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AP42 Section: 11.1

Reference Number: 286

Title: Source Sampling For Particulate Emissions, South Coast Carlsbad, Carlsbad, CA,

San Diego County Air Pollution, San Diego, CA,

October 20, 1992.



AP-42 Section 11.1
Reference
Report Sect. 4
Reference ~~285~~

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286

Air Pollution Control Officer
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November 18, 1992

Attn: Ken Kindler
South Coast Asphalt Products Company
P.O. Box 586324
Oceanside, CA. 92058-6324

SUBJECT: RENEWAL TEST REPORTS

The enclosed test reports are the result of testing done at your facilities.

If you have any questions, please call me at (619) 694-3359.


Robert Yelenosky
Senior Air Pollution Chemist

Enclosures

South Carlsbad (unit #1) on 10/20/92
 SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA. 92123
SOURCE TEST OF PARTICULATE EMISSIONS TO THE ATMOSPHERE

P.O.#926 TEST #92294.1

TEST SITE: South Coast Carlsbad (Unit #1)
 3701 Haymar Road
 Carlsbad, CA 92088

TEST #: 92294.1

P.O.#: 926

TEST DATE: 10/20/92

Type of plant (Asphalt/Ferrous/Combustion): **ASPHALT**

UNIT TESTED: Hot Mix Asphalt Plant #1

EQUIPMENT: Barber-Greene model number 894, vented to Barber-Greene model CF-07 Baghouse Appl #1830

TESTED BY: APCD: David Shina & Guy Alphin II	DATE: 10/20/92
SITE PERSONNEL: Ken Kinder	DATE: 10/20/92
APCD ENGINEER: Gary Smith	DATE: 10/20/92
LAB ANALYSIS BY: David N. Shina	DATE: 10/29/92
REPORT BY: David N. Shina	DATE: 10/29/92
REVIEWED BY: Guy Alphin II	DATE: 11/2/92
APPROVED BY: <i>Robert Yelenosky</i>	DATE: 11/3/92

ROBERT YELENOSKY, SENIOR AIR POLLUTION CHEMIST

This report has been reviewed and found to be representative of the testing that was performed.

SDAPCD RULES

TEST	LIMIT	MEASURED	EXCEEDANCE/NON-EXCEEDANCE
RULE 54 DUST & FUMES	40 lbs/hr	4.64 lbs/hr	NON-EXCEEDANCE
RULE 260.92	0.04 gr/dscf	0.032 gr/dscf	NON-EXCEEDANCE

TEST RESULTS SUMMARY:

ITEM	I	Cs	E
UNITS	%	gr/dscf	lbs/hr
VALUE	107	0.0321	4.64

ENGINEERING SUMMARY

Qstd	Fuel	Rate	Asphalt Production
dscfm	---	tons/hr	tons
16868	Natural gas	108.31	162.46

TEST PARAMETERS:

SYSTEM DESCRIPTION:

This asphalt plant combines crushed rock and sand with asphalt oil in batch loads of varying sizes. The rock and sand are heated in a rotary drum to dry them. The exhaust from this dryer is routed through a baghouse and finally to a stack. It is the emissions from this stack that are the subject of this report.

PROCEDURES:

The procedures utilized in these tests are based on EPA's 40 CFR, July 1, 1991, Part 60, Appendix A, Methods 1-5 inclusive. The sampling train was modified as follows: (1) Teflon tubing was run from the end of the probe to the first impinger in the cold box (the hot box was eliminated). (2) A back-end filter was used instead of a front-end filter (for both modifications see fig. 1).

CALCULATIONS

All equations are from the EPA's 40 CFR, July 1, 1991, Part 60, Appendix A, Methods 1-5 inclusive. All preliminary assumptions and calculations are based on data obtained from previous tests.

PARTICULATE SAMPLING:

The test consisted of sampling at 20 traverse points, 10 from each of 2 sample ports (fig.2), collected from 54 inches below the stack (fig.3). All field data was transferred to the computer printout. All calculations were done by the computer and the emissions were compared to rules 54 and 260.92 of the SDAPCD.

ANALYSES:

Gas: An integrated bag sample was collected during the test and analyzed at the APCD lab.

Particulate: All procedures follow EPA guidelines, except where noted in the SDAPCD QA manual.

EQUIPMENT:

All testing and analysis equipment was calibrated according to EPA guidelines (40 CFR, July 1, 1991, Part 60, Appendix A, Methods 1-5).

Analysis:	Collection:	Sampling:	Temp./Press.:
CO2-Anarad AP400	Filter-Geiman	L/S Box-Napp	Thermocouples-Omega
O2-Teledyne Ryan 320 P4	Holder-Geiman	Umbilical cord-Napp	Temp. read out-Omega
Microbalance-Sargent Welch	Beakers-Pyrex	Cold/Hot box-Napp	Aneroid Barometer-Taylor
Microbalance-Sartorius	Impingers-Ace	Pitot tube-Napp	Press. devices-Dwyer magnehelic

FIELD DATA:

