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CORRESPONDENCE/MEMORANDUM

Received 10/14/91

File Code: 4530

DATE: 10/17/91

PRELIMINARY STACK TEST REVIEW

By: Marty Burchholder Test Date: 9/19/91

Name of Source: Biehl Construction FID #: 999011970

Address: 26567 Campbell Road

City: Town of Byron Permit #: 999011970-001

Description of Source Tested: Asphalt Plant - 180 TPH Barber Greene Batch Mix

Description of Control Equipment: Astec Bayhouse

Test Firm: Badger Laboratories & Engineering Co. Inc.

Crew Chief & Phone#: Bruce Lamers 414/739-9213

Pollutant Tested: Part. Test Method: US EPA 5

Pollutant Tested: Formaldehyde Test Method: NIOSH 3500

Pollutant Tested: Test Method:

Test Production Level: @ 155 TPH (86% of rated) ~~Aggregate~~ Aggregate - wet

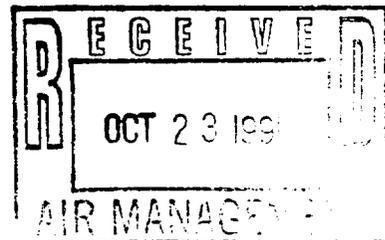
Rated Production Level: 180 TPH

Discussion of Results:

The stack test is invalid and will have to be redone because

The test average result of 0.007 lbs/1000 lbs. stack gas is X is not in compliance with the emission limit of 0.3 lbs/1000 lbs stack. Formaldehyde = 0.586 lb/hr. 0.67 lbs/hr. 40 lbs/hr.

cc: Joe Perez-AM/3 US EPA Region V



PARTICULATE CHECKLIST

Name of Source: Biehl Construction Test Date: 9/19/91

1. Are the isokinetics per run between 90 and 110%? YES NO
If the %I for a run is outside the range, void the run. See 5.
2. Is the sample volume per run \geq 30 DSCF? YES NO
If the sample volume for a run is $<$ 30 DSCF, void the run. See 5.
3. Is the sample time per run \geq 60 min.? YES NO
If the sample time for a run is $<$ 60 min., void the run. See 5.
4. Is the sample time per sample point \geq two min.? YES NO
If the sample time per point for a run is $<$ two min., void the run. See 5.
5. A stack test shall consist of three valid runs or, at a minimum, two valid runs if one run is voided. Is this a valid test? YES NO
If no, inform the District or the source that the test is unacceptable and should be redone. Your review is over.
6. Is the total particulate per run added correctly? YES NO
If an incorrect total is found, call the consultant and ask for a correction.
7. Was the backhalf included in the total particulate? YES NO
NSPS sources are exempt from including the backhalf. All other sources must include the backhalf. If they don't, the test is invalid. See 5.

Eq. 1 $Gr/DSCF = 15.43 * g \text{ of part./sample volume of run in DSCF}$

Eq. 2 $Lb/DSCF = (Gr/DSCF)/7000$

Eq. 3 $Lb/Hr = 60 * DSCFM * (Lb/DSCF)$

Eq. 4 $Lb/10^6 \text{ BTU} = (Lb/DSCF) * F \text{ Factor} * 20.9 / (20.9 - \text{Stack } O_2)$

8. If the emission limit is in Gr/DSCF, Lb/DSCF, Lb/Hr, or Lb/10⁶ BTU, solve Eq. 1-4. Do your results match the consultant's? YES NO
If no, fix the problem or call the consultant for a correction.
9. Is the three run(or two run) average correct? YES NO
If no, write in the correct average.
10. Is the average result in compliance? YES NO
If no, the District should issue an NOV.
11. Was the source operating at a level representative of full capacity? YES NO
If no, the permit release may need to provide conditions to cap the source at the test level until a stack test at a higher production level(showing compliance) is performed. If the test was not for permit release, other actions may be warranted.

Biehl Construction Asphalt Plant Emission Test

I. Introduction and Summary

Badger Laboratories & Engineering Co., Inc. was retained by Biehl Construction to determine the concentration of Particulate, Formaldehyde and Visible emissions in the exhaust from an Asphalt Plant located at W5659 Campbell Road, in the Town of Byron; Fond du Lac County. A Fabric Filter collection device is in place.

Emission tests were conducted September 19, 1991 by Bruce Lamers and Marcus Klaeser. Mr Jeff Jennerjohn, certified by the WDNR on April 10, 1991 performed the visual emission tests. Mr. Martin Burkholder from the Wisconsin Department of Natural Resources was present to witness the tests. Testing was performed following U.S. EPA Methods. Mr. Steve Biehl is the company contact.

A summary of the Particulate results are as follows:

PARTICULATE EMISSION RESULTS

Test Run	Volumetric Flow Rate <u>scfh</u>	Isokinetic Ratio, % <u>Ratio, %</u>	Particulate Emission <u>lb/hr.</u>	lbs./1000# <u>stack gas</u>
1	1.059x10 ⁶	102.9	0.78	0.008
2	1.038x10 ⁶	103.7	0.65	0.007
3	1.004x10 ⁶	104.2	0.59	0.006

Ave 103.6 Ave .67 Ave 0.007

The arithmetic average of the results is 0.007 lbs./1000 lbs. stack gas. The limitation for this source is given as 0.3 lbs./1000 lbs. stack gas. This source is operating at 2% of the limitation.

Location: Biehl Construction
Date: 9-19-91
Time: 7:46 - 8:52 AM
Test Run: #1

Stack Gas Data:

Temperature, °F.	175.7
Velocity, ft./sec.	40.176
Gas Volume, ACFM	27,068
Gas Volume, SCFM (Wet)	22,182
Gas Volume, SCFM (Dry)	17,657
Moisture, %	20.4
Carbon Dioxide, % (Dry)	4.3
Oxygen, % (Dry)	15.7
Carbon Monoxide + Nitrogen, % (Dry)	80.0
Molecular Weight (Wet)	27.007

Sampling Data:

Total Time, min.	60
Volume, SCF (Dry)	43.582
Isokinetic Ratio, %	102.9

Particulate:

Amount Collected, mg. (including condensable)	14.5
Concentration, grains/SCF	0.005
Emission Rate, lb/hr.	0.78
Emission Rate, lb/1000 lb stack gas	0.008

Location: Biehl Construction
Date: 9-19-91
Time: 10:30 - 11:35 AM
Test Run: #2

Stack Gas Data:

Temperature, °F.	175.7
Velocity, ft./sec.	39.902
Gas Volume, ACFM	26,884
Gas Volume, SCFM (Wet)	22,031
Gas Volume, SCFM (Dry)	17,294
Moisture, %	21.5
Carbon Dioxide, % (Dry)	5.3
Oxygen, % (Dry)	14.6
Carbon Monoxide + Nitrogen, % (Dry)	80.1
Molecular Weight (Wet)	26.974

Sampling Data:

Total Time, min.	60
Volume, SCF (Dry)	43.048
Isokinetic Ratio, %	103.7

Particulate:

Amount Collected, mg. (including condensable)	12.3
Concentration, grains/SCF	0.004
Emission Rate, lb/hr.	0.65
Emission Rate, lb/1000 lb stack gas	0.007

Location: Biehl Construction
Date: 9-19-91
Time: 1:00 - 2:05 PM
Test Run: #3

Stack Gas Data:

Temperature, °F.	181.8
Velocity, ft./sec.	39.338
Gas Volume, ACFM	26,504
Gas Volume, SCFM (Wet)	21,520
Gas Volume, SCFM (Dry)	16,743
Moisture, %	22.2
Carbon Dioxide, % (Dry)	5.2
Oxygen, % (Dry)	14.1
Carbon Monoxide + Nitrogen, % (Dry)	80.7
Molecular Weight (Wet)	26.866

Sampling Data:

Total Time, min.	60
Volume, SCF (Dry)	41.860
Isokinetic Ratio, %	104.2

Particulate:

Amount Collected, mg. (including condensable)	11.2
Concentration, grains/SCF	0.004
Emission Rate, lb/hr.	0.59
Emission Rate, lb/1000 lb stack gas	0.006

FORMALDEHYDE EMISSION RESULTS

<u>Test Run</u>	<u>V_{std}, ft.³</u>	<u>Formaldehyde</u>	
		<u>mg.</u>	<u>lb/hr.</u>
1	1.139	0.3644	0.747
2	1.062	0.2631	0.567
3	1.047	0.2101	0.444

The arithmetic average of the three results is 0.586 lb/hr. The Nr 445 limitation for Formaldehyde is 250 lb/year.

OPACITY EMISSION RESULTS

<u>Test Run</u>	<u>Highest 6 Min. Ave.</u>	<u>Hourly Ave.</u>
1	4.6	2.8
2	5.4	3.9
3	5.6	4.5

The limitation for this source is 40%.

II. Process Description

The stack carries exhaust gases from a Barber Greene Batch Mix Asphalt Plant rated at 180 tons/hr. The burner is fired with waste oil meeting the specifications of the permit. There is no recycle material used in the mix. An Astec baghouse is used to control Particulate Emissions.

The following is a summary of the Process Data:

Process Data

<u>Test Run</u>	<u>Asphalt Tons/hour</u>	<u>Pressure Drop Across Baghouse, in H₂O</u>
1	147	3.0
2	160	3.0
3	159	3.0

Formaldehyde Laboratory Data

	Test Run			
	<u>1</u>	<u>2</u>	<u>3</u>	<u>Blank</u>
Collection Solution Volume 1% Bisulfite, 20 mls/impinger	45	45	45	---
Volume Analyzed - impinger 1	1	1	1	
- impinger 2	4	4	4	4
Absorption - impinger 1	0.711	0.512	0.407	
- impinger 2	0.008	0.005	0.005	0.006
Calibration Curve Data:				
Standard Curve	<u>Blank</u>	<u>1 ppm</u>	<u>2 ppm</u>	<u>4 ppm</u>
	0.001	0.038	0.088	0.196

correlation coefficient = .9972
intercept = 0

Formaldehyde - Field Data

<u>Test Run</u>	<u>Time</u>	<u>V_{std}, ft.³</u>	<u>Flow Rate (Liters)</u>
1	7:55-8:25	1.139	1
2	10:35-11:10	1.062	1
3	1:05-1:35	1.047	1

Calculations

V _{std} , ft. ³	=	Sample Air Volume
Mn Formaldehyde	=	mg. Formaldehyde
C _s Formaldehyde	=	2.205 x 10 ⁻⁶ $\frac{Mn}{V_{std}}$
Q _s scfh	=	Volumetric Flow Rate
lb/hr. Formaldehyde	=	C _s formaldehyde x Q _s

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A summary of the Particulate results are as follows:

PARTICULATE EMISSION RESULTS

<u>Test Run</u>	<u>Volumetric Flow Rate</u> <u>scfh</u>	<u>Isokinetic Ratio, %</u>	<u>Particulate Emission</u> <u>lb/hr.</u>	<u>lbs./1000#</u> <u>stack gas</u>
1	1.059x10 ⁶	102.9	0.78	0.008
2	1.038x10 ⁶	103.7	0.65	0.007
3	1.004x10 ⁶	104.2	0.59	0.006

The arithmetic average of the results is 0.007 lbs./1000 lbs. stack gas. The limitation for this source is given as 0.3 lbs./1000 lbs. stack gas. This source is operating at 2% of the limitation.

