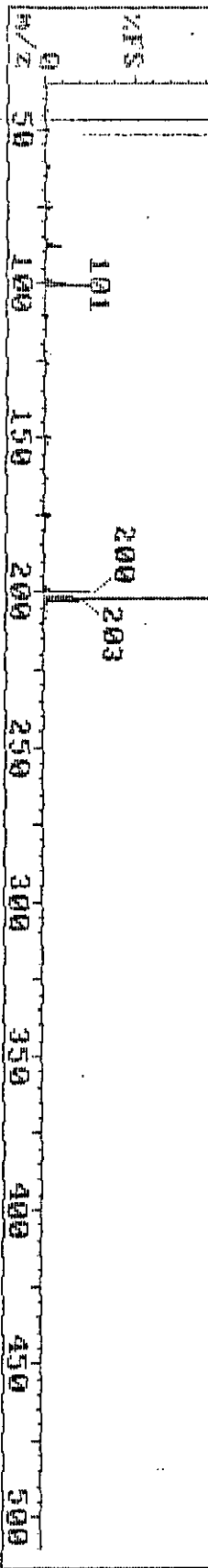
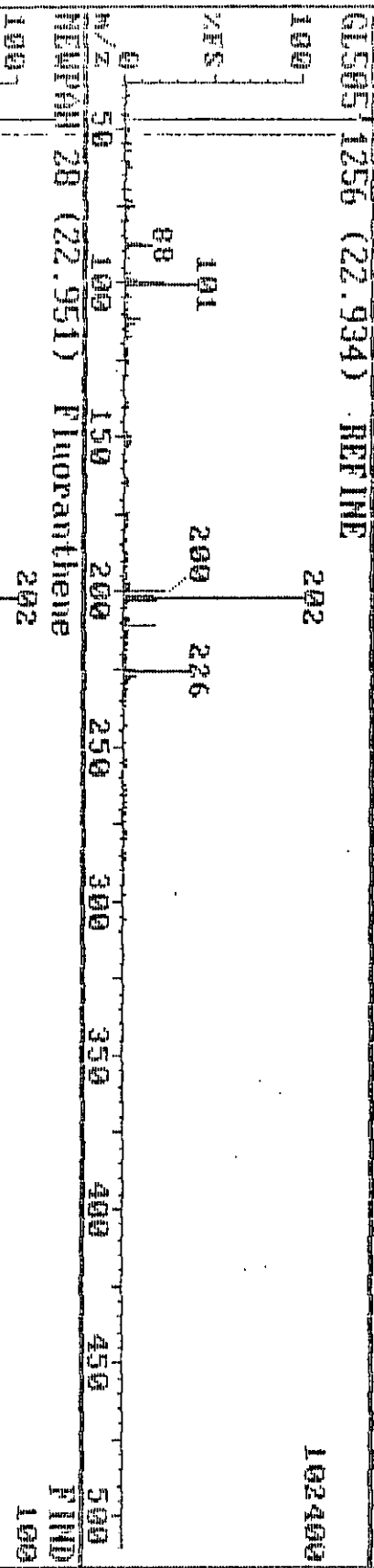
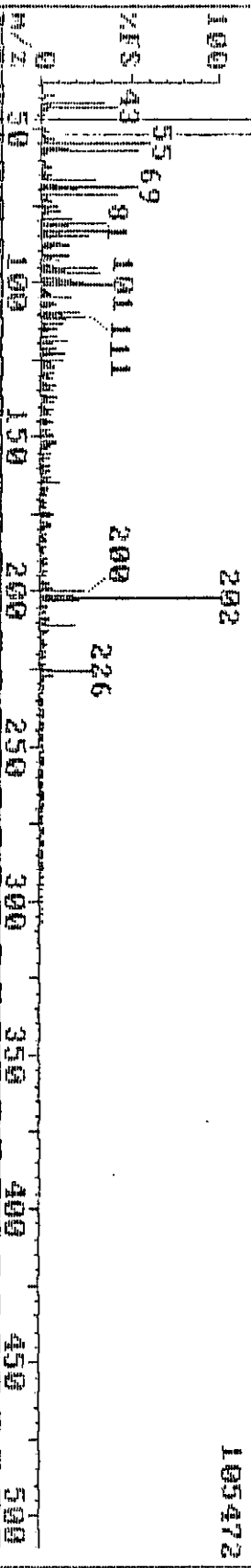
442368

446464

FIND 100

03-Jan-98 23:51 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: MUN #1 (1:4 DIL.) 226B0 Instrument G

GL505 1256 (22.935)

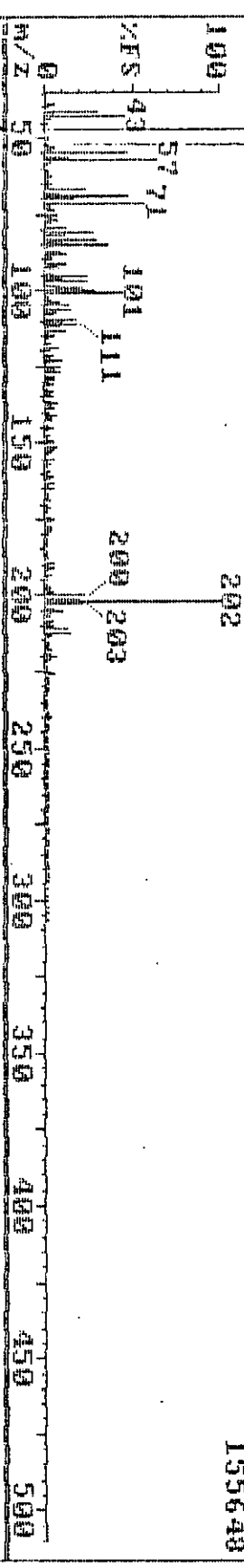




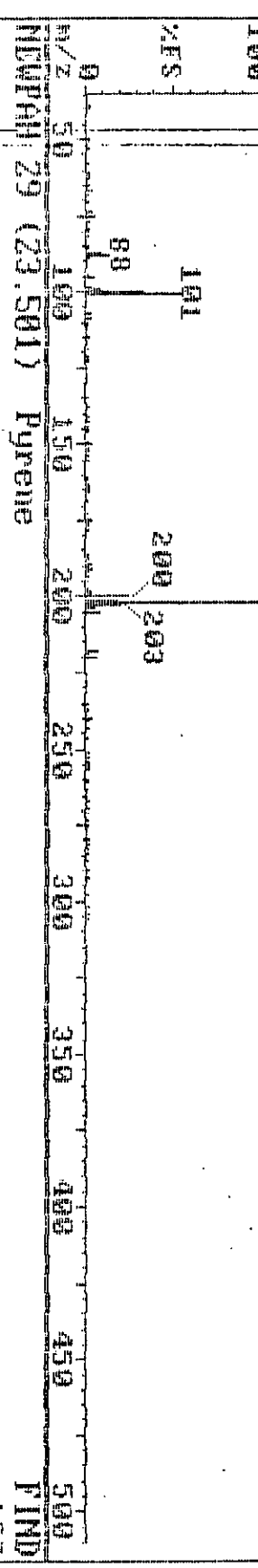
03-Jan-93 23:51 Triangle Laboratories of RTP, Inc. (919) 544-5729

Sample: NUM #1 (1:4 DIL.) 22680 Instrument G

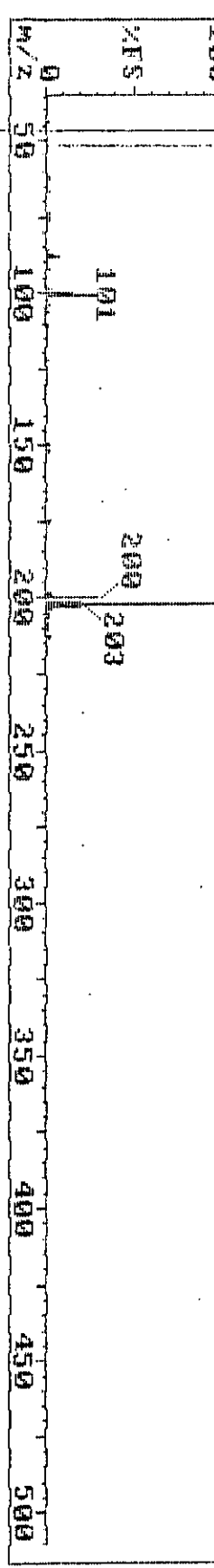
GL505 1288 (23.468) 155648



GL505 1288 (23.467) HEPTANE 152576

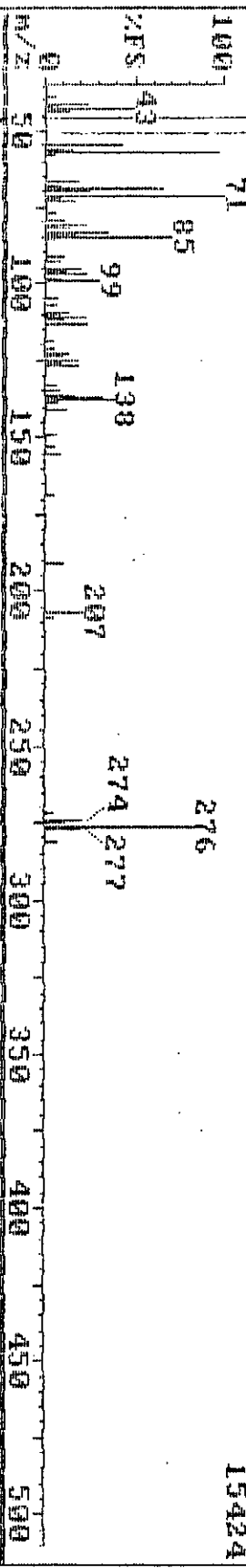


NUMPAN 29 (23.501) Pyrene FIND 100

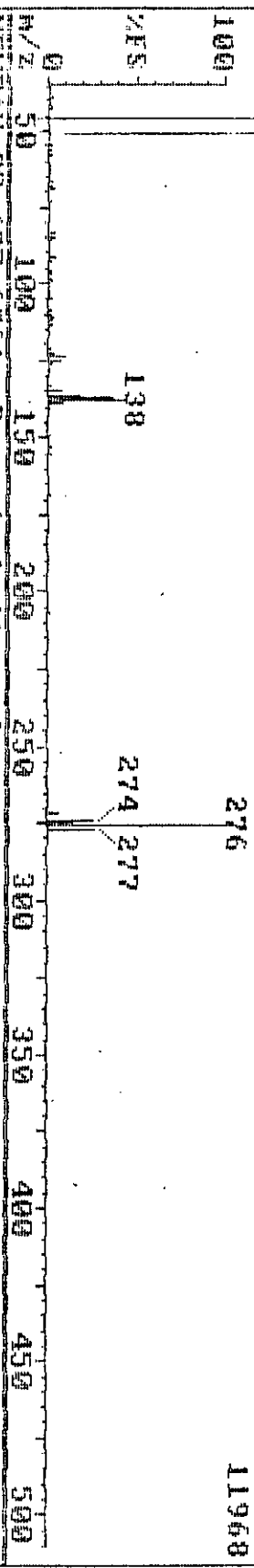


03-Jan-93 23:51 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #1 (1:4 DIL.) Z2680 Instrument G

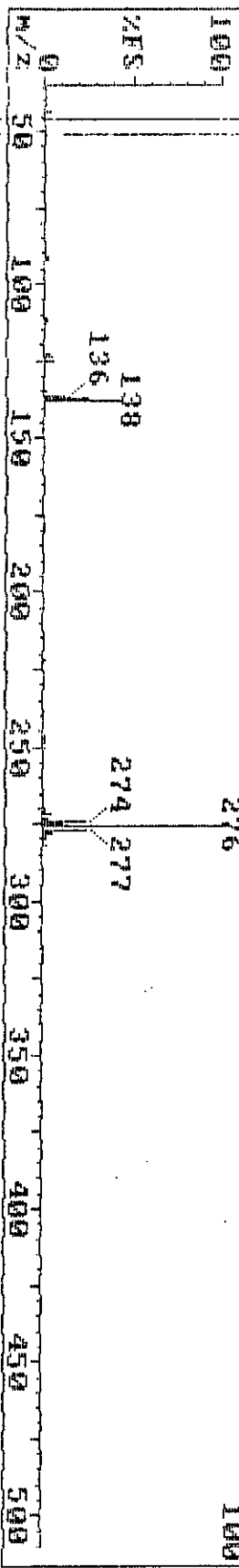
GL505 2016 (35.602) 15424



GL505/2016 (35.604) REFINE 11968



MPAH 39 (35.606) Benzo(g,h,i)perylene FIND 100



Triangle Laboratories of RTP, Inc.  
 801 Capitola Dr.  
 Durham, NC 27713  
 (919) 544-5729

Sample File : GL506  
 Response File : GL500  
 Date Analyzed : 01/04/93  
 Date Reported : 01/05/93  
 Project Number : 22680

Sample ID: RUN#2  
 TLI ID: 62.51.2A-I  
 Dilution Factor: 4.00

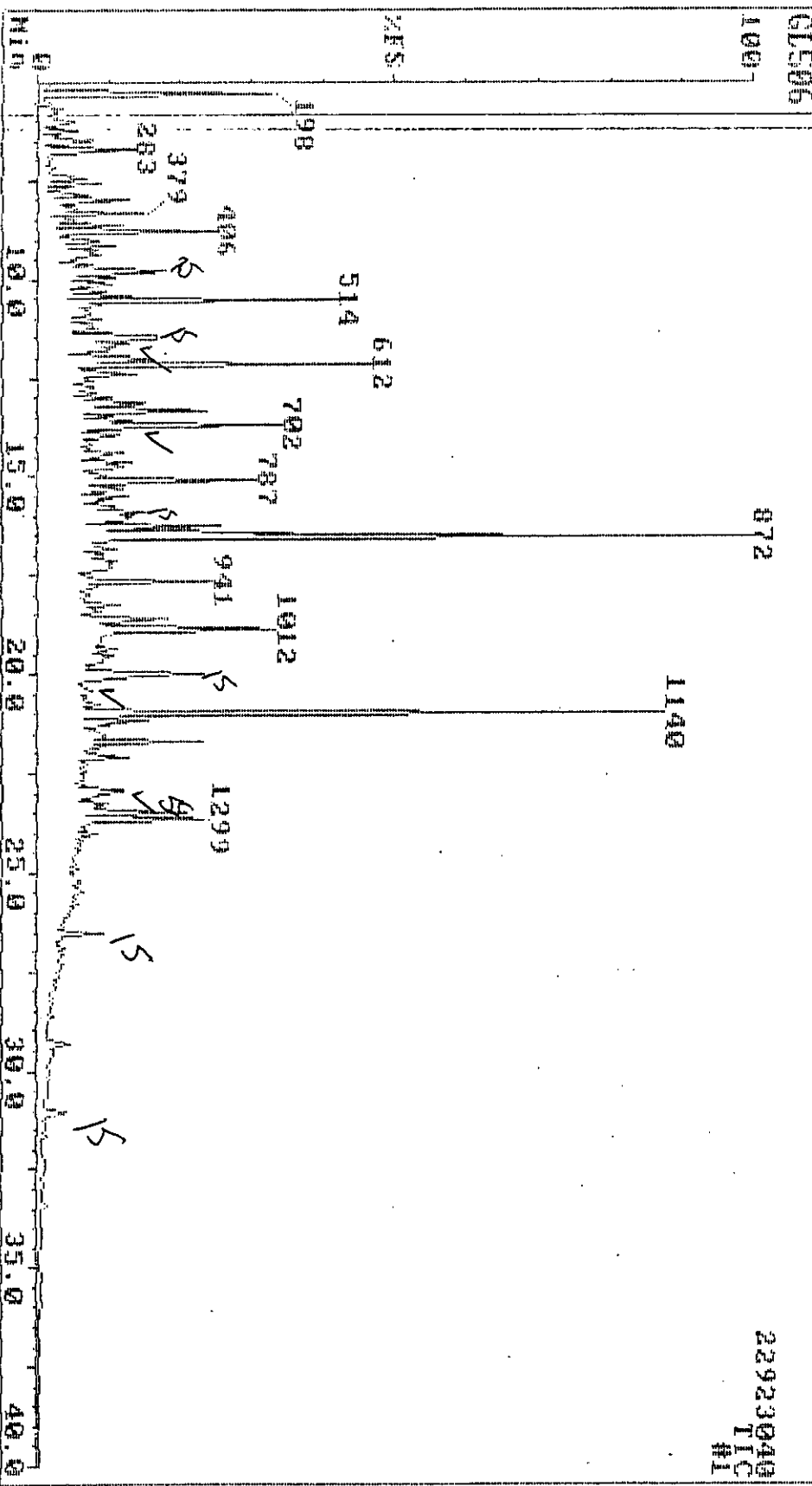
Quantitation Results Method 8270

Analyte	Area	RF	SCAN	ISID	Amt. Code (ug)	Quan	FLAG	Limit
1,4-Dichlorobenzene-d4	4012		420	1	I			
Naphthalene-d8	17425		599	2	I			
2-Methylnaphthalene	9852	0.679	705	2	133.23 D	40.0		
Naphthalene	9987	1.001	602	2	91.61 D	40.0		
Acenaphthene-d10	7835		857	3	I			
Acenaphthene	0	0.957	0	3	0.43 ND	40.0		
Fluorene	0	1.180	0	3	0.35 ND	40.0		
2-Chloronaphthalene	0	0.971	0	3	0.42 ND	40.0		
Acenaphthylene	0	1.680	0	3	0.24 ND	40.0		
Phenanthrene-d10	13104		1076	4	I			
Phenanthrene	9763	0.921	1080	4	129.43 D	40.0		
Anthracene	0	0.944	0	4	0.26 ND	40.0		
Fluoranthene	11941	1.115	1256	4	130.76 D	40.0		
Chrysene-d12	8812		1471	5	I			
Chrysene	0	0.995	0	5	0.36 ND	40.0		
Pyrene	23332	1.167	1289	5	363.00 D	40.0		
Benzo(a)anthracene	0	0.978	0	5	0.37 ND	40.0		
Perylene-d12	8499		1742	6	I			
Benzo(b)fluoranthene	0	1.380	0	6	0.27 ND	40.0		
Benzo(k)fluoranthene	0	1.785	0	6	0.21 ND	40.0		
Benzo(e)pyrene	0	1.423	0	6	0.26 ND	40.0		
Benzo(a)pyrene	0	1.321	0	6	0.28 ND	40.0		
Perylene	0	0.688	0	6	0.55 ND	40.0		
Indeno(1,2,3-cd)pyrene	0	0.876	0	6	0.43 ND	40.0		
Dibenz(a,h)anthracene	0	0.875	0	6	0.43 ND	40.0		
Benzo(g,h,i)perylene	0	1.068	0	6	0.35 ND	40.0		

Surrogate Summary	Area	RF	SCAN	ISID	Amount (ug)	Code	%REC
Anthracene-d10	4487	0.508	1084	4	107.86 D		107.9
Pyrene-d10	6062	1.066	1286	5	103.25 D		103.3

Received by Johnson Date 1/5/93  
 ND -Not Detected; D- Detected; E- Estimated; I- Internal Standard

04-Jan-93 00:43 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN 42 (1:4 DIL.) 22680 Instrument G



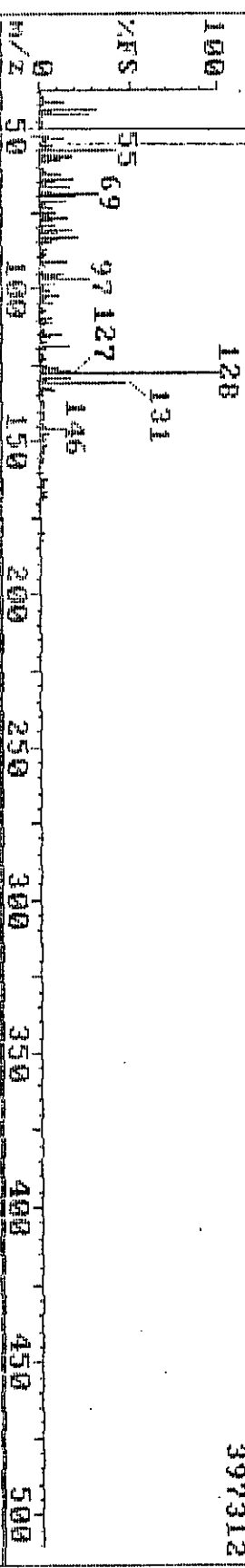
*Handwritten:* 9/1-5-93

No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	Qn	Name
1	93	52	97	0	401220	bv	420	152	1,4-Dichlorobenzene-d4
	90	54	90	0	1742500	vv	599	136	Naphthalene-d8
	74	32	87	0	783560	vv	857	164	Acenaphthene-d10
4	82	48	94	0	1310400	vv	1076	188	Phenanthrene-d10
5	87	55	95	-1	881240	bb	1471	240	Chrysene-d12
6	91	60	96	1	849980	bb	1742	264	Perylene-d12
7	0	0	0	0	0		0	112	2-Fluorophenol
8	0	0	0	0	0		0	132	2-Chlorophenol-d4
9	0	0	0	0	0		0	99	Phenol-d5
10	0	0	0	0	0		0	152	1,2-Dichlorobenzene-d4
11	0	0	0	0	0		0	82	Nitrobenzene-d5
12	0	0	0	0	0		0	185	1,3,5-Trichlorobenzene-d3
13	0	0	0	0	0		0	240	1,4-Dibromobenzene-d4
14	0	0	0	0	0		0	172	2-Fluorobiphenyl
15	0	0	0	0	0		0	330	2,4,6-Tribromophenol
16	71	29	85	-1	448780	vv	1084	188	Anthracene-d10
17	78	35	90	0	606200	vv	1286	212	Pyrene-d10
18	0	0	0	0	0		0	244	Terphenyl-d14
19	81	34	96	0	998720	vv	602	128	Naphthalene
20	87	53	86	0	985210	vb	705	142	2-Methylnaphthalene
21	0	0	0	0	0		0	162	2-Chloronaphthalene
22	0	0	0	0	0		0	152	Acenaphthylene
23	0	0	0	0	0		0	154	Acenaphthene
24	0	0	0	0	0		0	166	Fluorene
25	0	0	0	0	0		0	266	Pentachlorophenol
26	75	29	91	0	976310	vv	1080	178	Phenanthrene
27	0	0	0	0	0		0	178	Anthracene
	87	53	97	-1	1194100	vb	1256	202	Fluoranthene
29	98	62	95	0	2333200	vv	1289	202	Pyrene
30	0	0	0	0	0		0	228	Benzo(a)anthracene
31	0	0	0	0	0		0	228	Chrysene
32	0	0	0	0	0		0	252	Benzo(b)fluoranthene
33	0	0	0	0	0		0	252	Benzo(k)fluoranthene
34	0	0	0	0	0		0	252	Benzo(e)pyrene
35	0	0	0	0	0		0	252	Benzo(a)pyrene
36	0	0	0	0	0		0	252	Perylene
37	0	0	0	0	0		0	276	Indeno(1,2,3-cd)pyrene
38	0	0	0	0	0		0	278	Dibenz(a,h)anthracene
39	0	0	0	0	0		0	276	Benzo(g,h,i)perylene

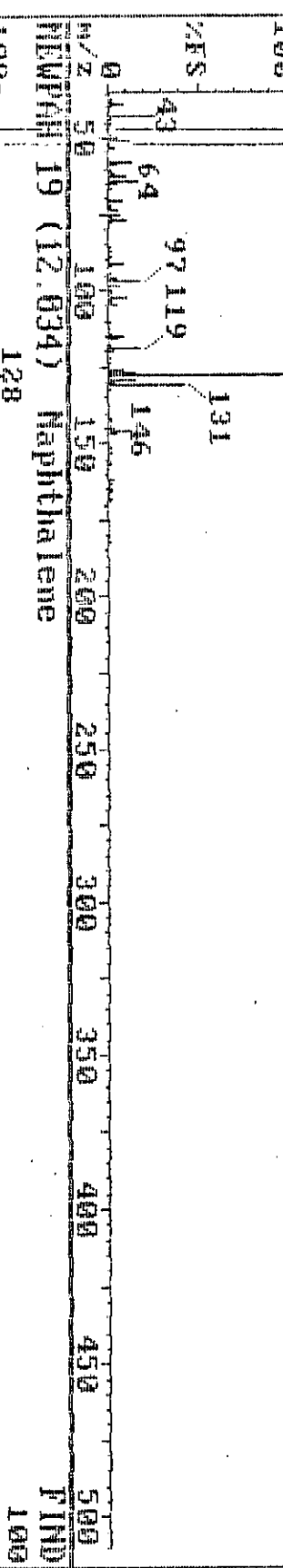
*JL*  
1-5-93

04-Jan-93 00:43 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: MUN #2 (1:4 DIL.) Z2680 Instrument G

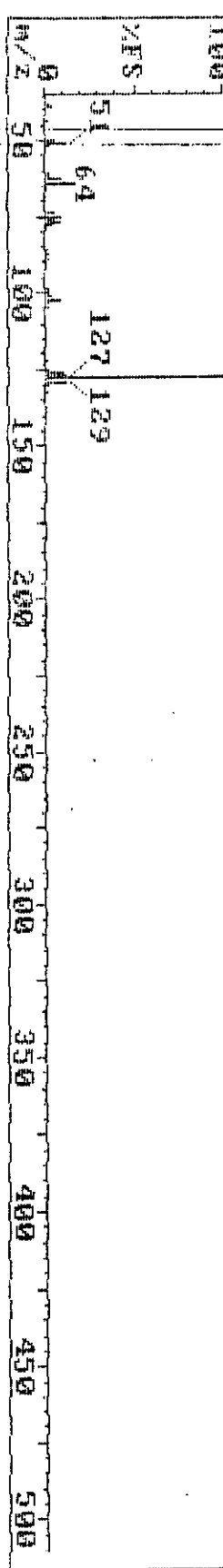
GL506 602 (12.034) 397312



389120



FIND 100



04-Jan-93 00:43

Triangle Laboratories of RTP, Inc.

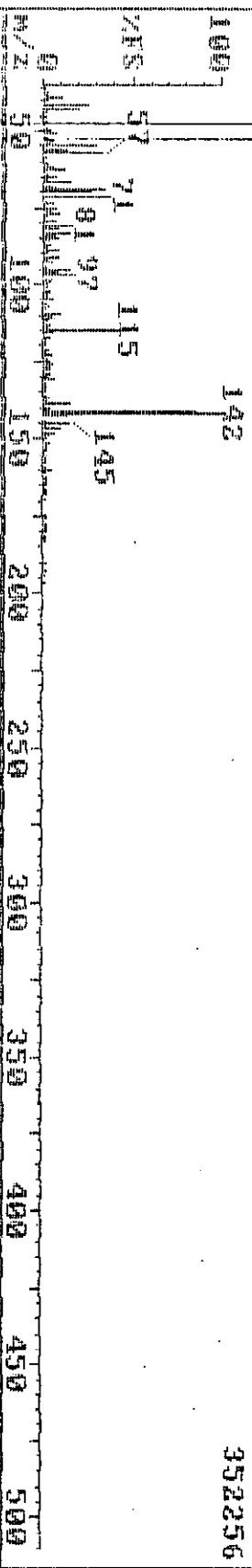
(919) 544-5729

Sample: MM #2 (1:4 DIL.)

22688

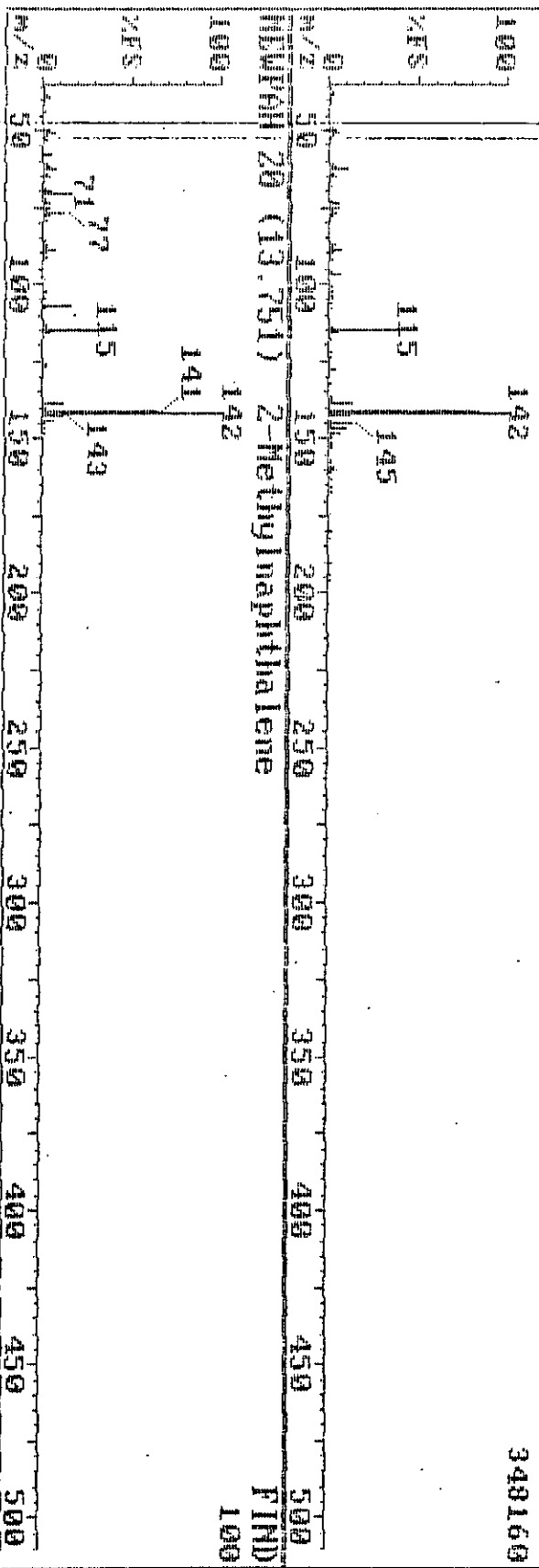
Instrument G

Q1586 705 (13.751)



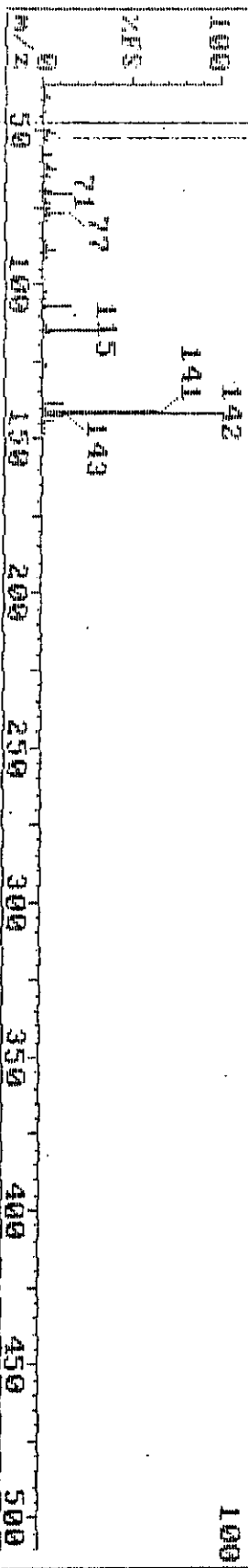
352256

Q1586 705 (13.751) REFINE



348160

HMW#11 20 (13.751) 2-Methylnaphthalene



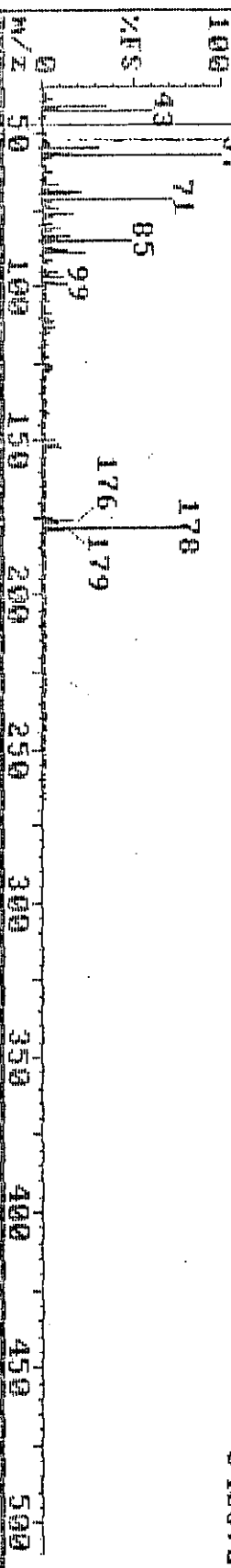
FIND

100

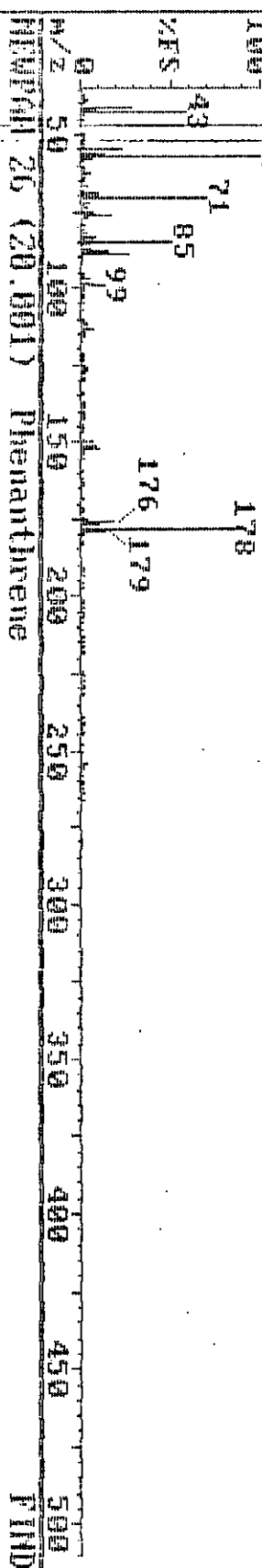
04-Jan-93 09:43 Triangle Laboratories of RTP, Inc. (919) 544-5729  
 Sample: MM 42 (1:4 DIL.) 22600 Instrument G

GL506 1000 (20.001)

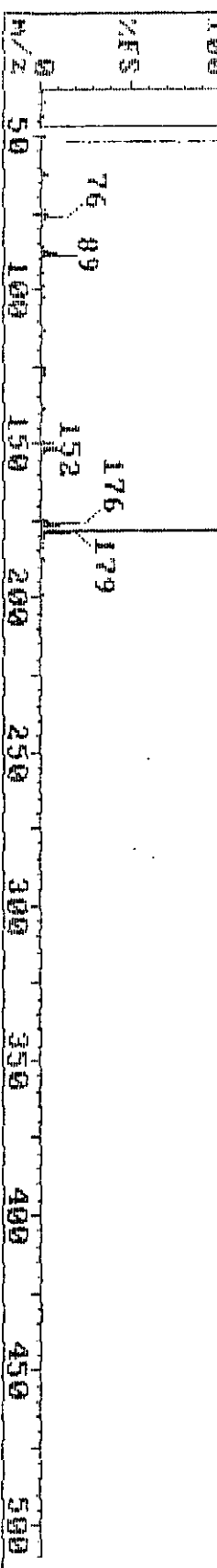
540672



475136



FINH 100



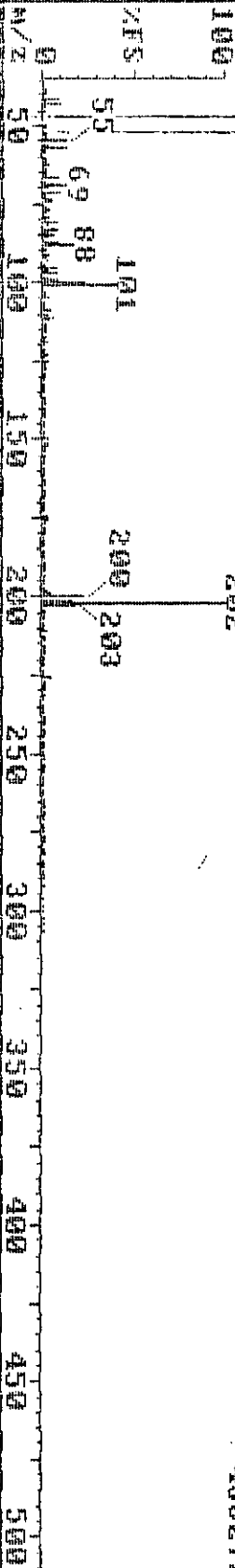


04-Jan-93 09:43 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #2 (1:4 DIL.) 22688 Instrument G

SM

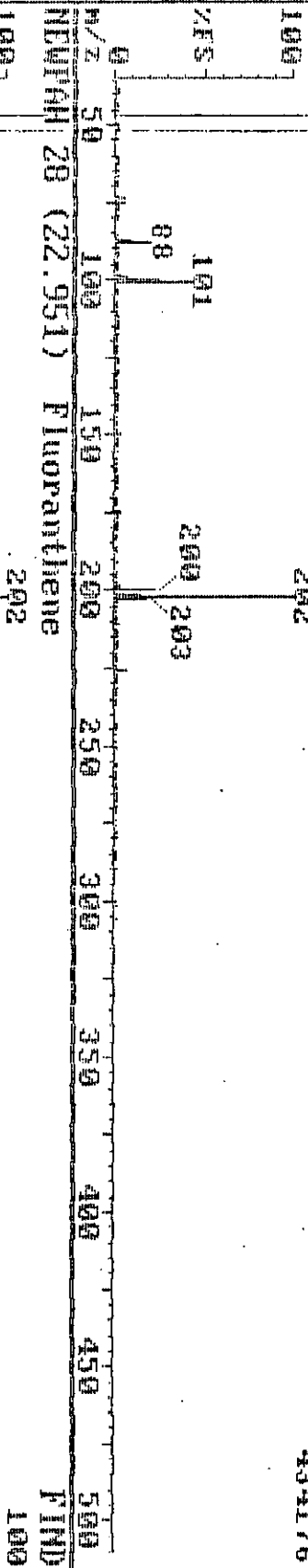
GL506 1256 (22.935)

438272



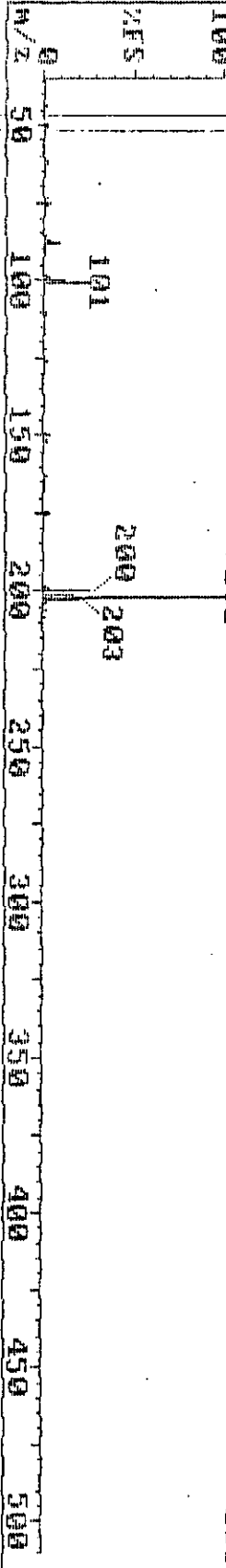
434176

GL506 1256 (22.934) REFINE



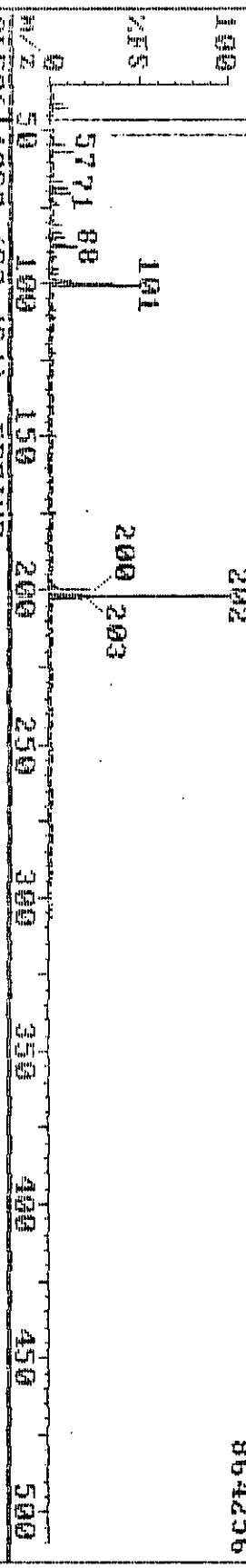
FIND 100

NEWMAN 28 (22.951) Fluoranthene

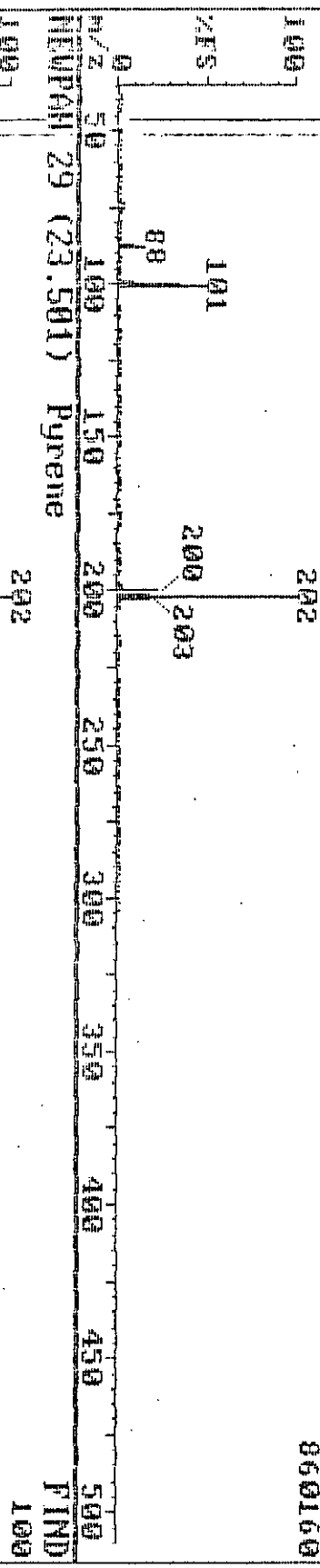


04-Jan-93 00:43 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #2 (1:4 DIL.) 22680 Instrument G

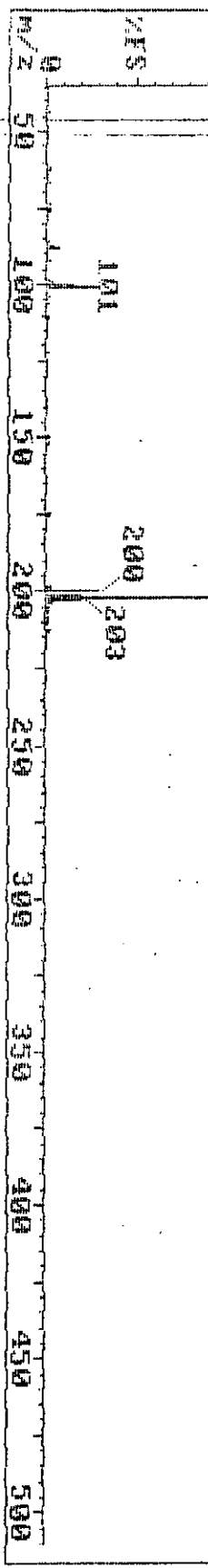
GI506 1209 (23.485) 864256



860160



FIND 100



Triangle Laboratories of RTP, Inc.  
801 Capitola Dr.  
Durham, NC 27713  
(919) 544-5729

Sample File : GL515  
Response File : GL509  
Date Analyzed : 01/04/93  
Date Reported : 01/05/93  
Project Number: 22680

Sample ID: RUN#3  
TLI ID: 62.51.3A-I  
Dilution Factor: 10.00

Quantitation Results Method 8270

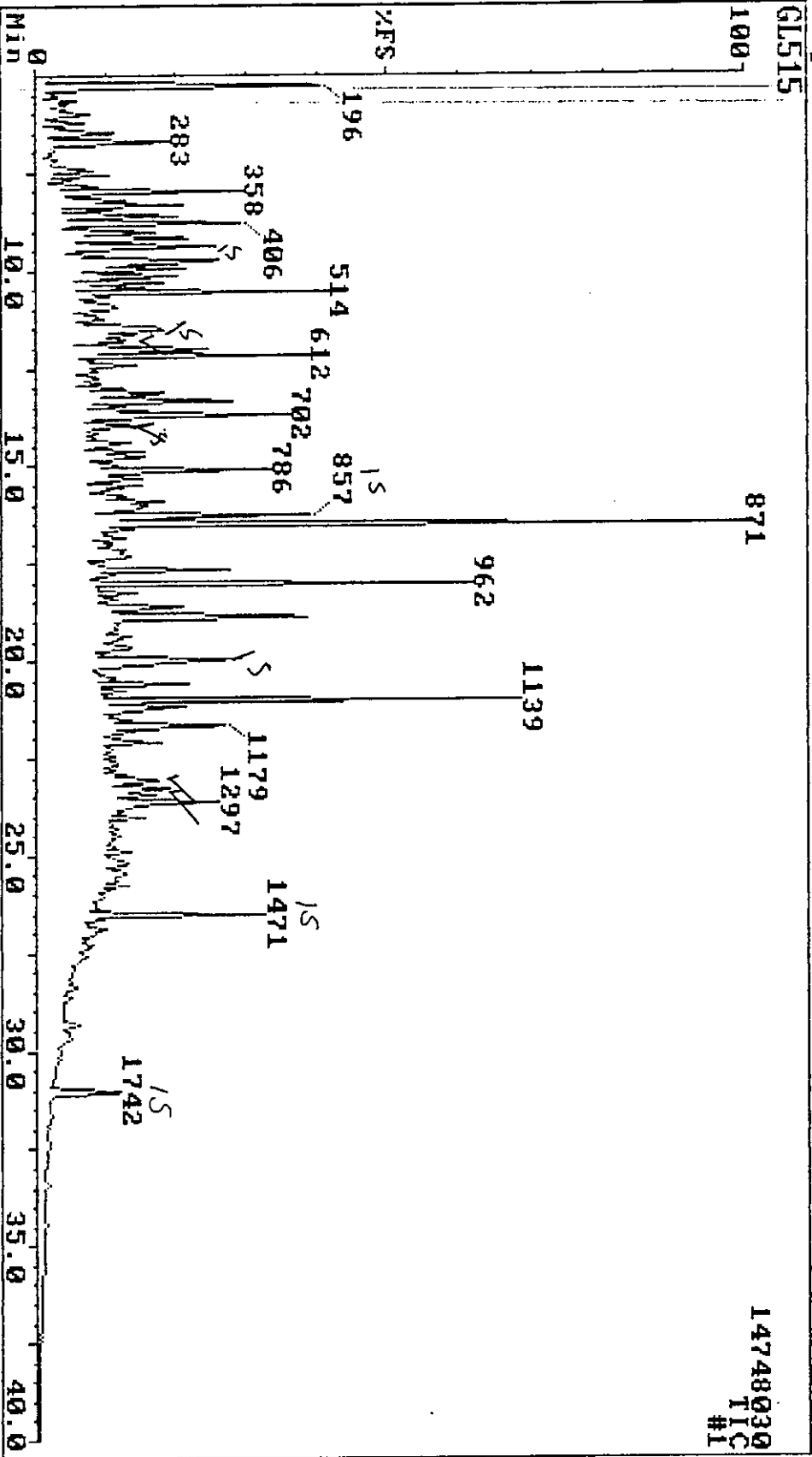
Analyte	Area	RF	SCAN	ISID	Amt. Code (ug)	Quan	FLAG	Limit
1,4-Dichlorobenzene-d4	6076		420	1	I			
Naphthalene-d8	24949		599	2	I			
2-Methylnaphthalene	7919	0.675	705	2	188.10 D	100.0		
Naphthalene	9273	0.940	602	2	158.17 D	100.0		
Acenaphthene-d10	13174		857	3	I			
Acenaphthene	0	0.969	0	3	0.63 ND	100.0		
Fluorene	0	1.170	0	3	0.52 ND	100.0		
2-Chloronaphthalene	0	1.006	0	3	0.60 ND	100.0		
Acenaphthylene	0	1.697	0	3	0.36 ND	100.0		
Phenanthrene-d10	26096		1076	4	I			
Phenanthrene	4259	0.915	1080	4	71.35 E	100.0		
Anthracene	0	0.959	0	4	0.32 ND	100.0		
Fluoranthene	2726	1.099	1256	4	38.02 E	100.0		
Chrysene-d12	29098		1471	5	I			
Chrysene	0	0.935	0	5	0.29 ND	100.0		
Pyrene	3172	0.996	1289	5	43.78 E	100.0		
Benzo(a)anthracene	0	0.962	0	5	0.29 ND	100.0		
Perylene-d12	20907		1742	6	I			
Benzo(b)fluoranthene	0	1.331	0	6	0.29 ND	100.0		
Benzo(k)fluoranthene	0	1.524	0	6	0.25 ND	100.0		
Benzo(e)pyrene	0	1.341	0	6	0.29 ND	100.0		
Benzo(a)pyrene	0	1.269	0	6	0.30 ND	100.0		
Perylene	0	0.669	0	6	0.57 ND	100.0		
Indeno(1,2,3-cd)pyrene	0	1.271	0	6	0.30 ND	100.0		
Dibenz(a,h)anthracene	0	0.984	0	6	0.39 ND	100.0		
Benzo(g,h,i)perylene	0	1.053	0	6	0.36 ND	100.0		

Surrogate Summary	Area	RF	SCAN	ISID	Amount (ug)	Code	%REC
Anthracene-d10	4025	0.492	1084	4	125.42 D		125.4
Pyrene-d10	5950	0.900	1286	5	90.89 D		90.9

Received by J. Lyon Date 1, 5, 93  
ND - Not Detected; D- Detected; E- Estimated; I- Internal Standard

Orgrep v2.5

04-Jan-93 14:02 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #3 (1:10 DIL.) 22680 Instrument G