Trav. Pt	Vm (ft ³)	ΔP (in H2O)	ΔH (in H2O)	Stack Temp (°F)	Box Temp (°F)	Imp Temp (°F)	t 1 (in) (°F)	t 2 (out) (°F)	velocity (ft/sec)
START	214.943								
1		0.98	4.60	213		48	74.00	984.00	065.03
2		0.98	4.60	199		48	72.00	990.00	064.38
3		0.98	4.60	194		47	72.00	992.00	063.78
4		0.98	4.10	195		51	74.00	994.00	060.48
5		0.90	4.20	208		49	74.00	995.00	061.77
6		0.92	4.30	216		49	74.00	995.00	062.52
7		0.68	3.10	222		45	75.00	996.00	054.26
8		0.78	3.50	221		43	74.00	997.00	058.07
9		0.76	3.50	214		40	75.00	998.00	057.02
10		0.71	2.35	222		45	75.00	999.00	055.44
1		1.08	5.00	237		52	74.00	995.00	069.12
2		1.05	5.00	235		51	75.00	996.00	069.37
3		1.00	4.60	238		58	76.50	999.00	066.56
4		0.92	4.20	235		55	75.50	999.00	063.54
5		0.93	4.30	237		58	76.50	999.00	064.14
6		0.98	4.50	219		57	76.00	100.00	064.99
7		1.00	4.60	207		57	79.00	101.00	065.07
8		0.95	4.50	198		51	79.00	101.00	064.03
9		0.92	4.30	199		50	79.50	101.50	062.03
10	283.630	0.92	4.35	223		51	80.00	102.00	063.15

Average:	Vm m ³	ΔP (in H2O)	ΔH (in H2O)	ts (°F)	tbox (°F)	t (°F)	t 1 (in) (°F)	t 2 (out) (°F)	vs (ft/sec)
	66.687	0.92	4.26	217	N/A	50	76.20	96.75	62.75

DATA SUMMARY:

LABORATORY DATA:	SAMPLING PARAMETERS:	SAMPLING DATA:
IMPINGER CATCH: Silica gel ? = <u>YES</u> Vlc = <u>262.17</u> ml	METER BOX: Box ID = <u>C138</u> ΔH ₀ = <u>1.8883</u> Y = <u>0.9924</u>	VOLUME & TIME: Ø (total time) = <u>60.0</u> min Final leak rate = <u>0.001</u> cfm Pass/Fail = <u>PASS</u> Vm = <u>66.687</u> ft ³
GAS ANALYSIS: CO ₂ = <u>2.20</u> % O ₂ = <u>16.68</u> % CO = <u>0.00</u> % N ₂ = <u>81.12</u> %	STACK DIMENSIONS: Circular ? = <u>YES</u> Ds = <u>1.96</u> ft Length = <u>N/A</u> ft As = <u>6.87</u> ft ²	PRESSURES: Pbar = <u>29.87</u> in Hg Pg = <u>-0.75</u> in H ₂ O Vpw @ ts = <u>29.92</u> in Hg Vpw @ t1 = <u>N/A</u> in Hg
PARTICULATE ANALYSIS: mn(front) = <u>0.063260</u> g mn(back) = <u>0.070892</u> g mn(total) = <u>0.13415</u> g	NOZZLE & PROBE: Dn = <u>0.274</u> in An = <u>0.0589</u> in ² Cp = <u>0.2400</u>	TEMPERATURES: t1 = <u>76.20</u> °F t = <u>50</u> °F t2 = <u>96.75</u> °F tbox = <u>N/A</u> °F tm = <u>86.48</u> °F ts = <u>217</u> °F

CALCULATIONS:

TEMPERATURES:

01)	$t_a = (T_{1st}/total\ n's)$	217 °F
02)	$T_a = t_a + 460$	677 °R
03)	$t_m = (T_{1st} + T_{2nd})/2 / total\ n's = (01 + 02)/2$	56 °F
04)	$T_m = (t_1 + t_2)/2 + 460$	546 °R
05)	$t_s = (T_{std}/total\ n's)$	50 °F
06)	T_{std}	528 °R

PRESSURES:

07)	$P_{bar} = (P @ 5.1) / (H @ 5.1) \times (C @ 5.1) \text{ in Hg}/(1000H)$	29.87 in Hg
08)	$P_g = \text{read from pressure sensing device}$	-0.75 in H2O
09)	$P_{st} = P_{bar} + (P_g / 1.358)$	29.81 in Hg
10)	ΔH	4.26 in H2O
11)	$P_{st} = P_{bar} + (\Delta H / 13.6)$	30.16 in Hg
12)	P_{std}	29.92 in Hg
13)	ΔP	0.9166 in H2O

VOLUME:

14)	$V_m = V_{m\ end} - V_{m\ begin}$	64.687 ft³
15)	Y	0.9924
16)	$V_m = V_m \cdot Y$	64.180 ft³
17)	$V_{m\ std} = [V_m \cdot (T_{std}/T_m) \cdot (P_m/P_{std})]$	64.505 ft³
18)	$V_{sc} = \text{Volume of impinger}$	282.17 ml
19)	ρ	0.002201 lb/ml
20)	R	21.85 in Hg-ft³/R-B-mo
21)	M_{wH2O}	18.00 g/g-mo
22)	$V_{w\ std} = [(V_{sc} \cdot R \cdot T_{std}) / (P_{std} \cdot M_{wH2O})]$	12.8409 ft³

MOISTURE:

23)	$B_{ws}(1) = (V_{w\ std} / (V_{w\ std} + V_{m\ std})) \cdot 100$	18.06 %
24)	$V_{pw} @ t_a = \text{from appendix}$	29.92 in Hg
25)	$B_{ws}(2) = [(V_{pw} @ t_a) / P_a] \cdot 100$	100.35 %
26)	$B_{ws} = \text{lower value of equation 24 or 25}$	18.06 %