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		<u>mg.</u>	<u>lb/hr.</u>
1	1.139	0.3644	0.747
2	1.062	0.2631	0.567
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3	5.6	4.5

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II. Process Description

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Process Data

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2	160	3.0
3	159	3.0

III. Comments

The testing on September 19, 1991 was performed without any problems to note. The production rate of 82% to 89% of the 180 tons/hour rating of the plant was the maximum production rate that day. The aggregate to be dried had a high moisture content due to recent rains.

IV. Stack Testing and Analytical Procedures

The procedures for sampling, testing, instrumentation and analysis as described by the U.S. EPA were followed. The EPA reference methods used in the testing program are summarized below.

Method 1: Sample and Velocity Traverse Locations

The sampling site lies in a straight section of 49" x 33" rectangular steel stack. The sampling ports (6) are 5.1 diameters downstream and 1.2 diameter upstream from the last flow disturbance. Twenty-four points were sampled, four on each traverse.

Sampling time was 2.5 minutes per point. The location of the ports and traverse points is shown below:

Location of Ports and Traverse Points From Stack Wall

Inside Stack Diameter = 49" x 33"

	<u>Sample Port Location from side wall</u>	<u>Sample Point Location from back wall</u>
1	4.1"	4.12"
2	12.2"	12.37"
3	20.4"	20.62"
4	28.6"	28.87"
5	36.7"	
6	44.9"	

Method 2: Stack gas velocity and Volumetric Flow Rate

For each test run, a velocity traverse was made with a calibrated "S" pitot tube having a co-efficient of 0.840. The velocity head was read on an inclined manometer to the nearest 0.01 inches of water. Temperature was measured with a chromel-alumel thermocouple.

Sampling site barometric pressure was read on site with a barometer and subsequently verified from National Weather Service data.

Method 3: Component Gas Analysis

Analysis for Carbon Dioxide (CO₂), Oxygen (O₂), and Nitrogen plus Carbon Monoxide (N₂ + CO) were performed in the field using an Orsat type analyzer. Prior to testing, the Orsat apparatus was checked for leaks and the activity of the absorbing solution was determined to be adequate. Results were read and recorded to the nearest 0.2 percent volume, dry basis.

Method 4: Moisture Content

The moisture content of the stack gas was determined by condensing in three impingers in an ice bath and absorbing any remaining moisture in a fourth impinger containing silica gel.

Method 5: Particulate Emission

Particulate material is withdrawn isokinetically from the stack and collected on a glass fiber filter maintained in the temperature range of 223° F. - 273° F. The sample gas stream is dried as in Method 4 above. The sample gas is then passed through a metering system which measures both the cumulative volume of gas sampled and the instantaneous sampling rate.

Sampling Train

A schematic of the sampling train used in this method is shown in Figure 5-1 (See Page #6). The sampling train consists of the following components:

- Stainless steel, buttonhook-type nozzle.
- Teflon tape gasket.
- Stainless steel probe.
- Fritted glass filter holder.
- Electrically heated enclosed sample box.
- Ice-water bath.
- Modified Greenburg-Smith impinger.
- Greenburg-Smith impinger.
- Modified Greenburg-Smith impinger.
- Modified Greenburg-Smith impinger.
- Check valve.
- Vacuum tube.
- Vacuum gauge.
- Main Valve.
- Leak-free vacuum pump.
- By-pass valve.
- Dry gas meter.
- Calibrated orifice.
- Dual manometer.
- Type "S" pitot tube.

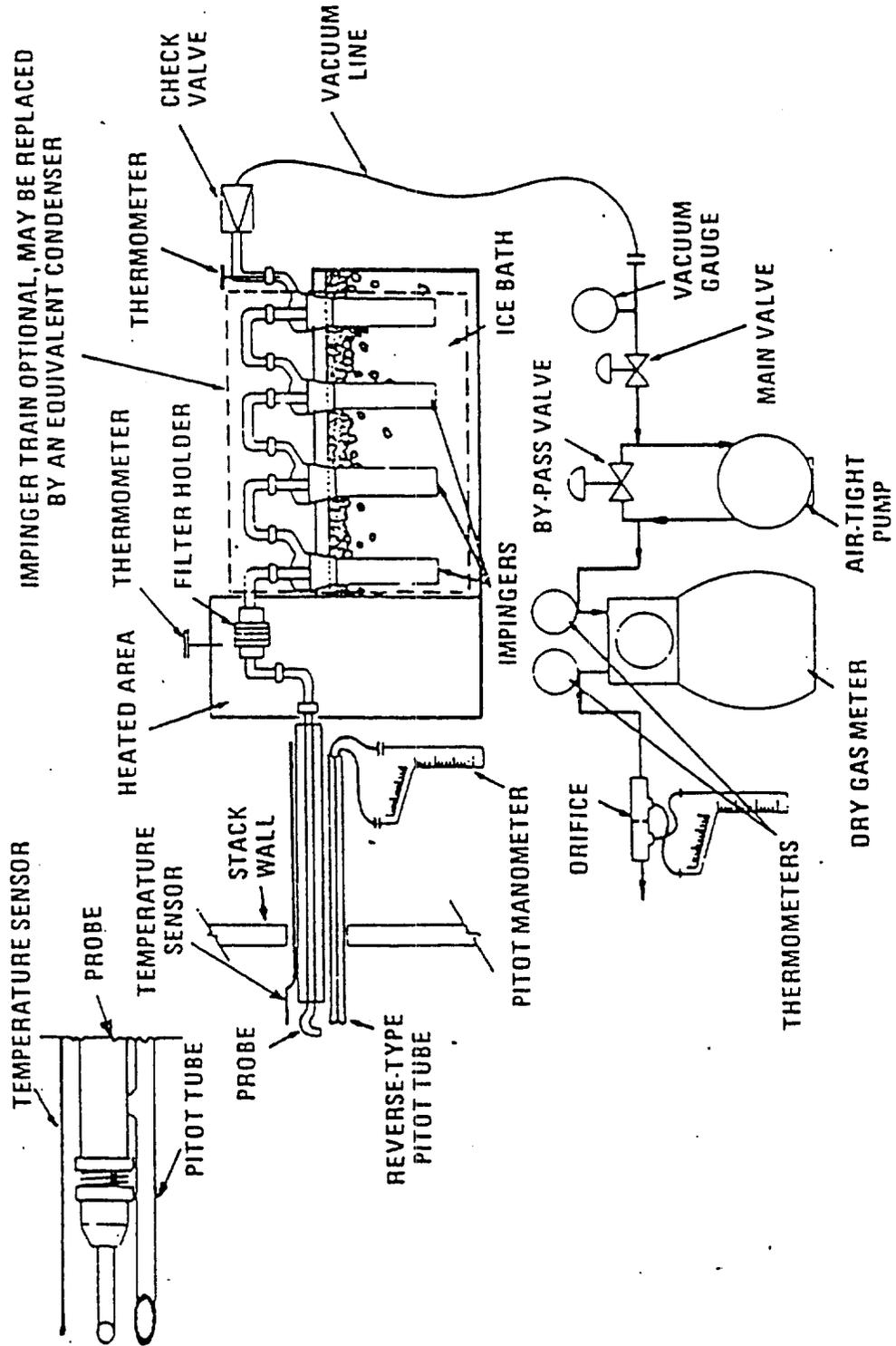


Figure 5-1. Particulate sampling train.

A more detailed description of the sampling train components follows:

1. Probe Nozzle: Stainless steel with sharp, tapered leading edge. A 0.287 inch diameter (as measured on site with a caliper) nozzle was used in all tests.
2. Probe Liner: Stainless steel with a heating system to maintain a gas temperature at the exit during sampling of 223° F. to 273° F.
3. Pitot Tube: A Type "S" pitot tube attached to the probe allowed constant monitoring of the stack gas velocity. The pitot tube has a coefficient of 0.840. ΔP was read from an inclined manometer.
4. Differential Pressure Gauge: A Dwyer magnehelic gauge with a range of 0 - 10 inches water was used to obtain ΔH .
5. Filter Holder: Borosilicate glass, with a glass frit filter support and a silicone rubber gasket.
6. Filter Heating System: Thermostat controlled electrical resistance type heater capable of maintaining a temperature of 223°F. - 273°F. around the filter holder.
7. Impingers: Four pyrex glass impingers connected in series with a leak-free ground glass fitting. The first, third, and fourth impingers were Greenburg-Smith design with a modified (straight) tip. The second impinger was a Greenburg-Smith design with a standard tip. A thermometer was in place to measure the temperature at the outlet of the fourth impinger.
8. Metering System: The vacuum gauge, leak-free pump, thermometer, temperature compensated dry gas meter, and related equipment are shown in Figure 5-1. The sampler is a LSI Model 31.

Sampling Procedures

Prior to testing, the sampling train is cleaned and set up as follows:

A four-inch diameter glass fiber filter was dried in a 105°C. oven overnight. The filter was then placed in a desiccator for two hours and weighed on an analytical balance to the nearest 0.1 milligram (mg.). One hundred milliliters (ml.) of distilled water was placed in each of the first two impingers. Two hundred grams dry silica gel (indicating) was placed in the fourth impinger. The third impinger was left dry and empty. The sampling train was assembled as shown in Figure 5-1 (Page #6). Based on the preliminary velocity and temperature traverse, an appropriate nozzle size was selected to provide an adequate sampling rate.

After assembly, the sampling train was leak-checked at the inlet to the nozzle at 15 inches mercury vacuum. If a leak rate of greater than 0.02 ft.³/min. was observed, the system was checked and leaks corrected. The leak-check procedure was repeated until the leakage rate was less than 0.02 ft.³/min.