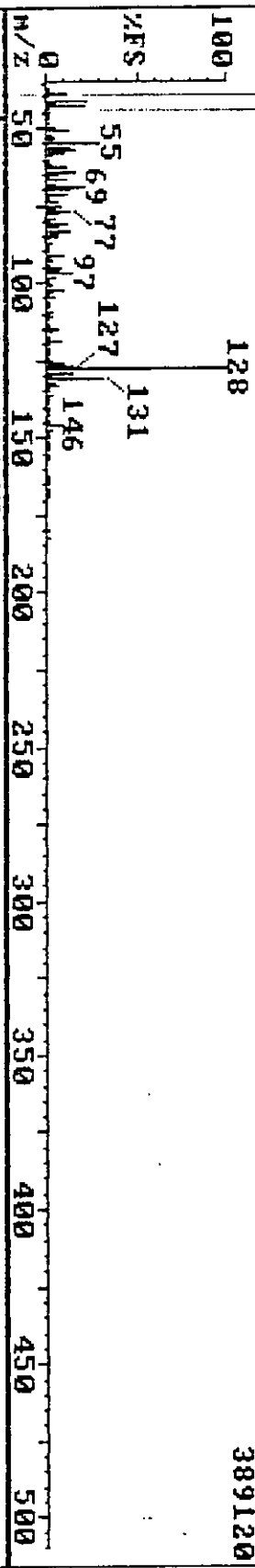
*BT*  
1-5-93

No.	MAT	FOR	REV	Delta	Area	P. Flags	Scan	QM	Name
1	92	61	97	1	607620	bv	420	152	1,4-Dichlorobenzene-d4
2	95	66	90	0	2494900	vv	599	136	Naphthalene-d8
3	90	50	94	0	1317400	vv	857	164	Acenaphthene-d10
4	100	65	97	0	2609500	bv	1076	188	Phenanthrene-d10
5	100	68	97	0	2909800	bv	1471	240	Chrysene-d12
6	96	71	95	1	2090700	bv	1742	264	Perylene-d12
7	0	0	0	0	0		0	112	2-Fluorophenol
8	0	0	0	0	0		0	132	2-Chlorophenol-d4
9	0	0	0	0	0		0	99	Phenol-d5
10	0	0	0	0	0		0	152	1,2-Dichlorobenzene-d4
11	0	0	0	0	0		0	82	Nitrobenzene-d5
12	0	0	0	0	0		0	185	1,3,5-Trichlorobenzene-d3
13	0	0	0	0	0		0	240	1,4-Dibromobenzene-d4
14	0	0	0	0	0		0	172	2-Fluorobiphenyl
15	0	0	0	0	0		0	330	2,4,6-Tribromophenol
16	71	28	85	-1	402600	vv	1084	188	Anthracene-d10
17	79	36	91	0	595090	vv	1286	212	Pyrene-d10
18	0	0	0	0	0		0	244	Terphenyl-d14
19	87	42	97	0	927390	vv	602	128	Naphthalene
20	89	56	87	0	791950	vv	705	142	2-Methylnaphthalene
21	0	0	0	0	0		0	162	2-Chloronaphthalene
22	0	0	0	0	0		0	152	Acenaphthylene
23	0	0	0	0	0		0	154	Acenaphthene
24	0	0	0	0	0		0	166	Fluorene
25	0	0	0	0	0		0	266	Pentachlorophenol
26	68	21	87	0	425940	vb	1080	178	Phenanthrene
27	0	0	0	0	0		0	178	Anthracene
28	71	23	90	0	272610	vb	1256	202	Fluoranthene
29	67	24	83	0	317230	vv	1289	202	Pyrene
30	0	0	0	0	0		0	228	Benzo(a)anthracene
31	0	0	0	0	0		0	228	Chrysene
32	0	0	0	0	0		0	252	Benzo(b)fluoranthene
33	0	0	0	0	0		0	252	Benzo(k)fluoranthene
34	0	0	0	0	0		0	252	Benzo(e)pyrene
35	0	0	0	0	0		0	252	Benzo(a)pyrene
36	0	0	0	0	0		0	252	Perylene
37	0	0	0	0	0		0	276	Indeno(1,2,3-cd)pyrene
38	0	0	0	0	0		0	278	Dibenz(a,h)anthracene
39	0	0	0	0	0		0	276	Benzo(g,h,i)perylene

*92*  
*1-5-93*

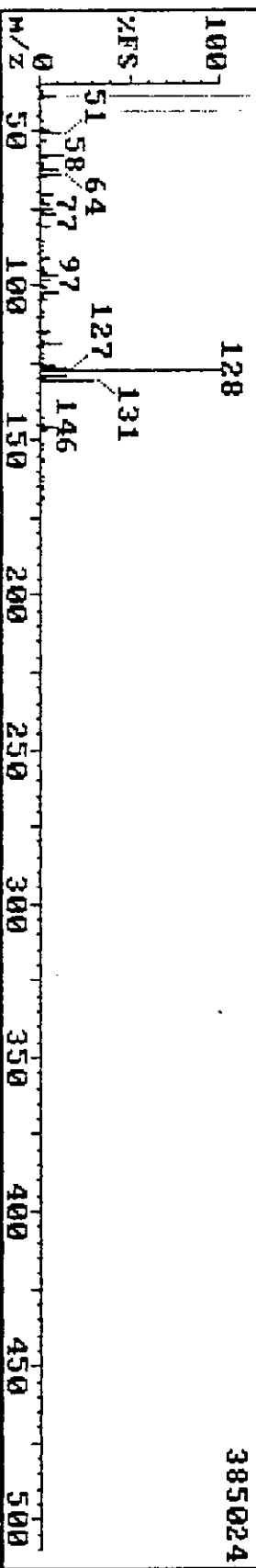
04-Jan-93 14:02 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #3 (1:10 DIL.) Z2680 Instrument G

GL515 602 (12.034)



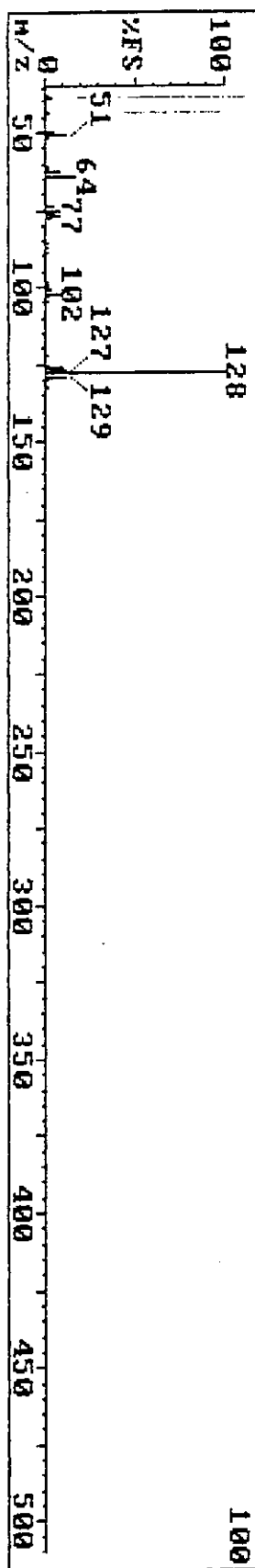
389120

GL515 602 (12.034) REFINE



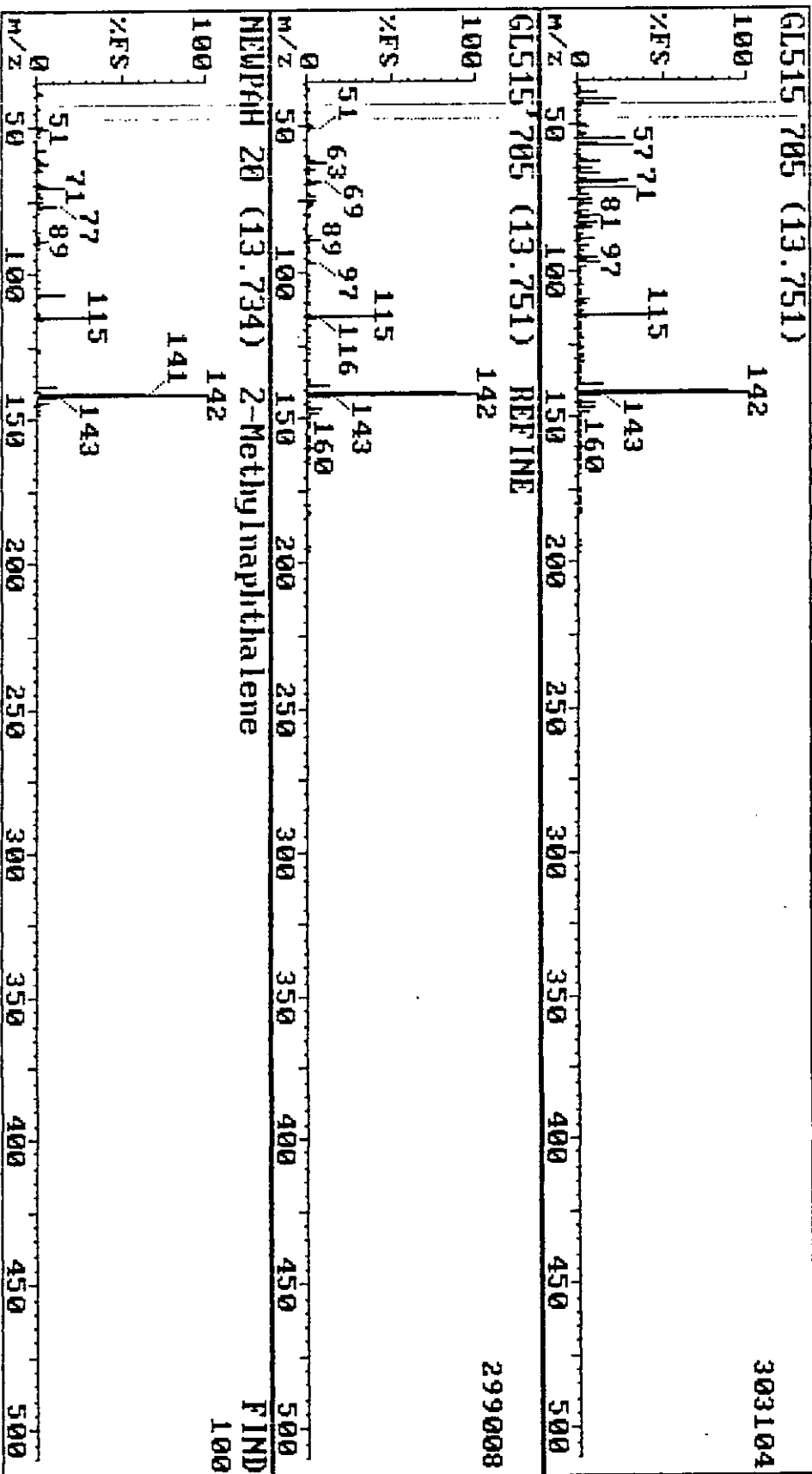
385024

NEWPAH 19 (12.017) Naphthalene

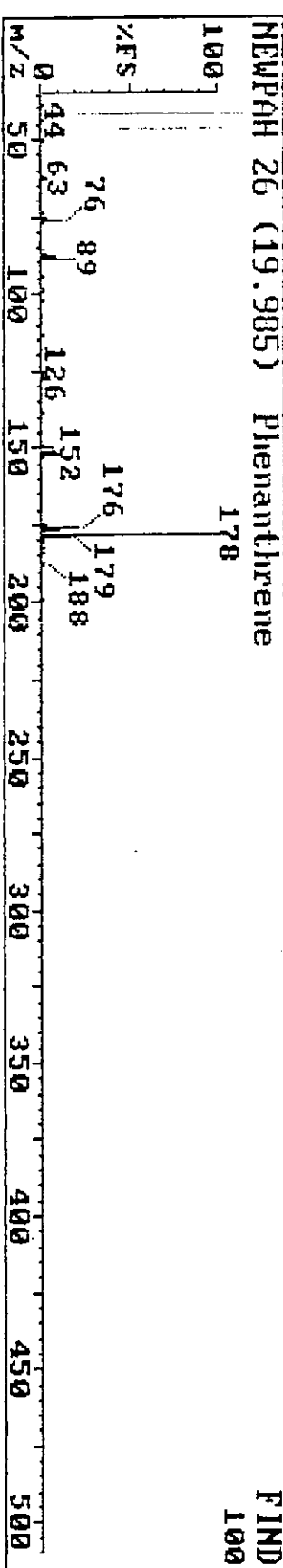
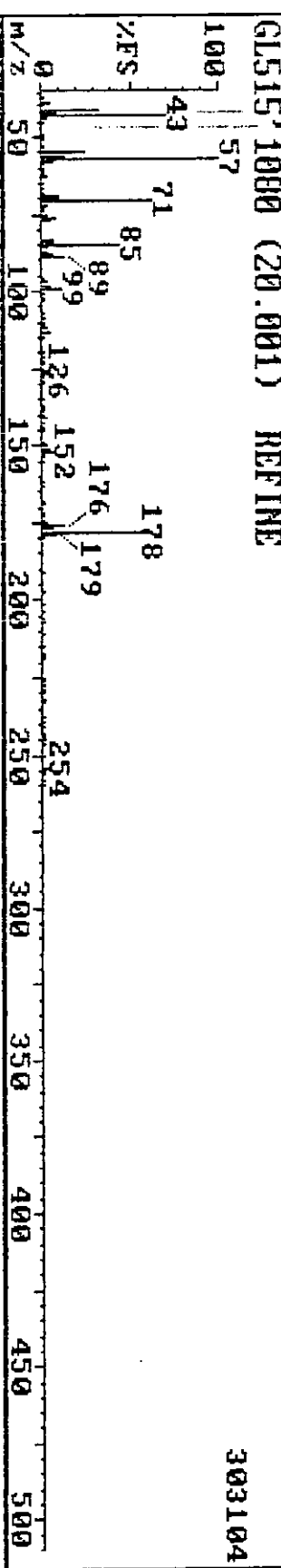
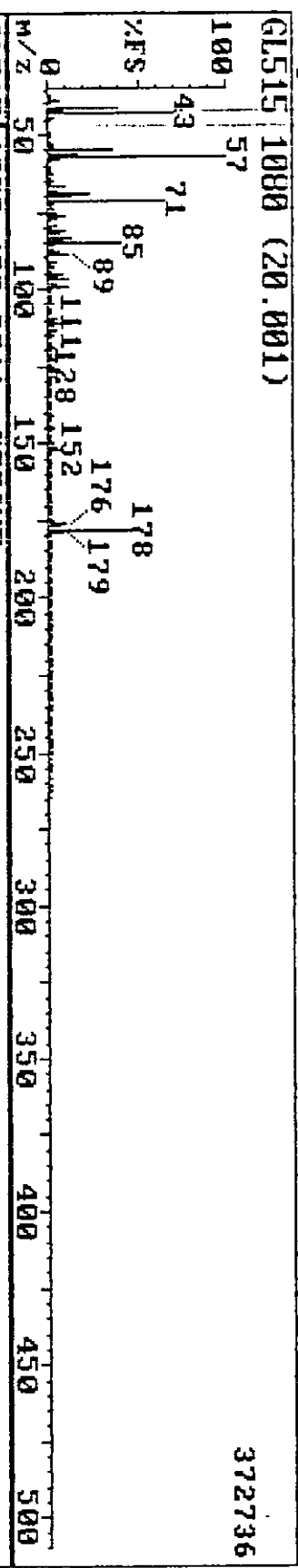


FIND 100

04-Jan-93 14:02 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #3 (1:10 DIL.) 22680 Instrument G

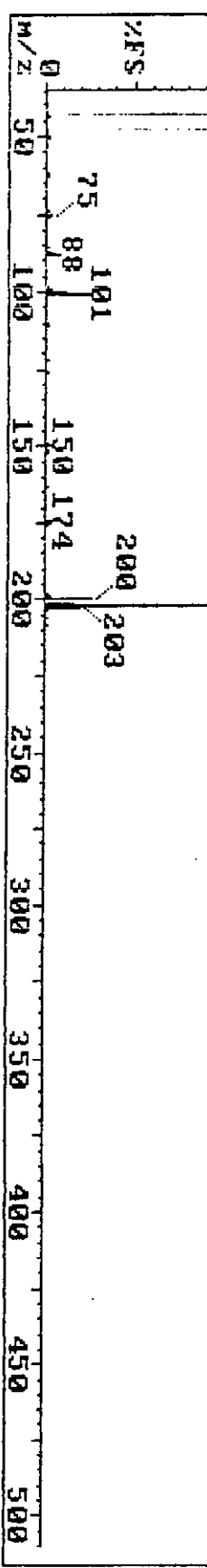
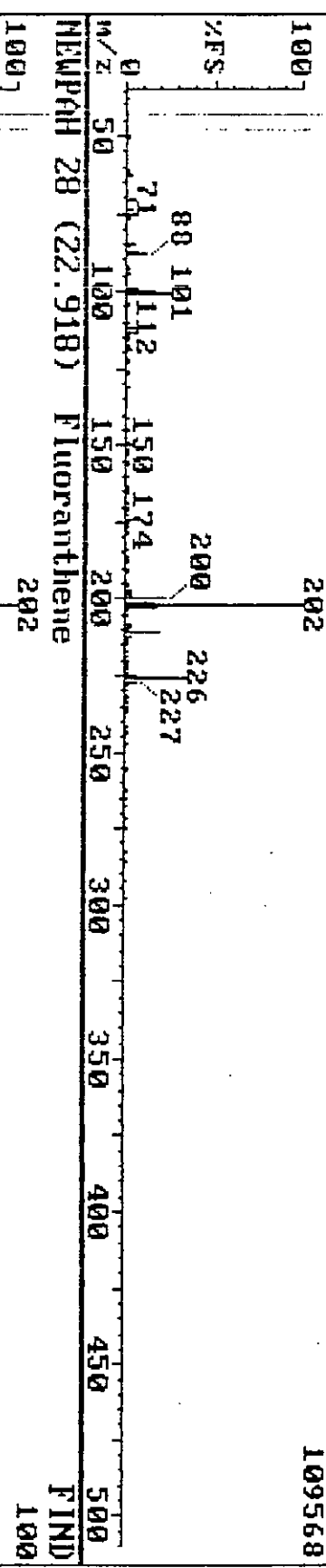
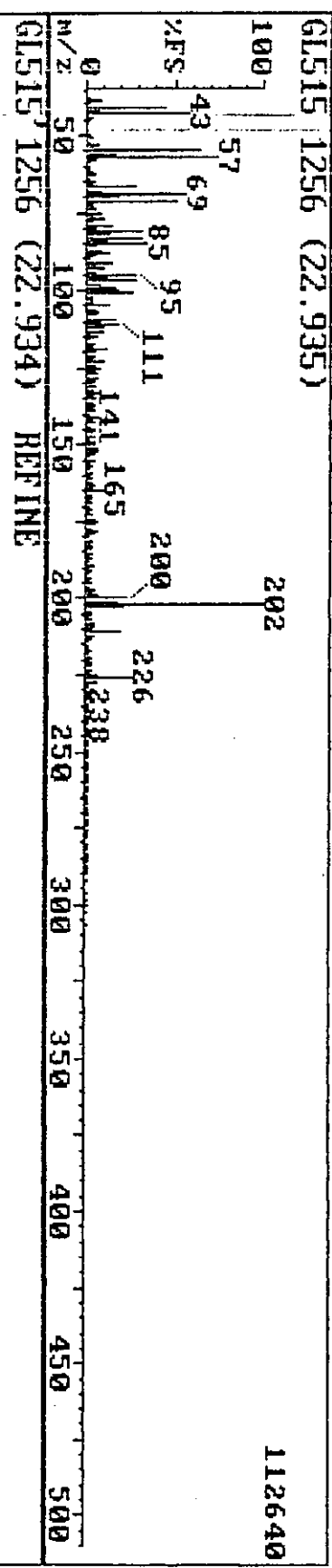


04-Jan-93 14:02 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #3 (1:10 DIL.) 22680 Instrument G

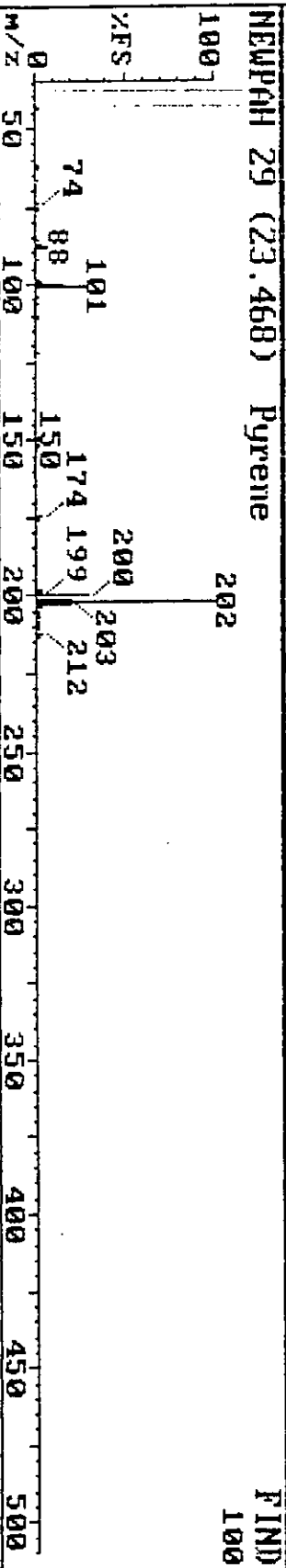
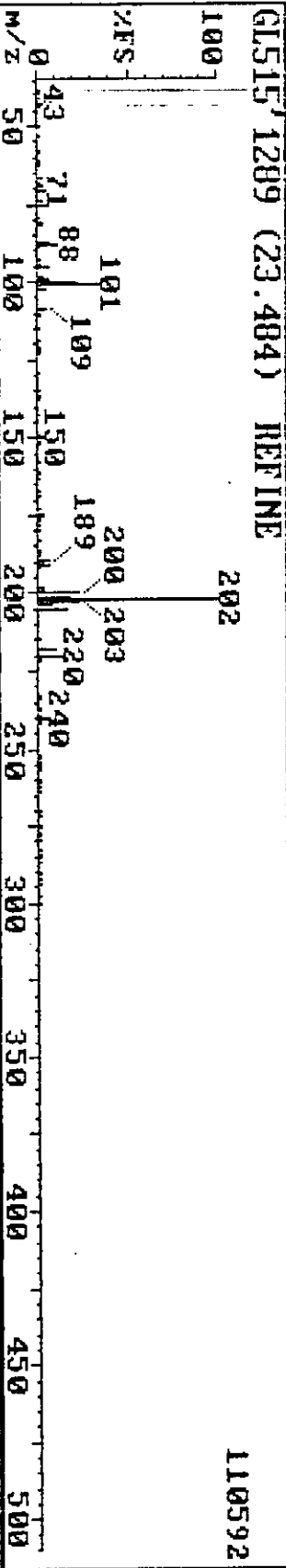
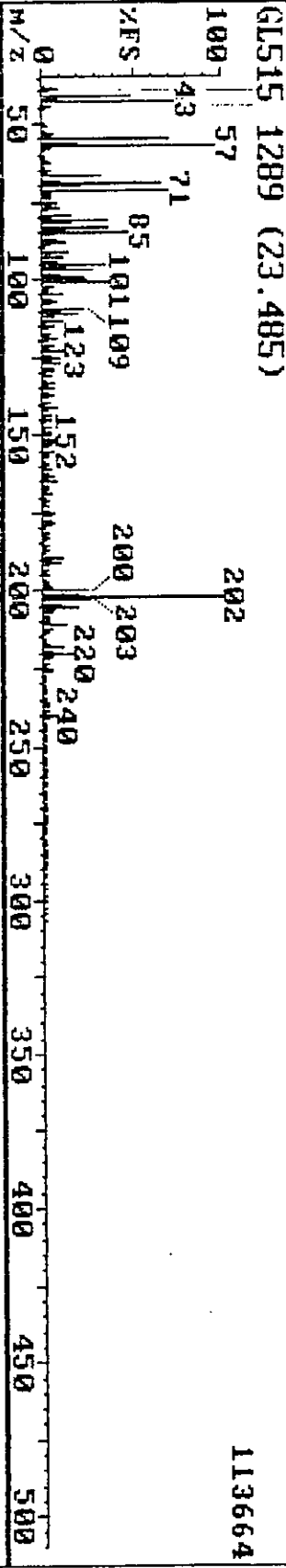




04-Jan-93 14:02 Triangle Laboratories of RTP, Inc. (919) 544-5729  
 Sample: RUN #3 (1:10 DIL.) 22680 Instrument G



04-Jan-93 14:02 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: RUN #3 (1:10 DIL.) 22680 Instrument G



113664

110592

FIND 100

Triangle Laboratories of RTP, Inc.  
 801 Capitola Dr.  
 Durham, NC 27713  
 (919) 544-5729

Sample File : GL472  
 Response File : GL467  
 Date Analyzed : 12/30/92  
 Date Reported : 01/06/93  
 Project Number: 22680

Sample ID: BLANK  
 TLI ID: 62.51.4A-I  
 Dilution Factor: 1.00

Quantitation Results Method 8270

Analyte	Area	RF	SCAN	ISID	Amt. (ug)	Code	Quan Limit	FLAG
1,4-Dichlorobenzene-d4	11477		433	1		I		
Naphthalene-d8	47513		612	2		I		
2-Methylnaphthalene	3709	0.449	718	2	6.96	E	10.0	
Naphthalene	4404	0.574	615	2	6.46	E	10.0	
Acenaphthene-d10	32562		871	3		I		
Acenaphthene	0	0.578	0	3	0.04	ND	10.0	
Fluorene	0	0.745	0	3	0.03	ND	10.0	
2-Chloronaphthalene	0	0.600	0	3	0.04	ND	10.0	
Acenaphthylene	0	1.001	0	3	0.02	ND	10.0	
Phenanthrene-d10	45344		1091	4		I		
Phenanthrene	5534	0.552	1095	4	8.84	E	10.0	
Anthracene	0	0.568	0	4	0.03	ND	10.0	
Fluoranthene	0	0.653	0	4	0.03	ND	10.0	
Chrysene-d12	24560		1488	5		I		
Chrysene	0	0.539	0	5	0.06	ND	10.0	
Pyrene	0	0.759	0	5	0.04	ND	10.0	
Benzo(a)anthracene	0	0.576	0	5	0.06	ND	10.0	
Perylene-d12	14917		1769	6		I		
Benzo(b)fluoranthene	0	0.709	0	6	0.08	ND	10.0	
Benzo(k)fluoranthene	0	0.870	0	6	0.06	ND	10.0	
Benzo(e)pyrene	0	0.691	0	6	0.08	ND	10.0	
Benzo(a)pyrene	0	0.666	0	6	0.08	ND	10.0	
Perylene	0	0.395	0	6	0.14	ND	10.0	
Indeno(1,2,3-cd)pyrene	0	0.612	0	6	0.09	ND	10.0	
Dibenz(a,h)anthracene	0	0.446	0	6	0.12	ND	10.0	
Benzo(g,h,i)perylene	0	0.540	0	6	0.10	ND	10.0	

Surrogate Summary	Area	RF	SCAN	ISID	Amount (ug)	Code	%REC
Anthracene-d10	30746	0.301	1100	4	90.11	D	90.1
Pyrene-d10	35025	0.672	1302	5	84.88	D	84.9

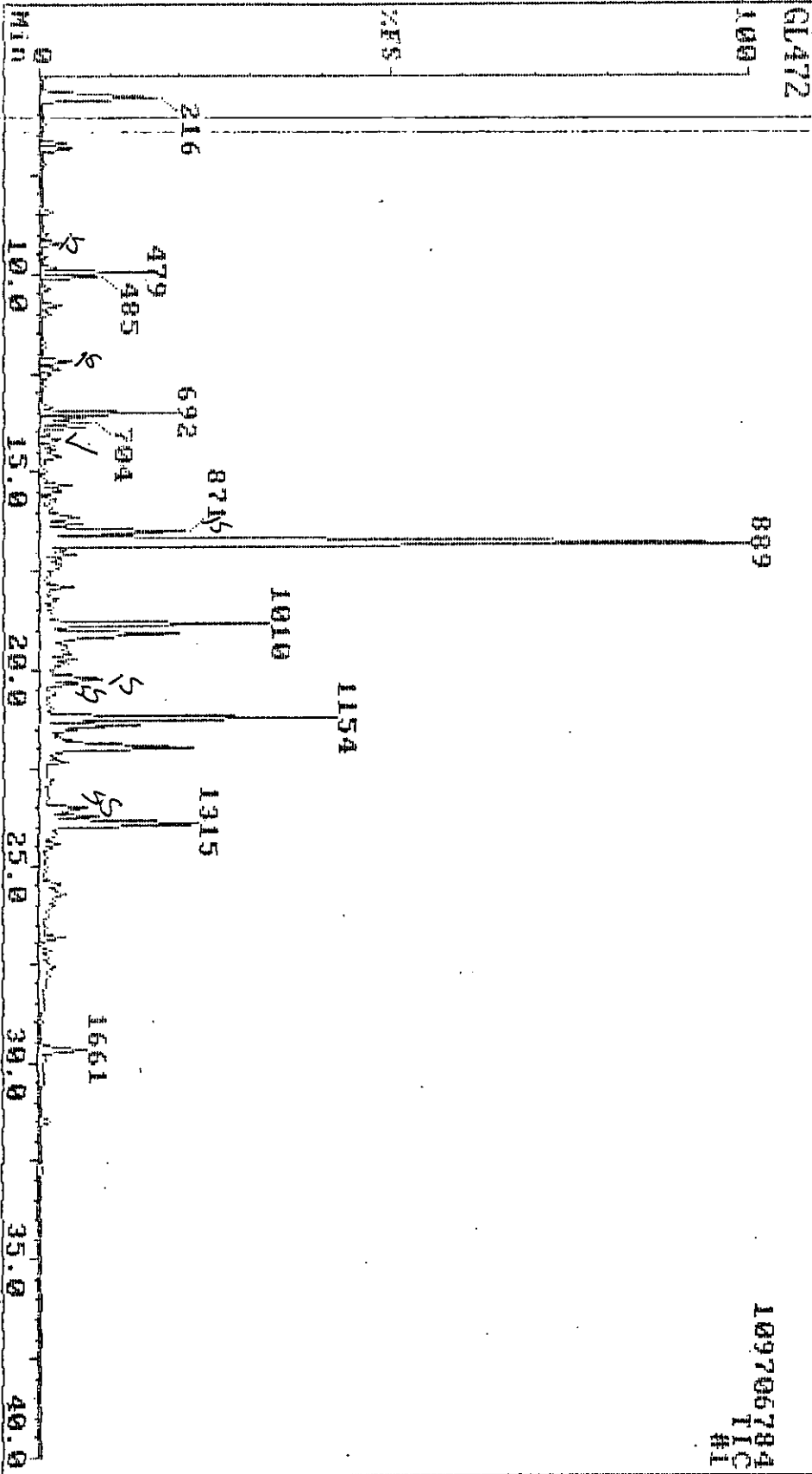
Received by J. Lynn Date 1/6/93  
 ND - Not Detected; D - Detected; E - Estimated; I - Internal Standard

N 12/30/92

30-Dec-92 16:17:43  
Sample: ~~1411D~~ BLANK

Triangle Laboratories of RTP, Inc.  
22688

(919) 544-5729  
Instrument G



109706784  
TIC  
#1

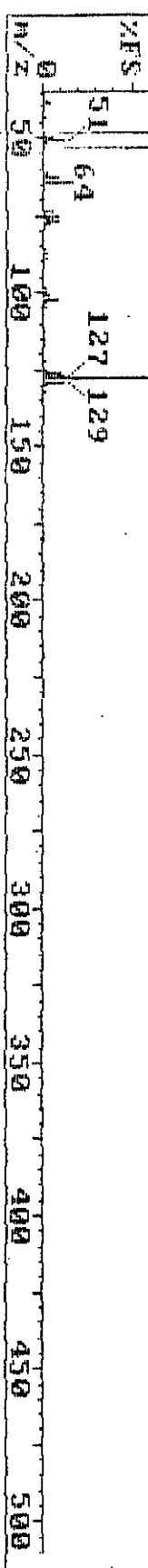
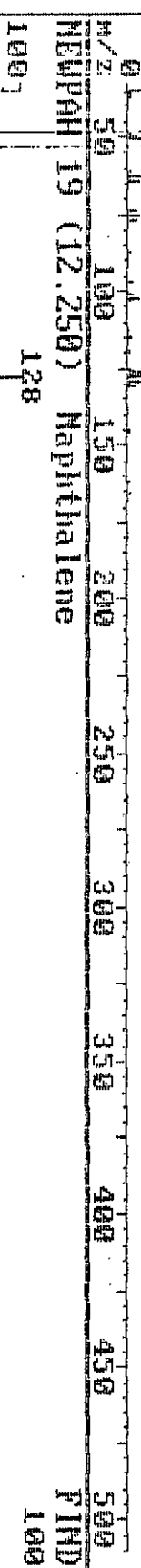
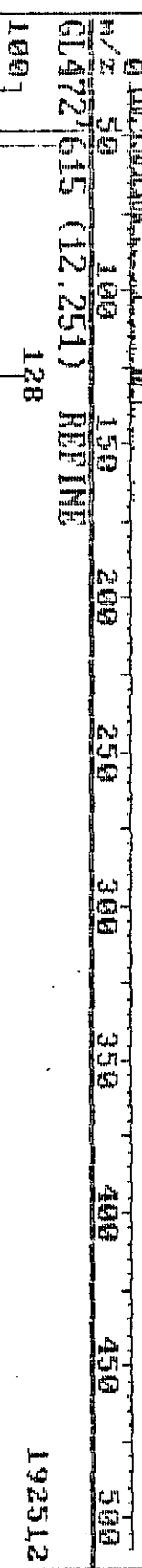
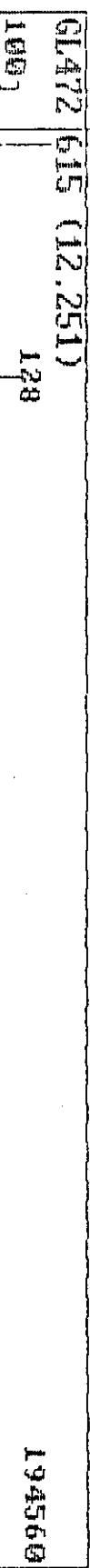
8/1-5-93

No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	79	100	1	1147700	bb	433	152 1,4-Dichlorobenzene-d4
2	100	83	94	0	4751300	bv	612	136 Naphthalene-d8
3	69	29	90	1	3256300	vv	871	164 Acenaphthene-d10
4	93	53	96	0	4534500	vv	1091	188 Phenanthrene-d10
5	100	65	96	0	2456100	bv	1488	240 Chrysene-d12
6	87	56	93	1	1491700	bv	1769	264 Perylene-d12
7	0	0	0	0	0		0	112 2-Fluorophenol
8	0	0	0	0	0		0	132 2-Chlorophenol-d4
9	0	0	0	0	0		0	99 Phenol-d5
10	0	0	0	0	0		0	152 1,2-Dichlorobenzene-d4
11	0	0	0	0	0		0	82 Nitrobenzene-d5
12	0	0	0	0	0		0	185 1,3,5-Trichlorobenzene-d3
13	0	0	0	0	0		0	240 1,4-Dibromobenzene-d4
14	0	0	0	0	0		0	172 2-Fluorobiphenyl
15	0	0	0	0	0		0	330 2,4,6-Tribromophenol
16	94	66	96	1	3074600	vv	1100	188 Anthracene-d10
17	85	55	91	1	3502500	vv	1302	212 Pyrene-d10
18	0	0	0	0	0		0	244 Terphenyl-d14
19	100	63	99	0	440420	bv	615	128 Naphthalene
20	95	62	90	0	370940	vb	718	142 2-Methylnaphthalene
21	0	0	0	0	0		0	162 2-Chloronaphthalene
22	0	0	0	0	0		0	152 Acenaphthylene
23	0	0	0	0	0		0	154 Acenaphthene
24	0	0	0	0	0		0	166 Fluorene
25	0	0	0	0	0		0	266 Pentachlorophenol
26	68	28	89	1	553470	vv	1095	178 Phenanthrene
27	0	0	0	0	0		0	178 Anthracene
28	0	0	0	0	0		0	202 Fluoranthene
29	0	0	0	0	0		0	202 Pyrene
30	0	0	0	0	0		0	228 Benzo(a)anthracene
31	0	0	0	0	0		0	228 Chrysene
32	26	18	24	-1	<del>4952</del> bb		<del>1484</del>	252 Benzo(b)fluoranthene
33	0	0	0	0	0		0	252 Benzo(k)fluoranthene
34	0	0	0	0	0		0	252 Benzo(e)pyrene
35	0	0	0	0	0		0	252 Benzo(a)pyrene
36	0	0	0	0	0		0	252 Perylene
37	0	0	0	0	0		0	276 Indeno(1,2,3-cd)pyrene
38	0	0	0	0	0		0	278 Dibenz(a,h)anthracene
39	0	0	0	0	0		0	276 Benzo(g,h,i)perylene

*JZ*  
1-5-93

12/30/92

30-Dec-92 16:17 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: FIELD BLANK 22680 Instrument G



12/30/92

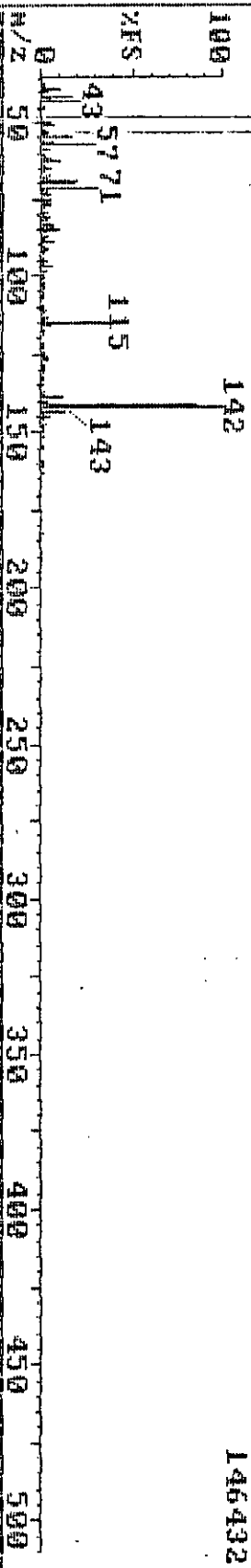
30-Dec-92 16:17  
Sample: FIELD BLANK

Triangle Laboratories of RTP, Inc.  
22680

(919) 544-5729  
Instrument G

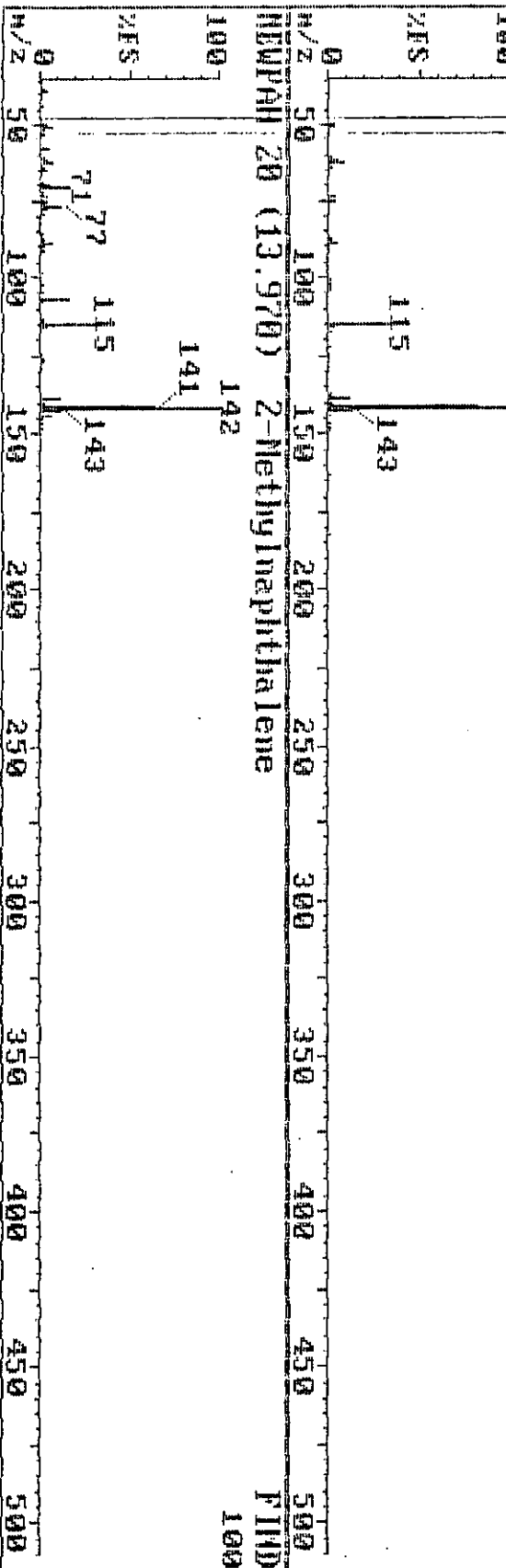
GL472718 (13.967)

146432



GL472718 (13.967) REFINE

145408



NEWPAN 20 (13.970) 2-Methylnaphthalene

100

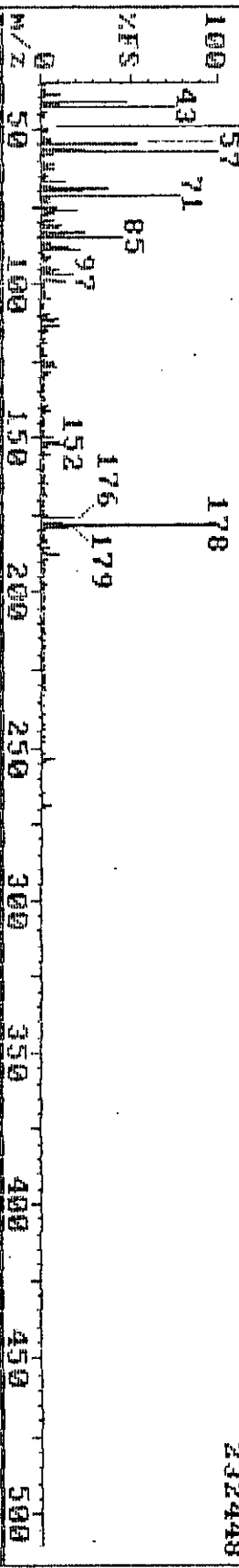
FOUND

✓ 12/30/92

30-Dec-92 16:17 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: FIELD BLANK 22680 Instrument G

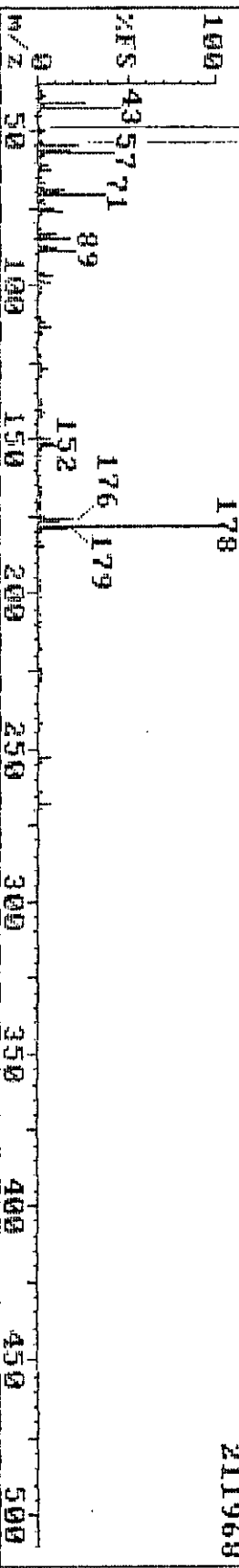
GL472 1095 (20.251)

232448



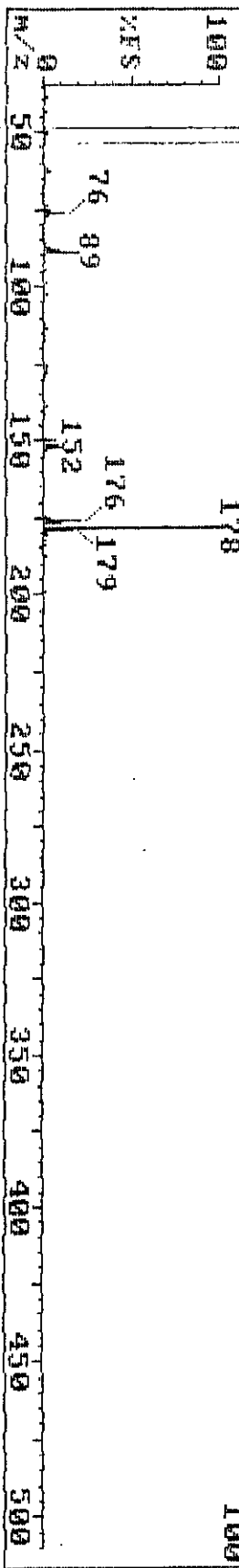
GL472 1095 (20.251) REFINE

211968



NEUPAH 26 (20.240) Phenanthrene

FIND 100





Triangle Laboratories of RTP, Inc.  
 801 Capicola Dr.  
 Durham, NC 27713  
 (919) 544-5729

Sample File : GL470  
 Response File : GL467  
 Date Analyzed : 12/30/92  
 Date Reported : 01/05/93  
 Project Number : 22680

Sample ID: SBLK 122492  
 TLI ID: N/A  
 Dilution Factor: 1.00

Quantitation Results Method 8270

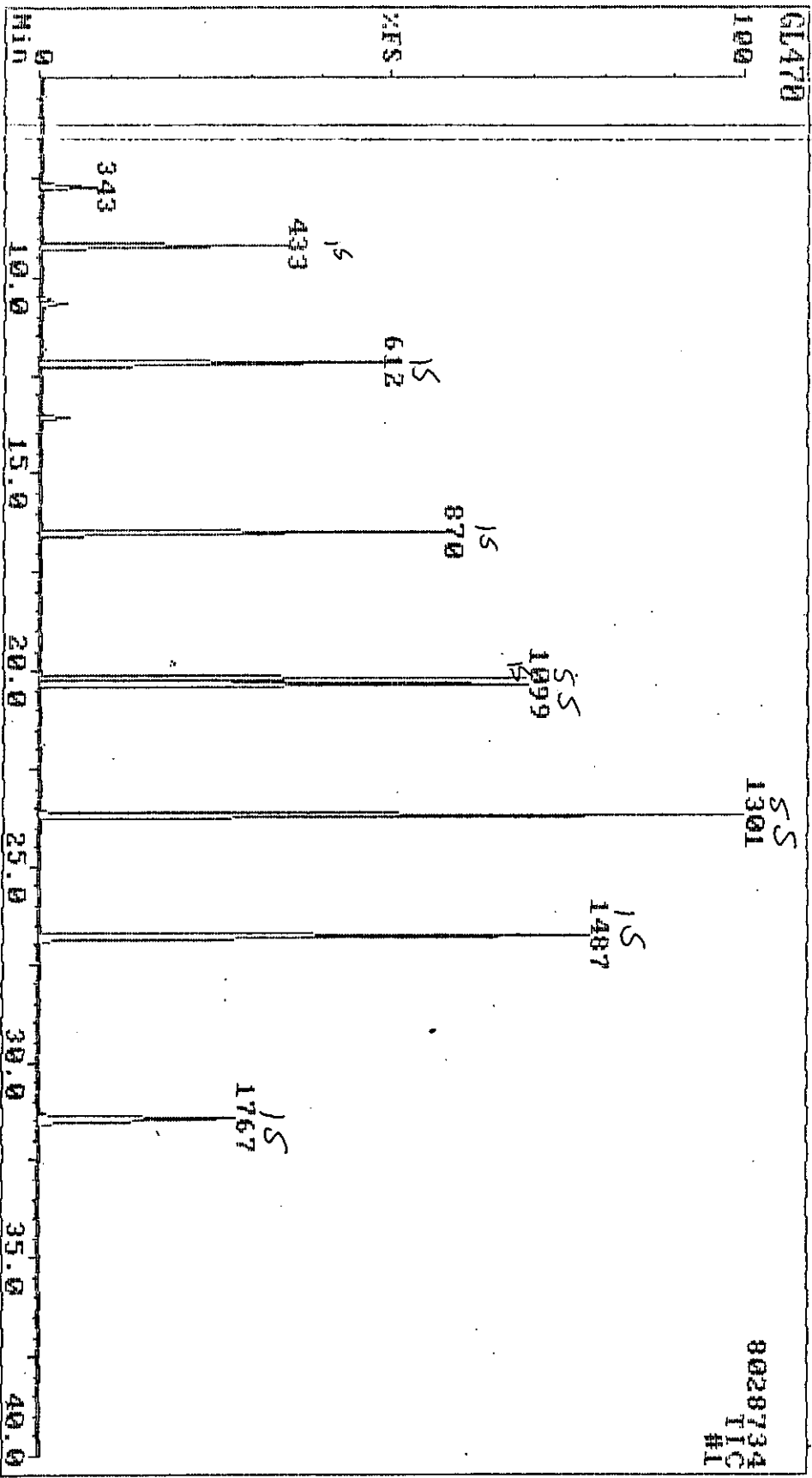
Analyte	Area	RF	SCAN	ISID	Amt. (ug)	Code	Quan	FLAG
							Limit	
1,4-Dichlorobenzene-d4	9751		433	1		I		
Naphthalene-d8	33764		612	2		I		
2-Methylnaphthalene	0	0.449	0	2	0.05	ND	10.0	
Naphthalene	849	0.574	615	2	1.75	E	10.0	
Acenaphthene-d10	25723		870	3		I		
Acenaphthene	0	0.578	0	3	0.05	ND	10.0	
Fluorene	0	0.745	0	3	0.04	ND	10.0	
2-Chloronaphthalene	0	0.600	0	3	0.05	ND	10.0	
Acenaphthylene	0	1.001	0	3	0.03	ND	10.0	
Phenanthrene-d10	58520		1090	4		I		
Phenanthrene	0	0.552	0	4	0.02	ND	10.0	
Anthracene	0	0.588	0	4	0.02	ND	10.0	
Fluoranthene	0	0.653	0	4	0.02	ND	10.0	
Chrysene-d12	63087		1487	5		I		
Chrysene	0	0.539	0	5	0.02	ND	10.0	
Pyrene	0	0.759	0	5	0.02	ND	10.0	
Benzo(a)anthracene	0	0.576	0	5	0.02	ND	10.0	
Perylene-d12	34005		1767	6		I		
Benzo(b)fluoranthene	0	0.709	0	6	0.03	ND	10.0	
Benzo(k)fluoranthene	0	0.870	0	6	0.03	ND	10.0	
Benzo(e)pyrene	0	0.691	0	6	0.03	ND	10.0	
Benzo(a)pyrene	0	0.666	0	6	0.04	ND	10.0	
Perylene	0	0.395	0	6	0.06	ND	10.0	
Indeno(1,2,3-cd)pyrene	0	0.612	0	6	0.04	ND	10.0	
Dibenz(a,h)anthracene	0	0.446	0	6	0.05	ND	10.0	
Benzo(g,h,i)perylene	0	0.540	0	6	0.04	ND	10.0	

