Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources.* AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

The file name refers to the reference number, the AP42 chapter and section. The file name "ref02_c01s02.pdf" would mean the reference is from AP42 chapter 1 section 2. The reference may be from a previous version of the section and no longer cited. The primary source should always be checked.

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BAY AREA
AIR QUALITY MANAGEMENT DISTRICT
939 Ellis Street
San Francisco, California 94109
(415) 771-6000

SUMMARY OF SOURCE TEST RESULTS

Report No. 92227

Test Date: 06/01/92

Test Times:

Run A: 0809-0859 (50Min)

Run B: 0916-1006 (50Min)

Run C: 1039-1130 (50Min)

SOURCE INFORMATION

Firm Name and Address
SAN RAFAEL ROCK QUARRY, INC.
1000 Pt. San Pedro Road
San Rafael, CA 94901

Firm Representative and Title
Mr. Bob Woodberry,
Manager
Phone No. (415) 459-7440

Source: Asphalt Plant (S-27)
Abated by Baghouse (A-8)

Plant No. 2164

Operates on demand

Permit Conditions # 3732
Specifies fuel & requires baghouse operation

BAAQMD REPRESENTATIVES

Source Test Engineers
C. McClure/H. Doi

Permit Services Division / Enforcement Division
R. Gaynor

Test Requested by:
G. Solomon (CDS)

Operating Parameters:

Plant operated continually at 150 to 175 TPH producing 896 ton of 1/2 inch Aggregate Asphalt during sampling. Rotary Kiln is natural gas fired consuming an average of 380 CFM. Baghouse inlet was 345°F with a differential pressure of 3.8 inches w.c.. Moisture content of the aggregate was 1.6%.

Applicable Regulations: Regulation 10, subpart I

VN Recommended: NO

Source Test Results and Comments:

METHOD:	TEST	RUN A	RUN B	RUN C	AVERAGE	LIMIT
ST-17	Stack Volume Flowrate, SDCFM				18,100	
	Stack Gas Temperature, °F	288	296	285	290	
ST-23	Water Content, Volume %	18.8	18.7	18.6	18.7	
ST-14	Oxygen, Volume %	15.0	15.3	15.5	15.3	
ST-5	Carbon Dioxide, Volume %	3.7	3.5	3.6	3.6	
ST-6	Carbon Monoxide, ppm	600	500	500	540	
	Carbon Monoxide, lb/hr	47.7	39.8	38.7	42.1	
ST-15	Particulate, gr/SDCF	.013	.021	.020	.018	.04
	Particulate, lb/hr	2.0	3.3	3.1	2.8	
	Isokinetic Ratio, Act./Theo.	1.00	.99	.99		

NO COMMERCIAL USE OF THESE RESULTS IS AUTHORIZED

Air Quality Engineer II	Date	Supervising Air Quality Engineer	Date	Approved by Source Test Manager	Date
C. McClure	6/18/92	K. Kunaniec	6/18/91	G. Karels	6/19/92
C. McClure		K. Kunaniec		G. Karels	

Form: Summary of Source Test Results

FSSTS: ej: 15 July 88

SOURCE TEST LAB DATA SHEET

IMPINGER DATA

PLANT: SAN RAFAEL ROCK & ASPHALT

PAGE: 1 OF 1

SOURCE OPERATION: ASPHALT BAGHOUSE

INITIAL: KC

SOURCE TEST NO.:

TEST DATE: 06-01-92

IMPINGER SOLUTION: DI H2O

DATA

IMPINGER#	A TARE WEIGHT(g)	B FILLED WEIGHT(g)	C FINAL WEIGHT(g)
P-1	468.0	568.1	692.4
P-2	489.3	589.0	590.1
P-3	501.7	601.7	720.6
P-4	501.9	602.0	602.9
P-5	488.4	588.2	702.7
P-6	499.1	599.1	600.4

IMPINGER#	C-A SAMPLE WEIGHT(g)	C-B CONDENSATE WT(g)	TOTAL WEIGHT(g)
P-1	224.4	124.3	RUN A
P-2	100.8	1.1	125.4
P-3	218.9	118.9	RUN B
P-4	101.0	.9	119.8
P-5	214.3	114.5	RUN C
P-6	101.3	1.3	115.8

GAS ANALYSIS

SPAN CYLINDER #LL10543

SAN RAFEL ROCK #2164

S-27 6/1/92

GAS	SPAN VALUE	SPAN UNITS
O_2	20.95%	7.57u
CO_2	14.8%	6.65u
CO	1210PPM	5.5u

RUN A)