MOLECULAR WEIGHT:

27)	%O2	16.68 %
28)	%CO2	2.20 %
29)	%N2+inerts+%CO	81.12 %
30)	$M_d = [(44 \cdot \%CO_2) + (32 \cdot \%O_2) + (28 \cdot \%N_2 + \text{inerts} + \%CO)]$	29.02 g/g-mole
31)	$M_s = M_d \cdot (1 - B_{ws}) + 18.0 \cdot (B_{ws})$	27.25 g/g-mole

VELOCITY:

32)	C_p	0.840
33)	$D_w =$	2.958 ft
34)	$V_w = 85.49 \cdot C_p \cdot [(T_a \cdot \Delta P) / (P_a \cdot M_d)]^{0.5}$	62.753 ft/sec
35)	$A_s = 3.14 \cdot [(D_w)^2 / 4]$	6.869 ft²
36)	$Q_s = (V_w \cdot A_s \cdot 60)$	25987 acfm
37)	$Q_{std} = 17.84 \cdot Q_s \cdot (1 - B_{ws}) \cdot P_a / T_a$	16868 dacfm

EMISSIONS:

FRONT HALF

38)	$m_n \text{ (front)}$	0.06326 g
39)	$C_s \text{ (front)} = 15.43 \cdot m_n \text{ (front)} / V_{m\ std}$	0.01519 grains/dacf
40)	$7000 \text{ grains} = 1 \text{ lb} \cdot 60 \text{ min} = 1 \text{ hr} \cdot 60 \text{ min} / \text{hr} / 7000 \text{ grains} / \text{lb}$	0.00857 lb-min/grains-hr
41)	$E \text{ (front)} = (0.00857) \cdot (Q_{std}) \cdot C_s \text{ (front)}$	2.19 lbs/hr

BACK HALF

42)	$m_n \text{ (back)}$	0.07089 g
43)	$C_s \text{ (back)} = 15.43 \cdot m_n \text{ (back)} / V_{m\ std}$	0.01696 grains/dacf
44)	$7000 \text{ grains} = 1 \text{ lb} \cdot 60 \text{ min} = 1 \text{ hr} \cdot 60 \text{ min} / \text{hr} / 7000 \text{ grains} / \text{lb}$	0.00857 lb-min/grains-hr
45)	$E \text{ (back)} = (0.00857) \cdot (Q_{std}) \cdot C_s \text{ (back)}$	2.45 lbs/hr

TOTAL

46)	$m_n \text{ (total)} = m_n \text{ (front)} + m_n \text{ (back)}$	0.13415 g
47)	$C_s \text{ (total)} = 15.43 \cdot m_n \text{ (total)} / V_{m\ std}$	0.03209 grains/dacf
48)	$7000 \text{ grains} = 1 \text{ lb} \cdot 60 \text{ min} = 1 \text{ hr} \cdot 60 \text{ min} / \text{hr} / 7000 \text{ grains} / \text{lb}$	0.00857 lb-min/grains-hr
49)	$E \text{ (total)} = (0.00857) \cdot (Q_{std}) \cdot C_s \text{ (total)}$	4.64 lbs/hr

ISOKINETICS:

50)	$D_n =$	0.274 in
51)	$A_n = 3.14 \cdot (D_n)^2 / 4$	0.589 in²
52)	ϕ	60 min
53)	$\phi = (0.450 \cdot V_{m\ std} / P_a \cdot \pi \cdot A_n \cdot (1 - B_{ws})) \cdot 100.96 \%$	107 %

So. Coast Carlsbad (#1) on 10/20/92

J. #:926 TEST#92294.1

SAN DIEGO AIR POLLUTION CONTROL DISTRICT, 9150 CHESAPEAKE DRIVE, SAN DIEGO, CA 92123

PARTICULATE TEST LABORATORY ANALYSIS DATA SHEET

TEST SITE: South Coast Carlsbad (Unit #1)
3701 Haymar Road
Carlsbad, CA 92088

TEST #: 92294.1

P.O.#: 926

TEST DATE: 10/20/92

LAB ANALYSIS BY: David N. Shina

DATE: 10/29/92

LAB REPORT BY: David N. Shina

DATE: 10/29/92

REVIEWED BY:

DATE:

(1) IMPINGER VOLUMES

FINAL WGT.	INIT WGT.	NET WGT.	
#1 777.14 g	- 564.76 g	= 212.38 g	Total impinger charge = 200.00 ml Particulates from impinger charge (Total impinger charge * H(water blank) = 0.00016 g Total weight collected = 262.17 g Total volume collected, Vc = 262.17 ml
#2 568.43 g	- 543.53 g	= 24.90 g	
#3 471.49 g	- 468.15 g	= 3.34 g	
#4 790.32 g	- 768.77 g	= 21.55 g	
#5 _____ g	- _____ g	= N/A g	
#6 _____ g	- _____ g	= N/A g	

(2) BLANKS

A	B	C	D	E	F	G	H	I	J	K	L
AREA	SOLVENT	ID	END WGT g	INIT WGT g	NET WGT. (E-F) g	RINSES ml (G/D)	g/ml (G/D)	% (H*100)	ppm (H*10*6)	PASS FAIL	LIMITS
BLANK	ACETONE	92059	28.7701	28.7676	0.00250	250.00	0.0000100	0.0010000	10.0	P	0.0010% = 10ppm
BLANK	WATER	92046	29.0631	29.0629	0.00020	250.00	0.0000008	0.0000800	0.8	P	0.0004% = 4ppm
BLANK	ORGANIC	N/A									

