Note: This is a reference cited in *AP 42, Compilation of Air Pollutant Emission Factors, Volume I Stationary Point and Area Sources.* AP42 is located on the EPA web site at www.epa.gov/ttn/chief/ap42/

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Background Report Reference

AP-42 Section Number: 10.6.3

Background Report Section: 4

Reference Number: 1

Title: Emission Test Results Particle PM-10 Formaldehyde, VOC, CO-Dryer Stacks, Press Vents, Former Stack and Boiler Stacks- Louisian Pacific Corporation, Clayton, Alabama Volume I and II

May 1992

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REPORT NO: 192-92-49

PROJECT: 1449-001

DATE: May 30, 1992

TYPE: **EMISSION TEST RESULTS**

EMISSION TEST RESULTS
PARTICULATE, PM_{10}, FORMALDEHYDE, VOC, CO
DRYER STACKS, PRESS VENTS, FORMER STACK AND BOILER STACKS
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

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SECTION 1

INTRODUCTION

Louisiana Pacific Corporation contracted Industrial & Environmental Analysts, Inc. (IEA) to conduct emission testing on 18 sources within the facility located in Clayton, Alabama. Emission testing was conducted from March 10 through March 21, 1992. The field effort was completed by personnel from IEA's Cary, North Carolina office under the direction of James Boswell, technical representation for Louisiana Pacific. Emission testing was observed by Al P. Bandur of the U.S. EPA Enforcement Investigations Center. Additional monitoring was performed by Albert E. Nugent and Richard P. Opem of Midwest Research Institute (MRI) as representatives of the U.S. EPA.

Table 1-1 summarizes the number and types of samples collected for this program. Testing was performed for permitting and internal engineering purposes on each of the following locations, for the parameters listed below:

- Dryer Stacks 1-4, 6, and 8
  - PM_{10} by EPA Method 201A
  - Particulate by EPA Method 5
  - Condensible Particulate by EPA Method 202
  - Carbon Monoxide by EPA Method 10
  - VOC's (Total Hydrocarbons as Propane) by EPA Method 25A
  - Formaldehyde by BIF Method 0011

- Press Vents 3-11
  - Particulate by EPA Method 5
  - Condensible Particulate by EPA Method 202
  - Carbon Monoxide by EPA Method 10
  - VOC's (Total Hydrocarbons as Propane) by EPA Method 25A
  - Formaldehyde by BIF Method 0011

- Boiler Stacks 1 and 2
  - Particulate by EPA Method 5
  - Condensible Particulate by EPA Method 202

- Former Stack
  - Particulate by EPA Method 5
  - Condensible Particulate by EPA Method 202

The remainder of this document summarizes the results, process rates, and the procedures and

quality control measures followed for this program. Section 2 contains tabulated results for each parameter of interest and is separated according to the unit tested. Section 3 summarizes the process rates for each day of testing. Section 4 summarizes the sampling and analytical procedures with a brief description and/or reference to the applicable methodologies. Section 5 discusses the basic quality control elements in place for this program to assure the collection of representative, accurate data.

The appendices provided in this document contain all of the necessary information to verify the reported results. Included as Appendices are: A -Example Calculations; B - Particulate Field and Recovery Data; C - PM_{10} Field and Recovery Data; D - Formaldehyde Field and Recovery Data; E - CEMS Field Data; F - CEMS Chart Recorder Traces; G - Laboratory Data and Chain-of-Custody Documentation; H - Instrument Calibration and Certification Data; I - Process Information ; and J -Project Participants.

TABLE 1-1
SUMMARY OF TEST SCHEDULE
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

DATE	DAY	SOURCE	PARAMETER	RUN #s
3/11/92	Wednesday	Dryer Stack 8	PM10	Runs 1,2, and 3
		Dryer Stack 8	Particulate	Runs 1,2, and 3
		Press Vent 5	Formaldehyde	Runs 1,2, and 3
		Press Vent 5	CEMS (CO and VOC)	Runs 1,2, and 3
		Press Vent 4	Formaldehyde	Run 1
		Press Vent 4	CEMS (CO and VOC)	Run 1
3/12/92	Thursday	Dryer Stack 6	PM10	Runs 1,2, and 3
		Dryer Stack 6	Particulate	Runs 1,2, and 3
		Former Stack	Particulate	Runs 1, and 2
		Press Vent 4	Formaldehyde	Runs 2, and 3
		Press Vent 4	CEMS (CO and VOC)	Runs 2, and 3
		Press Vent 3	Formaldehyde	Runs 1,2, and 3
		Press Vent 3	CEMS (CO and VOC)	Runs 1,2, and 3
3/13/92	Friday	Former Stack	Particulate	Run 3
		Dryer Stack 1	PM10	Runs 1,2, and 3
		Dryer Stack 1	Particulate	Runs 1,2, and 3
		Dryer Stack 2	PM10	Run 1
		Dryer Stack 2	Particulate	Run 1
		Press Vent 11	Formaldehyde	Runs 1,2, and 3
		Press Vent 11	CEMS (CO and VOC)	Runs 1,2, and 3
3/14/92	Saturday	Dryer Stack 2	PM10	Runs 2, and 3
		Dryer Stack 2	Particulate	Runs 2, and 3
		Dryer Stack 3	PM10	Runs 1, and 2
		Dryer Stack 3	Particulate	Runs 1, and 2
		Press Vent 6	Formaldehyde	Runs 1,2, and 3
		Press Vent 6	CEMS (CO and VOC)	Runs 1,2, and 3
3/16/92	Monday	Dryer Stack 4	PM10	Runs 1, and 2
		Dryer Stack 4	Particulate	Runs 1, and 2
		Boiler Stack 1	Particulate	Run 1
		Boiler Stack 2	Particulate	Runs 1, and 2
		Press Vent 7	Formaldehyde	Runs 1,2, and 3
		Press Vent 7	CEMS (CO and VOC)	Runs 1,2, and 3
		Press Vent 8	Formaldehyde	Runs 1,2, and 3
		Press Vent 8	CEMS (CO and VOC)	Runs 1,2, and 3

TABLE 1-1 (Continued)
SUMMARY OF TEST SCHEDULE
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

DATE	DAY	SOURCE	PARAMETER	RUN #s
3/17/92	Tuesday	Boiler Stack 1	Particulate	Runs 2, and 3
		Boiler Stack 2	Particulate	Run 3
		Press Vent 4	Particulate	Runs 1,2, and 3
		Press Vent 9	Particulate	Runs 1,2, and 3
		Press Vent 9	Formaldehyde	Runs 1,2, and 3
		Press Vent 9	CEMS (CO and VOC)	Runs 1,2, and 3
		Press Vent 10	Formaldehyde	Runs 1,2, and 3
		Press Vent 10	CEMS (CO and VOC)	Runs 1,2, and 3
3/18/92	Wednesday	Press Vent 3	Particulate	Runs 1,2, and 3
		Press Vent 10	Particulate	Run 1
		Press Vent 8	Particulate	Run 1
3/19/92	Thursday	Press Vent 10	Particulate	Runs 2, and 3
		Press Vent 8	Particulate	Runs 2, and 3
		Press Vent 5	Particulate	Runs 1,2, and 3
		Press Vent 6	Particulate	Runs 1,2, and 3
		Press Vent 7	Particulate	Runs 1,2, and 3
		Dryer Stack 1	Formaldehyde	Runs 1,2, and 3
		Dryer Stack 1	CEMS (CO and VOC)	Runs 1,2, and 3
		Dryer Stack 2	Formaldehyde	Runs 1, and 2
		Dryer Stack 2	CEMS (CO and VOC)	Runs 1, and 2
3/20/92	Friday	Dryer Stack 2	Formaldehyde	Run 3
		Dryer Stack 2	CEMS (CO and VOC)	Run 3
		Dryer Stack 6	Formaldehyde	Runs 1,2, and 3
		Dryer Stack 6	CEMS (CO and VOC)	Runs 1,2, and 3
		Dryer Stack 8	Formaldehyde	Runs 1,2, and 3
		Dryer Stack 8	CEMS (CO and VOC)	Runs 1,2, and 3
3/21/92	Saturday	Dryer Stack 4	Formaldehyde	Runs 1, and 2
		Dryer Stack 4	CEMS (CO and VOC)	Runs 1, and 2
		Dryer Stack 3	Formaldehyde	Runs 1, and 2
		Dryer Stack 3	CEMS (CO and VOC)	Runs 1, and 2

SECTION 2

SUMMARY OF RESULTS

This section has been divided into four subsections in accordance with the types of emission points tested. A brief discussion of the results is presented within each subsection. Data to verify all results is presented in the Appendices. Section 2.1 presents a comparative summary of the dryer stacks tested while Section 2.2 presents a comparative summary of the press vents tested. The results of the testing on the boiler stacks and Former Stack are presented in Sections 2.3 and 2.4, respectively.

A major component of this program was to determine the concentration and emission rate of particulate matter. Three types of particulate were evaluated: filterable particulate (standard EPA Method 5), condensible particulate (collected in impingers by EPA Method 202), and particulate matter exhibiting an aerodynamic particle size of less than 10 microns (PM_{10}). Testing for filterable particulate was accomplished using a standard EPA Method 5 sample train. Condensible particulate was obtained by analyzing the impinger contents for both organic and inorganic particulate. The organic component of each aqueous impinger catch was collected and segregated utilizing methylene chloride extractions. Testing for particulate matter was performed on each source. Each particulate test run includes the following:

1) Total *filterable particulate* matter comprised of the probe wash and filter fractions. This value is identical to total particulate as determined by EPA Method 5. This value is reported as **Total filterable PM.**

2) Particulate matter including *filterable* particulate matter, and the *inorganic* condensible component. This value is reported as: **Including only inorganic PM.**

3) Particulate matter including *filterable particulate* matter, the *organic* condensible components, and the *inorganic* condensible component. This value is reported as: **Including organic/inorganic PM.**

Testing for PM_{10} was accomplished using an in-stack cyclone designed to fractionate particulate at the 10 micron (10μm) cut-point utilizing aerodynamic settling properties. Each PM_{10} run consists of PM_{10} that includes only the *filterable* component from the cyclone and back-up filter. No condensible inorganic and organic components are included. This value is reported as: **$<PM_{10}$.**

The testing was segragated into two separate sampling efforts, due to the possibility of contamination of the DNPH absorbing solution by acetone (used in clean-up of the Method 5 train). To eliminate this potential interference the formaldehyde testing was performed separately from the particulate testing. Two separate test teams were utilized to perform testing, resulting in the following set of parameters being determined simultaneously: (1) particulate

matter, condensible particulate matter, and PM_{10} and (2) formaldehyde, carbon monoxide, and total hydrocarbons (VOC's). Volumetric flow rates from the concurrent formaldehyde test were used to calculate the mass emission rates from the CEMS (CO and VOC) testing. Moisture values for the PM_{10} runs were obtained from the concurrent particulate tests.

2.1 DRYER STACKS

A total of six (6) dryer stacks were tested for PM_{10} , particulate matter, condensible particulate matter, formaldehyde, carbon monoxide and total hydrocarbons (VOC's). Table 2.1-1 provides a comparison of each average emission measured from the dryer stacks. Table 2.1-2 presents a summary of the CEMS (CO and VOC) parameters. Figure 2.1-1 provides a diagram of the dryer stack sample locations and relates IEA's source identification numbers with Louisiana Pacific's source identification numbers. Due to the presence of cyclonic flow at some dryer locations, ports were moved farther downstream until a location acceptable to Method 1 criteria could be found. Data documenting acceptable flow profile characteristics for all test locations are in the Appendices.

2.1.1 Dryer Stack 1

Table 2.1.1-1 presents a summary of the emissions from Dryer Stack 1. Tables 2.1.1-2 through 2.1.1-6 summarize the individual test runs on the stack.

PM_{10} - results averaged 0.020 grains/dry standard cubic foot (gr/dscf) and 8.5 pounds per hour (lbs/hr).

Particulate Matter - concentrations averaged 0.080 gr/dscf resulting in 34.5 lbs/hr.

Particulate Matter (including condensibles)- concentrations averaged 0.083 gr/dscf resulting in 35.9 lbs/hr.

Formaldehyde - concentrations averaged 15.9 ppm resulting in 3.2 lbs/hr.

Carbon Monoxide - concentrations averaged 29.9 ppm resulting in 5.7 lbs/hr.

Total Hydrocarbons(VOC) - concentrations averaged 49.7 ppm resulting in 16.1 lbs/hr.

2.1.2 Dryer Stack 2

Table 2.1.2-1 presents a summary of the emissions from Dryer Stack 2. Tables 2.1.2-2 through 2.1.2-6 summarize the individual test runs on the stack.

PM_{10} - results averaged 0.014 gr/dscf and 5.8 lbs/hr.

Particulate Matter - concentrations averaged 0.088 gr/dscf resulting in 39.4 lbs/hr.

Particulate Matter (including condensibles)- concentrations averaged 0.092 gr/dscf resulting in 41.4 lbs/hr.

Formaldehyde - concentrations averaged 16.0 ppm resulting in 3.5 lbs/hr.

Carbon Monoxide - concentrations averaged 28.6 ppm resulting in 5.8 lbs/hr.

Total Hydrocarbons (VOC) - concentrations averaged 59.2 ppm resulting in 20.4 lbs/hr.

2.1.3 Dryer Stack 3

Table 2.1.3-1 presents a summary of the emissions from Dryer Stack 3. Tables 2.1.3-2 through 2.1.3-5 summarize the individual test runs on the stack. Only two test runs were performed on this source.

PM_{10} - results averaged 0.017 gr/dscf and 6.5 lbs/hr.

Particulate Matter - concentrations averaged 0.110 gr/dscf resulting in 44.0 lbs/hr.

Particulate Matter (including condensibles)- concentrations averaged 0.114 gr/dscf resulting in 45.7 lbs/hr.

Formaldehyde - concentrations averaged 16.2 ppm resulting in 3.4 lbs/hr.

Carbon Monoxide - concentrations averaged 14.5 ppm resulting in 2.8 lbs/hr.

Total Hydrocarbons (VOC) - concentrations averaged 48.1 ppm resulting in 15.5 lbs/hr.

2.1.4 Dryer Stack 4

Table 2.1.4-1 presents a summary of the emissions from Dryer Stack 4. Tables 2.1.4-2 through 2.1.4-5 summarize the individual test runs on the stack. Only two test runs were performed on this source.

PM_{10} - results averaged 0.021 gr/dscf and 7.6 lbs/hr.

Particulate Matter - concentrations averaged 0.126 gr/dscf ppm resulting in 51.5 lbs/hr.

Particulate Matter (including condensibles)- concentrations averaged 0.135 gr/dscf resulting in 55.0 lbs/hr.

Formaldehyde - concentrations averaged 17.3 ppm resulting in 3.4 lbs/hr.

Carbon Monoxide - concentrations averaged 9.0 ppm resulting in 1.7 lbs/hr.

Total Hydrocarbons (VOC) - concentrations averaged 42.1 ppm resulting in 13.0 lbs/hr.

2.1.5 Dryer Stack 6

Table 2.1.5-1 presents a summary of the emissions from Dryer Stack 6. Tables 2.1.5-2 through 2.1.5-6 summarize the individual test runs on the stack. Table 2.1.5-7 presents volumetric flow data for Dryer Stack 5.

PM_{10} - results averaged 0.011 gr/dscf and 3.4 lbs/hr.

Particulate Matter - concentrations averaged 0.131 gr/dscf resulting in 35.4 lbs/hr.

Particulate Matter (including condensibles)- concentrations averaged 0.139 gr/dscf resulting in 37.6 lbs/hr.

Formaldehyde - concentrations averaged 12.4 ppm resulting in 1.9 lbs/hr.

Carbon Monoxide - concentrations averaged 192.0 ppm resulting in 27.0 lbs/hr.

Total Hydrocarbons (VOC) - concentrations averaged 106.2 ppm resulting in 25.9 lbs/hr.

2.1.6 Dryer Stack 8

Table 2.1.6-1 presents a summary of the emissions from Dryer Stack 8. Tables 2.1.6-2 through 2.1.6-6 summarize the individual test runs on the stack. Table 2.1.6-7 presents volumetric flow data for Dryer 7.

PM_{10} - results averaged 0.006 gr/dscf and 1.7 lbs/hr.

Particulate Matter - concentrations averaged 0.047 gr/dsf resulting in 13.1 lbs/hr.

Particulate Matter (including condensibles)- concentrations averaged0.052 gr/dscf resulting in 14.6 lbs/hr.

Formaldehyde - concentrations averaged 14.7 ppm resulting in 2.1 lbs/hr.

Carbon Monoxide - concentrations averaged 216.8 ppm resulting in 29.4 lbs/hr.

Total Hydrocarbons (VOC) - concentrations averaged 101.9 ppm resulting in 24.3 lbs/hr.

TABLE 2.1-1
SUMMARY OF EMISSIONS
DRYER STACKS 1-4, 6, 8
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	DRYER #1	DRYER #2	DRYER #3	DRYER #4	DRYER #6	DRYER #8	AVERAGE
PM10							
Concentration, gr/dscf	0.020	0.014	0.017	0.021	0.011	0.006	0.015
Emission Rate, lb/hr	8.5	5.8	6.5	7.6	3.4	1.7	5.6
Particulate							
Concentration, gr/dscf	0.080	0.088	0.110	0.013	0.131	0.047	0.078
Emission Rate, lb/hr	34.5	39.4	44.0	51.5	35.4	13.1	36.3
Particulate (Including condensibles)							
Concentration, gr/dscf	0.083	0.092	0.114	0.135	0.139	0.052	0.103
Emission Rate, lb/hr	35.9	41.4	45.7	55.0	37.6	14.6	38.4
Formaldehyde							
Concentration, ppm	15.9	16.0	16.2	17.3	12.4	14.7	15.4
Emission Rate, lb/hr	3.2	3.5	3.4	3.4	1.9	2.1	2.9
Carbon Monoxide							
Concentration, ppm	29.9	28.6	14.5	9.0	192.0	216.8	81.8
Emission Rate, lb/hr	5.7	5.8	2.8	1.7	27.0	29.4	12.1
Total Hydrocarbons (VOC), as propane							
Concentration, ppm	49.7	59.2	48.1	42.1	106.2	101.9	67.9
Emission Rate, lb/hr	16.1	20.4	15.5	13.0	25.9	24.3	19.2

TABLE 2.1-2
DRYER STACKS 1-4, 6, 8
CEMS SUMMARY
LOUISIANA PACIFIC CORPORATION

			CEM Data (Corrected)		Volumetric Flow				Mass Emission Rates	
Run No.	Start Time	Stop Time	CO (ppm)	THC (ppm)	Qa (acfm)	Qs (dscfm)	Moisture (%)	Qsc (scfm)	CO (lb/hr)	THC (lb/hr)
Dryer 1 1	0752	0904	27.7	41.3	54,500	45,900	3.1	47,300	5.5	13.4
2	0957	1107	34.1	48.9	53,500	42,200	9.0	46,300	6.3	15.6
3	1151	1151	28.0	58.8	54,500	42,700	10.0	47,400	5.2	19.2
Dryer 2 1	1538	1644	34.9	56.8	55,200	44,800	7.4	48,300	6.8	18.9
2	1746	1845	27.9	67.1	55,800	45,100	7.8	48,900	5.5	22.5
3	0744	0847	23.0	53.8	60,700	50,300	6.3	53,600	5.0	19.8
Dryer 3 1	0753	0856	17.6	45.3	51,400	43,700	5.9	46,400	3.4	14.4
2	0910	1020	11.4	50.8	52,300	45,100	5.0	47,400	2.2	16.5
Dryer 4 1	1104	1207	8.6	42.0	48,400	41,900	4.5	43,800	1.6	12.7
2	1225	1225	9.4	42.1	50,000	43,200	5.1	45,500	1.8	13.2
Dryer 6 1	1603	1759	187.0	120.3	41,500	33,600	8.5	36,700	27.4	30.4
2	1729	1833	191.6	101.0	38,400	31,000	9.1	34,100	25.9	23.7
3	1853	1958	197.5	97.4	40,400	32,300	8.9	35,400	27.8	23.7
Dryer 8 1	1046	1159	222.2	100.5	39,700	31,800	9.5	35,100	30.8	24.2
2	1225	1330	209.2	88.8	39,900	31,300	11.1	35,200	28.6	21.5
3	1347	1452	219.0	116.5	38,500	30,300	11.2	34,100	28.9	27.3

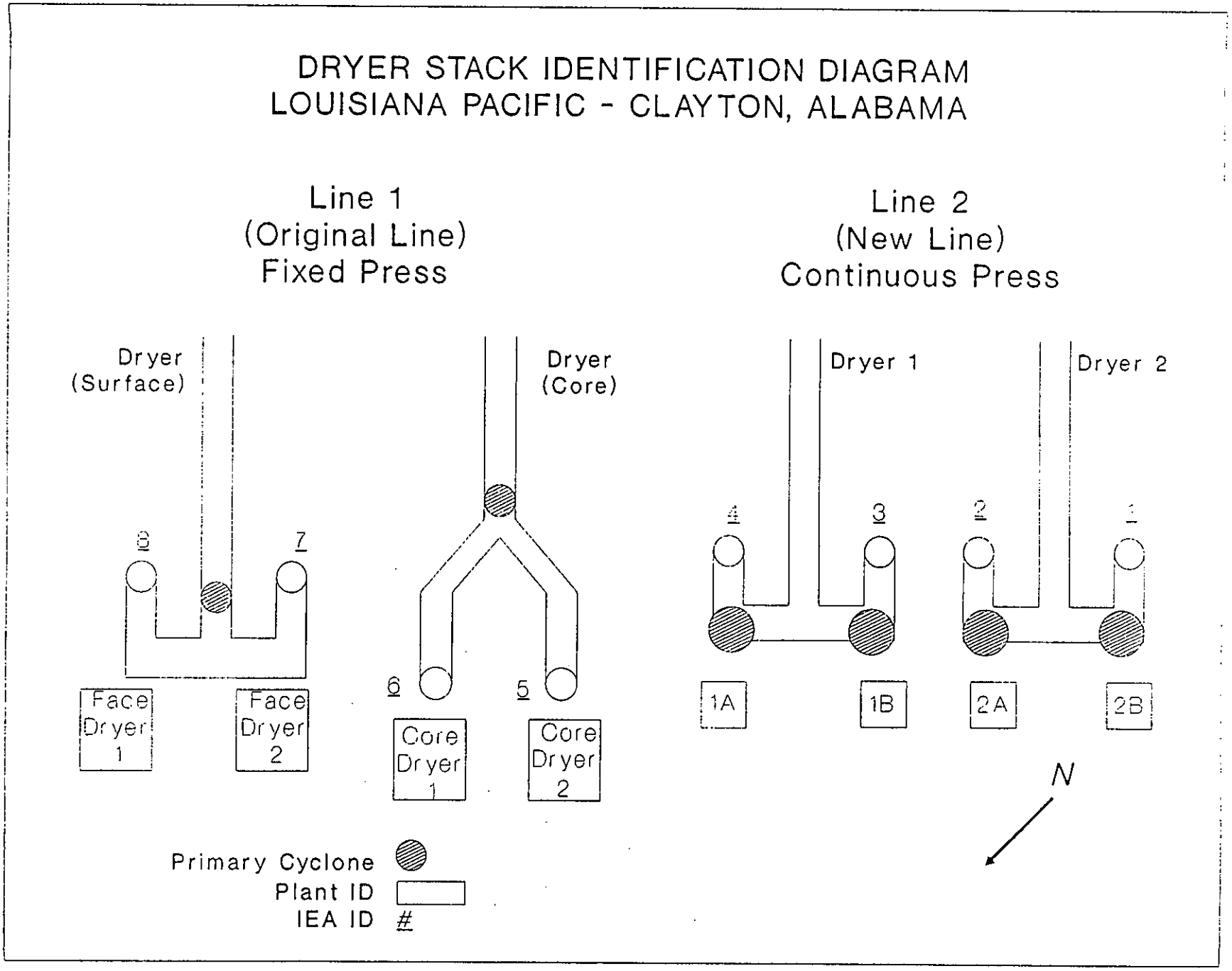
DRYER STACK IDENTIFICATION DIAGRAM
LOUISIANA PACIFIC - CLAYTON, ALABAMA
Line 1
(Original Line)
Fixed Press
Line 2
(New Line)
Continuous Press
Dryer
(Surface)
Dryer
(Core)
Dryer 1
Dryer 2
8
7
6
5
4
3
2
1
Face
Dryer
1
Face
Dryer
2
Core
Dryer
1
Core
Dryer
2
1A
1B
2A
2B
N
Primary Cyclone
Plant ID
IEA ID #

FIGURE 2.1-1

TABLE 2.1.1-1
SUMMARY OF EMISSIONS
DRYER STACK #1
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
PM10				
Concentration, gr/dscf	0.032	0.012	0.015	0.020
Emission Rate, lb/hr	14.4	5.0	6.1	8.5
Particulate				
Concentration, gr/dscf	0.063	0.084	0.092	0.080
Emission Rate, lb/hr	26.8	36.5	40.2	34.5
Particulate (Including condensibles)				
Concentration, gr/dscf	0.066	0.087	0.095	0.083
Emission Rate, lb/hr	28.1	38.1	41.6	35.9
Formaldehyde				
Concentration, ppm	15.9	16.2	15.6	15.9
Emission Rate, lb/hr	3.4	3.2	3.1	3.2
Carbon Monoxide				
Concentration, ppm	27.7	34.1	28.0	29.9
Emission Rate, lb/hr	5.5	6.3	5.2	5.7
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	41.3	48.9	58.8	49.7
Emission Rate, lb/hr	13.4	15.6	19.2	16.1

DRYER STACK 1

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	MEASURED DATA	
(Y)	Meter Box Y	1.005
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.74
(Vm)	Meter Volume, cu.ft	24.766
(Tm)	Avg Meter Temp, deg F	69.4
(Pg)	Static Pressure, inches H2O	-0.95
(Ts)	Avg Stack Temp, deg F	114.0
(Bws)	Moisture (from M5 run), %	5.6
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.782
(0)	Sample Time, min	61.56
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0440
(Mf)	Particulate Collected (filter), g	0.0070

DRYER STACK 1

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	24.698
(Ps)	Stack Pressure, inches Hg	29.67
(%Bws)	Moisture, %	5.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2
(Vs)	Velocity, ft/s	105.9
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	61,153
(Qstd)	Volumetric flow, dscfm	52,640
(I)	Isokinetic Rate, %	76.0
(Qs)	Cyclone flowrate (actual), cfm	0.466
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.26
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0319
(ER)	Particulate Emission Rate, lb/hr	14.4

TABLE 2.1.1-2

DRYER STACK 1

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	MEASURED DATA	
(Y)	Meter Box Y	1.005
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.74
(Vm)	Meter Volume, cu.ft	22.838
(Tm)	Avg Meter Temp, deg F	65.3
(Pg)	Static Pressure, inches H2O	-0.95
(Ts)	Avg Stack Temp, deg F	119.2
(Bws)	Moisture (from M5 run), %	5.5
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.618
(0)	Sample Time, min	57.51
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0010
(Mf)	Particulate Collected (filter), g	0.0173

DRYER STACK 1

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	22.951
(Ps)	Stack Pressure, inches Hg	29.67
(%Bws)	Moisture, %	5.5
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2
(Vs)	Velocity, ft/s	96.6
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	55,781
(Qstd)	Volumetric flow, dscfm	47,631
(I)	Isokinetic Rate, %	83.6
(Qs)	Cyclone flowrate (actual), cfm	0.467
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.24
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0123
(ER)	Particulate Emission Rate, lb/hr	5.0

TABLE 2.1.1-3

DRYER STACK 1

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	MEASURED DATA	
(Y)	Meter Box Y	1.005
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.74
(Vm)	Meter Volume, cu.ft	21.725
(Tm)	Avg Meter Temp, deg F	62.0
(Pg)	Static Pressure, inches H2O	-0.95
(Ts)	Avg Stack Temp, deg F	113.7
(Bws)	Moisture (from M5 run), %	4.6
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.581
(θ)	Sample Time, min	58.49
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0102
(Mf)	Particulate Collected (filter), g	0.0113

DRYER STACK 1

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	21.972
(Ps)	Stack Pressure, inches Hg	29.67
(%Bws)	Moisture, %	4.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.3
(Vs)	Velocity, ft/s	93.8
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	54,140
(Qstd)	Volumetric flow, dscfm	47,116
(I)	Isokinetic Rate, %	79.5
(Qs)	Cyclone flowrate (actual), cfm	0.432
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.84
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0151
(ER)	Particulate Emission Rate, lb/hr	6.1

TABLE 2.1.1-4

TABLE 2.1.1-5
DRYER STACK #1
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/13/92 1101-1213	RUN 2 3/13/92 1333-1527	RUN 3 3/13/92 1615-1725	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.60	1.72	1.67	1.66
(Bp)	Barometric Pressure, inches Hg	29.84	29.84	29.84	29.84
(Vm)	Meter Volume, cu.ft	41.731	41.556	41.006	41.431
(Tm)	Avg Meter Temp, deg F	73.9	63.1	59.3	65.4
(Pg)	Static Pressure, inches H2O	-1.95	-1.95	-1.95	-1.95
(Ts)	Avg Stack Temp, deg F	112.7	119.5	113.6	115.3
(Vlc)	Water Collected, ml	52.4	52.4	43.1	49.3
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.672	1.733	1.709	1.70
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.155	0.155	0.155	0.155
(D)	Stack Diameter, inches	42	42	42	42
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0501	0.0614	0.0840	0.0652
(Mf)	Particulate Collected (filter), g	0.1198	0.1664	0.1656	0.1506
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0028	0.0018	0.0048	0.0031
(Mio)	MeCl Impinger (organic) residue, g	0.0049	0.0080	0.0039	0.0056
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	41.388	42.078	41.819	41.762
(Ps)	Stack Pressure, inches Hg	29.70	29.70	29.70	29.70
(%Bws)	Moisture, %	5.6	5.5	4.6	5.3
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2	28.2	28.3	28.3
(Vs)	Velocity, ft/s	99.2	103.5	101.3	101.3
(As)	Stack Area, sq.ft	9.62	9.62	9.62	9.62
(Qa)	Volumetric flow, acfm	57,291	59,723	58,493	58,503
(Qs)	Volumetric flow, dscfm	49,457	50,998	50,948	50,468
(I)	Isokinetic Rate, %	102.4	101.0	100.5	101.3
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0633	0.0835	0.0921	0.0797
(ER)	Particulate Emission Rate, lb/hr	26.8	36.5	40.2	34.5
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0644	0.0842	0.0939	0.0808
(ER)	Particulate Emission Rate, lb/hr	27.3	36.8	41.0	35.0
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0662	0.0871	0.0953	0.0829
(ER)	Particulate Emission Rate, lb/hr	28.1	38.1	41.6	35.9
	Train Fractionation:				
	filterable, %	96	96	97	96
	condensible, %	4	4	3	4

TABLE 2.1.1-6

DRYER STACK #1

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/19/92 0752-0904	RUN 2 3/19/92 0957-1107	RUN 3 3/19/92 1151-1258	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	0.998	0.998	0.998	0.998
	Avg Delta H, inches H2O	4.30	1.57	2.76	2.88
(Bp)	Barometric Pressure, inches Hg	29.58	29.58	29.58	29.58
(Vm)	Meter Volume, cf	65.776	60.421	57.250	61.149
(Tm)	Avg Meter Temp, deg F	79.0	88.0	88.8	85.3
	Static Pressure, inches H2O	-1.10	-1.10	-1.10	-1.10
(Ts)	Avg Stack Temp, deg F	139.0	140.0	138.0	139.0
(Vlc)	Water Collected, ml	43.4	120.8	128.8	97.7
(CO2)	Carbon dioxide, %	1.0	0.0	0.0	0.3
(O2)	Oxygen, %	20.0	20.9	20.9	20.6
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	1.560	1.510	1.538	1.54
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.196	0.196	0.196	0.196
(Ds)	Stack Diameter, inches	42	42	42	42
(Mf)	Total Formaldehyde, mg	36	33	30	33
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	64.228	57.640	54.696	58.855
(Ps)	Stack Pressure, inches Hg	29.50	29.50	29.50	29.50
(%Bws)	Moisture (from impingers), %	3.1	9.0	10.0	7.3
(%Bws)	Moisture (at saturation), %	19.4	19.9	18.9	19.4
(Ms)	Molecular Weight-wet, lb/lb-mole	28.6	27.9	27.8	28.1
(Vs)	Velocity, ft/s	94.4	92.6	94.4	93.8
(As)	Stack Area, sq ft	9.62	9.62	9.62	9.62
(Qa)	Volumetric flow, acfm	5.45E+04	5.35E+04	5.45E+04	5.41E+04
(Qs)	Volumetric flow, dscfm	4.59E+04	4.22E+04	4.27E+04	4.36E+04
(I)	Isokinetic Rate, %	107.2	104.5	98.1	103.3
(Cf)	Formaldehyde Concentration, mg/dscf	0.56	0.57	0.55	0.56
(Cppm)	Formaldehyde Concentration, ppm	15.9	16.2	15.6	15.9
(ER)	Formaldehyde Emission Rate, lb/hr	3.40	3.20	3.11	3.24

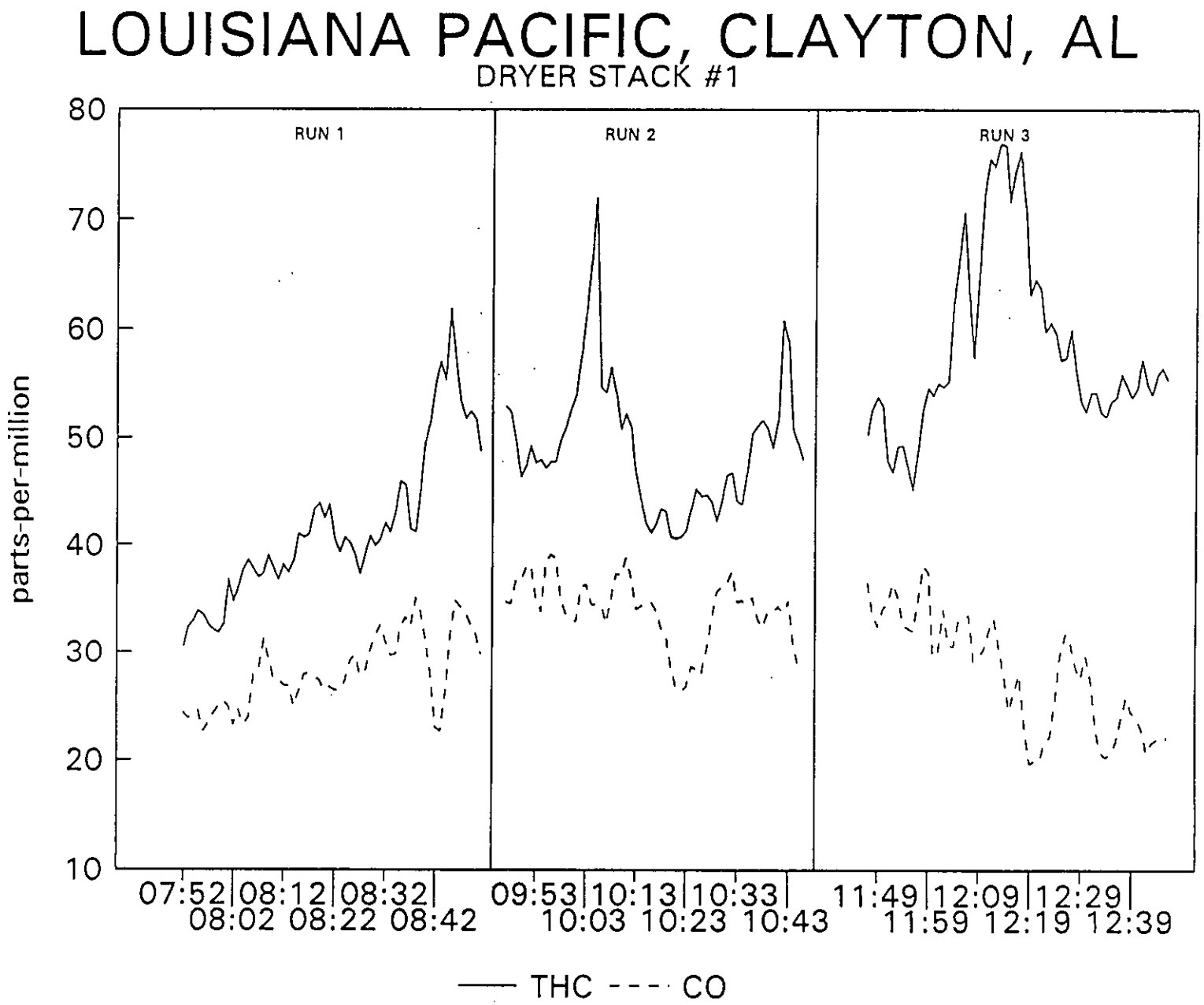
LOUISIANA PACIFIC, CLAYTON, AL
DRYER STACK #1
RUN 1
RUN 2
RUN 3
parts-per-million
80
70
60
50
40
30
20
10
07:52 08:12 08:32
08:02 08:22 08:42
09:53 10:13 10:33
10:03 10:23 10:43
11:49 12:09 12:29
11:59 12:19 12:39
THC
CO

FIGURE 2.1.1-1

TABLE 2.1.2-1
SUMMARY OF EMISSIONS
DRYER STACK #2
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
PM10				
Concentration, gr/dscf	0.016	0.015	0.011	0.014
Emission Rate, lb/hr	6.7	6.2	4.6	5.8
Particulate				
Concentration, gr/dscf	0.076	0.108	0.080	0.088
Emission Rate, lb/hr	35.0	48.2	35.1	39.4
Particulate (Including condensibles)				
Concentration, gr/dscf	0.079	0.114	0.085	0.092
Emission Rate, lb/hr	36.3	50.5	37.4	41.4
Formaldehyde				
Concentration, ppm	20.0	16.8	11.2	16.0
Emission Rate, lb/hr	4.2	3.6	2.6	3.5
Carbon Monoxide				
Concentration, ppm	34.9	27.9	23.0	28.6
Emission Rate, lb/hr	6.8	5.5	5.0	5.8
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	56.8	67.1	53.8	59.2
Emission Rate, lb/hr	18.9	22.5	19.8	20.4

DRYER STACK-2

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.74
(Vm)	Meter Volume, cu.ft	24.070
(Tm)	Avg Meter Temp, deg F	54.6
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	115.5
(Bws)	Moisture (from M5 run), %	4.7
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.650
(θ)	Sample Time, min	59.85
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0195
(Mf)	Particulate Collected (filter), g	0.0057

DRYER STACK-2

3-13-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	24.520
(Ps)	Stack Pressure, inches Hg	29.60
(%Bws)	Moisture, %	4.7
(Ms)	Molecular Weight-wet, lb/lb-mole	28.3
(Vs)	Velocity, ft/s	98.2
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	56,668
(Qstd)	Volumetric flow, dscfm	48,990
(I)	Isokinetic Rate, %	83.4
(Qs)	Cyclone flowrate (actual), cfm	0.474
(Qs)	Cyclone flowrate (target), cfm	0.485
(D50)	Particle Diam. with 50% penetration, um	10.16
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0159
(ER)	Particulate Emission Rate, lb/hr	6.7

TABLE ID 2.1.2-2

DRYER STACK-2

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	22.575
(Tm)	Avg Meter Temp, deg F	69.1
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	129.2
(Bws)	Moisture (from M5 run), %	5.8
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.651
(θ)	Sample Time, min	58.80
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0082
(Mf)	Particulate Collected (filter), g	0.0138

DRYER STACK-2

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	22.445
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	5.8
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2
(Vs)	Velocity, ft/s	99.5
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	57,415
(Qstd)	Volumetric flow, dscfm	48,087
(I)	Isokinetic Rate, %	79.2
(Qs)	Cyclone flowrate (actual), cfm	0.456
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.42
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0151
(ER)	Particulate Emission Rate, lb/hr	6.2

TABLE 2.1.2-3

DRYER STACK-2

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	23.713
(Tm)	Avg Meter Temp, deg F	81.6
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	131.5
(Bws)	Moisture (from M5 run), %	6.1
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.695
(θ)	Sample Time, min	60.12
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0029
(Mf)	Particulate Collected (filter), g	0.0134

DRYER STACK-2

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	23.029
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	6.1
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2
(Vs)	Velocity, ft/s	102.3
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	59,069
(Qstd)	Volumetric flow, dscfm	49,121
(I)	Isokinetic Rate, %	77.8
(Qs)	Cyclone flowrate (actual), cfm	0.461
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.35
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0109
(ER)	Particulate Emission Rate, lb/hr	4.6

TABLE 2.1.2-4

TABLE 2.1.2-5
DRYER STACK #2
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/13/92 1832-2007	RUN 2 3/14/92 0853-0958	RUN 3 3/14/92 1133-1325	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.88	1.82	1.81	1.84
(Bp)	Barometric Pressure, inches Hg	29.83	29.83	29.84	29.83
(Vm)	Meter Volume, cu.ft	40.874	43.168	41.690	41.911
(Tm)	Avg Meter Temp, deg F	52.2	69.0	78.9	66.7
(Pg)	Static Pressure, inches H2O	-2.00	-2.00	-2.00	-2.00
(Ts)	Avg Stack Temp, deg F	116.0	126.5	130.3	124.3
(Vlc)	Water Collected, ml	44.7	56.5	56.9	52.7
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.812	1.779	1.778	1.79
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.155	0.155	0.155	0.155
(D)	Stack Diameter, inches	42	42	42	42
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0653	0.0952	0.0725	0.0777
(Mf)	Particulate Collected (filter), g	0.1427	0.2084	0.1387	0.1633
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0006	0.0053	0.0054	0.0038
(Mio)	MeCl Impinger (organic) residue, g	0.0072	0.0092	0.0083	0.0082
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	42.270	43.219	40.985	42.158
(Ps)	Stack Pressure, inches Hg	29.68	29.68	29.69	29.69
(%Bws)	Moisture, %	4.7	5.8	6.1	5.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.3	28.2	28.2	28.2
(Vs)	Velocity, ft/s	107.7	106.9	107.3	107.3
(As)	Stack Area, sq.ft	9.62	9.62	9.62	9.62
(Qa)	Volumetric flow, acfm	62,176	61,722	61,917	61,939
(Qs)	Volumetric flow, dscfm	53,841	51,909	51,570	52,440
(I)	Isokinetic Rate, %	96.1	101.9	97.3	98.4
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0759	0.1084	0.0795	0.0879
(ER)	Particulate Emission Rate, lb/hr	35.0	48.2	35.1	39.5
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0761	0.1103	0.0815	0.0893
(ER)	Particulate Emission Rate, lb/hr	35.1	49.1	36.0	40.1
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0788	0.1136	0.0847	0.0923
(ER)	Particulate Emission Rate, lb/hr	36.3	50.5	37.4	41.4
	Train Fractionation:				
	filterable, %	96	95	94	95
	condensible, %	4	5	6	5

TABLE 2.1.2-6

DRYER STACK #2

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/19/92 1538-1644	RUN 2 3/19/92 1751-1855	RUN 3 3/20/92 0744-0847	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	0.998	0.998	0.998	0.998
	Avg Delta H, inches H2O	3.43	3.53	3.43	3.46
(Bp)	Barometric Pressure, inches Hg	29.58	29.58	29.58	29.58
(Vm)	Meter Volume, cf	58.923	61.121	62.316	60.787
(Tm)	Avg Meter Temp, deg F	87.5	85.4	59.1	77.4
(Pg)	Static Pressure, inches H2O	-0.83	-0.83	-0.83	-0.83
(Ts)	Avg Stack Temp, deg F	133.5	134.0	128.8	132.1
(Vlc)	Water Collected, ml	95.8	105.5	89.8	97.0
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	1.572	1.588	1.740	1.63
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.196	0.196	0.196	0.196
(Ds)	Stack Diameter, inches	42	42	42	42
(Mf)	Total Formaldehyde, mg	40	35	25	33
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	56.521	58.868	63.044	59.478
(Ps)	Stack Pressure, inches Hg	29.52	29.52	29.52	29.52
(%Bws)	Moisture (from impingers), %	7.4	7.8	6.3	7.2
(%Bws)	Moisture (at saturation), %	16.6	16.6	14.5	15.9
(Ms)	Molecular Weight-wet, lb/lb-mole	28.0	28.0	28.2	28.1
(Vs)	Velocity, ft/s	95.6	96.7	105.2	99.1
(As)	Stack Area, sq ft	9.62	9.62	9.62	9.62
(Qa)	Volumetric flow, acfm	5.52E+04	5.58E+04	6.07E+04	5.72E+04
(Qs)	Volumetric flow, dscfm	4.48E+04	4.51E+04	5.03E+04	4.68E+04
(I)	Isokinetic Rate, %	96.5	99.9	95.9	97.4
(Cf)	Formaldehyde Concentration, mg/dscf	0.71	0.59	0.40	0.57
(Cppm)	Formaldehyde Concentration, ppm	20.0	16.8	11.2	16.0
(ER)	Formaldehyde Emission Rate, lb/hr	4.20	3.55	2.64	3.46

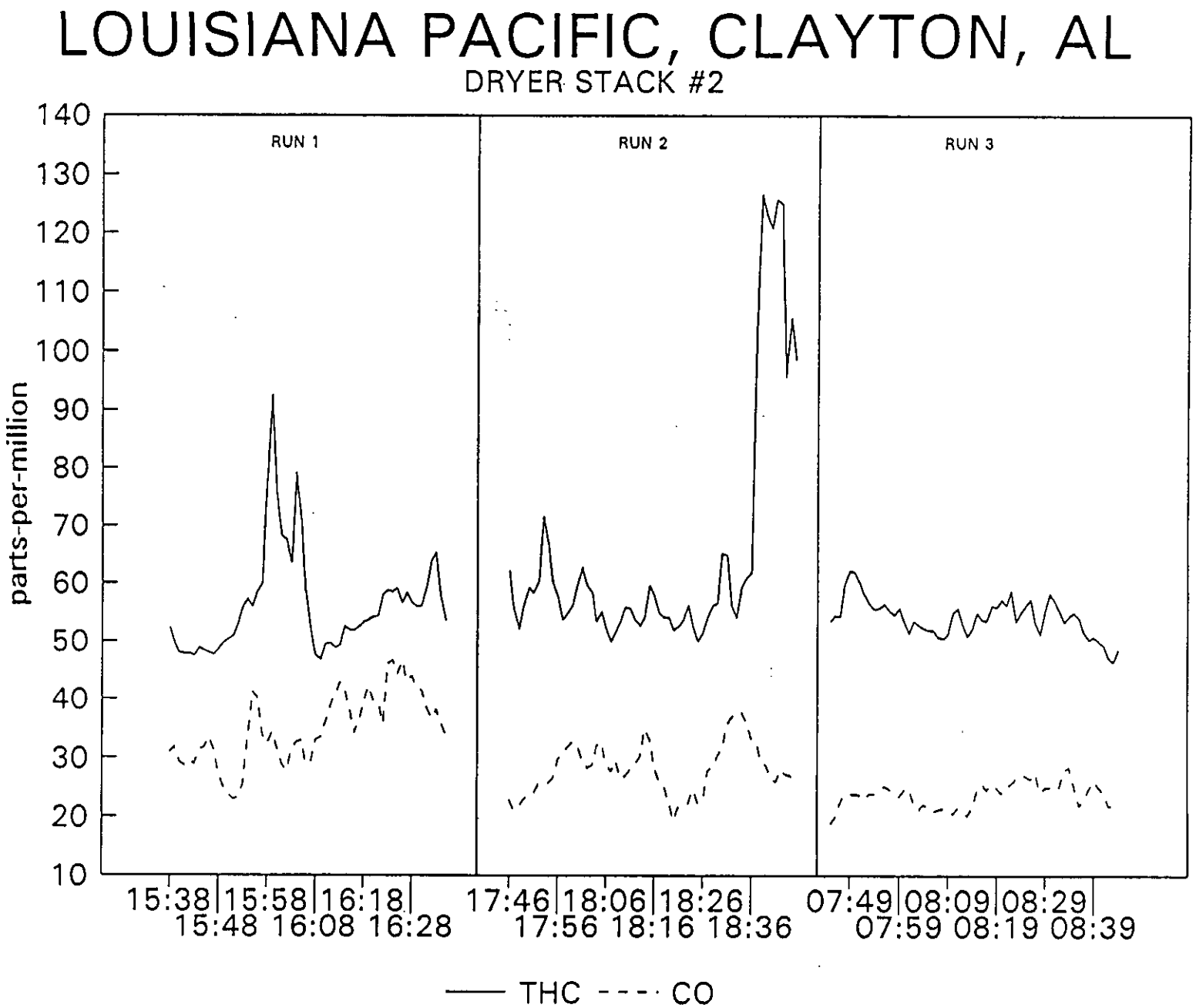
LOUISIANA PACIFIC, CLAYTON, AL
DRYER STACK #2
RUN 1
RUN 2
RUN 3
parts-per-million
140
130
120
110
100
90
80
70
60
50
40
30
20
10
15:38 15:58 16:18
15:48 16:08 16:28
17:46 18:06 18:26
17:56 18:16 18:36
07:49 08:09 08:29
07:59 08:19 08:39
THC
CO

FIGURE 2.1.2-1

TABLE 2.1.3-1
SUMMARY OF EMISSIONS
DRYER STACK #3
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	AVERAGE
PM10			
Concentration, gr/dscf	0.009	0.025	0.017
Emission Rate, lb/hr	3.3	9.6	6.5
Particulate			
Concentration, gr/dscf	0.115	0.104	0.110
Emission Rate, lb/hr	45.3	42.7	44.0
Particulate (Including condensibles)			
Concentration, gr/dscf	0.120	0.108	0.114
Emission Rate, lb/hr	47.0	44.3	45.7
Formaldehyde			
Concentration, ppm	16.1	16.3	16.2
Emission Rate, lb/hr	3.3	3.4	3.4
Carbon Monoxide			
Concentration, ppm	17.6	11.4	14.5
Emission Rate, lb/hr	3.4	2.2	2.8
Total Hydrocarbons (VOC), as propane			
Concentration, ppm	45.3	50.8	48.1
Emission Rate, lb/hr	14.4	16.5	15.5

DRYER STACK-3

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	19.798
(Tm)	Avg Meter Temp, deg F	80.8
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	125.8
(Bws)	Moisture (from M5 run), %	5.8
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.469
(θ)	Sample Time, min	52.81
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0001
(Mf)	Particulate Collected (filter), g	0.0112

DRYER STACK-3

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	19.256
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	5.8
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2
(Vs)	Velocity, ft/s	88.2
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	50,938
(Qstd)	Volumetric flow, dscfm	42,908
(I)	Isokinetic Rate, %	84.8
(Qs)	Cyclone flowrate (actual), cfm	0.433
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.81
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0091
(ER)	Particulate Emission Rate, lb/hr	3.3

TABLE 2.1.3-2

DRYER STACK-3

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	22.367
(Tm)	Avg Meter Temp, deg F	80.3
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	125.1
(Bws)	Moisture (from M5 run), %	6.3
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.554
(θ)	Sample Time, min	60.58
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0050
(Mf)	Particulate Collected (filter), g	0.0300

DRYER STACK-3

3-14-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	21.774
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	6.3
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2
(Vs)	Velocity, ft/s	93.4
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	53,888
(Qstd)	Volumetric flow, dscfm	45,206
(I)	Isokinetic Rate, %	79.3
(Qs)	Cyclone flowrate (actual), cfm	0.428
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.89
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0248
(ER)	Particulate Emission Rate, lb/hr	9.6

TABLE 2.1.3-3

TABLE 2.1.3-4
DRYER STACK #3
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/14/92 1516-1623	RUN 2 3/14/92 1744-1848	AVERAGE
	MEASURED DATA			
(Y)	Meter Box Y	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.41	1.56	1.49
(Bp)	Barometric Pressure, inches Hg	29.84	29.84	29.84
(Vm)	Meter Volume, cu.ft	36.487	38.526	37.507
(Tm)	Avg Meter Temp, deg F	75.0	72.4	73.7
(Pg)	Static Pressure, inches H2O	-1.95	-1.95	-1.95
(Ts)	Avg Stack Temp, deg F	124.4	125.5	125.0
(Vlc)	Water Collected, ml	47.6	55.1	51.4
(CO2)	Carbon dioxide, %	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.568	1.647	1.61
(0)	Sample Time, min	60	60	60
(Dn)	Nozzle Diameter, inches	0.155	0.155	0.155
(D)	Stack Diameter, inches	42	42	42
	Filterable PM			
(Mpw)	Particulate Collected (probe wash), g	0.0737	0.0738	0.0738
(Mf)	Particulate Collected (filter), g	0.1962	0.1843	0.1903
	Condensible PM			
(Mii)	H2O Impinger (inorganic) residue, g	0.0032	0.0054	0.0043
(Mio)	MeCl Impinger (organic) residue, g	0.0068	0.0047	0.0058
	CALCULATED DATA			
(Vmstd)	Standard Meter Volume, cu.ft	36.096	38.313	37.204
(Ps)	Stack Pressure, inches Hg	29.70	29.70	29.70
(%Bws)	Moisture, %	5.8	6.3	6.1
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2	28.1	28.2
(Vs)	Velocity, ft/s	94.1	99.0	96.5
(As)	Stack Area, sq.ft	9.62	9.62	9.62
(Qa)	Volumetric flow, acfm	54,297	57,141	55,719
(Qs)	Volumetric flow, dscfm	45,826	47,882	46,854
(I)	Isokinetic Rate, %	96.4	97.9	97.2
	Total filterable PM			
(Cs)	Particulate Concentration, grain/dscf	0.1154	0.1039	0.1097
(ER)	Particulate Emission Rate, lb/hr	45.3	42.7	44.0
	Including only inorganic PM			
(Cs)	Particulate Concentration, grain/dscf	0.1167	0.1061	0.1114
(ER)	Particulate Emission Rate, lb/hr	45.8	43.5	44.7
	Including organic/inorganic PM			
(Cs)	Particulate Concentration, grain/dscf	0.1197	0.1080	0.1138
(ER)	Particulate Emission Rate, lb/hr	47.0	44.3	45.7
	Train Fractionation:			
	filterable, %	96	96	96
	condensible, %	4	4	4

TABLE 2.1.3-5

DRYER STACK #3

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/21/92 0753-0856	RUN 2 3/21/92 0915-1020	AVERAGE
	MEASURED DATA			
(Y)	Meter Box Y	0.998	0.998	0.998
	Avg Delta H, inches H2O	3.00	3.09	3.05
(Bp)	Barometric Pressure, inches Hg	29.95	29.95	29.95
(Vm)	Meter Volume, cf	55.348	57.813	56.581
(Tm)	Avg Meter Temp, deg F	62.0	75.1	68.6
(Pg)	Static Pressure, inches H2O	1.00	1.00	1.00
(Ts)	Avg Stack Temp, deg F	127.0	123.4	125.2
(Vlc)	Water Collected, ml	74.4	63.6	69.0
(CO2)	Carbon dioxide, %	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	1.490	1.522	1.506
(0)	Sample Time, min	60	60	60
(Dn)	Nozzle Diameter, inches	0.196	0.196	0.196
(Ds)	Stack Diameter, inches	42	42	42
(Mf)	Total Formaldehyde, mg	32	33	33
	CALCULATED DATA			
(Vmstd)	Standard Meter Volume, dscf	56.318	57.398	56.858
(Ps)	Stack Pressure, inches Hg	30.02	30.02	30.02
(%Bws)	Moisture (from impingers), %	5.9	5.0	5.4
(%Bws)	Moisture (at saturation), %	13.9	12.5	13.2
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2	28.3	28.3
(Vs)	Velocity, ft/s	89.1	90.6	89.8
(As)	Stack Area, sq ft	9.62	9.62	9.62
(Qa)	Volumetric flow, acfm	5.14E+04	5.23E+04	5.19E+04
(Qs)	Volumetric flow, dscfm	4.37E+04	4.51E+04	4.44E+04
(I)	Isokinetic Rate, %	98.7	97.4	98.0
(Cf)	Formaldehyde Concentration, mg/dscf	0.57	0.57	0.57
(Cppm)	Formaldehyde Concentration, ppm	16.1	16.3	16.2
(ER)	Formaldehyde Emission Rate, lb/hr	3.28	3.43	3.36

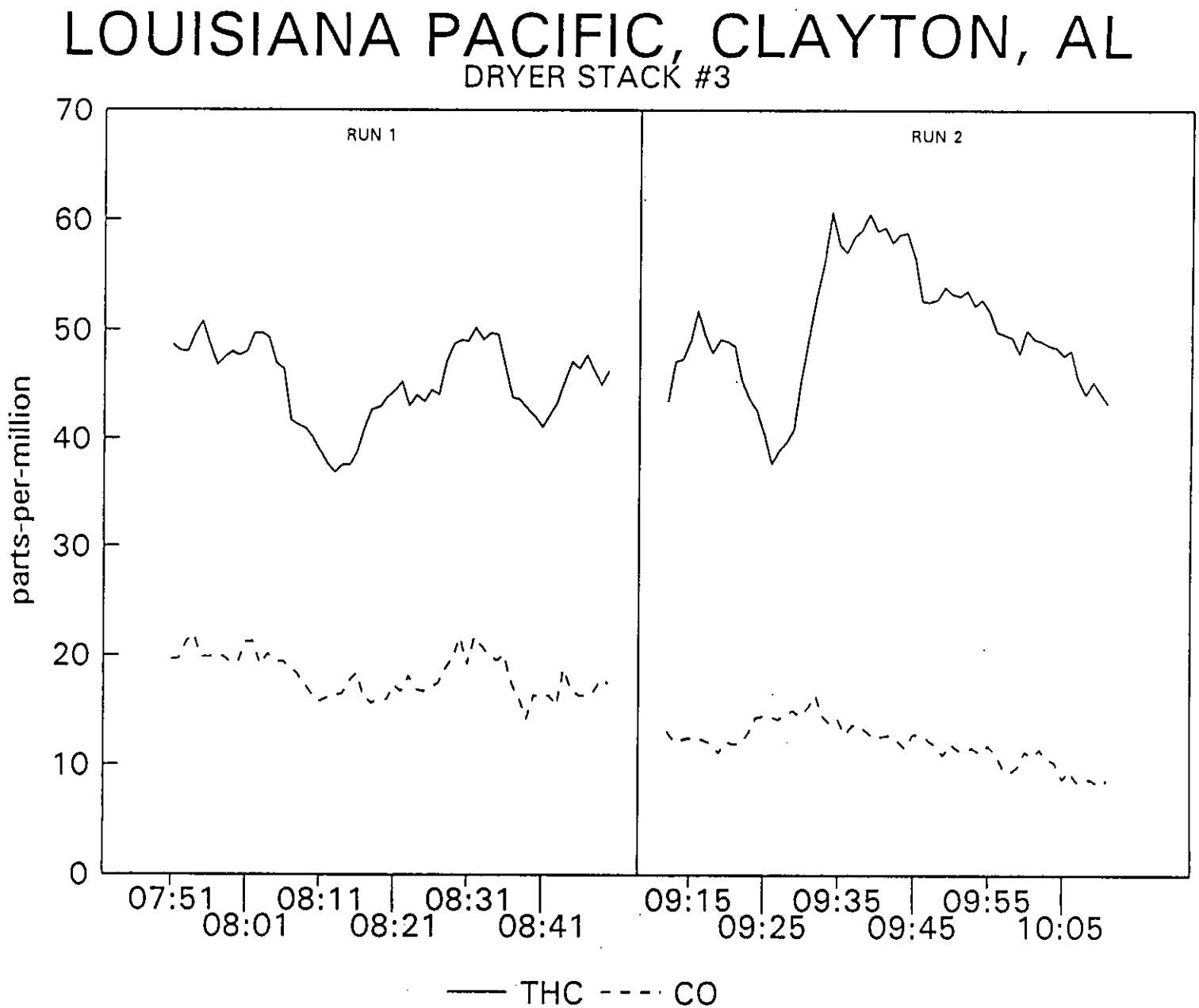
LOUISIANA PACIFIC, CLAYTON, AL
DRYER STACK #3
RUN 1
RUN 2
parts-per-million
70
60
50
40
30
20
10
0
07:51
08:01
08:11
08:21
08:31
08:41
09:15
09:25
09:35
09:45
09:55
10:05
THC
CO

FIGURE 2.1.3-1

TABLE 2.1.4-1
SUMMARY OF EMISSIONS
DRYER STACK #4
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	AVERAGE
PM10			
Concentration, gr/dscf	0.023	0.019	0.021
Emission Rate, lb/hr	8.2	7.0	7.6
Particulate			
Concentration, gr/dscf	0.132	0.121	0.126
Emission Rate, lb/hr	53.2	49.7	51.5
Particulate (Including condensibles)			
Concentration, gr/dscf	0.138	0.132	0.135
Emission Rate, lb/hr	55.8	54.2	55.0
Formaldehyde			
Concentration, ppm	18.5	16.1	17.3
Emission Rate, lb/hr	3.6	3.3	3.4
Carbon Monoxide			
Concentration, ppm	8.6	9.4	9.0
Emission Rate, lb/hr	1.6	1.8	1.7
Total Hydrocarbons (VOC), as propane			
Concentration, ppm	42.0	42.1	42.1
Emission Rate, lb/hr	12.7	13.2	13.0

DRYER STACK-4

3-16-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	20.961
(Tm)	Avg Meter Temp, deg F	60.8
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	132.6
(Bws)	Moisture (from M5 run), %	6.7
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.474
(θ)	Sample Time, min	56.60
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0113
(Mf)	Particulate Collected (filter), g	0.0196

DRYER STACK-4

3-16-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	21.170
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	6.7
(Ms)	Molecular Weight-wet, lb/lb-mole	28.1
(Vs)	Velocity, ft/s	89.2
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	51,488
(Qstd)	Volumetric flow, dscfm	42,463
(I)	Isokinetic Rate, %	87.9
(Qs)	Cyclone flowrate (actual), cfm	0.454
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.46
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0225
(ER)	Particulate Emission Rate, lb/hr	8.2

TABLE 2.1.4-2

DRYER STACK-4

3-16-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.53
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	23.051
(Tm)	Avg Meter Temp, deg F	78.7
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	130.5
(Bws)	Moisture (from M5 run), %	5.9
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.506
(θ)	Sample Time, min	57.77
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0059
(Mf)	Particulate Collected (filter), g	0.0215

DRYER STACK-4

3-16-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	22.508
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	5.9
(Ms)	Molecular Weight-wet, lb/lb-mole	28.2
(Vs)	Velocity, ft/s	90.8
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	52,420
(Qstd)	Volumetric flow, dscfm	43,757
(I)	Isokinetic Rate, %	88.8
(Qs)	Cyclone flowrate (actual), cfm	0.467
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam, with 50% penetration, um	10.25
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0188
(ER)	Particulate Emission Rate, lb/hr	7.0

TABLE 2.1.4-3

TABLE 2.1.4-4
DRYER STACK #4
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/16/92 0903-1016	RUN 2 3/16/92 1053-1200	AVERAGE
	MEASURED DATA			
(Y)	Meter Box Y	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.52	1.55	1.54
(Bp)	Barometric Pressure, inches Hg	30.05	30.05	30.05
(Vm)	Meter Volume, cu.ft	36.184	38.158	37.171
(Tm)	Avg Meter Temp, deg F	62.7	74.4	68.6
(Pg)	Static Pressure, inches H2O	-2.00	-2.00	-2.00
(Ts)	Avg Stack Temp, deg F	132.7	129.1	130.9
(Vlc)	Water Collected, ml	56.4	50.9	53.7
(CO2)	Carbon dioxide, %	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.628	1.645	1.64
(0)	Sample Time, min	60	60	60
(Dn)	Nozzle Diameter, inches	0.155	0.155	0.155
(D)	Stack Diameter, inches	42	42	42
	Filterable PM			
(Mpw)	Particulate Collected (probe wash), g	0.0964	0.0818	0.0891
(Mf)	Particulate Collected (filter), g	0.2189	0.2160	0.2175
	Condensible PM			
(Mii)	H2O Impinger (inorganic) residue, g	0.0056	0.0164	0.0110
(Mio)	MeCl Impinger (organic) residue, g	0.0101	0.0109	0.0105
	CALCULATED DATA			
(Vmstd)	Standard Meter Volume, cu.ft	36.905	38.069	37.487
(Ps)	Stack Pressure, inches Hg	29.90	29.90	29.90
(%Bws)	Moisture, %	6.7	5.9	6.3
(Ms)	Molecular Weight-wet, lb/lb-mole	28.1	28.2	28.2
(Vs)	Velocity, ft/s	98.2	98.7	98.5
(As)	Stack Area, sq.ft	9.62	9.62	9.62
(Qa)	Volumetric flow, acfm	56,672	57,002	56,837
(Qs)	Volumetric flow, dscfm	47,052	48,019	47,535
(I)	Isokinetic Rate, %	96.0	97.0	96.5
	Total filterable PM			
(Cs)	Particulate Concentration, grain/dscf	0.1318	0.1207	0.1263
(ER)	Particulate Emission Rate, lb/hr	53.2	49.7	51.4
	Including only inorganic PM			
(Cs)	Particulate Concentration, grain/dscf	0.1342	0.1273	0.1308
(ER)	Particulate Emission Rate, lb/hr	54.1	52.4	53.3
	Including organic/inorganic PM			
(Cs)	Particulate Concentration, grain/dscf	0.1384	0.1318	0.1351
(ER)	Particulate Emission Rate, lb/hr	55.8	54.2	55.0
	Train Fractionation:			
	filterable, %	95	92	93
	condensible, %	5	8	7

TABLE 2.1.4-5

DRYER STACK #4

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/21/92 1104-1207	RUN 2 3/21/92 1225-1329	AVERAGE
	MEASURED DATA			
(Y)	Meter Box Y	0.998	0.998	0.998
	Avg Delta H, inches H2O	3.36	3.61	3.48
(Bp)	Barometric Pressure, inches Hg	29.95	29.95	29.95
(Vm)	Meter Volume, cf	59.729	63.018	61.374
(Tm)	Avg Meter Temp, deg F	85.6	86.8	86.2
(Pg)	Static Pressure, inches H2O	1.00	1.00	1.00
(Ts)	Avg Stack Temp, deg F	124.9	121.4	123.2
(Vlc)	Water Collected, ml	58.4	70.3	64.4
(CO2)	Carbon dioxide, %	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	1.553	1.607	1.580
(0)	Sample Time, min	60	60	60
(Dn)	Nozzle Diameter, inches	0.196	0.196	0.196
(Ds)	Stack Diameter, inches	40	40	40
(Mf)	Total Formaldehyde, mg	38	35	37
	CALCULATED DATA			
(Vmstd)	Standard Meter Volume, dscf	58.198	61.304	59.751
(Ps)	Stack Pressure, inches Hg	30.02	30.02	30.02
(%Bws)	Moisture (from impingers), %	4.5	5.1	4.8
(%Bws)	Moisture (at saturation), %	12.8	11.8	12.3
(Ms)	Molecular Weight-wet, lb/lb-mole	28.3	28.3	28.3
(Vs)	Velocity, ft/s	92.5	95.5	94.0
(As)	Stack Area, sq ft	8.73	8.73	8.73
(Qa)	Volumetric flow, acfm	4.84E+04	5.00E+04	4.92E+04
(Qs)	Volumetric flow, dscfm	4.19E+04	4.32E+04	4.25E+04
(I)	Isokinetic Rate, %	96.5	98.5	97.5
(Cf)	Formaldehyde Concentration, mg/dscf	0.65	0.57	0.61
(Cppm)	Formaldehyde Concentration, ppm	18.5	16.1	17.3
(ER)	Formaldehyde Emission Rate, lb/hr	3.62	3.26	3.44

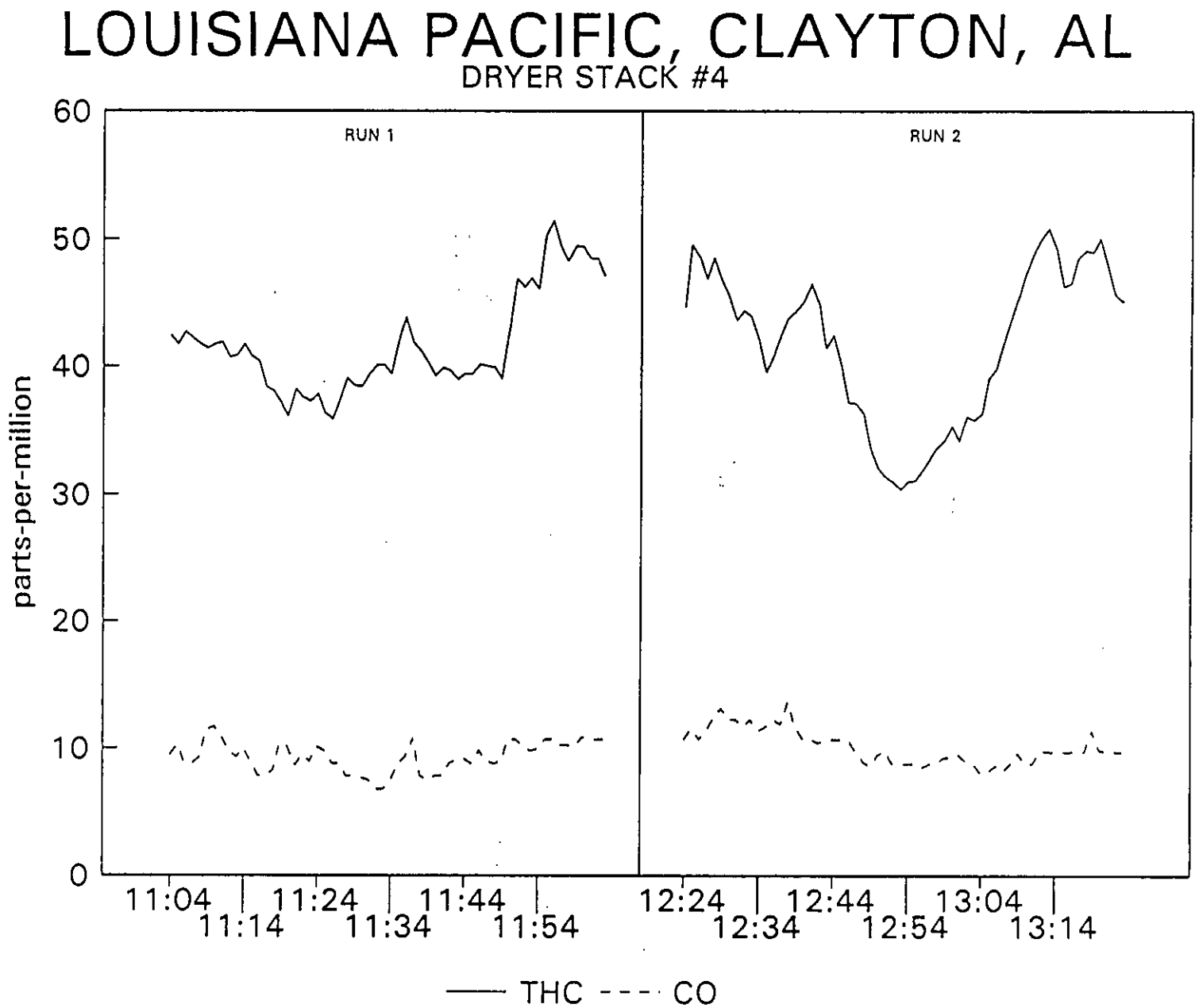
LOUISIANA PACIFIC, CLAYTON, AL
DRYER STACK #4
RUN 1
RUN 2
parts-per-million
60
50
40
30
20
10
0
11:04
11:14
11:24
11:34
11:44
11:54
12:24
12:34
12:44
12:54
13:04
13:14
THC
CO

FIGURE 2.1.4-1

TABLE 2.1.5-1
SUMMARY OF EMISSIONS
DRYER STACK #6
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
PM10				
Concentration, gr/dscf	0.018	0.006	0.010	0.011
Emission Rate, lb/hr	5.4	1.9	3.0	3.4
Particulate				
Concentration, gr/dscf	0.141	0.138	0.115	0.131
Emission Rate, lb/hr	38.1	37.2	30.9	35.4
Particulate (Including condensibles)				
Concentration, gr/dscf	0.150	0.145	0.123	0.139
Emission Rate, lb/hr	40.5	39.2	33.0	37.6
Formaldehyde				
Concentration, ppm	11.5	12.6	13.2	12.4
Emission Rate, lb/hr	1.8	1.8	2.0	1.9
Carbon Monoxide				
Concentration, ppm	187.0	191.6	197.5	192.0
Emission Rate, lb/hr	27.4	25.9	27.8	27.0
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	120.3	101.0	97.4	106.2
Emission Rate, lb/hr	30.4	23.7	23.7	25.9

DRYER STACK-6

3-12-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.27
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	16.996
(Tm)	Avg Meter Temp, deg F	55.2
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	139.1
(Bws)	Moisture (from M5 run), %	8.3
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.251
(θ)	Sample Time, min	58.47
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0039
(Mf)	Particulate Collected (filter), g	0.0162

DRYER STACK-6

3-12-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	17.342
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	8.3
(Ms)	Molecular Weight-wet, lb/lb-mole	27.9
(Vs)	Velocity, ft/s	76.3
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	44,058
(Qstd)	Volumetric flow, dscfm	35,329
(I)	Isokinetic Rate, %	83.7
(Qs)	Cyclone flowrate (actual), cfm	0.370
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	12.09
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0179
(ER)	Particulate Emission Rate, lb/hr	5.4

TABLE 2.1.5-2

DRYER STACK-6

3-12-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.27
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	17.126
(Tm)	Avg Meter Temp, deg F	66.2
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	137.7
(Bws)	Moisture (from M5 run), %	7.6
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.253
(θ)	Sample Time, min	58.68
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0012
(Mf)	Particulate Collected (filter), g	0.0056

DRYER STACK-6

3-12-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	17.109
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	7.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.0
(Vs)	Velocity, ft/s	76.3
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	44,024
(Qstd)	Volumetric flow, dscfm	35,654
(I)	Isokinetic Rate, %	81.6
(Qs)	Cyclone flowrate (actual), cfm	0.360
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	12.32
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0061
(ER)	Particulate Emission Rate, lb/hr	1.9

TABLE 2.1.5-3

DRYER STACK-6

3-12-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.27
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	17.787
(Tm)	Avg Meter Temp, deg F	68.1
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	136.1
(Bws)	Moisture (from M5 run), %	8.0
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.262
(θ)	Sample Time, min	61.16
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	42.0
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0025
(Mf)	Particulate Collected (filter), g	0.0086

DRYER STACK-6

3-12-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	17.706
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	8.0
(Ms)	Molecular Weight-wet, lb/lb-mole	28.0
(Vs)	Velocity, ft/s	76.8
(As)	Stack Area, sq.ft	9.62
(Qa)	Volumetric flow, acfm	44,308
(Qstd)	Volumetric flow, dscfm	35,822
(I)	Isokinetic Rate, %	80.6
(Qs)	Cyclone flowrate (actual), cfm	0.358
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	12.37
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0097
(ER)	Particulate Emission Rate, lb/hr	3.0

TABLE 2.1.5-4

TABLE 2.1.5-5
DRYER STACK #6
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/12/92 0842-0950	RUN 2 3/12/92 1049-1154	RUN 3 3/12/92 1312-1418	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.30	1.27	1.27	1.28
(Bp)	Barometric Pressure, inches Hg	29.83	29.83	29.83	29.83
(Vm)	Meter Volume, cu.ft	35.806	35.977	36.692	36.158
(Tm)	Avg Meter Temp, deg F	54.0	63.7	65.5	61.1
(Pg)	Static Pressure, inches H2O	-0.90	-0.90	-0.90	-0.90
(Ts)	Avg Stack Temp, deg F	138.7	138.8	135.0	137.5
(Vlc)	Water Collected, ml	70.9	63.9	68.5	67.8
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.231	1.218	1.219	1.22
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.178	0.178	0.178	0.178
(D)	Stack Diameter, inches	40	40	40	40
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.2567	0.2551	0.2174	0.2431
(Mf)	Particulate Collected (filter), g	0.0794	0.0705	0.0570	0.0690
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0066	0.0044	0.0100	0.0070
(Mio)	MeCl Impinger (organic) residue, g	0.0150	0.0125	0.0089	0.0121
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	36.847	36.335	36.930	36.704
(Ps)	Stack Pressure, inches Hg	29.76	29.76	29.76	29.76
(%Bws)	Moisture, %	8.3	7.6	8.0	8.0
(Ms)	Molecular Weight-wet, lb/lb-mole	27.9	28.0	28.0	28.0
(Vs)	Velocity, ft/s	75.0	74.1	74.0	74.4
(As)	Stack Area, sq.ft	8.73	8.73	8.73	8.73
(Qa)	Volumetric flow, acfm	39,276	38,815	38,752	38,948
(Qs)	Volumetric flow, dscfm	31,583	31,431	31,450	31,488
(I)	Isokinetic Rate, %	98.2	97.3	98.9	98.1
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.1407	0.1383	0.1147	0.1312
(ER)	Particulate Emission Rate, lb/hr	38.1	37.2	30.9	35.4
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.1435	0.1401	0.1188	0.1342
(ER)	Particulate Emission Rate, lb/hr	38.8	37.7	32.0	36.2
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.1498	0.1454	0.1225	0.1393
(ER)	Particulate Emission Rate, lb/hr	40.5	39.2	33.0	37.6
	Train Fractionation:				
	filterable, %	94	95	94	94
	condensible, %	6	5	6	6

TABLE 2.1.5-6

DRYER STACK #6

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/20/92 1603-1759	RUN 2 3/20/92 1729-1833	RUN 3 3/20/92 1853-1958	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	0.998	0.998	0.998	0.998
	Avg Delta H, inches H2O	2.34	2.07	2.18	2.20
(Bp)	Barometric Pressure, inches Hg	29.82	29.82	29.82	29.82
(Vm)	Meter Volume, cf	49.827	47.723	47.664	48.405
(Tm)	Avg Meter Temp, deg F	73.1	75.0	73.7	73.9
(Pg)	Static Pressure, inches H2O	1.20	1.20	1.20	1.20
(Ts)	Avg Stack Temp, deg F	136.8	134.0	141.0	137.3
(Vlc)	Water Collected, ml	97.5	100.0	98.0	98.5
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	1.306	1.209	1.264	1.26
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.195	0.195	0.195	0.195
(Ds)	Stack Diameter, inches	40	40	40	40
(Mf)	Total Formaldehyde, mg	20	21	22	21
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	49.350	47.071	47.136	47.852
(Ps)	Stack Pressure, inches Hg	29.91	29.91	29.91	29.91
(%Bws)	Moisture (from impingers), %	8.5	9.1	8.9	8.8
(%Bws)	Moisture (at saturation), %	17.7	16.8	20.2	18.2
(Ms)	Molecular Weight-wet, lb/lb-mole	27.9	27.9	27.9	27.9
(Vs)	Velocity, ft/s	79.3	73.3	77.1	76.6
(As)	Stack Area, sq ft	8.73	8.73	8.73	8.73
(Qa)	Volumetric flow, acfm	4.15E+04	3.84E+04	4.04E+04	4.01E+04
(Qs)	Volumetric flow, dscfm	3.36E+04	3.10E+04	3.23E+04	3.23E+04
(I)	Isokinetic Rate, %	103.1	106.5	102.5	104.0
(Cf)	Formaldehyde Concentration, mg/dscf	0.41	0.45	0.47	0.44
(Cppm)	Formaldehyde Concentration, ppm	11.5	12.6	13.2	12.4
(ER)	Formaldehyde Emission Rate, lb/hr	1.80	1.83	1.99	1.87

TABLE 2.1.5-7
DRYER STACK #5
VOLUMETRIC FLOW ONLY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/12/92 0908
	MEASURED DATA	
(Bp)	Barometric Pressure, inches Hg	29.83
(Pg)	Static Pressure, inches H2O	-1.20
(Ts)	Avg Stack Temp, deg F	141
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O	1.42
(D)	Stack Diameter, inches	40
	CALCULATED DATA	
(Ps)	Stack Pressure, inches Hg	29.74
(%Bws)	Moisture (from Dryer 8), %	7.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.0
(Vs)	Velocity, ft/s	86.7
(As)	Stack Area, sq.ft	8.73
(Qa)	Volumetric flow, acfm	45,415
(Qs)	Volumetric flow, dscfm	36,644

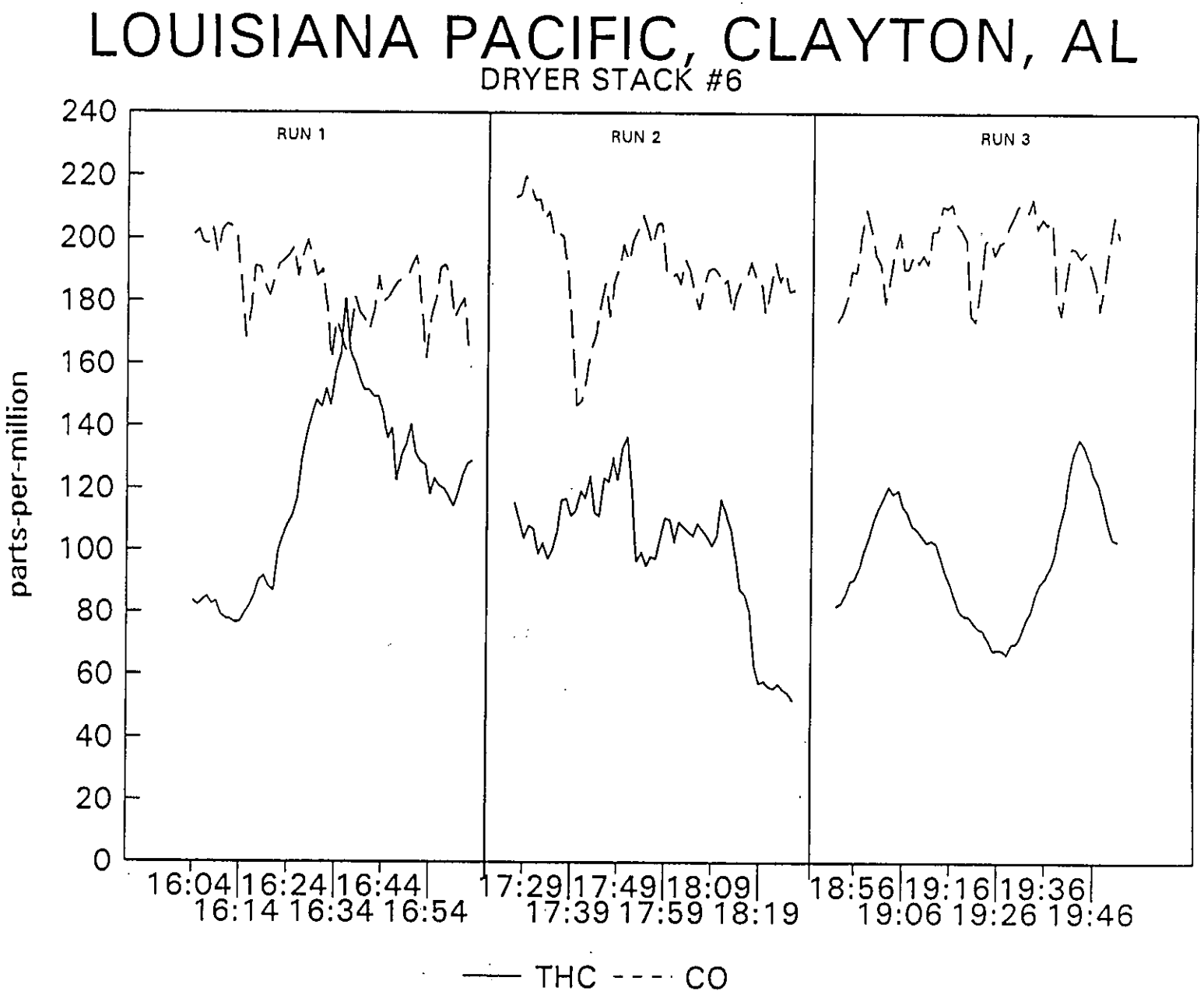
LOUISIANA PACIFIC, CLAYTON, AL
DRYER STACK #6
RUN 1
RUN 2
RUN 3
parts-per-million
240
220
200
180
160
140
120
100
80
60
40
20
0
16:04 16:24 16:44
16:14 16:34 16:54
17:29 17:49 18:09
17:39 17:59 18:19
18:56 19:16 19:36
19:06 19:26 19:46
THC
CO

FIGURE 2.1.5-1

TABLE 2.1.6-1
SUMMARY OF EMISSIONS
DRYER STACK #8
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
PM10				
Concentration, gr/dscf	0.006	0.005	0.007	0.006
Emission Rate, lb/hr	1.7	1.3	2.0	1.7
Particulate				
Concentration, gr/dscf	0.051	0.043	0.045	0.047
Emission Rate, lb/hr	14.2	12.2	13.0	13.1
Particulate (Including condensibles)				
Concentration, gr/dscf	0.055	0.050	0.050	0.052
Emission Rate, lb/hr	15.3	14.1	14.3	14.6
Formaldehyde				
Concentration, ppm	12.7	11.5	20.0	14.7
Emission Rate, lb/hr	1.9	1.7	2.8	2.1
Carbon Monoxide				
Concentration, ppm	222.2	209.2	219.0	216.8
Emission Rate, lb/hr	30.8	28.6	28.9	29.4
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	100.5	88.8	116.5	101.9
Emission Rate, lb/hr	24.2	21.5	27.3	24.3

DRYER STACK-8

3-11-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.47
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	21.883
(Tm)	Avg Meter Temp, deg F	56.3
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	130.4
(Bws)	Moisture (from M5 run), %	7.8
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.486
(θ)	Sample Time, min	58.56
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	37.5
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0014
(Mf)	Particulate Collected (filter), g	0.0069

DRYER STACK-8

3-11-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 1
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	22.293
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	7.8
(Ms)	Molecular Weight-wet, lb/lb-mole	28.0
(Vs)	Velocity, ft/s	89.9
(As)	Stack Area, sq.ft	7.67
(Qa)	Volumetric flow, acfm	41,379
(Qstd)	Volumetric flow, dscfm	33,851
(I)	Isokinetic Rate, %	89.4
(Qs)	Cyclone flowrate (actual), cfm	0.465
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.27
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0057
(ER)	Particulate Emission Rate, lb/hr	1.7

TABLE 2.1.6-2

DRYER STACK-8

3-11-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.47
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	22.531
(Tm)	Avg Meter Temp, deg F	52.5
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	127.7
(Bws)	Moisture (from M5 run), %	8.3
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.491
(θ)	Sample Time, min	59.48
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	37.5
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0011
(Mf)	Particulate Collected (filter), g	0.0056

DRYER STACK-8

3-11-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 2
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	23.123
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	8.3
(Ms)	Molecular Weight-wet, lb/lb-mole	27.9
(Vs)	Velocity, ft/s	90.1
(As)	Stack Area, sq.ft	7.67
(Qa)	Volumetric flow, acfm	41,464
(Qstd)	Volumetric flow, dscfm	33,890
(I)	Isokinetic Rate, %	91.2
(Qs)	Cyclone flowrate (actual), cfm	0.476
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.11
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0045
(ER)	Particulate Emission Rate, lb/hr	1.3

TABLE 2.1.6-3

DRYER STACK-8

3-11-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	MEASURED DATA	
(Y)	Meter Box Y	0.998
	Avg Delta H, inches H2O	0.47
(Bp)	Barometric Pressure, inches Hg	29.84
(Vm)	Meter Volume, cu.ft	22.025
(Tm)	Avg Meter Temp, deg F	61.3
(Pg)	Static Pressure, inches H2O	-1.95
(Ts)	Avg Stack Temp, deg F	128.2
(Bws)	Moisture (from M5 run), %	6.6
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.459
(θ)	Sample Time, min	58.14
(Dn)	Nozzle Diameter, inches	0.133
(Ds)	Stack Diameter, inches	37.5
	<PM10	
(Mpw)	Particulate Collected (probe wash), g	0.0043
(Mf)	Particulate Collected (filter), g	0.0057

DRYER STACK-8

3-11-92

PM10 SUMMARY

SYMBOL	PARAMETER	RUN 3
	CALCULATED DATA	
(Vmstd)	Standard Meter Volume, cu.ft	22.219
(Ps)	Stack Pressure, inches Hg	29.70
(%Bws)	Moisture, %	6.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.1
(Vs)	Velocity, ft/s	87.9
(As)	Stack Area, sq.ft	7.67
(Qa)	Volumetric flow, acfm	40,466
(Qstd)	Volumetric flow, dscfm	33,659
(I)	Isokinetic Rate, %	90.3
(Qs)	Cyclone flowrate (actual), cfm	0.459
(Qs)	Cyclone flowrate (target), cfm	0.483
(D50)	Particle Diam. with 50% penetration, um	10.36
	<PM10	
(Cs)	Particulate Concentration, grains/dscf	0.0069
(ER)	Particulate Emission Rate, lb/hr	2.0

TABLE 2.1.6-4

TABLE 2.1.6-5
DRYER STACK #8
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/11/92 1015-1128	RUN 2 3/11/92 1303-1419	RUN 3 3/11/92 1519-1626	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	0.96	1.00	1.01	0.99
(Bp)	Barometric Pressure, inches Hg	29.79	29.79	29.79	29.79
(Vm)	Meter Volume, cu.ft	31.619	32.988	33.736	32.781
(Tm)	Avg Meter Temp, deg F	53.9	58.3	59.6	57.3
(Pg)	Static Pressure, inches H2O	-1.00	-1.00	-1.00	-1.00
(Ts)	Avg Stack Temp, deg F	132.5	128.8	129.5	130.3
(Vlc)	Water Collected, ml	58.2	64.5	51.4	58.0
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.385	1.410	1.418	1.40
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.155	0.149	0.155	0.153
(D)	Stack Diameter, inches	38	38	38	38
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0830	0.0455	0.0700	0.0662
(Mf)	Particulate Collected (filter), g	0.0251	0.0484	0.0307	0.0347
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0049	0.0104	0.0050	0.0068
(Mio)	MeCl Impinger (organic) residue, g	0.0032	0.0043	0.0049	0.0041
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	32.474	33.596	34.272	33.447
(Ps)	Stack Pressure, inches Hg	29.72	29.72	29.72	29.72
(%Bws)	Moisture, %	7.8	8.3	6.6	7.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.0	27.9	28.1	28.0
(Vs)	Velocity, ft/s	83.9	85.3	85.5	84.9
(As)	Stack Area, sq.ft	7.88	7.88	7.88	7.88
(Qa)	Volumetric flow, acfm	39,665	40,295	40,415	40,125
(Qs)	Volumetric flow, dscfm	32,363	32,900	33,568	32,944
(I)	Isokinetic Rate, %	100.5	110.7	102.3	104.5
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0514	0.0431	0.0453	0.0466
(ER)	Particulate Emission Rate, lb/hr	14.2	12.2	13.0	13.1
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0537	0.0479	0.0476	0.0497
(ER)	Particulate Emission Rate, lb/hr	14.9	13.5	13.7	14.0
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0552	0.0499	0.0498	0.0516
(ER)	Particulate Emission Rate, lb/hr	15.3	14.1	14.3	14.6
	Train Fractionation:				
	filterable, %	93	86	91	90
	condensible, %	7	14	9	10

TABLE 2.1.6-6

DRYER STACK #8

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/20/92 1046-1159	RUN 2 3/20/92 1225-1330	RUN 3 3/92 1347-1452	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	0.998	0.998	0.998	0.998
	Avg Delta H, inches H2O	2.75	2.80	2.59	2.72
(Bp)	Barometric Pressure, inches Hg	29.82	29.82	29.82	29.82
(Vm)	Meter Volume, cf	53.569	54.985	53.116	53.890
(Tm)	Avg Meter Temp, deg F	67.8	78.9	77.8	74.8
(Pg)	Static Pressure, inches H2O	1.00	1.00	1.00	1.00
(Ts)	Avg Stack Temp, deg F	136.3	137.3	134.8	136.1
(Vlc)	Water Collected, ml	119.7	142.4	139.5	133.9
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	1.420	1.420	1.371	1.40
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.196	0.196	0.196	0.196
(Ds)	Stack Diameter, inches	38	38	38	38
(Mf)	Total Formaldehyde, mg	24	22	37	28
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	53.644	53.932	52.185	53.254
(Ps)	Stack Pressure, inches Hg	29.89	29.89	29.89	29.89
(%Bws)	Moisture (from impingers), %	9.5	11.1	11.2	10.6
(%Bws)	Moisture (at saturation), %	17.7	18.2	16.8	17.6
(Ms)	Molecular Weight-wet, lb/lb-mole	27.8	27.6	27.6	27.7
(Vs)	Velocity, ft/s	86.4	86.7	83.6	85.5
(As)	Stack Area, sq ft	7.67	7.67	7.67	7.67
(Qa)	Volumetric flow, acfm	3.97E+04	3.99E+04	3.85E+04	3.94E+04
(Qs)	Volumetric flow, dscfm	3.18E+04	3.13E+04	3.03E+04	3.11E+04
(I)	Isokinetic Rate, %	102.9	105.0	105.2	104.4
(Cf)	Formaldehyde Concentration, mg/dscf	0.45	0.41	0.71	0.52
(Cppm)	Formaldehyde Concentration, ppm	12.7	11.5	20.0	14.7
(ER)	Formaldehyde Emission Rate, lb/hr	1.88	1.69	2.84	2.14

TABLE 2.1.6-7
DRYER STACK #7
VOLUMETRIC FLOW ONLY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/11/92 1015
	MEASURED DATA	
(Bp)	Barometric Pressure, inches Hg	29.78
(Pg)	Static Pressure, inches H2O	-1.00
(Ts)	Avg Stack Temp, deg F	131
(CO2)	Carbon dioxide, %	0.0
(O2)	Oxygen, %	20.9
	Avg Sqrt Delta P, sqrt(inches H2O	1.28
(D)	Stack Diameter, inches	39.5
	CALCULATED DATA	
(Ps)	Stack Pressure, inches Hg	29.71
(%Bws)	Moisture (from Dryer 8), %	7.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.0
(Vs)	Velocity, ft/s	77.3
(As)	Stack Area, sq.ft	8.51
(Qa)	Volumetric flow, acfm	39,492
(Qs)	Volumetric flow, dscfm	32,338

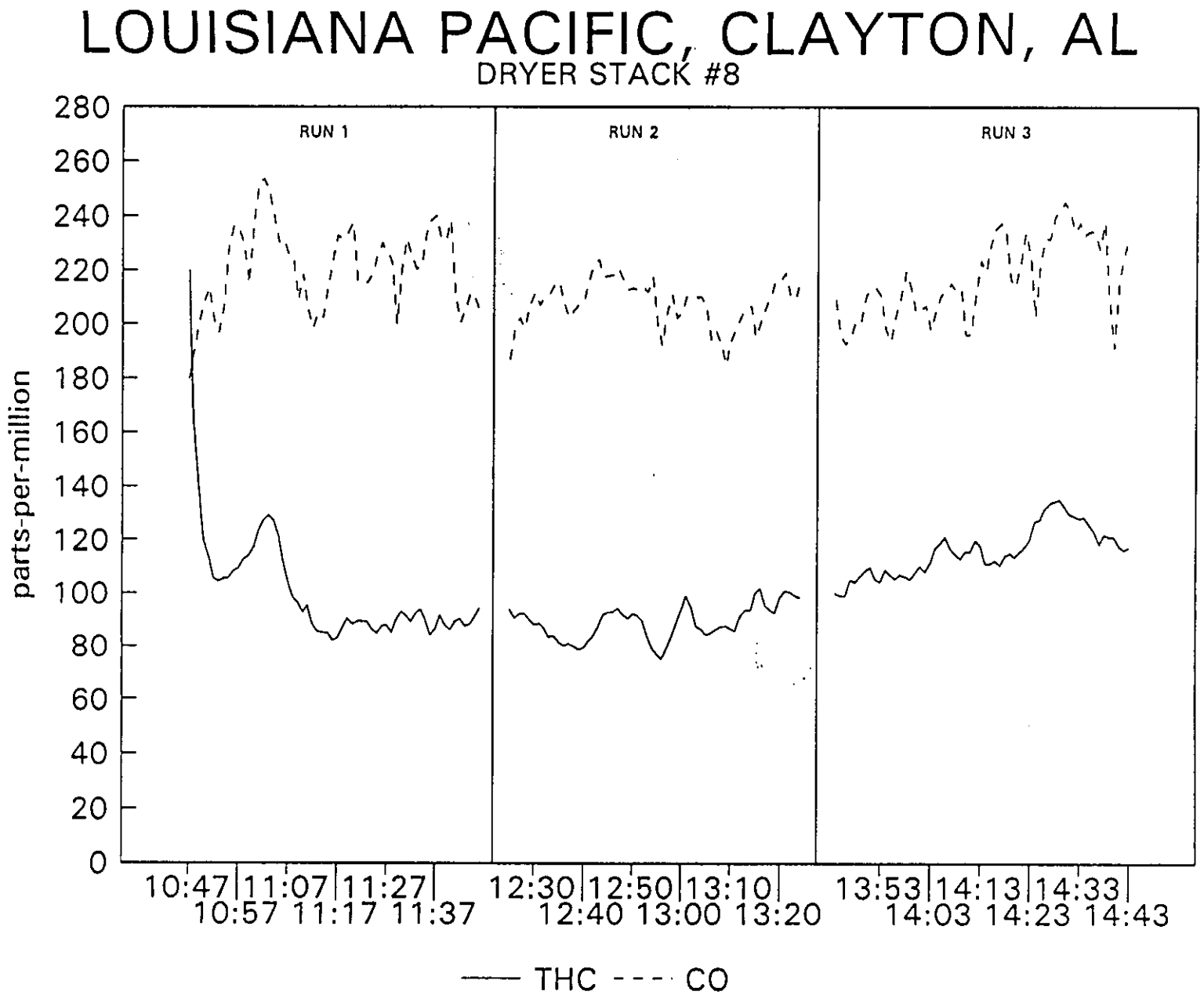
LOUISIANA PACIFIC, CLAYTON, AL
DRYER STACK #8
RUN 1
RUN 2
RUN 3
parts-per-million
280
260
240
220
200
180
160
140
120
100
80
60
40
20
0
10:47 11:07 11:27
10:57 11:17 11:37
12:30 12:50 13:10
12:40 13:00 13:20
13:53 14:13 14:33
14:03 14:23 14:43
THC
CO

FIGURE 2.1.6-1

2.2 PRESS VENTS

A total of nine (9) press vents were tested for particulate matter, condensible particulate matter, formaldehyde, carbon monoxide and total hydrocarbons. No PM_{10} testing was performed on the press vents. Three runs for each parameter were conducted on each press vent for the duration of one hour per run. Sections 2.2.1 - 2.2.9 summarize the individual runs/parameters for these sources. Table 2.2-1 provides a comparison of each average emission measured from the press vents. Table 2.2-2 presents a summary of the CEMS (CO and VOC) parameters. Figure 2.2-1 provides a diagram detailing the sample locations and identification numbers.

The press vents were tested utilizing a manufactured stack extension which was fitted over the existing vent. The gravity activated dampers were removed prior to installing the stack extension. Since each press vent consisted of an axial exhaust fan, the stack extension was manufactured with egg crate straightening vanes in order to reduce the existence of cyclonic flow patterns. Due to the difficult access, the stack extensions did not meet all of the EPA Method 1 criteria. Preliminary velocity determinations proved the existence of acceptable flow characteristics for isokinetic sampling. The US EPA gave official approval prior to the use of the stack extensions for testing the press vents.

2.2.1 Press Vent 3

Table 2.2.1-1 presents a summary of the emissions from Press Vent 3. Tables 2.2.1-2 through 2.2.1-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.002 gr/dscf resulting in 0.8 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.004 gr/dscf resulting in 1.5 lbs/hr.

Formaldehyde - concentration averaged 3.9 ppm resulting in 1.0 lbs/hr.

Carbon monoxide - concentrations averaged 3.3 ppm resulting in 0.8 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 2.0 ppm resulting in 0.8 lbs/hr (as propane).

2.2.2 Press Vent 4

Table 2.2.2-1 presents a summary of the emissions from Press Vent 4. Tables 2.2.2-2 through 2.2.2-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.002 gr/dscf resulting in 1.0 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.004 gr/dscf resulting in 1.7 lbs/hr.

Formaldehyde - concentration averaged 8.4 ppm resulting in 2.1 lbs/hr.

Carbon monoxide - concentrations averaged 3.9 ppm resulting in 0.9 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 2.3 ppm resulting in 0.9 lbs/hr (as propane).

2.2.3 Press Vent 5

Table 2.2.3-1 presents a summary of the emissions from Press Vent 5. Tables 2.2.3-2 through 2.2.3-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.002 gr/dscf resulting in 0.9 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.005 gr/dscf resulting in 2.2 lbs/hr.

Formaldehyde - concentration averaged 24.5 ppm resulting in 6.4 lbs/hr.

Carbon monoxide - concentrations averaged 3.0 ppm resulting in 0.7 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 10.0 ppm resulting in 3.8 lbs/hr (as propane).

2.2.4 Press Vent 6

Table 2.2.4-1 presents a summary of the emissions from Press Vent 6. Tables 2.2.4-2 through 2.2.4-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.002 gr/dscf resulting in 0.6 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.004 gr/dscf resulting in 1.2 lbs/hr.

Formaldehyde - concentration averaged 19.3 ppm resulting in 3.4 lbs/hr.

Carbon monoxide - concentrations averaged 1.1 ppm resulting in 0.2 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 6.8 ppm resulting in 1.7 lbs/hr (as propane).

2.2.5 Press Vent 7

Table 2.2.5-1 presents a summary of the emissions from Press Vent 7. Tables 2.2.5-2 through 2.2.5-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.003 gr/dscf resulting in 0.9 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.006 gr/dscf resulting in 1.6 lbs/hr.

Formaldehyde - concentration averaged 19.4 ppm resulting in 3.2 lbs/hr.

Carbon monoxide - concentrations averaged 2.6 ppm resulting in 0.4 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 5.3 ppm resulting in 1.3 lbs/hr (as propane).

2.2.6 Press Vent 8

Table 2.2.6-1 presents a summary of the emissions from Press Vent 8. Tables 2.2.6-2 through 2.2.6-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.003 gr/dscf resulting in 0.8 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.006 gr/dscf resulting in 2.0 lbs/hr.

Formaldehyde - concentration averaged 12.3 ppm resulting in 2.5 lbs/hr.

Carbon monoxide - concentrations averaged 2.1 ppm resulting in 0.4 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 4.3 ppm resulting in 1.3 lbs/hr (as propane).

2.2.7 Press Vent 9

Table 2.2.7-1 presents a summary of the emissions from Press Vent 9. Tables 2.2.7-2 through 2.2.7-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.001 gr/dscf resulting in 0.4 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.002 gr/dscf resulting in 0.5 lbs/hr.

Formaldehyde - concentration averaged 12.7 ppm resulting in 1.9 lbs/hr.

Carbon monoxide - concentrations averaged 3.9 ppm resulting in 0.6 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 2.9 ppm resulting in 0.7 lbs/hr (as propane).

2.2.8 Press Vent 10

Table 2.2.8-1 presents a summary of the emissions from Press Vent 10. Tables 2.2.8-2 through 2.2.8-3 summarize the testing on this vent.

Particulate Matter - concentration averaged 0.003 gr/dscf resulting in 0.8 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.004 gr/dscf resulting in 1.2 lbs/hr.

Formaldehyde - concentration averaged 9.6 ppm resulting in 1.7 lbs/hr.

Carbon monoxide - concentrations averaged 1.1 ppm resulting in 0.2 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 7.0 ppm resulting in 1.8 lbs/hr (as propane).

2.2.9 Press Vent 11

Table 2.2.9-1 presents a summary of the emissions from Press Vent 11. Table 2.2.9-2 summarizes the formaldehyde testing on this vent. No particulate testing was performed on Press Vent 11.

Formaldehyde - concentration averaged 49.8 ppm resulting in 4.5 lbs/hr.

Carbon monoxide - concentrations averaged 0.5 ppm resulting in 0.0 lbs/hr.