O_2	CO_2	CO
5 ~~6~~.29	1~~2~~.63	2.90
5 ~~6~~.45	1~~2~~.70	2.75
5 ~~6~~.50	1~~2~~.61	2.80
5 ~~6~~.50	1~~2~~.66	2.65
$\bar{X}$=5.435u	$\bar{X}$=1.65u	$\bar{X}$=2.77u

$\frac{20.95\%}{7.57u} \propto \frac{X\%O_2}{5.435u}$

$\frac{14.8\%}{6.65u} \propto \frac{X\%CO_2}{1.65u}$

$\frac{1210PPM}{5.5u} \propto \frac{X PPM CO}{2.77u}$

RUN A

O_2 = 15.0%

CO_2 = 3.7%

CO = 609PPM

RUN B)

O_2	CO_2	CO
5 ~~6~~.52	1.55	~~2.25~~ 2.25 − .08 = 2.17
5 ~~6~~.60	1.54	~~2.30~~ 2.25 − .08 = 2.17
5 ~~6~~.58	1.60	~~2.80~~ 2.30 − .09 = 2.21
5 ~~6~~.37	1.65	2.80 − .10 = 2.70
$\bar{X}$=5.52u	$\bar{X}$=1.585u	$\bar{X}$=2.31u

$\frac{20.95\%}{7.57u} \propto \frac{X\%O_2}{5.52u}$

$\frac{14.8\%}{6.65u} \propto \frac{X\%CO_2}{1.585u}$

$\frac{1210PPM}{5.5u} \propto \frac{X PPM CO}{2.31u}$

RUN B

O_2 = 15.3%

CO_2 = 3.5%

CO = 508PPM

RUN C)

O_2	CO_2	CO
5 ~~6~~.71	1.70	2.40 − .16 = 2.24
5 ~~6~~.58	1.50	2.35 − .17 = 2.18
5 ~~6~~.57	1.70	2.25 − .19 = 2.06
5 ~~6~~.60	1.55	2.70 − .20 = 2.50
$\bar{X}$=~~6.615u~~ 5.615	$\bar{X}$=1.61u	$\bar{X}$=2.245u

$\frac{20.95\%}{7.57u} \propto \frac{X\%O_2}{\cancel{6.615u}\ 5.615}$

$\frac{14.8\%}{6.65u} \propto \frac{X\%CO_2}{1.61u}$

$\frac{1210PPM}{5.5u} \propto \frac{X PPM CO}{2.245u}$

RUN C

O_2 = ~~18.3%~~ 15.5%

CO_2 = 3.6%

CO = 494PPM

O_{2AVG} = ~~16.2%~~ 15.3%

CO_{2AVG} = 3.6%

CO_{AVG} = 537PPM

SAN RAFAEL ROCK #2164
S-27 6/1/92

ISOKINETIC RATIOS

E.P.A. EQUATION 5-8

$$R_I = \frac{(T_s\,^\circ R)(V_o\ SDCF)(K_I)}{(V_s\ FPS)(100-\%H_2O)(A_n\ FT^2)(t_{MINUTES})(P_s\ IN\ Hg)}$$

$K_I = 9.414 \times 10^{-2}$ AT

$$P_s = P_{BAR} + \left(\frac{P_{STATIC}\ IN\ H_2O}{13.6\ IN\ H_2O/IN\ Hg}\right) = 29.95 + \left(\frac{-.35}{13.6}\right)$$

B.A.A.Q.M.D. STANDARD CONDITIONS OF 29.92" Hg AND 70°F

$P_s = 29.924$ "Hg

t = TIME = 50 MINUTES

$A_n = 8.454 \times 10^{-4} (D_{n\,cm})^2\ FT^2$

$D_n = 6.2\ mm = .62\ cm$

$A_n = 8.454 \times 10^{-4} (.62)^2\ FT^2$

$A_n = 3.25 \times 10^{-4}$

GROUP TERMS:

$$R_I = \frac{(T_s)(V_o)(9.414 \times 10^{-2})}{(V_s)(100-\%H_2O)(3.25 \times 10^{-4})(50)(29.924)} = \frac{(T_s)(V_o)(0.1936)}{V_s(100-\%H_2O)}$$

ROW A) $T_s = 745^\circ R$ $V_s = 47.0$ FPS $V_o = 26.60$ SDCF $\%H_2O = 18.8$ $100-\%H_2O = 81.2$

$$R_{IA} = \frac{(745)(26.60)(0.1936)}{(47.08)(81.2)} = 1.004 = \underline{\underline{1.00}}$$