(3) WEIGHTS & RINSES

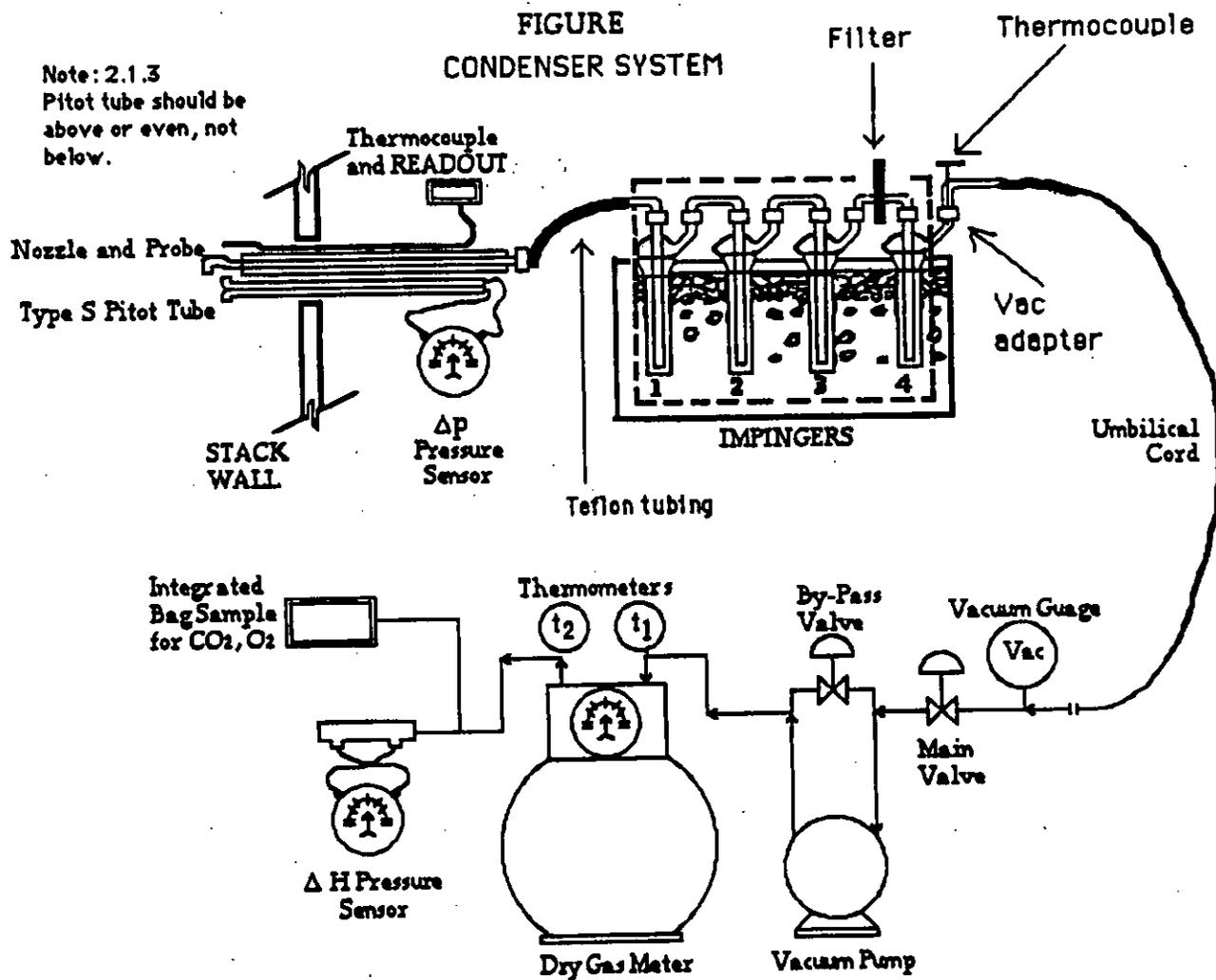
a	b	c	d	e	f	g	h	i	j	k
AREA	SOLVENT	ID	END WGT g	INIT. WGT g	NET WGT. (e-f) g	RINSES ml	SOLV. WGT (g*H) g	WGT (corr) (f-h) g	Subtotal (mn (AREA)) (Σ) g	Total (mn (tot)) (Σ) g
F	ACETONE	92074	29.1207	29.1131	0.0076	300.00	0.003000	0.00460		
R	WATER	92036	49.5716	49.5127	0.0589	300.00	0.000240	0.05866		
U	ORGANIC	N/A								
N	FILTER	N/A								
									mn(front) =	0.063260 g
B	ACETONE	92007	28.4900	28.4772	0.0128	290.00	0.002900	0.00990		
R	WATER **	92055	28.4169	28.3553	0.0616	560.00	0.000608	0.06099		
C	ORGANIC	N/A								
K	FILTER	91095	1.6085	1.6088	*0.0000	-----	-----	0.0000		
									mn(back) =	0.070892 g
TOTAL									mn(total) =	0.13415 g

* The filter net weight is corrected to give 0.0000 g.