Total hydrocarbons (VOC) - concentrations averaged 10.5 ppm resulting in 1.4 lbs/hr (as propane)

TABLE 2.2-1
SUMMARY OF EMISSIONS
PRESS VENTS 3-11
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	VENT #3	VENT #4	VENT #5	VENT #6	VENT #7	VENT #8	VENT #9	VENT #10	VENT #11	AVERAGE
Particulate										
Concentration, gr/dscf	0.002	0.002	0.002	0.002	0.003	0.003	0.001	0.003	NOT	0.002
Emission Rate, lb/hr	0.8	1.0	0.9	0.6	0.9	0.8	0.4	0.8	TESTED	0.8
Particulate (Including condensibles)										
Concentration, gr/dscf	0.004	0.004	0.005	0.004	0.006	0.006	0.002	0.004	NOT	0.004
Emission Rate, lb/hr	1.5	1.7	2.2	1.2	1.6	2.0	0.5	1.2	TESTED	1.5
Formaldehyde										
Concentration, ppm	3.9	8.4	24.5	19.3	19.4	12.3	12.7	9.6	49.8	17.8
Emission Rate, lb/hr	1.0	2.1	6.4	3.4	3.2	2.5	1.9	1.7	4.5	3.0
Carbon Monoxide										
Concentration, ppm	3.3	3.9	3.0	1.1	2.6	2.1	3.9	1.1	0.5	2.4
Emission Rate, lb/hr	0.8	0.9	0.7	0.2	0.4	0.4	0.6	0.2	0.0	0.5
Total Hydrocarbons (VOC), as propane										
Concentration, ppm	2.0	2.3	10.0	6.8	5.3	4.3	2.9	7.0	10.5	5.7
Emission Rate, lb/hr	0.8	0.9	3.8	1.7	1.3	1.3	0.7	1.8	1.4	1.5

TABLE 2.2-2
PRESS VENTS 3-11
CEMS SUMMARY
LOUISIANA PACIFIC CORPORATION

			CEM Data (Corrected)		Volumetric Flow				Mass Emission Rates	
Run No.	Start Time	Stop Time	CO (ppm)	THC (ppm)	Qa (acfm)	Qs (dscfm)	Moisture (%)	Qsc (scfm)	CO (lb/hr)	THC (lb/hr)
Vent 3 1	1329	1429	2.4	2.2	60,000	57,600	0.2	57,700	0.6	0.9
2	1502	1602	3.4	2.1	59,100	54,900	3.7	57,000	0.8	0.8
3	1628	1728	4.2	1.7	57,300	55,100	0.5	55,300	1.0	0.6
Vent 4 1	1800	1900	3.7	1.5	58,300	57,200	0.5	57,400	0.9	0.6
2	0750	0850	5.0	2.8	55,000	53,900	0.2	54,000	1.2	1.1
3	0920	1020	2.9	2.5	57,800	54,700	2.7	56,200	0.7	1.0
Vent 5 1	0957	1056	3.8	10.1	54,500	53,500	0.9	53,900	0.9	3.7
2	1210	1310	2.4	10.7	57,800	56,400	0.6	56,700	0.6	4.2
3	1345	1445	2.9	9.1	59,000	57,500	0.4	57,700	0.7	3.6
Vent 6 1	1155	1255	1.4	9.0	40,500	39,200	0.7	39,400	0.2	2.4
2	1516	1615	1.1	6.2	37,600	36,000	1.3	36,400	0.2	1.5
3	1648	1748	0.7	5.2	38,000	36,600	1.2	37,000	0.1	1.3
Vent 7 1	0757	0857	2.5	3.9	35,400	35,900	0.5	36,000	0.4	1.0
2	0932	1032	2.7	5.2	35,300	35,100	1.0	35,400	0.4	1.3
3	1100	1200	2.5	6.8	35,100	34,700	0.5	34,800	0.4	1.6
Vent 8 1	1453	1553	1.7	4.2	45,900	45,300	0.0	45,300	0.3	1.3
2	1642	1742	1.9	4.6	47,000	46,900	0.2	46,900	0.4	1.5
3	1812	1912	2.7	4.0	40,500	40,900	0.3	41,000	0.5	1.1
Vent 9 1	0854	0954	2.4	4.0	33,000	33,000	0.4	33,100	0.3	0.9
2	1028	1128	4.7	2.1	33,200	32,600	0.9	32,800	0.7	0.5
3	1158	1258	4.7	2.5	33,700	31,800	3.4	32,900	0.7	0.6
Vent 10 1	1155	1255	1.5	9.2	39,900	38,100	1.0	38,400	0.2	2.4
2	1516	1615	1.2	6.4	39,000	36,200	4.3	37,800	0.2	1.7
3	1648	1748	0.7	5.4	37,400	36,200	0.7	36,400	0.1	1.3
Vent 11 1	1022	1122	0.8	11.6	20,300	20,000	1.5	20,300	0.1	1.6
2	1241	1341	0.6	11.0	19,300	19,100	0.4	19,100	0.0	1.4
3	1440	1540	0.0	8.9	18,300	18,200	0.4	18,200	0.0	1.1

PRESS VENT IDENTIFICATION DIAGRAM
LOUISIANA PACIFIC - CLAYTON, ALABAMA

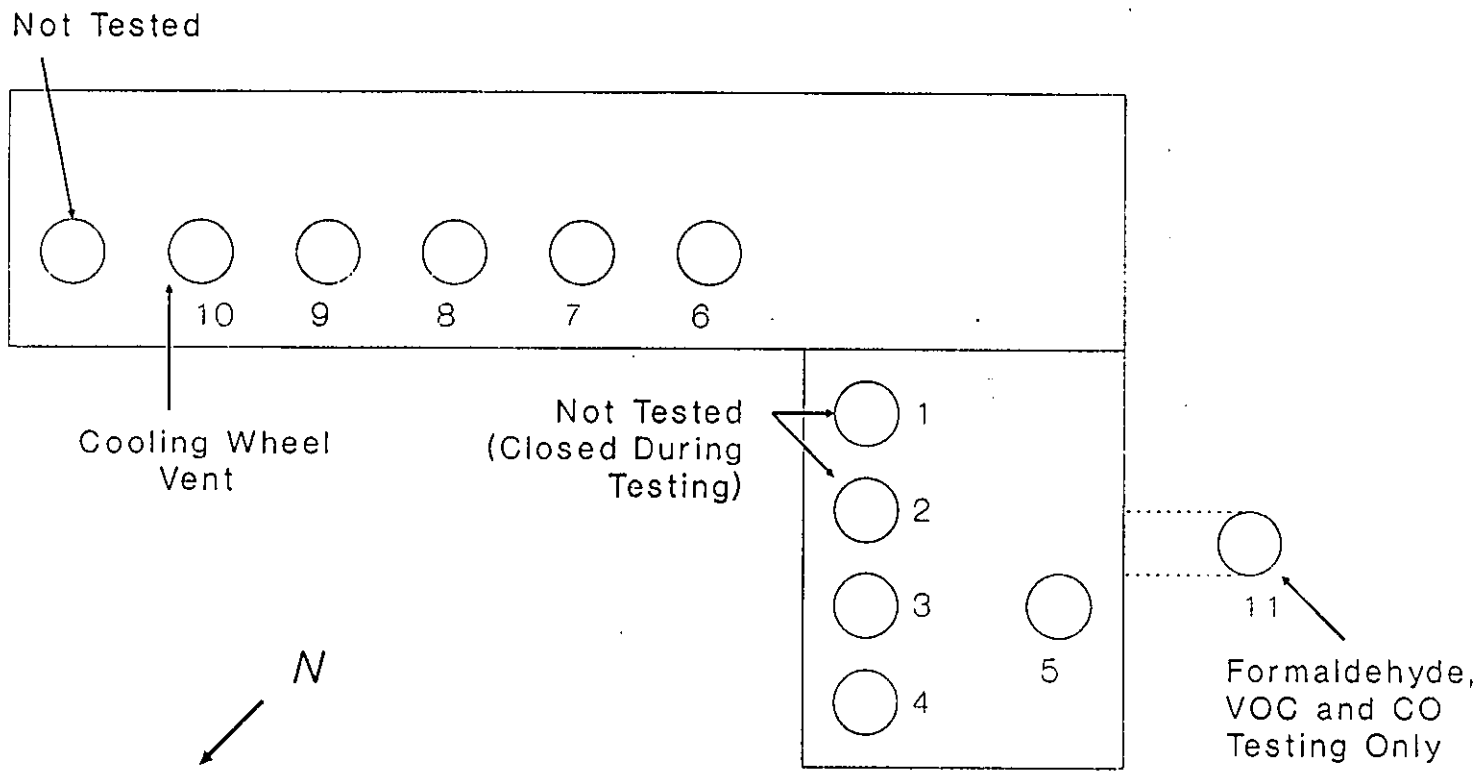

FIGURE 2.2-1

TABLE 2.2.1-1
SUMMARY OF EMISSIONS
PRESS VENT #3
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.001	0.002	0.002	0.002
Emission Rate, lb/hr	0.3	0.9	1.1	0.8
Particulate (Including condensibles)				
Concentration, gr/dscf	0.003	0.004	0.004	0.004
Emission Rate, lb/hr	1.1	1.5	1.9	1.5
Formaldehyde				
Concentration, ppm	5.6	3.7	2.3	3.9
Emission Rate, lb/hr	1.5	1.0	0.6	1.0
Carbon Monoxide				
Concentration, ppm	2.4	3.4	4.2	3.3
Emission Rate, lb/hr	0.6	0.8	1.0	0.8
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	2.2	2.1	1.7	2.0
Emission Rate, lb/hr	0.9	0.8	0.6	0.8

TABLE 2.2.1-2
PRESS VENT #3
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/18/92 0944-1106	RUN 2 3/18/92 1304-1445	RUN 3 3/18/92 1601-1704	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	2.08	1.84	2.06	1.99
(Bp)	Barometric Pressure, inches Hg	29.94	29.94	29.94	29.94
(Vm)	Meter Volume, cu.ft	46.123	43.748	45.981	45.284
(Tm)	Avg Meter Temp, deg F	67.1	67.1	67.1	67.1
(Pg)	Static Pressure, inches H2O	-0.30	-0.30	-0.30	-0.30
(Ts)	Avg Stack Temp, deg F	92.3	93.4	92.1	92.6
(Vlc)	Water Collected, ml	7.6	17.1	16.1	13.6
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.752	0.715	0.758	0.74
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.241	0.241	0.241	0.241
(D)	Stack Diameter, inches	62	62	62	62
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0021	0.0044	0.0059	0.0041
(Mf)	Particulate Collected (filter), g	0.0000	0.0018	0.0014	0.0011
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0023	0.0020	0.0040	0.0028
(Mio)	MeCl Impinger (organic) residue, g	0.0033	0.0025	0.0016	0.0025
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	46.915	44.473	46.768	46.052
(Ps)	Stack Pressure, inches Hg	29.92	29.92	29.92	29.92
(%Bws)	Moisture, %	0.8	1.8	1.6	1.4
(Ms)	Molecular Weight-wet, lb/lb-mole	28.8	28.6	28.7	28.7
(Vs)	Velocity, ft/s	43.3	41.3	43.7	42.7
(As)	Stack Area, sq.ft	20.97	20.97	20.97	20.97
(Qa)	Volumetric flow, acfm	54,431	51,904	54,942	53,759
(Qs)	Volumetric flow, dscfm	51,618	48,619	51,682	50,640
(I)	Isokinetic Rate, %	100.3	100.9	99.8	100.3
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0007	0.0022	0.0024	0.0018
(ER)	Particulate Emission Rate, lb/hr	0.3	0.9	1.1	0.8
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0014	0.0028	0.0037	0.0027
(ER)	Particulate Emission Rate, lb/hr	0.6	1.2	1.7	1.2
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0025	0.0037	0.0043	0.0035
(ER)	Particulate Emission Rate, lb/hr	1.1	1.5	1.9	1.5
	Train Fractionation:				
	filterable, %	27	58	57	47
	condensible, %	73	42	43	53

TABLE 2.2.1-3

PRESS VENT #3

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/12/92 1329-1432	RUN 2 3/12/92 1502-1605	RUN 3 3/12/92 1628-1731	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	2.47	2.40	2.33	2.40
(Bp)	Barometric Pressure, inches Hg	29.98	29.98	29.98	29.98
(Vm)	Meter Volume, cf	48.051	47.685	47.037	47.591
(Tm)	Avg Meter Temp, deg F	70.8	67.3	64.5	67.5
(Pg)	Static Pressure, inches H2O	-0.35	-0.35	-0.35	-0.35
(Ts)	Avg Stack Temp, deg F	90.0	87.4	86.8	88.1
(Vlc)	Water Collected, ml	2.0	39.8	5.0	15.6
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.832	0.816	0.797	0.82
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	62	62	62	62
(Mf)	Total Formaldehyde, mg	10	6	4	7
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	48.646	48.587	48.175	48.469
(Ps)	Stack Pressure, inches Hg	29.95	29.95	29.95	29.95
(%Bws)	Moisture (from impingers), %	0.2	3.7	0.5	1.5
(%Bws)	Moisture (at saturation), %	4.7	4.3	4.2	4.4
(Ms)	Molecular Weight-wet, lb/lb-mole	28.8	28.4	28.8	28.7
(Vs)	Velocity, ft/s	47.7	47.0	45.6	46.8
(As)	Stack Area, sq ft	20.97	20.97	20.97	20.97
(Qa)	Volumetric flow, acfm	6.00E+04	5.91E+04	5.73E+04	5.88E+04
(Qs)	Volumetric flow, dscfm	5.76E+04	5.49E+04	5.51E+04	5.59E+04
(I)	Isokinetic Rate, %	97.2	101.8	100.6	99.9
(Cf)	Formaldehyde Concentration, mg/dscf	0.20	0.13	0.08	0.14
(Cppm)	Formaldehyde Concentration, ppm	5.6	3.7	2.3	3.9
(ER)	Formaldehyde Emission Rate, lb/hr	1.50	0.96	0.61	1.02

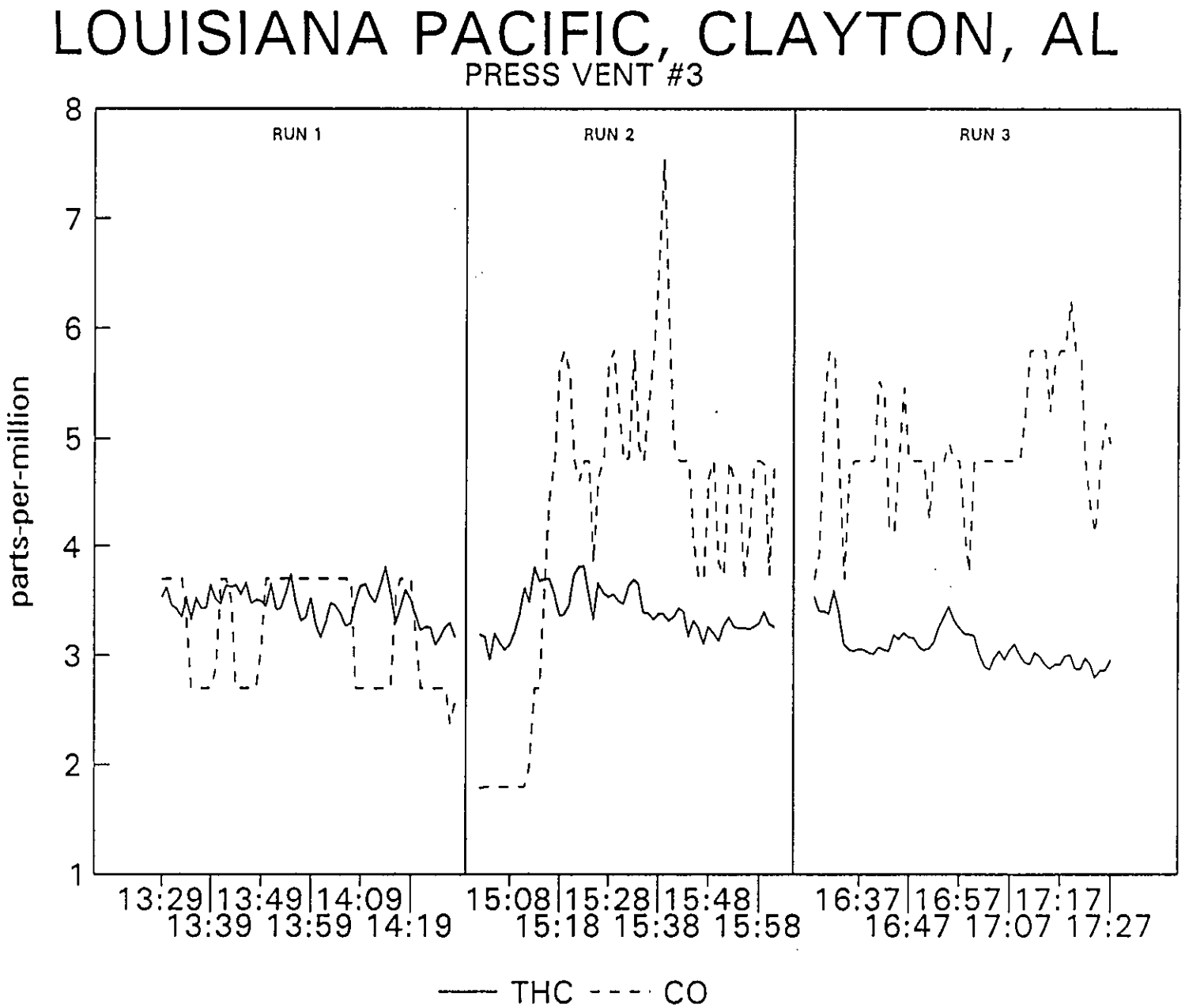
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #3
RUN 1
RUN 2
RUN 3
parts-per-million
8
7
6
5
4
3
2
1
13:29 13:39 13:49 13:59 14:09 14:19
15:08 15:18 15:28 15:38 15:48 15:58
16:37 16:47 16:57 17:07 17:17 17:27
THC
CO

FIGURE 2.2.1-1

TABLE 2.2.2-1
SUMMARY OF EMISSIONS
PRESS VENT #4
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.005	0.001	0.001	0.002
Emission Rate, lb/hr	1.9	0.6	0.5	1.0
Particulate (Including condensibles)				
Concentration, gr/dscf	0.006	0.003	0.003	0.004
Emission Rate, lb/hr	2.5	1.2	1.3	1.7
Formaldehyde				
Concentration, ppm	5.4	10.3	9.4	8.4
Emission Rate, lb/hr	1.4	2.6	2.4	2.1
Carbon Monoxide				
Concentration, ppm	3.7	5.0	2.9	3.9
Emission Rate, lb/hr	0.9	1.2	0.7	0.9
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	1.5	2.8	2.5	2.3
Emission Rate, lb/hr	0.6	1.1	1.0	0.9

TABLE 2.2.2-2
PRESS VENT #4
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/17/92 1339-1440	RUN 2 3/17/92 1510-1612	RUN 3 3/17/92 1652-1754	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.005	1.005	1.005	1.005
	Avg Delta H, inches H2O	1.85	1.98	1.94	1.92
(Bp)	Barometric Pressure, inches Hg	30.02	30.02	30.02	30.02
(Vm)	Meter Volume, cu.ft	43.377	46.401	44.038	44.605
(Tm)	Avg Meter Temp, deg F	86.8	84.7	79.6	83.7
(Pg)	Static Pressure, inches H2O	-0.35	-0.35	-0.35	-0.35
(Ts)	Avg Stack Temp, deg F	101.5	100.6	98.0	100.0
(Vlc)	Water Collected, ml	9.5	8.4	6.8	8.2
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.714	0.738	0.731	0.73
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.241	0.241	0.241	0.241
(D)	Stack Diameter, inches	62	62	62	62
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0094	0.0021	0.0021	0.0045
(Mf)	Particulate Collected (filter), g	0.0030	0.0020	0.0013	0.0021
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0025	0.0021	0.0023	0.0023
(Mio)	MeCl Impinger (organic) residue, g	0.0017	0.0020	0.0029	0.0022
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	42.410	45.556	43.641	43.869
(Ps)	Stack Pressure, inches Hg	29.99	29.99	29.99	29.99
(%Bws)	Moisture, %	1.0	0.9	0.7	0.9
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.7	28.8	28.7
(Vs)	Velocity, ft/s	41.4	42.7	42.2	42.1
(As)	Stack Area, sq.ft	20.97	20.97	20.97	20.97
(Qa)	Volumetric flow, acfm	52,071	53,760	53,113	52,981
(Qs)	Volumetric flow, dscfm	48,554	50,302	49,995	49,617
(I)	Isokinetic Rate, %	96.4	99.9	96.3	97.5
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0045	0.0014	0.0012	0.0024
(ER)	Particulate Emission Rate, lb/hr	1.9	0.6	0.5	1.0
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0054	0.0021	0.0020	0.0032
(ER)	Particulate Emission Rate, lb/hr	2.3	0.9	0.9	1.3
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0060	0.0028	0.0030	0.0040
(ER)	Particulate Emission Rate, lb/hr	2.5	1.2	1.3	1.7
	Train Fractionation:				
	filterable, %	75	50	40	55
	condensible, %	25	50	60	45

TABLE 2.2.2-3

PRESS VENT #4

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/11/92 1800-1904	RUN 2 3/12/92 0750-0853	RUN 3 3/12/92 0920-1024	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	2.40	2.10	2.40	2.30
(Bp)	Barometric Pressure, inches Hg	29.98	29.98	29.98	29.98
(Vm)	Meter Volume, cf	46.354	45.060	47.225	46.213
(Tm)	Avg Meter Temp, deg F	46.0	56.0	69.0	57.0
(Pg)	Static Pressure, inches H2O	-0.33	-0.33	-0.33	-0.33
(Ts)	Avg Stack Temp, deg F	76.0	79.0	83.0	79.3
(Vlc)	Water Collected, ml	5.3	1.7	28.1	11.7
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.819	0.771	0.802	0.80
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	62	62	62	62
(Mf)	Total Formaldehyde, mg	9	17	16	14
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	49.219	46.884	47.964	48.023
(Ps)	Stack Pressure, inches Hg	29.96	29.96	29.96	29.96
(%Bws)	Moisture (from impingers), %	0.5	0.2	2.7	1.1
(%Bws)	Moisture (at saturation), %	3.0	3.3	3.8	3.4
(Ms)	Molecular Weight-wet, lb/lb-mole	28.8	28.8	28.5	28.7
(Vs)	Velocity, ft/s	46.3	43.7	45.9	45.3
(As)	Stack Area, sq ft	20.97	20.97	20.97	20.97
(Qa)	Volumetric flow, acfm	5.83E+04	5.50E+04	5.78E+04	5.70E+04
(Qs)	Volumetric flow, dscfm	5.72E+04	5.39E+04	5.47E+04	5.52E+04
(I)	Isokinetic Rate, %	99.0	100.2	100.9	100.0
(Cf)	Formaldehyde Concentration, mg/dscf	0.19	0.36	0.33	0.30
(Cppm)	Formaldehyde Concentration, ppm	5.4	10.3	9.4	8.4
(ER)	Formaldehyde Emission Rate, lb/hr	1.44	2.58	2.41	2.15

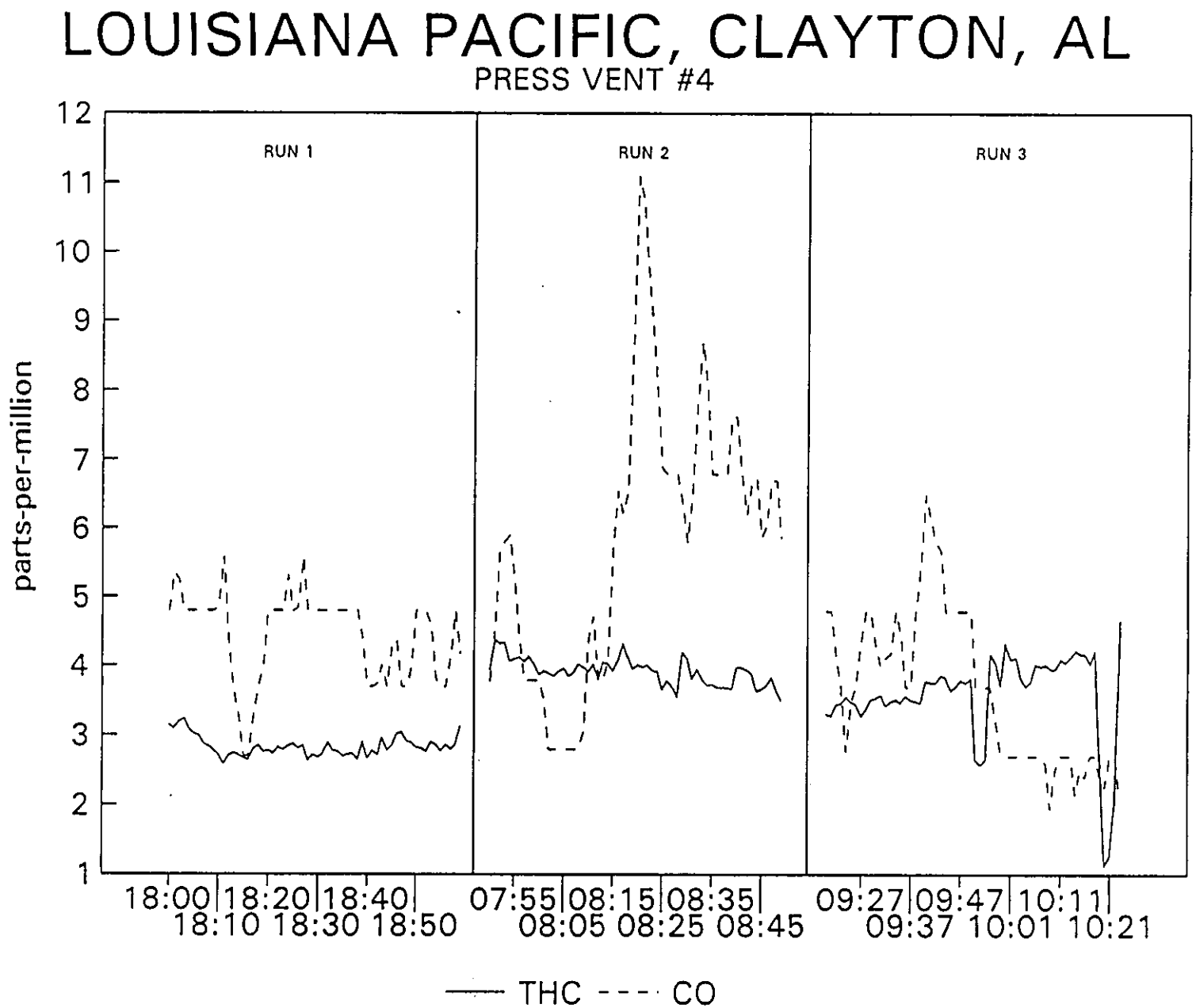
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #4
RUN 1
RUN 2
RUN 3
parts-per-million
12
11
10
9
8
7
6
5
4
3
2
1
18:00 18:20 18:40
18:10 18:30 18:50
07:55 08:15 08:35
08:05 08:25 08:45
09:27 09:47 10:11
09:37 10:01 10:21
THC
CO

FIGURE 2.2.2-1

TABLE 2.2.3-1
SUMMARY OF EMISSIONS
PRESS VENT #5
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.002	0.002	0.003	0.002
Emission Rate, lb/hr	0.7	0.6	1.4	0.9
Particulate (Including condensibles)				
Concentration, gr/dscf	0.004	0.005	0.007	0.005
Emission Rate, lb/hr	1.8	2.0	2.8	2.2
Formaldehyde				
Concentration, ppm	25.4	24.3	23.8	24.5
Emission Rate, lb/hr	6.4	6.4	6.4	6.4
Carbon Monoxide				
Concentration, ppm	3.8	2.4	2.9	3.0
Emission Rate, lb/hr	0.9	0.6	0.7	0.7
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	10.1	10.7	9.1	10.0
Emission Rate, lb/hr	3.7	4.2	3.6	3.8

TABLE 2.2.3-2
PRESS VENT #5
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/19/92 0828-0932	RUN 2 3/19/92 0952-1054	RUN 3 3/19/92 1135-1241	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.005	1.005	1.005	1.005
	Avg Delta H, inches H2O	2.02	2.11	1.88	2.00
(Bp)	Barometric Pressure, inches Hg	29.52	29.52	29.52	29.52
(Vm)	Meter Volume, cu.ft	45.341	46.745	47.364	46.483
(Tm)	Avg Meter Temp, deg F	75.1	82.0	86.8	81.3
(Pg)	Static Pressure, inches H2O	-0.30	-0.30	-0.30	-0.30
(Ts)	Avg Stack Temp, deg F	89.1	93.0	98.1	93.4
(Vlc)	Water Collected, ml	16.6	18.4	12.2	15.7
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.740	0.752	0.717	0.74
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.241	0.241	0.241	0.241
(D)	Stack Diameter, inches	62	62	62	62
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0032	0.0008	0.0046	0.0029
(Mf)	Particulate Collected (filter), g	0.0015	0.0035	0.0055	0.0035
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0020	0.0039	0.0023	0.0027
(Mio)	MeCl Impinger (organic) residue, g	0.0052	0.0054	0.0072	0.0059
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	44.567	45.373	45.544	45.161
(Ps)	Stack Pressure, inches Hg	29.50	29.50	29.50	29.50
(%Bws)	Moisture, %	1.7	1.9	1.2	1.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.6	28.6	28.7	28.7
(Vs)	Velocity, ft/s	42.8	43.7	41.8	42.8
(As)	Stack Area, sq.ft	20.97	20.97	20.97	20.97
(Qa)	Volumetric flow, acfm	53,884	54,968	52,588	53,813
(Qs)	Volumetric flow, dscfm	50,182	50,753	48,420	49,785
(I)	Isokinetic Rate, %	98.0	98.6	103.8	100.1
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0016	0.0015	0.0034	0.0022
(ER)	Particulate Emission Rate, lb/hr	0.7	0.6	1.4	0.9
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0023	0.0028	0.0042	0.0031
(ER)	Particulate Emission Rate, lb/hr	1.0	1.2	1.7	1.3
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0041	0.0046	0.0066	0.0051
(ER)	Particulate Emission Rate, lb/hr	1.8	2.0	2.8	2.2
	Train Fractionation:				
	filterable, %	39	32	52	41
	condensible, %	61	68	48	59

TABLE 2.2.3-3

PRESS VENT #5

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/11/92 0957-1103	RUN 2 3/11/92 1210-1315	RUN 3 3/11/92 1345-1449	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	2.20	2.00	2.50	2.23
(Bp)	Barometric Pressure, inches Hg	29.97	29.97	29.97	29.97
(Vm)	Meter Volume, cf	45.105	43.433	49.117	45.885
(Tm)	Avg Meter Temp, deg F	45.0	68.0	69.0	60.7
(Pg)	Static Pressure, inches H2O	-0.33	-0.33	-0.33	-0.33
(Ts)	Avg Stack Temp, deg F	74.0	78.0	79.0	77.0
(Vlc)	Water Collected, ml	9.0	5.2	4.7	6.3
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.767	0.809	0.826	0.80
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	62	62	62	62
(Mf)	Total Formaldehyde, mg	43	38	42	41
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	47.949	44.139	49.881	47.323
(Ps)	Stack Pressure, inches Hg	29.95	29.95	29.95	29.95
(%Bws)	Moisture (from impingers), %	0.9	0.6	0.4	0.6
(%Bws)	Moisture (at saturation), %	2.8	3.2	3.3	3.1
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.8	28.8	28.8
(Vs)	Velocity, ft/s	43.4	45.9	46.9	45.4
(As)	Stack Area, sq ft	20.97	20.97	20.97	20.97
(Qa)	Volumetric flow, acfm	5.45E+04	5.78E+04	5.90E+04	5.71E+04
(Qs)	Volumetric flow, dscfm	5.35E+04	5.64E+04	5.75E+04	5.58E+04
(I)	Isokinetic Rate, %	103.1	90.0	99.7	97.6
(Cf)	Formaldehyde Concentration, mg/dscf	0.90	0.86	0.84	0.87
(Cppm)	Formaldehyde Concentration, ppm	25.4	24.3	23.8	24.5
(ER)	Formaldehyde Emission Rate, lb/hr	6.35	6.43	6.41	6.39

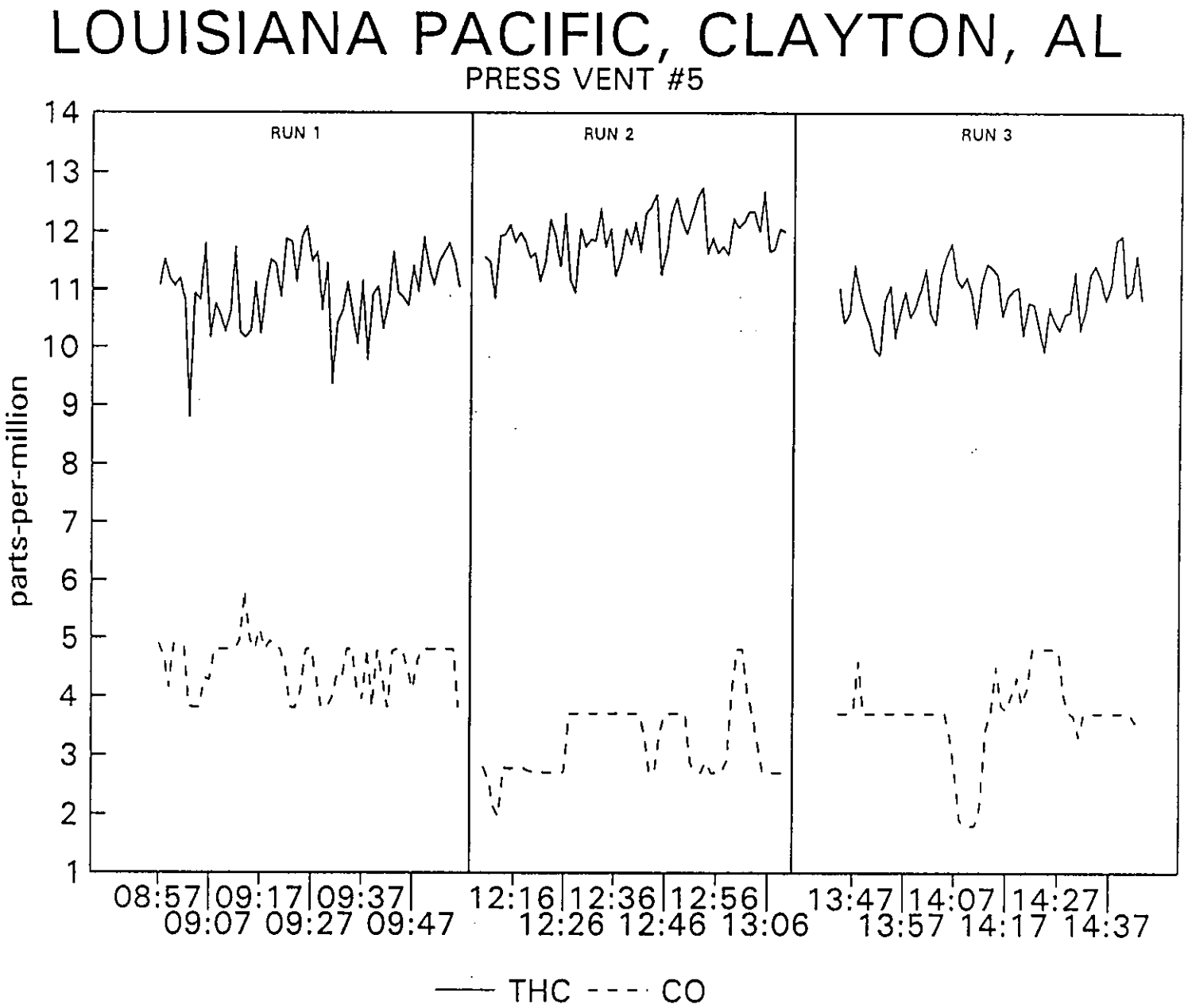
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #5
RUN 1
RUN 2
RUN 3
parts-per-million
14
13
12
11
10
9
8
7
6
5
4
3
2
1
08:57
09:07
09:17
09:27
09:37
09:47
12:16
12:26
12:36
12:46
12:56
13:06
13:47
13:57
14:07
14:17
14:27
14:37
THC
CO

FIGURE 2.2.3-1

TABLE 2.2.4-1
SUMMARY OF EMISSIONS
PRESS VENT #6
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.002	0.002	0.002	0.002
Emission Rate, lb/hr	0.7	0.5	0.6	0.6
Particulate (Including condensibles)				
Concentration, gr/dscf	0.004	0.004	0.004	0.004
Emission Rate, lb/hr	1.4	1.1	1.2	1.2
Formaldehyde				
Concentration, ppm	22.3	22.0	13.7	19.3
Emission Rate, lb/hr	4.1	3.7	2.4	3.4
Carbon Monoxide				
Concentration, ppm	1.4	1.1	0.7	1.1
Emission Rate, lb/hr	0.2	0.2	0.1	0.2
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	9.0	6.2	5.2	6.8
Emission Rate, lb/hr	2.4	1.5	1.3	1.7

TABLE 2.2.4-2
PRESS VENT #6
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/19/92 1218-1324	RUN 2 3/19/92 1414-1500	RUN 3 3/19/92 1600-1706	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	1.76	1.76	1.61	1.71
(Bp)	Barometric Pressure, inches Hg	29.58	29.58	29.58	29.58
(Vm)	Meter Volume, cu.ft	40.305	38.612	38.220	39.046
(Tm)	Avg Meter Temp, deg F	86.8	85.8	83.4	85.3
(Pg)	Static Pressure, inches H2O	0.05	0.05	0.05	0.05
(Ts)	Avg Stack Temp, deg F	90.4	90.8	88.2	89.8
(Vlc)	Water Collected, ml	13.6	9.0	6.9	9.8
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.681	0.627	0.618	0.64
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.235	0.241	0.241	0.239
(D)	Stack Diameter, inches	56	56	56	56
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0047	0.0028	0.0041	0.0039
(Mf)	Particulate Collected (filter), g	0.0006	0.0012	0.0008	0.0009
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0029	0.0024	0.0024	0.0026
(Mio)	MeCl Impinger (organic) residue, g	0.0028	0.0023	0.0026	0.0026
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	39.016	37.446	37.215	37.892
(Ps)	Stack Pressure, inches Hg	29.58	29.58	29.58	29.58
(%Bws)	Moisture, %	1.6	1.1	0.9	1.2
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.7	28.7	28.7
(Vs)	Velocity, ft/s	39.4	36.3	35.6	37.1
(As)	Stack Area, sq.ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	40,436	37,208	36,570	38,071
(Qs)	Volumetric flow, dscfm	37,720	34,858	34,511	35,696
(I)	Isokinetic Rate, %	97.9	96.7	97.1	97.2
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0021	0.0016	0.0020	0.0019
(ER)	Particulate Emission Rate, lb/hr	0.7	0.5	0.6	0.6
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0032	0.0026	0.0030	0.0030
(ER)	Particulate Emission Rate, lb/hr	1.0	0.8	0.9	0.9
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0044	0.0036	0.0041	0.0040
(ER)	Particulate Emission Rate, lb/hr	1.4	1.1	1.2	1.2
	Train Fractionation:				
	filterable, %	48	46	49	48
	condensible, %	52	54	51	52

TABLE 2.2.4-3

PRESS VENT #6

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/14/92 1156-1308	RUN 2 3/14/92 1516-1619	RUN 3 3/14/92 1650-1751	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	2.80	1.60	1.63	2.01
(Bp)	Barometric Pressure, inches Hg	29.84	29.84	29.84	29.84
(Vm)	Meter Volume, cf	51.002	38.949	39.316	43.089
(Tm)	Avg Meter Temp, deg F	78.0	80.0	76.3	78.1
(Pg)	Static Pressure, inches H2O	-0.42	-0.42	-0.42	-0.42
(Ts)	Avg Stack Temp, deg F	80.0	81.0	80.0	80.3
(Vlc)	Water Collected, ml	7.5	10.7	10.1	9.4
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.692	0.641	0.650	0.66
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	56	56	56	56
(Mf)	Total Formaldehyde, mg	40	30	19	30
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	50.747	38.497	39.131	42.792
(Ps)	Stack Pressure, inches Hg	29.81	29.81	29.81	29.81
(%Bws)	Moisture (from impingers), %	0.7	1.3	1.2	1.1
(%Bws)	Moisture (at saturation), %	3.5	3.6	3.5	3.5
(Ms)	Molecular Weight-wet, lb/lb-mole	28.8	28.7	28.7	28.7
(Vs)	Velocity, ft/s	39.5	36.6	37.1	37.7
(As)	Stack Area, sq ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	4.05E+04	3.76E+04	3.80E+04	3.87E+04
(Qs)	Volumetric flow, dscfm	3.92E+04	3.60E+04	3.66E+04	3.73E+04
(I)	Isokinetic Rate, %	121.6	100.3	100.4	107.4
(Cf)	Formaldehyde Concentration, mg/dscf	0.79	0.78	0.49	0.68
(Cppm)	Formaldehyde Concentration, ppm	22.3	22.0	13.7	19.4
(ER)	Formaldehyde Emission Rate, lb/hr	4.08	3.71	2.35	3.38

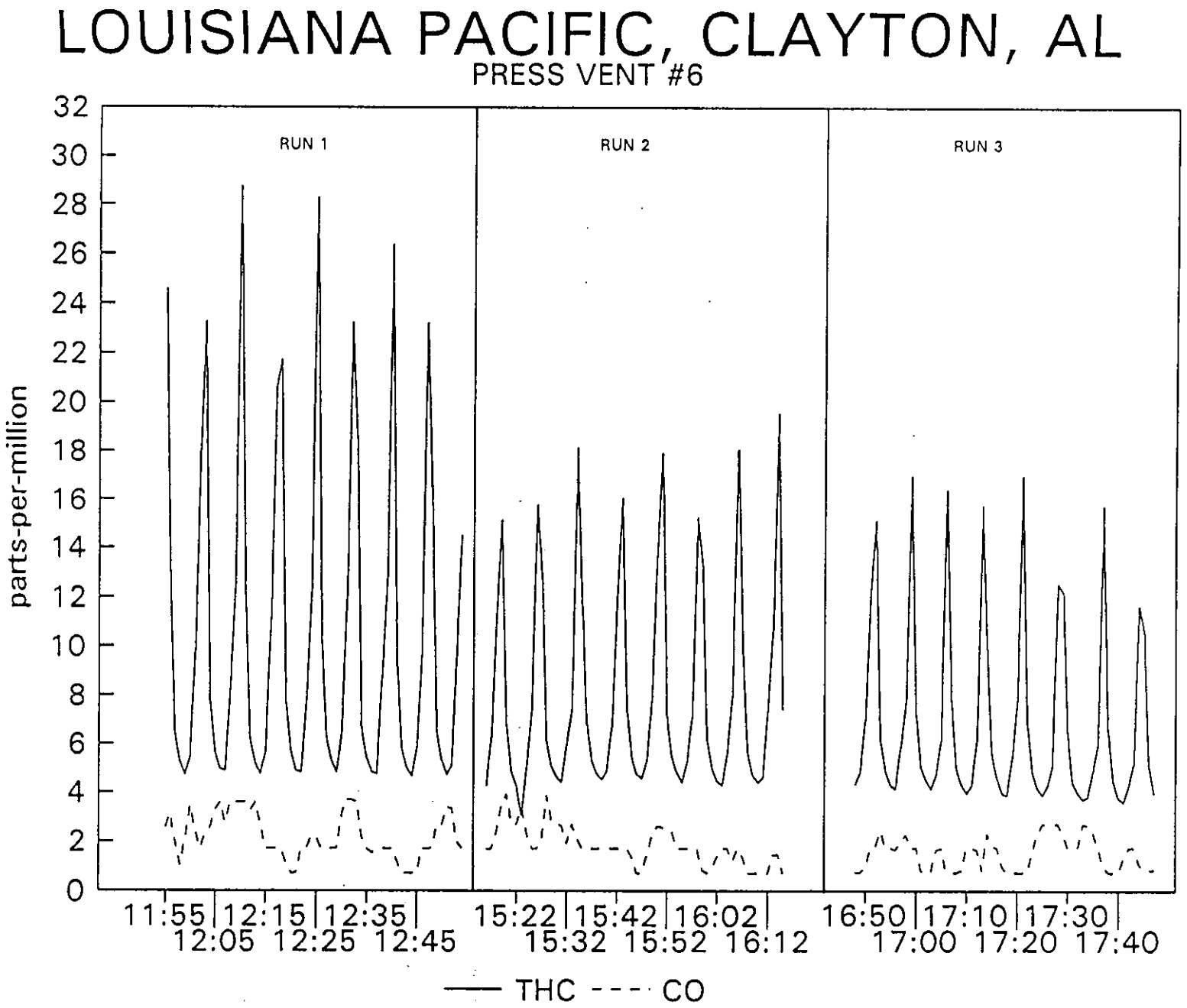
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #6
RUN 1
RUN 2
RUN 3
parts-per-million
32
30
28
26
24
22
20
18
16
14
12
10
8
6
4
2
0
11:55
12:05
12:15
12:25
12:35
12:45
15:22
15:32
15:42
15:52
16:02
16:12
16:50
17:00
17:10
17:20
17:30
17:40
THC
CO

FIGURE 2.2.4-1

TABLE 2.2.5-1
SUMMARY OF EMISSIONS
PRESS VENT #7
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.002	0.004	0.004	0.003
Emission Rate, lb/hr	0.6	1.0	1.0	0.9
Particulate (Including condensibles)				
Concentration, gr/dscf	0.005	0.006	0.007	0.006
Emission Rate, lb/hr	1.4	1.6	1.8	1.6
Formaldehyde				
Concentration, ppm	15.2	19.6	23.4	19.4
Emission Rate, lb/hr	2.5	3.2	3.8	3.2
Carbon Monoxide				
Concentration, ppm	2.5	2.7	2.5	2.6
Emission Rate, lb/hr	0.4	0.4	0.4	0.4
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	3.9	5.2	6.8	5.3
Emission Rate, lb/hr	1.0	1.3	1.6	1.3

TABLE 2.2.5-2
PRESS VENT #7
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/19/92 1205-1214	RUN 2 3/19/92 1345-1550	RUN 3 3/19/92 1523-1629	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.46	1.27	1.40	1.38
(Bp)	Barometric Pressure, inches Hg	29.58	29.58	29.58	29.58
(Vm)	Meter Volume, cu.ft	38.498	36.560	38.294	37.784
(Tm)	Avg Meter Temp, deg F	85.7	86.6	88.3	86.9
(Pg)	Static Pressure, inches H2O	-0.15	-0.15	-0.15	-0.15
(Ts)	Avg Stack Temp, deg F	93.2	92.6	91.3	92.4
(Vlc)	Water Collected, ml	11.8	13.0	11.7	12.2
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.591	0.548	0.587	0.58
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.242	0.242	0.242	0.242
(D)	Stack Diameter, inches	56	56	56	56
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0037	0.0074	0.0057	0.0056
(Mf)	Particulate Collected (filter), g	0.0012	0.0012	0.0031	0.0018
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0038	0.0018	0.0028	0.0028
(Mio)	MeCl Impinger (organic) residue, g	0.0034	0.0033	0.0038	0.0035
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	37.019	35.081	36.643	36.247
(Ps)	Stack Pressure, inches Hg	29.57	29.57	29.57	29.57
(%Bws)	Moisture, %	1.5	1.7	1.5	1.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.7	28.7	28.7
(Vs)	Velocity, ft/s	34.3	31.8	34.0	33.4
(As)	Stack Area, sq.ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	35,180	32,618	34,882	34,227
(Qs)	Volumetric flow, dscfm	32,680	30,260	32,514	31,818
(I)	Isokinetic Rate, %	101.1	103.5	100.6	101.7
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0020	0.0038	0.0037	0.0032
(ER)	Particulate Emission Rate, lb/hr	0.6	1.0	1.0	0.9
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0036	0.0046	0.0049	0.0044
(ER)	Particulate Emission Rate, lb/hr	1.0	1.2	1.4	1.2
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0050	0.0060	0.0065	0.0059
(ER)	Particulate Emission Rate, lb/hr	1.4	1.6	1.8	1.6
	Train Fractionation:				
	filterable, %	40	63	57	53
	condensible, %	60	37	43	47

TABLE 2.2.5-3

PRESS VENT #7

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/16/92 0800-0905	RUN 2 3/16/92 0935-1040	RUN 3 3/16/92 1101-1202	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	1.76	1.40	1.40	1.52
(Bp)	Barometric Pressure, inches Hg	30.05	30.05	30.05	30.05
(Vm)	Meter Volume, cf	35.605	36.522	35.998	36.042
(Tm)	Avg Meter Temp, deg F	53.2	64.0	74.0	63.7
(Pg)	Static Pressure, inches H2O	-0.42	-0.42	-0.42	-0.42
(Ts)	Avg Stack Temp, deg F	59.7	67.0	73.0	66.6
(Vlc)	Water Collected, ml	4.2	8.1	4.1	5.5
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.619	0.613	0.607	0.61
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	56	56	56	56
(Mf)	Total Formaldehyde, mg	20	26	30	25
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	37.304	37.443	36.215	36.987
(Ps)	Stack Pressure, inches Hg	30.02	30.02	30.02	30.02
(%Bws)	Moisture (from impingers), %	0.5	1.0	0.5	0.7
(%Bws)	Moisture (at saturation), %	1.7	2.2	2.7	2.2
(Ms)	Molecular Weight-wet, lb/lb-mole	28.8	28.7	28.8	28.8
(Vs)	Velocity, ft/s	34.5	34.4	34.2	34.4
(As)	Stack Area, sq ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	3.54E+04	3.53E+04	3.51E+04	3.53E+04
(Qs)	Volumetric flow, dscfm	3.59E+04	3.51E+04	3.47E+04	3.52E+04
(I)	Isokinetic Rate, %	97.6	100.0	98.0	98.6
(Cf)	Formaldehyde Concentration, mg/dscf	0.54	0.69	0.83	0.69
(Cppm)	Formaldehyde Concentration, ppm	15.2	19.6	23.4	19.4
(ER)	Formaldehyde Emission Rate, lb/hr	2.54	3.23	3.80	3.19

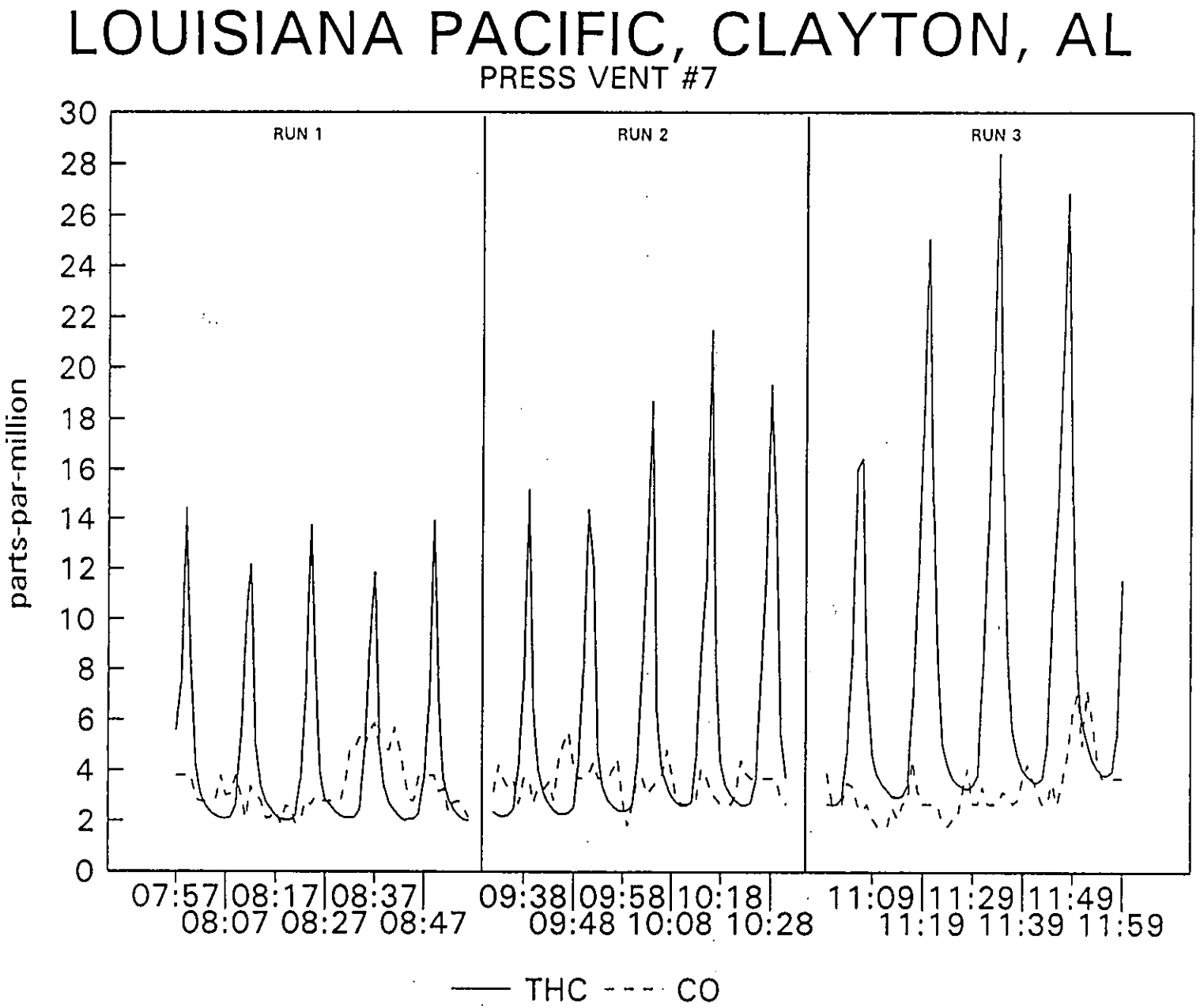
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #7
RUN 1
RUN 2
RUN 3
parts-par-million
30
28
26
24
22
20
18
16
14
12
10
8
6
4
2
0
07:57
08:07
08:17
08:27
08:37
08:47
09:38
09:48
09:58
10:08
10:18
10:28
11:09
11:19
11:29
11:39
11:49
11:59
THC
CO

FIGURE 2.2.5-1

TABLE 2.2.6-1
SUMMARY OF EMISSIONS
PRESS VENT #8
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.002	0.002	0.003	0.003
Emission Rate, lb/hr	0.6	0.7	1.0	0.8
Particulate (Including condensibles)				
Concentration, gr/dscf	0.007	0.007	0.005	0.006
Emission Rate, lb/hr	2.2	2.3	1.4	2.0
Formaldehyde				
Concentration, ppm	10.4	11.0	15.6	12.3
Emission Rate, lb/hr	2.2	2.4	3.0	2.5
Carbon Monoxide				
Concentration, ppm	1.7	1.9	2.7	2.1
Emission Rate, lb/hr	0.3	0.4	0.5	0.4
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	4.2	4.6	4.0	4.3
Emission Rate, lb/hr	1.3	1.5	1.1	1.3

TABLE 2.2.6-2
PRESS VENT #8
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/18/92 1240-1350	RUN 2 3/19/92 0753-0925	RUN 3 3/19/92 0953-1057	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	1.50	1.53	1.45	1.49
(Bp)	Barometric Pressure, inches Hg	29.85	29.58	29.58	29.67
(Vm)	Meter Volume, cu.ft	36.606	37.376	36.784	36.922
(Tm)	Avg Meter Temp, deg F	66.9	72.0	82.5	73.8
(Pg)	Static Pressure, inches H2O	0.03	0.03	0.01	0.02
(Ts)	Avg Stack Temp, deg F	72.5	79.5	87.7	79.9
(Vlc)	Water Collected, ml	18.7	18.8	16.0	17.8
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.632	0.645	0.623	0.63
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.235	0.235	0.235	0.235
(D)	Stack Diameter, inches	56	56	56	56
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0031	0.0054	0.0067	0.0051
(Mf)	Particulate Collected (filter), g	0.0014	0.0002	0.0011	0.0009
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0060	0.0056	0.0021	0.0046
(Mio)	MeCl Impinger (organic) residue, g	0.0070	0.0065	0.0008	0.0048
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	37.084	37.166	35.862	36.704
(Ps)	Stack Pressure, inches Hg	29.85	29.58	29.58	29.67
(%Bws)	Moisture, %	2.3	2.3	2.1	2.2
(Ms)	Molecular Weight-wet, lb/lb-mole	28.6	28.6	28.6	28.6
(Vs)	Velocity, ft/s	35.9	37.0	36.0	36.3
(As)	Stack Area, sq.ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	36,793	37,969	36,934	37,232
(Qs)	Volumetric flow, dscfm	35,542	35,871	34,464	35,292
(I)	Isokinetic Rate, %	98.8	98.1	98.5	98.5
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0019	0.0023	0.0034	0.0025
(ER)	Particulate Emission Rate, lb/hr	0.6	0.7	1.0	0.8
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0044	0.0046	0.0043	0.0044
(ER)	Particulate Emission Rate, lb/hr	1.3	1.4	1.3	1.3
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0073	0.0073	0.0046	0.0064
(ER)	Particulate Emission Rate, lb/hr	2.2	2.3	1.4	1.9
	Train Fractionation:				
	filterable, %	26	32	73	43
	condensible, %	74	68	27	57

TABLE 2.2.6-3

PRESS VENT #8

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/16/92 1453-1556	RUN 2 3/16/92 1642-1745	RUN 3 3/16/92 1813-1916	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	1.80	1.75	1.50	1.68
(Bp)	Barometric Pressure, inches Hg	30.05	30.05	30.05	30.05
(Vm)	Meter Volume, cf	41.190	41.361	37.112	39.888
(Tm)	Avg Meter Temp, deg F	82.0	79.2	63.0	74.7
(Pg)	Static Pressure, inches H2O	-0.35	-0.35	-0.35	-0.35
(Ts)	Avg Stack Temp, deg F	76.0	70.7	63.0	69.9
(Vlc)	Water Collected, ml	0.0	1.5	2.2	1.2
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.689	0.710	0.616	0.67
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	60	60	60	60
(Mf)	Total Formaldehyde, mg	15	16	21	17
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	40.866	41.244	38.130	40.080
(Ps)	Stack Pressure, inches Hg	30.02	30.02	30.02	30.02
(%Bws)	Moisture (from impingers), %	0.0	0.2	0.3	0.1
(%Bws)	Moisture (at saturation), %	3.0	2.5	1.9	2.5
(Ms)	Molecular Weight-wet, lb/lb-mole	28.8	28.8	28.8	28.8
(Vs)	Velocity, ft/s	38.9	39.9	34.4	37.7
(As)	Stack Area, sq ft	19.63	19.63	19.63	19.63
(Qa)	Volumetric flow, acfm	4.59E+04	4.70E+04	4.05E+04	4.45E+04
(Qs)	Volumetric flow, dscfm	4.53E+04	4.69E+04	4.09E+04	4.44E+04
(I)	Isokinetic Rate, %	97.2	94.8	100.5	97.5
(Cf)	Formaldehyde Concentration, mg/dscf	0.37	0.39	0.55	0.44
(Cppm)	Formaldehyde Concentration, ppm	10.4	11.0	15.6	12.3
(ER)	Formaldehyde Emission Rate, lb/hr	2.20	2.41	2.98	2.53

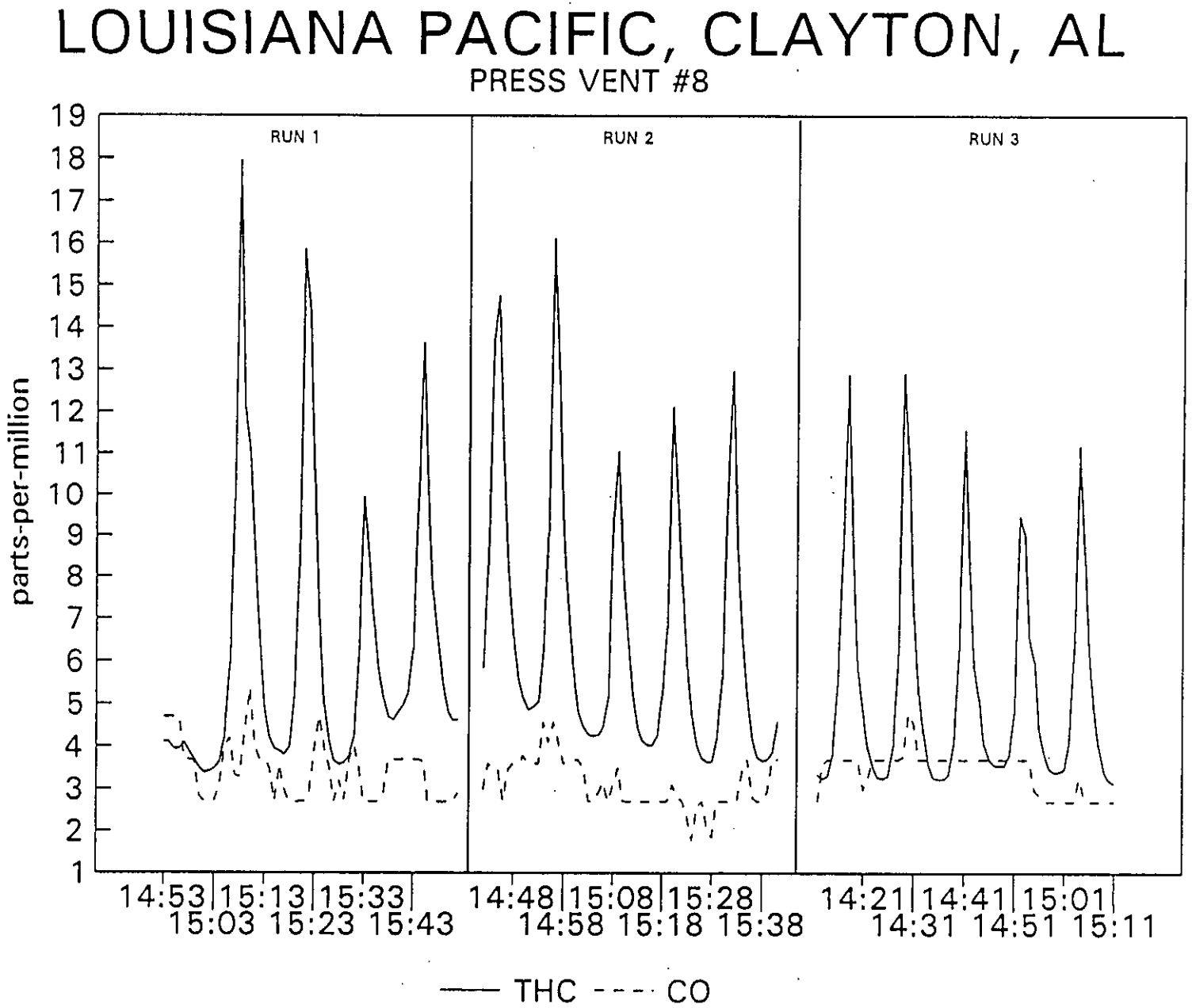
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #8
RUN 1
RUN 2
RUN 3
parts-per-million
19
18
17
16
15
14
13
12
11
10
9
8
7
6
5
4
3
2
1
14:53 15:13 15:33
15:03 15:23 15:43
14:48 15:08 15:28
14:58 15:18 15:38
14:21 14:41 15:01
14:31 14:51 15:11
THC
CO

FIGURE 2.2.6-1

TABLE 2.2.7-1
SUMMARY OF EMISSIONS
PRESS VENT #9
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.001	0.002	0.002	0.001
Emission Rate, lb/hr	0.2	0.5	0.4	0.4
Particulate (Including condensibles)				
Concentration, gr/dscf	0.001	0.003	0.002	0.002
Emission Rate, lb/hr	0.4	0.7	0.5	0.5
Formaldehyde				
Concentration, ppm	11.4	13.1	13.5	12.7
Emission Rate, lb/hr	1.8	2.0	2.0	1.9
Carbon Monoxide				
Concentration, ppm	2.4	4.7	4.7	3.9
Emission Rate, lb/hr	0.3	0.7	0.7	0.6
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	4.0	2.1	2.5	2.9
Emission Rate, lb/hr	0.9	0.5	0.6	0.7

TABLE 2.2.7-2
PRESS VENT #9
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/17/92 1456-1559	RUN 2 3/17/92 1628-1741	RUN 3 3/17/92 1807-1909	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.38	1.45	1.31	1.38
(Bp)	Barometric Pressure, inches Hg	30.02	30.02	30.02	30.02
(Vm)	Meter Volume, cu.ft	38.948	37.952	36.004	37.635
(Tm)	Avg Meter Temp, deg F	80.3	76.6	71.1	76.0
(Pg)	Static Pressure, inches H2O	-0.29	-0.29	-0.29	-0.29
(Ts)	Avg Stack Temp, deg F	82.6	79.7	75.4	79.2
(Vlc)	Water Collected, ml	9.4	8.2	8.2	8.6
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.581	0.592	0.554	0.58
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.242	0.242	0.242	0.242
(D)	Stack Diameter, inches	56	56	56	56
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0009	0.0029	0.0029	0.0022
(Mf)	Particulate Collected (filter), g	0.0013	0.0011	0.0010	0.0011
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0014	0.0021	0.0005	0.0013
(Mio)	MeCl Impinger (organic) residue, g	0.0000	0.0000	0.0002	0.0001
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	38.379	37.662	36.086	37.376
(Ps)	Stack Pressure, inches Hg	30.00	30.00	30.00	30.00
(%Bws)	Moisture, %	1.1	1.0	1.1	1.1
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.7	28.7	28.7
(Vs)	Velocity, ft/s	33.1	33.6	31.4	32.7
(As)	Stack Area, sq.ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	33,984	34,527	32,184	33,565
(Qs)	Volumetric flow, dscfm	32,766	33,510	31,474	32,583
(I)	Isokinetic Rate, %	104.6	100.3	102.3	102.4
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0009	0.0016	0.0017	0.0014
(ER)	Particulate Emission Rate, lb/hr	0.2	0.5	0.4	0.4
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0014	0.0025	0.0019	0.0019
(ER)	Particulate Emission Rate, lb/hr	0.4	0.7	0.5	0.5
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0014	0.0025	0.0020	0.0020
(ER)	Particulate Emission Rate, lb/hr	0.4	0.7	0.5	0.6
	Train Fractionation:				
	filterable, %	61	66	85	70
	condensible, %	39	34	15	30

TABLE 2.2.7-3

PRESS VENT #9

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/17/92 0855-0957	RUN 2 3/17/92 1027-1131	RUN 3 3/17/92 1158-1301	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	1.30	1.30	1.29	1.30
(Bp)	Barometric Pressure, inches Hg	30.02	30.02	30.02	30.02
(Vm)	Meter Volume, cf	34.209	34.926	36.608	35.248
(Tm)	Avg Meter Temp, deg F	67.0	84.0	90.6	80.5
(Pg)	Static Pressure, inches H2O	-0.21	-0.21	-0.21	-0.21
(Ts)	Avg Stack Temp, deg F	67.0	75.0	80.6	74.2
(Vlc)	Water Collected, ml	3.1	6.5	40.0	16.5
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.574	0.573	0.574	0.57
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	56	56	56	56
(Mf)	Total Formaldehyde, mg	14	16	17	16
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	34.829	34.448	35.673	34.983
(Ps)	Stack Pressure, inches Hg	30.00	30.00	30.00	30.00
(%Bws)	Moisture (from impingers), %	0.4	0.9	5.0	2.1
(%Bws)	Moisture (at saturation), %	2.2	2.9	3.4	2.9
(Ms)	Molecular Weight-wet, lb/lb-mole	28.8	28.7	28.5	28.7
(Vs)	Velocity, ft/s	32.2	32.4	32.8	32.5
(As)	Stack Area, sq ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	3.30E+04	3.32E+04	3.37E+04	3.33E+04
(Qs)	Volumetric flow, dscfm	3.30E+04	3.26E+04	3.18E+04	3.25E+04
(I)	Isokinetic Rate, %	99.0	99.2	105.2	101.1
(Cf)	Formaldehyde Concentration, mg/dscf	0.40	0.46	0.48	0.45
(Cppm)	Formaldehyde Concentration, ppm	11.4	13.1	13.5	12.7
(ER)	Formaldehyde Emission Rate, lb/hr	1.76	2.00	2.01	1.92

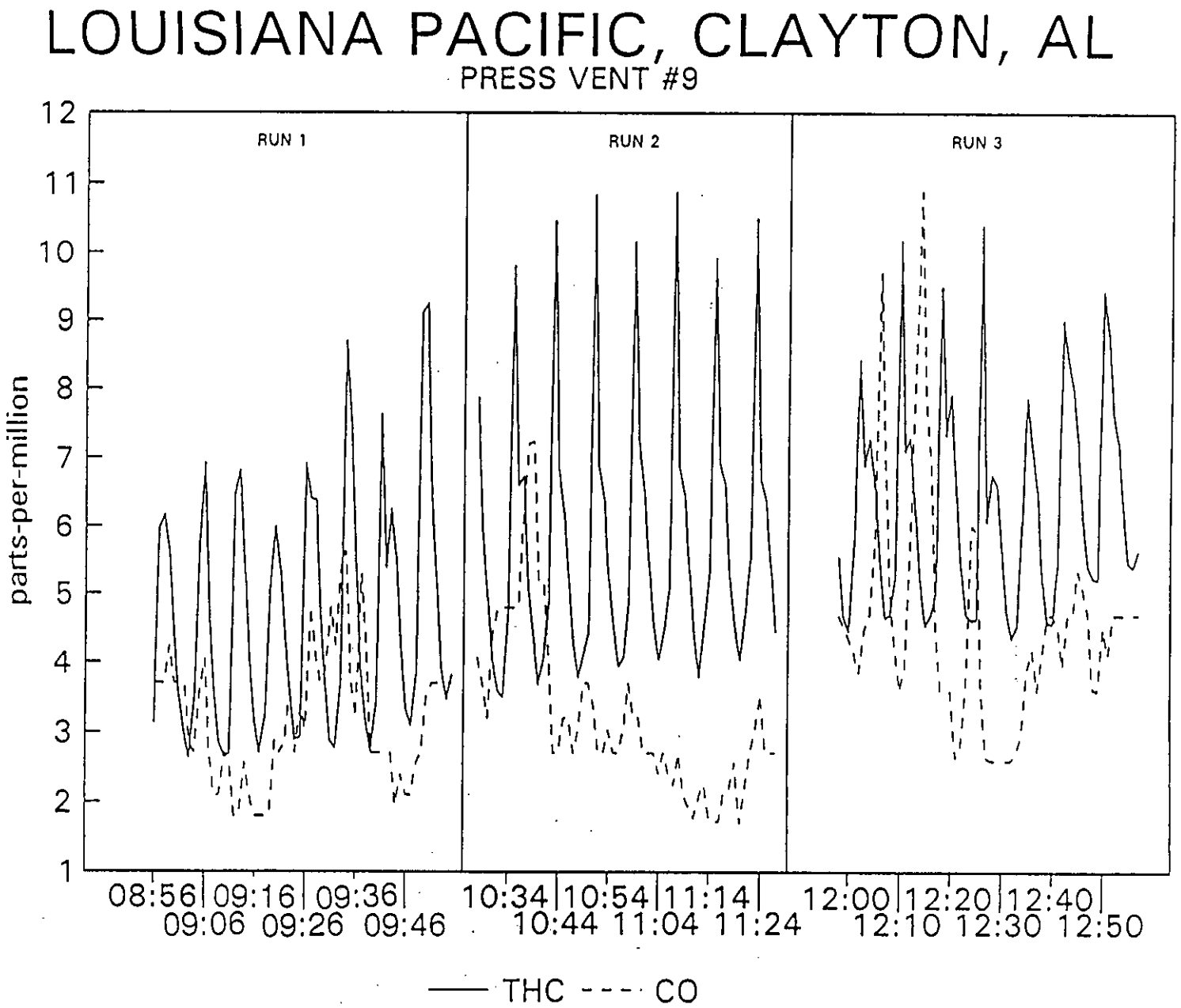
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #9
RUN 1
RUN 2
RUN 3
parts-per-million
12
11
10
9
8
7
6
5
4
3
2
1
08:56
09:06
09:16
09:26
09:36
09:46
10:34
10:44
10:54
11:04
11:14
11:24
12:00
12:10
12:20
12:30
12:40
12:50
THC
CO

FIGURE 2.2.7-1

TABLE 2.2.8-1
SUMMARY OF EMISSIONS
PRESS VENT #10
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Particulate				
Concentration, gr/dscf	0.002	0.004	0.003	0.003
Emission Rate, lb/hr	0.5	1.2	0.8	0.8
Particulate (Including condensibles)				
Concentration, gr/dscf	0.003	0.004	0.005	0.004
Emission Rate, lb/hr	0.7	1.3	1.5	1.2
Formaldehyde				
Concentration, ppm	9.1	10.9	8.8	9.6
Emission Rate, lb/hr	1.6	1.8	1.5	1.7
Carbon Monoxide				
Concentration, ppm	1.5	1.2	0.7	1.1
Emission Rate, lb/hr	0.2	0.2	0.1	0.2
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	9.2	6.4	5.4	7.0
Emission Rate, lb/hr	2.4	1.7	1.3	1.8

TABLE 2.2.8-2
PRESS VENT #10
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/18/92 0914-1018	RUN 2 3/19/92 0732-0901	RUN 3 3/19/92 0938-1044	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.25	1.83	1.72	1.60
(Bp)	Barometric Pressure, inches Hg	29.85	29.58	29.58	29.67
(Vm)	Meter Volume, cu.ft	32.327	41.829	42.215	38.790
(Tm)	Avg Meter Temp, deg F	62.5	72.7	89.3	74.8
(Pg)	Static Pressure, inches H2O	-0.20	-0.20	-0.20	-0.20
(Ts)	Avg Stack Temp, deg F	78.7	83.3	91.9	84.6
(Vlc)	Water Collected, ml	9.2	15.5	15.4	13.4
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	0.539	0.668	0.647	0.62
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.242	0.242	0.242	0.242
(D)	Stack Diameter, inches	56	56	56	56
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0021	0.0058	0.0050	0.0043
(Mf)	Particulate Collected (filter), g	0.0022	0.0040	0.0020	0.0027
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0010	0.0013	0.0032	0.0018
(Mio)	MeCl Impinger (organic) residue, g	0.0000	0.0000	0.0023	0.0008
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	32.743	41.241	40.353	38.112
(Ps)	Stack Pressure, inches Hg	29.84	29.57	29.57	29.66
(%Bws)	Moisture, %	1.3	1.7	1.8	1.6
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.6	28.6	28.7
(Vs)	Velocity, ft/s	30.7	38.4	37.5	35.5
(As)	Stack Area, sq.ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	31,510	39,428	38,492	36,477
(Qs)	Volumetric flow, dscfm	30,382	37,191	35,732	34,435
(I)	Isokinetic Rate, %	96.2	99.0	100.8	98.7
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0020	0.0037	0.0027	0.0028
(ER)	Particulate Emission Rate, lb/hr	0.5	1.2	0.8	0.8
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0025	0.0042	0.0039	0.0035
(ER)	Particulate Emission Rate, lb/hr	0.7	1.3	1.2	1.1
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0025	0.0042	0.0048	0.0038
(ER)	Particulate Emission Rate, lb/hr	0.7	1.3	1.5	1.1
	Train Fractionation:				
	filterable, %	81	88	56	75
	condensible, %	19	12	44	25

TABLE 2.2.8-3

PRESS VENT #10

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/17/92 1523-1626	RUN 2 3/17/92 1649-1752	RUN 3 3/17/92 1812-1916	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.010	1.010	1.010	1.010
	Avg Delta H, inches H2O	1.70	1.60	1.50	1.60
(Bp)	Barometric Pressure, inches Hg	30.02	30.02	30.02	30.02
(Vm)	Meter Volume, cf	40.640	39.146	38.390	39.392
(Tm)	Avg Meter Temp, deg F	83.0	78.0	74.0	78.3
(Pg)	Static Pressure, inches H2O	-0.24	-0.24	-0.24	-0.24
(Ts)	Avg Stack Temp, deg F	89.0	87.0	82.0	86.0
(Vlc)	Water Collected, ml	8.4	38.3	6.0	17.6
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.679	0.661	0.640	0.66
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.236	0.236	0.236	0.236
(Ds)	Stack Diameter, inches	56	56	56	56
(Mf)	Total Formaldehyde, mg	13	15	12	13
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	40.197	39.069	38.592	39.286
(Ps)	Stack Pressure, inches Hg	30.00	30.00	30.00	30.00
(%Bws)	Moisture (from impingers), %	1.0	4.4	0.7	2.0
(%Bws)	Moisture (at saturation), %	4.6	4.3	3.7	4.2
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.4	28.8	28.6
(Vs)	Velocity, ft/s	38.9	38.0	36.4	37.8
(As)	Stack Area, sq ft	17.10	17.10	17.10	17.10
(Qa)	Volumetric flow, acfm	3.99E+04	3.90E+04	3.74E+04	3.88E+04
(Qs)	Volumetric flow, dscfm	3.81E+04	3.62E+04	3.62E+04	3.68E+04
(I)	Isokinetic Rate, %	99.0	101.4	99.9	100.1
(Cf)	Formaldehyde Concentration, mg/dscf	0.32	0.38	0.31	0.34
(Cppm)	Formaldehyde Concentration, ppm	9.1	10.9	8.8	9.6
(ER)	Formaldehyde Emission Rate, lb/hr	1.63	1.84	1.49	1.65

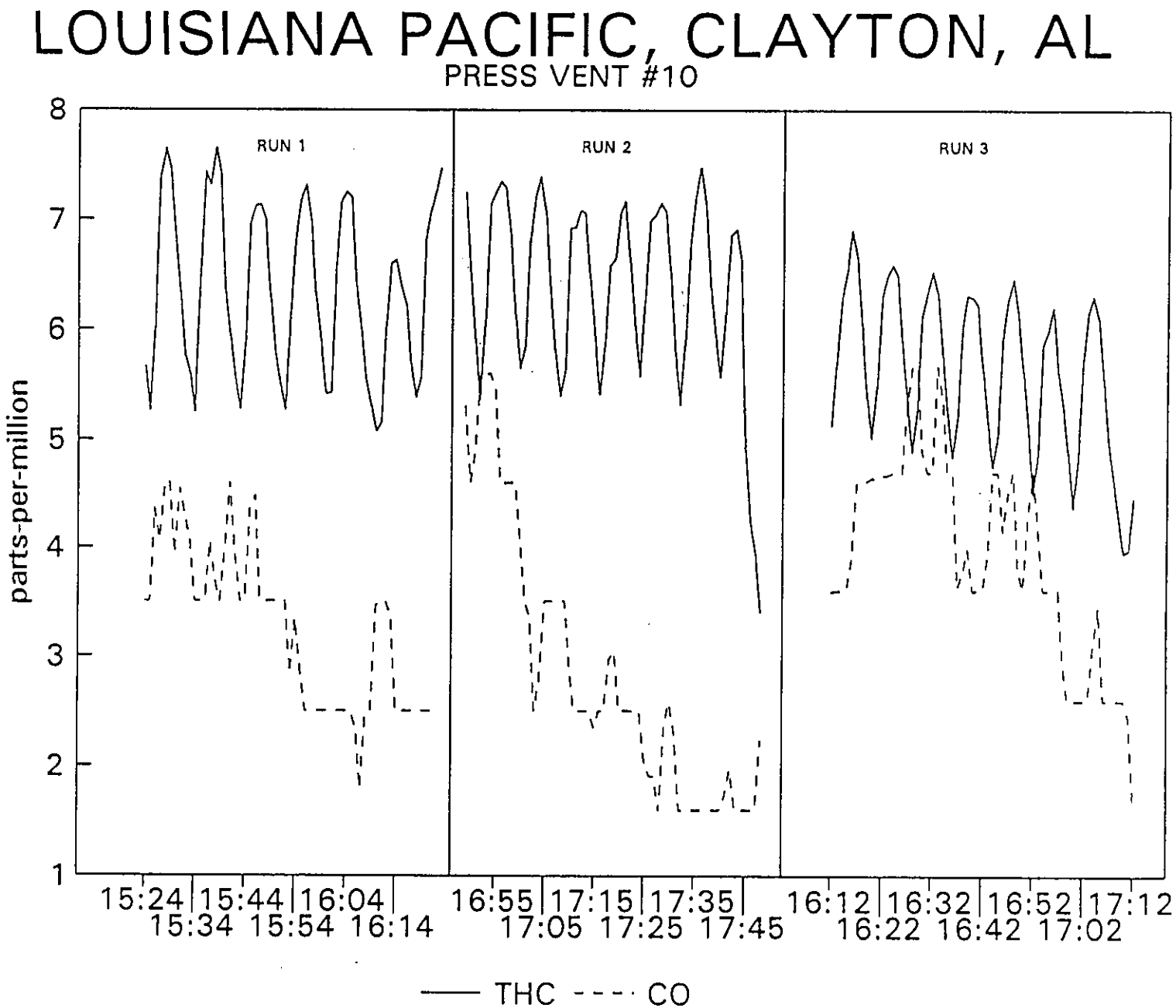
LOUISIANA PACIFIC, CLAYTON, AL
PRESS VENT #10
RUN 1
RUN 2
RUN 3
parts-per-million
8
7
6
5
4
3
2
1
15:24
15:34
15:44
15:54
16:04
16:14
16:55
17:05
17:15
17:25
17:35
17:45
16:12
16:22
16:32
16:42
16:52
17:02
17:12
THC
CO

FIGURE 2.2.8-1

TABLE 2.2.9-1
SUMMARY OF EMISSIONS
PRESS VENT #11
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

PARAMETER	RUN 1	RUN 2	RUN 3	AVERAGE
Formaldehyde				
Concentration, ppm	58.5	45.2	45.8	49.8
Emission Rate, lb/hr	5.5	4.1	3.9	4.5
Carbon Monoxide				
Concentration, ppm	0.8	0.6	0.0	0.5
Emission Rate, lb/hr	0.1	0.0	0.0	0.0
Total Hydrocarbons (VOC), as propane				
Concentration, ppm	11.6	11.0	8.9	10.5
Emission Rate, lb/hr	1.6	1.4	1.1	1.4

TABLE 2.2.9-2

PRESS VENT #11

FORMALDEHYDE TEST SUMMARY

LOUISIANA PACIFIC-CLAYTON,ALABAMA

SYMBOL	PARAMETER	RUN 1 3/13/92 1021-1130	RUN 2 3/13/92 1242-1348	RUN 3 3/13/92 1440-1546	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	0.998	0.998	0.998	0.998
	Avg Delta H, inches H2O	1.29	1.20	1.38	1.29
(Bp)	Barometric Pressure, inches Hg	30.00	30.00	30.00	30.00
(Vm)	Meter Volume, cf	36.517	36.724	35.067	36.103
(Tm)	Avg Meter Temp, deg F	73.8	85.4	87.5	82.2
(Pg)	Static Pressure, inches H2O	-0.44	-0.44	-0.44	-0.44
(Ts)	Avg Stack Temp, deg F	68.8	71.9	70.0	70.2
(Vlc)	Water Collected, ml	11.8	2.9	2.9	5.9
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, (inches H2O) ^ 1/2	0.888	0.843	0.801	0.84
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.196	0.196	0.196	0.196
(Ds)	Stack Diameter, inches	35	35	35	35
(Mf)	Total Formaldehyde, mg	75	57	55	62
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, dscf	36.244	35.667	33.942	35.284
(Ps)	Stack Pressure, inches Hg	29.97	29.97	29.97	29.97
(%Bws)	Moisture (from impingers), %	1.5	0.4	0.4	0.8
(%Bws)	Moisture (at saturation), %	2.3	2.6	2.5	2.4
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.8	28.8	28.8
(Vs)	Velocity, ft/s	50.0	47.5	45.1	47.5
(As)	Stack Area, sq ft	6.78	6.78	6.78	6.78
(Qa)	Volumetric flow, acfm	2.03E+04	1.93E+04	1.83E+04	1.93E+04
(Qs)	Volumetric flow, dscfm	2.00E+04	1.91E+04	1.82E+04	1.91E+04
(I)	Isokinetic Rate, %	97.6	100.5	100.5	99.5
(Cf)	Formaldehyde Concentration, mg/dscf	2.07	1.60	1.62	1.76
(Cppm)	Formaldehyde Concentration, ppm	58.5	45.2	45.8	49.8
(ER)	Formaldehyde Emission Rate, lb/hr	5.48	4.05	3.90	4.48

LOUISIANA PACIFIC, CLAYTON, AL

PRESS VENT #11

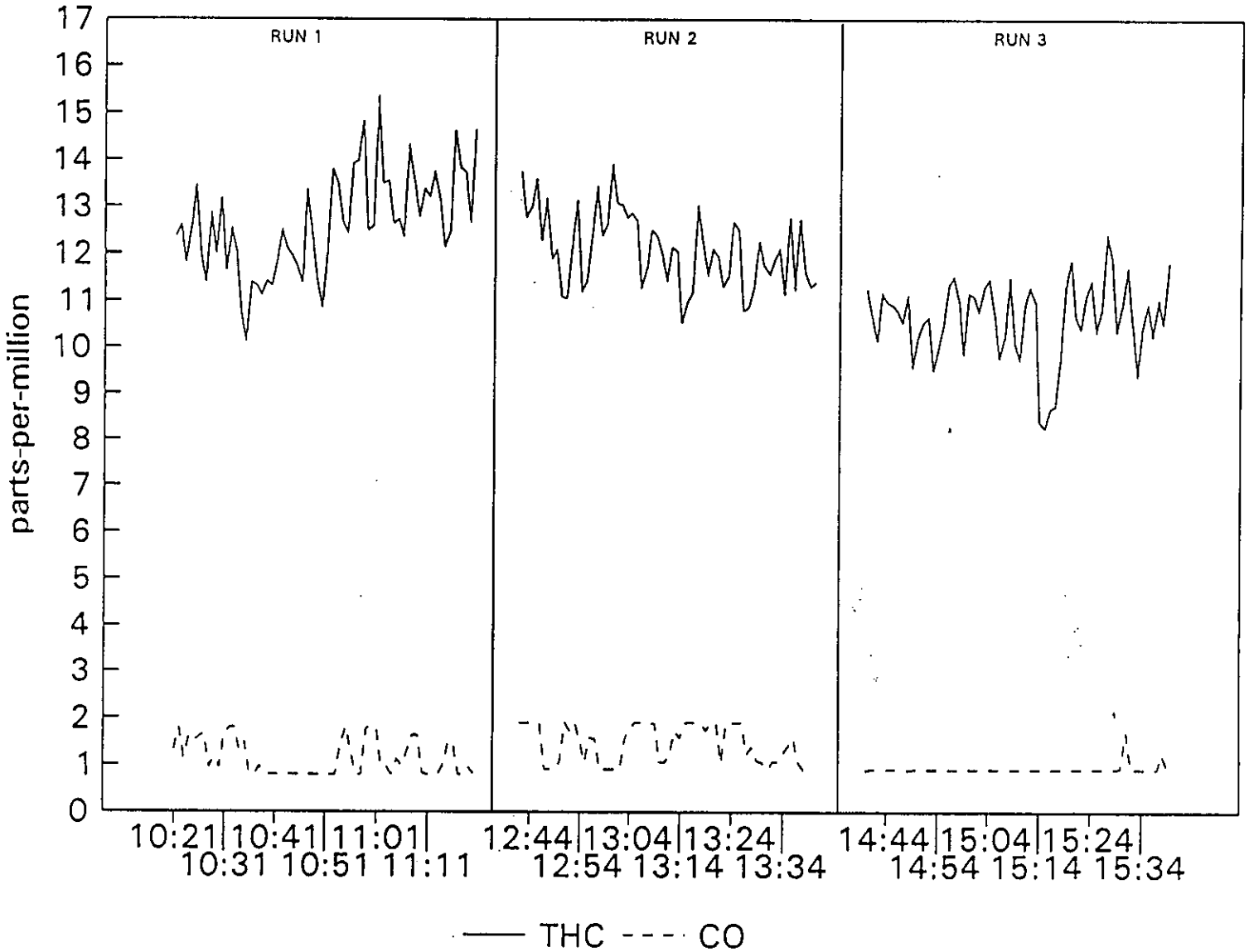

FIGURE 2.2.9-1

2.3 BOILER STACKS

2.3.1 Boiler Stack 1

Table 2.3.1-1 presents a summary of the particulate emissions from Boiler Stack 1.

Particulate Matter - concentration averaged 0.084 gr/dscf resulting in 9.6 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.094 gr/dscf resulting in 10.8 lbs/hr.

2.3.2 Boiler Stack 2

Table 2.3.2-1 presents a summary of the emissions from Boiler Stack 2.

Particulate Matter - concentration averaged 0.104 gr/dscf resulting in 9.4 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 0.106 gr/dscf resulting in 9.6 lbs/hr.

2.4 Former Stack

Tables 2.4-1 summarizes the particulate emission testing on the Former Stack.

Particulate Matter - concentration averaged 1.056 gr/dscf resulting in 77.7 lbs/hr.

Particulate Matter (including condensibles) - concentration averaged 1.062 gr/dscf resulting in 78.2 lbs/hr.

TABLE 2.3.1-1
BOILER STACK #1
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/16/92 1710-1813	RUN 2 3/17/92 0833-0945	RUN 3 3/17/92 1046-1155	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	2.66	2.47	2.52	2.55
(Bp)	Barometric Pressure, inches Hg	30.05	30.02	30.02	30.03
(Vm)	Meter Volume, cu.ft	51.996	49.126	50.586	50.569
(Tm)	Avg Meter Temp, deg F	70.2	75.4	92.9	79.5
(Pg)	Static Pressure, inches H2O	0.00	0.00	0.00	0.00
(Ts)	Avg Stack Temp, deg F	257.5	262.7	273.6	264.6
(Vlc)	Water Collected, ml	50.1	61.8	58.9	56.9
(CO2)	Carbon dioxide, %	6.5	6.5	6.5	6.5
(O2)	Oxygen, %	14.0	14.0	14.0	14.0
	Avg Sqrt Delta P, sqrt(inches H2O)	0.274	0.263	0.266	0.27
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.473	0.473	0.473	0.473
(D)	Stack Diameter, inches	58	58	58	58
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0507	0.0858	0.0034	0.0466
(Mf)	Particulate Collected (filter), g	0.2140	0.2645	0.1954	0.2246
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0023	0.0840	0.0030	0.0298
(Mio)	MeCl Impinger (organic) residue, g	0.0023	0.0080	0.0015	0.0039
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	52.427	48.981	48.846	50.085
(Ps)	Stack Pressure, inches Hg	30.05	30.02	30.02	30.03
(%Bws)	Moisture, %	4.3	5.6	5.4	5.1
(Ms)	Molecular Weight-wet, lb/lb-mole	29.1	28.9	29.0	29.0
(Vs)	Velocity, ft/s	17.8	17.2	17.5	17.5
(As)	Stack Area, sq.ft	18.35	18.35	18.35	18.35
(Qa)	Volumetric flow, acfm	19,621	18,960	19,311	19,297
(Qs)	Volumetric flow, dscfm	13,872	13,114	13,191	13,392
(I)	Isokinetic Rate, %	94.7	93.6	92.8	93.7
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0779	0.1104	0.0628	0.0837
(ER)	Particulate Emission Rate, lb/hr	9.3	12.4	7.1	9.6
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0786	0.1368	0.0637	0.0930
(ER)	Particulate Emission Rate, lb/hr	9.3	15.4	7.2	10.6
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0793	0.1393	0.0642	0.0943
(ER)	Particulate Emission Rate, lb/hr	9.4	15.7	7.3	10.8
	Train Fractionation:				
	filterable, %	98	79	98	92
	condensible, %	2	21	2	8

TABLE 2.3.2-1
BOILER STACK #2
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/16/92 1518-1621	RUN 2 3/16/92 1718-1822	RUN 3 3/17/92 0844-0947	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	0.998	0.998	0.998	0.998
	Avg Delta H, inches H2O	1.80	1.75	1.75	1.77
(Bp)	Barometric Pressure, inches Hg	30.05	30.05	30.02	30.04
(Vm)	Meter Volume, cu.ft	42.224	40.876	39.708	40.936
(Tm)	Avg Meter Temp, deg F	88.5	77.4	70.4	78.8
(Pg)	Static Pressure, inches H2O	0.00	0.00	0.00	0.00
(Ts)	Avg Stack Temp, deg F	301.6	320.0	317.1	312.9
(Vlc)	Water Collected, ml	61.4	65.9	63.3	63.5
(CO2)	Carbon dioxide, %	9.0	9.0	9.0	9.0
(O2)	Oxygen, %	11.5	11.5	11.5	11.5
	Avg Sqrt Delta P, sqrt(inches H2O)	0.227	0.224	0.213	0.22
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.464	0.464	0.464	0.464
(D)	Stack Diameter, inches	58	58	58	58
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	0.0556	0.0339	0.0422	0.0439
(Mf)	Particulate Collected (filter), g	0.2026	0.2205	0.2634	0.2288
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0026	0.0045	0.0026	0.0032
(Mio)	MeCl Impinger (organic) residue, g	0.0008	0.0033	0.0015	0.0019
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	40.904	40.411	39.735	40.350
(Ps)	Stack Pressure, inches Hg	30.05	30.05	30.02	30.04
(%Bws)	Moisture, %	6.6	7.1	7.0	6.9
(Ms)	Molecular Weight-wet, lb/lb-mole	29.1	29.1	29.1	29.1
(Vs)	Velocity, ft/s	15.2	15.2	14.4	14.9
(As)	Stack Area, sq.ft	18.35	18.35	18.35	18.35
(Qa)	Volumetric flow, acfm	16,743	16,739	15,890	16,457
(Qs)	Volumetric flow, dscfm	10,884	10,564	10,073	10,507
(I)	Isokinetic Rate, %	97.9	99.6	102.8	100.1
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	0.0974	0.0971	0.1187	0.1044
(ER)	Particulate Emission Rate, lb/hr	9.1	8.8	10.2	9.4
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0984	0.0989	0.1197	0.1056
(ER)	Particulate Emission Rate, lb/hr	9.2	9.0	10.3	9.5
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	0.0987	0.1001	0.1203	0.1064
(ER)	Particulate Emission Rate, lb/hr	9.2	9.1	10.4	9.6
	Train Fractionation:				
	filterable, %	99	97	99	98
	condensible, %	1	3	1	2

TABLE 2.4-1
FORMER STACK #1
PARTICULATE/CONDENSIBLE SUMMARY
LOUISIANA PACIFIC CORPORATION

SYMBOL	PARAMETER	RUN 1 3/12/92 1340-1645	RUN 2 3/12/92 1730-1910	RUN 3 3/13/92 0730-0834	AVERAGE
	MEASURED DATA				
(Y)	Meter Box Y	1.002	1.002	1.002	1.002
	Avg Delta H, inches H2O	1.66	1.66	1.57	1.63
(Bp)	Barometric Pressure, inches Hg	29.83	29.83	29.84	29.83
(Vm)	Meter Volume, cu.ft	41.731	41.556	41.006	41.431
(Tm)	Avg Meter Temp, deg F	61.3	57.9	52.1	57.1
(Pg)	Static Pressure, inches H2O	-1.50	-1.50	-1.50	-1.50
(Ts)	Avg Stack Temp, deg F	73.6	71.2	71.8	72.2
(Vlc)	Water Collected, ml	10.2	2.4	9.9	7.5
(CO2)	Carbon dioxide, %	0.0	0.0	0.0	0.0
(O2)	Oxygen, %	20.9	20.9	20.9	20.9
	Avg Sqrt Delta P, sqrt(inches H2O)	1.659	1.662	1.600	1.64
(0)	Sample Time, min	60	60	60	60
(Dn)	Nozzle Diameter, inches	0.155	0.155	0.155	0.155
(D)	Stack Diameter, inches	17	17	17	17
	Filterable PM				
(Mpw)	Particulate Collected (probe wash), g	1.5891	1.4081	1.5200	1.5057
(Mf)	Particulate Collected (filter), g	1.6639	1.1926	1.3323	1.3963
	Condensible PM				
(Mii)	H2O Impinger (inorganic) residue, g	0.0031	0.0036	0.0021	0.0029
(Mio)	MeCl Impinger (organic) residue, g	0.0130	0.0163	0.0137	0.0143
	CALCULATED DATA				
(Vmstd)	Standard Meter Volume, cu.ft	42.380	42.480	42.397	42.419
(Ps)	Stack Pressure, inches Hg	29.72	29.72	29.73	29.72
(%Bws)	Moisture, %	1.1	0.3	1.1	0.8
(Ms)	Molecular Weight-wet, lb/lb-mole	28.7	28.8	28.7	28.7
(Vs)	Velocity, ft/s	94.2	94.0	90.7	93.0
(As)	Stack Area, sq.ft	1.58	1.58	1.58	1.58
(Qa)	Volumetric flow, acfm	8,909	8,891	8,576	8,792
(Qs)	Volumetric flow, dscfm	8,655	8,752	8,365	8,591
(I)	Isokinetic Rate, %	98.2	97.3	101.6	99.1
	Total filterable PM				
(Cs)	Particulate Concentration, grain/dscf	1.1844	0.9447	1.0381	1.0557
(ER)	Particulate Emission Rate, lb/hr	87.9	70.9	74.4	77.7
	Including only inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	1.1855	0.9460	1.0388	1.0568
(ER)	Particulate Emission Rate, lb/hr	87.9	70.9	74.5	77.8
	Including organic/inorganic PM				
(Cs)	Particulate Concentration, grain/dscf	1.1902	0.9519	1.0438	1.0620
(ER)	Particulate Emission Rate, lb/hr	88.3	71.4	74.8	78.2
	Train Fractionation:				
	filterable, %	100	99	99	99
	condensible, %	0	1	1	1

SECTION 3

PROCESS DESCRIPTION

Louisiana Pacific Corporation operates a Medium Density Fiber Board (MDF) production facility in Clayton, Alabama. The Clayton facility mixes raw green wood chips and dry planer shavings at a ratio of 3:2, respectively, and passes them through a series of shaker screens for sizing. The wood mixture is then conveyed to a digester where it is reduced to wood fiber. Any material not conveyed to the digester is sent to the hammermill to be used as fuel for the rotary kiln dryers.

The cooked and softened fiber material from the digester is sent to any one of the four rotary kiln dryers where it is dried to a predetermined moisture level. The moisture laden gas from the dryers is channeled through cyclones to remove particulate matter and exhausted to the atmosphere through a series of eight dryer stacks (see figure 2.1-1 of this report).

After exiting the dryers, the prepared fiber material is transported to the press building. The fiber material is then blended with resin and wax and sent to the formers where the material is metered out on a continuously moving screen system.

The Clayton facility operates two press lines: a fixed press line and the continuous press line (see figure 2.2-1 of this report). Line 1 is the fixed press line (original line) where the continuously formed mat is separated into 24-foot lengths by a travelling saw and passed to the accumulating loader. Sixteen mats are accumulated in the loader so that the loader can charge the press. The press applies heat and pressure to activate the resin and bond the material into a solid sheet of board. Emissions from the fixed press line were determined from press vents designated numbers 6-10 on Figure 2.2-1.

Line 2 is the continuous press line (new line) where the mat is not cut but fed into the continuous press where heat and pressure are applied. Emission from the continuous press line were determined from press vents designated numbers 3,4,5 and 11 on Figure 2.2-1.

A complete copy of all process rate information over the entire test period (as supplied by Louisiana Pacific Corporation) is presented in Appendix I.

SECTION 4

SAMPLING AND ANALYSIS PROCEDURES

Table 1 summarizes the sampling and analytical effort completed during this project. The following subsections provide descriptions and/or refer to applicable methodologies employed for this project. Any deviations from the specified methodologies are outlined in this report.

4.1 PRE-SAMPLING ACTIVITIES

Pre-sampling activities included equipment calibration, sample media preparation, cleaning of sample train glassware, and other miscellaneous tasks. Each of these activities are described or referenced in the following subsections. Other pre-sampling activities included such details as team meetings, equipment packing and shipment, travel, equipment setup, mobile laboratory setup, and the finalization of all details leading up to the coordinated initiation of the sampling program.

4.1.1 Equipment Calibration

The inspection and calibration of the equipment is a crucial step in assuring the successful completion of the field effort. Equipment was inspected for proper operation and durability prior to calibration. Calibration of the equipment is conducted in accordance to the procedures outlined in the EPA document entitled Quality Assurance Handbook for Air Pollution Measurement Systems; Volume III -Stationary Source Specific Methods" (EPA-600/4-77-027b). All calibrations were performed prior to the field sampling effort.

4.1.2 Glassware Preparation

Sample train glassware and sample containers were precleaned to avoid contamination of the sample from the collection container or devices. Cleaning procedures for the sample train glassware are summarized below. Sample containers were purchased precleaned to specified EPA protocols.

- Method 5 glassware - soap and water wash, DI water rinse, acetone rinse, air dry.
- Method 0011 glassware - soap and water wash, DI water rinse, methylene chloride rinse, air dry.
- Method 202 glassware - soap and water wash, DI water rinse, methylene chloride rinse, air dry.

4.2 STACK GAS SAMPLING AND ANALYSIS

The following subsections describe the types of equipment and techniques used by IEA for collection of stack gas samples. Specific procedures followed are contained in the EPA Method procedure given in 40 CFR 60 Appendix A, EPA-SW-846, or Methods Manual for Compliance With the BIF Regulations, EPA/530-SW-91-010, whenever applicable. Any modifications to these methodologies are at the approval of EPA and are specified in this subsection.

4.2.1 EPA Reference Method 1 - Sampling Point Determination

IEA utilized EPA Reference Method 1 to determine the number and location of the selected traverse points. Each stack was circular in shape and had two ports (designated as A and B) that were accessible for sampling.

Individual sampling points for each source are included in Appendices B, C and D.

4.2.2 EPA Method 2 - Stack Gas Velocity Determination

Gas velocity was measured using EPA Method 2 (Determination of Stack Gas Velocity and Volumetric Flow Rate) procedures and equipment. A Type-S pitot tube in conjunction with an inclined manometer was used to record the pressure head at each traverse point. Temperature was measured with a type K thermocouple.

4.2.3 EPA Method 3 - Stack Gas Molecular Weight Determination

IEA analyzed integrated gas samples collected during each sample run utilizing a Fyrite analyzer allowed by EPA Method 3. In each case all concentrations were determined on a dry, volume-volume basis. The measured gas values indicated concentrations at or near ambient conditions. This was anticipated considering the nature of the source tested.

4.2.4 EPA Method 4 - Moisture Determination

Stack gas moisture was measured concurrently with the particulate testing. Moisture determinations were made by gravimetric analysis of the Method 5 impingers and calculated using the gas volume collected.

4.2.5 EPA Method 5 - Particulate Determination

4.2.5.1 Sample Collection

A preliminary velocity traverse was used to set up parameters for the first particulate test run. EPA Method 2 (Stack Gas Velocity and Volumetric Flow Rate) procedures were followed during each particulate test run to measure stack gas velocity head or Δp.

Particulate concentrations in the stack gas were determined using EPA Method 5 (Determination of Particulate Emissions from Stationary Sources) procedures. The stack sample was withdrawn isokinetically from the source with particulate emissions collecting in the heated probe and on the heated filter. The filter assembly consisted of a glass filter supported by a Teflon frit. The probe was glass lined and connected to the stainless steel nozzle with a 5/8" union.

The gaseous emissions were collected in a series of chilled impingers. Impingers one and two each contained 100 ml of distilled water. Impinger three was empty. Impinger four contained silica gel. Impinger two was of Greenburg-Smith design while all other impingers were modified Greenburg-Smith design. Initial and final leak check rates, recovery data, and all train operation parameters for each test run can be found on the field data sheets in Appendix B. A diagram of the sample train is presented in Figure 4.2.5.1.

4.2.5.2 Recovery Procedures

Upon completion of the sample run for particulate matter the train was carefully removed from the stack, leak-checked, and moved to the clean-up area. Sample recovery was performed according to the methodology described in Method 5. The probe was first rinsed with acetone and then brushed a minimum of three times using a nylon brush to remove any adhering particulate matter. The probe was then rinsed while being rotated to insure particulate collection. This rinse was captured in a flask modified with a ball socket to prevent sample loss. The sample was then transferred to a uniquely identified nalgene sample container. The collection flask was then rinsed and combined with the sample rinse.

The filter was removed from the filter holder and stored in a tared uniquely identified aluminum foil pouch and placed inside a protective manila envelope. The glass filter holder was then rinsed with acetone. This rinse was combined with the probe rinse. The container was sealed and liquid levels were marked for transport to the laboratory. Representative blank samples of the acetone rinse and filter were prepared as a check against potential contamination.

4.2.5.3 Analytical Methodology

Samples were transported from the field to the laboratory for analysis. Sample fractions were handled in the laboratory according to the procedures identified in Method 5. The filter in the aluminum foil (container 1) was placed in the desiccator. Particulate concentrations were determined by allowing probe wash (container 2) to reduce to dryness (unheated) in a tared glass beaker. Both containers 1 and 2 (filter and probe wash) were desiccated to a constant weight. The filter and beaker tare weights and blank corrections were subtracted from the final weights in order to obtain a mass of particulate collected in the filter and probe wash fractions. All weight measurements were made on the same Mettler balance accurate to 0.1 mg. Complete laboratory data sheets are presented in Appendix G.

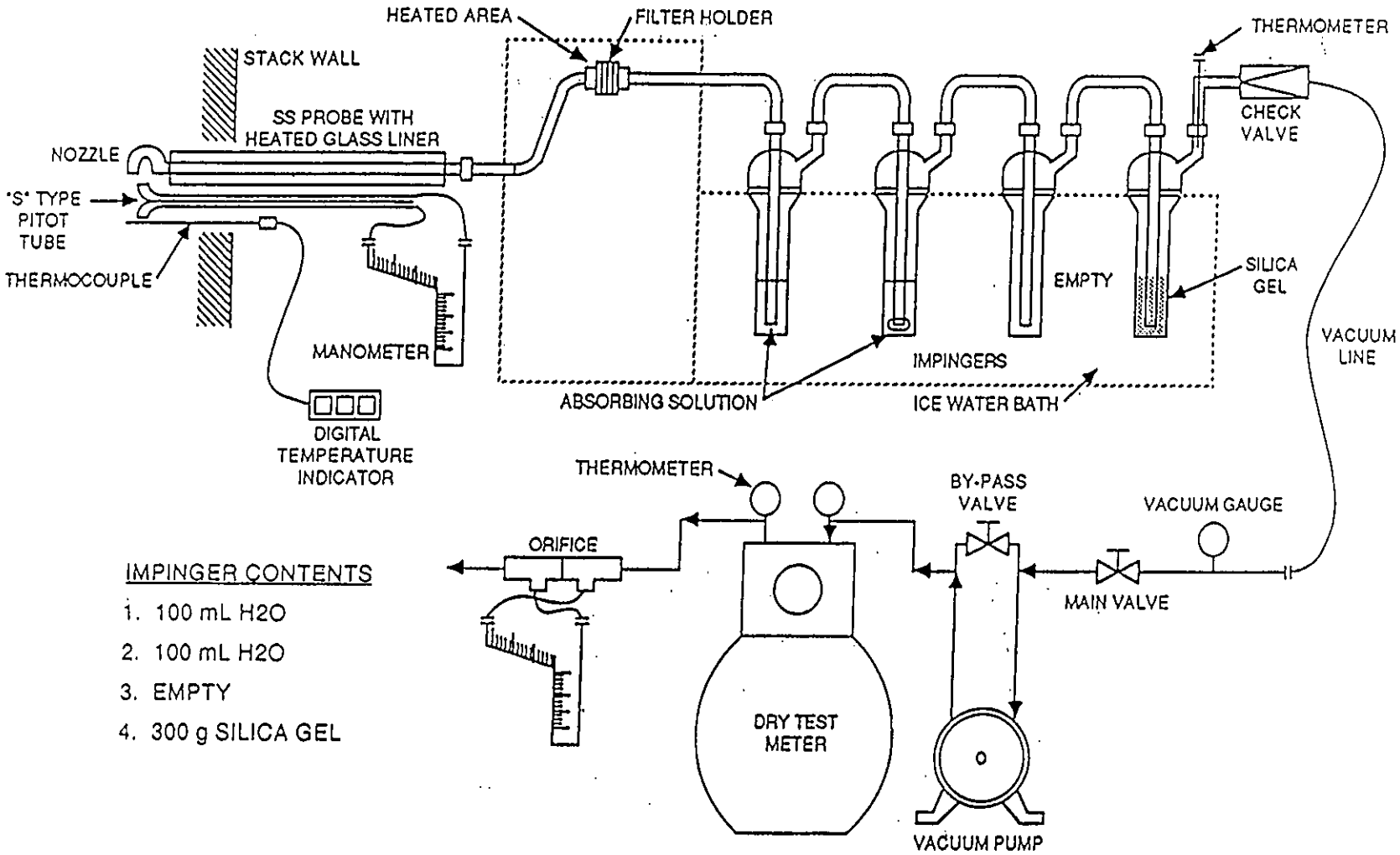

FIGURE 4.2.5.1
PARTICULATE SAMPLE TRAIN

4.2.6 EPA Method 201A

4.2.6.1 Sample Collection

EPA Method 201A utilizes principles of sample collection similar to those described in Section 4.2.5.1 (of this report) for EPA Method 5. Method 201A features an in-stack fractionating cyclone that, when operated at the correct flow rate, performs an aerodynamic separation of particulate at approximately the 10 micron level. Since the cut point is determined aerodynamically in the cyclone, a constant sampling flow rate is required. Flow rate through the cyclone must be varied when the temperature of the stack gas changes by more than +/- 50°F due to gas density and flow rate variation. This procedure allows additional flexibility when compared to EPA Method 5, since isokinetics are permitted to vary by a wider range (80-120% or more depending on particle size).

Method 201A utilizes an in-stack filter immediately following the fractionating cyclone. A sample was withdrawn isokinetically from the source with the in-stack cyclone removing any particulate aerodynamically larger than 10 μm. Smaller particulate collected in the central core of the cyclone and settled on the filter. A diagram of the sample train is included in Figure 4.2.6.1.

Although moisture was collected in a series of chilled impingers, the individual Method 4 moisture percentage calculations were made using the Method 5 train that was run concurrently with the PM_{10} train.

4.2.6.2 Recovery Procedures

Upon completion of the sample run for particulate matter the train was carefully removed from the stack, leak-checked, and moved to the clean-up area. Sample recovery was performed according to the methodology described in Method 201A. The fractionating cyclone was carefully removed from the probe to prevent any dislodging of particulate matter. The cyclone was then disassembled and recovered by rinsing the interior surfaces with acetone. Cyclone geometry dictated separation of less than and greater than PM_{10} fractions. All surfaces were brushed with a nylon brush to remove any adhering particulate matter. These fractions were carefully labeled to indicate the respective particle size.

The filter was removed from the filter holder and stored in a tared uniquely identified petri dish. The glass filter holder was then rinsed with acetone and then combined with the rinse containing the less than PM_{10} fraction. The collection flask was then rinsed and combined with the sample rinse. The container was sealed and liquid levels were marked for gravimetric analysis. Representative blank samples of the acetone rinse and filter were prepared as a check against potential contamination.

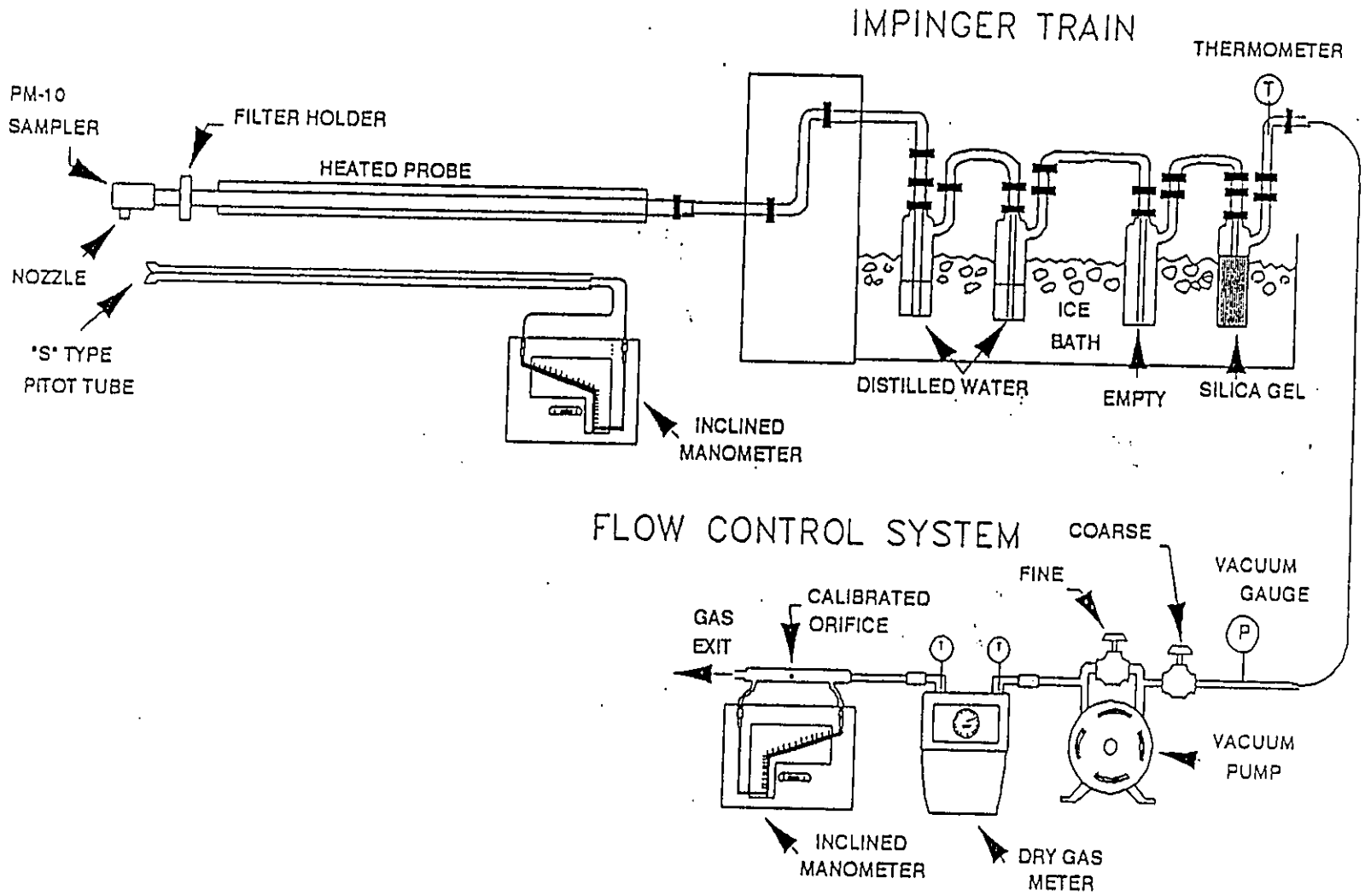

FIGURE 4.2.6.1
PM_{10} SAMPLE TRAIN

4.2.6.3 Analytical Methodology

Sample fractions were handled in the laboratory according to the procedures identified in Method 5 and detailed in section 4.2.5.3 (of this report).

4.2.7 EPA METHOD 202 - CONDENSIBLE PARTICULATE

4.2.7.1 Sample Collection

EPA Method 202 was performed using the back-half of the Method 5 sample train. Sample collection was performed in accordance with section 4.2.5.1 (of this report).

Condensible particulate matter was collected in a series of chilled impingers. Impingers one and two each contained 100 ml of distilled water. Impinger three was empty. Impinger four contained silica gel. Impinger two was of Greenburg-Smith design while all other impingers were modified Greenburg-Smith design. Initial and final leak check rates, recovery data, and all train operation parameters for each test run can be found on the field data sheets in Appendix B.

4.2.7.2 Recovery Procedures

The impingers containing the condensible particulate portion of the sample were recovered according to the procedures identified in EPA Method 202. Impinger contents were recovered into a uniquely identified glass sample bottle and all connecting glassware and impingers were rinsed twice with distilled water. This water rinse was combined with the impinger contents.

All connecting glassware and impingers were then rinsed with methylene chloride ($MeCl_2$) and transferred to separate sample bottles.

4.2.7.3 Analytical Methodology

Method 202 - Condensible Particulate

Sample analysis of the condensible particulate rinse fractions were performed according to EPA Method 202. In the laboratory, the contents of the distilled water fraction were combined with the $MeCl_2$ fraction in a 1000-ml separator funnel in order to segregate the organic and inorganic components. After mixing, the aqueous and organic phases were allowed to fully separate. The organic phase was then drawn off. Seventy-five milliliters of $MeCl_2$ was then combined with the remaining aqueous portion and drawn off upon separation. This process was then repeated with an additional 75 ml of $MeCl_2$. Each time a small amount of organic/$MeCl_2$ phase was left in the separator funnel to ensure no water was captured in the organic phase.

Both organic and aqueous fractions were then allowed to evaporate and desiccate to constant

weight in tared glass beakers. Gravimetric analysis of these fractions was identical to the gravimetric determinations described in EPA Method 5.

4.2.8 Continuous Emission Monitoring System: Methods 10 and 25A

4.2.8.1 Sampling Procedure

A continuous stack gas sample for instrumental measurement of carbon monoxide and total hydrocarbons was collected using a stainless steel probe which was fitted with a sintered stainless steel particulate filter. An unheated 3/8-inch Teflon line was used to transport the sample to the IEA trailer for instrumental analysis. An unheated Teflon recovery gas line was also connected to the back of the probe through which calibration gases from the mobile trailer were sent to the probe and drawn back down the sample line in order to provide through-the-sample-system calibration and ensure sample recovery integrity. A schematic of IEA's CEM system is shown in Figure 4.2.8.1.

The end of the sample line was connected through a VIA MAK 2-2 refrigerated-type sample conditioner and connected to a Teflon-lined sample pump. The gas sample was then divided and directed to individual instrumental analyzers.

Output from the instrumental analyzers is directed to a Molytek Model 2702 32-channel analog/digital strip chart recorder for hard copy output, and downloaded via the serial port to a PC utilizing custom data acquisition software. Data for each of the analyzers was recorded each second with a one-minute average written over to the PC diskette. Data were further averaged over the test period and corrected for calibration error and drift using a spreadsheet program.

After completion of the pre-test calibration routine (described in Section 5.3.3.7), each CEM system was ready for operation. No further adjustments of sample flow rates, analyzer zero or span, or other critical CEMS operating parameters were made until testing and post-test calibrations were complete. A complete copy of data sheets and chart recorder traces is attached in Appendices E and F.

4.2.8.2 Instrumentation

IEA's CEM trailer housed the following continuous monitors:

- Thermo Electron Model 48, CO Analyzer
- J.U.M. Engineering Model VE-7, Total Hydrocarbon Analyzer

A short description of each of the above analyzers follows:

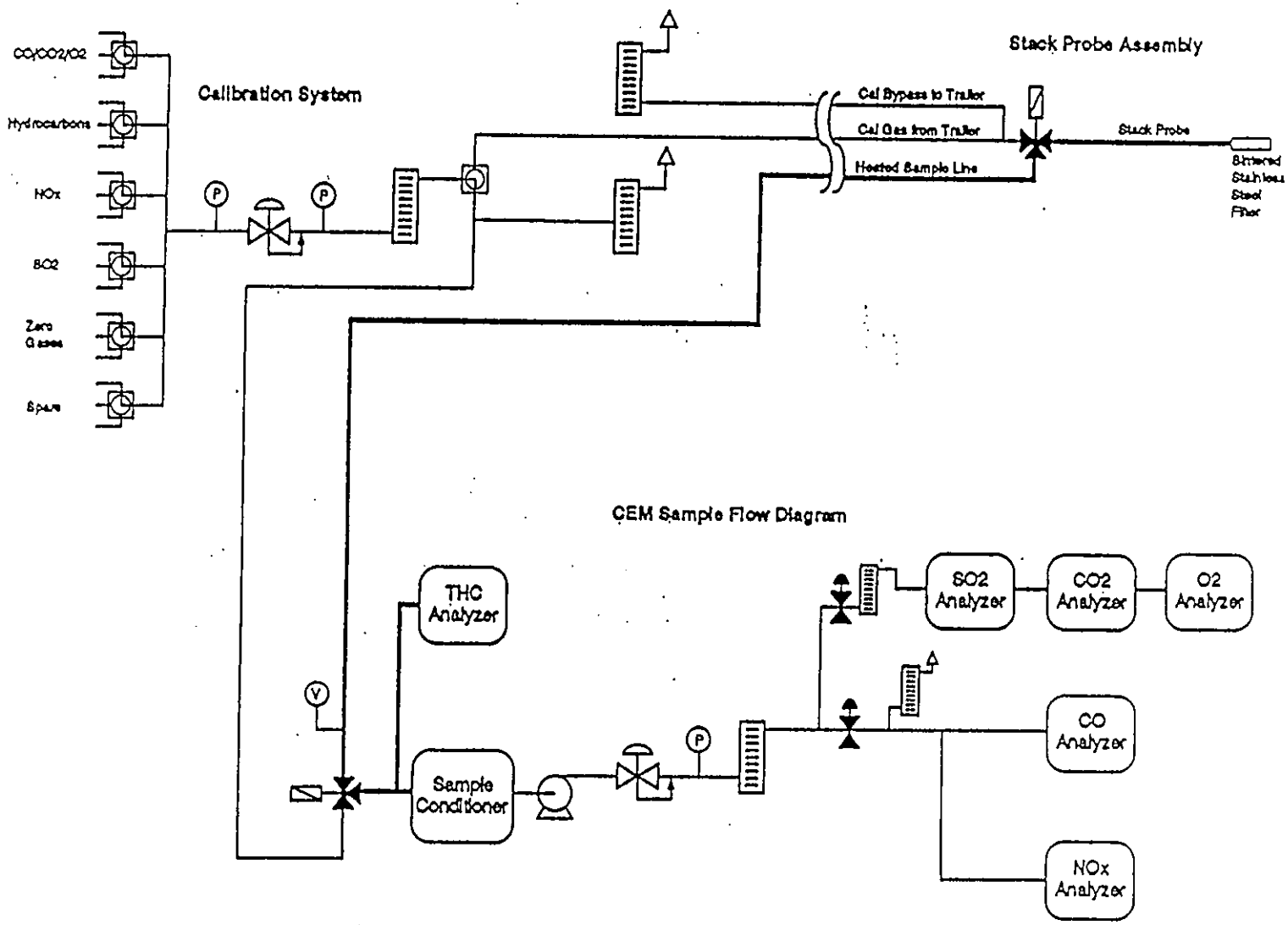

FIGURE 4.2.8.1
CEMS SYSTEM

Thermo Electron Model 48, CO Analyzer

The basic components of the Thermo Electron Model 48 Gas Filter Correlation Analyzer are illustrated in Figure 4.2.8.2-1. Radiation from an infrared source is chopped and then passed through a gas filter which alternates between CO and N_2 due to the rotation of the filter wheel. The radiation then passes through a narrow band-pass filter and a multiple optical pass sample cell where absorption by the sample gas occurs. The IR radiation exits the sample cell and falls on a solid state detector.