Approximately one half hour before the start of the test, the probe and filter box heaters were turned on and allowed to warm up to sampling temperatures. Ice was placed around the impingers. At the start of a test run, the dry gas meter reading was recorded on the data sheet, the probe was placed in the stack at the first sampling point, and the velocity pressure was read. Using an isokinetic flow rate calculator, the desired orifice meter pressure was determined. The sample pump was then turned on and the time was recorded. The main and by-pass valves were immediately adjusted to give the desired sampling rate. For each point, the following data was recorded: Traverse Point Number, Sampling Time, Stack Temperature, Velocity Head, Orifice Meter Reading, Dry Gas Meter Volume, Meter Temperature, Box Temperature, and Pump Vacuum. Near the end of the sampling time (approximately 10 seconds remaining), the nozzle was moved to the next point and exactly at the start of the next sampling period, the dry gas meter volume was recorded. The point by point sampling procedures were then repeated until the test run was completed. While moving between ports, the pump was turned off. At the completion of the test run, the pump was turned off, the dry gas meter volume recorded, and the probe was removed from the stack. The sampling train was leak-checked from the sample nozzle at the highest vacuum pulled during the test to verify the leak-free integrity of the system.

Sample Recovery

Sample recovery of the probe and probe nozzle was accomplished near the sampling site. The inner surfaces of each was rinsed with acetone along with cleaning by a brush until no visible particulate was present in the rinse. The impingers and filter holder contents were recovered back at the lab. The contents of the first three impingers were measured volumetrically and placed in a clean container. The silica gel in the fourth impinger was transferred to a clean, dry container and weighed. The filter was carefully transferred to a petri dish. Any filter material which stuck to the gasket was scraped loose and transferred to the petri dish. The upstream portion of the filter holder was washed with acetone. The wash from the filter holder was combined with the washes from the probe and probe nozzle. The container was labelled to identify the test run.

Sample Analysis

In the laboratory, the filter and any loose particulate were placed in a desiccator for 24-hours. The material was then weighed on an analytical balance to the nearest 0.1 mg.

The volume of the upstream acetone wash was measured and transferred to a tared beaker. The acetone was evaporated at room temperature. After desiccation, the beaker was reweighed. Simultaneously, a 100 ml. acetone blank was evaporated and the residue weight was determined. The net residue weight of the sample washes has been adjusted for the acetone blank.

The water collected from the first three impingers was measured to the nearest ml. All the sample exposed glassware was rinsed with acetone and placed in a separate clean, dry container. This was evaporated in the same manner as the probe wash. The water collected was extracted with 3-50 ml. portions of methylene chloride. The extracts were evaporated in a tarred beaker at 20°C. A 100 ml. portion of the remaining water was evaporated in a tarred beaker at 103°C. The two weight gains were included in the total particulate. The total particulate collected is then the summation of the acetone wash weight gain plus the filter weight gain, plus the water extract weight gain plus the water residue weight gain.

The silica gel from each run was weighed to the nearest 0.1 gr. The weight gain of the silica gel was added to the volume of the liquid water collected in the first three impingers to obtain the total amount of water collected.

Particulate Emission Rate Equation

- 1). Volume, DG Meter scf wet = $\frac{\text{Volume, DG Meter scf dry}}{(1 - B_{wo})}$
- 2). Particulate, lbs./scf wet = $\frac{\text{Particulate, mg. } (2.205 \times 10^{-6})}{\text{Volume, DG Meter scf wet}}$
- 3). $C''_s = C_s \frac{1}{R} \frac{1}{M_s} 1000$

where...

B_{wo} = Proportion of water vapor in gas stream.

C''_s = Concentration of particulate, lbs./1000 lbs. stack gas-wet.

C_s = Concentration of particulate, lbs./scf - wet.

R = Ideal gas constant $\frac{1 \text{ lb. - mole}}{386 \text{ scf}}$

M_s = Molecular weight of stack gas, wet $\frac{\text{lb.}}{\text{lb. mole}}$

FORMALDEHYDE TEST METHOD

NIOSH Method 3500 was followed for sampling and analysis of formaldehyde. A sampling rate of one liter per minute for 30 minutes was performed. The two midget impingers contained 20 mls. of 1% Sodium Bisulfite solution. Formaldehyde was analyzed using the Chromatropic Acid Colormetric Procedure. The sampling system used was a Napp, Inc.; Model 63 Gas Sampling System. The system consist of a diaphragm pump, rotameter and dry gas meter with inlet and outlet thermometers.

Data Handling and Calculations

All mathematical calculations were made according to accepted techniques using U.S. EPA equations. Standard conditions of 29.92 inches mercury pressure and 68°F. temperature were used. Field calculations were rechecked, and the final results for each test run are presented in detail in the Appendix.

Appendix

Location: Biehl Construction
Date: 9-19-91
Time: 7:46 - 8:52 AM
Test Run: #1

Stack Gas Data:

Temperature, °F.	175.7
Velocity, ft./sec.	40.176
Gas Volume, ACFM	27,068
Gas Volume, SCFM (Wet)	22,182
Gas Volume, SCFM (Dry)	17,657
Moisture, %	20.4
Carbon Dioxide, % (Dry)	4.3
Oxygen, % (Dry)	15.7
Carbon Monoxide + Nitrogen, % (Dry)	80.0
Molecular Weight (Wet)	27.007

Sampling Data:

Total Time, min.	60
Volume, SCF (Dry)	43.582
Isokinetic Ratio, %	102.9

Particulate:

Amount Collected, mg. (including condensible)	14.5
Concentration, grains/SCF	0.005
Emission Rate, lb/hr.	0.78
Emission Rate, lb/1000 lb stack gas	0.008

Location:	Biehl Construction
Date:	9-19-91
Time:	10:30 - 11:35 AM
Test Run:	#2

Stack Gas Data:

Temperature, °F.	175.7
Velocity, ft./sec.	39.902
Gas Volume, ACFM	26,884
Gas Volume, SCFM (Wet)	22,031
Gas Volume, SCFM (Dry)	17,294
Moisture, %	21.5
Carbon Dioxide, % (Dry)	5.3
Oxygen, % (Dry)	14.6
Carbon Monoxide + Nitrogen, % (Dry)	80.1
Molecular Weight (Wet)	26.974

Sampling Data:

Total Time, min.	60
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Isokinetic Ratio, %	103.7

Particulate:

Amount Collected, mg. (including condensable)	12.3
Concentration, grains/SCF	0.004
Emission Rate, lb/hr.	0.65
Emission Rate, lb/1000 lb stack gas	0.007

Location: Biehl Construction
Date: 9-19-91
Time: 1:00 - 2:05 PM
Test Run: #3

Stack Gas Data:

Temperature, °F.	181.8
Velocity, ft./sec.	39.338
Gas Volume, ACFM	26,504
Gas Volume, SCFM (Wet)	21,520
Gas Volume, SCFM (Dry)	16,743
Moisture, %	22.2
Carbon Dioxide, % (Dry)	5.2
Oxygen, % (Dry)	14.1
Carbon Monoxide + Nitrogen, % (Dry)	80.7
Molecular Weight (Wet)	26.866

Sampling Data:

Total Time, min.	60
Volume, SCF (Dry)	41.860
Isokinetic Ratio, %	104.2

Particulate:

Amount Collected, mg. (including condensible)	11.2
Concentration, grains/SCF	0.004
Emission Rate, lb/hr.	0.59
Emission Rate, lb/1000 lb stack gas	0.006

Laboratory Data

Company: Biehl Construction
Date: 10-3-91
Test Run: 1

Filter: No. 13

Final Weight, mg.	623.8	
Tare Weight, mg.	619.1	
Weight Gain, mg.		4.7

Acetone Probe Wash:

Final Weight, mg.	68290.8	
Tare Weight, mg.	68286.7	
Blank Correction, mg.	0.0	
Volume, ml.	45	
Weight Gain, mg.		4.1

Impinger Acetone Wash:

Final Weight, mg.	66099.7	
Tare Weight, mg.	66098.9	
Blank Correction, mg.	0.0	
Volume, ml.	60	
Weight Gain, mg.		0.8

Impinger Water Extracts:
(CH₂CL₂)

Final Weight, mg.	66450.8	
Tare Weight, mg.	66445.3	
Blank Correction, mg.	1.2	
Weight Gain, mg.		4.3

Impinger Water Residue: (100 ml. Aliquot)

Final Weight, mg.	50496.8	
Tare Weight, mg.	50496.2	
Blank Correction, mg.	0.0	
Volume, ml.	460	
Weight Gain, mg.		0.6

Total Particulate, mg.	14.5
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Laboratory Data

Company: Biehl Construction
Date: 10-3-91
Test Run: 2

Filter: No. 14

Final Weight, mg.	620.1	
Tare Weight, mg.	617.5	
Weight Gain, mg.		2.6

Acetone Probe Wash:

Final Weight, mg.	69107.2	
Tare Weight, mg.	69102.8	
Blank Correction, mg.	0.0	
Volume, ml.	50	
Weight Gain, mg.		4.4

Impinger Acetone Wash:

Final Weight, mg.	80218.1	
Tare Weight, mg.	80215.8	
Blank Correction, mg.	0.0	
Volume, ml.	74	
Weight Gain, mg.		2.3

Impinger Water Extracts:
(CH₂CL₂)

Final Weight, mg.	68764.8	
Tare Weight, mg.	68760.9	
Blank Correction, mg.	1.2	
Weight Gain, mg.		2.7

Impinger Water Residue: (100 ml. Aliquot)

Final Weight, mg.	50403.5	
Tare Weight, mg.	50403.2	
Blank Correction, mg.	0.0	
Volume, ml.	500	
Weight Gain, mg.		0.3

Total Particulate, mg.	12.3
------------------------	------

Laboratory Data

Company: Biehl Construction
Date: 10-3-91
Test Run: 3

Filter: No. 15

Final Weight, mg.	609.3	
Tare Weight, mg.	606.8	
Weight Gain, mg.		2.5

Acetone Probe Wash:

Final Weight, mg.	80581.5	
Tare Weight, mg.	80579.0	
Blank Correction, mg.	0.0	
Volume, ml.	36	
Weight Gain, mg.		2.5

Impinger Acetone Wash:

Final Weight, mg.	80766.4	
Tare Weight, mg.	80763.3	
Blank Correction, mg.	0.0	
Volume, ml.	64	
Weight Gain, mg.		3.1

Impinger Water Extracts:
(CH₂CL₂)

Final Weight, mg.	81136.3	
Tare Weight, mg.	81132.0	
Blank Correction, mg.	1.2	
Weight Gain, mg.		3.1

Impinger Water Residue: (100 ml. Aliquot)

Final Weight, mg.	51139.2	
Tare Weight, mg.	51139.5	
Blank Correction, mg.	0.0	
Volume, ml.	520	
Weight Gain, mg.		0.0

Total Particulate, mg.		11.2
------------------------	--	------

Laboratory Data

Company: Biehl Construction
Date: 10-3-91
Test Run: Blanks

Filter: No.