Surrogate Summary	Area	RF	SCAN	ISID	Amount (ug)	Code	%REC
Anthracene-d10	47850	0.301	1099	4	108.66	D	108.7
Pyrene-d10	67201	0.672	1301	5	63.41	D	63.4

Received by J. Lyon Date 1/5/93  
 ND -Not Detected; D-Detected; E- Estimated; I- Internal Standard

Orgrep v2.5

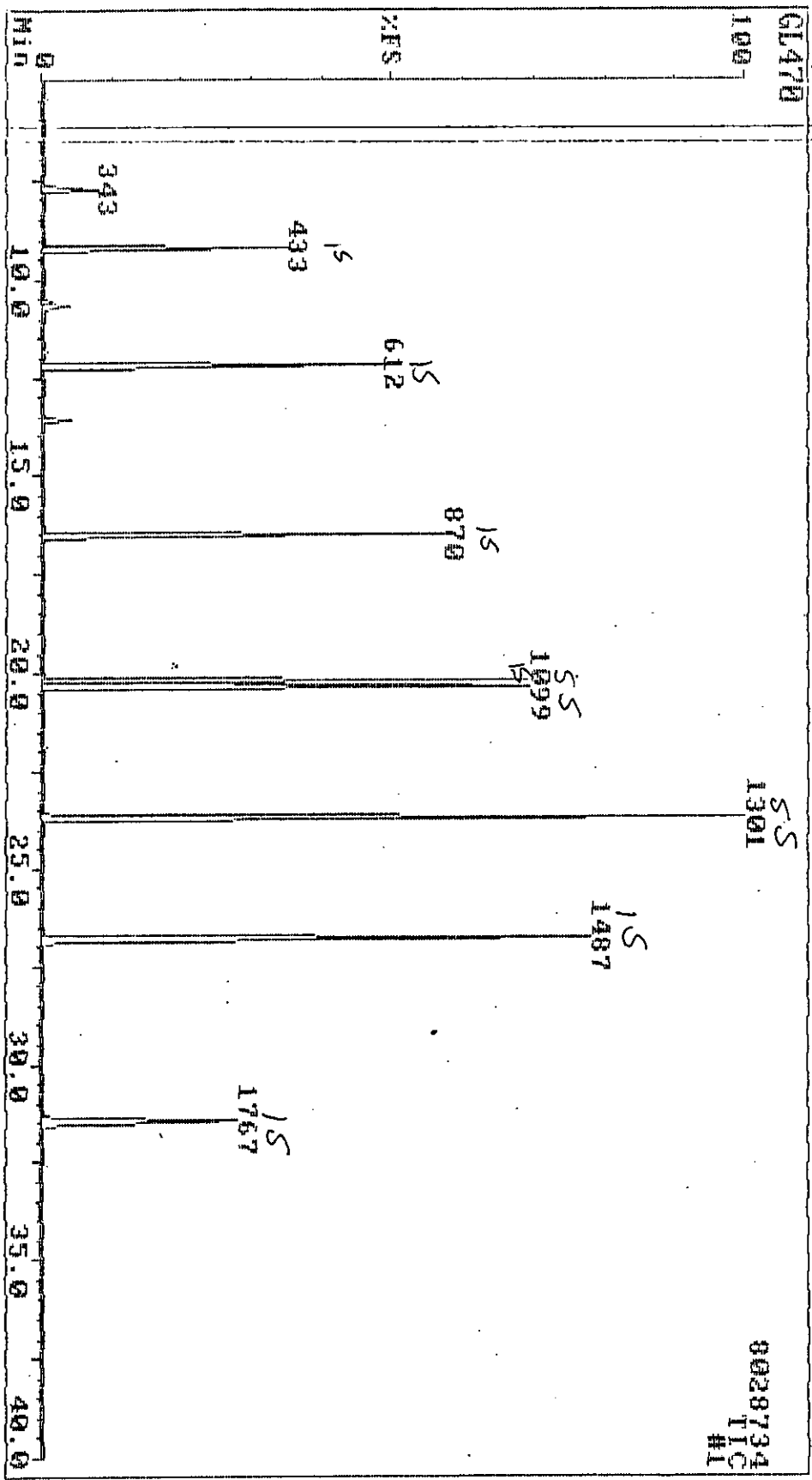
30-Dec-92 14:32 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: SBLK 122492 22680 Instrument G



97-5-93

8028734  
TIC  
#1

30-Dec-92 14:32 Triangle Laboratories of RTP, Inc. (919) 544-5729  
Sample: SHLK 122492 22688 Instrument G



97-5-93

0028734  
TIC  
#1

30-Dec-92 14:32

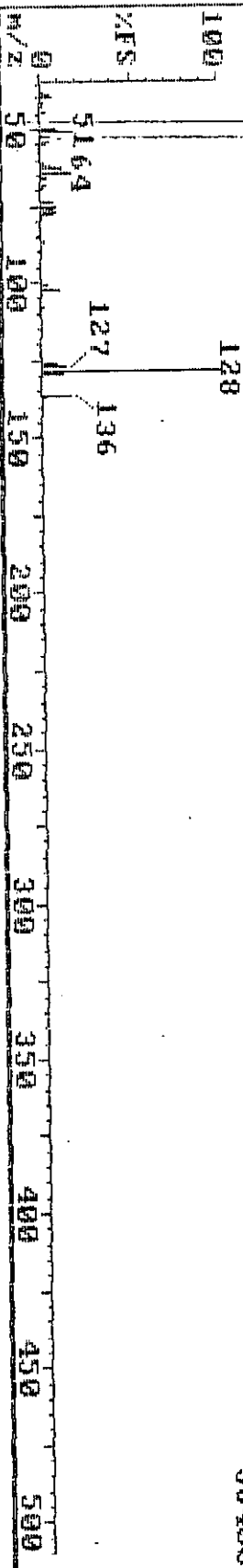
Sample: SBLK 122492

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G

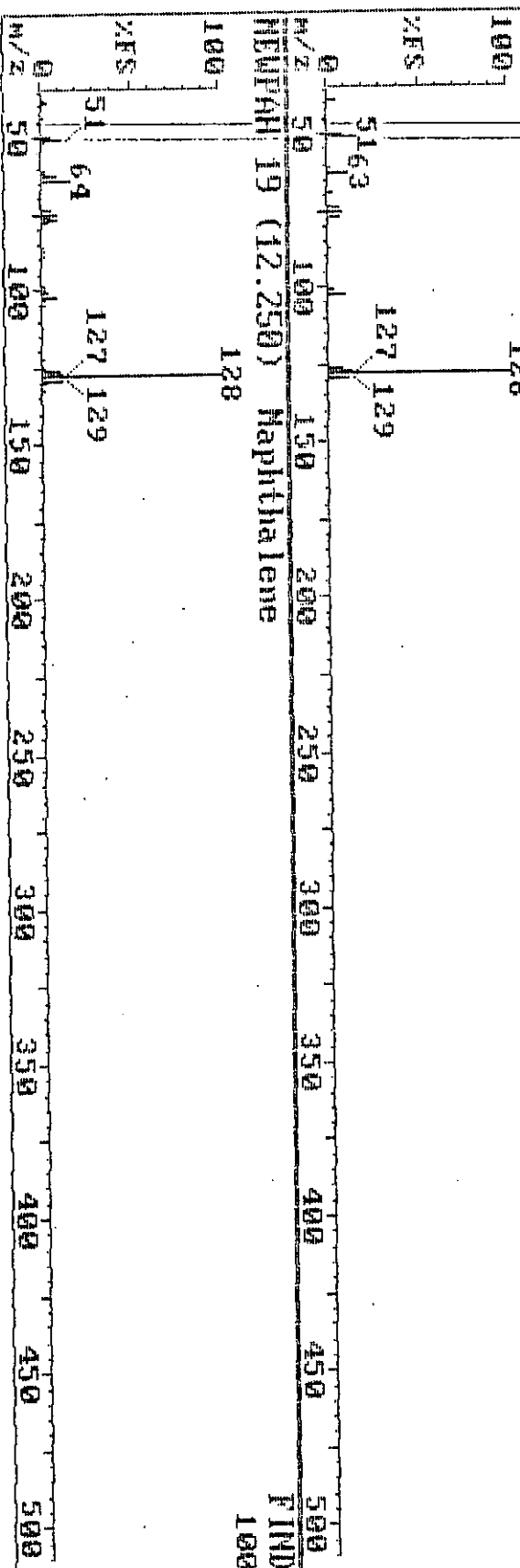
GL470 615 (12.251)

38400



GL470 615 (12.251) REFINE

38400



NEWFAH 19 (12.250) Naphthalene

FIND  
100

Triangle Laboratories of RTP, Inc.  
Continuing Calibration Curve

114

CCAL File: GL509 Date of Analysis :01/04/93 Analyte List: PAH  
CAL File: ICALGJ03

Analyte	Flag	RF50	RFMEAN	%D
1,4-Dichlorobenzene-d4	I			
Naphthalene-d8	I			
2-Methylnaphthalene		0.675	0.729	7.4
Naphthalene		0.940	1.058	11.2
Acenaphthene-d10	I			
Acenaphthene	C	0.969	1.019	4.9
Fluorene		1.170	1.253	6.6
2-Chloronaphthalene		1.006	1.048	4.0
Acenaphthylene		1.697	1.791	5.2
Phenanthrene-d10	I			
Phenanthrene		0.915	0.950	3.7
Anthracene		0.959	0.959	0.0
Fluoranthene	C	1.099	1.152	4.6
Chrysene-d12	I			
Chrysene		0.935	1.011	7.5
Pyrene		0.996	1.176	15.3
Benzo(a)anthracene		0.962	1.048	8.2
Perylene-d12	I			
Benzo(b)fluoranthene		1.331	1.575	15.5
Benzo(k)fluoranthene		1.524	1.704	10.6
Benzo(e)pyrene		1.341	1.497	10.4
Benzo(a)pyrene	C	1.269	1.424	10.9
Perylene		0.669	0.755	11.4
Indeno(1,2,3-cd)pyrene		1.271	1.057	-20.2
Dibenz(a,h)anthracene		0.984	1.047	6.0
Benzo(g,h,i)perylene		1.053	1.193	11.7

Surrogate	Flag	RF50	RFMEAN	%D
Anthracene-d10	S	0.492	0.527	6.6
Pyrene-d10	S	0.900	1.103	18.4

Approved by: J. Lynn Date 1/5/93

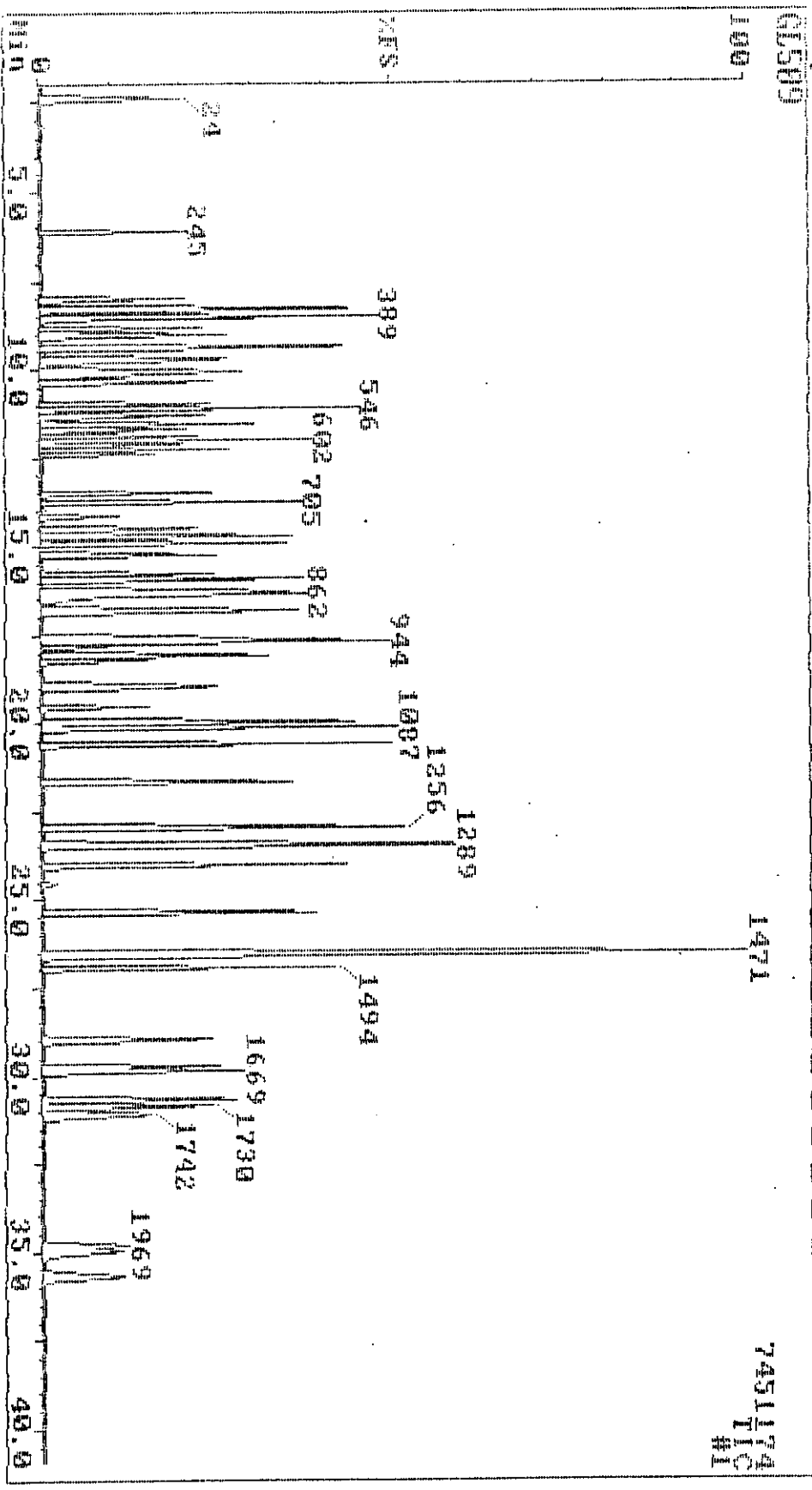
\* - Fails QC Criteria for %D; << - Rf less than minimum QC RF; >> - RF greater than maximum QC RF

CCAL.EXE v2.5

04-Jan-93 00:50  
Sample: 881050

Triangle Laboratories of TN, Inc.

(919) 544-5729  
Instrument G



No.	MAT	FOR	REV	Delta	area	P.Flags	Scan	Qm	Name
1	100	82	100	0	561390	bb	420	152	1,4-Dichlorobenzene-d4
2	100	86	91	0	2294600	bb	599	136	Naphthalene-d8
3	100	93	97	0	1241800	bb	857	164	Acenaphthene-d10
4	100	89	96	0	2604000	bv	1076	188	Phenanthrene-d10
5	83	49	94	-1	3082500	bb	1471	240	Chrysene-d12
6	100	87	93	1	1796400	bb	1742	264	Perylene-d12
7	100	95	97	-1	1252000	bb	244	112	2-Fluorophenol
8	89	55	99	-1	1124100	bb	388	132	2-Chlorophenol-d4
9	96	67	99	-1	1606500	bv	377	99	Phenol-d5
10	100	92	99	0	697090	bb	440	152	1,2-Dichlorobenzene-d4
11	100	81	98	0	1408800	bb	498	82	Nitrobenzene-d5
12	97	57	98	0	783090	bb	546	185	1,3,5-Trichlorobenzene-d3
13	100	93	99	0	562160	bb	607	240	1,4-Dibromobenzene-d4
14	100	90	98	0	1796200	bb	762	172	2-Fluorobiphenyl
15	100	81	100	-1	306780	bb	973	330	2,4,6-Tribromophenol
16	100	87	97	-1	1601300	vb	1084	188	Anthracene-d10
17	100	86	97	0	3467000	vb	1286	212	Pyrene-d10
18	100	86	97	1	2490700	bb	1320	244	Terphenyl-d14
19	100	95	98	0	2696500	bb	602	128	Naphthalene
20	100	89	91	-1	1936500	vb	704	142	2-Methylnaphthalene
21	100	95	98	0	1561900	bb	775	162	2-Chloronaphthalene
22	100	94	97	0	2634500	bb	835	152	Acenaphthylene
23	100	88	90	0	1504600	bb	862	154	Acenaphthene
24	100	92	97	-1	1816500	vb	938	166	Fluorene
25	100	83	99	0	378070	bv	1050	266	Pentachlorophenol
26	100	93	98	0	2976900	bv*	1080	178	Phenanthrene
27	100	93	98	-1	3121600	vb	1087	178	Anthracene
28	100	95	99	-1	3576100	bb	1256	202	Fluoranthene
29	100	94	98	0	3835900	bb	1289	202	Pyrene
30	100	88	98	0	3706300	bv	1469	228	Benzo(a)anthracene
31	100	93	99	0	3601900	vv	1475	228	Chrysene
32	82	69	73	-1	2989200	bv	1663	252	Benzo(b)fluoranthene
33	100	93	98	-2	3423300	vv	1669	252	Benzo(k)fluoranthene
34	100	94	98	-1	5012300	bv	1719	252	Benzo(e)pyrene
35	100	94	99	-2	2850300	vv	1730	252	Benzo(a)pyrene
36	100	94	99	-1	1502900	vv	1747	252	Perylene
37	100	95	100	0	2853500	bv	1969	276	Indeno(1,2,3-cd)pyrene
38	100	90	99	1	2210600	bv	1978	278	Dibenz(a,h)anthracene
39	100	94	99	-1	2364300	bv	2020	276	Benzo(g,h,i)perylene

INITIAL CHECK REPORT

117

Raw Data File: 6LS06  
 Date: 04-Jan-93  
 Time: 09:33

M/E	ION ABUNDANCE CRITERIA	RELATIVE ABUNDANCE	TUNE
51	30.0 - 60.0% of mass 198	50.00	PASS
68	Less than 2.0% of mass 69	0.00( 0.0)1	PASS
69	Mass 69 relative abundance	62.99	PASS
70	Less than 2.0% of mass 69	0.62( 1.0)1	PASS
127	40.0 - 60.0% of mass 198	59.06	PASS
197	Less than 1% of mass 198	0.17	PASS
198	Base peak, 100% relative abundance	100.00	PASS
199	5 - 9% of mass 198	6.99	PASS
275	10 - 30% of mass 198	20.08	PASS
365	Greater than 1% of mass 198	1.97	PASS
441	Present, but less than mass 443	9.45	PASS
442	Greater than 40% of mass 198	59.06	PASS
443	17 - 23% of mass 442	11.61( 19.7)2	PASS



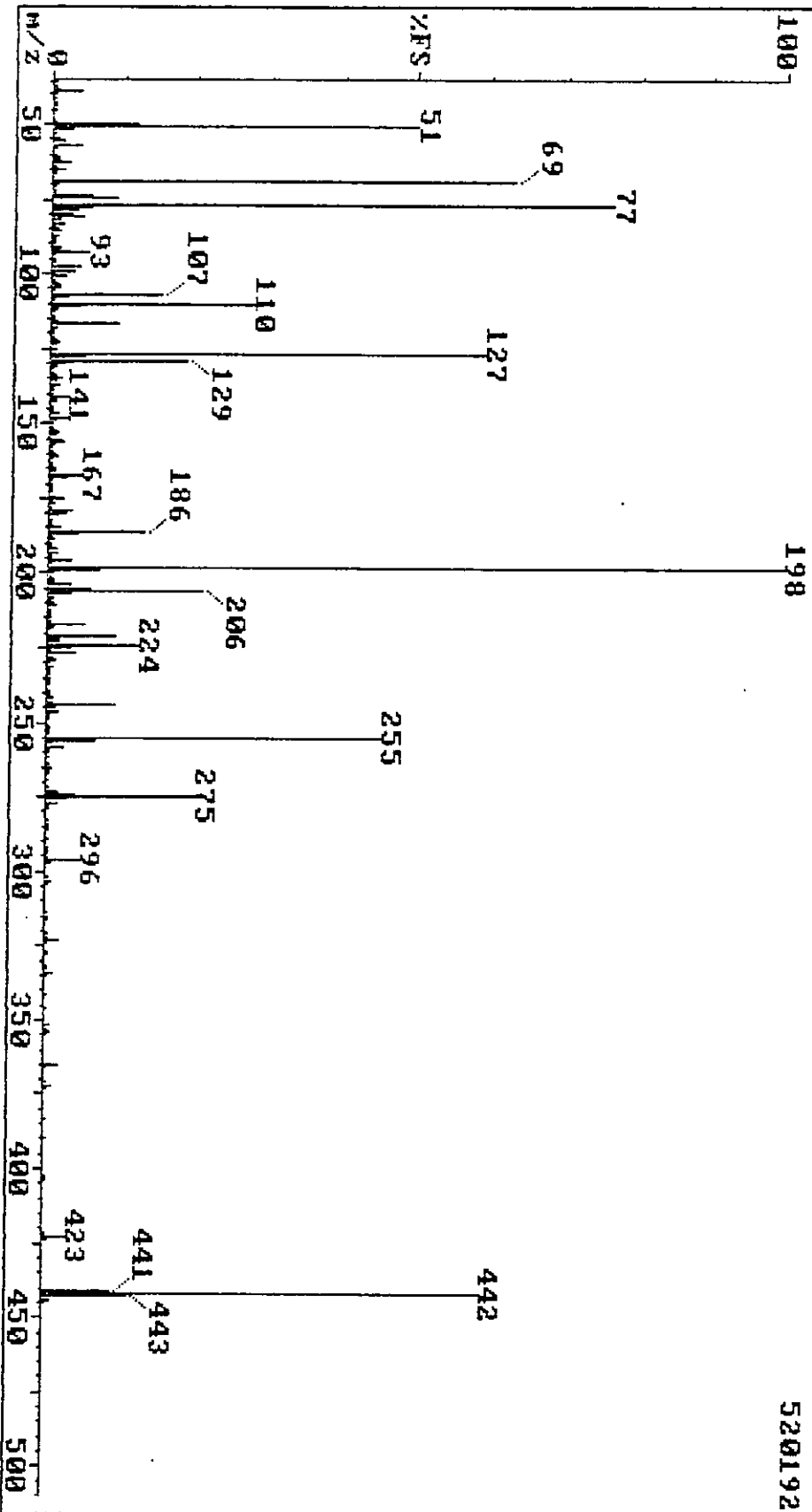
04-Jan-93 08:33  
Sample: DFTPP

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G

GL508 740 (9.167)

520192



PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int
1	26	750	0.15	55	99	17132	3.30	109	154	4352	0.84	163	205	4620	0.73	187	257	952	0.12
2	37	1122	0.22	56	100	1352	0.32	110	155	7232	1.35	164	205	1824	0.35	188	267	802	0.15
3	38	3296	0.63	57	101	7752	1.38	111	156	10616	2.08	165	210	4282	0.92	189	272	928	0.18
4	39	20736	3.99	58	102	1312	0.25	112	157	3620	0.71	166	211	5312	1.02	190	273	8320	1.60
5	40	2364	0.44	59	103	3520	0.68	113	158	2352	0.45	167	212	2096	0.40	191	274	1948	0.37
6	41	2528	0.49	60	104	5696	1.09	114	159	2128	0.41	168	213	1088	0.21	192	275	10448	20.02
7	43	1784	0.38	61	105	8080	1.17	115	160	3500	0.59	169	214	1056	0.20	193	276	14272	2.74
8	44	1248	0.24	62	106	1616	0.31	116	161	5882	1.13	170	215	1504	0.29	194	277	8128	1.56
9	45	736	0.14	63	107	7384	15.16	117	162	2080	0.40	171	216	2624	0.50	195	278	1760	0.34
10	49	1264	0.24	64	108	12224	2.35	118	163	1024	0.20	172	217	27136	5.22	196	279	700	0.13
11	50	51696	11.86	65	109	1616	0.31	119	164	1020	0.20	173	218	4480	0.86	197	283	1424	0.27
12	51	260096	50.00	66	110	143360	27.56	120	165	4928	0.95	174	219	876	0.17	198	284	1216	0.23
13	52	14208	2.73	67	111	21248	4.08	121	166	3952	0.76	175	221	45396	9.40	199	285	2026	0.40
14	53	1648	0.32	68	112	3482	0.67	122	167	22784	4.38	176	222	7360	1.41	200	286	784	0.15
15	55	3232	0.62	69	113	1680	0.32	123	168	12864	2.47	177	223	7424	1.43	201	289	638	0.13
16	56	8640	1.66	70	114	872	0.17	124	169	2944	0.57	178	224	65536	12.60	202	292	704	0.14
17	57	20430	3.94	71	115	1636	0.33	125	170	1216	0.23	179	225	16640	3.20	203	293	2480	0.48
18	58	1472	0.28	72	116	3904	0.75	126	171	1552	0.30	180	226	2176	0.42	204	294	832	0.16
19	60	548	0.16	73	117	47572	9.20	127	172	2208	0.42	181	227	21248	4.09	205	295	764	0.14
20	61	3584	0.69	74	118	4224	0.91	128	173	2944	0.57	182	228	3520	0.62	206	296	23552	4.53
21	62	4224	0.91	75	119	1230	0.25	129	174	4608	0.89	183	229	6272	1.21	207	297	3584	0.69
22	63	11520	2.21	76	120	1568	0.30	130	175	9152	1.76	184	230	1584	0.30	208	302	808	0.16
23	64	2048	0.39	77	121	820	0.16	131	176	2976	0.57	185	231	3280	0.63	209	303	3792	0.73
24	65	7620	1.48	78	122	4416	0.85	132	177	4282	0.82	186	232	1216	0.23	210	304	1168	0.22
25	66	980	0.19	79	123	6720	1.29	133	178	1632	0.31	187	233	924	0.18	211	314	1600	0.31
26	67	956	0.19	80	124	3456	0.66	134	179	15488	2.98	188	234	1808	0.35	212	315	2800	0.54
27	69	327680	62.99	81	125	3648	0.70	135	180	11840	2.28	189	235	2320	0.45	213	316	2096	0.40
28	70	3216	0.62	82	127	307200	59.06	136	181	6592	1.27	190	236	2048	0.39	214	321	1104	0.21
29	71	2128	0.41	83	128	24576	4.72	137	182	2976	0.57	191	237	2480	0.48	215	322	724	0.14
30	72	1728	0.33	84	129	96256	18.50	138	183	1344	0.26	192	239	1360	0.26	216	323	9792	1.88
31	73	1848	0.35	85	130	9600	1.95	139	184	1568	0.30	193	240	1216	0.23	217	324	2048	0.39
32	74	29184	5.61	86	131	3088	0.59	140	185	8000	1.54	194	241	1648	0.32	218	327	1920	0.37
33	75	46080	8.86	87	132	2160	0.42	141	186	69632	13.39	195	242	3968	0.76	219	328	1204	0.21
34	77	397312	76.38	88	133	1632	0.31	142	187	19712	3.79	196	243	3502	0.73	220	332	744	0.14
35	78	27392	5.27	89	134	3312	0.54	143	188	2528	0.49	197	244	49408	9.50	221	333	1082	0.21
36	79	18176	3.49	90	135	8256	1.59	144	189	3712	0.71	198	245	7040	1.35	222	334	6016	1.16
37	80	15194	2.90	91	136	3632	0.70	145	190	1104	0.21	199	246	8256	1.59	223	335	1696	0.33
38	81	21760	4.18	92	137	5568	1.07	146	191	2048	0.39	200	247	2128	0.41	224	341	1136	0.22
39	82	6720	1.29	93	138	1776	0.34	147	192	5440	1.05	201	248	912	0.16	225	346	2560	0.49
40	83	7808	1.50	94	139	1568	0.30	148	193	5696	1.09	202	249	2224	0.43	226	352	3168	0.61
41	84	1963	0.38	95	140	1600	0.31	149	194	1696	0.33	203	251	796	0.15	227	353	2240	0.43
42	85	4288	0.82	96	141	11548	2.24	150	195	1232	0.24	204	252	696	0.13	228	354	3296	0.63
43	86	5858	1.13	97	142	4992	0.96	151	196	15680	3.01	205	253	1200	0.23	229	355	748	0.14
44	87	3376	0.65	98	143	3872	0.74	152	197	868	0.17	206	254	852	0.16	230	365	10240	1.97
45	88	3123	0.61	99	144	1728	0.33	153	198	520192	100.00	207	255	236544	45.47	231	366	1632	0.31
46	89	1568	0.30	100	145	1344	0.26	154	199	36352	6.99	208	256	34816	6.69	232	371	868	0.17
47	90	840	0.16	101	146	2560	0.49	155	200	4608	0.89	209	257	3152	0.61	233	372	5120	0.98
48	91	5440	1.05	102	147	6144	1.18	156	201	2464	0.47	210	258	12282	2.36	234	373	1536	0.30
49	92	4544	0.87	103	148	12928	2.49	157	202	3872	0.74	211	259	2704	0.52	235	383	1424	0.27
50	93	27136	5.22	104	149	3488	0.67	158	203	3456	0.66	212	260	1020	0.20	236	390	768	0.15
51	94	2816	0.54	105	150	1568	0.30	159	204	16192	3.11	213	261	976	0.19	237	402	1994	0.37
52	95	1938	0.36	106	151	2912	0.56	160	205	29696	5.71	214	264	1104	0.21	238	403	2932	0.54
53	96	2528	0.49	107	152	3152	0.61	161	206	109568	21.06	215	265	4864	0.94	239	404	1640	0.29
54	98	19456	3.74	108	153	5376	1.03	162	207	15488	2.98	216	266	1952	0.38	240	421	2202	0.42

11138 740 0.1674

PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int
271	422	3120	0.41	1273	424	3264	0.63	1275	442	307200	19.06	1277	444	4144	1.16				
272	423	16896	3.25	1274	441	49152	9.45	1276	443	60416	11.61	1278	445	1024	0.28				

Triangle Laboratories of RTP, Inc.  
Initial Calibration Curve

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ICAL File: ICALGD30 Date of Analysis :12/30/92 Analyte List: PAH

RF20 GL462 RF50 GL467 RF80 GL463  
RF120 GL464 RF160 GL465

Analyte	Flag	RF20	RF50	RF80	RF120	RF160	RFMEAN	%RSD
1,4-Dichlorobenzene-d4	I							
Naphthalene-d8	I							
2-Methylnaphthalene		0.591	0.449	0.472	0.472	0.484	0.493	11.3
Naphthalene		0.782	0.574	0.600	0.590	0.573	0.624	14.3
Acenaphthene-d10	I							
Acenaphthene	C	0.722	0.578	0.573	0.581	0.593	0.609	10.4
Fluorene		0.920	0.745	0.761	0.758	0.766	0.790	9.3
2-Chloronaphthalene		0.778	0.600	0.625	0.625	0.645	0.655	10.8
Acenaphthylene		1.219	1.001	0.987	0.994	0.959	1.032	10.2
Phenanthrene-d10	I							
Phenanthrene		0.694	0.552	0.553	0.507	0.478	0.557	14.9
Anthracene		0.695	0.568	0.567	0.498	0.468	0.559	15.7
Fluoranthene	C	0.769	0.653	0.648	0.590	0.535	0.639	13.6
Chrysene-d12	I							
Chrysene		0.705	0.539	0.562	0.554	0.524	0.577	12.7
Pyrene		0.948	0.759	0.791	0.621	0.519	0.727	22.6
Benzo(a)anthracene		0.687	0.576	0.597	0.575	0.560	0.599	8.5
Perylene-d12	I							
Benzo(b)fluoranthene		0.644	0.709	0.734	0.835	0.882	0.761	12.7
Benzo(k)fluoranthene		1.200	0.870	0.966	0.942	0.904	0.977	13.4
Benzo(e)pyrene		0.740	0.691	0.745	0.794	0.831	0.760	7.1
Benzo(a)pyrene	C	0.770	0.666	0.728	0.764	0.780	0.742	6.3
Perylene		0.670	0.395	0.431	0.431	0.393	0.464	25.1
Indeno(1,2,3-cd)pyrene		0.478	0.612	0.668	0.763	0.875	0.679	22.2
Dibenz(a,h)anthracene		0.286	0.446	0.477	0.566	0.649	0.485	28.2
Benzo(g,h,i)perylene		0.459	0.540	0.601	0.659	0.718	0.595	16.9
=====								
Surrogate	Flag	RF20	RF50	RF80	RF120	RF160	RFMEAN	%RSD
Anthracene-d10	S	0.362	0.301	0.315	0.309	0.316	0.321	7.5
Pyrene-d10	S	0.823	0.672	0.753	0.655	0.575	0.695	13.7

Approved by:

*J. Lyon*

Date

1/5/93

\* - Fails QC Criteria for %RSD; << - Rf less than minimum QC RF; >>- RF greater than maximum QC RF

ICAL.EXE v2.5

CCAL File: GL467 Date of Analysis :12/30/92 Analyte List: PAH  
ICAL File: ICALGD30

Analyte	Flag	RF50	RFMEAN	%D
1,4-Dichlorobenzene-d4	I			
Naphthalene-d8	I			
2-Methylnaphthalene		0.449	0.493	8.9
Naphthalene		0.574	0.624	8.0
Acenaphthene-d10	I			
Acenaphthene	C	0.578	0.609	5.1
Fluorene		0.745	0.790	5.7
2-Chloronaphthalene		0.600	0.655	8.4
Acenaphthylene		1.001	1.032	3.0
Phenanthrene-d10	I			
Phenanthrene		0.552	0.557	0.9
Anthracene		0.568	0.559	-1.6
Fluoranthene	C	0.653	0.639	-2.2
Chrysene-d12	I			
Chrysene		0.539	0.577	6.6
Pyrene		0.759	0.727	-4.4
Benzo(a)anthracene		0.576	0.599	3.8
Perylene-d12	I			
Benzo(b)fluoranthene		0.709	0.761	6.8
Benzo(k)fluoranthene		0.870	0.977	11.0
Benzo(e)pyrene		0.691	0.760	9.1
Benzo(a)pyrene	C	0.666	0.742	10.2
Perylene		0.395	0.464	14.9
Indena(1,2,3-cd)pyrene		0.612	0.679	9.9
Dibenz(a,h)anthracene		0.446	0.485	8.0
Benzo(g,h,i)perylene		0.540	0.595	9.2
=====				
Surrogate	Flag	RF50	RFMEAN	%D
=====				
Anthracene-d10	S	0.301	0.321	6.2
Pyrene-d10	S	0.672	0.695	3.3

Approved by: J. Lyon Date 1/5/93

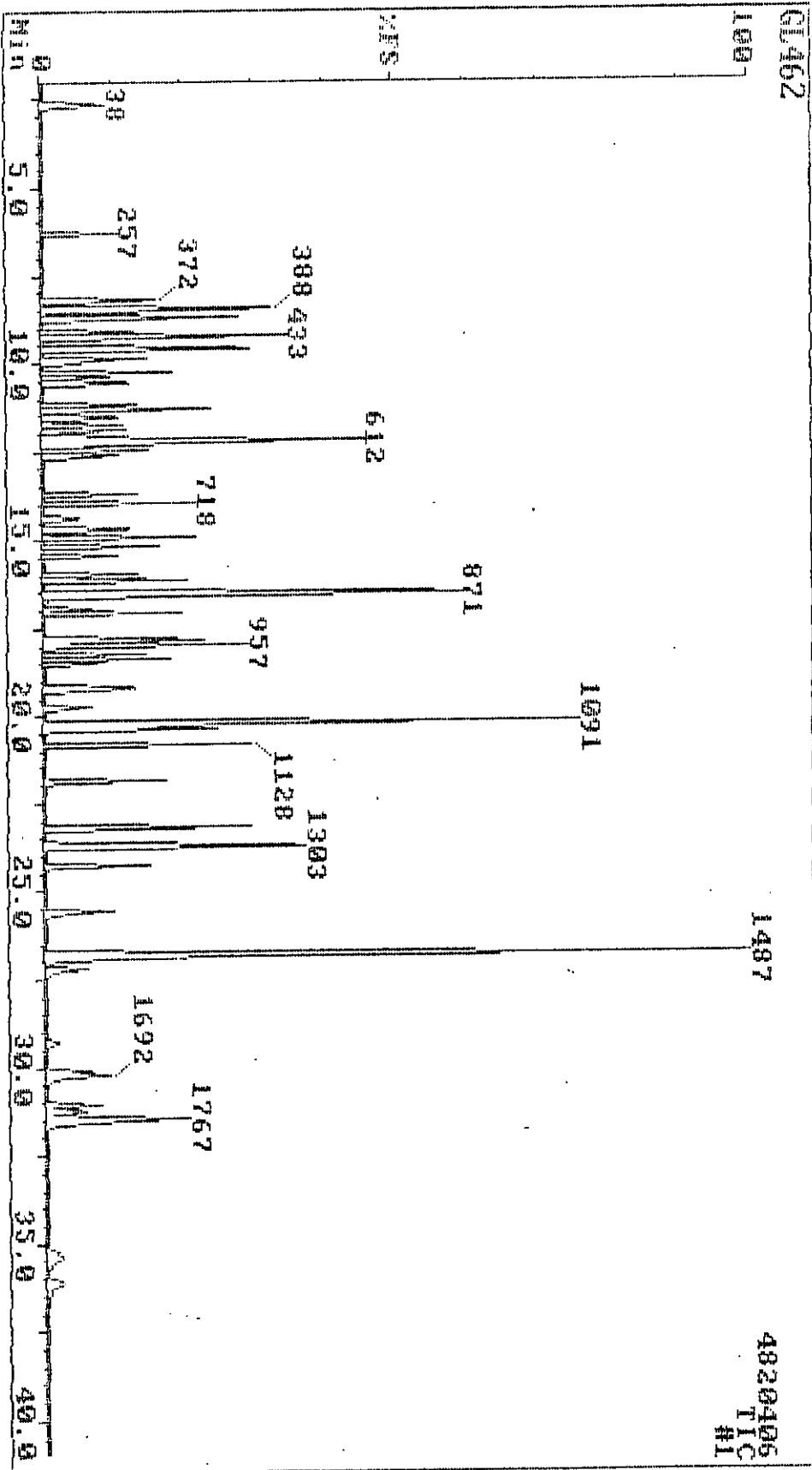
\*- Fails QC Criteria for %D; << - Rf less then minimum QC RF; >>- RF greater than maximum QC RF

CCAL.EXE v2.5

38-Dec-92 08:13  
Sample: SST0020

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(919) 544-5729  
Instrument G



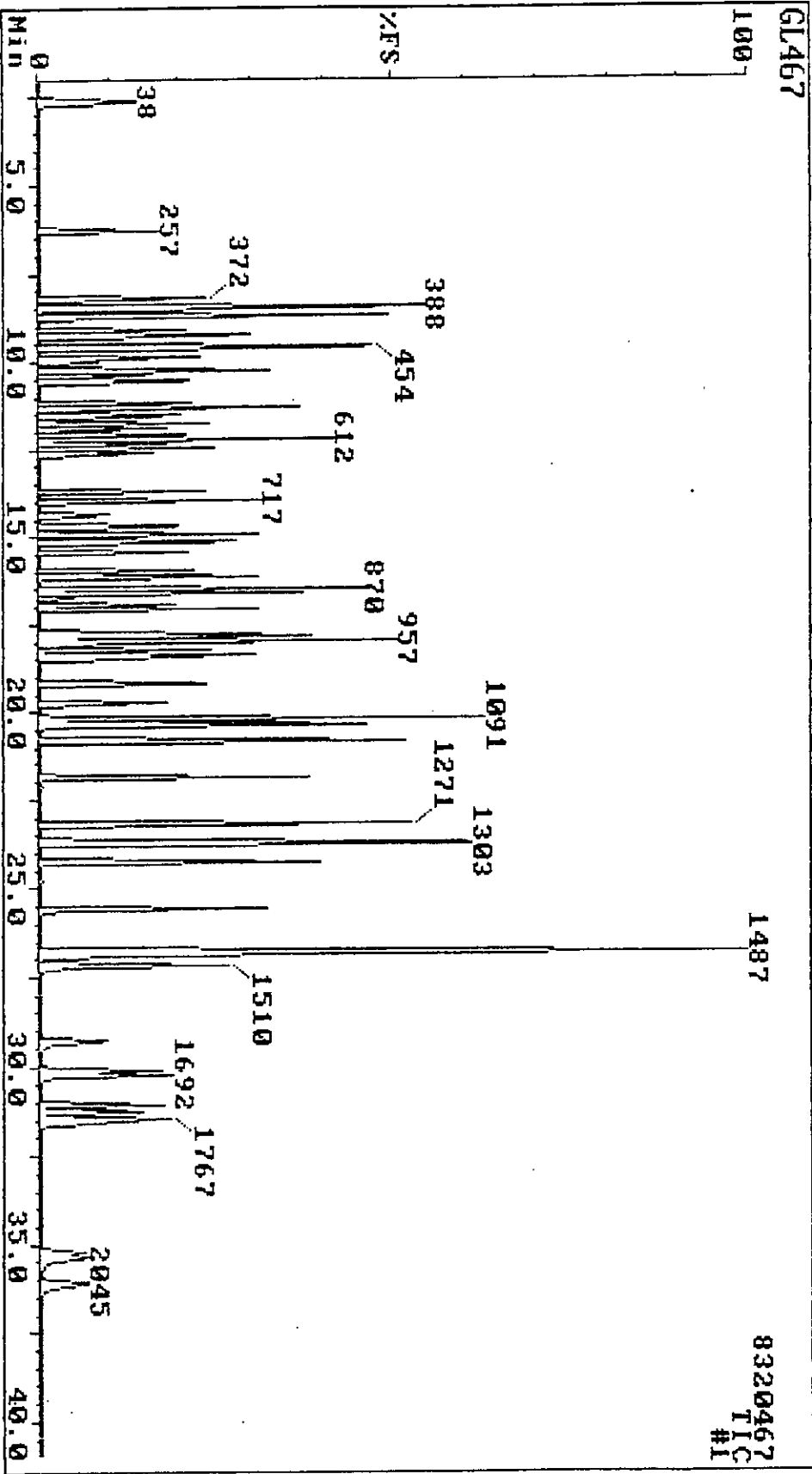
No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	100	82	99	1	605760	bb	433	152 1,4-Dichlorobenzene-d4
2	100	89	94	0	2338500	bb	612	136 Naphthalene-d8
3	100	95	99	1	1642400	bb	871	164 Acenaphthene-d10
4	100	90	97	0	3708600	bv	1091	188 Phenanthrene-d10
5	97	69	98	-1	3466100	bv	1487	240 Chrysene-d12
6	100	88	98	-1	1596700	bv	1767	264 Perylene-d12
7	100	96	98	0	307160	bb	257	112 2-Fluorophenol
8	86	41	97	0	354030	bb	401	132 2-Chlorophenol-d4
9	86	52	96	-1	379160	bb	388	99 Phenol-d5
10	100	89	98	0	284160	bb	453	152 1,2-Dichlorobenzene-d4
11	100	83	99	0	352780	bb	510	82 Nitrobenzene-d5
12	100	64	97	0	348400	bb	559	185 1,3,5-Trichlorobenzene-d3
13	100	93	98	0	204100	bb	620	240 1,4-Dibromobenzene-d4
14	100	91	98	0	762820	bb	775	172 2-Fluorobiphenyl
15	100	81	99	-1	93724	bb	987	330 2,4,6-Tribromophenol
16	100	86	97	0	672030	vb*	1099	188 Anthracene-d10
17	100	85	97	0	1426300	bb	1301	212 Pyrene-d10
18	100	89	98	0	720310	bb	1334	244 Terphenyl-d14
19	100	95	98	0	914460	bb	615	128 Naphthalene
20	100	88	90	0	690750	bb	718	142 2-Methylnaphthalene
21	100	96	98	0	639110	bb	788	162 2-Chloronaphthalene
22	100	94	97	0	1001000	bb	849	152 Acenaphthylene
23	100	86	88	0	592620	vb	875	154 Acenaphthene
24	100	93	98	0	755790	bb	952	166 Fluorene
25	100	84	98	0	92748	bv	1064	266 Pentachlorophenol
26	100	93	98	0	1287500	bv	1094	178 Phenanthrene
27	100	95	98	-1	1289400	vb*	1101	178 Anthracene
28	100	95	99	0	1426100	bb	1271	202 Fluoranthene
29	100	91	98	-1	1642600	bb	1303	202 Pyrene
30	86	62	75	0	1189700	bv	1486	228 Benzo(a)anthracene
31	97	75	92	-1	1222400	vv	1491	228 Chrysene
32	81	68	71	-1	514370	b!v	1686	252 Benzo(b)fluoranthene
33	100	92	97	-1	958380	!v	1692	252 Benzo(k)fluoranthene
34	100	94	98	-1	590460	bv	1743	252 Benzo(e)pyrene
35	100	94	97	-1	614730	vv	1754	252 Benzo(a)pyrene
36	91	69	77	0	534550	vv	1773	252 Perylene
37	98	76	92	-1	381320	M	1993	276 Indeno(1,2,3-cd)pyrene
38	95	75	88	-1	228260	A	2002	278 Dibenz(a,h)anthracene
39	93	80	94	-2	366580	bv	2046	276 Benzo(g,h,i)perylene

*Handwritten notes:*  
 b!v ✓  
 !v ✓  
 12-26-92

30-Dec-92 11:55  
Sample: SSTD050

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(919) 544-5729  
Instrument G





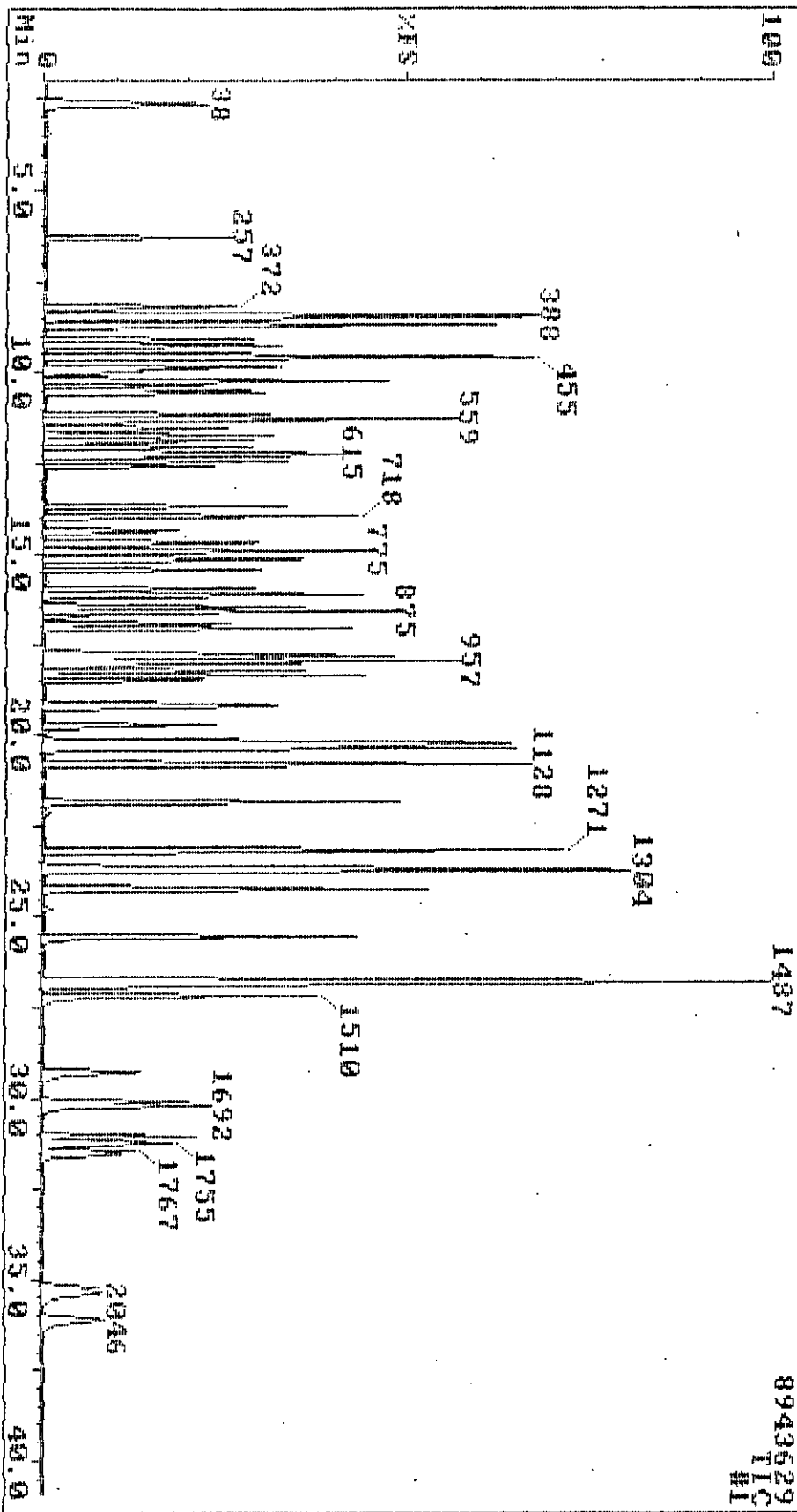
No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	GM Name
1	100	78	99	1	882830	bb	433	152 1,4-Dichlorobenzene-d4
2	100	83	93	0	3297000	bv	612	136 Naphthalene-d8
3	100	95	99	0	2183300	bb	870	164 Acenaphthene-d10
4	100	90	97	-1	5186300	bv	1090	188 Phenanthrene-d10
5	88	56	96	-1	4784200	bv	1487	240 Chrysene-d12
6	100	85	93	-1	2429100	bv	1767	264 Perylene-d12
7	100	95	97	0	933830	bb	257	112 2-Fluorophenol
8	84	46	98	0	959140	bb	401	132 2-Chlorophenol-d4
9	85	50	97	-1	1234900	bb	388	99 Phenol-d5
10	100	80	94	0	729440	bb	453	152 1,2-Dichlorobenzene-d4
11	100	83	99	0	1237100	bb	510	82 Nitrobenzene-d5
12	98	59	98	0	852670	bb	559	185 1,3,5-Trichlorobenzene-d3
13	100	92	98	0	540100	bb	620	240 1,4-Dibromobenzene-d4
14	100	90	98	0	1905000	bb	775	172 2-Fluorobiphenyl
15	100	80	99	-1	371440	bb	987	330 2,4,6-Tribromophenol
16	100	83	96	0	1949800	vb	1099	188 Anthracene-d10
17	100	85	97	0	4016200	bb	1301	212 Pyrene-d10
18	100	86	97	0	2578100	bb	1334	244 Terphenyl-d14
19	100	96	99	0	2364900	bb	615	128 Naphthalene
20	100	89	91	-1	1848900	bb	717	142 2-Methylnaphthalene
21	100	96	98	0	1638500	bb	788	162 2-Chloronaphthalene
22	100	94	97	0	2732300	bb	849	152 Acenaphthylene
23	100	88	90	0	1576600	vb	875	154 Acenaphthene
24	100	96	99	0	2032500	bb	952	166 Fluorene
25	100	85	99	-1	453910	bv	1063	266 Pentachlorophenol
26	100	93	98	0	3581700	bv*	1094	178 Phenanthrene
27	100	94	98	0	3684800	vv*	1102	178 Anthracene
28	100	95	99	0	4231300	bv	1271	202 Fluoranthene
29	100	93	99	-1	4536900	vv	1303	202 Pyrene
30	100	85	97	0	3446200	bv	1486	228 Benzo(a)anthracene
31	100	89	99	-1	3222900	vv	1491	228 Chrysene
32	81	67	72	-1	2151900	bv	1686	252 Benzo(b)fluoranthene
33	100	92	97	-1	2643000	vv	1692	252 Benzo(k)fluoranthene
34	100	93	98	-1	2098300	vv	1743	252 Benzo(e)pyrene
35	100	94	99	-1	2023500	vv	1754	252 Benzo(a)pyrene
36	100	89	96	0	1198900	vv	1773	252 Perylene
37	100	94	100	-2	1857500	b? ✓	1992	276 Indeno(1,2,3-cd)pyrene
38	100	90	97	-2	1352900	b? ✓	2001	278 Dibenz(a,h)anthracene
39	95	94	99	-3	1639700	bv	2045	276 Benzo(g,h,i)perylene