The CO gas filter acts to produce a reference beam which cannot be further affected by CO in the sample chamber. The N_2 side of the filter wheel is transparent to IR radiation and, therefore, produces a measure beam which can be absorbed by CO. The chopped detector signal is modulated by the alternation between the two gas filters with an amplitude proportional to the concentration of CO in the sample chamber. Other gases do not cause modulation of the detector signals since they absorb the reference and measure beams equally. Thus the gas filter correlation analyzer responds solely to CO.

J.U.M. Engineering Model VE-7, Total Hydrocarbon Analyzer

A fraction of the sample gas was diverted to the J.U.M. analyzer prior to introduction of the sample gas to the sample conditioner in order to provide a heated, "wet" sample to the analyzer.

The J.U.M. VE-7 is a flame ionization total hydrocarbon analyzer with a heated particulate filter, sample pump and detector. A schematic of the J.U.M. VE-7 is shown in Figure 4.2.8.2-2. The sample passes through an in-line particulate filter, sample pump, and a flow restricting capillary prior to entering the detector. The particulate filter, sample pump and detector are contained in a heated enclosure which is maintained at a temperature well above the sample dew point.

Once inside the detector, the sample is passed through a small flame where the hydrocarbon molecules are broken apart and ionized. The resulting ions are collected on one of two oppositely charged plates. The resulting signal is amplified to provide the analyzer output.

4.2.9 BIF Method 0011

All sampling procedures used in this formaldehyde testing are contained in Boilers and Industrial Furnaces Test Method 0011 and EPA 40 CFR Part 60, Appendix A. Figure 4.2.9 shows a diagram of the sampling train.

Analysis of the recovered samples for formaldehyde was performed by Mercury Research Laboratories using the procedures outlined in BIF Method 0011.

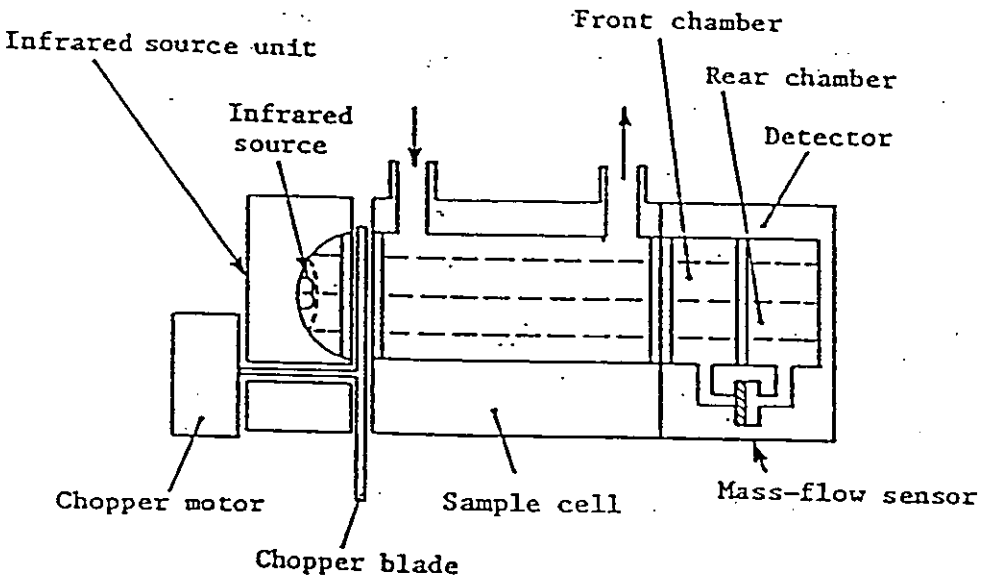

FIGURE 4.2.8.2-1
CARBON MONOXIDE ANALYER

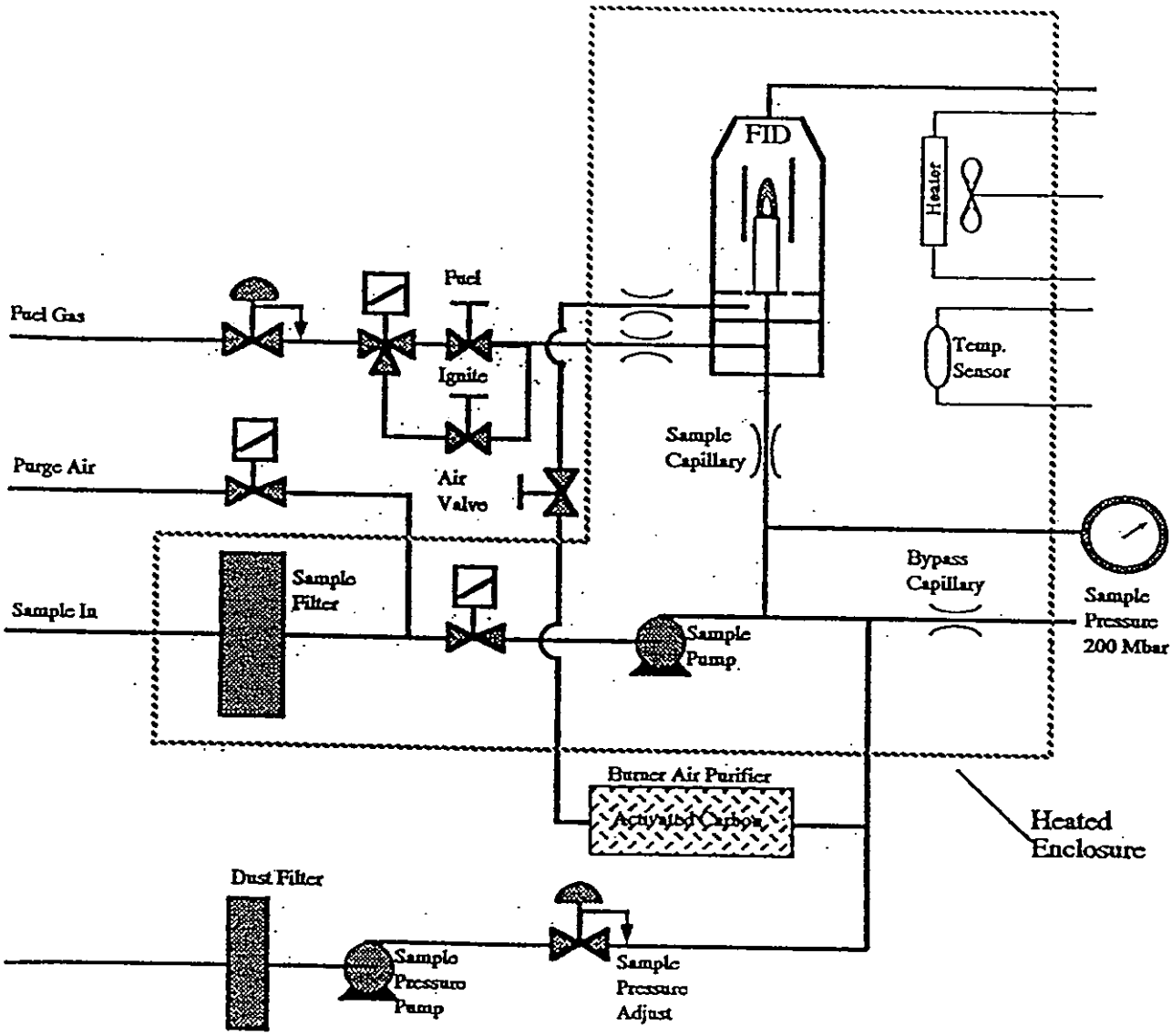

FIGURE 4.2.8.2-2
TOTAL HYDROCARBON ANALYZER

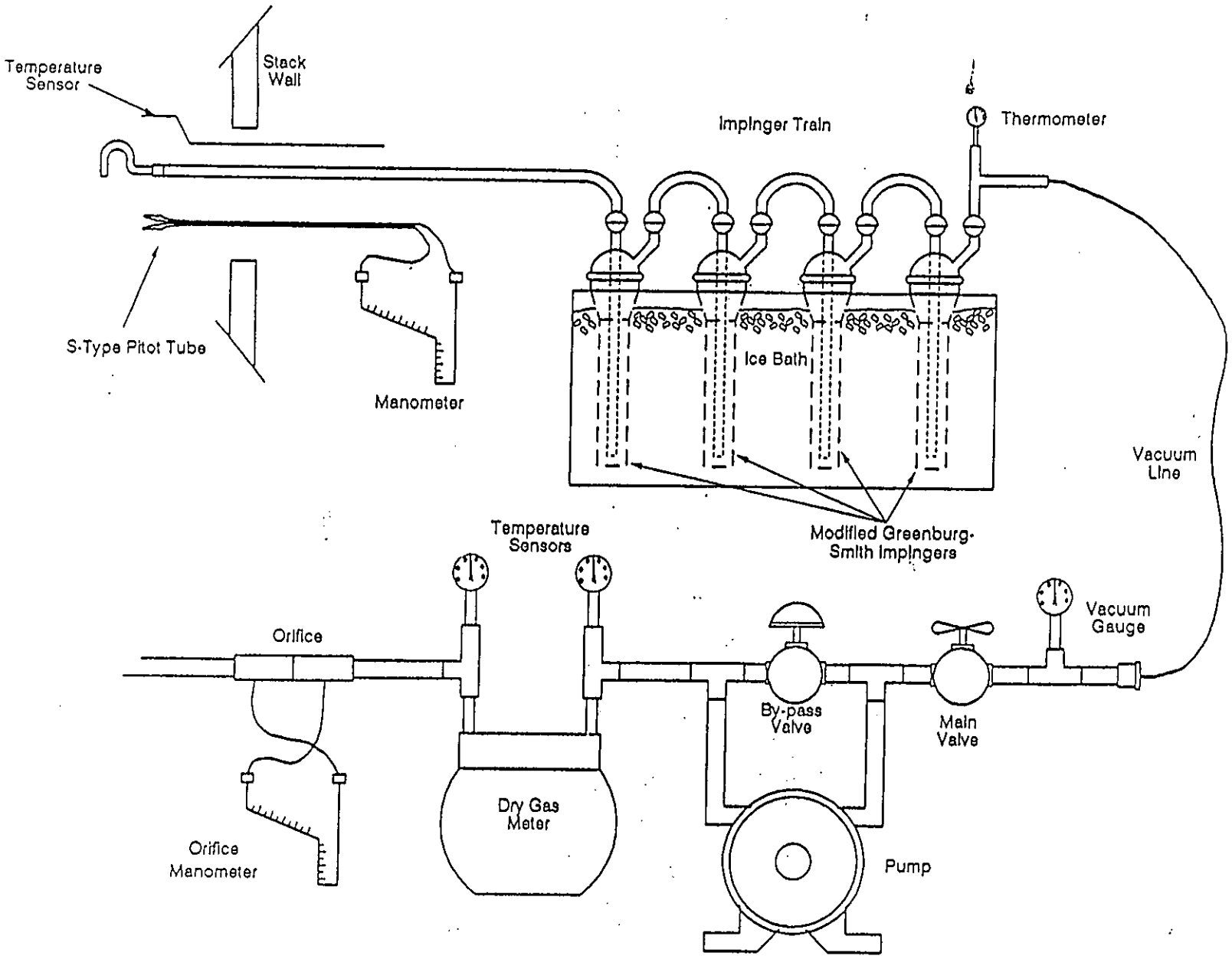

FIGURE 4.2.9
FORMALDEHYDE SAMPLE TRAIN

4.2.9.1 Sample Collection

Formaldehyde concentrations in the stack gas were determined using EPA Method 5 (Determination of Particulate Emissions from Stationary Sources and BIF Method 0011) procedures. The stack sample was withdrawn isokinetically from the source with emissions collecting in the heated probe and in a series of chilled impingers. The probe was glass coupled to a glass nozzle with a 5/8" Teflon union. Initial and final leak check rates, recovery data, and all train operation parameters for each test run were recorded on the field data sheets in Appendix D.

Impingers one and two each contained 100 ml of aqueous acidic 2,4-dinitrophenyl-hydrazine. Formaldehyde present in the emissions reacts with the 2,4-dinitrophenyl-hydrazine to form the formaldehyde dinitrophenylhydrazone derivative. The dinitrophenylhydrazone derivative is extracted, solvent-exchanged, concentrated, and then analyzed by high performance liquid chromatography (HPLC).

4.2.9.2 Sample Recovery Procedure

Upon completion of the sample run for formaldehyde, the train was carefully removed from the stack, leak-checked, and moved to the clean-up area. The probe and connecting glassware were brushed with teflon wool and rinsed with methylene chloride followed by distilled water. The probe was then rinsed while being rotated to insure complete collection. This rinse was captured in a flask modified with a ball socket to prevent sample loss. The sample was then transferred to a uniquely identified glass sample container. The collection flask was then rinsed and combined with the sample rinse.

The impinger collection contents were volumetrically determined to calculate the moisture percentage. Repeated rinses of the impingers with methylene chloride and water were performed to insure complete sample collection. The impinger contents and rinses were combined with the probe rinse. The containers were sealed and liquid levels were marked for transportation to the laboratory. Representative blank samples of the distilled water and absorbing solution were prepared as a check against potential contamination.

4.2.9.3 Analytical Procedure

Several samples contained high concentrations of formaldehyde. In some cases, almost complete derivatization of the DNPH solution occurred. Typically, 30 or 40 mg represents the maximum amount of formaldehyde that can be effectively collected with 200 ml of DNPH solution. Therefore, samples that contained more than 30 or 40 mg of formaldehyde may not represent actual concentrations due to the reduced collection efficiency of the depleted DNPH solution.

Analysis of the samples collected was in accordance to the procedures outlined in Method 0011A. This protocol is a high performance liquid chromatographic (HPLC) method optimized

for the determination of formaldehyde in aqueous environmental matrices, including stack samples collected by Method 0011.

The entire sample train is extracted with methylene chloride and the methylene chloride extract is brought to a known volume. An aliquot of the extract is solvent exchanged and concentrated or diluted as necessary.

The operating conditions for the HPLC as defined in the method are:

Column type Reverse phase C18 column
250 nm x 4.6 mm, 5um particle size
Mobile phase isocratic elution using methanol/water
(75:25, v/v)
Flow rate 1.0 mL/minute
UV Detector 360 nm
Injection Volume 20 uL

The extraction is summarized as follows:

Measure the final volume of the sample prior to extraction. Pour the sample into a separator funnel and drain the methylene chloride into a volumetric flask. Extract the aqueous solution with three aliquots of methylene chloride. Add the methylene chloride to the volumetric flask. Fill the flask to volume with methylene chloride. Mix well and remove an aliquot.

If high levels of formaldehyde are present, the sample can be diluted with mobile phase. The sample may also be concentrated if low levels are anticipated. Prior to the HPLC analysis, the sample must be solvent exchanged to methanol.

Standards are prepared from stock solutions at concentrations of 50, 20 and 10 ug/mL. Additional concentrations were prepared from these solutions at the following concentrations: 5, 0.5, 2, 0.2, 1 and 0.1 ug/mL. The calibration curve must be verified on each working day to demonstrate agreement within 10%.

4.3 DEVIATIONS FROM STANDARD METHODOLOGIES

IEA made every effort to collect and analyze all samples in accordance to standard or mutually accepted methodologies. There were few instances during which IEA made minor modifications to the standard methodologies. In every case, the impact on overall data quality was minimized whenever possible.

SECTION 5

PROJECT SPECIFIC QUALITY CONTROL MEASURES

Specific QC measures were used to ensure the generation of reliable data from sampling and analysis activities. Proper collection and organization of accurate information followed by clear and concise reporting of the data is a primary goal in all projects.

The objective of a quality assurance/quality control (QA/QC) program is to assure that the precision and accuracy of all environmental data generated by IEA are commensurate with data quality objectives (DQO's). DQO's are based on a common understanding of the intended end use(s) of the data, the measurement process, and the availability of resources. Once DQO's are established, formally or informally, QC protocol can be defined for the measurements.

In this project, the final data user will be Louisiana Pacific and the US EPA. The data quality objectives in this project are to generate legally-defensible data to be used for air permitting purposes.

Two basic concepts used in a QC program are to:

1) Control errors, and
2) Verify that the entire analytical method is operating within acceptable performance limits.

Use of qualified personnel, reliable and well-maintained equipment, appropriate calibrations and standards, and close supervision of all operations are important components of the QC system. The following sections describe the QC results for maintaining instruments and equipment in a state of calibration (defines the accuracy or bias error), results for measuring/calculating the repeatability of a measurement (defines precision, or random error), results of maintaining a state of cleanliness (eliminates interferences or contamination), and the paper trail which documents that the methods were performed to instructions, calibrated within method performance standards, and traceable to NIST standard reference materials.

5.1 FIELD DATA REDUCTION

Appendices B-E of this report presents the standardized forms that were used to record field sampling data. The data collected was reviewed in the field by the Field Team Leader. Errors or discrepancies were noted on the data sheet. Appendix A provides the calculation work sheets used in the field to check on sampling conditions and a listing of formulas to be used to reduce the field data.

5.2 LABORATORY ANALYSIS DATA REDUCTION

Analytical results were reduced to concentration units specified by the analytical procedure, using the equations given in the applicable reference method.

5.3 INTERNAL QUALITY CONTROL CHECKS AND FREQUENCY

Quality control checks were performed to ensure the collection of representative samples and the generation of valid analytical results on these samples. These checks were performed by project participants throughout the program under the guidance of the QA Director.

5.3.1 Field Sampling QC Checks and Frequency

IEA's checks for the process data collection and sampling aspects of this program included the following:

1. Use of standardized checklists and field notebooks to ensure accuracy and completeness, traceability, and comparability of the process information and samples collected.

2. Field checking of standardized forms by a second person to ensure accuracy and completeness.

3. Strict adherence to the sample traceability procedures.

4. Submission of field biased blanks.

5. Leak checks of sample trains before and after sample collection.

Calibration of the field sampling equipment was performed prior to the field sampling effort. Copies of the calibration sheets are provided in the Appendix H.

Leak checks of the sample trains were conducted in accordance with the protocol called out for each method. Leak checks were conducted prior to and at the end of each sample run.

5.3.2 Laboratory QC Check

IEA's Quality Control program for laboratory analysis makes use of a number of different types of QC samples to document the validity of the generated data. The following types of QC samples were used during the program.

- *Method Blanks* - Method blanks contain all the reagents used in the preparation and analysis of samples and are processed through the entire analytical scheme

to assess spurious contamination arising from reagents, glassware, and other materials used in the analysis.

- *Calibration Check Samples* - One of the working calibration standards is periodically used to check that the original calibration is still valid.

5.3.3 Equipment Calibration

All of the equipment used was calibrated according to the procedures outlined in the Quality Assurance Handbook for Air Pollution Measurement Systems, Volume III, EPA-600/4-77-027b.

5.3.3.1 Barometer

Barometric pressure values were obtained from a calibrated Airguide barometer, verified by phone call to a local airport, and corrected for elevation to sample port level (0.01 inches Hg per 10 ft. elevation).

5.3.3.2 Probe Nozzle

The probe nozzles used during testing were calibrated initially by the manufacturer and thereafter by the field sampling crew by checking for dimensional roundness. This was done by taking three separate measurements using alternative inside diameters and calculating the average. A micrometer with a minimum tolerance of 0.001 inch is used for measuring. If a deviation of more than 0.004 inch is found between any measurements, the nozzle is either discarded or repaired and remeasured.

5.3.3.3 Pitot Tubes

Each pitot tube used in sampling meets the design specifications for type-S pitot tubes in EPA Method 2. Therefore, a maximum value baseline coefficient (C_p) of 0.84 is assigned to each pitot tube. Calibration at the manufacturer for pitot face-opening alignment included measuring the external tubing diameter (dimension D_t), the base-to-opening plane distance (dimensions P_a and P_b), and the face opening misalignment angles, with all terms as described in Figures 2-2 and 2-3 of EPA Method 2. Pitot tubes were visually inspected for structural integrity at the completion of each test.

5.3.3.4 Calibration Meter and Metering System

The secondary reference meter equipment arrangement for calibration is shown in Figure 5.7 of EPA Method 5. The prescribed procedures were followed. A wet test meter with a 1 ft^3/rev capacity and $\pm$ 1 percent accuracy is used as the primary calibrant. The dry gas meter's pump is run for a minimum of 5 minutes at a flow rate of 0.35 cfm to condition the interior surface of the wet test meter. Leak checks are performed and if satisfactory, triplicate runs at each of no less than five different flow rates are done. A calibration curve is prepared and the meter is recalibrated after 200 hours of operation or annually, whichever comes first.

The calibration set-up for the dry gas metering system using the secondary reference meter in lieu of the wet test meter is given in Figure 5.5 of EPA Method 5. A leak check of the metering system before calibration was performed as shown in Figure 5.4 of EPA Method 5. The metering systems's pump is operated for 5 minutes at an orifice manometer setting of 0.5 inches H_20 to heat up the pump and system to stabilize the meter inlet and outlet temperatures. Values for the orifice setting (delta H), wet test meter volume (V_w), corresponding dry test meter volume (V_d) dry test meter inlet and outlet gas temperatures (t_{di} and t_{dn}), and time are recorded for the initial calibration. Then the ratio of the wet test meter to the dry test meter (gamma) and the orifice pressure differential that equates to 0.75 cfm at standard conditions (delta H@) are calculated.

A post-test meter calibration was made on the dry gas meter used during the test to check its accuracy against the pre-test calibration. This post-test calibration check was made using the average orifice setting obtained during each test run and setting the vacuum at the maximum value obtained during each test run. These test runs were made against IEA's secondary reference dry gas meter which was calibrated against a wet test meter.

5.3.3.5 Thermocouples and Digital Indicators

Thermocouples are calibrated by comparing them against an ASTM-3F mercury-in-glass thermometer at approximately 32°F (ice water), ambient temperature, approximately 100°F (hot oil). Each thermocouple is calibrated against temperature ranges to which it is typically exposed during test conditions, and they must agree within 1.5 percent (expressed in °R) of the reference thermometer throughout the entire calibration range. Also, thermocouples are checked at ambient temperature at the test site to verify calibration.

Digital indicators are checked by feeding a series of millivolt signal strengths to the input and comparing the indicator reading with the reading the signal should have generated. Acceptable calibration error must not exceed 0.5 percent when temperatures are expressed in °R.

5.3.3.6 Analytical Balance

The analytical balance is calibrated by comparing its readings against NBS Class-S1 standard weights, with acceptable agreement within 0.5 mg.

5.3.3.7 CEMS Calibrations

Calibration procedures were performed in accordance with that outlined in EPA Reference Methods. Analyzers were calibrated before and after each test. EPA Protocol #1 gases were used for calibration.

The pre-test calibrations consisted of the following two steps:

- Internal (direct to instrument) calibration of each analyzer to adjust calibration and check linearity.

- External (through the entire sampling system) calibration to check the system bias on zero and span gases.

The post-test calibration consisted of an external system bias calibration check.

The analyzer was calibrated using a certified zero and span (mid range) gas. Zero and span gases were directed to each analyzer through the appropriate plumbing, the calibration gas flow rates were adjusted to the correct flow rate and the analyzer was adjusted with the appropriate span potentiometer.

After the analyzer was properly adjusted, the linearity was checked using a low and high range calibration gas. The maximum allowable limit for linearity $\pm 2\%$ of the analyzer range. All analyzers were demonstrated to be linear within these limits.

The external calibration bias check was performed by placing the CEM system in the sampling mode and injecting a zero and span gas into the sample line at the probe exit. This check shows if there is any sampling system related bias, and also serves as a check of the sample line integrity.

5.3.3.8 Formaldehyde Analysis

Logs of all calibration curve documentation and HPLC instrument performance are provided in Appendix G. Copies of all chromatograms as provided by Mercury Research Labs are present in the attached Appendix.

5.4 BLANKS

Filter, acetone, and methylene chloride blanks were provided for gravimetric analysis as a check against potential sample contamination. All of these samples had an acceptable weight increase as allowed by the method. Due to minimal blank values, particulate samples were not blank corrected.

5.5 REAGENTS

All reagents used met or exceeded the specifications stated in the referenced methods. The use of Baker-Instra Analyzed reagents and pre-tested distilled water that was transported and stored on-site in pre-cleaned nalgene containers insured contaminant free absorbing solutions.

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REPORT NO: 192-92-49

PROJECT: 1449-001

DATE: May 29, 1992

TYPE: **APPENDICES**

EMISSION TEST RESULTS
PARTICULATE, PM_{10}, FORMALDEHYDE, VOC, CO
DRYER STACKS, PRESS VENTS, FORMER STACK AND BOILER STACKS
LOUISIANA PACIFIC CORPORATION
CLAYTON, ALABAMA

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APPENDIX A

EXAMPLE CALCULATIONS

EPA METHOD 5 CALCULATIONS

Plant LOUISIANA PACIFIC Location Sampled DRYER STACK 1

Date 5/22/92 Run No. 1 Calc By J. BURDETTE

Dry gas meter calibration factor = Y = 1.002

Volume of gas at meter conditions (ft^3) = V_m = 41.731

Average meter temperature (^oF + 460)^oR = T_m = 73.9 + 460

Barometric pressure absolute (in. Hg) = P_{bar} = 29.84

Average orifice pressure drop (in. H_2O) = ΔH = 1.60

$V_{m(std)}$ = Volume of gas sampled at the dry gas meter corrected to standard conditions (dscf)

$$V_{m(std)} = \frac{Y\,(17.64)(V_m)(P_{bar} + (\Delta H/13.6))}{(T_m)}$$

$$V_{m(std)} = \frac{(1.002)(17.64)(41.731)[(29.84)+(1.60)/13.6]}{(533.9)}$$

$V_{m(std)}$ = 41.388 dscf

Total volume of water collected (mL) = V_{lc} = 52.4

$V_{wc(std)}$ = volume of water vapor at standard conditions (scf)

$V_{wc(std)} = (0.04707)(V_{lc}) = (0.04707)(52.4) = 2.47$

Mole fraction of water vapor = B_{ws}

$$B_{ws} = \frac{V_{wc(std)}}{V_{m(std)} + V_{wc(std)}} = \frac{(2.47)}{(41.388) + (2.47)}$$

B_{ws} = 0.056

Percent moisture = $(100)(B_{ws})$ = 100 (0.056)

Percent moisture = 5.6 %

Mole fraction of dry gas = MF = 1 - (B_{ws}) = 1 - (0.056)

MF = 0.944

EPA5CALC.SHT

Percent O_2 by volume dry basis = O_2 = 20.9 %
Percent CO by volume dry basis = CO = 0 %
Percent CO_2 by volume dry basis = CO_2 = 0.0 %

Percent N_2 by volume dry basis = 100 - (O_2 + CO + CO_2)

N_2 = 100 - [(20.9)+(0)+(0)]

N_2 = 79.1 %

Molecular weight of dry gas (lb/lb-mole) = M_d

M_d = 0.44 (CO_2) + 0.32 (O_2) + 0.28 (N_2 + CO)

M_d = 0.44 (0) + 0.32 (20.9) + 0.28 (79.1 + 0)

M_d = 28.84 lb/lb-mole

Molecular weight of wet stack gas (lb/lb-mole) = M_s

M_s = (M_d) (1 - B_{ws}) + 18 (B_{ws})

M_s = (28.84) [1 - (0.056)] + 18 (0.056)

M_s = 28.23 lb/lb-mole

Percent excess air (%) = % EA

$$\% \text{ EA} = \frac{(\% O_2) - [0.5 (\% CO)]}{[0.264 (\% N_2)] - (\% O_2) - [0.5 (\% CO)]} \times 100$$

$$\% \text{ EA} = \frac{(\quad) - [0.5 (\quad)]}{[0.264 (\quad)] - (\quad) - [0.5 (\quad)]} \times 100$$

% EA = _____

Average stack temperature (^oF+460) = T_s = 112.7 + 460

Avg of sq root of velocity head (in $H_2O)^{1/2}$ = $\sqrt{\Delta p}$ = 1.672

Absolute pressure of stack gas (in. Hg) = P_s = 29.84 - 1.95/13.6
note P_s = barometric pressure (in. Hg) ± [gauge pressure (in. H_2O)/13.6]

Pitot tube coefficient, type S = C_p = 0.84

V_s = average stack gas velocity (ft/s)

$$V_s = 85.49 \times C_p \times \sqrt{\frac{T_s}{P_s \times M_s}} \times (\sqrt{\Delta p})avg$$

$$V_s = 85.49 \times (0.84) \times \sqrt{\frac{(572.7)}{(29.70) \times (28.2)}} \times (1.672)$$

V_s = 99.3 ft/s

Area of stack (ft^2) = A = 9.62

Testing time (min) = θ = 60

Volumetric gas flow rate in stack (dscfm) = Q_{sd}

$$Q_{sd} = 60 \times (1 - B_{ws}) \times V_s \times A \times (528/T_s) \times (P_s/29.92)$$

$$Q_{sd} = 60 \times (1 - 0.056) \times (99.3) \times (9.62) \times \left(\frac{528}{572.7}\right) \times \left(\frac{29.70}{29.92}\right)$$

Q_{sd} = 49,500 dscfm

Diameter of sampling nozzle (in.) = d_n = 0.155

Area of nozzle (ft^2) = A_n = 54.54E-4 $(d_n)^2$

A_n = (0.005454) $(0.155)^2$ = 1.31×10^{-4} ft^2

Isokinetic sampling rate (%) = I

$$I = \frac{100\ T_s[0.002669\ V_{lc} + (V_m\ Y/T_m)(P_{bar} + \Delta H/13.6)]}{60\ \theta\ V_s\ P_s\ A_n}$$

$$I = \frac{100\ (572.7)[0.00267(52.4) + ((41.731)(1.002)/(533.9))((29.24) + (1.60)/13.6)]}{60\ (60)(99.3)(29.70)\ 1.31 \times 10^{-4}}$$

I = 102.3 %

Particulate catch, front half (mg) (Filterable) 50.1 mg 119.8 mg = M_p = 169.9

Particulate catch, total (mg) (Filterable & Condensible) 2.8 mg 4.9 mg = M_t = 177.6

Particulate concentration, front half (gr/dscf) = C_{AP}

$C_{AP} = (0.0154)(M_p)/(V_{m(std)}) = (0.0154)(169.9)/(41.388)$

C_{AP} = 0.063 gr/dscf

Particulate concentration, total (gr/dscf) = C_{AT}

$C_{AT} = (0.0154)(M_t)/(V_{m(std)}) = (0.0154)(177.6)/(41.388)$

C_{AT} = 0.066 gr/dscf

Particulate concentration, front half (lb/dscf) = C_{BP}

$C_{BP} = (2.205E-6)(M_p)/(V_{m(std)}) = (2.205E-6)(169.9)/(41.388)$

C_{BP} = 9.05×10^{-6} lb/dscf

Particulate concentration, total (lb/dscf) = C_{BT}

$C_{BT} = (2.205E-6)(M_t)/(V_{m(std)}) = (2.205E-6)(177.6)/(41.388)$

C_{BT} = 9.46×10^{-6} lb/dscf

Emission rate front half (lb/hr) = E_p

$E_p = (60)(C_{BP})(Q_{sd}) = (60)(9.05 \times 10^{-6})(49,500)$

E_p = 26.9 lb/hr

Emission rate total (lb/hr) = E_T

$E_T = (60)(C_{BT})(Q_{sd}) = (60)(9.46 \times 10^{-6})(49,500)$

E_T = 28.1 lb/hr

PM$_{10}$ EXAMPLE CALCULATIONS

Dryer stack 8 Run 2

Barometric pressure, P_{bar}, in. Hg = 29.84

Stack static pressure, P_g, in. H_2O = -1.95

Average stack temperature, t_s, °F = 127.7

Meter temperature, t_m, °F = 52.5

Orifice ΔH_a, in. H_2O = 1.92

Gas analysis:

$\%CO_2$ = 0

$\%O_2$ = 20.9

$\%N_2 + \%CO$ = 79.1

Fraction moisture content, B_{ws} = 8.3

Molecular weight of stack gas, dry basis:

$$M_d = 0.44(\%CO_2) + .32(\%O_2) + 0.28(\%N_2 + \%CO) = \underline{28.84} \text{ lb/lb mole}$$

Molecular weight of stack gas, wet basis:

$$M_w = M_d(1 - B_{ws}) + 18(B_{ws}) = \underline{27.9} \text{ lb/lb mole}$$

Absolute stack pressure:

$$P_s = P_{bar} + \frac{P_g}{13.6} = \underline{29.7} \text{ in. Hg}$$

Viscosity of stack gas:

$$\mu_s = 152.418 + 0.2552\ t_s + 3.2355 \times 10^{-5}\ t_s^2 + 0.53147\ (\%O_2) - 74.143\ B_{ws} = \underline{190} \text{ micropoise}$$

Cyclone flow rate:

$$Q_s = 0.002837\ \mu_s \left(\frac{t_s + 460}{M_w\ P_s}\right)^{0.2949} = \underline{0.487} \text{ ft}^3/\text{min}$$

Figure 4. Example worksheet 1 (Page 1 of 2), cyclone flow rate and ΔH.

DS8-2
PM10

Orifice pressure head (ΔH) needed for cyclone flow rate:

$$\Delta H = \left[\frac{Q_s(1-B_{ws})P_s}{t_s + 460}\right]^2 \frac{(t_m + 460)\ M_d\ (1.083)\ \Delta H_a}{P_{bar}} = \underline{0.52}\ \text{in. } H_2O$$

Calculate ΔH for three temperatures:

t_s, °F	77.7	127.7	177.7
ΔH, in. H_2O	0.62	0.52	0.44

Figure 4. Example worksheet 1 (Page 2 of 2), cyclone flow rate and ΔH.

DS8-2

Stack viscosity, μ_s, micropoise = 188.85
Absolute stack pressure, P_s, in. Hg = 29.70
Average stack temperature, t_s, °F = 127.7
Meter temperature, t_m, °F = 52.5
Method 201A pitot coefficient, C_p = 0.84
Cyclone flow rate, ft^3/min, Q_s = 0.484
Method 2 pitot coefficient, C_p = 0.84
Molecular weight of stack gas, wet basis, M_w = 27.9
Nozzle diameter, D_n, in. = 0.133

Nozzle velocity

$$v_n = \frac{3.056\ Q_s}{D_n^2} = \underline{83.612}\ \text{ft/sec}$$

Maximum and minimum velocities:

Calculate R_{min}.

$$R_{min} = 0.2457 + \sqrt{0.3072 - \frac{0.2603\ (\sqrt{Q_s}\ )\ \mu_s}{v_n^{1.5}}} = \underline{0.758}$$

If R_{min} is less than 0.5, <u>or</u> if an imaginary number occurs when calculating R_{min}, use Equation 1 to calculate v_{min}. Otherwise, use Equation 2.

Eq. 1 $\quad v_{min} = v_n\ (0.5) = \underline{41.81}$ ft/sec

Eq. 2 $\quad v_{min} = v_n\ R_{min} = \underline{63.38}$ ft/sec ✓

Calculate R_{max}.

$$R_{max} = 0.4457 + \sqrt{0.5690 + \frac{0.2603\ (\sqrt{Q_s}\ )\ \mu_s}{v_n^{1.5}}} = \underline{1.229}$$

Figure 5. Example worksheet 2 (page 1 of 2), nozzle selection.

If R_{max} is greater than 1.5, use Equation 3 to calculate v_{max}. Otherwise, use Equation 4.

Eq. 3 $\quad v_{max} = v_n\ (1.5) =$ 125.42 ft/sec

Eq. 4 $\quad v_{max} = v_n\ R_{max} =$ 102.77 ft/sec ✓

Maximum and minimum velocity head values:

$$\Delta p_{min} = 1.3686 \times 10^{-4}\ \frac{P_s\ M_w\ (v_{min})^2}{(t_s + 460)\ C_p^2} = \underline{1.10}\ \text{in. } H_2O$$

$$\Delta p_{max} = 1.3686 \times 10^{-4}\ \frac{P_s\ M_w\ (v_{max})^2}{(t_s + 460)\ C_p^2} = \underline{2.89}\ \text{in. } H_2O$$

Nozzle Number	1	2	3	4
D_n, in.	0.133	0.161	0.182	0.196
v_n, ft/sec	83.6	57.06	44.6	38.5
v_{min}, ft/sec	63.4	41.3	30.6	25.1
v_{max}, ft/sec	102.8	71.4	56.8	49.7
Δp_{min}, in. H_2O	1.10	0.47	0.26	0.17
Δp_{max}, in. H_2O	2.89	1.40	0.88	0.68

Velocity traverse data:

$$\Delta p(\text{Method 201A}) = \Delta p(\text{Method 2}) \left(\frac{C_p'}{C_p}\right)^2$$

Figure 5. Example worksheet 2 (page 2 of 2), nozzle selection.

DS8-2

Total run time, minutes = 60

Number of traverse points = 12

$$t_1 = \sqrt{\frac{\Delta p_1'}{\Delta p_{avg}'}} \left(\frac{\text{Total run time}}{\text{Number of points}} \right)$$

where:

t_1 = dwell time at first traverse point, minutes.

$\Delta p'_1$ = the velocity head at the first traverse point (from a previous traverse), in. H_2O.

$\Delta p'_{avg}$ = the square of the average square root of the Δp's (from a previous velocity traverse), in. H_2O.

At subsequent traverse points, measure the velocity Δp and calculate the dwell time by using the following equation:

$$t_n = \frac{t_1}{\sqrt{\Delta p_1}} \sqrt{\Delta p_n}, \text{ where } n = 2,3,\ldots.\text{total number of sampling points}$$

where:

t_n = dwell time at traverse point n, minutes.

Δp_n = measured velocity head at point n, in. H_2O.

Δp_1 = measured velocity head at point 1, in. H_2O.

Figure 6. Example worksheet 3 (page 1 of 2), dwell time.

DS8-2

Port No A Port No B Port No_____ Port No_____

Point Number	Δp	t	Δp	t	Δp	t	Δp	t
1	2.1	4.83	1.8	4.47				
2	2.3	5.06	2.3	5.06				
3	2.4	5.16	2.5	5.27				
4	2.4	5.16	2.3	5.06				
5	2.1	4.83	2.3	5.06				
6	2.3	5.06	1.8	4.47				

Figure 6. Example worksheet 3 (page 2 of 2), dwell time.

APPENDIX B

PARTICULATE (including condensibles) FIELD AND RECOVERY DATA

DRYER STACKS

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL.	3/13/92	Dryer Stack # 1	M-5/M 202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terll	29.84	-.95	52°	F 340	42"	0.84	4 B Glass	#05	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-1	1.87	1.002	4-B	T-4B	H-4	—	15	0.000	15	0.000	0.57

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite	%O2	20.9					✓	✓
Analysis Method		%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	11.01	717.512	2.20	1.26	107	247	246	59	72	—	2
2	2½		719.009	2.40	1.37	113	247	247	66	74	—	2
3	5		720.801	2.60	1.48	114	246	246	55	73	—	2
4	7½		722.308	2.90	1.65	116	246	246	50	73	—	2
5	10		723.808	2.60	1.48	117	246	246	51	73	—	2
6	12½		725.504	2.90	1.65	115	250	249	51	74	—	3
7	15		727.204	2.70	1.54	114	250	249	53	75	—	4
8	17½		728.905	2.90	1.65	111	250	249	53	73	—	4
9	20		730.630	3.10	1.76	110	250	250	53	73	—	4
10	22½		732.210	3.20	1.82	112	250	250	53	72	—	4
11	25		734.005	3.20	1.82	112	250	250	56	74	—	6
12	27½		735.910	3.30	1.88	116	250	250	56	76	—	7
	30/off		737.722									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3-13-92	Dryer Stack # 1	M5 / M202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B 1	30/0		737.722	2.00	1.14	107	248	245	57	73	—	3
2	2½		739.267	2.10	1.19	113	248	245	53	75	—	3
3	5		740.702	2.60	1.48	112	248	245	53	75	—	3
4	7½		742.303	2.80	1.60	114	248	245	53	74	—	3
5	10		744.310	2.90	1.65	113	249	247	52	75	—	3
6	12½		745.607	3.10	1.76	113	250	247	52	75	-	4
7	15		747.402	3.00	1.71	113	250	247	52	75	-	4
8	17½		749.202	2.50	1.42	111	250	247	51	74	—	5
9	20		750.910	3.00	1.71	113	250	248	51	74	-	5
10	22½		752.801	3.00	1.71	113	250	248	51	74	-	5
11	25		754.208	3.30	1.88	113	250	248	51	74	-	5
12	27½		756.002	3.10	1.76	112	250	248	51	74	-	5
	Off	12:13	757.777									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		40.265	1.672	1.549	112.7	

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

J. Thompson (3/26/92)

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL.	3/12/92	Dryer Stack # 1	M-5 / M 202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrill	29.84	-.95	52°	F-342	42"	0.84	4-6 Glass	D-5	.155

ASSUMED MOIST (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	T-4-C	3	H-3	–	0.050	0.000	12	0.004	0.57

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite	%O2	20.9					✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0/0	13:33	757.935	2.80	1.60	117	247	251	52	60	–	3
2	2½		759.510	2.10	1.19	114	247	251	50	61	–	3
3	5		761.001	2.70	1.54	117	249	251	50	61	–	3
4	7½		762.602	2.80	1.60	119	250	251	49	65	–	3
5	10		764.302	2.90	1.65	120	245	252	50	63	–	3
6	12½		766.106	3.20	1.82	120	245	250	47	65	–	4
7	15		767.905	3.40	1.93	119	245	250	47	65	–	5
8	17½		769.905	2.60	1.48	118	245	250	47	65	–	5
9	20		771.504	2.70	1.54	121	245	250	47	65	–	5
10	22½		773.203	3.20	1.82	120	245	250	49	65	–	5
11	25		774.899	3.50	1.99	120	245	250	50	65	–	8
12	27½		776.801	3.70	2.10	120	245	250	50	65	–	10
	30/OFF		778.475									

Down - 13:42
Start - 14:26

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3-13-92	Dryer Stack #1	M-5/M202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP (F)	SAMPLE TRAIN ACUU (In. Hg)
A-1	30/0		778.475	2.50	1.42	120	250	250	56	61	–	5
2	2½		780.105	2.30	1.31	120	250	250	56	61	–	5
3	5		781.205	3.50	1.99	120	250	250	53	62	–	10
4	7½		783.405	3.70	2.10	120	250	250	53	62	–	10
5	10		785.302	2.80	1.60	120	250	250	53	62	–	6
6	12½		787.103	2.80	1.60	120	250	250	56	63	–	7
7	15		788.902	3.20	1.82	122	250	250	56	63	–	9
8	17½		790.201	2.80	1.60	120	250	250	56	63	–	6
9	20		792.001	3.20	2.10	120	250	250	56	63	–	6
10	22½		793.707	3.50	1.99	121	250	250	56	63	–	6
11	25		795.706	3.50	1.99	120	250	250	56	63	–	6
12	27½		797.705	3.50	1.99	120	250	250	56	63	–	6
	60/OFF	15:27	799.211									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	41.276	1.7325	1.74	119.5	63.1

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton	3/1/92	Dryer Stack #1	M-5 / M 202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrill	29.84	-0.95	55°	F-341	42"	0.84	B-4 Glass	#05	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	F-134	4	H-4	—	8.15	0.000	10	0.000	0.57

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite	%O2	20.9					✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0	16:15	799.401	2.30	1.31	114	247	249	50	61	—	2
2	2½		801.110	2.60	1.48	114	251	249	50	61	—	2
3	5		802.700	3.00	1.71	114	251	249	50	61	—	3
4	7½		804.206	3.10	1.76	114	251	249	50	61	—	3
5	10		806.006	3.20	1.82	114	251	249	52	61	—	4
6	12½		807.010	3.00	1.71	115	251	249	52	61	—	4
7	15		809.708	2.70	1.54	114	250	250	52	61	—	4
8	17½		811.406	3.00	1.71	114	250	250	52	61	—	4
9	20		813.102	3.30	1.88	114	251	250	53	60	—	5
10	22½		814.999	3.50	1.99	114	251	251	53	60	—	5
11	25		816.607	3.50	1.99	114	251	251	53	60	—	5
12	27½		817.508	3.40	1.94	114	251	250	53	60	—	6
	30		819.325									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LA-PACIFIC, AL.	3/13/92	DRYER STACK # 1	M-5/M202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
B-1	30/2½		819.325	2.30	1.31	113	249	251	51	59	–	2
2	5		821.000	2.40	1.36	114	250	251	51	59	–	2
3	7½		822.502	2.50	1.42	114	250	251	51	59	–	2
4	10		824.109	2.70	1.54	115	250	249	51	58	–	3
5	12½		825.707	3.00	1.71	115	250	249	51	58	–	4
6	15		827.605	3.20	1.82	113	250	249	51	58	–	4
7	17½		829.208	3.10	1.76	112	250	249	51	58	–	4
8	20		831.007	2.80	1.60	112	250	249	51	58	–	4
9	22½		832.703	2.50	1.42	112	250	249	51	58	–	4
10	25		834.402	2.70	1.54	112	250	249	51	58	–	4
11	27½		835.999	3.30	1.88	112	250	249	50	58	–	4
12	30		837.705	3.30	1.88	112	250	249	50	58	–	5
	OFF/60	17.25	838.564									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	39.163	1.7093	1.67	113.5	59.3

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L-P Stack #1 DRYER Sampling Date(s): 3/13/92

RUN No.: #1 Recovery Date: 3/13/92 Recovered By: BR

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	606.1	603.8	469.2				689.9
Initial Wt.	586.5	585.0	466.8				678.3
Net Weight	19.6	18.8	2.4				11.6

Total Moisture = 52.4 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: 10 %
Filter I.D. No.: F340 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: #2 Recovery Date: 3/13/92 Recovered By: BR

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	597.1	584.7	460.2				711.1
Initial Wt.	569.9	574.0	457.9				698.9
Net Weight	27.2	10.7	2.3				12.2

Total Moisture = 52.4 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F342 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: #3 Recovery Date: Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	586.6	573.5	469.5				699.6
Initial Wt.	565.9	564.3	466.0				689.9
Net Weight	20.7	9.2	3.5				9.7

Total Moisture = 43.1 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F341 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA Pacific CLATON, AL	3/26/92	DRYER STACK #2	M5/M-202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrill	29.84	-1.95	50°	F-~~342~~ 343	42"	0.84	4-C GLASS	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	4C	HCT	H-3	—	15	0.003	15	0.000	0.57

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite	%O2	20.9					✓	✓
Analysis Method		%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0/0	18:32	838.681	2.10	1.19	114	250	247	52	50	—	2
2	2½		840.210	2.80	1.60	114	250	247	52	50	—	3
3	5		841.707	3.10	1.76	116	250	247	50	51	—	5
4	7½		843.510	3.20	1.82	117	250	247	50	51	—	5
5	10		845.108	3.30	1.88	118	250	247	50	52	—	5
6	12½		846.909	3.50	1.99	118	250	247	50	52	—	6
7	15		848.708	3.40	1.94	118	250	247	50	52	—	6
8	17½		850.610	2.90	1.65	117	250	247	50	52	—	6
9	20		852.303	2.80	1.60	117	250	247	50	53	—	6
10	22½		854.103	3.00	1.71	117	250	248	50	53	—	6
11	25		855.810	3.40	1.94	117	250	248	50	53	—	6
12	27½		857.510	3.40	1.94	116	250	249	50	53	—	6
	30/OFF	19:36	859.131									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/13/92	Dryer STACK #2	M-5 / M 202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A 1	30/0		859.131	2.60	1.48	115	248	250	50	53	—	4
2	2½		860.802	2.90	1.65	115	248	250	50	54	—	4
3	5		862.408	3.30	1.88	115	249	250	50	54	—	4
4	7½		864.106	3.90	2.22	114	250	250	50	54	—	4
5	10		865.905	3.90	2.22	115	250	250	50	54	—	8
6	12½		868.000	3.80	2.16	116	250	250	50	54	—	6
7	15		869.705	3.10	1.76	116	250	250	50	54	—	6
8	17½		871.405	3.40	1.94	116	250	250	50	54	—	6
9	20		873.102	3.70	2.10	116	250	250	50	50	—	7
10	22½		874.910	3.90	2.22	116	250	250	50	50	—	7
11	25		876.801	3.90	2.22	116	250	249	50	50	—	7
12	27½		878.705	3.90	2.22	116	250	249	50	50	—	7
	60/OFF	2002	879.555									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	40.874	1.812	1.88	116	52.2

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL.	3/14/92	Dryer Stack # 2	M-5 / M202	2

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrill	29.89	- 2.0	57°	F-344	42"	0.84	4 ft - Glass	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	TB4	HBT	H-4	—	15	0.001	10	0.000	.57

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Fyrite	%O2	20.9					✓	✓
Analysis Method:	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A 1	0/0	0.853	879.708	2.50	1.42	124	245	247	45	66	—	2
2	2½		881.502	2.60	1.48	127	247	253	50	66	—	2
3	5		883.110	3.40	1.94	129	247	249	43	66	—	2
4	7½		884.908	3.50	1.99	129	249	251	43	66	—	3
5	10		886.707	3.60	2.05	130	249	251	44	66	—	4
6	12½		888.808	3.60	2.05	129	249	251	44	66	—	4
7	15		890.510	3.00	1.71	126	249	251	44	66	—	4
8	17½		892.308	3.30	1.88	125	250	251	45	68	—	5
9	20		894.109	3.60	2.05	125	250	251	45	68	—	7
10	22½		895.602	3.70	2.11	124	250	251	45	68	—	7
11	25		898.501	3.70	2.11	126	250	251	45	69	—	5
12	27½		900.006	3.80	2.16	125	250	251	45	69	—	5
	30/OFF		902.492									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton	3-14-92	Dryer stack # 2	M-5-/M202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		902.892	2.20	1.25	128	250	250	54	70	–	3
2	2½		904.105	2.70	1.54	125	250	250	54	70	–	3
3	5		905.708	3.00	1.71	125	250	250	54	70	–	3
4	7½		907.504	3.60	2.05	125	250	250	53	70	–	4
5	10		909.410	3.40	1.93	127	250	250	53	70	–	4
6	12½		911.207	3.40	1.93	127	250	250	53	70	–	4
7	15		913.105	3.50	1.99	127	251	250	53	72	–	4
8	17½		915.005	3.50	1.99	127	250	250	53	72	–	5
9	20		916.910	2.90	1.65	127	250	250	53	72	–	6
10	22½		918.702	3.00	1.71	128	250	250	53	72	–	6
11	25		920.307	2.50	1.42	128	250	250	53	72	–	7
12	27½		921.907	2.40	1.37	127	250	250	53	72	–	7
	W/OFF	09:58	922.876									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F.	AVG DGM F
	60	43.168	1.779	1.81	126.5	69

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL.	3/14/92	~~M-5 - M 202~~ Dryer Stack #2	M-5/M 202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrill	29.89	-2.0	64°	F-343	42"	0.84	4-C	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	T-4C	4-C	14-3	—	15	0.000	10	0.000	.57

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Fyrite	%O2	20.9					✓	✓
Analysis Method:	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0/0	11:33	923.004	2.50	1.42	119	248	249	64	79	—	4
2	2½		924.704	2.90	1.65	127	249	250	64	79	—	4
3	5		926.405	3.30	1.88	129	249	250	64	79	—	4
4	7½		928.205	3.20	1.82	131	249	250	64	79	—	6
5	10		929.999	3.20	1.82	131	249	250	60	81	—	6
6	12½		931.910	3.40	1.93	130	249	250	60	81	—	6
7	15		934.100	3.40	1.93	130	250	250	60	81	—	6
8	17½		935.606	2.70	1.54	132	250	250	60	81	—	6
9	20		937.410	2.70	1.54	133	250	250	60	80	—	6
10	22½		939.110	3.00	1.71	132	250	250	60	80	—	6
11	25		940.910	3.20	1.82	132	250	250	60	79	—	7
12	27½		942.602	3.20	1.82	132	250	250	60	78	—	7
	30/OFF		944.307									

1134. STOP PLANT Problem

START 12:19

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific, Clayton, AL	3-14-92	Dryer Stack #2	M-5/M202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A 1	30/0		944.707	2.10	1.19	130	250	250	62	76	-	4
2	2½		947.701	2.70	1.54	131	250	250	62	76	-	4
3	5		946.807	3.40	1.93	130	250	250	62	76	-	5
4	7½		948.507	3.20	1.82	130	250	250	62	79	-	5
5	10		950.401	3.50	1.99	131	249	248	60	79	-	5
6	12½		952.207	3.50	1.99	132	249	248	60	78	-	6
7	15		953.505	3.20	1.82	130	249	248	60	78	-	6
8	17½		955.403	3.50	1.99	132	249	248	60	78	-	7
9	20		957.306	3.60	2.05	131	249	249	60	79	-	7
10	22½		959.310	3.70	2.11	130	249	249	60	79	-	7
11	25		961.202	3.60	2.05	131	249	249	60	79	-	7
12	27½		963.102	3.50	1.99	130	249	249	60	79	-	7
	60/OFF	13:25	964.694									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	41.69	1.778	1.81	130.3	78.9

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L-P Stack #2 DRYER Sampling Date(s): 3/14/92

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	613.2	583.5	460.0				722.3
Initial Wt.	585.1	577.1	461.0				711.1
Net Weight	28.1	6.4	-1.0				11.2

Total Moisture = 44.7 grams

Description of Impinger Contents: _____
Silica Gel Color: F343 Percent Spent: _____ %
Filter I.D. No.: _____ Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	620.2	594.4	467.4				708.0
Initial Wt.	578.9	588.5	466.5				699.6
Net Weight	41.3	5.9	0.9				8.4

Total Moisture = 56.5 grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: F344 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	632.2	578.8	459.6				731.7
Initial Wt.	591.4	572.6	459.0				722.4
Net Weight	40.8	6.2	0.6				9.3

Total Moisture = 56.9 grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: F345 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL.	3/1/92	Dryer Stack # 3	M-5/M202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. TERLL	29.84	-1.95	57	F.3-44 3/6	42"	0.84	4 B GLASS	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	T34	B4T	H4	-	15	0.005	15	0.000	0.57

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Tyrite Grab	%O2	20.9					✓	✓
Analysis Method:	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	15:16	964.917	1.50	0.85	123	252	247	55	75	-	2
2	2½		966.205	1.70	0.97	124	252	247	55	74	-	2
3	5		967.504	1.90	1.08	125	252	247	55	74	-	2
4	7½		968.607	2.30	1.31	126	252	249	55	73	-	2
5	10		969.708	2.40	1.37	126	252	249	55	75	-	4
6	12½		971.502	2.40	1.37	127	252	249	55	75	-	4
7	15		972.901	2.50	1.42	127	251	250	55	75	-	4
8	17½		974.501	2.40	1.37	126	251	250	55	75	-	4
9	20		976.006	2.50	1.42	126	251	250	55	76	-	5
10	22½		977.609	2.70	1.54	125	251	250	55	76	-	5
11	25		979.305	2.70	1.54	125	251	250	55	76	-	5
12	27½		981.004	2.70	1.54	126	251	250	55	76	-	5
	30/off		982.551									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/14/92	Dryer Stack # 2	M5/M202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		982.551	1.90	1.08	121	250	249	56	75	—	2
2	2½		984.107	2.40	1.37	121	250	249	56	75	—	2
3	5		985.610	2.50	1.42	124	250	249	56	75	—	2
4	7½		987.205	2.50	1.42	124	250	249	56	75	—	2
5	10		988.810	2.80	1.59	125	250	249	56	75	—	4
6	12½		990.405	3.00	1.71	125	250	249	56	75	—	4
7	15		992.201	2.40	1.37	123	250	249	56	75	—	4
8	17½		993.605	2.80	1.59	124	250	249	56	75	—	4
9	20		995.105	2.80	1.59	124	250	249	56	75	—	4
10	22½		996.902	3.00	1.71	123	250	249	56	75	—	4
11	25		998.505	2.80	1.59	123	250	249	56	75	—	4
12	27½		000.305	2.80	1.59	123	250	249	56	75	—	4
	60/OFF	16:23	1001.404									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/14/92	DRYER STACK #3	M-5 / M202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terll	29.84	-1.95	57	F-347	42"	0.84	4-C GLASS	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	T.4C	4-C	H-3	–	15	0.004			.57

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB Fyrite	%O2	20.9					✓	
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
~~B~~ 1	0/0	15:44 17:44	00 2.708	1.90	1.08	~~124~~	256	246	60	72	–	2
2	2½		00 4.302	2.60	1.48	124	255	246	60	72	–	2
3	5		00 4.905	2.90	1.65	125	255	246	60	72	–	4
4	7½		0 7.109	3.00	1.71	125	255	246	60	72	–	4
5	10		0 8.907	3.00	1.71	125	255	246	60	72	–	4
6	12½		10.606	2.90	1.65	125	255	246	60	72	–	4
7	15		12.302	3.10	1.77	125	255	246	60	73	–	5
8	17½		14.102	3.10	1.77	125	255	246	60	73	–	5
9	20		15.810	3.30	1.88	124	255	246	60	73	–	5
10	22½		17.310	3.50	1.99	124	255	246	60	73	–	5
11	25		19.110	3.40	1.94	124	255	246	61	73	–	5
12	27½		21.101	2.70	1.54	124	255	246	61	73	–	5
	30 OFF		22.418	~~1.50~~								

Stopped Test Plugged Noz

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/14/92	Dryer Stack #3	M5/M202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A-1	30/0		22.418	1.50	0.85	122	255	250	61	71	–	2
2	2½		23.801	2.00	1.14	126	255	250	61	71	–	4
3	5		25.005	2.10	1.19	126	255	250	61	71	–	4
4	7½		26.506	2.40	1.37	126	255	250	62	72	–	5
5	10		27.806	3.10	1.77	126	255	250	62	72	–	5
6	12½		29.508	2.50	1.42	128	255	250	62	73	–	5
7	15		31.109	2.50	1.42	128	255	250	62	73	–	5
8	17½		32.750	2.40	1.37	127	250	250	62	73	–	5
9	20		34.410	2.70	1.54	127	250	250	62	73	–	5
10	22½		36.005	2.90	1.65	127	250	250	62	73	–	5
11	25		37.710	3.10	1.77	127	250	250	62	73	–	5
12	27½		39.405	3.10	1.77	127	250	250	62	73	–	5
	60/OFF	18:48	41.234									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L-P Stack #3 Sampling Date(s): _____

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	612.5	594.8	469.2	X	X	X	716.5
Initial Wt.	585.1	585.7	466.6	X	X	X	708.0
Net Weight	27.4	9.1	2.6	X	X	X	8.5

Total Moisture = 47.6 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: F346 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	634.4	579.8	458.5	X	X	X	740.5
Initial Wt.	596.0	573.3	457.1	X	X	X	731.7
Net Weight	38.4	6.5	1.4	X	X	X	8.8

Total Moisture = 55.1 grams

Description of Impinger Contents: clear

Silica Gel Color: Blue-White 50% Percent Spent: 50 %

Filter I.D. No.: F347 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: _____ Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.							
Initial Wt.							
Net Weight							

Total Moisture = _____ grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: _____ Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/1/92	Dryer Stack # 4	M-5/M 202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terll	30.05	- 2.0	50	F-348	42"	0.84	6-4	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	T-4	T-4	TH-4	—	15	0.000	10	0.000	0.57

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Grab Fyrite	%O2	20.9					✓	✓
Analysis Method:	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	0903	41.902	2.50	1.42	130	252	247	45	51	—	3
2	2½		43.601	3.00	1.71	132	252	247	45	53	—	3
3	5		45.210	2.70	1.54	134	252	247	45	55	—	3
4	7½		46.807	3.00	1.71	134	252	247	45	57	—	3
5	10		48.005	3.10	1.77	133	252	247	45	58	—	3
6	12½		49.802	3.10	1.77	135	252	248	45	62	—	3
7	15		51.603	2.80	1.60	134	252	248	43	62	—	3
8	17½		53.306	2.60	1.48	134	252	248	43	62	—	3
9	20		55.110	2.70	1.54	135	252	248	43	62	—	3
10	22½		56.710	2.60	1.48	134	252	248	43	62	—	4
11	25		58.03	2.70	1.54	135	250	248	43	66	—	4
12	27½		59.604	2.60	1.48	132	250	248	43	64	—	4
	30 off		60.615									

922 STOP Nozzle Plug

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL.	3-16-92	Dryer Stack # 4	M-5 - / M 202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B 1	30/0		60.6.15	1.90	1.08	124	250	249	47	64	-	2
2	2½		62.105	1.70	0.97	129	250	249	47	66	-	2
3	5		63.510	2.00	1.14	131	250	249	47	66	-	2
4	7½		65.002	2.40	1.37	132	250	249	47	66	-	2
5	10		66.499	2.50	1.42	132	250	249	47	66	-	2
6	12½		68.109	2.80	1.60	135	250	249	47	66	-	3
7	15		69.808	2.80	1.60	132	250	249	47	64	-	3
8	17½		71,110	2.80	1.60	132	250	249	47	64	-	3
9	20		71.410	2.70	1.54	134	250	249	47	66	-	3
10	22½		72.809	2.90	1.65	134	250	249	47	67	-	3.5
11	25		74.508	3.00	1.71	134	250	249	47	68	-	3.5
12	27½		76.305	3.00	1.71	134	250	249	47	68	-	3.5
	60/OFF	10:16	78.086									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/6/92	Dryer Stack # 4	M-5/M 202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terll	30.05	-2.00	50	F-349	42"	0.84	B-4	D-5	*8.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	T-34	B4	H-3	—	15	0.006	7	0.003	0.57

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Grab Fyrite	%O2	20.9					✓	✓
Analysis Method:	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0/0	10:53	78.347	1.80	1.03	127	249	250	39	71	—	3
2	2½		80.407	2.00	1.14	130	249	250	42	71	—	3
3	5		82.103	2.40	1.37	131	249	250	45	73	—	4
4	7½		83.710	2.50	1.42	130	249	250	45	73	—	4
5	10		85.275	2.70	1.54	132	249	250	47	72	—	4
6	12½		86.901	3.00	1.71	129	249	250	48	72	—	4
7	15		88.602	3.30	1.88	132	249	250	49	72	—	4
8	17½		90.408	2.80	1.60	130	250	250	49	72	—	4
9	20		92.105	2.80	1.60	130	250	250	50	73	—	4
10	22½		93.802	2.80	1.60	128	250	250	50	72	—	4
11	25		94.504	3.00	1.71	129	250	250	50	72	—	5
12	27½		96.110	3.00	1.71	130	250	250	50	72	—	5
	30/OFF		97.783									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/6/92	Dryer STACK # 4	M-5-/M202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30/0		997.83	1.80	1.03	130	250	250	49	77	—	3
2	2½		991.08	2.50	1.42	130	250	250	49	77	—	3
3	5		100.601	2.50	1.42	129	250	250	49	77	-	3
4	7½		102.105	3.10	1.77	130	250	250	49	77	—	3
5	10		103.707	3.20	1.82	130	250	250	50	80	-	5
6	12½		105.506	3.20	1.82	130	250	250	52	80	—	5
7	15		107.003	2.60	1.48	130	250	250	55	82	—	5
8	17½		108.210	2.60	1.48	126	250	250	55	75	—	5
9	20		110.100	2.90	1.65	126	250	250	55	74	—	5
10	22½		111.506	2.90	1.65	127	250	250	55	74	—	5
11	25		113.104	2.90	1.65	127	250	250	55	74	-	5
12	27½		114.801	3.00	1.71	126	250	250	55	74	—	5
	60/OFF	12:00	116.505									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L-P/STACK 4 DRYER Sampling Date(s): 3/16/92

RUN No.: #1 Recovery Date: 3/16/92 Recovered By: BR

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	619.2	595.4	467.1				696.5
Initial Wt.	578.0	590.4	466.3				687.1
Net Weight	41.2	5.0	0.8				9.4

Total Moisture = 56.4 grams

Description of Impinger Contents: clear

Silica Gel Color: Blue Percent Spent: 5% %

Filter I.D. No.: F348 Filter Container I.D.:

Description of Particulate on Filter: Sealed: Y N

Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N

Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: #2 Recovery Date: 3/16/92 Recovered By: BR

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	625.1	584.7	459.7				713.4
Initial Wt.	596.8	575.2	457.5				702.5
Net Weight	28.3	9.5	2.2				10.9

Total Moisture = 50.9 grams

Description of Impinger Contents:

Silica Gel Color: Percent Spent: %

Filter I.D. No.: F349 Filter Container I.D.:

Description of Particulate on Filter: Sealed: Y N

Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N

Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: Recovery Date: Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.							
Initial Wt.							
Net Weight							

Total Moisture = grams

Description of Impinger Contents:

Silica Gel Color: Percent Spent: %

Filter I.D. No.: Filter Container I.D.:

Description of Particulate on Filter: Sealed: Y N

Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N

Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/12/92	DRYER STACK # 6	M-5/M 202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S Tell	29.83	-.9	40°	F-334	40"	0.84	4C GLASS	D-6	.178

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-1	1.87	1.002	1	PT-4	3	—	15	0.004	5	0.001	.85

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Finite	%O2	20.9					✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0/0	08:42	482.929	.93	0.79	131	245	249	50	46	-	1
2	2½		484.102	1.05	0.89	134	247	249	48	48	-	1
3	5		485.306	1.50	1.27	1.34	245	247	49	49	-	1
4	7½		486.905	1.60	1.36	137	248	249	53	51	-	2
5	10		488.275	1.70	1.44	138	248	249	56	51	-	2
6	12½		489.805	1.80	1.53	139	253	250	57	52	-	2
7	15		491.464	1.80	1.53	137	250	252	56	52	-	3
8	17½		493.110	1.80	1.53	141	250	249	56	52	-	3
9	20		494.606	1.70	1.44	140	246	246	59	54	-	3
10	22½		496.206	1.60	1.36	140	246	247	59	54	-	3
11	25		497.704	1.30	1.10	139	246	249	61	55	-	3
12	27½		499.204	1.20	1.02	139	246	249	61	55	-	3
	30/OFF		500.506									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3-12-92	Dryer STACK # 6	M-5/M202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A-1	30/0		500.506	1.10	0.93	136	248	251	58	54	–	1
2	2½		501.807	1.50	1.27	137	248	251	58	55	–	1
3	5		503.208	1.50	1.27	139	248	250	58	56	–	1
4	7½		504.905	1.70	1.44	140	248	250	58	56	–	2
5	10		506.310	1.70	1.44	137	249	248	58	57	–	2
6	12½		507.602	1.90	1.61	141	249	248	58	57	–	2
7	15		509.504	1.80	1.53	141	249	248	58	57	–	2
8	17½		511.207	1.70	1.44	141	249	248	58	57	–	2
9	20		512.801	1.60	1.36	141	249	249	58	57	–	2
10	22½		514.402	1.60	1.36	143	249	249	59	57	–	2
11	25		515.902	1.50	1.27	142	249	248	59	57	–	2
12	27½		517.501	1.10	0.93	142	249	248	59	57	–	2
	60/OFF	09:50	518.735									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/11/92	Dryer Stack #6	M-5/M-202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S Terll	29.83	-.9	50°	F385 335	40"	0.84	4-C	R-6	1.78

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	1	+ 4C	C-3	—	15	0.001	7	0.000	.85

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Finite	%O2	20.9					✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	10:49	519.118	1.00	0.85	134	250	249	59	60	—	1
A 2	2½		520.401	1.40	1.19	139	250	249	59	60	—	1
3	5		521.910	1.50	1.27	138	250	249	59	60	—	1
4	7½		523.306	1.60	1.36	138	250	249	59	60	—	1
5	10		524.808	1.70	1.44	139	250	250	60	61	—	2
6	12½		526.501	1.90	1.61	138	250	250	60	61	—	2
7	15		528.110	1.70	1.44	139	250	251	60	61	—	2
8	17½		529.602	1.60	1.36	140	250	251	60	62	—	2
9	20		531.108	1.60	1.36	139	250	252	60	62	—	2
10	22½		532.804	1.50	1.27	138	251	252	60	62	—	2
11	25		534.303	1.40	1.19	135	251	252	60	63	—	3
12	27½		535.806	0.90	0.76	134	250	249	60	63	—	3
	30		537.076									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3-12-92	Dryer stack # 6	M-5/M202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A-1	30/0		537.076	1.00	.85	141	250	251	60	64	–	2
B-2	2½		538.305	1.40	1.19	140	250	250	60	64	–	2
3	5		539.707	1.50	1.27	137	249	250	60	66	–	2
4	7½		541.304	1.50	1.27	137	249	250	60	66	–	2
5	10		542.702	1.70	1.44	139	249	250	60	66	–	2
6	12½		544.204	1.80	1.53	140	249	250	60	66	–	3
7	15		545.903	1.80	1.53	141	249	250	60	66	–	4
8	17½		547.825	1.60	1.36	143	249	250	60	67	–	4
9	20		549.103	1.70	1.44	142	250	250	60	67	–	4
10	22½		550.705	1.60	1.36	141	250	250	58	67	–	4
11	25		552.207	1.30	1.10	140	250	250	58	67	–	4
12	27½		553.706	1.20	.93	139	250	250	58	66	–	4
	60/OFF	11:54	555.095									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3 1/2 92	Dryer Stack #6	M-5/M202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S Terrell	29.83	-.9	55°	F-336	40"	4B	4-B	D-6	.178

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-7	1.87	1.002	r 4B	H-4B	H-4	—	15	0.000	10	0000	.85

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fizite	%O2	20.9					✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B 1	0/0	13:12	555.252	0.90	0.76	129	245	247	63	62	—	1
2	2½		556.408	1.20	1.02	135	245	247	50	63	—	1
3	5		557.807	1.50	1.27	135	248	247	48	64	—	1
4	7½		559.303	1.60	1.36	136	248	248	49	64	—	1
5	10		560.901	1.70	1.44	137	249	248	50	64	—	2
6	12½		562.502	1.80	1.53	137	250	248	49	64	—	2
7	15		544.200	1.80	1.53	137	250	248	49	65	—	3
8	17½		565.802	1.80	1.53	139	250	248	49	66	—	3
9	20		567.502	1.70	1.44	138	250	250	49	67	—	3
10	22½		569.106	1.70	1.44	136	250	250	49	67	—	3
11	25		570.810	1.50	1.27	135	250	250	49	66	—	3
12	27½		572.309	1.10	0.93	137	250	250	49	66	—	3
	30 ~~off~~		573.811									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL.	3-12-92	Dryer stack #6	M-5-/202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
A 1	30/0		573.811	1.10	0.93	132	249	250	58	67	-	1
2	2½		575.107	1.30	1.10	135	249	248	51	69	-	2
3	5		576.508	1.50	1.27	135	249	248	51	69	-	2
4	7½		578.104	1.60	1.36	135	249	248	51	69	-	2
5	10		579.607	1.60	1.36	137	249	249	45	65	-	2
6	12½		581.204	1.90	1.61	134	249	250	48	65	-	2
7	15		582.901	1.70	1.44	135	248	249	48	65	-	2
8	17½		584.604	1.70	1.44	135	248	249	48	65	-	2
9	20		586.206	1.50	1.27	135	249	249	48	65	-	3
10	22½		587.609	1.40	1.19	134	249	249	48	65	-	3
11	25		589.203	1.30	1.10	132	249	249	48	65	-	3
12	27½		590.604	1.05	0.89	131	249	249	48	65	-	3
	60/OFF	14:18	591.944									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L/P Clayton AL Sampling Date(s): 3/12/92

RUN No.: DRYER STACK #6 Run #1 Recovery Date: 3/12 Recovered By: JM

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	610.0	603.8	496.4				707.4
Initial Wt.	576.2	584.1	491.7				694.7
Net Weight	33.8	19.7	4.7				12.7

Total Moisture = 70.9 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: F334 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

Stack #6

RUN No.: Run #2 Recovery Date: 3/12 Recovered By: JM

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	612.6	587.5	463.0				715.4
Initial Wt.	582.0	571.0	458.5				703.1
Net Weight	30.6	16.5	4.5				12.3

Total Moisture = 63.9 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: F335 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

Stack #6

RUN No.: Run #3 Recovery Date: 3/12 Recovered By: JM

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	633.3	597.2	466.9				715.0
Initial Wt.	583.6	587.5	465.4				707.4
Net Weight	49.7	9.7	1.5				7.6

Total Moisture = 68.5 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: F336 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON AL	3/11/92	DRYER STACK # 8	M5 / M 202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. TERLL	29.79	-1.00	50°	F331	37.5	0.84	4-C GLASS	5-A	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
12	M-7	1.87	1.002	1	PT-5	3	—	15	0.000	10	0.000	0.5

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Finite	%O2	20.9					✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	10:15	383.549	1.30	0.65	130	248	248	44	50	—	2
A-2	2½		384.208	1.70	0.85	130	248	248	44	50	—	2
A-3	5		385.509	1.70	0.85	135	248	248	44	50	—	3
A-4	7½		386.801	2.00	1.00	132	248	248	44	50	—	3
A-5	10		388.008	2.10	1.05	135	248	248	44	52	—	3
A-6	12½		388.407	2.40	1.20	132	248	248	44	52	—	4
A-7	15		390.910	2.20	1.10	133	248	248	44	53	—	5
A-8	17½		392.303	2.10	1.05	133	248	248	45	53	—	4
A-9	20		393.710	2.10	1.05	133	248	248	45	53	—	4
A-10	22½		395.202	2.00	1.00	137	248	248	47	54	—	4
A-11	25		396.506	2.00	1.00	133	248	248	47	54	—	4
A-12	27½		397.808	1.80	~~0.90~~ 0.90	~~0.93~~	248	248	47	54	-	4
	30/OFF		399.158		0.90	133						

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LA. PACIFIC CLAYTON AL.	3/11/92	DRYER STACK #8	M5-M 202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	0/30		399.158	0.95	0.47	126	248	248	49	54	–	1
B-2	2½		400.410	1.60	0.80	138	248	248	49	54	–	2
B-3	5		401.604	1.80	0.90	132	248	248	49	54	–	2
B-4	7½		402.901	1.90	0.95	132	248	248	48	55	–	3
B-5	10		404.202	2.10	1.05	134	248	248	48	54	–	3
B-6	12½		405.605	2.10	1.05	134	248	248	48	54	–	3
B-7	15		407.003	2.20	1.10	134	248	248	48	54	–	3
B-8	17½		408.403	2.10	1.05	134	248	248	48	56	–	3
B-9	20		409.709	2.30	1.15	134	248	248	48	57	–	3
B-10	22½		411.107	2.10	1.05	131	248	248	50	59	–	3
B-11	25		412.505	2.00	1.00	131	248	248	52	59	–	3
B-12	27½		413.901	1.70	0.85	129	248	248	52	59	–	3
	OFF/60	11:28	415.168									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/11/92	Dryer Stack # 8	M-5 / M 202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terll	29.79	-1.00	50	F-332	37.5	0.84	4-B	5-B	.149

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
	M-7	1.87	1.002	#4B	P4B		—	15	0.005	5	0.000	0.5

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT.	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fisite	%O2 20.9					✓	✓
Analysis Method		%CO2						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B 1	0/0	13:03	415.535	1.20	0.60	129	249	246	53	56	-	1
2	2½		416.606	1.40	0.70	129	250	249	53	56	-	1
3	5		417.801	1.80	0.90	130	249	247	51	57	-	1
4	7½		419.007	1.90	0.95	131	249	249	50	57	-	1
5	10		420.308	2.10	1.05	130	249	249	50	57	-	2
6	12½		421.801	2.20	1.10	129	251	248	50	57	-	2
7	15		423.107	2.30	1.15	128	251	248	53	58	-	2
8	17½		424.701	2.20	1.10	128	250	250	53	58	-	2
9	20		426.007	2.20	1.10	128	250	250	53	58	-	2
10	22½		427.504	2.10	1.05	129	249	249	53	58	-	2
11	25		429.908	1.90	0.95	129	249	245	59	59	-	2
12	27½		430.206	1.70	0.85	128	249	249	59	58	-	2
	30/OFF		431.205									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL.	3-11-92	DRYER STACK # 8	M-5 / M 202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
A 1	30/0		431.205	1.80	0.90	128	249	249	54	58	–	1
2	2½		433.008	1.70	0.85	128	249	249	54	58	–	1
3	5		434.305	1.95	0.97	128	249	250	53	59	–	1
4	7½		435.704	2.20	1.10	129	249	250	53	59	–	1
5	10		437.201	2.40	1.20	128	249	250	53	59	–	1
6	12½		438.604	2.50	1.25	129	249	250	53	59	–	2
7	15		440.101	2.25	1.12	129	249	249	53	59	–	2
8	17½		441.535	2.20	1.10	129	249	247	55	60	–	2
9	20		442.908	2.20	1.10	129	249	247	55	60	–	2
10	22½		444.406	2.10	1.05	129	249	247	55	60	–	2
11	25		445.910	2.00	1.00	128	249	247	55	60	–	2
12	27½		447.208	1.70	0.85	128	249	247	55	60	–	2
	60/OFF	14:19	448.523									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL.	3/11/92	Dryer Stack # 8	M-5 / M 202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terll	29.79	-1.00	60°	F-333	37.5	0.84	4-C Glass	5-A	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
12	M7	1.87	1.002	1	PT-5	3	-	15	0.005	5	0.003	~~1.55~~ .5

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fritz	%O2	20.9					✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	15:19	448.674	1.50	0.75	129	249	246	52	58	-	1
2	2½		449.809	1.70	0.85	129	249	247	52	59	-	1
3	5		451.103	2.00	1.00	128	251	248	53	60	-	1
4	7½		452.525	2.10	1.05	129	252	248	53	60	-	2
5	10		453.903	2.20	1.10	129	251	247	53	60	-	2
6	12½		455.406	2.50	1.25	129	251	247	57	60	-	3
7	15		456.901	2.20	1.10	129	251	247	57	60	-	4
8	17½		458.309	2.20	1.10	129	251	247	57	60	-	3
9	20		459.805	2.10	1.05	132	250	248	57	60	-	3
10	22½		461.305	2.00	1.00	133	250	248	57	60	-	3
11	25		462.810	2.00	1.00	132	250	248	57	60	-	4
12	27½		464.206	1.80	.90	130	250	249	57	60	-	3
	30/~~0~~		465.558									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clanton AL.	3-11-92	Dryer stack # 8	m-5 / m202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30/0		465.558	1.50	.75	127	251	249	55	58	–	1
2	2½		466.708	1.70	.85	128	249	249	55	58	–	1
3	5		468.003	1.90	0.95	128	249	249	55	59	–	1
4	7½		469.308	2.00	1.00	129	248	249	55	59	–	2
5	10		470.705	2.10	1.05	129	249	249	56	59	–	2
6	12½		472.206	2.20	1.10	130	248	249	59	60	–	2
7	15		473.610	2.30	1.15	130	248	249	59	60	–	3
8	17½		475.009	2.20	1.10	130	249	249	60	60	–	3
9	20		476.504	2.20	1.10	130	249	248	60	60	–	3
10	22½		478.045	2.10	1.05	129	249	248	60	60	–	3
11	25		479.503	2.00	1.00	130	249	248	61	60	–	3
12	27½	16:26	481.110	1.90	0.95	131	249	249	61	60	–	3
	60/off		482.410									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L-P/CLAYTON, AL Sampling Date(s): 3/11/92

RUN No.: STACK8-#1 Recovery Date: 3/11/92 Recovered By: BHR

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	638.3	574.6	458.0				704.9
Initial Wt.	583.7	580.0	456.4				697.5
Net Weight	54.6	-5.4 *	1.6				7.4

Total Moisture = 58.2 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F331 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: STACK8-#2 Recovery Date: 3/11/92 Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	593.6	578.3	493.5				694.7
Initial Wt.	558.8	562.1	489.4				685.3
Net Weight	34.8	16.2	4.1				9.4

Total Moisture = 64.5 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F332 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: STACK8-#3 Recovery Date: 3/11/92 Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	624.8	588.6	459.3				703.1
Initial Wt.	585.3	579.9	457.3				~~704.9~~ 691.9
Net Weight	39.5	8.7	2.0				11.2

Total Moisture = 51.4 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F333 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

PRESS VENTS

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL.	3/18/92	PRESS VENT #3	M5/202	1

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.85	-0.30		F362	62"	0.84	6A GLASS	D8	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M8	1.88	~~0.998~~ 1.005 2ND.	6A-5	PT-1	64	—	15.0	0.014	15.0	0.013	3.50

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9						
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P. VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC. (In. Hg)
A 1	0/0	0944	857.564	0.34	1.19	93	248	253	60	65	—	4.0
2	2.5		859.15	.54	1.89	94	248	250	58	65		6.0
3	5		860.93	.53	1.86	93	249	251	58	65		6.0
4	7.5		862.73	.82	2.87	91	248	252	58	66		9.5
5	10		864.94	.62	2.17	90	248	251	58	67		7.5
6	12.5		869.99	.36	1.26	90	249	250	57	67		4.5
7	15		868.54	.26	.91	90	250	252	57	67		3.5
8	17.5		869.86	.35	1.23	90	251	251	56	67		4.5
9	20	1004/1012	871.31	.87	3.05	91	251	250	59	66		10.0
10	22.5		873.67	.92	3.22	91	250	254	59	67		11.0
11	25		876.02	.67	2.35	93	248	252	57	67		8.0
12	27.5		878.14	.65	2.28	93	246	250	58	67		7.5
B 1	30/0	1022/1036	880.15	.46	1.61	93	246	250	58	67		5.5

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/18/92	PRESS VENT 3	M5/202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B2	2.5		881.76	0.45	1.58	93	248	247	57	67	—	5.0
3	5		883.61	.50	1.75	92	249	250	58	67		6.0
4	7.5		885.40	.62	2.17	91	248	249	58	67		7.0
5	10		887.36	.41	1.44	92	248	250	58	68		5.0
6	12.5		889.06	.31	1.09	91	249	252	58	68		4.0
7	15		890.46	.49	2.80	92	249	253	58	68		9.0
8	17.5		892.70	.67	2.35	93	250	251	58	68		8.5
9	20		894.80	1.00	3.50	93	250	251	58	68		13.0
10	22.5		897.3	.76	2.66	95	248	250	59	69		9.0
11	25		899.59	.65	2.28	96	249	251	59	69		8.0
12	27.5		901.65	.71	2.49	95	249	252	59	69		8.5
	30/60	1106	903.687									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC, CLAYTON, AL	3 18/92	PRESS VENT #3	M5/202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.85	-0.30		F364	62"	0.84	6A GLASS	D-8	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M-8	1.88	~~0.998~~ 1.005 JQ	GAS	PT. 1	64	–	15.0	0.009	12.0	0.009	3.50

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					✓	
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	1340	904.811	0.34	1.19	93	237	240	61	65	—	3.5
2	2.5		906.33	.55	1.93	95	243	246	60	65		5.0
3	5		908.27	.51	1.79	95	247	248	59	65		4.5
4	7.5		910.10	.79	2.77	93	249	257	58	66		6.5
5	10		912.30	.53	1.86	92	250	251	58	66		5.0
6	12.5		914.22	.30	1.03	92	251	250	58	67		5.0
7	15		916.21	.30	1.03	92	250	252	57	67		3.0
8	17.5		917.57	.38	1.33	93	250	253	57	67		3.5
9	20		919.07	.85	2.98	93	250	257	57	67		6.5
10	22.5		921.30	.91	3.19	93	250	257	57	68		7.5
11	25		923.66	.30	1.03	93	257	252	57	68		3.0
12	27.5		925.14	.55	1.93	93	250	252	57	68		5.0
B 1	30/0	1410/1415	926.88/	.34	1.19	91	252	254	57	67		3.5

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

JEJ 3/24/92

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/18/92	~~M6/202~~ PRESS VENT 2	M5/202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P. VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B2	2.5		928.35	0.49	1.72	94	245	246	57	67	—	4.0
3	5		930.10	.57	2.00	96	245	247	55	67		5.0
4	7.5		932.04	.74	2.59	95	247	252	52	67		6.0
5	10		934.16	.57	2.00	94	250	253	52	68		5.0
6	12.5		935.08	.35	1.23	93	250	251	54	68		4.0
7	15		937.56	.35	1.23	93	250	254	54	68		3.5
8	17.5		939.05	.56	1.96	93	251	254	55	68		5.0
9	20		940.39	.86	3.01	93	251	256	56	68		7.0
10	22.5		943.19	.63	2.21	94	252	250	54	68		6.0
11	25		945.26	.52	1.82	95	250	251	53	68		5.0
12	27.5		947.17	.35	1.23	94	251	252	53	68		3.5
	30/60	12:45	948.559									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

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EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/18/92	PRESS VENT #3	M5/202	3

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.85	-.30		F 369	62"	0.84	6A GLASS	D-8	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M8	1.88	0.998	6A5	PT-1	64	—	15.0	0.005			350

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	1.005 26.2. ~~TEDLAR~~ GRAB	%O2							
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A 1	0/0	1601	949.861	0.34	1.19	90	249	254	61	65	—	4.0
2	2.5		951.35	.54	1.89	92	250	254	60	66		7.5
3	5		953.45	.63	2.21	92	251	253	59	66		7.5
4	7.5		955.31	.72	~~2.45~~ 3.56	92	252	252	57	67		8.0
5	10		957.40	.59	2.07	92	257	253	57	66		7.0
6	12.5		959.32	.40	1.40	91	257	252	57	66		5.0
7	15		960.94	.47	1.65	91	252	251	57	66		6.0
8	17.5		962.68	.81	2.84	91	251	252	57	67		10.0
9	20		964.88	1.10	3.85	93	250	254	57	67		14.0
10	22.5		967.45	.70	2.45	93	249	253	57	68		8.0
11	25		969.61	.72	2.52	94	250	253	58	67		8.5
12	27.5		971.67	.62	2.17	93	257	253	58	67		8.5
B 1	30/0	1631/1634	973.81	.45	1.58	94	251	252	58	67		5.5

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON	3/18/92	PRESS VENT #3	M5/202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
B2	2.5		975.55	0.53	1.86	95	251	253	57	67	—	5.0
3	5		977.29	.57	2.00	95	252	252	57	67		6.8
4	7.5		979.18	.79	2.77	91	253	253	57	68		8.0
5	10.5		981.20	.55	1.93	91	253	251	57	68		6.5
6	12.5		983.21	.31	1.09	91	251	253	57	68		4.0
7	15.5		984.78	.35	1.23	91	250	252	58	67		4.5
8	17.5		986.30	.47	1.65	90	250	251	58	68		6.0
9	20.5		988.03	.92	3.22	92	253	252	58	68		10.0
10	22.5		990.39	.55	1.93	92	253	252	57	68		6.5
11	25		992.30	.59	2.06	92	251	250	57	68		6.5
12	27.5		994.20	.40	1.40	93	250	252	57	68		4.0
	30/60	1704	995.842									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P. Press Vent 3 Sampling Date(s): 3/18/ & 3/19/92

RUN No.: #1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	576.1	601.7	457.7	X	X	X	700.7
Initial Wt.	591.2	600.0	457.2	X	X	X	680.2
Net Weight	-15.1	1.7	0.5	X	X	X	20.5

* Total Moisture = 7.6 grams

Description of Impinger Contents: _____

Silica Gel Color: blue-purple Percent Spent: 50% %

Filter I.D. No.: F-362 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: #2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	574.0	567.3	482.5	X	X	X	731.8
Initial Wt.	573.0	564.5	481.3	X	X	X	719.7
Net Weight	1.0	2.8	1.2	X	X	X	12.1

Total Moisture = 17.1 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: F-364 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: #3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	586.3	587.6	459.9	X	X	X	731.8
Initial Wt.	595.7	584.3	458.2	X	X	X	711.3
Net Weight	-9.4	3.3	1.7	X	X	X	20.5

* Total Moisture = 16.1 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: _____ Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/11/92	# 4 PRESS STACK	M5/202	1

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	30.02	-0.3		F 356	62"	0.84	6A GLASS	D 8	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
3	M8	1.88	~~0.998~~ 1.005 JEJ					15.0	0.015	10.0	0.014	.50

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9						
Analysis Method	FYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A 1	0/0	1339	718.820	0.50	1.75	106	243	247	61	85	—	4.0
2	2.5		720.56	.52	1.82	104	248	248	60	84		4.5
3	5.0		722.35	.62	2.17	106	248	251	60	85		5.0
4	7.5		724.35	.84	2.94	105	250	252	58	85		6.5
5	10.0		726.65	.50	1.75	104	250	251	52	86		4.0
6	12.5		728.44	.35	1.23	103	251	250	57	87		3.0
7	15		729.98	.20	.70	103	252	251	58	87		2.5
8	17.5		731.20	.43	1.51	98	252	251	58	87		4.0
9	20		732.83	.67	2.35	96	252	251	58	87		5.5
10	22.5		734.81	.63	2.21	96	253	249	57	88		5.0
11	25		736.82	.45	1.58	96	254	249	57	88		4.0
12	27.5		738.56	.74	2.59	96	253	251	57	88		6.0
	30/0	1409/1410	740.66									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/12/92	#4 PRESS VENT	M5/202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
B1	30/3		740.66	0.41	1.44	104	251	253	57	88	—	3.0
2	2.5		742.31	.43	1.51	105	252	252	57	88		4.0
3	5		743.95	.57	2.00	104	252	254	57	88		5.0
4	7.5		745.90	.81	2.84	104	253	253	58	88		6.0
5	10.0		748.25	.49	1.72	103	253	254	58	88		4.0
6	12.5		750.12	.27	.95	103	253	255	58	87		3.0
7	15		751.73	.25	.88	100	253	253	53	87		2.5
8	17.5		752.72	.69	2.42	98	252	253	57	86		5.0
9	20		754.79	1.00	3.50	100	257	252	56	86		8.0
10	22.5		757.25	.72	2.52	100	251	252	56	87		5.5
11	25		759.40	.30	1.05	102	250	250	56	87		3.0
12	27.5		760.80	.31	1.09	101	250	248	56	87		3.0
	30/60	1440	762.201									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

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EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/17/92	PRESS VENT #4 STACK	M5/202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	30.02	-0.35		F358	62	0.84	6A GLASS	D8	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
3	M-8	1.88	~~2.998~~ 1.005	6A S	PT-1	6-4		15.0	0.007	15.	0.006	3.50

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9						
Analysis Method	FYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	1510	764.552	0.45	1.58	104	253	251	61	84	—	4.0
2	2.5		766.08	.53	1.86	106	251	252	60	84		5.0
3	5.0		767.95	.74	2.59	105	250	251	58	85		8.0
4	7.5		769.97	.87	3.05	104	252	253	56	85		9.0
5	10		772.32	.52	1.82	104	252	251	56	85		6.0
6	12.5		774.30	.34	1.19	102	250	252	56	85		4.0
7	15		775.86	.26	.91	98	251	252	57	85		3.0
8	17.5		777.18	.48	1.68	97	251	253	57	85		5.0
9	20		778.92	.87	3.12	94	251	254	57	85		9.5
10	22.5		781.29	.82	2.87	96	250	252	57	85		9.0
11	25		783.56	.47	1.65	96	250	251	57	85		5.0
12	27.5		785.33	.75	2.63	97	251	250	57	85		8.0
B 1	30/0	1540/1542	787.52	.30	1.05	102	251	250	56	85		4.0

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC-CLAYTON, AL	3/17/93	PRESS VENT #4 STACK	M5/202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
B2	2.5		789.00	0.54	1.89	103	252	254	56	85	—	5.0
3	5		790.80	.60	2.10	103	251	253	57	85		6.0
4	7.5		792.74	.81	2.84	103	251	253	57	85		8.5
5	10		795.00	.46	1.61	103	250	254	57	85		5.0
6	12.5		796.78	.25	.88	103	249	254	57	85		3.0
7	15		798.07	.32	1.12	98	250	252	58	84		4.0
8	17.5		800.98	.71	2.49	98	250	252	58	84		7.0
9	20		803.10	1.00	3.50	98	250	252	58	84		11.0
10	22.5		805.65	.77	2.70	100	252	254	58	84		8.5
11	25		808.00	.40	1.40	100	252	254	58	84		5.0
12	27.5		809.48	.30	1.05	100	253	253	58	84		3.5
	30/60	1612	810.953									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/17/92	PRESS VENT #4 STACK	M5/202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	30.02	-0.35		F 360	62"	0.84	64 GLASS		0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
3	M8	1.88	~~0.998~~ 1.005	64.5	PT-1	64		15.0	0.013	15.0	0.011	3.50

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT.	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9						
Analysis Method	FIRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	1652	813.009	0.30	1.05	102	257	247	58	80	—	3.0
2	2.5		814.37	.60	2.10	103	252	249	58	80		5.0
3	5		816.24	.72	2.52	103	250	251	52	80		6.0
4	7.5		818.38	.87	2.94	102	257	252	56	80		7.5
5	10		820.69	.53	1.86	101	253	249	56	80		5.0
6	12.5		822.60	.35	1.23	100	255	248	56	80		3.5
7	15		824.14	.26	.91	97	254	249	56	80		3.0
8	17.5		825.44	.56	1.96	93	253	251	54	80		5.0
9	20		827.34	.70	2.45	93	255	251	52	80		6.0
10	22.5		829.43	.53	1.86	94	250	252	50	80		5.5
11	25		831.33	.66	2.31	94	250	249	47	80		6.0
12	27.5		833.43	.71	2.49	95	251	249	47	80		6.5
B 1	30.0	1722/1724	835.57	.25	.88	91	257	250	47	80		

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL.	3/17/92	PRESS VENT #4 STACK	M5/202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B.2	2.5		836.83	0.56	1.96	100	249	251	47	79	—	5.0
3	5		838.57	.62	2.17	101	249	250	47	79		5.0
4	7.5		840.58	.81	2.84	101	250	251	47	79		7.0
5	10		842.82	.47	1.65	99	251	252	47	80		3.5
6	12.5		844.60	.31	1.09	99	252	249	48	80		3.0
7	15		846.06	.36	1.26	97	252	251	48	79		4.0
8	17.5		847.64	.69	2.42	96	253	250	49	79		6.0
9	20		849.68	1.00	3.50	97	253	252	49	79		9.0
10	22.5		852.21	.74	2.59	97	254	252	49	79		5.0
11	25		854.08	.39	1.37	97	253	253	49	79		4.0
12	27.5		855.65	.30	1.05	99	253	254	49	79		3.5
	30/60	1254	857.047									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/ SAMPLE RECOVERY DATA SHEET

Client/Location: Press Vent 4 [redacted] Sampling Date(s): 3/17/92

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3 (8 gsm)	4	5	6	Silica Gel
Final Wt.	566.6	560.8	481.4	X	X	X	736.7
Initial Wt.	568.1	559.8	480.5	X	X	X	727.6
Net Weight	-1.5	1.0	0.9	X	X	X	9.1

727.6 gsm

*

Total Moisture = 9.5 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue (New) Percent Spent: _____ %
Filter I.D. No.: F-356 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	571.2	586.3	458.4	X	X	X	680.2
Initial Wt.	576.4	585.3	457.4	X	X	X	668.6
Net Weight	-5.2	1.0	1.0	X	X	X	11.6

*

Total Moisture = 8.4 grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: F-358 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	553.1	551.6	481.3	X	X	X	745.6
Initial Wt.	557.8	549.4	480.9	X	X	X	736.7
Net Weight	-4.7	2.2	0.4	X	X	X	8.9

*

Total Moisture = 6.8 grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: F-360 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/19/92	PRESS VENT 5	M5/202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.52	-0.3		F-372	62"	0.84	6A GLASS	D8	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M8	1.88	~~0.998~~	6A-5	PT-1	64		15.0	0.004	15.0	0.004	3.52

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					✓	✓
Analysis Method	FYRITE	%CO2							

1.003 X3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	0828	996.070	0.38	1.33	87	242	254	60	70	--	4.0
2	2.5		997.79	.56	1.96	90	245	252	59	71		5.0
3	5		999.67	.75	2.63	92	249	253	58	71		6.0
4	7.5		1001.77	.88	3.08	89	250	252	56	72		7.5
5	10		4.14	.55	1.93	88	251	251	56	72		5.0
6	12.5		6.05	.30	1.05	86	250	249	56	73		3.0
7	15		7.47	.23	.81	85	250	249	57	73		3.0
8	17.5		8.72	.35	1.23	84	249	248	57	74		4.0
9	20		10.23	.63	2.21	87	249	249	57	74		5.0
10	22.5		12.19	.78	2.73	87	249	250	57	75		7.0
11	25		14.40	1.00	3.50	89	251	251	55	75		9.0
12	27.5		17.01	.62	2.17	91	250	250	55	76		5.5
B 1	30/0	0858/0902	19.00	.35	1.23	88	250	249	56	76		4.0

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/19/92	PRESS VENT #5	M5/202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP. (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B2	2.5		20.65	0.50	1.75	92	250	252	54	76	—	4.5
3	5		22.37	.62	2.17	91	250	251	53	76		5.5
4	7.5		24.33	.85	2.98	92	251	252	53	77		7.0
5	10		26.67	.45	1.58	92	250	254	54	77		4.5
6	12.5		28.42	.26	.91	93	250	253	54	78		4.0
7	15		29.74	.37	1.30	94	250	253	54	78		3.5
8	17.5		31.23	.87	3.05	85	252	254	54	78		3.5
9	20		33.65	1.05	3.68	87	250	254	54	78		9.5
10	22.5		36.18	.98	3.43	90	247	253	54	78		9.0
11	25		39.68	.26	.91	89	247	251	56	78		3.0
12	27.5		40.07	.26	.91	90	248	250	56	78		3.0
	30/00	0932	41.411									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/19/92	PRESS VENT # 5	M5/202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.52	-0.30		F-373	6 2"	0.84	6A GLASS	D3	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M-8	1.88	~~0.998~~	6A-2	P7-1	C-1		15.0	0.003	15.0	0.002	3.50

				RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
EPA METHOD 3	1.005 DEG									
Collection Method	GRAB	%O2		20.9					✓	✓
Analysis Method	FYRITE	%CO2		—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0/0	0952	41.560	0.27	0.95	84	248	249	62	80	—	3.5
2	2.5		42.92	.55	1.93	93	249	257	62	80		5.5
3	5		44.81	.79	2.77	96	251	250	61	80		8.0
4	7.5		47.11	.87	3.06	92	250	252	61	80		9.5
5	10		49.38	.56	1.96	91	250	253	60	81		6.0
6	12.5		51.38	.25	.88	91	252	254	59	80		3.0
7	15		52.67	.91	3.19	92	250	254	58	81		10.0
8	17.5		55.06	.35	1.23	93	251	252	58	82		4.0
9	20		56.57	.82	2.87	92	249	253	58	82		9.0
10	22.5		58.92	.95	3.33	91	250	252	58	82		11.0
11	25		61.30	.95	3.33	91	251	253	58	82		11.0
12	27.5		63.77	.70	2.45	94	253	253	58	82		8.0
B1	30/0	1022/1024	65.94	.44	1.54	94	253	254	58	82		5.0

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, NC	3/19/92	PRESS VENT #5	M5/202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B2	2.5		67.81	0.55	1.93	96	253	255	58	82	—	6.0
3	5		69.70	.62	2.17	97	253	254	57	82		6.5
4	7.5		71.72	.85	2.98	96	251	254	57	82		9.0
5	10		74.03	.49	1.72	97	252	251	56	82		6.0
6	12.5		75.85	.29	1.02	94	252	250	56	83		4.0
7	15		77.31	.46	1.61	93	249	252	56	83		5.0
8	17.5		79.03	.69	2.42	91	250	252	56	83		7.0
9	20		81.15	.82	2.87	92	250	251	56	83		9.0
10	22.5		83.42	.73	2.56	93	249	250	56	84		7.5
11	25		85.59	.39	1.37	95	251	254	57	84		4.5
12	27.5		87.18	.17	.60	93	251	253	57	84		2.5
	30/60	1054	88.305									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON AL	3/19/92	PRESSVENT 6	M5/202	#1

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B. RAYFI	29.58	±0.08 VARIABLE	77	GLASS F376	56"	0.84	5' A GLASS	K25	0.235

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	5A	PT14	—	—	12"	0.010	10"	0.005	3.49

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT.	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: DIRECT	%O2				21	21	✓	
Analysis Method: FYRITE	%CO2				0	0		

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
B-1	0	12:18	057.457	0.08	0.28	86	239	242	68	86		1
2	2.5		058.22	0.14	0.49	99	248	250	65	87		1
3	5		059.17	0.40	1.40	98	250	249	65	89		2
4	7.5		060.73	0.66	2.30	94	250	249	60	89		3
5	10		062.66	0.67	2.33	91	249	251	59	89		3
6	12.5		063.03	0.08	0.28	93	246	249	61	89		1
7	15		065.60	0.45	1.57	87	249	249	60	89		2
8	17.5		067.26	0.50	1.75	86	248	247	59	88		2
9	20		068.97	0.85	2.97	90	245	248	59	87		4
10	22.5		071.18	0.89	3.11	92	245	247	59	88		4
11	25		073.53	0.91	3.18	91	246	249	60	87		4
12	27.5		075.86	0.85	2.97	91	243	249	62	88		4
—	30	12:48	078.135									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC / CLAYTON AL	3/19/92	PRESS VENT 6	M5/202	#1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A-1	0	12:54	078.135	0.52	1.81	88	240	248	64	86		2
2	2.5		079.93	0.57	1.99	91	239	247	62	86		2
3	5		081.76	0.45	1.57	93	244	249	60	87		2
4	7.5		083.44	0.64	2.23	89	247	246	59	86		3
5	10		085.39	0.53	1.84	88	243	248	60	87		2
6	12.5		087.15	0.15	0.52	91	249	249	61	86		1
7	15		088.19	0.22	0.77	90	247	246	62	86		1
8	17.5		089.38	0.24	0.84	87	246	248	63	86		1
9	20		090.59	0.35	1.22	89	243	248	62	85		1
10	22.5		092.02	0.49	1.71	90	246	249	61	85		2
11	25		093.68	0.65	2.27	87	246	246	60	84		3
12	27.5		095.63	0.80	2.80	88	246	248	60	84		4
END	30/60	13:24	097.762									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

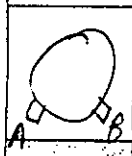
Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON AL	3/19/92	PRESS VENT 6	M5/202	#2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B RAYFIELD	29.58	+0.05	80	GLASS/F378	56"	0.84	5' A GLASS	5/25	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
		2.00	1.01	5A	PT14	—	—	10"	0.008	10"	0.005	3.83



EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: DIRECT	%O2				21	21	✓	✓
Analysis Method: FYRITE	%CO2				0	0		

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0	2:14	097.922	0.07	0.27	86	247	251	67	83		1
2	2.5		098.65	0.07	0.27	91	250	246	64	84		1
3	5		099.36	0.17	0.65	93	252	248	61	85		2
4	7.5		100.34	0.42	1.61	91	246	249	57	85		2
5	10		101.98	0.74	2.83	90	249	249	56	85		5
6	12.5		104.15	0.52	1.99	91	246	247	55	85		4
7	15		106.04	0.08	0.31	94	249	245	58	85		1
8	17.5		106.83	0.35	1.34	90	251	250	62	86		2
9	20		108.31	0.54	2.07	86	245	250	59	85		3
10	22.5		110.20	0.63	2.41	91	240	248	57	85		4
11	25		112.22	0.80	3.06	92	241	248	57	86		5
12	27.5		114.59	0.90	3.45	92	244	249	57	86		6
—	30	2:44	116.859									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON	3/19/92	PRESS VENT 6	M5/202	#2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A-1	0	2:54	116.859	0.50	1.92	92	250	249	67	84		3
2	2.5		118.69	0.62	2.37	94	251	249	49	86		4
3	5		120.69	0.62	2.37	92	249	246	48	87		4
4	7.5		122.52	0.49	1.88	91	247	251	50	87		3
5	10		124.50	0.15	0.57	95	245	248	52	87		1
6	12.5		125.63	0.11	0.42	91	244	245	54	87		1
7	15		126.53	0.18	0.69	88	247	248	56	86		2
8	17.5		127.62	0.30	1.15	90	246	248	56	87		2
9	20		129.03	0.35	1.34	89	249	249	56	87		3
10	22.5		130.54	0.45	1.72	88	247	249	55	87		3
11	25		132.24	0.67	2.57	88	246	248	60	86		5
12	27.5		134.31	0.76	2.91	94	248	250	55	88		5
END	30/60		136.534									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

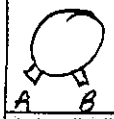
Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC/CLAYTON	3/1992	PRESS VENT 6	M5/202	#3

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B. RAYFIELD	29.58	+0.05	80	GLASS/F380	56"	0.84	5' A GLASS	55.25	0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	5A	PT4	—	—	0.018	10"	8"	0.015	3.83



EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: DIRECT DRAW	%O2				21	21	✓	✓
Analysis Method: FYRITE	%CO2				0	0		

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0	4:00	136.839	0.07	0.27	85	248	251	66	83		1
2	2.5		137.61	0.07	0.27	86	249	250	62	83		1
3	5		138.42	0.08	0.31	92	247	250	59	83		1
4	7.5		139.15	0.49	1.88	90	249	249	58	84		2
5	10		140.87	0.75	2.87	88	249	250	54	84		4
6	12.5		143.03	0.48	1.84	91	248	246	55	84		3
7	15		144.82	0.08	0.31	90	250	250	57	85		1
8	17.5		145.69	0.32	1.23	90	246	248	58	85		2
9	20		147.17	0.39	1.49	87	239	248	57	84		2
10	22.5		148.75	0.65	2.49	91	245	249	56	84		2
11	25		150.76	0.67	2.57	89	248	249	56	84		3
12	27.5		152.85	0.71	2.72	88	246	250	57	85		4
—	30	4:30	155.019									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON, AL	3/19/92	PRESS VENT 6	M5/202	#3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A-1	0	4:36	155.019	0.50	1.92	89	246	245	64	82		3
2	2.5		156.82	0.71	2.72	90	248	251	54	82		4
3	5		159.94	0.50	1.92	88	239	249	53	83		3
4	7.5		160.78	0.60	2.30	86	239	248	54	83		3
5	10		162.70	0.39	1.49	91	242	249	56	83		3
6	12.5		164.29	0.13	0.50	87	238	248	57	83		1
7	15		165.36	0.23	0.88	85	246	248	59	83		1
8	17.5		166.60	0.25	0.96	85	244	247	59	83		2
9	20		167.93	0.32	1.23	87	243	252	57	83		2
10	22.5		169.38	0.45	1.72	86	245	248	55	83		3
11	25		171.08	0.65	2.49	84	243	246	53	83		4
12	27.5		173.10	0.60	2.30	91	240	246	53	83		4
END	30/60		175.059									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P. Press Vent #6 Sampling Date(s): 3/18/92

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	608.9	591.7	468.4				698.9
Initial Wt.	606.9	589.3	469.1				689.0
Net Weight	2.0	2.4	-0.7				9.9

Total Moisture = 13.6 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue purple Percent Spent: 25% %
Filter I.D. No.: F-376 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	576.9	607.4	471.6				749.8
Initial Wt.	575.6	606.9	471.5				742.7
Net Weight	1.3	0.5	0.1				7.1

Total Moisture = 9.0 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue-white Percent Spent: _____ %
Filter I.D. No.: F-378 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	606.8	558.9	468.6				707.1
Initial Wt.	594.5	572.1	469.0				698.9
Net Weight	12.3	-13.2	-0.4				8.2

* * Total Moisture = 6.9 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue-white Percent Spent: 25% %
Filter I.D. No.: 380 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/19/92	Press Vent # 7	M-5 / M 202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S Terll	29.58	-.15	90	F-374	56"	0.84	C-5 SS	B-8	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M87	1.87	1.002	TGC	F-5-C	H-4	—	15	0.004	7	0.000	K=3.91

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite	%O2	20.9					✓	✓
Analysis Method	—	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	12:05	509.008	.30	1.14	95	249	250	65	85	—	2
2	2½		510.702	.43	1.64	90	249	250	63	86	—	2
3	5		512.710	.25	.95	95	249	250	63	87	—	2
4	7½		513.907	.33	1.26	97	249	250	62	87	—	3
5	10		515.409	.55	2.09	93	249	250	62	87	—	4
6	12½		517.401	.35	1.33	90	249	250	64	87	—	4
7	15		519.103	0.05	.19	99	249	251	65	87	—	4
8	17½		520.104	0.49	1.87	95	249	251	65	88	—	4
9	20		521.810	.70	2.67	92	249	251	65	88	—	5
10	22½		523.808	.50	1.90	92	249	250	65	88	—	4
11	25		525.803	.50	1.90	99	249	250	65	87	—	4
12	27½		527.703	.37	1.41	92	249	250	65	87	—	4
	30/OFF		529.408									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3-19-92	Press Vent # 7	M5/M202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		529.408	.60	2.29	97	251	249	60	86	–	3
2	2½		531.705	.65	2.48	93	251	248	60	86	–	4
3	5		533.109	.39	1.48	93	251	248	60	86	–	4
4	7½		535.602	.25	0.95	93	251	248	60	86	–	4
5	10		536.906	.08	.30	92	251	249	62	85	–	1
6	12½		538.002	.05	.19	87	251	249	62	84	–	1
7	15		538.708	.15	.57	91	251	249	63	84	–	1.5
8	17½		539.703	.15	.57	92	251	249	63	84	–	1.5
9	20		540.804	.30	1.14	92	251	249	64	83	–	2
10	22½		542.205	.35	1.33	92	251	249	64	83	–	4
11	25		543.810	.53	2.02	92	251	249	64	83	–	4
12	27½		545.503	.57	2.17	93	251	249	64	83	–	4
	60/off	13:14	547.506									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/4/92	Press Vent # 7	M5/M202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terll	29.58	.100	80	F 377	56"	0.84	C-5 SS	B-8	.242

ASSUMED MOIST (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M-7	1.87	1.002	T4	T-C-5	#4	—	15	0.005	10	0.004	K= 3.81

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Tyrite	%O2	20.9					✓	✓
Analysis Method	GRAB	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	13:45	547.607	.30	1.14	89	245	247	62	86	—	1
2	2½		549.109	.40	1.52	87	247	247	64	87	—	1
3	5		550.810	.35	1.33	96	247	247	68	87	—	1
4	7½		552.405	.25	0.95	96	247	247	63	88	—	1
5	10		553.804	.65	2.48	91	247	249	65	89	—	1
6	12½		556.004	.35	1.33	85	248	249	57	87	—	2
7	15		558.110	.05	.19	93	248	249	57	87	—	2
8	17½		559.207	.39	1.48	90	248	249	56	87	—	2
9	20		560.709	.55	2.09	87	248	249	56	87	—	2
10	22½		562.607	.43	1.64	93	250	250	56	83	—	2
11	25		564.705	.43	1.64	93	250	250	56	83	—	2
12	27½		566.210	.47	1.79	94	250	250	56	83	—	2
	30 off		567.935									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/19/92	Press Vent # 7	M-5/m202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		567.935	.50	1.90	93	250	250	62	85	–	1
2	2½		569.807	.47	1.79	88	250	250	62	85	–	1
3	5		571.607	.40	1.52	91	250	250	62	85	–	1
4	7½		573.410	.15	.57	94	250	250	62	85	–	1
5	10		574.509	.05	.19	95	250	250	62	85	–	1
6	12½		575.402	.05	.19	90	250	250	63	87	–	1
7	15		576.210	.05	.19	90	250	250	63	85	–	1
8	17½		577.005	.15	.57	99	250	250	63	89	–	1
9	20		578.004	.15	.57	98	250	250	63	89	–	1
10	22½		579.206	.30	1.14	94	250	250	64	89	–	3
11	25		580.606	.45	1.71	99	250	250	64	90	–	3
12	27½		582.400	.55	2.09	98	250	250	64	90	–	3
	60/0FD	15:50	584.167									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/18/92	Press Vent #7	M-5 / M202	3

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrill	29.58	-.1	80°	F 379	56"	0.84	C-5	B-8	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M-7	1.87	1.002	CT-4	T-C-5	H-4	—	15	0.000	10	0.000	K= 381

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite	%O2	20.9					✓	✓
Analysis Method	Grab	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	15:27	584.414	.35	1.33	95	246	249	61	92	—	1
2	2½		586.101	.35	1.33	88	246	249	61	92	—	1
3	5		587.707	.30	1.14	92	246	249	62	92	—	2
4	7½		589.302	.33	1.26	93	246	249	62	90	—	2
5	10		590.803	.49	1.87	90	246	249	62	90	—	3
6	12½		592.506	.45	1.71	90	246	249	62	90	—	3
7	15		594.600	.05	0.19	93	247	248	61	89	—	1
8	17½		595.405	.30	1.14	91	247	248	61	89	—	1
9	20		598.810	.75	2.86	89	250	250	63	89	—	5
10	22½		599.010	.45	1.71	95	250	250	63	89	—	4
11	25		600.709	.45	1.71	95	250	250	65	89	—	4
12	27½		602.507	.40	1.52	93	250	250	65	89	—	3
	30/OFF		604.315									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Claytonville	3-19-92	Press Vent # 7	M-5 / M 202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		604.315	.50	1.90	91	250	250	60	88	–	3
2	2½		606.205	.53	2.02	85	250	250	55	84	–	3
3	5		608.104	.40	1.52	93	249	250	55	88	–	3
4	7½		610.000	.25	0.95	90	249	250	55	88	–	3
5	10		611.502	.15	0.57	88	249	249	55	87	–	1
6	12½		612.710	.05	.19	93	249	249	55	87	–	1
7	15		613.404	.25	0.95	90	249	250	55	87	–	2
8	17½		614.805	.20	.76	87	249	250	55	86	–	1
9	20		616.004	.25	0.95	90	249	250	55	86	–	2
10	22½		617.402	.47	1.79	94	249	250	55	86	–	3
11	25		619.105	.55	2.09	92	249	250	55	86	–	3
12	27½		621.010	.55	2.09	93	249	250	55	86	–	4
	60/OFF	16.29	622.708									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P. Press Vent #7 Sampling Date(s): _____

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	~~576.6~~ 575.3	589.6	467.5				743.7
Initial Wt.	~~466.5~~	588.3	466.7				735.3
Net Weight	1.3	1.3	0.8				8.4

Total Moisture = 11.8 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue - Purple Percent Spent: 30% %
Filter I.D. No.: F-374 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	614.0	569.7	452.8				750.4
Initial Wt.	611.8	568.0	452.4				741.7
Net Weight	2.2	1.7	0.4				8.7

Total Moisture = 13.0 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue-White Percent Spent: 10% %
Filter I.D. No.: F-377 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	579.6	585.9	~~469.~~ 467.9				~~752.3~~ 743.8
Initial Wt.	578.3	585.6	466.3				~~578.3~~
Net Weight	1.3	0.3	1.6				8.5

Total Moisture = 11.7 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue - purple Percent Spent: 25% %
Filter I.D. No.: F-379 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON	3/18/92	PRESS VENT #8	M5/M202	#1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B RAYFIELD	29.85	0.03	61	GLASS/F-366	56"	0.84	5' GLASS	K25	0.235

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL. FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	5A	PT 14	—	—	17"	0.005	10"	0.0	3.49

EPA METHOD 3
Collection Method: DIRECT
Analysis Method: FYRITE

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2					
%CO2					

PITOT SYSTEM LEAK CHECK: INIT ✓ FINAL ✓

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0	12:40	946.313	0.14	0.489	~~249~~ 65	248	248	63	64		1
2	2.5		947.14	0.45	1.57	77	248	251	62	64		1
3	5		948.80	0.45	1.57	77	248	247	48	65		1
4	7.5		950.34	0.25	0.87	75	245	251	46	65		1
5	10		951.57	0.22	0.77	72	247	253	48	66		1
6	12.5		952.75	0.11	0.38	74	246	250	49	66		1
7	15		953.62	0.2	0.84	72	248	250	50	67		1
8	17.5		954.67	0.14	0.49	71	247	248	50	68		1
9	20		955.66	0.2	0.84	71	246	248	50	67		1
10	22.5		957.07	0.49	1.71	76	247	248	49	67		2
11	25		958.52	0.57	1.99	72	246	254	49	67		2
12	27.5		960.28	0.57								
—	30	13:10	962.067									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC / CLAYTON	3/18/92	PRESS VENT 8	M5/202	#1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP. (F)	PROBE TEMP. (F)	FILTER OVEN TEMP. (F)	SIL GEL IMPINGER TEMP. (F)	DGM IN/OUT TEMP. (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	0	13:20	962.067	0.36	1.26	75	245	247	60	67		1
2	2.5		963.50	0.38	1.33	75	247	247	52	67		2
3	5		964.96	0.52	1.82	78	246	248	51	67		2
4	7.5		966.67	0.73	2.55	74	248	250	49	67		2
5	10		968.63	0.91	3.18	70	247	249	48	68		3
6	12.5		970.88	0.25	0.87	72	247	248	48	68		1
7	15		972.30	0.25	0.87	70	248	247	52	68		1
8	17.5		973.54	0.77	2.68	69	248	246	53	63		3
9	20		975.57	0.82	2.86	71	249	249	52	69		3
10	22.5		977.78	0.58	2.02	74	248	246	53	70		2
11	25		979.56	0.45	1.57	70	245	251	53	69		2
12	27.5		981.17	0.52	1.82	69	245	248	54	69		2
END	30/60	13:50	982.919								✓	

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

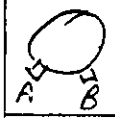
Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON AL	3/1/92	PRESS VENT 8	M5/M202	#2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B. RAYFIELD	29.58	0.03	66	GLASS/F367	56"	0.84	5' GLASS	K25	0.235

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	5A	PT14	—	—	12"	0.008	12"	0.010	3.49



EPA METHOD 3
Collection Method: DIRECT
Analysis Method: FYRITE

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2			→	21	21
%CO2			→	0	0

PITOT SYSTEM LEAK CHECK: INIT ✓ FINAL ✓

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0	7:53	983.044	0.16	0.56	73	245	246	59	65		1
2	2.5		984.04	0.22	0.77	82	246	245	56	66		1
3	5		985.18	0.19	0.66	82	247	251	54	67		1
4	7.5		986.27	0.49	1.71	78	251	249	53	67		2
5	10		987.89	0.80	2.79	76	245	250	50	68		2
6	12.5		989.97	0.29	1.01	75	246	251	51	69		1
7	15		991.38	0.29	1.01	78	243	249	50	69		1
8	17.5		992.70	0.66	2.30	75	244	247	49	69		3
9	20		994.58	0.93	3.25	73	245	248	49	70		4
10	22.5		996.91	0.49	1.71	75	244	247	48	71		2
11	25		998.62	0.36	1.26	78	248	248	50	71		2
12	27.5		1000.06	0.36	1.26	75	249	248	51	71		2
—	30		001.478									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL.	3/19/92	PRESS VENT #5	M5/202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.52	-0.30		F 375	62"	0.84	6A GLASS	D-8	~~0.470~~ 0.241

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M-8	1.88	~~0.998~~ 1.005	6A5	PT-1	64		15.0	0.005	15.0	0.002	3.50

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					✓	✓
Analysis Method	PYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0/0	1135	85.49	0.33	1.16	94	247	254	60	84	—	3.0
2	2.5		90.03	.56	1.96	101	248	254	50	84		5.0
3	5		91.90	.64	2.31	100	250	252	50	85		6.0
4	7.5		94.00	.84	2.94	98	257	254	50	85		7.0
5	10		96.36	.50	1.75	98	251	255	50	86		5.0
6	12.5		98.19	.35	1.23	98	250	253	51	86		3.5
7	15		99.70	.18	.63	98	250	253	52	86		2.5
8	17.5		100.82	.41	1.44	95	251	254	53	86		4.0
9	20		102.44	.72	2.52	95	253	250	52	86		6.0
10	22.5		104.70	.85	~~2.98~~	95	254	250	51	87		6.5
11	25		106.98	.52	1.82	97	254	249	52	88		5.0
12	27.5		108.34	.64	2.24	97	252	251	53	88		6.0
B1	30/0	1205/1207	110.86	.40	1.40	100	251	253	54	87		4.0

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/19/92	PRESS VENT 5	M5/202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
02	2.5		112.51	0.68	2.38	99	253	255	52	87	—	6.0
3	5		114.60	.63	2.21	102	252	254	52	87		6.0
4	7.5	1212/12.A	116.81	.77	2.70	102	251	253	52	88		6.0
5	10		118.89	.50	1.75	102	250	252	54	87		5.0
6	12.5		120.71	.24	.84	100	251	253	54	88		3.0
7	15		122.00	.28	.98	98	249	251	54	88		3.0
8	17.5		123.41	.74	2.59	97	250	254	54	88		6.0
9	20		125.61	.93	3.26	97	249	253	54	88		8.5
10	22.5		128.16	.67	2.35	98	249	250	54	88		5.0
11	25		130.14	.28	.98	97	250	251	54	88		3.0
12	27.5		131.56	.23	.81	97	248	250	54	88		2.5
	30/60	1241	132.854									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P. Clayton Ala. #5 PRESS VENT Sampling Date(s): 3/19/92

RUN No.: #1 ~~Recovery Date:~~ Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	564.0	563.9	482.2				741.7
Initial Wt.	564.5	558.1	481.1				731.5
Net Weight	-.5	5.8	1.1				10.2

Total Moisture = 16.6 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F-372 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: #2 Recovery Date: Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	597.6	592.3	459.6				743.2
Initial Wt.	595.1	589.7	457.7				731.8
Net Weight	2.5	2.6	1.9				11.4

Total Moisture = 18.4 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F-373 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: #3 Recovery Date: Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	583.0	569.6	481.2				750.0
Initial Wt.	580.6	567.7	481.6				741.7
Net Weight	2.4	1.9	-0.4				8.3

Total Moisture = 12.2 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: ~~F-357~~ 375 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON	3/19/92	PRESS VENT 8	M5/202	#2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A-1	0	8:30	001.478	0.59	2.06	78	241	251	56	70		2
2	2.5	8:32	003.32	0.50	1.75	80	243	247	59	73		2
3	5	8:58	005.00	0.43	1.50	89	248	245	55	74		2
4	7.5		006.57	0.58	2.02	84	249	248	54	75		3
5	10		008.38	0.20	0.70	80	245	250	50	75		1
6	12.5		009.52	0.25	0.87	81	243	248	51	76		1
7	15		010.75	0.25	0.87	86	244	247	51	76		2
8	17.5		012.02	0.27	0.94	80	249	251	51	76		2
9	20		013.31	0.35	1.22	81	247	248	52	77		2
10	22.5		014.76	0.58	2.02	86	247	246	52	78		3
11	25		016.60	0.56	1.95	83	247	247	51	78		3
12	27.5		018.37	0.73	2.55	79	245	250	51	78		3
END	30/60		020.409									

STOPPED 8:32:30 PLANT PROBLEM?