Final Weight, mg.
Tare Weight, mg.
Weight Gain, mg.

Acetone Blank Wash:

Final Weight, mg.	80536.2	
Tare Weight, mg.	80536.2	
Blank Concentration, mg.		
Volume, ml.		
Weight Gain, mg.		0mg./100ml.

Impinger Acetone Wash:

Final Weight, mg.
Tare Weight, mg.
Blank Concentration, mg.
Volume, ml.
Weight Gain, mg.

Impinger Water Extracts:
(CH₂CL₂)

Final Weight, mg.	80882.9	
Tare Weight, mg.	80881.7	
Blank Concentration, mg.		
Weight Gain, mg.		1.2mg.

Impinger Water Residue: (100 ml. Aliquot)

Final Weight, mg.	72854.5	
Tare Weight, mg.	72854.5	
Blank Concentration, mg.		
Volume, ml.	135	
Weight Gain, mg.		0.0 mg./100 ml.

Total Particulate, mg. _____

Formaldehyde Laboratory Data

	Test Run			
	1	2	3	Blank
Collection Solution Volume 1% Bisulfite, 20 mls/impinger	45	45	45	---
Volume Analyzed - impinger 1	1	1	1	
- impinger 2	4	4	4	4
Absorption - impinger 1	0.711	0.512	0.407	
- impinger 2	0.008	0.005	0.005	0.006
Calibration Curve Data: Standard Curve	<u>Blank</u> 0.001	<u>1 ppm</u> 0.038	<u>2 ppm</u> 0.088	<u>4 ppm</u> 0.196

correlation coefficient = .9972
intercept = 0

Formaldehyde - Field Data

<u>Test Run</u>	<u>Time</u>	<u>V_{std}, ft.³</u>	<u>Flow Rate (Liters)</u>
1	7:55-8:25	1.139	1
2	10:35-11:10	1.062	1
3	1:05-1:35	1.047	1

Calculations

V _{std} , ft. ³	=	Sample Air Volume
Mn Formaldehyde	=	mg. Formaldehyde
C _s Formaldehyde	=	2.205 x 10 ⁻⁶ $\frac{\text{Mn}}{\text{V}_{\text{std}}}$
Q _s scfh	=	Volumetric Flow Rate
lb/hr. Formaldehyde	=	C _s formaldehyde x Q _s

CALCULATIONS FOR: Biehl Construction - Fond du Lac Date: 9/19/91 Test Run: 1

Dry Gas Meter Volume	$V_n = 42.502 \text{ ft}^3$	Particulates Collected	$H = 14.5 \text{ mg}_2$
Total Water Collected	$V_{lc} = 237.4 \text{ ml}$	Stack Area	$A_n = 11.229 \text{ ft}^2$
Absolute Stack Pressure	$P_s = 29.52 \text{ in. Hg}$	Total Sampling Time	$t = 60 \text{ min}$
Absolute Meter Pressure	$P_n = 29.67 \text{ in. Hg}$	Pitot Tube Coefficient	$C_p = .84$
Absolute Stack Temperature	$T_s = 435.7 \text{ }^\circ\text{K}$	Average Velocity Head (fDP)	$\text{avg } P = .62653 \text{ ft}^2$
Absolute Meter Temperature	$T_n = 522.3 \text{ }^\circ\text{K}$	Nozzle Area	$A_n = .000449 \text{ ft}^2$

Volume of Sample at Standard Conditions, Dry Basis.

$$Y [17.647] V_n \frac{P_n}{T_n} = 1.0229 [17.647] (42.502) \left(\frac{29.67}{522.3} \right) = V_{\text{std}} = 43.582 \text{ ft}^3$$

Volume of Water Vapor in Sample at Standard Conditions.

$$[0.04707] V_{lc} = [0.04707] (237.4) = V_{\text{wstd}} = 11.174 \text{ ft}^3$$

Proportion of Water Vapor in Gas Stream.

$$\frac{V_{\text{wstd}}}{V_{\text{std}} + V_{\text{wstd}}} = \frac{(11.174)}{(43.582 + 11.174)} = B_{\text{wo}} = 0.204$$

Concentration of Particulate Matter, Dry Basis.

$$[0.0154] \frac{H_n}{V_{\text{std}}} = [0.0154] \left(\frac{14.5}{43.582} \right) = c'_s = .005 \text{ gr/scf}$$

$$[2.205 \times 10^{-6}] \frac{H_n}{V_{\text{std}}} = [2.205 \times 10^{-6}] \left(\frac{14.5}{43.582} \right) = c_s = 2.734 \times 10^{-6} \text{ lb/scf}$$

Dry Molecular Weight of Stack Gas.

$$0.44(\% \text{CO}_2) + 0.32(\% \text{O}_2) + 0.28(\% \text{N}_2 + \% \text{CO}) = \frac{0.44 \times 4.3}{0.32 \times 15.7 + 0.28 \times 22.4} = \frac{1.892}{5.024 + 22.4} = M_d = 29.316$$

Molecular Weight of Stack Gas, Wet Basis.

$$M_d (1 - B_{\text{wo}}) + 18 B_{\text{wo}} = (29.316)(.796) + 18(.204) = M_s = 27.007$$

Stack Gas Velocity.

$$[85.49] C_p (fDP) \text{ avg.} \sqrt{\frac{T_s}{P_s M_s}} = [85.49] (.84) (.62653) \sqrt{\frac{1635.7}{(29.52)(27.01)}} = V_s = 40.176$$

Volumetric Flow Rate, Dry Basis, Standard Conditions.

$$[63529] (1 - B_{\text{wo}}) V_s A \frac{P_s}{T_s} = [63529] (.796) (40.176) (11.229) \left(\frac{29.52}{635.9} \right) = Q_s = 6059408 \text{ scfh}$$

Emission Rate.

$$Q_s \times c_s = (6059 \times 10^3) (2.734 \times 10^{-6}) = \text{E.R.} = 0.78 \text{ lb/hr}$$

Percent of Isokinetic Sampling.

$$\frac{K_1 \left(K_2 V_{lc} + \frac{V_n}{T_n} P_n \right) T_s}{V_s P_s A_n} = \frac{[1.667] \left([1.00267] (237.4) + \frac{1.0229(42.502)}{522.3} (29.67) \right) (635.7)}{60 (40.176) (29.52) (.000449)} = I = 102.9 \%$$

CALCULATIONS FOR: Bickel Construction Ford Du Lac Date: 9/19/91 Test Run: 2

Dry Gas Meter Volume	$V_n = 42.375 \text{ ft}^3$	Particulates Collected	$M = 12.3 \text{ mg}_2$
Total Water Collected	$V_{lc} = 250.5 \text{ ml}$	Stack Area	$A = 11.229 \text{ ft}^2$
Absolute Stack Pressure	$P_s = 29.52 \text{ in. Hg}$	Total Sampling Time	$t = 60 \text{ min}$
Absolute Meter Pressure	$P_m = 29.67 \text{ in. Hg}$	Pitot Tube Coefficient	$C_p = .84$
Absolute Stack Temperature	$T_s = 635.7 \text{ }^\circ\text{R}$	Average Velocity Head (fAP)	$\text{avg } P = 62188$
Absolute Meter Temperature	$T_m = 527.2 \text{ }^\circ\text{R}$	Nozzle Area	$A_n = 0.00449 \text{ ft}^2$

Volume of Sample at Standard Conditions, Dry Basis.

$$V_n \left(17.647\right) \frac{P_m}{T_m} = 1.0229 (17.647) (42.375) \left(\frac{29.67}{527.2} \right) = V_{nstd} = 43.048 \text{ ft}^3$$

Volume of Water Vapor in Sample at Standard Conditions.

$$(0.04707) V_{lc} = (0.04707) (250.5) = V_{wstd} = 11.791 \text{ ft}^3$$

Proportion of Water Vapor in Gas Stream.

$$\frac{V_{wstd}}{V_{nstd} + V_{wstd}} = \frac{11.791}{43.048 + 11.791} = B_{wo} = .215$$

Concentration of Particulate Matter, Dry Basis.

$$(0.0154) \frac{M_n}{V_{nstd}} = (0.0154) \left(\frac{12.3}{43.048} \right) = c'_s = .004 \text{ gr/scf}$$

$$(2.205 \times 10^{-6}) \frac{M_n}{V_{nstd}} = (2.205 \times 10^{-6}) \left(\frac{12.3}{43.048} \right) = c_s = .630 \times 10^{-6} \text{ lb/s}$$

Dry Molecular Weight of Stack Gas.

$$0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2 + \%CO) = 0.44 \times \frac{5.3}{80.1} + 0.32 \times \frac{14.6}{80.1} + 0.28 \times \frac{28.01}{80.1} = M_d = 29.432$$

Molecular Weight of Stack Gas, Wet Basis.

$$M_d (1 - B_{wo}) + 18 B_{wo} = (29.432) (.785) + 18 (.215) = M_s = 26.974$$

Stack Gas Velocity.

$$(85.49) C_p (fAP) \text{ avg.} \sqrt{\frac{T_s}{P_s M_s}} = (85.49) (.84) (62188) \sqrt{\frac{635.7}{29.52 (26.97)}} = V_s = 39.902$$

Volumetric Flow Rate, Dry Basis, Standard Conditions.

$$(63529) (1 - B_{wo}) V_s A \frac{P_s}{T_s} = (63529) (.785) (39.902) (11.229) \left(\frac{29.52}{635.7} \right) = Q_s = 4037643 \text{ scfh}$$

Emission Rate.

$$Q_s \times c_s = (1.038 \times 10^9) (.630 \times 10^{-6}) = \text{E.R.} = 0.65 \text{ lb/hr}$$

Percent of Isokinetic Sampling.

$$K_1 \left[\frac{K_2 V_{lc} + \frac{V_n P_m}{T_m} T_s}{V_s P_s A_n} \right] = \frac{1.667 \left[(1.00267) (250.5) + \frac{1.0229 (42.375)}{527.2} (29.67) (635.7) \right]}{60 (39.902) (29.52) (0.00449)} = I = 103.7 \%$$