30-Dec-92 09:02  
Sample: SST0080

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G

GL463



8943529  
TIC  
#1

No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM	Name
1	100	76	99	1	764300	bb	433	152	1,4-Dichlorobenzene-d4
2	100	87	93	0	2708100	bb	612	136	Naphthalene-d8
3	100	95	99	0	2006700	bv	870	164	Acenaphthene-d10
4	100	88	97	0	4760500	bv	1091	188	Phenanthrene-d10
5	96	58	96	-1	4054900	bv	1487	240	Chrysene-d12
6	100	82	93	-1	1814200	bv	1767	264	Perylene-d12
7	100	94	96	0	1161700	bb	257	112	2-Fluorophenol
8	84	39	96	0	1294600	bb	401	132	2-Chlorophenol-d4
9	84	49	95	-1	1518700	bv	388	99	Phenol-d5
10	100	85	96	0	1041500	bb	453	152	1,2-Dichlorobenzene-d4
11	100	82	98	0	1781400	bb	510	82	Nitrobenzene-d5
12	98	59	98	0	1386900	bb	559	185	1,3,5-Trichlorobenzene-d3
13	100	92	98	0	881960	bb	620	240	1,4-Dibromobenzene-d4
14	100	90	98	0	2981600	bb	775	172	2-Fluorobiphenyl
15	100	78	99	-1	468710	bb	987	330	2,4,6-Tribromophenol
16	100	84	96	0	3001400	vv	1099	188	Anthracene-d10
17	100	86	96	0	6102800	bv	1301	212	Pyrene-d10
18	100	86	97	0	3738300	bb	1334	244	Terphenyl-d14
19	100	95	98	0	3251500	bb	615	128	Naphthalene
20	100	89	91	0	2557500	bb	718	142	2-Methylnaphthalene
21	100	95	98	0	2506600	bb	788	162	2-Chloronaphthalene
22	100	93	97	0	3961900	bb	849	152	Acenaphthylene
23	100	88	90	0	2301500	bb	875	154	Acenaphthene
24	100	95	99	0	3052200	vb	952	166	Fluorene
25	100	84	99	0	594490	bv	1064	266	Pentachlorophenol
26	100	93	98	0	5266600	bv*	1094	178	Phenanthrene
27	100	93	98	0	5394700	vb*	1102	178	Anthracene
28	100	94	99	0	6173200	bb	1271	202	Fluoranthene
29	100	94	99	0	6414000	vv	1304	202	Pyrene
30	100	77	94	0	4844500	bv	1486	228	Benzo(a)anthracene
31	100	89	99	-1	4559800	vv	1491	228	Chrysene
32	83	69	74	-1	2662000	bv	1686	252	Benzo(b)fluoranthene
33	100	92	98	-1	3506200	vv	1692	252	Benzo(k)fluoranthene
34	100	93	98	-1	2702100	bv	1743	252	Benzo(e)pyrene
35	100	94	99	-1	2643100	vv	1754	252	Benzo(a)pyrene
36	100	91	97	0	1564400	vv	1773	252	Perylene
37	100	94	99	-1	2425500	bv	1993	276	Indeno(1,2,3-cd)pyrene
38	100	88	97	-1	1732500	bv	2002	278	Dibenz(a,h)anthracene
39	100	94	99	-2	2181100	b?	2046	276	Benzo(g,h,i)perylene

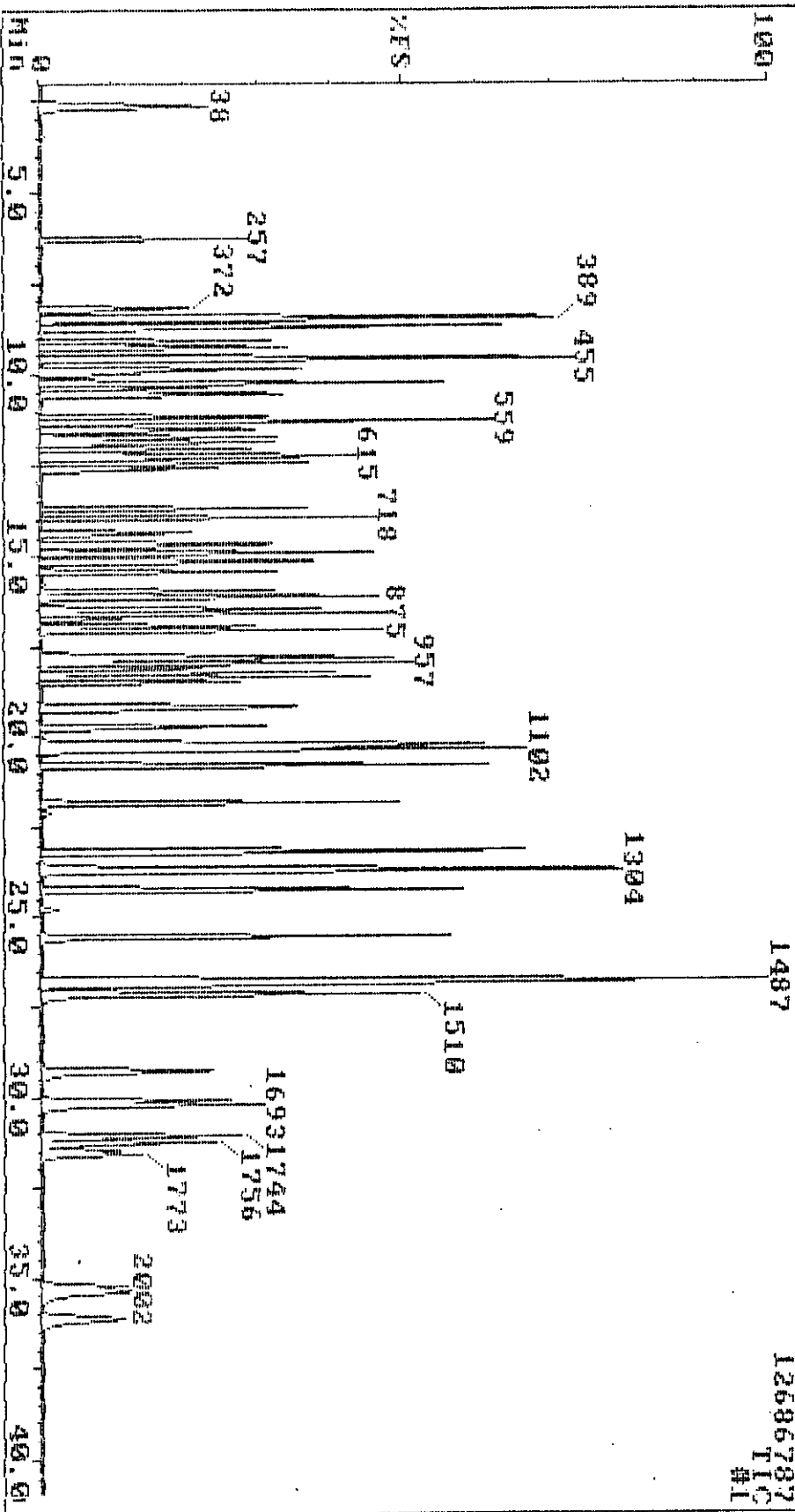
*Ins 12.30.92*

30-Dec-92 09:54  
Sample: SSTD128

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(919) 544-5729  
Instrument G

GL464



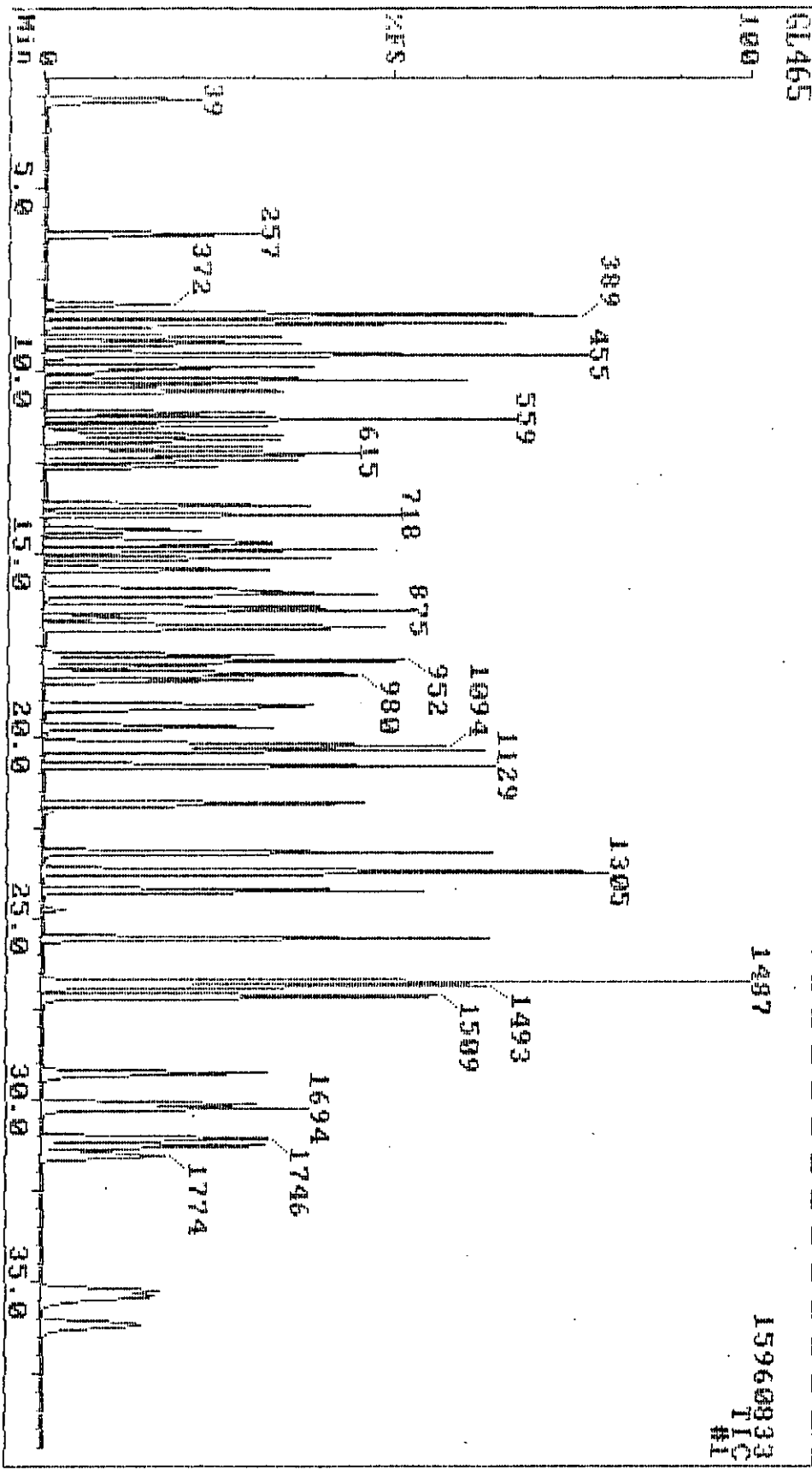
12686787  
TIC  
#1

No.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	QM Name
1	99	71	99	1	766540	bb	433	152 1,4-Dichlorobenzene-d4
2	100	87	93	0	2795600	bv	612	136 Naphthalene-d8
3	100	93	99	0	1970900	bv	870	164 Acenaphthene-d10
4	100	86	97	0	4722600	bv	1091	188 Phenanthrene-d10
5	88	46	95	0	4362400	bv	1488	240 Chrysene-d12
6	100	82	93	0	2102900	bv	1768	264 Perylene-d12
7	100	94	96	0	1884100	bb	257	112 2-Fluorophenol
8	84	39	96	0	1982200	bb	401	132 2-Chlorophenol-d4
9	91	49	96	0	2575800	bv	389	99 Phenol-d5
10	100	84	95	0	1561900	bb	453	152 1,2-Dichlorobenzene-d4
11	100	82	98	0	2939500	bb	510	82 Nitrobenzene-d5
12	96	56	98	0	2003500	bb	559	185 1,3,5-Trichlorobenzene-d3
13	100	92	98	0	1325900	bb	620	240 1,4-Dibromobenzene-d4
14	100	90	98	0	4310300	bb	775	172 2-Fluorobiphenyl
15	100	80	99	0	813340	bv	988	330 2,4,6-Tribromophenol
16	100	84	96	0	4382700	vv	1099	188 Anthracene-d10
17	100	86	97	0	8571700	bb	1301	212 Pyrene-d10
18	100	86	97	0	6000300	bv	1334	244 Terphenyl-d14
19	100	95	98	0	4952300	bv	615	128 Naphthalene
20	100	88	91	0	3956800	vb	718	142 2-Methylnaphthalene
21	100	95	98	0	3695300	bb	788	162 2-Chloronaphthalene
22	100	93	97	0	5875400	bb	849	152 Acenaphthylene
23	100	87	90	0	3434300	bv	875	154 Acenaphthene
24	100	95	99	0	4482800	bb	952	166 Fluorene
25	100	82	98	0	1063900	bv	1064	266 Pentachlorophenol
26	100	92	97	0	7180800	bv*	1094	178 Phenanthrene
27	100	93	99	0	7059400	vv*	1102	178 Anthracene
28	100	93	98	0	8357300	bv	1271	202 Fluoranthene
29	100	92	98	0	8125200	bv	1304	202 Pyrene
30	100	81	99	0	7526200	bv	1486	228 Benzo(a)anthracene
31	100	92	99	0	7249100	vv	1492	228 Chrysene
32	89	68	74	0	5265400	bv	1687	252 Benzo(b)fluoranthene
33	100	91	97	0	5940900	v? <i>12-21-92</i>	1693	252 Benzo(k)fluoranthene
34	100	93	98	0	5011200	vv	1744	252 Benzo(e)pyrene
35	100	94	99	0	4819800	vv	1755	252 Benzo(a)pyrene
36	100	92	99	0	2719800	v? <i>12-21-92</i>	1773	252 Perylene
37	100	94	99	0	4816000	b? <i>12-21-92</i>	1994	276 Indeno(1,2,3-cd)pyrene
38	100	90	98	0	3567700	bb	2003	278 Dibenz(a,h)anthracene
39	100	94	99	0	4160600	bv	2048	276 Benzo(g,h,i)perylene

30-Dec-92 10:46  
Sample: SSTD160

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G



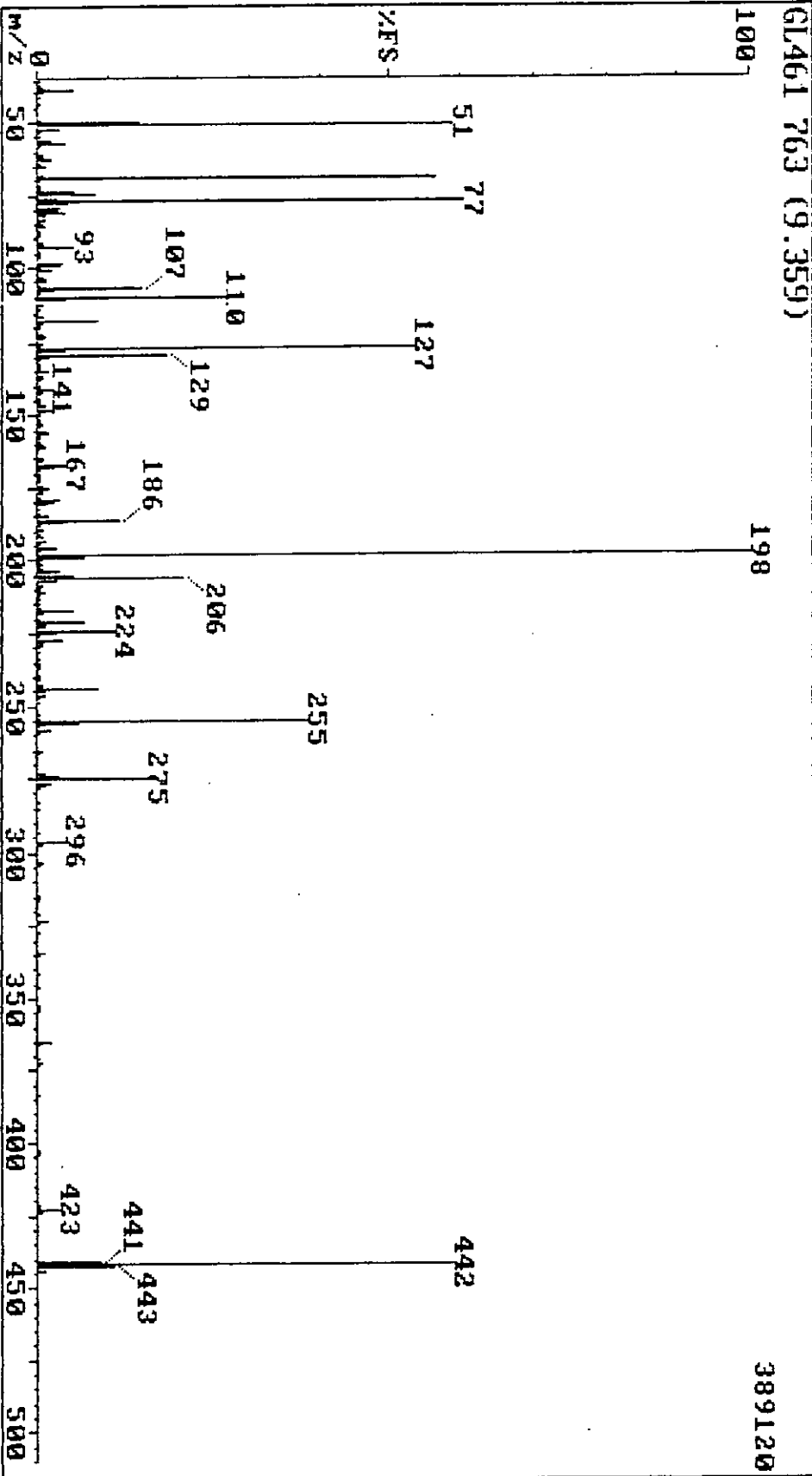
15960833  
TIC  
#1

No.	MAT	FOR	REV	Delta	Area	P. Flags	Scan	QM	Name
1	100	82	99	1	758980	bb	433	152	1,4-Dichlorobenzene-d4
2	100	86	94	0	2826100	bv	612	136	Naphthalene-d8
3	100	90	98	0	1906200	bv	870	164	Acenaphthene-d10
4	100	87	97	-1	4492300	bv	1090	188	Phenanthrene-d10
5	86	53	95	0	4440200	bv	1488	240	Chrysene-d12
6	100	84	95	1	2587000	vv	1769	264	Perylene-d12
7	100	94	96	0	2789900	bb	257	112	2-Fluorophenol
8	85	40	96	0	2786400	bb	401	132	2-Chlorophenol-d4
9	93	51	97	0	3948100	bv	389	99	Phenol-d5
10	100	83	95	0	2128800	bb	453	152	1,2-Dichlorobenzene-d4
11	100	77	98	1	4036800	bb	511	82	Nitrobenzene-d5
12	95	54	98	0	2583100	bb	559	185	1,3,5-Trichlorobenzene-d3
13	100	91	98	0	1739900	bb	620	240	1,4-Dibromobenzene-d4
14	100	89	98	0	5551900	bb	775	172	2-Fluorobiphenyl
15	100	76	98	0	1248800	bv	988	330	2,4,6-Tribromophenol
16	100	85	97	0	5675000	bb	1099	188	Anthracene-d10
17	100	86	97	1	10205000	vv	1302	212	Pyrene-d10
18	100	85	97	0	7211700	bv	1334	244	Terphenyl-d14
19	100	95	98	0	6481300	bv	615	128	Naphthalene
20	100	88	91	0	5471700	vv	718	142	2-Methylnaphthalene
21	100	95	98	0	4920700	bb	788	162	2-Chloronaphthalene
22	100	93	97	0	7310800	bb	849	152	Acenaphthylene
23	100	88	90	0	4524100	bv	875	154	Acenaphthene
24	100	91	97	0	5841900	bv	952	166	Fluorene
25	100	82	98	0	1469400	bv	1064	266	Pentachlorophenol
26	100	91	97	0	8596200	bv*	1094	178	Phenanthrene
27	100	92	98	0	8404800	vv*	1102	178	Anthracene
28	100	92	97	0	9614400	vv	1271	202	Fluoranthene
29	100	90	96	1	9222100	bv	1305	202	Pyrene
30	100	82	99	0	9945500	bv	1486	228	Benzo(a)anthracene
31	100	91	98	1	9301300	vv	1493	228	Chrysene
32	81	67	73	1	9129500	b! <i>1.304</i>	1688	252	Benzo(b)fluoranthene
33	100	91	97	1	9354000	vv	1694	252	Benzo(k)fluoranthene
34	100	92	98	1	8601700	bv	1745	252	Benzo(e)pyrene
35	100	93	99	2	8073700	vv	1757	252	Benzo(a)pyrene
36	100	93	99	1	4063300	vv	1774	252	Perylene
37	100	93	99	2	9050200	b? <i>1.304</i>	1996	276	Indeno(1,2,3-cd)pyrene
38	100	89	98	1	6710900	bb	2004	278	Dibenz(a,h)anthracene
39	100	94	99	2	7424800	bv	2050	276	Benzo(g,h,i)perylene

30-Dec-92 07:56  
Sample: DFTPP

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G





11/01 7:3 11/01/01

12/12/01

PK#	mass	Abs Int	Rel Int	PK#	mass	Abs Int	Rel Int	PK#	mass	Abs Int	Rel Int	PK#	mass	Abs Int	Rel Int	PK#	mass	Abs Int	Rel Int
1	36	1440	0.37	49	96	1328	0.34	97	149	2240	0.58	145	202	3008	0.77	193	258	7424	1.71
2	37	1136	0.29	50	98	17440	3.45	98	150	792	0.20	146	202	676	0.17	194	259	1536	0.39
3	38	5136	0.31	51	99	12224	3.14	99	151	1440	0.37	147	203	2516	0.72	195	265	2380	0.74
4	39	19200	4.93	52	100	1396	0.33	100	152	876	0.23	148	204	12238	3.16	196	266	744	0.19
5	40	2194	0.61	53	101	7296	1.38	101	153	2624	0.67	149	205	20224	5.20	197	273	4864	1.25
6	41	812	0.21	54	103	2368	0.61	102	154	2176	0.56	150	206	79872	20.55	198	274	11392	2.93
7	44	1680	0.43	55	104	4224	1.09	103	155	4928	1.27	151	207	10944	2.81	199	275	60672	15.39
8	49	1712	0.44	56	105	3324	0.98	104	156	6784	1.74	152	208	5136	0.81	200	276	8064	2.07
9	50	56320	14.47	57	106	1772	0.46	105	157	1648	0.42	153	209	1408	0.36	201	277	4544	1.17
10	51	228352	58.68	58	107	53112	14.93	106	158	1824	0.47	154	210	2128	0.55	202	278	1956	0.27
11	52	12672	3.26	59	108	9216	2.37	107	159	1408	0.36	155	211	4800	1.23	203	283	800	0.21
12	53	928	0.24	60	109	1824	0.47	108	160	2752	0.71	156	212	1408	0.36	204	285	1232	0.32
13	55	1296	0.33	61	110	193424	26.58	109	161	4032	1.04	157	213	748	0.19	205	293	1360	0.35
14	56	6912	1.78	62	111	13872	4.08	110	162	1504	0.39	158	215	1344	0.35	206	296	14784	3.80
15	57	14848	3.82	63	112	2592	0.67	111	165	2656	0.68	159	216	1872	0.48	207	297	2352	0.60
16	58	1104	0.28	64	113	1120	0.29	112	166	2368	0.61	160	217	19712	5.07	208	303	2320	0.60
17	61	2480	0.64	65	116	3408	0.88	113	167	14848	3.32	161	218	3088	0.79	209	304	680	0.17
18	62	3056	0.79	66	117	33792	8.68	114	168	9024	2.32	162	220	732	0.19	210	314	884	0.23
19	63	7680	1.97	67	118	3216	0.83	115	169	1680	0.43	163	221	25112	6.71	211	315	1760	0.45
20	64	1328	0.34	68	119	764	0.20	116	170	900	0.23	164	222	4928	1.27	212	316	1168	0.30
21	65	4672	1.20	69	120	1872	0.28	117	171	848	0.22	165	223	4928	1.27	213	321	764	0.20
22	68	2992	0.77	70	122	3232	0.33	118	172	1376	0.35	166	224	41984	10.79	214	323	6400	1.64
23	69	220160	56.56	71	123	5056	1.30	119	173	2128	0.55	167	225	10752	2.76	215	324	1216	0.31
24	70	1840	0.47	72	124	2576	0.66	120	174	3184	0.82	168	226	1472	0.38	216	327	1072	0.28
25	71	1120	0.29	73	125	2448	0.63	121	175	6336	1.63	169	227	14208	3.65	217	334	3936	1.01
26	72	780	0.20	74	126	916	0.24	122	176	2384	0.61	170	228	2352	0.60	218	335	1104	0.28
27	73	1376	0.35	75	127	206848	53.16	123	177	3152	0.81	171	229	3552	0.91	219	341	688	0.18
28	74	19456	5.00	76	128	15552	4.00	124	178	1024	0.26	172	230	784	0.20	220	346	1200	0.31
29	75	31232	8.03	77	129	70656	18.16	125	179	11904	3.06	173	231	2256	0.58	221	352	1824	0.47
30	76	11200	2.98	78	130	6464	1.66	126	180	8640	2.22	174	234	1168	0.30	222	353	1344	0.35
31	77	234496	60.26	79	131	1898	0.49	127	181	4480	1.15	175	235	1360	0.35	223	354	1936	0.50
32	78	17408	4.47	80	132	904	0.23	128	182	732	0.19	176	236	1104	0.28	224	365	7360	1.89
33	79	11904	3.06	81	133	832	0.21	129	184	1008	0.26	177	237	1568	0.40	225	366	988	0.25
34	80	10496	2.70	82	134	2964	0.53	130	185	5888	1.51	178	239	848	0.22	226	371	728	0.19
35	81	14720	3.78	83	135	5312	1.37	131	186	45824	11.73	179	240	772	0.20	227	372	3360	0.86
36	82	4224	1.09	84	136	2672	0.69	132	187	13120	3.37	180	241	776	0.20	228	373	820	0.21
37	83	4288	1.10	85	137	3504	0.90	133	188	1472	0.38	181	242	2496	0.64	229	383	872	0.22
38	84	1088	0.28	86	138	1072	0.28	134	189	2384	0.61	182	243	2288	0.59	230	402	1200	0.31
39	85	2416	0.62	87	139	1296	0.33	135	191	1280	0.33	183	244	32768	8.42	231	403	1936	0.50
40	86	3984	1.02	88	140	844	0.22	136	192	3776	0.97	184	245	4416	1.13	232	404	684	0.18
41	87	2208	0.57	89	141	7936	2.04	137	193	4032	1.04	185	246	5120	1.32	233	421	1456	0.37
42	88	1264	0.32	90	142	2992	0.77	138	194	980	0.25	186	247	1504	0.39	234	422	1520	0.39
43	89	1120	0.29	91	143	2224	0.57	139	196	11264	2.89	187	249	1296	0.33	235	423	11712	3.01
44	91	3344	0.86	92	144	802	0.21	140	197	1584	0.41	188	253	712	0.19	236	424	2496	0.64
45	92	3200	0.32	93	145	876	0.23	141	198	389120	100.00	189	254	760	0.20	237	441	35328	9.08
46	93	19200	4.93	94	146	1728	0.44	142	199	26112	6.71	190	255	148480	38.16	238	442	229376	58.95
47	94	1856	0.48	95	147	4160	1.07	143	200	2976	0.76	191	256	22016	5.66	239	443	42240	10.86
48	95	856	0.22	96	148	8256	2.12	144	201	808	0.21	192	257	2160	0.56	240	444	4608	1.18

DATA TUNE CHECK REPORT

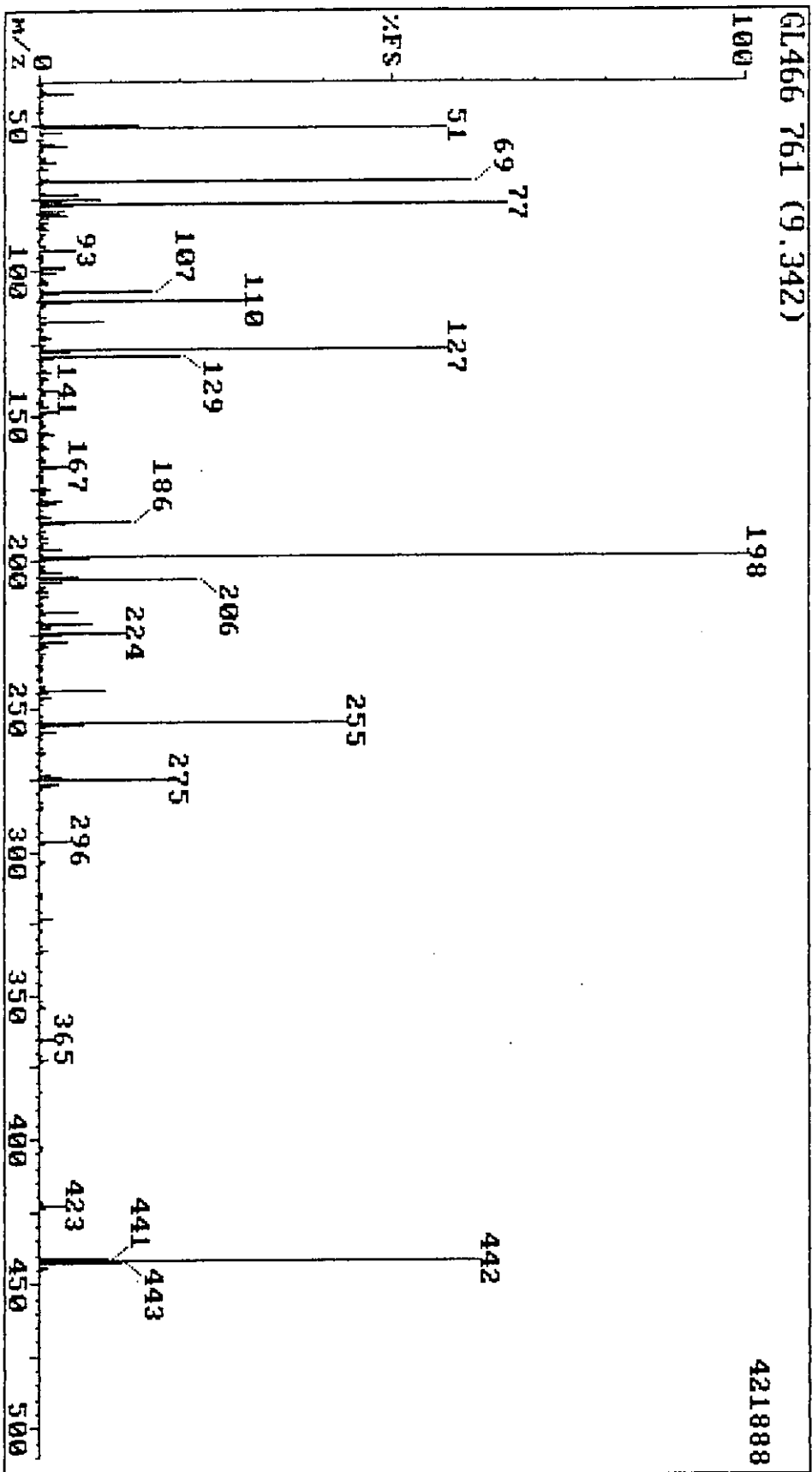
Raw Data File: CL461  
 Date: 30-Dec-72  
 Time: 07:56

m/e	ION ABUNDANCE CRITERIA	RELATIVE ABUNDANCE	TUNE
51	30.0 - 60.0% of mass 198	58.68	PASS
68	Less than 2.0% of mass 69	0.77( 1.4)1	PASS
69	Mass 69 relative abundance	56.58	PASS
70	Less than 2.0% of mass 69	0.47( 0.8)1	PASS
127	40.0 - 60.0% of mass 198	53.16	PASS
197	Less than 1% of mass 198	0.41	PASS
198	Base peak. 100% relative abundance	100.00	PASS
199	5 - 9% of mass 198	6.71	PASS
275	10 - 30% of mass 198	15.59	PASS
365	Greater than 1% of mass 198	1.89	PASS
441	Present. but less than mass 443	9.08	PASS
442	Greater than 40% of mass 198	58.95	PASS
443	17 - 23% of mass 442	10.86( 18.4)2	PASS

30-Dec-92 11:38  
Sample: DFTPP

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G



SI 1966 Feb 19, 3411

Pkt#	Mass	Abs Int	Rel Int	Pkt#	Mass	Abs Int	Rel Int	Pkt#	Mass	Abs Int	Rel Int	Pkt#	Mass	Abs Int	Rel Int	Pkt#	Mass	Abs Int	Rel Int
1	36	1888	0.44	51	99	14288	1.37	103	154	2384	0.57	1194	203	3696	0.88	1205	274	13388	3.27
2	37	1040	0.25	52	100	1776	0.41	104	155	5504	1.30	1195	209	1620	0.40	1206	275	77824	18.45
3	38	3652	0.86	54	101	9088	1.15	105	156	7808	1.95	1196	210	4416	1.05	1207	276	10916	2.56
4	39	19456	4.61	55	102	944	0.22	106	157	2320	0.55	1197	211	4160	0.99	1208	277	5760	1.37
5	40	2443	0.58	56	103	3156	0.74	107	158	2224	0.53	1198	212	688	0.16	1209	278	1360	0.32
6	41	788	0.19	57	104	5440	1.29	108	159	1488	0.35	1199	214	716	0.17	1210	283	988	0.23
7	44	1424	0.34	58	105	5056	1.20	109	160	3088	0.73	1150	215	1312	0.31	1211	284	860	0.20
8	45	708	0.17	59	106	2932	0.48	110	161	4416	1.05	1161	216	1984	0.47	1212	285	1456	0.35
9	49	1472	0.35	60	107	67384	16.02	111	162	1648	0.39	1162	217	23040	5.46	1213	293	1744	0.41
10	50	58624	13.90	61	108	10944	2.59	112	164	796	0.19	1163	218	3696	0.52	1214	296	18688	4.43
11	51	242688	57.52	62	109	2288	0.54	113	165	3488	0.93	1164	220	712	0.17	1215	297	2672	0.63
12	52	13248	3.14	63	110	121356	28.38	114	166	2976	0.71	1155	221	30720	7.28	1216	303	2912	0.69
13	53	1328	0.31	64	111	18432	4.37	115	167	16640	3.94	1166	222	5824	1.39	1217	304	832	0.20
14	55	1488	0.35	65	112	2864	0.58	116	168	10496	2.49	1167	223	5888	1.40	1218	314	1280	0.30
15	56	7516	1.81	66	113	1376	0.33	117	169	2096	0.50	1168	224	51200	12.14	1219	315	2448	0.59
16	57	16896	4.00	67	116	3744	0.39	118	170	864	0.20	1169	225	12736	3.02	1220	316	1456	0.35
17	58	1264	0.30	68	117	38144	9.04	119	171	1040	0.25	1170	226	1472	0.35	1221	321	1008	0.24
18	59	864	0.20	69	118	3792	0.90	120	172	1792	0.42	1171	227	17152	4.07	1222	323	7936	1.88
19	61	2928	0.59	70	119	1020	0.24	121	173	2336	0.55	1172	228	2864	0.68	1223	324	1520	0.36
20	62	3520	0.83	71	120	864	0.20	122	174	3744	0.89	1173	229	4672	1.11	1224	327	1312	0.31
21	63	9688	2.45	72	122	3968	0.74	123	175	7360	1.74	1174	230	1056	0.25	1225	328	808	0.19
22	64	1824	0.43	73	123	5952	1.41	124	176	2528	0.60	1175	231	2528	0.60	1226	333	796	0.19
23	65	5568	1.32	74	124	2300	0.56	125	177	3456	0.82	1176	232	808	0.19	1227	334	4928	1.17
24	68	4352	1.03	75	125	2736	0.55	126	178	1216	0.29	1177	233	804	0.19	1228	335	1328	0.31
25	69	258048	61.17	76	126	1372	0.33	127	179	13184	3.13	1178	234	1328	0.31	1229	341	960	0.23
26	70	1696	0.40	77	127	243712	57.77	128	180	9408	2.23	1179	235	1952	0.46	1230	346	1600	0.38
27	73	2512	0.60	78	128	18176	4.31	129	181	4928	1.17	1180	236	1248	0.30	1231	352	2432	0.59
28	74	22784	5.40	79	129	83968	19.90	130	182	1072	0.25	1181	237	1968	0.47	1232	353	1872	0.44
29	75	36864	8.74	80	130	7744	1.94	131	184	1280	0.30	1182	239	1040	0.25	1233	354	2640	0.63
30	76	13952	3.31	81	131	2272	0.54	132	185	6656	1.56	1183	240	700	0.17	1234	365	9024	2.14
31	77	273528	66.02	82	132	1744	0.41	133	186	53504	12.68	1184	241	1232	0.29	1235	366	1376	0.33
32	78	20460	4.95	83	134	2800	0.66	134	187	15104	3.58	1185	242	2880	0.68	1236	371	856	0.20
33	79	14144	3.35	84	135	6656	1.58	135	188	1872	0.44	1186	243	2944	0.70	1237	372	4480	1.06
34	80	12288	2.91	85	136	3040	0.72	136	189	3008	0.71	1187	244	39168	9.28	1238	373	1088	0.26
35	81	16896	4.00	86	137	4224	1.00	137	191	1632	0.39	1188	245	5312	1.26	1239	383	1168	0.28
36	82	4992	1.18	87	138	1552	0.37	138	192	4608	1.09	1189	246	5824	1.38	1240	402	1680	0.40
37	83	5056	1.20	88	139	1004	0.24	139	193	4664	1.15	1190	247	1456	0.35	1241	403	2176	0.52
38	84	1328	0.31	89	140	1520	0.36	140	194	1104	0.26	1191	249	1664	0.39	1242	404	820	0.19
39	85	3040	0.72	90	141	9664	2.29	141	195	796	0.19	1192	253	840	0.20	1243	421	2080	0.49
40	86	4416	1.05	91	142	3504	0.83	142	196	13696	3.25	1193	254	956	0.23	1244	422	1664	0.39
41	87	2576	0.61	92	143	2800	0.66	143	197	1024	0.24	1194	255	18272	43.20	1245	423	14016	3.32
42	88	1728	0.41	93	144	1024	0.24	144	198	421888	100.00	1195	256	26624	6.31	1246	424	2816	0.67
43	89	1216	0.29	94	145	1088	0.26	145	199	29440	6.98	1196	257	2672	0.53	1247	441	41216	9.77
44	91	3952	0.94	95	146	2000	0.47	146	200	3264	0.77	1197	258	9280	2.20	1248	442	262144	62.14
45	92	4000	0.75	96	147	4928	1.17	147	201	3104	0.74	1198	259	1968	0.47	1249	443	49640	11.53
46	93	21248	5.04	97	148	9664	2.29	148	202	2080	0.49	1199	261	1020	0.24	1250	444	5440	1.29
47	94	2032	0.48	98	149	2536	0.54	149	203	3040	0.72	1200	264	820	0.19	1251	445	960	0.23
48	95	1168	0.28	99	150	1020	0.24	150	204	13760	3.26	1201	265	3824	0.91				
49	96	2032	0.48	100	151	2016	0.48	151	205	23552	5.58	1202	266	1168	0.28				
50	97	928	0.22	101	152	1248	0.30	152	206	93184	22.09	1203	272	820	0.19				
51	98	14784	3.50	102	153	3216	0.76	153	207	12900	3.03	1204	273	6080	1.44				

OFIPE TUNE CHECK REPORT

Raw Data File: 01488  
 Date: 30-Dec-92  
 Time: 11:38

M/E	ION ABUNDANCE CRITERIA	RELATIVE ABUNDANCE	TUNE
51	30.0 - 60.0% of mass 198	57.52	PASS
68	Less than 2.0% of mass 69	1.03( 1.7)1	PASS
69	Mass 69 relative abundance	61.17	PASS
70	Less than 2.0% of mass 69	0.40( 0.7)1	PASS
127	40.0 - 60.0% of mass 198	57.77	PASS
197	Less than 1% of mass 198	0.24	PASS
198	Base peak. 100% relative abundance	100.00	PASS
199	5 - 9% of mass 198	6.98	PASS
275	10 - 30% of mass 198	18.45	PASS
365	Greater than 1% of mass 198	2.14	PASS
441	Present, but less than mass 443	9.77	PASS
442	Greater than 40% of mass 198	62.14	PASS
443	17 - 23% of mass 442	11.53( 18.6)2	PASS

Triangle Laboratories of RTP, Inc.  
Initial Calibration Curve

139

ICAL File: ICALGJ03 Date of Analysis :01/03/93 Analyte List: PAH

RF20 GL497 RF50 GL496 RF80 GL495  
RF120 GL494 RF160 GL498

Analyte	Flag	RF20	RF50	RF80	RF120	RF160	RFMEAN	%RSD
1,4-Dichlorobenzene-d4	I							
Naphthalene-d8	I							
2-Methylnaphthalene		0.684	0.672	0.714	0.773	0.802	0.729	7.7
Naphthalene		1.028	0.975	1.032	1.109	1.148	1.058	8.6
Acenaphthene-d10	I							
Acenaphthene	C	0.975	0.951	1.015	1.097	1.057	1.019	5.8
Fluorene		1.225	1.176	1.234	1.320	1.310	1.253	4.9
2-Chloronaphthalene		1.033	0.982	1.035	1.114	1.078	1.048	4.8
Acenaphthylene		1.705	1.683	1.766	1.952	1.848	1.791	6.2
Phenanthrene-d10	I							
Phenanthrene		0.976	0.919	0.922	0.987	0.947	0.950	3.2
Anthracene		0.981	0.937	0.940	1.005	0.934	0.959	3.3
Fluoranthene	C	1.143	1.117	1.143	1.214	1.143	1.152	3.2
Chrysene-d12	I							
Chrysene		1.038	0.984	0.975	1.020	1.041	1.011	3.0
Pyrene		1.208	1.189	1.250	1.179	1.057	1.176	6.1
Benzo(a)anthracene		1.052	0.989	1.058	1.072	1.068	1.048	3.2
Perylene-d12	I							
Benzo(b)fluoranthene		1.392	1.436	1.587	1.719	1.740	1.575	10.1
Benzo(k)fluoranthene		1.624	1.727	1.720	1.718	1.733	1.704	2.7
Benzo(e)pyrene		1.378	1.419	1.505	1.560	1.623	1.497	6.7
Benzo(a)pyrene	C	1.286	1.343	1.399	1.505	1.585	1.424	8.5
Perylene		0.756	0.711	0.753	0.766	0.787	0.755	3.7
Indeno(1,2,3-cd)pyrene		0.733	0.877	1.046	1.234	1.396	1.057	25.2
Dibenz(a,h)anthracene		0.770	0.890	1.007	1.217	1.349	1.047	22.6
Benzo(g,h,i)perylene		0.923	1.046	1.193	1.341	1.462	1.193	18.2
=====								
Surrogate	Flag	RF20	RF50	RF80	RF120	RF160	RFMEAN	%RSD
Anthracene-d10	S	0.522	0.508	0.516	0.553	0.537	0.527	3.4
Pyrene-d10	S	1.081	1.081	1.162	1.125	1.065	1.103	3.6

Approved by: J. Lyon Date 1,5,93

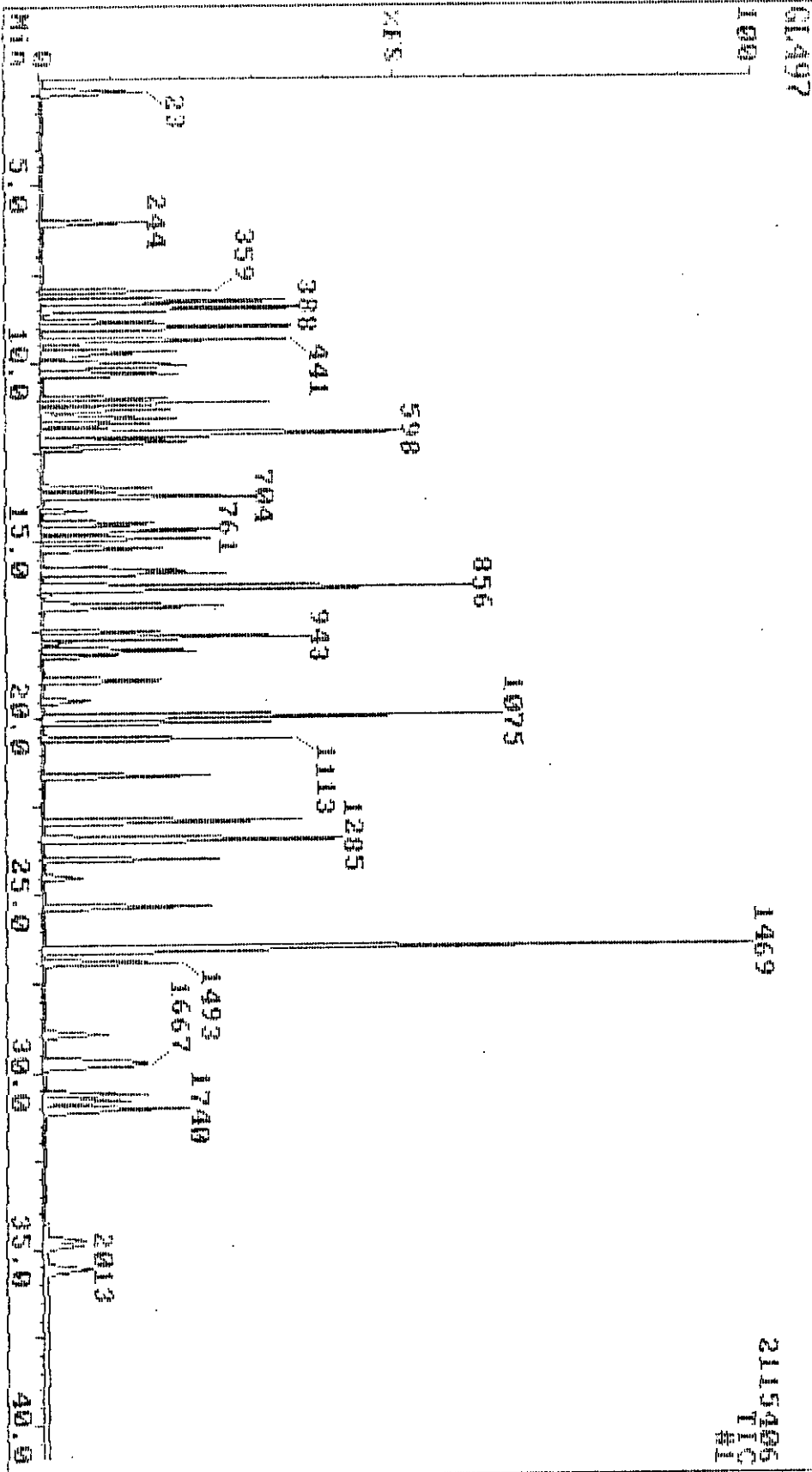
\*- Fails QC Criteria for %RSD; << - Rf less than minimum QC RF; >>- RF greater than maximum QC RF ICAL.EXE v2.5

1/3/93

03-Jan-93 16:59  
Sample: SST1029

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G



no.	RAT	FOR	REV	Delta	Area	P. Flags	Scan	QM	Name
1	100	85	100	-1	270610	bb	419	152	1,4-Dichlorobenzene-d4
2	100	89	93	0	1154300	bb	598	136	Naphthalene-d8
3	100	94	97	0	630640	bb	856	164	Acenaphthene-d10
4	100	92	97	0	1301700	bv	1075	188	Phenanthrene-d10
5	95	68	96	-2	1327100	bb	1469	240	Chrysene-d12
6	99	90	95	1	667600	bb	1739	264	Perylene-d12
7	100	97	97	-1	263320	bb	243	112	2-Fluorophenol
8	90	56	99	-1	235130	bb	387	132	2-Chlorophenol-d4
9	95	64	99	-1	327920	bb	376	99	Phenol-d5
10	100	95	99	0	144290	bb	439	152	1,2-Dichlorobenzene-d4
11	100	84	99	0	306170	bb	497	82	Nitrobenzene-d5
12	98	60	97	0	180130	bb	545	185	1,3,5-Trichlorobenzene-d3
13	100	96	99	0	117180	bb	606	240	1,4-Dibromobenzene-d4
14	100	93	98	0	400560	bb	761	172	2-Fluorobiphenyl
15	100	81	98	0	56244	bb	973	330	2,4,6-Tribromophenol
16	100	93	97	-1	339660	vb	1083	188	Anthracene-d10
17	100	87	96	1	717080	bb	1285	212	Pyrene-d10
18	100	91	97	2	440590	bb	1319	244	Terphenyl-d14
19	100	96	98	0	593060	bb	601	128	Naphthalene
20	100	89	90	0	395050	bb	704	142	2-Methylnaphthalene
21	100	98	98	0	325760	bb	774	162	2-Chloronaphthalene
22	100	96	98	0	537570	bb	834	152	Acenaphthylene
23	100	87	88	0	307360	bb	861	154	Acenaphthene
24	100	97	99	-1	386320	bb	937	166	Fluorene
25	100	96	99	0	48328	bb	1049	266	Pentachlorophenol
26	100	95	97	0	635560	bv*	1079	178	Phenanthrene
27	100	96	99	-1	638590	vb*	1086	178	Anthracene
28	100	97	99	-1	743660	bb	1255	202	Fluoranthene
29	100	96	99	0	801330	bb	1287	202	Pyrene
30	97	79	88	1	697820	bv	1468	228	Benzo(a)anthracene
31	100	91	98	0	688860	vb	1473	228	Chrysene
32	83	65	67	0	464780	bv	1661	252	Benzo(b)fluoranthene
33	100	95	95	-1	542140	vb*	1667	252	Benzo(k)fluoranthene
34	100	97	98	-1	459930	bv	1716	252	Benzo(e)pyrene
35	100	96	96	-2	429150	vv	1727	252	Benzo(a)pyrene
36	100	89	91	0	252270	vb	1745	252	Perylene
37	98	89	94	-2	244740	bv	1964	276	Indeno(1,2,3-cd)pyrene
38	100	86	92	-1	257020	vb	1973	278	Dibenz(a,h)anthracene
39	73	87	94	-5	307970	bb	2013	276	Benzo(g,h,i)perylene

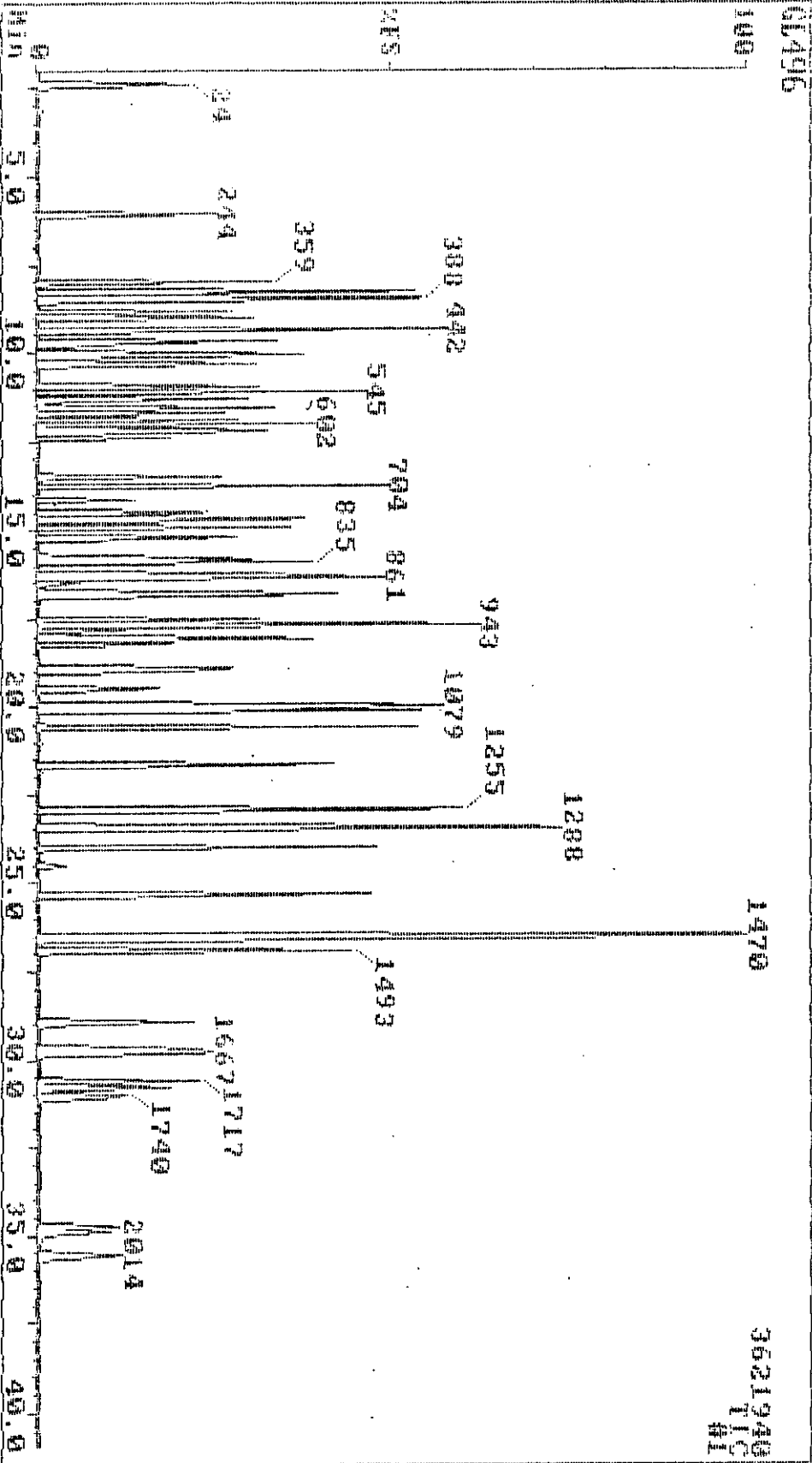


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03-Jan-93 16:10  
Sample: 5810050

Triangle Laboratories of RTP, Inc.