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

iea

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC/CLAYTON AL	3/19/92	PRESS VENT #8	M5/202	#3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B RAYFIELD	29.58	+0.01	74	GLASS/F371	56"	0.84	5' A GLASS	K25	0.235

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	5A	PTA	—	—	0.010	11"			3.49

A - B

EPA METHOD 3
Collection Method: DIRECT DRAW
Analysis Method: FYRITE

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2			→	21	21
%CO2			→	0	0

PITOT SYSTEM LEAK CHECK: INIT ✓ FINAL

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0	9:53	020.551	0.09	0.31	89	240	242	63	78		0
2	2.5		021.32	0.29	1.01	86	248	248	64	79		1
3	5		022.60	0.14	0.49	90	252	253	61	79		1
4	7.5		023.60	0.45	1.57	91	251	249	61	80		2
5	10		025.20	0.72	2.51	86	247	247	57	80		3
6	12.5		027.26	0.27	0.94	84	248	250	56	82		1
7	15		028.58	0.27	0.94	89	247	248	57	82		1
8	17.5		029.91	0.81	2.83	86	245	248	58	83		3
9	20		032.05	0.9	3.14	83	247	250	57	83		4
10	22.5		034.38	0.45	1.57	83	245	250	58	84		2
11	25		036.05	0.38	1.32	88	249	248	59	84		2
12	27.5		037.51	0.29	1.01	84	248	248	59	83		2
—	30	10:23	038.922	—								

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON AL	3/19/92	PRESS VENT 8	M5/202	#3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
A-1	0	10:27	038.922	0.40	1.40	89	242	247	63	82		2
2	2.5		040.44	0.45	1.57	88	245	248	62	83		2
3	5		042.09	0.47	1.64	88	244	247	61	83		2
4	7.5		043.75	0.45	1.57	91	246	248	60	84		2
5	10		045.40	0.44	1.54	88	246	246	60	83		2
6	12.5		047.04	0.11	0.38	87	243	248	62	83		2 1
7	15		047.93	0.32	1.12	89	245	248	62	83		2
8	17.5		049.27	0.19	0.66	90	245	247	62	84		1
9	20		050.42	0.32	1.12	86	246	245	63	84		2
10	22.5		051.81	0.40	1.40	87	240	248	63	85		2
11	25		053.38	0.60	2.10	93	240	249	64	84		2
12	27.5		055.23	0.75	2.61	90	245	250	64	85		3
END	30/60		057.335									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P./Press Vent 8 Sampling Date(s): _____

RUN No.: #1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	600.4	564.1	458.4				733.8
Initial Wt.	594.7	559.4	457.2				726.7
Net Weight	5.7	4.7	1.2				7.1

Total Moisture = 18.7 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue-White (New) Percent Spent: _____ %
Filter I.D. No.: F-366 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: #2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	603.9	588.3	468.5				689.0
Initial Wt.	596.4	585.8	468.0	468.0			680.7
Net Weight	7.5	2.5	0.5				8.3

Total Moisture = 18.8 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue-white (New) Percent Spent: 10% %
Filter I.D. No.: F-367 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: #3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	606.5	560.1	452.7				741.7
Initial Wt.	601.8	557.9	451.5				733.8
Net Weight	4.7	2.2	1.2				7.9

Total Moisture = 16.0 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue-white Percent Spent: 5% %
Filter I.D. No.: F-371 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

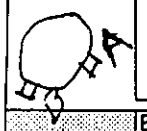
NOTES: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/17/92	Press Vent # 9	M-5/M202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S, Terll	30.02	-.29	79°	F 357	56"	0.84	5A	8-B	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M-7	1.87	1.002	T-5A	Pt.14	#2	—	15	0.004	7	0.000	3.81



EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite Grab	%O2	20.9					✓	✓
Analysis Method		%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	14:56	270.057	0.14	0.53	83	247	245	63	81	—	2
2	2½		272.710	.24	0.91	85	246	250	48	80	—	2
3	5		273.809	.35	1.33	82	246	250	48	80	—	3
4	7½		275.410	.72	2.74	82	246	250	49	80	—	3
5	10		277.308	.78	2.97	83	246	250	49	81	—	5
6	12½		279.705	.25	0.95	82	246	250	49	81	—	2
7	15		281.403	.07	.26	82	245	250	49	81	—	1
8	17½		282.407	.43	1.64	81	245	250	52	81	—	3
9	20		283.808	.72	2.97	84	245	250	55	81	—	5
10	22½		286.900	.35	1.33	83	245	250	55	81	—	5
11	25		287.701	.39	1.48	81	247	250	55	81	—	5
12	27½		289.401	.35	1.33	82	245	250	57	81	—	5
	30/OFF		290.964									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3-17-92	Press Vent # 9	M-5/M 202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		290.964	.15	.57	81	247	250	59	79	–	1
2	2½		292.102	.14	.53	83	247	250	59	79	–	1
3	5		293.100	.37	1.41	88	247	250	58	80	–	3
4	7½		294.665	.39	1.48	85	248	250	55	80	–	3
5	10		296.304	.29	1.10	85	249	250	55	80	–	2
6	12½		297.805	.24	.91	82	249	250	56	80	–	2
7	15		299.108	.32	1.22	82	249	250	56	80	–	2
8	17½		300.608	.50	1.90	80	249	250	56	80	–	2
9	20		302.408	.37	1.41	81	249	250	56	80	–	2
10	22½		304.107	.37	1.41	81	249	250	56	80	–	2
11	25		305.709	.39	1.48	82	249	250	56	80	–	2
12	27½		307.408	.30	1.14	82	249	250	56	80	–	2
	60/OFF	15:59	309.005									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/17/92	Press Vent # 9	M-5/M 202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrell BR	30.02	-.29	75	F 359	56"	0.84	5-A	8-B	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M-7	1.87	1.002	T.5A	7+14	H-2	–	15	0.002	10	0.000	3.81

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fyrite	%O2						✓	✓
Analysis Method	–	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	16:28	309.355	.15	.57	81	243	242	62	77	–	1
2	2½		310.502	.30	1.14	83	243	245	62	77	–	2
3	5		311.801	.41	1.56	84	243	245	62	77	–	2
4	7½		313.407	.83	3.12	81	243	245	62	77	–	3
5	10		315.506	.85	3.24	81	244	245	62	78	–	3
6	12½		317.910	.35	1.33	81	244	245	62	78	–	3
7	15		319.804	.08	0.30	80	244	245	62	78	–	2
8	17½		321.106	.60	2.28	79	244	245	62	78	–	2
9	20		322.709	.65	2.48	79	244	245	62	78	–	2
10	22½		324.910	.33	1.26	81	244	245	62	77	–	3
11	25		326.504	.35	1.33	80	246	249	62	77		4
12	27½		328.203	.39	1.48	78	246	249	62	78	–	3
	30/off		329.708									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3-17-92	Press Vent # 9	M-5 / M202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		329.708	0.07	1.26	77	249	250	62	76	—	1
2	2½		330.503	.13	0.49	79	249	250	62	76	—	1
3	5		331.406	.15	.57	80	249	250	62	76	—	1
4	7½		332.504	.33	1.26	81	249	250	62	76	—	1
5	10		333.999	.41	1.56	80	249	250	62	76	—	2
6	12½		335.607	.27	1.03	80	249	250	60	76	—	2
7	15		337.204	.32	1.22	80	249	250	60	76	—	2
8	17½		338.785	.35	1.33	77	249	250	60	76	—	2
9	20		340.309	.73	2.78	78	249	250	60	76	—	5
10	22½		342.403	.37	1.41	79	249	250	60	75	—	3
11	25		340.907	.39	1.48	77	249	250	60	75	—	3
12	27½		345.101	.32	1.22	77	249	250	60	74	—	3
	60/OFF	17:41	347.307									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/1/92	Press Vent #9	M5/M202	3

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Stern/BR	30.02	-.29	79°	F 361	56 4	0.84	5-A	8-B	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M07	1.898	1.002	T-5A	Pt 14	H-2	—	15	0.000	10	0.000	K= 3.81

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Fyrite	%O2	20.9				✓	✓	✓
Analysis Method:	%CO2	—				✓		

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A-1	0/0	18:07	347.581	.23	.88	76	240	247	59	71	—	1.5
2	2½		348.907	.27	1.03	80	240	247	53	71	—	2
3	5		350.403	.30	1.14	80	240	247	53	71	—	2
4	7½		351.906	.78	2.97	77	240	247	53	71	—	5
5	10		354.107	.82	3.12	77	245	249	53	72	—	5
6	12½		356.410	.27	1.03	79	247	249	54	73	—	4
7	15		358.005	.07	.26	76	247	249	54	73	—	1
8	17½		358.905	.42	1.60	75	247	249	54	71	—	5
9	20		360.306	.53	2.22	78	247	249	54	71	—	5
10	22½		362.401	.37	1.41	75	250	250	54	72	—	4
11	25		364.007	.35	1.37	75	250	250	52	72	—	3
12	27½		365.605	.35	1.33	75	250	250	52	72	—	3
	30		367.175									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AK	3-17-92	Press Vent #9	M-5/M202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		367.175	0.07	.26	74	250	250	54	70	-	1
2	2½		367.903	0.07	.26	75	250	250	54	70	-	1
3	5		368.606	0.09	.34	78	250	250	53	70	-	1
4	7½		369.501	0.41	1.56	76	250	250	53	70	-	4
5	10		370.007	.35	1.33	75	250	250	53	70	-	5
6	12½		372.606	.27	1.03	77	250	250	53	71	-	4
7	15		374.105	.25	.95	73	250	250	53	71	-	3
8	17½		375.505	.31	1.18	71	250	250	50	70	-	3
9	20		376.999	.43	1.64	74	250	250	50	71	-	3
10	22½		378.710	.35	1.33	72	250	250	50	71	-	3
11	25		380.209	.31	1.64	71	250	250	50	71	-	3
12	27½		381.905	.31	1.64	70	250	250	50	71	-	3
	60/OFF	19:09	383.585									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P. Press Vent 9 Sampling Date(s): _____

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	567.2	578.8	486.6				769.8
Initial Wt.	565.7	578.3	486.7				762.3
Net Weight	1.5	0.5	-0.1				7.5

* Total Moisture = 9.1 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue Percent Spent: 25% %
Filter I.D. No.: F-357 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	571.5	573.5	466.6				719.4
Initial Wt.	572.7	574.1	466.6				709.4
Net Weight	-1.2	-0.6	0				10.0

Total Moisture = 8.2 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue (new) Percent Spent: 5% %
Filter I.D. No.: F-359 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	561.9	583.0	486.3				775.5
Initial Wt.	560.5	582.0	486.2				769.8
Net Weight	1.4	1.0	0.1				5.7

Total Moisture = 8.2 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue-purple Percent Spent: 25% %
Filter I.D. No.: F-361 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

3/18/92 (J Johnson 3/24/92)

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/18/92	Press Vent # 10	M-5-/M202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S Terrill	29.85	-.20	61°	F-363	56"	0.84	C-9	B-8	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M-1	1.87	1.002	T-C9	9 at	HT2	—	15	0.003	10	0.000	3.81

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Fyrite	%O2	20.9					✓	✓
Analysis Method: —	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	09:14	383.798	.49	1.87	76	249	250	54	61	—	3
2	2½		385.702	.70	2.67	79	249	250	54	62	—	5
3	5		387.605	.20	0.76	82	249	250	49	62	—	1
4	7½		389.203	.15	.57	81	249	250	50	62	—	1
5	10		390.310	.10	.29	81	249	250	50	62	—	1
6	12½		391.204	.10	.29	81	249	250	50	62	—	1
7	15		392.001	.07	.26	79	249	250	50	62	—	1
8	17½		392.704	.07	.26	79	249	250	50	62	—	1
9	20		393.409	.20	0.76	78	249	250	50	62	—	1
10	22½		394.604	.20	0.76	78	249	250	50	62	—	1
11	25		395.810	.22	0.84	74	249	250	50	62	—	1.5
12	27½		397.110	.25	.95	77	249	250	50	62	—	1.5
	30 OFF		398.402									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

3/18/92 (J Thomas 3/24/92)

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AR	3/18/92	Press Vent # 10	m-5 / m 202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		398.402	.32	1.32	76	249	249	56	63	–	2
2	2½		400.010	.57	2.17	79	251	250	56	63	–	2
3	5		401.403	.65	2.48	78	251	250	56	63	–	2
4	7½		403.110	.57	2.17	77	251	250	56	63	–	2
5	10		404.610	.55	2.09	77	251	250	56	63	–	2
6	12½		406.065	.15	.57	80	251	250	56	63	–	2
7	15		407.207	.32	1.22	79	249	250	56	63	–	2
8	17½		408.704	.70	2.67	78	249	250	56	63	–	2
9	20		410.304	.88	3.35	81	249	250	56	63	–	2
10	22½		412.605	.22	.84	81	249	250	56	63	–	2
11	25		414.310	.07	.26	80	249	250	56	63	–	2
12	27½		413.004	.20	0.76	81	249	250	56	63	–	2
	30/OFF	10:18	416.125									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/4/92	Press Vent # 10	M-5 / M202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
STerll	24.58	-.20	65°	F-363 369	56"	0.84	C-S SS	B-8	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	m-7	1.87	1.002	CT-5	C S-4	H-4	—	15	0.061	10	0.000	3.81

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Fyrite - Grab	%O2						✓	✓
Analysis Method:	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	07:32	424.714	.52	1.98	81	247	251	66	66	—	2
2	2½		426.604	.65	2.48	84	247	251	63	67	—	3
3	5		428.610	.57	2.17	84	248	247	62	68	—	3
4	7½		430.610	.25	.95	86	248	247	63	68	—	3
5	10		432.202	.20	.76	86	248	247	63	68	—	3
6	12½		433.355	.08	.30	83	248	247	62	69	—	1
7	15		434.202	.05	.19	82	248	247	63	70	—	1
8	17½		434.902	.25	.95	82	247	247	63	70	—	1.5
9	20		436.102	.33	1.26	83	250	249	61	72	—	2
10	22½		437.406	.60	2.29	82	250	249	62	74	—	4
11	25		439.310	.80	3.05	81	250	249	62	74	—	5
12	27½		441.606	.70	2.67	83	250	249	60	74	—	5
	30		443.827									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/19/92	Press Vent # 10	m5/m202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		443.827	.55	2.09	81	250	250	66	74	–	5
2	2½		445.709	.60	2.29	82	250	250	59	73	–	5
3	5		447.802	.63	2.40	85	250	250	59	73	–	5
4	7½		449.806	.75	2.86	82	250	250	59	73	–	5
5	10		452.010	.60	2.29	85	250	250	59	73	–	5
6	12½		444.110	.15	.57	87	250	250	60	76	–	1
7	15		455.325	.33	1.26	85	250	250	60	75	–	2
8	17½		456.706	.63	2.40	84	250	250	60	75	–	4
9	20		458.703	.75	2.86	87	250	250	60	76	–	4
10	22½		460.809	.40	1.52	86	250	250	60	76	–	4
11	25	0832 STOP	462.608	.60	2.29	80	250	250	62	80	–	4
12	27½		464.509	.53	2.02	79	250	250	62	80	–	4
	60/~~OFF~~		46									
		0.901	466.543									

START 0855

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clinton, AL	3/19/92	Press Vent # 10	M-5 / M 202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Tarll	29.58	-.20	65	F 370	56"	0.84	C-5 SS	13-8	.242

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M-7	1.87	1.002	CT-5	154	H-4	—	15	0.000	10	0.000	K=3.81

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Fyrite	%O2	20.9					✓	✓
Analysis Method:	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	09:38	466.688	.48	1.83	93	250	250	65	85	—	4
2	2½		468.602	.60	2.29	92	250	250	63	86	—	4
3	5		470.704	.43	1.64	94	250	250	63	87	—	4
4	7½		472.310	.20	.76	95	250	250	64	88	—	2
5	10		473.605	.10	.38	92	250	250	64	88	—	1
6	12½		474.605	.39	1.48	93	250	250	64	88	—	3
7	15		475.907	.05	.19	93	250	250	64	88	—	3
8	17½		477.702	.20	.76	87	250	250	64	87	—	3
9	20		478.805	.33	1.26	89	250	250	64	87	—	2
10	22½		480.410	.63	2.40	88	250	250	64	89	—	4
11	25		482.303	.75	2.86	89	250	250	64	89	—	4
12	27½		484.505	.60	2.29	89	250	250	64	89	—	5
	30/off		486.607									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON AL	3-19-92	Press Vent #10	M-5 / M202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-1	30/0		486.607	.43	1.64	92	250	250	63	90	–	3
2	2½		488.405	.53	2.02	91	250	250	63	90	–	5
3	5		490.303	.70	2.67	92	250	250	63	90	–	5
4	7½		492.403	.68	2.59	94	250	250	63	90	–	5
5	10		494.673	.55	2.09	92	250	250	63	90	–	3
6	12½		496.801	.10	.38	93	250	250	63	90	–	1
7	15		497.825	.29	1.12	95	250	250	63	90	–	2
8	17½		499.202	.53	2.02	94	250	250	62	92	–	4
9	20		501.005	.94	3.58	92	250	250	62	92	–	4
10	22½		503.502	.53	2.02	93	250	250	64	92	–	4
11	25		505.408	.47	1.79	92	250	250	64	93	–	3
12	27½		507.504	.33	1.26	91	250	250	64	93	–	2
	60/OFF	10.44	508.903									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P./ Press Vent #10 Sampling Date(s): 3/17/92

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	569.8	574.5	466.1				726.6
Initial Wt.	567.3	574.5	466.6				719.4
Net Weight	2.5	0.0	-0.5 *				7.2

Total Moisture = 9.2 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue Percent Spent: _____ %
Filter I.D. No.: F-363 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.							
Initial Wt.	570.1	591.1	486.5				775.5
Net Weight							

VOID Broken Train

Total Moisture = _____ grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: F-365 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	590.5	582.4	472.9				735.3
Initial Wt.	587.8	585.3	465.9				726.6
Net Weight	2.7	-2.9	7.0				8.7

Total Moisture = 15.5 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue ~~[illegible]~~ gm Percent Spent: 10% %
Filter I.D. No.: F-368 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P./Press Vent #10 Sampling Date(s): 3/17/92

RUN No.: 3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	574.8	598.4	472.3	X	X	X	782.2
Initial Wt.	569.9	595.1	470.7	X	X	X	776.6
Net Weight	4.9	3.3	1.6	X	X	X	5.6

Total Moisture = 15.4 grams

Description of Impinger Contents: _____

Silica Gel Color: Blue-Purple Percent Spent: 25% %

Filter I.D. No.: F-370 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: _____ Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.							
Initial Wt.							
Net Weight							

Total Moisture = _____ grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: _____ Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: _____ Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.							
Initial Wt.							
Net Weight							

Total Moisture = _____ grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: _____ Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

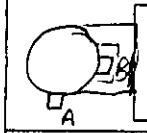
BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/1/92	Boiler Stack # 7	M-5 / 202	#1

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B. Rayfield S. Terrell	30.05	0.0	67	Glass Fiber / F350	58"	0.84	6' Glass	~~15~~ ~~12~~ B	~~.369~~ 0.473

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M-7	1.87	1.002	6-B	6B	—	—	0.015	13"	22	0.005	~~13.76~~ 35.28



EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Tedlar Bag	%O2	14.5	14.5	14.5	14.5	21	✓	✓
Analysis Method	Orsat/Fyrite	%CO2	6.5	6.5	6.5	6.5	0		

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A-1	0	17:10	116.791	0.06	2.12	215	250	248	62	73		5
2	3	17:13	119.29	0.06	2.12	194	250	247	55	72		5
3	6	17:16	121.78	0.07	2.47	271	249	247	52	73		7
4	9	17:19	124.16	0.08	2.82	276	249	246	53	73		8
5	12	17:22	126.78	0.08	2.82	275	248	248	56	73		8
6	15	17:25	129.40	0.08	2.82	274	248	247	56	73		9
7	18	17:28	132.04	0.08	2.82	274	249	241	59	72		10
8	21	17:31	134.67	0.08	2.82	270	249	247	60	72		10
9	24	17:34	137.30	0.08	2.82	270	248	248	61	72		12
10	27	17:37	139.93	0.05	1.76	185	248	255	61	67		9
B-1	30	17:45	142.63	0.07	2.47	234	249	249	61	68		11
2	33	17:48	145.03	0.07	2.47	261	249	247	61	68		11
3	36	17:51	147.50	0.08	2.82	267	245	247	62	67		13

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

BOILER STACKS

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC/CLAYTON AL	3/16/92	BOILER STACK #1	M5/202	#1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-4	39	17:54	150.07	0.08	2.82	271	241	247	61	69		15
5	42	17:57	152.69	0.09	3.18	271	245	248	61	68		17
6	45	18:01	155.47	0.09	3.18	269	247	248	61	68		20
7	48	18:04	158.27	0.09	3.10	269	247	248	61	67		20
8	51	18:07	160.00	0.09	3.00	270	249	249	60	67		20
9	54	18:10	163.71	0.08	2.82	268	249	249	61	71		20
10	57	~~18:13~~	166.405	0.05	1.76	266	2	248	64	71		20
	60	18:18	168.787									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC / CLAYTON AL	3/17/92	BOILER STACK #1	M5 / M202	RUN #2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
BRAYFIELD / S. TERLL	30.02	0.0	68	GLASS / F351	58"	0.84	6' GLASS	15-B	0.473

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M-7	1.87	1.002	6-B	6-B	—	—	16"	0.017	21"	0.012	35.28

EPA METHOD 3
Collection Method: TEDLAR
Analysis Method: FYRITE

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	14.5	14.5	14.5	14.5	21
%CO2	6.5	6.5	6.5	6.5	0

PITOT SYSTEM LEAK CHECK: INIT. ✓ FINAL ✓

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B-1	0	8:33	169.700	0.04	1.41	236	248	248	56	62		5
2	3	8:36	171.71	0.06	2.12	233	247	248	56	64		6
3	6	8:39	173.92	0.07	2.46	261	247	248	56	66		7
4	9	8:42	176.33	0.08	2.82	268	248	248	50	67		9
5	12	8:45	179.90	0.07	2.46	272	247	251	50	71		10
6	15	8:48	181.40	0.08	2.82	274	248	249	54	72		11
7	18	8:51	184.00	0.08	2.82	273	246	247	58	73		12
8	21	8:54	186.61	0.08	2.82	273	247	247	61	74		13
9	24	8:57	189.23	0.07	2.46	274	249	248	61	76		12
10	27	9:00	191.67	0.06	2.12	274	250	249	64	76		11
~~B~~	30	9:03	194.008									
A B-1	0	9:15	194.008	0.04	1.41	160	246	247	63	77		7
2	3	9:18	195.94	0.05	1.76	245	251	242	56	77	✓	9

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON AL	3/17/92	BOILER STACK #1	M5/M202	RUN #2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
A-3	6	9:21	198.01	0.07	2.46	272	249	245	56	78		13
4	9	9:24	200.42	0.08	2.82	277	250	248	57	79		16
5	12	9:27	203.04	0.08	2.82	276	249	247	60	80		17
6	15	9:30	205.67	0.08	2.82	275	250	251	60	82		18
7	18	9:33	208.29	0.08	2.82	279	249	248	65	83		19
8	21	9:36	210.99	0.08	2.82	278	248	249	65	83		20
9	24	9:39	213.68	0.08	2.82	278	247	248	66	83		20
10	27	9:42	216.30	0.07	2.46	276	250	251	65	85		20
END	30/60	9:45	218.826									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC/CLAYTON	3/17/92	BOILER STACK #1	M5/M202	RUN #3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
B. RAYFIELD S. TERLI	30.02	0.0	72	GLASS/F355	58"	0.84	6' GLASS	15B	0.473

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M-7	1.87	1.002	6-B	6-B	—	—	16"	0.008	16"	0.012	35.28

A

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	DIRECT DRAW	%O2					21		
Analysis Method	FYRITE	%CO2	6.5	6.			0	✓	✓

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0	10:46	219.169	0.05	1.76	232	248	242	66	83		4
2	3	10:49	221.38	0.05	1.76	195	250	249	62	89		4
3	6	10:52	223.50	0.08	2.82	283	249	247	60	91		7
4	9	10:55	226.15	0.08	2.82	286	251	249	58	91		7
5	12	10:58	228.82	0.08	2.82	287	249	251	58	90		8
6	15	11:01	231.52	0.08	2.82	287	250	251	60	92		8
7	18	11:04	234.18	0.08	2.82	290	249	250	61	93		9
8	21	11:07	236.88	0.08	2.82	288	249	249	61	92		9
9	24	11:10	239.54	0.08	2.82	287	249	248	61	93		10
10	27	11:13	242.21	0.07	2.46	287	249	248	62	94		10
—	30	11:16	244.757	—	—	—	—	—	—	—		—
B-1	0	11:25	244.757	0.04	1.41	205	247	249	62	95		6
2	3	11:28	246.70	0.06	2.12	265	246	248	62	95	↓	8

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA-PACIFIC / CLAYTON AL	3/17/92	BOILER STACK #1	M5/M202	RUN 3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B-3	6	11:31	249.00	0.07	2.46	282	246	248	61	95		9
4	9	11:34	251.49	0.07	2.46	280	248	248	60	93		10
5	12	11:37	254.02	0.07	2.46	287	248	247	62	95		10
6	15	11:40	256.53	0.07	2.46	285	247	249	63	94		10
7	18	11:43	259.04	0.08	2.82	286	248	248	64	96		12
8	21	11:46	261.71	0.08	2.82	287	245	248	65	96		13
9	24	11:49	264.40	0.08	2.82	285	246	248	65	95		14
10	27	11:52	267.07	0.08	2.82	287	248	249	66	95		14
END	30/60	11:55	269.755									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: L.P. Boiler Stack #1 Sampling Date(s): 3/16/ & 3/17/ 99

RUN No.: 1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	589.2	598.9	471.4				712.7
Initial Wt.	573.3	585.6	466.7				696.5
Net Weight	15.9	13.3	4.7				16.2

3/16

573.3 gsm

Total Moisture = 50.1 grams

Description of Impinger Contents: _____

Silica Gel Color: Blue - purple Percent Spent: 25% %

Filter I.D. No.: F-350 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	586.8	596.2	490.6				762.3
Initial Wt.	565.8	580.4	485.5				742.4
Net Weight	21.0	15.8	5.1				19.9

3/17

Total Moisture = 61.8 grams

Description of Impinger Contents: _____

Silica Gel Color: Blue - purple Percent Spent: 20% %

Filter I.D. No.: F-351 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: 3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	603.2	588.4	468.8				725.7
Initial Wt.	570.0	578.1	466.4				712.7
Net Weight	33.2	10.3	2.4				13.0

3/17

Total Moisture = 58.9 grams

Description of Impinger Contents: _____

Silica Gel Color: Blue - white - purple Percent Spent: 50% %

Filter I.D. No.: F-355 Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/4/92	#2 BOILER STACK	M5/M202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	30.05	0.0		F 352	58"	0.84	6A GLASS	D15	0.464

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M-8	1.88	0.998	GAS	PT-1	64	-	15.0	0.014	15.0	0.009	34.25

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	INTEGRATED BAG	%O2						✓	✓
Analysis Method	ORSAT	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	1518	593.552	0.04	1.37	295	252	254	62	85	—	4.0
2	3		595.45	.07	2.40	303	252	254	57	85		7.5
3	6		597.86	.07	2.40	305	253	254	49	85		7.5
4	9		600.35	.07	2.40	311	253	252	49	86		8.5
5	12		602.72	.06	2.06	313	253	252	50	86		8.0
6	15		605.05	.06	2.06	314	250	247	50	87		8.0
7	18		607.41	.06	2.06	314	252	249	50	88		8.0
8	21		609.55	.06	2.06	314	252	251	50	88		9.0
9	24		611.80	.06	2.06	313	251	253	52	88		8.5
10	27		614.10	.05	1.71	312	250	253	52	89		8.5
B 1	30/0	1548/1551	616.01	.02	.69	300	250	252	54	90		4.0
2	3		617.57	.03	1.03	305	251	252	54	90		4.0
3	6		619.18	.04	1.37	310	251	252	53	90		7.0

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/16/92	#2 BOILER STACK	M5/202	1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B4	9		621.00	0.06	1.37	312	251	253	52	91	—	7.5
5	12		622.90	.05	1.71	315	251	253	52	91		9.5
6	15		624.95	.05	1.71	316	252	254	51	91		9.5
7	18		627.05	.07	2.40	315	253	254	50	90		14.0
8	21		629.47	.05	1.71	316	250	252	50	90		11.0
9	24		631.66	.06	2.06	315	250	253	52	90		12.0
10	27		633.86	.04	1.37	313	250	252	52	90		9.5
	30/60	1621	635.776									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

Page ____ of ____

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/6/92	BOILER STACK 2	M5/202	2

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	30.05	0.0		F 353	58"	0.84	6A GLASS	D 15	0.464

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M-8	1.88	0.998	6A5	PT-1	64		15.0	0.015			34.25

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2							
Analysis Method	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A 1	0/0	1718	636.433	0.04	1.37	299	250	252	60	83	—	3.0
2	3		638.20	.04	1.37	305	251	253	56	82		3.0
3	6		640.06	.05	2.06	324	251	252	52	81		6.0
4	9		642.37	.07	2.40	324	252	253	52	81		7.0
5	12		644.65	.06	2.06	325	251	253	52	81		6.0
6	15		646.92	.05	1.71	326	251	253	54	79		6.0
7	18		649.05	.05	1.71	325	252	253	54	79		6.0
8	21		651.14	.04	1.37	327	252	254	55	79		5.0
9	24		653.02	.06	2.06	326	251	253	56	78		8.0
10	27		655.24	.05	1.71	323	253	251	56	78		8.0
B 1	30/0	1748/1752	657.34	.02	.69	305	252	251	56	78		9.0
2	3		658.67	.03	1.03	303	250	252	57	75		5.0
3	6		660.30	.04	1.37	315	246	251	57	75		6.0

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL.	3/16/92	BOILER STACK 2	M5/202	2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP. (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B4	9		662.07	0.05	1.71	322	250	252	57	74	—	8.0
5	12		664.10	.05	1.71	324	251	253	57	74		8.0
6	15		666.10	.06	2.06	325	253	252	57	74		10.0
7	18		667.22	.06	2.06	325	253	251	58	74		10.0
8	21		670.62	.07	2.40	326	253	253	58	74		13.0
9	24		672.80	.07	2.40	326	250	250	58	74		14.0
10	27		675.21	.05	1.71	324	251	250	58	74		11.0
	30/60	1022	677.309									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLANTON, AL	3/17/92	BOILER STACK 2	M5/202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	30.02	0.0		F354	58"		6A GLASS	D15	0.464

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M-8	1.88	0.998	6A-5	PT-1	64		15.0	0.011	15.0	0.015	34.55

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	INTEGRATED BAG	%O2							
Analysis Method	ORSAT	%CO2	9.0					✓	✓

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0/0	0844	677.695	0.03	1.04	290	251	250	54	61	—	4.0
2	3		679.42	.05	1.73	295	249	253	50	64		6.0
3	6		681.38	.05	1.73	310	250	252	48	67		6.0
4	9		683.43	.06	2.07	321	255	254	46	68		8.0
5	12		685.69	.06	2.07	324	254	253	46	67		9.0
6	15		687.92	.05	1.73	322	253	251	46	69		8.0
7	18		690.05	.05	1.73	324	251	249	48	70		8.0
8	21		692.09	.05	1.73	324	250	248	48	70		8.0
9	24		694.15	.04	1.38	322	257	249	48	71		8.0
10	27		696.06	.03	1.04	318	250	249	48	71		6.5
B 1	30/0	0914/0917	697.72	.03	1.04	300	251	250	48	71		6.5
2	3		699.38	.04	1.38	308	252	250	48	72		8.5
3	6		701.24	.03	1.04	317	251	250	48	72		7.0

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/17/91	BOILER STACK 2	M5/202	3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B4	9		702.92	0.04	1.38	320	250	252	47	72	—	9.0
5	12		704.69	.05	1.73	320	250	252	47	72		11.5
6	15		706.78	.06	2.07	321	253	249	47	72		14.5
7	18		709.04	.06	2.07	327	253	250	48	74		15.0
8	21		711.29	.05	1.73	328	252	251	49	74		14.0
9	24		713.27	.05	1.73	326	251	252	49	74		14.0
10	27		715.30	.04	1.38	325	253	250	49	76		13.0
	30/60	0947	717.403									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: Boiler Stack #2 Sampling Date(s): 3/16

RUN No.: #1 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	634.6	582.7	458.7				723.8
Initial Wt.	573.9	593.1	458.0				713.4
Net Weight	60.9	-10.4	+.7				10.4

Total Moisture = 61.4 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue - white Percent Spent: 20% %
Filter I.D. No.: 352 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: #2 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	595.6	567.5	484.2				727.6
Initial Wt.	565.2	549.7	479.4				714.7
Net Weight	30.4	17.8	4.8				12.9

Total Moisture = 65.9 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue - white Percent Spent: 20% %
Filter I.D. No.: F-353 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: #3 Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	642.2	596.0	458.6				732.2
Initial Wt.	596.3	588.0	457.6				723.8
Net Weight	45.9	8.0	1.0				8.4

Total Moisture = 63.3 grams

Description of Impinger Contents: _____
Silica Gel Color: Blue - purple - white Percent Spent: 50% %
Filter I.D. No.: F-354 Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton, AL	3/17/92	Former EX Stack 1	M-5 / M 202	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrell	29.83	-1.5	60°	F 357	17"	0.84	4-C	D5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
3	M-7	1.87	1.002	Tent	4-C	H-3	—	15	0.005	7	0.003	K- 0.60

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method: Fyrite	%O2	20.9					✓	✓
Analysis Method:	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	13:40	592.086	2.20	1.32	71	248	251	59	61	—	2
2	5		595.303	2.40	1.44	73	250	249	57	61	—	2
3	10		598.506	2.80	1.68	75	250	249	59	62	—	2
4	15		602.005	3.00	1.80	74	250	249	59	62	—	4
5	20		605.504	2.90	1.74	74	250	249	59	62	—	4
6	25		609.204	2.60	1.56	74	250	249	58	62	—	4
B-1	30/0		612.565	2.50	1.50	73	250	250	55	61	—	4
2	5		615.902	2.90	1.75	73	250	250	55	61	—	5
3	10		619.104	3.20	1.92	74	250	250	53	61	—	5
4	15		623.106	3.00	1.80	74	250	250	53	61	—	5
5	20		626.705	2.90	1.74	74	250	250	53	61	—	5
6	25		630.405	2.70	1.62	74	249	250	53	61	—	5
	60/OFF	16:45	633.817									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

FORMER STACK

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/12/92	Fromon Ex Stack #1	M-5 / 202	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S Terrell	29.83	-1.5	60	F-338	17"	0.84	4-13	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
3	M-7	1.87	1.002	T-43		64	—	15	0.000	10	0.000	.60

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Firite	%O2	20.9					✓	✓
Analysis Method		%CO2							

	TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
	A-1	0/0	17:30	634.688	2.60	1.56	71	250	248	58	59	—	2
	2	5		638.108	2.50	1.50	71	250	248	58	59	—	2
	3	10		641.404	2.90	1.74	71	250	248	58	59	—	2
Plant Problem	4	15		644.903	3.00	1.80	72	250	248	58	59	—	3
	5	20		648.505	2.70	1.62	72	250	248	58	59	—	3
Stop Test 24 min →	6	25		651.407	2.50	1.50	72	250	248	59	58	—	3
Start 18:15	B 1	30/0		655.302	2.60	1.56	70	248	248	62	57	—	3
	2	5		658.509	2.90	1.74	70	248	248	62	57	—	3
Stoped	3	10		661.995	3.00	1.80	71	248	248	62	57	—	3
	4	15		665.608	3.00	1.80	70	247	248	60	57	—	3
Stop	5	20		669.303	2.80	1.68	72	247	248	60	57	—	4
	6	25	19:10	672.801	2.70	1.62	72	247	248	60	57	—	5
		60/OFF		676.244									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton AL	3/13/92	Former Ex Stack # 1	M-5/M202	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
S. Terrell	29.84	-1.5	42°	F-339	17"	0.84	4-C	D-5	.155

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
3	M-7	1.87	1.002	T-4C	TH-C	C-4	—	15	0.006	8	0000	0.60

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Fisher	%O2 20.9					✓	✓
Analysis Method		%CO2						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A-1	0/0	07:30	676.410	2.10	1.26	69	245	247	52	47	—	2
2	5		679.208	2.60	1.56	71	245	247	59	48	—	2
3	10		682.408	3.00	1.80	72	248	247	50	49	—	4
4	15		686.009	3.10	1.86	72	251	248	61	51	—	5
5	20		689.705	2.80	1.68	72	251	248	61	52	—	5
6	25		693.105	2.50	1.50	73	251	248	61	53	—	5
B-1	30/0		696.442	2.50	1.50	71	249	248	60	52	—	5
2	5		699.705	2.80	1.68	71	249	248	60	53	—	5
3	10		703.103	3.00	1.80	73	248	248	60	54		5
4	15		706.606	3.20	1.92	73	248	248	60	55	—	6
5	20		710.209	2.90	1.74	72	250	249	58	55	—	5
6	25		713.805	2.80	1.68	72	250	249	58	56	—	5
	60/OFF	0834	717.416									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

L-P

Client/Location: Forme- Exaust Sampling Date(s): 3/12-3/13/92

RUN No.: Run #1 Recovery Date: 3/12 Recovered By: JM

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	582.8	582.0	459.5				822.2
Initial Wt.	589.7	578.3	457.3				811.0
Net Weight	-6.9	3.7	2.2				11.2

* Total Moisture = 10.2 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F337 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: #2 Recovery Date: 3/13 Recovered By: JM

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	570.0	594.8	467.6				728.9
Initial Wt.	585.0	592.6	466.3				715.0
Net Weight	-15.0	2.2	1.3				13.9

* Total Moisture = 2.4 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F338 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: #3 Recovery Date: 3/13 Recovered By: BR

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	581.5	576.3	459.4				833.1
Initial Wt.	587.6	573.0	457.6				822.2
Net Weight	-6.1	3.3	1.8				10.9

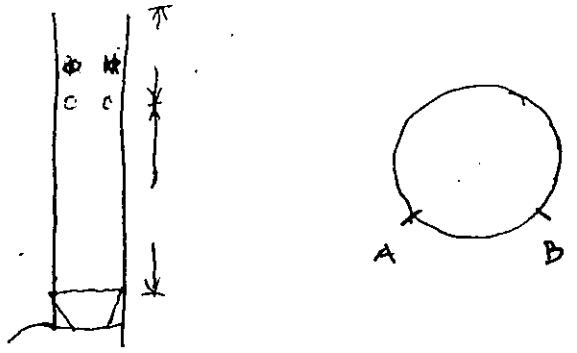
* Total Moisture = 9.9 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: F339 Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT LOUISIANA PACIFIC
CITY CLAYTON STATE ALABAMA
SAMPLING LOCATION DRYER STACK #1
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 42
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) ~~42~~ 0
NEAREST UPSTREAM DISTURBANCE
DISTURBANCE
NEAREST DOWNSTREAM DISTURBANCE
DISTURBANCE
SAMPLER S. TERILL DATE 3/13/92



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	0.021	42"			1"
2	.067				2 7/8
3	.118				5
4	.177				7 3/8
5	.25				10 1/2
6	.356				15
7	.644				27
8	.75				31 1/2
9	.823				34 5/8
10	.882				37
11	.933				39 1/8
12	.979				41 1/8

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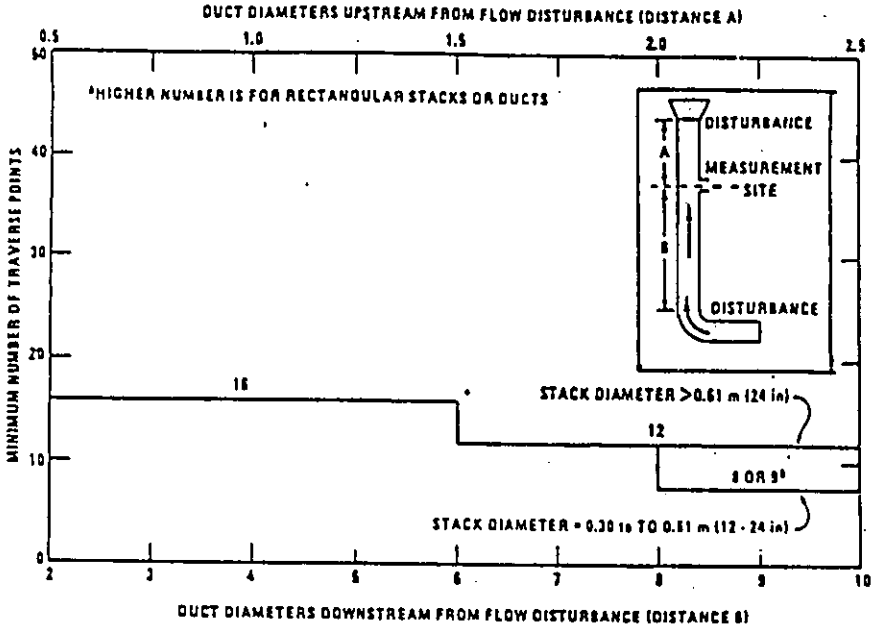


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

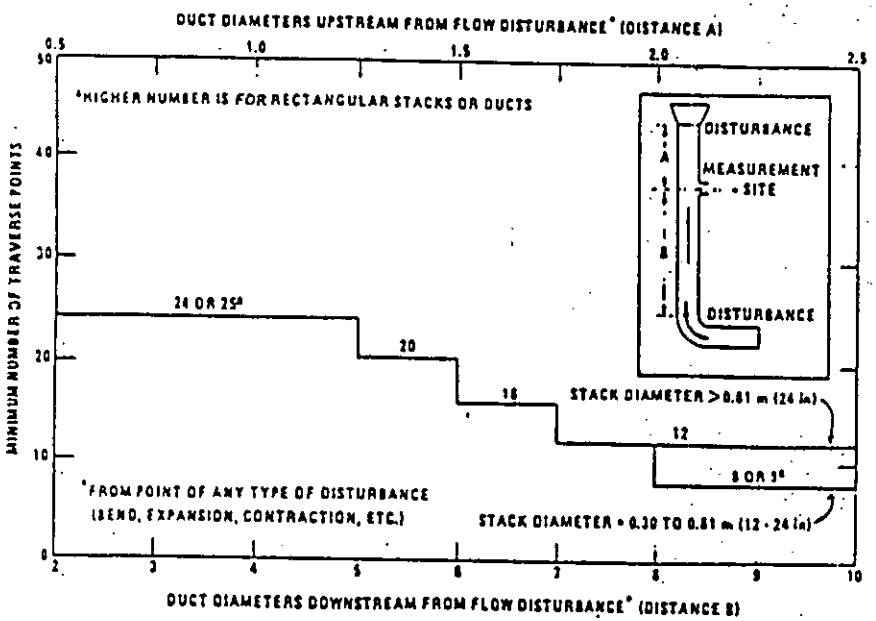


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

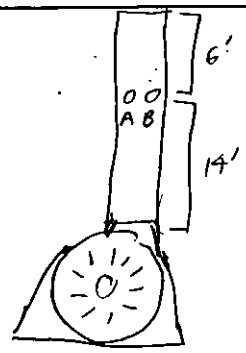
2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT L.P.
CITY Clayton STATE Ala
SAMPLING LOCATION Stack # 5
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 46"
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) 6"
NEAREST UPSTREAM DISTURBANCE 6'
DISTURBANCE EXIT
NEAREST DOWNSTREAM DISTURBANCE 14'
DISTURBANCE BLOWER TRANSITION
SAMPLER B. RAYFIELD DATE 3/12/92



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	2.1%	40"	7/8"	6"	6 7/8
2	6.7	↓	2 5/8"	↓	8 5/8
3	11.8		4 7/8"		10 7/8
4	17.7		7 1/8"		13 1/8
5	25.0		10"		16
6	35.6		14 1/4"		20 1/4
7	64.4		25 3/4"		31 3/4
8	75.0		30"		36
9	82.3		32 7/8"		38 7/8
10	88.2		35 1/4"		41 1/4
11	93.3		37 3/8"		43 3/8
12	97.9	↓	39 1/8"	↓	45 1/8

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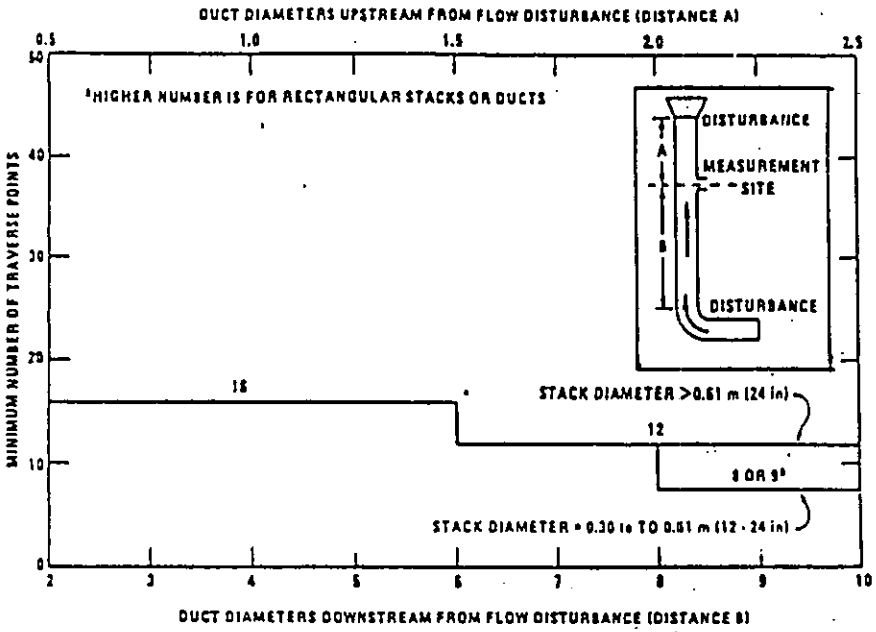


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

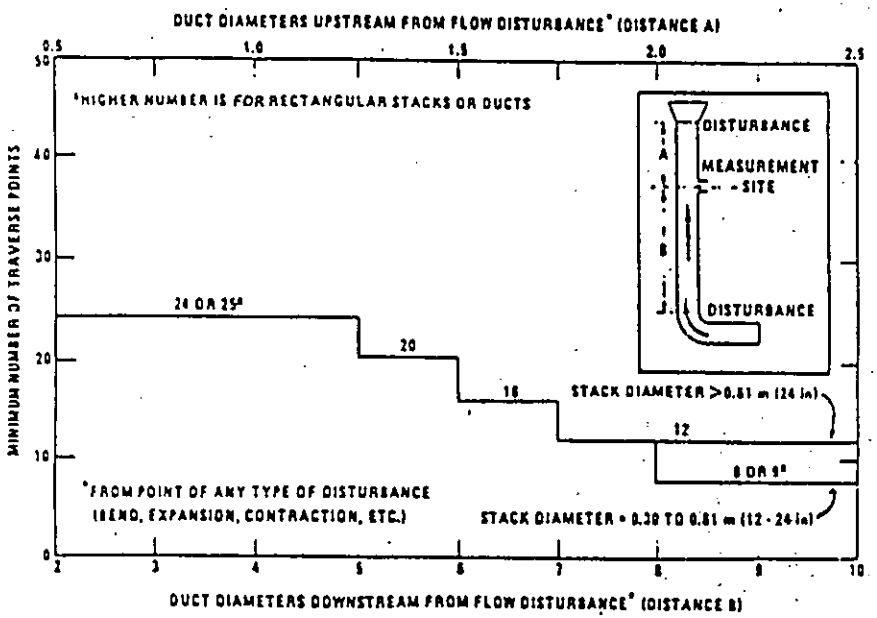


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

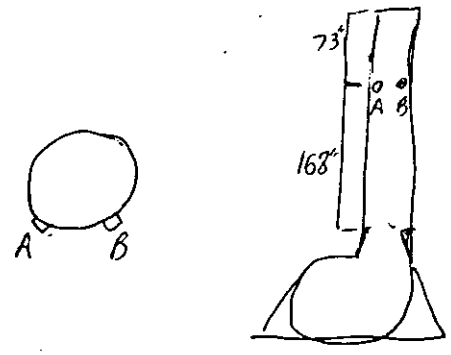
2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT L.P
CITY EUFAULA STATE Alabama
SAMPLING LOCATION Dryer Stack #7
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 45½"
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) 6"
NEAREST UPSTREAM DISTURBANCE 73"
DISTURBANCE EXIT
NEAREST DOWNSTREAM DISTURBANCE 168"
DISTURBANCE BLOWER TRANSITION
SAMPLER BHR DATE 3/11/92



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
B-1	2.1	39.5	7/8"	6"	6 7/8
B-2			2 5/8"		8 5/8
B-3			4 5/8"		10 5/8
B-4			7"		13
B-5			9 3/4"		15 3/4
B-6			14 1/8"		20 1/8
B-7			25 3/8		31 3/8
B-8			29 5/8		35 5/8
B-9			32 1/2		38 1/2
B-10			34 7/8		40 7/8
B-11			36 7/8		42 7/8
B-12			38 3/4		44 3/4

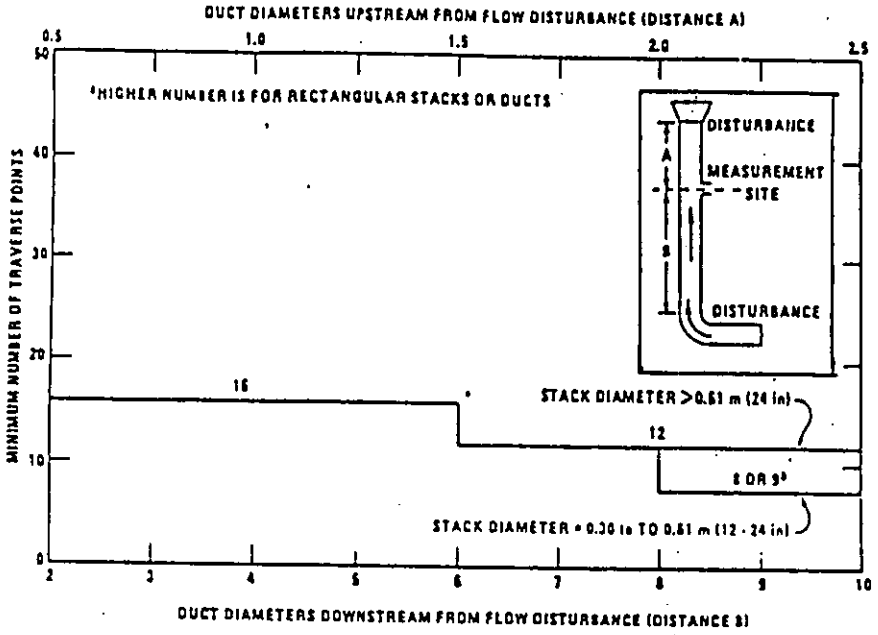


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

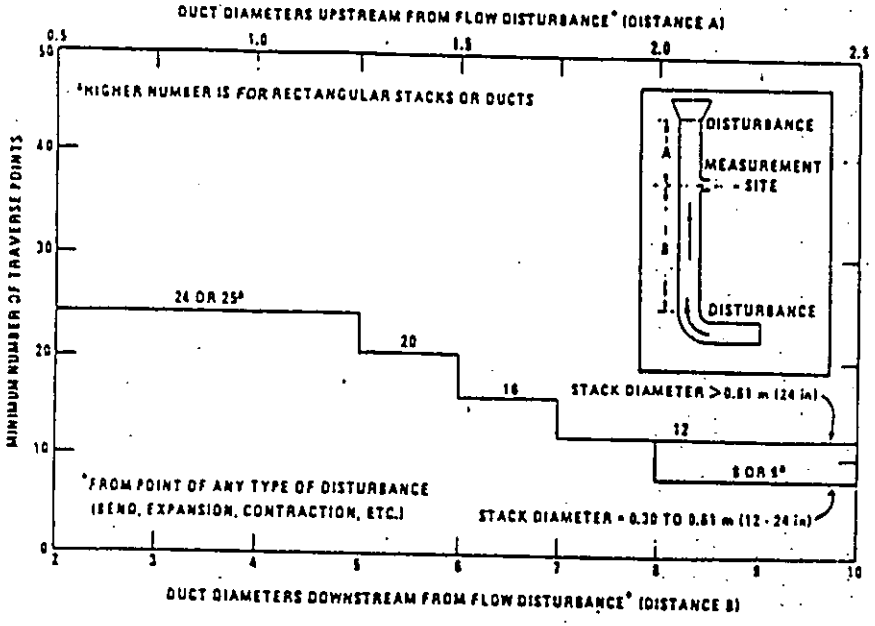


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

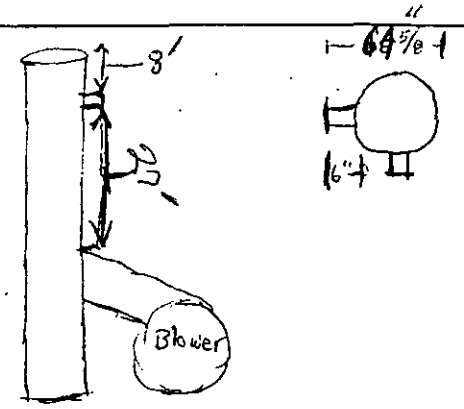
2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT L.P.
CITY Clayton STATE ALA
SAMPLING LOCATION Boiler Stack #1 & 2
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 64 5/8
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) 6 5/8
NEAREST UPSTREAM DISTURBANCE 7'
DISTURBANCE Top of Stack
NEAREST DOWNSTREAM DISTURBANCE 27'
DISTURBANCE blower inlet
SAMPLER Malone DATE 3-16-92



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	.026	58"	1.51	6.6	~~7.5~~ 8.1
2	.082		4.76		11.4
3	.146		8.5		15.1
4	.226		13.11		19.7
5	.342		19.84		26.5
6	.658		38.16		44.8
7	.774		44.89		51.5
8	.854		49.53		56.1
9	.918		53.24		59.9
10	.974		56.49		63.1
~~11~~					
~~12~~					
~~13~~					

epa1circ.wk1

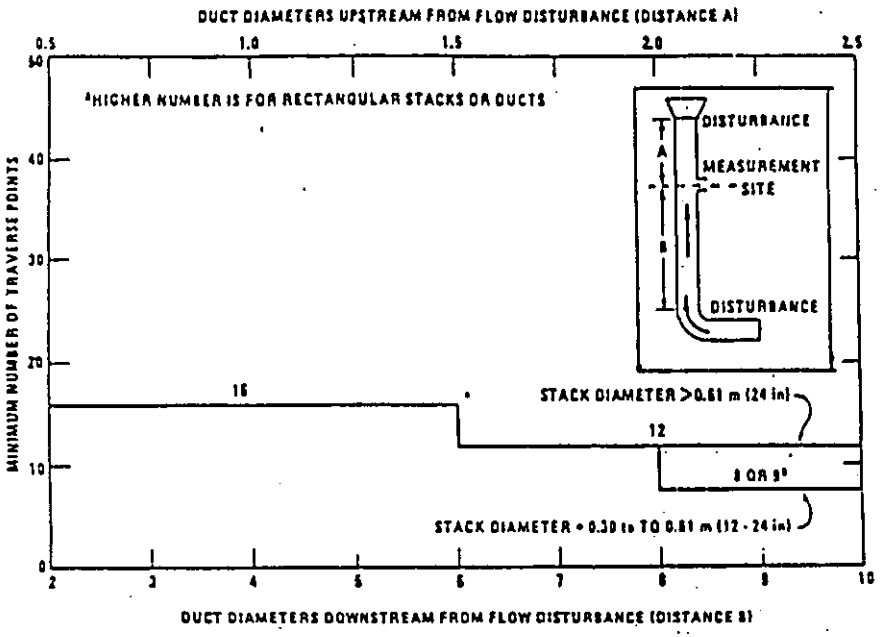


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

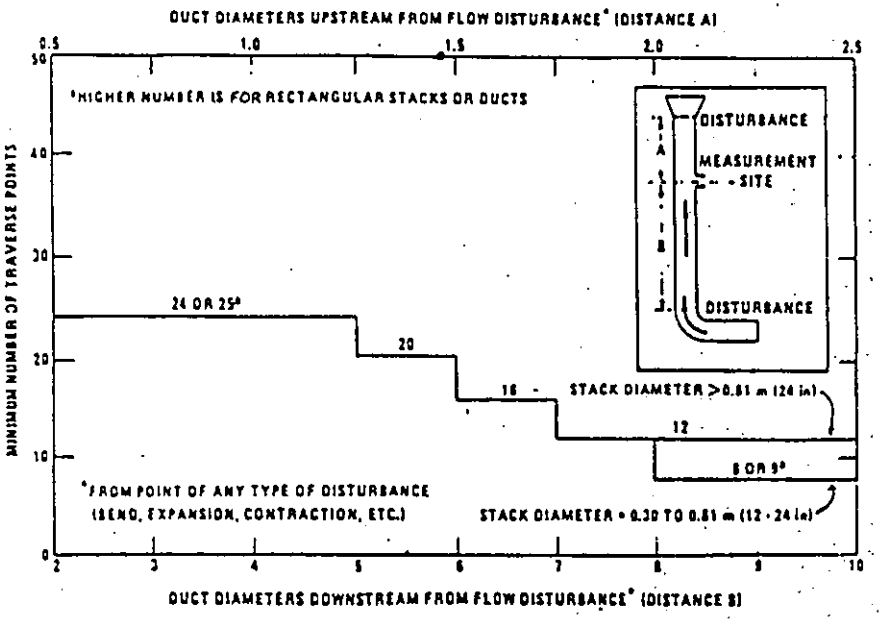


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

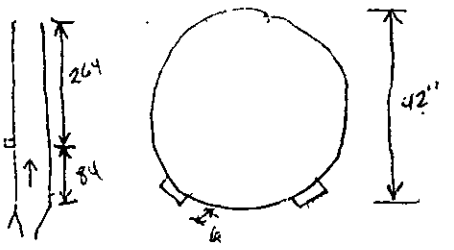
Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

8/2

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT Louisiana Pacific
CITY Clayton STATE Alabama
SAMPLING LOCATION Dryer
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 48
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) 6 ID=42
NEAREST UPSTREAM DISTURBANCE 84" (2)
DISTURBANCE
NEAREST DOWNSTREAM DISTURBANCE 264 (6.3)
DISTURBANCE
SAMPLER DATE



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	0.021	42	0.88	6	6.88 (7)
2	0.067		2.8		8.8
3	0.118		5.0		11.0
4	0.177		7.4		13.4
5	0.250		10.5		16.5
6	0.356		15.0		21.0
7	0.644		27.0		33.0
8	0.750		31.5		37.5
9	0.823		34.6		40.6
10	0.882		37.0		43.0
11	0.933		39.2		45.2
12	0.979		41.1		47.1 (47)

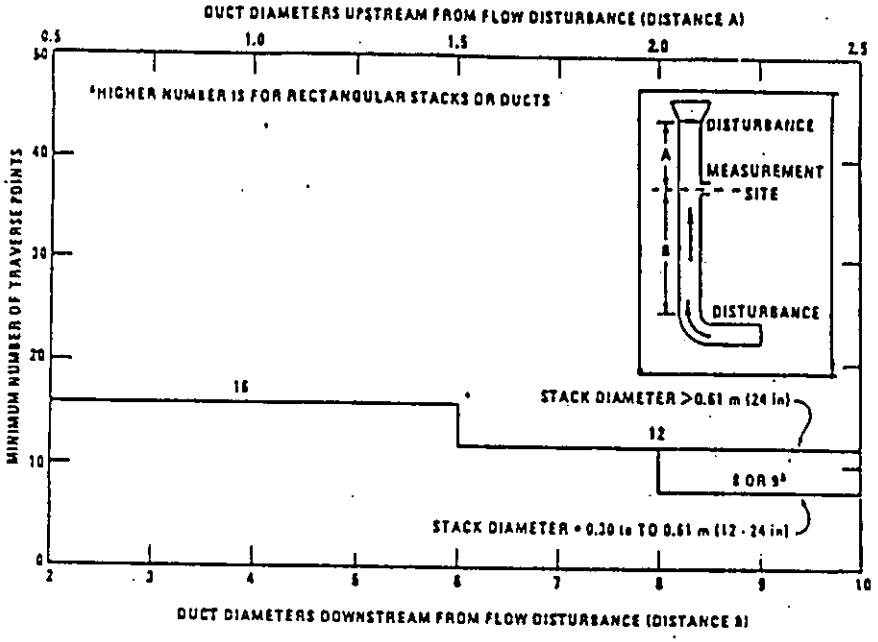


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

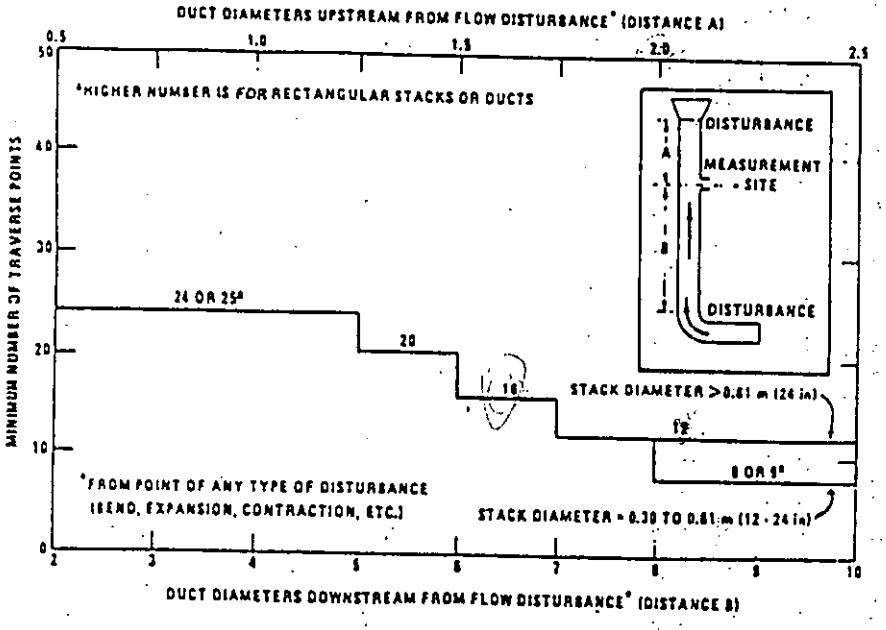


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

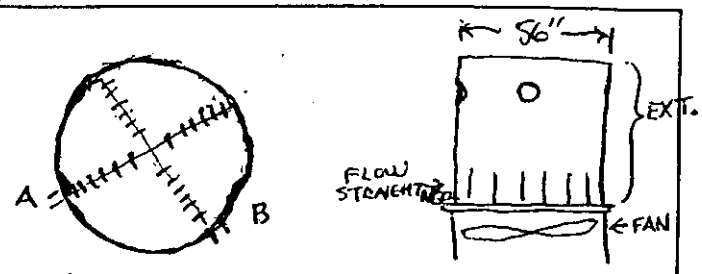
2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT Louisiana Pacific
CITY Clayton STATE AL
SAMPLING LOCATION Press Vent 6-10
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 61.5
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) 5.5 ID 56
NEAREST UPSTREAM DISTURBANCE
DISTURBANCE
NEAREST DOWNSTREAM DISTURBANCE
DISTURBANCE
SAMPLER gm DATE 3/14/92



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	0.021	56	1.18	5.5	6.68
2	0.067		3.75		9.25
3	0.118		6.61		12.11
4	0.177		9.91		15.41
5	0.250		14.0		19.50
6	0.356		19.94		25.44
7	0.644		36.1		41.60
8	0.750		42.0		47.5
~~3~~ 9	0.823		46.1		51.6
~~4~~ 10	0.882		49.4		54.9
~~5~~ 11	0.933		52.2		57.7
~~6~~ 12	0.979		54.8		60.3

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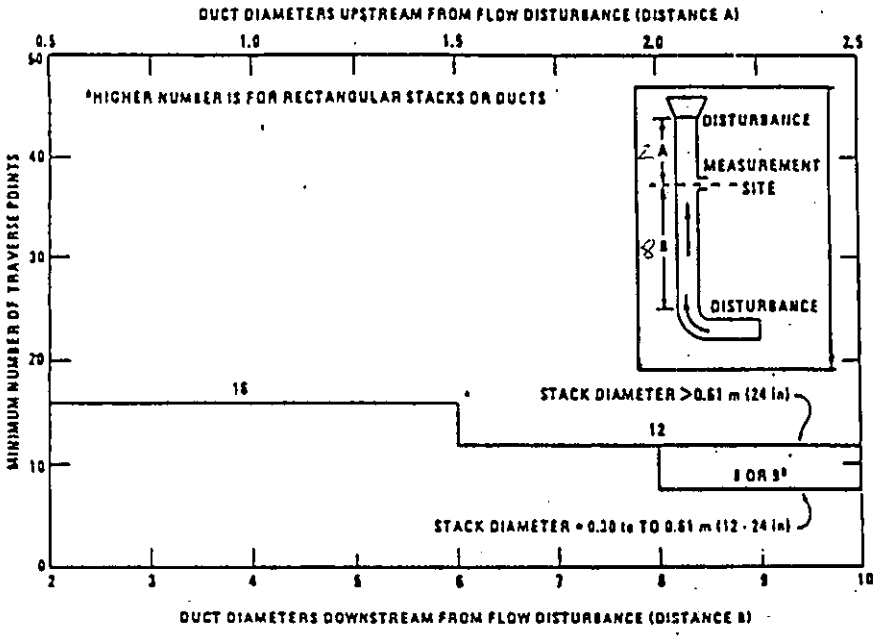


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

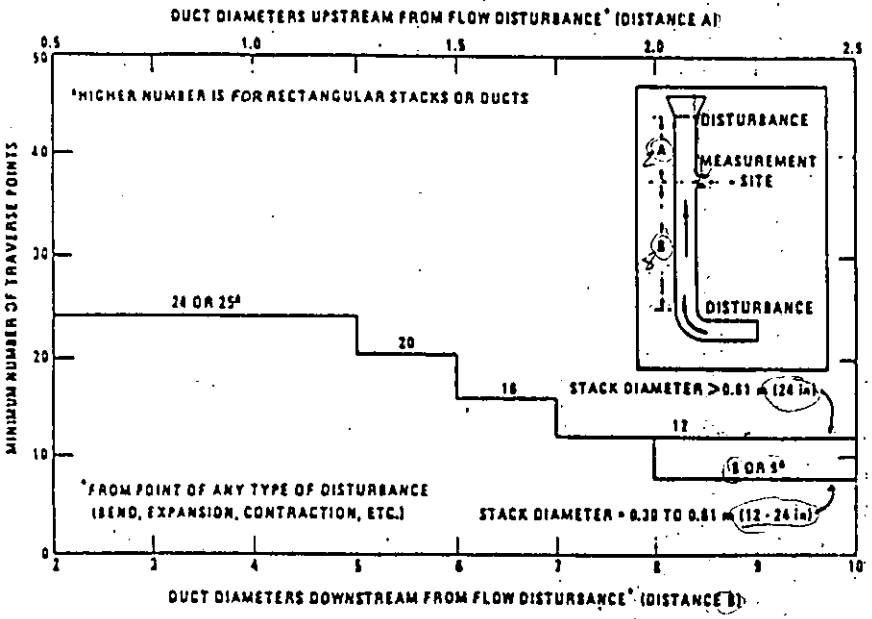


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

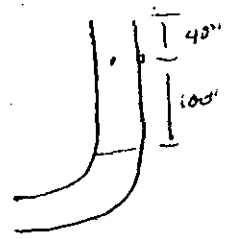
2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT Louisiana Pacific
CITY Clayton STATE
SAMPLING LOCATION Press Vent #11
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 35.25
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) N/A
NEAREST UPSTREAM DISTURBANCE 100" (2.8)
DISTURBANCE Elbow
NEAREST DOWNSTREAM DISTURBANCE 40" (1)
DISTURBANCE Stack Exit
SAMPLER JM DATE 3/13/92



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	0.021	35.25	0.74	Ø	NA
2	0.067		2.36		
3	0.118		4.16		
4	0.177		6.24		
5	0.250		8.81		
6	0.356		12.55		
7	0.644		22.70		
8	0.750		26.44		
9	0.823		29.00		
10	0.882		31.10		
11	0.933		32.89		
12	0.979		34.51		

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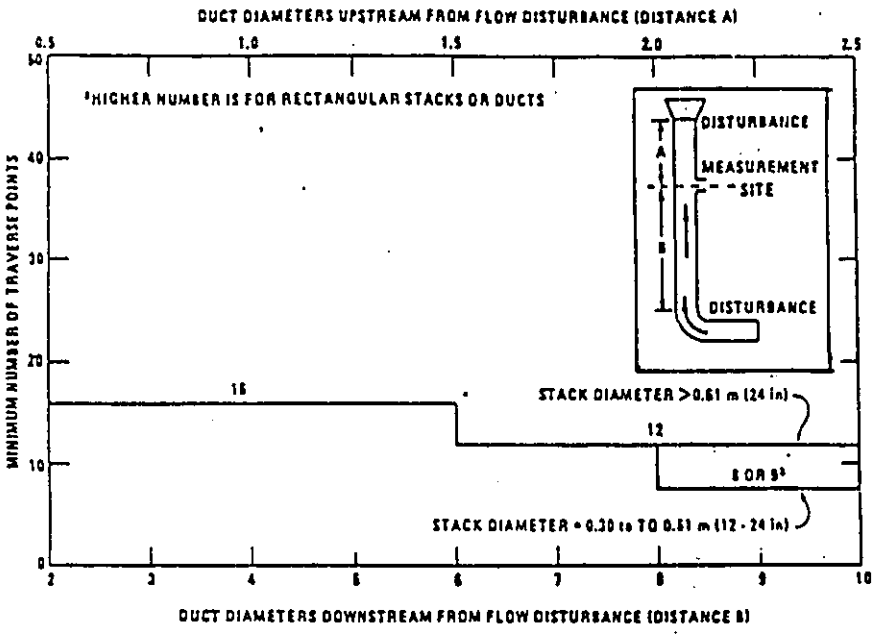


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

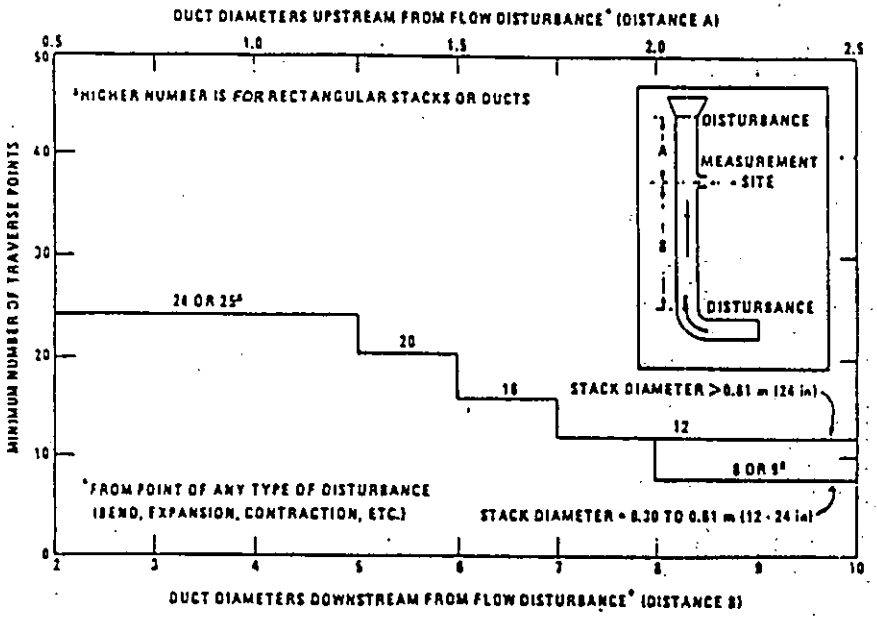


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

EPA Method 2
Gas Velocity and Cyclonic Flow Check

Plant: Louisiana Pacific
City: Clayton
Sampling Location: Press Vent #5
Operator: gm
Ambient Temperature: 34 deg. F
Barometric Pressure: 29.79 in. Hg
Static Pressure: 0.33 in. H2O
Stack ID Side 1: 62 in.
Stack ID Side 2: 62 in.

Run Date: 3/11/92
Clock Time: 0730
Run No.: 1
Mol. Wt.: 28.83
Pitot Cp: 0.84

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null. Δp
1		0.54	70	ok	
2		0.94	70		
3		0.82	70	ok	
4		0.72	70		
5		0.37	70	ok	
6		0.25	70		
7		0.20	70	ok	
8		0.37	68		
9		0.73	65	ok	
10		0.75	70		
11		0.73	70	ok	
12		0.46	69		
				Average angle (α)*	ok

* Average of α must be <10 degrees to be acceptable.

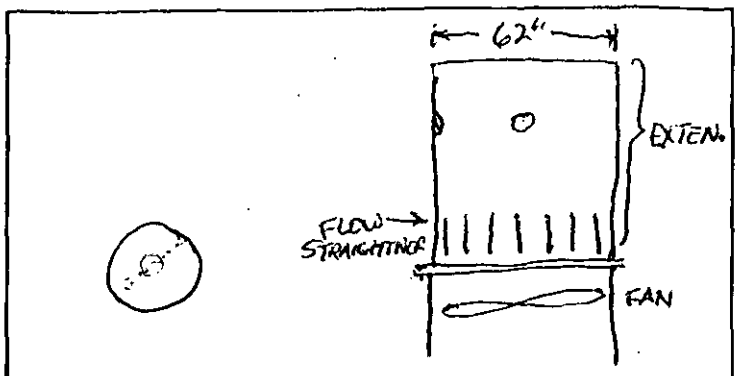
.236

cyclonic.wk1

=9.34

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT Louisiana Pacific
CITY Clayton STATE AL
SAMPLING LOCATION Press Vent # 4, 5, 6
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 67.5
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) ~~5.5~~ ID= 62.0
NEAREST UPSTREAM DISTURBANCE
DISTURBANCE
NEAREST DOWNSTREAM DISTURBANCE
DISTURBANCE
SAMPLER DATE



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	Stat-0.42 STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	velocity for #4 0.80				
2	0.58				
3	0.16				
4	0.53		Static -0.42		
5	0.72				
6	0.22				
7	0.66				
8	0.33				
9	0.24				
10	0.20				
11	0.15				
12	0.48				

0.2593

epa1circ.wk1

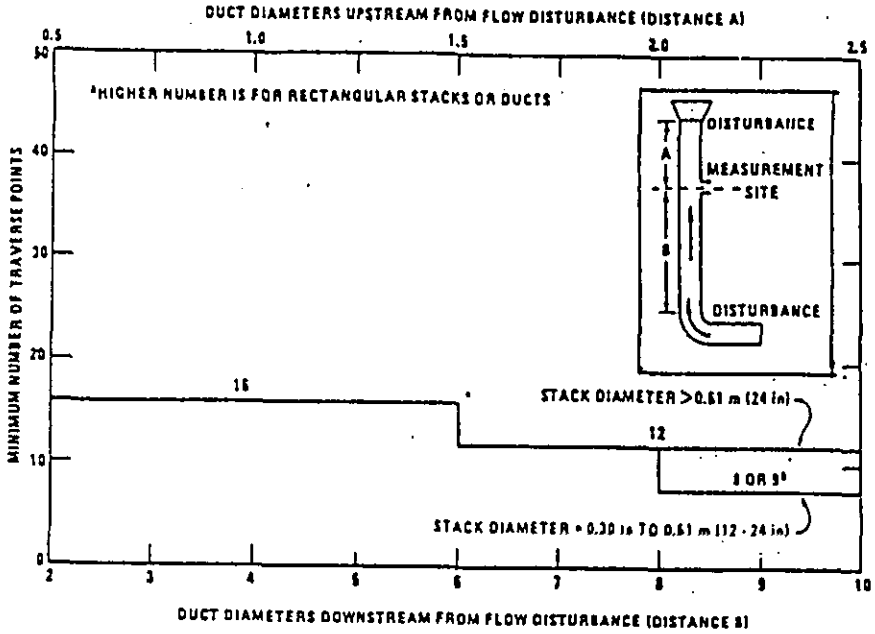


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

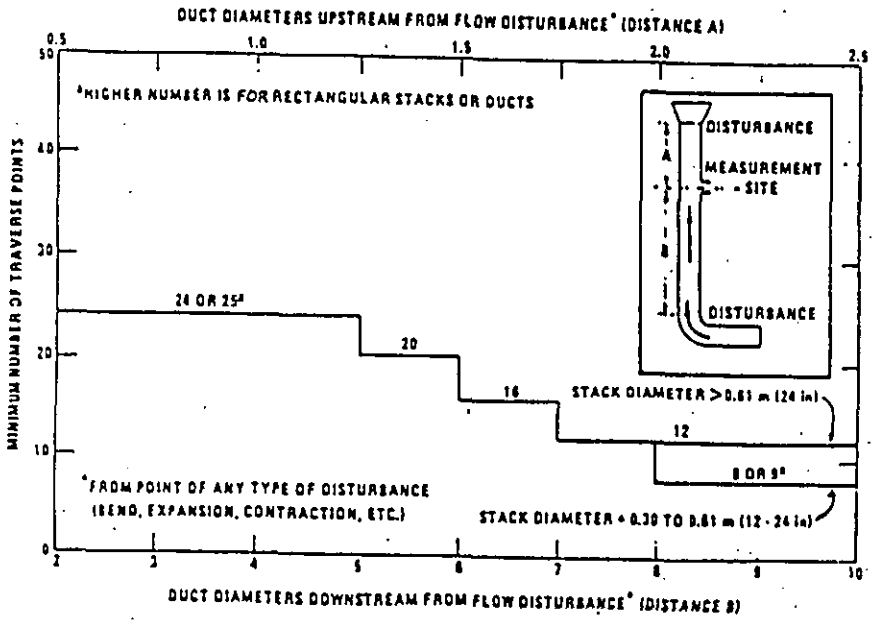


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

EPA Method 2
Gas Velocity and Cyclonic Flow Check

Plant: Louisiana Pacific
City: Clayton
Sampling Location: Press Vent #6
Operator: RM, OM
Ambient Temperature: 40 deg. F
Barometric Pressure: 29.84 in. Hg
Static Pressure: -0.44 in. H2O
Stack ID Side 1: 54 in.
Stack ID Side 2: 56 in.

Run Date: 3/14/92
Clock Time: 1000
Run No.: 1
Mol. Wt.:
Pitot Cp: 0.84

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null. Δp
1		0.54	45		
2		0.62	38		
3		0.79	38		
4		0.46	38		
5		0.47	38		
6		0.47	40		
7		0.98	41		
8		1.1	39		
9		1.1	38		
10		0.89	38		
11		0.87	37		
12		0.64	37		
				Average angle (α)*	

* Average of α must be <10 degrees to be acceptable.

KZO
0.196

cyclonic.wk1

EPA Method 2
Gas Velocity and Cyclonic Flow Check

Plant: LOUISIANA PACIFIC
City: CLAYTON, ALA.
Sampling Location: DRYER STACK #5
Operator: T. THOMPSON, J. MALONE
Ambient Temperature: _____ deg. F
Barometric Pressure: 29.82 in. Hg
Static Pressure: -1.0 in. H2O
Stack ID Side 1: _____ in.
Stack ID Side 2: _____ in.

Run Date: 3/20/92
Clock Time: 1652
Run No.: 2T
Mol. Wt.: _____
Pitot Cp: 0.84

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null. Δp
B1		1.5	140		
2		1.8	140		
3		2.0	141		
4		1.8	140		
5		1.8	141		
6		2.0	141		
7		2.3	141		
8		2.4	141		
9		2.3	140		
10		2.3	140		
11		2.0	140		
12		1.6	140		

Average angle (α)* _____

* Average of α must be <10 degrees to be acceptable.

cyclonic.wk1

EPA Method 2
Gas Velocity and Cyclonic Flow Check

Plant: LOUISIANA PACIFIC
City: CLAYTON, ALA.
Sampling Location: DRYER STACK #5
Operator: T. THOMPSON J. MALONE
Ambient Temperature: _____ deg. F
Barometric Pressure: 29.82 in. Hg
Static Pressure: 1.0 in. H2O
Stack ID Side 1: _____ in.
Stack ID Side 2: _____ in.

Run Date: 3/20/92
Clock Time: 16:30
Run No.: 2T
Mol. Wt.: _____
Pitot Cp: 0.84

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null. Δp
A1	B	1.8	139		
2	B	1.8	140		
3	B	2.0	141		
4	B	2.0	140		
5	B	2.0	140		
6	B	2.2	140		
7	B	2.0	140		
8	B	2.1	140		
9	B	2.1	141		
10	B	2.0	141		
11	B	1.8	141		
12	B	1.2	141		

Average angle (α)*: _____

* Average of α must be <10 degrees to be acceptable.

cyclonic.wk1

EPA Method 2
Gas Velocity and Cyclonic Flow Check

Plant: LOUISIANA PACIFIC
City: CLAYTON, ALABAMA
Sampling Location: DRYER STACK #7
Operator: T. THOMPSON, J. MACON'E
Ambient Temperature: _____ deg. F
Barometric Pressure: 29.82 in. Hg
Static Pressure: -1.5 in. H2O
Stack ID: Side 1 _____ in.; Side 2 _____ in.

Run Date: 3/20/92
Clock Time: 1400
Run No.: 3T DS-7
Mol. Wt.: _____
Pitot Cp: 0.84

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null Δp
A 1	.9	135°			
2	1.3	135°			
3	1.5	135°			
4	1.6	135°			
5	1.9	135°			
6	2.0	135°			
7	2.0	135°			
8	2.0	135°			
9	1.9	135°			
10	1.7	134°			
11	1.5	132°			
12	.9	134°			
				Average angle (α)*	

* Average of α must be <10 degrees to be acceptable.

EPA Method 2
Gas Velocity and Cyclonic Flow Check

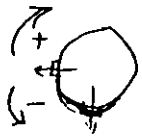
Plant: Louisiana Pacific
City: Clayton Ala
Sampling Location: DS 7
Operator: T. THOMPSON, J. MALONE
Ambient Temperature: _____ deg. F
Barometric Pressure: _____ in. Hg
Static Pressure: -1.5 in. H2O
Stack ID: Side 1 _____ in.; Side 2 _____ in.

Run Date: 3/20/92
Clock Time: / / 13:55
Run No.: 37
Mol. Wt.: _____
Pitot Cp: 0.84

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null. Δp
B1	B	1.0	135°		
2	B	1.4	135°		
3	B	1.6	135°		
4	B	2.0	135°		
5	B	2.2	135°		
6	B	2.1	135°		
7	B	2.0	135°		
8	B	2.0	134°		
9	B	~~2.1~~ 1.9	134°		
10	B	1.8	132°		
11	B	1.7	129.6		
12	B	1.0	~~134°~~ 126°		
				Average angle (α)*	

* Average of α must be <10 degrees to be acceptable.

cyclonic.wk1

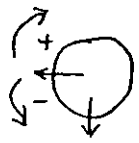


EPA Method 2
Gas Velocity and Cyclonic Flow Check

Plant: LOUISIANA-PACIFIC
Run Date: 3/10/92
City: Clayton, AL
Clock Time:
Sampling Location: Dryer 1
Operator: BR
Run No.: Flow check
Ambient Temperature: deg. F
Barometric Pressure: in. Hg
Mol. Wt.:
Static Pressure: in. H2O
Pitot Cp:
Stack ID Side 1: 42 in.
Side 2: 42 in.

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null. Δp
A-12		3.1	133	3.2	-4°
A-11		3.2	133	3.5	-5°
A-10		3.6	133	3.6	0°
A-9		3.5	132	3.5	0°
A-8		3.2	132	3.2	0°
A-7		2.7	133	2.8	+5°
A-6		3.1	133	3.0	+5°
A-5		3.5	134	3.4	+20°
A-4		3.6	134	3.5	+15°
A-3		4.0	129	4.0	+35°
A-2		3.7	115	3.9	+35°
A-1		3.3	124	3.7	+35°
				Average angle (α)*	

* Average of α must be <10 degrees to be acceptable.



EPA Method 2
Gas Velocity and Cyclonic Flow Check

Plant: LOUISIANA-PACIFIC
City: Clayton
Sampling Location: Dryer 1
Operator: BR
Ambient Temperature: — deg. F
Barometric Pressure: — in. Hg
Static Pressure: — in. H2O
Stack ID Side 1: — in.
Side 2: — in.

Run Date: 3/10/92
Clock Time: —
Run No.: Flow check
Mol. Wt.: —
Pitot Cp: —

Traverse point number	Position in.	Velocity head Δp in. H2O	Stack temperature deg. F	Cyclonic Flow Determination: Δp at 0° reference	Cyclonic Flow Determination: Angle (α) which yields a null. Δp
B-12		4.5	136	~~4.7°~~	~~92°~~ +2°
B-11		4.3	137	4.3	~~90°~~ 0°
B-10		3.6	137	3.6	0°
B-9		2.9	138	2.9	-3°
B-8		2.6	138	2.7	-8°
B-7		2.5	137	2.6	-13°
B-6		2.8	137	2.9	+8°
B-5		2.9	137	3.1	+20°
B-4		3.3	138	3.4	+28°
B-3		3.4	136	3.4	+30
B-2		2.9	136	3.3	+35
B-1		1.9	135	3.2	+45
				Average angle (α)*	

* Average of α must be <10 degrees to be acceptable.

Plant - L.P. Clayton Ala.

Date 3/12/92

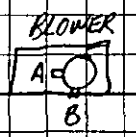
Bar Press (HG) 29.83

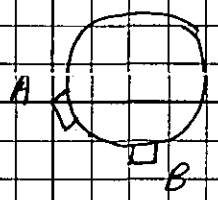
Start Time 9:08

Port	Point	Delta P	TS
B	1	1.90	145.4
	2	2.0	145.0
	3	2.2	144.5
	4	2.4	143.4
	5	2.4	143.0
	6	2.2	142.6
	7	2.4	142.5
	8	2.4	142.0
	9	2.3	142.0
	10	2.2	141.0
	11	2.0	140.0
	12	1.0	139.0
A	1	1.9	133.6
	2	2.2	137.8
	3	2.3	140.6
	4	2.4	141.5
	5	2.4	141.0
	6	2.4	140.0
	7	2.0	140.0
	8	1.9	140.0
	9	1.9	140.0
	10	1.7	139.5
	11	1.6	138.0
	12	1.0	137.0

STATIC PRESSURE:
-1.2" AVG.

STACK #5





CYCLONIC FLOW

ALL POINTS LESS THAN 10%

B. RAYFIELD

J. MALONE

Plant LP
City Eufaula Ala.
Operator BC
Date 3/11/92

Bar Press (in HG) 29.78

Start time 10:15

Port	Point	Delta P	Ts
B	1	1.0	123
B	2	1.2	123
B	3	1.4	125
B	4	1.6	130
B	5	1.7	132
B	6	1.8	133
B	7	2.0	133.5
B	8	2.0	133
B	9	1.9	133
B	10	1.7	133
B	11	1.5	133
B	12	1.3	133
A	1	0.9	132
A	2	1.4	132
A	3	1.6	133
A	4	1.9	132
A	5	2.0	132
A	6	2.0	132
A	7	2.0	132
A	8	2.0	132
A	9	1.9	132
A	10	1.8	132
A	11	1.6	132
A	12	1.4	132

STATIC PRESSURE -1.0

Stack #7

CYCLONIC FLOW

ALL POINTS <10° CHECKED

22-141 50 SHEETS
22-142 100 SHEETS
22-144 200 SHEETS
AMPAD

APPENDIX C

PM10 FIELD AND RECOVERY DATA

DRYER STACKS

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/13/92	DRYER STACK 1	PM-10	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.74	-0.95	52	62QOO	42	0.84	4A GLASS	2	0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.88	1.005	4A5	PT-1	6-4	—	~~[illegible]~~ 5	0.004			

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					—	
Analysis Method	FYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B 6	0/0	1101	362.836	3.60	0.53	118	250	250	60	65	—	2.5
5	5.48		365.05	3.10	.53	117	251	251	55	67		2.5
4	10.56		367.19	2.80	.53	115	251	252	51	68		2.5
3	15.36		369.16	3.20	.53	113	251	252	50	69		2.5
2	20.55		371.09	3.00	.53	110	254	253	50	69		2.5
NOZZLE PLUG → 1	25.55		372.55	3.10	.53	110	253	254	50	69		2.5
A 6	30.64/0		374.61	3.70	.53	117	252	254	50	69		2.5
5	5.55		376.90	3.60	.53	114	252	250	48	70		2.5
4	11.03		379.15	3.00	.53	114	253	251	48	71		2.5
3	16.03		381.05	3.10	.53	113	253	252	47	72		2.5
2	21.11		383.35	3.30	.53	113	252	252	47	72		2.5
1	26.30		385.40	3.50	.53	113	250	250	47	72		2.5
	30.92	1213	387.602									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	61.56	24.766	1.777	.53	114	69.4

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.74	in.Hg
Pg	Static Pressure	-0.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.67	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.05	1.54	1.20	0.96	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.503	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.24	ft/sec	Delta p min.	1.156	in.H2O
V max	maximum velocity	102.67	ft/sec	Delta p max.	3.048	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.984	44.592	38.450	32.254	27.443	21.355	16.522	12.629
R min.	0.722	0.682	0.648	0.589	0.503	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.13	30.43	24.91	19.00	13.79	10.68	8.26	6.31
Vmax	71.33	56.79	49.64	42.46	36.93	30.01	24.58	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.712	0.521	0.394	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	3.000

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	3.60	1.90	5.48	3.70	1.92	5.55
2	3.10	1.76	5.08	3.60	1.90	5.48
3	2.80	1.67	4.83	3.00	1.73	5.00
4	3.20	1.79	5.16	3.10	1.76	5.08
5	3.00	1.73	5.00	3.30	1.82	5.24
6	3.10	1.76	5.08	2.50	1.58	4.56
		Time(min)	30.64		Time(min)	30.92

PM10 DATA

SOURCE DRYER STACK 1 RUN 1 DATE 3-13-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.48	3.60	1.90	0.53	118.0	65.0
	2	5.08	3.10	1.76	0.53	117.0	67.0
	3	4.83	2.80	1.67	0.53	115.0	68.0
	4	5.16	3.20	1.79	0.53	113.0	69.0
	5	5.00	3.00	1.73	0.53	110.0	69.0
	6	5.08	3.10	1.76	0.53	110.0	69.0
Port B	1	5.55	3.70	1.92	0.53	117.0	69.0
	2	5.48	3.60	1.90	0.53	114.0	70.0
	3	5.00	3.00	1.73	0.53	114.0	71.0
	4	5.08	3.10	1.76	0.53	113.0	72.0
	5	5.24	3.30	1.82	0.53	113.0	72.0
	6	4.56	2.50	1.58	0.53	113.0	72.0
		61.56		1.78	0.53	114.0	69.4

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	1.005
Meter volume, ft^3	24.766
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.74
Static Pressure, in. Hg	-0.95

ANALYTICAL RECOVERY DATA

Moisture, %	5.6
Mass (probe wash)<PM10, g	0.0440
Mass (filter)<PM10, g	0.0070

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/13/92	DRYER STACK 1	PM-10	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.74	-0.95		62G008	42	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.88	1.005	4A5	PT-1	6-4	—	5.0	0.001	5.0	0.002	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2						✓	✓
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A6	0/0	13.33	387.731	3.50	0.53	116	255	251	55	68	—	2.5
5	5.59		390.02	3.00	.53	119	256	252	53	68		2.5
4	10.77		392.07	2.20	.53	121	254	253	50	66		2.5
3	15.20		393.84	2.60	.53	120	256	249	46	65		2.5
2	20.02		396.09	2.80	.53	118	254	251	46	65		2.5
1	25.02		398.14	2.20	.53	118	254	251	45	65		2.5
B6	29.45/0	1403/1450	399.82	3.50	.53	121	251	253	45	65		2.5
5	5.59		402.23	2.75	.53	120	252	252	45	65		2.5
4	10.55		404.21	2.10	.53	119	251	252	44	64		2.5
3	14.88		405.88	2.30	.53	121	251	253	44	64		2.5
2	19.41		407.66	2.20	.53	120	257	253	46	64		2.5
1	23.84		408.91	2.06	.53	118	251	253	46	64		
	28.06	1526	410.369									

7.40 STOP

178 NOZZLE PLUG

1340 OFF
1425 START

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	57.51	22.838	1.618	.53	~~47.2~~ 119.2	65.3

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.74	in.Hg
Pg	Static Pressure	-0.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.67	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.05	1.54	1.20	0.96	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.503	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.24	ft/sec	Delta p min.	1.156	in.H2O
V max	maximum velocity	102.67	ft/sec	Delta p max.	3.048	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.984	44.592	38.450	32.254	27.443	21.355	16.522	12.629
R min.	0.722	0.682	0.648	0.589	0.503	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.13	30.43	24.91	19.00	13.79	10.68	8.26	6.31
Vmax	71.33	56.79	49.64	42.46	36.93	30.01	24.58	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.712	0.521	0.394	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	2.800

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	3.50	1.87	5.59	3.50	1.87	5.59
2	3.00	1.73	5.18	2.75	1.66	4.96
3	2.20	1.48	4.43	2.10	1.45	4.33
4	2.60	1.61	4.82	2.30	1.52	4.53
5	2.80	1.67	5.00	2.20	1.48	4.43
6	2.20	1.48	4.43	2.00	1.41	4.23
		Time(min)	29.45		Time(min)	28.06

PM10 DATA

SOURCE DRYER STACK 1 RUN 2 DATE 3-13-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.59	3.50	1.87	0.53	116.0	68.0
	2	5.18	3.00	1.73	0.53	119.0	68.0
	3	4.43	2.20	1.48	0.53	121.0	66.0
	4	4.82	2.60	1.61	0.53	120.0	65.0
	5	5.00	2.80	1.67	0.53	118.0	65.0
	6	4.43	2.20	1.48	0.53	118.0	65.0
Port B	1	5.59	3.50	1.87	0.53	121.0	65.0
	2	4.96	2.75	1.66	0.53	120.0	65.0
	3	4.33	2.10	1.45	0.53	119.0	64.0
	4	4.53	2.30	1.52	0.53	121.0	64.0
	5	4.43	2.20	1.48	0.53	120.0	64.0
	6	4.23	2.00	1.41	0.53	118.0	64.0
		57.51		1.62	0.53	119.2	65.3

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	1.005
Meter volume, ft^3	22.838
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.74
Static Pressure, in. Hg	-0.95

ANALYTICAL RECOVERY DATA

Moisture, %	5.5
Mass (probe wash)<PM10, g	0.0010
Mass (filter)<PM10, g	0.0173

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC - CLAYTON AL	3/13/92	DRYER STACK 1	PM 10	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.74	-0.95	55	62Q009	42	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.88	1.005	4A5	~~PT-1~~ PT-1	G-4	—	5	0.005	5	0.003	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					✓	✓
Analysis Method	FYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B6	0/0		410.681	3.10	0.53	114	251	250	49	62	—	2.5
5	5.49		412.88	2.40	.53	113	252	251	47	62		2.5
4	10.32		414.83	2.00	.53	115	250	252	46	63		2.5
3	14.73		416.63	2.40	.53	114	250	253	46	63		2.5
2	19.57		418.51	2.30	.53	113	252	253	46	63		2.5
1	24.30		420.43	1.40	.53	112	250	251	46	63		2.5
A 6	27.99/0	1146/16	421.85	3.45	.53	115	257	257	47	63		2.5
5	5.79		423.91	3.00	.53	116	257	253	47	63		2.5
4	11.20		426.13	2.20	.53	114	250	253	46	62		2.5
3	15.82		427.93	2.60	.53	113	252	254	46	60		2.5
2	20.85		429.91	2.60	.53	113	252	253	47	60		2.5
1	25.88		431.60	2.20	.53	112	251	251	47	60		2.5
	30.51		432.406									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	58.49			.53	113.7	62

1.58

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.74	in.Hg
Pg	Static Pressure	-0.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.67	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

MEAN TEMP

	1	2	3	4	5	6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.05	1.54	1.20	0.96	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches			
Vn	Nozzle Velocity	83.503	ft/sec			
R min.	minimum R	0.757				
R max.	maximum R	1.230				
V min	minimum velocity	63.24	ft/sec	Delta p min.	1.156	in.H2O
V max	maximum velocity	102.67	ft/sec	Delta p max.	3.048	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.984	44.592	38.450	32.254	27.443	21.355	16.522	12.629
R min.	0.722	0.682	0.648	0.589	0.503	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.13	30.43	24.91	19.00	13.79	10.68	8.26	6.31
Vmax	71.33	56.79	49.64	42.46	36.93	30.01	24.58	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.712	0.521	0.394	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^2 (from LAST velocity traverse)	2.570

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	3.10	1.76	5.49	3.45	1.86	5.79
2	2.40	1.55	4.83	3.00	1.73	5.40
3	2.00	1.41	4.41	2.20	1.48	4.63
4	2.40	1.55	4.83	2.60	1.61	5.03
5	2.30	1.52	4.73	2.60	1.61	5.03
6	1.40	1.18	3.69	2.20	1.48	4.63
		Time(min)	27.99		Time(min)	30.51

PM10 DATA

SOURCE DRYER STACK 1 RUN 3 DATE 3-13-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.49	3.10	1.76	0.53	114.0	62.0
	2	4.83	2.40	1.55	0.53	113.0	62.0
	3	4.41	2.00	1.41	0.53	115.0	63.0
	4	4.83	2.40	1.55	0.53	114.0	63.0
	5	4.73	2.30	1.52	0.53	113.0	63.0
	6	3.69	1.40	1.18	0.53	112.0	63.0
Port B	1	5.79	3.45	1.86	0.53	115.0	63.0
	2	5.40	3.00	1.73	0.53	116.0	63.0
	3	4.63	2.20	1.48	0.53	114.0	62.0
	4	5.03	2.60	1.61	0.53	113.0	60.0
	5	5.03	2.60	1.61	0.53	113.0	60.0
	6	4.63	2.20	1.48	0.53	112.0	60.0
		58.49		1.58	0.53	113.7	62.0

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	1.005
Meter volume, ft^3	21.725
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.74
Static Pressure, in. Hg	-0.95

ANALYTICAL RECOVERY DATA

Moisture, %	4.6
Mass (probe wash)<PM10, g	0.0102
Mass (filter)<PM10, g	0.0113

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC-CLATON AL.	3/1/92	DRYER STACK 2	M-10	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.74	-1.95		629009	42	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.89	0.998	4AS	PT-1	64	—	5.0	0.002	5.0	0.002	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					✓	✓
Analysis Method	FYRITE	%CO2	~~20~~						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 6	0/0	1832	432.513	3.20	0.53	116	255	252	44	53	—	2.5
5	5.68		434.84	3.20	.53	117	245	253	44	54		2.5
4	11.34		437.08	2.55	.53	117	249	251	44	54		2.5
3	16.19		439.04	2.80	.53	117	255	252	44	55		2.5
2	21.29		441.13	2.90	.53	116	254	251	44	55		2.5
1	26.47		443.22	2.40	.53	114	253	251	44	56		2.5
B 6	31.18/0	1904/1907	445.14	3.10	.53	114	253	252	44	54		2.5
5	5.36		447.41	2.60	.53	114	252	251	44	55		2.5
4	10.26		449.30	2.15	.53	114	254	252	45	55		2.5
3	14.73		451.14	2.50	.53	116	256	252	45	55		2.5
2	19.54		453.05	2.30	.53	116	256	251	45	55		2.5
1	24.15		454.84	2.20	.53	115	256	250	45	55		2.5
	28.67	1936	456.583									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	59.85	24.070		.53	115.5	54.6

1.62

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.74	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	116	deg.F
Tm	Meter temperature	55	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.60	in.Hg
Us	Viscosity of Stack gas	192.02	micropoise
Qs	Cyclone flow rate	0.485	ft^3/min.