ROW B) $T_s = 756^\circ R$ $V_o = 25.416$ SDCF $V_s = 46.33$ FPS $\%H_2O = 18.7$ $100-\%H_2O = 81.3$

$$R_{IB} = \frac{(756)(25.416)(0.1936)}{(46.33)(81.3)} = 0.988 = \underline{\underline{0.99}}$$

ROW C) $T_s = 745^\circ R$ $V_o = 24.802$ SDCF $V_s = 44.56$ FPS $\%H_2O = 18.6\%$ $100-\%H_2O = 81.4$

$$R_{IC} = \frac{(745)(24.802)(0.1936)}{(44.56)(81.4)} = 0.986 = \underline{\underline{0.99}}$$

SAN RAFAEL ROCK # 2164
S-27 6/1/92

GRAIN LOADING $G_{gr/SDCF} = 15.43 \frac{(WPg)}{(V_{o\,SDCF})}$

$G_A = 15.43 \frac{(0.0225)}{26.60} = 0.0131 = 0.013 gr/SDCF$ $W_{PA} = 0.0225g$

$W_{PB} = 0.0352g$

$G_B = 15.43 \frac{(0.0352)}{25.416} = 0.0214 = 0.021 gr/SDCF$

$W_{PC} = 0.0322g$

$G_C = 15.43 \frac{(0.0322)}{24.802} = 0.0200 = 0.020 gr/SDCF$ $V_{OA} = 26.60 SDCF$

$V_{OB} = 25.416 SDCF$

$G_{AVG} = 0.018 gr/SDCF$

$V_{OC} = 24.802 SDCF$

MASS EMISSIONS $M = \frac{G \cdot Q}{116.67}$ Lb/HR

$Q_o = 18053 SDCFM$

$M_A = \frac{(0.0131)(18053)}{116.67} = 2.0 Lb/HR$

$M_B = 3.3 Lb/HR$

$M_C = 3.1 Lb/HR$

$M_{AVG} = 2.8 Lb/HR.$

SOURCE TEST LAB DATA SHEET

PLANT: SAN RAFAEL ROCK & ASPHALT

PAGE: 1 OF 1

SOURCE OPERATION: ASPHALT BAGHOUSE

INITIAL: KC

SOURCE TEST NO.:

TEST DATE: 6/1/92

FILTER MEDIA: GLASS FIBER, 110 MM

FILTER DATA

RUN #	FILTER #	TARE WEIGHT(g)		FINAL WEIGHT(g)		TOTAL(g)
A	625	.6156	.6157	.6256	.6256	.0099
B	626	.6131	.6130	.6279	.6279	.0148
C	627	.6124	.6125	.6359	.6360	.0234
DATE/TIME		4/7(AM)	4/8(AM)	6/5(AM)	6/5(PM)	

PROBE & NOZZLE RINSE DATA

RUN #	JAR #	TARE WEIGHT(g)		FINAL WEIGHT(g)		TOTAL(g)
A	15	64.4354	64.4354	64.4480	64.4480	.0126
B	18	58.0733	58.0733	58.0938	58.0937	.0204
C	19	55.6727	55.6727	55.6815	55.6815	.0088
DATE/TIME		5/20(PM)	5/22(PM)	6/5(AM)	6/5(PM)	

TOTAL WEIGHTS (FILTER AND PROBE & NOZZLE)

RUN #	FILTER FINAL WT(g)	P & N FINAL WT(g)	TOTAL(g)
A	.0099	.0126	.0225
B	.0148	.0204	.0352
C	.0234	.0088	.0322

SOURCE TEST LAB DATA SHEET

PLANT: SAN RAFAEL ROCK & ASPHALT
SOURCE OPERATION: ASPHALT BAGHOUSE.
SOURCE TEST NO.:
FILTER MEDIA:

PAGE 1 OF 1
INITIAL KC
TEST DATE 6/1/92

Drying Procedure: *105 °C 24 hours before and after test, desiccated*

FILTER DATA

RUN NO.	FILTER NO.	TARE WEIGHT (g) 4/7 (Am)	4/8 (Am)	FINAL WEIGHT (g) 6/5 (Am)	6/5 (pm)	SAMPLE WEIGHT (g)
A	625	.6156	.6157	.6256	.6256	
B	626	.6131	.6130	.6279	.6279	
C	627	.6124	.6125	.6359	.6360	