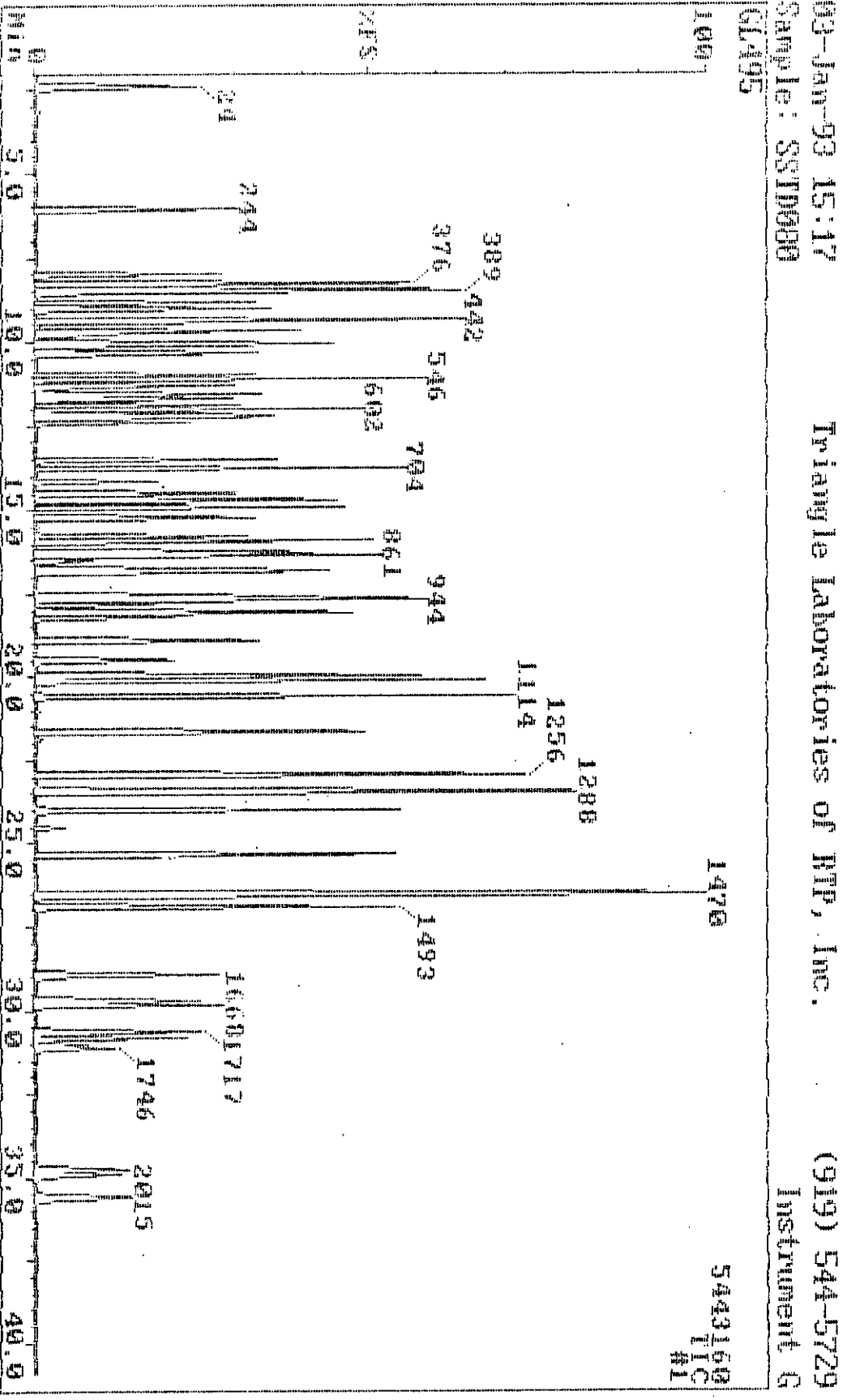
(919) 544-5729  
Instrument: G



3621940  
TIC  
#1

NO.	RAT	FOR	REV	Delta	Area	P. Freqs	Scan	Qm	Name
1	100	85	100	-1	317900	bb	419	152	1,4-Dichlorobenzene-d4
2	100	90	94	0	1300600	bb	598	136	Naphthalene-d8
3	100	93	98	0	716270	bb	856	164	Acenaphthene-d10
4	100	91	97	0	1555900	bv	1075	188	Phenanthrene-d10
5	83	49	94	-1	1542700	bb	1470	240	Chrysene-d12
6	100	89	95	0	671920	bb	1740	264	Perylene-d12
7	100	96	97	0	728240	bb	244	112	2-Fluorophenol
8	93	61	99	0	651270	bb	388	132	2-Chlorophenol-d4
9	94	62	99	-1	894450	bv	376	99	Phenol-d5
10	100	95	99	1	389120	bb	440	152	1,2-Dichlorobenzene-d4
11	100	85	99	0	825660	bb	497	82	Nitrobenzene-d5
12	97	59	99	0	462560	bb	545	185	1,3,5-Trichlorobenzene-d3
13	100	94	99	0	311620	bb	606	240	1,4-Dibromobenzene-d4
14	100	91	98	0	1038800	bb	761	172	2-Fluorobiphenyl
15	100	79	99	0	182360	bb	973	330	2,4,6-Tribromophenol
16	100	84	96	0	987970	vb	1084	188	Anthracene-d10
17	100	88	97	0	2083800	bb	1285	212	Pyrene-d10
18	100	88	97	1	1421800	bb	1319	244	Terphenyl-d14
19	100	97	99	0	1584500	bb	601	128	Naphthalene
20	100	89	91	0	1092900	vb	704	142	2-Methylnaphthalene
21	100	97	99	0	878850	bb	774	162	2-Chloronaphthalene
22	100	95	98	0	1506600	bb	834	152	Acenaphthylene
23	100	88	89	0	851310	vb	861	154	Acenaphthene
24	100	95	98	0	1053000	bb	938	166	Fluorene
25	100	86	99	0	195430	bb	1049	266	Pentachlorophenol
26	100	93	97	0	1788000	bv*	1079	178	Phenanthrene
27	100	94	98	0	1822400	vb*	1087	178	Anthracene
28	100	96	99	-1	2172400	bb	1255	202	Fluoranthene
29	100	95	99	0	2292200	bb	1288	202	Pyrene
30	100	90	99	0	1907600	bv*	1468	228	Benzo(a)anthracene
31	100	94	99	0	1897700	vv	1474	228	Chrysene
32	81	68	71	-1	1206000	bv	1661	252	Benzo(b)fluoranthene
33	100	94	97	-2	1450600	vv	1667	252	Benzo(k)fluoranthene
34	100	96	98	-1	1192100	bv	1717	252	Benzo(e)pyrene
35	96	96	99	-3	1127800	vv	1727	252	Benzo(a)pyrene
36	100	98	99	-1	597010	vb	1745	252	Perylene
37	96	96	99	-3	736640	bv	1964	276	Indeno(1,2,3-cd)pyrene
38	100	94	98	-2	747280	vb	1973	278	Dibenz(a,h)anthracene
39	70	96	99	-6	878350	bv	2013	276	Benzo(g,h,i)perylene

1/3/93



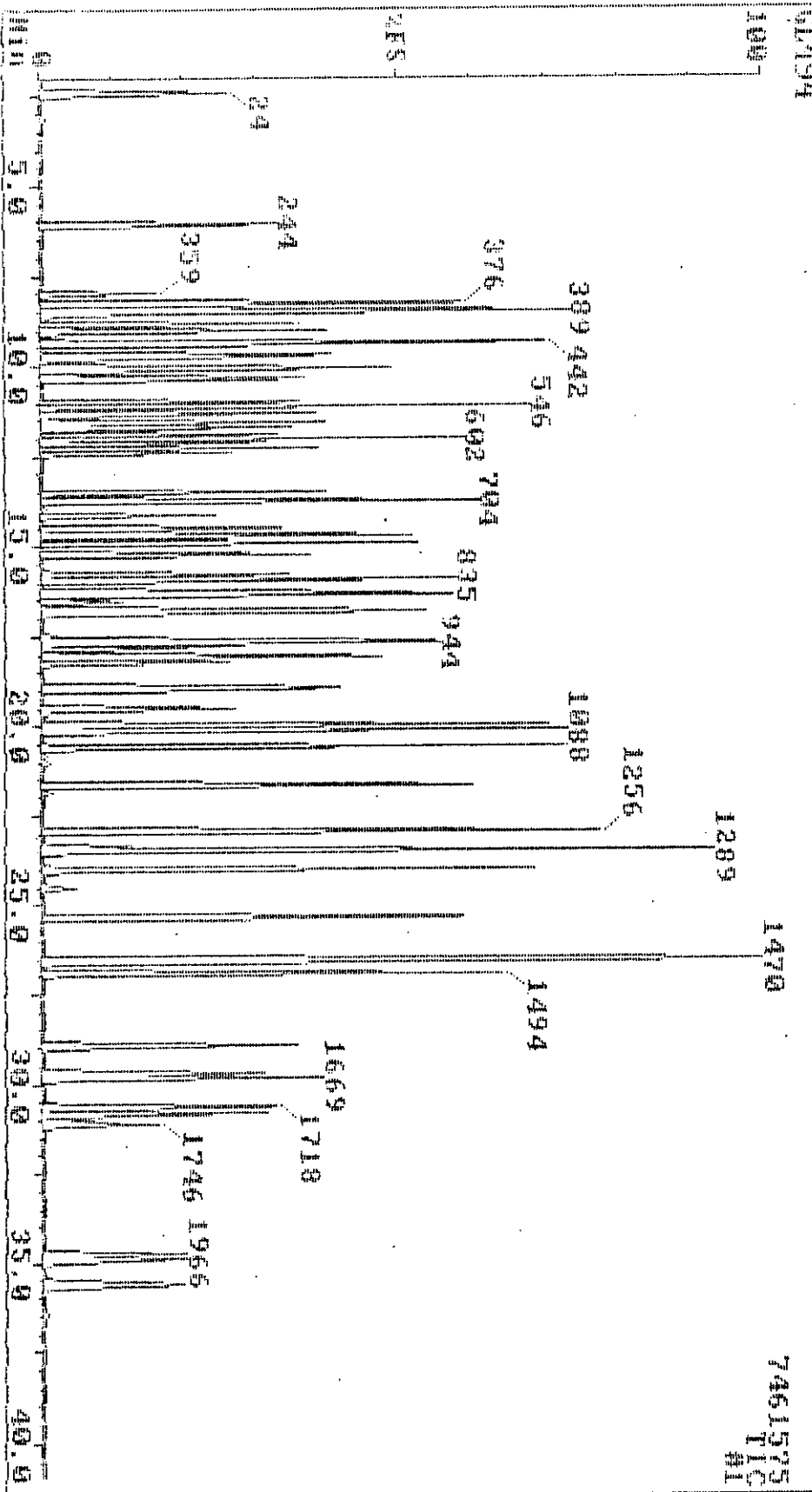
NO.	MAT	FOR	REV	Delta	Area	P. Flags	Scan	Q#	Name
1	100	85	100	0	320770	bb	420	152	1,4-Dichlorobenzene-d4
2	100	87	94	0	1530500	bb	599	136	Naphthalene-d8
3	100	88	97	-1	737180	bb	856	164	Acenaphthene-d10
4	100	87	96	1	1633600	bv	1076	188	Phenanthrene-d10
5	RL	45	94	-2	1549800	bb	1470	240	Chrysene-d12
6	100	87	93	0	663170	bb	1740	264	Perylene-d12
7	100	95	97	-1	1244700	bb	244	112	2-Fluorophenol
8	86	49	99	-1	1124600	bb	388	132	2-Chlorophenol-d4
9	96	66	99	-1	1498300	bv	377	99	Phenol-d5
10	100	86	97	0	677300	bb	440	152	1,2-Dichlorobenzene-d4
11	100	86	99	-1	1412100	bb	497	82	Nitrobenzene-d5
12	97	57	98	0	778180	bb	546	185	1,3,5-Trichlorobenzene-d3
13	100	94	100	-1	531860	bb	606	240	1,4-Dibromobenzene-d4
14	100	90	98	1	1768300	bb	762	172	2-Fluorobiphenyl
15	100	80	100	0	339710	bb	973	330	2,4,6-Tribromophenol
16	100	86	97	-1	1638000	vb	1084	188	Anthracene-d10
17	100	84	97	1	3601800	vb	1286	212	Pyrene-d10
18	100	88	97	1	2551600	bb	1319	244	Terphenyl-d14
19	100	96	98	0	2756600	bb	602	128	Naphthalene
20	100	89	92	-1	1906600	vb	704	142	2-Methylnaphthalene
21	100	95	98	1	1527100	bb	775	162	2-Chloronaphthalene
22	100	94	97	1	2606600	bb	835	152	Acenaphthylene
23	100	88	90	0	1498300	bb	861	154	Acenaphthene
24	100	95	98	0	1821500	bb	938	166	Fluorene
25	100	86	99	-1	389840	bv	1049	266	Pentachlorophenol
26	100	93	98	-1	3015800	bv*	1079	178	Phenanthrene
27	100	93	98	-1	3075000	vb	1087	178	Anthracene
28	100	95	98	-1	3740300	bb	1256	202	Fluoranthene
29	100	93	98	1	3874800	bb	1289	202	Pyrene
30	100	85	98	1	3278900	bv*	1469	228	Benzo(a)anthracene
31	100	93	99	0	3021200	vv	1474	228	Chrysene
32	88	68	72	0	2105500	bv	1662	252	Benzo(b)fluoranthene
33	100	93	97	-1	2280600	vv	1668	252	Benzo(k)fluoranthene
34	100	95	98	-1	1996400	bv	1717	252	Benzo(e)pyrene
35	100	96	99	-2	1856100	vv	1728	252	Benzo(a)pyrene
36	100	97	99	0	999390	vv	1746	252	Perylene
37	100	96	100	-2	1387200	bv	1965	276	Indeno(1,2,3-cd)pyrene
38	100	93	99	-2	1336200	vv	1973	278	0ibenz(a,h)anthracene
39	87	96	99	-4	1582100	bv	2015	276	Benzo(g,h,i)perylene

~ 1/3/93

88-Jan-93 14:13  
Sample: SST0120

Triangle Laboratories of RTI, Inc.

(919) 544-5729  
Instrument G



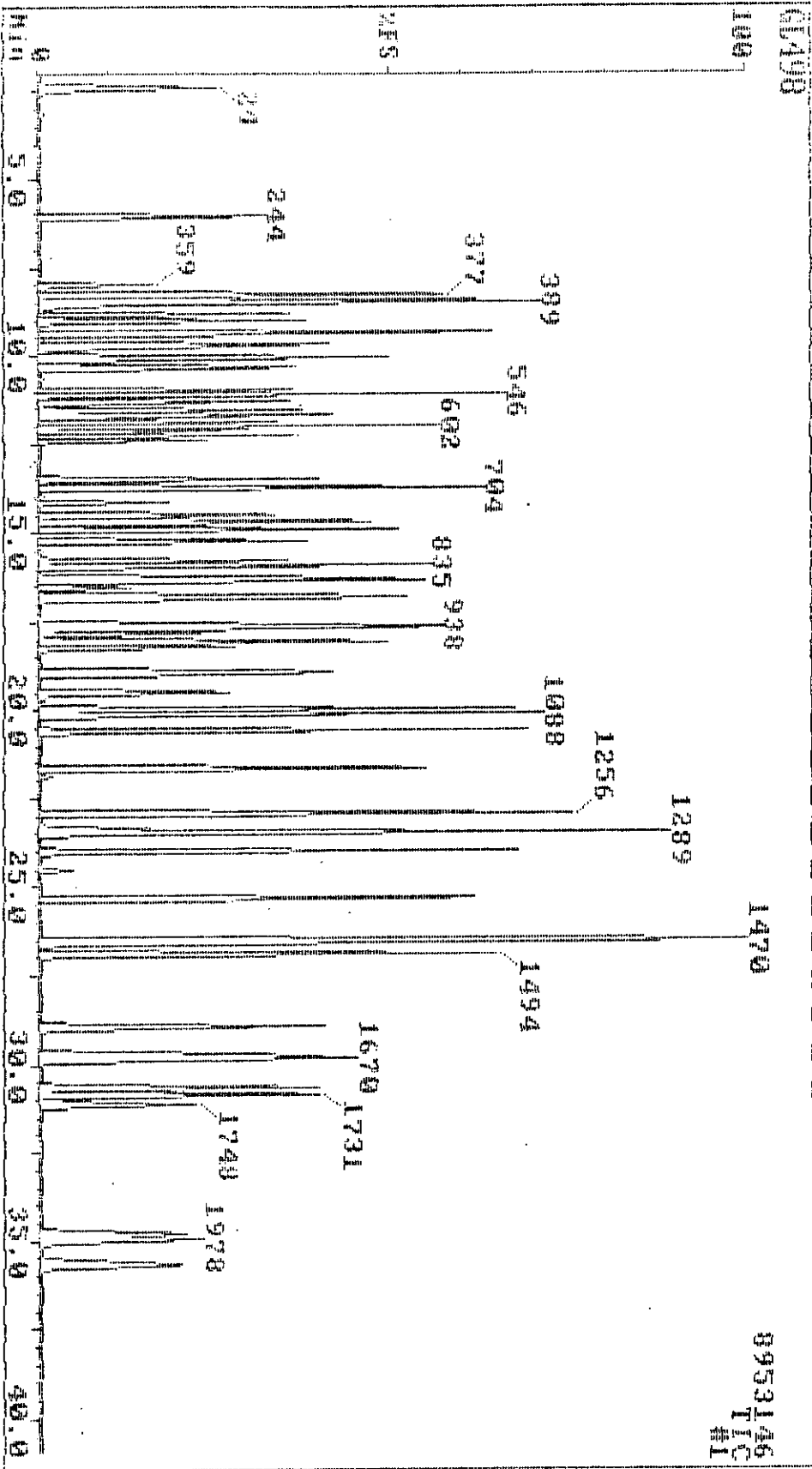
NO.	MAT	FOR	REV	Delta	Area	P.Flags	Scan	Q#	Name
1	100	83	100	0	312450	bb	420	152	1,4-Dichlorobenzene-d4
2	100	86	94	0	1536500	bb	599	156	Naphthalene-d8
3	100	90	97	0	703760	bb	857	164	Acenaphthene-d10
4	100	85	96	0	1512300	bv	1076	188	Phenanthrene-d10
5	73	32	94	-1	1559600	bb	1471	240	Chrysene-d12
6	100	86	95	0	776940	bb	1741	264	Perylene-d12
7	100	95	97	-1	1967600	bv	244	112	2-Fluorophenol
8	89	54	99	-1	1814700	bb	388	132	2-Chlorophenol-d4
9	95	65	99	-1	2375600	bv	377	99	Phenol-d5
10	100	87	98	0	1073100	bb	440	152	1,2-Dichlorobenzene-d4
11	100	81	99	0	2239200	bb	498	82	Nitrobenzene-d5
12	96	55	98	0	1177200	bb	546	185	1,3,5-Trichlorobenzene-d3
13	100	92	99	0	858880	bb	607	240	1,4-Dibromobenzene-d4
14	100	89	98	0	2656800	bb	762	172	2-Fluorobiphenyl
15	100	77	99	0	544160	bb	974	330	2,4,6-Tribromophenol
16	100	86	97	0	2510600	vb	1085	188	Anthracene-d10
17	100	86	97	0	5262000	vb	1286	212	Pyrene-d10
18	100	85	96	1	3952700	vb	1320	244	Terphenyl-d14
19	100	96	98	0	4445700	bb	602	128	Naphthalene
20	100	89	92	-1	3098300	vb	704	142	2-Methylnaphthalene
21	100	95	98	0	2351600	bb	775	162	2-Chloronaphthalene
22	100	94	97	0	4120900	bb	835	152	Acenaphthylene
23	100	88	90	0	2516000	bb	862	154	Acenaphthene
24	100	95	98	-1	2786400	bb	938	166	Fluorene
25	100	83	99	0	637220	bv	1050	266	Pentachlorophenol
26	100	92	97	0	4475700	bv*	1080	178	Phenanthrene
27	100	93	97	0	4558200	vv*	1088	178	Anthracene
28	100	94	98	-1	5509800	bb	1256	202	Fluoranthene
29	100	94	99	0	5514500	vb	1289	202	Pyrene
30	100	88	99	0	5017300	bv	1469	228	Benzo(a)anthracene
31	100	93	99	0	4770100	vv	1475	228	Chrysene
32	88	68	72	0	4006500	bv	1663	252	Benzo(b)fluoranthene
33	100	93	97	-1	4003400	vv	1669	252	Benzo(k)fluoranthene
34	100	94	98	-1	3635900	bv	1718	252	Benzo(e)pyrene
35	100	95	99	-2	3508900	vv	1729	252	Benzo(a)pyrene
36	100	95	99	-1	1785900	vv	1746	252	Perylene
37	100	96	100	-2	2875900	bv	1966	276	Indeno(1,2,3-cd)pyrene
38	100	92	99	-2	2837300	bv	1974	278	Dibenz(a,h)anthracene
39	87	96	99	-4	3126000	b? <sup>90-93</sup>	2016	276	Benzo(g,h,i)perylene

1/3/73

63-Jan-93 10:00  
Sample: S810100

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument: G



No.	HAT	FOR	REV	Delta	Area	P.Flags	Scan	GM	Name
1	100	80	100	-1	202340	bb	419	152	1,4-Dichlorobenzene-d4
2	100	80	93	1	1093400	bb	597	138	Naphthalene-d8
3	100	86	90	-1	643100	bb	856	164	Acenaphthene-d10
4	100	82	96	1	1458000	bv	1076	188	Phenanthrene-d10
5	67	24	92	-1	1546600	bb	1471	240	Chrysene-d12
6	100	86	94	1	875380	bb	1742	264	Perylene-d12
7	100	95	97	0	2240900	bb	244	112	2-Fluorophenol
8	94	52	98	0	1995900	bb	388	132	2-Chlorophenol-d4
9	100	61	99	0	2784000	bv	377	99	Phenol-d5
10	100	84	96	1	1187750	bb	440	152	1,2-Dichlorobenzene-d4
11	100	79	99	0	2622900	bb	498	82	Nitrobenzene-d5
12	95	54	98	0	1440000	bb	546	188	1,3,5-Trichlorobenzene-d3
13	100	94	99	0	937220	bb	606	240	1,4-Dibromobenzene-d4
14	100	89	98	1	3225400	bb	762	172	2-Fluorobiphenyl
15	100	76	98	1	632330	bb	974	330	2,4,6-Tribromophenol
16	100	85	97	-1	3129800	vb	1084	188	Anthracene-d10
17	100	85	96	0	6587000	vb	1286	212	Pyrene-d10
18	100	85	96	1	4753100	vb	1320	244	Terphenyl-d14
19	100	96	98	0	5023000	bb	602	128	Naphthalene
20	100	89	92	-1	3509500	vb	704	142	2-Methylnaphthalene
21	100	95	98	1	2773900	bb	775	162	2-Chloronaphthalene
22	100	93	97	1	4754400	bb	835	152	Acenaphthylene
23	100	88	90	0	2718200	bb	861	154	Acenaphthene
24	100	94	98	0	3370400	bb	938	166	Fluorene
25	100	84	99	-1	763020	bv	1049	266	Pentachlorophenol
26	100	91	97	0	5521400	bv*	1080	178	Phenanthrene
27	100	92	97	0	5447000	vb*	1088	178	Anthracene
28	100	94	98	-1	6663900	vv	1256	202	Fluoranthene
29	100	93	98	0	6540600	vv	1289	202	Pyrene
30	100	89	99	0	6604700	bv	1469	228	Benzo(a)anthracene
31	100	92	98	1	6439600	vv	1476	228	Chrysene
32	86	67	71	0	6094000	b!	1664	252	Benzo(b)fluoranthene
33	100	92	97	-1	6066800	vv	1670	252	Benzo(k)fluoranthene
34	100	93	98	0	5683500	bv	1720	252	Benzo(e)pyrene
35	100	94	99	-1	5551300	vv	1731	252	Benzo(a)pyrene
36	100	94	97	0	2755500	vv	1748	252	Perylene
37	100	95	99	0	4887900	bv	1969	276	Indeno(1,2,3-cd)pyrene
38	100	92	99	1	4723700	bb	1978	278	Dibenz(a,h)anthracene
39	100	96	99	0	5120900	bv	2021	276	Benzo(g,h,i)perylene

11/93



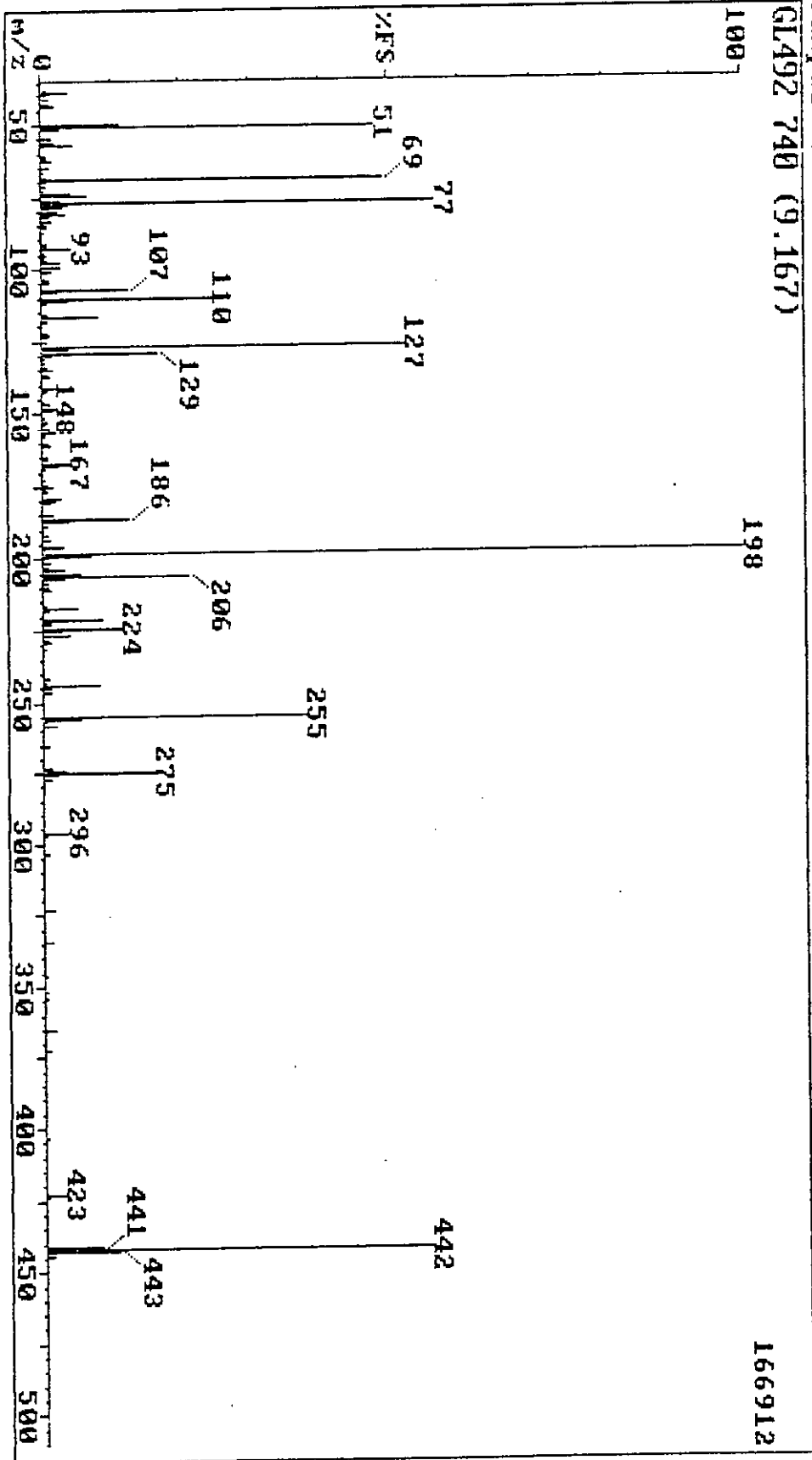
03-Jan-93 12:23  
Sample: DFTPP

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G

GL492 740 (9.167)

166912



Raw Data File: 61490  
 Date: 88-Jan-98  
 Time: 10:28

M/E	ION ABUNDANCE CRITERIA	RELATIVE ABUNDANCE	TUNE
51	30.0 - 60.0% of mass 198	47.85	PASS
68	Less than 2.0% of mass 69	0.62( 1.3)1	PASS
69	Mass 69 relative abundance	49.08	PASS
70	Less than 2.0% of mass 69	0.63( 1.4)1	PASS
127	40.0 - 60.0% of mass 198	52.15	PASS
197	Less than 1% of mass 198	0.42	PASS
198	Base peak, 100% relative abundance	100.00	PASS
199	5 - 9% of mass 198	7.02	PASS
275	10 - 30% of mass 198	15.80	PASS
365	Greater than 1% of mass 198	1.56	PASS
441	Present, but less than mass 443	8.24	PASS
442	Greater than 40% of mass 198	55.21	PASS
443	17 - 23% of mass 442	10.43( 18.9)2	PASS

PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int
28	1088	0.55	1	34	95	1534	0.73	67	170	684	0.41	100	181	1664	1.00	113	242	1104	0.66
29	6400	3.33	3	35	86	1511	0.77	68	134	992	0.59	101	185	2304	1.38	114	243	940	0.56
3	40	1040	0.62	36	37	786	0.47	69	135	2320	1.39	102	186	20992	12.58	115	244	13563	8.13
4	41	1852	1.17	37	91	1434	0.85	70	136	1120	0.67	103	187	6208	3.72	116	245	1920	1.19
5	43	2150	1.29	38	92	1376	0.82	71	137	1648	0.99	104	189	954	0.57	117	246	2240	1.34
6	44	3120	1.87	39	93	6976	4.19	72	141	3312	1.98	105	192	1446	0.86	118	245	62976	37.73
7	50	18683	11.20	40	94	304	0.48	73	142	1456	0.87	106	193	1728	1.04	119	246	9152	5.48
8	51	79972	47.93	41	95	1000	0.60	74	143	332	0.50	107	196	4928	2.95	120	257	808	0.48
9	52	4416	2.65	42	96	792	0.47	75	146	728	0.44	108	197	704	0.42	121	258	3152	1.99
10	55	2560	1.53	43	97	1040	0.62	76	147	1952	1.17	109	198	166912	100.00	122	263	1216	0.73
11	56	3152	1.89	44	98	4844	2.91	77	148	3472	2.08	110	199	11712	7.02	123	273	2096	1.26
12	57	7680	4.60	45	99	4736	2.84	78	149	2768	1.66	111	200	1360	0.81	124	274	4928	2.95
13	61	1056	0.63	46	101	2532	1.55	79	151	680	0.41	112	201	1840	1.10	125	275	26368	15.90
14	62	1104	0.66	47	103	904	0.54	80	153	1072	0.64	113	203	1184	0.71	126	276	5424	2.95
15	63	2832	1.70	48	104	1648	0.99	81	154	908	0.54	114	204	5056	3.03	127	277	2016	1.21
16	65	2096	1.26	49	105	1303	1.08	82	155	1272	1.12	115	205	9344	5.60	128	296	5760	3.45
17	67	364	0.52	50	107	20992	12.58	83	156	3120	1.87	116	206	35328	21.17	129	297	860	0.52
18	68	1040	0.62	51	108	3616	2.17	84	157	320	0.49	117	207	4992	2.99	130	303	976	0.58
19	69	31920	19.08	52	110	40960	24.54	85	158	736	0.44	118	208	1376	0.82	131	323	2416	1.45
20	70	1136	0.68	53	111	6528	3.91	86	160	1136	0.68	119	210	1232	0.74	132	334	1656	1.02
21	71	1296	0.78	54	112	1040	0.62	87	161	1712	1.03	120	211	2160	1.29	133	346	692	0.41
22	73	912	0.55	55	116	1200	0.72	88	163	1232	0.74	121	216	788	0.47	134	352	800	0.48
23	74	7232	4.33	56	117	13504	8.09	89	166	1040	0.62	122	217	8256	4.95	135	354	944	0.57
24	75	11328	6.79	57	118	1280	0.77	90	167	6720	4.03	123	218	1312	0.79	136	363	2608	1.56
25	76	4224	2.53	58	122	1568	0.94	91	168	4016	2.41	124	221	14208	8.51	137	372	1296	0.75
26	77	94208	56.44	59	123	2256	1.35	92	169	704	0.42	125	222	2160	1.29	138	403	736	0.44
27	78	6592	3.95	60	124	1120	0.67	93	173	620	0.49	126	223	2272	1.36	139	423	4800	2.98
28	79	4992	2.99	61	125	1168	0.70	94	174	1408	0.84	127	224	18688	11.20	140	424	916	0.55
29	80	3840	2.30	62	127	37040	22.15	95	175	2560	1.53	128	225	4672	2.80	141	441	13760	8.24
30	81	6030	3.64	63	128	6592	3.95	96	176	936	0.56	129	227	6336	3.80	142	442	92160	55.21
31	82	2000	1.20	64	129	27648	16.56	97	177	1136	0.68	130	223	1024	0.61	143	443	17408	10.43
32	83	2624	1.57	65	130	2576	1.54	98	179	4288	2.57	131	229	1664	1.00	144	444	1808	1.02
33	84	716	0.43	66	131	768	0.58	99	180	3472	2.08	132	231	876	0.52				

Triangle Laboratories of RTP, Inc.  
Continuing Calibration Curve

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CCAL File: GL500 Date of Analysis :01/03/93 Analyte List: PAH  
ICAL File: ICALGJ03

Analyte	Flag	RF50	RFMEAN	%D
1,4-Dichlorobenzene-d4	I			
Naphthalene-d8	I			
2-Methylnaphthalene		0.679	0.729	6.9
Naphthalene		1.001	1.058	5.4
Acenaphthene-d10	I			
Acenaphthene	C	0.957	1.019	6.1
Fluorene		1.180	1.253	5.8
2-Chloronaphthalene		0.971	1.048	7.3
Acenaphthylene		1.680	1.791	6.2
Phenanthrene-d10	I			
Phenanthrene		0.921	0.950	3.1
Anthracene		0.944	0.959	1.6
Fluoranthene	C	1.115	1.152	3.2
Chrysene-d12	I			
Chrysene		0.995	1.011	1.6
Pyrene		1.167	1.176	0.8
Benzo(a)anthracene		0.978	1.048	6.7
Perylene-d12	I			
Benzo(b)fluoranthene		1.380	1.575	12.4
Benzo(k)fluoranthene		1.785	1.704	-4.8
Benzo(e)pyrene		1.423	1.497	4.9
Benzo(a)pyrene	C	1.321	1.424	7.2
Perylene		0.688	0.755	8.9
Indeno(1,2,3-cd)pyrene		0.876	1.057	17.1
Dibenz(a,h)anthracene		0.875	1.047	16.4
Benzo(g,h,i)perylene		1.068	1.193	10.5
=====				
Surrogate	Flag	RF50	RFMEAN	%D
Anthracene-d10	S	0.508	0.527	3.6
Pyrene-d10	S	1.066	1.103	3.4

Approved by: J. Lyon Date 1/5/93

\*- Fails QC Criteria for %D; << - Rf less then minimum QC RF; >>- RF greater than maximum QC RF

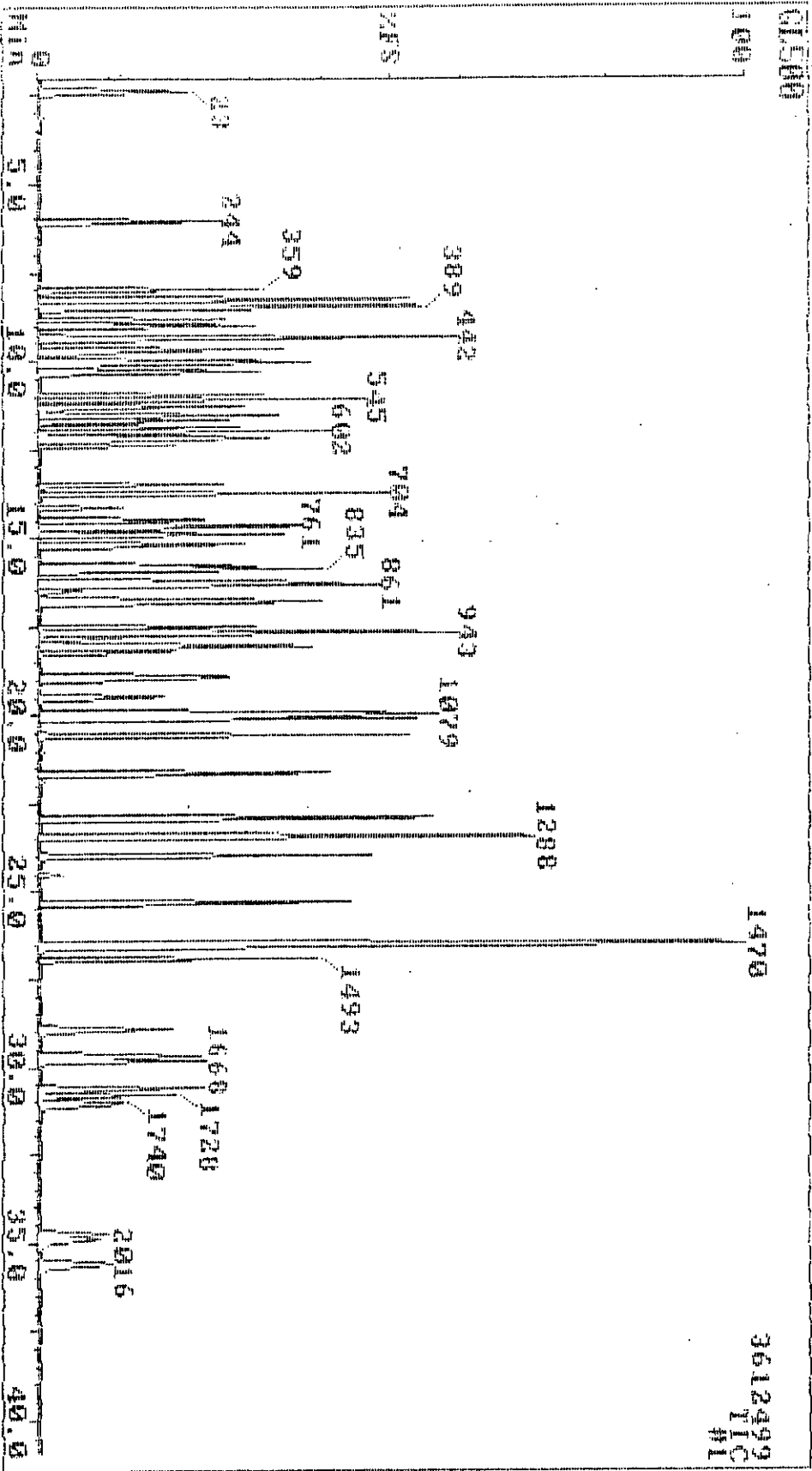
CCAL.EXE v2.5

1/3/97

10-Jan-93 19:23  
Sample: S810M50  
015M

Triangle Laboratories of RTP, Inc.