CALCULATIONS FOR: Biedl Construction - Ford Du Lac Date: 9/19/91 Test Run: 3

Dry Gas Meter Volume	$V_n = 41.550 \text{ ft}^3$	Particulates Collected	$M_n = 11.2 \text{ mg}$
Total Water Collected	$V_{lc} = 253.7 \text{ ml}$	Stack Area	$A = 11.229 \text{ ft}^2$
Absolute Stack Pressure	$P_s = 29.53 \text{ in. Hg}$	Total Sampling Time	$t = 60 \text{ min}$
Absolute Meter Pressure	$P_m = 29.67 \text{ in. Hg}$	Pitot Tube Coefficient	$C_p = .84$
Absolute Stack Temperature	$T_s = 1641.8 \text{ }^\circ\text{K}$	Average Velocity Head (f.d.P)	$avg. v = 1.0906 \text{ ft}^2$
Absolute Meter Temperature	$T_m = 531.6 \text{ }^\circ\text{K}$	Nozzle Area	$A_n = .000449 \text{ ft}^2$

Volume of Sample at Standard Conditions, Dry Basis.

$$Y [17.647] V_n \frac{P_n}{T_n} = 7.029 [17.647] (41.550) \left(\frac{29.67}{531.6} \right) = V_{std} = 41.860 \text{ ft}^3$$

Volume of Water Vapor in Sample at Standard Conditions.

$$[0.04707] V_{lc} = [0.04707] (253.7) = V_{std} = 11.942 \text{ ft}^3$$

Proportion of Water Vapor in Gas Stream.

$$\frac{V_{std}}{V_{std} + V_{std}} = \frac{(41.860)}{41.860 + 11.942} = B_{wo} = .222$$

Concentration of Particulate Matter, Dry Basis.

$$[0.0154] \frac{M_n}{V_{std}} = [0.0154] \left(\frac{11.2}{41.860} \right) = c'_s = .004 \text{ gr/scf}$$

$$[2.205 \times 10^{-6}] \frac{M_n}{V_{std}} = [2.205 \times 10^{-6}] \left(\frac{11.2}{41.860} \right) = c_s = .590 \times 10^{-6} \text{ lb/sc}$$

Dry Molecular Weight of Stack Gas.

$$0.44(\%CO_2) + 0.32(\%O_2) + 0.28(\%N_2 + \%CO) = \frac{0.44 \times 5.2}{22.596} + \frac{0.32 \times 14.1}{22.596} + \frac{0.28 \times 28.0}{22.596} = M_d = 29.396$$

Molecular Weight of Stack Gas, Wet Basis.

$$M_d (1 - B_{wo}) + 18 B_{wo} = (29.396) (.778) + 18 (.222) = M_s = 26.866$$

Stack Gas Velocity.

$$[85.49] C_p (f.d.P) avg. \sqrt{\frac{T_s}{P_s M_s}} = [85.49] (.84) (1.0906) \sqrt{\frac{1641.8}{29.53 \times 26.866}} = v_s = 39.338$$

Volunetric Flow Rate, Dry Basis, Standard Conditions.

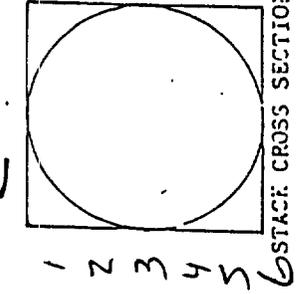
$$[63529] (1 - B_{wo}) V_s A \frac{P_s}{T_s} = [63529] (.778) (11.229) (39.338) \left(\frac{29.53}{1641.8} \right) = Q_s = 1,004,558 \text{ scfh}$$

Emission Rate.

$$Q_s \times c_s = (1.004 \times 10^6) (.590 \times 10^{-6}) = E.R. = 0.59 \text{ lb/hr}$$

Percent of Isokinetic Sampling.

$$\frac{K_1 [R_2 V_{lc} + \frac{V_n P_n}{T_n}] T_s}{V_s P_s A_n} = \frac{[1.667] [(1.00267) (253.7) + \frac{1.0229 \times 41.55}{531.6}] (1641.8)}{[60] [39.338] [29.53] [0.000449]} = I = 104.2 \%$$



STACK CROSS SECTION

COMPANY Build Control
 LOCATION: Asphalt plant
 DATE 9/19
 TEST RUN # 1
 STACK AREA 49 x 33
 OPERATOR BJ

AMBIENT TEMPERATURE 50
 BAROMETRIC PRESSURE 30.34 - 8
 ASSUMED MOISTURE, % 20
 HEATER BOX SETTING 23
 PROBE HEATER SETTING 250
 FILTER NUMBER 13

SAMPLE BOX # _____
 METER BOX # _____
 METER # 1.99
 C FACTOR 10229
 PROBE LENGTH 3'
 NOZZLE DIAMETER, 2.87

TRAVERSE POINT NUMBER	SAMPLING TIME (e, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	VELOCITY (v _{ap}) (√Δp)	CRIFICS METER (LH)	DRY GAS METER VOLUME (V _m , ft ³)	DRY GAS METER INLET TEMP (T _{in} , °F)	DRY GAS METER OUTLET TEMP (T _{out} , °F)	BOX TEMP (°F)	PUMP VACUUM (in. Hg)
7:46.5	1	2.5	165	.40	6324	1.76	21.620	42	44	250	3.0
49	2		169	.44	6633	1.91	23.40	59	45		
51.5	3		174	.44	6633	1.96	25.22	67	46		25.20
54/50.5	4		173	.35	5916	1.57	27.03	70	46		27.06
7:57.5	2	-21	172	.50	9707	2.24	28.74	70	47		28.72
8:00	2		175	.43	6557	1.93	30.70	74	47		30.70
8:25	3		179	.41	6403	1.85	32.56	77	47		32.53
5 7.5	4		179	.36	16	1.62	34.37	77	47		34.33
9	3		177	.52	7211	2.34	36.11	75	48		4.0
11.5	2		177	.40	6324	1.81	38.12	77	48		38.04
14	3		175	.40	6324	1.82	39.89	80	49		39.82
16.5	4		180	.40	6324	1.82	41.68	81	49		41.60
TOTAL		-21	2095		7.7320	22.63	43.47	849	563		
AVERAGE											

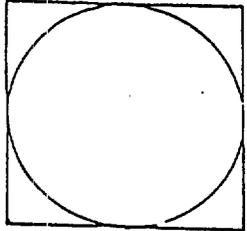
ORBITS TIME	CO ₂	O ₂	CO	H ₂
7:45				
AVERAGE				

WATER COLLECTED	TRAP VOLUME (ml)	L	PARTICULATE COLLECTED	FILTER	PROBE WASH
FINAL	420	2174	FINAL		
INITIAL	200	200	TARE		
NET H ₂ O	220	17.4	NET GAIN		
TOTAL H ₂ O COLLECTED, ml	2374		TOTAL WEIGHT, gf		

CONCENTR:
 lead ck before
 at 15" Hg OK
 lead ck inlet data
 before at 73" H₂O
 OK

COMPANY Bird Construction
 LOCATION _____
 DATE 9/19
 TEST RUN # 1
 STACK AREA _____
 OPERATOR BR

AMBIENT TEMPERATURE 50
 BAROMETRIC PRESSURE _____
 ASSUMED HUMIDITY, % _____
 HEATER BOX SETTING _____
 PROBE HEATER SETTING _____
 FILTER NUMBER 13



STACK CROSS SECTION

TIME	TRAVERSE POINT NUMBER	SAMPLING TIME (e, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	VELOCITY (√Δp)	ORIFICE METER (L=)	DRI GAS METER		EXH TEMP (°F)	PUFF VACUUM (in. H ₂ F)
								VOLUME (V _m , ft ³)	INLET (T _{m1} , °F)		
8:20	41	25		176	50	7071	2.28	43.47	74	49	43.39
22.5	2			179	35	5916	1.59	45.43	81	50	45.38
25	3			180	35	5916	1.59	47.12	82	50	47.06
27.30	4		-20	181	37	6083	1.68	48.80	82	50	48.72
31	5			178	46	6782	2.09	50.55	80	50	50.44
33.5	2			182	31	5568	1.41	52.47	81	51	52.36
36	3			183	32	5657	1.46	54.10	83	51	53.93
38.5	4			177	35	5916	1.60	55.67	83	51	55.52
42	6			171	39	6245	1.78	57.35	80	51	57.20
44.5	2			175	34	5831	1.56	59.13	83	51	58.96
47	3			174	34	5831	1.57	60.80	84	52	61.62
49.5	4			166	34	5831	1.58	62.45	84	52	62.27
TOTAL			-20	2122		712697	20.19	64.122	977	608	63.94
AVERAGE			-20	175.7		6000	1.78	42.502	76.08	48.79	

ORIFICE TIME	CO ₂	O ₂	CO	H ₂
	4.2	15.8		
	4.4	15.6		
AVERAGE	4.3	15.7		800

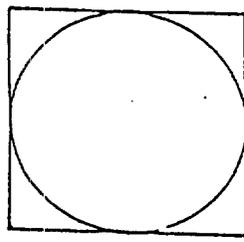
WATER COLLECTED	IMPINGERS			PARTICULATE COLLECTED	FILTER	PROBE WASH
	1	2	3			
FINAL				FINAL		
INITIAL				TARE		
NET H ₂ O				NET GAIN		
TOTAL H ₂ O COLLECTED, ml				TOTAL WEIGHT, g		

COMMENTS:

check after at
 6" Hg
 .005 CFM
 OK

COMPANY Bird Construction
 LOCATION Asphalt plant
 DATE 9/19/91
 TEST RUN # 2
 STACK AREA 49x33
 OPERATOR BD

AMBIENT TEMPERATURE 55
 BAROMETRIC PRESSURE 30.34
 ASSUMED MOISTURE, % 20
 HEATER BOX SETTING 250
 PROBE HEATER SETTING 250
 FILTER NUMBER 14
 SAMPLE BOX # _____
 METER BOX # _____
 METER R# 1.99
 C FACTOR 1.0229
 PROBE LENGTH 3
 NOZZLE DIAMETER 2.87



STACK CROSS SECTION

TRAVERSE POINT NUMBER	SAMPLING TIME (e, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	VELOCITY HEAD (√Δp)	CRUISE METER (LH)	VOLUME (V _m , SC)	DRY GAS METER INLET (T _{inlet} , °F)	OUTLET (T _{outlet} , °F)	BOX TEMP (°F)	PUSH VACUUM (in. Hg)
10:30	1	2.5	153	.44	.6633	1.95	064.407	50	52	250	
32.5	2		161	.51	.7141	2.30	66.30	67	53		64.26
35	3		166	.46	.6782	2.11	68.33	71	53		68.26
37/40	4		161	.37	.6083	1.69	70.27	76	53		70.19
41	2	1	167	.53	.7280	2.44	72.00	74	53		4.0
43.5	2	-2.6	170	.46	.6782	2.13	74.05	78	52		73.98
47	3		173	.42	.6481	1.93	75.99	81	52		75.91
48.5/52	4		173	.42	.6481	1.93	77.84	82	52		3.0
52	3		173	.56	.7483	2.57	79.69	82	52		4.0
54.5	2		175	.37	.6083	1.70	81.79	82	52		4
57	3		178	.36	.6	1.66	83.51	84	52		83.43
59.5/62	4		180	.36	.6	1.65	85.21	85	53		85.13
TOTAL		-2.6	2030		7.9229	2406	8692	912	629		
AVERAGE											