PROBE & NOZZLE RINSE DATA (total all runs)

RUN NO.	FILTER NO.	JAR SAMPLE FINAL WEIGHT (g)	FILTER SAMPLE FINAL WEIGHT (g)	SAMPLE WEIGHT (g)
A				
B				
C				

PROBE & NOZZLE RINSE DATA (each run)

RUN NO.	PROBE/NOZZLE NOS.	JAR TARE WEIGHT (g)		JAR FINAL WEIGHT (g)		JAR SAMPLE WEIGHT (g)
A	15	64.4354	64.4354	64.4480	64.4480	
B	18	58.0733	58.0733	58.0938	58.0937	
C	19	55.6727	55.6727	55.6815	55.6815	
		5/20 (pm)	5/22 (pm)	6/5 (Am)	6/5 (pm)	

IMPINGER DATA

SOLUTION	NO.	A TARE WEIGHT	B FILLED WEIGHT	C FINAL WEIGHT	C-A SAMPLE WEIGHT	C-B CONDENSATE WEIGHT

~~56500~~ TIME 21 min ~~5651~~ 5652500

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Source Test Data Sheet

16,000 / 21.583 = 741.3 CFM

Source Operation	S-27		
Plant	SAN RAFEL ROCK #2164		
Sample Type	PARTICULATE & COMBUSTION		
Process Cycle	B/H STACK		
Duct Size	R-47"	R-47"	227 / 102
Duct Pressure	-.35" H_2O		329 / -200 / 129
ASSUMED H_2O	18%		

I_{60} = .826

Source Test No.		
Run No.	T&A	
Date:	6/1/92	

6.2 mm	Nozzle Diameter
P-44 .829	Pitot Tube
VAN #12	Gas Collector No.
29.95	Barometric Pressure
0.003 at 20	Leak Rate
5	TIME EACH POINT
10	# OF POINTS
50	TIME EACH RUN

MAG GAGE RACK # V12-111 METER (γ) = 1.000

Sampling Train: PROBE ⇒ FILTER # ____ ⇒ IMP# P-1 IMP# P-2 ⇒ PUMP# VAN #12 ⇒ METER# 510950 ⇒ EXH.

Traverse Point	Dist. From WALL inches	INITIAL TRAVERSE Duct Temp °F	INITIAL TRAVERSE ΔP H_2O	SAMPLING Traverse Point	ΔP H_2O	V_s FPS	0809 Time	METER Rate CFH	METER Temp °F	METER Volume Ft^3	Vac "Hg	Sat'd Gas Temp °F	T_s Duct Temp °F	REMARKS
T_s = 303°F, $C_p I_{p.60}$ = .826							0			754.06				
A-1 .25	1.2	B-1	.24	B-1	.34	38.0	5	27.3	60	56.33 / 756.35	7	34	235	
2 .35	3.8		.34	2	.38	40.7	10	28.5	60	58.72 / 758.73	7	41	253	
3 .42	6.9		.39	3	.41	42.8	15	29.2	61	61.16 / 761.18	8	41	272	
4 .42	10.6		.42	4	.39	42.1	20	28.3	61	63.53 / 763.56	7.5	41	283	
5 .43	16.1		.42	5	.43	44.6	25	29.4	61	66.01 / 766.03	8.5	41	298	
6 .47	30.9		.47	6	.50	48.4	30	31.5	62	68.66 / 768.58	10	41	306	
7 .50	36.4		.47	7	.54	50.3	35	32.7	62	71.31 / 771.33	11	42	306	
8 .49	40.1		.46	8	.57	51.7	40	33.6	63	74.13 / 774.18	14	42	307	
9 .50	43.2		.47	9	.65	55.2	45	35.9	64	77.17 / 777.19	15	42	306	
10 .48	45.8		.45	10	.62	53.9	~~0809~~ ~~0909~~ 50	35.1	64	80.11 / 780.21	14	42	306	
ΔP = .45							0859		61.8	26.15	10.2	40.7	287.6	
T_s = 763°R									521.5	X 1.000 / 26.15 Ft^3			745	

$$D_n = 13.7\left[\frac{\cancel{T_s + 460}\ 763°R}{\cancel{V_s}\ 45.6\ \cancel{(100-\%H_2O)}\ 82}\right]^{1/2} = 6.2\,mm$$

Condensate 129 (g)

V_o 26.60 SCF

$\%H_2O$ 18.7%

$$Q_m = \left[(2.638 \times 10^{-3})\ \cancel{(100-\%H_2O)}\ 82\ D_{mm}^2\right]\frac{V_s}{T_s}$$