(919) 544-5729  
Instrument G



3612499  
TIC  
#1

No.	MAT	FOR	REV	Delta	Area	P. Flags	Scan	Qn	Name
1	100	85	100	-1	505790	bb	419	152	1,4-Dichlorobenzene-d4
2	100	86	93	1	1267900	bb	599	136	Naphthalene-d8
3	100	93	98	-1	712780	bb	858	164	Acenaphthene-d10
4	100	91	96	1	1491100	bv	1076	188	Phenanthrene-d10
5	78	49	96	-2	1498800	bb	1470	240	Chrysene-d12
6	100	89	93	0	672400	bb	1740	264	Perylene-d12
7	100	96	97	0	718060	bb	244	112	2-Fluorophenol
8	93	61	99	0	639450	bb	388	132	2-Chlorophenol-d4
9	94	62	99	-1	882900	bv	376	99	Phenol-d5
10	100	95	99	1	377340	bb	440	152	1,2-Dichlorobenzene-d4
11	100	85	99	-1	822920	bb	497	82	Nitrobenzene-d5
12	91	58	99	-1	454030	bb	545	185	1,3,5-Trichlorobenzene-d3
13	100	94	99	0	310990	bb	606	240	1,4-Dibromobenzene-d4
14	100	91	98	0	1025600	bb	761	172	2-Fluorobiphenyl
15	100	80	99	0	185340	bb	973	330	2,4,6-Tribromophenol
16	100	84	96	-1	947080	vb	1084	188	Anthracene-d10
17	100	88	97	0	1997200	bb	1285	212	Pyrene-d10
18	100	88	97	1	1361400	bb	1319	244	Terphenyl-d14
19	100	97	98	0	1610700	bb	602	128	Naphthalene
20	100	89	91	-1	1092700	vb	704	142	2-Methylnaphthalene
21	100	97	99	0	864960	bb	774	162	2-Chloronaphthalene
22	100	94	97	1	1496600	bb	835	152	Acenaphthylene
23	100	88	90	0	852700	vb	861	154	Acenaphthene
24	100	90	98	0	1051000	bb	938	166	Fluorene
25	100	85	99	-1	202210	bb	1049	266	Pentachlorophenol
26	100	93	97	-1	1716600	bv*	1079	178	Phenanthrene
27	100	94	98	-1	1759100	vb	1087	178	Anthracene
28	100	96	99	-2	2078800	bb	1255	202	Fluoranthene
29	100	95	99	0	2185800	bb	1288	202	Pyrene
30	100	90	99	1	1832600	bv*	1469	228	Benzo(a)anthracene
31	100	93	99	0	1865000	vv	1474	228	Chrysene
32	86	67	71	0	1159500	bv	1662	252	Benzo(b)fluoranthene
33	100	94	97	-2	1500100	vb*	1667	252	Benzo(k)fluoranthene
34	100	95	98	-1	1195800	bv	1717	252	Benzo(e)pyrene
35	100	96	99	-2	1110400	vv	1728	252	Benzo(a)pyrene
36	100	98	99	-1	578120	vb	1745	252	Perylene
37	100	97	100	-1	736080	bv	1966	276	Indeno(1,2,3-cd)pyrene
38	100	94	97	-1	735290	bv	1974	278	Dibenz(a,h)anthracene
39	96	96	99	-3	897850	bv	2016	276	Benzo(g,h,i)perylene

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03-Jan-93 18:54

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(919) 544-5729

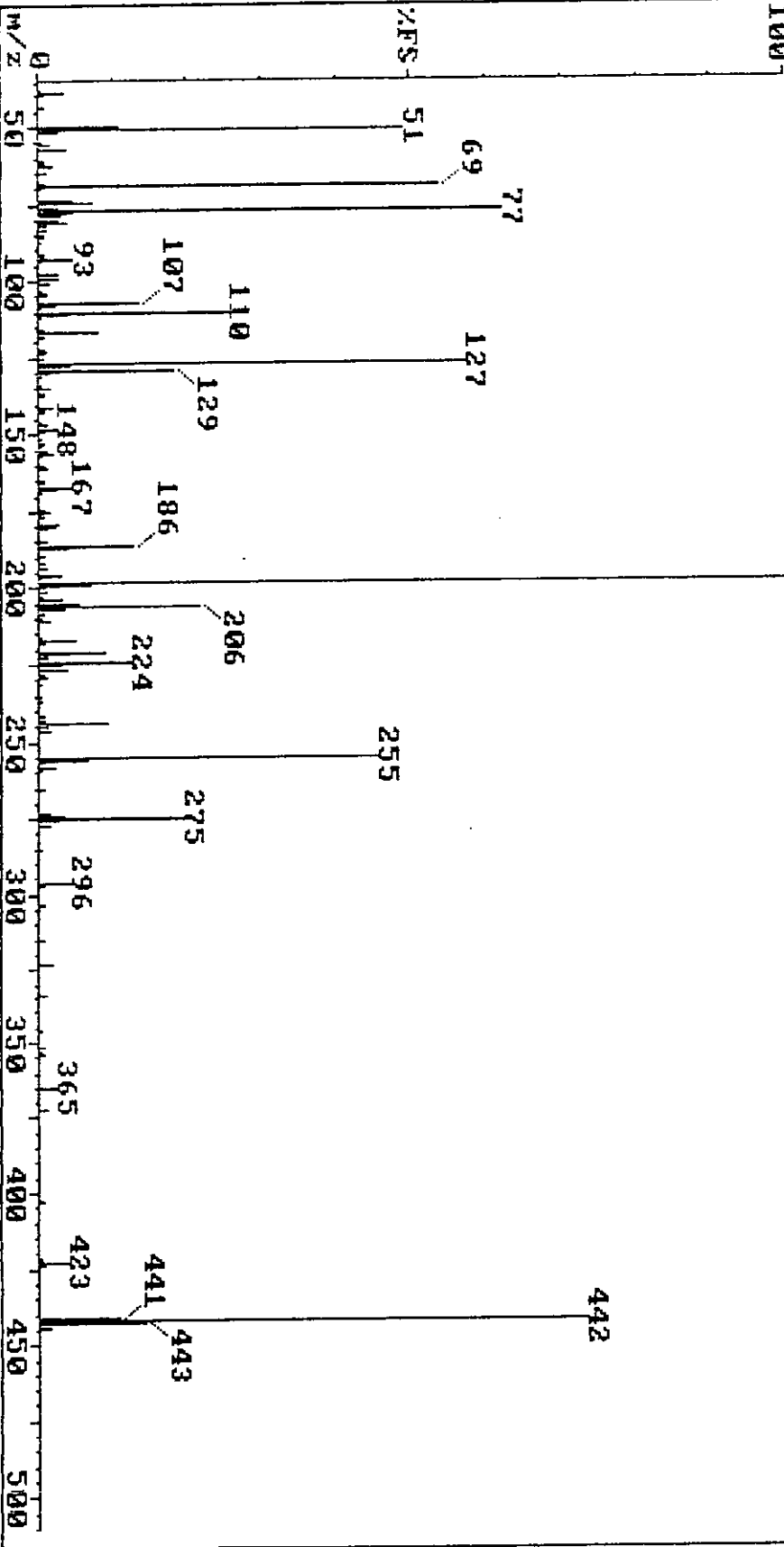
Sample: DFTPP

Instrument G

GL499 737 (9.142)

198

152576



PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int	PK#	Mass	Abs Int	Rel Int
1	38	5194	3.40	35	72	4416	2.89	58	148	3360	2.20	101	201	1820	1.05	114	265	1392	0.91
3	40	922	0.51	36	79	4288	2.81	59	149	700	0.59	102	203	740	0.49	115	273	2320	1.52
4	44	1056	0.69	37	101	2560	1.68	70	151	692	0.45	103	204	4864	2.14	116	274	5672	3.59
5	50	16640	10.71	38	107	864	0.57	71	153	958	0.53	104	205	8576	5.02	117	275	29952	19.63
6	51	74752	48.99	39	104	1584	1.04	72	154	828	0.54	105	206	33280	21.81	118	276	4080	2.67
7	52	4160	2.73	40	105	1504	0.99	73	155	1356	1.22	106	207	5056	3.31	119	277	2352	1.54
8	55	840	0.55	41	107	20992	13.76	74	156	3088	2.02	107	208	1296	0.85	140	285	688	0.45
9	56	2454	1.41	42	108	3360	2.20	75	157	712	0.47	108	210	724	0.47	141	286	6784	4.45
10	57	5696	3.73	43	109	648	0.42	76	160	904	0.59	109	211	2096	1.37	142	297	1104	0.72
11	61	956	0.63	44	110	59168	25.67	77	161	1596	1.11	110	216	680	0.45	143	303	1040	0.68
12	62	1016	0.67	45	111	5824	3.82	78	165	1168	0.77	111	217	7808	5.10	144	315	904	0.59
13	63	2752	1.80	46	112	336	0.55	79	166	964	0.63	112	218	1248	0.82	145	323	2976	1.95
14	65	1872	1.23	47	116	1200	0.79	80	167	6464	4.24	113	221	13388	9.10	146	334	1872	1.23
15	68	1088	0.71	48	117	12608	8.26	81	168	3760	2.46	114	222	1920	1.21	147	346	796	0.52
16	69	81920	53.69	49	118	1312	0.86	82	169	648	0.42	115	223	2064	1.35	148	352	1040	0.68
17	70	768	0.50	50	122	1328	0.87	83	174	1136	0.74	116	224	18744	12.42	149	353	708	0.46
18	74	7104	4.66	51	123	1984	1.30	84	175	2464	1.61	117	225	4800	3.15	150	354	1104	0.72
19	75	11456	7.51	52	124	996	0.65	85	176	836	0.55	118	227	6208	4.07	151	365	3376	2.21
20	76	4160	2.73	53	125	1004	0.66	86	177	1120	0.73	119	228	960	0.58	152	372	1696	1.11
21	77	95232	62.42	54	127	87040	57.05	87	179	3920	2.57	120	229	1712	1.12	153	402	640	0.42
22	78	7168	4.70	55	128	6464	4.24	88	180	3360	2.20	121	231	912	0.53	154	403	896	0.59
23	79	4928	3.23	56	129	27904	18.29	89	181	1616	1.06	122	235	676	0.44	155	421	772	0.51
24	80	3904	2.56	57	130	2592	1.70	90	185	2032	1.35	123	237	692	0.45	156	422	780	0.51
25	81	5696	3.73	58	131	688	0.45	91	186	19712	12.72	124	242	1088	0.71	157	423	5952	3.90
26	82	1744	1.14	59	134	856	0.56	92	187	5760	3.78	125	245	956	0.63	158	424	1264	0.83
27	83	1936	1.27	60	135	2336	1.53	93	189	948	0.62	126	244	14144	9.27	159	441	16384	10.74
28	85	1168	0.77	61	136	988	0.65	94	192	1392	0.91	127	245	2000	1.31	160	442	111616	73.15
29	86	1328	0.87	62	137	1472	0.96	95	193	1584	1.04	128	246	2240	1.47	161	443	21760	14.26
30	87	764	0.51	63	141	3072	2.01	96	196	4544	2.98	129	255	69332	45.64	162	444	2400	1.57
31	91	1152	0.76	64	142	1200	0.79	97	197	734	0.51	130	256	10176	6.67				
32	92	1200	0.79	65	143	900	0.59	98	198	152576	100.00	131	257	940	0.62				
33	93	7040	4.61	66	146	724	0.47	99	199	10888	7.01	132	258	3328	2.18				



CFIAPP TUNE CHECK REPORT

Raw Data File: 31499  
 Date: 05-Jan-93  
 Time: 18:54

M/E	ION ABUNDANCE CRITERIA	RELATIVE ABUNDANCE	TUNE
51	30.0 - 60.0% of mass 198	48.99	PASS
68	Less than 2.0% of mass 69	0.71( 1.3)1	PASS
69	Mass 69 relative abundance	53.69	PASS
70	Less than 2.0% of mass 69	0.50( 0.9)1	PASS
127	40.0 - 60.0% of mass 198	57.05	PASS
197	Less than 1% of mass 198	0.51	PASS
198	Base peak, 100% relative abundance	100.00	PASS
199	5 - 9% of mass 198	7.01	PASS
275	10 - 30% of mass 198	19.63	PASS
365	Greater than 1% of mass 198	2.21	PASS
441	Present, but less than mass 442	10.74	PASS
442	Greater than 40% of mass 198	73.15	PASS
443	17 - 23% of mass 442	14.26( 19.5)2	PASS

**VII. LABORATORY ANALYSIS RESULTS**

**C. Particulate Analysis Results**

## SAMPLE ANALYTICAL DATA FORM

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Company Name MC ASPHALT NAPA METH. 202 DW  
 Sample Location MELBORNE, FL Relative Humidity in Lab 42 %  
 Blank Volume ( $V_a$ ) 100 ml Density of Acetone ( $\rho_a$ ) .7857 mg/ml  
 Date/Time wt. blank 12/17 4:00P Gross wt. 99.1794 g  
 Date/Time wt. blank 12/21 8:30A Gross wt. 99.1793 g  
 Ave. Gross wt. 99.1794 g  
 Tare wt. 99.1792 g  
 Weight of blank ( $m_{ab}$ ) .0002 g

Acetone blank residue concentration ( $C_a$ ): ( $C_a$ ) = ( $m_{ab}$ ) / ( $V_a$ ) ( $\rho_a$ ) = (.000003 mg/g)

Acetone Blank Wt.:  $W_a = C_a V_{aw} \rho_a = (.000003)(300)(.7857) = (.0007$  g)

	Run # 1	Run # 2	Run # 3
Acetone rinse volume ( $V_{aw}$ ) ml	300	300	300
Date/Time of wt. <u>12/17 4:00P</u> Gross wt. g	96.7948	98.5074	107.2859
Date/Time of wt. <u>12/21 8:30A</u> Gross wt. g	96.7952	98.5079	107.2864
Average Gross wt. g	96.7950	98.5077	107.2862
Tare wt. g	96.7618	98.4438	107.1989
Less Acetone blank wt. ( $W_a$ ) g	.0007	.0007	.0007
Weight of particulate in acetone rinse ( $m_a$ ) g	.0325	.0632	.0866

Filter Numbers #	TS00018	TS6575	TS00025
Date/Time of wt. <u>12/17 4:00P</u> Gross wt. g	.6881	.6600	.6753
Date/Time of wt. <u>12/21 8:30A</u> Gross wt. g	.6876	.6603	.6750
Average Gross wt. g	.6879	.6602	.6752
Tare wt. g	.5713	.5716	.5735

Weight of particulate on filter ( $m_f$ ) g	.1166	.0886	.1017
Weight of particulate in acetone rinse ( $m_a$ ) g	.0325	.0632	.0866
Total weight of particulate ( $m_n$ ) g	.1491	.1318	.1883

NOTE: In no case should a blank residue greater than 0.01 mg/g (or 0.001% of the blank weight) be subtracted from the sample weight.

Remarks:

Signature of Analyst Thomas SouthSignature of Reviewer [Signature]

COMPANY NAME: MAC ASPHALT MELBORNE, FL  
 Methylene Chloride Extraction for EPA Method 202

Relative humidity in lab 42 %  
 Density of Methylene Chloride 1.3255 g/ml

Methylene Chloride rinse volume ml

Volume of Solution

Date/time of wt 12/22 10:00A

Date/time of wt 12/22 4:00P

Less Methylene Chloride Blank

Wt./particulate: Methylene Chloride rinse

Water evaporation

Date/time of wt 12/21 9:00A

Date/time of wt 12/22 10:00A

Less H<sub>2</sub>O blank wt.

Weight of particulate from water (m<sub>w</sub>)

Wt./particulate: Methylene Chloride rinse

Total weight of particulate (m<sub>T</sub>)

	RUN 1	RUN 2	RUN 3
Methylene Chloride rinse volume ml	330	300	300
Volume of Solution	700	600	600
Gross wt. g	165.4784	162.1471	167.4280
Gross wt. g	165.4780	162.1469	167.4278
Avg. Gross wt. g	165.4782	162.1470	167.4279
Tare wt. g	165.4339	162.1190	167.4035
Less Methylene Chloride Blank	.0001	.0001	.0001
Wt./particulate: Methylene Chloride rinse	.0442	.0279	.0243
Water evaporation			
Gross wt. g	164.2958	164.0520	171.8910
Gross wt. g	164.2955	164.0525	171.8909
Avg. Gross wt. g	164.2957	164.0523	171.8910
Tare wt. g	164.2380	164.0360	171.8230
Less H <sub>2</sub> O blank wt.	.0002	.0002	.0002
Weight of particulate from water (m <sub>w</sub> )	.0575	.0161	.0678
Wt./particulate: Methylene Chloride rinse	.0442	.0279	.0243
Total weight of particulate (m <sub>T</sub> )	.1017	.0440	.0921

**NOTE:** In no case should a blank residue 0.02 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Remarks:

Signature of Analyst:

*Thomas South*

Signature of Reviewer:

*[Signature]*

**VII. LABORATORY ANALYSIS RESULTS**

**D. Fuel Analysis Results**



1145 EAST CASS STREET, TAMPA, FLORIDA 33602  
P. O. BOX 2880, TAMPA, FLORIDA 33601-2880  
MRS# 84147 MRS# E64100

TELEPHONE (813) 223-9702  
FAX (813) 223-9332

24-Dec-1992  
Page 1

Report For: National Asphalt Pavement  
5100 Forbes rd.  
Lanham, MD. 20706-4413

Sample Identification:

Fuel oil APAC Melbourne Plant Attn: Tom Brumagin  
#6 /bunker C

Date Received: 11-Dec-1992

Laboratory Number: 843619

CERTIFICATE OF ANALYSIS

Method	Parameter	Result	Units
ASTM D287	API Gravity @ 60 oF	11.2	
	Specific Gravity @ 60/60 oF	0.9916	
ASTM D93	Flash Point, (PMCC)	255	oF
ASTM D240	Heating Value (BTU)	18316	BTU/lb
	Heating Value (BTU)	152254	BTU/gal
ASTM D129	Sulfur (S)	1.9	%

THORNTON LABORATORIES, INC.  
Fred Hartlage, Jr. Ph.D.

**VIII. EQUIPMENT CALIBRATION DATA**

**A. GC CALIBRATION DATA**

DEC 2<sup>nd</sup>

ANALYSIS OF METHOD 18 FIELD SAMPLES

BENZENE

Date: 12-2-92 Analyst: DS Plant: MAC ASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: BTEX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP-1200/75% BENTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75 Program Rate: \_\_\_\_\_ Final: 75  
 Sample Loop Volume: 100 Loop Temperature: 75 Inject. Port Temp.: 75  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data <u>PRE</u>	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.05</u>	<u>10.5</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>NA</u>	<u>NA</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA</u>	<u>NA</u>	<u>1</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>1</u>
Peak retention time (min)	<u>1.766/1.766</u>	<u>1.466/1.466</u>	<u>1</u>
Peak retention time range (min)	<u>1.766</u>	<u>1.466</u>	
Peak area	<u>7.82/7.65</u>	<u>70.85/68.66</u>	<u>1</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>7.235</u>	<u>69.255</u>	
Percent deviation from average	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.05</u>	<u>10.5</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (m): <u>6.567</u> y-intercept (b): <u>.844</u>			

Sample Analysis Data <u>POST</u>	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.05</u>	<u>10.5</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>NA</u>	<u>NA</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA</u>	<u>NA</u>	<u>1</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>1</u>
Peak retention time (min)	<u>1.766/1.766</u>	<u>1.466/1.466</u>	<u>1</u>
Peak retention time range (min)	<u>1.766</u>	<u>1.466</u>	
Peak area	<u>7.50/7.59</u>	<u>70.65/67.97</u>	<u>1</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>7.50</u>	<u>69.81</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.05</u>	<u>10.5</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$



## ANALYSIS OF METHOD 18 FIELD SAMPLES

ETHYL BENZENE

Date: 12-2-92 Analyst: DS Plant: MAC ASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: BETX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200 / 1.75% BANTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
PRE			
First analysis/second analysis			
Standard concentration (C <sub>std</sub> )	<u>1.28</u>	<u>9.70</u>	
Flow rate through loop (ml/min)	<u>600 / 600</u>	<u>600 / 600</u>	
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	
Detector attenuation	<u>32 / 32</u>	<u>32 / 32</u>	
Peak retention time (min)	<u>2.78 / 2.78</u>	<u>2.78 / 2.78</u>	
Peak retention time range (min)	<u>2.78</u>	<u>2.78</u>	
Peak area	<u>969 / 10.11</u>	<u>822.0 / 85.13</u>	
Peak area x attenuation factor	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>9.89</u>	<u>83.67</u>	
Percent deviation from average	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.28</u>	<u>9.7</u>	
% deviation from actual (%D <sub>std</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (m):	<u>8.762</u>		y-intercept (b): <u>-1.326</u>

Sample Analysis Data	Sample 1	Sample 2	Sample 3
POST			
First analysis/second analysis			
Sample identification	<u>1.28</u>	<u>9.70</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600 / 600</u>	<u>600 / 600</u>	
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	
Detector attenuation	<u>32 / 32</u>	<u>32 / 32</u>	
Peak retention time (min)	<u>2.78 / 2.78</u>	<u>2.78 / 2.78</u>	
Peak retention time range (min)	<u>2.78</u>	<u>2.78</u>	
Peak area	<u>86.7 / 9.59</u>	<u>81.92 / 86.27</u>	
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>9.13</u>	<u>84.1</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.28</u>	<u>9.7</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{std} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

TOLUENE

Date: 12-2-92 Analyst: DS Plant: MACASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: UNKNOWN Target Compound: BTEX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200 / 1.75% BENTONE 3A  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.18</u>	<u>11</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>1</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>1</u>
Peak retention time (min)	<u>5.08/5.08</u>	<u>5.13/5.73</u>	<u>1</u>
Peak retention time range (min)	<u>5.08</u>	<u>5.13</u>	
Peak area	<u>13.37/13.62</u>	<u>90.63/98.51</u>	<u>1</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>13.5</u>	<u>94.57</u>	
Percent deviation from average	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.18</u>	<u>11</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation; slope (m):	<u>8.254</u>		y-intercept (b): <u>3.76</u>

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.18</u>	<u>11</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>1</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>1</u>
Peak retention time (min)	<u>5.08/5.08</u>	<u>5.11/5.73</u>	<u>1</u>
Peak retention time range (min)	<u>5.08</u>	<u>5.1</u>	
Peak area	<u>14.41/14.34</u>	<u>92.45/97.23</u>	<u>1</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>14.38</u>	<u>94.84</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.18</u>	<u>11</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

O XYLENE

Date: 12-2-92 Analyst: DS Plant: MACASWALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: BTEX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200 / 1.75% DEWTONEXA  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 1cc Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.18</u>	<u>10.2</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>NA/</u>	<u>NA/</u>	
Injection time (24-hr clock)	<u>/</u>	<u>/</u>	
Chart speed (cm/min)	<u>NA/</u>	<u>NA/</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>6.98/6.98</u>	<u>7.03/7.08</u>	
Peak retention time range (min)	<u>6.98</u>	<u>7.03</u>	
Peak area	<u>13.52/13.14</u>	<u>97.94/105.54</u>	
Peak area x attenuation factor	<u>/</u>	<u>/</u>	
Average peak area value (Y)	<u>13.34</u>	<u>101.75</u>	
Percent deviation from average	<u>5.5%</u>	<u>2.5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.18</u>	<u>10.2</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (m):	<u>9.802</u>	y-intercept (b):	<u>1.774</u>

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.18</u>	<u>10.2</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>NA/</u>	<u>NA/</u>	
Injection time (24-hr clock)	<u>/</u>	<u>/</u>	
Chart speed (cm/min)	<u>NA/</u>	<u>NA/</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>6.98/6.98</u>	<u>7.03/7.08</u>	
Peak retention time range (min)	<u>6.98</u>	<u>7.03</u>	
Peak area	<u>11.88/11.94</u>	<u>77.51/106.07</u>	
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>/</u>	<u>/</u>	
Average peak area value (Y)	<u>11.92</u>	<u>101.79</u>	
% deviation from average (%D <sub>avg</sub> )	<u>2.5%</u>	<u>2.5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.18</u>	<u>10.2</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

## ANALYSIS OF METHOD 18 FIELD SAMPLES

METHANE  
 Date: 12-2-92 Analyst: DS Plant: MACASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: METHANE  
 Number of Standards: 3 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP 1200 / 1.25% BENTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 1cc Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>acc</sub> )	<u>11</u>	<u>310</u>	<u>495</u>
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>600/600</u>
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>32/32</u>
Peak retention time (min)	<u>433/433</u>	<u>433/450</u>	<u>433/433</u>
Peak retention time range (min)	<u>433</u>	<u>433</u>	<u>433</u>
Peak area	<u>15.54/16.05</u>	<u>480.34/472.32</u>	<u>744.77/764.84</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>15.81</u>	<u>476.33</u>	<u>754.81</u>
Percent deviation from average	<u>&lt;5%</u>	<u>&lt;5%</u>	<u>&lt;5%</u>
Calculated concentration (C <sub>std</sub> )	<u>10.35</u>	<u>311.71</u>	<u>493.94</u>
% deviation from actual (%D <sub>acc</sub> )	<u>4.11</u>	<u>.4</u>	<u>.1</u>
Linear regression equation: slope (m)	<u>1.528</u>	y-intercept (b): <u>-0.001</u>	

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>11</u>	<u>310</u>	<u>495</u>
Interface dilution factor	<u>1</u>	<u>1</u>	<u>1</u>
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>600/600</u>
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	<u>N/A</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>32/32</u>
Peak retention time (min)	<u>433/433</u>	<u>433/450</u>	<u>433/433</u>
Peak retention time range (min)	<u>433</u>	<u>433</u>	<u>433</u>
Peak area	<u>15.27/15.13</u>	<u>480.00/472.14</u>	<u>742.63/761.34</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>15.20</u>	<u>476.08</u>	<u>751.99</u>
% deviation from average (%D <sub>avg</sub> )	<u>&lt;5%</u>	<u>&lt;5%</u>	<u>&lt;5%</u>
Calculated concentration (C <sub>s</sub> )	<u>9.948</u>	<u>311.55</u>	<u>492.10</u>

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{acc} = \frac{C_{std} - C_{acc}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

BENZENE

Date: 12-3-92 Analyst: D.S Plant: MACASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: BETA  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200 / 1.75% BENTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75 C Program Rate: \_\_\_\_\_ Final: 75 C  
 Sample Loop Volume: LCC Loop Temperature: 75 C Inject. Port Temp.: 75 C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data <u>PRE</u>	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.05</u>	<u>10.5</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>NA</u>	<u>NA</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>NA</u>	<u>NA</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>1.383/1.383</u>	<u>1.366/1.383</u>	
Peak retention time range (min)	<u>1.383</u>	<u>1.366</u>	
Peak area	<u>8.29/8.30</u>	<u>86.4/90.23</u>	
Peak area x attenuation factor	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>8.30</u>	<u>88.35</u>	
Percent deviation from average	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.05</u>	<u>10.5</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (m):	<u>8.47/1</u>	y-intercept (b):	<u>-0.594</u>

Sample Analysis Data <u>POST</u>	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.05</u>	<u>10.5</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>NA</u>	<u>NA</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>NA</u>	<u>NA</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>1.383/1.383</u>	<u>1.366/1.383</u>	
Peak retention time range (min)	<u>1.383</u>	<u>1.366</u>	
Peak area	<u>8.79/8.51</u>	<u>87.03/88.08</u>	
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>8.65</u>	<u>87.56</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.05</u>	<u>10.5</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

ETHYL - BENZENE

Date: 12-3-92 Analyst: D.S. Plant: MACASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: NETX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRF Column Used: 5% SP 1200 / 1.25% BENTON 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 4000/min  
 Column Temperatures, Initial: 175C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 78C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data <u>PRE</u>	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.28</u>	<u>9.70</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>NA</u>	<u>NA</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA</u>	<u>NA</u>	<u>1</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>1</u>
Peak retention time (min)	<u>2.614/2.633</u>	<u>2.600/2.633</u>	<u>1</u>
Peak retention time range (min)	<u>2.616</u>	<u>2.600</u>	
Peak area	<u>9.981/9.82</u>	<u>105.97/106.97</u>	<u>1</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>9.90</u>	<u>106.47</u>	
Percent deviation from average	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.28</u>	<u>9.70</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (m): <u>11.47</u>		y-intercept (b): <u>-4.78</u>	

Sample Analysis Data <u>POST</u>	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.28</u>	<u>9.70</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>NA</u>	<u>NA</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA</u>	<u>NA</u>	<u>1</u>
Detector attenuation	<u>32/32</u>	<u>32/32</u>	<u>1</u>
Peak retention time (min)	<u>2.614/2.633</u>	<u>2.600/2.633</u>	<u>1</u>
Peak retention time range (min)	<u>2.616</u>	<u>2.600</u>	
Peak area	<u>8.791/8.81</u>	<u>87.031/88.08</u>	<u>1</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>8.65</u>	<u>87.56</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.28</u>	<u>9.70</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

TOLUENE

Date: 12-3-93 Analyst: D.S. Plant: MAZASPAALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: DETX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRE Column Used: 5% SP 1200 / 1.75% BENTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data <u>PRE</u>	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.18</u>	<u>1.60</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	
Injection time (24-hr clock)			
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>4.783/4.864</u>	<u>4.800/4.85</u>	
Peak retention time range (min)	<u>4.783</u>	<u>4.800</u>	
Peak area	<u>1409/1343</u>	<u>121.87/112.47</u>	
Peak area x attenuation factor			
Average peak area value (Y)	<u>13.76</u>	<u>121.170</u>	
Percent deviation from average	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.18</u>	<u>1.1</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (m): <u>10.94</u>		y-intercept (b): <u>0.853</u>	

Sample Analysis Data <u>POST</u>	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.18</u>	<u>1.1</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	
Injection time (24-hr clock)			
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>4.783/4.864</u>	<u>4.800/4.85</u>	
Peak retention time range (min)	<u>4.783</u>	<u>4.800</u>	
Peak area	<u>14.11/13.44</u>	<u>126.56/118.20</u>	
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )			
Average peak area value (Y)	<u>13.78</u>	<u>122.38</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.18</u>	<u>1.1</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

ORTO XYLENE

Date: 12-3-93 Analyst: DS Plant: MACASPART  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: DET X  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200 / 1.25% PENTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 400 C/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 1cc Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.18</u>	<u>10.2</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	
Detector attenuation	<u>321/32</u>	<u>321/32</u>	
Peak retention time (min)	<u>6.583/6.75</u>	<u>6.600/6.683</u>	
Peak retention time range (min)	<u>6.583</u>	<u>6.600</u>	
Peak area	<u>12.94/13.30</u>	<u>137.53/131.25</u>	
Peak area x attenuation factor	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>13.13</u>	<u>135.64</u>	
Percent deviation from average	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.18</u>	<u>10.2</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (a): <u>13.58</u> y-intercept (b): <u>-2.899</u>			

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.18</u>	<u>10.2</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	
Detector attenuation	<u>321/32</u>	<u>321/32</u>	
Peak retention time (min)	<u>6.583/6.75</u>	<u>6.600/6.683</u>	
Peak retention time range (min)	<u>6.583</u>	<u>6.600</u>	
Peak area	<u>13.57/13.32</u>	<u>140.72/129.22</u>	
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>13.45</u>	<u>135.07</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.18</u>	<u>10.2</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$



ANALYSIS OF METHOD 18 FIELD SAMPLES

METHANE

Date: 12-3-92 Analyst: D.S. Plant: MACAS DEALT  
 Location: MILLBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: METHANE  
 Number of Standards: 3 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200 / 1.75% OXTOR 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 CC/MIN  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>acc</sub> )	<u>11</u>	<u>310</u>	<u>495</u>
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>600/600</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Detector attenuation	<u>321 32</u>	<u>321 32</u>	<u>321 32</u>
Peak retention time (min)	<u>416.416</u>	<u>416.433</u>	<u>416.416</u>
Peak retention time range (min)	<u>416</u>	<u>416</u>	<u>416</u>
Peak area	<u>18.79/18.4</u>	<u>609.45/587.80</u>	<u>847.13/807.12</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>18.40</u>	<u>592.63</u>	<u>827.13</u>
Percent deviation from average	<u>&lt; 5%</u>	<u>&lt; 5%</u>	<u>&lt; 5%</u>
Calculated concentration (C <sub>std</sub> )	<u>8.81</u>	<u>341.083</u>	<u>475.80</u>
% deviation from actual (%D <sub>acc</sub> )	<u>57.41</u>	<u>155.42</u>	<u>100.00</u>
Linear regression equation; slope (m)	<u>6694</u>	y-intercept (b): <u>20.094</u>	

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>11</u>	<u>310</u>	<u>495</u>
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>600/600</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Detector attenuation	<u>321 32</u>	<u>321 32</u>	<u>321 32</u>
Peak retention time (min)	<u>416.416</u>	<u>416.433</u>	<u>416.416</u>
Peak retention time range (min)	<u>416</u>	<u>416</u>	<u>416</u>
Peak area	<u>18.44/18.19</u>	<u>607.69/586.57</u>	<u>845.11/805.60</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>18.29</u>	<u>597.11</u>	<u>825.61</u>
% deviation from average (%D <sub>avg</sub> )	<u>&lt; 5%</u>	<u>&lt; 5%</u>	<u>&lt; 5%</u>
Calculated concentration (C <sub>s</sub> )	<u>8.31</u>	<u>340.95</u>	<u>475.88</u>

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{acc} = \frac{C_{std} - C_{acc}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

BENZENE

Date: 12-4-72 Analyst: D.S. Plant: MAC ASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: BETA  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SAE Column Used: 5% SP1200 / 1.75% BENTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.05</u>	<u>10.5</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Detector attenuation	<u>32132</u>	<u>32132</u>	<u>1</u>
Peak retention time (min)	<u>1.35/1.35</u>	<u>1.35/1.35</u>	<u>1</u>
Peak retention time range (min)	<u>1.35</u>	<u>1.35</u>	
Peak area	<u>86.018.80</u>	<u>86.52186.77</u>	<u>1</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>8.7</u>	<u>86.65</u>	
Percent deviation from average	<u>5.5%</u>	<u>5.5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.05</u>	<u>10.5</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation: slope (m):	<u>8.25</u>	y-intercept (b):	<u>0.39</u>

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.05</u>	<u>10.5</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Detector attenuation	<u>32132</u>	<u>32132</u>	<u>1</u>
Peak retention time (min)	<u>1.35/1.35</u>	<u>1.35/1.35</u>	<u>1</u>
Peak retention time range (min)	<u>1.35</u>	<u>1.35</u>	
Peak area	<u>86.318.80</u>	<u>87.56187.06</u>	<u>1</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>8.72</u>	<u>87.31</u>	
% deviation from average (%D <sub>avg</sub> )	<u>5.5%</u>	<u>5.5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.05</u>	<u>10.5</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

ETHYL BENZENE

Date: 12-4-92 Analyst: DS. Plant: MACASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: BETX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200 / 1.75% DEWTONEX 3F  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 4000 ml/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.28</u>	<u>9.70</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Detector attenuation	<u>32 132</u>	<u>32 132</u>	<u>1</u>
Peak retention time (min)	<u>2.564/2.550</u>	<u>2.564/2.564</u>	<u>1</u>
Peak retention time range (min)	<u>2.550</u>	<u>2.564</u>	
Peak area	<u>9.87 19.72</u>	<u>104.49 101.05</u>	<u>1</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>9.80</u>	<u>102.75</u>	
Percent deviation from average	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.28</u>	<u>9.70</u>	
% deviation from actual (%D <sub>act</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation; slope (m):	<u>11.04</u>	y-intercept (b):	<u>-4.33</u>

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.28</u>	<u>9.70</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>1</u>
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	<u>1</u>
Detector attenuation	<u>32 132</u>	<u>32 132</u>	<u>1</u>
Peak retention time (min)	<u>2.564/2.550</u>	<u>2.564/2.564</u>	<u>1</u>
Peak retention time range (min)	<u>2.550</u>	<u>2.564</u>	
Peak area	<u>10.49/10.71</u>	<u>105.22/103.18</u>	<u>1</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>10.60</u>	<u>104.20</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt;5%</u>	<u>&lt;5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.28</u>	<u>9.70</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{act} = \frac{C_{std} - C_{act}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

TOLUENE

Date: 12-4-93 Analyst: DS Plant: M/ACASPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: BETX  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP 1200 / 1.25% PENTONE 34  
 Carrier Gas Used: N2 Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 100 Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>1.18</u>	<u>11</u>	
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>4.66/4.63</u>	<u>4.66/4.68</u>	
Peak retention time range (min)	<u>4.63</u>	<u>4.66</u>	
Peak area	<u>13.74/14.18</u>	<u>103.28/107.58</u>	
Peak area x attenuation factor	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>13.94</u>	<u>105.43</u>	
Percent deviation from average	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>std</sub> )	<u>1.18</u>	<u>11</u>	
% deviation from actual (%D <sub>acc</sub> )	<u>0</u>	<u>0</u>	
Linear regression equation; slope (m):	<u>9.32</u>		y-intercept (b): <u>2.97</u>

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.18</u>	<u>11</u>	
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	
Liquid injection volume (tubes)	<u>N/A</u>	<u>N/A</u>	
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	
Chart speed (cm/min)	<u>N/A</u>	<u>N/A</u>	
Detector attenuation	<u>32/32</u>	<u>32/32</u>	
Peak retention time (min)	<u>4.66/4.63</u>	<u>4.66/4.68</u>	
Peak retention time range (min)	<u>4.63</u>	<u>4.66</u>	
Peak area	<u>14.48/14.86</u>	<u>104.69/109.35</u>	
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	
Average peak area value (Y)	<u>14.68</u>	<u>107.02</u>	
% deviation from average (%D <sub>avg</sub> )	<u>&lt; 5%</u>	<u>&lt; 5%</u>	
Calculated concentration (C <sub>s</sub> )	<u>1.18</u>	<u>11</u>	

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{acc} = \frac{C_{std} - C_{acc}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

ORTO-XYLENE

Date: 12-4-92 Analyst: D.S. Plant: MACASPIHANT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CILINDER Target Compound: BETA  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% ST1200/1.75%  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 1cc Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>std</sub> )	<u>1.18</u>	<u>10.2</u>	<u>_____</u>
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>_____</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>_____</u>
Injection time (24-hr clock)	<u>_____</u>	<u>_____</u>	<u>_____</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>_____</u>
Detector attenuation	<u>321.32</u>	<u>321.32</u>	<u>_____</u>
Peak retention time (min)	<u>6.41/6.4</u>	<u>6.41/6.46</u>	<u>_____</u>
Peak retention time range (min)	<u>6.4</u>	<u>6.41/6.4</u>	<u>_____</u>
Peak area	<u>13.57/13.75</u>	<u>105.71/113.02</u>	<u>_____</u>
Peak area x attenuation factor	<u>_____</u>	<u>_____</u>	<u>_____</u>
Average peak area value (Y)	<u>13.47</u>	<u>109.37</u>	<u>_____</u>
Percent deviation from average	<u>&lt;5%</u>	<u>&lt;5%</u>	<u>_____</u>
Calculated concentration (C <sub>std</sub> )	<u>1.18</u>	<u>10.2</u>	<u>_____</u>
% deviation from actual (%D <sub>acc</sub> )	<u>0</u>	<u>0</u>	<u>_____</u>
Linear regression equation; slope (m):	<u>10.61</u>	y-intercept (b):	<u>1.150</u>

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>1.18</u>	<u>10.2</u>	<u>_____</u>
Interface dilution factor	<u>_____</u>	<u>_____</u>	<u>_____</u>
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>_____</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>_____</u>
Injection time (24-hr clock)	<u>_____</u>	<u>_____</u>	<u>_____</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>_____</u>
Detector attenuation	<u>321.32</u>	<u>321.32</u>	<u>_____</u>
Peak retention time (min)	<u>6.41/6.4</u>	<u>6.41/6.46</u>	<u>_____</u>
Peak retention time range (min)	<u>6.4</u>	<u>6.41/6.4</u>	<u>_____</u>
Peak area	<u>14.63/13.75</u>	<u>10.72/115.11</u>	<u>_____</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>_____</u>	<u>_____</u>	<u>_____</u>
Average peak area value (Y)	<u>14.19</u>	<u>111.42</u>	<u>_____</u>
% deviation from average (%D <sub>avg</sub> )	<u>&lt;5%</u>	<u>&lt;5%</u>	<u>_____</u>
Calculated concentration (C <sub>s</sub> )	<u>1.18</u>	<u>10.2</u>	<u>_____</u>

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{acc} = \frac{C_{std} - C_{acc}}{Y} \times 100\%$$

ANALYSIS OF METHOD 18 FIELD SAMPLES

METHANE

Date: 12-4-92 Analyst: D.S. Plant: MACALPHALT  
 Location: MELBOURNE FL Sample Type: GAS  
 Type of Calibration Standard: CYLINDER Target Compound: METHANE  
 Number of Standards: 2 Date Prepared: \_\_\_\_\_ Prepared By: \_\_\_\_\_

GC Used: SRI Column Used: 5% SP1200/1.75% DEXTONE 34  
 Carrier Gas Used: N<sub>2</sub> Carrier Gas Flow Rate: 40 cc/min  
 Column Temperatures, Initial: 75C Program Rate: \_\_\_\_\_ Final: 75C  
 Sample Loop Volume: 1cc Loop Temperature: 75C Inject. Port Temp.: 75C  
 Detector Temp.: \_\_\_\_\_ Auxiliary Gases: \_\_\_\_\_

Calibration Data	Standard 1	Standard 2	Standard 3
First analysis/second analysis			
Standard concentration (C <sub>act</sub> )	<u>11</u>	<u>310</u>	<u>495</u>
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>600/600</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Detector attenuation	<u>321.32</u>	<u>321.32</u>	<u>321.32</u>
Peak retention time (min)	<u>400.416</u>	<u>400.416</u>	<u>400.400</u>
Peak retention time range (min)	<u>.400</u>	<u>.400</u>	<u>.400</u>
Peak area	<u>18.621/19.27</u>	<u>509.25/508.58</u>	<u>888.54/843.78</u>
Peak area x attenuation factor	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>18.95</u>	<u>508.92</u>	<u>866.01</u>
Percent deviation from average	<u>&lt; 5%</u>	<u>&lt; 5%</u>	<u>&lt; 5%</u>
Calculated concentration (C <sub>std</sub> )	<u>15.79</u>	<u>297.46</u>	<u>502.75</u>
% deviation from actual (%D <sub>acc</sub> )	<u>25.3%</u>	<u>2.5%</u>	<u>1.9%</u>
Linear regression equation; slope (m):	<u>1.74</u>	y-intercept (b): <u>-8.52</u>	

Sample Analysis Data	Sample 1	Sample 2	Sample 3
First analysis/second analysis			
Sample identification	<u>11</u>	<u>310</u>	<u>495</u>
Interface dilution factor			
Flow rate through loop (ml/min)	<u>600/600</u>	<u>600/600</u>	<u>600/600</u>
Liquid injection volume (tubes)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Injection time (24-hr clock)	<u>1</u>	<u>1</u>	<u>1</u>
Chart speed (cm/min)	<u>NA1</u>	<u>NA1</u>	<u>NA1</u>
Detector attenuation	<u>321.32</u>	<u>321.32</u>	<u>321.32</u>
Peak retention time (min)	<u>400.416</u>	<u>400.416</u>	<u>400.400</u>
Peak retention time range (min)	<u>.400</u>	<u>.400</u>	<u>.400</u>
Peak area	<u>18.66/18.61</u>	<u>509.07/506.63</u>	<u>831.77/832.52</u>
Peak area x atten. factor (A <sub>1</sub> /A <sub>2</sub> )	<u>1</u>	<u>1</u>	<u>1</u>
Average peak area value (Y)	<u>18.64</u>	<u>507.84</u>	<u>857.15</u>
% deviation from average (%D <sub>avg</sub> )	<u>&lt; 5%</u>	<u>&lt; 5%</u>	<u>&lt; 5%</u>
Calculated concentration (C <sub>s</sub> )	<u>15.61</u>	<u>296.85</u>	<u>497.65</u>

$$C_{std} \text{ or } C_s = \frac{(Y - b)}{m} \quad \%D_{avg} = \left| \frac{A_1 - Y}{Y} \right| \times 100\% \quad \%D_{acc} = \frac{C_{std} - C_{acc}}{Y} \times 100\%$$

**VIII. EQUIPMENT CALIBRATION DATA**

**B. CEMS CALIBRATION DATA**

DILUENT O<sub>2</sub> AND CO<sub>2</sub> MONITORS

Plant NAPA-MacAsphalt

Location Coconut Beach, FL

Date 12-2-92

Operator TM

Initial Calibration (Accuracy: ± 2% Span)

O <sub>2</sub>			CO <sub>2</sub>		
Gas Type	Actual Concentration	Analyzer Response	Gas Type	Actual Concentration	Analyzer Response
O <sub>2</sub> -Zero	0.0	0.0	CO <sub>2</sub> -Zero	0.0	0.0
O <sub>2</sub> -High	20.9	21.1	CO <sub>2</sub> -High	17.1	17.3
O <sub>2</sub> -Mid	10.0	10.0	CO <sub>2</sub> -Mid	10.0	10.0

System Bias Reponse: Analyzer Response-Initial Bias = ± 5% Span  
 Final Bias - Initial Bias = ± 3% Span

Run # 1 Time: 14:16-14:16

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.0	0.0	0.0	0.1	
CO <sub>2</sub> /O <sub>2</sub>	10.0	10.0	10.0	10.0	

12-3-92 Run # 2 Time: 10:25-12:22

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.1	0.1	0.2	-0.3	
CO <sub>2</sub> /O <sub>2</sub>	10.1	10.1	9.3	9.9	

12-3-92 Run # 3 Time: 12:55 → 13:22 + 14:59 → 16:40

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.1	0.1	-0.5	-0.5	
CO <sub>2</sub> /O <sub>2</sub>	10.0	10.1	9.5	9.7	

12-4-92 Run # 4 Time: 9:26 → 9:20 + 10:41 → 11:50

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.1	0.1	0.3	-0.3	
CO <sub>2</sub> /O <sub>2</sub>	10.0	10.0	10.0	9.7	



DILUENT O<sub>2</sub> AND CO<sub>2</sub> MONITORS

Plant NAPA - Mac Asphalt

Location Coconut Beach, FL

Date 12-4-92

Operator TM

Initial Calibration (Accuracy: ± 2% Span)

O <sub>2</sub>			CO <sub>2</sub>		
Gas Type	Actual Concentration	Analyzer Response	Gas Type	Actual Concentration	Analyzer Response
O <sub>2</sub> -Zero			CO <sub>2</sub> -Zero		
O <sub>2</sub> -High			CO <sub>2</sub> -High		
O <sub>2</sub> -Mid			CO <sub>2</sub> -Mid		

System Bias Response: Analyzer Response-Initial Bias = ± 5% Span  
 Final Bias - Initial Bias = ± 3% Span

Run # 5 Time: 12:18-14:02

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.0	0.0	0.2	-0.1	
CO <sub>2</sub> /O <sub>2</sub>	10.0	10.0	9.7	9.9	

Run # 6 Time: 14:46-16:02

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero	0.0	0.0	0.1	0.2	
CO <sub>2</sub> /O <sub>2</sub>	10.0	10.0	10.1	10.2	

Run # Time:

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero					
CO <sub>2</sub> /O <sub>2</sub>					

Run # Time:

Gas Type	Initial Bias Response		Final Bias Response		Drift
Zero					
CO <sub>2</sub> /O <sub>2</sub>					

INSTRUMENTAL ANALYSIS CALIBRATION DATA

TOTAL HYDROCARBONS

PLANT NAPA - Mal Asphalt LOCATION Cocoa Beach, FL  
 DATE 12-2-92 OPERATOR TM  
 HC RANGE 0-1000 ppm Methane RESPONSE TIME \_\_\_\_\_

INITIAL CALIBRATION: (Accuracy ±5% of calibration gas value)

Gas Type	Actual Concentration	Analyzer	Gas Type	Actual Concentration	Analyzer
HC - Zero	0	0.4	HC - Mid	5495	493
HC - High	999	996	HC - Low	310	309.8

ZERO & SPAN DRIFT: (Accuracy ±3% of span)

12-3-92

Run # 1 Time: 14:16-16:16		
Gas Type	Initial Response	Final Response
HC - Zero	0.4	0.4
HC - 310	309.8	309.1

12-4-92

Run # 4 Time: 8:26 → 9:26 + 10:41 → 11:56		
Gas Type	Initial Response	Final Response
HC - Zero	0.4	6.5
HC - 310	308.5	302.4

12-3-92

Run # 2 Time: 10:25-12:22		
Gas Type	Initial Response	Final Response
HC - Zero	-0.1	3.0
HC - 310	307.9	309.9

12-4-92

Run # 5 Time: 12:18-14:02		
Gas Type	Initial Response	Final Response
HC - Zero	1.0	0.3
HC - 310	308.3	306.9

12-3-92

Run # 3 Time: 12:55 → 13:22 + 14:59 → 16:40		
Gas Type	Initial Response	Final Response
HC - Zero	0.4	0.7
HC - 310	307.1	312.8

Run # 6 Time: 14:46-16:02		
Gas Type	Initial Response	Final Response
HC - Zero	0.3	-1.1
HC -	306.9	300.6

CARBON MONOXIDE

Plant NAPA - Mac Asphalt

Location Coconut Beach, FL

Date 12-2-92

Operator TM

CO Range 0-1000 ppm

Initial Calibration: (Accuracy: ± 5% Span)

Gas Type	Actual Concentration	Anayzer Response
CO-Zero	0	-0.1
CO-High	904	914
CO-Mid	536	528
CO-Low	290	295

Zero & Span Drift: (Accuracy ± 5% Span)

End Run # 1 Time: 14:16-15:16

Gas Type	Initial Response	Final Response	Drift
CO-Zero	-0.1	<del>-0.1</del> -3.1	
CO-904	914	907	

12-3-92 End Run # 2 Time: 10:25-12:22

Gas Type	Initial Response	Final Response	Drift
CO-Zero	0.3	-7.4	
CO-290	293	272	

12-3-92 End Run # 3 Time: 12:55 → 13:22 + 14:59 → 16:40

Gas Type	Initial Response	Final Response	Drift
CO-Zero	0.3	-5.0	
CO-290	291	291.6	

12-4-92 End Run # 4 Time: 8:26 → 9:20 + 10:41 → 11:50

Gas Type	Initial Response	Final Response	Drift
CO-Zero	0.9	-5.1	
CO-290	290	294.7	

CARBON MONOXIDE

Plant NAPA-Mal Asphalt

Location Cocoa Beach, FL

Date 12-4-92

Operator TW

CO Range 0-1000 ppm

Initial Calibration: (Accuracy:  $\pm$  5% Span)

Gas Type	Actual Concentration	Anayzer Response
CO-Zero	0	
CO-High		
CO-Mid		
CO-Low		

Zero & Span Drift: (Accuracy  $\pm$  5% Span)

End Run # 5 Time: 12:18 - 14:02

Gas Type	Initial Response	Final Response	Drift
CO-Zero	0.8	-1.1	
CO-290	294.7	292.7	

End Run # 6 Time: 14:46 - 16:02

Gas Type	Initial Response	Final Response	Drift
CO-Zero	1.0	-1.1	
CO-	294.0	290.1	

End Run # Time:

Gas Type	Initial Response	Final Response	Drift
CO-Zero			
CO-			

End Run # Time:

Gas Type	Initial Response	Final Response	Drift
CO-Zero			
CO-			

NO<sub>x</sub> MONITOR

Plant NAPA-Mal Asphalt

Location Coconut Beach, FL

Date 12-2-92

Operator TM

Initial Calibration (Accuracy: ± 2% Span)

Gas Type	Actual Concentration	Analyzer Response
NO <sub>x</sub> -Zero	0.0	0.1
NO <sub>x</sub> -High	200	204
NO <sub>x</sub> -Mid	143	144.8

System Bias Reponse: Analyzer Response-Initial Bias = ± 5% Span  
 Final Bias - Initial Bias = ± 3% Span

Run # 1 Time: 14:16-15:16

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	0.1	2.4	
NO <sub>x</sub>	144.8	147.0	

12-3-92 Run # 2 Time: 10:25-12:22

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	0.8	3.5	
NO <sub>x</sub>	143.9	148.1	

12-3-92 Run # 3 Time: 12:55 → 13:22 + 14:59 → 16:46

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	0.3	-1.0	
NO <sub>x</sub>	144.7	139.0	

12-4-92 Run # 4 Time: 8:26 → 9:26 + 10:41 → 11:50

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	0.9	14.1	
NO <sub>x</sub>	142.8	172.3	

NO<sub>x</sub> MONITOR

Plant NAPA - Mac Asphalt

Location Coconut Beach, FL

Date 12-4-92

Operator TM

Initial Calibration (Accuracy: ± 2% Span)

Gas Type	Actual Concentration	Analyzer Response
NO <sub>x</sub> -Zero		
NO <sub>x</sub> -High		
NO <sub>x</sub> -Mid		

System Bias Response: Analyzer Response-Initial Bias = ± 5% Span  
 Final Bias - Initial Bias = ± 3% Span

Run # 5 Time: 12:18-14:02

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	<u>1.0</u>	<u>15.1</u>	
NO <sub>x</sub>	<u>141.9</u>	<u>165.3</u>	

Run # 6 Time: 14:46-16:02

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	<u>0.2</u>	<u>0.0</u>	
NO <sub>x</sub>	<u>144.7</u>	<u>139.8</u>	

Run # Time:

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero			
NO <sub>x</sub>			

Run # Time:

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero			
NO <sub>x</sub>			

INSTRUMENTAL ANALYSIS CALIBRATION DATA

SO<sub>2</sub> MONITORS

Plant NAPA - Mac Asphalt

Location Cocoa Beach, FL

Date 12-2-92

Operator Tm

Initial Calibration (Accuracy: ± 2% Span)

Gas Type	Actual Concentration	Analyzer Response
SO <sub>2</sub> -Zero	0.0	<del>0.0</del> 2.0
SO <sub>2</sub> -High	828	836
SO <sub>2</sub> -Mid	555	556

System Bias Response: Analyzer Response-Initial Bias = ± 5% Span  
 Final Bias - Initial Bias = ± 3% Span

Run # 1 Time: 14:16 - 15:16

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	2.0	3.0	
SO <sub>2</sub>	556	555	

12-3-92 Run # 2 Time: 10:25 - 12:22

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	3.0	5.0	
SO <sub>2</sub>	555	561	

12-3-92 Run # 3 Time: 12:55 → 13:22 + 14:59 → 16:40

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	3.0	7.0	
SO <sub>2</sub>	548	559	

12-4-92 Run # 4 Time: 8:26 → 9:20 + 10:41 → 11:50

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	2.0	4.0	
SO <sub>2</sub>	549	558	

SO<sub>2</sub> MONITORS

Plant NAPA - Mac Asphalt

Location Cocoa Beach, FL

Date 12-4-92

Operator TM

Initial Calibration (Accuracy: ± 2% Span)

Gas Type	Actual Concentration	Analyzer Response
SO <sub>2</sub> -Zero		
SO <sub>2</sub> -High		
SO <sub>2</sub> -Mid		

System Bias Response: Analyzer Response-Initial Bias = ± 5% Span  
 Final Bias - Initial Bias = ± 3% Span

Run # 5 Time: 12:18-14:02

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	<del>3.0</del> 3.0	3.0	
SO <sub>2</sub>	558	562	

Run # 6 Time: 14:46-16:02

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero	3.0	4.0	
SO <sub>2</sub>	562	559	

Run # Time:

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero			
SO <sub>2</sub>			

Run # Time:

Gas Type	Initial Bias Response	Final Bias Response	Drift
Zero			
SO <sub>2</sub>			



**VIII. EQUIPMENT CALIBRATION DATA**

**C. PARTICULATE CALIBRATION DATA**

## TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level?  yes  no

Pitot tube openings damaged?  yes (explain below)  no

$\alpha_1 = 1.3^\circ$  ( $<10^\circ$ ),  $\alpha_2 = 0.8^\circ$  ( $<10^\circ$ ),  $\beta_1 = 0.5^\circ$  ( $<5^\circ$ ),

$\beta_2 = 1.8^\circ$  ( $<5^\circ$ )

$\gamma = 2.9^\circ$ ,  $\theta = 1.7^\circ$ ,  $A = .97$  cm (in.)