** The Back Water-SOLV.WGT is corrected for the initial impinger charge
([g(back water) * H(blank water)] + [Particulates from impinger charge]).

SAN DIEGO COUNTY AIR POLLUTION CONTROL DISTRICT

FIGURE
CONDENSER SYSTEM



Note: 2.1.3
Pitot tube should be
above or even, not
below.

LEGEND

- No. 1 Mod- 100 ML Deionized Water
- No. 2 Std - 100 ML Deionized Water
- No. 3 Mod- Dry
- No. 4 Mod- Silica gel

- Mod - Modified Type Greenburg-Smith
- Std - Standard Type

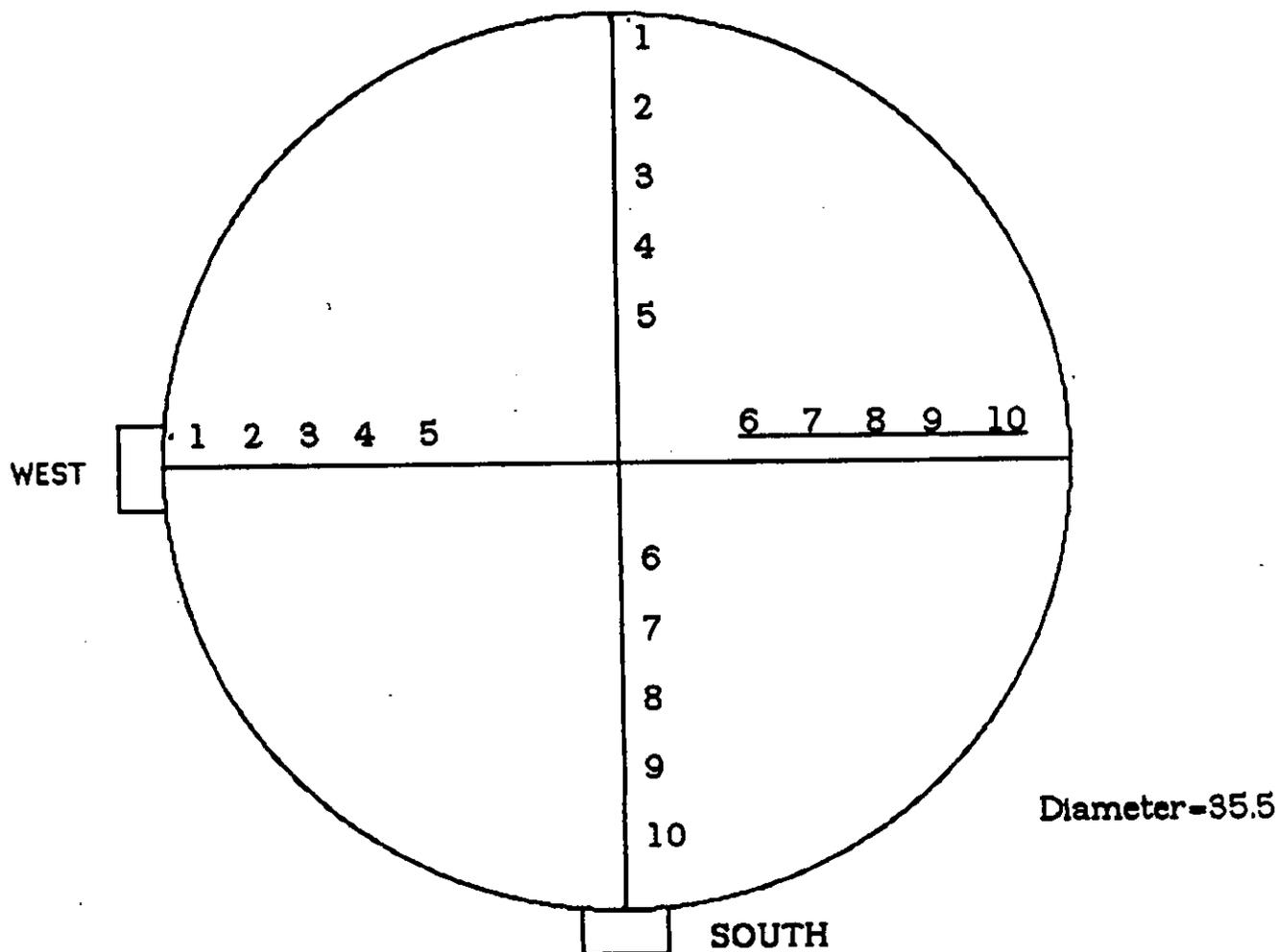
FIELD DATA ABBREVIATIONS

- PT = Point Number
- T_s = Stack Temperature
- Δp = Pitot Tube Pressure Differential, in H_2O
- V_s = Stack Velocity, fps
- ΔH = Orifice Meter Pressure Drop, in H_2O
- t_1 = Meter Inlet Temperature, °F
- t_2 = Meter Outlet Temperature, °F
- F_m = Pump Vacuum, in Hg
- t_i = Impinger Temperature
- P_{bar} = Barometric Pressure