$(6.2)^2$

$$V_s = (K)(C_p)\sqrt{T_s \cdot \Delta P''}$$

2.983, I = .826, R = .826

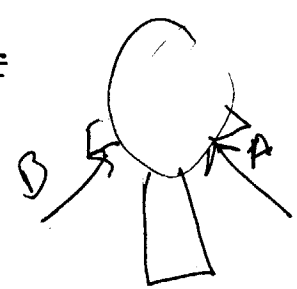
$$K = \frac{85.49}{\sqrt{(P_b \pm \frac{P_d}{13.6})\,MW}} = 2.983$$

$$V_o = \frac{17.71\,(V_m)(P_b)}{T_m\ °R} = 26.60\ SCF$$

26.15, 29.95, 521.5

$$\left[(29.95 - \frac{.35}{13.6})\,27.45\right]^{1/2}$$

28.6604



B-SITUATION

Source Test Team
CHUCK McCLURE
Source Test Engineer II
H. DOI
OVER THE TOP

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939 Ellis Street, San Francisco, Calif. 94109 • 771-6000

Source Test Data Sheet

Source Operation: S-27
Plant: S/R Roch #2164
Sample Type: PARTICULATE & COMBUSTION
Process Cycle: B/H STACK
Duct Size: R-47"
Duct Pressure: -.35" H_2O
ASSUMED H_2O: 18%

Source Test No.:
Run No.: B
Date: 6/1/92

6.2 min Nozzle Diameter
.829 Pitot Tube
VAN #12 Gas Collector No.
29.95 Barometric Pressure
0.0020 @ 22 Leak Rate
5 TIME EACH POINT
10 # OF POINTS
50 TIME EACH RUN

MAG GAGE RACK # V12-111 METER (Y) = 1.000

Sampling Train: PROBE ⇒ FILTER # ____ ⇒ IMP # P-3 IMP # P-4 ⇒ PUMP # VAN #12 ⇒ METER # 510950 ⇒ EXH.

Traverse Point	Dist. From inches	INITIAL TRAVERSE Duct Temp °F	INITIAL TRAVERSE ΔP H_2O	Traverse Point	ΔP "H_2O	V_s FPS	Time (0916)	METER Rate CFH	METER Temp °F	METER Volume Ft³	Vac "Hg	Sat'd Gas Temp °F	T_s Duct Temp °F	REMARKS
					.36	42.4	0	28.8		780.54			221	
				A-1	.41	42.8	5	29.2	66	82.97 782.93	7.5	35	272 274	
				2	.42	43.7	10	29.3	67	85.37 785.40	8	38	284	
				3	.42	43.7	15	29.3	67	87.84 787.85	8.5	38	285	
				4	.42	44.2	20	29.0	68	90.27 790.32	9	39	300	
				5	.41	43.7	25	28.6	68	92.70 792.62	8.5	41	302	
				6	.48	47.4	30	30.9	69	95.20 795.23	9.5	40	304	
				7	.50	48.3	35	31.6	70	97.86 797.85	10	41	304	
				8	.50	48.3	40	31.6	70	100.48 800.47	10	40	304	
				9	.53	49.7	45	32.5	69	103.18 803.15	10.5	41	302	
				10	.52	49.2	50	32.2	69	105.84 805.84	10	41	302	
							(1006)		68.3	25.30	(9.15)	(39.4)	296.1	
									528	X1.000 25.3047 ft³			(756)	

$$D_n = 13.7\left[\frac{T_s + 460}{V_s(100-\%H_2O)}\right]^{1/2}$$

$$Q_{in} = \left[(2.638 \times 10^{-3})\ (100-\%H_2O)\,D_{nun}^2\right]\frac{V_s}{T_s}$$

$$V_s = (K)(C_p)\sqrt{T_s \cdot \Delta P''}$$

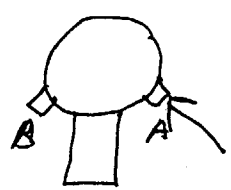
$$K = \frac{85.49}{\sqrt{(P_b \pm P_d/13.6)\,MW}}$$