MEAN TEMP

	1	2	3	4	5	6
Stack temp	-134.5	-84.5	-34.5	15.5	65.5	115.5
Meter Temp.	54.6	54.6	54.6	54.6	54.6	54.6
Delta H(in.H2O)	1.98	1.48	1.16	0.93	0.76	0.63

	7	8	9	10	11	12
Stack temp	165.5	215.5	265.5	315.5	365.5	415.5
Meter Temp.	54.6	54.6	54.6	54.6	54.6	54.6
Delta H(in.H2O)	0.53	0.46	0.40	0.35	0.31	0.27

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.788	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.46	ft/sec	Delta p min.	1.158	in.H2O
V max	maximum velocity	103.02	ft/sec	Delta p max.	3.053	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	57.179	44.745	38.581	32.364	27.537	21.428	16.578	12.672
R min.	0.722	0.683	0.648	0.589	0.503	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.316	1.346	1.405	1.487	1.604
Vmin.	41.27	30.54	25.01	19.08	13.86	10.71	8.29	6.34
Vmax	71.57	56.98	49.80	42.60	37.05	30.10	24.65	19.01
Dp min.	0.490	0.268	0.180	0.105	0.055	0.033	0.020	0.012
Dp max.	1.473	0.934	0.713	0.522	0.395	0.261	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	2.700

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	3.75	1.94	5.89	3.10	1.76	5.36
2	3.20	1.79	5.44	2.60	1.61	4.91
3	2.55	1.60	4.86	2.15	1.47	4.46
4	2.80	1.67	5.09	2.50	1.58	4.81
5	2.90	1.70	5.18	2.30	1.52	4.61
6	2.40	1.55	4.71	2.20	1.48	4.51
		Time(min)	31.18		Time(min)	28.67

PM10 DATA

SOURCE DRYER STACK-2 RUN 1 DATE 3-13-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.89	3.75	1.94	0.53	116.0	53.0
	2	5.44	3.20	1.79	0.53	117.0	54.0
	3	4.86	2.55	1.60	0.53	117.0	54.0
	4	5.09	2.80	1.67	0.53	117.0	55.0
	5	5.18	2.90	1.70	0.53	116.0	55.0
	6	4.71	2.40	1.55	0.53	114.0	56.0
Port B	1	5.36	3.10	1.76	0.53	114.0	54.0
	2	4.91	2.60	1.61	0.53	114.0	55.0
	3	4.46	2.15	1.47	0.53	114.0	55.0
	4	4.81	2.50	1.58	0.53	116.0	55.0
	5	4.61	2.30	1.52	0.53	116.0	55.0
	6	4.51	2.20	1.48	0.53	115.0	55.0
		59.85		1.65	0.53	115.5	54.6

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	24.070
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.74
Static Pressure, in. Hg	-1.95

ANALYTICAL RECOVERY DATA

Moisture, %	4.7
Mass (probe wash)<PM10, g	0.0195
Mass (filter)<PM10, g	0.0057

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC · CLAYTON AL.	3/14/92	#2 DRYER STACK	PM 10	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.84	-1.95	57	62Q0[illegible]	42"	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	[illegible]	1.88	0.998	4A-S	PT-1	64	—	5.0	0.001	5.0	0.001	

M8 3

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2						✓	✓
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
B 6	0/0	0853	456.678	3.50	0.53	130	255	253	54	59	—	2.0
5	5.59		459.01	2.55	.53	131	254	254	45	63		2.0
4	10.36		459.95	2.25	.53	132	252	253	47	65		2.0
3	14.84		462.73	2.55	.53	130	253	253	48	67		2.0
2	19.62		464.62	2.80	.53	129	254	255	49	68		2.0
1	24.34		466.02	2.45	.53	128	254	253	49	69		2.0
A 6	29.07/0.		467.96	3.60	.53	129	252	253	55	71		2.0
5	5.67		470.24	3.40	.53	129	252	254	53	72		2.0
4	11.18		472.07	2.50	.53	129	253	254	51	73		2.0
3	15.90		473.48	2.50	.53	129	254	253	51	74		2.0
2	20.69		474.	2.45	.53	128	254	253	50	74		
1	25.31		477.43	2.25	.53	126	255	253	50	75		
	29.79	0959	479.253									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	58.80	22.575	1.65	.53	129.5	68.2

1.65

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.04	1.53	1.19	0.95	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	2.800

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	3.50	1.87	5.59	3.60	1.90	5.67
2	2.55	1.60	4.77	3.40	1.84	5.51
3	2.25	1.50	4.48	2.50	1.58	4.72
4	2.55	1.60	4.77	2.50	1.58	4.72
5	2.50	1.58	4.72	2.45	1.57	4.68
6	2.45	1.57	4.68	2.25	1.50	4.48
		Time(min)	29.02		Time(min)	29.79

PM10 DATA

SOURCE DRYER STACK-2 RUN 2 DATE 3-14-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.59	3.50	1.87	0.53	130.0	59.0
	2	4.77	2.55	1.60	0.53	131.0	63.0
	3	4.48	2.25	1.50	0.53	132.0	65.0
	4	4.77	2.55	1.60	0.53	130.0	67.0
	5	4.72	2.50	1.58	0.53	129.0	68.0
	6	4.68	2.45	1.57	0.53	128.0	69.0
Port B	1	5.67	3.60	1.90	0.53	129.0	71.0
	2	5.51	3.40	1.84	0.53	129.0	72.0
	3	4.72	2.50	1.58	0.53	129.0	73.0
	4	4.72	2.50	1.58	0.53	129.0	74.0
	5	4.68	2.45	1.57	0.53	128.0	74.0
	6	4.48	2.25	1.50	0.53	126.0	75.0
		58.80		1.65	0.53	129.2	69.1

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft ^ 3	22.575
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.84
Static Pressure, in. Hg	-1.95

ANALYTICAL RECOVERY DATA

Moisture, %	5.8
Mass (probe wash)<PM10, g	0.0082
Mass (filter)<PM10, g	0.0138

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON AL	3/4/92	#2 DRYER STACK #2	PM 10	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.84	-1.95		62Q012	42"	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.8°	0.998	4A-5	PT-1	64	—	5.0	0.004	5.0	0.004	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					—	✓
Analysis Method	FYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
STOP 1134 START 1200												
A 6	0/0	1133	479.576	3.90	0.53	128	251	253	57	84	—	2.0
5	5.90		482.00	3.85	.53	130	250	252	54	82		2.0
4	11.76		484.38	3.00	.53	131	250	253	53	82		2.0
3	16.94		486.51	2.50	.53	133	257	254	53	82		2.0
2	21.66		488.05	2.70	.53	133	257	255	53	82		2.0
1	26.57		489.86	1.90	.53	130	252	254	54	81		2.0
B 6	30.69/0	/1254	491.	3.50	.53	132	252	253	54	81		2.0
5	5.59		493.83	2.85	.53	133	250	253	54	81		2.0
4	10.63		495.83	2.45	.53	133	250	251	55	81		2.0
3	15.31		497.69	2.65	.53	132	251	251	56	81		2.0
2	20.18		499.52	2.50	.53	132	251	253	57	81		2.0
1	24.90		501.47	2.30	.53	132	250	252	57	81		2.0
	29.43	1324	503.289									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60.12	23.713	1.69	.53	131.5	81.6

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.04	1.53	1.19	0.95	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	2.800

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	3.90	1.97	5.90	3.50	1.87	5.59
2	3.85	1.96	5.86	2.85	1.69	5.04
3	3.00	1.73	5.18	2.45	1.57	4.68
4	2.50	1.58	4.72	2.65	1.63	4.86
5	2.70	1.64	4.91	2.50	1.58	4.72
6	1.90	1.38	4.12	2.30	1.52	4.53
		Time(min)	30.69		Time(min)	29.43

PM10 DATA

SOURCE DRYER STACK-2 RUN 3 DATE 3-14-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.90	3.90	1.97	0.53	128.0	84.0
	2	5.86	3.85	1.96	0.53	130.0	82.0
	3	5.18	3.00	1.73	0.53	131.0	82.0
	4	4.72	2.50	1.58	0.53	133.0	82.0
	5	4.91	2.70	1.64	0.53	133.0	82.0
	6	4.12	1.90	1.38	0.53	130.0	81.0
Port B	1	5.59	3.50	1.87	0.53	132.0	81.0
	2	5.04	2.85	1.69	0.53	133.0	81.0
	3	4.68	2.45	1.57	0.53	133.0	81.0
	4	4.86	2.65	1.63	0.53	132.0	81.0
	5	4.72	2.50	1.58	0.53	132.0	81.0
	6	4.53	2.30	1.52	0.53	132.0	81.0
		60.12		1.69	0.53	131.5	81.6

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	23.713
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.84
Static Pressure, in. Hg	-1.95

ANALYTICAL RECOVERY DATA

Moisture, %	6.1
Mass (probe wash)<PM10, g	0.0029
Mass (filter)<PM10, g	0.0134

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/4/92	#1 DRYER STACK 3	PM 10	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.84	-1.95	57	62Q013	42	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL in. Hg	TRAIN LEAK CHECK (INITIAL CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.88	0.998	4A5	PT-1	64	—	5.0	0.003	5.0	0.002	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					✓	✓
Analysis Method	FYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B 6	0/0	1518	503.418	2.80	0.53	120	252	252	59	83	—	2.0
5	5.09		505.48	2.80	.53	127	251	253	57	81		2.0
4	10.18		507.56	2.10	.53	126	252	254	57	81		2.0
3	14.59		509.06	2.25	.53	126	251	254	57	81		2.0
2	19.16		510.91	2.20	.53	125	251	255	56	81		2.0
1	23.67		512.73	1.70	.53	125	252	254	56	81		2.0
A 6	27.64/0	1514/1523	513.96	2.80	.53	125	253	254	57	81		2.0
5	5.09		515.77	2.60	.53	126	252	255	57	80		2.0
4	10.00		517.65	1.80	.53	126	250	254	58	80		2.0
3	14.08		519.28	1.70	.53	124	251	253	58	80		2.0
2	18.05		520.32	1.55	.53	124	250	251	58	80		2.0
1	21.84		521.95	1.20	.53	124	251	252	58	80		2.0
	25.87	1549	523.216									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	52.87	19.798	1.47	.53	125.0	

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.04	1.53	1.19	0.95	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	
V min	minimum velocity	63.22	ft/sec
V max	maximum velocity	102.65	ft/sec

Delta p min.	1.157	in.H2O
Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt)^2 (from LAST velocity traverse)	2.700

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	2.80	1.67	5.09	2.80	1.67	5.09
2	2.80	1.67	5.09	2.60	1.61	4.91
3	2.10	1.45	4.41	1.80	1.34	4.08
4	2.25	1.50	4.56	1.70	1.30	3.97
5	2.20	1.48	4.51	1.55	1.24	3.79
6	1.70	1.30	3.97	1.20	1.10	3.33
		Time(min)	27.64		Time(min)	25.17

PM10 DATA

SOURCE DRYER STACK-3 RUN 1 DATE 3-14-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.09	2.80	1.67	0.53	130.0	83.0
	2	5.09	2.80	1.67	0.53	127.0	81.0
	3	4.41	2.10	1.45	0.53	126.0	81.0
	4	4.56	2.25	1.50	0.53	126.0	81.0
	5	4.51	2.20	1.48	0.53	125.0	81.0
	6	3.97	1.70	1.30	0.53	125.0	81.0
Port B	1	5.09	2.80	1.67	0.53	125.0	81.0
	2	4.91	2.60	1.61	0.53	126.0	80.0
	3	4.08	1.80	1.34	0.53	126.0	80.0
	4	3.97	1.70	1.30	0.53	124.0	80.0
	5	3.79	1.55	1.24	0.53	124.0	80.0
	6	3.33	1.20	1.10	0.53	124.0	80.0
		52.81		1.47	0.53	125.8	80.8

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft ^ 3	19.798
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.84
Static Pressure, in. Hg	-1.95

ANALYTICAL RECOVERY DATA

Moisture, %	5.8
Mass (probe wash)<PM10, g	0.0001
Mass (filter)<PM10, g	0.0112

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AZ.	3/14/92	#1 STACK DRYER #3	PM10	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.84	-1.95		62Q014	42"	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	~~[illegible]~~	1.88	0.998	4A5	PT 1	64	—	5.0	0.007			

M8 EPA METHOD 3
Collection Method: GRAB
Analysis Method: FYRITE

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	20.9				
%CO2					

PITOT SYSTEM LEAK CHECK INIT	FINAL
✓	

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 6	0/0	1744	523.594	3.00	0.55	125	252	251	60	79	—	2.0
5	5.71		526.01	2.70	.55	125	251	252	58	80		2.0
4	11.13		528.25	2.25	.55	125	251	252	54	80		2.0
3	16.07		530.27	1.90	.55	125	249	252	54	80		2.0
2	20.62		532.16	1.75	.55	123	249	251	54	80		2.0
1	24.98		533.76	1.30	.55	120	249	250	55	80		2.0
A 6	28.74-0-	1814/1819	534.81	3.25	.55	127	250	252	55	80		2.0
5	5.94		537.17	3.10	.55	127	251	252	56	81		2.0
4	11.75		539.54	2.65	.55	127	249	251	56	81		2.0
3	17.12		541.84	2.35	.55	127	251	252	56	81		2.0
2	22.17		544.09	2.20	.55	126	250	251	57	81		2.0
1	27.06		545.97	2.10	.55	122	251	252	57	81		2.0
	31.84	1851	545.96									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60.58	22.367			125.1	

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.04	1.53	1.19	0.95	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt)^2 (from LAST velocity traverse)	2.300

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	3.00	1.73	5.71	3.25	1.80	5.94
2	2.70	1.64	5.42	3.10	1.76	5.80
3	2.25	1.50	4.95	2.65	1.63	5.37
4	1.90	1.38	4.54	2.35	1.53	5.05
5	1.75	1.32	4.36	2.20	1.48	4.89
6	1.30	1.14	3.76	2.10	1.45	4.78
		Time(min)	28.74		Time(min)	31.84

PM10 DATA

SOURCE DRYER STACK-3 RUN 2 DATE 3-14-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.71	3.00	1.73	0.53	125.0	79.0
	2	5.42	2.70	1.64	0.53	125.0	80.0
	3	4.95	2.25	1.50	0.53	125.0	80.0
	4	4.54	1.90	1.38	0.53	125.0	80.0
	5	4.36	1.75	1.32	0.53	123.0	80.0
	6	3.76	1.30	1.14	0.53	120.0	80.0
Port B	1	5.94	3.25	1.80	0.53	127.0	80.0
	2	5.80	3.10	1.76	0.53	127.0	81.0
	3	5.37	2.65	1.63	0.53	127.0	81.0
	4	5.05	2.35	1.53	0.53	127.0	81.0
	5	4.89	2.20	1.48	0.53	126.0	81.0
	6	4.78	2.10	1.45	0.53	122.0	81.0
		60.58		1.55	0.53	125.1	80.3

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	22.367
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.84
Static Pressure, in. Hg	-1.95

ANALYTICAL RECOVERY DATA

Moisture, %	6.3
Mass (probe wash)<PM10, g	0.0050
Mass (filter)<PM10, g	0.0300

EMISSION TEST[illegible] FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AK	3/16/92	#1 DRYER STACK Y	PM-10	~~2~~ 1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	30.05	-2.00		62Q 015	42"	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.92	0.998	4A5	PT-1	G4	—	50	0.007	5.0	0.002	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	GRAB	%O2	20.9					✓	✓
Analysis Method	FYRITE	%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B ~~5~~ 6	0/0	0930	548.881	2.90	0.53	132	250	252	47	51	—	2.0
5	5.5	0912/0923	550.97	2.40	.53	134	251	254	47	53		2.0
4	10.5		552.87	2.20	.53	134	249	254	46	55		2.0
3	15.28		554.51	2.30	.53	138	250	255	46	60		2.0
2	20.18		556.36	2.00	.53	136	250	256	46	62		2.0
1	24.74		558.11	1.40	.53	130	250	254	47	62		2.0
A ~~5~~ 6	28.56/0	~~0~~ 0947	559.63	2.65	.53	136	251	254	47	63		2.0
5	5.25		561.43	1.90	.53	134	251	254	47	64		2.0
4	9.70		563.22	2.10	.53	132	250	253	48	65		2.0
3	14.38		565.10	2.20	.53	130	250	253	48	65		2.0
2	19.17		567.04	2.20	.53	127	251	253	48	66		2.0
1	23.95		568.13	1.60	.53	127	251	255	47	67		2.0
	28.04	1016	569.842									

STOP TO CLEAN M-5 NOZZLE

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	56.60	20.961	1.461	0.53	132.5	~~61.1~~ 60.8

JB

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.04	1.53	1.19	0.95	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt)^2 (from LAST velocity traverse)	2.400

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	2.90	1.70	5.50	2.65	1.63	5.25
2	2.40	1.55	5.00	1.90	1.38	4.45
3	2.20	1.48	4.79	2.10	1.45	4.68
4	2.30	1.52	4.89	2.20	1.48	4.79
5	2.00	1.41	4.56	2.20	1.48	4.79
6	1.40	1.18	3.82	1.60	1.26	4.08
		Time(min)	28.56		Time(min)	28.04

PM10 DATA

SOURCE DRYER STACK-4 RUN 1 DATE 3-16-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.50	2.90	1.70	0.53	132.0	51.0
	2	5.00	2.40	1.55	0.53	134.0	53.0
	3	4.79	2.20	1.48	0.53	134.0	55.0
	4	4.89	2.30	1.52	0.53	138.0	60.0
	5	4.56	2.00	1.41	0.53	136.0	62.0
	6	3.82	1.40	1.18	0.53	130.0	62.0
Port B	1	5.25	2.65	1.63	0.53	136.0	63.0
	2	4.45	1.90	1.38	0.53	134.0	64.0
	3	4.68	2.10	1.45	0.53	132.0	65.0
	4	4.79	2.20	1.48	0.53	130.0	65.0
	5	4.79	2.20	1.48	0.53	127.0	66.0
	6	4.08	1.60	1.26	0.53	127.0	67.0
		56.60		1.47	0.53	132.6	60.8

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	20.961
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	30.05
Static Pressure, in. Hg	-2.00

ANALYTICAL RECOVERY DATA

Moisture, %	6.7
Mass (probe wash)<PM10, g	0.0113
Mass (filter)<PM10, g	0.0196

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON AK	3/16/92	#1 DRYERSTACK 4	PM-10	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE NUMBER AND TYPE	NOZZLE I.D.	NOZZLE NO.
T. THOMPSON	30.05	-2.00		62Q016	42	0.84	4A GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-8	1.92	0.998	4A-5	PT1	64	—	5.0	0.003			

EPA METHOD 3
Collection Method: GRAB
Analysis Method: FYRITE

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	20.9				
%CO2	—				

PITOT SYSTEM LEAK CHECK INIT	FINAL
✓	

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
A6	0/0	1055	570.150	2.70	0.53	132	251	250	61	75	—	2.5
5	5.30		572.08	2.60	.53	132	252	250	60	76		2.5
4	10.51		574.18	2.60	.53	131	252	252	57	76		2.5
3	15.71		576.30	2.65	.53	132	252	252	56	77		2.5
2	20.97		578.44	2.15	.53	127	253	251	55	78		2.5
1	25.70		580.41	1.50	.53	126	254	250	55	79		2.5
B6	29.65/0	1125/	581.69	2.60	.53	131	254	257	55	80		2.5
5	5.20		583.79	2.50	.53	131	255	252	55	80		2.5
4	10.31		585.88	2.20	.53	132	254	253	55	81		2.5
3	15.09		587.81	2.10	.53	132	253	250	55	82		2.5
2	19.77		589.67	1.85	.53	130	252	251	55	81		2.5
1	24.16		591.49	1.50	.53	126	252	252	56	81		2.5

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	59.77 (28.11)	593.201				

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.88	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	6 (MEAN TEMP)
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.04	1.53	1.19	0.95	0.78	0.65

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.55	0.47	0.41	0.36	0.32	0.28

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	2.400

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	2.70	1.64	5.30	2.60	1.61	5.20
2	2.60	1.61	5.20	2.50	1.58	5.10
3	2.60	1.61	5.20	2.20	1.48	4.79
4	2.65	1.63	5.25	2.10	1.45	4.68
5	2.15	1.47	4.73	1.85	1.36	4.39
6	1.50	1.22	3.95	1.50	1.22	3.95
		Time(min)	29.65		Time(min)	28.11

PM10 DATA

SOURCE DRYER STACK-4 RUN 2 DATE 3-16-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	5.30	2.70	1.64	0.53	132.0	75.0
	2	5.20	2.60	1.61	0.53	134.0	76.0
	3	5.20	2.60	1.61	0.53	131.0	76.0
	4	5.25	2.65	1.63	0.53	132.0	77.0
	5	4.73	2.15	1.47	0.53	127.0	78.0
	6	3.95	1.50	1.22	0.53	126.0	79.0
Port B	1	5.20	2.60	1.61	0.53	131.0	80.0
	2	5.10	2.50	1.58	0.53	131.0	80.0
	3	4.79	2.20	1.48	0.53	132.0	81.0
	4	4.68	2.10	1.45	0.53	132.0	82.0
	5	4.39	1.85	1.36	0.53	130.0	81.0
	6	3.95	1.50	1.22	0.53	126.0	81.0
		57.77		1.51	0.53	130.5	78.7

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	23.051
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	30.05
Static Pressure, in. Hg	-2.00

ANALYTICAL RECOVERY DATA

Moisture, %	5.9
Mass (probe wash)<PM10, g	0.0059
Mass (filter)<PM10, g	0.0215

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/17/92	DRYER STACK #6	PM 10	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.83	-0.9		620004	40	0.84	4 GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-5	1.92	0.998				—	Ø.7	0.005			

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2	20.7					✓	✓
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 6	0/0	0842	816.831	1.35	0.27	137	250	253	51	48	—	1.0
5	4.6		818.15	1.65	.27	137	249	252	50	49		1.0
4	9.67 ~~5.66~~		819.58	1.85	.27	139	251	251	50	51		1.0
3	15.05		821.07	1.80	.27	137	251	253	50	53		1.0
2	20.35		822.58	1.50	.27	137	250	252	53	55		1.0
1	25.19		823.98	.85	.27	136	248	251	54	55		1.0
B 6	29.84/0	0911/0921	825.08	1.50	.27	140	249	253	54	56		1.0
5	4.84		826.50	1.90	.27	141	250	250	54	58		1.0
4	10.29		828.11	1.90	.27	139	250	252	54	58		1.0
3	15.74		829.72	1.80	.27	142	251	255	54	59		1.0
2	21.04		831.29	1.50	.27	143	250	251	54	60		1.0
1	25.88		832.72	.90	.27	150	251	252	55	61		1.0
	29.63	0950	833.827									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	58.47	16.996	1.233	.27	137.1	55.2

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.92	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.09	1.57	1.22	0.97	0.80	0.66

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.56	0.48	0.42	0.37	0.32	0.29

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	1.600

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	1.35	1.16	4.59	1.50	1.22	4.84
2	1.65	1.28	5.08	1.90	1.38	5.45
3	1.85	1.36	5.38	1.90	1.38	5.45
4	1.80	1.34	5.30	1.80	1.34	5.30
5	1.50	1.22	4.84	1.50	1.22	4.84
6	0.85	0.92	3.64	0.90	0.95	3.75
		Time(min)	28.84		Time(min)	29.63

PM10 DATA

SOURCE DRYER STACK-6 RUN 1 DATE 3-12-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	4.59	1.35	1.16	0.27	137.0	48.0
	2	5.08	1.65	1.28	0.27	137.0	49.0
	3	5.38	1.85	1.36	0.27	139.0	51.0
	4	5.30	1.80	1.34	0.27	137.0	53.0
	5	4.84	1.50	1.22	0.27	137.0	55.0
	6	3.64	0.85	0.92	0.27	136.0	55.0
Port B	1	4.84	1.50	1.22	0.27	140.0	56.0
	2	5.45	1.90	1.38	0.27	141.0	58.0
	3	5.45	1.90	1.38	0.27	139.0	58.0
	4	5.30	1.80	1.34	0.27	142.0	59.0
	5	4.84	1.50	1.22	0.27	143.0	60.0
	6	3.75	0.90	0.95	0.27	140.0	61.0
		58.47		1.25	0.27	139.1	55.2

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	16.996
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.83
Static Pressure, in. Hg	0.90

ANALYTICAL RECOVERY DATA

Moisture, %	8.3
Mass (probe wash)<PM10, g	0.0039
Mass (filter)<PM10, g	0.0162

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/12/92	DRYER STACK #6	PM10	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.83	-0.70		62@005	40	0.84	4 GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-5	1.92	0.998					5.6	0.002	5.0	0.001	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2	20.9					✓	✓
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 6	0/0	1049	839.971	1.55	0.27	145	240	247	54	63	—	1.0
5	4.92		835.35	1.90	.27	139	247	250	47	65		1.0
4	10.37		836.85	1.90	.27	139	250	252	44	65		1.0
3	15.82		838.41	1.75	.27	139	257	253	44	65		1.0
2	21.05		839	1.70	.27	136	251	252	45	67		1.0
1	26.20		841.31	.85	.27	125	252	251	46	67		1.0
A 6	29.85	1118	842.33	1.30	.27	137	250	252	46	67		1.0
5	4.51		843.74	1.65	.27	137	250	252	47	67		1.0
4	9.58		845.27	1.70	.27	139	252	253	48	67		1.0
3	14.74		846.84	1.80	.27	142	252	253	49	68		1.0
2	20.40		848.56	1.50	.27	136	253	253	48	67		1.0
1	24.88		849.90	1.00	.27	133	253	254	49	67		1.0
	28.84	1157	851.097									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	58.68	~~23.126~~ 17.126	1.25 ↑	.27	137.7	66.2

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.92	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.09	1.57	1.22	0.97	0.80	0.66

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.56	0.48	0.42	0.37	0.32	0.29

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	1.600

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	1.55	1.24	4.92	1.30	1.14	4.51
2	1.90	1.38	5.45	1.65	1.28	5.08
3	1.90	1.38	5.45	1.70	1.30	5.15
4	1.75	1.32	5.23	1.80	1.34	5.30
5	1.70	1.30	5.15	1.50	1.22	4.84
6	0.85	0.92	3.64	1.00	1.00	3.95
		Time(min)	29.85		Time(min)	28.84

PM10 DATA

SOURCE DRYER STACK-6 RUN 2 DATE 3-12-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	4.92	1.55	1.24	0.27	145.0	63.0
	2	5.45	1.90	1.38	0.27	139.0	65.0
	3	5.45	1.90	1.38	0.27	139.0	65.0
	4	5.23	1.75	1.32	0.27	139.0	65.0
	5	5.15	1.70	1.30	0.27	136.0	67.0
	6	3.64	0.85	0.92	0.27	125.0	67.0
Port B	1	4.51	1.30	1.14	0.27	137.0	67.0
	2	5.08	1.65	1.28	0.27	137.0	67.0
	3	5.15	1.70	1.30	0.27	139.0	67.0
	4	5.30	1.80	1.34	0.27	142.0	68.0
	5	4.84	1.50	1.22	0.27	136.0	67.0
	6	3.95	1.00	1.00	0.27	133.0	67.0
		58.68		1.25	0.27	137.7	66.2

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	17.126
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.83
Static Pressure, in. Hg	0.90

ANALYTICAL RECOVERY DATA

Moisture, %	7.6
Mass (probe wash)<PM10, g	0.0012
Mass (filter)<PM10, g	0.0056

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/12/92	DRYER STACK 6	PM 10	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.83	-0.9		629006	40	0.84	4 GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M-5	1.92	0.998		PT-1	6-4	—	5.0	0.002	5.0	0.002	

EPA METHOD 3
Collection Method
Analysis Method: FYRITE

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	20.9				
%CO2	—				

PITOT SYSTEM LEAK CHECK INIT	FINAL
✓	✓

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A6	0/0	1312	851.287	1.40	0.27	136	245	244	56	66	—	1.0
5	4.83		852.69	1.60	.27	137	247	248	51	66		1.0
4	9.99		854.17	1.85	.27	137	249	251	48	67		1.0
3	15.55		855.82	1.70	.27	137	250	251	46	68		1.0
2	20.87		857.34	1.50	.27	135	251	253	46	68		1.0
1 1	25.87		852.77	.90	.27	135	251	252	46	68		1.0
B6	29.74	1342/1349	859.94	1.70	.27	136	252	253	49	68		1.0
5	5.32		861.48	1.80	.27	136	252	257	49	69		1.0
4	10.86		863.16	1.80	.27	139	252	254	50	69		1.0
3	16.28		864.69	1.75	.27	136	250	253	50	69		1.0
2	21.68		866.26	1.85	.27	136	251	253	51	69		1.0
1	27.23		867.85	1.05	.27	132	250	252	51	70		1.0
	31.41		869.074									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	~~[illegible]~~ 61.16	17.787				

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Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.92	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.09	1.57	1.22	0.97	0.80	0.66

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.56	0.48	0.42	0.37	0.32	0.29

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt)^2 (from LAST velocity traverse)	1.500

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	1.40	1.18	4.83	1.70	1.30	5.32
2	1.60	1.26	5.16	1.80	1.34	5.48
3	1.85	1.36	5.55	1.80	1.34	5.48
4	1.70	1.30	5.32	1.75	1.32	5.40
5	1.50	1.22	5.00	1.85	1.36	5.55
6	0.90	0.95	3.87	1.05	1.02	4.18
		Time(min)	29.74		Time(min)	31.41

PM10 DATA

SOURCE DRYER STACK-6 RUN 3 DATE 3-12-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	4.83	1.40	1.18	0.27	136.0	66.0
	2	5.16	1.60	1.26	0.27	137.0	66.0
	3	5.55	1.85	1.36	0.27	137.0	67.0
	4	5.32	1.70	1.30	0.27	137.0	68.0
	5	5.00	1.50	1.22	0.27	135.0	68.0
	6	3.87	0.90	0.95	0.27	135.0	68.0
Port B	1	5.32	1.70	1.30	0.27	136.0	68.0
	2	5.48	1.80	1.34	0.27	136.0	69.0
	3	5.48	1.80	1.34	0.27	139.0	69.0
	4	5.40	1.75	1.32	0.27	136.0	69.0
	5	5.55	1.85	1.36	0.27	136.0	69.0
	6	4.18	1.05	1.02	0.27	132.0	70.0
		61.16		1.26	0.27	136.1	68.1

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft ^ 3	17.787
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	42.0
Barometric Pressure, in. Hg	29.83
Static Pressure, in. Hg	0.90

ANALYTICAL RECOVERY DATA

Moisture, %	8.0
Mass (probe wash)<PM10, g	0.0025
Mass (filter)<PM10, g	0.0086

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AL	3/11/92	DRYER STACK # 8	PM10	1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.79	-1.00	40	62Q002	37.5	0.84	5 STAINLESS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
12	M-5	1.92	0.998		PT-1	G-4		0.004	15	0.000	4	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2	20.7					✓	✓
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B 6	0/0	1015	750.047	~~2.00~~ 1.90	0.47	127	251	248	43	52	—	2.0
5	4.59		751.88	2.20	.47	132	251	249	44	53		2.0
4	9.31		753.49	2.40	.47	132	252	249	45	54		2.0
3	14.47		755.38	2.40	.47	133	250	252	45	55		2.0
2	19.64		757.34	2.60	.47	134	250	251	46	56		2.0
1	25.01		759.36	2.10	.47	127	251	253	46	57		2.0
A 6	29.84/0		761.17	2.40	.47	130	251	252	47	56		2.0
5	5.16		763.09	2.40	.47	133	251	253	48	58		2.0
4	10.53		765.09	2.30	.47	135	251	253	48	58		2.0
3	15.38		767.04	2.40	.47	133	253	255	48	58		2.0
2	20.55		768.87	2.16	.47	125	250	255	49	59		2.0
1	25.38		770.68	1.00	.47	119	250	253	49	60		2.0
	28.71		771.930									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	58.55	21.883	1.49	0.47	130.4	56.3

1.47

2.16

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.92	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.09	1.57	1.22	0.97	0.80	0.66

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.56	0.48	0.42	0.37	0.32	0.29

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt)^2 (from LAST velocity traverse)	2.250

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	1.90	1.38	4.59	2.40	1.55	5.16
2	2.20	1.48	4.72	2.40	1.55	5.16
3	2.40	1.55	5.16	2.30	1.52	5.06
4	2.40	1.55	5.16	2.40	1.55	5.16
5	2.60	1.61	5.37	2.10	1.45	4.83
6	2.10	1.45	4.83	1.00	1.00	3.33
		Time(min)	29.85		Time(min)	28.71

PM10 DATA

SOURCE DRYER STACK-8 RUN 1 DATE 3-11-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	4.59	1.90	1.38	0.47	127.0	52.0
	2	4.72	2.20	1.48	0.47	132.0	53.0
	3	5.16	2.40	1.55	0.47	132.0	54.0
	4	5.16	2.40	1.55	0.47	133.0	55.0
	5	5.37	2.60	1.61	0.47	134.0	56.0
	6	4.83	2.10	1.45	0.47	127.0	57.0
Port B	1	5.16	2.40	1.55	0.47	130.0	56.0
	2	5.16	2.40	1.55	0.47	133.0	58.0
	3	5.06	2.30	1.52	0.47	135.0	58.0
	4	5.16	2.40	1.55	0.47	133.0	58.0
	5	4.83	2.10	1.45	0.47	125.0	59.0
	6	3.33	1.00	1.00	0.47	119.0	60.0
		58.56		1.49	0.47	130.4	56.3

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft ^ 3	21.883
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	37.5
Barometric Pressure, in. Hg	29.79
Static Pressure, in. Hg	-1.00

ANALYTICAL RECOVERY DATA

Moisture, %	7.8
Mass (probe wash)<PM10, g	0.0014
Mass (filter)<PM10, g	0.0069

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOISIANA PACIFIC CLAYTON, AL	3/11/92	DRYER STACK 8	PM-10	2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.76	-1.00	49	62Q001	37.5	0.84	5 STAINLESS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
12	M-5	1.92	0.958		PT1	65	—	5	0.005	5	0.004	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	FYRITE	%O2	20.9					✓	✓
Analysis Method		%CO2	—						

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 6	0/0	1303	771.932	2.10	0.47	131	245	240	52	59	—	1.0
5	4.83		77	2.30	.47	131	249	247	50	59		1.0
4	9.87		775.65	2.40	.47	129	250	249	50	59		1.0
3	15.05		778.56	2.4	.47	129	251	250	50	59		1.0
2	20.21		779.57	2.1	.47	125	250	252	50	60		1.0
1	25.04		781.38	2.3	.47	123	251	252	50	60		1.0
B 6	30.1/0	1323/1349	783.37	1.8	.47	129	250	250	52	60		1.0
5	4.47		785.08	2.3	.47	129	251	251	53	61		1.0
4	9.53		786.97	2.5	.47	129	250	249	54	61		1.0
3	14.80		789.97	2.3	.47	129	251	250	55	61		1.0
2	19.85		790.87	2.3	.47	127	252	253	57	62		1.0
1	24.91		792.78	1.8	.47	121	252	252	57	63		1.0
	29.38	1420	794.463									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	54.42	22.531				
	5946					

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.92	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

	1	2	3	4	5	MEAN TEMP 6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.09	1.57	1.22	0.97	0.80	0.66

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.56	0.48	0.42	0.37	0.32	0.29

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches			
Vn	Nozzle Velocity	83.481	ft/sec			
R min.	minimum R	0.757				
R max.	maximum R	1.230				
V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt) ^ 2 (from LAST velocity traverse)	2.250

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	2.10	1.45	4.83	1.80	1.34	4.47
2	2.30	1.52	5.06	2.30	1.52	5.06
3	2.40	1.55	5.16	2.50	1.58	5.27
4	2.40	1.55	5.16	2.30	1.52	5.06
5	2.10	1.45	4.83	2.30	1.52	5.06
6	2.30	1.52	5.06	1.80	1.34	4.47
		Time(min)	30.10		Time(min)	29.38

PM10 DATA

SOURCE DRYER STACK-8 RUN 2 DATE 3-11-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	4.83	2.10	1.45	0.47	131.0	52.0
	2	5.06	2.30	1.52	0.47	131.0	50.0
	3	5.16	2.40	1.55	0.47	129.0	50.0
	4	5.16	2.40	1.55	0.47	129.0	50.0
	5	4.83	2.10	1.45	0.47	125.0	50.0
	6	5.06	2.30	1.52	0.47	123.0	50.0
Port B	1	4.47	1.80	1.34	0.47	129.0	52.0
	2	5.06	2.30	1.52	0.47	129.0	53.0
	3	5.27	2.50	1.58	0.47	129.0	54.0
	4	5.06	2.30	1.52	0.47	129.0	55.0
	5	5.06	2.30	1.52	0.47	127.0	57.0
	6	4.47	1.80	1.34	0.47	121.0	57.0
		59.48		1.49	0.47	127.7	52.5

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	22.531
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	37.5
Barometric Pressure, in. Hg	29.76
Static Pressure, in. Hg	-1.00

ANALYTICAL RECOVERY DATA

Moisture, %	8.3
Mass (probe wash)<PM10, g	0.0011
Mass (filter)<PM10, g	0.0056

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
LOUISIANA PACIFIC CLAYTON, AC	3/11/92	DRYER STACK #8	PM 10	3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
T. THOMPSON	29.79	-1.00		62Q003	37.5	0.84	4 GLASS		0.133

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
12	M-5	1.92	0.998		PT-1	G-5	—	7	0.004	3	0.001	

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2	20.9						
Analysis Method	FYRITE	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
B 6	0/0	1518	794.546	2.00	0.47	130	247	250	52	61	—	1.0
5	4.71		796.29	2.25	.47	130	249	251	50	62		1.0
4	9.71		798.17	2.50	.47	129	250	252	50	62		1.0
3	14.98		800.15	2.25	.47	129	250	251	50	62		1.0
2	19.98		802.00	1.90	.47	127	250	253	50	62		1.0
1	24.58		803.83	1.85	.47	127	251	252	51	62		1.0
A 6	29.11/0	1546/1553	805.41	2.10	.47	129	257	252	53	61		1.0
5	4.83		807.54	2.30	.47	129	256	253	53	61		1.0
4	9.89		809.44	2.40	.47	131	257	255	54	61		1.0
3	15.05		811.37	2.40	.47	131	252	255	54	61		1.0
2	20.21		813.30	1.80	.47	125	252	254	54	61		1.0
1	24.69		814.96	1.70	.47	120	250	255	55	60		1.0
	29.03	1624	816.571									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	58.14					

Sheet Checked By: _____ Date _____

CYCLONE FLOW RATE and DELTA H WORKSHEET

Pb	Barometric Pressure	29.84	in.Hg
Pg	Static Pressure	-1.95	in.H20
Ts	Average Stack Temp.	114	deg.F
Tm	Meter temperature	69	deg.F
	Delta H@	1.92	in.H20
CO2	Carbon dioxide concentration	0.0	%
O2	Oxygen concentration	20.9	%
N2+CO	Nitrogen(+ CO) concentration	79.1	%
Bws	Fraction moisture content	0.000	(Ex. 4% = 0.04)
Md	Molecular Weight(Dry)	28.84	lb/lb mole
Mw	Molecular Weight(Wet)	28.84	lb/lb mole
Ps	Absolute Stack Pressure	29.70	in.Hg
Us	Viscosity of Stack gas	191.65	micropoise
Qs	Cyclone flow rate	0.483	ft^3/min.

MEAN TEMP

	1	2	3	4	5	6
Stack temp	-136	-86	-36	14	64	114
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	2.09	1.57	1.22	0.97	0.80	0.66

	7	8	9	10	11	12
Stack temp	164	214	264	314	364	414
Meter Temp.	69.4	69.4	69.4	69.4	69.4	69.4
Delta H(in.H2O)	0.56	0.48	0.42	0.37	0.32	0.29

MAXIMUM AND MINIMUM VELOCITIES

Dn	Nozzle diameter	0.133	inches
Vn	Nozzle Velocity	83.481	ft/sec
R min.	minimum R	0.757	
R max.	maximum R	1.230	

V min	minimum velocity	63.22	ft/sec	Delta p min.	1.157	in.H2O
V max	maximum velocity	102.65	ft/sec	Delta p max.	3.049	in.H2O

DELTA P VARIATION OVER NOZZLE RANGE

Nozzle #	1	2	3	4	5	6	7	8
Dn in.	0.161	0.182	0.196	0.214	0.232	0.263	0.299	0.342
Vn	56.969	44.581	38.440	32.245	27.436	21.349	16.518	12.625
R min.	0.722	0.682	0.648	0.589	0.502	ERR	ERR	ERR
R max.	1.252	1.274	1.291	1.317	1.346	1.405	1.488	1.604
Vmin.	41.11	30.42	24.90	18.99	13.78	10.67	8.26	6.31
Vmax	71.31	56.78	49.62	42.45	36.92	30.00	24.57	18.94
Dp min.	0.489	0.268	0.179	0.104	0.055	0.033	0.020	0.012
Dp max.	1.471	0.933	0.713	0.521	0.395	0.260	0.175	0.104

DWELL TIME CALCULATION

Total run time	60
Number of points	12
(avg.Sq rt)^2 (from LAST velocity traverse)	2.250

	PORT A			PORT B		
Point Number	Delta P	SQRT Delta P	Sample Time	Delta P	SQRT Delta P	Sample Time
1	2.00	1.41	4.71	2.10	1.45	4.83
2	2.25	1.50	5.00	2.30	1.52	5.06
3	2.50	1.58	5.27	2.40	1.55	5.16
4	2.25	1.50	5.00	2.40	1.55	5.16
5	1.90	1.38	4.59	1.80	1.34	4.47
6	1.85	1.36	4.53	1.70	1.30	4.35
		Time(min)	29.11		Time(min)	29.03

PM10 DATA

SOURCE DRYER STACK-8 RUN 3 DATE 3-11-92

Delta p and Temperature data

Port A	Point	Dwell Time	Delta P	Sqrt Dp	Delta H	Stack Temp	Meter Temp
	1	4.71	2.00	1.41	0.47	130.0	61.0
	2	5.00	2.25	1.50	0.47	130.0	62.0
	3	5.27	2.50	1.58	0.47	129.0	62.0
	4	5.00	2.25	1.50	0.47	129.0	62.0
	5	4.59	1.90	1.38	0.47	127.0	62.0
	6	4.53	1.85	1.36	0.47	127.0	62.0
Port B	1	4.83	2.10	1.45	0.47	129.0	61.0
	2	5.06	2.30	1.52	0.47	129.0	61.0
	3	5.16	2.40	1.55	0.47	131.0	61.0
	4	5.16	2.40	1.55	0.47	131.0	61.0
	5	4.47	1.80	1.34	0.47	125.0	61.0
	6	4.35	1.70	1.30	0.47	120.0	60.0
		58.14		1.46	0.47	128.2	61.3

INPUT DATA FOR ISOKINETIC CALCULATIONS

Meter Box y	0.998
Meter volume, ft^3	22.025
CO2 concentration, %	0.0
Oxygen concentration, %	20.9
Nozzle diameter, inches	0.133
Stack diameter, inches	37.5
Barometric Pressure, in. Hg	29.79
Static Pressure, in. Hg	-1.00

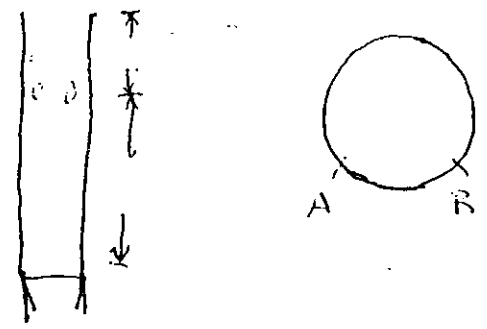
ANALYTICAL RECOVERY DATA

Moisture, %	6.6
Mass (probe wash)<PM10, g	0.0043
Mass (filter)<PM10, g	0.0057

/

EPA METHOD 1
TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

PLANT LOUISIANA PACIFIC
CITY CLAYTON STATE ALABAMA
SAMPLING LOCATION DRYER STACK 1
INSIDE OF FAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE A) 42"
INSIDE OF NEAR WALL TO OUTSIDE OF NIPPLE, (DISTANCE B) 0
NEAREST UPSTREAM DISTURBANCE
DISTURBANCE
NEAREST DOWNSTREAM DISTURBANCE
DISTURBANCE
SAMPLER T. THOMPSON DATE 3/13/92



SCHEMATIC OF SAMPLING LOCATION

TRAVERSE POINT NUMBER	FRACTION OF STACK I.D.	STACK I.D.	PRODUCT OF COLUMNS 2 AND 3 (TO NEAREST 1/8-INCH)	DISTANCE B	TRAVERSE DISTANCE FROM OUTSIDE OF NIPPLE (SUM OF COLUMNS 4 & 5)
1	0.044	42"			1 7/8"
2	.146				6 1/8
3	.296				12 3/8
4	.704				29 5/8
5	.854				35 7/8
6	.956				40 1/8

epa1circ.wk1

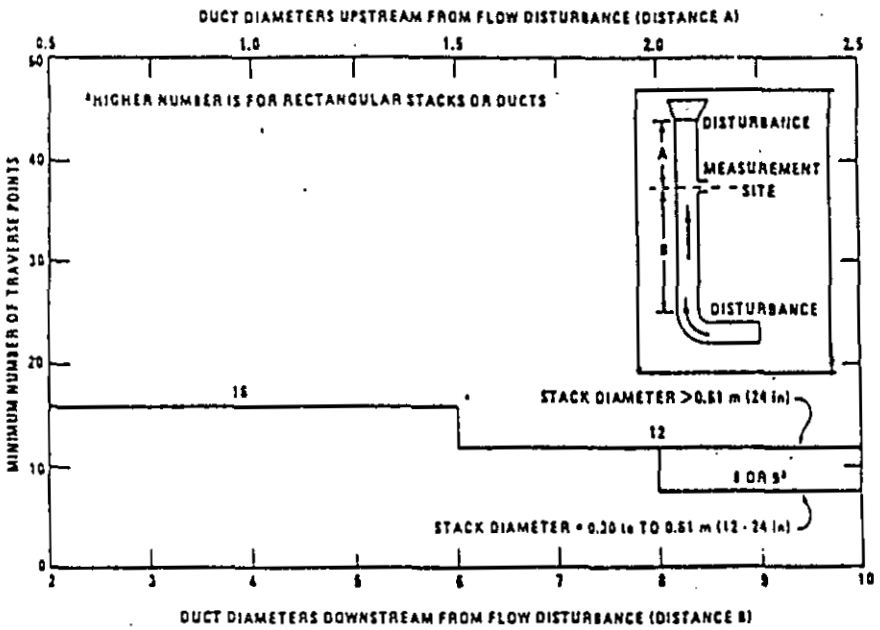


Figure 1-2. Minimum number of traverse points for velocity (nonparticulate) traverses.

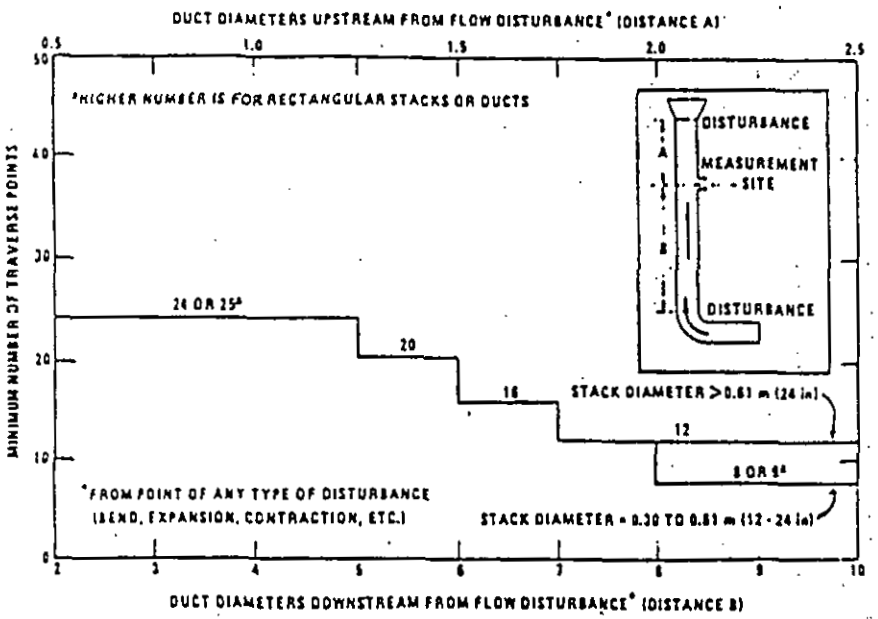


Figure 1-1. Minimum number of traverse points for particulate traverses.

CIRCULAR DUCTS

Traverse point number on a diameter	Number of Points in Traverse (Percent of stack diameter from inside wall to traverse point)					
	2	4	6	8	10	12
1	14.6	6.7	4.4	3.2	2.6	2.1
2	85.4	25.0	14.6	10.5	8.2	6.7
3		75.0	29.6	19.4	14.6	11.8
4		93.3	70.4	32.3	22.6	17.7
5			85.4	67.7	34.2	25.0
6			95.6	80.6	65.8	35.6
7				89.5	77.4	64.4
8				96.8	85.4	75.0
9					91.8	82.3
10					97.4	88.2
11						93.3
12						97.9

2.3.1 Circular Stacks. Locate the traverse points on two perpendicular diameters according to Table 1-2 and the example shown in Figure 1-3. Any equation (for examples, see Citations 2 and 3 in the Bibliography) that gives the same values as those in Table 1-2 may be used in lieu of Table 1-2.

For particulate traverses, one of the diameters must be in a plane containing the greatest expected concentration variation, e.g., after bends, one diameter shall be in the plane of the bend. This requirement becomes less critical as the distance from the disturbance increases; therefore, other diameter locations may be used, subject to approval of the Administrator.

2.3.1.1 Stacks With Diameters Greater Than 0.61 m (24 in.). When any of the traverse points as located in Section 2.3.1 fall within 2.5 cm (1.00 in.) of the stack walls, relocate them away from the stack walls to: (1) a distance of 2.5 cm (1.00 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger. These relocated traverse points (on each end of a diameter) shall be the "adjusted" traverse points.

Whenever two successive traverse points are combined to form a single adjusted traverse point, treat the adjusted point as two separate traverse points, both in the sampling (or velocity measurement) procedure, and in recording the data.

2.3.1.2 Stacks With Diameters Equal to or Less Than 0.61 m (24 in.). Follow the procedure in Section 2.3.1.1, noting only that any "adjusted" points should be relocated away from the stack walls to: (1) a distance of 1.3 cm (0.50 in.); or (2) a distance equal to the nozzle inside diameter, whichever is larger.

APPENDIX D

FORMALDEHYDE FIELD AND RECOVERY DATA

DRYER STACKS

EMISSION TESTING FIELD DATA

ANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
ana Pacific - Clayton	3/14/92	Dryer Stack #1	M0011	DS1-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
gm	29.58	-1.1	66	NA	42	0.84	4 ft glass	K20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.92	0.998	4C	4C	4C	N/A	15	0.001	5	Ø	1.76

EPA METHOD 3
Collection Method
Analysis Method

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	20	20	20	20	
%CO2	1	1	1	1	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	0752	984.495	2.6	3.9	132	244	253	64	68		3
2	2.5		987.07	2.6	3.9	136	245	250	58	71		3
3	5	801	989.55	2.3	4.0	139	247	250	54	73		3
4	7.5			2.2	3.9	141	248	251	54	74		3
5	10	0	995.01	2.2	3.9	139	247	250	53	76		3
6	12.5		997.45	2.1	3.7	143	248	250	54	75		3
7	15		000.03	2.1	3.7	144	249	249	54	77		3
8	17.5		3.37	2.2	3.9	143	248	251	54	78		3
9	20		5.17	2.2	3.9	143	247	250	56	77		3
10	22.5		7.77	2.2	3.9	142	249	253	56	77		5
11	25		10.45	2.4	4.2	140	247	247	56	79		5
12	27.5		13.24	2.3	4.0	140	248	247	56	78		5
	30	0825	15.896									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/18/92	Dryer Stack #1	M0011	DS1 - F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP. (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	833	15.896	2.9	5.1	136	243	251	62	81		5
2	32.5		18.76	2.9	5.1	139	247	249	61	79		6
3	35		21.64	3.2	5.6	139	249	252	58	80		5
4	37.5		24.75	3.2	5.6	139	248	251	54	81		5
5	40		28.00	3.1	5.5	139	247	250	54	81		5
6	42.5		31.13	2.8	4.9	139	248	251	54	82		5
7	45		34.24	2.1	3.7	140	245	246	56	82		3
8	47.5		36.83	2.1	3.7	142	246	248	57	83		5
9	50		39.52	2.2	3.9	142	248	249	56	83		5
10	52.5		42.50	2.3	4.0	139	249	247	56	83		4
11	55		44.96	2.3	4.0	139	249	251	56	84		4
12	57.5		47.70	2.3	4.0	138	248	249	57	84		4
	60	904	50.271									
			65.776	1.5613	4.3	139				79		
				33.212								

33.4

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		65.776	1.5613	4.3	139.7	79

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/19/92

Sample Location: Dryer Stack #1

Recovery Date: 3/19/92

Recovered By: RM

Run No.: DS1-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	596.0	591.6	483.2	750.0	grams
Initial Weight	597.6	571.8	480.4	727.6	grams
Net Weight	-1.6	19.8	2.8	22.4	grams

Description of impinger water _____ 0 % spent

Blue Sil Gel Color

Total Moisture 43.4 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING . IELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/19/92	Dryer Stack #1	M0011	DS1-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Am	29.58	-1.1	70	N/A	42	0.84	4 ft glass	K20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M5	1.92	0.998	4C	4C	4C	N/A	15	0.001			1.5
												Btrain

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Grab	%O2	21	21	21	21			
Analysis Method	Fyrite	%CO2	0	0	0	0		ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	0757	50.368	2.2	3.3	140	252	252	64	86		5
2	2.5		52.80	2.2	3.3	140	250	247	58	86		5
3	5		55.23	2.1	3.2	140	253	247	58	87		5
4	7.5		57.65	2.0	3.0	140	244	249	57	88		4
5	10		60.01	2.0	3.0	140	247	250	56	88		4
6	12.5		62.41	2.0	3.0	140	249	252	54	88		4
7	15		64.62	2.1	3.2	140	249	250	54	88		4
8	17.5		67.27	2.0	3.0	140	247	249	54	88		4
9	20		69.61	2.1	3.2	140	248	249	54	88		4
10	22.5		72.02	2.2	3.3	140	251	250	55	88		4
11	25		74.50	2.2	3.3	138	248	251	55	88		5
12	27.5		76.95	2.6	3.9	137	248	250	55	88		6
	30	1027	79.532									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/19/92	Dryer Stack #1	M0011	DS1-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1037	79.532	2.8	4.2	139	245	251	65	86		6
2	32.5		82.23	2.8	4.2	139	248	250	58	86		6
3	35.		85.00	3.2	4.8	141	249	250	57	87		7
4	37.5		87.85	3.0	4.5	140	248	250	55	87		7
5	40		90.79	2.8	4.2	140	248	241	54	88		6
6	42.5		93.54	2.5	3.8	139	249	245	54	88		5
7	45		96.29	2.0	3.0	140	248	253	54	87		5
8	47.5		98.71	2.0	3.0	141	247	253	54	88		5
9	50		101.05	2.1	3.2	141	247	246	55	88		5
10	52.5		103.45	2.1	3.2	140	250	254	55	89		5
11	55		105.75	2.1	3.2	137	249	249	56	88		7
12	57.5		108.35	2.1	3.2	139	248	249	54	88		5
	60	1107	110.789									
			60.421	1.524	3.5	140				88		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		60.421	1.524	3.5	140	88

37.06

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 19 MAR 92

Sample Location: DRYER STACK #1

Recovery Date: 19 MAR 92

Recovered By: RM

Run No.: DS1-F2

B train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	662.4	585.6	464.8	725.4	grams
Initial Weight	577.0	571.1	457.5	711.3	grams
Net Weight	85.9	14.5	06.3	14.1	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture 120.8 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

iea

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/4/92	Dryer Stack #1	M0011	DS1-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM	29.58	-1.1	80	N/A	42	0.84	4 ft glass	R20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
3	M5	1.92	0.988	4C	4C	4C	N/A	15	0.004			1.34 / C train

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Grab	%O2	21	21	21	21		ok	ok
Analysis Method	Fyrite	%CO2	0	0	0	0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1151	110.870	2.5	~~3.8~~ 3.4	141	240	249	67	87		3
2	2.5		113.20	2.5	3.4	145	249	251	60	88		3
3	5		115.94	2.3	3.1	143	249	254	55	88		3
4	7.5		118.38	2.2	2.9	142	248	248	56	88		3
5	10		120.90	2.0	2.7	139	248	253	56	88		3
6	12.5		123.12	2.0	2.7	138	247	250	56	88		3
7	15		125.35	2.1	2.8	142	248	251	56	88		3
8	17.5		127.70	2.0	2.7	138	248	249	55	90		3
9	20		129.93	2.2	2.9	138	250	252	56	90		3
10	22.5		132.35	2.3	3.1	138	249	246	56	90		3
11	25		134.70	2.3	3.1	138	249	247	57	90		3
12	27.5		137.09	2.3	3.1	138	250	252	57	90		3
	30		139.431									

120.8

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/19/92	Dryer Stack #1	M0011	DS1-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP. (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1228	139.431	2.9	3.9	136	251	250	65	90		4
2	32.5		142.11	2.9	3.9	136	244	250	58	91		4
3	35		144.66	3.0	4.0	135	250	250	56	93		4
4	37.5		146.82	3.1	4.2	137	247	248	56	89		4
5	40		149.40	3.0	4.0	137	247	243	55	88		4
6	42.5		152.28	2.7	3.6	138	247	244	56	88		4
7	45		154.80	2.0	2.7	138	249	252	56	88		4
8	47.5		156.98	2.0	2.7	138	249	251	56	88		3
9	50		159.29	2.1	2.8	135	250	249	56	88		3
10	52.5		161.57	2.2	2.9	134	248	255	55	88		3
11	55		163.90	2.2	2.9	134	249	251	56	88		4
12	57.5		165.97	2.2	2.9	133	245	244	57	88		4
	60	1258	168.120									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	57.250	1.5387	~~[illegible]~~	138	88.8

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 19 MAR 92

Sample Location: Dryer Stack #1

Recovery Date: 19 MAR 92

Recovered By: RM

Run No.: DS1 - F3

C train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	671.3	634.5	486.5	722.6	grams
Initial Weight	593.7	619.0	485.6	707.8	grams
Net Weight	77.6	35.5	0.9	14.8	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture 128.8 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/14/92	Dryer Stack #2	M0011	DS2-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
RM	29.58	-0.83	86	N/A	42	0.84	4ft Glass	K20	0.197 .196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M5	1.92	0.998	4c	4c	4c	NA	15	0.005	6	0.003	1.37

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2							
Analysis Method		%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1538	177.329	1.39	1.9	133	222	250	67	85		1
2	2.5		179.25	2.8	3.8	135	245	252	66	88		2
3	5		181.40	1.3	1.8	135	244	251	65	88		2
4	7.5		183.54	3.3	4.5	135	250	250	65	89		4
5	10		186.19	3.3 ~~4.6~~ 4.6	4.6	133	248	246	66	89		4
6	12.5		189.47	2.4	3.3	133	249	255	66	90		5
7	15		192.14	2.4	3.3	135	249	249	65	89		3
8	17.5		194.60	2.2	3.0	135	250	253	64	88		3
9	20		196.42	2.4	3.3	133	250	252	63	88		3
10	22.5		198.69	2.7	3.7	133	245	253	61	89		3
11	25		201.19	2.8	3.8	133	244	250	61	89		3
12	27.5		203.89	3.0	4.1	132	246	249	60	89		4
	30	1608	206.542									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-4-92	Dryer Stack #2	M0011	DSZ-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1614	206.542	2.4	3.3	131	252	252	59	87		3
2	32.5		208.98	2.3	3.2	131	248	247	58	87		3
3	35		211.45	2.4	3.3	131	244	245	58	87		4
4	37.5		213.92	2.1	2.9	132	249	252	58	87		3
5	40		216.28	2.5	3.4	133	248	253	59	87		4
6	42.5		218.73	2.5	3.4	134	249	250	58	86		3
7	45		220.26	2.7	3.7	134	248	252	58	87		4
8	47.5		223.15	2.7	3.7	136	244	246	59	87		4
9	50		225.48	2.6	3.6	135	249	250	57	86		4
10	52.5		228.17	2.6	3.6	134	249	251	55	86		4
11	55		230.73	2.7	3.7	134	250	250	56	86		4
12	57.5		233.35	2.4	3.3	134	249	251	55	86		4
	60	1644	236.252									
			~~58.92~~ LRM									
			58.923	1.572	3.425	133.5				87.5		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		58.923	1.572	3.425	133.5	87.5

Sheet Checked By: RM Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/14/92	Dryer Stack 2	M0011	DS2 - F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Rm	29.58	-0.83	86	N/A	42	0.84	4ft Glass	K20	0.197

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M5	1.92	0.998	4C	4C	4C	N/A	10	0.000	8	0.000	1.37

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2					
%CO2					

PITOT SYSTEM LEAK CHECK INIT.	PITOT SYSTEM LEAK CHECK FINAL

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	17:51	239.373	3.8	5.2	134	248	270	52	82		1
2	2.5		241.99	1.4	1.9	134	246	271	50	84		3
3	5		244.57	1.3	1.9	134	249	264	51	84		3
4	7.5		246.43	1.2	1.6	133	248	260	49	84		3
5	10		248.29	1.1	1.5	133	249	246	50	85		3
6	12.5		249.64	2.9	3.9	133	246	252	51	84		3
7	15		252.59	2.8	3.8	134	246	251	50	85		5
8	17.5		255.22	3.1	4.2	135	246	251	51	~~85~~ 85		5
9	20		257.97	3.2	4.4	134	243	249	50	86		5
10	22.5		260.79	3.3	4.5	134	242	250	51	86		6
11	25		263.63	3.1	4.2	134	244	250	52	87		6
12	27.5		266.41	3.3	4.5	134	249	250	50	87		6
	30	1821	269.210									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clarion	3-19-92	Dryer Stack 2	M0011	DS2-FZ

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1825	269.210	2.9	3.9	132	250	250	50	84		5
2	32.5		272.37	3.0	4.1	135	251	249	51	86		5
3	35		274.99	2.9	3.9	136	249	251	52	86		5
4	37.5		277.72	2.8	3.8	135	251	250	50	86		5
5	40		280.34	2.7	3.7	135	251	250	51	87		5
6	42.5		282.96	2.6	3.6	136	250	250	49	86		6
7	45		285.46	2.6	3.6	136	251	250	50	86		7
8	47.5		288.07	2.6	3.6	135	250	251	52	86		5
9	50		290.72	2.6	3.6	135	247	250	51	86		5
10	52.5		293.29	2.7	3.7	135	246	250	50	86		5
11	55		295.86	2.6	3.6	134	252	249	51	86		5
12	57.5		298.42	1.5	2.0	125	246	249	50	86		3
	60	1855	300.494									
			61.121	1.588	3.529	133.958				85.417		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		61.121	1.588	3.529	133.958	85.417

Sheet Checked By: [illegible] Date [illegible]

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/24/92	Dryer Stack #2	M0011	DS2-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jm	29.82	1.2	47	N/A	42	0.84	4ft Glass	~~0.20~~	~~0.197~~ 0.195

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
8	M5	1.92	0.998	4C	4C	4C	N/A	15	0.001			1.25/1.3

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Grab	%O2	~~20~~ 21	21				ok	ok
Analysis Method	Fyrite	%CO2	0	0					

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	744	300.693	3.7	4.6	128	245	248	45	53		4
2	2.5		303.84	3.7	4.6	127		248	42	55		4
3	5		306.62	3.3	4.1	127		247	43	57		4
4	7.5		309.35	3.0	3.8	127		247	43	57		4
5	10		311.92	2.9	3.6	127		250	43	57		3
6	12.5		314.48	2.5	3.1	127		253	43	58		3
7	15		316.53	3.1	3.9	127		250	43	58		3
8	17.5		319.40	3.2	4.0	127		250	43	59		4
9	20		321.87	3.3	4.1	127		249	43	59		4
10	22.5		324.57	3.2	4.0	126		251	43	60		4
11	25		327.22	3.2	4.0	126		249	43	59		4
12	27.5		329.85	3.2	4.0	126		250	43	60		4
	30	814										

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	~~3-19-92~~ 3-20-92	Dryer Stack 2	M0011	~~DS2-ft~~ DS2-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P. VELOCITY HEAD (in. H2O)	H. ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B 1	30	817	332.488	3.4	4.4	128		253	46	59		4
2	32.5		335.23	3.4	4.4	131		249	43	59		4
3	35		338.00	3.1	4.0	132		250	42	60		4
4	37.5		340.69	3.0	3.8	132		251	42	61		4
5	40		343.29	3.0	3.8	131		257	42	61		4
6	42.5		346.02	3.1	4.0	132		250	42	60		4
7	45		348.55	2.5	3.3	131		249	43	61		4
8	47.5		351.15	2.4	3.1	131		250	43	61		3
9	50		353.68	2.5	3.3	131		248	43	61		3
10	52.5		355.60	2.8	3.6	131		252	45	62		3
11	55		358.08	2.7	3.5	128		250	44	61		3
12	57.5		360.58	2.7	3.5	130		250	44	61		3
	60	0847	363.009									
			62.316	1.740	3.433	128.750				59.125		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		62.316	1.740	3.854	128.750	59.125

Sheet Checked By: [illegible] Date [illegible]

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: Louisiana Pacific - Clayton Sampling Date(s): 3/19 - 3/20/92

RUN No.: DS2-F1 Recovery Date: 3/19 Recovered By: [illegible]

Impingers: C train

	1	2	3	4	5	6	Silica Gel
Final Wt.	654.5	613.5	488.8	X	X	X	738.6
Initial Wt.	592.5	597.9	486.6	X	X	X	722.6
Net Weight	62.0	15.6	2.2	X	X	X	16.0

Total Moisture = 95.8 grams

Description of Impinger Contents:
Silica Gel Color: Blue Percent Spent: 25 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: DS2-F2 Recovery Date: Recovered By:

Impingers: A train

	1	2	3	4	5	6	Silica Gel
Final Wt.	674.3	605.1	483.7	X	X	X	761.9
Initial Wt.	600.2	588.8	480.5	X	X	X	750.0
Net Weight	74.1	16.3	3.2	X	X	X	11.9

Total Moisture = 105.5 grams

Description of Impinger Contents:
Silica Gel Color: Blue Percent Spent: 40 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: DS2-F3 Recovery Date: Recovered By:

Impingers: C train

	1	2	3	4	5	6	Silica Gel
Final Wt.	648.0	613.6	486.6	X	X	X	748.3
Initial Wt.	583.3	600.4	486.0	X	X	X	737.0
Net Weight	64.7	13.2	0.6	X	X	X	11.3

Total Moisture = 89.8 grams

Description of Impinger Contents:
Silica Gel Color: Blue Percent Spent: 25 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/21/92	Dryer Stack #3	M0011	D53-F1

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
RM	29.95	1.0	45	N/A	42	0.84	4ft Glass	L20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.92	0.998	4B	40	40	N/A	15	0.001	6	0.001	1.3 / 1.35

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2	21	21		21		OK	OK
Analysis Method	%CO2	0	0		0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
1	0	753	671.464	2.4	3.1	126	252	252	54	46		3
2	2.5		673.79	2.5	3.3	127	249	250	52	47		3
3	5		676.17	2.5	3.3	127	249	251	50	49		3
4	7.5		678.56	2.3	3.0	127	249	251	50	50		3
5	10		680.92	2.2	2.9	128	249	250	49	52		3
6	12.5		683.13	2.2	2.9	129	249	250	49	53		3
7	15		685.41	2.0	2.6	128	249	252	48	55		3
8	17.5		687.61	2.0	2.6	127	248	249	49	56		3
9	20		689.76	1.9	2.5	127	249	251	48	58		3
10	22.5		691.99	1.9	~~2.9~~ 2.5	128	251	248	49	59		3
11	25		694.05	1.8	2.3	127	251	250	48	62		3
12	27.5		696.22	1.7	2.2	125	251	251	49	62		2
	30	823	698.122									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3-21-92	Dryer Stack #3	M0011	DS3-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	8:26	698.122	2.9	3.9	126	250	247	49	62		4
2	32.5		700.71	2.9	3.9	128	250	248	49	65		4
3	35		703.35	2.9	3.9	129	250	248	48	67		4
4	37.5		705.96	2.2	3.0	130	250	253	49	68		4
5	40		708.37	2.5	3.4	129	249	250	49	69		3
6	42.5		710.77	~~3.1~~ 2.3 RM	3.1	129	249	250	49	69		3
7	45		713.16	2.3	3.1	129	250	250	50	70		3
8	47.5		715.52	2.2	3.0	129	249	249	48	71		3
9	50		717.84	2.2	3.0	128	249	251	49	72		3
10	52.5		720.21	2.1	2.8	125	247	247	48	72		3
11	55		722.47	1.9	2.5	116	247	247	48	73		3
12	57.5		724.67	1.8	2.4	105	247	246	48	73		3
	60	8:56	726.812									
			55.348	1.4903	3.0	127				62		
				$\sqrt{P}$ = 36.107								

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		55.348	1.4903	3.0	126.2	61.66

Sheet Checked By: [illegible] Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/2/92	Dryer Stack #3	M0011	D53-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
RM	29.95	1.0	45	NA	42	0.84	4ft Glass	K20	0.195

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.92	0.998	4A	4A	4A	N/A	16	0.004	6	0.004	1.35

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	21	21		21	
%CO2	0	0		0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
OK	OK

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	915	727.749	2.4	3.2	120	240	245	52 ~~230~~	70		5
2	2.5		730.11	2.4	3.2	124	249	240	50	72		5
3	5		732.58	2.4	3.2	123	248	249	50	73		5
4	7.5		735.03	2.3	3.0	124	250	250	49	74		5
5	10		737.42	2.2	2.9	124	248	251	49	73		5
6	12.5		739.73	2.1	2.8	124	250	250	48	74		4
7	15		742.07	2.2	2.9	124	248	251	49	74		4
8	17.5		744.41	2.3	3.0	124	251	250	48	74		4
9	20		746.72	2.3	3.0	124	250	251	48	73		4
10	22.5		749.08	2.3	3.0	124	250	251	48	74		4
11	25		751.39	2.1	2.8	124	248	250	50	74		4
12	27.5		753.72	2.1	2.8	120	248	250	49	75		4
	30	945	756.092									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3-21-92	Dryer Stack #3	M0011	DS3-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	9:50	756.092	2.6	3.5	~~123~~ 124	250	248	50	73 ~~124~~		5
2	32.5		758.46	2.7	3.6	124	247	251	47	75		5
3	35		760.98	2.6	3.5	124	248	250	48	75		5
4	37.5		763.54	2.4	3.2	124	248	251	51	76		5
5	40		766.02	2.5	3.4	124	249	251	50	77		5
6	42.5		768.57	2.3	~~3.0~~ 3.1	125	250	251	49	77		5
7	45		771.07	2.4	3.2	125	250	251	51	78		5
8	47.5		773.58	2.4	3.2	124	250	251	50	78		5
9	50		775.97	2.3	3.1	124	251	253	49	78		5
10	52.5		778.47	2.3	3.1	123	249	251	50	78		5
11	55		780.89	2.1	2.8	122	249	251	51	78		5
12	57.5		783.26	2.0	2.7	122	244	251	50	79		4
	60	1020	785.562									
			57.813	1.522	2.808	123.375				72.083		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		57.813	1.522	3.[illegible]	123.33	75.08

Sheet Checked By: P.H Date [illegible]/92

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: Louisiana Pacific - Clayton Sampling Date(s): 3/21/92

RUN No.: DS3-F1 Recovery Date: 3/21/92 Recovered By: JM

Impingers: ATRAW	1	2	3	4	5	6	Silica Gel
Final Wt.	640.1	598.6	487.0	X	X	X	766.6
Initial Wt.	595.1	586.6	485.7	X	X	X	758.5
Net Weight	45.0	12.0	1.3	X	X	X	16.1

Total Moisture = 74.4 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: _____ Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: DS3-F2 Recovery Date: 3/21/92 Recovered By: ~~3/21/92~~ JM

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	626.5	586.7	466.2	X	X	X	778.3
Initial Wt.	583.5	579.7	464.3	X	X	X	766.6 ~~744.2~~
Net Weight	43.0	7.0	1.9	X	X	X	11.7

Total Moisture = 63.6 grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: _____ Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: _____ Recovery Date: _____ Recovered By: _____

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.							
Initial Wt.							
Net Weight							

Total Moisture = _____ grams

Description of Impinger Contents: _____

Silica Gel Color: _____ Percent Spent: _____ %

Filter I.D. No.: _____ Filter Container I.D.: _____

Description of Particulate on Filter: _____ Sealed: Y N

Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N

Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ Impinger: _____ Filter: _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/11/92	Dryer Stack #4	M0011	DS4 - F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM	29.95	1.0	45	N/A	42	0.84	4ft Glass	C20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.92	0.998	4A	4A	4A	N/A	15	0.007	5	Ø	1.35/1.4

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	21	21	21	21	
%CO2	0	0	0	0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1104	785.710	2.8	3.8	123	249	251	60	78		3
2	2.5		788.25	2.7	3.6	127	247	251	54	81		3
3	5		790.90	2.5	3.4	124	248	252	53	80		3
4	7.5		793.35	2.4	3.4	123	249	250	53	80		3
5	10		795.53	2.3	3.2	125	249	251	50	82		3
6	12.5		798.25	2.3	3.2	126	249	250	49	82		3
7	15		800.72	2.5	3.4	126	250	249	49	84		3
8	17.5		803.17	2.3	3.2	125	251	251	49	84		3
9	20		805.62	2.3	3.2	125	250	250	50	85		3
10	22.5		808.18	2.3	3.2	124	251	250	50	85		3
11	25		810.50	2.4	3.4	123	249	251	50	86		3
12	27.5		812.96	2.4	3.4	123	248	250	51	86		3
	30											

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-21-92	Dryer Stack #4	M0011	DS4-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU. (in. Hg)
1	30	1137	815.460	2.6	3.6	124	245	249	52	87		3
2	32.5		818.04	2.7	3.8	125	250	250	51	87		3
3	35		820.62	2.8	3.9	131	249	250	51	90		3
4	37.5		823.33	2.9	4.0	129	249	249	51	90		3
5	40		825.99	2.9	4.0	127	249	251	51	89		3
6	42.5		828.75	2.8	3.9	126	252	251	52	90		3
7	45		831.46	2.3	3.2	126	249	249	52	89		3
8	47.5		834.01	2.1	2.9	125	249	250	53	89		3
9	50		836.31	2.0	2.8	124	249	251	53	89		3
10	52.5		838.63	2.0	2.8	121	249	250	54	88		3
11	55		840.93	1.9	2.7	122	248	250	54	87		3
12	57.5		~~83~~844.22	1.9	2.7	124	249	250	56	87		3
	60	1207	845.439									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		59.729	1.5528	3.36	124.9	85.6

Sheet Checked By: C.W. Date

iec

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/4/92	Dryer Stack # 4	M0011	~~DS4-F1~~ RM DS4-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
RM	29.95	1.0	45	N/A	42	0.84	4ft 6 Ass	K20	0.195

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	175	1.92	0.998	4A	4A	4A	N/A	5	0.005	6	0.002	1.4

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2	21	21		21	
%CO2	0	0		0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
OK	OK

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	12:25	845.549	2.9	4.0	120	231	220	53	85		4
2	2.5		848.32	2.8	3.9	121	242	238	52	85		4
3	5		850.99	2.7	3.8	122	245	250	50	86		4
4	7.5		853.68	2.6	3.6	122	249	251	49	87		4
5	10		856.29	2.6	3.6	122	249	252	51	87		4
6	12.5		858.99	2.6	3.6	121	247	252	52	88		4
7	15		861.47	2.6	3.6	122	249	252	51	88		3
8	17.5		864.08	2.6	3.6	121	250	250	50	88		3
9	20		866.71	2.5	3.5	121	251	251	50	88		3
10	22.5		869.26	2.7	3.8	121	249	251	51	88		3
11	25		871.94	2.5	3.5	120	247	248	50	87		3
12	27.5		874.53	2.7	3.8	121	250	250	51	87		3
	30	12:55	877.224									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-24-92	Dryer Stack #4	M0011	~~DS4 pm F1~~ DS4-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P. VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1259	877.224	2.8	3.9	117	247	251	50	85		4
2	32.5		879.93	2.9	4.0	121	245	251	51	86		4
3	35		882.69	3.1	4.3	121	250	250	49	86		4
4	37.5		885.47	3.0	4.2	121	246	251	50	87		4
5	40		888.33	3.0	4.2	121	251	251	51	87		4
6	42.5		pm ~~890~~. 891.18	2.7	3.8	122	248	251	50	87		4
7	45		893.89	2.4	3.4	123	250	250	50	88		4
8	47.5		896.57	2.2	3.0	123	249	250	50	87		3
9	50		898.97	2.1	2.9	123	251	251	50	87		3
10	52.5		901.36	2.1	2.9	123	246	251	51	87		3
11	55		903.79	2.0	2.8	122	248	248	50	86		3
12	57.5		906.17	2.1	2.9	123	248	249	50	86		3
	60	1329	908.567									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		63.018	1.607	3.608	121.4	86.8

Sheet Checked By: _____ Date _____

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: Louisiana Pacific - Clayton Sampling Date(s): 3/21/92

RUN No.: D54-F1 Recovery Date: 3/21/92 Recovered By: gm

C train

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	639.2	596.5	487.6				777.4
Initial Wt.	599.7	586.9	487.0				768.7
Net Weight	39.5	9.6	0.6				8.7

Total Moisture = 58.4 grams

Description of Impinger Contents:
Silica Gel Color: Blue Percent Spent: 20 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: D54-F2 Recovery Date: 3/21/92 Recovered By: RM

A train

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.	613.9	586.3	486.8				793.9
Initial Wt.	574.5	573.1	484.7				778.3
Net Weight	39.4	13.2	2.1				15.6

Total Moisture = 70.3 grams

Description of Impinger Contents:
Silica Gel Color: Blue Percent Spent: 30 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: Recovery Date: Recovered By:

Impingers:	1	2	3	4	5	6	Silica Gel
Final Wt.							
Initial Wt.							
Net Weight							

Total Moisture = grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/12/92	Dryer Stack #6	M0011	DSC -F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM	29.82	-0.+1.2	64	N/A	40	0.84	4 ft glass	L20	0.195

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	m5	1.92	0.998	4C	4C	4C	NA	15	0.01			1.35

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2					
%CO2					

PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1603	525.724	1.8	2.4	134	246	248	52	68		3
2	2.5		527.75	1.7	2.3	135	249	251	48	69		3
3	5		529.95	1.8	2.4	136	249	251	49	69		3
4	7.5		531.96	1.9	2.6	136	244	250	46	70		3
5	10		533.94	1.8	2.4	136	249	251	47	70		3
6	12.5		536.02	1.8	2.4	136	251	251	47	71		3
7	15		538.16	1.8	2.4	136	244	251	46	73		3
8	17.5		540.30	1.8	2.4	137	249	250	47	73		3
9	20		542.26	1.7	2.3	137	248	251	47	73		3
10	22.5		544.34	1.5	2.0	137	251	250	47	73		2
11	25		546.32	1.6	2.2	137	250	250	47	73		3
12	27.5		548.28	1.6	2.2	136	249	249	47	73		3
	30		550.290									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/20/92	Dryer Stack #6	M0011	DS6 -F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1638	550.290	1.8	2.4	136	249	250	50	71		3
2	32.5		552.38	1.8	2.4	137	248	250	48	74		3
3	35		554.52	1.9	2.6	137	249	249	48	74		3
4	37.5		556.64	2.0	2.7	136	250	250	48	74		3
5	40		558.85	1.9	2.6	137	250	250	49	74		3
6	42.5		561.08	2.6	3.5	137	247	249	50	76		3
7	45		563.52	1.9	2.6	137	248	250	48	76		3
8	47.5		565.78	1.8	2.4	138	249	250	48	75		3
9	50		567.90	1.8	2.4	142	246	251	48	77		3
10	52.5		570.01	1.8	2.4	139	248	250	47	76		3
11	55		572.12	0.35	0.47	138	250	250	48	76		1
12	57.5		573.44	1.2	1.6	137	250	249	48	76		3
	60	1708	575.551									
										73.083		
			49.827	1306	2.336	136.833						

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		49.827	1.306	2.336	136.833	73.083

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EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clinton	3/6/92	~~DS6~~ Rm DRYER STACK 6	MEOH	DS6-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
	29.82			N/A		0.84	4ft Glass	K20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL in. Hg	TRAIN LEAK CHECK (INITIAL CFM	TRAIN LEAK CHECK (FINAL in. Hg	TRAIN LEAK CHECK (FINAL CFM	K FACTOR
	115	1.92	0.988					15	0.012	5	0.003	1.35

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2							
Analysis Method	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1729	575.748	1.4	1.9	136	233	224	57	71		3
2	2.5		577.72	1.4	1.9	136	239	250	53	73		3
3	5		579.66	1.5	2.0	136	244	253	53	74		3
4	7.5		581.61	1.6	2.2	136	249	254	51	74		3
5	10		583.63	1.7	2.3	135	250	253	50	75		3
6	12.5		585.72	1.7	2.3	135	250	253	48	76		3
7	15		587.79	1.7	2.3	134	250	251	48	76		3
8	17.5		589.87	1.6	2.2	134	249	252	49	76		3
9	20		~~Rm 49~~ 591.91	1.6	2.2	134	248	251	50	76		3
10	22.5		593.96	1.5	2.0	133	249	249	48	76		3
11	25		595.94	1.3	1.8	133	250	250	49	76		3
12	27.5		597.82	1.3	1.8	131	246	250	49	76		3
	30	1759										

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-20-92	Dryer Stack #6	M0011	DS6-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1803	599.675	1.8	2.4	134	244	250	53	73		4
2	32.5		601.72	1.6	2.2	134	251	250	50	75		4
3	35		603.81	1.7	2.3	134	250	251	49	75		4
4	37.5		605.84	1.8	2.4	134	248	251	48	75		4
5	40		607.89	1.9	2.6	133	250	249	50	75		4
6	42.5		610.09	1.7	2.3	133	250	250	49	75		4
7	45		612.16	1.7	2.3	134	249	249	48	76		4
8	47.5		614.21	0.05 ~~0.5~~ RA	0.68	133	248	250	50	76		4
9	50		615.86	1.8	2.4	134	249	249	51	75		4
10	52.5		617.90	1.5	2.0	135	250	250	49	75		4
11	55		619.86	1.2	1.6	135	249	251	50	75		4
12	57.5		621.71	1.2	1.6	130	250	250	49	75		3
	60	1833	623.471									
			47.723	1.209	2.070	134.000				74.958		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		47.723	1.209	2.07	134.0	74.958

Sheet Checked By: [illegible] Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Chalmette	3-1-92	DRYER STACK #6	MCEM	DSG-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM	29.82	1.2	56	N/A	40	0.84	4ft Glass	1.20	0.195

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.72	0.998	4A	4A	4A	N/A	15	0.001			1.35

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Grab	%O2	21	21				ok	ok
Analysis Method	Fyrite	%CO2	0	0					

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1853	623.069	1.5	2.0	143	237	231	55	69		2
2	2.5		625.58	1.5	2.0	143	248	242	49	70		2
3	5		627.47	1.5	2.0	144	251	247	48	71		2
4	7.5		629.35	1.7	2.3	143	251	251	48	72		2
5	10		631.37	1.7	2.3	143	251	251	48	72		2
6	12.5		633.45	1.7	2.3	144	249	251	47	73		2
7	15		635.52	1.8	2.4	142	252	251	46	~~78~~ 74		2
8	17.5		637.53	1.9	2.3	142	250	252	46	74		2
9	20		639.61	1.6	2.2	143	243	252	46	74		2
10	22.5		641.68	1.6	2.2	142	242	251	46	75		2
11	25		643.65	1.5	2.0	139	250	250	46	75		2
12	27.5		645.55	1.5	2.0	137	245	251	46	75		2
	30	1923	647.448									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-20-92	DRYER STACK #6	METOX	DS6 - F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1925	647.448	1.8	2.4	139	250	250	48	71		2
2	32.5		649.55	1.8	2.4	140	249	251	46	75		2
3	35		651.62	1.9	2.6	140	248	252	45	74		2
4	37.5		653.75	1.9	2.6	141	247	250	45	75		2
5	40		655.91	1.9	2.6	141	249	250	45	75		2
6	42.5		658.10	1.8	2.4	140	244	250	45	76		2
7	45		660.26	1.5	2.4	141	242	250	45	75		2
8	47.5		662.38	1.8	2.4	141	245	250	45	75		2
9	50		664.50	0.43	0.58	140	250	250	45	75		2
10	52.5		665.77	~~0~~ 1.4	1.9	140	242	250	45	74		2
11	55		667.60	1.5	2.0	137	245	251	45	75		2
12	57.5		669.46	1.5	2.0	138	247	250	46	75		2
	60	1958	671.333									
			47.664	1.264	2.083	140.875				73.708		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		47.664	1.264	2.083	140.9583	73.708

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PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: Louisiana Pacific - Clayton Sampling Date(s): 3/20/92

RUN No.: D56-F1 Recovery Date: 3/20/92 Recovered By: AM

Impingers: A train

	1	2	3	4	5	6	Silica Gel
Final Wt.	682.7	625.1	486.1				757.4
Initial Wt.	609.8	612.4	485.0				746.6
Net Weight	72.9	12.7	1.1				10.8

Total Moisture = 97.5 grams

Description of Impinger Contents:
Silica Gel Color: Blue Percent Spent: 10 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: D56-F2 Recovery Date: 3/20/92 Recovered By: RM

Impingers: B train

	1	2	3	4	5	6	Silica Gel
Final Wt.	655.8	567.3	465.6				744.2
Initial Wt.	580.6	556.6	463.6				732.1
Net Weight	75.2	10.7	2.0				12.1

Total Moisture = 100.0 grams

Description of Impinger Contents:
Silica Gel Color: Percent Spent: 0 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

RUN No.: D56-F3 Recovery Date: 3/21/92 Recovered By:

Impingers: C train

	1	2	3	4	5	6	Silica Gel
Final Wt.	674.5	625.5	487.0				768.2
Initial Wt.	597.7	614.1	487.6				757.8
Net Weight	76.8	11.4	-0.6				10.4

Total Moisture = 98 grams

Description of Impinger Contents:
Silica Gel Color: Blue Percent Spent: 10 %
Filter I.D. No.: Filter Container I.D.:
Description of Particulate on Filter: Sealed: Y N
Probe Rinse Container I.D.: Liquid Level Marked/Sealed: Y N
Impinger Contents Container: Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: Impinger: Filter:

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/12/92	Dryer Stack #8	M0011	DS8-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
SM	29.82	1.0	47	N/A		0.8	4ft glass	K20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL. FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.92	0.998	4C	4C	4C	N/A	12	0.001			1.35

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Grab	%O2	21	21				ok	ok
Analysis Method	Fyrite	%CO2	0	0					

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	1046	363.229	2.1	2.7	133	247	253	63	60		3
2	2.5		365.45	2.2	3.0	135	250	248	47	61		3
3	5		367.68	2.2	3.0	139	250	247	48	60		3
4	7.5		370.00	2.2	3.0	138	248	247	50	62		3
5	10		372.35	2.3	3.1	140	250	248	50	62		3
6	12.5		374.88	2.3	3.1	140	251	252	49	63		3
7	15		377.09	1.9	2.6	141	249	250	50	64		3
8	17.5		379.20	1.7	2.3	141	245	250	51	65		3
9	20		381.22	1.6	2.2	139	249	249	53	66		3
10	22.5		383.39	1.3	1.8	137	249	252	53	66		2
11	25		385.17	2.2	3.0	137	246	251	54	67		3
12	27.5		387.39	2.2	3.0	137	249	253	55	70		3
	30	1116	389.720									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/24/92	Dryer stack #8	M0011	DS8-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1129	389.720	2.2	3.0	132	249	252	59	67		3
2	32.5		392.01	2.3	3.1	133	249	250	48	70		3
3	35		394.38	2.3	3.1	133	249	250	47	72		3
4	37.5		396.72	2.3	3.1	~~249~~ 137	249	250	47	71		3
5	40		399.10	2.3	3.1	134	250	250	46	72		3
6	42.5		401.49	2.3	3.1	134	249	240	46	72		3
7	45		403.82	1.5	2.1	135	250	248	47	72		2
8	47.5		405.85	2.0	2.7	135	246	250	47	72		3
9	50		408.05	2.0	2.7	135	250	253	47	72		3
10	52.5		410.40	1.7	2.3	135	243	251	48	74		3
11	55		412.45	1.8	2.5	135	248	251	49	74		3
12	57.5		414.65	1.8	2.5	135	248	251	49	74		3
	60	1159	416.798									
			53.569	1.359	2.754	136.250				67.833		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		53.569	1.4205	2.754	136.25	67.833

Sheet Checked By: [illegible] Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/2/92	Dryer Stack #8	M0011	DS8-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
	29.82	+1.0		N/A		0.84	4ft glass	L20	0.195

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.92	0.998	4B	4B	4B	N/A	15	0.016	7	0.004	1.37

EPA METHOD 3
Collection Method
Analysis Method

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2					
%CO2					

PITOT SYSTEM LEAK CHECK INIT	FINAL

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1225	417.196	2.1	2.9	137	58	249	60	75		4
2	2.5		419.45	2.1	2.9	137	88	252	49	75		4
3	5		421.71	2.2	3.0	136	92	252	48	75		4
4	7.5		424.08	2.3	3.2 3.6	138	93	252	50	76		4
5	10		426.50	3.1	4.2	137	92	254	49	76		6
6	12.5		429.12	2.3	3.2	139	92	253	50	76		5
7	15		431.59	2.3	3.2	139	92	250	49	77		5
8	17.5		434.09	2.3	3.2	139	92	248	50	76		5
9	20		436.49	2.1	2.9	140	92	252	48	78		4
10	22.5		438.86	2.0	2.7	140	91	249	48	78		4
11	25		441.20	1.4	1.9	135	91	250	49	78		3
12	27.5		443.22	1.2	1.6	136	90	252	48	78		3
	30	1255	445.023									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/20/92	Dryer Stack	M0011	DS8 - F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. *(F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1300	445.023	2.2	3.0	138	79	250	49	78		4
2	32.5		447.34	2.3	3.2	138	92	251	52	79		4
3	35		449.75	2.2	3.0	137	94	251	51	80		4
4	37.5		452.14	2.5	3.4	137	94	251	50	81		5
5	40		454.61	2.4	3.3	137	95	249	49	81		5
6	42.5		457.19	2.3	3.2	137	94	249	49	81		5
7	45		459.57	1.4	1.9	137	95	251	48	83		3
8	47.5		461.61	2.0	2.7	138	95	251	49	83		4
9	50		463.82	2.0	2.7	137	95	251	50	83		4
10	52.5		466.10	1.8	2.5	137	95	249	48	83		4
11	55		468.32	1.6	2.2	135	93	251	49	82		4
12	57.5		470.46	0.98	1.3	134	92	252	50	82		2
	60	1330	472.181									
			54.985	1.420	2.804	137.291				78.917		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		54.985	1.420	2.804	137.291	78.917

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/20/92	Dryer Stack	M0011	DS 8 - F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
RM	29.82	+1.0	59	N/A	40	0.84	4ft Glass	K 20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
6	M5	1.92	0.998	4A	4A	4A	N/A	15	0.006	7	0.002	1.37

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Grab	%O2							
Analysis Method	Fyrite	%CO2							

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	1347	472.380	1.8	2.5	133	242	228	55	77		2
2	2.5		474.57	2.0	2.7	134	250	245	53	77		2
3	5		476.81	2.1	2.9	134	249	244	50	77		3
4	7.5		478.99	2.1	2.9	135	251	247	49	77		3
5	10		481.42	2.1	2.9	133 ~~249~~ RM	249	249	49	77		3
6	12.5		483.80	2.2	3.0	136	250	253	51	77		3
7	15		486.15	2.2	3.0	137	248	254	48	77		3
8	17.5		488.48	2.2	3.0	136	250	250	49	77		2
9	20		490.84	2.1	2.9	136	249	253	48	78		2
10	22.5		493.17	1.9	2.6	136	249	249	51	79		2
11	25		495.42	1.3	1.8	129	250	252	52	79		2
12	27.5		497.34	1.4	1.9	125	247	251	53	78		2
	30	1417	499.208									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-20-92	Dryer Stack	M0011	DS8 - F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1422	499.208	1.9	2.6	133	250	253	57	76		2
2	32.5		501.28	1.8	2.5	136	248	249	55	78		2
3	35		503.61	2.1	2.9	136	248	251	50	78		2
4	37.5		505.86	2.2	3.0	138	248	249	48	78		3
5	40		508.26	2.2	3.0	137	249	251	49	79		3
6	42.5		510.67	2.2	3.0	137	250	250	47	78		3
7	45		513.07	1.4	1.9	138	250	251	47	78		2
8	47.5		515.06	1.9	2.6	139	246	251	48	78		2
9	50		517.25	1.8	2.5	138	248	250	49	79		2
10	52.5		519.48	1.7	2.3	137	250	252	48	78		2
11	55		521.59	1.4	1.9	134	246	251	50	78		2
12	57.5		523.57	1.4	1.9	127	251	249	48	78		2
	60	1452	525.496									
			53.116	1.247	2.591	134.833				77.75		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		53.116	1.3707	2.592	134.833	77.75

Sheet Checked By: [illegible] Date [illegible]

PARTICULATE/SAMPLE RECOVERY DATA SHEET

Client/Location: Louisiana Pacific - Clayton Sampling Date(s): _____

RUN No.: DS 8 - F1 Recovery Date: _____ Recovered By: _____

Impingers: A train

	1	2	3	4	5	6	Silica Gel
Final Wt.	682.1	595.2	486.4				746.2
Initial Wt.	599.3	576.3	485.5				729.1
Net Weight	82.8	18.9	0.9				17.1

Total Moisture = 119.7 grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: _____ Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: DS 8 - F2 Recovery Date: _____ Recovered By: _____

Impingers: B train

	1	2	3	4	5	6	Silica Gel
Final Wt.	657.1	604.2	464.7				758.0
Initial Wt.	~~600.2~~ 572.4	~~588.8~~ 591.1	~~480.5~~ 462.7				715.4
Net Weight	84.7	13.1	2.0				42.6

Total Moisture = ~~132.5~~ 142.4 grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: _____ Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

RUN No.: DS 8 - F3 Recovery Date: _____ Recovered By: _____

Impingers: C train

	1	2	3	4	5	6	Silica Gel
Final Wt.	692.2	626.1	488.1				779.8
Initial Wt.	607.6	609.3	486.8				743.0
Net Weight	84.6	16.8	1.3				36.8

Total Moisture = 139.5 grams

Description of Impinger Contents: _____
Silica Gel Color: _____ Percent Spent: _____ %
Filter I.D. No.: _____ Filter Container I.D.: _____
Description of Particulate on Filter: _____ Sealed: Y N
Probe Rinse Container I.D.: _____ Liquid Level Marked/Sealed: Y N
Impinger Contents Container: _____ Liquid Level Marked/Sealed: Y N

BLANKS: Probe rinse: _____ **Impinger:** _____ **Filter:** _____

PRESS VENTS

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/12/92	Press Vent #3	M 0011	PV3 - F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Gm RM	29.98	-0.35	54	N/A	62	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	N/A	15	0.009	5	0.010	3.5 A train

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2				21		ok	ok
Analysis Method	%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	13:29	218.234	0.77	2.5	90	248	241	46	65		2.5
2	2.5		220.28	0.74	2.6	89	252	245	45	65		2.5
3	5		222.35	0.73	2.5	89	251	246	48	66		2.0
4	7.5		224.39	0.95	3.3	88	251	250	49	66		3.0
5	10		226.69	0.57	2.0	89	251	249	50	67		2.0
6	12.5		~~228.56~~ 228.56	0.51	1.8	88	251	247	51	68		1.5
7	15		230.38	0.34	1.2	89	247	248	51	69		1.0
8	17.5		231.80	0.85	3.0	90	245	244	51	69		3.0
9	20		233.61	0.94	3.3	90	244	250	51	70		3.0
10	22.5		235.97	0.85	3.0	89	245	247	51	70		3.0
11	25		238.19	0.63	2.2	92	250	251	52	71		2.0
12	27.5		240.17	0.59	2.1	92	249	250	52	72		2.0
	30		242.024									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY		DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	Clayton	3/12/92	Press Vent #3	M0011	PV3-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	14:02	242.024	0.73	2.6	89	253	251	55	70		2.5
2	32.5		244.06	0.71	2.5	91	248	246	51	73		2.5
3	35		245.70	0.95	3.3	92	247	244	50	73		3.0
4	37.5		248.50	1.0	3.5	91	250	248	51	73		3.5
5	40		250.89	0.77	2.7	91	244	249	52	75		2.5
6	42.5		253.07	0.39	1.4	89	248	247	52	74		1.0
7	45		254.68	0.36	1.3	89	249	249	52	74		1.0
8	47.5		256.17	0.45	1.6	90	245	247	52	74		1.5
9	50		257.75	0.75	2.6	91	251	250	52	74		2.0
10	52.5		259.80	0.81	2.8	~~90~~ 90	249	247	51	74		3.0
11	55		261.95	0.77	2.7	91	245	248	52	74		2.5
12	57.5		264.09	0.80	2.8	91	247	246	52	74		3.0
	60	14:32	266.285									
			48.051	0.832	2.471	90.00				70.833		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		48.051	0.832	2.471	90.00	70.9

Sheet Checked By: [illegible] Date

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3-12-92

Sample Location: Press Vent #3

Recovery Date: 3-12-92

Recovered By: JM

Run No.: PV3-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	584.8	594.6	481.3	701.4	grams
Initial Weight	593.0	593.3	480.7	693.1	grams
Net Weight	-8.2	1.3	0.6	8.3	grams

Description of impinger water _____ 30 % spent

Blue Sil Gel Color

Total Moisture 2.0 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/11/92	Press Vent #3	M0011	PV3-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM RM	29.98	-0.35	54	N/A	62	0.84	6ft Glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	N/A	16	0.016	5	0.016	3.5 B train

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				21	
%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1502	267.107	0.65	2.3	87	252	213	49	67		2.5
2	2.5		269.04	0.79	2.8	87	245	232	50	67		3.5
3	5		271.18	0.74	2.6	87	250	239	52	67		3.0
4	7.5		273.35	0.85	3.0	88	247	247	51	68		4.0
5	10		275.49	0.35	1.2	87	252	249	52	68		1.0
6	12.5		277.04	0.20	0.7	86	246	248	52	68		1.0
7	15		278.26	0.72	2.5	85	245	245	51	67		3.0
8	17.5		280.17	0.47	1.6	86	250	250	51	68		1.0
9	20		281.89	0.79	2.8	87	252	249	52	68		3.0
10	22.5		283.97	0.82	2.9	88	247	249	52	68		4.0
11	25		286.18	0.83	2.9	89	253	248	53	68		4.0
12	27.5		288.42	0.82	2.9	87	247	249	54	68		4.0
	30		290.631									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: RN Date 5/14/92

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-12-92	Press Vent 3	M0011	PV3-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU. (in. Hg)
1	30	15:35	290.631	0.78	2.7	89	251	252	54	66		3.0
2	32.5		292.72	0.75	2.6	90	246	248	52	67		3.0
3	35		294.84	0.75	2.6	90	246	248	53	67		3.0
4	37.5		296.89	0.93	3.3	89	248	246	54	67		4.0
5	40		299.21	0.78	2.7	89	252	247	54	67		4.0
6	42.5		301.39	0.46	1.6	86	251	248	55	67		2.0
7	45		303.13	0.36	1.3	86	246	248	55	67		2.0
8	47.5		304.67	0.43	1.5	87	250	248	55	67		2.0
9	50		306.20	0.70	2.5	87	250	248	55	67		3.0
10	52.5		308.21	0.82	2.9	87	250	246	55	67		4.0
11	55		310.39	0.82	2.9	87	244	248	56	67		4.0
12	57.5		312.64	0.78	2.7	87	247	248	56	67		
	60	1605	314.792									
			47.685	0.816	2.396	87.417				67.292		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		47.685	0.8162	2.396	87.417	67.292

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: LOUISIANA PACIFIC

Sample Date: 3-12-92

Sample Location: PRESS VENT 3

Recovery Date: 3-12-92

Recovered By: KM

Run No.: PV3 - F2

B - TRAIN

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	557.0	580.7	462.4	695.3	grams
Initial Weight	546.0	563.9	461.6	684.2	grams
Net Weight	11.0	16.8	0.8	11.2	grams

Description of impinger water _____ 35 % spent

Blue Sil Gel Color

Total Moisture 39.8 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clatskanie	3/12/92	Press Vent 3	M0071	DV3-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM RM	29.98	-0.35	48	N/A	62	0.84	6ft Glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	15	0.008	5	0.001	3.5
												C train

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21			
Analysis Method		%CO2				0		ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1628	314.995	0.65	2.3	88	245	220	54	63		2
2	2.5		316.98	0.66	2.3	89	245	235	54	64		2
3	5		318.98	0.64	2.3	88	252	247	55	64		2
4	7.5		320.98	0.67	2.3	88	257	246	55	65		2
5	10		322.96	0.48	1.7	86	248	245	54	65		2
6	12.5		324.88	0.35	1.2	86	248	245	54	65		2
7	15		326.35	0.33	1.2	87	248	244	54	65		2
8	17.5		327.81	0.86	3.0	86	248	244	55	64		2
9	20		330.03	0.91	3.2	87	252	249	56	65		3
10	22.5		332.33	0.63	2.2	88	257	248	57	65		2
11	25		334.49	0.62	2.2	89	245	249	57	65		2
12	27.5		336.31	0.61	2.1	89	248	248	57	65		2
	30		338.188									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-12-92	Press Vent 3	M0011	PV3-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	M01	30	388.188	0.98	3.4	86	252	249	55	64		3
2		32.5	340.57	1.0	3.5	87	247	249	56	65		3
3		35	342.99	1.0	3.5	87	244	249	57	65		3
4		37.5	345.33	0.94	3.3	88	247	249	59	65		2
5		40	347.72	0.63	2.2	86	247	247	58	65		2
6		42.5	349.65	0.47	1.6	85	252	248	58	65		2
7		45	351.31	0.28	0.98	84	247	250	57	64		2
8		47.5	353.96	0.28	0.98	85	248	248	57	64		2
9		50	353.96	0.76	2.7	86	248	248	57	64		2
10		52.5	356.07	0.65	2.3	86	249	248	58	64		2
11		55	358.06	0.64	2.2	86	251	248	58	64		2
12		57.5	360.07	0.65	2.3	87	248	249	59	64		2
	1731	60	362.032									
			~~23.944~~ RM	1.593	2.331	86.833				64.5		
			47.037									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		47.037	0.7967	2.29	86.833	64.5

Sheet Checked By: [illegible] Date

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3-12-92

Sample Location: Press Vent 3

Recovery Date: 3-12-92

Recovered By: JM

Run No.: PV3 - F3

C - Train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	581.1	588.2	485.2	710.7	grams
Initial Weight	593.9	589.1	486.6	690.6	grams
Net Weight	-12.8	-0.9	-1.4	20.1	grams

Description of impinger water _____ 30 % spent

Blue Sil Gel Color

Total Moisture 5.0 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/11/92	Press Vent 4	M0011	PV4-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
RM, JM	29.97	-0.33	40	N/A	62	.84	6ft glass	225	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	15	.003	7.0	.004	3.45

EPA METHOD 3
Collection Method
Analysis Method

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				21	
%CO2				0	

PITOT SYSTEM LEAK CHECK INIT.	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	18:00	078.294	0.88	3.1	74	250	249	37	46		5.0
2	2.5		080.39	0.88	3.1	73	252	249	35	46		5.0
3	5		082.65	0.93	~~3.4~~ 3.2	74	249	247	38	46		5.0
4	7.5		084.89	0.41	1.4	74	250	247	38	45		2.0
5	10		086.54	0.27	0.9	75	251	247	37	45		1.5
6	12.5		087.95	0.31	1.0	76	251	249	37	45		1.0
7	15		089.14	0.62	2.1	77	249	247	37	45		3.0
8	17.5		090.91	0.99	3.4	77	248	249	37	45		5.5
9	20		093.14	0.77	2.7	79	247	247	38	46		5.0
10	22.5		095.59	0.75	2.6	78	248	249	37	46		4.0
11	25		097.34	~~0.77~~ 0.74	2.6	78	252	249	38	46		4.0
12	27.5		099.39	0.74	2.6	78	248	247	38	46		4.0
	30		101.457									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3-1-92	Press Vent 4	M0011	PV4-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	18:34	101.457	0.77	2.7	75	246	248	38	44		4.0
2	32.5		103.51	0.74	2.6	75	251	247	37	45		4.0
3	35		105.56	1.1	3.8	74	250	247	37	45		6.0
4	37.5		~~105.~~ 108.11	1.1	3.8	74	248	247	38	45		6.0
5	40		110.39	0.56	1.9	74	247	247	38	46		3.0
6	42.5		112.28	0.36	1.2	74	249	248	38	46		2.0
7	45		113.69	0.32	1.1	75	250	249	38	45		2.0
8	47.5		115.05	0.47	1.6	76	251	249	37	45		2.0
9	50		116.59	0.77	2.7	77	250	248	37	45		3.0
10	52.5		118.65	0.74	2.6	77	251	248	38	46		4.0
11	55		120.68	0.69	2.4	77	248	250	39	46		4.0
12	57.5		122.66	0.70	~~3.5~~ 2.4	77	249	248	40	48		4.0
	60	1904	124.648									
				0.8185	2.4	76				46		
				Tsqrt 13.94996								

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		46.354	0.8185	2.4	76	46

Sheet Checked By: E. Hoss Date 3-11-92

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/11/92

Sample Location: Press Vent #4

Recovery Date: 3/12/92

Recovered By: [illegible]

Run No.: PV4-F1

A-TRAIN

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	582.6	567.5	482.6	695.7	grams
Initial Weight	588.0	567.5	482.0	685.6	grams
Net Weight	-5.4	0	0.6	10.1	grams

Description of impinger water _____ 20 % spent

Blue Sil Gel Color

Total Moisture 5.3 grams ✓ CH

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/2/92	Press Vent #4	M0011	PV4-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM, RM	29.98	-0.33	142	N/A	62	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	MZ	2.00	1.01	GC	GC	GC	N/A	10	0.01	6	0.01	3.45/3.5 B train

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				21	
%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	0750	125.565	0.80	2.7	72	246	249	42	48		3
2	2.5		127.20	0.84	2.9	75	249	247	41	48		3
3	5		129.82	0.85	2.9	75	250	248	42	49		3
4	7.5		132.00	0.84	2.9	75	257	247	42	51		3
5	10		134.20	0.33	1.1	76	250	240	42	57		2
6	12.5		135.64	0.29	1.0	76	257	250	42	51		2
7	15		136.93	0.21	0.72	77	250	248	42	52		2
8	17.5		138.09	0.50	1.7	79	248	249	43	53		2
9	20		139.71	0.82	2.8	80	248	249	43	54		3
10	22.5		141.84	0.67	2.3	81	248	248	44	55		3
11	25		143.82	0.68	2.3	81	248	247	45	56		3
12	27.5		145.81	0.66	2.3	80	248	247	45	57		3
	30	0820	147.763									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/12/92	Press Vent #4	M0011	PV4 - F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	0823	147.763	0.84	2.9	78	248	247	47	56		4
2	32.5		149.94	0.87	3.0	77	247	247	44	58		4
3	35		152.17	0.83	2.9	79	248	250	45	59		4
4	37.5		154.40	1.0	3.5	78	248	247	46	60		4
5	40		156.76	0.57	2.0	78	248	247	47	60		3
6	42.5		158.64	0.36	1.3	78	245	247	47	60		2
7	45		160.15	0.20	0.70	80	257	249	46	60		2
8	47.5		161.32	0.32	1.1	81	246	249	46	60		2
9	50		162.63	0.76	2.7	81	249	247	46	60		3
10	52.5		164.70	0.66	2.3	83	245	249	46	61		3
11	55		166.68	0.52	1.8	82	249	250	47	62		3
12	57.5		168.65	0.46	1.6	83	245	247	48	63		3
	60	0853	170.625									
				0.7709	2.1	79				56		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		45.06	0.7709	2.1	79	56

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisinna Pacific

Sample Date: 3-12-92

Sample Location: PRESS VENT #4

Recovery Date: 3-12-92

Recovered By: Rm

Run No.: PV4 - F2

B - TRAIN

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	556.6	549.7	462.5	685.0	grams
Initial Weight	563.5	548.9	463.5	676.2	grams
Net Weight	-6.9	0.8	-1	8.8	grams

Description of impinger water _____ 25 % spent

_____ BLUE Sil Gel Color

Total Moisture 1.7 grams VAN

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific Clayton	3/12/92	Press Vent #4	M0011	PV4-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
GM, RM	29.98	-0.33	47	N/A	62	0.84	6ft glass	.125	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	MZ	2.00	1.01	6C	6C	N/A	N/A	15	0.002	5	~~0~~	3.55 / B train

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				21	
%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	0920	170.828	0.89	3.1	80	252	235	49	63		3
2	2.5		173.10	0.88	3.1	80	257	244	46	65		3
3	5		175.40	0.90	3.2	80	248	250	50	66		3
4	7.5		177.70	0.88	3.1	80	246	250	49	66		3
5	10		180.00	0.42	1.5	81	257	248	47	67		2
6	12.5		181.61	0.32	1.1	82	252	247	46	67		2
7	15		182.97	0.29	1.0	83	249	251	45	67		2
8	17.5		184.32	0.56	2.0	83	245	248	44	67		2
9	20		186.15	0.92	3.3	84	247	250	45	67		3
10	22.5		188.47	0.72	2.6	83	246	248	44	68		3
11	25		190.55	0.70	2.5	84	246	247	45	68		3
12	27.5		192.64	0.67	2.4	85	252	248	45	68		2
	30	0950	194.667									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/12/92	Press Vent #4	M001	PV4-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B 1	30	0954	194.667	0.80	2.8	82	243	249	52	68		3
2	32.5		196.98	0.81	2.9	82	251	249	44	70		3
3	35		199.03	0.84	3.0	83	245	249	45	72		3
4	37.5		201.31	1.1	3.9	83	248	248	45	72		3
5	40		203.81	0.72	2.6	81	250	249	46	73		2
6	42.5		205.95	0.40	1.4	82	248	248	46	72		2
7	45		207.53	0.22	0.78	84	247	247	46	72		2
8	47.5		208.74	0.36	1.3	86	248	249	46	72		2
9	50		210.18	0.77	2.7	86	248	251	45	72		2
10	52.5		212.28	0.75	2.7	87	245	248	45	72		3
11	55		214.44	0.54	1.9	88	252	248	46	72		2
12	57.5		216.26	0.54	1.9	88	247	249	46	72		2
	60	1024	218.053									
			47.225	0.8023	2.4	83				69		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		47.225	0.8023	2.4	83	69

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3-12-91

Sample Location: Press Vent #4

Recovery Date: 3-12-91

Recovered By: Rm

Run No.: PVF-F3

C-Train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	576.5	601.4	486.1	691.0	grams
Initial Weight	565.4	584.1	486.4	691.0	grams
Net Weight	11.1	17.3	-.3	0	grams

Description of impinger water _____ 30 % spent

Blue Sil Gel Color

Total Moisture 28.1 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/11/92	Press Vent # 5	M0011	PV5-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM, RM	29.97	-0.33	39	N/A	62	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M2	2.00	1.01	6C	6C	6e	NA	15	0.002	5	Ø	3.4 A train

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	Grab	%O2	21	21		21		ok	ok
Analysis Method	Fyrite	%CO2	0	0		0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	0957	931.025	0.65	2.21	71	247	247	39	42		2
2	2.5		940.59	0.65	2.2	71	252	248	36	42		2
3	5		942.50	0.67	2.3	71	252	248	36	42		2
4	7.5		944.70	0.79	2.7	71	249	247	36	42		3
5	10		946.81	0.45	1.5	71	249	247	37	43		2
6	12.5		948.37	0.26	0.88	72	248	249	38	43		2
7	15		949.57	0.21	0.71	73	252	248	38	43		2
8	17.5		950.68	0.49	1.7	74	249	248	38	43		2
9	20		952.30	0.80	2.7	76	244	249	37	44		3
10	22.5		954.32	0.77	2.6	74	246	248	38	45		3
11	25		956.41	0.65	2.2	77	248	249	39	46		3
12	27.5		958.28	0.65	2.2	79	252	248	39	47		3
	30		960.173									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/11/92	Press Vent #5	M0011	PV5 - F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B 1	30	1033	960.173	0.84	2.9	73	245	247	42	46		4
2	32.5		962.31	0.80	2.7	74	257	249	36	46		4
3	35		964.43	0.84	2.9	74	246	249	37	47		4
4	37.5		966.61	1.1	3.7	74	244	247	37	47		4
5	40		969.04	0.80	2.7	73	257	249	37	46		3
6	42.5		971.15	0.60	2.0	73	244	248	37	46		3
7	45		973.15	0.28	0.95	74	248	250	37	45		2
8	47.5		974.45	0.41	1.4	75	251	249	37	45		2
9	50		975.85	0.86	2.9	78	249	246	38	46		4
10	52.5		977.84	0.80	2.7	78	248	249	38	47		4
11	55		979.96	0.75	2.6	79	250	250	39	48		4
12	57.5		982.05	0.76	2.6	80	250	249	40	50		
	60	1103	984.130									
				0.7666	2.2	74				45		
				17.7								

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		45.105	0.8007	2.2	74	45

Sheet Checked By: [illegible] Date

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Location: Press Vent #5

Sample Date: 3/11/92

Recovery Date: 3/11/92

Recovered By: 3/11/92 gm

Run No.: PV5-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	585.8	570.0	482.1	688.4	grams
Initial Weight	589.4	569.7	481.4	676.8	grams
Net Weight	-3.6	0.3	0.7	11.6	grams

Description of impinger water _____ 0 % spent

_____ Blue Sil Gel Color

Total Moisture 9 grams ✓ gm

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific – Clayton	3/11/92	Press Vent # 5	M0011	PV5-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
gm RM	29.97	-0.33	50	N/A	62	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	15	0.005	5	0.008	3.0
												B train

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				21	
%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	1210	985.327	0.86	2.6	73	247	251	39	64		3.0
2	2.5		987.39	0.82	2.5	75	249	245	39	66		3.0
3	5		989.43	0.82	2.5	73	249	248	40	66		3.0
4	7.5		991.49	0.81	2.4	74	251	252	41	65		3.0
5	10		993.48	0.41	1.2	76	249	247	43	67		2.0
6	12.5		995.29	0.21	0.6	76	244	249	43	68		1.0
7	15		996.31	0.27	0.8	77	246	251	41	66		1.0
8	17.5		997.51	0.47	1.4	79	244	249	43	67		1.0
9	20		998.93	0.77	2.3	79	252	247	42	67		1.0
10	22.5		000.44	0.72	2.2	81	244	249	43	68		3.0
11	25		002.30	0.68	2.0	82	250	246	43	68		
12	27.5		004.15	0.65	2.0	81	247	247	44	70		
	30											

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: [illegible] Date [illegible]-92

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3-11-92	Press Vent #5	M0011	PV5-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	12:45	~~005.98~~ 005.978	0.99	2.7	76	250	247	41	69		3.0
2	32.5		008.05	1.1	3.3	76	244	248	37	65		4.0
3	35		010.35	0.99	2.7	77	251	248	39	65		3.0
4	37.5		012.55	1.1	3.3	80	251	243	43	69		4.0
5	40		015.16	0.76	2.3	79	246	247	43	70		3.0
6	42.5		016.98	0.46	1.4	78	244	248	43	71		2.0
7	45		018.59	0.27	0.8	79	244	250	43	71		1.0
8	47.5		019.85	0.40	1.2	77	248	251	40	68		1.0
9	50		021.24	0.80	2.4	79	247	250	40	68		3.0
10	52.5		023.19	0.68	2.0	80	248	246	41	69		2.0
11	55		025.06	0.66	2.0	81	251	247	42	70		2.0
12	57.5		027.01	0.65	2.0	80	246	250	41	69		2.0
	60	13:15	028.760									
			43.433	0.8094	2.0	78				68		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		41.9230	0.8094	2.0	78	68