FIGURE : PARTICULATE MATTER SAMPLING TRAIN

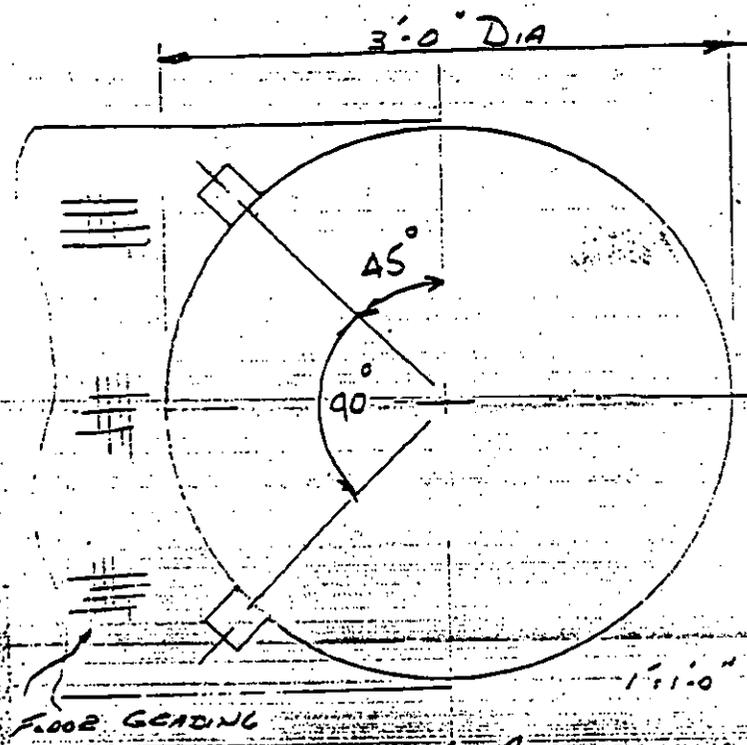
SAN DIEGO COUNTY AIR POLLUTION CONTROL DISTRICT

Figure
TRAVERSE POINTS



<u>POINT</u>	<u>DISTANCE</u>
1	1 inch
2	2.91
3	5.18
4	8.02
5	12.14
6	23.36
7	27.48
8	30.32
9	32.59
10	34.50

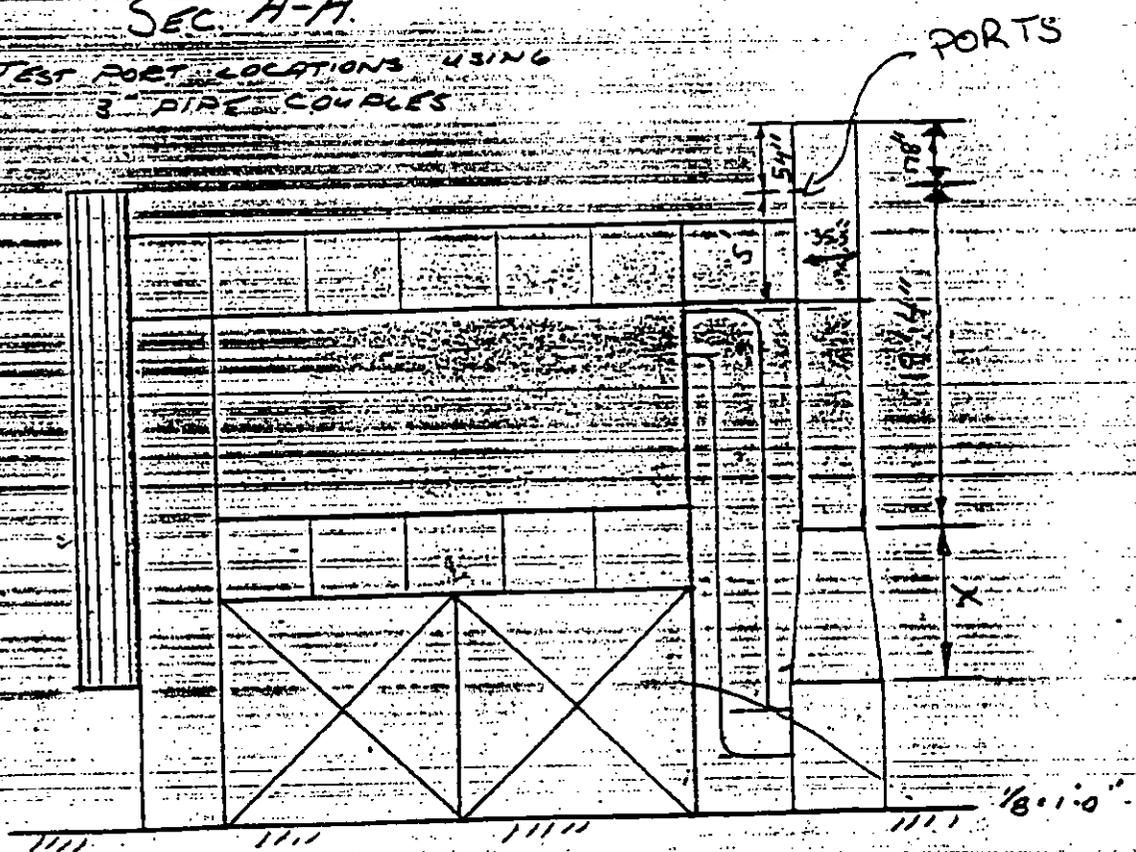
FIG. 3



$I.D. = 2' 11\frac{1}{2}'' = 2.958'$

DOWNSTREAM = 6.53 D
UPSTREAM = 1.52 D

SEC. A-A
TEST PORT LOCATIONS USING
3" PIPE COUPLERS



X = DIMENSION OF LAST RESTRICTOR TO BLOWER.
ESTIMATED TO BE 3'-0"