25.30 29.95

$$V_o = \frac{17.71\,(V_m)(P_b)}{T_m\ °R} = (25.416\ SCF)$$

528

Condensate (g)
V_o ____ SCF
%H_2O ____



Source Test Team
CHUCK McCLURE
Source Test Engineer II

H. WOI
B-STATION
OVER THE TOP

33806000
33811000 TIME ~~8min 9sec~~ 13MIN 9SEC
5000

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Source Test Data Sheet

$\frac{5000}{13.15 MN} = 380$ CFM

Source Operation	S-27	6.2mm	Nozzle Diameter
Plant	S/R Rock #2164	.829	Pitot Tube
Sample Type	PART & COMB	VAN#12	Gas Collector No.
Process Cycle	B/H STACK	29.95	Barometric Pressure
Duct Size	R-47"	0.003 at 19	Leak Rate
Duct Pressure	-.35" H_2O	5	TIME EACH POINT
ASSUMED H_2O	18%	10	# OF POINTS
		50	TIME EACH RUN

Source Test No. _____
Run No. C
Date: 6/1/92

MAG GAGE RACK # V12-111 METER(γ) = 1.000

Sampling Train: PROBE ⇒ FILTER # _____ ⇒ IMP# P-5 IMP# P-6 ⇒ PUMP# VAN#12 ⇒ METER# 510950 ⇒ EXH.

Traverse Point	Dist. From inches	INITIAL TRAVERSE Duct Temp °F	ΔP H_2O		SAMPLING Traverse Point	ΔP "H_2O	V_s FPS	(1039) Time	METER Rate CFH	Temp °F	Volume Ft^3	Vac "Hg	Sat'd Gas Temp °F	T_s Duct Temp °F	REMARKS
								0			816.84				
					A-1	.40	41.2	5	29.6	72	19.31 819.34	9	38	235	
					2	.39	41.3	10	28.8	72	21.74 821.78	8.5	40	254	
					3	.50	47.6	15	32.0	71	24.45 824.47	10	41	281	
	30 SEC → PLANT OFF/OFF				4	.45	45.5	20	30.2	70	26.99 827.00	10	41	291	
					5	.45	45.5	25	30.2	70	29.51 829.50	9.5	40	293	
					6	.45	45.7	30	30.0	71	32.00 832.00	9.5	41	299	
					7	.47	46.7	35	30.7	71	34.56 834.54	10	41	300	
					8	.41	43.6	40	28.6	71	36.93 836.94	9	41	300	
					9	.42	44.1	45	29.0	71	39.36 839.35	9	41	299	
					10	.38	42.0	50	27.6	72	41.65 841.66	8	42	298	
								1130		71.1	24.82	9.25	40.6	285	
										530.8	x1.000			745	
											24.82 ~~SDCF~~ Ft^3				

$$D_n = 13.7\left[\frac{T_s + 460}{V_s(100-\%H_2O)}\right]^{1/2}$$

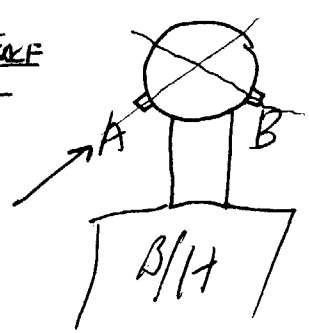
$$Q_m = \left[(2.638 \times 10^{-3})\ (100-\%H_2O)\,D_{nun}^2\right]\frac{V_s}{T_s}$$

$$V_s = (K)(C_p)\sqrt{T_s \cdot \Delta P''} \qquad K = \frac{85.49}{\sqrt{(P_b \pm \frac{P_d}{13.6})\,MW}}$$

$$V_o = \frac{17.71\,(\cancel{V_m})(P_b)}{\cancel{T_m}\ R} = 24.802\ SDCF$$

24.82 29.95
530.8

Condensate (9)
V_o SDCF
$\%H_2O$ _____



Source Test Team
CHUCK McCLURE
Source Test Engineer II
H. DOI

PLANT: SAN RAFEL ROCK

DATE: 6/1/92

ADDRESS:

OPERATOR: GEORGE

PLANT #: 2164

A/C

1) What are you producting: 1/4", 1/2", 3/4"

2) What rate are you producing at: 175 A&B 160 C Tons/Hour - Average

3) What is your maximum rate of production: Tons/Hour

4) How much will you produce today: 896 TONS Tons-Average

5) What type of fuel are you burning: ~~PROP~~ NAT'L GAS

6) What is your rate of fuel useage: READ

7) What is your baghouse inlet temperature averaging: ≈ 348°F

8) What is your baghouse differential pressure: 3.8 "H_2O

9) What is the mositure content of the agregate: 1.6 % H_2O

10) Are there any abnormal conditions in the plant today: NO

Thank You

COMB