$z = A \sin \gamma = .05$  cm (in.);  $<0.32$  cm ( $<1/8$  in.),

$w = A \sin \theta = .03$  cm (in.);  $<.08$  cm ( $<1/32$  in.)

$P_A = .48$  cm (in.)  $P_B = .49$  cm (in.)

$D_t = .38$  cm (in.)

Comments: \_\_\_\_\_  
 \_\_\_\_\_  
 \_\_\_\_\_

Calibration required?  yes  no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level?  yes  no

Pitot tube openings damaged?  yes (explain below)  no

$\alpha_1 = 2.3^\circ (<10^\circ)$ ,  $\alpha_2 = .5^\circ (<10^\circ)$ ,  $\beta_1 = 1.8^\circ (<5^\circ)$ ,  
 $\beta_2 = 1.8^\circ (<5^\circ)$

$\gamma = 3.2^\circ$ ,  $\theta = 1.0^\circ$ ,  $A = .98$  cm (in.)

$z = A \sin \gamma = .05$  cm (in.);  $<0.32$  cm ( $<1/8$  in.),

$w = A \sin \theta = .02$  cm (in.);  $<.08$  cm ( $<1/32$  in.)

$P_A = .49$  cm (in.)  $P_B = .49$  cm (in.)

$D_t = .38$  cm (in.)

Comments: \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

Calibration required?  yes  no

Lear Siegler Stack Sampler

Nozzle Diameter Calibration

Date \_\_\_\_\_ Signature \_\_\_\_\_

Nozzle No.	Average Diameter	Nozzle No.	Average Diameter
1	_____	7	_____
2	_____	8	_____
3	_____	9	_____
4	_____	10	_____
5	_____	11	_____
6	_____	12	_____

Pitot Tube Calibration (S Type)

Pitot Tube Identification No. 6-4 Date 6-9-91

Calibrated by: S Buch

"A" SIDE CALIBRATION

Run No.	$\Delta p$ std cm H <sub>2</sub> O (in. H <sub>2</sub> O)	$\Delta p$ (s) cm H <sub>2</sub> O (in. H <sub>2</sub> O)	$C_p$ (s)	DEVIATION $C_p(s) - \bar{C}_p(A)$
1	2.2	3.2	.829	.001
2	1.8	2.6	.832	.002
3	1.1	1.6	.829	.001
			$\bar{C}_p$ (SIDE A)	.830

"B" SIDE CALIBRATION

Run No.	$\Delta p$ std cm H <sub>2</sub> O (in. H <sub>2</sub> O)	$\Delta p$ (s) cm H <sub>2</sub> O in. H <sub>2</sub> O)	$C_p$ (s)	DEVIATION $C_p(s) - \bar{C}_p(B)$
1	2.2	3.2	.829	.001
2	1.8	2.6	.832	.002
3	1.1	1.6	.829	.001
			$\bar{C}_p$ (SIDE B)	.830

$$\text{AVERAGE DEVIATION} = \sigma(A \text{ OR } B) = \frac{\sum |C_p(s) - \bar{C}_p(A \text{ OR } B)|}{3} \quad + \text{MUST BE } \leq 0.01$$

$$|\bar{C}_p(\text{SIDE A}) - \bar{C}_p(\text{SIDE B})| \quad + \text{MUST BE } \leq 0.01$$

$$C_p(s) = C_p(\text{std}) \sqrt{\frac{\Delta p \text{ std}}{\Delta p s}}$$

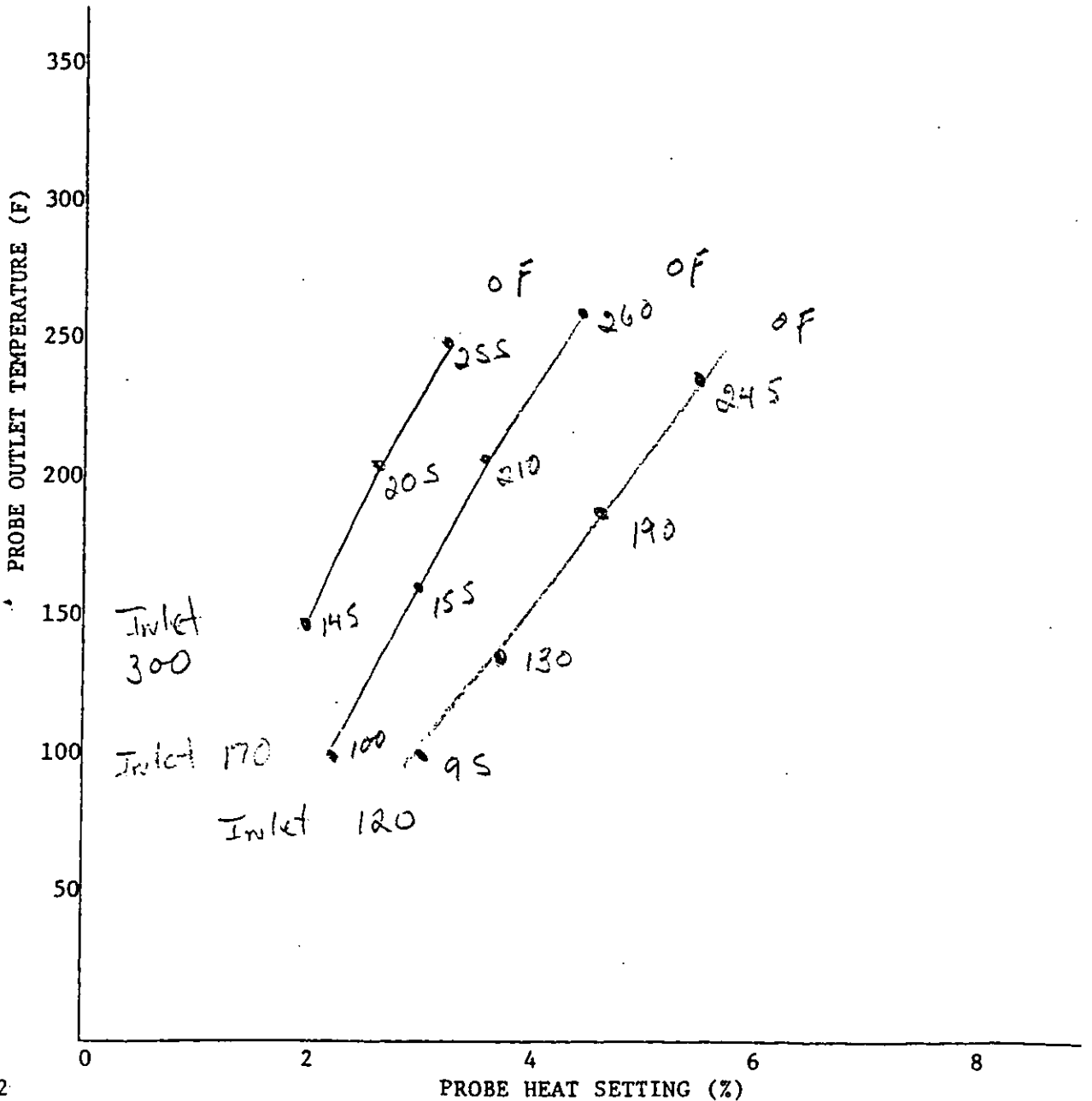
RAMCON

Lear Siegler Stack Sampler

Heating Probe Calibration

Probe No. 64 Probe Length 6'  
 Date of Calibration 5-7-90 Signature Sam Turner  
 Name of Company to be tested \_\_\_\_\_

Note: 3 ft. probe - 5 min. warmup  
 6 ft. probe - 15 min. warmup  
 10 ft. probe - 30 min. warmup  
 Calibration flow rate = .75 CFM



## STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Date 5-5-90 Thermocouple number 64  
 Ambient temperature 20 °C Barometric pressure 29.88 in. Hg  
 Calibrator Stume Reference: mercury-in-glass   
 other \_\_\_\_\_

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference, % <sup>b</sup>
A	Ice Bath	32	32	0
B	Boiling water	212	211	.005
C	Boiling oil	381	378	.008
D	Ambient			

<sup>a</sup>Type of calibration system used.

<sup>b</sup>
$$\left[ \frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] 100 \leq 1.5\%$$

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number \_\_\_\_\_ Date 1/2/93 Meter box number 90-800 Plant \_\_\_\_\_

Barometric pressure,  $P_b = 30.26$  in. Hg Dry gas meter number 26940 Pretest Y \_\_\_\_\_

Orifice manometer setting, $(\Delta H)$ , in. $H_2O$	Gas volume		Temperature				Time $(\theta)$ , min	Vacuum setting, in. Hg	$Y_i$	$V_w P_b (t_d + 460)$ $V_d \left( P_b + \frac{\Delta H}{13.6} \right) (t_w + 460)$
	Wet test meter $(V_w)$ , $ft^3$	Dry gas meter $(V_d)$ , $ft^3$	Wet test meter $(t_w)$ , $^{\circ}F$	Dry gas meter		Average $(t_d)$ , $^{\circ}F$				
				Inlet $(t_{d_i})$ , $^{\circ}F$	Outlet $(t_{d_o})$ , $^{\circ}F$					
1.0	10	<del>342.143</del> 352.883	640	<del>104</del> 118	<del>85</del> 88	98.75	19.2	6"	.99	1.89
2.0	10	<del>380.616</del> 341.298	640	<del>107</del> 120	<del>79</del> 85	97.25	13.73	5"	.99	1.94
3.0	10	<del>317.841</del> 328.402	640	<del>96</del> 119	<del>69</del> 75	89.25	11.13	7"	.985	1.94
									Y =	

<sup>a</sup> If there is only one thermometer on the dry gas meter, record the temperature under  $t_d$  where

$V_w$  = Gas volume passing through the wet test meter,  $ft^3$ .

$V_d$  = Gas volume passing through the dry gas meter,  $ft^3$ .

$t_w$  = Temperature of the gas in the wet test meter,  $^{\circ}F$ .

$t_{d_i}$  = Temperature of the inlet gas of the dry gas meter,  $^{\circ}F$ .

$t_{d_o}$  = Temperature of the outlet gas of the dry gas meter,  $^{\circ}F$ .

$t_d$  = Average temperature of the gas in the dry gas meter, obtained by the average of  $t_{d_i}$  and  $t_{d_o}$ ,  $^{\circ}F$ .

$\Delta H$  = Pressure differential across orifice, in.  $H_2O$ .

$Y_i$  = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest Y  $\pm$  0.05Y.

$P_b$  = Barometric pressure, in. Hg.

$\theta$  = Time of calibration run, min.

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number \_\_\_\_\_ Date 11/28 Meter box number Anderson Plant 1204  
 Barometric pressure,  $P_b = 30.18$  in. Hg Dry gas meter number \_\_\_\_\_ Pretest Y \_\_\_\_\_

Orifice manometer setting, ( $\Delta H$ ), in. H <sub>2</sub> O	Gas volume		Temperature			Time ( $\theta$ ), min	Vacuum setting, in. Hg	$Y_i$	$V_w P_b (t_d + 460)$ $V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)$
	Wet test meter ( $V_w$ ), ft <sup>3</sup>	Dry gas meter ( $V_d$ ), ft <sup>3</sup>	Wet test meter ( $t_w$ ), °F	Inlet ( $t_d$ ), °F	Outlet ( $t_o$ ), °F				
10.17 3 $\phi$	10	<del>940.565</del> 551.782	63°	92°	<del>85°</del> 85°	95	5	.979	1.920
5.324 .50	10	<del>551.663</del> 551.582	63	85°	<del>84</del> 82	87	2	.981	1.803
1.5	10	<del>557.383</del> 557.035	63	93°	<del>82</del> 86	90.3	3	.971	1.833
								Y =	1.852

<sup>a</sup> If there is only one thermometer on the dry gas meter, record the temperature under  $t_d$  where

$V_w$  = Gas volume passing through the wet test meter, ft<sup>3</sup>.

$V_d$  = Gas volume passing through the dry gas meter, ft<sup>3</sup>.

$t_w$  = Temperature of the gas in the wet test meter, °F.

$t_{d_i}$  = Temperature of the inlet gas of the dry gas meter, °F.

$t_{d_o}$  = Temperature of the outlet gas of the dry gas meter, °F.

$t_d$  = Average temperature of the gas in the dry gas meter, obtained by the average of  $t_{d_i}$  and  $t_{d_o}$ , °F.

$\Delta H$  = Pressure differential across orifice, in. H<sub>2</sub>O.

$Y_i$  = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest Y  $\pm$  0.05Y.

$P_b$  = Barometric pressure, in. Hg.

$\theta$  = Time of calibration run, min.

Quality Assurance Handbook M4-2.4A



POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number 12-11-92 Date 12-11-92 Meter box number C-185 Plant Pretest Y  
 Barometric pressure,  $P_b =$  30.10 in. Hg Dry gas meter number 638809

Orifice manometer setting, $(\Delta H)$ , in. H <sub>2</sub> O	Gas volume		Temperature			Time $(\theta)$ , min	Vacuum setting, in. Hg	$Y_i$	$V_w P_b (t_w + 460)$ $V_d (P_b + \frac{\Delta H}{13.6}) (t_w + 460)$
	Wet test meter $(V_w)$ , ft <sup>3</sup>	Dry gas meter $(V_d)$ , ft <sup>3</sup>	Wet test meter $(t_w)$ , °F	Inlet $(t_{d_i})$ , °F	Outlet $(t_{d_o})$ , °F				
5.105	10	862.311	66	90	70	11.98	1	1.006	1.546
10.225	10	488.162	66	93.46	72.22	16.9	3	1.007	1.532
	10	852.050	66	90	68.90	9.65	6	1.023	1.503
								$Y = 1.012$	1.527

<sup>a</sup> If there is only one thermometer on the dry gas meter, record the temperature under  $t_d$  where

$V_w$  = Gas volume passing through the wet test meter, ft<sup>3</sup>.

$V_d$  = Gas volume passing through the dry gas meter, ft<sup>3</sup>.

$t_w$  = Temperature of the gas in the wet test meter, °F.

$t_{d_i}$  = Temperature of the inlet gas of the dry gas meter, °F.

$t_{d_o}$  = Temperature of the outlet gas of the dry gas meter, °F.

$t_d$  = Average temperature of the gas in the dry gas meter, obtained by the average of  $t_{d_i}$  and  $t_{d_o}$ , °F.

$\Delta H$  = Pressure differential across orifice, in. H<sub>2</sub>O.

$Y_i$  = Ratio of accuracy of wet test meter to dry gas meter for each run.

$Y$  = Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest  $Y \pm 0.05Y$ .

$P_b$  = Barometric pressure, in. Hg.

$\theta$  = Time of calibration run, min.

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Test number 11-2352 Date 1-23-52 Meter box number C-185 Plant                       
 Barometric pressure,  $P_b =$  29.90 in. Hg Dry gas meter number 658805 Pretest Y                     

Orifice manometer setting, $(\Delta H)$ , in. H <sub>2</sub> O	Gas volume		Temperature			Time $(\theta)$ , min	Vacuum setting, in. Hg	Y <sub>i</sub>	Y <sub>i</sub> <u>539</u> V <sub>w</sub> P <sub>b</sub> (t <sub>d</sub> + 460) V <sub>d</sub> (P <sub>b</sub> + $\frac{\Delta H}{13.6}) (t_w + 460)$
	Wet test meter (V <sub>w</sub> ), ft <sup>3</sup>	Dry gas meter (V <sub>d</sub> ), ft <sup>3</sup>	Wet test meter (t <sub>w</sub> ), °F	Inlet (t <sub>d,i</sub> ), °F	Dry gas meter Outlet (t <sub>d,o</sub> ), °F				
5.15	10.5	514.442	65	92	70	81	2	997	1.555
10.363	10	515.601	65	89	79	79	4	988	1.515
10.27	10	515.295	65	88	70	81	7	996	1.524
		515.478		88	70	81		Y = .994	1.531

<sup>a</sup> If there is only one thermometer on the dry gas meter, record the temperature under t<sub>d</sub> where

V<sub>w</sub> = Gas volume passing through the wet test meter, ft<sup>3</sup>

V<sub>d</sub> = Gas volume passing through the dry gas meter, ft<sup>3</sup>

t<sub>w</sub> = Temperature of the gas in the wet test meter, °F

t<sub>d,i</sub> = Temperature of the inlet gas of the dry gas meter, °F

t<sub>d,o</sub> = Temperature of the outlet gas of the dry gas meter, °F

t<sub>d</sub> = Average temperature of the gas in the dry gas meter, obtained by the average of t<sub>d,i</sub> and t<sub>d,o</sub>, °F

$\Delta H$  = Pressure differential across orifice, in. H<sub>2</sub>O

Y<sub>i</sub> = Ratio of accuracy of wet test meter to dry gas meter for each run.

Y = Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest Y ± 0.05Y.

P<sub>b</sub> = Barometric pressure, in. Hg.

$\theta$  = Time of calibration run, min.

Macasphalt - NAFA

## RUN # 1 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS. TENNESSEE

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.....
CHAN NAME          HC          SO2          CO2          CO          O2          NOX
CHAN UNITS         PPM          PPM          %            PPM          %            PPM
FULL SCALE         1000.0      1000.0      20.0         500.0        25.0        250.0
ZERO OFFSET        0.0         0.0         0.0          0.0          0.0         0.0
START / CHANNEL    01          02          03          04          05          06
.....

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.....
12/02/92 14:18  54.0  151.5  5.2  52.0  14.2  141.4
12/02/92 14:19  69.0  158.5  5.3  52.0  14.2  137.5
12/02/92 14:20  77.5  150.0  5.0  48.5  14.5  128.9
12/02/92 14:21  77.5  141.5  4.9  48.0  14.8  125.3
12/02/92 14:22  78.5  139.5  5.1  54.0  14.6  130.5
12/02/92 14:23  79.5  145.5  5.3  56.0  14.3  136.9
12/02/92 14:24  85.0  146.5  5.5  62.0  14.2  138.4
12/02/92 14:25  76.5  144.5  5.7  118.5  14.0  136.3
12/02/92 14:26  97.0  141.5  5.4  140.0  14.3  126.6
12/02/92 14:27  91.5  135.0  5.1  140.0  14.7  118.0
12/02/92 14:28  102.5  130.0  5.0  147.5  14.9  114.8
12/02/92 14:29  119.5  126.5  5.0  153.0  15.0  113.3
12/02/92 14:30  121.5  120.5  5.0  166.0  15.0  112.4
12/02/92 14:31  126.0  124.5  5.0  184.5  15.0  113.0
12/02/92 14:32  122.5  131.0  5.1  196.5  14.8  115.0
12/02/92 14:33  102.5  129.0  5.1  170.0  14.9  115.0
12/02/92 14:34  94.5  125.5  5.0  131.0  15.0  116.3
12/02/92 14:35  95.0  125.5  4.9  100.5  15.2  115.5
12/02/92 14:36  89.0  129.0  4.9  79.5  15.2  120.3
12/02/92 14:37  86.5  141.5  5.3  71.5  14.5  131.5
12/02/92 14:38  82.0  151.5  5.7  68.5  14.1  137.9
12/02/92 14:39  71.0  142.5  5.6  57.5  14.2  136.3
12/02/92 14:40  70.0  145.5  5.4  48.0  14.4  129.5
12/02/92 14:41  72.5  146.0  5.8  48.5  14.1  140.9
12/02/92 14:42  75.5  156.0  6.1  52.5  13.7  145.4
12/02/92 14:43  76.0  161.5  6.1  54.5  13.7  143.4
12/02/92 14:44  75.5  168.5  6.1  53.5  13.7  145.3
12/02/92 14:45  74.5  170.0  6.2  55.0  13.6  145.8
12/02/92 14:46  76.5  171.0  6.1  57.5  13.7  144.8
12/02/92 14:47  79.0  163.5  6.0  62.5  13.9  142.0
12/02/92 14:48  78.0  162.5  6.0  66.5  13.9  143.1
12/02/92 14:49  76.0  161.5  6.1  70.0  13.9  143.8
12/02/92 14:50  76.0  162.0  6.1  70.5  13.9  144.4
12/02/92 14:51  75.5  163.0  6.1  68.0  13.8  146.4
12/02/92 14:52  76.5  164.0  6.2  62.0  13.8  148.3
12/02/92 14:53  74.0  165.0  6.2  59.0  13.8  147.3
12/02/92 14:54  70.5  163.5  6.1  55.0  13.9  146.0
12/02/92 14:55  66.5  153.5  5.6  53.5  14.4  134.8
12/02/92 14:56  66.0  151.5  5.5  51.0  14.5  133.9
12/02/92 14:57  62.5  151.5  5.5  50.5  14.4  134.6
12/02/92 14:58  62.0  155.5  5.5  50.5  14.5  134.4
.....

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Macasphalt - NAPA

RUN # 1 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

CHAN NAME		HC	SO2	CO2	CO	O2	NOX
CHAN UNITS		PPM	PPM	%	PPM	%	PPM
FULL SCALE		1000.0	1000.0	20.0	500.0	25.0	250.0
ZERO OFFSET		0.0	0.0	0.0	0.0	0.0	0.0
START / CHANNEL		01	02	03	04	05	06
12/02/92	14:59	64.5	155.0	5.5	50.5	14.6	134.5
12/02/92	15:00	66.0	155.5	5.4	53.0	14.6	134.1
12/02/92	15:01	65.0	154.0	5.6	57.0	14.4	137.1
12/02/92	15:02	67.0	156.5	5.6	58.0	14.4	138.0
12/02/92	15:03	69.0	156.5	5.6	58.0	14.4	136.5
12/02/92	15:04	66.5	154.0	5.6	58.5	14.4	138.5
12/02/92	15:05	68.5	156.0	5.6	55.0	14.5	138.4
12/02/92	15:06	74.0	161.5	5.5	53.0	14.4	138.5
12/02/92	15:07	71.5	161.5	5.5	50.0	14.5	134.6
12/02/92	15:08	70.0	157.5	5.4	46.5	14.6	133.1
12/02/92	15:09	73.0	160.5	5.3	42.0	14.7	128.9
12/02/92	15:10	77.0	151.5	5.3	39.5	14.7	130.0
12/02/92	15:11	76.0	147.0	5.4	38.5	14.7	130.0
12/02/92	15:12	73.0	147.0	5.4	38.5	14.7	129.3
12/02/92	15:13	68.5	143.0	5.4	38.0	14.5	130.9
12/02/92	15:14	70.0	148.5	5.4	36.5	14.6	130.0
12/02/92	15:15	74.5	150.0	5.3	35.5	14.7	128.4
12/02/92	15:16	70.5	147.0	5.3	35.0	14.7	128.5
12/02/92	15:17	59.5	147.5	5.3	34.0	14.7	127.3
12/02/92	15:18	64.5	145.5	5.3	34.0	14.7	128.5
12/02/92	15:19	70.0	145.0	5.3	35.0	14.7	130.0
12/02/92	15:20	68.0	150.5	5.4	38.0	14.6	131.4
12/02/92	15:21	68.5	148.5	5.4	38.5	14.5	130.4
Averages:		77.8	149.5	5.5	68.9	14.4	132.9

Macasphalt - NAPA

## RUN # 2 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

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.....
CHAN NAME          HC          SO2          CO2          CO          O2          NOX
CHAN UNITS         PPM          PPM          %            PPM          %            PPM
FULL SCALE        100.0        400.0        20.0         500.0        25.0        9000.0
ZERO OFFSET       0.0          0.0          0.0          0.0          0.0          0.0
START / CHANNEL   01           02           03           04           05           06
.....

```

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.....
12/03/92 10:25 69.5 137.0 4.0 43.0 14.9 133.3
12/03/92 10:26 68.0 150.0 4.2 52.0 14.7 136.0
12/03/92 10:27 70.0 153.0 4.3 53.0 14.5 136.0
12/03/92 10:28 72.5 153.5 4.4 55.5 14.5 136.6
12/03/92 10:29 73.5 157.0 4.3 62.0 14.6 134.5
12/03/92 10:30 75.0 147.0 4.3 66.0 14.7 132.5
12/03/92 10:31 86.5 143.5 4.4 85.5 14.7 133.4
12/03/92 10:32 95.5 149.0 4.4 95.5 14.6 129.4
12/03/92 10:33 94.5 144.5 4.4 78.0 14.7 130.1
12/03/92 10:34 97.5 141.5 4.4 75.0 14.6 132.8
12/03/92 10:35 102.5 145.0 4.6 88.5 14.5 137.3
12/03/92 10:36 102.0 139.5 4.6 92.5 14.5 137.1
12/03/92 10:37 105.0 139.0 4.6 89.5 14.4 138.6
12/03/92 10:38 96.5 138.0 4.7 77.0 14.4 139.5
12/03/92 10:39 85.0 141.5 4.7 70.0 14.4 141.0
12/03/92 10:40 74.5 142.5 4.7 65.0 14.4 142.1
12/03/92 10:41 96.0 142.5 4.7 59.0 14.3 143.0
12/03/92 10:42 95.0 153.5 4.8 55.0 14.3 143.3
12/03/92 10:43 92.5 154.0 4.7 52.0 14.4 139.6
12/03/92 10:44 85.0 151.5 4.6 51.5 14.5 137.5
12/03/92 10:45 89.5 159.0 4.8 49.5 14.3 143.3
12/03/92 10:46 91.0 161.0 4.9 48.5 14.3 146.3
12/03/92 10:47 93.0 163.5 4.9 53.0 14.2 145.6
12/03/92 10:48 89.0 159.5 4.9 58.0 14.2 145.8
12/03/92 10:49 93.5 164.0 4.9 57.5 14.2 145.4
12/03/92 10:50 95.5 159.5 4.9 60.5 14.3 143.9
12/03/92 10:51 102.0 158.0 4.8 74.5 14.2 142.4
12/03/92 10:52 104.0 158.5 4.8 79.0 14.3 141.1
12/03/92 10:53 96.0 156.5 4.8 74.0 14.3 141.3
12/03/92 10:54 91.0 153.0 4.8 58.5 14.4 141.8
12/03/92 10:55 98.5 155.0 4.8 53.0 14.3 142.8
12/03/92 10:56 101.5 154.5 4.8 55.0 14.3 142.9
12/03/92 10:57 97.5 156.0 4.9 58.5 14.2 145.3
12/03/92 10:58 94.0 155.5 4.9 59.5 14.2 143.3
12/03/92 10:59 90.0 154.5 4.8 58.0 14.4 141.1
12/03/92 11:00 92.5 155.5 4.7 52.5 14.4 138.5
12/03/92 11:01 93.0 152.5 4.7 51.0 14.5 136.6
12/03/92 11:02 93.0 153.5 4.7 55.5 14.5 137.1
12/03/92 11:03 93.5 153.0 4.7 62.5 14.5 136.6
12/03/92 11:04 96.0 153.5 4.7 64.5 14.5 138.3
12/03/92 11:05 91.5 149.0 4.7 53.5 14.5 138.3
.....

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## RUN # 2 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

CHAN NAME		HC	SO2	CO2	CO	O2	NOX
CHAN UNITS		PPM	PPM	%	PPM	%	PPM
FULL SCALE		100.0	400.0	20.0	500.0	25.0	9000.0
ZERO OFFSET		0.0	0.0	0.0	0.0	0.0	0.0
START / CHANNEL		01	02	03	04	05	06
12/03/92	11:06	84.5	149.5	4.7	42.0	14.4	141.1
12/03/92	11:07	84.5	156.0	4.7	36.0	14.4	141.5
12/03/92	11:08	84.0	152.0	4.7	35.5	14.4	141.9
12/03/92	11:09	81.5	152.5	4.7	37.0	14.4	143.0
12/03/92	11:10	85.0	154.0	4.7	34.5	14.5	139.5
12/03/92	11:11	78.5	150.5	4.6	31.0	14.6	141.1
12/03/92	11:12	77.0	152.0	4.7	30.0	14.5	142.1
12/03/92	11:13	73.5	152.0	4.7	30.0	14.4	143.1
12/03/92	11:14	78.5	159.0	4.7	31.0	14.3	143.0
12/03/92	11:15	80.5	161.5	4.7	29.0	14.4	139.4
12/03/92	11:16	72.0	154.0	4.7	27.5	14.5	140.9
12/03/92	11:17	76.5	157.5	4.8	31.5	14.3	146.6
12/03/92	11:18	80.5	164.0	4.9	36.5	14.1	149.8
12/03/92	11:19	75.5	157.5	4.9	38.5	14.1	149.3
12/03/92	11:20	76.5	160.5	4.9	35.0	14.2	147.1
12/03/92	11:21	74.5	158.5	4.8	32.5	14.2	146.6
12/03/92	11:22	72.5	158.0	4.8	30.5	14.3	146.0
12/03/92	11:23	77.5	159.5	4.8	29.5	14.3	146.6
12/03/92	11:24	83.5	160.0	4.8	30.5	14.2	148.3
12/03/92	11:25	90.0	161.0	4.8	37.5	14.3	148.3
12/03/92	11:26	86.0	159.0	4.8	42.0	14.2	149.6
12/03/92	11:27	78.0	150.5	4.8	37.5	14.2	149.6
12/03/92	11:28	80.5	156.5	4.8	33.0	14.2	150.9
12/03/92	11:29	84.5	161.5	4.9	32.5	14.2	150.9
12/03/92	11:30	83.5	162.0	4.9	31.5	14.2	151.3
12/03/92	11:31	83.0	163.0	4.9	31.5	14.1	152.9
12/03/92	11:32	78.0	161.0	5.0	31.5	14.0	152.9
12/03/92	11:33	80.5	166.0	5.0	31.5	14.0	154.3
12/03/92	11:34	82.5	166.5	5.0	30.0	14.0	154.1
12/03/92	11:35	82.5	164.5	4.9	27.0	14.0	153.1
12/03/92	11:36	79.5	162.5	4.9	25.0	14.0	151.5
12/03/92	11:37	75.0	160.5	4.9	26.0	14.1	150.6
12/03/92	11:38	73.5	157.5	4.9	27.0	14.1	150.9
12/03/92	11:39	79.0	161.0	4.9	29.0	14.1	150.5
12/03/92	11:40	84.5	158.0	4.8	30.5	14.1	149.5
12/03/92	11:41	85.5	155.0	4.7	31.5	14.4	144.4
12/03/92	11:42	96.0	151.5	4.6	37.5	14.5	135.9
12/03/92	11:43	104.0	132.0	4.4	88.0	14.8	125.5
12/03/92	11:44	108.5	132.0	4.6	110.0	14.4	136.9
12/03/92	11:45	103.5	135.0	4.7	103.5	14.3	143.6
12/03/92	11:46	92.5	141.0	4.8	83.0	14.2	146.4
12/03/92	11:47	85.0	145.5	4.8	69.0	14.1	149.9
12/03/92	11:48	79.0	149.5	4.8	61.0	14.1	151.1
12/03/92	11:49	70.0	150.5	4.8	43.5	14.1	151.1

## RUN # 2 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

CHAN NAME		HC	SO2	CO2	CO	O2	NOX
CHAN UNITS		PPM	PPM	%	PPM	%	PPM
FULL SCALE		100.0	400.0	20.0	500.0	25.0	9000.0
ZERO OFFSET		0.0	0.0	0.0	0.0	0.0	0.0
START / CHANNEL		01	02	03	04	05	06
12/03/92	11:50	71.5	153.5	4.8	28.5	14.1	152.0
12/03/92	11:51	72.0	156.0	4.8	24.0	14.1	154.0
12/03/92	11:52	73.0	160.0	4.8	23.0	14.1	153.0
12/03/92	11:53	71.0	162.5	4.8	23.0	14.1	152.4
12/03/92	11:54	69.0	159.5	4.7	21.0	14.2	151.8
12/03/92	11:55	72.0	161.5	4.7	19.5	14.3	151.4
12/03/92	11:56	76.5	162.5	4.7	16.5	14.2	151.5
12/03/92	11:57	73.0	160.5	4.7	16.0	14.2	151.9
12/03/92	11:58	71.0	162.0	4.6	17.5	14.3	151.8
12/03/92	11:59	70.5	158.0	4.6	17.5	14.4	150.5
12/03/92	12:00	73.0	159.0	4.5	18.0	14.4	149.5
12/03/92	12:01	72.0	159.5	4.6	17.5	14.4	151.3
12/03/92	12:02	70.0	160.0	4.6	17.0	14.3	152.1
12/03/92	12:03	68.5	163.5	4.6	16.5	14.3	151.6
12/03/92	12:04	67.0	161.0	4.6	15.0	14.3	151.5
12/03/92	12:05	67.0	161.5	4.6	13.5	14.2	152.4
12/03/92	12:06	71.5	162.5	4.6	12.5	14.2	152.3
12/03/92	12:07	68.0	156.5	4.6	13.0	14.3	151.0
12/03/92	12:08	49.5	149.5	4.6	12.5	14.2	150.8
12/03/92	12:09	38.5	147.5	4.6	12.5	14.3	152.4
12/03/92	12:10	51.5	143.0	4.6	14.0	14.2	146.5
12/03/92	12:11	63.0	115.5	3.5	24.0	15.8	103.1
12/03/92	12:12	66.0	86.5	3.2	70.5	16.2	118.9
12/03/92	12:13	68.5	109.0	4.4	42.0	14.6	141.0
12/03/92	12:14	69.0	122.5	4.4	47.0	14.4	145.1
12/03/92	12:15	65.5	121.5	4.5	46.5	14.3	147.3
12/03/92	12:16	62.5	115.5	4.5	38.0	14.4	145.6
12/03/92	12:17	62.0	113.5	4.4	29.0	14.5	145.8
12/03/92	12:18	66.5	116.0	4.4	29.0	14.4	144.5
12/03/92	12:19	69.5	118.5	4.4	40.0	14.5	140.3
12/03/92	12:20	68.5	120.0	4.3	43.5	14.7	132.0
12/03/92	12:21	67.5	101.5	3.0	50.5	16.2	98.3
12/03/92	12:22	71.5	97.5	4.0	44.5	15.1	137.9
Averages:		81.0	150.0	4.6	44.3	14.4	143.6







Macasphalt - NAPA

## RUN # 3B DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

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.....
CHAN NAME          HC          SO2          CO2          CO          O2          NOX
CHAN UNITS         PPM          PPM          %            PPM          %            PPM
FULL SCALE         100.0        400.0        20.0         500.0        25.0        9000.0
ZERO OFFSET        0.0          0.0          0.0          0.0          0.0          0.0
START / CHANNEL    01           02           03           04           05           06
.....
12/03/92  15:40  63.0  114.0  3.0  57.0  16.7  77.4
12/03/92  15:41  51.0  74.5  2.3  231.5  17.5  89.4
12/03/92  15:42  59.5  106.0  3.9  44.5  15.5  128.1
12/03/92  15:43  53.0  126.5  4.2  39.0  15.1  131.9
12/03/92  15:44  45.0  130.0  4.2  38.0  15.0  133.0
12/03/92  15:45  47.5  133.5  4.3  40.5  15.0  133.1
12/03/92  15:46  52.5  135.5  4.3  46.5  15.0  133.5
12/03/92  15:47  39.5  140.5  4.3  48.0  14.9  133.9
12/03/92  15:48  66.5  141.5  4.4  46.5  14.7  139.1
12/03/92  15:49  64.0  156.0  4.5  42.0  14.7  133.6
12/03/92  15:50  68.5  135.0  3.5  42.5  15.9  105.5
12/03/92  15:51  77.5  136.5  4.0  50.0  15.3  129.9
12/03/92  15:52  76.0  156.0  4.4  42.0  14.8  137.5
12/03/92  15:53  83.5  160.5  4.3  44.0  15.0  126.3
12/03/92  15:54  76.5  143.5  3.8  41.0  15.6  111.5
12/03/92  15:55  74.0  129.0  3.6  53.0  15.8  121.9
12/03/92  15:56  73.5  156.0  4.4  54.5  14.8  136.0
12/03/92  15:57  79.0  164.5  4.4  53.5  14.9  132.4
12/03/92  15:58  63.0  127.0  3.0  79.0  16.6  88.6
12/03/92  15:59  66.0  129.0  3.8  80.0  15.5  129.1
12/03/92  16:00  65.5  144.0  4.3  38.0  15.0  131.3
12/03/92  16:01  61.5  142.0  4.2  32.5  15.1  129.0
12/03/92  16:02  60.0  143.0  4.3  33.5  14.9  133.1
12/03/92  16:03  57.0  137.5  4.2  37.5  15.0  132.3
12/03/92  16:04  57.5  138.5  4.3  37.5  15.0  133.8
12/03/92  16:05  60.5  141.5  4.4  37.0  14.9  134.0
12/03/92  16:06  58.0  135.5  4.3  38.5  15.0  131.1
12/03/92  16:07  54.0  143.0  4.4  37.5  14.9  131.4
12/03/92  16:08  56.0  147.0  4.3  34.0  15.0  127.1
12/03/92  16:09  66.0  140.5  4.2  31.5  15.1  122.8
12/03/92  16:10  68.5  117.5  3.2  54.5  16.3  87.0
12/03/92  16:11  66.0  104.5  3.6  119.0  15.9  121.5
12/03/92  16:12  71.5  139.5  4.4  35.5  14.8  133.8
12/03/92  16:13  72.5  146.0  4.4  35.0  14.7  132.5
12/03/92  16:14  68.0  141.5  4.2  32.5  15.1  123.4
12/03/92  16:15  79.0  140.0  4.2  39.5  15.2  123.0
12/03/92  16:16  92.5  139.5  4.4  76.5  14.9  122.3
12/03/92  16:17  95.0  133.0  4.3  105.0  15.0  117.5
12/03/92  16:18  92.0  133.0  4.2  99.0  15.1  115.9
12/03/92  16:19  85.0  128.5  4.1  89.0  15.2  113.1
12/03/92  16:20  79.0  124.5  4.0  78.0  15.4  110.1
12/03/92  16:21  79.0  119.0  3.5  65.5  15.9  103.3
12/03/92  16:22  74.0  117.5  4.1  61.5  15.3  118.4
12/03/92  16:23  77.0  139.0  4.4  54.5  14.8  125.4

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## RUN # 35 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

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.....
CHAN NAME          HC          SO2          CO2          CO          O2          NOX
CHAN UNITS         PPM          PPM          %            PPM          %            PPM
FULL SCALE         100.0        400.0        20.0         500.0        25.0         9000.0
ZERO OFFSET        0.0          0.0          0.0          0.0          0.0          0.0
START / CHANNEL    01           02           03           04           05           06
.....

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12/03/92 16:24 78.5 133.5 4.5 51.0 14.8 127.0
12/03/92 16:25 72.0 132.0 4.4 54.0 15.0 125.4
12/03/92 16:26 68.0 127.5 4.4 51.0 15.0 126.6
12/03/92 16:27 65.0 127.5 4.4 48.5 15.0 126.4
12/03/92 16:28 60.5 124.0 4.4 48.0 15.0 125.1
12/03/92 16:29 61.0 128.0 4.5 44.5 14.8 130.1
12/03/92 16:30 59.0 129.0 4.5 47.0 14.8 130.3
12/03/92 16:31 63.5 133.5 4.5 50.0 14.8 129.5
12/03/92 16:32 64.5 132.0 4.5 53.0 14.8 128.9
12/03/92 16:33 66.0 134.5 4.5 54.0 14.7 129.6
12/03/92 16:34 64.0 134.5 4.6 53.5 14.7 130.4
12/03/92 16:35 61.5 132.0 4.6 52.5 14.6 130.9
12/03/92 16:36 63.5 134.0 4.7 55.0 14.6 130.6
12/03/92 16:37 66.0 135.5 4.7 60.0 14.6 130.4
12/03/92 16:38 63.0 131.0 4.7 61.5 14.6 130.6

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Averages:          62.8 132.8 4.2 52.5 15.1 127.3

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Macasphalt - NAPA

RUN # 4B DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

CHAN NAME		HC	SO2	CO2	CO	O2	NOX
CHAN UNITS		PPM	PPM	%	PPM	%	PPM
FULL SCALE		100.0	400.0	20.0	500.0	25.0	9000.0
ZERO OFFSET		0.0	0.0	0.0	0.0	0.0	0.0
START / CHANNEL		01	02	03	04	05	06
12/04/92	10:36	29.5	115.0	3.5	104.0	15.9	142.6
12/04/92	10:37	28.0	162.5	3.8	45.5	15.4	147.6
12/04/92	10:38	30.5	157.0	3.6	39.0	15.8	130.3
12/04/92	10:39	49.5	125.5	3.0	55.5	16.6	126.9
12/04/92	10:40	63.0	149.5	4.1	37.0	15.3	155.8
12/04/92	10:41	70.5	166.5	4.4	39.0	14.9	161.9
12/04/92	10:42	63.0	171.0	4.5	36.5	14.8	162.5
12/04/92	10:43	64.5	170.0	4.5	31.0	14.9	160.6
12/04/92	10:44	65.5	167.5	4.5	29.0	14.8	161.4
12/04/92	10:45	69.0	162.0	4.6	28.5	14.8	164.0
12/04/92	10:46	94.5	146.0	4.6	34.0	14.8	156.5
12/04/92	10:47	130.0	127.0	4.6	98.0	14.9	144.0
12/04/92	10:48	131.5	119.5	4.6	181.0	14.9	137.0
12/04/92	10:49	115.5	122.5	4.5	197.0	15.1	134.4
12/04/92	10:50	103.0	122.0	4.4	153.5	15.2	137.9
12/04/92	10:51	106.5	124.0	4.7	122.5	14.8	150.8
12/04/92	10:52	130.0	128.0	4.7	120.5	14.8	146.3
12/04/92	10:53	144.0	131.5	4.7	180.0	14.8	137.1
12/04/92	10:54	141.0	130.5	4.6	233.0	14.9	130.9
12/04/92	10:55	133.0	120.0	4.4	211.5	15.3	126.0
12/04/92	10:56	127.0	115.0	4.2	170.0	15.5	127.4
12/04/92	10:57	118.0	118.0	4.3	150.0	15.4	130.6
12/04/92	10:58	111.0	123.5	4.3	129.0	15.4	134.6
12/04/92	10:59	108.0	128.0	4.4	105.5	15.3	140.0
12/04/92	11:00	99.0	132.5	4.5	83.5	15.1	145.4
12/04/92	11:01	103.0	140.0	4.6	74.5	15.0	148.3
12/04/92	11:02	113.0	140.5	4.7	91.0	14.9	147.3
12/04/92	11:03	118.5	141.5	4.8	113.5	14.7	148.6
12/04/92	11:04	111.5	141.5	4.9	116.0	14.6	150.4
12/04/92	11:05	111.0	142.0	4.9	107.0	14.6	150.6
12/04/92	11:06	112.5	138.0	4.9	112.0	14.5	150.5
12/04/92	11:07	112.5	135.5	5.0	117.0	14.5	151.3
12/04/92	11:08	106.5	138.5	5.0	112.0	14.5	151.9
12/04/92	11:09	103.0F	142.5F	5.0F	107.0F	14.5F	150.8F
12/04/92	11:10	101.0	144.5	4.9	101.5	14.6	150.4
12/04/92	11:11	99.0	142.5	4.7	86.0	14.8	145.5
12/04/92	11:12	91.5	140.0	4.4	66.5	15.2	140.3
12/04/92	11:13	88.0	142.0	4.4	56.5	15.3	140.9
12/04/92	11:14	94.0	145.0	4.6	60.5	15.0	146.6
12/04/92	11:15	95.0	148.5	4.8	67.5	14.8	152.9
12/04/92	11:16	86.0	148.0	4.7	61.5	14.8	154.8

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Macasphalt - NAPA

## RUN # 4B DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

CHAN NAME	HC	SO2	CO2	CO	O2	NOX
CHAN UNITS	PPM	PPM	%	PPM	%	PPM
FULL SCALE	100.0	400.0	20.0	500.0	25.0	9000.0
ZERO OFFSET	0.0	0.0	0.0	0.0	0.0	0.0
START / CHANNEL	01	02	03	04	05	06
12/04/92 11:17	79.5	148.5	4.8	54.0	14.7	155.4
12/04/92 11:18	76.0	149.0	4.8	53.5	14.6	156.9
12/04/92 11:19	77.5	148.5	4.8	52.5	14.7	156.1
12/04/92 11:20	77.5	145.5	4.8	51.5	14.6	156.9
12/04/92 11:21	78.0	144.5	4.8	52.0	14.6	156.6
12/04/92 11:22	76.0	142.5	4.8	51.0	14.6	156.8
12/04/92 11:23	73.5	143.0	4.8	49.0	14.7	157.4
12/04/92 11:24	73.0	143.0	4.8	45.0	14.7	155.5
12/04/92 11:25	69.5	141.0	4.8	43.5	14.8	154.0
12/04/92 11:26	69.5	144.0	4.7	42.5	14.8	153.9
12/04/92 11:27	71.0	142.5	4.7	42.0	14.8	154.5
12/04/92 11:28	69.0	142.0	4.8	43.5	14.7	155.4
12/04/92 11:29	68.0	142.5	4.8	40.0	14.7	156.3
12/04/92 11:30	66.0	144.5	4.8	36.5	14.7	156.8
12/04/92 11:31	65.0	146.0	4.8	35.0	14.7	156.3
12/04/92 11:32	54.5	154.5	4.8	34.0	14.7	153.5
12/04/92 11:33	37.0	102.0	2.5	19.5	18.0	62.6
12/04/92 11:34	36.0	49.0	1.6	7.0	19.3	56.1
12/04/92 11:35	35.5	36.0	1.6	10.0	19.3	56.0
12/04/92 11:36	36.0	29.5	1.6	14.5	19.3	54.4
12/04/92 11:37	72.0	49.5	2.7	27.5	17.4	116.3
12/04/92 11:38	71.0	107.0	4.4	63.5	15.0	146.4
12/04/92 11:39	68.5	124.0	4.5	57.0	14.8	150.9
12/04/92 11:40	66.5	130.5	4.5	50.0	14.8	152.5
12/04/92 11:41	66.5	133.5	4.6	46.5	14.8	153.0
12/04/92 11:42	64.5	133.5	4.6	47.5	14.7	153.5
12/04/92 11:43	65.0	134.5	4.7	47.0	14.7	154.3
12/04/92 11:44	66.5	137.0	4.7	44.5	14.7	155.3
12/04/92 11:45	67.5	136.0	4.7	45.5	14.7	154.6
12/04/92 11:46	78.5	127.0	4.7	60.5	14.7	150.5
12/04/92 11:47	88.0	118.0	4.7	94.0	14.7	145.8
12/04/92 11:48	95.5	113.5	4.7	123.0	14.7	143.8
12/04/92 11:49	96.5	115.5	4.7	141.0	14.7	144.6
12/04/92 11:50	93.0	118.0	4.7	135.0	14.7	147.1
Averages:	84.2	130.4	4.3	76.2	15.0	141.5





## RUN # 5 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

CHAN NAME		HC	SO2	CO2	CO	O2	NOX
CHAN UNITS		PPM	PPM	%	PPM	%	PPM
FULL SCALE		100.0	400.0	20.0	500.0	25.0	9000.0
ZERO OFFSET		0.0	0.0	0.0	0.0	0.0	0.0
START / CHANNEL		01	02	03	04	05	06
12/04/92	13:01	69.5	148.5	4.8	40.0	15.1	131.8
12/04/92	13:02	66.0	147.0	4.8	36.5	15.1	131.8
12/04/92	13:03	65.0	149.5	4.8	34.0	15.1	131.6
12/04/92	13:04	68.0	149.5	4.8	33.5	15.2	131.1
12/04/92	13:05	68.0	151.5	4.7	33.5	15.2	131.1
12/04/92	13:06	67.5	153.0	4.8	33.0	15.2	131.3
12/04/92	13:07	67.5	155.5	4.8	33.0	15.1	131.9
12/04/92	13:08	64.5	154.0	4.8	33.0	15.1	132.1
12/04/92	13:09	61.0	158.0	4.8	33.0	15.1	132.0
12/04/92	13:10	57.5	157.0	4.8	33.0	15.0	132.8
12/04/92	13:11	57.0	155.0	4.8	33.0	15.1	133.1
12/04/92	13:12	58.5	152.5	4.8	33.0	15.1	132.8
12/04/92	13:13	57.5	153.5	4.8	34.5	15.1	132.1
12/04/92	13:14	59.5	152.0	4.7	38.5	15.2	131.1
12/04/92	13:15	58.0	150.0	4.7	41.0	15.1	131.6
12/04/92	13:16	58.0	151.0	4.8	42.0	15.1	132.4
12/04/92	13:17	60.0	150.5	4.8	41.5	15.1	132.5
12/04/92	13:18	63.0	155.0	4.8	41.0	15.1	132.5
12/04/92	13:19	64.0	155.5	4.8	40.5	15.1	133.0
12/04/92	13:20	63.5	153.5	4.8	38.5	15.1	134.0
12/04/92	13:21	67.0	152.0	4.8	41.0	15.0	133.8
12/04/92	13:22	72.5	151.0	4.8	48.0	15.0	132.9
12/04/92	13:23	75.5	149.5	4.8	57.5	15.0	132.6
12/04/92	13:24	77.5	149.5	4.8	57.5	15.0	133.4
12/04/92	13:25	76.5	147.0	4.8	53.0	15.1	134.0
12/04/92	13:26	73.5	149.5	4.8	47.0	15.1	134.5
12/04/92	13:27	74.5	153.5	4.8	44.0	15.1	135.1
12/04/92	13:28	105.0	147.0	4.8	54.5	15.0	130.3
12/04/92	13:29	168.5	142.5	4.8	182.5	15.0	116.0
12/04/92	13:30	210.0	147.5	4.9	434.0	14.9	109.4
12/04/92	13:31	202.0	152.0	5.0	536.0	14.8	112.6
12/04/92	13:32	176.0	149.5	5.0	474.5	14.7	120.8
12/04/92	13:33	162.5	143.5	5.1	356.0	14.7	129.0
12/04/92	13:34	235.0	145.0	5.0	352.5	14.7	118.4
12/04/92	13:35	297.0	155.5	5.0	646.5	14.7	108.4
12/04/92	13:36	277.0	161.0	5.1	793.5	14.6	111.5
12/04/92	13:37	222.5	159.0	5.0	647.5	14.7	118.6
12/04/92	13:38	180.0	147.0	5.0	452.0	14.8	123.9
12/04/92	13:39	168.5	137.5	4.8	313.0	15.0	123.9
12/04/92	13:40	191.0	138.0	4.9	312.5	14.9	123.9
12/04/92	13:41	171.0	142.5	5.0	411.5	14.7	124.9

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