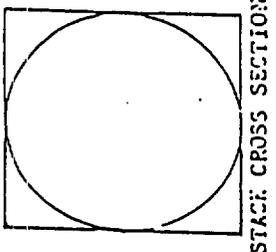
WATER COLLECTED	1	2	3	4	PARTICULATE COLLECTED	FILTER	PROBE WASH
FINAL			434	216.5	FINAL		
INITIAL			200	200	TARE		
NET H ₂ O			234	16.5	NET GAIN		
TOTAL H ₂ O COLLECTED, g			250.5		TOTAL WEIGHT, g		

COMMENTS:

leak ch. before
 at 15" Hg
 OK

COMPANY Buhl Construction
 LOCATION Fordville, Pa
 DATE 9/19/91
 TEST RUN # 2
 STACK AREA 49x33
 OPERATOR BE

AMBIENT TEMPERATURE _____
 BAROMETRIC PRESSURE _____
 ASSUMED HUMIDITY, % _____
 HEATER BOX SETTING _____
 PROBE HEATER SETTING _____
 FILTER NUMBER _____



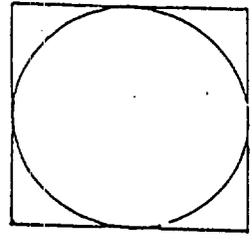
TRAVERS POINT NUMBER	SAMPLING TIME (e, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	VELOCITY (√Δp)	GRIFICE METER (L/S)	DRI GAS METER		EXH TEMP (°F)	PUMP VACUUM (in. Hg)	
							VOLUME (V _m , ft ³)	INLET (T _{in} , °F)			
11:03	41	2.5	180	.49	.7	2.25	86.92	82	53	250	86.83
5.5	2		181	.32	.5657	1.47	88.87	85	53		88.82
8	3		184	.33	.5744	1.52	90.50	86	54		90.42
10.5	4		185	.36	.6	1.66	92.10	86	54	30	92.05
14	51	-2.0	184	.41	.6403	1.89	97.89	84	54		93.76
16.5	2		182	.31	.5568	1.43	95.60	86	54		95.58
19	3		185	.31	.5568	1.43	97.20	87	55		97.16
21.5	4		184	.31	.5568	1.43	98.78	88	55		98.74
11:25	61		179	.37	.6083	1.71	100.36	82	55		100.32
275	2		184	.31	.5568	1.43	2.69	87	55		2.06
30	3		183	.30	.5477	1.39	3.69	88	56		3.64
325	4		176	.29	.5385	1.35	5.25	89	56		5.20
TOTAL			2187		7.0021	18.96	106.782	1030	654		6.74
AVERAGE			175.7		0.62188	1.79	42.375	67.2			

WATER COLLECTED	INSPIRERS	L	PARTICULATE COLLECTED	FILTER	PROBE WASH	ORSAT		
						CO ₂	O ₂	CO
FINAL			FINAL			5.4	14.6	80.0
INITIAL			TARE			5.2	14.6	80.2
NET H ₂ O			NET GAIN					
TOTAL H ₂ O COLLECTED, ml			TOTAL WEIGHT, g			5.3	14.6	80.1

COMMENTS:
 check after
 at 6:11 AM
 2.005 CFM
 check pilot tube for
 at 7:30 H₂O
 OK

COMPANY Bird Control
 LOCATION Fordville, August Pt
 DATE 9/19/91
 TEST RUN # 3
 STACK AREA 49 x 33
 OPERATOR BB

AMBIENT TEMPERATURE 55
 BAROMETRIC PRESSURE 30.1
 ASSUMED HUMIDITY, % 20
 HEATER BOX SETTING 250
 PROBE HEATER SETTING 250
 FILTER NUMBER 15



STACK CROSS SECTION

NOZZLE DIAMETER .287

TRAVERS POINT NUMBER	SAMPLING TIME (e, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	CRIFICE METER (LH)	DRY GAS METER		OUTLET TEMP (T _{out} , °F)	BOX TEMP (°F)	PUMP VACUUM (in. Hg)
						VOLUME (V _m , SC3)	INLET TEMP (T _{in} , °F)			
1.00	1	2.5	167	.40	1.83	102.108	58	57	250	5.0
2.5	2		174	.46	2.11	8.87	73	57		8.90
5	3		177	.44	2.03	110.80	78	58		10.92
7.5/10	4		179	.32	1.47	12.70	80	58		12.71
11	2		178	.47	2.16	14.33	80	58		14.31
13.5	2	-20	179	.43	1.98	16.20	83	58		16.25
16	3		171	.55	2.55	18.06	86	58		18.12
18.5/21	4		182	.37	1.72	20.12	87	58		20.23
22	3		182	.45	2.10	21.86	84	58		21.97
24.5	2		182	.35	1.63	23.73	87	58		23.88
27	3		186	.36	1.67	25.48	88	58		25.57
29.5/32	4		186	.39	1.81	27.20	89	58		27.28
TOTAL		-20	2143		23.06	29.00	973	694		
AVERAGE										

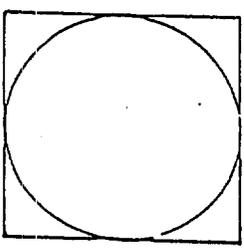
COMMENTS: *check before at 15' Hg OK*

ORBITS TIME	CO ₂	O ₂	CO	H ₂
1:00				
AVERAGE				

WATER COLLECTED	IMPINGERS	PARTICULATE COLLECTED	FILTER	PROBE WASH
FINAL		FINAL		
INITIAL		TARE		
NET H ₂ O		NET GAIN		
TOTAL H ₂ O COLLECTED, mL		TOTAL WEIGHT, GF		

COMPANY _____
 LOCATION _____
 DATE 9-19-91
 TEST RUN # 3
 STACK AREA _____
 OPERATOR BT

AMBIENT TEMPERATURE _____
 BAROMETRIC PRESSURE _____
 ASSUMED MOISTURE, % _____
 HEATER BOX SETTING _____
 PROBE HEATER SETTING _____
 FILTER NUMBER _____
 NOZZLE DIAMETER _____



STACK CROSS SECTION

TRAVERSE POINT NUMBER	SAMPLING TIME (e, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	VELOCITY (√Δp)	ORIFICE METER (LH)	DRY GAS METER VOLUME (V _m , SCF)	INLET TEMP (T _{in} , °F)	OUTLET TEMP (T _o , °F)	BOX TEMP (°F)	PUMP VACUUM (in. Hg)
33	41	2.5	179	.49	.7	2.27	29.00	85	58	250	29.06
35.5	2		181	.32	.5657	1.48	30.95	89	58		31.06
38	3		187	.33	.5744	1.53	32.61	89	58		32.66
40-5/4	4		188	.33	.5744	1.52	34.24	90	59		34.30
40	5		183	.45	.6708	2.07	35.84	86	58		35.93
42.5	2		182	.32	.5657	1.48	37.75	89	59		37.84
49	3		187	.30	.5477	1.40	39.42	91	59		39.45
51-5/4	4		187	.30	.5477	1.40	40.97	91	59		41.01
55	6	-15	185	.31	.5568	1.44	42.52	86	59		42.58
57.5	2		190	.29	.5385	1.35	44.08	89	59		44.17
2100	3		191	.29	.5385	1.35	45.62	91	59		45.70
2-3/65	4		180	.27	.5196	1.26	47.15	91	59		47.24
TOTAL		-15	2220		6.8998	18.55	148.658	106.7	704		48.72
AVERAGE		-18	181.8		6.0906	1.73	41.550	71.6			

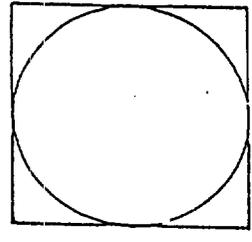
WATER COLLECTED	IMPINGERS	L	PARTICULATE COLLECTED	FILTER	PROBE WASH
FINAL	2	438	FINAL		
INITIAL	3	215.7	TARE		
NET H ₂ O		200	NET GAIN		
TOTAL H ₂ O COLLECTED, ml		238	TOTAL WEIGHT, g		
		253.7			

COMMENTS:

Rechecked after at 7" Hg 2.01 CFM OK

COMPANY: Buehl Construction
 LOCATION: Food de Gas
 DATE: 9/19/91
 TEST RUN # 1
 STACK AREA: 49.33
 OPERATOR: BJT

AMBIENT TEMPERATURE: 60.2
 BAROMETRIC PRESSURE: _____
 ASSUMED MOISTURE, %: _____
 HEATER BOX SETTING: _____
 PROBE HEATER SETTING: _____
 FILTER NUMBER: _____



STACK CROSS SECTION

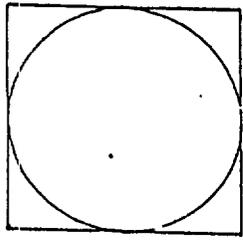
TIME	TRAVERSE SAMPLING POINT NUMBER	SAMPLING TIME (θ, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	VELOCITY HEAD (√Δp)	ORIFICE METER (L/s)	DRY GAS METER		BOX TEMP (°F)	PUMP VACUUM (in. Hg)
								VOLUME (V _m , ft ³)	INLET (T _{in} , °F)		
7:55		0					11 LPM	258.826	38	412	
8:00		5						59.01	40	46	
8:05		10						59.19	40	46	V _m = 1.10
8:10		15						59.35	41	46	T _m = 43.4
8:15		20						59.55	42	46	1.10 x 17.647 x 29.54
8:20		25						59.76	42	46	V _m std = 1.139
8:25		30						259.926	42	46	
10:35		0						259.926	43	48	
40		5						60.10	43	48	V _m = 1.032
50		10						60.27	43	48	T _m = 46.8
55		15						60.44	45	49	1.032 x 17.647 x 29.54
17:00		20						60.62	46	49	V _m std = 1.062
17:05		25						60.79	47	50	
17:10		30						60.958	47	50	

COMMENTS:

ORIFICE TIME	CO ₂	O ₂	CO	H ₂
AVERAGE				

WATER COLLECTED	IMPINGERS			PARTICULATE COLLECTED	PROBE WASH
	1	2	3		
FINAL				FINAL	
INITIAL				TARE	
NET H ₂ O				NET GAIN	
TOTAL H ₂ O COLLECTED, ml				TOTAL WEIGHT, g	

Formaldehyde Test



STACK CROSS SECTION

COMPANY: Biall Construction AMBIENT TEMPERATURE _____ SAMPLE BOX # _____
 LOCATION: Food du Jac BAROMETRIC PRESSURE _____ METER BOX # _____
 DATE: 9/19/91 ASSUMED MOISTURE, % _____ METER # _____
 TEST RUN # 3 HEATER BOX SETTING _____ C FACTOR _____
 STACK AREA _____ PROBE HEATER SETTING _____ PROBE LENGTH _____
 OPERATOR _____ FILTER NUMBER _____ NOZZLE DIAMETER _____

TRAVERSE POINT NUMBER	SAMPLING TIME (t, min)	STATIC PRESSURE (in. H ₂ O)	STACK TEMP (T _s , °F)	VELOCITY HEAD (Δp)	VELOCITY HEAD (√Δp)	CRIFICE METER (LH)	VOLUME (V _m , ft ³)	DRY GAS METER		EXH TEMP (°F)	PUSH VACUUM (in. Hg)
								INLET (T _m , °F)	OUTLET (T _{ex} , °F)		
1:05	0					1 LPM	260.958	49	53		
1:10	5					}	61.13	48	53		
1:15	10						61.30	49	53		
1:20	15						61.47	50	53		
1:25	20						61.65	50	53		
1:30	25						61.81	49	53		
1:35	30					261.985	49	53			
						6027		511			
							1.027 × 17.647 × $\frac{29.54}{52.11}$				V _{m, std} = 1047
TOTAL											
AVERAGE											

WATER COLLECTED	TRIPMETERS			L	PARTICULATE COLLECTED	FILTER	PROBE WASH
	1	2	3				
FINAL					FINAL		
INITIAL					TARE		
NET H ₂ O					NET GAIN		
TOTAL H ₂ O COLLECTED, ml					TOTAL WEIGHT, g		

COMMENTS:

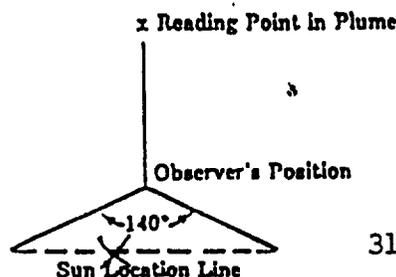
Name of Company <i>Biehl Construction</i>		Date <i>9-19-91</i>	Run #1	SEC MIN	0	15	30	45	SEC MIN	0	15	30	45
Location <i>Fond du Lac</i>		FID Number		0	5	5	0	5	30	0	0	0	5
State, Zip Code <i>WI</i>		Observer Certification Date <i>April 10, 1991</i>		1	5	5	0	0	31	0	5	0	0
Discharge Location <i>Boathouse Stack</i>		Control Device		2	0	10	5	0	32	0	5	0	5
Height of Discharge Above Ground <i>35 ft.</i>		Steam Plume? Yes <input checked="" type="checkbox"/> No <input type="checkbox"/> Attached <input checked="" type="checkbox"/> Detached <input type="checkbox"/>		3	0	0	5	5	33	5	0	5	0
Time of Observation Initial <i>7:55:00</i> Final <i>8:54:55</i>				4	0	0	5	0	34	0	0	5	5
Observer Location				5	10	0	0	5	35	5	0	0	5
Distance to Discharge <i>800 ft</i>		<i>same</i>		6	5	0	5	5	36	0	0	5	0
Direction from Discharge <i>SE</i>		<i>same</i>		7	0	0	0	10	37	0	0	5	0
Height of Observation Point in Relation to Discharge <i>ground 35 ft</i>		<i>same</i>		8	10	10	5	0	38	5	0	5	5
Plume Description Color, Length, etc.) <i>white 500 ft</i>		<i>white 350 ft</i>		9	5	10	0	5	39	0	0	0	5
Plume Background Description <i>white clouds blue skies</i>		<i>blue skies</i>		10	0	5	0	0	40	0	5	0	5
Weather Conditions Wind Direction <i>NW 5-8 mph</i>		<i>NW</i>		11	0	0	5	5	41	0	0	5	5
Wind Speed <i>5-8 mph</i>		<i>3-5-ph</i>		12	15	10	0	5	42	0	5	0	5
Ambient Temperature <i>37°F</i>		<i>39°F</i>		13	0	10	10	0	43	0	0	5	5
Weather Conditions (clear, overcast, % clouds, etc.) <i>clouds 60%</i>		<i>blue skies 0% clouds</i>		14	5	5	5	5	44	0	5	0	5
Describe Point in Plume at Which Opacity was Determined <i>approx 800-1000 ft after steam dissipation</i>				15	0	5	0	0	45	0	0	0	5
Remarks: <i>readings here NW</i>				16	0	5	0	0	46	5	0	5	0
				17	5	0	0	0	47	5	5	0	0
				18	0	0	5	0	48	0	5	5	5
				19	5	0	0	0	49	0	0	5	5
				20	5	5	0	0	50	0	5	5	0
				21	0	5	0	5	51	5	5	0	5
				22	0	5	0	5	52	5	10	5	0
				23	0	5	5	5	53	5	0	5	5
				24	0	0	5	5	54	0	5	0	0
				25	5	5	0	0	55	0	5	5	0
				26	0	0	10	5	56	5	0	0	5
				27	0	5	5	5	57	0	5	0	0
				28	0	5	5	0	58	0	5	0	0
				29	5	5	0	5	59	5	5	0	0

Summary of Average Opacity
(From Computer Program)

Set Number	Time	Opacity	
	Start - End	Sum	Average
1	8-13	110	4.6
2	48-53	85	3.5
3	0-5	80	3.3
4	22-27	75	3.1
5	38-43	60	2.5
6	28-33	55	2.3
7	14-19	45	1.8
8	54-59	45	1.8

Signature of Observer
Jeff Jennerjohn

Name of Observer (Please print)
Jeff Jennerjohn



Allowable Source Opacity

40%

hourly ave 2.8

Name of Company <i>Biehl Construction</i>		Date <i>9-19-91 Run #2</i>		SPEC MIN	0	16	30	45	SEC MIN	0	15	30	45
Address <i>Fond du lac</i>		FID Number		0	0	5	0	0	30	5	5	5	10
State, Zip Code <i>WI</i>		Observer Certification Date <i>April 10, 1991</i>		1	0	0	5	10	31	5	5	5	5
Discharge Location <i>Bayhouse Stack</i>		Control Device		2	0	0	5	0	32	5	5	5	5
Height of Discharge Above Ground <i>35 ft.</i>		Steam Plume? Attached <input checked="" type="checkbox"/> No Detached		3	0	5	0	0	33	0	0	5	5
Time of Observation		Initial <i>10:35:00</i>	Final <i>11:34:55</i>	4	5	5	5	0	34	5	5	5	0
Observer Location		Distance to Discharge <i>400 ft</i>		5	5	5	0	5	35	5	10	5	5
Direction from Discharge <i>SE</i>		Direction from Discharge <i>SAME</i>		6	5	10	5	5	36	5	5	10	5
Height of Observation Point in Relation to Discharge <i>ground - 35 ft</i>		Height of Observation Point in Relation to Discharge <i>SAME</i>		7	0	5	5	0	37	5	5	0	0
Plume Description (Color, Length, etc.) <i>White 200 ft</i>		Plume Description (Color, Length, etc.) <i>SAME</i>		8	10	5	5	0	38	5	5	0	5
Weather Background Description <i>Blue sky white clouds</i>		Weather Background Description <i>White/grey clouds</i>		9	5	0	5	5	39	0	5	5	0
Other Conditions		Other Conditions		10	5	5	5	5	40	5	5	5	0
Wind Direction <i>N.</i>		Wind Direction <i>SAME</i>		11	0	0	0	5	41	5	0	0	5
Wind Speed <i>2-6 mph</i>		Wind Speed <i>4-8 mph</i>		12	5	0	0	5	42	5	0	5	5
Ambient Temperature <i>40°F</i>		Ambient Temperature <i>SAME</i>		13	5	0	0	5	43	5	5	5	5
Weather Conditions (clear, overcast, % clouds, etc.) <i>Clouds 70%</i>		Weather Conditions (clear, overcast, % clouds, etc.) <i>Clouds 100%</i>		14	0	5	5	5	44	5	5	5	0
Describe Point in Plume at Which Opacity was Determined <i>approx 400-500 ft after steam dispersion</i>		Describe Point in Plume at Which Opacity was Determined		15	5	10	5	5	45	0	10	5	5
Remarks: <i>readings taken here</i>		Remarks:		16	5	5	0	5	46	5	5	5	5
<i>collected etc 1200m down</i>		<i>Baghouse</i>		17	5	0	5	5	47	0	5	5	5
				18	5	0	5	0	48	5	5	10	5
				19	5	0	5	10	49	5	0	0	5
				20	5	5	5	5	50	5	5	5	5
				21	10	5	5	5	51	5	0	5	5
				22	0	5	5	5	52	0	5	10	5
				23	0	0	0	0	53	0	0	0	5
				24	5	5	0	0	54	10	5	5	5
				25	0	0	5	0	55	5	5	10	5
				26	5	0	5	0	56	5	5	0	5
				27	5	10	5	5	57	0	5	0	5
				28	5	10	5	5	58	5	5	0	10
				29	5	5	5	0	59	0	5	5	5

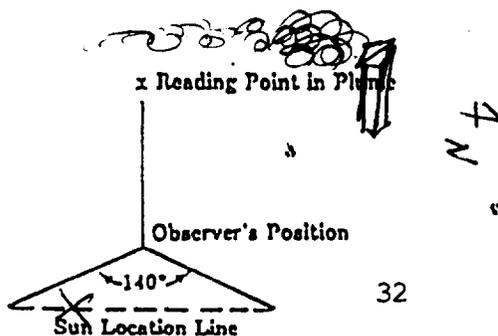
Summary of Average Opacity
(From Computer Program)

Set Number	Time	Opacity	
	Start - End	Sum	Average
1	27-32	130	5.4
2	43-48	115	4.8
3	50-55	110	4.6
4	5-10	105	4.4
5	15-20	105	4.4
6	33-38	100	4.2
7	21-26	105	2.7

Signature of Observer
Jeff Jennerjohn

Name of Observer (Please print)
Jeff Jennerjohn

Location of Observer, Discharge, and Sun Location.