FIG. 3

NOMENCLATURE

symbol	units	explanation	equation
H			
A_n	in ²	nozzle area	$\pi/4(D_n)^2$
A_s	ft ²	stack area	$\pi/4(D_s)^2$ or $L \times W$
B			
Bws(1)	%	fractional stack gas moisture-equ 1	$(V_w \text{ std}) / (V_w \text{ std} + V_m \text{ std}) \times 100$
Bws(2)	%	fractional stack gas moisture-equ 2	$((V_{pw} @ ts) / P_s) \times 100$
Bws	%	water vapor in the gas stream	lower of Bws(1) and Bws(2)
C			
CO	%	carbon monoxide	read from measuring device (0 for Asphal plants)
CO ₂	%	carbon dioxide	read from measuring device
Corr V _w m	ft ³	correction for V _w w/o silica gel	$(V_m \times (V_{pw} @ ts) / P_s \times P_s \times T_{std}) / (T_{std} \times P_{std})$
C _p	none	pilot tube correction factor	see EPA method 3
C _{a(front)}	gr/dscf	concentration of particulate in stack gas, corrected to STP-for front	$(15.43 \text{ mm(front)}) / (V_m \text{ std})$
C _{a(back)}	gr/dscf	concentration of particulate in stack gas, corrected to STP-for back	$(15.43 \text{ mm(back)}) / (V_m \text{ std})$
C _{a(total)}	gr/dscf	concentration of particulate in stack gas, corrected to STP-for total	$(15.43 \text{ mm(total)}) / (V_m \text{ std})$
C _{a2(front, back, total)}		same as C _a (front, back, total) except corrected for grain loading at 12% CO ₂	$(12 / \%CO_2) \times (15.43 \text{ mm}(f, \text{back, total})) / (V_m \text{ std})$
D			
ρ (density)	lb/ml	density of water at STP	0.002201 (see CRC)
D _s	in or ft	stack diameter	measure at site
D _n	in	nozzle diameter	avg of at least three measurements
E			
E.A.	%	Excess air (for combustion)	$((\%O_2 - 5\%CO) \times 100) / (26.4\%N_2 - \%O_2 - 5\%CO)$
E _(front)	lbs/hr	part. emissions rate-front	$(0.00857)(Q_{sd} \times C_{a(front)})$
E _(back)	lbs/hr	part. emissions rate-back	$(0.00857)(Q_{sd} \times C_{a(back)})$
E _(total)	lbs/hr	part. emissions rate-total	$(0.00857)(Q_{sd} \times C_{a(total)})$
H			
ΔH	in H ₂ O	average differential pressure across the orifice meter	avg of the readings from the pressure measuring device
ΔH_0	none	orifice pressure differential at STP	see EPA Method 5 Appendix
I			
I	%	isokinetic	$(0.09450 \times T \times V_m \text{ std}) / [P_s \times V \times 2 \times (A_n / 144) \times (1 - (Bws / 100))]$
M			
M _d	g/g-mole	dry stack gas molecular wgt	$0.44(\%CO_2) + 0.320(\%O_2) + 0.280(\%N_2 + \text{inerts} + CO)$
mn(back)	g	particulate in impingers	measurement from lab analysis
mn(front)	g	particulate in nozzle & probe	measurement from lab analysis
mn(total)	g	total particulate collected	measurement from lab analysis
M _s	g/g-mole	wet stack gas molecular wgt	$M_d(1 - Bws) + 18.0(Bws)$
MW CO ₂	g/mole	mo. wgt of carbon dioxide	44 (see periodic table)
MW N ₂	g/mole	mo. wgt of nitrogen	28 (see periodic table)
MW O ₂	g/mole	mo. wgt of oxygen	32 (see periodic table)
MW H ₂ O	g/mole	mo. wgt of water	18 (see periodic table)
N			
N ₂	%	percent nitrogen	$100 - (\%CO_2 + \%O_2 + \%CO + \text{inerts})$
O			
O ₂	%	percent oxygen	read from measuring device

NOMENCLATURE (cont.)

NOMENCLATURE (concl.)