```

    .....
    CHAN NAME          HC      SO2      CO2      CO      O2      NOX
    CHAN UNITS          PPM      PPM      %        PPM      %        PPM
    FULL SCALE          100.0    400.0    20.0     500.0    25.0    9000.0
    ZERO OFFSET         0.0      0.0      0.0      0.0      0.0      0.0
    START / CHANNEL     01       02       03       04       05       06
    .....
    12/04/92  13:42  143.0  141.5    5.0  397.5    14.7  128.5
    12/04/92  13:43  123.0  139.0    5.1  311.0    14.7  134.6
    12/04/92  13:44  101.0  140.5    5.1  209.0    14.7  137.4
    12/04/92  13:45  107.5  145.0    5.0  192.0    14.7  134.1
    12/04/92  13:46  111.0  145.5    5.0  222.5    14.7  132.6
    12/04/92  13:47  109.0  143.5    4.9  192.0    14.9  133.5
    12/04/92  13:48  109.5  145.5    4.9  153.0    14.8  135.0
    12/04/92  13:49   81.0  143.5    4.9  139.0    14.8  135.5
    12/04/92  13:50   84.0  139.0    4.9  130.0    14.9  136.1
    12/04/92  13:51  127.5  137.0    4.9  164.5    14.8  131.0
    12/04/92  13:52  126.5  125.5    4.3  262.0    15.6  110.4
    12/04/92  13:53  148.0  135.5    4.8  310.5    14.9  124.9
    12/04/92  13:54  118.0  137.0    4.8  263.5    15.0  125.8
    12/04/92  13:55   96.0  132.0    4.6  202.0    15.2  122.1
    12/04/92  13:56  100.5  128.0    4.7  167.0    15.1  127.9
    12/04/92  13:57   93.5  131.5    4.9  160.5    14.9  132.3
    12/04/92  13:58   97.0  133.0    5.0  180.0    14.7  134.8
    12/04/92  13:59  130.0  128.5    5.0  191.0    14.7  131.3
    12/04/92  14:00  190.0  130.0    5.0  349.0    14.7  118.6
    12/04/92  14:01  210.0  133.0    5.0  563.5    14.6  114.8
    12/04/92  14:02  193.0  131.0    5.0  567.5    14.7  117.8
    Averages:          96.5  146.1    4.8  138.4    15.0  128.1
    
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## Macasphalt - NAPA

## RUN # 6 DATA LISTING

NAME: RAMCON ENVIRONMENTAL LOCATION: MEMPHIS, TENNESSEE

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:.....:
CHAN NAME          HC          SO2          CO2          CO          O2          NOX
CHAN UNITS         PPM          PPM          %            PPM          %            PPM
FULL SCALE         100.0        400.0        20.0         500.0        25.0        9000.0
ZERO OFFSET        0.0          0.0          0.0          0.0          0.0          0.0
START / CHANNEL    01           02           03           04           05           06
:.....:

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12/04/92  14:50  147.5  130.5  3.6  231.5  16.2  93.1
12/04/92  14:51  146.0  150.0  4.2  222.5  15.4  104.5
12/04/92  14:52  145.5  145.5  4.2  160.0  15.5  105.4
12/04/92  14:53  138.0  143.5  4.4  183.5  15.3  106.8
12/04/92  14:54  127.0  144.5  4.5  212.0  15.3  109.5
12/04/92  14:55  113.5  145.0  4.6  185.5  15.2  113.5
12/04/92  14:56  100.0  144.0  4.7  158.5  15.1  117.3
12/04/92  14:57  89.5   143.5  4.6  129.5  15.1  115.9
12/04/92  14:58  91.0   142.5  4.5  112.0  15.4  112.0
12/04/92  14:59  93.5   145.0  4.5  124.0  15.4  111.0
12/04/92  15:00  93.0   143.0  4.6  135.0  15.4  111.8
12/04/92  15:01  95.0   146.0  4.6  136.0  15.3  111.9
12/04/92  15:02  99.0   146.5  4.7  136.5  15.3  112.4
12/04/92  15:03  105.5  144.5  4.7  145.0  15.3  111.3
12/04/92  15:04  109.5  141.5  4.7  157.5  15.3  110.4
12/04/92  15:05  116.5  140.5  4.7  176.0  15.2  108.9
12/04/92  15:06  123.0  140.5  4.8  199.0  15.2  108.4
12/04/92  15:07  136.0  140.5  4.8  211.5  15.2  107.1
12/04/92  15:08  165.5  140.5  4.8  277.0  15.1  99.8
12/04/92  15:09  178.5  139.5  4.9  378.0  15.0  101.9
12/04/92  15:10  196.0  141.0  5.0  419.0  15.0  100.3
12/04/92  15:11  190.0  138.5  4.9  455.5  15.1  101.1
12/04/92  15:12  169.5  133.5  4.9  405.0  15.2  99.8
12/04/92  15:13  148.5  127.0  4.7  324.5  15.3  100.8
12/04/92  15:14  130.0  121.0  4.7  257.0  15.4  102.4
12/04/92  15:15  120.5  121.5  4.6  194.5  15.5  104.6
12/04/92  15:16  118.5  122.0  4.6  161.0  15.5  106.1
12/04/92  15:17  128.5  121.0  4.6  157.0  15.5  106.1
12/04/92  15:18  144.5  125.0  4.7  212.0  15.2  104.0
12/04/92  15:19  143.5  128.5  4.9  268.0  15.1  106.3
12/04/92  15:20  137.5  129.0  4.9  254.5  15.1  108.4
12/04/92  15:21  138.0  124.5  4.9  232.5  15.1  107.5
12/04/92  15:22  139.5  121.0  4.9  242.5  15.1  104.4
12/04/92  15:23  138.5  119.5  4.9  255.5  15.2  104.1
12/04/92  15:24  132.0  124.0  4.9  246.5  15.2  105.4
12/04/92  15:25  124.0  122.5  4.8  223.0  15.2  106.3
12/04/92  15:26  119.5  123.5  4.8  202.5  15.3  107.8
12/04/92  15:27  117.0  123.0  4.8  185.5  15.2  108.8
12/04/92  15:28  115.0  120.0  4.8  176.0  15.2  110.8
12/04/92  15:29  108.5  116.5  4.8  160.5  15.2  113.3
12/04/92  15:30  100.0  123.0  4.8  138.5  15.2  115.6

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**IX. FIELD DATA**

**B. GAS CHROMATOGRAPHY**

Plant MACASPHALT Date 12-2-92

Location MELBOURNE FL.

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	
Probe temp. (°C)	_____	Initial (°C)/time (min)	<u>75C</u>
Ambient temp. (°C)	_____	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	<u>75C</u>
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	<u>40 ml/min</u>
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	<u>600 lpm</u>	Injection time (24-hr basis)	_____
Sample loop volume (ml)	<u>1ml</u>	Chart speed (mm/min)	<u>NA</u>
Sample loop temp. (°C)	<u>75C</u>	Dilution ratio	<u>NA</u>
Dilution gas flow rate (ml/min)	<u>-</u>	Dilution gas used (symbol)	<u>NA</u>

2. Field Analysis Data:

Run # 1 Time 1<sup>st</sup> CONDENSABLES

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>INT 1</u>	<u>METHANE</u>	<u>26.01</u>	<u>32</u>	<u>-</u>	<u>17.027</u>
<u>2</u>	<u>METHANE</u>	<u>19.89</u>	<u>32</u>	<u>-</u>	<u>13.022</u>
<u>3</u>	<u>METHANE</u>	<u>6.39</u>	<u>32</u>	<u>-</u>	<u>4.187</u>
<u>4</u>	<u>METHANE</u>	<u>7.18</u>	<u>32</u>	<u>-</u>	<u>4.704</u>
<u>5</u>	<u>METHANE</u>	<u>6.46</u>	<u>32</u>	<u>-</u>	<u>4.233</u>

Run # 1 Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>6</u>	<u>METHANE</u>	<u>4.85</u>	<u>32</u>	<u>-</u>	<u>3.180</u>
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____

Run # \_\_\_\_\_ Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____

Plant MACAS PHALT Date 12-3-92  
 Location MELBOURNE FL

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	
Probe temp. (°C)	_____	Initial (°C)/time (min)	<u>75C</u>
Ambient temp. (°C)	_____	Program rate (°C/min)	<u>=</u>
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	<u>75C</u>
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	<u>40 ml/min</u>
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	<u>600 l/m</u>	Injection time (24-hr basis)	_____
Sample loop volume (ml)	<u>1 ml</u>	Chart speed (mm/min)	<u>NA</u>
Sample loop temp. (°C)	<u>75C</u>	Dilution ratio	<u>NA</u>
Dilution gas flow rate (ml/min)	<u>-</u>	Dilution gas used (symbol)	<u>NA</u>

2. Field Analysis Data: 1<sup>st</sup> PAH

Run # 1 Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>INT 1</u>	<u>METHANE</u>	<u>7.61</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>2</u>	<u>METHANE</u>	<u>17.29</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>3</u>	<u>METHANE</u>	<u>8.74</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>4</u>	<u>METHANE</u>	<u>4.33</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>5</u>	<u>METHANE</u>	<u>10.34</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>

Run # 1 Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>6</u>	<u>METHANE</u>	<u>7.68</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>7</u>	<u>METHANE</u>	<u>7.51</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>8</u>	<u>METHANE</u>	<u>5.72</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>9</u>	<u>METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>10</u>	<u>METHANE</u>	<u>8.78</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>

Run # 1 Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>11</u>	<u>METHANE</u>	<u>6.84</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>12</u>	<u>METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>13</u>	<u>METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>14</u>	<u>METHANE</u>	<u>7.76</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>15</u>	<u>METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>

Plant MACASphalt Date 12-3-92

Location MELBOURNE FL

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	
Probe temp. (°C)	_____	Initial (°C)/time (min)	<u>75 C</u>
Ambient temp. (°C)	_____	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	<u>75 C</u>
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	<u>40 cc/min</u>
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	<u>.400 L/m</u>	Injection time (24-hr basis)	_____
Sample loop volume (ml)	<u>1 ml</u>	Chart speed (mm/min)	<u>NA</u>
Sample loop temp. (°C)	<u>75 C</u>	Dilution ratio	<u>NA</u>
Dilution gas flow rate (ml/min)	<u>-</u>	Dilution gas used (symbol)	<u>NA</u>

2. Field Analysis Data: 2<sup>nd</sup> CONDENSABLES + PAH

Run # 2 Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>INT 1 METHANE</u>	<u>8.25</u>	<u>32</u>	<u>-</u>	<u>BTDL 1.65</u>
<u>2 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>3 METHANE</u>	<u>6.18</u>	<u>32</u>	<u>-</u>	<u>BTDL 1.24</u>
<u>4 METHANE</u>	<u>6.27</u>	<u>32</u>	<u>-</u>	<u>BTDL 1.26</u>
<u>5 METHANE</u>	<u>30.50</u>	<u>32</u>	<u>-</u>	<u>6.135</u>

Run # \_\_\_\_\_ Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>6 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>7 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>8 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>9 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>10 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>

Run # \_\_\_\_\_ Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>11 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>12 METHANE</u>	<u>12.78</u>	<u>32</u>	<u>-</u>	<u>BTDL 2.57</u>
<u>13 METHANE</u>	<u>5.23</u>	<u>32</u>	<u>-</u>	<u>BTDL 1.05</u>
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____



FIELD ANALYSIS DATA SHEETS

Plant MACASPIHART Date 12-4-92 216  
 Location MELBOURNE FL.

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	
Probe temp. (°C)	_____	Initial (°C)/time (min)	<u>75C</u>
Ambient temp. (°C)	_____	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	<u>75C</u>
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	<u>40ml/min</u>
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	<u>1.600ml/min</u>	Injection time (24-hr basis)	_____
Sample loop volume (ml)	<u>1ml</u>	Chart speed (mm/min)	<u>NA</u>
Sample loop temp. (°C)	<u>75C</u>	Dilution ratio	<u>NA</u>
Dilution gas flow rate (ml/min)	<u>-</u>	Dilution gas used (symbol)	<u>NA</u>

2. Field Analysis Data: 3<sup>rd</sup> CONDENSABLES + PAH

Run # 3 Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>1M</u> 1 METHANE	<u>16.68</u>	<u>32</u>	<u>-</u>	<u>14.487</u>
2 METHANE	<u>17.26</u>	<u>32</u>	<u>-</u>	<u>14.820</u>
3 METHANE	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
4 METHANE	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
5 METHANE	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>

Run # 3 Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
6 METHANE	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
7 METHANE	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
8 METHANE	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
9 METHANE	<u>14.24</u>	<u>32</u>	<u>-</u>	<u>13.084</u>
10 METHANE	<u>21.41</u>	<u>32</u>	<u>-</u>	<u>17.206</u>

Run # 3 Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
11 METHANE	<u>17.41</u>	<u>32</u>	<u>-</u>	<u>14.907</u>
12 METHANE	<u>17.67</u>	<u>32</u>	<u>-</u>	<u>16.189</u>
13 METHANE	<u>9.03</u>	<u>32</u>	<u>-</u>	<u>10.089</u>
14 METHANE	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
15 METHANE	<u>8.90</u>	<u>32</u>	<u>-</u>	<u>10.015</u>

FIELD ANALYSIS DATA SHEETS

Plant MACASPHALT Date 12-4-92 217

Location MELBOURNE FL.

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	
Probe temp. (°C)	_____	Initial (°C)/time (min)	<u>75C</u>
Ambient temp. (°C)	_____	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	<u>75C</u>
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	<u>40 ml/min</u>
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	<u>.600 ml/min</u>	Injection time (24-hr basis)	_____
Sample loop volume (ml)	<u>1 ml</u>	Chart speed (mm/min)	<u>NA</u>
Sample loop temp. (°C)	<u>75C</u>	Dilution ratio	<u>NA</u>
Dilution gas flow rate (ml/min)	<u>-</u>	Dilution gas used (symbol)	<u>NA</u>

2. Field Analysis Data: 1<sup>st</sup> FORMALDEHYDE

Run # 1 Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>INS 1. METHANE</u>	<u>8.75</u>	<u>32</u>	<u>-</u>	<u>10.043</u>
<u>2 METHANE</u>	<u>8.90</u>	<u>32</u>	<u>-</u>	<u>10.051</u>
<u>3 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>4 METHANE</u>	<u>9.76</u>	<u>32</u>	<u>-</u>	<u>10.336</u>
<u>5 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>

Run # 1 Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>6 METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

Run # \_\_\_\_\_ Time \_\_\_\_\_

Components	Area	Attenuation	A x A Factor	Concentration (ppm)
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____
_____	_____	_____	_____	_____

Plant MACASPIHALT Date 12-4-92 218

Location MELBOURNE FL

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	
Probe temp. (°C)	_____	Initial (°C)/time (min)	<u>75C</u>
Ambient temp. (°C)	_____	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	<u>75C</u>
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	<u>40 ml/min</u>
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	<u>6.00 ml/min</u>	Injection time (24-hr basis)	_____
Sample loop volume (ml)	<u>1ul</u>	Chart speed (mm/min)	<u>NA</u>
Sample loop temp. (°C)	<u>75C</u>	Dilution ratio	<u>NA</u>
Dilution gas flow rate (ml/min)	<u>-</u>	Dilution gas used (symbol)	<u>NA</u>

2. Field Analysis Data: 2<sup>nd</sup> FORMALDEHYDE

Run # 2 Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>INS 1</u>	<u>METHANE</u>	<u>7.38</u>	<u>32</u>	<u>-</u>	<u>9.141</u>
<u>2</u>	<u>METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>3</u>	<u>METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTDL</u>
<u>4</u>	<u>METHANE</u>	<u>7.18</u>	<u>32</u>	<u>-</u>	<u>9.026</u>
<u>5</u>	<u>METHANE</u>	<u>21.36</u>	<u>32</u>	<u>-</u>	<u>17.177</u>

Run # 2 Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
<u>6</u>	<u>METHANE</u>	<u>105.38</u>	<u>32</u>	<u>-</u>	<u>65.478</u>
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____

Run # \_\_\_\_\_ Time \_\_\_\_\_

	<u>Components</u>	<u>Area</u>	<u>Attenuation</u>	<u>A x A Factor</u>	<u>Concentration (ppm)</u>
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____
	_____	_____	_____	_____	_____

FIELD ANALYSIS DATA SHEETS

Plant MACASPIHART Date 12-4-92 219

Location MELBOURNE FL

1. General Information:

Source temp. (°C)	_____	Columnar temperature:	
Probe temp. (°C)	_____	Initial (°C)/time (min)	<u>75C</u>
Ambient temp. (°C)	_____	Program rate (°C/min)	<u>-</u>
Atmospheric press. (in. Hg)	_____	Final (°C)/time (min)	<u>75C</u>
Source press. (in. Hg)	_____	Carrier gas flow rate (ml/min)	<u>40 ml/min</u>
Absolute source press. (mm)	_____	Detector temperature (°C)	_____
Sampling rate (liter/min)	<u>.600 ml/min</u>	Injection time (24-hr basis)	_____
Sample loop volume (ml)	<u>1 ml</u>	Chart speed (mm/min)	<u>NA</u>
Sample loop temp. (°C)	<u>75C</u>	Dilution ratio	<u>NA</u>
Dilution gas flow rate (ml/min)	<u>-</u>	Dilution gas used (symbol)	<u>NA</u>

2. Field Analysis Data: 3<sup>rd</sup> FORMALDEHYDE

Run # 3 Time \_\_\_\_\_

	Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>INT 1</u>	<u>METHANE</u>	<u>19.12</u>	<u>32</u>	<u>-</u>	<u>15.89</u>
<u>2</u>	<u>METHANE</u>	<u>17.21</u>	<u>32</u>	<u>-</u>	<u>15.94</u>
<u>3</u>	<u>METHANE</u>	<u>64.91</u>	<u>32</u>	<u>-</u>	<u>43.363</u>
<u>4</u>	<u>METHANE</u>	<u>0.00</u>	<u>32</u>	<u>-</u>	<u>BTOL</u>
<u>5</u>	<u>METHANE</u>	<u>17.68</u>	<u>32</u>	<u>-</u>	<u>15.062</u>

Run # 3 Time \_\_\_\_\_

	Components	Area	Attenuation	A x A Factor	Concentration (ppm)
<u>6</u>	<u>METHANE</u>	<u>18.26</u>	<u>32</u>	<u>-</u>	<u>15.395</u>
_____	_____	_____	_____	_____	_____
_____	_____	_____	_____	_____	_____
_____	_____	_____	_____	_____	_____

Run # \_\_\_\_\_ Time \_\_\_\_\_

	Components	Area	Attenuation	A x A Factor	Concentration (ppm)
_____	_____	_____	_____	_____	_____
_____	_____	_____	_____	_____	_____
_____	_____	_____	_____	_____	_____
_____	_____	_____	_____	_____	_____

**IX. FIELD DATA**

**C. PAH**

Plant MacAsphalt (Pch)

Location Melbourne  
 Operator [Signature]  
 Date 12/4  
 Run No. 1443  
 Sample Box No. [Signature]  
 Meter Box No. 1.52  
 Meter H @ 910  
 C Factor  
 Pitot Tube Coefficient Cp .17

Ambient Temperature 58  
 Barometric Pressure 30.00 FINAL 553  
 Assumed Moisture, % INITIAL 200  
 Probe Length, m (ft) 6 DIFFERENCE 353  
 Nozzle Identification No. .068576  
 Avg. Calibrated Nozzle Dia., (in.) .325/.325/.325  
 Probe Heater Setting 4  
 Leak Rate, m<sup>3</sup>/min. (cfm) .018 @ 25"  
 Probe Liner Material [Signature]  
 Static Pressure, mm Hg (in. Hg) [Signature]  
 Filter No. TS S00026

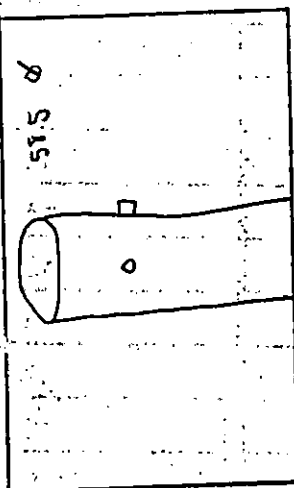
Schematic of Stack Cross Section

TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in. H <sub>2</sub> O	PRESSURE DIFF. ORF. MIR in. H <sub>2</sub> O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
1	8:11.30	20	237	.66	4.97	171.04	72	66	237	65
2	8:15.15	20	241	.65	4.4	188.1	78	65	237	59
3	8:22.15	15	253	.45	3.05	191.3	85	65	242	59
4	8:26.30	16	255	.47	3.18	194.5	94	66	250	56
5	8:30.15	16	262	.47	3.18	197.7	101	69	252	57
6	8:34	15	266	.46	3.12	200.9	106	71	251	57
7	8:37.45	12	269	.35	2.37	204.0	110	74	253	58
8	8:41.30	12	271	.35	2.37	207.2	117	76	256	57
9	8:45.15	13	271	.40	2.71	210.6	122	79	260	58
10	8:49	13	272	.40	2.71	214.1	123	82	261	59
11	8:52.45	13	272	.40	2.71	217.4	124	85	260	61
12	8:56.30	13	270	.35	2.37	220.649	127	87	258	61



Plant Mac Asphal (Pah)

Location Melbourne, Fl  
 Operator mw  
 Date 12/3  
 Run No. 1  
 Sample Box No. Anderson  
 Meter Box No. 1.152  
 Meter H @ 0.410  
 C Factor 1.14  
 Pitot Tube Coefficient Cp 1.14



Ambient Temperature 66  
 Barometric Pressure 30.02 FINAL  
 Assumed Moisture, % 21 INITIAL  
 Probe Length, m(ft) 6 DIFFERENCE  
 Nozzle Identification No. .000576  
 Avg. Calibrated Nozzle Dia., (in.) 325/325/325  
 Probe Heater Setting 4  
 Leak Rate, m<sup>3</sup>/min. (cfm) Grey Quartz  
 Probe Liner Material  
 Static Pressure, mm Hg (in. Hg)  
 Filter No. T5 633Z

Schematic of Stack Cross Section.

TRAV. PT NO.	SAMPLING TIME (Ø) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A1-1	10:25 10:25.45	17	243	32	2.04	26.85 24.6	71	71	224	65
2	10:32.30	23	254	41	2.61	32.8	100	72	226	55
3	10:36.15	22	257	39	2.40	35.7	106	74	228	58
4	10:40	21	262	35	2.23	38.8	110	78	232	59
5	10:43.45	19	270	34	2.16	41.8	117	82	237	61
6	10:47.30	20	272	37	2.36	44.992	124	84	244	62
7	10:57 11:00.45	14	283	27	1.72	45.490 48.3	105	88	239	63
8	11:04.30	13	287	25	1.59	50.8	114	88	236	61
9	11:08.15	12	286	21	1.34	53.3	119	89	237	61
10	11:12	10	285	20	1.27	55.7	120	90	237	64
11	11:15.45	11	286	22	1.40	58.1	121	92	237	64
12	11:19.10	13	285	25	1.59	60.740	123	94	237	64

MACASF72





Plant Macapagal (Pet)  
 Location Melbourne, Fla  
 Operator mw  
 Date 12/3  
 Run No. 2  
 Sample Box No. Anderson  
 Meter Box No. 152  
 Meter H @ 910  
 C Factor 1.1  
 Pitot Tube Coefficient Cp 1.1

Ambient Temperature 66  
 Barometric Pressure 30.02 FINAL  
 Assumed Moisture, % 39.2 INITIAL  
 Probe Length, m(ft) 200 DIFFERENCE  
 Nozzle Identification No. 0005241  
 Avg. Calibrated Nozzle Dia., (in.) 310/310/310  
 Probe Heater Setting 4  
 Leak Rate, m<sup>3</sup>/min. (cfm) .017 @ 15"  
 Probe Liner Material Pyrex Quartz  
 Static Pressure, mm Hg (in. Hg) TS @ 6333  
 Filter No. TS @ 6333

SILICA GEL WEIGHT.	
MPH VOL. AM	
525	39.2
200	311.8
325	6.4

Schematic of Stack Cross Section

TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (TS) (°C)	VELOCITY HEAD (Ps) (ft-H <sub>2</sub> O)	PRESSURE DIFF. ORF. MTR (ft-H <sub>2</sub> O)	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							AT DRY GAS METER	Inlet to Outlet		
1-1	12:55 12:58:45	6	259°	25	1.32	107.575 109.5	95°	88°	222°	65°
2	13:02:30	9	259°	40	2.12	112.7	110°	98°	246°	62°
3	13:06:15	12	260°	53	2.82	116.1	116°	89°	254°	60°
4	13:10	13	260°	61	3.24	119.9	125°	91°	260°	62°
5	13:13:45	10	261°	44	2.33	123.0	129°	94°	256°	69°
6	13:17:30	9	262°	41	2.18	126.2	129°	96°	253°	65°
7	13:21:15	8	263°	32	1.70	128.933	130°	97°	250°	60°
8	15:04 15:07:45	6	255°	20	1.06	131.1	80°	80°	260°	65°
9	15:11:00 15:14:45	9	264°	38	2.02	134.0	95°	79°	225°	63°
10	15:28:30	9	265°	36	1.91	136.9	107°	80°	239°	62°
11	15:32:15	9	264°	36	1.91	139.7	111°	81°	251°	63°
12	15:36	10	269°	38	2.02	142.681	108°	84°	258°	64°



**IX. FIELD DATA**

**D. PARTICULATE**

Plant MACASPHACT

Location Metairie, LA

Operator J.C. Brooks

Date 12-2-92

Run No. 1

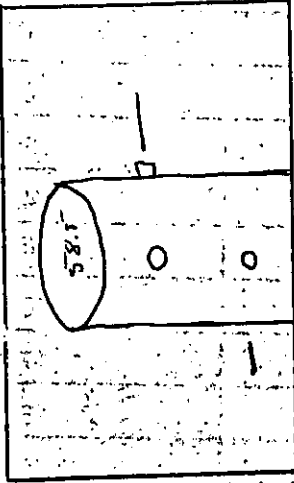
Sample Box No. 1

Meter Box No. L-185

Meter H @ 1.531

C Factor .987

Pitot Tube Coefficient Cp .84



Ambient Temperature 70  
 Barometric Pressure 30.01 FINAL 33.8  
 Assumed Moisture, % 18 INITIAL 32.7  
 Probe Length, m(ft) 6.1 DIFFERENCE 2.3  
 Nozzle Identification No. 0004908  
 Avg. Calibrated Nozzle Dia., (in.) 30/30/30  
 Probe Heater Setting 1  
 Leak Rate, m<sup>3</sup>/min. (cfm) .005 AT 8"  
 Probe Liner Material PTFE  
 Static Pressure, mm Hg (in. Hg) 1.05  
 Filter No. T.S. 00018

Schematic of Stack Cross Section

2.5 min's Point Condensables

TRAV. PT NO.	SAMPLING TIME (0)min.	VACUUM in. Hg	STACK TEMP (Ts)	VELOCITY HEAD (Ps) in H <sub>2</sub> O	PRESSURE DIFF. ORF. MTR in H <sub>2</sub> O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. AT DRY GAS METER in H <sub>2</sub> O	FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
1	14:15 14:20:30	2	230	35	1.4	531.18 532.9	80	259	67
2	14:23	3	231	40	1.6	534.8	82	263	65
3	14:25:30	3	245	36	1.4	536.4	84	268	62
4	14:28	2	253	30	1.2	538.2	90	271	61
5	14:30:30	2	258	26	1.0	539.8	92	264	62
6	14:33	2	262	23	.93	541.2	94	259	62
7	14:35:30	2	261	27	1.0	542.7	96	252	62
8	14:38	2	269	28	1.1	544.3	98	246	61
9	14:40:30	3	265	30	1.2	545.9	98	242	61
10	14:43	3	271	30	1.2	547.4	100	240	61
11	14:45:30	2	274	27	1.0	549.1	100	247	61
12	14:48	2	279	27	1.0	550.6	100	254	62



Plant MACASPART

Location Melbourne, FLA

Operator T. CRACK

Date 12-3-72

Run No. 2

Sample Box No. 1

Meter Box No. 0-185

Meter H @ 1.531

C Factor 987

Pitot Tube Coefficient Cp .84

Ambient Temperature 70

Barometric Pressure 30.02 FINAL

Assumed Moisture, % .21 INITIAL

Probe Length, m(ft) 0.71 DIFFERENCE

Nozzle Identification No. 0004908

Avg. Calibrated Nozzle Dia., (in.) .30/30/30

Probe Heater Setting 4

Leak Rate, m<sup>3</sup>/min. (cfm) 0.15 @ 14"

Probe Liner Material PPEX

Static Pressure, mm Hg (in. Hg) ±.05

Filter No. T.S.6575

SLICA GR. WEIGHT.	VOLUME ml
427.4	460
422.5	300
4.9	160

Schematic of Stack Cross Section

Condensates

TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in. H <sub>2</sub> O	PRESSURE DIFF. ORF. MTR in. H <sub>2</sub> O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
1	<del>14:57</del> 15:01.50	4	230	.35	1.3	<del>576.587</del> 575.1	80	79	217	67
2	15:04	5	247	.40	1.5	580.0	82	79	224	66
3	15:06.30	6	251	.38	1.5	581.9	88	79	230	65
4	<del>15:10</del> 15:10.45.20	6	254	.38	1.5	582.7	90	79	232	65
5	<del>15:20</del> 15:22.30	3	236	.30	1.1	584.9	82	79	204	67
6	15:25	4	265	.30	1.1	586.6	90	79	214	62
7	15:27.30	4	266	.30	1.1	588.1	92	79	227	61
8	15:30	4	265	.33	1.2	589.8	92	79	227	61
9	15:32.30	4	269	.27	1.0	591.3	91	79	231	62
10	15:35	4	270	.31	1.1	592.8	96.	76	231	63
11	15:37.30	3	269	.26	0.7	594.3	94	76	237	65
12	15:40	8	273	.55	2.0	596.4	98	76	243	63





Plant MACASPhos

Location Melbourne, Fla

Operator T.L. Cook

Date 12-4-52

Run No. 3

Sample Box No. 1

Meter Box No. 2-185

Meter H @ 1.531

C Factor .987

Pitot Tube Coefficient Cp .84

Ambient Temperature 50

Barometric Pressure 30.00

Assumed Moisture, % .20

Probe Length, m(ft) 18.2

Nozzle Identification No. 0009108

Avg. Calibrated Nozzle Dia., (in.) .30/.30/.30

Probe Heater Setting 4

Leak Rate, m<sup>3</sup>/min. (cfm) 0.19 AT 9"

Probe Liner Material PIREX

Static Pressure, mm Hg (in. Hg) 4.95

Filter No. 7S.00025

INITIAL	FINAL	DIFFERENCE	SLICIA GEL WEIGHT, g
300	400	100	400
392.4	492.4	100	392.4
18.2	7.7	10.5	7.7

Schematic of Stack Cross Section

CONDENSATES

TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts)	VELOCITY HEAD (Ps) in H <sub>2</sub> O	PRESSURE DIFF. ORF. MTR in H <sub>2</sub> O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
1	8:26 8:28.30	4	254	.38	1.5	618.91 620.0	66	60	262	60
2	8:31	7	261	.50	2.1	622.2	72	60	265	55
3	8:33.30	6	264	.47	1.9	624.3	74	60	268	54
4	8:36	5	264	.35	1.4	626.2	78	62	270	58
5	8:38.30	5	266	.35	1.4	627.9	80	62	262	60
6	8:41	5	268	.34	1.4	629.7	82	62	250	59
7	8:43.30	3	266	.23	.94	631.1	84	64	247	57
8	8:46	3	269	.20	.84	632.5	86	64	242	56
9	8:48.30	3	269	.17	.71	633.8	86	64	252	56
10	8:51	3	271	.18	.75	635.1	88	64	257	56
11	8:53.30	3	271	.20	.84	636.5	88	64	261	57
12	8:56	3	272	.22	.92	638.0	90	68	261	57



**IX. FIELD DATA**

**E. FORMALDEHYDE**

Plant MACASACT

Location McLbourne, FLA

Operator T.C. Book

Date 12-4-92

Run No. 1

Sample Box No. 1

Meter Box No. C-185

Meter H @ 1.531

C Factor 587

Pitot Tube Coefficient Cp : .84

Ambient Temperature 70

Barometric Pressure 30.00 FINAL

Assumed Moisture, % 2.0 INITIAL

Probe Length, m(ft) 6 FT DIFFERENCE

Nozzle Identification No. 0004908

Avg. Calibrated Nozzle Dia., (in.) .30/.30/.30

Probe Heater Setting 4

Leak Rate, m<sup>3</sup>/min. (cfm) .007879"

Probe Liner Material PYREX

Static Pressure, mm Hg (in. Hg) 7.05

Filter No. N/A

SEICA DEL WEIGHT	
VOLUME	
FINAL	30016
INITIAL	353.7
DIFFERENCE	6.7

Schematic of Stack Cross Section

FORMAL DENY DE

3 MW POINTS TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A1	<del>10:45</del> 10:52	3	251	.34	1.4	<del>662.5</del> 664.4	90	80	N/A	68
2	10:55	4	270	.35	1.5	666.6	98	82	N/A	65
3	10:58	4	276	.33	1.4	668.8	102	82	N/A	62
4	11:01	3	279	.30	1.2	670.7	102	82	N/A	61
5	12:04	2	279	.22	.92	672.5	104	82	N/A	62
6	12:07	2	273	.22	.92	674.3	104	84	N/A	61
7	12:10	3	257	.28	1.2	676.3	106	84	N/A	60
8	12:13	3	259	.28	1.2	678.3	108	84	N/A	59
9	12:14	4	252	.42	1.7	680.7	108	86	N/A	59
10	12:19	4	247	.35	1.5	683.0	110	86	N/A	59
11	12:22	3	247	.30	1.2	685.0	110	86	N/A	60
12	12:25	6	253	.50	2.1	687.9	110	86	N/A	60



(ONPH)

Plant Macapagal H  
 Location Melbourne  
 Operator mw  
 Date 12/4  
 Run No. 2  
 Sample Box No. 1  
 Meter Box No. Anderson  
 Meter H @ 1.952  
 C Factor 790  
 Pitot Tube Coefficient Cp .11

Ambient Temperature 70  
 Barometric Pressure 30.80 FINAL  
 Assumed Moisture, % 8 INITIAL  
 Probe Length, m(ft) L DIFFERENCE 240  
 Nozzle Identification No. 000574  
 Avg. Calibrated Nozzle Dia., (in.) .325/.325  
 Probe Heater Setting 4  
 Leak Rate, m<sup>3</sup>/min. (cfm) .002 @ 15'  
 Probe Liner Material Quartz  
 Static Pressure, mm Hg (in. Hg) 1/A  
 Filter No. 1/A

MAKING VOL. CAL. REGR.	
440	436.1
200	428.3
240	413

Schematic of Stack Cross Section

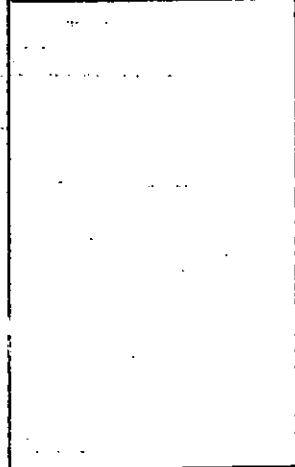
TRAV. PT NO.	SAMPLING TIME (θ) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in-H <sub>2</sub> O	PRESSURE DIFF. ORF. MTR in-H <sub>2</sub> O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
A1-1	13:03 13:05:30	4	275°	35	2.37	151.274 260.4	92°	82°	N/A	52°
2	13:08	5	281°	38	2.57	262.55	99°	73°	/	49°
3	13:10:30	5	281°	40	2.71	269.79	102°	82°	/	50°
4	13:13	5	282°	38	2.57	266.92	109°	83°	/	63°
5	13:15:30	5	283°	42	2.95	249.16	114°	75°	/	67°
6	13:16	5	285°	40	2.71	271.4	117°	86°	/	67°
7	13:20:30	5	285°	44	2.98	273.74	119°	87°	/	67°
8	13:23	6	285°	50	3.39	276.25	120°	88°	/	69°
9	13:25:30	6	287°	50	3.37	278.715	123°	90°	/	68°
10	13:28	8	287°	65	4.40	281.55	127°	93°	/	61°
11	13:30:30	8	287°	65	4.40	284.495	130°	94°	/	62°
12										

MACASF3



Plant MACAS Plant

Location McLoughlin FCA  
 Operator T.C. Row  
 Date 12-4-92  
 Run No. 3  
 Sample Box No. 1  
 Meter Box No. C-185  
 Meter H @ 1.53'  
 C Factor .587  
 Pitot Tube Coefficient Cp .84



Ambient Temperature 70  
 Barometric Pressure 30.00  
 Assumed Moisture, % 20  
 Probe Length, m(ft) 6.17  
 Nozzle Identification No. .0004908  
 Avg. Calibrated Nozzle Dia., (in.) .30/.50/.30  
 Probe Heater Setting 4  
 Leak Rate, m<sup>3</sup>/min. (cfm) .003 at 23"  
 Probe Liner Material P/Rex  
 Static Pressure, mm Hg (in. Hg) 0.05  
 Filter No. NA

BARICAGE VOLUME, ml	FINAL	INITIAL	DIFFERENCE
	45.0	49.6	2.80
SCALE WEIGHT, g			
	45.7	49.6	5.4

Schematic of Stack Cross Section

TRAV. PT NO.	3 MIN RIMTS SAMPLING TIME (Ø) min.	VACUUM in. Hg	STACK TEMP (Ts) °F	VELOCITY HEAD (Ps) in H2O	PRESSURE DIFF. ORF. MTR in H2O	GAS SAMPLE VOLUME ft <sup>3</sup>	GAS SAMPLE TEMP. AT DRY GAS METER °F		FILTER HOLDER TEMP °F	GAS TEMP LVG CONDENSER OR LAST IMPINGER °F
							Inlet	Outlet		
AT	14:48 14:51	2	250	.25	1.0	<del>712.08</del> 113.8	94	NA	NA	61
2	14:54	8	251	.53	2.2	716.3	92	NA	NA	55
3	14:57	8	253	.50	2.1	718.9	92	NA	NA	55
4	15:00	8	255	.50	2.1	721.6	90	NA	NA	57
5	15:03	7	262	.47	1.9	724.1	90	NA	NA	58
6	15:06	7	265	.45	1.9	726.7	90	NA	NA	58
7	15:09	4	267	.32	1.3	728.8	90	NA	NA	57
8	15:12	4	267	.28	1.1	730.9	92	NA	NA	58
9	15:15	3	268	.25	1.0	732.4	92	NA	NA	59
10	15:18	3	270	.25	1.0	734.5	92	NA	NA	59
11	15:21	4	268	.27	1.1	736.4	92	NA	NA	59
12	15:24	4	258	.32	1.3	738.4	92	NA	NA	59





DATA ON FACILITY BEING STACK TESTED

TODAY'S DATE: 12/3/92

COMPANY NAME MacAsphalt - 0408 COMPANY REP. Eddie Co. Jr. PHONE (407) 242-1732  
 LOCATION OF FACILITY Melbourne ORIGINAL START-UP DATE 72 St. Ste. DESIGNED CAPACITY 6000 # 6 bbl/hr  
 OEM \_\_\_\_\_ MODEL NO. \_\_\_\_\_ TYPE \_\_\_\_\_ AC TYPE \_\_\_\_\_

1 Time (24 HR)	2 Fuel Use # <input checked="" type="checkbox"/> Fuel Oil <input type="checkbox"/> Nat. Gas <input type="checkbox"/> Propane <input type="checkbox"/> Coal <input type="checkbox"/> other	3 Burner Setting %	4 Blower Pressure	5 Production Rate		6 Asphalt Cement %	7 Mix Temp. °F	8 <del>Exhaust</del> Exhaust Gas Temp. °F	9 Venturi Scrubber Baghouse		10 Ambient Temp. °F	11 Relative Humidity %	12 Exhaust Damper Position Draft
				Mix Aggregate TPH	RAP TPH				Pressure Drop in w.g.	Water Pressure psi			
1430		60%		145	Type III	4.6	325°	315°	3				.09
1435		60%		145	Dist. #1152	4.6	320°	340°	3.5				.08
1455		95%		164	#1152	4.6	310°	350°	4				.162
1505		90%		164		4.6	340°	350°	4				.14
1520		65%		151		4.6	325°	375°	3.5				.12
<hr/>													
12/3/92		65		127	Type III	4.6	340	325	4				.11
10:30		65		127		4.6	340	315	4	55			.14
10:45		80		137		4.6	340	330	4				.10
11:00		78		144		4.6	350	340	4.2				.13
11:15		82		148		4.6	325	350°	4				.10
11:30		95		150		4.6	320	340	4				.11
11:45		95		154		4.6	350	340	4				.13
12:00		95		150		4.6	340	320	4				.13
12:15		95		129	S-1	4.4	320	310	3.5				.13
12:30		80		150		4.4	335	305	3.5				.13
12:45		70		150		4.4	330	305	3.5				.12
1:00		65		154		4.4	330	305	3.5				.10



DATA ON FACILITY BEING STACK TESTED

TODAY'S DATE: 12/4/92

COMPANY NAME \_\_\_\_\_ COMPANY REP. \_\_\_\_\_ PHONE ( ) \_\_\_\_\_  
 LOCATION OF FACILITY \_\_\_\_\_ ORIGINAL START-UP DATE \_\_\_\_\_ DESIGNED CAPACITY \_\_\_\_\_  
 OEM \_\_\_\_\_ MODEL NO. \_\_\_\_\_ TYPE \_\_\_\_\_ AC TYPE \_\_\_\_\_

1 Time (24 HR)  NOTE: check small box in column when moisture sample is taken	2 Fuel Use  ☐ # Fuel Oil ☐ Nat. Gas ☐ Propane ☐ Coal ☐ other	3 Burner Setting	4 Blower Pressure	5 Production Rate		6 Asphalt Cement %	7 Mix Temp. °F	8 Baghouse Exhaust Gas Temp. °F	9 Venturi Scrubber Baghouse		10 Ambient Temp. °F	11 Relative Humidity %	12 Exhaust Damper Position
				☐ Mix Aggregate TPH	☐ RAP TPH				Pressure Drop in w.g.	Water Pressure psi			
Plant Start 8:10 am													
8:15		95		159	5-1	4.4	325	290	4.5				0.12
8:30		95		152	5-1		335	320	4.5				0.14
8:45		95		150	5-1		310	320	4				0.12
9:00		95		150	5-1		325	320	3.5				0.12
9:15	Plant Start	88		150				325	3.5				0.13
10:30	Plant Start	45											
10:45		65		140			295	310	4				0.15
11:00		70		135			350	330	4				0.11
11:15		95		152			325	330	4.5				0.13
11:30		95		152			325	330	4.5				0.13
11:45		95		152			320	315	4.5				0.13
12:00		10		100	Lean mix		320	290	3				0.13
12:15		20		100	11		320	290	3				0.13
12:30		95		150	5-1		335	320	4				0.12
12:45		20		150	5-1		325	325	4				0.12
13:00		95		152	11		335	320	4				0.14
13:15		95		152	11		325	320	4				0.13



AGGREGATE

1. Name/type of mix \_\_\_\_\_
2. Name/type of 2nd mix (if used) \_\_\_\_\_
3. Type/temperature of Liquid Asphalt \_\_\_\_\_ / \_\_\_\_\_ °F
4. Sieve/Screening analysis: \_\_\_\_\_ % Passing; \_\_\_\_\_ Moisture on Aggregate

	1st mix / 2nd mix	1st mix / 2nd mix	1st mix / 2nd mix
1"	___/___	3/8" ___/___	# ___/___
3/4"	___/___	#200 ___/___	# ___/___
1/2"	___/___	# ___/___	# ___/___

CONTROL SYSTEM

Manufacturer: Estee Model 10-612  
 @ 168 tph / upto 50% RAP Heat Input 59.9 (10<sup>6</sup>) Btu/hr N<sup>o</sup> 6 Max 1.9%

- A. Baghouse:
  1. Type of bags: Nomex # of bags 528 Sq. ft. of bags \_\_\_\_\_
  2. Air to cloth ratio: 4.07 to 1 Designed ACFM 65,000 35,000 DSCF
  3. Type of cleaning - pulse jet  reverse air \_\_\_\_\_ plenum pulse \_\_\_\_\_ other \_\_\_\_\_
  4. Cleaning cycle time: 13 sec Interval between cleaning cycle: \_\_\_\_\_
  5. Pulse pressure on cleaning cycle: 100 psi
- B. Scrubber:
  1. Type - Venturi: \_\_\_\_\_ Wet Washer: \_\_\_\_\_  
 Spray Booth: \_\_\_\_\_ Other: \_\_\_\_\_
  2. Gallons per minute through system: \_\_\_\_\_
  3. Water source: \_\_\_\_\_ (i.e., pond, lagoon, etc.)
  4. Number of spray nozzles: \_\_\_\_\_

Company Name: \_\_\_\_\_ Date: \_\_\_\_\_

Company Representative: \_\_\_\_\_

**Name:** Mr. Sumner Buck

**Title:** President

**Qualifications:** Mr. Buck is a graduate of the University of Mississippi with graduate studies at Memphis State University and State Technical Institute of Memphis. He is a graduate of the EPA 450 "Source Sampling for Particulate Pollutant's" course and the 474 "Continuous Emissions Monitoring" courses outlined by EPA at Research Triangle Park, N.C. He has been directly involved in conducting and supervising air emission testing for over 15 years. He has personally conducted over 400 air emission tests. He currently sponsors and directs visual emission certification schools for US EPA Method 9.

**Project Duties:** Mr. Buck is responsible for the overall supervision of each testing project. This includes the correspondence to the State Regulatory Agency and the plant personnel regarding scheduling, testing requirements, etc. He will assist in supervision of the project preparation for each team involved and the overall organization between the testing crew(s) and facility.

**Name:** Mr. Joe Sewell

**Title:** Vice President

**Qualifications:** Mr. Sewell is currently serving as the Vice President of RAMCON Environmental Corporation. Mr. Sewell is a graduate of Christian Brothers University in Memphis, Tennessee where he obtained a Bachelor of Science degree in Chemical Engineering. He has conducted and supervised air emissions testing projects ranging a broad spectrum of facility process categories. His accomplishments include the development of the instrumental branch of emissions testing utilizing continuous emission monitors and gas chromatography. Mr. Sewell performs a major role in the upgrading of testing capabilities and professional quality that RAMCON Environmental Corporation offers.

**Project Duties:** Mr. Sewell provides staff engineering and project administration to ensure the integrity of the requested services. He serves as the primary contact person for RAMCON Environmental Corporation handling all correspondence between the facility personnel involved in the project and respective state agency representative(s). He provides project leadership to RAMCON Environmental Corporation field supervisors and managers involved in the testing project.

**Name:** Mr. Ray Jenkins  
**Title:** Source Sampling Director

**Qualifications:** Mr. Jenkins is serving as the Source Sampling Director for RAMCON Environmental Corporation. He was promoted to this leadership position after gaining a significant amount of experience in conducting and providing field supervision of a variety of air testing projects. Mr. Jenkins has personally conducted and/or supervised all of the prevalent EPA approved procedures with expertise in the instrumental analyzer procedures. He graduated from Memphis State University obtaining a Bachelor of Science degree in Biology. He is also currently certified to conduct US EPA Reference Method 9 for the visual determination of emission opacity.

**Project Duties:** Mr. Jenkins provides project leadership to the Team Leaders and Field Technicians. He ensures the test crew(s) involved in the test project will be properly informed to his respective duties and responsibilities during the testing process. Mr. Jenkins also serves as the Quality Assurance/Quality Control Coordinator and provides guidance in QA/QC to each Team Leader with regard to sample integrity.