Allowable Source Opacity

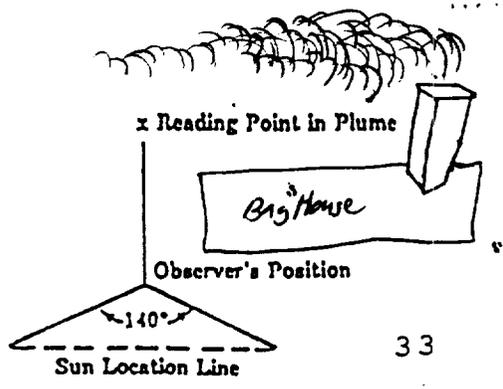
40%
3.9% hourly ave

Name of Company <i>Bichl Construction</i>		Date <i>9-19-91 Ran#3</i>		SEC MIN	0	15	30	45	SEC MIN	0	15	30	45
FID Number <i>FON On LAC</i>		Observer Certification Date <i>April 10, 1991</i>		0	5	0	5	0	30	10	5	5	5
State, Zip Code <i>WI</i>		Control Device		1	5	0	0	5	31	0	10	5	5
Emission Location <i>Bayhouse Stack</i>		Steam Plume? Attached <input checked="" type="checkbox"/> No Detached		2	5	5	0	5	32	5	5	5	5
Height of Discharge Above Ground <i>35 ft.</i>		Initial <i>1:05:00</i>		3	5	10	5	5	33	5	5	5	10
Time of Observation		Final <i>2:04:55</i>		4	10	5	5	5	34	5	0	5	5
Emission Location		Distance to Discharge <i>400 ft.</i>		5	5	5	5	5	35	5	5	5	5
Direction from Discharge <i>SE</i>		SAME		6	0	5	5	0	36	0	0	5	5
Height of Observation Point in Relation to Discharge <i>ground - 35 ft.</i>		SAME		7	5	5	5	5	37	5	5	10	5
Plume Description (Color, Length, etc.) <i>white 200 ft.</i>		SAME		8	5	5	5	0	38	5	0	0	5
Plume Background Description <i>white/grey clouds</i>		SAME		9	0	0	10	0	39	5	5	5	5
Weather Conditions		Wind Direction <i>N-NW</i>		10	10	5	5	0	40	5	10	5	5
Wind Speed <i>5-8 mph</i>		SAME		11	0	5	0	5	41	5	5	5	10
Ambient Temperature <i>40°F</i>		SAME		12	0	0	5	5	42	5	5	5	5
Weather Conditions (clear, overcast, % clouds, etc.) <i>100% clouds</i>		SAME		13	5	5	5	5	43	5	5	0	5
Describe Point in Plume at Which Opacity was Determined <i>approx 300-400 ft after steam dissipation</i>		SAME		14	5	5	10	5	44	5	0	0	5
Remarks: <i>Production 159 tons/hour</i>		SAME		15	5	5	0	5	45	0	10	5	5
		SAME		16	0	5	5	0	46	0	5	5	5
		SAME		17	5	5	5	5	47	0	5	5	5
		SAME		18	0	0	5	0	48	5	5	5	5
		SAME		19	5	5	5	5	49	0	5	5	5
		SAME		20	5	0	5	5	50	5	5	0	5
		SAME		21	5	5	5	10	51	0	5	5	10
		SAME		22	5	5	5	0	52	5	5	10	5
		SAME		23	5	0	5	5	53	5	5	5	0
		SAME		24	5	10	5	5	54	5	5	5	5
		SAME		25	0	5	5	0	55	5	0	5	5
		SAME		26	5	5	5	0	56	0	5	5	5
		SAME		27	5	5	10	5	57	5	5	5	5
		SAME		28	5	5	10	5	58	5	0	5	5
		SAME		29	5	5	5	5	59	0	0	5	5

Summary of Average Opacity
(From Computer Program)

Set Number	Time	Opacity	
	Start - End	Sum	Average
1	27-32	135	5.6
2	37-42	135	5.6
3	47-52	120	5.0
4	3-8	115	4.8
5	19-24	115	4.8
6	53-58	110	4.6
7	10-15	100	4.2

Signature of Observer: *Jeff Jennerphn*
Name of Observer (Please print): *Jeff Jennerphn*



Allowable Source Opacity *40%*

hourly ave. *4.5%*

Thermocouple Calibration

Room Temperature:	NBS Certified Thermometer	=	68°F.
	Stack Sampler Thermocouple	=	67°F.
Hot Water Temperature:	NBS Certified Thermometer	=	192°F.
	Stack Sampler Thermocouple	=	193°F.

Calibrated September 12, 1991 by Bruce Lamers

Dry Gas Meter Calibration

Meter calibrated by Wisconsin Public Service in Green Bay on September 11, 1991.

Reading before:		Reading after adjustment:	
open%	check%	open%	check%
99.0	99.0	100.0	100.0

The dry gas meter which was used in the testing was calibrated against the above by Bruce Lamers on September 11, 1991. The calibration factor is 1.0229.

Average Orifice ΔH Calibration = 1.99

PITOT TUBE CALIBRATION

Date 9/12/91

Calibrated by BJL

1. Face opening alignment OK? ✓

2. External tubing diameter $D_t = \underline{.375}$ in.

3. Base-to-opening plane distances $P_A = \underline{.500}$ in.

$P_B = \underline{.469}$ in.

4. Pitot-nozzle distance $X = \underline{3/4}$ in.

5. Pitot-probe sheath distance $Y = \underline{2}$ in.

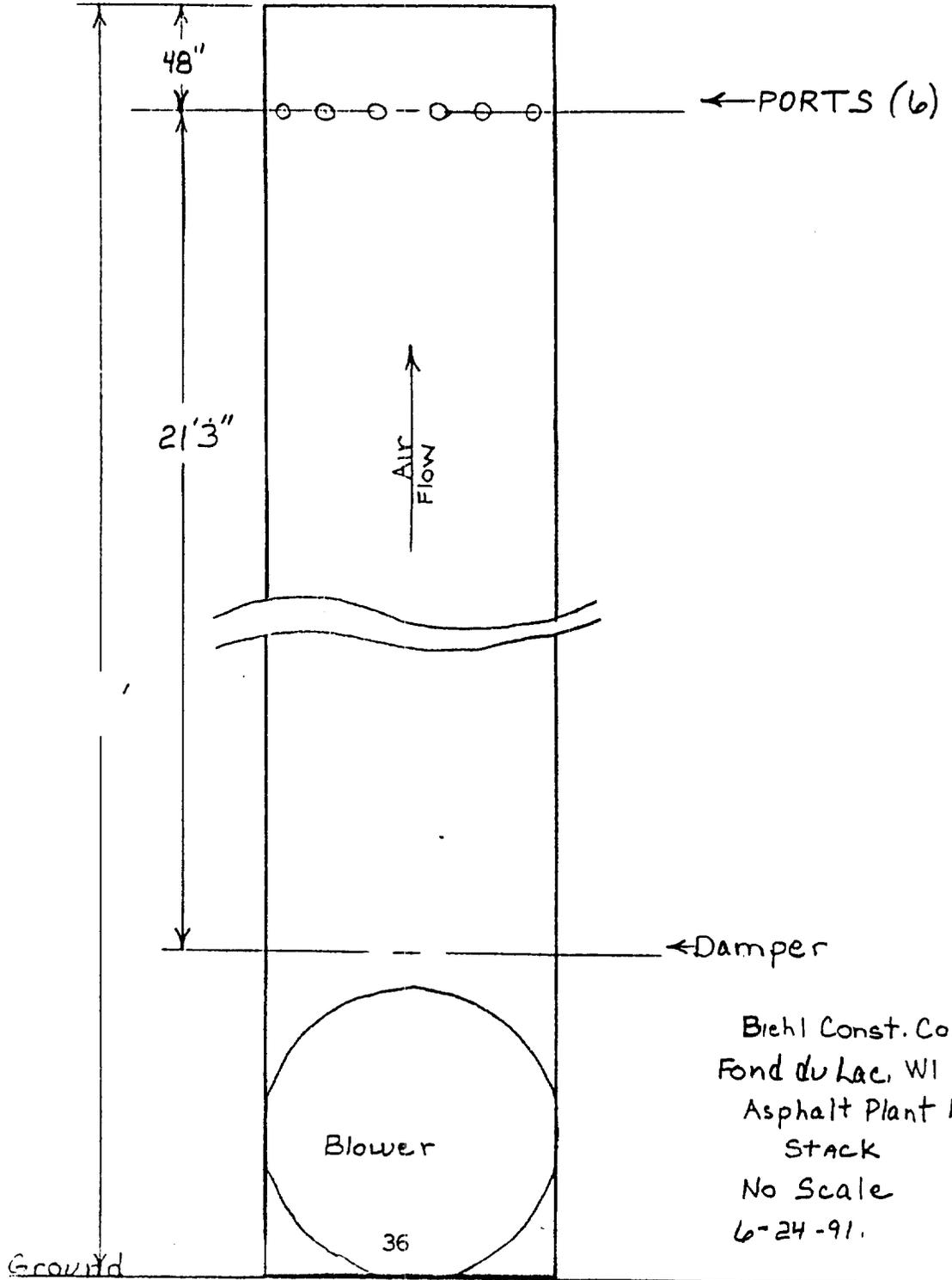
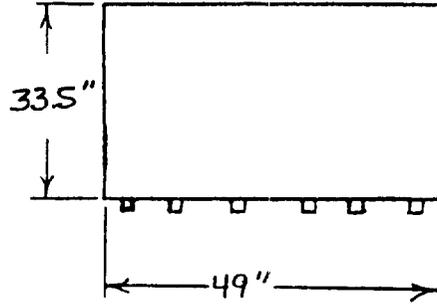
6. Pitot-thermocouple distance $Z = \underline{6.25}$ in.

"A" SIDE CALIBRATION

RUN NO.	ΔP_{std} in. H ₂ O	ΔP_{std} in. H ₂ O	$\Delta P_{std} \Delta P_{(s)}$	$C_{P(s)}$	DEVIATION $ C_{P(s)} - \bar{C}_P(A) $
1					
2					
3					
				$\bar{C}_P(A) = \underline{.84}$	$\sigma =$

$$C_{P(s)} = 0.99 \sqrt{\frac{\Delta P_{std}}{\Delta P_{(s)}}}$$

$$\sigma(A) = \frac{\sum |C_{P(s)} - \bar{C}_P(A)|}{3}$$



Biehl Const. Co., Inc.
 Fond du Lac, WI
 Asphalt Plant Exhaust
 Stack
 No Scale
 6-24-91.