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/11/92

Sample Location: Press Vent # 5

Recovery Date: 3/11/92

Recovered By: RM

Run No.: PV5- F2

B train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	566.1	569.7	461.6	676.7	grams
Initial Weight	570.0	569.1	461.6	668.2	grams
Net Weight	-3.9	0.6	0	8.5	grams

Description of impinger water _____ 0 % spent

Blue Sil Gel Color

Total Moisture 5.2 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/11/92	Press Vent # 5	M/0011	PV5-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
[illegible]	27.97	-0.33	53	N/A	62	0.84	6ft glass	.125	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
2	M2	2.00	1.01	6C	6C	6	N/A	15	0.004	5	0.001	3.5

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21		ok	ok
Analysis Method		%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1345	28.942	0.75	2.3	72	256	233	40	68		2.0
2	2.5		030.95	0.71	2.5	78	247	242	39	68		2.0
3	5		~~030.07~~ RM 032.01	0.75	2.6	79	252	~~25~~ RM 247	41	68		2.0
4	7.5		035.18	0.77	2.7	78	250	251	43	69		2.0
5	10		037.29	0.41	1.4	77	252	250	42	67		1.0
6	12.5		~~039.45~~ RM 042.45	0.26	1.0	76	245	250	42	65		1.0
7	15		040.60	0.27	1.0	81	250	250	44	68		1.0
8	17.5		041.97	0.49	1.7	81	250	246	44	69		1.0
9	20		043.58	0.83	3.0	78	247	249	42	69		2.0
10	22.5		045.78	0.80	3.0	78	250	249	43	68		3.0
11	25		048.03	0.80	3.0	81	251	247	44	69		2.5
12	27.5		050.28	0.80	3.0	81	251	248	44	71		2.5
	30.0	1415	052.544									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: [illegible] Date [illegible]

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pac. C.C	3/11/92	Press Vent 5	M0011	PV5-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM, RM	29.97	-0.33	52	NA	62	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	MZ	2.00	1.01	6C	6C	6C	NA	15	0.008	4	0.004	3.5

C-TRAIN

EPA METHOD 3
Collection Method
Analysis Method

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				21	
%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	30	14:19	052.544	1.1	4.0	80	244	247	44	70		3.0
2	32.5		055.05	1.1	4.0	78	246	252	42	70		3.0
3	35		057.68	1.1	3.9	80	246	249	43	70		3.0
4	37.5		060.22	1.1	3.9	79	248	246	43	68		3.0
5	40		062.81	0.72	2.5	79	250	247	44	71		2.0
6	42.5		064.98	0.47	1.6	79	246	248	44	71		2.0
7	45		066.79	0.26	0.9	79	250	249	43	70		2.0
8	47.5		068.03	0.41	1.4	80	247	250	42	69		2.0
9	50		069.57	0.84	2.9	83	248	248	43	70		2.0
10	52.5		071.68	0.76	2.7	82	244	247	42	70		2.0
11	55		073.81	0.75	2.6	81	251	251	41	67		1.0
12	57.5		075.93	0.75	2.6	83	251	247	43	69		1.0
	60	14:49	078.059									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		49.117	.8259	2.5	79	69

2.5

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/11/92

Sample Location: Press Vent #5

Recovery Date: 3/11/92

Recovered By: JM

Run No.: PV5 - F3

C train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	527.2	604.4	486.8	691.0	grams
Initial Weight	581.5	597.6	484.8	680.8	grams
Net Weight	-14.3	6.8	2	10.2	grams

Description of impinger water _____ 0 % spent

Blue Sil Gel Color

Total Moisture 4.7 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/14/92	Press Vent #6	M0011	PV6-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
cm	29.84	-0.42	70	N/A	56	0.84	6ft glass	L25	0.263

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.20	1.01	6C	6C	6C	NA	17	0.018	5	0.006	5.4/5.6 A train

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2				21		ok	ok
Analysis Method	%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC. (in. Hg)
A1	0	1156	362.292	0.86	4.6	80	250	249	61	~~67~~ 73		4
2	2.5		365.42	0.88	4.8	77	251	249	52	75		4
3	5		367.82	0.68	3.7	75	249	245	53	76		3
4	7.5		370.40	0.47	2.5	80	248	248	55	76		2
5	10		372.41	0.47	2.5	77	246	243	56	76		2
6	12.5		374.47	0.37	2.0	76	248	249	57	76		2
7	15		376.30	0.10	0.54	80	248	257	59	77		2
8	17.5		377.40	0.30	1.6	78	250	249	59	78		2
9	20		379.12	0.52	2.8	80	247	249	58	77		3
10	22.5		381.60	0.65	3.5	82	247	251	58	78		3
11	25		383.33	0.62	3.3	80	251	249	59	78		3
12	27.5		385.80	0.63	3.5	79	250	248	58	79		3
	30	1226	388.232									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
					444	49

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/14/92	Press Vent #6	M0011	PV6-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1238	388.232	0.88	4.9	78	250	245	62	77		4
2	32.5		390.99	0.90	5.0	82	248	247	57	80		4
3	35		394.12	0.81	4.5	81	248	250	52	79		4
4	37.5		397.00	0.63	3.5	78	250	250	54	82		3
5	40		398.98	0.30	1.7	81	247	241	53	82		2
6	42.5		401.15	0.11	0.62	80	248	250	54	80		2
7	45		402.32	0.55	3.1	79	245	250	54	80		2
8	47.5		404.45	0.65	3.6	83	250	242	53	81		3
9	50		406.90	0.26	1.5	81	245	252	54	81		2
10	52.5		408.65	0.225	1.4	81	248	250	55	81		2
11	55		410.20	0.23	1.3	86	257	257	55	80		2
12	57.5		411.75	0.23	1.3	82	248	249	55	80		2
	60	1308	413.294									
			~~413~~	0.6924	2.8	80				78		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	51.002	0.6924	2.8	80	78

Sheet Checked By: [illegible] Date 5/1/92

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/14/92

Sample Location: Press Vent #6

Recovery Date: 3/15/92

Recovered By: RM

Run No.: PS6-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	572.3	574.5	481.2	716.8	grams
Initial Weight	576.5	572.0	481.2	707.6	grams
Net Weight	-4.2	2.5	0	9.2	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture 7.5 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/11/92	Press Vent #6	M0011	PV6 - F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JMRM	29.84	-0.42	75	N/A	56	0.84	6ft glass	.225	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	N/A	15	0.12	6	0.002	3.63

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21		ok	ok
Analysis Method		%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A 1	0	1516	413.431	0.86	3.1	78	251	249	55	78		6
2	2.5		415.76	0.75	2.7	80	250	248	56	79		5
3	5		418.02	0.65	2.3	79	250	247	56	79		4
4	7.5		420.02	0.42	1.5	77	249	247	56	79		3
5	10		421.62	0.23	0.83	81	251	250	58	79		2
6	12.5		422.87	0.11	0.40	81	248	250	59	80		1
7	15		423.81	0.10	0.36	81	250	247	59	80		1
8	17.5		424.67	0.27	0.97	84	248	247	57	80		2
9	20		425.97	0.43	1.5	84	249	248	54	81		2
10	22.5		427.56	0.50	1.8	81	245	247	54	81		2
11	25		429.32	0.53	1.9	81	247	249	53	81		3
12	27.5		431.14	0.75	2.7	84	251	246	51	81		4
	30	1546	433.260									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/14/92	Press Vent #6	M0011	PV6 - F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	0	1549	433.260	0.73	2.6	81	248	248	58	80		4
2	2.5		435.35	0.72	2.6	86	247	253	52	81		5
3	5		437.48	0.69	2.5	80	244	257	53	81		5
4	7.5		439.57	0.72	2.6	77	247	247	53	81		5
5	10		441.70	0.49	1.8	82	249	246	54	82		3
6	12.5		443.45	0.11	0.40	79	245	257	56	81		1
7	15		444.41	0.43	1.5	78	249	248	56	81		2
8	17.5		445.96	0.73	2.6	82	244	252	53	80		4
9	20		448.00	0.32	1.2	79	252	243	54	80		2
10	22.5		449.21	~~0.24~~ 0.13	0.47	79	245	259	55	80		1
11	25		450.55	0.10	0.36	83	243	247	57	79		1
12	27.5		451.42	0.13	0.47	80	249	250	57	79		1
	30	1619	452.380									
			38.949	0.6403	1.6	81				80		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	38.949	0.6408	1.6	81	80

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/14/92

Sample Location: Press Vent #6

Recovery Date: 3/15/92

Recovered By: [illegible]

Run No.: PS6 -FZ

B train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	559.2	579.2	462.7	654.8	grams
Initial Weight	559.0	578.8	461.5	645.9	grams
Net Weight	0.2	0.4	1.2	8.9	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture 10.7 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/1/92	Press Vent #6	M0011	PV6-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JMRM	29.84	-0.42	75	NA	56	0.84	6 ft glass	.625	0.2360

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	15	0.001	5	Ø	3.6
												C train

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2				21		ok	ok
Analysis Method	%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	1650	452.568	0.64	2.3	76	250	249	60	75		2
2	2.5		454.57	0.63	2.3	80	250	244	47	76		2
3	5		456.56	0.45	1.6	77	247	248	49	77		1
4	7.5		458.22	0.27	0.97	74	246	250	52	77		1
5	10		459.61	0.31	1.1	77	251	250	52	77		1
6	12.5		461.01	0.10	0.36	77	251	249	53	76		1
7	15		461.95	0.09	0.32	75	245	247	55	76		1
8	17.5		462.77	0.25	0.90	79	244	249	55	76		1
9	20		464.05	0.68	2.4	77	246	248	51	77		2
10	22.5		465.94	0.62	2.2	77	248	248	52	78		2
11	25		467.92	0.60	2.2	81	249	250	53	77		2
12	27.5		469.86	0.53	1.9	77	247	249	53	77		2
	30		471.677									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-14-92	Press Vent # 6	M0011	PVG-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1721	471.677	0.71	2.6	78	244	243	57	76		2
2	32.5		473.81	0.73	2.6	76	249	251	53	77		2
3	35		475.93	0.65	2.3	75	248	247	53	77		2
4	37.5		478.06	0.66	2.4	79	249	247	53	77		2
5	40		480.19	0.45	1.6	76	244	248	54	77		2
6	42.5		481.86	0.11	0.40	76	240	248	55	77		1
7	45		482.80	0.40	1.4	75	250	250	55	76		1
8	47.5		484.14	0.80	2.9	76	244	246	52	76		2
9	50		486.28	0.52	1.9	76	247	248	52	76		2
10	52.5		488.12	0.24	0.86	80	252	245	54	75		1
11	55		489.43	0.20	0.72	78	250	246	54	75		1
12	57.5		490.57	0.27	0.97	75	251	251	54	74		1
	60	1751	491.884									

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		39.316	0.6438	1.63	77	76.3

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific **Sample Date:** 3/14/92

Sample Location: Press Vent #6 **Recovery Date:** 3/14/92

Recovered By: JMM

Run No.: PV 6 - F3

C train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	585.2	598.6	485.5	708.9	grams
Initial Weight	586.6	598.0	485.4	698.1	grams
Net Weight	-1.4	0.6	0.1	10.8	grams

Description of impinger water _____ _____ **% spent**

_____ _____ **Sil Gel Color**

Total Moisture 10.1 **grams**

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ **Date** _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/16/92	Press Vent #7	MC011	PV7-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
gm, RM	30.05	-0.42		N/A	56	0.84	6 ft glass	2.25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	N/A	15	0.009	5	0.006	3.5

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21			
Analysis Method		%CO2				0		ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	8:00	492.020	0.46	~~[illegible]~~ 1.6	63	243	244	41	44		1.0
2	2.5		493.65	0.48	1.7	61	235	247	37	47		1.0
3	5		495.30	0.43	1.5	58	236	252	37	48		1.0
4	7.5		496.84	0.43	1.5	58	237	247	39	49		1.0
5	10		498.39	0.53	1.9	57	235	250	40	50		1.5
6	12.5		500.14	0.14	0.50	62	241	246	40	50		1.0
7	15		501.26	0.11	0.40	59	249	244	40	50		1.0
8	17.5		501.69	0.27	0.95	57	244	245	40	51		1.0
9	20		502.83	0.30	1.1	57	250	245	40	52		1.0
10	22.5		504.18	0.30	1.1	58	251	250	39	53		1.0
11	25		505.54	0.24	0.84	62	247	244	38	53		1.0
12	17.5		506.77	0.26	0.91	58	251	251	38	53		1.0
	30	8:30	508.034									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/16/92	Press Vent # 7	M0011	PV7-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	8:35	508.034	0.44	1.5	57	246	277	41	52		1.0
2	32.5		509.63	0.47	1.6	60	246	248	39	55		1.0
3	35		511.27	0.47	1.6	62	245	246	39	56		1.0
4	37.5		512.89	0.53	1.9	58	244	250	38	56		1.5
5	40		514.68	0.44	1.5	57	242	252	39	56		1.0
6	42.5		516.39	0.13	0.46	59	243	247	40	57		1.0
7	45		517.30	0.37	1.3	60	244	248	40	57		1.0
8	47.5		518.69	0.79	2.8	62	240	244	39	57		2.0
9	50		520.68	0.51	1.8	62	240	252	39	58		1.0
10	52.5		522.53	0.51	1.8	61	236	247	39	57		1.0
11	55		524.22	0.44	1.5	62	240	250	40	58		1.0
12	57.5		525.82	0.56	2.0	63	240	250	40	58		1.0
	60		527.625									
			35.605	0.619	1.407	59.708	~~242.919~~			53.208		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		35.605	0.619	1.407	59.708	53.208

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/16/91

Sample Location: Press Vent #7

Recovery Date: 3/16/91

Recovered By: _____

Run No.: PV7-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
~~Final~~ Net Weight	[illegible]	[illegible]	[illegible]	[illegible]	grams
Initial Weight	584.4	576.2	481.3	683.3	grams
Final ~~Net Weight~~	581.1	576.4	480.4	691.5	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture [illegible] grams [illegible]

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/16/92	Press Vent #7	M0011	PU7-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jim Rm	30.05	-0.42	45	N/A	56	0.84	6 ft Glass	<25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	17	0.018	5	Ø	3.5/3.6

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21			
Analysis Method		%CO2				0		ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0135	0	527.812	0.45	1.6	65	48	241	246	58		2.0
2		2.5	529.31	0.46	1.7	71	246	251	45	~~45~~ 62		2
3		5.0	531.88	0.41	1.5	68	238	250	45	62		2
4		7.5	533.62	0.27	0.97	65	244	249	44	62		1
5		10	534.92	0.24	0.86	65	238	251	43	63		1
6		12.5	536.16	0.16	0.58	64	247	247	44	64		1
7		15	537.16	0.08	0.29	67	238	245	44	63		1
8		17.5	537.96	0.13	0.47	64	237	249	44	62		1
9		20	538.33	0.24	0.86	62	238	249	43	62		1
10		22.5	539.94	0.33	1.2	62	236	248	42	62		1
11		25	541.35	0.32	1.2	64	240	249	43	63		1
12		27.5	542.78	0.29	1.0	68	246	249	43	62		1
		30	543.781									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-16-92	PresVent #7	M0011	PV7-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	~~30~~ 5m	543.781	0.60	1.8	65	247	250	45	62		2
2	32.5		545.52	0.51	1.8	65	248	243	43	64		2
3	35		547.21	0.46	1.7	66	243	248	43	64		2
4	37.5		548.80	0.69	2.5	70	244	250	43	64		3
5	40		550.80	0.60	2.2	68	246	247	44	65		3
6	42.5		552.71	0.15	0.54	66	247	247	45	65		1
7	45		553.68	0.34	1.2	65	246	249	46	65		2
8	47.5		555.05	0.69	2.5	66	252	246	46	67		4
9	50		557.05	0.73	2.6	72	247	249	46	67		4
10	52.5		559.15	0.46	1.7	69	246	249	46	66		2
11	55		560.79	0.53	1.9	70	247	249	46	67		3
12	57.5		562.55	0.54	1.9	70	249	248	47	69		3
	60		564.334									
			36.522	0.6130	1.4	67				64		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		36.522	0.6130	1.4	67	64

Sheet Checked By: C H Date

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/16/91

Sample Location: PressVent #7

Recovery Date: 3/16/91

Recovered By: _____

Run No.: PV7-F2

B train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	[illegible]	[illegible]	[illegible]	[illegible]	grams
Initial Weight	562.4	572.4	462.6	654.8	grams
Net Weight	558.5	571.5	462.8	659.7	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture [illegible] grams ✓ PIN

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/16/92	Press Vent #7	M0011	PV7-F3

OPERATORS	BAROM PRESS (In. Hg)	STATIC PRESS (In. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (In.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JMRM	30.05	-0.42	63	N/A	56	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	15	0.001	4	Ø	3.6
												C train

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT
Collection Method	%O2				21	
Analysis Method	%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
OK	OK

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (In. Hg)
A1	0	1101	564.455	0.50	1.8	70	240	240	56	68		2
2	2.5		566.19	0.52	1.9	70	248	248	43	68		2
3	5		567.95	0.46	1.7	77	248	248	44	69		2
4	7.5		569.65	0.30	1.1	74	248	248	46	70		1
5	10		571.03	0.14	0.50	68	237	240	45	70		1
6	12.5		572.03	0.09	0.32	68	238	249	45	70		1
7	15		572.81	0.28	1.0	68	247	251	45	70		1
8	17.5		574.08	0.31	1.1	72	245	248	44	71		1
9	20		575.51	0.32	1.2	76	252	250	44	72		1
10	22.5		576.04	0.28	1.0	71	249	246	44	72		1
11	25		578.28	0.30	1.1	70	249	248	44	73		1
12	27.5		579.66	0.28	1.0	71	248	~~550~~ 250	45	75		1
	30		580.963									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/16/92	Press Vent #7	M0011	PV7-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	11:32	580.963	0.45	1.6	77	250	247	47	74		1
2	32.5		582.69	0.47	1.7	77	250	250	45	76		1
3	35		584.22	0.47	1.7	74	251	249	45	77		1
4	37.5		585.92	0.42	1.5	72	250	249	46	78		1
5	40		587.50	0.60	2.2	71	244	251	46	79		2
6	42.5		589.39	0.14	0.50	70	251	248	45	77		1
7	45		590.35	0.34	1.2	77	250	249	46	76		1
8	47.5		591.78	0.66	2.4	74	252	249	46	76		2
9	50		593.77	0.68	2.4	72	249	248	46	77		2
10	52.5		595.79	0.43	1.5	72	250	249	46	77		1
11	55		597.40	0.36	1.3	74	246	249	48	77		1
12	57.5		598.87	0.43	1.5	76	249	248	48	78		1
	60		600.453									
			35.998	.6065	1.4	73				74		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	35.998	.6065	1.4	73	74

Sheet Checked By: RN

Date 3/16/92

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/16/91

Sample Location: Press Vent #7

Recovery Date: 3/16/91

Recovered By: _____

Run No.: PV7-F3

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	585.9	577.4	485.6	715.5	grams
Initial Weight	588.0	577.4	486.0	708.8	grams
Net Weight	[illegible]	0	[illegible]	[illegible]	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture [illegible] grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

iea

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/11/92	Press Vent #8	M0011	PV8-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
gm	30.05	-0.35	65	N/A	56	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	15	0.004	5	Ø	3.45 A train

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2				21		ok	ok
Analysis Method	%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	√P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1453	600.608	0.83	3.0	80	248	246	56	78		3
2	2.5		602.85	0.83	3.0	80	244	247	47	79		3
3	5		605.15	0.67	2.4	76	250	249	50	79		2
4	7.5		607.04	0.61	2.2	74	245	247	51	79		2
5	10		608.95	0.30	1.1	74	246	246	51	80		1
6	12.5		610.40	0.14	0.51	75	249	248	52	80		1
7	15		611.38	0.10	0.37	81	247	247	53	80		1
8	17.5		612.18	0.37	1.4	78	247	250	53	80		1
9	20		613.67	0.47	1.7	76	245	249	51	81		1
10	22.5		615.35	0.49	1.8	78	250	245	50	81		1
11	25		617.10	0.43	1.6	78	245	244	50	81		1
12	27.5		618.75	0.40	1.5	81	245	248	51	82		1
	30	1523	620.332									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60					

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/16/92	Press Vent # 8	M0011	PV8 - F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP. (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1526	620.332	0.54	2.0	75	251	246	55	81		2
2	32.5		622.17	0.56	2.0	74	248	250	51	83		2
3	35		624.00	0.56	2.0	74	244	246	51	84		2
4	37.5		625.83	0.88	3.2	77	247	249	52	85		3
5	40		628.00	0.83	3.0	73	250	248	53	86		3
6	42.5		630.34	0.34	1.2	73	250	246	54	86		1
7	45		631.83	0.27	0.99	72	245	248	55	86		1
8	47.5		633.18	0.82	3.0	74	250	248	55	87		3
9	50		635.41	0.74	2.7	75	244	250	52	86		2
10	52.5		637.61	0.32	1.2	74	250	245	53	86		1
11	55		639.08	0.31	1.1	75	248	248	54	85		1
12	57.5		640.47	0.27	0.99	75	251	252	54	84		1
	60	1556	641.798									
			41.190	0.6889	1.8	76				82		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	41.190	0.6889	1.8	76	82

Sheet Checked By: [illegible] Date [illegible]

15,949

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/16/92

Sample Location: Press, Vent #3

Recovery Date: 3/17/92

Recovered By: JM

Run No.: PV8-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	585.3	562.1	480.3	698.4	grams
Initial Weight	592.9	561.4	480.6	693.0	grams
Net Weight	~~0~~ -7.6	0.7	-0.3	5.4	grams

Description of impinger water N/A

0 % spent

Blue Sil Gel Color

Total Moisture -1.8 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/1/92	PRESS VENT #8	M0011	PV8-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jm Rm	30.05	-0.35	65	NA	56	0.84	6ft Glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	~~2.00~~ 1.0	6c	6C	6C	N/A	15	0.009	5	0.006	3.65

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21			
Analysis Method		%CO2				0		ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1642	641.937	0.86	3.1	71	250	246	55	80		4.0
2	2.5		644.22	0.69	2.5	78	251	248	55	81		4
3	5		646.52	0.61	2.2	~~53~~ 72	253	246	53	82		3
4	7.5		648.57	0.36	1.3	70	253	248	53	81		2
5	10		650.17	0.28	1.0	68	248	249	52	81		2
6	12.5		651.69	0.15	0.54	69	251	248	51	81		1
7	15		652.65	0.12	0.43	75	248	249	51	81		1
8	17.5		653.55	0.31	1.1	71	246	249	51	81		2
9	20		654.94	0.26	0.95	71	252	248	50	81		2
10	22.5		656.25	0.48	1.8	71	253	248	50	81		2
11	25		657.92	0.54	2.0	72	251	248	49	82		2
12	27.5		659.69	0.56	2.0	73	244	247	49	81		2
	30	1712	661.537									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clinton	3-16-97	Press Vent #8	M0011	DU8-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P. VELOCITY HEAD (In. H2O)	H ORIFICE (In. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (In. Hg)
1	30	17:14	661.537	0.46	1.7	69	252	249	52	79		2
2	32.5		663.25	0.48	1.8	69	245	248	49	80		2
3	35		665.11	0.47	1.7	73	244	248	49	80		2
4	37.5		666.72	*0.70	2.6	70	251	248	49	79		3
5	40		668.81	0.75	2.7	67	251	247	50	78		4
6	42.5		670.99	0.48	1.8	66	249	249	50	78		3
7	45		672.81	0.27	0.98	67	244	249	50	77		1
8	47.5		674.18	0.88	3.2	73	249	249	50	76		4
9	50		676.39	0.58	2.1	71	252	248	50	76		3
10	52.5		678.37	0.44	1.6	68	251	248	50	76		2
11	55 ~~55~~		679.75	0.41	1.5	71	252	248	50	75		2
12	57.5		681.68	0.41	1.5	71	247	249	49	74		2
	60	1745	683.298									
			41.361	0.71	1.754	70.667				79.167		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	41.361	0.6775	1.754	70.667	79.167

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific - Clayton

Sample Date: 3/16/92

Sample Location: Press Vent # 8

Recovery Date: 3/17/92

Recovered By: AM

Run No.: PV8-F2

B-TRAIN

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	559.4	568.5	462.5	667.5	grams
Initial Weight	565.8	568.3	462.0	660.3	grams
Net Weight	-6.4	0.2	0.5	7.2	grams

Description of impinger water N/A

0 % spent

Blue Sil Gel Color

Total Moisture 1.5 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING . IELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/16/92	Press Vent #9	M0011	PVG-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jim Am	30.05	-0.35	65	N/A	56	0.84	6 ft Glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.61	6c	6c	6c	N/A	16	0.009	9	0.012	3.65
												C train

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT
Collection Method		%O2				21	
Analysis Method		%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	18 13	683.478	0.59	2.2	64	226	226	~~226~~ 50	64		1
2	2.5		686.22	0.63	2.3	67	246	249	46	64		2
3	5		~~687.~~ 688.18	0.44	1.6	67	244	250	47	65		1
4	7.5		689.82	0.26	0.95	64	244	250	46	65		1
5	10		691.17	0.13	0.47	62	244	248	45	65		1
6	12.5		692.13	0.11	0.40	61	246	249	45	64		2
7	15		692.98	0.13	0.47	67	248	248	46	64		1
8	17.5		693.89	0.13	0.47	64	251	248	45	64		1
9	20		694.80	0.24	0.88	63	245	248	45	64		1
10	22.5		695.99	0.24	0.88	64	250	248	44	65		1
11	25		697.27	0.25	0.91	64	246	248	43	63		1
12	27.5		698.52	0.26	0.95	67	253	248	43	63		1
	30		699.288			~~63~~			~~43~~	~~63~~		~~1~~

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clatskanie	3-16-92	Press Vent #8	M0011	PV8-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1846	699.288	0.39	Run 1-4 ~~0.56~~	62	246	249	46	62		1
2	32.5		700.24	0.45	1.6	62	252	248	43	62		1
3	35		701.79	0.57	2.1	64	251	247	42	62		1
4	37.5		703.73	0.72	2.6	63	252	248	42	63		1
5	40		705.83	0.78	2.8	60	252	248	42	63		2
6	42.5		708.09	0.35	1.3	59	247	247	43	63		2
7	45		709.74	0.39	1.4	59	245	249	43	63		1
8	47.5		711.32	0.79	2.9	63	253	249	43	63		1
9	50		713.49	0.59	2.2	60	245	249	43	63		1
10	52.5		715.49	0.49	1.8	60	246	248	44	63		1
11	55		717.29	0.38	1.4	61	245	248	44	62		1
12	57.5		718.91	0.44	1.6	63	247	247	44	62		1
	60	1916	720.590									
			37.112	0.6155	1.5	63				63		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		37.1120	0.6155	1.5	63	63

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/16/92

Sample Location: Press Vent #8

Recovery Date: 3/17/92

Recovered By: JM

Run No.: PV8-F3

C train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	573.9	598.8	486.2	720.2	grams
Initial Weight	578.8	597.0	486.4	714.7	grams
Net Weight	-4.9	1.8	-0.2	5.5	grams

Description of impinger water N/A

0 % spent

Blue Sil Gel Color

Total Moisture 2.2 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/11/92	Press Vent #9	M0011	P/9-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jim Rm	30.02	-0.21	67	N/A	~~52~~ 56	0.84	6ft Glass	1.25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	C6	C6	C6	N/A	15	0.002	5	Ø	3.63 / A train

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21			
Analysis Method		%CO2				0		etc.	etc.

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	0855	720.852	0.36	~~0.36~~ 1.3	~~63~~ 62	251	249	55	61		1
2	2.5		722.40	0.36	1.3	63	250	248	52	62		1
3	5		723.84	0.38	1.4	62	251	249	52	63		1
4	7.5		725.35	0.50	1.8	61	250	248	51	64		1
5	10		727.05	0.32	1.2	64	250	250	50	65		1
6	12.5		728.56	0.23	0.83	62	247	249	49	65		1
7	15		729.82	0.32	1.2	65	251	249	49	65		1
8	17.5		731.22	0.38	1.4	68	251	248	49	66		1
9	20		732.71	0.43	1.5	65	249	250	49	66		1
10	22.5		734.28	0.15	0.54	65	251	248	48	66		1
11	25		735.31	0.11	0.40	70	246	247	50	66		1
12	27.5		736.18	0.17	0.61	67	248	250	50	66		
	30		737.214									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-17-91	Press Vent # 9	M0011	PV9-F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	0927	737.214	0.56	2.0	67	245	246	54	66		2
2	32.5		738.99	0.52	1.9	64	248	247	48	67		2
3	35		740.80	0.45	1.6	66	248	248	48	68		1
4	37.5		742.44	0.73	2.6	68	249	250	49	69		2
5	40		744.43	~~1.1~~ 0.3	1.1	66	244	245	50	70		1
6	42.5		745.82	0.05	0.18	69	240	250	53	70		1
7	45		746.44	0.21	0.76	71	247	252	54	70		1
8	47.5		747.59	0.52	1.9	68	248	246	52	71		1
9	50		749.31	0.70	2.5	69	255	248	51	70		1
10	52.5		751.33	0.25	0.90	72	245	251	51	71		1
11	55		752.65	0.24	0.86	71	249	249	53	71		1
12	57.5		753.91	0.21	0.76	74	250	246	54	72		1
	60	~~1000~~ 0957	755.061									
			34.209	0.5737 ✓	3	67				67		
				$\sqrt{P_{bs}}$ = 13	M01							

32.2 fps

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	34.209	0.5737	1.3	67	67

Sheet Checked By: _____ Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/17/92

Sample Location: Press Vent #9

Recovery Date: 3/17/92

Recovered By: JM

Run No.: PV9 - F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	580.3	570.9	480.4	704.0	grams
Initial Weight	582.0	570.5	480.4	698.8	grams
Net Weight	-1.7	0.4	Ø	5.2	grams

Description of impinger water _____ 10 % spent

Blue Sil Gel Color

Total Moisture 3.9 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/11/92	Press Vent #9	M0011	PV9-F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jm Rm	30.02	-0.21	75	N/A	56	0.84	6 ft Glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	m2	2.00	1.01	6c	6c	6c	N/A	15	0.01	5	0.008	3.63 3.68 B train

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT
Collection Method	%O2				21	
Analysis Method	%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1027	755.275	0.36	1.3	72	247	252	64	76		2
2	2.5		756.73	0.36	1.3	69	249	250	54	78		2
3	5		758.21	0.36	1.3	68	246	250	51	78		2
4	7.5		759.68	0.57	2.1	72	251	249	53	79		3
5	10		761.47	0.34	1.2	72	252	249	54	80		2
6	12.5		762.98	0.24	0.86	71	250	250	55	81		2
7	15		764.25	0.21	0.76	73	248	249	55	82		1
8	17.5		765.44	0.40	1.4	77	244	248	53	82		2
9	20		766.97	0.39	1.4	76	246	248	57	83		2
10	22.5		768.55	0.23	0.825	78	249	248	51	83		1
11	25		769.80	0.11	0.41	81	248	249	52	84		1
12	27.5		770.77	0.10	0.37	79	247	248	53	84		1
	30		771.624									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	2-17-92	Press Vent #9	M0011	PV9-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1101	771.624	0.49	1.8	75	246	249	59	84		3
2	32.5		773.62	0.51	1.9	75	245	247	52	85		3
3	35		775.17	0.51	1.9	76	247	250	52	86		3
4	37.5		776.98	0.69	2.6	76	250	251	53	86		3
5	40		779.05	0.41	1.5	73	248	250	54	86		2
6	42.5		780.70	0.05	0.19	76	249	250	56	86		1
7	45		781.40	0.21	0.78	77	248	249	57	87		1
8	47.5		782.58	0.77	2.8	77	248	247	57	87		3
9	50		784.72	0.62	2.3	78	248	248	53	89		3
10	52.5		786.67	0.17	0.63	79	249	250	55	89		1
11	55		787.82	0.20	0.74	79	247	248	56	89		1
12	57.5		788.99	0.22	0.81	81	250	250	56	89		1
	60	1131	790.201									
			34.926	0.5727	1.3	75				84		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	34.9260	0.5727	1.3	75	84

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/17/92

Sample Location: Press Vent #9

Recovery Date: 3/17/92

Recovered By: RM

Run No.: PV9 - F2

B train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	566.7	578.3	462.0	703.8	grams
Initial Weight	567.7	579.5	462.1	695.0	grams
Net Weight	-1	-1.2	-.1	8.8	grams

Description of impinger water _____ 10 % spent

Blue Sil Gel Color

Total Moisture 6.5 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/1/92	Press Vent #9	M0011	PU9-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jm Rm	30.02	-0.21	75	N/A	56	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	NA	15	0.001	6	0.000	3.68

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				20			
Analysis Method		%CO2				0			
								ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1158	~~790.618~~ 790.118	0.37	1.4	77	250	250	~~250~~ 60	87		1
2	2.5		792.39	0.36	1.3	78	246	251	56	88		1
3	5		793.99	0.37	1.4	81	251	249	59	89		1
4	7.5		795.63	0.60	2.2	78	247	251	58	89		1
5	10		797.60	0.28	1.0	77	250	252	56	89		1
6	12.5		799.11	0.16	0.59	79	251	249	56	88		1
7	15		800.24	0.32	1.2	79	247	250	58	89		1
8	17.5		801.67	0.39	1.4	78	244	246	56	89		1
9	20		803.28	0.41	1.5	84	245	251	56	90		1
10	22.5		804.99	0.24	0.88	82	251	248	56	90		1
11	25		806.29	0.16	0.59	84	251	247	57	91		1
12	27.5		807.38	0.18	0.66	86	250	247	58	90		1
	30		808.494									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/17/92	Press Vent #9	M0011	N9 - F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	~~1233~~ 1231	808.494	0.37	1.4	80	244	246	66	90		1
B2	32.5		810.14	0.37	1.4	81	244	249	57	91		1
3	35		811.79	0.52	1.9	82	249	249	56	91		2
4	37.5		813.61	0.62	2.3	79	249	250	52	92		2
5	40		815.27	0.49	1.8	79	251	250	53	93		1
6	42.5		817.46	0.10	0.37	82	250	238	55	92		1
7	45		818.45	0.23	0.85	82	251	249	57	92		1
8	47.5		819.69	0.74	2.7	80	250	245	56	92		1
9	50		821.78	0.56	2.1	81	245	249	53	93		2
10	52.5		823.78	0.11	0.40	81	247	246	54	93		2
11	55		824.51	0.24	0.88	81	245	247	58	93		1
12	57.5		826.09	0.22	0.81	84	250	247	56	93		1
	60	1301	827.326									
			36.608	0.574	1.293	80.625				~~86~~		
										90.583		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	36.608	0.5744	1.293	80.625	90.583

Sheet Checked By: CN

Date

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific - Clayton Sample Date: 3/17/92

Sample Location: Press Vent #9 Recovery Date: 3/17/92

Recovered By: [illegible]

Run No.: PV9-F3

C TRAIN

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	586.7	600.7	485.5	726.3	grams
Initial Weight	571.1	581.3	486.5	720.3	grams
Net Weight	15.6	19.4	-1.0	6.0	grams

Description of impinger water _____ _____ % spent

_____ _____ Sil Gel Color

Total Moisture 40 grams VOH

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/17/92	Press Vent #10	M001L	PV10 - F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
AM, RM	30.02	-0.24	77	N/A	56	0.84	6ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	MZ	2.00	1.01	6C	6C	6C	N/A	12	0.001	5	Ø	3.6 A train

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				20.8	
%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP (F)	SAMPLE TRAIN VAC (in. Hg)
A1	0	1523	827.473	0.57	2.1	87	250	249	68	79		2
2	2.5		829.35	0.52	1.9	88	249	249	58	80		2
3	5		831.17	0.53	1.9	90	248	250	56	80		2
4	7.5		833.01	0.82	3.0	89	247	250	54	81		3
5	10		835.16	0.68	2.4	89	245	248	53	81		2
6	12.5		837.18	0.37	1.3	43	246	249	53	82		1
7	15		838.68	0.15	0.54	92	247	248	55	82		1
8	17.5		839.75	0.51	1.9	90	249	249	56	82		1
9	20		841.52	0.55	2.0	88	251	248	53	83		2
10	22.5		843.32	0.56	2.0	90	251	248	53	83		2
11	25		845.15	0.47	1.7	90	244	248	53	83		2
12	27.5		846.87	0.48	1.7	89	251	249	53	84		2
	30		848.556									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/17/91	Press Vent # 10	M0011	PV10 - F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP. (F)	PROBE TEMP. (F)	FILTER OVEN TEMP. (F)	SIL GEL IMPINGER TEMP. (F)	DGM IN/OUT TEMP. (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B 1	30	1556	848.556	0.74	2.7	87	247	245	59	83		3
2	32.5		850.70	0.76	2.7	87	246	250	53	85		3
3	35		852.93	0.49	1.8	89	244	248	53	85		2
4	37.5		854.67	0.42	1.5	90	246	258	54	86		2
5	40		856.30	0.31	1.1	88	244	248	55	85		1
6	42.5		857.71	0.19	0.68	86	244	248	56	84		1
7	45		858.85	0.16	0.58	88	244	248	56	84		1
8	47.5		859.93	0.16	0.58	90	248	248	56	84		1
9	50		860.95	0.35	1.3	89	248	250	57	84		1
10	52.5		862.38	0.49	1.8	89	247	251	55	84		2
11	55		864.13	0.65	2.3	90	251	247	53	84		2
12	57.5		866.10	0.62	2.2	90	257	250	53	84		2
	60	1626	868.113									
			40.640	0.6788	1.7	89				83		
					$\sqrt{P_{avg}}$ = 17.4048							

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		40.64	0.6788	1.7	89	83

Sheet Checked By: [illegible] Date 5/14/91

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific - Clayton **Sample Date:** 3/17/92

Sample Location: Press Vent #10 **Recovery Date:** 3/18/92

Recovered By: RM

Run No.: PV10-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	577.0	574.3	480.8	710.7	grams
Initial Weight	577.5	572.1	480.5	704.3	grams
Net Weight	-.5	2.2	0.3	6.4	grams

Description of impinger water _____ 10 % spent

Blue Sil Gel Color

Total Moisture 8.4 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ **Date** _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific – Clayton	3/17/92	~~M001~~ Press Vent # 10	M0011	PV10 – F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Am RM	30.02	-0.24	72	N/A	0.56	0.84	6 ft glass	1.25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6C	N/A	15	0.002	6	0	3.6 B train

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT
Collection Method		%O2				21	
Analysis Method		%CO2				0	

PITOT SYSTEM LEAK CHECK INIT	FINAL
ok	ok

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	1649	868.248	0.43	1.5	87	232	242	66	79		2
2	2.5		869.89	0.46	1.7	86	237	243	51	79		2
3	5		871.50	0.49	1.8	89	237	247	55	79		2
4	7.5		873.26	0.74	2.7	88	242	250	55	79		3
5	10		875.34	0.64	2.3	86	245	248	54	79		3
6	12.5		877.34	0.28	1.0	88	250	250	54	79		2
7	15		878.64	0.13	0.47	89	249	250	56	79		1
8	17.5		879.55	0.47	1.7	86	250	247	55	79		2
9	20		881.21	0.54	1.9	86	246	248	53	80		2
10	22.5		883.03	0.58	2.1	87	246	248	53	80		3
11	25		884.90	0.45	1.6	86	251	248	53	79		2
12	27.5		886.57	0.46	1.7	85	250	247	53	79		2
	30		888.242									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific	3/17/92	Press Vent # 10	M0011	PV10 - F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1722	888.242	0.61	2.2	85	251	247	57	78		3
2	32.5		890.17	0.59	2.1	83	246	250	52	78		3
3	35		892.08	0.43	1.5	83	245	249	53	78		2
4	37.5		893.68	0.25	0.9	85	247	249	54	78		1
5	40		894.94	0.16	0.58	85	249	247	55	77		1
6	42.5		895.98	0.14	0.50	88	251	248	55	77		1
7	45		896.94	0.19	0.68	88	251	248	55	77		1
8	47.5		898.05	0.50	1.8	87	251	247	54	77		2
9	50		899.70	0.61	2.2	88	250	246	53	77		2
10	52.5		901.65	0.60	2.2	89	251	247	53	77		3
11	55		903.58	0.62	2.2	87	248	249	54	77		3
12	57.5		905.45	0.61	2.2	87	251	248	55	77		3
	60	1752	907.394									
			39.146	0.6609	1.4	87				78		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	39.146	0.6609	1.647	87	78

Sheet Checked By: [illegible] Date

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific - Clayton **Sample Date:** 3/17/92

Sample Location: Press Vent # 10 **Recovery Date:** 3/18/92

Recovered By: JM

Run No.: PV10-F2

B-train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	562.2	571.3	461.8	711.1	grams
Initial Weight	549.4	552.5	462.0	704.2	grams
Net Weight	12.8	18.8	-.2	+6.9	grams

Description of impinger water _____ 20 % spent

Blue Sil Gel Color

Total Moisture 38.3 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Container No: _____ **Liquid level**

_____ **blank** **Marked/Sealed** _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ **Date** _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/17/92	Press Vent #10	M0011	PV10 - F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
GM RM	30.02	-0.24	68	N/A	56	0.84	6 ft glass	L25	0.236

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M2	2.00	1.01	6C	6C	6R	N/A	13	Ø	5	Ø	3.6
												C train

EPA METHOD 3
Collection Method _____
Analysis Method _____

	RUN 1	RUN 2	RUN 3	AVG	AMBIENT
%O2				21	
%CO2				0	

PITOT SYSTEM LEAK CHECK: INIT OK; FINAL OK

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
A 1	0	1812	907.576	0.56	2.0	83	220	222	60	73		1
2	2.5	~~1846~~	909.43	0.53	1.9	87	225	235	57	73		1
3	5		911.26	0.42	1.5	85	230	246	56	74		1
4	7.5		912.94	0.79	2.8	83	235	249	54	74		2
5	10		915.10	0.60	2.2	86	241	249	49	74		2
6	12.5		917.18	0.22	0.79	83	248	245	48	74		1
7	15		918.39	0.17	0.10	81	244	249	49	74		1
8	17.5		919.02	0.40	1.4	82	245	248	51	74		2
9	20		920.42	0.47	1.7	83	246	248	47	74		1
10	22.5		922.20	0.51	1.8	82	250	248	46	74		2
11	25		924.16	0.53	1.9	81	250	247	46	75		2
12	27.5		925.82	0.53	1.9	83	251	248	46	75		2
	30	1842	927.611									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/17/92	Press Vent #10	M0011	PV10 - F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
B1	30	1846	Rm ~~922.611~~ 927.611	0.63	2.3	80	246	249	53	73		2
2	32.5		929.65	0.42	1.5	81	248	249	47	74		2
3	35		931.34	0.43	1.5	79	251	247	47	74		1
4	37.5		932.98	0.34	1.2	79	251	248	48	74		1
5	40		934.52	0.20	0.72	80	251	248	48	74		1
6	42.5		935.78	0.67	2.4	80	245	250	50	74		2
7	45		937.59	0.08	0.29	80	249	249	49	74		2
8	47.5		938.44	0.10	0.36	84	242	247	52	74		1
9	50		939.27	0.33	1.2	83	251	248	52	73		1
10	52.5		940.63	0.47	1.7	82	251	248	50	74		2
11	55		942.32	0.49	1.8	79	249	248	50	74		2
12	57.5		944.16	0.49	1.8	81	249	248	50	71		2
	60	1916	945.966									
			38.390	0.6401	1.5	82				74		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
	60	38.390	0.6401	1.5	82	74

Sheet Checked By: [illegible] Date 5/14

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific - Clayton Sample Date: 3/17/92

Sample Location: Press Vent #10 Recovery Date: 3/18/92

Recovered By: JM

Run No.: PV10-F3

C-train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	582.4	605.1	485.8	733.0	grams
Initial Weight	582.6	605.0	486.4	726.3	grams
Net Weight	-0.2	-0.1	-0.6	6.7	grams

Description of impinger water _____ 10 % spent

_____ Blue Sil Gel Color

Total Moisture ~~5.8~~ 6.0 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/13/92	Press Vent #11	M0011	PV11-F1

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jm Rm	30.00	-0.44	54	N/A	35.25	0.84	4 ft Glass	K20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) in. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) in. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M5	1.92	0.998	GC	GC	GC	N/A	15	0.002	5	0.010	1.6

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21		ok	ok
Analysis Method		%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	10:21	869.224	0.71	1.1	69	249	248	~~54~~ 49	62		1.5
2	2.5		870.65	0.71	1.1	70	244	251	49	63		1.5
3	5		872.07	0.71	1.1	71	240	249	49	65		1.0
4	7.5		873.47	0.71	1.1	70	238	249	50	66		1.0
5	10		874.87	0.79	1.3	69	238	249	50	68		1.5
6	12.5		876.36	0.92	1.5	69	235	247	50	69		2.0
7	15		878.09	0.55	0.88	69	233	248	49	70		1.0
8	17.5		879.34	0.43	0.69	69	231	253	50	71		1.0
9	20		880.49	0.48	0.77	68	234	250	50	72		1.0
10	22.5		881.69	0.45	0.72	68	235	252	50	73		1.0
11	25		882.83	0.43	0.69	68	238	251	50	74		1.0
12	27.5		883.97	0.43	0.69	69	241	251	50	74		1.0
	30	1051	885.093									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		36.517				

Sheet Checked By: C.H. Date 5/14/92

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-13-92	Press Vent 11	M0011	PV11 - F1

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	11:00	885.093	1.2	1.9	68	247	251	59	74		2.5
2	32.5		886.93	1.2	1.9	68	248	250	50	76		2.5
3	35		888.78	1.2	1.9	68	245	247	49	77		2.5
4	37.5		890.64	1.2	1.9	68	241	250	49	78		2.5
5	40		892.48	1.2	1.9	68	237	247	49	79		2.5
6	42.5		894.35	1.1	1.8	69	233	247	49	80		2.5
7	45		896.18	~~0.81~~ 0.87	1.4	70	232	251	49	80		2.0
8	47.5		897.83	0.86	1.4	70	235	250	49	79		2.0
9	50		899.41	0.85	1.4	70	237	249	50	80		2.0
10	52.5		901.05	0.82	1.3	68	243	251	49	80		2.0
11	55		902.60	0.83	1.3	67	242	249	50	81		1.5
12	57.5		904.18	0.84	1.3	67	242	247	50	81		1.5
	60	11:30	905.741									
			36.517	0.746	1.293	68.75	~~239.125~~	~~279.454~~		73.833		
				0.83	1.2							

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		36.517	0.8488	1.293	68.75	73.833

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3-13-91

Sample Location: Press Vent 11

Recovery Date: 3-13-91

Recovered By: RM

Run No.: PV11-F1

A train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	592.4	587.6	482.4	707.6	grams
Initial Weight	589.6	585.2	482.0	701.4	grams
Net Weight	2.8	2.4	.4	6.2	grams

Description of impinger water _____ 40 % spent

_____ Sil Gel Color

Total Moisture 11.3 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/13/92	Press Vent 11	M0011	PV11 - F2

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
JM RM	30.00	-0.44	54	N/A	35.25	0.84	4ft Glass	K 20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M5	1.92	0.998	6C	6C	6C	N/A	15	0.002	6	0.008	1.69

EPA METHOD 3		RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method	%O2				21			
Analysis Method	%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	~~1247~~ 1247	906.738	0.67	1.1	~~54~~ 54	249	250	58	83		3.0
2	2.5		908.34	0.67	1.1	~~48~~ 48	249	247	52	81		3.0
3	5		909.84	0.70	0.9	77	247	247	50	82		3.0
4	7.5		911.20	0.69	1.2	73	246	248	50	82		3.0
5	10		912.61	0.70	0.9	74	243	251	51	83		2.0
6	12.5		913.95	0.82	1.4	72	243	250	52	84		3.0
7	15		915.46	0.60	1.0	73	240	247	52	85		3.0
8	17.5		916.95	0.35	0.60	73	239	248	52	86		1.5
9	20		918.11	0.43	0.73	72	243	251	53	85		2.0
10	22.5		919.30	0.49	0.83	69	240	247	~~56~~ 53	85		2.0
11	25		920.59	0.44	0.74	69	239	250	53	85		2.0
12	27.5		921.75	0.49	0.83	72	239	251	54	86		2.0
	30		923.046									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		36.724				

Sheet Checked By: [illegible] Date [illegible]

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/13/92	~~PV11~~ Press Vent 11	M0011	PV11-F2

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1318	923.046	1.0	~~1.6~~ Rm 1.7	74	249	251	61	85		4.0
2	32.5		924.78	1.0	1.7	~~77~~ Rm 72	248	251	52	85		4.0
3	35		926.59	0.97	1.6	72	244	250	52	86		4.0
4	37.5		928.36	0.97	1.6	72	242	251	52	86		4.0
5	40		930.12	0.91	1.5	72	240	250	53	86		4.0
6	42.5		931.85	0.88	1.5	71	237	242	54	87		4.0
7	45		933.58	0.81	1.4	72	234	253	55	88		4.0
8	47.5		935.26	0.79	1.3	73	237	250	54	88		3.5
9	50		936.91	0.75	1.3	72	234	252	55	88		3.5
10	52.5		938.58	0.74	1.3	69	234	247	55	88		3.0
11	55		940.21	0.74	1.3	69	232	252	55	88		3.0
12	57.5		941.84	0.74	1.3	69	232	251	55	88		3.0
	60	1348	943.462									
				0.843	1.201	71.864				~~86~~ Rm 85.417		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		36.7240	0.843	1.201	71.864	85.417

Sheet Checked By: [illegible] Date _____

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/13/92

Sample Location: Press Vent #11

Recovery Date: 3/13/92

Recovered By: RM

Run No.: PV11-F2

B train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	558.0	563.4	462.3	699.9	grams
Initial Weight	558.7	563.5	463.2	695.3	grams
Net Weight	-.7	-.1	-.9	4.6	grams

Description of impinger water _____ 50% % spent

_____ Sil Gel Color

Total Moisture 2.9 grams JCN

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

EMISSION TESTING FIELD DATA

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3/12/92 (3/17/92 JG)	Press Vent 11	M0011	PV11-F3

OPERATORS	BAROM PRESS (in. Hg)	STATIC PRESS (in. H2O)	AMBIENT TEMP (F)	FILTER TYPE & FILTER NUMBER(S)	STACK ID (in.)	PITOT TUBE Cp	PROBE LENGTH AND LINER TYPE	NOZZLE I.D.	NOZZLE Diameter
Jm Rm	30.00	-0.44	54	N/A	35.25	0.84	4ft Glass	K20	0.196

ASSUMED MOIST. (%)	DGM BOX NO.	DGM H@	DGM CAL FACTOR (Y)	STACK THERM NO.	STACK PITOT NO.	IMPINGER THERM NO.	ORSAT NO.	TRAIN LEAK CHECK (INITIAL) In. Hg	TRAIN LEAK CHECK (INITIAL) CFM	TRAIN LEAK CHECK (FINAL) In. Hg	TRAIN LEAK CHECK (FINAL) CFM	K FACTOR
1	M5	1.92	0.998	GC	GC	GC	NA	15	0.002	5	0.000	1.71

EPA METHOD 3			RUN 1	RUN 2	RUN 3	AVG	AMBIENT	PITOT SYSTEM LEAK CHECK INIT	PITOT SYSTEM LEAK CHECK FINAL
Collection Method		%O2				21		ok	ok
Analysis Method		%CO2				0			

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN VAC (in. Hg)
1	0	1440	943.621	0.63	1.1	69	RM ~~66~~ 249	252	66	86		1.0
2	2.5		945.09	0.63	1.1	71	249	253	51	86		1.0
3	5		946.56	0.62	1.0	72	247	251	50	81		1.0
4	7.5		947.01	0.62	1.0	71	247	252	50	88		1.0
5	10		949.45	0.62	1.0	71	245	251	49	88		1.0
6	12.5		950.88	0.39	1.4	71	250	250	49	89		1.0
7	15		952.48	0.35	0.6	70	247	250	47	89		1.0
8	17.5		953.71	0.24	0.4	70	249	252	47	88		1.0
9	20		RM ~~953~~ 954.75	0.31	0.5	70	250	251	48	88		1.0
10	22.5		955.67	0.31	0.5	69	250	250	48	89		1.0
11	25		956.67	0.28	0.5	70	249	250	48	88		1.0
12	27.5		957.68	0.28	0.5	69	249	251	47	87		1.0
	30		958.794									

Run Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F

Sheet Checked By: CH Date 3/19/92

EMISSION TESTING FIELD DATA

3/13/92 J. Shorter 3/23/92

PLANT AND CITY	DATE	SAMPLING LOCATION	SAMPLE TYPE	RUN NUMBER
Louisiana Pacific - Clayton	3-13-92	Press Vent 11	M0011	PV11-F3

TRAV. POINT NO.	ELAPSED TEST TIME (min)	CLOCK TIME (24-hr)	GAS METER READING Vm (ft3)	P VELOCITY HEAD (in. H2O)	H ORIFICE (in. H2O)	STACK TEMP (F)	PROBE TEMP (F)	FILTER OVEN TEMP (F)	SIL GEL IMPINGER TEMP (F)	DGM IN/OUT TEMP (F)	AUX. TEMP. (F)	SAMPLE TRAIN ACUU (in. Hg)
1	30	1516	958.794	0.94	1.6	69	249	251	58	86		1.0
2	32.5		960.40	1.1	1.9	70	249	250	46	87		1.0
3	35		962.25	1.1	1.9	69	244	249	46	87		1.5
4	37.5		964.10	1.0	1.7	69	238	250	46	88		1.5
5	40		965.89	0.94	1.6	72	237	250	47	88		1.0
6	42.5		967.62	0.89	1.5	70	235	250	47	88		1.0
7	45		969.34	0.75	1.3	70	236	250	47	88		1.0
8	47.5		970.96	0.77	1.3	71	238	250	48	88		1.0
9	50		972.55	0.75	1.3	70	239	250	48	88		1.0
10	52.5		974.13	0.72	1.2	70	242	251	48	88		1.0
11	55		975.66	0.72	1.2	70	246	250	48	88		1.0
12	57.5		977.18	0.72	1.2	68	241	251	48	88		1.0
	60	1546	978.688									
			35.067	0.801	1.1375	70.042				87.458		

Page Totals	TOTAL TIME	DGM VOLUME	AVG SQRT P	AVG H	AVG STK F	AVG DGM F
		35.067	0.801	1.1375	70.042	87.458

Sheet Checked By: [illegible] Date [illegible]

FORMALDEHYDE 0011 SAMPLE RECOVERY AND INTEGRITY DATA SHEET

Plant: Louisiana Pacific

Sample Date: 3/13/92

Sample Location: Press Vent #11

Recovery Date: 3/13/92

Recovered By: AM

Run No.: PV11-F3

C train

MOISTURE

Impingers	1	2	3	Silica Gel	
Final	589.1	605.2	486.1	715.5	grams
Initial Weight	589.4	606.4	486.0	711.0	grams
Net Weight	-.3	-1.2	-.1	4.5	grams

Description of impinger water _____ ~~50~~ 40% spent

Sil Gel Color _____

Total Moisture 2.9 grams

RECOVERED SAMPLE

Probe Rinse & Impinger Contents

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Container No: _____ Liquid level

_____ blank Marked/Sealed _____

Samples stored and locked _____

Remarks: _____

Relinquished by: _____ Date _____

APPENDIX E

CEMS FIELD DATA

DRYER STACKS

DRYER STACKS 1-4, 6, 8
CEMS SUMMARY
LOUISIANA PACIFIC CORPORATION

			CEM Data (Raw Data)		Calibration Data						CEM Data (Cal. Error Corrected)		Volumetric Flow		Mass Emission Rates	
	Start	Stop	CO	THC	CO			THC			CO	THC	Qa	Qa	CO	THC
Run No.	Time	Time	(ppm)	(ppm)	Cma	Co	Cm	Cma	Co	Cm	(ppm)	(ppm)	(scfm)	(dscfm)	(lb/hr)	(lb/hr)
Dryer1 1	0752	0904	28.1	41.7	566.1	0.9	557.0	55.2	1.6	55.2	27.7	41.3	54,500	49,500	6.0	14.0
2	0957	1107	33.9	49.2	566.1	0.4	555.9	55.2	2.0	55.2	34.1	48.9	53,500	42,200	6.3	14.1
3	1151	1151	28.2	58.5	566.1	0.8	554.4	55.2	2.4	55.0	28.0	58.8	54,500	42,700	5.2	17.2
Dryer2 1	1538	1641	34.9	56.1	566.1	0.8	553.9	55.2	2.6	54.6	34.9	56.8	55,200	44,800	6.8	17.4
2	1746	1845	28.1	65.3	566.1	0.8	554.3	55.2	3.1	54.3	27.9	67.1	55,800	45,100	5.5	20.7
3	0744	0847	23.7	54.2	566.1	0.9	562.5	55.2	2.0	55.6	23.0	53.8	60,700	50,300	5.0	18.8
Dryer3 1	0753	0856	18.2	45.1	566.1	1.1	553.1	55.2	2.1	54.6	17.6	45.3	51,400	43,700	3.4	13.6
2	0910	1020	12.0	50.2	566.1	1.0	552.0	55.2	2.0	54.4	11.4	50.8	52,300	45,100	2.2	15.7
Dryer4 1	1104	1207	9.3	41.7	566.1	0.9	551.1	55.2	1.8	54.2	8.6	42.0	48,400	41,900	1.6	13.3
2	1225	1225	10.0	41.7	566.1	0.9	550.7	55.2	1.8	54.1	9.4	42.1	50,000	43,200	1.8	12.5
Dryer6 1	1603	1759	185.3	119.5	566.1	0.9	559.3	510	1.9	500.3	187.0	120.3	93,400	75,600	61.6	62.3
2	1729	1833	190.0	100.8	566.1	0.9	559.5	510	1.9	501.4	191.6	101.0	86,400	69,700	58.3	48.2
3	1853	1958	195.9	97.7	566.1	0.9	559.7	510	1.9	503.8	197.5	97.4	90,800	72,600	62.6	48.4
Dryer8 1	1046	1159	220.7	100.9	566.1	0.9	561.0	510	2.6	501.6	222.2	100.5	39,700	31,800	30.8	21.9
2	1225	1330	207.7	89.0	566.1	0.9	560.5	510	2.3	500.6	209.2	88.8	39,900	31,300	28.6	19.0
3	1347	1452	217.1	115.8	566.1	0.9	559.7	510	2.0	500.1	219.0	116.5	38,500	30,300	28.9	24.2

CEM Reference Method Data

Client Louisiana Pacific
Source Dryer Stacks 1,2,3,4,6,8
Date 03/19/92-03/21/92
Project No.1449-001

			CEM Data (Raw Data)				Calibration Data						CEM Data (Calibration Error Corrected)						Mass Emission Rates			
Run No.	Start Time	Stop Time	CO (ppm)	CO2 (%)	O2 (%)	THC (ppm)	CO Cma	Co	Cm	THC Cma	Co	Cm	CO (ppm)	CO2 (%)	O2 (%)	THC (ppm)	NOx (ppm)	SO2 (ppm)	Qa (scfm)	Qs (dscfm)	CO (lb/hr)	THC (lb/hr)
Dryer1 1	0752	0904	28.1			41.7	566.1	0.9	557.0	55.2	1.6	55.2	27.7			41.3			54,500	49,500	6.0	14.0
2	0957	1107	33.9			49.2	566.1	0.4	555.9	55.2	2.0	55.2	34.1			48.9			53,500	42,200	6.3	14.1
3	1151	1151	28.2			58.5	566.1	0.8	554.4	55.2	2.4	55.0	28.0			58.8			54,500	42,700	5.2	17.2
Dryer2 1	1538	1644	34.9			56.1	566.1	0.8	553.9	55.2	2.6	54.6	34.9			56.8			55,200	44,800	6.8	17.4
2	1746	1845	28.1			65.3	566.1	0.8	554.3	55.2	3.1	54.3	27.9			67.1			55,800	45,100	5.5	20.7
3	0744	0847	23.7			54.2	566.1	0.9	562.5	55.2	2.0	55.6	23.0			53.8			60,700	50,300	5.0	18.8
Dryer3 1	0753	0856	18.2			45.1	566.1	1.1	553.1	55.2	2.1	54.6	17.6			45.3			51,400	43,700	3.4	13.6
2	0910	1020	12.0			50.2	566.1	1.0	552.0	55.2	2.0	54.4	11.4			50.8			52,300	45,100	2.2	15.7
Dryer4 1	1104	1207	9.3			41.7	566.1	0.9	551.1	55.2	1.8	54.2	8.6			42.0			48,400	41,900	1.6	13.3
2	1225	1225	10.1			41.7	566.1	0.9	550.7	55.2	1.8	54.1	9.4			42.1			50,000	43,200	1.8	12.5
Dryer6 1	1603	1759	185.3			119.5	566.1	0.9	559.3	510	1.9	500.3	187.0			120.3			93,400	75,600	61.6	62.3
2	1729	1833	190.0			100.8	566.1	0.9	559.5	510	1.9	501.4	191.6			101.0			86,400	69,700	58.3	48.2
3	1853	1958	195.9			97.7	566.1	0.9	559.7	510	1.9	503.8	197.5			97.4			90,800	72,600	62.6	48.4
Dryer8 1	1046	1159	220.7			100.9	566.1	0.9	561.0	510	2.6	501.6	222.2			100.5			39,700	31,800	30.8	21.9
2	1225	1330	207.7			89.0	566.1	0.9	560.5	510	2.3	500.6	209.2			88.8			39,900	31,300	28.6	19.0
3	1347	1452	217.1			115.8	566.1	0.9	559.7	510	2.0	500.1	219.0			116.5			38,500	30,300	28.9	24.2

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#1 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	19 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.90	-0.09	0.80	0.01	0.85
CO Low	302.00	302.10	-0.01					
CO Mid	566.10	565.00	0.11	558.60	0.64	555.30	0.33	556.95
CO High	910.00	908.80	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		1.50	-1.50	1.70	-0.20	1.60
THC Low	29.70	30.30	-0.60	31.10	-0.80	31.20	-0.10	
THC Mid	55.20	55.00	0.20	55.20	-0.20	55.10	0.10	55.15
THC High	85.80	84.00	1.80	84.20	-0.20	84.50	-0.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#1 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	19 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.0	0.0	0.9	-0.09	0.8	0.01	0.85
CO Low	302.00	302.1	~~-0.23~~ 0.0					
CO Mid	566.10	565.0	-0.11	558.6	-0.64	555.3	0.33	556.95
CO High	910.00	908.8	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	1.5	-1.5	1.7	-0.20	1.60
THC Low	29.70	30.3	-0.50	31.1	-0.90	31.2	-0.10	
THC Mid	55.20	55.0	0.20	55.2	-0.2	55.1	0.10	55.15
THC High	85.80	84.0	1.80	84.3	-0.2	84.5	-0.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0752 -0801
0804 - 0856

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#1 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	19 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.08	-0.01	0.80	-0.07	0.44
CO Low	302.00	302.10	-0.01					
CO Mid	566.10	565.00	0.11	555.30	0.97	556.40	-0.11	555.85
CO High	910.00	908.80	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		1.70	-1.70	2.30	-0.60	2.00
THC Low	29.70	30.30	-0.60	31.20	-0.90	31.20	0.00	
THC Mid	55.20	55.00	0.20	55.10	-0.10	55.30	-0.20	55.20
THC High	85.80	84.00	1.80	84.50	-0.50	83.60	0.90	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#1 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	19 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.0	0.0	0.8	-0.01	0.8	-0.07	0.44
CO Low	302.00	302.1	-0.23					
CO Mid	566.10	565.0	0.11	555.3	0.97	556.4	-0.11	555.85
CO High	910.00	908.8	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	1.7	~~-1~~.7	2.3	-0.60	2.00
THC Low	29.70	30.3	-0.50	31.2	-0.9	31.2	0.00	
THC Mid	55.20	55.0	0.20	55.1	-0.10	55.3	-0.20	55.20
THC High	85.80	84.0	1.80	84.5	-0.50	83.6	0.90	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0957 - 1057

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#1 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	19 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.80	-0.08	0.80	0.00	0.80
CO Low	302.00	302.10	-0.01					
CO Mid	566.10	565.00	0.11	556.40	0.86	552.40	0.40	554.40
CO High	910.00	908.80	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.30	-2.30	2.40	-0.10	2.35
THC Low	29.70	30.30	-0.60	31.20	-0.90	30.90	0.30	
THC Mid	55.20	55.00	0.20	55.30	-0.30	54.70	0.60	55.00
THC High	85.80	84.00	1.80	83.60	0.40	82.30	1.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#1 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	19 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00	0.0	0.50	-0.08	.08	0.0	0.80
CO Low	302.00	302.1	-0.01					
CO Mid	566.10	565.00	0.11	556.4	0.86	552.4	.04	554.4
CO High	910.00	908.80	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00	0.00	2.3	-2.30	2.4	-0.10	2.35
THC Low	29.70	30.3	-0.60	31.2	-0.90	30.9	0.30	
THC Mid	55.20	55.0	0.20	55.3	-0.30	54.7	0.60	55.0
THC High	85.80	84.0	1.80	83.6	0.40	82.3	1.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1147 - 1247

Dryer Stack #1

Run 1

	THC100 PPM	CO PPM
03-19-199 07:52:00	30.51	24.28
03-19-199 07:53:00	32.37	23.82
03-19-199 07:54:00	32.95	24.03
03-19-199 07:55:00	33.87	24.51
03-19-199 07:56:00	33.42	22.64
03-19-199 07:57:00	32.53	23.35
03-19-199 07:58:00	32.07	24.25
03-19-199 07:59:00	31.82	24.94
03-19-199 08:00:01	32.57	25.39
03-19-199 08:05:00	36.78	24.87
03-19-199 08:06:00	34.67	23.19
03-19-199 08:07:00	36.10	24.61
03-19-199 08:08:00	37.79	23.24
03-19-199 08:09:00	38.63	23.85
03-19-199 08:10:00	37.78	27.88
03-19-199 08:11:00	37.01	28.11
03-19-199 08:12:00	37.39	31.21
03-19-199 08:13:00	39.06	29.41
03-19-199 08:14:00	37.94	27.52
03-19-199 08:15:00	36.77	27.46
03-19-199 08:16:00	38.23	26.93
03-19-199 08:17:00	37.46	26.88
03-19-199 08:18:00	38.54	24.97
03-19-199 08:19:00	41.03	26.28
03-19-199 08:20:00	40.68	27.90
03-19-199 08:21:00	40.95	28.03
03-19-199 08:22:00	43.37	27.66
03-19-199 08:23:00	43.94	27.43
03-19-199 08:24:00	42.48	26.49
03-19-199 08:25:00	43.81	26.80
03-19-199 08:26:00	40.51	26.49
03-19-199 08:27:00	39.29	26.44
03-19-199 08:28:00	40.69	27.27
03-19-199 08:29:00	40.19	29.11
03-19-199 08:30:00	39.12	29.69
03-19-199 08:31:00	37.30	27.82
03-19-199 08:32:00	39.18	28.15
03-19-199 08:33:00	40.84	30.21
03-19-199 08:34:00	39.90	31.63
03-19-199 08:35:00	40.55	32.50
03-19-199 08:36:00	42.07	31.01
03-19-199 08:37:00	41.13	29.70
03-19-199 08:38:00	43.13	29.80
03-19-199 08:39:00	45.96	32.39
03-19-199 08:40:00	45.59	33.28
03-19-199 08:41:00	41.51	32.40
03-19-199 08:42:00	41.22	35.03
03-19-199 08:43:00	45.12	33.75
03-19-199 08:44:00	49.67	31.21
03-19-199 08:45:00	51.64	27.75
03-19-199 08:46:00	55.02	23.03
03-19-199 08:47:00	57.03	22.69
03-19-199 08:48:00	55.35	26.34
03-19-199 08:49:00	61.89	32.20
03-19-199 08:50:00	57.26	34.80
03-19-199 08:51:00	53.35	34.22
03-19-199 08:52:00	51.77	33.59
03-19-199 08:53:00	52.45	32.55
03-19-199 08:54:00	51.74	31.67
03-19-199 08:55:00	48.79	29.85
	41.70	28.07

Dryer Stack #1

Run 2

03-19-199	09:47:01	52.88	34.67
03-19-199	09:48:01	52.33	34.52
03-19-199	09:49:01	49.65	36.71
03-19-199	09:50:01	46.32	36.70
03-19-199	09:51:01	47.36	37.90
03-19-199	09:52:01	49.31	38.20
03-19-199	09:53:01	47.69	35.03
03-19-199	09:54:01	47.94	33.84
03-19-199	09:55:01	47.21	38.50
03-19-199	09:56:01	47.79	39.13
03-19-199	09:57:01	47.84	38.81
03-19-199	09:58:01	49.83	34.81
03-19-199	09:59:00	50.95	33.56
03-19-199	10:00:01	52.60	33.22
03-19-199	10:01:01	53.86	32.86
03-19-199	10:02:00	57.55	36.16
03-19-199	10:03:01	61.40	36.36
03-19-199	10:04:00	66.22	34.50
03-19-199	10:05:00	72.03	34.46
03-19-199	10:06:01	54.63	34.34
03-19-199	10:07:00	54.12	32.70
03-19-199	10:08:00	56.55	35.02
03-19-199	10:09:01	54.17	37.36
03-19-199	10:10:00	50.74	37.33
03-19-199	10:11:00	52.22	38.80
03-19-199	10:12:00	51.00	37.00
03-19-199	10:13:00	46.57	34.03
03-19-199	10:14:00	44.19	34.32
03-19-199	10:15:00	42.01	34.34
03-19-199	10:16:00	41.13	34.63
03-19-199	10:17:00	41.90	33.85
03-19-199	10:18:00	43.39	32.30
03-19-199	10:19:00	43.14	31.41
03-19-199	10:20:00	40.76	28.60
03-19-199	10:21:00	40.59	26.74
03-19-199	10:22:00	40.80	26.42
03-19-199	10:23:00	41.38	26.76
03-19-199	10:24:00	43.39	28.62
03-19-199	10:25:00	45.23	28.44
03-19-199	10:26:00	44.56	27.90
03-19-199	10:27:00	44.69	30.11
03-19-199	10:28:00	44.07	33.19
03-19-199	10:29:00	42.19	35.64
03-19-199	10:30:00	44.18	36.16
03-19-199	10:31:00	46.52	36.52
03-19-199	10:32:00	46.75	37.50
03-19-199	10:33:00	44.13	34.63
03-19-199	10:34:00	43.87	34.82
03-19-199	10:35:00	46.79	34.49
03-19-199	10:36:00	50.43	35.13
03-19-199	10:37:00	51.08	33.12
03-19-199	10:38:00	51.64	32.30
03-19-199	10:39:00	50.81	33.83
03-19-199	10:40:00	49.08	33.83
03-19-199	10:41:00	51.62	34.29
03-19-199	10:42:00	60.81	33.70
03-19-199	10:43:00	58.86	34.77
03-19-199	10:44:00	50.78	30.71
03-19-199	10:45:00	49.45	28.61
03-19-199	10:46:00	47.99	28.40
		49.15	33.88

Dryer Stack #1
Run 3

03-19-1992	11:47:00	50.35	36.57
03-19-1992	11:48:00	52.71	33.77
03-19-1992	11:49:00	53.81	32.43
03-19-1992	11:50:00	52.94	34.09
03-19-1992	11:51:00	47.89	34.65
03-19-1992	11:52:00	46.86	36.48
03-19-1992	11:53:00	49.27	35.23
03-19-1992	11:54:00	49.33	32.63
03-19-1992	11:55:00	47.24	32.34
03-19-1992	11:56:00	45.21	32.07
03-19-1992	11:57:00	48.90	34.84
03-19-1992	11:58:01	52.63	38.18
03-19-1992	11:59:00	54.65	37.61
03-19-1992	12:00:00	53.89	29.64
03-19-1992	12:01:01	55.08	30.13
03-19-1992	12:02:01	54.76	33.96
03-19-1992	12:03:01	55.29	30.82
03-19-1992	12:04:01	62.63	30.59
03-19-1992	12:05:01	66.68	32.95
03-19-1992	12:06:01	70.75	33.14
03-19-1992	12:07:01	63.29	33.56
03-19-1992	12:08:01	57.46	29.22
03-19-1992	12:09:01	65.22	29.64
03-19-1992	12:10:01	72.52	30.27
03-19-1992	12:11:01	75.59	32.02
03-19-1992	12:12:01	74.88	33.20
03-19-1992	12:13:01	76.93	30.42
03-19-1992	12:14:01	76.76	27.84
03-19-1992	12:15:01	71.69	24.55
03-19-1992	12:16:01	74.60	26.32
03-19-1992	12:17:01	76.22	28.02
03-19-1992	12:18:01	71.22	23.22
03-19-1992	12:19:00	63.18	19.76
03-19-1992	12:20:01	64.61	20.02
03-19-1992	12:21:01	63.78	19.99
03-19-1992	12:22:01	59.79	21.78
03-19-1992	12:23:01	60.68	22.17
03-19-1992	12:24:00	59.63	25.39
03-19-1992	12:25:00	57.20	29.82
03-19-1992	12:26:01	57.40	31.77
03-19-1992	12:27:01	60.06	30.82
03-19-1992	12:28:00	56.20	28.66
03-19-1992	12:29:00	53.42	27.62
03-19-1992	12:30:00	52.46	29.64
03-19-1992	12:31:00	54.21	27.43
03-19-1992	12:32:00	54.20	22.87
03-19-1992	12:33:00	52.38	20.83
03-19-1992	12:34:00	52.01	20.30
03-19-1992	12:35:00	53.44	20.72
03-19-1992	12:36:00	53.81	21.73
03-19-1992	12:37:00	55.91	23.81
03-19-1992	12:38:00	54.86	25.81
03-19-1992	12:39:00	53.74	24.40
03-19-1992	12:40:00	54.57	24.00
03-19-1992	12:41:00	57.30	22.92
03-19-1992	12:42:00	54.93	20.70
03-19-1992	12:43:00	54.07	21.60
03-19-1992	12:44:00	55.85	21.92
03-19-1992	12:45:00	56.48	21.75
03-19-1992	12:46:00	55.41	22.11
		58.48	28.18

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#2 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	19 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK				
				PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	0.00		0.80	-0.08	0.80	0.00	0.80
CO Low	302.00	302.10	-0.01					
CO Mid	566.10	565.00	0.11	552.40	1.26	555.30	-0.29	553.85
CO High	910.00	908.80	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.40	-2.40	2.80	-0.40	2.60
THC Low	29.70	30.30	-0.60	30.90	-0.60	31.30	-0.40	
THC Mid	55.20	55.00	0.20	54.70	0.30	54.40	0.30	54.55
THC High	85.80	84.00	1.80	82.30	1.70	82.20	0.10	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#2 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	19 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	0.0	0.0	0.80	-0.08	.8	0.0	0.80
CO Low	302.00	302.1	-0.01					
CO Mid	566.10	565.0	0.12	552.4	1.26	555.3	0.29	558.85
CO High	910.00	908.8	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	2.4	-2.4	2.8	0.40	2.60
THC Low	29.70	30.3	~~0.3~~ -0.6	30.9	-0.60	31.3	-0.40	
THC Mid	55.20	55.0	0.2	54.7	0.3	54.4	0.30	54.65
THC High	85.80	84.0	1.80	82.3	1.7	82.2	0.10	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

~~1448~~ 1534 - 1636
~~1446~~

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#2 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	19 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.80	-0.08	0.80	0.00	0.80
CO Low	302.00	302.10	-0.01					
CO Mid	566.10	565.00	0.11	555.30	0.97	553.30	0.20	554.30
CO High	910.00	908.80	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.80	-2.80	3.30	-0.50	3.05
THC Low	29.70	30.30	-0.60	31.30	-1.00	30.70	0.60	
THC Mid	55.20	55.00	0.20	54.40	0.60	54.10	0.30	54.25
THC High	85.80	84.00	1.80	82.20	1.80	83.20	-1.00	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#2 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	19 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.0	0.0	0.40	-0.08	.8	0.0	0.80
CO Low	302.00	302.1	0.01					
CO Mid	566.10	565.0	0.11	555.3	0.97	553.3		
CO High	910.00	908.8	0.12					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	2.8	-2.80	3.3	-0.5	3.05
THC Low	29.70	30.3	-0.6	51.3	-1.00	30.7	0.6	
THC Mid	55.20	55.0	0.2	54.4	0.60	54.1	0.3	54.25
THC High	85.80	84.0	1.8	82.2	1.80	83.2		
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1846 - 1846

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#2 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Calibration Correction Factor Co/Cm
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	563.50	0.19	561.40	0.21	562.45
CO High	910.00	913.60	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		1.80	-1.80	2.10	-0.30	1.95
THC Low	29.70	30.30	-0.60	31.50	-1.20	31.70	-0.20	
THC Mid	55.20	55.10	0.10	56.00	-0.90	55.20	0.80	55.60
THC High	85.80	84.80	1.00	85.20	-0.40	84.80	0.40	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#2 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	20 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-.2	0.02	.9	-0.11	0.9	0.00	.9
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	565.4	0.07	563.5	.19	561.4	0.21	562.45
CO High	910.00	913.6	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	1.8	-1.80	2.1	-0.30	1.95
THC Low	29.70	30.3	-.60	31.5	-1.20	31.7	-0.20	
THC Mid	55.20	55.1	0.10	~~55.5~~ 55.60	-0.3	55.2	0.80	55.60
THC High	85.80	84.8	1.0	85.2	-0.40	84.8	0.40	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0744

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.0	0.0	1.1	-0.11	1.0	0.01	1.05
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	564.6	0.15	553.6	1.1	552.5	0.11	553.05
CO High	910.00	911.9	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.1	-0.1	2.0	-2.1	2.2	-0.2	2.1
THC Low	29.70	30.3	-0.6	30.9	-0.60	30.9	0.0	
THC Mid	55.20	55.3	-0.1	54.5	0.80	54.6	-0.1	54.55
THC High	85.80	85.4	0.40	83.5	1.90	83.1	0.4	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0751 - 0851

Dryer Stack #2

Run 1

	THC100 PPM	CO PPM
03-19-1992 15:36:00	49.04	39.97
03-19-1992 15:37:00	50.71	32.44
03-19-1992 15:38:00	52.28	30.93
03-19-1992 15:39:00	49.70	31.80
03-19-1992 15:40:00	47.97	29.29
03-19-1992 15:41:00	47.77	28.73
03-19-1992 15:42:00	47.78	29.52
03-19-1992 15:43:00	47.44	28.91
03-19-1992 15:44:00	48.81	31.31
03-19-1992 15:45:00	48.41	31.78
03-19-1992 15:46:00	48.04	33.46
03-19-1992 15:47:00	47.65	31.38
03-19-1992 15:48:00	48.59	27.06
03-19-1992 15:49:00	49.76	24.99
03-19-1992 15:50:00	50.35	23.77
03-19-1992 15:51:00	50.98	22.92
03-19-1992 15:52:00	52.76	23.21
03-19-1992 15:53:00	55.91	25.56
03-19-1992 15:54:00	57.21	33.55
03-19-1992 15:55:00	55.99	41.22
03-19-1992 15:56:00	58.55	40.24
03-19-1992 15:57:00	59.88	33.89
03-19-1992 15:58:00	77.84	32.33
03-19-1992 15:59:00	92.60	34.35
03-19-1992 16:00:00	75.55	31.79
03-19-1992 16:01:00	68.17	28.86
03-19-1992 16:02:00	67.56	27.80
03-19-1992 16:03:00	63.44	31.21
03-19-1992 16:04:00	79.25	32.68
03-19-1992 16:05:00	70.99	32.97
03-19-1992 16:06:00	58.44	28.94
03-19-1992 16:07:00	51.83	29.28
03-19-1992 16:08:00	47.42	33.10
03-19-1992 16:09:00	46.73	33.54
03-19-1992 16:10:00	49.48	36.01
03-19-1992 16:11:00	49.68	38.90
03-19-1992 16:12:00	48.93	40.82
03-19-1992 16:13:00	49.43	42.90
03-19-1992 16:14:00	52.55	41.56
03-19-1992 16:15:00	51.89	37.94
03-19-1992 16:16:00	51.83	34.29
03-19-1992 16:17:00	52.56	36.53
03-19-1992 16:18:00	53.28	39.55
03-19-1992 16:19:00	53.60	42.20
03-19-1992 16:20:00	54.16	39.56
03-19-1992 16:21:00	54.26	39.42
03-19-1992 16:22:00	58.12	35.80
03-19-1992 16:23:00	58.72	46.10
03-19-1992 16:24:00	58.54	46.62
03-19-1992 16:25:00	59.12	44.34
03-19-1992 16:26:00	56.61	46.47
03-19-1992 16:27:00	58.37	43.11
03-19-1992 16:28:00	56.66	43.98
03-19-1992 16:29:00	55.96	41.84
03-19-1992 16:30:00	56.21	41.56
03-19-1992 16:31:00	59.04	38.53
03-19-1992 16:32:00	63.93	36.70
03-19-1992 16:33:00	65.37	38.26
03-19-1992 16:34:00	57.20	35.65
03-19-1992 16:35:00	53.62	33.92
	56.08	34.92

Dryer Stack 2

Run 2

03-19-1992 17:46:00	62.10	22.79
03-19-1992 17:47:00	55.40	21.13
03-19-1992 17:48:00	52.10	21.68
03-19-1992 17:49:00	56.20	22.93
03-19-1992 17:50:00	59.24	23.70
03-19-1992 17:51:00	58.32	23.87
03-19-1992 17:52:00	60.28	25.67
03-19-1992 17:53:00	71.70	25.67
03-19-1992 17:54:00	66.94	25.82
03-19-1992 17:55:00	59.83	26.63
03-19-1992 17:56:00	57.70	29.69
03-19-1992 17:57:00	53.66	30.91
03-19-1992 17:58:00	54.88	31.82
03-19-1992 17:59:00	56.15	32.63
03-19-1992 18:00:00	59.76	32.19
03-19-1992 18:01:00	62.74	29.49
03-19-1992 18:02:00	59.61	28.31
03-19-1992 18:03:00	58.37	28.78
03-19-1992 18:04:00	53.39	31.99
03-19-1992 18:05:00	55.04	32.57
03-19-1992 18:06:00	52.17	29.05
03-19-1992 18:07:00	49.95	27.65
03-19-1992 18:08:00	51.77	29.50
03-19-1992 18:09:00	53.56	26.55
03-19-1992 18:10:00	55.86	26.99
03-19-1992 18:11:00	55.60	28.07
03-19-1992 18:12:00	53.73	28.97
03-19-1992 18:13:00	52.71	30.22
03-19-1992 18:14:00	54.20	34.92
03-19-1992 18:15:00	59.67	33.19
03-19-1992 18:16:00	57.98	28.37
03-19-1992 18:17:00	54.88	25.97
03-19-1992 18:18:00	54.10	25.25
03-19-1992 18:19:00	54.09	22.34
03-19-1992 18:20:00	51.98	19.42
03-19-1992 18:21:00	52.67	21.70
03-19-1992 18:22:00	53.67	21.69
03-19-1992 18:23:00	56.21	22.37
03-19-1992 18:24:00	52.48	24.59
03-19-1992 18:25:00	50.04	22.43
03-19-1992 18:26:00	51.51	22.62
03-19-1992 18:27:00	54.22	27.83
03-19-1992 18:28:00	56.08	28.54
03-19-1992 18:29:00	56.51	30.33
03-19-1992 18:30:00	65.22	31.76
03-19-1992 18:31:00	64.90	35.72
03-19-1992 18:32:00	56.09	36.93
03-19-1992 18:33:00	54.08	37.85
03-19-1992 18:34:00	59.33	37.70
03-19-1992 18:35:00	60.87	36.20
03-19-1992 18:36:00	61.90	33.33
03-19-1992 18:37:00	104.40	32.77
03-19-1992 18:38:00	126.49	29.28
03-19-1992 18:39:00	122.89	28.74
03-19-1992 18:40:00	120.82	26.42
03-19-1992 18:41:00	125.61	26.05
03-19-1992 18:42:00	124.90	28.01
03-19-1992 18:43:00	95.64	27.22
03-19-1992 18:44:00	105.68	27.01
03-19-1992 18:45:00	98.59	25.61
	65.27	28.12

DRYER STACK #2

RUN #3		THC	CO
03-20-1992	07:45	53.5	18.8
03-20-1992	07:46	54.4	19.8
03-20-1992	07:47	54.4	22.3
03-20-1992	07:48	59.8	23.8
03-20-1992	07:49	62.2	23.8
03-20-1992	07:50	62.0	23.8
03-20-1992	07:51	60.1	23.6
03-20-1992	07:52	58.0	23.0
03-20-1992	07:53	56.3	24.0
03-20-1992	07:54	55.5	23.8
03-20-1992	07:55	55.8	24.9
03-20-1992	07:56	56.4	25.2
03-20-1992	07:57	55.2	24.7
03-20-1992	07:58	54.6	23.8
03-20-1992	07:59	55.7	23.5
03-20-1992	08:00	53.3	24.5
03-20-1992	08:01	51.5	24.9
03-20-1992	08:02	53.5	22.4
03-20-1992	08:03	52.8	21.2
03-20-1992	08:04	52.3	22.0
03-20-1992	08:05	52.0	21.5
03-20-1992	08:06	51.9	20.9
03-20-1992	08:07	50.8	21.2
03-20-1992	08:08	50.6	21.5
03-20-1992	08:09	51.3	21.2
03-20-1992	08:10	54.9	20.5
03-20-1992	08:11	55.8	21.5
03-20-1992	08:12	53.0	21.0
03-20-1992	08:13	50.9	20.1
03-20-1992	08:14	52.3	21.8
03-20-1992	08:15	54.9	24.3
03-20-1992	08:16	53.7	25.6
03-20-1992	08:17	53.6	24.5
03-20-1992	08:18	56.2	25.6
03-20-1992	08:19	55.9	24.9
03-20-1992	08:20	57.2	24.0
03-20-1992	08:21	56.1	25.0
03-20-1992	08:22	58.8	25.7
03-20-1992	08:23	53.5	26.5
03-20-1992	08:24	55.0	27.1
03-20-1992	08:25	56.1	27.0
03-20-1992	08:26	57.3	26.5
03-20-1992	08:27	53.3	27.5
03-20-1992	08:28	51.3	24.2
03-20-1992	08:29	55.2	25.0
03-20-1992	08:30	58.3	25.1
03-20-1992	08:31	57.0	24.5
03-20-1992	08:32	55.2	25.2
03-20-1992	08:33	53.4	28.0
03-20-1992	08:34	54.5	28.4
03-20-1992	08:35	55.0	25.2
03-20-1992	08:36	54.0	21.8
03-20-1992	08:37	51.7	22.8
03-20-1992	08:38	50.3	24.8
03-20-1992	08:39	50.9	26.2
03-20-1992	08:40	50.1	25.0
03-20-1992	08:41	49.4	24.0
03-20-1992	08:42	47.1	21.8
03-20-1992	08:43	46.4	21.8
03-20-1992	08:44	48.5	21.8
RUN #3 AVERAGE		54.2	23.7

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		1.10	-0.11	1.00	0.01	1.05
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	564.60	0.15	553.60	1.10	552.50	0.11	553.05
CO High	910.00	911.90	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.10	0.10	2.00	-2.10	2.20	-0.20	2.10
THC Low	29.70	30.30	-0.60	30.90	-0.60	30.90	0.00	
THC Mid	55.20	55.30	-0.10	54.50	0.80	54.60	-0.10	54.55
THC High	85.80	85.40	0.40	83.50	1.90	83.10	0.40	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.0	0.0	1.0	-0.10	.9	0.01	0.95
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	564.6	0.15	552.5	1.21	551.4	0.11	551.95
CO High	910.00	911.9	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.1	-0.1	2.2	2.3	1.8	0.40	2.00
THC Low	29.70	30.3	-0.6	30.9	-0.6	30.6	0.3	
THC Mid	55.20	55.3	-0.1	54.6	0.7	54.2	0.40	54.4
THC High	85.80	85.4	0.4	83.0	2.3	82.8	0.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

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* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		1.00	-0.10	0.90	0.01	0.95
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	564.60	0.15	552.50	1.21	551.40	0.11	551.95
CO High	910.00	911.90	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.10	0.10	2.20	-2.30	1.80	0.40	2.00
THC Low	29.70	30.30	-0.60	30.90	-0.60	30.60	0.30	
THC Mid	55.20	55.30	-0.10	54.60	0.70	54.20	0.40	54.40
THC High	85.80	85.40	0.40	83.10	2.30	82.80	0.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

DRYER STACK #3

RUN #1		THC	CO
03-21-1992	07:51	48.6	19.6
03-21-1992	07:52	48.1	19.7
03-21-1992	07:53	48.1	21.2
03-21-1992	07:54	49.7	21.9
03-21-1992	07:55	50.8	19.9
03-21-1992	07:56	48.7	19.8
03-21-1992	07:57	46.9	20.0
03-21-1992	07:58	47.6	19.9
03-21-1992	07:59	48.0	19.3
03-21-1992	08:00	47.7	19.4
03-21-1992	08:01	48.0	21.2
03-21-1992	08:02	49.7	21.3
03-21-1992	08:03	49.7	19.1
03-21-1992	08:04	49.3	20.2
03-21-1992	08:05	47.0	19.4
03-21-1992	08:06	46.5	19.4
03-21-1992	08:07	41.8	18.9
03-21-1992	08:08	41.3	18.3
03-21-1992	08:09	41.0	17.3
03-21-1992	08:10	40.1	16.4
03-21-1992	08:11	38.8	15.8
03-21-1992	08:12	37.7	16.1
03-21-1992	08:13	36.9	16.4
03-21-1992	08:14	37.6	16.5
03-21-1992	08:15	37.6	17.7
03-21-1992	08:16	38.8	18.4
03-21-1992	08:17	41.1	16.2
03-21-1992	08:18	42.8	15.6
03-21-1992	08:19	43.0	16.0
03-21-1992	08:20	43.8	15.9
03-21-1992	08:21	44.4	17.3
03-21-1992	08:22	45.3	16.7
03-21-1992	08:23	43.1	18.1
03-21-1992	08:24	44.1	16.9
03-21-1992	08:25	43.5	16.8
03-21-1992	08:26	44.5	17.1
03-21-1992	08:27	44.1	17.5
03-21-1992	08:28	47.1	18.8
03-21-1992	08:29	48.7	19.8
03-21-1992	08:30	49.1	21.6
03-21-1992	08:31	49.0	19.2
03-21-1992	08:32	50.2	21.7
03-21-1992	08:33	49.1	20.8
03-21-1992	08:34	49.7	20.0
03-21-1992	08:35	49.6	19.5
03-21-1992	08:36	46.8	20.1
03-21-1992	08:37	43.9	17.4
03-21-1992	08:38	43.7	16.1
03-21-1992	08:39	42.8	14.2
03-21-1992	08:40	42.1	16.4
03-21-1992	08:41	41.1	16.2
03-21-1992	08:42	42.2	16.4
03-21-1992	08:43	43.4	15.4
03-21-1992	08:44	45.3	18.8
03-21-1992	08:45	47.1	17.0
03-21-1992	08:46	46.5	16.4
03-21-1992	08:47	47.8	16.3
03-21-1992	08:48	46.3	16.7
03-21-1992	08:49	45.0	17.8
03-21-1992	08:50	46.2	17.5
RUN #1 AVERAGE		45.1	18.2

DRYER STACK #3

RUN #2		THC	CO
03-21-1992	09:12	43.5	13.1
03-21-1992	09:13	47.2	12.1
03-21-1992	09:14	47.4	12.3
03-21-1992	09:15	49.1	12.5
03-21-1992	09:16	51.7	12.4
03-21-1992	09:17	49.4	12.3
03-21-1992	09:18	47.9	12.0
03-21-1992	09:19	49.1	11.1
03-21-1992	09:20	49.0	12.1
03-21-1992	09:21	48.5	11.9
03-21-1992	09:22	45.5	12.0
03-21-1992	09:23	43.8	12.9
03-21-1992	09:24	42.7	14.3
03-21-1992	09:25	40.5	14.5
03-21-1992	09:26	37.7	14.5
03-21-1992	09:27	39.0	14.1
03-21-1992	09:28	39.7	14.6
03-21-1992	09:29	40.9	15.0
03-21-1992	09:30	45.5	14.5
03-21-1992	09:31	49.5	15.2
03-21-1992	09:32	53.2	16.3
03-21-1992	09:33	56.3	14.4
03-21-1992	09:34	60.7	13.8
03-21-1992	09:35	57.7	14.2
03-21-1992	09:36	57.0	12.8
03-21-1992	09:37	58.4	13.6
03-21-1992	09:38	59.1	13.6
03-21-1992	09:39	60.5	13.0
03-21-1992	09:40	59.0	12.5
03-21-1992	09:41	59.3	12.7
03-21-1992	09:42	57.9	12.7
03-21-1992	09:43	58.7	12.2
03-21-1992	09:44	58.8	11.6
03-21-1992	09:45	56.5	12.8
03-21-1992	09:46	52.6	12.8
03-21-1992	09:47	52.6	12.3
03-21-1992	09:48	52.8	11.8
03-21-1992	09:49	54.0	10.9
03-21-1992	09:50	53.3	12.0
03-21-1992	09:51	53.1	11.4
03-21-1992	09:52	53.6	11.4
03-21-1992	09:53	52.2	11.6
03-21-1992	09:54	52.8	11.1
03-21-1992	09:55	51.7	11.8
03-21-1992	09:56	49.8	11.1
03-21-1992	09:57	49.6	9.8
03-21-1992	09:58	49.4	9.3
03-21-1992	09:59	47.8	9.9
03-21-1992	10:00	50.0	11.3
03-21-1992	10:01	49.2	10.8
03-21-1992	10:02	49.0	11.4
03-21-1992	10:03	48.6	10.6
03-21-1992	10:04	48.4	10.3
03-21-1992	10:05	47.7	8.7
03-21-1992	10:06	48.2	9.5
03-21-1992	10:07	45.4	8.5
03-21-1992	10:08	44.1	8.7
03-21-1992	10:09	45.3	8.7
03-21-1992	10:10	44.3	8.2
03-21-1992	10:11	43.3	8.6
RUN #2 AVERAGE		50.2	12.0

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#4 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	0.0	0.0	0.9	-0.09	0.9	0.0	0.9
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	564.6	0.15	551.4	1.32	550.7	0.07	551.5
CO High	910.00	911.9	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.10	0.1	1.8	-1.9	1.7	0.10	1.75
THC Low	29.70	30.3	-0.6	30.6	-0.3	30.4	0.20	
THC Mid	55.20	55.3	-0.1	54.2	1.1	54.2	0.0	54.2
THC High	85.80	85.4	0.4	82.8	2.6	82.3	0.5	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

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* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#4 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.90	-0.09	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	564.60	0.15	551.40	1.32	550.70	0.07	551.05
CO High	910.00	911.90	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.10	0.10	1.80	-1.90	1.70	0.10	1.75
THC Low	29.70	30.30	-0.60	30.60	-0.30	30.40	0.20	
THC Mid	55.20	55.30	-0.10	54.20	1.10	54.20	0.00	54.20
THC High	85.80	85.40	0.40	82.80	2.60	82.30	0.50	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#4 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	0.0	0.0	0.9	-0.09	0.9	0.0	0.9
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	564.6	0.15	550.7	1.39	550.6		
CO High	910.00	911.9	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.10	0.1	1.7	-1.8	1.9		
THC Low	29.70	30.3	-0.6	30.4	-0.1	30.3		
THC Mid	55.20	55.3	-0.1	54.2	1.1	54.0		
THC High	85.80	85.4	0.4	82.3	3.1	81.8		
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#4 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	21 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.90	-0.09	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	564.60	0.15	550.70	1.39	550.60	0.01	550.65
CO High	910.00	911.90	-0.19					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.10	0.10	1.70	-1.80	1.90	-0.20	1.80
THC Low	29.70	30.30	-0.60	30.40	-0.10	30.30	0.10	
THC Mid	55.20	55.30	-0.10	54.20	1.10	54.00	0.20	54.10
THC High	85.80	85.40	0.40	82.30	3.10	81.80	0.50	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

DRYER STACK #4

RUN #1		THC	CO
03-21-1992	11:04	42.4	9.5
03-21-1992	11:05	41.7	10.2
03-21-1992	11:06	42.8	8.8
03-21-1992	11:07	42.2	8.8
03-21-1992	11:08	41.8	9.3
03-21-1992	11:09	41.4	11.4
03-21-1992	11:10	41.8	11.7
03-21-1992	11:11	41.9	10.9
03-21-1992	11:12	40.8	9.8
03-21-1992	11:13	40.9	9.3
03-21-1992	11:14	41.8	10.0
03-21-1992	11:15	40.8	8.8
03-21-1992	11:16	40.4	7.8
03-21-1992	11:17	38.5	7.8
03-21-1992	11:18	38.1	8.3
03-21-1992	11:19	37.2	10.4
03-21-1992	11:20	36.1	10.1
03-21-1992	11:21	38.2	8.6
03-21-1992	11:22	37.6	9.5
03-21-1992	11:23	37.3	9.0
03-21-1992	11:24	37.9	10.1
03-21-1992	11:25	36.4	9.8
03-21-1992	11:26	35.9	8.8
03-21-1992	11:27	37.4	8.8
03-21-1992	11:28	39.1	7.8
03-21-1992	11:29	38.5	7.8
03-21-1992	11:30	38.5	7.6
03-21-1992	11:31	39.4	7.5
03-21-1992	11:32	40.1	6.8
03-21-1992	11:33	40.1	6.8
03-21-1992	11:34	39.4	7.5
03-21-1992	11:35	42.1	8.8
03-21-1992	11:36	43.9	9.3
03-21-1992	11:37	41.8	10.7
03-21-1992	11:38	41.2	7.8
03-21-1992	11:39	40.3	7.5
03-21-1992	11:40	39.3	7.8
03-21-1992	11:41	39.9	7.8
03-21-1992	11:42	39.7	8.8
03-21-1992	11:43	39.0	9.1
03-21-1992	11:44	39.4	9.1
03-21-1992	11:45	39.4	8.8
03-21-1992	11:46	40.2	9.8
03-21-1992	11:47	40.0	9.0
03-21-1992	11:48	39.9	8.8
03-21-1992	11:49	39.1	9.0
03-21-1992	11:50	42.7	10.7
03-21-1992	11:51	46.9	10.7
03-21-1992	11:52	46.2	10.1
03-21-1992	11:53	46.9	9.8
03-21-1992	11:54	46.0	9.9
03-21-1992	11:55	50.3	10.7
03-21-1992	11:56	51.4	10.7
03-21-1992	11:57	49.5	10.3
03-21-1992	11:58	48.3	10.3
03-21-1992	11:59	49.4	10.1
03-21-1992	12:00	49.4	10.9
03-21-1992	12:01	48.5	10.7
03-21-1992	12:02	48.4	10.7
03-21-1992	12:03	47.1	10.7
RUN #1 AVERAGE		41.7	9.3

DRYER STACK #4

RUN #2		THC	CO
03-21-1992	12:24	44.6	10.7
03-21-1992	12:25	49.5	11.5
03-21-1992	12:26	48.5	10.7
03-21-1992	12:27	46.9	11.4
03-21-1992	12:28	48.5	12.4
03-21-1992	12:29	46.8	13.1
03-21-1992	12:30	45.5	12.3
03-21-1992	12:31	43.7	12.3
03-21-1992	12:32	44.4	11.7
03-21-1992	12:33	43.9	12.2
03-21-1992	12:34	42.2	11.4
03-21-1992	12:35	39.5	11.7
03-21-1992	12:36	40.8	12.2
03-21-1992	12:37	42.6	11.9
03-21-1992	12:38	43.9	13.6
03-21-1992	12:39	44.4	11.7
03-21-1992	12:40	45.1	10.7
03-21-1992	12:41	46.5	10.7
03-21-1992	12:42	44.9	10.4
03-21-1992	12:43	41.5	10.7
03-21-1992	12:44	42.5	10.7
03-21-1992	12:45	40.1	10.7
03-21-1992	12:46	37.3	10.7
03-21-1992	12:47	37.2	9.8
03-21-1992	12:48	36.3	9.0
03-21-1992	12:49	33.6	8.6
03-21-1992	12:50	32.1	9.5
03-21-1992	12:51	31.4	9.8
03-21-1992	12:52	31.0	8.8
03-21-1992	12:53	30.4	8.6
03-21-1992	12:54	31.0	8.8
03-21-1992	12:55	31.1	8.8
03-21-1992	12:56	32.0	8.5
03-21-1992	12:57	32.8	8.8
03-21-1992	12:58	33.8	8.8
03-21-1992	12:59	34.4	9.3
03-21-1992	13:00	35.4	9.3
03-21-1992	13:01	34.3	9.4
03-21-1992	13:02	36.2	9.0
03-21-1992	13:03	35.9	8.8
03-21-1992	13:04	36.4	8.0
03-21-1992	13:05	39.1	8.1
03-21-1992	13:06	39.9	8.6
03-21-1992	13:07	41.9	8.1
03-21-1992	13:08	43.8	8.8
03-21-1992	13:09	45.5	9.6
03-21-1992	13:10	47.5	8.8
03-21-1992	13:11	48.9	8.8
03-21-1992	13:12	50.0	9.7
03-21-1992	13:13	50.8	9.7
03-21-1992	13:14	49.3	9.7
03-21-1992	13:15	46.3	9.7
03-21-1992	13:16	46.5	9.7
03-21-1992	13:17	48.4	9.7
03-21-1992	13:18	49.1	9.7
03-21-1992	13:19	48.9	11.4
03-21-1992	13:20	50.0	9.9
03-21-1992	13:21	47.7	9.7
03-21-1992	13:22	45.6	9.7
03-21-1992	13:23	45.0	9.7
RUN #2 AVERAGE		41.7	10.1

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	559.10	0.63	559.40	-0.03	559.25
CO High	910.00	913.60	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		1.90	-0.19	1.90	0.00	1.90
THC Low	303.00	303.90	-0.09	300.10	0.38	300.60	-0.05	
THC Mid	510.00	511.30	-0.13	500.50	1.08	500.00	0.05	500.25
THC High	858.00	858.30	-0.03	844.70	1.36	844.60	0.01	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

*

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	20 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.2	0.02	0.9	-0.11	0.9	0.00	0.90
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	566.4	0.07	559.1	0.63	559.4	-0.03	559.25
CO High	910.00	913.6	0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	1.9	-0.19	1.8	0.00	1.9
THC Low	303.00	303.9	0.09	300.1	0.38	300.6	-0.05	
THC Mid	510.00	511.3	0.13	500.5	1.08	500.0	0.05	500.25
THC High	858.00	858.3	0.03	844.7	1.36	844.6	0.01	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1603 - 1803

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK				
				PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	559.40	0.60	559.60	-0.02	559.50
CO High	910.00	913.60	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		1.90	-0.19	1.80	0.01	1.85
THC Low	303.00	303.90	-0.09	300.60	0.33	301.60	-0.10	
THC Mid	510.00	511.30	-0.13	500.00	1.13	502.80	-0.28	501.40
THC High	858.00	858.30	-0.03	844.60	1.37	849.10	-0.45	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

*

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	20 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.2	0.02	0.9	-.11	.09	0.0	6.90
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	565.4	0.07	559.4	0.60	559.6	0.02	559.5
CO High	910.00	913.6	0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	1.9	-0.19	1.8	0.01	1.85
THC Low	303.00	303.9	0.09	300.6	0.33	301.6	-0.10	
THC Mid	510.00	511.3	0.13	500.5	1.13	502.8	-0.28	501.4
THC High	858.00	858.3	0.03	844.7	1.37	849.1	-0.45	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1727-1827

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	559.60	0.58	559.80	-0.02	559.70
CO High	910.00	913.60	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		1.80	-0.18	1.90	-0.01	1.85
THC Low	303.00	303.90	-0.09	301.60	0.23	303.60	-0.20	
THC Mid	510.00	511.30	-0.13	502.80	0.85	504.70	-0.19	503.75
THC High	858.00	858.30	-0.03	849.10	0.92	850.90	-0.18	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	20 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.2	0.02	0.9	-0.11	0.9	0.00	0.90
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	565.4	0.07	559.6	0.58	559.8	-0.02	559.7
CO High	910.00	913.6	0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	1.8	-0.18	1.9	-0.01	1.85
THC Low	303.00	303.9	0.09	301.6	0.23	303.6	-0.26	
THC Mid	510.00	511.3	0.13	502.8	0.85	504.7	-0.19	503.75
THC High	858.00	858.3	0.03	849.1	0.92	850.9	-0.18	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1852 - 1952

DRYER STACK #6

RUN #1		THC	CO
03-20-1992	16:04	83.5	201.2
03-20-1992	16:05	82.2	202.8
03-20-1992	16:06	83.5	198.5
03-20-1992	16:07	84.9	198.2
03-20-1992	16:08	82.6	203.2
03-20-1992	16:09	83.6	195.0
03-20-1992	16:10	79.0	202.7
03-20-1992	16:11	78.0	204.5
03-20-1992	16:12	77.7	203.8
03-20-1992	16:13	76.7	201.4
03-20-1992	16:14	76.8	188.0
03-20-1992	16:15	79.6	168.2
03-20-1992	16:16	81.9	176.2
03-20-1992	16:17	84.9	191.1
03-20-1992	16:18	90.2	190.6
03-20-1992	16:19	91.6	185.4
03-20-1992	16:20	88.3	181.6
03-20-1992	16:21	86.8	187.4
03-20-1992	16:22	99.6	191.6
03-20-1992	16:23	104.5	193.0
03-20-1992	16:24	108.5	194.5
03-20-1992	16:25	111.3	197.1
03-20-1992	16:26	116.7	187.9
03-20-1992	16:27	129.7	194.9
03-20-1992	16:28	137.5	199.4
03-20-1992	16:29	143.5	193.4
03-20-1992	16:30	148.4	188.0
03-20-1992	16:31	146.0	190.2
03-20-1992	16:32	151.9	178.5
03-20-1992	16:33	146.8	161.5
03-20-1992	16:34	157.6	173.7
03-20-1992	16:35	163.0	169.6
03-20-1992	16:36	180.8	164.4
03-20-1992	16:37	164.4	168.8
03-20-1992	16:38	160.5	181.2
03-20-1992	16:39	155.7	176.2
03-20-1992	16:40	151.6	174.3
03-20-1992	16:41	151.6	170.7
03-20-1992	16:42	149.4	177.1
03-20-1992	16:43	149.6	187.9
03-20-1992	16:44	144.9	179.9
03-20-1992	16:45	136.2	181.4
03-20-1992	16:46	139.3	183.8
03-20-1992	16:47	122.6	186.1
03-20-1992	16:48	130.6	187.0
03-20-1992	16:49	134.1	187.2
03-20-1992	16:50	140.7	191.5
03-20-1992	16:51	131.1	194.3
03-20-1992	16:52	128.5	178.8
03-20-1992	16:53	127.5	161.9
03-20-1992	16:54	118.2	174.8
03-20-1992	16:55	123.3	180.1
03-20-1992	16:56	120.8	190.5
03-20-1992	16:57	120.0	191.6
03-20-1992	16:58	117.5	188.0
03-20-1992	16:59	114.4	174.7
03-20-1992	17:00	118.8	178.1
03-20-1992	17:01	124.5	180.9
03-20-1992	17:02	127.8	165.8
03-20-1992	17:03	128.9	165.1
RUN #1 AVERAGE		119.5	185.3

DRYER STACK #6

RUN #2		THC	CO
03-20-1992	17:27	115.5	213.3
03-20-1992	17:28	109.8	214.0
03-20-1992	17:29	103.7	219.8
03-20-1992	17:30	108.0	216.6
03-20-1992	17:31	107.0	212.4
03-20-1992	17:32	99.0	212.4
03-20-1992	17:33	102.4	206.2
03-20-1992	17:34	97.5	208.7
03-20-1992	17:35	100.6	200.5
03-20-1992	17:36	105.7	201.7
03-20-1992	17:37	116.4	200.7
03-20-1992	17:38	116.8	189.3
03-20-1992	17:39	111.3	168.7
03-20-1992	17:40	113.1	146.7
03-20-1992	17:41	119.4	148.0
03-20-1992	17:42	117.0	155.0
03-20-1992	17:43	124.0	165.0
03-20-1992	17:44	112.2	169.2
03-20-1992	17:45	111.3	178.5
03-20-1992	17:46	123.6	185.8
03-20-1992	17:47	122.3	175.1
03-20-1992	17:48	130.2	186.1
03-20-1992	17:49	122.9	190.6
03-20-1992	17:50	133.0	198.1
03-20-1992	17:51	136.8	192.8
03-20-1992	17:52	120.9	199.6
03-20-1992	17:53	96.6	202.9
03-20-1992	17:54	99.8	207.4
03-20-1992	17:55	95.2	202.7
03-20-1992	17:56	98.3	198.1
03-20-1992	17:57	97.5	204.7
03-20-1992	17:58	103.8	204.8
03-20-1992	17:59	110.8	189.3
03-20-1992	18:00	110.2	187.6
03-20-1992	18:01	102.7	189.1
03-20-1992	18:02	109.4	185.7
03-20-1992	18:03	107.7	193.2
03-20-1992	18:04	106.1	190.3
03-20-1992	18:05	104.7	182.9
03-20-1992	18:06	109.1	177.7
03-20-1992	18:07	106.5	185.5
03-20-1992	18:08	104.5	190.2
03-20-1992	18:09	101.6	190.8
03-20-1992	18:10	104.7	189.1
03-20-1992	18:11	116.9	185.4
03-20-1992	18:12	112.7	187.1
03-20-1992	18:13	107.2	176.9
03-20-1992	18:14	98.7	183.1
03-20-1992	18:15	87.5	187.0
03-20-1992	18:16	85.7	188.1
03-20-1992	18:17	80.7	192.8
03-20-1992	18:18	63.2	187.3
03-20-1992	18:19	57.4	186.9
03-20-1992	18:20	58.1	176.4
03-20-1992	18:21	56.3	184.3
03-20-1992	18:22	55.6	192.4
03-20-1992	18:23	57.1	186.3
03-20-1992	18:24	55.3	189.8
03-20-1992	18:25	54.3	183.2
03-20-1992	18:26	52.2	183.8
RUN #2 AVERAGE		100.8	190.0

DRYER STACK #6

RUN #3		THC	CO
03-20-1992	18:52	82.3	173.7
03-20-1992	18:53	83.1	176.3
03-20-1992	18:54	86.0	181.1
03-20-1992	18:55	90.3	189.8
03-20-1992	18:56	91.2	189.4
03-20-1992	18:57	95.1	201.9
03-20-1992	18:58	100.8	209.4
03-20-1992	18:59	104.7	203.3
03-20-1992	19:00	110.9	194.8
03-20-1992	19:01	114.4	192.1
03-20-1992	19:02	117.9	179.5
03-20-1992	19:03	120.9	187.5
03-20-1992	19:04	118.6	196.4
03-20-1992	19:05	119.8	202.1
03-20-1992	19:06	114.6	190.4
03-20-1992	19:07	112.6	190.7
03-20-1992	19:08	108.3	195.1
03-20-1992	19:09	107.1	192.2
03-20-1992	19:10	104.9	194.9
03-20-1992	19:11	102.9	192.0
03-20-1992	19:12	103.5	202.7
03-20-1992	19:13	102.5	202.8
03-20-1992	19:14	98.1	210.5
03-20-1992	19:15	93.3	210.0
03-20-1992	19:16	89.5	211.2
03-20-1992	19:17	84.7	205.0
03-20-1992	19:18	80.7	203.0
03-20-1992	19:19	79.3	199.8
03-20-1992	19:20	79.0	175.8
03-20-1992	19:21	77.0	173.7
03-20-1992	19:22	75.3	184.7
03-20-1992	19:23	74.6	199.2
03-20-1992	19:24	71.4	200.3
03-20-1992	19:25	67.9	194.9
03-20-1992	19:26	68.3	198.6
03-20-1992	19:27	68.2	199.7
03-20-1992	19:28	66.6	204.4
03-20-1992	19:29	70.2	207.4
03-20-1992	19:30	70.2	210.8
03-20-1992	19:31	73.3	208.7
03-20-1992	19:32	78.1	208.8
03-20-1992	19:33	80.6	212.9
03-20-1992	19:34	86.0	203.2
03-20-1992	19:35	89.8	206.6
03-20-1992	19:36	91.7	204.6
03-20-1992	19:37	94.9	206.5
03-20-1992	19:38	99.6	182.0
03-20-1992	19:39	108.0	175.6
03-20-1992	19:40	114.8	187.7
03-20-1992	19:41	125.7	197.4
03-20-1992	19:42	132.6	197.0
03-20-1992	19:43	136.5	193.9
03-20-1992	19:44	133.8	196.1
03-20-1992	19:45	129.8	191.7
03-20-1992	19:46	124.7	186.9
03-20-1992	19:47	121.8	177.1
03-20-1992	19:48	115.3	187.4
03-20-1992	19:49	108.8	198.1
03-20-1992	19:50	104.0	207.1
03-20-1992	19:51	103.4	200.4
RUN #3 AVERAGE		97.7	195.9

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	561.40	0.40	560.60	0.08	561.00
CO High	910.00	913.60	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.80	-0.28	2.40	0.04	2.60
THC Low	303.00	303.90	-0.09	301.90	0.20	301.20	0.07	
THC Mid	510.00	511.30	-0.13	501.80	0.95	501.40	0.04	501.60
THC High	858.00	858.30	-0.03	850.70	0.76	847.60	0.31	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	18	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-.20	0.02	.90	0.11	0.9	0.0	0.90
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	565.4	0.07	561.4	0.40	560.6	0.08	561.0
CO High	910.00	913.6	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	2.8	-0.28	2.4	0.04	2.60
THC Low	303.00	303.9	-0.09	301.9	0.20	301.2	0.07	
THC Mid	510.00	511.3	-0.13	501.8	0.95	501.4	0.04	501.6
THC High	858.00	858.3	-0.03	850.7	0.76	847.6	0.31	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

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CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	560.60	0.48	560.30	0.03	560.45
CO High	910.00	913.60	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.40	-0.24	2.10	0.03	2.25
THC Low	303.00	303.90	-0.09	301.20	0.27	301.10	0.01	
THC Mid	510.00	511.30	-0.13	501.40	0.99	499.70	0.17	500.55
THC High	858.00	858.30	-0.03	847.60	1.07	844.00	0.36	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-.12	0.02	0.9	-0.11	.9	0.0	0.9
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	565.4	0.07	560.6	0.48	560.3	0.03	560.45
CO High	910.00	913.6	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0		2.4	-0.24	2.1	0.03	2.25
THC Low	303.00	303.9	-0.09	301.2	0.27	301.1	0.01	
THC Mid	510.00	511.3	0.13	501.4	0.99	499.7	0.17	500.55
THC High	858.00	858.3	0.03	847.6	1.07	844.0	0.36	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1224-1324

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.90	0.00	0.90
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	560.30	0.51	559.10	0.12	559.70
CO High	910.00	913.60	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.10	-0.21	1.90	0.02	2.00
THC Low	303.00	303.90	-0.09	301.10	0.28	300.10	0.10	
THC Mid	510.00	511.30	-0.13	499.70	1.16	500.50	-0.08	500.10
THC High	858.00	858.30	-0.03	844.00	1.43	844.70	-0.07	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Dryer Stack	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	20 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-.2	0.02	0.9	-0.11	0.9	0.0	0.90
CO Low	302.00	303.1	-0.11					
CO Mid	566.10	565.4	0.07	560.3	0.51	559.1	0.12	559.7
CO High	910.00	913.6	-0.36					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	2.1	-0.21	1.9	0.02	2.00
THC Low	303.00	303.9	-0.09	301.1	0.28	300.1	0.10	
THC Mid	510.00	511.3	0.13	499.7	1.16	500.5	-0.08	500.1
THC High	858.00	858.3	0.03	844.0	1.43	844.7	-0.07	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

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DRYER STACK #8

RUN #1		THC	CO
03-20-1992	10:47	219.9	179.8
03-20-1992	10:48	162.9	189.2
03-20-1992	10:49	138.4	200.4
03-20-1992	10:50	119.2	208.0
03-20-1992	10:51	113.3	213.4
03-20-1992	10:52	105.6	201.8
03-20-1992	10:53	104.5	196.9
03-20-1992	10:54	105.4	206.5
03-20-1992	10:55	105.7	229.3
03-20-1992	10:56	108.3	236.6
03-20-1992	10:57	109.4	235.1
03-20-1992	10:58	112.8	229.5
03-20-1992	10:59	114.0	214.8
03-20-1992	11:00	117.2	238.6
03-20-1992	11:01	123.6	252.3
03-20-1992	11:02	127.3	253.3
03-20-1992	11:03	129.3	249.6
03-20-1992	11:04	127.4	240.1
03-20-1992	11:05	121.5	230.4
03-20-1992	11:06	111.3	231.3
03-20-1992	11:07	104.4	226.1
03-20-1992	11:08	98.6	224.7
03-20-1992	11:09	96.5	209.2
03-20-1992	11:10	92.8	218.3
03-20-1992	11:11	95.6	205.2
03-20-1992	11:12	88.2	198.5
03-20-1992	11:13	85.5	203.9
03-20-1992	11:14	85.1	202.4
03-20-1992	11:15	85.0	213.6
03-20-1992	11:16	82.3	223.4
03-20-1992	11:17	83.0	232.8
03-20-1992	11:18	86.9	231.4
03-20-1992	11:19	90.5	233.7
03-20-1992	11:20	88.3	237.3
03-20-1992	11:21	89.2	216.1
03-20-1992	11:22	89.5	216.7
03-20-1992	11:23	89.2	215.2
03-20-1992	11:24	86.1	218.7
03-20-1992	11:25	84.7	225.8
03-20-1992	11:26	87.6	229.9
03-20-1992	11:27	87.9	226.8
03-20-1992	11:28	85.0	222.4
03-20-1992	11:29	90.2	200.0
03-20-1992	11:30	93.1	220.2
03-20-1992	11:31	91.3	231.3
03-20-1992	11:32	89.1	225.3
03-20-1992	11:33	92.5	220.4
03-20-1992	11:34	93.8	221.4
03-20-1992	11:35	89.9	232.9
03-20-1992	11:36	84.2	238.2
03-20-1992	11:37	86.2	240.0
03-20-1992	11:38	91.6	231.8
03-20-1992	11:39	87.8	230.9
03-20-1992	11:40	86.2	238.2
03-20-1992	11:41	89.2	210.3
03-20-1992	11:42	90.2	200.7
03-20-1992	11:43	87.5	205.6
03-20-1992	11:44	88.4	211.6
03-20-1992	11:45	91.1	209.7
03-20-1992	11:46	94.3	204.3
RUN 1 AVERAGE		100.9	220.7

DRYER STACK #8

RUN 2		THC	CO
03-20-1992	12:25	93.9	186.9
03-20-1992	12:26	90.5	198.3
03-20-1992	12:27	92.1	202.2
03-20-1992	12:28	92.5	198.5
03-20-1992	12:29	90.0	206.9
03-20-1992	12:30	88.2	211.4
03-20-1992	12:31	88.4	207.0
03-20-1992	12:32	87.1	209.8
03-20-1992	12:33	83.4	211.1
03-20-1992	12:34	83.7	214.3
03-20-1992	12:35	81.5	215.5
03-20-1992	12:36	80.1	207.4
03-20-1992	12:37	80.9	202.4
03-20-1992	12:38	79.9	205.2
03-20-1992	12:39	78.7	207.3
03-20-1992	12:40	79.4	208.6
03-20-1992	12:41	81.9	215.9
03-20-1992	12:42	84.0	222.4
03-20-1992	12:43	87.4	223.7
03-20-1992	12:44	92.1	217.7
03-20-1992	12:45	92.8	217.9
03-20-1992	12:46	93.0	218.2
03-20-1992	12:47	94.3	220.5
03-20-1992	12:48	92.1	216.8
03-20-1992	12:49	90.5	212.8
03-20-1992	12:50	92.3	213.4
03-20-1992	12:51	91.7	212.5
03-20-1992	12:52	89.5	213.7
03-20-1992	12:53	83.6	211.8
03-20-1992	12:54	79.2	217.2
03-20-1992	12:55	76.6	199.4
03-20-1992	12:56	75.1	192.3
03-20-1992	12:57	79.0	204.4
03-20-1992	12:58	83.5	210.7
03-20-1992	12:59	88.7	202.2
03-20-1992	13:00	93.7	204.1
03-20-1992	13:01	99.0	210.2
03-20-1992	13:02	95.0	209.9
03-20-1992	13:03	87.4	209.9
03-20-1992	13:04	86.4	209.9
03-20-1992	13:05	84.4	206.1
03-20-1992	13:06	85.0	194.1
03-20-1992	13:07	86.2	197.3
03-20-1992	13:08	87.4	192.3
03-20-1992	13:09	87.5	185.0
03-20-1992	13:10	86.6	193.9
03-20-1992	13:11	85.8	197.9
03-20-1992	13:12	91.5	202.5
03-20-1992	13:13	93.8	205.7
03-20-1992	13:14	93.7	206.7
03-20-1992	13:15	100.1	195.4
03-20-1992	13:16	101.9	200.9
03-20-1992	13:17	95.2	206.1
03-20-1992	13:18	93.7	210.6
03-20-1992	13:19	92.7	216.3
03-20-1992	13:20	98.6	216.3
03-20-1992	13:21	100.9	218.8
03-20-1992	13:22	100.4	209.6
03-20-1992	13:23	99.0	209.9
03-20-1992	13:24	98.4	216.6
RUN 2 AVERAGE		89.0	207.7

DRYER STACK #8

RUN #3		THC	CO
03-20-1992	13:44	100.0	208.9
03-20-1992	13:45	99.3	195.4
03-20-1992	13:46	99.0	192.7
03-20-1992	13:47	104.9	195.0
03-20-1992	13:48	104.2	201.2
03-20-1992	13:49	106.2	200.4
03-20-1992	13:50	108.4	210.3
03-20-1992	13:51	109.6	213.0
03-20-1992	13:52	105.4	213.4
03-20-1992	13:53	104.2	210.5
03-20-1992	13:54	108.9	198.1
03-20-1992	13:55	106.8	193.8
03-20-1992	13:56	105.3	202.8
03-20-1992	13:57	107.0	209.7
03-20-1992	13:58	106.1	219.6
03-20-1992	13:59	105.2	213.5
03-20-1992	14:00	107.7	204.1
03-20-1992	14:01	110.1	205.4
03-20-1992	14:02	107.9	206.9
03-20-1992	14:03	111.5	197.8
03-20-1992	14:04	117.2	205.0
03-20-1992	14:05	118.9	210.6
03-20-1992	14:06	120.9	212.1
03-20-1992	14:07	116.8	215.1
03-20-1992	14:08	114.8	212.6
03-20-1992	14:09	112.9	213.2
03-20-1992	14:10	115.8	196.0
03-20-1992	14:11	115.6	196.4
03-20-1992	14:12	119.7	210.5
03-20-1992	14:13	117.8	223.3
03-20-1992	14:14	111.0	219.3
03-20-1992	14:15	111.1	228.9
03-20-1992	14:16	112.2	235.2
03-20-1992	14:17	110.5	237.1
03-20-1992	14:18	114.1	235.1
03-20-1992	14:19	115.1	216.8
03-20-1992	14:20	113.5	213.9
03-20-1992	14:21	115.6	222.1
03-20-1992	14:22	117.5	233.9
03-20-1992	14:23	120.0	225.4
03-20-1992	14:24	127.0	202.6
03-20-1992	14:25	127.5	222.3
03-20-1992	14:26	131.6	231.4
03-20-1992	14:27	133.7	231.5
03-20-1992	14:28	134.4	239.9
03-20-1992	14:29	135.1	242.2
03-20-1992	14:30	132.5	245.0
03-20-1992	14:31	129.7	241.7
03-20-1992	14:32	129.0	234.0
03-20-1992	14:33	128.1	237.3
03-20-1992	14:34	128.7	232.8
03-20-1992	14:35	125.7	234.1
03-20-1992	14:36	123.0	234.0
03-20-1992	14:37	118.5	227.7
03-20-1992	14:38	122.0	237.6
03-20-1992	14:39	121.0	209.3
03-20-1992	14:40	121.2	191.1
03-20-1992	14:41	117.8	216.2
03-20-1992	14:42	116.4	225.6
03-20-1992	14:43	117.1	232.5
RUN 3 AVERAGE		115.8	217.1.