symbol	units	explanation	equation
P			
AP	in H ₂ O	pitot diff. press. velocity head of stack gas	read from measuring device
P _{bar}	in Hg	barometric pressure at sampling pt.	read from press. measuring device
n(pi)	none	the ratio of the circumference of a circle to its diameter	3.14165 (see CRC)
P _m	in Hg	absolute meter pressure	$P_{bar} + (\Delta H / 13.6)$
P _s	in Hg	absolute stack pressure	$P_{bar} + (P_{static} / 13.6)$
P _g	in H ₂ O	static pressure of stack	read from pressure sensing device
P _{std}	in Hg	press. at std. conditions (29.92)	see CFR
Q			
Q _s	acfm	flow rate	$v_s \cdot A_o \cdot 60$
Q _{std}	dscfm	dry volumetric stack gas flow rate, corrected to STP	$17.64 \cdot Q_s (1 - B_{ws}) \cdot (P_s / T_s)$
R			
R	in Hg-ft ³ /°R-lb-mo	ideal gas constant	21.85 (see CRC)
S			
S.L.	none	Sea Level	read from a relief map
T			
T _i	°F	dry gas meter inlet temp, uncorrected	read from temp. sensing device
T _o	°F	dry gas meter outlet temp, uncorrected	read from temp. sensing device
T _i corr.	°R	dry gas meter inlet temp, corrected	T _i + temperature correction
T _o corr.	°R	dry gas meter outlet temp, corrected	T _o + temperature correction
Q(thesa)	min	sampling time / point	Q / n
Q(Tthesa)	min	total sampling time	none
T _i	°F	impinger outlet temp.	read from temp. sensing device
T _m	°F	dry gas meter temp. in F	$(T_i + T_o) / 2$
T _m	°R	dry gas meter temp. in R	T _m + 460
n	none	total number of traverses per	summation of the traverse points
T _s	°F	stack temp. in F	read from temp. sensing device
T _s	°R	stack temp. in R	T _s + 460
T _{std}	°R	temp. at std. conditions (528)	see CFR
U			
V _{lc}	ml	water collected from impingers and the silica gel (if applicable)	from lab analysis
V _m	ft ³	sample gas volume, uncorrected	read from dry gas meter
V _m '	ft ³	sample gas volume, corrected	$V_m \cdot Y$
V _m std	ft ³	volume of gas sample by the dry gas meter, corrected to STP	$((V_m \cdot T_{std}) / P_m) / ((P_{std} \cdot T_m) - \text{corr } V_m)$
V _{pw@ts}	in Hg	vapor pressure of water at ts	see CRC water vapor press. tables
V _{pw@ti}	in Hg	vapor pressure of water at ti	see CRC water vapor press. tables
v _s	ft/sec	stack gas velocity	$85.49 \cdot C_p (T_s \cdot \Delta P) / (P_s \cdot M_a) \cdot 0.5$
V _w std	ft ³	Vol. of water vapor in gas sample, corrected to STP	$(V_{lc} \cdot \partial \cdot R \cdot T_{std}) / (P_{std} \cdot MW_{H_2O}) + \text{corr } V_{wm}$
Y			
Y	none	dry gas meter calibration factor	see CFR (6, parts 53-60)

Conversion Factors

(multiply by the number)			
0.002669	in Hg-ft ³ /°R-ml	conversion to get in Hg-ft ³ /R	see CRC
0.00857	lb/gr-min/hr	conv from gr/min to lb/hr (60/7000)	see Lange's Handbook of Chemistry
0.04707	ft ³ /ml	$(\partial \cdot R \cdot T_{std}) / (P_{std} \cdot MW_{H_2O})$	see Lange's Handbook of Chemistry
15.43	gr/g	conversion from g to gr	see Lange's Handbook of Chemistry
17.64	°R/in H ₂ O	T _{std} / P _{std} (528/29.92)	see Lange's Handbook of Chemistry
85.49	(ft/sec)-(lb-in Hg/lb-mo-°R-in H ₂ O)) ^{0.5}	conversion factor to get velocity in ft/sec	see CRC
(divide by the number)			
144	in ² /ft ²	conversion from in ² to ft ²	see CRC
13.6	in H ₂ O/in Hg	conversion from in H ₂ O to in Hg	see CRC
(add to the number)			
460	°R/°F	conversion from F to R	see CRC

MECHANICAL ENGINEERING
SOURCE TEST REPORT
PERMIT RENEWAL TEST

TEST DATE: 20-Oct-92
TEST CREW: DAVID SHINA, GUY ALPHIN

ENGINEER: GARY SMITH

SOURCE: SOUTH COAST ASPHALT
3701 HAYMAR RD. CARLSBAD, CA 92008

PERMIT NUMBER: 926, HOT MIX ASPHALT BATCH PLANT

EQUIPMENT: ASPHALT BATCH PLANT, HOT-MIX (125 TONS/HR CAPACITY)

SITE PERSONNEL: KEN KINDLER, FOREMAN

VISIBLE

EMISSIONS: A WATER PLUME WAS VISIBLE DURING SOME OF THE TEST PERIOD. OPACITY DID NOT EXCEED 20%. A WATER TRUCK WAS OBSERVED IN OPERATION DURING THE TEST. VISIBLE EMISSIONS FROM TRAFFIC WERE BELOW 20% OPACITY.

FUEL USAGE: THE GAS LINE FOR THIS EQUIPMENT DID NOT HAVE A DESIGNATED METER TO DETERMINE FUEL CONSUMPTION.

PRODUCTION: 162.46 TONS OF ASPHALT USING THE FOLLOWING MIX DESIGNS WERE PRODUCED DURING THE TEST PERIOD.

3/8 FINE: 27% BIN #2, 73% BIN #1, 6.0% OIL
1/2 MED: 15% BIN #3, 30% BIN #2, 55% BIN #1, 5.3% OIL
3/4 MED: 10% BIN #4, 20% BIN #3, 25% BIN #2,
45% BIN #1, 5.1% OIL
SCHOOL MIX: 25% BIN #2, 75% BIN #1, 6.2% OIL

BIN #1	BIN #2	BIN #3	BIN #4
25% SAND, 75% DUST	3/8 INCH ROCK	1/2 INCH ROCK	3/4 INCH ROCK

START TIME: 8:10 AM
END TIME: 9:40 AM
ELAPSED TIME: 90 MINUTES
IDLE TIME: 0 MINUTES
NET TIME: 90 MINUTES

PRODUCTION RATE: 108.31 TONS/HR