PRESS VENTS

PRESS VENTS 3-11
CEMS SUMMARY
LOUISIANA PACIFIC CORPORATION

			CEM Data (Raw Data)		Calibration Data						CEM Data (Cal. Error Corrected)		Volumetric Flow		Mass Emission Rates	
	Start	Stop	CO	THC	CO			THC			CO	THC	Qa	Qs	CO	THC
Run No.	Time	Time	(ppm)	(ppm)	Cma	Co	Cm	Cma	Co	Cm	(ppm)	(ppm)	(scfm)	(dscfm)	(lb/hr)	(lb/hr)
Vent 5 1	0957	1056	4.5	11.0	600.0	0.8	595.8	49.3	0.9	50.3	3.8	10.1	54,500	53,500	0.9	3.6
2	1210	1310	3.2	11.9	600.0	0.8	593.4	49.3	1.3	50.0	2.4	10.7	57,800	56,400	0.6	4.1
3	1345	1445	3.7	10.9	600.0	0.8	595.5	49.3	2.1	49.5	2.9	9.1	59,000	57,500	0.7	3.5
Vent 4 1	1800	1900	4.4	2.8	600.0	0.8	592.7	49.3	1.4	48.7	3.7	1.5	58,300	57,200	0.9	0.6
2	0750	0850	5.6	3.9	600.0	0.9	597.4	49.3	1.1	50.2	5.0	2.8	55,000	53,900	1.2	1.0
3	0920	1020	3.7	3.6	600.0	0.8	594.4	49.3	1.1	49.8	2.9	2.5	57,800	54,700	0.7	1.0
Vent 3 1	1329	1429	3.2	3.5	600.0	0.8	596.0	49.3	1.3	49.7	2.4	2.2	60,000	57,600	0.6	0.9
2	1502	1602	4.2	3.4	600.0	0.8	596.9	49.3	1.3	50.0	3.4	2.1	59,100	54,900	0.8	0.8
3	1628	1728	4.9	3.1	600.0	0.8	595.9	49.3	1.4	50.3	4.2	1.7	57,300	55,100	1.0	0.6
Vent 11 1	1022	1122	1.1	12.7	600.0	0.3	596.7	49.3	1.2	49.9	0.8	11.6	20,300	20,000	0.1	1.5
2	1241	1341	1.5	12.1	600.0	0.9	595.5	49.3	1.2	50.1	0.6	11.0	19,300	19,100	0.0	1.4
3	1440	1540	0.9	10.6	600.0	0.9	597.7	49.3	1.8	50.7	0.0	8.9	18,300	18,200	0.0	1.1
Vent 6 1	1155	1255	2.2	10.4	566.1	0.8	596.0	510.0	1.7	496.2	1.4	9.0	40,500	39,200	0.2	2.4
2	1516	1615	1.8	7.9	566.1	0.7	564.5	510.0	2.1	487.8	1.1	6.2	37,600	36,000	0.2	1.5
3	1648	1748	1.5	6.8	566.1	0.8	564.5	510.0	1.8	487.5	0.7	5.2	38,000	36,600	0.1	1.3
Vent 7 1	0757	0857	3.4	4.3	566.1	0.9	562.9	55.2	0.5	54.9	2.5	3.9	35,400	35,900	0.4	0.9
2	0932	1032	3.5	5.7	566.1	0.8	558.2	55.2	0.7	54.6	2.7	5.2	35,300	35,100	0.4	1.2
3	1100	1200	3.3	7.9	566.1	0.8	556.7	55.2	1.3	54.6	2.5	6.8	35,100	34,700	0.4	1.6
Vent 8 1	1453	1553	3.4	6.3	566.1	1.7	565.0	55.2	2.1	55.9	1.7	4.2	45,800	45,400	0.3	1.3
2	1642	1742	3.1	6.6	566.1	1.3	561.9	55.2	2.2	56.3	1.9	4.6	47,000	46,900	0.4	1.4
3	1812	1912	3.4	5.3	566.1	0.8	559.7	55.2	1.4	56.2	2.7	4.0	40,500	40,900	0.5	1.1
Vent 9 1	0854	0954	3.2	4.7	566.1	0.9	559.4	55.2	0.8	54.6	2.4	4.0	33,000	33,000	0.3	0.9
2	1028	1128	5.8	3.2	566.1	1.3	552.4	55.2	1.2	54.2	4.7	2.1	33,200	32,600	0.7	0.5
3	1158	1258	6.3	4.6	566.1	1.7	553.4	55.2	2.2	54.3	4.7	2.5	33,700	31,800	0.7	0.6
Vent 10 1	1155	1255	2.2	10.4	566.1	0.8	551.3	55.2	1.7	53.6	1.5	9.2	39,900	38,100	0.2	2.4
2	1516	1615	1.8	7.9	566.1	0.7	549.7	55.2	2.1	52.8	1.2	6.4	39,000	36,200	0.2	1.6
3	1648	1748	1.5	6.8	566.1	0.8	550.7	55.2	1.8	52.9	0.7	5.4	37,400	36,200	0.1	1.3

CEM Reference Method Data

Client Louisiana Pacific
Source Press Vents 3, 4, 5, 6, 7, 8, 9, 10, 11
Date 03/11/92-03/17/92
Project No.1449-001

			CEM Data (Raw Data)				Calibration Data						CEM Data (Calibration Error Corrected)						Mass Emission Rates			
Run No.	Start Time	Stop Time	CO (ppm)	CO2 (%)	O2 (%)	THC (ppm)	CO Cma	Co	Cm	THC Cma	Co	Cm	CO (ppm)	CO2 (%)	O2 (%)	THC (ppm)	NOx (ppm)	SO2 (ppm)	Qa (scfm)	Qs (dscfm)	CO (lb/hr)	THC (lb/hr)
Vent 5	1 0957	1056	4.5			11.0	600.0	0.8	595.8	49.3	0.9	50.3	3.8			10.1			54,500	53,500	0.9	3.6
	2 1210	1310	3.2			11.9	600.0	0.8	593.4	49.3	1.3	50.0	2.4			10.7			57,800	56,400	0.6	4.1
	3 1345	1445	3.7			10.9	600.0	0.8	595.5	49.3	2.1	49.5	2.9			9.1			59,000	57,500	0.7	3.5
Vent 4	1 1800	1900	4.4			2.8	600.0	0.8	592.7	49.3	1.4	48.7	3.7			1.5			58,300	57,200	0.9	0.6
	2 0750	0850	5.8			3.9	600.0	0.9	597.4	49.3	1.1	50.2	5.0			2.8			55,000	53,900	1.2	1.0
	3 0920	1020	3.7			3.6	600.0	0.8	594.4	49.3	1.1	49.8	2.9			2.5			57,800	54,700	0.7	1.0
Vent 3	1 1329	1429	3.2			3.5	600.0	0.8	596.0	49.3	1.3	49.7	2.4			2.2			60,000	57,600	0.6	0.9
	2 1502	1602	4.2			3.4	600.0	0.8	596.9	49.3	1.3	50.0	3.4			2.1			59,100	54,900	0.8	0.8
	3 1628	1728	4.9			3.1	600.0	0.8	595.9	49.3	1.4	50.3	4.2			1.7			57,300	55,100	1.0	0.6
Vent 11	1 1022	1122	1.1			12.7	600.0	0.3	596.7	49.3	1.2	49.9	0.8			11.6			20,300	20,000	0.1	1.5
	2 1241	1341	1.5			12.1	600.0	0.9	595.5	49.3	1.2	50.1	0.6			11.0			19,300	19,100	0.0	1.4
	3 1440	1540	0.9			10.6	600.0	0.9	597.7	49.3	1.8	50.7	0.0			8.9			18,300	18,200	0.0	1.1
Vent 6	1 1155	1255	2.2			10.4	566.1	0.8	596.0	510.0	1.7	496.2	1.4			9.0			40,500	39,200	0.2	2.4
	2 1516	1615	1.8			7.9	566.1	0.7	564.5	510.0	2.1	487.8	1.1			6.2			37,600	36,000	0.2	1.5
	3 1648	1748	1.5			6.8	566.1	0.8	564.5	510.0	1.8	487.5	0.7			5.2			38,000	36,600	0.1	1.3
Vent 7	1 0757	0857	3.4			4.3	566.1	0.9	562.9	55.2	0.5	54.9	2.5			3.9			35,400	35,900	0.4	0.9
	2 0932	1032	3.5			5.7	566.1	0.8	558.2	55.2	0.7	54.6	2.7			5.2			35,300	35,100	0.4	1.2
	3 1100	1200	3.3			7.9	566.1	0.8	556.7	55.2	1.3	54.6	2.5			6.8			35,100	34,700	0.4	1.6
Vent 8	1 1453	1553	3.4			6.3	566.1	1.7	565.0	55.2	2.1	55.9	1.7			4.2			45,800	45,400	0.3	1.3
	2 1642	1742	3.1			6.6	566.1	1.3	561.9	55.2	2.2	56.3	1.9			4.6			47,000	46,900	0.4	1.4
	3 1812	1912	3.4			5.3	566.1	0.8	559.7	55.2	1.4	56.2	2.7			4.0			40,500	40,900	0.5	1.1
Vent 9	1 0854	0954	3.2			4.7	566.1	0.9	559.4	55.2	0.8	54.6	2.4			4.0			33,000	33,000	0.3	0.9
	2 1028	1128	5.8			3.2	566.1	1.3	552.4	55.2	1.2	54.2	4.7			2.1			33,200	32,600	0.7	0.5
	3 1158	1258	6.3			4.6	566.1	1.7	553.4	55.2	2.2	54.3	4.7			2.5			33,700	31,800	0.7	0.6
Vent 10	1 1155	1255	2.2			10.4	566.1	0.8	551.3	55.2	1.7	53.6	1.5			9.2			39,900	38,100	0.2	2.4
	2 1516	1615	1.8			7.9	566.1	0.7	549.7	55.2	2.1	52.8	1.2			6.4			39,000	36,200	0.2	1.6
	3 1648	1748	1.5			6.8	566.1	0.8	550.7	55.2	1.8	52.9	0.7			5.4			37,400	36,200	0.1	1.3

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Press Vent	Team Leader	T Thompson
Project Number	1449-001	CEM Operator	D Prater
Run Number	1	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.0	-0.30	0.03	0.80	-0.11	0.80	0.00	0.80
CO Low	302	307.10	-0.51					
CO Mid	600	599.4	0.06	595.40	0.40	596.5	-0.11	595.95
CO High	910	930.10	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	1.3	-1.30	1.2	0.10	1.25
THC Low	29.70	30.30	-0.60	31.2	-0.90	30.8	.40	
THC Mid	49.3	49.4	-0.10	49.8	-0.40	49.6	.20	49.70
THC High	85.8	86.0	0.80	84.3	0.70	83.3	1.00	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1329-1332

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.30	0.03	0.80	-0.11	0.80	0.00	0.80
CO Low	302.00	307.10	-0.51					
CO Mid	600.00	599.40	0.06	595.40	0.40	596.50	-0.11	595.95
CO High	910.00	930.10	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		1.30	-1.30	1.20	0.10	1.25
THC Low	29.70	30.30	-0.60	31.20	-0.90	30.80	0.40	
THC Mid	49.30	49.40	-0.10	49.80	-0.40	49.60	0.20	49.70
THC High	85.80	85.00	0.80	84.30	0.70	83.30	1.00	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.30	0.03	0.80	-0.11	0.80	0.00	0.80
CO Low	302.00	307.10	-0.51					
CO Mid	600.00	599.40	0.06	596.50	0.29	597.30	-0.08	596.90
CO High	910.00	930.10	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		1.20	-1.20	1.30	-0.10	1.25
THC Low	29.70	30.30	-0.60	30.80	-0.50	31.20	-0.40	
THC Mid	49.30	49.40	-0.10	49.60	-0.20	50.30	-0.70	49.95
THC High	85.80	85.00	0.80	83.30	1.70	84.50	-1.20	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

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CEM CALIBRATION DATA

Plant Name	LA PACIFIC	Plant Rep.	Billy Adams
Sampling Location	#3 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.0	-0.3	0.03	0.8	-0.11	0.8	0.0	0.80
CO Low	302.0	307.10	-0.51					
CO Mid	600.0	599.4	0.06	597.3	0.21	594.4	0.29	595.85
CO High	900.0	930.1	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	1.3	-1.30	1.5	-0.20	1.40
THC Low	29.7	30.3	-0.60	31.2	-0.90	31.4	-0.20	
THC Mid	49.3	49.4	-0.10	50.3	-0.90	50.2	0.10	50.25
THC High	85.9	85.0	-0.80	84.5	0.50	84.3	0.20	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1628 — 1730

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#3 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.30	0.03	0.80	-0.11	0.80	0.00	0.80
CO Low	302.00	307.10	-0.51					
CO Mid	600.00	599.40	0.06	597.30	0.21	594.40	0.29	595.85
CO High	910.00	930.10	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		1.30	-1.30	1.50	-0.20	1.40
THC Low	29.70	30.30	-0.60	31.20	-0.90	31.40	-0.20	
THC Mid	49.30	49.40	-0.10	50.30	-0.90	50.20	0.10	50.25
THC High	85.80	85.00	0.80	84.50	0.50	84.30	0.20	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press Vent 3

Run 1

03-12-199	13:29:00	3.54	3.70
03-12-199	13:30:00	3.62	3.70
03-12-199	13:31:00	3.46	3.70
03-12-199	13:32:00	3.43	3.70
03-12-199	13:33:00	3.35	3.70
03-12-199	13:34:00	3.54	3.36
03-12-199	13:35:00	3.32	2.70
03-12-199	13:36:00	3.53	2.70
03-12-199	13:37:00	3.43	2.70
03-12-199	13:38:00	3.44	2.70
03-12-199	13:39:00	3.65	2.70
03-12-199	13:40:00	3.51	2.87
03-12-199	13:41:00	3.47	3.70
03-12-199	13:42:00	3.64	3.70
03-12-199	13:43:00	3.63	3.53
03-12-199	13:44:00	3.64	2.70
03-12-199	13:45:00	3.56	2.70
03-12-199	13:46:00	3.67	2.70
03-12-199	13:47:00	3.48	2.70
03-12-199	13:48:00	3.51	2.70
03-12-199	13:49:00	3.50	3.04
03-12-199	13:50:00	3.45	3.70
03-12-199	13:51:00	3.66	3.70
03-12-199	13:52:00	3.42	3.70
03-12-199	13:53:00	3.43	3.70
03-12-199	13:54:00	3.58	3.70
03-12-199	13:55:00	3.74	3.70
03-12-199	13:56:00	3.47	3.70
03-12-199	13:57:00	3.32	3.70
03-12-199	13:58:00	3.35	3.70
03-12-199	13:59:00	3.53	3.70
03-12-199	14:00:00	3.28	3.70
03-12-199	14:01:00	3.16	3.70
03-12-199	14:02:00	3.31	3.70
03-12-199	14:03:00	3.48	3.70
03-12-199	14:04:01	3.45	3.70
03-12-199	14:05:01	3.38	3.70
03-12-199	14:06:00	3.27	3.70
03-12-199	14:07:01	3.29	3.69
03-12-199	14:08:00	3.50	2.70
03-12-199	14:09:01	3.63	2.70
03-12-199	14:10:01	3.65	2.70
03-12-199	14:11:00	3.54	2.70
03-12-199	14:12:01	3.49	2.70
03-12-199	14:13:01	3.64	2.70
03-12-199	14:14:01	3.81	2.70
03-12-199	14:15:01	3.57	2.70
03-12-199	14:16:01	3.29	3.56
03-12-199	14:17:01	3.44	3.70
03-12-199	14:18:01	3.60	3.70
03-12-199	14:19:01	3.52	3.70
03-12-199	14:20:01	3.36	3.17
03-12-199	14:21:01	3.23	2.70
03-12-199	14:22:01	3.26	2.70
03-12-199	14:23:01	3.26	2.70
03-12-199	14:24:01	3.10	2.70
03-12-199	14:25:01	3.18	2.70
03-12-199	14:26:01	3.27	2.70
03-12-199	14:27:01	3.30	2.38
03-12-199	14:28:01	3.17	2.58
	Avg.	3.45	3.21

Press Vent 7
Run 2

03-12-199	15:02:00	3.19	1.79
03-12-199	15:03:00	3.17	1.80
03-12-199	15:04:00	2.96	1.80
03-12-199	15:05:00	3.21	1.80
03-12-199	15:06:00	3.12	1.80
03-12-199	15:07:00	3.05	1.80
03-12-199	15:08:00	3.10	1.80
03-12-199	15:09:00	3.22	1.80
03-12-199	15:10:00	3.37	1.80
03-12-199	15:11:00	3.62	1.80
03-12-199	15:12:00	3.49	1.98
03-12-199	15:13:00	3.80	2.70
03-12-199	15:14:00	3.68	2.70
03-12-199	15:15:00	3.70	3.56
03-12-199	15:16:00	3.70	4.47
03-12-199	15:17:00	3.56	4.80
03-12-199	15:18:00	3.37	5.66
03-12-199	15:19:00	3.37	5.80
03-12-199	15:20:00	3.46	5.60
03-12-199	15:21:00	3.74	4.80
03-12-199	15:22:00	3.81	4.62
03-12-199	15:23:00	3.82	4.80
03-12-199	15:24:00	3.58	4.80
03-12-199	15:25:00	3.33	3.85
03-12-199	15:26:00	3.66	4.65
03-12-199	15:27:00	3.57	4.80
03-12-199	15:28:00	3.54	5.66
03-12-199	15:29:00	3.56	5.80
03-12-199	15:30:00	3.50	5.27
03-12-199	15:31:00	3.47	4.80
03-12-199	15:32:00	3.63	4.83
03-12-199	15:33:00	3.69	5.80
03-12-199	15:34:00	3.65	4.94
03-12-199	15:35:00	3.39	4.80
03-12-199	15:36:00	3.39	5.33
03-12-199	15:37:00	3.33	5.80
03-12-199	15:38:00	3.38	6.58
03-12-199	15:39:00	3.38	7.54
03-12-199	15:40:00	3.31	6.07
03-12-199	15:41:00	3.35	4.94
03-12-199	15:42:00	3.43	4.80
03-12-199	15:43:00	3.40	4.80
03-12-199	15:44:00	3.17	4.80
03-12-199	15:45:00	3.32	4.03
03-12-199	15:46:00	3.25	3.70
03-12-199	15:47:00	3.10	3.70
03-12-199	15:48:00	3.27	4.65
03-12-199	15:49:00	3.21	4.80
03-12-199	15:50:00	3.13	3.85
03-12-199	15:51:00	3.27	3.73
03-12-199	15:52:00	3.35	4.80
03-12-199	15:53:00	3.26	4.62
03-12-199	15:54:00	3.25	4.58
03-12-199	15:55:00	3.25	3.70
03-12-199	15:56:00	3.24	4.10
03-12-199	15:57:00	3.26	4.80
03-12-199	15:58:00	3.29	4.80
03-12-199	15:59:00	3.40	4.77
03-12-199	16:00:00	3.28	3.74
03-12-199	16:01:00	3.26	4.80
Avg		3.39	4.22

Press Vent #3
Run 3

03-12-199	16:28:01	3.54	3.70
03-12-199	16:29:00	3.40	3.92
03-12-199	16:30:00	3.40	5.35
03-12-199	16:31:01	3.38	5.80
03-12-199	16:32:00	3.60	5.74
03-12-199	16:33:01	3.40	4.74
03-12-199	16:34:01	3.10	3.70
03-12-199	16:35:01	3.05	4.68
03-12-199	16:36:01	3.05	4.80
03-12-199	16:37:01	3.06	4.80
03-12-199	16:38:01	3.06	4.80
03-12-199	16:39:01	3.02	4.80
03-12-199	16:40:01	3.02	4.80
03-12-199	16:41:01	3.08	5.52
03-12-199	16:42:01	3.05	5.41
03-12-199	16:43:01	3.04	4.19
03-12-199	16:44:01	3.19	4.13
03-12-199	16:45:01	3.15	4.80
03-12-199	16:46:01	3.21	5.46
03-12-199	16:47:01	3.17	4.80
03-12-199	16:48:01	3.17	4.80
03-12-199	16:49:01	3.08	4.80
03-12-199	16:50:01	3.05	4.80
03-12-199	16:51:01	3.06	4.25
03-12-199	16:52:01	3.12	4.80
03-12-199	16:53:00	3.26	4.80
03-12-199	16:54:01	3.35	4.80
03-12-199	16:55:01	3.45	4.96
03-12-199	16:56:00	3.33	4.80
03-12-199	16:57:01	3.26	4.80
03-12-199	16:58:00	3.20	4.19
03-12-199	16:59:00	3.20	3.76
03-12-199	17:00:01	3.18	4.80
03-12-199	17:01:00	3.01	4.80
03-12-199	17:02:00	2.91	4.80
03-12-199	17:03:01	2.87	4.80
03-12-199	17:04:00	2.98	4.80
03-12-199	17:05:00	3.04	4.80
03-12-199	17:06:00	2.96	4.80
03-12-199	17:07:00	3.05	4.80
03-12-199	17:08:00	3.11	4.80
03-12-199	17:09:00	3.01	4.80
03-12-199	17:10:00	2.94	5.19
03-12-199	17:11:00	2.92	5.80
03-12-199	17:12:00	3.03	5.80
03-12-199	17:13:00	2.99	5.80
03-12-199	17:14:00	2.92	5.80
03-12-199	17:15:00	2.88	5.24
03-12-199	17:16:00	2.92	5.69
03-12-199	17:17:00	2.91	5.80
03-12-199	17:18:00	2.99	5.80
03-12-199	17:19:00	3.01	6.25
03-12-199	17:20:00	2.88	5.80
03-12-199	17:21:00	2.88	5.74
03-12-199	17:22:00	2.98	4.80
03-12-199	17:23:00	2.92	4.37
03-12-199	17:24:00	2.80	4.13
03-12-199	17:25:00	2.87	4.80
03-12-199	17:26:00	2.86	5.14
03-12-199	17:27:00	2.96	4.96
	Avg.	3.09	4.94

No. 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Belly Adams
Sampling Location	# 4 Press Vent	Team Leader	T Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	11 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	0.0	0.0	0.8	-0.08	0.8	0.0	0.80
CO Low	302.0	305.9	-.39					
CO Mid	600.0	601.1	-0.11	596.3	0.48	589.0	0.73	592.65
CO High	910.0	921.3	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	2.1	-2.10	0.7	1.40	1.40
THC Low	29.7	30.1	-0.40	30.9	-0.80	29.3	1.60	
THC Mid	49.3	49.1	0.20	49.5	-0.40	47.9	1.60	48.70
THC High	85.8	84.5	1.30	83.0	1.50	81.1	1.90	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1800 - 1900

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#4 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	11 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.80	-0.08	0.80	0.00	0.80
CO Low	302.00	305.90	-0.39					
CO Mid	600.00	601.10	-0.11	596.30	0.48	589.00	0.73	592.65
CO High	910.00	921.30	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		2.10	-2.10	0.70	1.40	1.40
THC Low	29.70	30.10	-0.40	30.90	-0.80	29.30	1.60	
THC Mid	49.30	49.10	0.20	49.50	-0.40	47.90	1.60	48.70
THC High	85.80	84.50	1.30	83.00	1.50	81.10	1.90	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	LA Pacifics	Plant Rep.	Billy Adams
Sampling Location	#4 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	12 MAR 97

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.3	0.03	0.9	-0.12	0.8	0.01	0.85
CO Low	302	307.1	-0.51					
CO Mid	600	599.4	0.06	601.4	-0.20	593.4	0.80	597.40
CO High	910	930.1	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	0.0	1.2	-1.20	0.9	0.30	1.05
THC Low	29.70	30.3	-0.60	31.4	-1.10	30.7	0.70	
THC Mid	49.30	49.40	-0.10	50.7	-1.30	49.7	1.00	50.20
THC High	85.80	85.0	0.80	85.2	-0.20	83.8	1.40	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0950-0853

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#4 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK				
				PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.30	0.03	0.90	-0.12	0.80	0.01	0.85
CO Low	302.00	307.10	-0.51					
CO Mid	600.00	599.40	0.06	601.40	-0.20	593.40	0.80	597.40
CO High	910.00	930.10	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		1.20	-1.20	0.90	0.30	1.05
THC Low	29.70	30.30	-0.60	31.40	-1.10	30.70	0.70	
THC Mid	49.30	49.40	-0.10	50.70	-1.30	49.70	1.00	50.20
THC High	85.80	85.00	0.80	85.20	-0.20	83.80	1.40	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	LA PACIFIC	Plant Rep.	Billy ADAMS
Sampling Location	#4 PRESS VENT	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. PRATER
Run Number	3	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.3	0.03	0.80	-0.11	0.80	0.00	0.80
CO Low	302.0	307.1	-0.51					
CO Mid	600.0	599.40	0.06	593.4	0.60	595.4	-0.20	594.40
CO High	910.0	930.1	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	0.90	-0.90	1.3	-0.40	1.10
THC Low	29.7	30.3	-0.60	30.70	-0.40	31.2	-0.50	
THC Mid	49.3	49.4	-0.10	49.70	-0.30	49.8	-0.10	49.75
THC High	85.8	85.0	0.80	83.8	1.20	84.3	-0.50	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0920 -0951
0954- 1025

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#4 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	12 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.30	0.03	0.80	-0.11	0.80	0.00	0.80
CO Low	302.00	307.10	-0.51					
CO Mid	600.00	599.40	0.06	593.40	0.60	595.40	-0.20	594.40
CO High	910.00	930.10	-2.01					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		0.90	-0.90	1.30	-0.40	1.10
THC Low	29.70	30.30	-0.60	30.70	-0.40	31.20	-0.50	
THC Mid	49.30	49.40	-0.10	49.70	-0.30	49.80	-0.10	49.75
THC High	85.80	85.00	0.80	83.80	1.20	84.30	-0.50	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press Vent 4

Run 1

03-11-199 19:00:00	3.14	4.80
03-11-199 19:01:00	3.09	5.34
03-11-199 19:02:00	3.19	5.23
03-11-199 19:03:00	3.24	4.80
03-11-199 19:04:00	3.09	4.80
03-11-199 19:05:00	3.02	4.80
03-11-199 19:06:00	3.00	4.80
03-11-199 19:07:00	2.88	4.80
03-11-199 19:08:00	2.84	4.80
03-11-199 19:09:00	2.78	4.80
03-11-199 19:10:00	2.72	4.86
03-11-199 19:11:00	2.58	5.57
03-11-199 19:12:00	2.71	4.37
03-11-199 19:13:00	2.74	3.70
03-11-199 19:14:00	2.72	3.31
03-11-199 19:15:00	2.67	2.70
03-11-199 19:16:00	2.64	2.70
03-11-199 19:17:00	2.80	3.25
03-11-199 19:18:00	2.85	3.70
03-11-199 19:19:00	2.77	3.95
03-11-199 19:20:00	2.78	4.80
03-11-199 19:21:00	2.73	4.80
03-11-199 19:22:00	2.82	4.80
03-11-199 19:23:00	2.79	4.80
03-11-199 19:24:00	2.84	5.30
03-11-199 19:25:00	2.88	4.80
03-11-199 19:26:00	2.81	4.85
03-11-199 19:27:00	2.85	5.57
03-11-199 19:28:00	2.63	4.80
03-11-199 19:29:00	2.72	4.80
03-11-199 19:30:00	2.68	4.80
03-11-199 19:31:00	2.74	4.80
03-11-199 19:32:00	2.89	4.80
03-11-199 19:33:00	2.78	4.80
03-11-199 19:34:00	2.77	4.80
03-11-199 19:35:00	2.70	4.80
03-11-199 19:36:00	2.73	4.80
03-11-199 19:37:00	2.74	4.80
03-11-199 19:38:00	2.65	4.80
03-11-199 19:39:00	2.90	4.38
03-11-199 19:40:00	2.67	3.70
03-11-199 19:41:00	2.77	3.70
03-11-199 19:42:00	2.71	3.75
03-11-199 19:43:00	2.96	4.01
03-11-199 19:44:00	2.79	3.70
03-11-199 19:45:01	2.86	4.32
03-11-199 19:46:01	3.02	4.37
03-11-199 19:47:00	3.04	3.70
03-11-199 19:48:00	2.92	3.70
03-11-199 19:49:01	2.89	3.95
03-11-199 19:50:01	2.83	4.80
03-11-199 19:51:01	2.82	4.80
03-11-199 19:52:01	2.77	4.80
03-11-199 19:53:01	2.90	4.62
03-11-199 19:54:01	2.86	3.81
03-11-199 19:55:01	2.77	3.70
03-11-199 19:56:01	2.87	3.70
03-11-199 19:57:01	2.80	4.13
03-11-199 19:58:01	2.86	4.80
03-11-199 19:59:01	3.13	4.18
Avg	2.84	4.44

Press Vent 4

Run 2

	THC100 PPM	CO PPM
03-12-199 07:50:00	3.96	3.79
03-12-199 07:51:00	4.39	4.51
03-12-199 07:52:00	4.33	5.65
03-12-199 07:53:00	4.34	5.81
03-12-199 07:54:00	4.07	5.90
03-12-199 07:55:00	4.11	5.32
03-12-199 07:56:00	4.13	4.45
03-12-199 07:57:00	4.07	3.80
03-12-199 07:58:00	4.15	3.80
03-12-199 07:59:00	4.03	3.80
03-12-199 08:00:01	3.89	3.80
03-12-199 08:01:00	3.93	3.55
03-12-199 08:02:00	3.90	2.80
03-12-199 08:03:00	3.86	2.80
03-12-199 08:04:00	3.92	2.80
03-12-199 08:05:00	3.97	2.80
03-12-199 08:06:00	3.85	2.80
03-12-199 08:07:00	3.91	2.80
03-12-199 08:08:00	4.03	2.80
03-12-199 08:09:00	3.99	3.05
03-12-199 08:10:00	3.92	4.38
03-12-199 08:11:00	4.03	4.72
03-12-199 08:12:00	3.81	3.80
03-12-199 08:13:00	4.05	3.80
03-12-199 08:14:00	4.04	4.05
03-12-199 08:15:00	3.93	5.71
03-12-199 08:16:00	4.07	6.54
03-12-199 08:17:00	4.34	6.22
03-12-199 08:18:00	4.14	6.53
03-12-199 08:19:00	3.96	8.55
03-12-199 08:20:00	4.02	11.09
03-12-199 08:21:00	3.99	10.78
03-12-199 08:22:00	4.02	9.78
03-12-199 08:23:00	3.94	8.95
03-12-199 08:24:00	3.92	7.88
03-12-199 08:25:00	3.66	6.88
03-12-199 08:26:00	3.80	6.80
03-12-199 08:27:00	3.70	6.80
03-12-199 08:28:00	3.57	6.80
03-12-199 08:29:00	4.21	6.38
03-12-199 08:30:00	4.11	5.80
03-12-199 08:31:00	3.82	6.45
03-12-199 08:32:00	3.96	7.82
03-12-199 08:33:00	3.82	8.70
03-12-199 08:34:00	3.72	8.06
03-12-199 08:35:00	3.74	6.79
03-12-199 08:36:00	3.70	6.79
03-12-199 08:37:00	3.69	6.79
03-12-199 08:38:00	3.69	6.79
03-12-199 08:39:00	3.68	7.62
03-12-199 08:40:00	3.98	7.62
03-12-199 08:41:00	3.98	6.78
03-12-199 08:42:00	3.94	6.21
03-12-199 08:43:00	3.89	6.67
03-12-199 08:44:00	3.64	6.74
03-12-199 08:45:00	3.67	5.88
03-12-199 08:46:00	3.72	6.02
03-12-199 08:47:00	3.84	6.71
03-12-199 08:48:00	3.64	6.70
03-12-199 08:49:00	3.51	5.87
Avg.	3.93	5.84

Press Vent #4

Run 3

03-12-199	09:20:00	3.31	4.80
03-12-199	09:21:01	3.28	4.80
03-12-199	09:22:01	3.46	4.14
03-12-199	09:23:00	3.47	3.70
03-12-199	09:24:00	3.56	2.77
03-12-199	09:25:01	3.49	3.47
03-12-199	09:26:01	3.45	3.70
03-12-199	09:27:01	3.28	4.36
03-12-199	09:28:00	3.37	4.80
03-12-199	09:29:01	3.52	4.80
03-12-199	09:30:01	3.55	4.32
03-12-199	09:31:01	3.59	4.00
03-12-199	09:32:01	3.43	4.13
03-12-199	09:33:01	3.49	4.19
03-12-199	09:34:01	3.52	4.80
03-12-199	09:35:01	3.47	4.50
03-12-199	09:36:01	3.58	3.70
03-12-199	09:37:01	3.52	3.70
03-12-199	09:38:01	3.50	4.74
03-12-199	09:39:01	3.47	5.41
03-12-199	09:40:01	3.79	6.50
03-12-199	09:41:01	3.77	6.15
03-12-199	09:42:01	3.77	5.80
03-12-199	09:43:01	3.87	5.69
03-12-199	09:44:01	3.85	4.80
03-12-199	09:45:01	3.66	4.80
03-12-199	09:46:00	3.72	4.80
03-12-199	09:47:01	3.81	4.80
03-12-199	09:48:01	3.76	4.80
03-12-199	09:49:01	3.83	4.80
03-12-199	09:54:00	2.65	3.70
03-12-199	09:55:01	2.58	3.70
03-12-199	09:56:01	2.66	3.70
03-12-199	09:57:00	4.19	3.70
03-12-199	09:58:00	4.06	3.20
03-12-199	09:59:00	3.72	2.75
03-12-199	10:00:01	4.35	2.70
03-12-199	10:01:00	4.11	2.70
03-12-199	10:02:00	4.14	2.70
03-12-199	10:03:00	3.84	2.70
03-12-199	10:04:00	3.71	2.70
03-12-199	10:05:00	3.78	2.70
03-12-199	10:06:00	4.03	2.70
03-12-199	10:07:00	4.01	2.70
03-12-199	10:08:00	4.02	2.60
03-12-199	10:09:00	3.96	1.95
03-12-199	10:10:00	3.96	2.50
03-12-199	10:11:00	4.11	2.70
03-12-199	10:12:00	4.06	2.70
03-12-199	10:13:00	4.14	2.70
03-12-199	10:14:00	4.24	2.15
03-12-199	10:15:00	4.19	2.50
03-12-199	10:16:00	4.18	2.40
03-12-199	10:17:00	4.04	2.70
03-12-199	10:18:00	4.24	2.70
03-12-199	10:19:00	2.63	2.40
03-12-199	10:20:00	1.12	2.25
03-12-199	10:21:00	1.26	2.70
03-12-199	10:22:00	2.00	2.70
03-12-199	10:23:00	4.67	2.14
	Avg -	3.60	3.67

CEM CALIBRATION DATA

Plant Name	LA PACEFEC	Plant Rep.	Billy Adams
Sampling Location	#5 Press vent	Team Leader	T Thompson
Project Number	1449-001	CEM Operator	S. PRATER
Run Number	1	Date	11 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero								
CO Low								
CO Mid								
CO High								
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	1.1	-1.1	0.6	.50	.85
THC Low	29.7	30.1	~~-0.04~~ 0.4	30.8	-0.7	31.8	-1.00	
THC Mid	49.3	49.1	0.2	50.1	-1	50.5	-.40	50.30
THC High	85.8	84.5	1.3	84.3	0.2	83.8	0.50	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0957 1110-

~~1210~~

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#5 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	11 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.70	-0.07	0.80	-0.01	0.75
CO Low	302.00	305.90	-0.39					
CO Mid	600.00	601.10	-0.11	599.40	0.17	592.10	0.73	595.75
CO High	910.00	921.30	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		1.10	-1.10	0.60	0.50	0.85
THC Low	29.70	30.10	-0.40	30.80	-0.70	31.80	-1.00	
THC Mid	49.30	49.10	0.20	50.10	-1.00	50.50	-0.40	50.30
THC High	85.80	84.50	1.30	84.30	0.20	83.80	0.50	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	LA PACIFIC	Plant Rep.	
Sampling Location	#5 Press Vent	Team Leader	J. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	11 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	0.0	0.0	0.7	-0.07	0.8	-0.01	0.75
CO Low	302	305.9	-0.39					
CO Mid	600	601.1	-0.11	599.4	0.17	592.1	~~1.12~~ 0.73	595
CO High	910	921.3	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.2	-0.02	0.4	-0.02	0		
THC Low	303	303.7	-0.07	304.6	-0.09			
THC Mid	510	509.6	0.04	508.2	0.14			
THC High	858	860.0	-0.2	858.2	0.18			
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0957 - 1110

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#5 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	11 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	0.0	0.0	0.8	-0.08	0.8	0.00	0.80
CO Low	302	305.9	-0.39					
CO Mid	600	601.1	-0.11	592.1	0.90	594.6	-0.25	593.35
CO High	910	921.3	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	0.6	-.60	2.0	-1.40	1.30
THC Low	29.7	30.1	-0.4	31.8	-1.70	31.0	0.80	
THC Mid	49.3	49.1	0.2	50.5	-1.40	49.5	1.00	50.00
THC High	85.8	84.5	1.3	85.8	0.70	83.1	0.70	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1210 - 1315

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#5 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	11 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.80	-0.08	0.80	0.00	0.80
CO Low	302.00	305.90	-0.39					
CO Mid	600.00	601.10	-0.11	592.10	0.90	594.60	-0.25	593.35
CO High	910.00	921.30	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		0.60	-0.60	2.00	-1.40	1.30
THC Low	29.70	30.10	-0.40	31.80	-1.70	31.00	0.80	
THC Mid	49.30	49.10	0.20	50.50	-1.40	49.50	1.00	50.00
THC High	85.80	84.50	1.30	83.80	0.70	83.10	0.70	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Betty Adams
Sampling Location	#5 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Drager
Run Number	3	Date	11 mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	0.0	0.0	0.80	-0.08	0.8	0.00	0.80
CO Low	302.0	305.9	-0.39					
CO Mid	600.0	601.1	-0.11	594.6	0.65	596.3	-0.17	595.45
CO High	910.0	921.3	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	2.00	-2.0	2.1	-0.10	2.05
THC Low	29.7	30.10	-0.40	31.00	-0.90	30.9	0.10	
THC Mid	49.3	49.1	0.20	49.50	-0.40	49.5	0.00	49.50
THC High	85.8	84.5	1.30	83.10	1.40	83.0	0.10	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1345 - 1247

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#5 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	11 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	0.00		0.80	-0.08	0.80	0.00	0.80
CO Low	302.00	305.90	-0.39					
CO Mid	600.00	601.10	-0.11	594.60	0.65	596.30	-0.17	595.45
CO High	910.00	921.30	-1.13					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.00		2.00	-2.00	2.10	-0.10	2.05
THC Low	29.70	30.10	-0.40	31.00	-0.90	30.90	0.10	
THC Mid	49.30	49.10	0.20	49.50	-0.40	49.50	0.00	49.50
THC High	85.80	84.50	1.30	83.10	1.40	83.00	0.10	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press VenT # 5

Run 1	THC PPM	CO PPM
03-11-199 10:57:00	11.09	4.90
03-11-199 10:58:00	11.52	4.70
03-11-199 10:59:00	11.19	4.15
03-11-199 11:00:01	11.07	4.89
03-11-199 11:01:00	11.20	4.87
03-11-199 11:02:00	10.84	4.85
03-11-199 11:03:00	8.80	3.82
03-11-199 11:04:00	10.93	3.80
03-11-199 11:05:00	10.83	3.80
03-11-199 11:06:00	11.79	4.30
03-11-199 11:07:00	10.16	4.28
03-11-199 11:08:00	10.76	4.80
03-11-199 11:09:00	10.54	4.80
03-11-199 11:10:00	10.26	4.80
03-11-199 11:11:00	10.61	4.80
03-11-199 11:12:00	11.74	4.80
03-11-199 11:13:00	10.25	4.95
03-11-199 11:14:00	10.16	5.80
03-11-199 11:15:00	10.27	4.99
03-11-199 11:16:00	11.14	4.80
03-11-199 11:17:00	10.23	5.14
03-11-199 11:18:00	11.01	4.80
03-11-199 11:19:00	11.52	4.95
03-11-199 11:20:00	11.44	4.82
03-11-199 11:21:00	10.89	4.80
03-11-199 11:22:00	11.88	4.49
03-11-199 11:23:00	11.82	3.80
03-11-199 11:24:00	11.14	3.80
03-11-199 11:25:00	11.91	4.12
03-11-199 11:26:00	12.10	4.80
03-11-199 11:27:00	11.48	4.80
03-11-199 11:28:00	11.65	4.32
03-11-199 11:29:00	10.64	3.80
03-11-199 11:30:00	11.46	3.80
03-11-199 11:31:00	9.36	3.95
03-11-199 11:32:00	10.43	4.33
03-11-199 11:33:00	10.62	4.28
03-11-199 11:34:00	11.15	4.80
03-11-199 11:35:00	10.56	4.80
03-11-199 11:36:00	10.05	4.15
03-11-199 11:37:00	11.15	3.94
03-11-199 11:38:00	9.77	4.80
03-11-199 11:39:00	10.93	3.82
03-11-199 11:40:00	11.06	4.78
03-11-199 11:41:00	10.32	4.32
03-11-199 11:42:00	10.76	3.80
03-11-199 11:43:00	11.65	4.78
03-11-199 11:44:00	10.95	4.80
03-11-199 11:45:00	10.86	4.80
03-11-199 11:46:00	10.72	4.48
03-11-199 11:47:00	11.42	4.13
03-11-199 11:48:00	10.97	4.61
03-11-199 11:49:00	11.90	4.80
03-11-199 11:50:00	11.39	4.80
03-11-199 11:51:00	11.08	4.80
03-11-199 11:52:00	11.48	4.80
03-11-199 11:53:00	11.65	4.80
03-11-199 11:54:00	11.81	4.80
03-11-199 11:55:00	11.51	4.80
03-11-199 11:56:00	11.05	3.81
Avg	10.98	4.53

Press Vent #5
Run 2

03-11-199 13:10:00	11.55	2.80
03-11-199 13:11:00	11.49	2.60
03-11-199 13:12:00	10.86	2.13
03-11-199 13:13:00	11.92	1.97
03-11-199 13:14:00	11.96	2.79
03-11-199 13:15:00	12.12	2.78
03-11-199 13:16:00	11.82	2.78
03-11-199 13:17:00	11.98	2.78
03-11-199 13:18:00	11.85	2.78
03-11-199 13:19:00	11.55	2.74
03-11-199 13:20:00	11.63	2.72
03-11-199 13:21:00	11.15	2.70
03-11-199 13:22:00	11.47	2.70
03-11-199 13:23:00	12.21	2.70
03-11-199 13:24:00	11.93	2.70
03-11-199 13:25:00	11.41	2.70
03-11-199 13:26:00	12.32	2.72
03-11-199 13:27:00	11.15	3.70
03-11-199 13:28:00	10.96	3.70
03-11-199 13:29:00	12.06	3.70
03-11-199 13:30:00	11.74	3.70
03-11-199 13:31:00	11.88	3.70
03-11-199 13:32:00	11.85	3.70
03-11-199 13:33:00	12.40	3.70
03-11-199 13:34:00	11.74	3.70
03-11-199 13:35:00	12.05	3.70
03-11-199 13:36:00	11.24	3.70
03-11-199 13:37:00	11.54	3.70
03-11-199 13:38:00	12.05	3.70
03-11-199 13:39:00	11.79	3.70
03-11-199 13:40:00	12.17	3.70
03-11-199 13:41:00	11.65	3.70
03-11-199 13:42:00	12.32	3.35
03-11-199 13:43:00	12.43	2.70
03-11-199 13:44:00	12.64	2.70
03-11-199 13:45:00	11.26	3.38
03-11-199 13:46:00	11.64	3.70
03-11-199 13:47:00	12.33	3.70
03-11-199 13:48:00	12.57	3.70
03-11-199 13:49:00	12.19	3.70
03-11-199 13:50:00	11.97	3.70
03-11-199 13:51:00	12.27	2.86
03-11-199 13:52:00	12.59	2.72
03-11-199 13:53:00	12.74	2.71
03-11-199 13:54:00	11.62	2.89
03-11-199 13:55:00	11.90	2.70
03-11-199 13:56:00	11.63	2.71
03-11-199 13:57:00	11.75	2.70
03-11-199 13:58:00	11.60	2.89
03-11-199 13:59:00	12.23	4.09
03-11-199 14:00:00	12.07	4.80
03-11-199 14:01:00	12.17	4.80
03-11-199 14:02:00	12.35	4.05
03-11-199 14:03:00	12.35	3.70
03-11-199 14:04:00	12.01	3.18
03-11-199 14:05:00	12.68	2.70
03-11-199 14:06:00	11.66	2.70
03-11-199 14:07:00	11.71	2.70
03-11-199 14:08:00	12.05	2.70
03-11-199 14:09:00	12.01	2.70
Avg.	11.90	3.19

Press Vent #5
Run #3

03-11-199	14:45:00	11.03	3.70
03-11-199	14:46:00	10.42	3.70
03-11-199	14:47:00	10.59	3.70
03-11-199	14:48:00	11.43	3.74
03-11-199	14:49:00	10.97	4.59
03-11-199	14:50:00	10.62	3.70
03-11-199	14:51:00	10.39	3.70
03-11-199	14:52:00	9.96	3.70
03-11-199	14:53:00	9.86	3.70
03-11-199	14:54:00	10.83	3.70
03-11-199	14:55:00	11.06	3.70
03-11-199	14:56:00	10.17	3.70
03-11-199	14:57:00	10.61	3.70
03-11-199	14:58:00	10.97	3.70
03-11-199	14:59:01	10.51	3.70
03-11-199	15:00:00	10.70	3.70
03-11-199	15:01:00	10.98	3.70
03-11-199	15:02:01	11.37	3.70
03-11-199	15:03:01	10.57	3.70
03-11-199	15:04:01	10.39	3.70
03-11-199	15:05:01	11.29	3.70
03-11-199	15:06:01	11.60	3.70
03-11-199	15:07:01	11.80	3.32
03-11-199	15:08:01	11.21	2.70
03-11-199	15:09:01	11.05	1.91
03-11-199	15:10:01	11.22	1.80
03-11-199	15:11:01	10.93	1.80
03-11-199	15:12:01	10.34	1.80
03-11-199	15:13:01	11.13	2.15
03-11-199	15:14:01	11.45	3.43
03-11-199	15:15:01	11.38	3.70
03-11-199	15:16:01	11.26	4.50
03-11-199	15:17:01	10.53	3.83
03-11-199	15:18:01	10.88	3.76
03-11-199	15:19:01	11.00	4.02
03-11-199	15:20:01	11.04	4.32
03-11-199	15:21:00	10.21	3.86
03-11-199	15:22:01	10.77	4.13
03-11-199	15:23:01	10.74	4.80
03-11-199	15:24:01	10.34	4.80
03-11-199	15:25:01	9.91	4.80
03-11-199	15:26:00	10.69	4.80
03-11-199	15:27:01	10.43	4.80
03-11-199	15:28:00	10.29	4.80
03-11-199	15:29:00	10.57	4.02
03-11-199	15:30:00	10.60	3.72
03-11-199	15:31:00	11.32	3.66
03-11-199	15:32:00	10.29	3.30
03-11-199	15:33:00	10.63	3.70
03-11-199	15:34:00	11.28	3.70
03-11-199	15:35:00	11.42	3.70
03-11-199	15:36:00	11.18	3.70
03-11-199	15:37:00	10.79	3.70
03-11-199	15:38:00	11.09	3.70
03-11-199	15:39:00	11.85	3.70
03-11-199	15:40:00	11.93	3.70
03-11-199	15:41:00	10.88	3.70
03-11-199	15:42:00	10.99	3.70
03-11-199	15:43:00	11.60	3.55
03-11-199	15:44:00	10.83	3.70
	Avg	10.87	3.68

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Press Vent	Team Leader	T. Thompson
Project Number	1419-001	CEM Operator	D. Prater
Run Number	1	Date	14 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.2	-0.02	0.8	-.10	0.7	0.01	0.75
CO Low	302	303.1	-0.11					
CO Mid	566.1	565.4	0.07	566.4	-.10	565.5	0.09	565.95
CO High	910	914.6	-0.46					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	1.3	0.13	2.1	-0.08	1.70
THC Low	303	304.8	-0.18	301.6	0.32	295.5	0.61	
THC Mid	510	509.6	0.04	502.4	0.72	490.0	1.24	496.20
THC High	858	858.4	-0.04	846.8	1.16	827.3	1.85	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1155 - 1205

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	14 ~~13~~ MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.80	-0.10	0.70	0.01	0.75
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	566.40	-0.10	565.50	0.09	565.95
CO High	910.00	914.60	-0.46					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		1.30	-0.13	2.10	-0.08	1.70
THC Low	303.00	304.80	-0.18	301.60	0.32	295.50	0.61	
THC Mid	510.00	509.60	0.04	502.40	0.72	490.00	1.24	496.20
THC High	858.00	858.40	-0.04	845.80	1.26	827.30	1.85	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	14 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.2	0.02	0.70	-0.09	.70	0.00	0.70
CO Low	302	303.1	-0.11					
CO Mid	566.1	565.4	0.07	565.5	0.01	563.4	0.21	564.45
CO High	910	914.6	-0.46					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	2.10	-0.21	2.0	0.01	2.05
THC Low	303	304.8	-0.18	295.5	.93	291.9	0.36	
THC Mid	510	509.6	0.04	490	1.96	485.5	0.45	487.75
THC High	858	858.4	-0.04	827.3	3.11	816.3	0.90	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1516 - 1616

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	14 ~~13~~ MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.70	-0.09	0.70	0.00	0.70
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	565.50	-0.01	563.40	0.21	564.45
CO High	910.00	914.60	-0.46					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.10	-0.21	2.00	0.01	2.05
THC Low	303.00	304.80	-0.18	295.50	0.93	291.90	0.36	
THC Mid	510.00	509.60	0.04	490.00	1.96	485.50	0.45	487.75
THC High	858.00	858.40	-0.04	827.30	3.11	818.30	0.90	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

*

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	# Press Vent	Team Leader	T. Thompson
Project Number		CEM Operator	D. Prater
Run Number		Date	MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.2	0.02	0.70	0.09	0.80	0.01	0.75
CO Low	302.0	303.1	-0.11					
CO Mid	566.1	565.4	0.07	563.4	0.20	564.3	-0.09	563.85
CO High	910.0	914.6	-0.46					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.0	0.0	2.0	-0.20	1.6	0.04	1.80
THC Low	303.0	304.8	-0.18	291.9	1.29	292.8	-0.09	
THC Mid	510.0	509.6	0.04	485.5	2.41	489.5	-0.40	487.50
THC High	868.0	858.4	-0.04	818.3	4.01	825.0	-0.67	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

16-48 -174 B

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#6 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	14 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Calibration Correction Factor Co/Cm
CO Zero	0.00	-0.20	0.02	0.70	-0.09	0.80	-0.01	0.75
CO Low	302.00	303.10	-0.11					
CO Mid	566.10	565.40	0.07	563.40	0.20	564.30	-0.09	563.85
CO High	910.00	914.60	-0.46					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.00		2.00	-0.20	1.60	0.04	1.80
THC Low	303.00	304.80	-0.18	291.90	1.29	292.80	-0.09	
THC Mid	510.00	509.60	0.04	485.50	2.41	489.50	-0.40	487.50
THC High	858.00	858.40	-0.04	818.30	4.01	825.00	-0.67	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

PRESS VENT #6

RUN #1		THC PPM	CO PPM
03-14-1992	11:55:02	24.59	2.60
03-14-1992	11:56:01	13.01	3.11
03-14-1992	11:57:01	6.45	1.99
03-14-1992	11:58:01	5.22	1.03
03-14-1992	11:59:01	4.75	2.16
03-14-1992	12:00:01	5.43	3.44
03-14-1992	12:01:00	9.80	2.44
03-14-1992	12:02:00	18.03	1.70
03-14-1992	12:03:00	23.30	2.32
03-14-1992	12:04:00	7.70	2.60
03-14-1992	12:05:00	5.63	3.28
03-14-1992	12:06:00	4.97	3.60
03-14-1992	12:07:00	4.92	2.77
03-14-1992	12:08:00	8.27	3.60
03-14-1992	12:09:00	12.40	3.60
03-14-1992	12:10:00	28.75	3.60
03-14-1992	12:11:00	12.07	3.60
03-14-1992	12:12:00	6.19	3.27
03-14-1992	12:13:00	5.17	3.60
03-14-1992	12:14:00	4.79	2.73
03-14-1992	12:15:00	5.64	1.70
03-14-1992	12:16:00	11.09	1.70
03-14-1992	12:17:00	20.65	1.70
03-14-1992	12:18:00	21.74	1.70
03-14-1992	12:19:00	7.64	1.17
03-14-1992	12:20:00	5.65	0.70
03-14-1992	12:21:00	4.90	0.72
03-14-1992	12:22:00	4.83	1.70
03-14-1992	12:23:00	7.80	1.70
03-14-1992	12:24:00	12.23	2.21
03-14-1992	12:25:00	28.28	2.17
03-14-1992	12:26:00	10.08	1.70
03-14-1992	12:27:00	6.24	1.70
03-14-1992	12:28:00	5.32	1.70
03-14-1992	12:29:00	4.82	1.70
03-14-1992	12:30:00	6.42	3.06
03-14-1992	12:31:00	11.92	3.70
03-14-1992	12:32:00	23.25	3.70
03-14-1992	12:33:00	18.55	3.62
03-14-1992	12:34:00	6.65	2.18
03-14-1992	12:35:00	5.39	1.70
03-14-1992	12:36:00	4.85	1.53
03-14-1992	12:37:00	4.78	1.70
03-14-1992	12:38:00	8.81	1.70
03-14-1992	12:39:00	12.76	1.70
03-14-1992	12:40:00	26.38	1.70
03-14-1992	12:41:00	9.15	1.18
03-14-1992	12:42:00	5.81	0.70
03-14-1992	12:43:00	5.02	0.70
03-14-1992	12:44:00	4.66	0.70
03-14-1992	12:45:00	5.82	0.72
03-14-1992	12:46:00	9.63	1.70
03-14-1992	12:47:00	23.24	1.70
03-14-1992	12:48:00	15.78	1.72
03-14-1992	12:49:00	6.48	2.70
03-14-1992	12:50:00	5.33	2.70
03-14-1992	12:51:00	4.75	3.39
03-14-1992	12:52:00	5.11	3.34
03-14-1992	12:53:00	9.54	2.01
03-14-1992	12:54:00	14.51	1.72
RUN #1 AVERAGE		10.38	2.20

PRESS VENT #6

RUN #2

03-14-1992	15:16:00	4.27	1.69
03-14-1992	15:17:00	6.27	1.70
03-14-1992	15:18:00	11.37	2.41
03-14-1992	15:19:00	15.16	3.48
03-14-1992	15:20:00	6.76	3.93
03-14-1992	15:21:00	4.84	2.70
03-14-1992	15:22:00	4.27	2.70
03-14-1992	15:23:00	3.06	3.36
03-14-1992	15:24:00	5.05	2.31
03-14-1992	15:25:00	7.34	1.70
03-14-1992	15:26:00	15.80	1.70
03-14-1992	15:27:00	12.72	2.14
03-14-1992	15:28:00	6.07	3.86
03-14-1992	15:29:00	5.06	2.81
03-14-1992	15:30:00	4.63	2.70
03-14-1992	15:31:00	4.43	2.64
03-14-1992	15:32:00	5.95	1.91
03-14-1992	15:33:00	7.41	2.70
03-14-1992	15:34:00	18.16	2.14
03-14-1992	15:35:00	11.59	1.70
03-14-1992	15:36:00	6.80	1.70
03-14-1992	15:37:00	5.26	1.70
03-14-1992	15:38:00	4.76	1.70
03-14-1992	15:39:00	4.53	1.70
03-14-1992	15:40:00	4.88	1.70
03-14-1992	15:41:00	6.72	1.70
03-14-1992	15:42:00	12.09	1.70
03-14-1992	15:43:00	16.07	1.70
03-14-1992	15:44:00	7.33	1.70
03-14-1992	15:45:00	5.37	1.32
03-14-1992	15:46:00	4.76	0.70
03-14-1992	15:47:00	4.59	0.70
03-14-1992	15:48:00	5.32	1.43
03-14-1992	15:49:00	7.78	2.20
03-14-1992	15:50:00	13.69	2.60
03-14-1992	15:51:00	17.94	2.60
03-14-1992	15:52:00	7.14	2.45
03-14-1992	15:53:00	5.46	2.41
03-14-1992	15:54:00	4.82	1.70
03-14-1992	15:55:00	4.42	1.70
03-14-1992	15:56:00	5.22	1.70
03-14-1992	15:57:00	7.08	1.70
03-14-1992	15:58:00	15.26	1.70
03-14-1992	15:59:00	13.33	0.82
03-14-1992	16:00:00	6.11	0.70
03-14-1992	16:01:00	4.98	0.92
03-14-1992	16:02:00	4.48	1.37
03-14-1992	16:03:00	4.30	1.70
03-14-1992	16:04:00	5.59	1.70
03-14-1992	16:05:00	7.93	1.21
03-14-1992	16:06:00	18.10	1.70
03-14-1992	16:07:00	9.67	1.31
03-14-1992	16:08:00	5.62	0.70
03-14-1992	16:09:00	4.72	0.70
03-14-1992	16:10:00	4.42	0.70
03-14-1992	16:11:00	4.61	0.70
03-14-1992	16:12:00	7.34	0.70
03-14-1992	16:13:01	10.64	1.44
03-14-1992	16:14:00	19.57	1.46
03-14-1992	16:15:01	7.42	0.70

RUN #2 AVERAGE 7.94 1.82

PRESS VENT #6

RUN #3

03-14-1992	16:48:00	4.33	0.70
03-14-1992	16:49:00	4.80	0.70
03-14-1992	16:50:00	6.99	0.94
03-14-1992	16:51:00	12.36	1.70
03-14-1992	16:52:00	15.11	1.77
03-14-1992	16:53:00	6.07	2.39
03-14-1992	16:54:00	4.82	1.70
03-14-1992	16:55:00	4.28	1.70
03-14-1992	16:56:00	4.14	1.63
03-14-1992	16:57:00	5.89	1.98
03-14-1992	16:58:00	7.72	2.23
03-14-1992	16:59:00	16.97	1.70
03-14-1992	17:00:01	7.13	1.70
03-14-1992	17:01:00	5.04	0.80
03-14-1992	17:02:00	4.50	0.70
03-14-1992	17:03:00	4.13	0.70
03-14-1992	17:04:00	4.72	1.61
03-14-1992	17:05:00	6.11	1.70
03-14-1992	17:06:00	16.41	0.79
03-14-1992	17:07:00	7.75	0.70
03-14-1992	17:08:00	5.00	0.70
03-14-1992	17:09:00	4.30	0.78
03-14-1992	17:10:00	3.95	1.70
03-14-1992	17:11:00	4.27	1.70
03-14-1992	17:12:00	6.09	1.63
03-14-1992	17:13:00	15.73	0.78
03-14-1992	17:14:00	9.86	2.27
03-14-1992	17:15:00	5.55	1.80
03-14-1992	17:16:00	4.57	1.70
03-14-1992	17:17:00	3.95	0.96
03-14-1992	17:18:00	3.84	0.70
03-14-1992	17:19:00	5.33	0.70
03-14-1992	17:20:00	7.72	0.70
03-14-1992	17:21:00	16.97	0.70
03-14-1992	17:22:00	6.78	0.70
03-14-1992	17:23:00	4.80	1.60
03-14-1992	17:24:00	4.16	2.27
03-14-1992	17:25:00	3.84	2.70
03-14-1992	17:26:00	4.24	2.70
03-14-1992	17:27:00	5.06	2.70
03-14-1992	17:28:00	12.53	2.70
03-14-1992	17:29:00	12.19	2.29
03-14-1992	17:30:00	6.44	1.70
03-14-1992	17:31:00	4.37	1.70
03-14-1992	17:32:00	3.95	1.76
03-14-1992	17:33:00	3.69	2.69
03-14-1992	17:34:00	3.80	2.63
03-14-1992	17:35:00	4.86	2.37
03-14-1992	17:36:00	5.95	1.70
03-14-1992	17:37:00	15.72	0.97
03-14-1992	17:38:00	6.53	0.70
03-14-1992	17:39:00	4.45	0.70
03-14-1992	17:40:00	3.76	0.70
03-14-1992	17:41:00	3.57	1.28
03-14-1992	17:42:00	4.21	1.70
03-14-1992	17:43:00	5.14	1.73
03-14-1992	17:44:00	11.64	1.04
03-14-1992	17:45:00	10.62	0.80
03-14-1992	17:46:00	5.04	0.80
03-14-1992	17:47:00	3.95	0.80

RUN #3 AVERAGE 6.79 1.47

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#7 Press Vent	Team Leader	T. Thompson
Project Number	1649-001	CEM Operator	D. Prater
Run Number	1	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.2	0.02	.9	-0.11	0.8		0.85
CO Low	302.0	309.2	-0.12					
CO Mid	566.1	565.5	0.06	565.5	0.00	560.3		562.90
CO High	910.0	920.7	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	-0.1	0.10	.5	-0.60	0.5	0.00	0.50
THC Low	29.7	28.6	1.10	28.9	-0.30	28.4	0.50	
THC Mid	55.2	55.3	-0.10	55.1	0.20	54.7	0.40	54.90
THC High	85.8	80.7	5.10	80.0	0.70	79.2	0.80	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0959-0867

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#7 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.80	0.01	0.85
CO Low	302.00	303.20	-0.12					
CO Mid	566.10	565.50	0.06	565.50	0.00	560.30	0.52	562.90
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	-0.10	0.10	0.50	-0.60	0.50	0.00	0.50
THC Low	29.70	28.60	1.10	28.90	-0.30	28.40	0.50	
THC Mid	55.20	55.30	-0.10	55.10	0.20	54.70	0.40	54.90
THC High	85.80	80.70	5.10	80.00	0.70	79.20	0.80	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	# 7 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.2	0.2	0.8	-0.10	0.8	0.0	0.80
CO Low	302.0	303.2	-0.12					
CO Mid	566.1	565.5	0.06	560.3	0.52	556.0	0.43	558.15
CO High	910.0	920.7	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.1	0.10	0.5	-0.60	0.8	-0.30	0.65
THC Low	29.7	28.6	1.10	28.4	0.20	28.6	-0.20	
THC Mid	55.2	55.3	-0.10	54.7	0.60	54.4	0.30	54.55
THC High	85.8	80.7	5.10	79.2	1.50	78.3	0.90	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0932 - 1032

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#7 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK				
				PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.20	0.02	0.80	-0.10	0.80	0.00	0.80
CO Low	302.00	303.20	-0.12					
CO Mid	566.10	565.50	0.06	560.30	0.52	556.00	0.43	558.15
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	-0.10	0.10	0.50	-0.60	0.80	-0.30	0.65
THC Low	29.70	28.60	1.10	28.40	0.20	28.60	-0.20	
THC Mid	55.20	55.30	-0.10	54.70	0.60	54.40	0.30	54.55
THC High	85.80	80.70	5.10	79.20	1.50	78.30	0.90	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	# 7 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.2	0.02	68	-0.10	0.8	0.00	0.80
CO Low	302	303.2	-0.12					
CO Mid	566.1	565.5	0.06	556.0	0.95	557.3	-0.13	556.65
CO High	910.0	920.7	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.1	0.10	0.40	-0.90	1.8	-1.00	1.30
THC Low	29.7	28.6	1.10	28.6	0.00	29.4	-0.80	
THC Mid	55.2	55.3	-0.10	54.4	0.90	54.8	-0.40	54.60
THC High	85.8	80.7	5.10	78.3	2.40	79.0	-0.70	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1100-1200

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#7 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.80	-0.10	0.80	0.00	0.80
CO Low	302.00	303.20	-0.12					
CO Mid	566.10	565.50	0.06	556.00	0.95	557.30	-0.13	556.65
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	-0.10	0.10	0.80	-0.90	1.80	-1.00	1.30
THC Low	29.70	28.60	1.10	28.60	0.00	29.40	-0.80	
THC Mid	55.20	55.30	-0.10	54.40	0.90	54.80	-0.40	54.60
THC High	85.80	80.70	5.10	78.30	2.40	79.00	-0.70	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press Vent #7

Run 1	THC100 PPM	CO PPM
03-16-199 07:57:49	5.62	3.80
03-16-199 07:58:01	7.42	3.80
03-16-199 07:59:01	14.45	3.80
03-16-199 08:00:01	7.82	3.80
03-16-199 08:01:01	4.14	2.86
03-16-199 08:02:01	3.05	2.80
03-16-199 08:03:01	2.61	2.80
03-16-199 08:04:01	2.35	2.80
03-16-199 08:05:01	2.20	2.91
03-16-199 08:06:00	2.12	3.80
03-16-199 08:07:01	2.10	3.03
03-16-199 08:08:01	2.14	3.08
03-16-199 08:09:01	2.61	3.80
03-16-199 08:10:01	5.29	3.02
03-16-199 08:11:00	9.86	2.10
03-16-199 08:12:00	12.16	3.37
03-16-199 08:13:01	4.97	3.02
03-16-199 08:14:00	3.38	2.80
03-16-199 08:15:00	2.76	2.10
03-16-199 08:16:00	2.48	2.15
03-16-199 08:17:00	2.21	2.40
03-16-199 08:18:00	2.07	1.90
03-16-199 08:19:00	2.04	2.60
03-16-199 08:20:00	2.06	2.54
03-16-199 08:21:00	2.21	1.90
03-16-199 08:22:00	3.63	2.01
03-16-199 08:23:00	6.79	2.80
03-16-199 08:24:00	13.74	2.65
03-16-199 08:25:00	7.78	2.97
03-16-199 08:26:00	3.85	2.80
03-16-199 08:27:00	2.87	2.80
03-16-199 08:28:00	2.62	2.80
03-16-199 08:29:00	2.39	2.80
03-16-199 08:30:00	2.22	2.80
03-16-199 08:31:00	2.13	3.42
03-16-199 08:32:00	2.14	4.84
03-16-199 08:33:00	2.16	4.90
03-16-199 08:34:00	2.47	5.31
03-16-199 08:35:00	4.83	4.94
03-16-199 08:36:00	9.16	5.60
03-16-199 08:37:00	11.89	5.87
03-16-199 08:38:00	4.79	4.86
03-16-199 08:39:00	3.30	4.83
03-16-199 08:40:00	2.71	4.81
03-16-199 08:41:00	2.45	5.70
03-16-199 08:42:00	2.19	4.94
03-16-199 08:43:00	2.02	3.80
03-16-199 08:44:00	2.08	2.85
03-16-199 08:45:00	2.08	2.80
03-16-199 08:46:00	2.28	3.75
03-16-199 08:47:00	3.61	3.80
03-16-199 08:48:00	6.54	3.80
03-16-199 08:49:00	13.91	3.80
03-16-199 08:50:00	6.68	3.17
03-16-199 08:51:00	3.62	3.29
03-16-199 08:52:00	2.85	2.35
03-16-199 08:53:00	2.45	2.76
03-16-199 08:54:00	2.21	2.80
03-16-199 08:55:00	2.07	2.47
03-16-199 08:56:00	2.02	2.17
Avg	4.34	3.35

Press Vent #7
Run 2

03-16-199	09:32:00	2.36	3.16
03-16-199	09:33:00	2.23	4.20
03-16-199	09:34:00	2.19	3.62
03-16-199	09:35:00	2.24	3.33
03-16-199	09:36:00	2.50	3.58
03-16-199	09:37:00	4.21	2.70
03-16-199	09:38:00	7.55	3.68
03-16-199	09:39:00	15.18	3.70
03-16-199	09:40:00	6.38	2.74
03-16-199	09:41:00	3.96	3.32
03-16-199	09:42:00	3.14	3.24
03-16-199	09:43:00	2.71	3.54
03-16-199	09:44:00	2.45	2.83
03-16-199	09:45:00	2.28	4.39
03-16-199	09:46:00	2.28	5.09
03-16-199	09:47:00	2.34	5.50
03-16-199	09:48:00	2.53	4.11
03-16-199	09:49:00	4.19	3.70
03-16-199	09:50:00	7.99	3.70
03-16-199	09:51:00	14.36	3.83
03-16-199	09:52:00	12.13	4.30
03-16-199	09:53:00	4.62	3.70
03-16-199	09:54:00	3.37	3.70
03-16-199	09:55:00	2.84	3.70
03-16-199	09:56:00	2.64	4.02
03-16-199	09:57:00	2.45	4.44
03-16-199	09:58:00	2.40	2.85
03-16-199	09:59:00	2.44	1.80
03-16-199	10:00:00	2.66	2.65
03-16-199	10:01:00	4.35	3.70
03-16-199	10:02:00	8.29	3.70
03-16-199	10:03:00	13.11	3.08
03-16-199	10:04:00	18.70	3.33
03-16-199	10:05:00	6.30	3.54
03-16-199	10:06:00	4.05	3.84
03-16-199	10:07:00	3.45	4.80
03-16-199	10:08:01	3.01	3.91
03-16-199	10:09:01	2.75	2.89
03-16-199	10:10:01	2.61	2.70
03-16-199	10:11:01	2.64	2.70
03-16-199	10:12:01	2.77	2.70
03-16-199	10:13:01	4.48	2.84
03-16-199	10:14:01	8.75	4.05
03-16-199	10:15:01	11.50	3.77
03-16-199	10:16:01	21.45	3.18
03-16-199	10:17:01	8.14	2.89
03-16-199	10:18:01	4.30	2.70
03-16-199	10:19:01	3.44	2.70
03-16-199	10:20:01	3.07	2.70
03-16-199	10:21:01	2.83	3.01
03-16-199	10:22:01	2.67	4.41
03-16-199	10:23:01	2.65	3.91
03-16-199	10:24:01	2.74	3.70
03-16-199	10:25:01	3.62	3.70
03-16-199	10:26:01	7.86	3.70
03-16-199	10:27:01	11.43	3.70
03-16-199	10:28:01	19.35	3.70
03-16-199	10:29:01	14.15	3.70
03-16-199	10:30:01	5.39	2.89
03-16-199	10:31:01	3.74	2.70
	Avg	5.70	3.50

Press Vent #7

Run 3

03-16-199	11:00:01	2.69	3.90
03-16-199	11:01:00	2.66	2.71
03-16-199	11:02:00	2.70	2.70
03-16-199	11:03:00	2.93	2.70
03-16-199	11:04:00	4.65	3.52
03-16-199	11:05:00	8.52	3.39
03-16-199	11:06:00	16.06	2.70
03-16-199	11:07:00	16.46	2.40
03-16-199	11:08:00	7.54	2.70
03-16-199	11:09:00	4.61	2.12
03-16-199	11:10:00	3.81	1.80
03-16-199	11:11:00	3.45	1.80
03-16-199	11:12:00	3.24	1.80
03-16-199	11:13:00	2.98	2.54
03-16-199	11:14:00	2.96	2.10
03-16-199	11:15:00	3.04	2.70
03-16-199	11:16:00	3.42	2.85
03-16-199	11:17:00	6.48	4.44
03-16-199	11:18:00	11.19	3.22
03-16-199	11:19:00	17.38	2.70
03-16-199	11:20:00	25.09	2.70
03-16-199	11:21:00	14.61	2.70
03-16-199	11:22:00	8.25	2.70
03-16-199	11:23:00	5.00	1.97
03-16-199	11:24:00	4.19	1.80
03-16-199	11:25:00	3.69	2.08
03-16-199	11:26:00	3.49	2.12
03-16-199	11:27:00	3.34	3.18
03-16-199	11:28:00	3.29	4.09
03-16-199	11:29:00	3.40	2.71
03-16-199	11:30:00	3.78	2.70
03-16-199	11:31:00	7.73	3.37
03-16-199	11:32:00	12.96	2.70
03-16-199	11:33:00	18.92	2.70
03-16-199	11:34:00	28.40	2.70
03-16-199	11:35:00	15.76	3.19
03-16-199	11:36:00	8.46	3.05
03-16-199	11:37:00	5.59	2.70
03-16-199	11:38:00	4.59	2.85
03-16-199	11:39:00	4.03	3.70
03-16-199	11:40:00	3.78	4.25
03-16-199	11:41:00	3.61	3.70
03-16-199	11:42:00	3.55	3.21
03-16-199	11:43:00	3.70	2.70
03-16-199	11:44:00	4.97	2.70
03-16-199	11:45:00	10.42	3.53
03-16-199	11:46:00	14.18	2.70
03-16-199	11:47:00	19.91	3.52
03-16-199	11:48:00	26.89	4.60
03-16-199	11:49:00	14.67	6.22
03-16-199	11:50:00	7.90	7.07
03-16-199	11:51:00	5.86	4.99
03-16-199	11:52:00	5.18	7.17
03-16-199	11:53:00	4.42	5.97
03-16-199	11:54:00	4.09	4.43
03-16-199	11:55:00	3.86	3.72
03-16-199	11:56:00	3.82	3.70
03-16-199	11:57:00	3.97	3.70
03-16-199	11:58:00	5.34	3.70
03-16-199	11:59:00	11.59	3.70
Avg		7.88	3.26

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	16 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.4	0.04	1.7	-0.21	1.7	0.00	1.7
CO Low	302.00	303.8	-0.18					
CO Mid	566.10	567.3	-0.12	566.5	0.08	563.5	0.30	565.0
CO High	910.00	915.7	0.57					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.1	0.10	1.7	-1.80	2.6	-0.90	2.14
THC Low	29.70	30.2	-0.50	32.2	2.00	31.9	0.30	
THC Mid	55.20	55.3	-0.10	55.7	-0.40	56.1	-0.40	55.90
THC High	85.80	84.5	1.30	85.9	-1.00	84.2	1.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

~~1444~~
1453 -1553

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.40	0.04	1.70	-0.21	1.70	0.00	1.70
CO Low	302.00	303.80	-0.18					
CO Mid	566.10	567.30	-0.12	566.50	0.08	563.50	0.30	565.00
CO High	910.00	915.70	-0.57					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	-0.10	0.10	1.70	-1.80	2.60	-0.90	2.15
THC Low	29.70	30.20	-0.50	32.20	-2.00	31.90	0.30	
THC Mid	55.20	55.30	-0.10	55.70	-0.40	56.10	-0.40	55.90
THC High	85.80	84.50	1.30	85.50	-1.00	84.20	1.30	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	16 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.4	-0.04	1.70	-0.21	0.8	0.09	1.25
CO Low	302.00	303.8	-0.18					
CO Mid	566.10	567.3	-0.12	563.5	0.38	560.2	0.33	561.85
CO High	910.00	915.7	-0.57					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.1	0.10	2.6	-2.70	1.7	0.90	2.15
THC Low	29.70	30.20	-0.50	31.9	-1.70	32.2	-0.30	
THC Mid	55.20	55.30	-0.10	56.1	-0.80	56.6	-0.40	56.30
THC High	85.80	84.50	1.30	84.20	0.30	85.5	-1.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1642 - 1742

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.40	0.04	1.70	-0.21	0.80	0.09	1.25
CO Low	302.00	303.80	-0.18					
CO Mid	566.10	567.30	-0.12	563.50	0.38	560.20	0.33	561.85
CO High	910.00	915.70	-0.57					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	-0.10	0.10	2.60	-2.70	1.70	0.90	2.15
THC Low	29.70	30.20	-0.50	31.90	-1.70	32.20	-0.30	
THC Mid	55.20	55.30	-0.10	56.10	-0.80	56.50	-0.40	56.30
THC High	85.80	84.50	1.30	84.20	0.30	85.50	-1.30	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	16 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	0.80	0.04	.80	-0.12	.80	0.0	0.80
CO Low	302.00	303.8	-0.18					
CO Mid	566.10	567.3	-0.12	560.2	0.17	559.1	.11	559.65
CO High	910.00	915.7	-0.57					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	-0.1	0.10	1.7	-1.80	1.1	0.60	1.40
THC Low	29.70	30.2	-0.50	32.2	-2.00	31.4	0.80	
THC Mid	55.20	55.30	-0.10	56.6	-1.20	55.8	0.70	56.15
THC High	85.80	84.5	1.30	85.5	1.00	85.5	0.0	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1812 - 1912

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#8 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK				
				PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.40	0.04	0.80	-0.12	0.80	0.00	0.80
CO Low	302.00	303.80	-0.18					
CO Mid	566.10	567.30	-0.12	560.20	0.71	559.10	0.11	559.65
CO High	910.00	915.70	-0.57					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	-0.10	0.10	1.70	-1.80	1.10	0.60	1.40
THC Low	29.70	30.20	-0.50	32.20	-2.00	31.40	0.80	
THC Mid	55.20	55.30	-0.10	56.50	-1.20	55.80	0.70	56.15
THC High	85.80	84.50	1.30	85.50	-1.00	85.50	0.00	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press Vent #8

Run #1	THC100 PPM	CO PPM
03-16-199 14:53:00	4.11	4.70
03-16-199 14:54:01	4.13	4.70
03-16-199 14:55:00	3.95	4.70
03-16-199 14:56:01	3.95	4.68
03-16-199 14:57:00	4.10	3.70
03-16-199 14:58:00	3.90	3.70
03-16-199 14:59:01	3.72	3.67
03-16-199 15:00:00	3.50	2.84
03-16-199 15:01:01	3.39	2.70
03-16-199 15:02:01	3.41	2.70
03-16-199 15:03:01	3.48	2.70
03-16-199 15:04:01	3.63	3.07
03-16-199 15:05:01	4.20	4.02
03-16-199 15:06:01	5.94	4.20
03-16-199 15:07:01	9.87	3.32
03-16-199 15:08:01	17.95	3.28
03-16-199 15:09:01	12.07	4.36
03-16-199 15:10:01	11.05	5.38
03-16-199 15:11:01	8.61	3.99
03-16-199 15:12:01	6.47	3.70
03-16-199 15:13:01	4.92	3.70
03-16-199 15:14:01	4.23	3.49
03-16-199 15:15:01	3.96	2.70
03-16-199 15:16:01	3.90	3.57
03-16-199 15:17:01	3.82	2.99
03-16-199 15:18:00	3.99	2.70
03-16-199 15:19:01	5.14	2.70
03-16-199 15:20:01	8.24	2.70
03-16-199 15:21:00	15.85	2.70
03-16-199 15:22:01	14.41	2.91
03-16-199 15:23:01	10.57	3.91
03-16-199 15:24:00	6.98	4.70
03-16-199 15:25:00	4.98	3.99
03-16-199 15:26:00	4.11	3.49
03-16-199 15:27:01	3.67	2.70
03-16-199 15:28:00	3.58	3.19
03-16-199 15:29:00	3.63	2.74
03-16-199 15:30:01	3.78	3.70
03-16-199 15:31:00	4.24	4.03
03-16-199 15:32:00	6.23	3.49
03-16-199 15:33:00	9.95	2.70
03-16-199 15:34:00	8.45	2.70
03-16-199 15:35:00	6.95	2.70
03-16-199 15:36:00	5.79	2.70
03-16-199 15:37:00	5.14	2.90
03-16-199 15:38:00	4.70	3.70
03-16-199 15:39:00	4.64	3.70
03-16-199 15:40:00	4.83	3.70
03-16-199 15:41:00	4.97	3.70
03-16-199 15:42:00	5.27	3.70
03-16-199 15:43:00	6.28	3.70
03-16-199 15:44:00	9.90	3.70
03-16-199 15:45:00	13.64	3.66
03-16-199 15:46:00	10.02	2.70
03-16-199 15:47:00	7.64	2.70
03-16-199 15:48:00	6.49	2.70
03-16-199 15:49:00	5.47	2.70
03-16-199 15:50:00	4.83	2.70
03-16-199 15:51:00	4.62	2.70
03-16-199 15:52:00	4.63	2.89
Avg	6.26	3.41

Press Vent #8

Run 2

03-16-199	16:42:00	5.86	2.99
03-16-199	16:43:00	8.30	3.60
03-16-199	16:44:00	13.73	3.44
03-16-199	16:45:00	14.75	3.44
03-16-199	16:46:00	10.80	2.72
03-16-199	16:47:00	8.10	3.48
03-16-199	16:48:00	6.59	3.60
03-16-199	16:49:00	5.59	3.60
03-16-199	16:50:00	5.15	3.78
03-16-199	16:51:00	4.88	3.60
03-16-199	16:52:00	4.94	3.60
03-16-199	16:53:00	5.06	3.60
03-16-199	16:54:00	6.19	4.57
03-16-199	16:55:00	9.06	4.10
03-16-199	16:56:00	16.11	4.57
03-16-199	16:57:00	12.98	4.10
03-16-199	16:58:00	9.00	3.60
03-16-199	16:59:00	7.35	3.63
03-16-199	17:00:00	5.82	3.68
03-16-199	17:01:00	4.81	3.70
03-16-199	17:02:00	4.47	3.49
03-16-199	17:03:00	4.30	2.70
03-16-199	17:04:00	4.25	2.70
03-16-199	17:05:00	4.29	2.91
03-16-199	17:06:00	4.46	3.15
03-16-199	17:07:00	5.15	2.70
03-16-199	17:08:00	9.45	3.08
03-16-199	17:09:00	11.07	3.49
03-16-199	17:10:00	8.13	2.70
03-16-199	17:11:00	6.51	2.70
03-16-199	17:12:00	5.21	2.70
03-16-199	17:13:00	4.43	2.70
03-16-199	17:14:00	4.14	2.70
03-16-199	17:15:00	4.05	2.70
03-16-199	17:16:00	4.04	2.70
03-16-199	17:17:00	4.27	2.70
03-16-199	17:18:01	5.23	2.70
03-16-199	17:19:00	6.81	2.70
03-16-199	17:20:01	12.11	3.10
03-16-199	17:21:01	9.83	2.80
03-16-199	17:22:01	7.73	2.70
03-16-199	17:23:01	5.86	2.34
03-16-199	17:24:01	4.70	1.80
03-16-199	17:25:00	4.02	2.60
03-16-199	17:26:01	3.72	2.70
03-16-199	17:27:01	3.64	2.04
03-16-199	17:28:01	3.65	1.86
03-16-199	17:29:01	4.17	2.70
03-16-199	17:30:01	5.61	2.70
03-16-199	17:31:01	9.94	2.70
03-16-199	17:32:01	12.96	2.70
03-16-199	17:33:01	8.66	2.70
03-16-199	17:34:01	6.52	3.43
03-16-199	17:35:01	5.14	3.70
03-16-199	17:36:01	4.17	2.80
03-16-199	17:37:01	3.75	2.70
03-16-199	17:38:01	3.68	2.70
03-16-199	17:39:01	3.71	2.93
03-16-199	17:40:01	3.86	3.70
03-16-199	17:41:01	4.59	3.70
	Avg	6.62	3.10

Press Vent # 8

Run # 3

03-16-199	18:12:00	3.34	2.70
03-16-199	18:13:00	3.25	3.59
03-16-199	18:14:00	3.32	3.70
03-16-199	18:15:00	3.79	3.70
03-16-199	18:16:00	5.45	3.70
03-16-199	18:17:00	8.65	3.70
03-16-199	18:18:00	12.89	3.70
03-16-199	18:19:00	8.45	3.70
03-16-199	18:20:00	5.79	3.70
03-16-199	18:21:00	4.81	2.98
03-16-199	18:22:00	3.96	3.26
03-16-199	18:23:00	3.52	3.70
03-16-199	18:24:00	3.28	3.70
03-16-199	18:25:00	3.25	3.70
03-16-199	18:26:00	3.32	3.70
03-16-199	18:27:00	4.01	3.70
03-16-199	18:28:00	6.20	3.70
03-16-199	18:29:00	12.90	3.76
03-16-199	18:30:00	10.79	4.80
03-16-199	18:31:00	7.06	4.55
03-16-199	18:32:00	5.28	3.70
03-16-199	18:33:00	4.32	3.70
03-16-199	18:34:00	3.58	3.70
03-16-199	18:35:00	3.27	3.70
03-16-199	18:36:00	3.24	3.70
03-16-199	18:37:00	3.24	3.70
03-16-199	18:38:00	3.34	3.70
03-16-199	18:39:00	4.06	3.70
03-16-199	18:40:00	6.29	3.70
03-16-199	18:41:00	11.57	3.70
03-16-199	18:42:00	8.09	3.70
03-16-199	18:43:00	5.85	3.70
03-16-199	18:44:00	5.12	3.70
03-16-199	18:45:00	4.04	3.70
03-16-199	18:46:00	3.71	3.70
03-16-199	18:47:00	3.57	3.70
03-16-199	18:48:00	3.56	3.70
03-16-199	18:49:00	3.55	3.70
03-16-199	18:50:00	3.81	3.70
03-16-199	18:51:00	4.80	3.70
03-16-199	18:52:00	9.48	3.70
03-16-199	18:53:00	9.05	3.70
03-16-199	18:54:00	6.56	3.70
03-16-199	18:55:00	6.00	2.98
03-16-199	18:56:00	4.41	2.87
03-16-199	18:57:00	3.84	2.70
03-16-199	18:58:00	3.48	2.70
03-16-199	18:59:00	3.40	2.70
03-16-199	19:00:00	3.41	2.70
03-16-199	19:01:00	3.47	2.70
03-16-199	19:02:00	4.09	2.70
03-16-199	19:03:00	6.38	2.70
03-16-199	19:04:00	11.20	3.25
03-16-199	19:05:00	8.55	2.81
03-16-199	19:06:00	6.16	2.70
03-16-199	19:07:00	4.85	2.70
03-16-199	19:08:00	3.99	2.70
03-16-199	19:09:00	3.41	2.70
03-16-199	19:10:00	3.20	2.70
03-16-199	19:11:00	3.14	2.70
	Avg.	5.34	3.43

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#9 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	17 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.2	0.02	0.9	-0.11	0.8	0.01	0.85
CO Low	302.00	304.9	0.29					
CO Mid	566.10	566.6	-0.05	566.4	0.02	552.4	1.40	559.4
CO High	910.00	920.7	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.1	-0.10	0.8	-0.70	0.8	0.00	0.80
THC Low	29.70	30.1	-0.40	30.4	-0.30	30.1	0.30	
THC Mid	55.20	55.0	-0.20	54.9	0.10	54.2	0.70	54.55
THC High	85.80	84.2	1.60	83.6	0.60	81.9	1.70	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

0856 - 0956

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#9 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	17 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	0.90	-0.11	0.80	0.01	0.85
CO Low	302.00	304.90	-0.29					
CO Mid	566.10	566.60	-0.05	566.40	0.02	552.40	1.40	559.40
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.10	-0.10	0.80	-0.70	0.80	0.00	0.80
THC Low	29.70	30.10	-0.40	30.40	-0.30	30.10	0.30	
THC Mid	55.20	55.00	0.20	54.90	0.10	54.20	0.70	54.55
THC High	85.80	84.20	1.60	83.60	0.60	81.90	1.70	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#9 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	17 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK				
				PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-.2	0.02	0.8	-0.10	1.7	-0.09	1.25
CO Low	302.00	304.9	-0.29					
CO Mid	566.10	566.6	-0.05	552.4	1.42	552.4	0.0	552.4
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.1	-0.10	0.80	-0.70	1.6	-0.80	1.20
THC Low	29.70	30.1	-0.40	30.1	0.00	30.5	-0.40	
THC Mid	55.20	55.2	0.20	54.2	0.80	54.2	0.00	54.2
THC High	85.80	84.2	1.6	81.9	2.30	81.9		
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1028 -1128

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#9 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	17 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Calibration Correction Factor Co/Cm
CO Zero	0.00	-0.20	0.02	0.80	-0.10	1.70	-0.09	1.25
CO Low	302.00	304.90	-0.29					
CO Mid	566.10	566.60	-0.05	552.40	1.42	552.40	0.00	552.40
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.10	-0.10	0.80	-0.70	1.60	-0.80	1.20
THC Low	29.70	30.10	-0.40	30.10	0.00	30.50	-0.40	
THC Mid	55.20	55.00	0.20	54.20	0.80	54.20	0.00	54.20
THC High	85.80	84.20	1.60	81.90	2.30	81.50	0.40	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#9 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	17 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-.2	0.02	1.7	0.19	1.7	0.00	1.7
CO Low	302.00	304.9	-0.29					
CO Mid	566.10	566.6	-0.05	552.4	1.42	554.3	-0.19	553.35
CO High	910.00	920.70	1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High						ND		
THC Zero	0.00	0.1	-0.10	1.6	-1.50	8.825	-1.10	2.15
THC Low	29.70	30.1	0.40	30.5	-0.40	30.9	-0.40	
THC Mid	55.20	55.2	0.20	54.2	0.80	54.4	-0.20	54.30
THC High	85.80	84.2	1.6	81.50	2.70	81.2	0.30	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1158 - 1258

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#9 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	17 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	1.70	-0.19	1.70	0.00	1.70
CO Low	302.00	304.90	-0.29					
CO Mid	566.10	566.60	-0.05	552.40	1.42	554.30	-0.19	553.35
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.10	-0.10	1.60	-1.50	2.70	-1.10	2.15
THC Low	29.70	30.10	-0.40	30.50	-0.40	30.90	-0.40	
THC Mid	55.20	55.00	0.20	54.20	0.80	54.40	-0.20	54.30
THC High	85.80	84.20	1.60	81.50	2.70	81.20	0.30	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press Vent #9

Run#7	THC100 PPM	CO PPM
03-17-199 08:56:03	3.13	3.70
03-17-199 08:57:00	5.98	3.70
03-17-199 08:58:00	6.18	3.70
03-17-199 08:59:00	5.66	4.25
03-17-199 09:00:00	4.35	3.70
03-17-199 09:01:00	3.49	3.70
03-17-199 09:02:00	2.98	3.70
03-17-199 09:03:00	2.63	2.86
03-17-199 09:04:00	3.51	2.70
03-17-199 09:05:00	5.79	3.57
03-17-199 09:06:00	6.93	4.05
03-17-199 09:07:00	4.57	2.70
03-17-199 09:08:00	3.48	2.09
03-17-199 09:09:00	2.84	2.10
03-17-199 09:10:00	2.67	2.70
03-17-199 09:11:00	2.69	2.55
03-17-199 09:12:00	6.49	1.80
03-17-199 09:13:00	6.83	1.80
03-17-199 09:14:00	5.29	2.56
03-17-199 09:15:00	3.99	2.11
03-17-199 09:16:00	3.11	1.80
03-17-199 09:17:00	2.69	1.80
03-17-199 09:18:00	3.20	1.80
03-17-199 09:19:00	5.09	1.81
03-17-199 09:20:00	6.00	2.87
03-17-199 09:21:00	5.35	2.70
03-17-199 09:22:00	4.30	2.86
03-17-199 09:23:00	3.50	3.70
03-17-199 09:24:00	2.91	2.70
03-17-199 09:25:00	2.92	3.36
03-17-199 09:26:00	6.92	3.04
03-17-199 09:27:00	6.41	4.80
03-17-199 09:28:00	6.38	4.07
03-17-199 09:29:00	4.63	3.70
03-17-199 09:30:00	3.65	3.88
03-17-199 09:31:00	2.87	4.80
03-17-199 09:32:00	2.78	4.25
03-17-199 09:33:00	3.67	5.47
03-17-199 09:34:00	8.70	5.63
03-17-199 09:35:00	7.51	3.75
03-17-199 09:36:00	5.45	3.20
03-17-199 09:37:00	3.88	5.29
03-17-199 09:38:00	3.18	4.26
03-17-199 09:39:00	2.73	2.70
03-17-199 09:40:00	3.38	2.70
03-17-199 09:41:00	7.64	2.70
03-17-199 09:42:00	5.38	2.70
03-17-199 09:43:00	6.26	2.70
03-17-199 09:44:00	5.57	1.96
03-17-199 09:45:00	4.20	2.40
03-17-199 09:46:00	3.32	2.11
03-17-199 09:47:00	3.10	2.10
03-17-199 09:48:00	3.82	2.54
03-17-199 09:49:00	9.13	2.70
03-17-199 09:50:00	9.25	3.53
03-17-199 09:51:00	6.38	3.70
03-17-199 09:52:00	5.16	3.70
03-17-199 09:53:00	3.90	3.70
03-17-199 09:54:00	3.46	3.70
03-17-199 09:55:00	3.82	3.70
Avg	4.68	3.18

Press Vent #9

Run #2

03-17-199	10:28:01	7.88	4.07
03-17-199	10:29:01	5.90	3.70
03-17-199	10:30:01	4.93	3.20
03-17-199	10:31:01	4.02	4.43
03-17-199	10:32:01	3.59	4.80
03-17-199	10:33:01	3.50	4.80
03-17-199	10:34:01	4.71	4.80
03-17-199	10:35:01	9.81	4.80
03-17-199	10:36:01	6.60	4.80
03-17-199	10:37:01	6.74	6.24
03-17-199	10:38:01	5.04	7.22
03-17-199	10:39:01	4.39	7.25
03-17-199	10:40:01	3.68	5.14
03-17-199	10:41:00	4.04	5.13
03-17-199	10:42:01	4.85	4.08
03-17-199	10:43:00	10.47	2.71
03-17-199	10:44:01	6.82	2.70
03-17-199	10:45:00	6.20	3.19
03-17-199	10:46:00	5.23	3.21
03-17-199	10:47:00	4.24	2.70
03-17-199	10:48:00	3.78	3.02
03-17-199	10:49:00	4.12	3.70
03-17-199	10:50:00	4.41	3.70
03-17-199	10:51:00	10.84	3.37
03-17-199	10:52:00	6.84	2.70
03-17-199	10:53:00	6.40	2.70
03-17-199	10:54:00	5.20	3.03
03-17-199	10:55:00	4.48	2.70
03-17-199	10:56:00	3.94	2.70
03-17-199	10:57:00	4.08	3.02
03-17-199	10:58:00	4.86	3.70
03-17-199	10:59:00	10.16	3.20
03-17-199	11:00:01	7.22	3.21
03-17-199	11:01:00	6.53	2.70
03-17-199	11:02:00	5.40	2.70
03-17-199	11:03:00	4.51	2.70
03-17-199	11:04:00	4.04	2.41
03-17-199	11:05:00	4.45	2.70
03-17-199	11:06:00	5.05	2.40
03-17-199	11:07:00	10.88	2.24
03-17-199	11:08:00	6.84	2.70
03-17-199	11:09:00	6.48	2.10
03-17-199	11:10:00	5.35	1.94
03-17-199	11:11:00	4.35	1.78
03-17-199	11:12:00	3.80	2.08
03-17-199	11:13:00	4.58	2.26
03-17-199	11:14:00	5.30	1.75
03-17-199	11:15:00	9.92	1.72
03-17-199	11:16:00	6.92	1.73
03-17-199	11:17:00	6.63	2.18
03-17-199	11:18:00	5.21	2.20
03-17-199	11:19:00	4.52	2.56
03-17-199	11:20:00	4.04	1.70
03-17-199	11:21:00	4.69	2.18
03-17-199	11:22:00	5.52	2.70
03-17-199	11:23:00	10.50	3.01
03-17-199	11:24:00	6.67	3.55
03-17-199	11:25:00	6.40	2.70
03-17-199	11:26:00	5.39	2.70
03-17-199	11:27:00	4.45	2.70
	Avg.	5.79	3.23

Press Vent #9

Run #3

03-17-199	11:58:00	5.56	4.69
03-17-199	11:59:00	4.68	4.55
03-17-199	12:00:00	4.46	4.35
03-17-199	12:01:00	5.73	4.16
03-17-199	12:02:00	8.44	3.87
03-17-199	12:03:00	6.90	4.49
03-17-199	12:04:00	7.30	4.70
03-17-199	12:05:00	6.58	5.71
03-17-199	12:06:00	5.49	9.73
03-17-199	12:07:00	4.66	6.94
03-17-199	12:08:00	4.72	4.90
03-17-199	12:09:00	5.22	4.20
03-17-199	12:10:00	10.20	3.60
03-17-199	12:11:00	7.12	3.93
03-17-199	12:12:00	7.32	5.74
03-17-199	12:13:00	6.17	8.37
03-17-199	12:14:00	5.19	10.90
03-17-199	12:15:00	4.54	7.85
03-17-199	12:16:00	4.69	7.02
03-17-199	12:17:00	5.04	4.43
03-17-199	12:18:00	9.52	3.60
03-17-199	12:19:00	7.35	3.60
03-17-199	12:20:00	7.94	3.60
03-17-199	12:21:00	6.48	2.65
03-17-199	12:22:00	5.39	2.73
03-17-199	12:23:00	4.70	3.60
03-17-199	12:24:00	4.64	6.02
03-17-199	12:25:00	4.65	5.91
03-17-199	12:26:00	10.41	3.65
03-17-199	12:27:00	6.08	2.64
03-17-199	12:28:00	6.78	2.60
03-17-199	12:29:00	6.61	2.60
03-17-199	12:30:00	5.65	2.60
03-17-199	12:31:00	4.74	2.60
03-17-199	12:32:00	4.36	2.60
03-17-199	12:33:00	4.53	2.73
03-17-199	12:34:00	6.07	2.98
03-17-199	12:35:00	7.90	3.89
03-17-199	12:36:00	7.19	4.20
03-17-199	12:37:00	6.54	3.60
03-17-199	12:38:01	5.18	4.13
03-17-199	12:39:01	4.59	4.70
03-17-199	12:40:01	4.58	4.70
03-17-199	12:41:01	5.40	4.54
03-17-199	12:42:01	9.01	3.94
03-17-199	12:43:01	8.42	4.70
03-17-199	12:44:01	8.02	4.70
03-17-199	12:45:01	7.33	5.35
03-17-199	12:46:01	6.12	5.06
03-17-199	12:47:01	5.42	4.70
03-17-199	12:48:01	5.24	3.63
03-17-199	12:49:01	5.21	3.60
03-17-199	12:50:01	9.44	4.52
03-17-199	12:51:01	8.82	4.12
03-17-199	12:52:01	7.66	4.70
03-17-199	12:53:01	7.25	4.70
03-17-199	12:54:01	6.29	4.70
03-17-199	12:55:01	5.46	4.70
03-17-199	12:56:01	5.40	4.70
03-17-199	12:57:01	5.65	4.70
	Avg	6.30	4.55

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#10 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	17 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.20	0.02	1.70	-0.19	1.6	0.01	1.65
CO Low	302.00	303.2	-0.12					
CO Mid	566.10	565.5	0.06	554.3	1.12	548.2	0.61	551.25
CO High	910.00	920.7	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.10	-0.10	2.70	-2.60	1.6	1.10	2.15
THC Low	29.70	30.10	-0.40	30.90	-0.80	29.2	1.70	
THC Mid	55.20	55.20	0.00	54.40	0.80	52.8	1.60	53.6
THC High	85.80	84.20	1.60	81.20	3.00	78.1	3.10	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1524 - 1624

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#10 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	1.70	-0.19	1.60	0.01	1.65
CO Low	302.00	303.20	-0.12					
CO Mid	566.10	565.50	0.06	554.30	1.12	548.20	0.61	551.25
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.10	-0.10	2.70	-2.60	1.60	1.10	2.15
THC Low	29.70	30.10	-0.40	30.90	-0.80	29.20	1.70	
THC Mid	55.20	55.20	0.00	54.40	0.80	52.80	1.60	53.60
THC High	85.80	84.20	1.60	81.20	3.00	78.10	3.10	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#10 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	17 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	1.6	-0.18	1.6	0.00	1.60
CO Low	302.00	303.2	-0.12					
CO Mid	566.10	565.5	0.06	548.2	1.73	548.2	-0.30	549.7
CO High	910.00	920.7	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.10	0.10	1.60	-1.50	1.4	0.20	1.50
THC Low	29.70	30.10	0.40	29.20	0.90	29.0	0.20	
THC Mid	55.20	55.20	0.00	52.8	2.40	52.8	0.00	52.8
THC High	85.80	84.20	1.60	78.1	6.10	78.1	0.00	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1619 — 1749

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#10 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK				
				PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.20	0.02	1.60	-0.18	1.60	0.00	1.60
CO Low	302.00	303.20	-0.12					
CO Mid	566.10	565.50	0.06	548.20	1.73	551.20	-0.30	549.70
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.10	-0.10	1.60	-1.50	1.40	0.20	1.50
THC Low	29.70	30.10	-0.40	29.20	0.90	29.00	0.20	
THC Mid	55.20	55.20	0.00	52.80	2.40	52.80	0.00	52.80
THC High	85.80	84.20	1.60	78.10	6.10	78.10	0.00	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	Louisiana Pacific	Plant Rep.	Billy Adams
Sampling Location	#10 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	17 Mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.20	0.02	1.6	-0.18	0.7	0.09	1.15
CO Low	302.00	303.2	-0.12					
CO Mid	566.10	565.5	0.06	561.2	1.43	550.2	0.10	550.70
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.0	-0.10	1.40	-1.3	0.9	0.50	1.15
THC Low	29.70	29.7	-0.40	29.0	1.1	28.8	0.20	
THC Mid	55.20	55.20	0.00	52.8	2.4	52.9	-0.10	52.85
THC High	85.80	84.2	1.60	78.1	6.1	78.9	-0.80	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1812-1912

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#10 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	16 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.20	0.02	1.60	-0.18	0.70	0.09	1.15
CO Low	302.00	303.20	-0.12					
CO Mid	566.10	565.50	0.06	551.20	1.43	550.20	0.10	550.70
CO High	910.00	920.70	-1.07					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.00	0.10	-0.10	1.40	-1.30	0.90	0.50	1.15
THC Low	29.70	30.10	-0.40	29.00	1.10	28.80	0.20	
THC Mid	55.20	55.20	0.00	52.80	2.40	52.90	-0.10	52.85
THC High	85.80	84.20	1.60	78.10	6.10	78.90	-0.80	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press Vent #10

Run #1

	THC100 PPM	CO PPM
03-17-199 15:24:00	5.66	3.50
03-17-199 15:25:00	5.26	3.50
03-17-199 15:26:00	6.01	4.36
03-17-199 15:27:00	7.41	4.06
03-17-199 15:28:00	7.65	4.60
03-17-199 15:29:00	7.47	4.60
03-17-199 15:30:00	6.85	3.93
03-17-199 15:31:00	6.33	4.54
03-17-199 15:32:00	5.76	4.30
03-17-199 15:33:00	5.58	4.05
03-17-199 15:34:00	5.25	3.50
03-17-199 15:35:00	6.48	3.50
03-17-199 15:36:00	7.43	3.50
03-17-199 15:37:00	7.32	4.06
03-17-199 15:38:00	7.65	3.69
03-17-199 15:39:00	7.43	3.50
03-17-199 15:40:00	6.35	3.99
03-17-199 15:41:00	5.93	4.60
03-17-199 15:42:00	5.54	3.93
03-17-199 15:43:00	5.27	3.50
03-17-199 15:44:00	5.88	3.50
03-17-199 15:45:00	6.97	4.36
03-17-199 15:46:00	7.13	4.48
03-17-199 15:47:00	7.14	3.50
03-17-199 15:48:00	7.00	3.50
03-17-199 15:49:00	6.28	3.50
03-17-199 15:50:00	5.77	3.50
03-17-199 15:51:00	5.49	3.50
03-17-199 15:52:01	5.27	3.50
03-17-199 15:53:00	6.15	2.84
03-17-199 15:54:00	6.81	3.34
03-17-199 15:55:01	7.18	2.88
03-17-199 15:56:00	7.32	2.50
03-17-199 15:57:01	6.98	2.50
03-17-199 15:58:00	6.31	2.50
03-17-199 15:59:01	5.90	2.50
03-17-199 16:00:01	5.42	2.50
03-17-199 16:01:01	5.43	2.50
03-17-199 16:02:01	6.60	2.50
03-17-199 16:03:01	7.17	2.50
03-17-199 16:04:01	7.25	2.50
03-17-199 16:05:01	7.21	2.50
03-17-199 16:06:01	6.39	2.35
03-17-199 16:07:01	5.99	1.78
03-17-199 16:08:01	5.54	2.47
03-17-199 16:09:01	5.31	2.50
03-17-199 16:10:01	5.07	3.46
03-17-199 16:11:01	5.15	3.50
03-17-199 16:12:01	6.03	3.50
03-17-199 16:13:01	6.60	3.37
03-17-199 16:14:01	6.62	2.50
03-17-199 16:15:01	6.38	2.50
03-17-199 16:16:01	6.20	2.50
03-17-199 16:17:01	5.70	2.50
03-17-199 16:18:01	5.38	2.50
03-17-199 16:19:01	5.56	2.50
03-17-199 16:20:01	6.83	2.50
03-17-199 16:21:01	7.10	2.50
03-17-199 16:22:01	7.25	2.50
03-17-199 16:23:00	7.47	2.50
Avg.	6.36	3.24

Press Vent #10

Run #2

03-17-199	16:49:00	7.24	5.30
03-17-199	16:50:00	6.51	4.60
03-17-199	16:51:00	5.88	4.89
03-17-199	16:52:00	5.36	5.60
03-17-199	16:53:00	6.09	5.60
03-17-199	16:54:00	7.15	5.60
03-17-199	16:55:00	7.25	5.47
03-17-199	16:56:00	7.34	4.60
03-17-199	16:57:00	7.29	4.60
03-17-199	16:58:00	6.88	4.60
03-17-199	16:59:00	6.13	4.60
03-17-199	17:00:01	5.65	4.09
03-17-199	17:01:00	5.84	3.50
03-17-199	17:02:00	6.81	3.37
03-17-199	17:03:00	7.21	2.50
03-17-199	17:04:00	7.39	2.80
03-17-199	17:05:00	7.08	3.50
03-17-199	17:06:00	6.39	3.50
03-17-199	17:07:00	5.80	3.50
03-17-199	17:08:00	5.39	3.50
03-17-199	17:09:00	5.63	3.50
03-17-199	17:10:00	6.92	2.87
03-17-199	17:11:00	6.92	2.50
03-17-199	17:12:00	7.09	2.50
03-17-199	17:13:00	7.05	2.50
03-17-199	17:14:00	6.48	2.50
03-17-199	17:15:00	5.94	2.35
03-17-199	17:16:00	5.41	2.50
03-17-199	17:17:00	5.86	2.50
03-17-199	17:18:00	6.58	2.97
03-17-199	17:19:00	6.64	3.04
03-17-199	17:20:00	7.07	2.50
03-17-199	17:21:00	7.17	2.50
03-17-199	17:22:00	6.61	2.50
03-17-199	17:23:00	6.02	2.50
03-17-199	17:24:00	5.57	2.51
03-17-199	17:25:00	6.26	2.08
03-17-199	17:26:00	6.99	1.91
03-17-199	17:27:00	7.04	1.90
03-17-199	17:28:00	7.16	1.60
03-17-199	17:29:00	7.08	2.38
03-17-199	17:30:00	6.54	2.58
03-17-199	17:31:00	5.80	2.30
03-17-199	17:32:00	5.32	1.60
03-17-199	17:33:00	5.91	1.60
03-17-199	17:34:00	6.82	1.60
03-17-199	17:35:00	7.21	1.60
03-17-199	17:36:00	7.48	1.60
03-17-199	17:37:00	7.14	1.60
03-17-199	17:38:00	6.38	1.60
03-17-199	17:39:00	5.94	1.60
03-17-199	17:40:00	5.57	1.60
03-17-199	17:41:00	6.15	1.72
03-17-199	17:42:00	6.86	1.97
03-17-199	17:43:00	6.91	1.60
03-17-199	17:44:00	6.64	1.60
03-17-199	17:45:00	4.90	1.60
03-17-199	17:46:00	4.23	1.60
03-17-199	17:47:00	3.95	1.60
03-17-199	17:48:00	3.40	2.23
	Avg.	6.36	2.85

Press Vent #10

Run #3

03-17-199	18:12:00	5.13	3.59
03-17-199	18:13:00	5.72	3.60
03-17-199	18:14:00	6.30	3.60
03-17-199	18:15:00	6.53	3.60
03-17-199	18:16:00	6.91	3.90
03-17-199	18:17:00	6.66	4.61
03-17-199	18:18:00	6.05	4.61
03-17-199	18:19:00	5.38	4.62
03-17-199	18:20:01	5.02	4.65
03-17-199	18:21:01	5.50	4.64
03-17-199	18:22:00	6.32	4.67
03-17-199	18:23:00	6.49	4.68
03-17-199	18:24:01	6.59	4.69
03-17-199	18:25:01	6.49	4.70
03-17-199	18:26:01	5.89	4.70
03-17-199	18:27:01	5.40	5.32
03-17-199	18:28:01	4.89	5.67
03-17-199	18:29:01	5.28	5.68
03-17-199	18:30:00	6.13	4.90
03-17-199	18:31:01	6.35	4.70
03-17-199	18:32:01	6.53	4.70
03-17-199	18:33:01	6.34	5.68
03-17-199	18:34:01	5.78	5.39
03-17-199	18:35:01	5.27	4.70
03-17-199	18:36:01	4.84	4.70
03-17-199	18:37:01	5.21	3.62
03-17-199	18:38:01	6.04	3.76
03-17-199	18:39:01	6.32	3.99
03-17-199	18:40:01	6.29	3.60
03-17-199	18:41:01	6.23	3.60
03-17-199	18:42:01	5.67	3.60
03-17-199	18:43:01	5.16	3.95
03-17-199	18:44:00	4.75	4.70
03-17-199	18:45:01	5.04	4.70
03-17-199	18:46:01	5.94	4.15
03-17-199	18:47:01	6.29	4.52
03-17-199	18:48:01	6.46	4.70
03-17-199	18:49:01	6.18	3.80
03-17-199	18:50:01	5.66	3.60
03-17-199	18:51:01	5.13	4.31
03-17-199	18:52:00	4.50	4.70
03-17-199	18:53:00	4.86	4.17
03-17-199	18:54:00	5.88	3.60
03-17-199	18:55:01	5.99	3.60
03-17-199	18:56:00	6.21	3.60
03-17-199	18:57:00	5.60	3.60
03-17-199	18:58:00	5.33	2.95
03-17-199	18:59:00	4.90	2.60
03-17-199	19:00:01	4.37	2.60
03-17-199	19:01:00	4.82	2.60
03-17-199	19:02:00	5.75	2.60
03-17-199	19:03:00	6.16	2.60
03-17-199	19:04:00	6.31	3.08
03-17-199	19:05:00	6.10	3.45
03-17-199	19:06:00	5.55	2.60
03-17-199	19:07:00	4.99	2.60
03-17-199	19:08:00	4.64	2.60
03-17-199	19:09:00	4.28	2.60
03-17-199	19:10:00	3.96	2.60
03-17-199	19:11:00	3.98	2.45
03-17-199	19:12:00	4.46	1.70
Avg		5.63	3.94

CEM CALIBRATION DATA

Plant Name	LA PACIFIC	Plant Rep.	Billy Adams
Sampling Location	#11 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	13 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.3	0.03	-0.2	-0.01	0.8	-0.50	0.30
CO Low	302	303.9	0.19					
CO Mid	600	601.1	0.11	599.3	0.18	594.0	0.53	596.65
CO High	910	934.2	2.42					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.1	-0.10	0.7	-0.6	1.8	-0.90	1.15
THC Low	29.70	30.2	-0.50	30.7	-0.5	30.8	-0.10	
THC Mid	49.3	49.3	-0.00	49.8	-0.5	49.9	-0.90	49.65
THC High	85.8	84.3	1.50	84.6	-0.3	83.7	0.90	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1022 - 1230

CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#11 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	1	Date	13 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.00	-0.30	0.03	-0.20	-0.01	0.80	-0.10	0.30
CO Low	302.00	303.90	-0.19					
CO Mid	600.00	601.10	-0.11	599.30	0.18	594.00	0.53	596.65
CO High	910.00	934.20	-2.42					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.10	-0.10	0.70	-0.60	1.60	-0.90	1.15
THC Low	29.70	30.20	-0.50	30.70	-0.50	30.80	-0.10	
THC Mid	49.30	49.30	0.00	49.80	-0.50	49.90	-0.10	49.85
THC High	85.80	84.30	1.50	84.60	-0.30	83.70	0.90	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#11 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	13 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.0	-0.3	0.03	-0.8	-0.01	0.9	-0.01	0.85
CO Low	302	303.9	0.19					
CO Mid	600	601.1	0.11	594.0	0.71	597	-0.30	595.50
CO High	910	934.2	2.42					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.1	-0.10	1.6	-1.50	1.6	0.00	1.6
THC Low	29.70	30.2	-0.50	30.8	-0.6	31.1	-0.30	
THC Mid	49.3	49.3	0.00	49.9	-0.6	50.2	0.30	50.05
THC High	85.8	84.3	1.50	83.7	0.6	84.4	-0.70	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1241-~~T350~~
1341

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#11 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	2	Date	13 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.30	0.03	0.80	-0.11	0.90	-0.01	0.85
CO Low	302.00	303.90	-0.19					
CO Mid	600.00	601.10	-0.11	594.00	0.71	597.00	-0.30	595.50
CO High	910.00	934.20	-2.42					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.10	-0.10	1.60	-1.50	1.60	0.00	1.60
THC Low	29.70	30.20	-0.50	30.80	-0.60	31.10	-0.30	
THC Mid	49.30	49.30	0.00	49.90	-0.60	50.20	-0.30	50.05
THC High	85.80	84.30	1.50	83.70	0.60	84.40	-0.70	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#11 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prestek
Run Number	3	Date	13 mar 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		POST TEST		Calibration Correction Factor Co/Cm
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	
CO Zero	0.0	-0.3	0.03	0.90	-0.12	0.9	0.0	0.90
CO Low	302	303.9	0.19					
CO Mid	600	601.1	0.11	597.0	0.41	598.3	0.13	597.65
CO High	910	934.2	2.42					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero	0.0	0.1	-0.10	1.6	-1.50	1.9	-0.30	1.75
THC Low	29.70	30.2	-0.50	31.1	-0.90	31.7	-0.60	
THC Mid	49.3	49.3	0.00	50.20	-0.90	51.2	-1.00	50.70
THC High	85.8	84.3	1.50	84.4	-0.10	85.8	-1.40	
NOx Zero								
NOx Low								
NOx Mid								
NOx High								
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

1440 - 1540

* CEM CALIBRATION DATA

Plant Name	LA Pacific	Plant Rep.	Billy Adams
Sampling Location	#11 Press Vent	Team Leader	T. Thompson
Project Number	1449-001	CEM Operator	D. Prater
Run Number	3	Date	13 MAR 92

	CALIBRATION ERROR			SYSTEM BIAS CHECK PRETEST		SYSTEM BIAS CHECK POST TEST		Calibration Correction Factor
	Cylinder Value	Analyzer Calibration Response	Difference (% of Span)	System Response	System Bias (% of Span)	System Response	Drift (% of Span)	Co/Cm
CO Zero	0.00	-0.30	0.03	0.90	-0.12	0.90	0.00	0.90
CO Low	302.00	303.90	-0.19					
CO Mid	600.00	601.10	-0.11	597.00	0.41	598.30	-0.13	597.65
CO High	910.00	934.20	-2.42					
CO2 Zero								
CO2 Low								
CO2 Mid								
CO2 High								
O2 Zero								
O2 Low								
O2 Mid								
O2 High								
THC Zero								
THC Low								
THC Mid								
THC High								
THC Zero	0.00	0.10	-0.10	1.60	-1.50	1.90	-0.30	1.75
THC Low	29.70	30.20	-0.50	31.10	-0.90	31.70	-0.60	
THC Mid	49.30	49.30	0.00	50.20	-0.90	51.20	-1.00	50.70
THC High	85.80	84.30	1.50	84.40	-0.10	85.80	-1.40	
SO2 Zero								
SO2 Low								
SO2 Mid								
SO2 High								

Press Vent # 11

Run #1	THC100 PPM	CO PPM	
			0
			0
03-13-199 10:22:00	12.59	1.78	
03-13-199 10:23:00	11.81	1.16	
03-13-199 10:24:00	12.53	1.61	
03-13-199 10:25:00	13.45	1.49	
03-13-199 10:26:00	11.92	1.61	
03-13-199 10:27:00	11.39	1.66	
03-13-199 10:28:00	12.87	0.94	
03-13-199 10:29:00	12.01	1.16	
03-13-199 10:30:00	13.17	0.94	
03-13-199 10:31:00	11.63	1.63	
03-13-199 10:32:00	12.53	1.80	
03-13-199 10:33:00	12.04	1.80	
03-13-199 10:34:00	10.70	1.30	
03-13-199 10:35:00	10.11	1.49	
03-13-199 10:36:00	11.39	0.80	
03-13-199 10:37:00	11.32	0.80	
03-13-199 10:38:00	11.12	0.97	
03-13-199 10:39:00	11.41	0.80	
03-13-199 10:40:00	11.32	0.80	
03-13-199 10:41:00	11.81	0.80	
03-13-199 10:42:00	12.50	0.80	
03-13-199 10:43:00	12.10	0.80	
03-13-199 10:44:00	11.95	0.80	
03-13-199 10:45:00	11.75	0.80	
03-13-199 10:46:00	11.38	0.80	
03-13-199 10:47:00	13.36	0.80	
03-13-199 10:48:00	12.33	0.80	
03-13-199 10:49:00	11.41	0.80	
03-13-199 10:50:00	10.85	0.80	
03-13-199 10:51:00	11.98	0.80	
03-13-199 10:52:00	13.79	0.80	
03-13-199 10:53:00	13.52	0.80	
03-13-199 10:54:00	12.65	1.44	
03-13-199 10:55:00	12.44	1.80	
03-13-199 10:56:00	13.92	1.32	
03-13-199 10:57:00	13.98	0.80	
03-13-199 10:58:00	14.83	0.80	
03-13-199 10:59:00	12.49	1.78	
03-13-199 11:00:00	12.58	1.80	
03-13-199 11:01:00	15.35	1.80	
03-13-199 11:02:00	13.50	0.99	
03-13-199 11:03:00	13.56	0.97	
03-13-199 11:04:00	12.63	0.80	
03-13-199 11:05:00	12.73	1.11	
03-13-199 11:06:00	12.36	0.98	
03-13-199 11:07:00	14.33	1.28	
03-13-199 11:08:00	13.57	1.63	
03-13-199 11:09:00	12.79	1.63	
03-13-199 11:10:00	13.38	0.82	
03-13-199 11:11:00	13.21	0.80	
03-13-199 11:12:00	13.75	0.80	
03-13-199 11:13:00	13.15	0.80	
03-13-199 11:14:00	12.13	0.97	
03-13-199 11:15:00	12.45	1.45	
03-13-199 11:16:00	14.62	1.49	
03-13-199 11:17:00	13.81	0.80	
03-13-199 11:18:00	13.74	0.80	
03-13-199 11:19:00	12.67	0.94	
03-13-199 11:20:00	14.64	0.82	
03-13-199 11:21:00	16.13	0.80	
Avg.	12.69	1.12	

Press Vent #11

Run #2

03-13-199	12:41:00	13.61	1.87
03-13-199	12:42:00	13.73	1.90
03-13-199	12:43:00	12.77	1.90
03-13-199	12:44:00	12.99	1.90
03-13-199	12:45:00	13.58	1.89
03-13-199	12:46:00	12.28	1.89
03-13-199	12:47:00	13.19	0.90
03-13-199	12:48:00	11.89	0.90
03-13-199	12:49:00	12.09	0.90
03-13-199	12:50:00	11.10	1.07
03-13-199	12:51:00	11.07	1.90
03-13-199	12:52:00	12.13	1.73
03-13-199	12:53:00	13.15	1.89
03-13-199	12:54:00	11.19	1.55
03-13-199	12:55:00	11.44	1.06
03-13-199	12:56:00	12.35	1.57
03-13-199	12:57:00	13.44	1.56
03-13-199	12:58:00	12.38	0.90
03-13-199	12:59:00	12.60	0.90
03-13-199	13:00:00	13.90	0.90
03-13-199	13:01:00	13.07	0.90
03-13-199	13:02:00	13.05	0.90
03-13-199	13:03:00	12.77	1.56
03-13-199	13:04:00	12.87	1.74
03-13-199	13:05:00	12.70	1.90
03-13-199	13:06:00	11.26	1.90
03-13-199	13:07:00	11.69	1.90
03-13-199	13:08:00	12.50	1.88
03-13-199	13:09:00	12.37	1.89
03-13-199	13:10:00	12.02	1.06
03-13-199	13:11:00	11.42	1.06
03-13-199	13:12:00	12.13	1.24
03-13-199	13:13:00	12.04	1.72
03-13-199	13:14:00	10.54	1.57
03-13-199	13:15:00	10.97	1.90
03-13-199	13:16:00	11.18	1.90
03-13-199	13:17:00	13.04	1.90
03-13-199	13:18:00	12.23	1.90
03-13-199	13:19:00	11.54	1.73
03-13-199	13:20:00	12.11	1.90
03-13-199	13:21:00	11.93	1.90
03-13-199	13:22:00	11.29	1.06
03-13-199	13:23:00	11.52	1.90
03-13-199	13:24:00	12.68	1.90
03-13-199	13:25:00	12.49	1.90
03-13-199	13:26:00	10.79	1.90
03-13-199	13:27:00	10.87	1.23
03-13-199	13:28:00	11.27	1.39
03-13-199	13:29:00	12.26	1.08
03-13-199	13:30:00	11.76	1.06
03-13-199	13:31:00	11.57	0.90
03-13-199	13:32:00	11.89	1.07
03-13-199	13:33:00	12.11	1.07
03-13-199	13:34:00	11.14	1.24
03-13-199	13:35:00	12.77	1.39
03-13-199	13:36:00	11.24	1.58
03-13-199	13:37:00	12.74	1.05
03-13-199	13:38:00	11.60	0.90
03-13-199	13:39:00	11.31	0.90
03-13-199	13:40:00	11.40	0.90
	Avg	12.12	1.46

Press Vent #11

Run #3

03-13-199	14:40:00	11.24	0.88
03-13-199	14:41:01	10.71	0.90
03-13-199	14:42:00	10.15	0.90
03-13-199	14:43:00	11.17	0.90
03-13-199	14:44:00	10.98	0.90
03-13-199	14:45:00	10.91	0.90
03-13-199	14:46:00	10.78	0.90
03-13-199	14:47:00	10.55	0.90
03-13-199	14:48:00	11.14	0.89
03-13-199	14:49:00	9.58	0.90
03-13-199	14:50:00	10.22	0.90
03-13-199	14:51:00	10.55	0.90
03-13-199	14:52:00	10.66	0.90
03-13-199	14:53:00	9.51	0.90
03-13-199	14:54:00	10.01	0.90
03-13-199	14:55:00	10.49	0.90
03-13-199	14:56:00	11.35	0.90
03-13-199	14:57:00	11.52	0.90
03-13-199	14:58:00	11.02	0.90
03-13-199	14:59:00	9.86	0.90
03-13-199	15:00:01	11.18	0.90
03-13-199	15:01:00	11.10	0.90
03-13-199	15:02:00	10.77	0.90
03-13-199	15:03:00	11.29	0.90
03-13-199	15:04:00	11.47	0.90
03-13-199	15:05:00	10.74	0.90
03-13-199	15:06:00	9.77	0.90
03-13-199	15:07:00	10.22	0.90
03-13-199	15:08:00	11.50	0.90
03-13-199	15:09:00	10.08	0.90
03-13-199	15:10:00	9.74	0.90
03-13-199	15:11:00	10.94	0.90
03-13-199	15:12:00	11.31	0.90
03-13-199	15:13:00	10.99	0.90
03-13-199	15:14:00	8.38	0.90
03-13-199	15:15:00	8.26	0.90
03-13-199	15:16:00	8.66	0.90
03-13-199	15:17:00	8.74	0.90
03-13-199	15:18:00	9.73	0.90
03-13-199	15:19:00	11.32	0.90
03-13-199	15:20:00	11.85	0.90
03-13-199	15:21:00	10.67	0.90
03-13-199	15:22:00	10.41	0.90
03-13-199	15:23:00	11.14	0.90
03-13-199	15:24:00	11.43	0.90
03-13-199	15:25:00	10.34	0.90
03-13-199	15:26:00	10.80	0.90
03-13-199	15:27:00	12.41	0.90
03-13-199	15:28:00	11.93	0.90
03-13-199	15:29:00	10.35	0.90
03-13-199	15:30:00	10.88	0.94
03-13-199	15:31:00	11.71	1.69
03-13-199	15:32:00	10.59	0.90
03-13-199	15:33:00	9.38	0.90
03-13-199	15:34:00	10.46	0.90
03-13-199	15:35:00	10.95	0.90
03-13-199	15:36:00	10.24	0.90
03-13-199	15:37:00	11.05	0.90
03-13-199	15:38:00	10.52	1.23
03-13-199	15:39:00	11.82	0.90
Avg		10.62	0.92

APPENDIX F

CEMS CHART RECORDER TRACES

CO THC

THC ZERO TRC/CO

11 MAR 92 10 20 1

CO

THC

CO

11 MAR 92 10 21 57

START INTERNAL calibration

11 MAR 92 90 7 11 12 80 70 60 50 40 30 20 10 0

0 RECORDER DATA LOGGER 20 TRC SH 30 40 50 60 70 80 90 100

CO

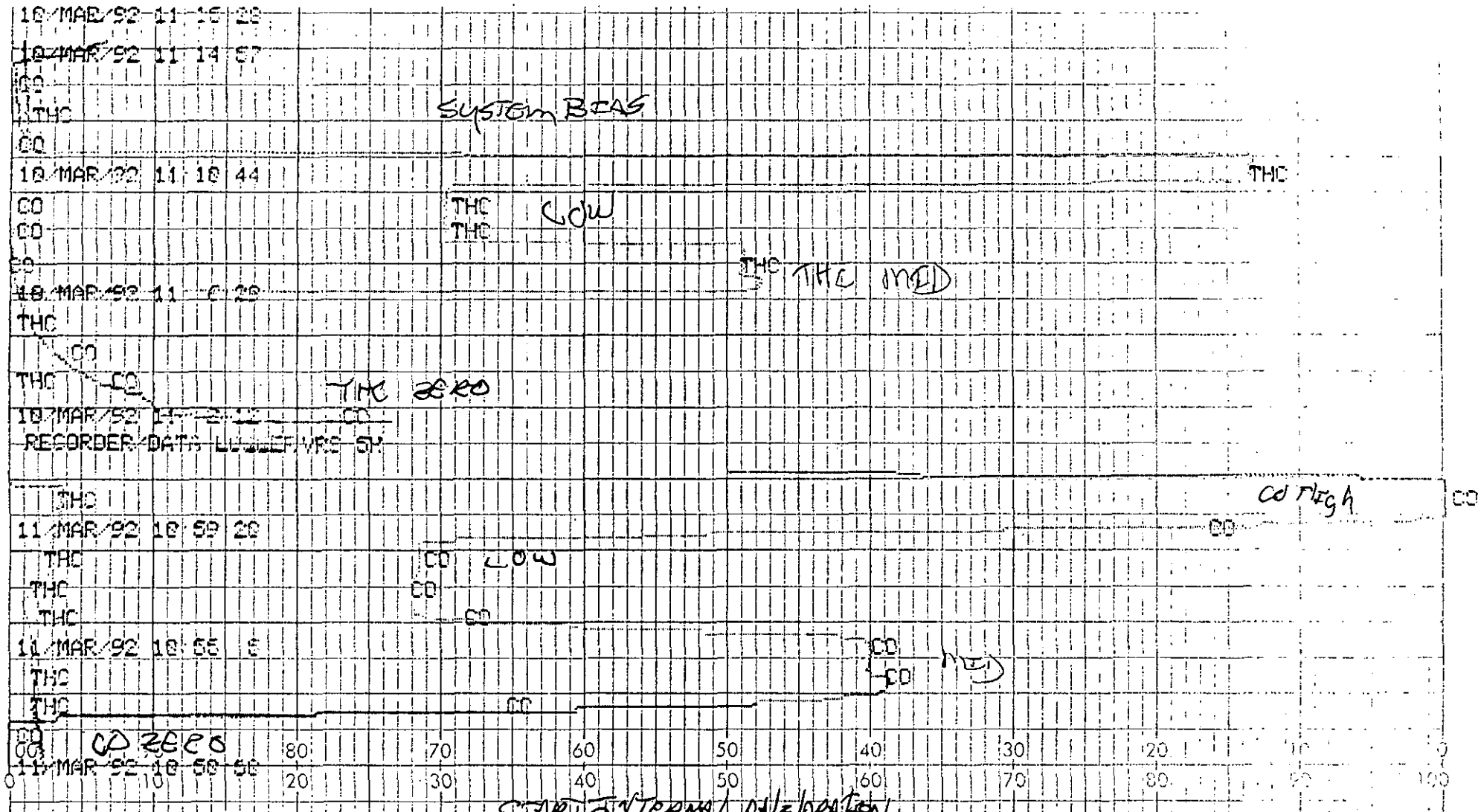
THC

CO

11 MAR 92 7 11 12

RECORDER DATA LOGGER TRC SH

RECORDER DATA LOGGER TRC SH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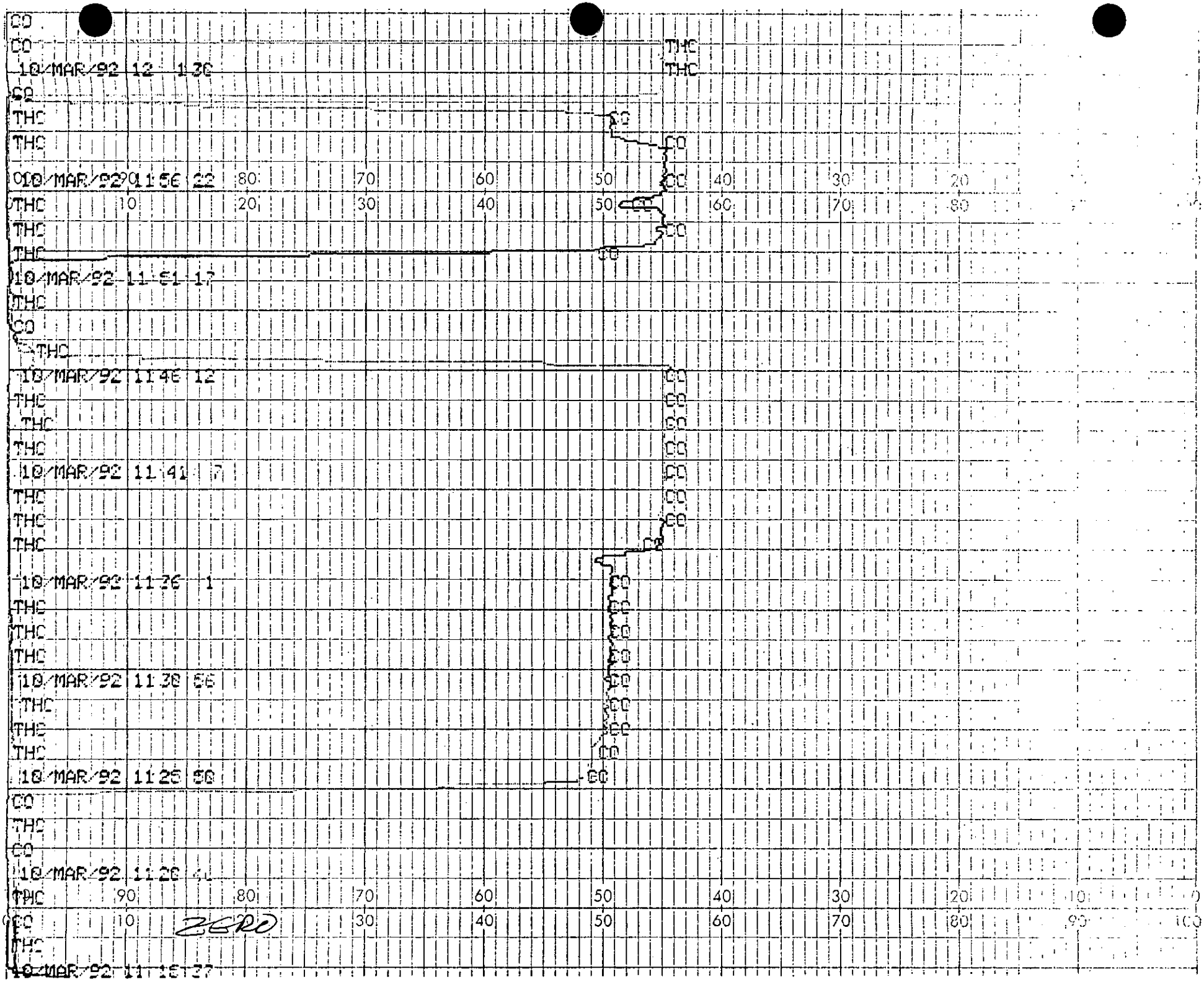
10 MAR 92 11 14 57
CO
THC
SYSTEM BIAS
CO
10 MAR 92 11 10 44
THC
CO
THC
THC
LOW
CO
THC
THC MID
10 MAR 92 11 0 20
THC
CO
THC
CO
THC ZERO
10 MAR 92 11 2 12
CO
RECORDER DATA
THC
CO HIGH
CO
11 MAR 92 10 59 20
CO
THC
CO
LOW
THC
CO
THC
CO
11 MAR 92 10 55 8
CO
THC
CO
MID
THC
CO
CO
CO ZERO
11 MAR 92 10 50 56
0
10
20
30
40
50
60
70
80
90
100
START INTERNAL CALIBRATION


CO
CO
10/MAR/92 12 1 30
CO
THC
THC
THC
THC
10/MAR/92 11 56 22
THC
THC
THC
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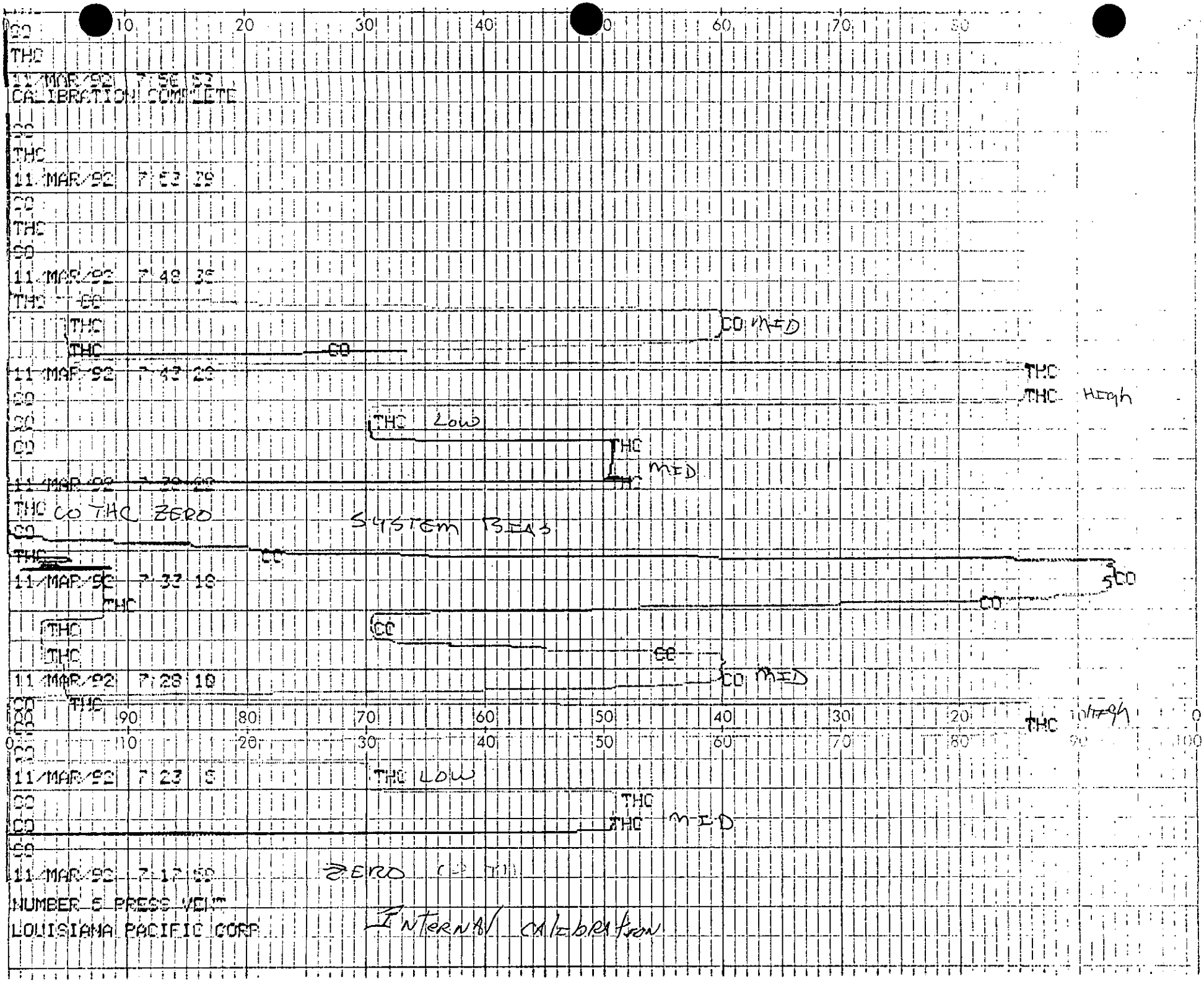
THC
CO
THC
10/MAR/92 11 46 12
THC
THC
THC
10/MAR/92 11 41 7
THC
THC
THC
10/MAR/92 11 36 1
THC
THC
THC
10/MAR/92 11 30 56
THC
THC
THC
10/MAR/92 11 25 50
CO
THC
CO
10/MAR/92 11 20 46
THC
CO
THC
10/MAR/92 11 16 37
90 80 70 60 50 40 30 20 10 0
10 20 30 40 50 60 70 80 90 100
ZERO

100 90 80 70 60 50 40 30 20

0 10 20 30 40 50 60 70 80

10/MAR 12 E 35


CO
THC
11 MAR 92 7 56 52
CALIBRATION COMPLETE
CO
THC
11 MAR 92 7 53 29
CO
THC
CO
11 MAR 92 7 48 35
THC CO
THC
THC
CO
CO MED
11 MAR 92 7 43 20
THC
THC High
CO
CO
THC Low
CO
THC
MED
11 MAR 92 7 38 00
THC CO THC ZERO
SYSTEM BIAS
CO
THC
CO
11 MAR 92 7 32 10
5 CO
THC
CO
THC
THC
CO
CO
CO MED
11 MAR 92 7 28 10
CO
THC
THC High
CO
11 MAR 92 7 23 5
THC LOW
CO
THC
THC MED
CO
11 MAR 92 7 17 50
ZERO
NUMBER 5 PRESS VENT
LOUISIANA PACIFIC CORP
INTERNAL CALIBRATION

THC

11 MAR 92 8 47 49

THC

11 MAR 92 8 42 44

THC

11 MAR 92 908 37 29

THC

11 MAR 92 8 32 34

THC

11 MAR 92 8 27 26

THC

11 MAR 92 8 22 21

THC

11 MAR 92 8 17 16

THC

11 MAR 92 8 12 11

THC

11 MAR 92 8 7 6

THC

11 MAR 92 8 2 2

11/MAR/92 9:43 10

THC

THC

THC High

11/MAR/92 9:38 11

THC MED

THC MED LOW

THC

11/MAR/92 9:33 7

THC ZERO

THC

EXTERNAL BIAS

THC

11/MAR/92 9:28 2

THC High

THC LOW

THC

THC MID

11/MAR/92 9:22 52 ZERO

RECALIBRATE FOR ZERO TO 100 RANGE

Internal calibration

THC

CO

90 80 70 60 50 40 30 20

11/MAR/92 9:17 16

10 20 30 40 50 60 70 80

THC

CO

THC

11/MAR/92 9:9 14

CO

THC

CO

11/MAR/92 9:3 9

THC

CO

THC

11/MAR/92 8:58 0

CO

THC

CO

11/MAR/92 8:52 52

THC

11 MAR 92 10 28 13
CO THC
CO THC
CO THC
80 70 60 50 40 30 20

11 MAR 92 10 33 5
20 30 40 50 60 70 80
CO THC
CO THC
CO THC

11 MAR 92 10 28 2
CO THC
CO THC
CO THC

11 MAR 92 10 22 54
CO THC
CO THC
CO THC

11 MAR 92 10 17 56
CO THC
CO THC
CO THC

11 MAR 92 10 12 46
CO THC
CO THC
CO THC

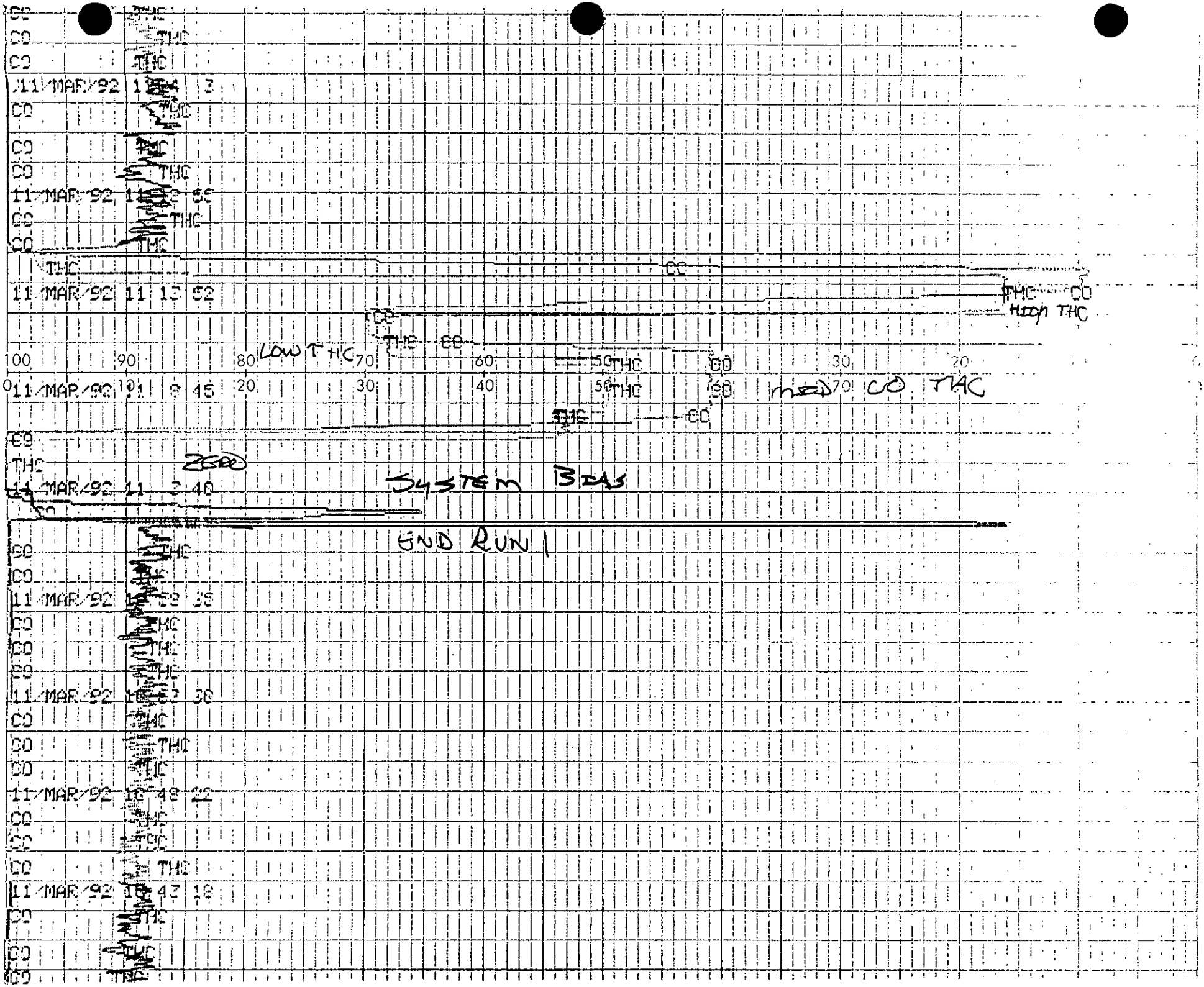
11 MAR 92 10 7 37
CO THC
CO THC
CO THC

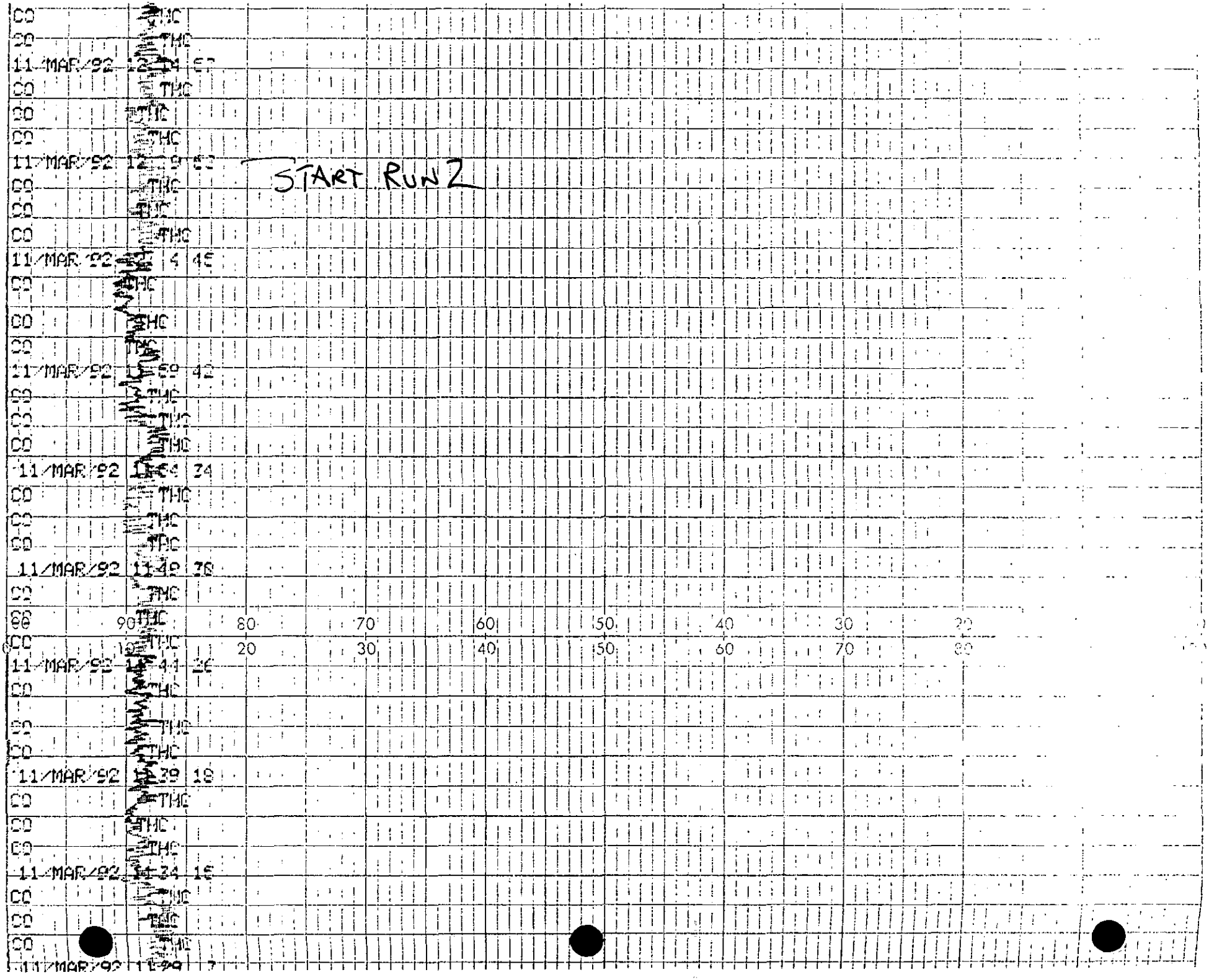
11 MAR 92 10 2 33
CO THC
CO THC
CO THC
90 80 70 60 50 40 30 20 10 0

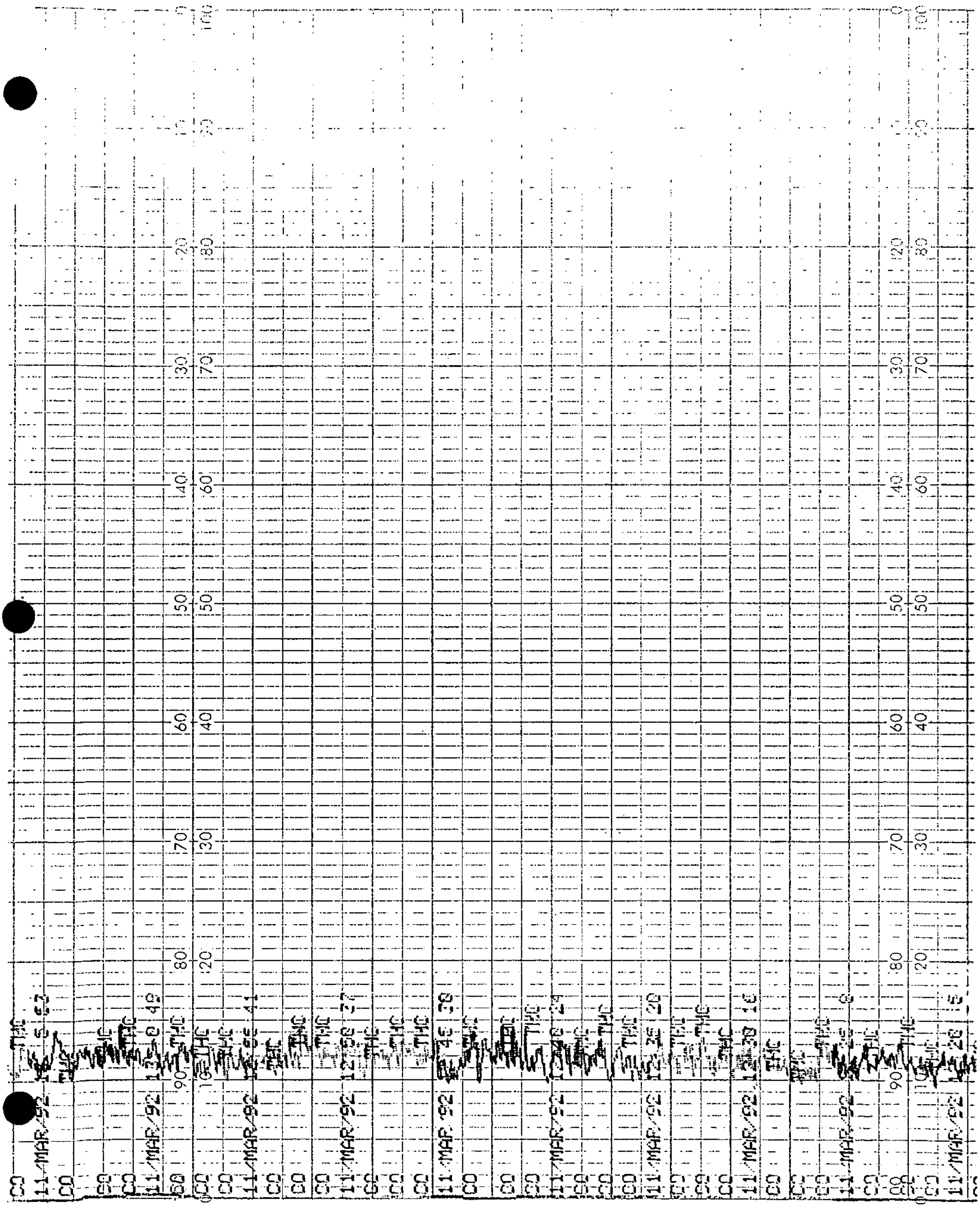
11 MAR 92 10 57 29
20 30 40 50 60 70 80 90 100
CO THC
CO THC
CO THC

START RUN 1

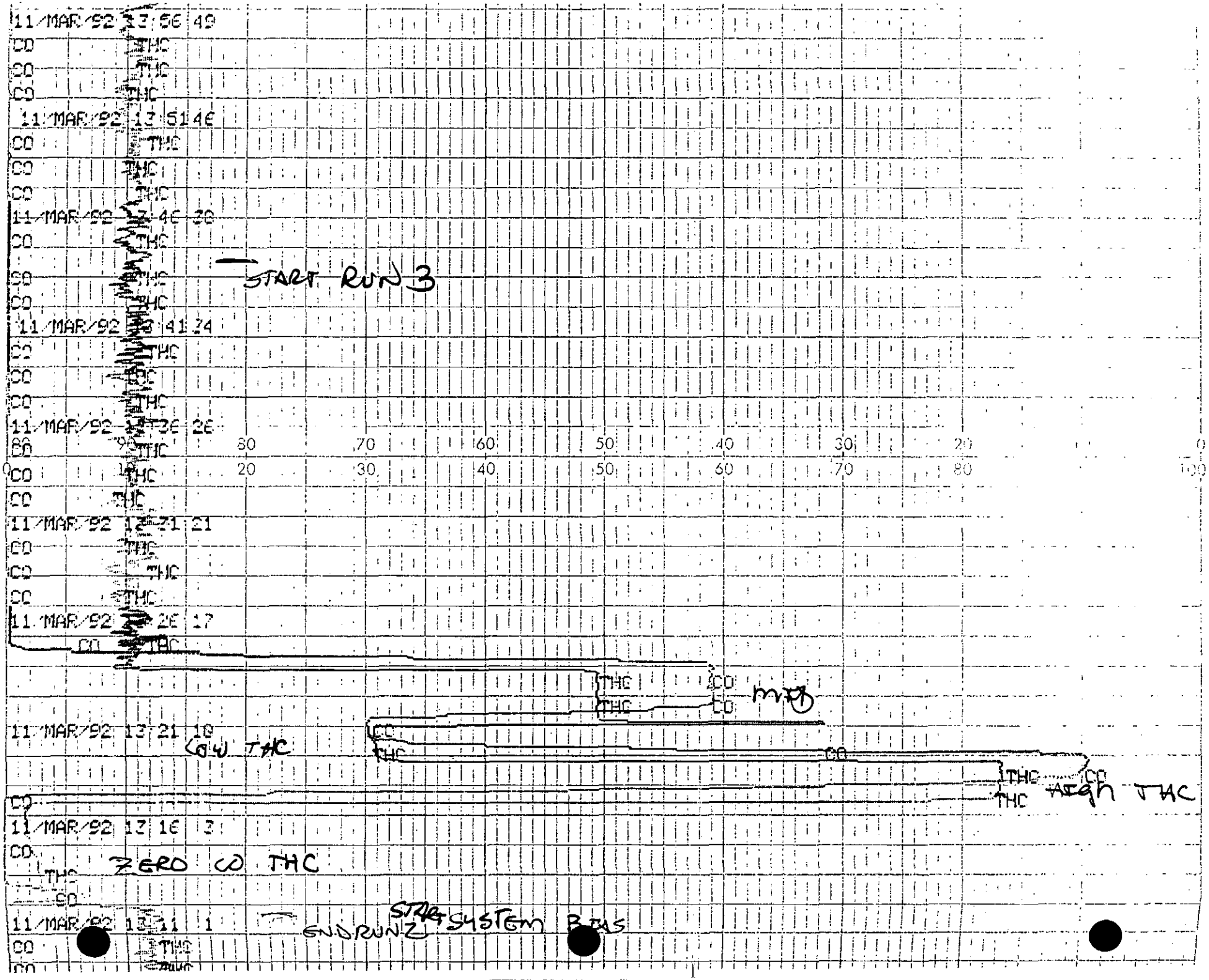
11 MAR 92 9 49 22
CO THC
CO THC


CO
THC
11/MAR/92 11 04 3
11/MAR/92 11 08 55
11/MAR/92 11 12 52
11/MAR/92 11 16 45
11/MAR/92 11 20 40
11/MAR/92 11 24 35
11/MAR/92 11 28 30
11/MAR/92 11 32 22
11/MAR/92 11 36 18
High THC
LOW THC
mod CO THC
2500
SYSTEM BIAS
END RUN 1


START RUN 2
11/MAR/92
THC
90 80 70 60 50 40 30 20
10 20 30 40 50 60 70 80



CO
THC
11/MAR/92


11/MAR/92 13:56:49
CO
THC
START RUN 3
11/MAR/92 13:41:24
11/MAR/92 13:21:21
11/MAR/92 13:21:10
LOW THC
11/MAR/92 13:16:3
ZERO CO THC
11/MAR/92 13:11:1
END RUN 2
STRG SYSTEM BIAS
HIGH THC
80 70 60 50 40 30 20 0
0 20 30 40 50 60 70 80 100

System

STOP RUN 3

CO THC

CO THC

11/MAR/92 14 42 29

CO THC

CO THC

CO THC

11/MAR/92 14 37 36

CO THC

CO THC

CO THC

11/MAR/92 14 32 29

CO THC

CO THC

CO THC

11/MAR/92 14 27 24

CO THC

CO THC

CO THC

11/MAR/92 14 22 16

CO THC

CO THC

CO THC

11/MAR/92 14 17 12

CO THC

CO THC

CO THC

11/MAR/92 14 12 8

CO THC

CO THC

CO THC

11/MAR/92 14 7 1

CO THC

CO THC

CO THC

11/MAR/92 14 1 [illegible]

CO THC

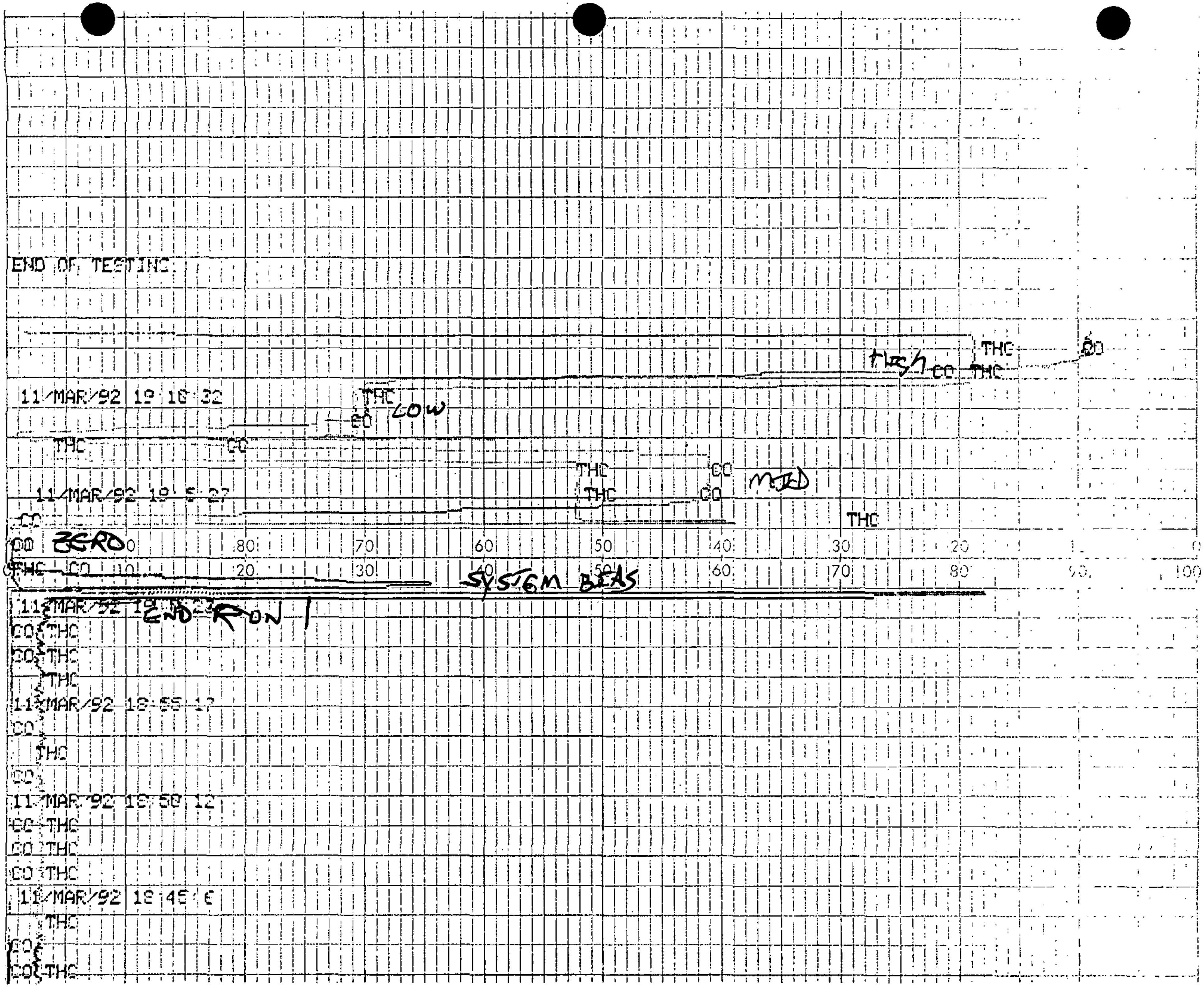
CO THC

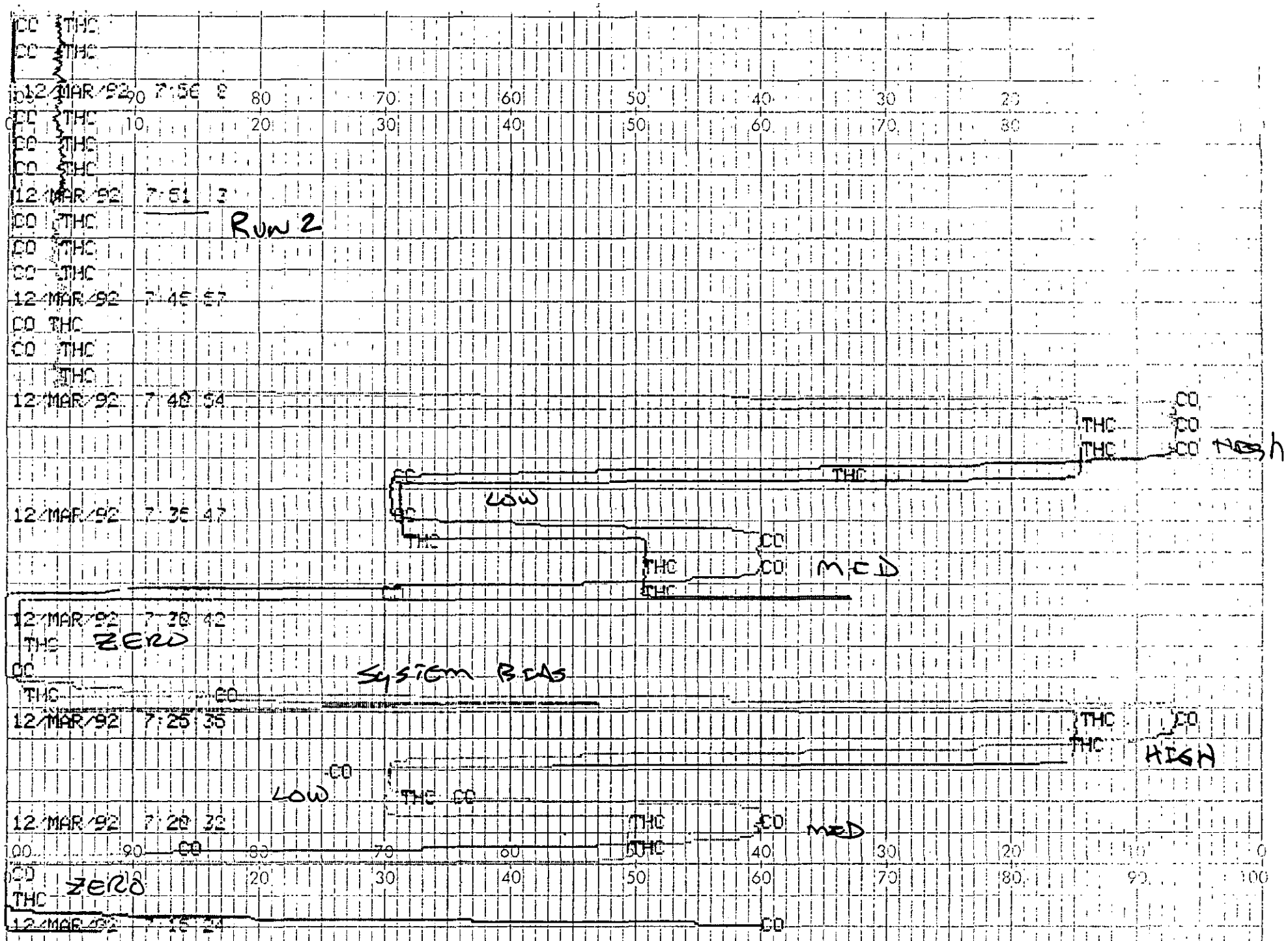
11/MAR/92 18 40 0
THC
CO
THC
11/MAR/92 18 34 55
CO
CO THC
THC
11/MAR/92 18 29 50
CO
100 THC 90 80 70 60 50 40 30 20 10 0
0 CO 10 20 30 40 50 60 70 80 90 100
11/MAR/92 18 24 45
THC
CO
THC
11/MAR/92 18 19 39
CO
CO THC
THC
11/MAR/92 18 14 34
CO
CO THC
CO THC
11/MAR/92 18 9 29
THC
CO
CO THC
11/MAR/92 18 4 20
CO THC
CO THC
CO THC
11/MAR/92 17 59 14

— START RUN 1
#4 PRESS VENT

CO
THC High THC

11/MAR/92 14 52 51
CO
LOW THC THC CO
CO THC MID THC CO
CO
ZERO


END OF TESTING.
THC
CO
flash
CO
THC
11/MAR/92 19 10 32
THC
LOW
CO
THC
CO
THC
CO
MID
11/MAR/92 19 5 27
THC
CO
CO
CO
ZERO
0
80
70
60
50
40
30
20
10
0
THC
CO
10
20
30
40
50
60
70
80
90
100
SYSTEM BIAS
11/MAR/92 19 0 22
END RUN 1
CO THC
CO THC
THC
11/MAR/92 18 55 17
CO
THC
CO
11/MAR/92 18 50 12
CO THC
CO THC
CO THC
11/MAR/92 18 45 6
THC
CO
CO THC


CO THC
12 MAR 92 7:56 8
12 MAR 92 7:51 3
RUN 2
12 MAR 92 7:46 57
12 MAR 92 7:40 54
THC
CO
HIGH
LOW
12 MAR 92 7:35 47
MED
12 MAR 92 7:30 42
ZERO
SYSTEM BIAS
12 MAR 92 7:25 35
HIGH
LOW
12 MAR 92 7:20 32
MED
ZERO
12 MAR 92 7:15 24
INTERNAL CALIBRATION
RESUME TESTING NUMBER 4 PRESS VENT

CO THC
12/MAR/92 8 47 5
CO THC
CO THC
CO THC
12/MAR/92 8 42 0
CO THC
CO THC
CO THC
12/MAR/92 8 36 53
CO THC
CO THC
CO THC
12/MAR/92 908 31 48 80 70 60 50 40 30 20 10 0
CO THC 10 20 30 40 50 60 70 80 90 100
CO THC
CO THC
12/MAR/92 8 26 42
CO THC
CO THC
CO THC
12/MAR/92 8 21 37
CO THC
CO THC
CO THC
12/MAR/92 8 16 31
CO THC
CO THC
CO THC
12/MAR/92 8 11 25
CO THC
CO THC
CO THC
12/MAR/92 8 6 20
CO THC
CO THC
CO THC
12/MAR/92 8 1 14

12/MAR/92 9 33 1
CO THC
CO THC
CO THC
12/MAR/92 9 32 55
CO THC
CO THC
CO THC
12/MAR/92 9 27 49
CO THC
CO THC
CO THC
12/MAR/92 9 22 44
CO THC
CO THC — KVN 3
CO THC
12/MAR/92 9 17 38
CO THC
CO THC
CO THC
12/MAR/92 9 12 32
CO THC
CO THC
CO THC
12/MAR/92 9 7 27
CO THC
THC
CO
THC
high
12/MAR/92 9 2 24
CO
low
THC
CO
THC
CO
mid
CO
THC
12/MAR/92 8 57 15
zero
THC
CO
system 1223
CO THC
CO THC — END KVN 2
12/MAR 8 52 11
CO THC

12/MAR/92 10:28:08
CO ZERO
THC CO
CO THC
12/MAR/92 10:22:51 END RUN 3 START SYSTEM BIAS
CO THC
THC
CO 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
12/MAR/92 10:18:44
CO THC
CO THC
CO THC
12/MAR/92 10:17:42
CO THC
CO THC
CO THC
12/MAR/92 10:8:36
CO THC
CO THC
CO THC
12/MAR/92 10:3:36
CO THC
CO THC
CO THC
12/MAR/92 9:58:24
CO THC
THC
CO
12/MAR/92 9:53:19 up 0954
CO THC
CO THC SHUT 0951
CO THC DOWN PRESS
12/MAR/92 9:48:17
CO THC
CO THC
CO THC 90 80 70 60 50 40 30 20 10 0
0 12/MAR/92 10:9:43 20 30 40 50 60 70 80 90 100
CO THC
CO THC

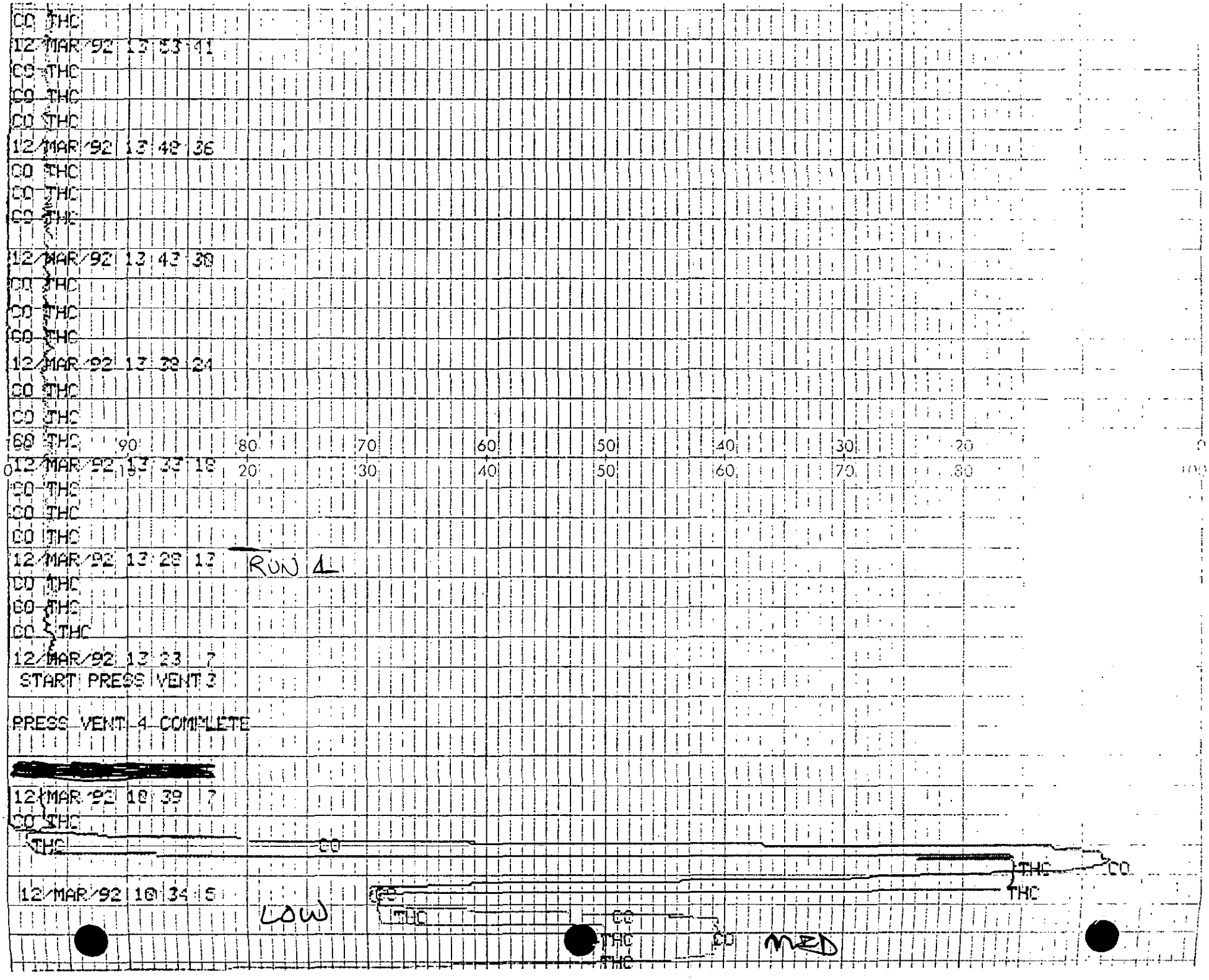
CO THC
12/MAR/92 13:53:41
CO THC
CO THC
CO THC
12/MAR/92 13:48:36
CO THC
CO THC
CO THC

12/MAR/92 13:43:30
CO THC
CO THC
CO THC
12/MAR/92 13:38:24
CO THC
CO THC
CO THC
12/MAR/92 13:33:18
CO THC
CO THC
CO THC
12/MAR/92 13:28:12 RUN 1
CO THC
CO THC
CO THC
12/MAR/92 13:23:7
START PRESS VENT 3

PRESS VENT 4 COMPLETE

[redacted]

12/MAR/92 10:39:7
CO THC



12/MAR/92 14:44:40

CO

THC — CO

CO

THC High

12/MAR/92 14:39:32 LOW

CO

THC

CO

THC

CO

MID

CO

THC

12/MAR/92 14:34:29 ZERO

CO

CO THC — STOP RUN 1 START SYSTEM BIAS

CO THC

12/MAR/92 14:29:21

CO THC

CO THC

CO THC

12/MAR/92 14:24:15

CO THC

CO THC

CO THC

12/MAR/92 14:19:9

CO THC

CO THC

CO THC

12/MAR/92 14:14:4

CO THC

CO THC

CO THC

12/MAR/92 14:8:58

CO THC

CO THC

CO THC

12/MAR/92 14:3:52

CO THC

CO THC

CO THC

12/MAR/92 13:58:47

CO THC

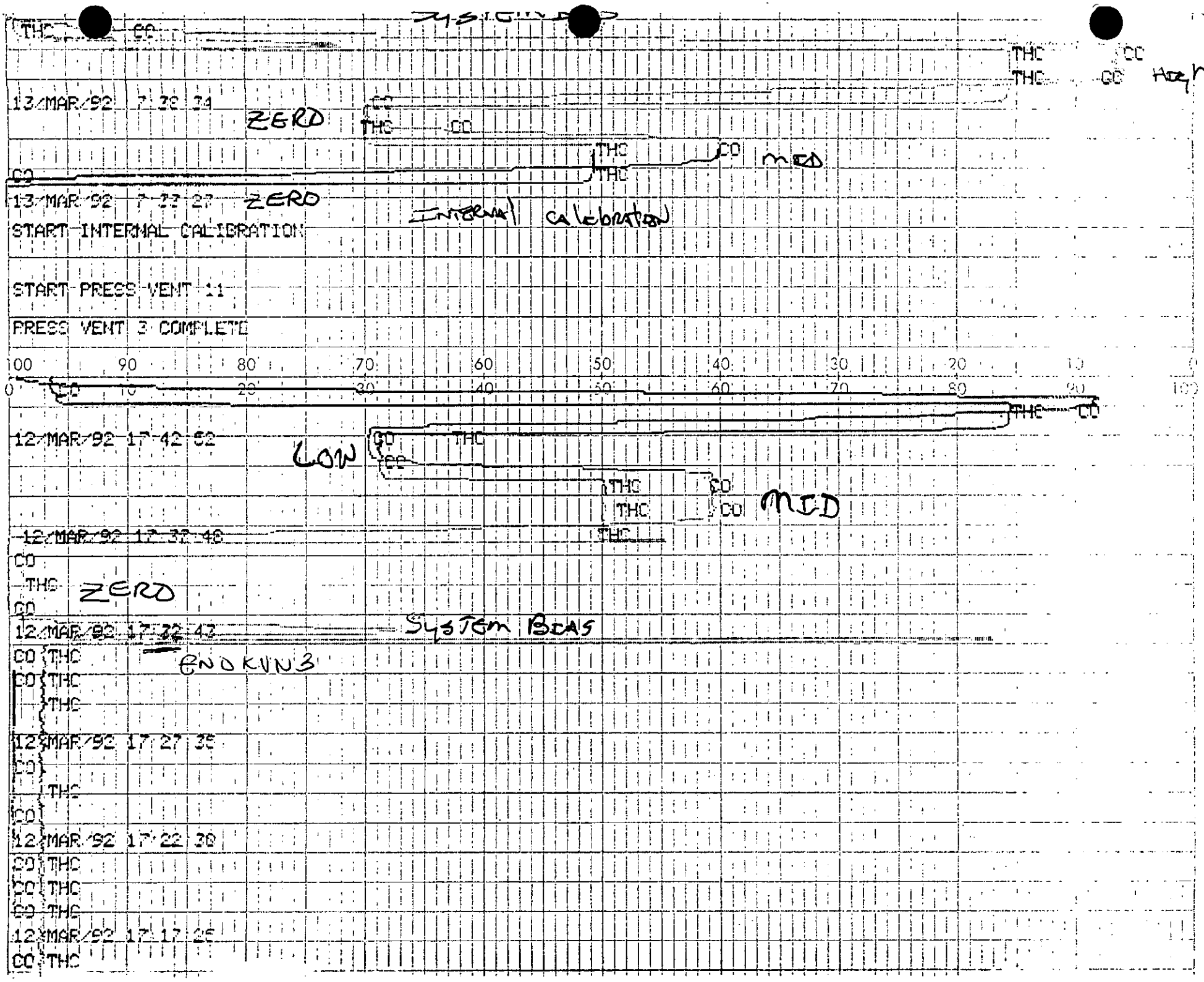
CO THC
CO THC
CO THC
12/MAR/92 15 30 28
CO THC
CO THC
CO THC
12/MAR/92 15 25 22
CO THC
CO THC
CO THC
12/MAR/92 15 20 16
CO THC
CO THC
CO THC
12/MAR/92 15 15 10
CO THC
CO THC
CO THC
12/MAR/92 15 10 5
CO THC
CO THC
CO THC
12/MAR/92 15 4 59
CO THC
CO THC
CO THC
RUN 2
12/MAR/92 14 59 57
CO THC
CO THC
CO THC
12/MAR/92 14 54 51
CO THC
CO THC
CO THC
12/MAR/92 14 49 45
CO THC
CO THC
CO THC

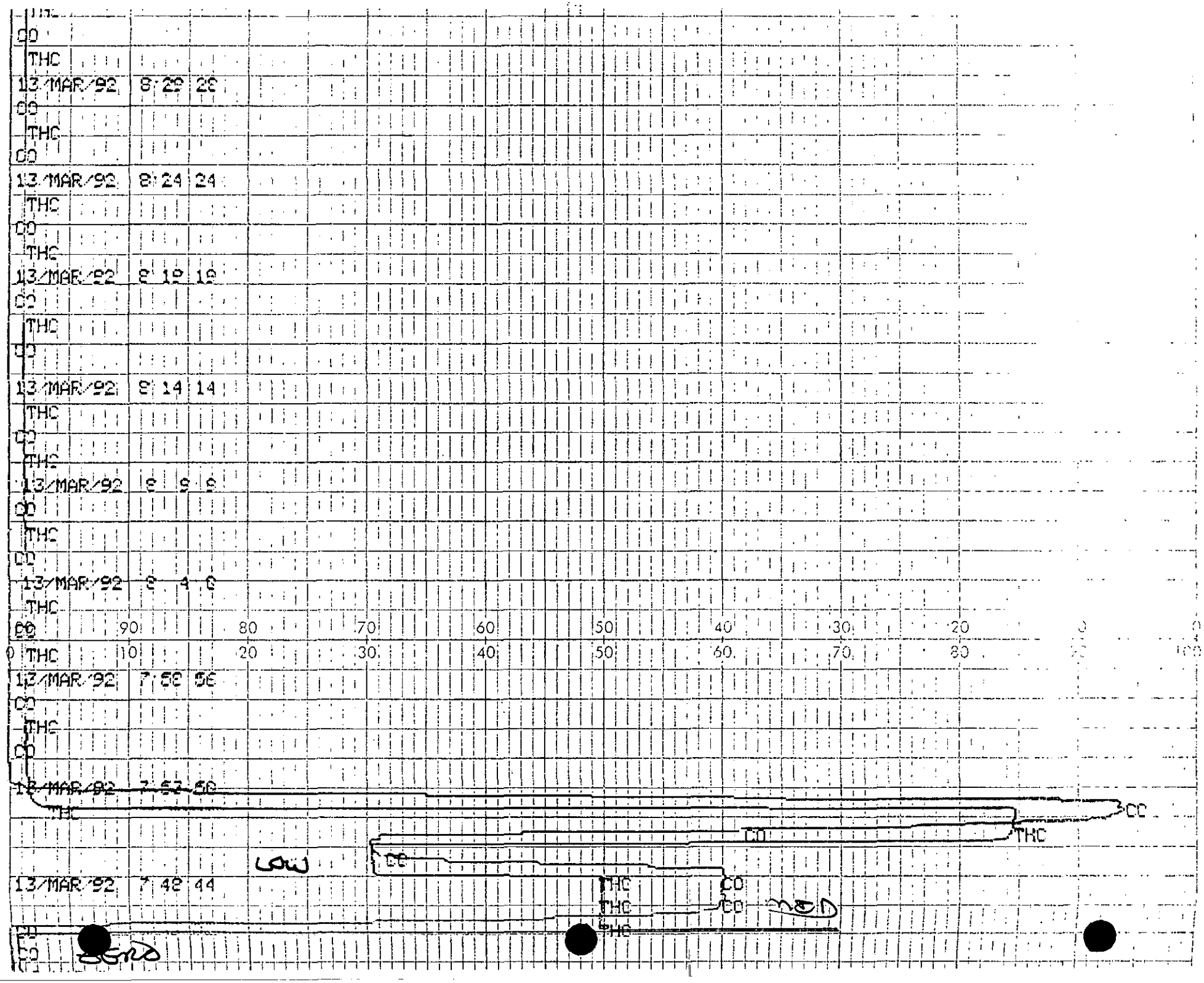
90 80 70 60 50 40 30 20

20 30 40 50 60 70 80

CO THC
CO THC
12/MAR/92 16 21 26
CO THC
CO THC
CO THC
12/MAR/92 16 16 20
THC
CO
THC High
CO
LOW THC
CO
12/MAR/92 16 11 14
THC
CO MED
THC
CO
THC
CO
S ZERO
12/MAR/92 16 6 8
System BIAS
THC CO
END RUN 2
CO THC
CO THC
12/MAR/92 16 1 1
CO THC
CO THC
CO THC
90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
12/MAR/92 15 55 55
CO THC
CO THC
CO THC
12/MAR/92 15 50 50
CO THC
CO THC
CO THC
12/MAR/92 15 45 44
CO THC
CO THC
CO THC
12/MAR/92 15 40 39
CO THC
CO THC
CO THC
12/MAR/92 15 35 33

CO THC
12 MAR 92 17 12 20
CO THC
CO THC 90 80 70 60 50 40 30 20
CO THC 10 20 30 40 50 60 70 80
12 MAR 92 17 7 14
CO THC
CO THC
CO THC
12 MAR 92 17 2 8
CO THC
CO THC
CO THC
12 MAR 92 16 57 4
CO THC
CO THC
CO THC
12 MAR 92 16 51 56
CO THC
CO THC
CO THC
12 MAR 92 16 46 53
CO THC
CO THC
CO THC
12 MAR 92 16 41 47
CO THC
CO THC
CO THC
12 MAR 92 16 36 42
CO THC
CO THC 90 80 70 60 50 40 30 20
CO THC 10 20 30 40 50 60 70 80
12 MAR 92 16 31 37
CO THC
CO THC
CO THC — 1628 START RUN 3
12 MAR 92 16 26 31


THC
CO
THC
CO
High
13 MAR 92 7 38 34
ZERO
CO
THC
CO
THC
THC
CO
MID
CO
13 MAR 92 7 37 27
ZERO
INTERNAL CALIBRATION
START INTERNAL CALIBRATION
START PRESS VENT 11
PRESS VENT 3 COMPLETE
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
CO
THC
CO
12 MAR 92 17 42 52
LOW
CO
THC
CO
THC
THC
CO
CO
MID
12 MAR 92 17 37 40
CO
THC
ZERO
CO
12 MAR 92 17 32 47
SYSTEM BIAS
CO
THC
ENOKIN3
CO
THC
THC
12 MAR 92 17 27 35
CO
THC
CO
12 MAR 92 17 22 30
CO
THC
CO
THC
CO
THC
12 MAR 92 17 17 26
CO
THC


CO
THC
13/MAR/92 8:29 29
CO
THC
CO
13/MAR/92 8:24 24
THC
CO
THC
13/MAR/92 8:19 19
CO
THC
CO
13/MAR/92 8:14 14
THC
CO
THC
13/MAR/92 8:9 9
CO
THC
CO
13/MAR/92 8:4 0
THC
CO
90 80 70 60 50 40 30 20
THC
10 20 30 40 50 60 70 80
13/MAR/92 7:59 59
CO
THC
CO
13/MAR/92 7:54 50
THC
CO
CO
THC
CO
13/MAR/92 7:49 44
THC
CO
THC
CO
THC
CO
CO

THC

13/MAR/92 9:20 25

CO

THC

CO

13/MAR/92 9:15 20

CO 90 80 70 60 50 40 30 20

THC 10 20 30 40 50 60 70 80

CO

THC

13/MAR/92 9:10 15

CO

THC

CO

13/MAR/92 9:5 10

THC

CO

THC

13/MAR/92 9:0 2

CO

THC

CO

13/MAR/92 8:54 57

THC

CO

THC

13/MAR/92 8:49 52

CO

THC

CO

13/MAR/92 8:44 47

THC

CO

THC

13/MAR/92 8:39 42

CO

CO 90 80 70 60 50 40 30 20 10 0

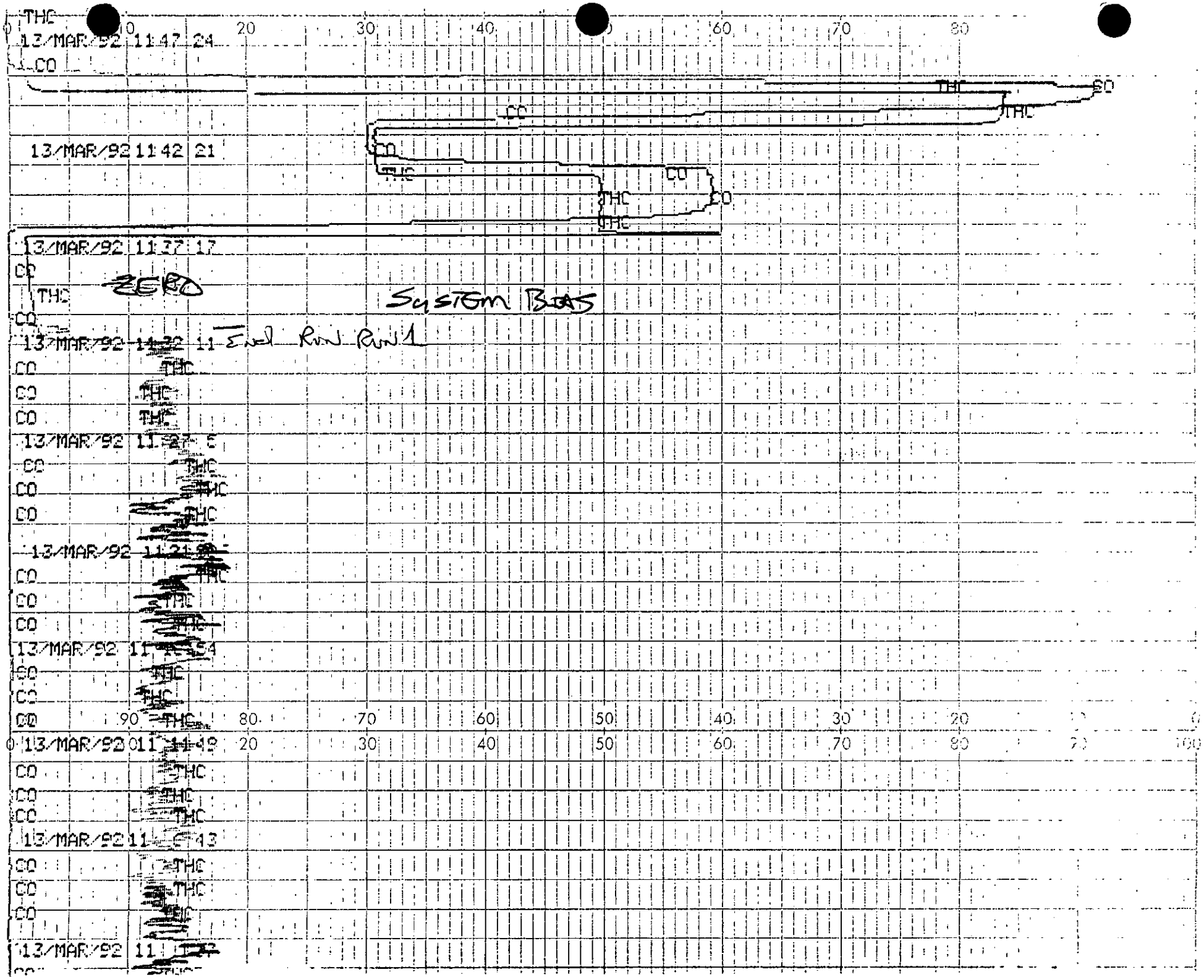
THC 10 20 30 40 50 60 70 80 90 100

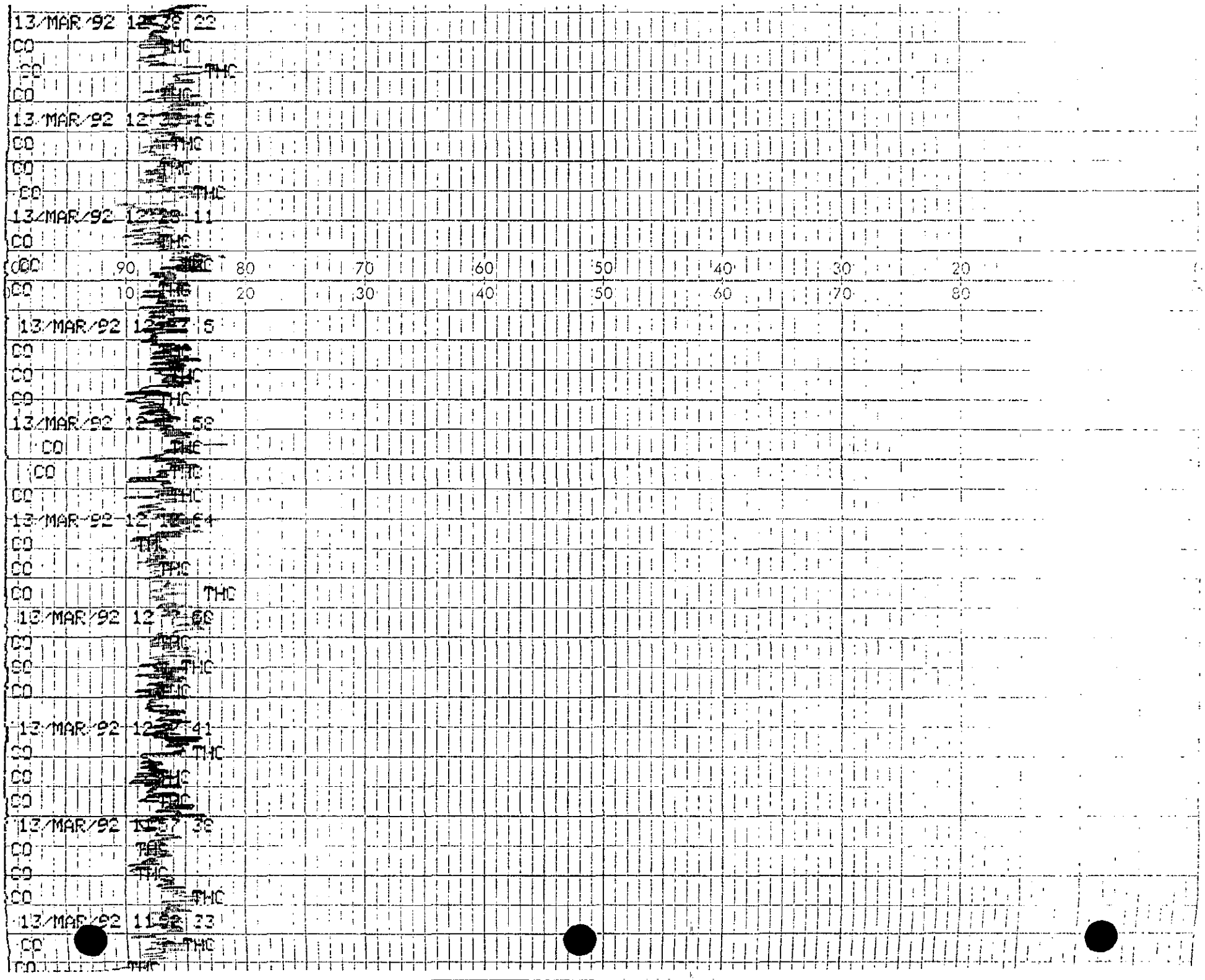
CO

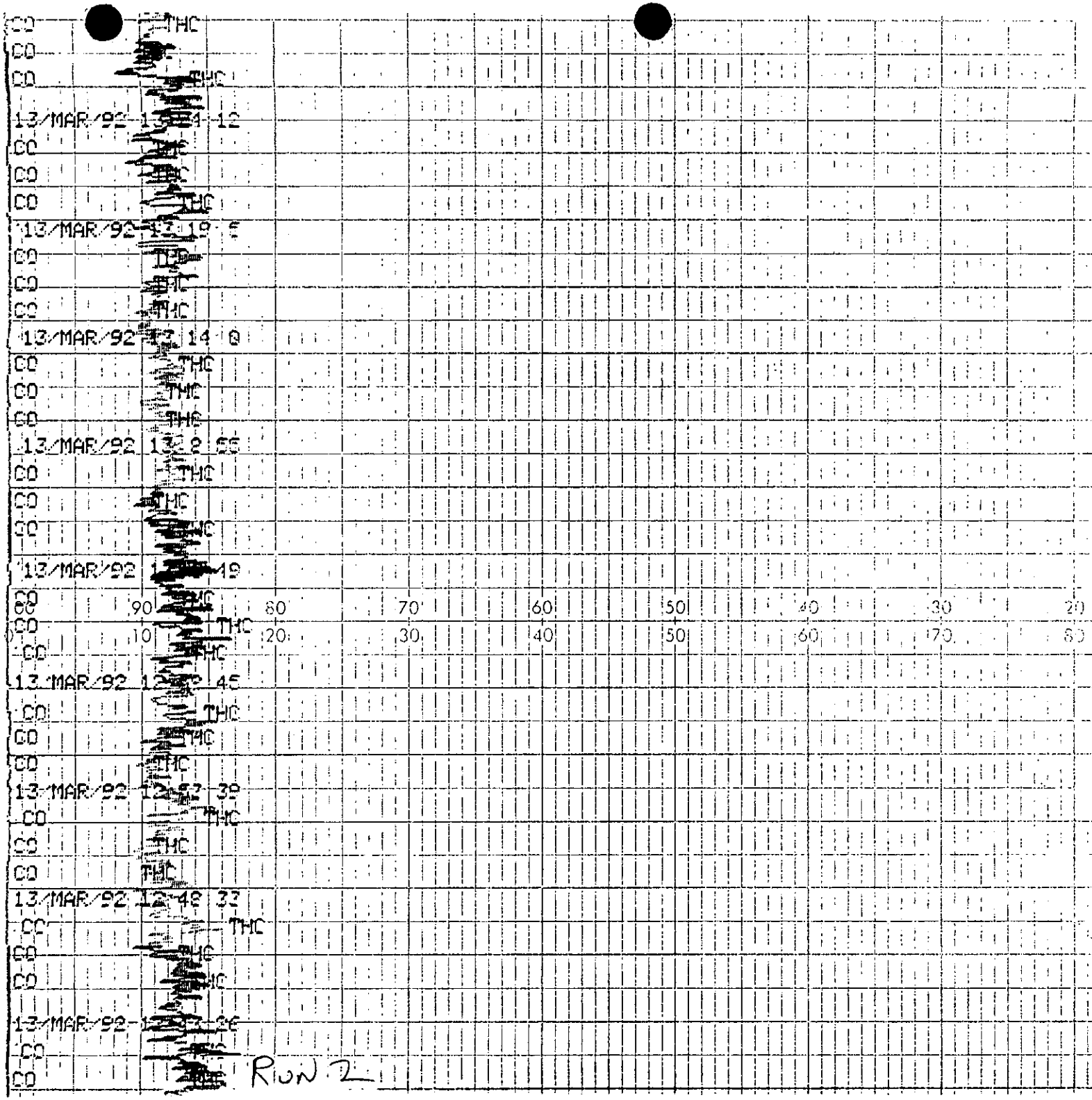
13/MAR/92 8:34 33

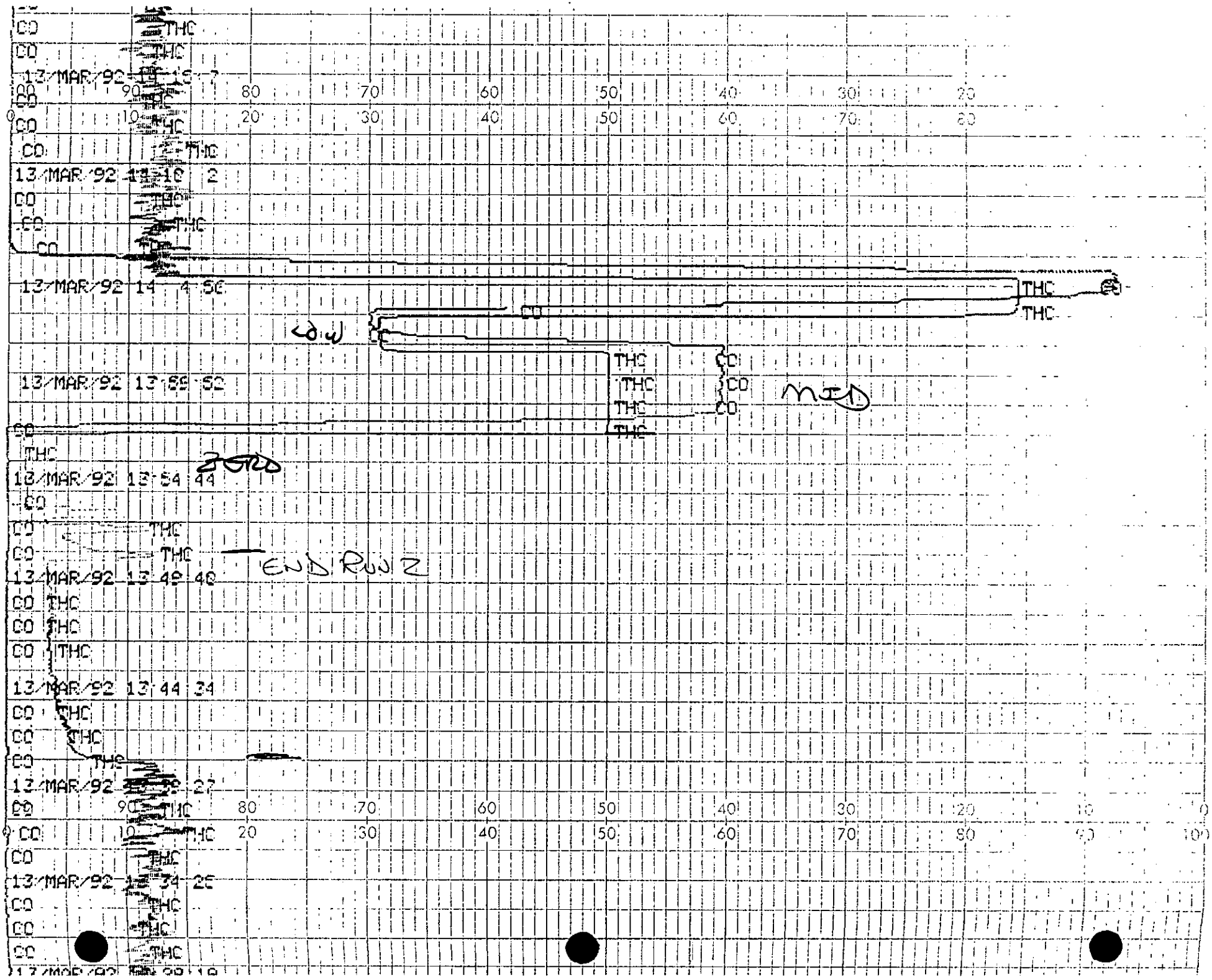
CO THC
CO THC
13/MAR/92 10 [illegible] 20
CO THC
CO THC
CO THC
13/MAR/92 10 51 24
CO THC
CO THC
CO THC
13/MAR/92 10 46 17
CO THC
CO THC
CO THC
13/MAR/92 10 41 13
CO THC
CO THC
CO THC
13/MAR/92 10 36 7
CO THC
CO THC
CO THC
13/MAR/92 10 31 4
CO THC
CO THC
CO THC
13/MAR/92 10 25 57
CO THC
CO THC
CO THC
13/MAR/92 10 20 50 — START RUN 1
CO
THC
13/MAR/92 9 30 35
CO
THC
CO
13/MAR/92 9 25 30
THC

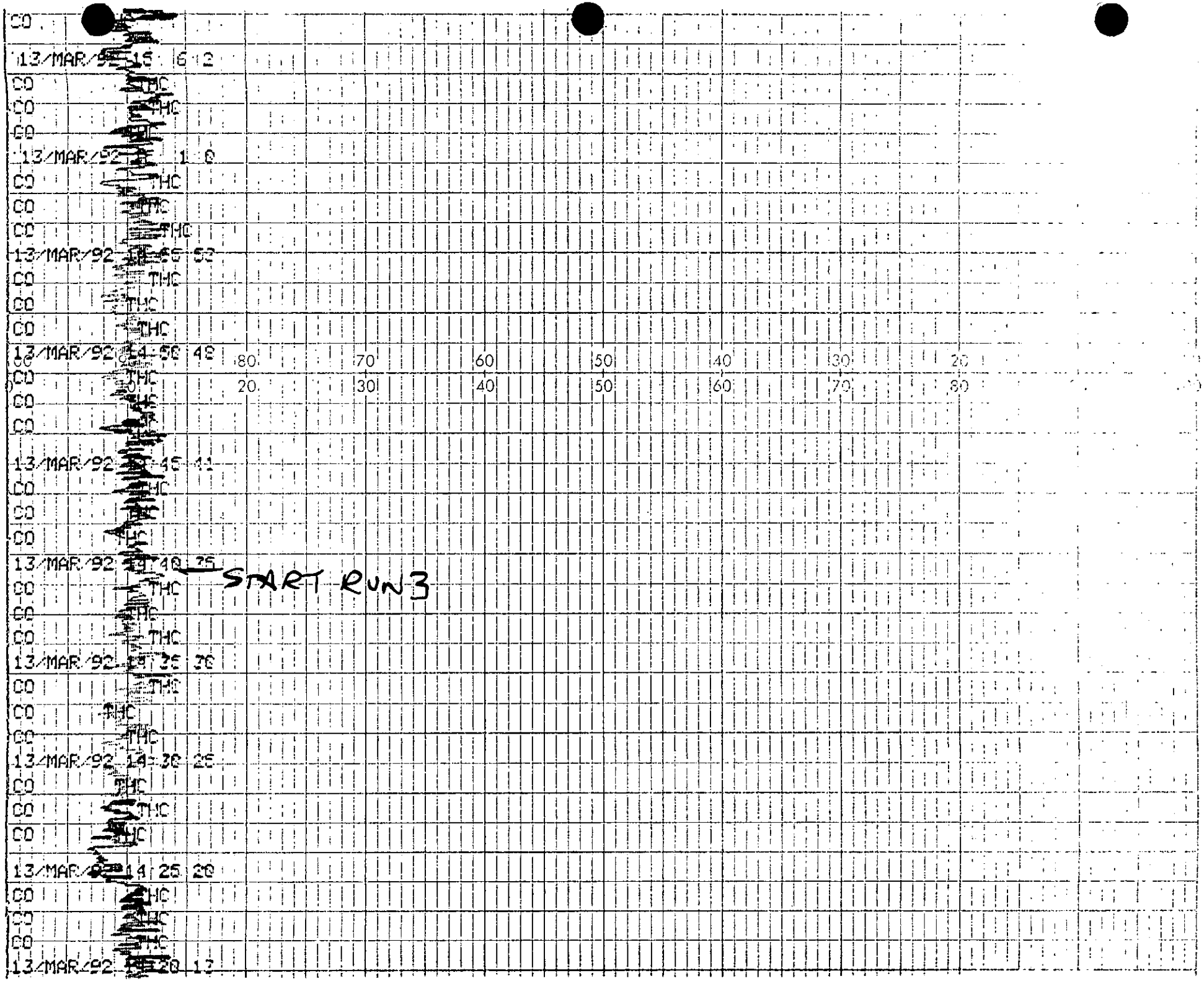
80 70 60 50 40 30 20 10 0
20 30 40 50 60 70 80 90 100

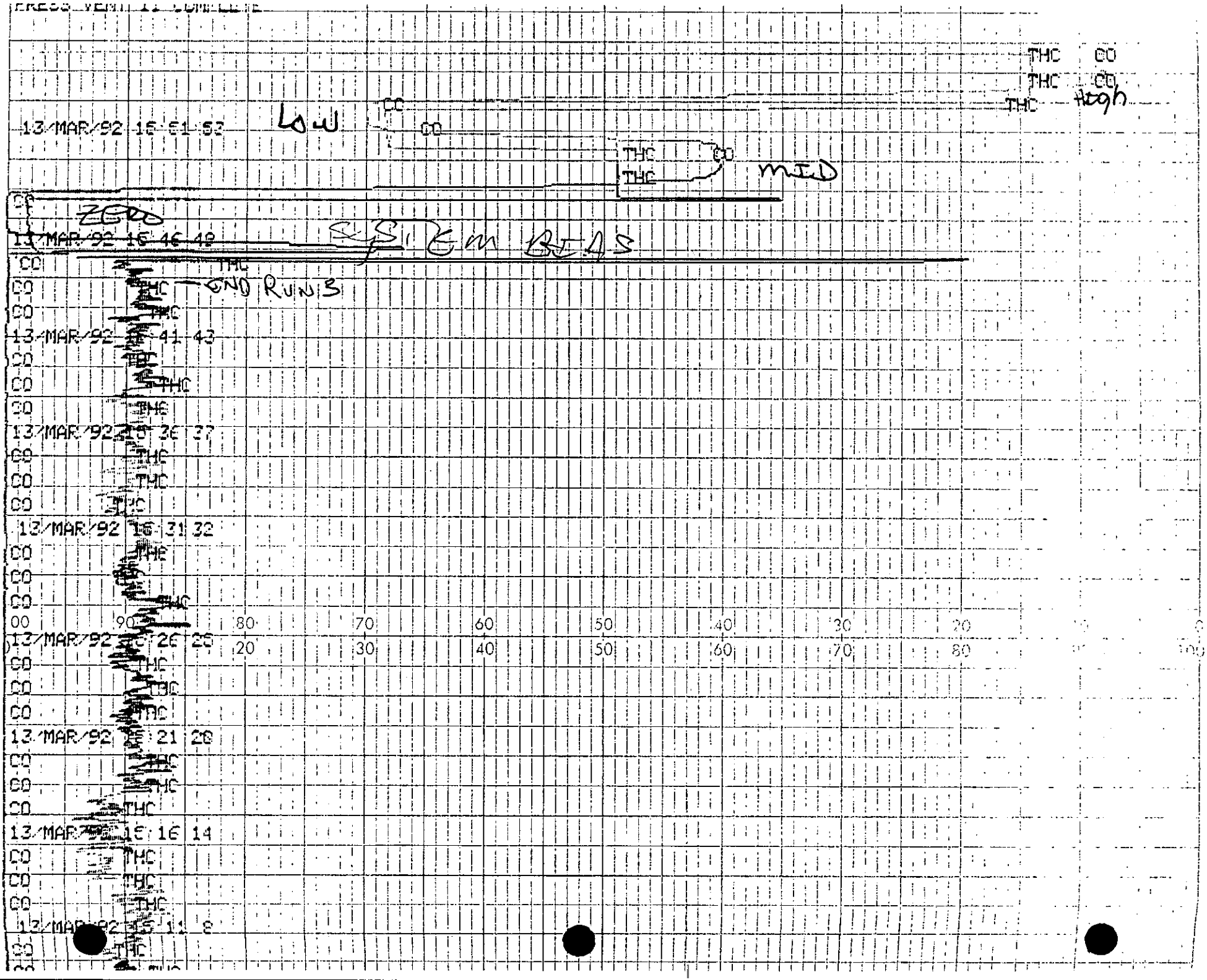

THC
13/MAR/92 11:47:24
CO
THC
CO
THC
13/MAR/92 11:42:21
CO
THC
CO
THC
CO
THC
13/MAR/92 11:37:17
CO
THC
ZERO
System Bias
CO
13/MAR/92 11:32:11 End Run Run 1
CO
THC
CO
THC
CO
THC
13/MAR/92 11:27:5
CO
THC
CO
THC
CO
THC
13/MAR/92 11:21:
CO
THC
CO
THC
CO
THC
13/MAR/92 11:
CO
THC
CO
THC
CO
THC
13/MAR/92 11:11:49
CO
THC
CO
THC
CO
THC
13/MAR/92 11:
CO
THC
CO
THC
CO
13/MAR/92 11:
CO
THC


13/MAR/92 12 38 22
CO
THC
CO
THC
CO
THC
13/MAR/92 12 38 16
CO
THC
CO
THC
CO
THC
13/MAR/92 12 38 11
CO
THC
CO
THC
90
80
70
60
50
40
30
20
CO
THC
10
20
30
40
50
60
70
80
13/MAR/92 12 37 5
CO
CO
THC
CO
THC
13/MAR/92 12 36 58
CO
THC
CO
THC
CO
THC
13/MAR/92 12 36 54
CO
THC
CO
THC
CO
THC
13/MAR/92 12 36 50
CO
THC
CO
THC
CO
THC
13/MAR/92 12 36 41
CO
THC
CO
THC
CO
THC
13/MAR/92 12 36 36
CO
THC
CO
THC
CO
THC
13/MAR/92 12 36 33
CO
THC
CO
THC


CO
THC
13/MAR/92
90
80
70
60
50
40
30
20
10
Run 2


CO
THC
13/MAR/92 14 4 56
13/MAR/92 13 59 52
13/MAR/92 13 54 44
13/MAR/92 13 49 40
13/MAR/92 13 44 34
13/MAR/92 13 34 26
LOW
MID
HIGH
END RUN 2
90
80
70
60
50
40
30
20
10
0
100


CO
13/MAR/92 15 6 12
CO THC
CO THC
CO
13/MAR/92 1 0
CO THC
CO THC
CO THC
13/MAR/92 14 56 52
CO THC
CO THC
CO THC
13/MAR/92 14 50 48
80 70 60 50 40 30 20
20 30 40 50 60 70 80
CO THC
CO
CO
13/MAR/92 14 45 41
CO THC
CO
CO THC
13/MAR/92 14 40 36
START RUN 3
CO THC
CO THC
CO THC
13/MAR/92 14 35 36
CO THC
CO THC
CO THC
13/MAR/92 14 30 26
CO THC
CO THC
CO THC
13/MAR/92 14 25 20
CO THC
CO THC
CO THC
13/MAR/92 14 20 17


THC
CO
THC
CO
THC
High
13/MAR/92 16 51 53
LOW
CO
CO
THC
CO
THC
MID
CO
ZERO
13/MAR/92 16 46 48
SYSTEM BLAS
CO
THC
CO
THC
END RUNS
CO
THC
13/MAR/92 16 41 43
CO
THC
CO
THC
CO
THC
13/MAR/92 16 36 37
CO
THC
CO
THC
CO
THC
13/MAR/92 16 31 32
CO
THC
CO
CO
THC
CO
90
80
70
60
50
40
30
20
13/MAR/92 16 26 28
20
30
40
50
60
70
80
CO
THC
CO
THC
CO
THC
13/MAR/92 16 21 23
CO
THC
CO
THC
CO
THC
13/MAR/92 16 16 14
CO
THC
CO
THC
CO
THC
13/MAR/92 16 11 8
CO
THC

14/MAR/92 8:20:12
THC
CO
THC
14/MAR/92 8:15:7
CO
CO
THC HIGH
CO
THC LOW
14/MAR/92 8:10:0
THC
THC MID
CO
THC
CO
CO MID
14/MAR/92 8:4:57
CO
ZERO
THC
CO
14/MAR/92 7:59:49
THC
Sample probe not hooked up
CO
THC
External TRACE
14/MAR/92 7:54:46
CO
THC EA
THC
CO HIGH
14/MAR/92 7:49:39
CO
THC
CO LOW
THC
CO
THC
CO MID
14/MAR/92 7:44:32
CO
THC HIGH
CO
THC LOW
CO
THC MID
14/MAR/92 7:39:25
ZERO
START PRESS VENT
Internal calibration

RECORDER/DATA LOGGER

CO THC

THC

14/MAR/92 12 14 57

CO

THC

CO

14/MAR/92 12 9 52

THC

CO

THC

14/MAR/92 12 4 47

CO

THC

CO

14/MAR/92 11 59 42

THC

CO

THC

14/MAR/92 11 54 37

14/MAR/92 8 45 41

CO

THC

CO

14/MAR/92 8 40 36

THC

CO

THC

14/MAR/92 8 35 27

CO

THC

CO

14/MAR/92 8 30 22

THC

CO

THC

14/MAR/92 8 25 17

CO

THC

90 80 70 60 50 40 30 20

20 RUN 1 30 11:65 40 50 60 70 80

CO

14/MAR/92 13 5 52

THC

CO

CO THC

14/MAR/92 12 0 47

THC

CO

THC

14/MAR/92 12 55 41

CO

THC

CO

14/MAR/92 12 50 36

THC

CO

THC

14/MAR/92 12 45 31

CO

THC

CO

14/MAR/92 12 40 27

THC

CO

THC

14/MAR/92 12 35 21

CO

CO THC

THC

14/MAR/92 12 30 12

CO

THC

CO

14/MAR/92 12 25 7

THC

CO

THC

14/MAR/92 12 20 2

Run 1 complete

14/MAR/92 13:56:48
CO
CO THC
THC
14/MAR/92 13:51:43
CO
THC
CO
14/MAR/92 13:46:38
THC
CO
CO
THC
14/MAR/92 13:41:33
CO
THC
CO
14/MAR/92 13:36:27
THC
CO
THC
14/MAR/92 13:31:22
CO
THC
CO
14/MAR/92 13:26:14
THC
CO
CO
14/MAR/92 13:21:10
CO
CO
CO
14/MAR/92 13:16:4
THC
THC
CO
THC
14/MAR/92 13:11:0
CO

90 80 70 60 50 40 30 20 0

10 20 30 40 50 60 70 80 100

THC
THC
THC High

THC Low

THC Low

THC CO

CO MID

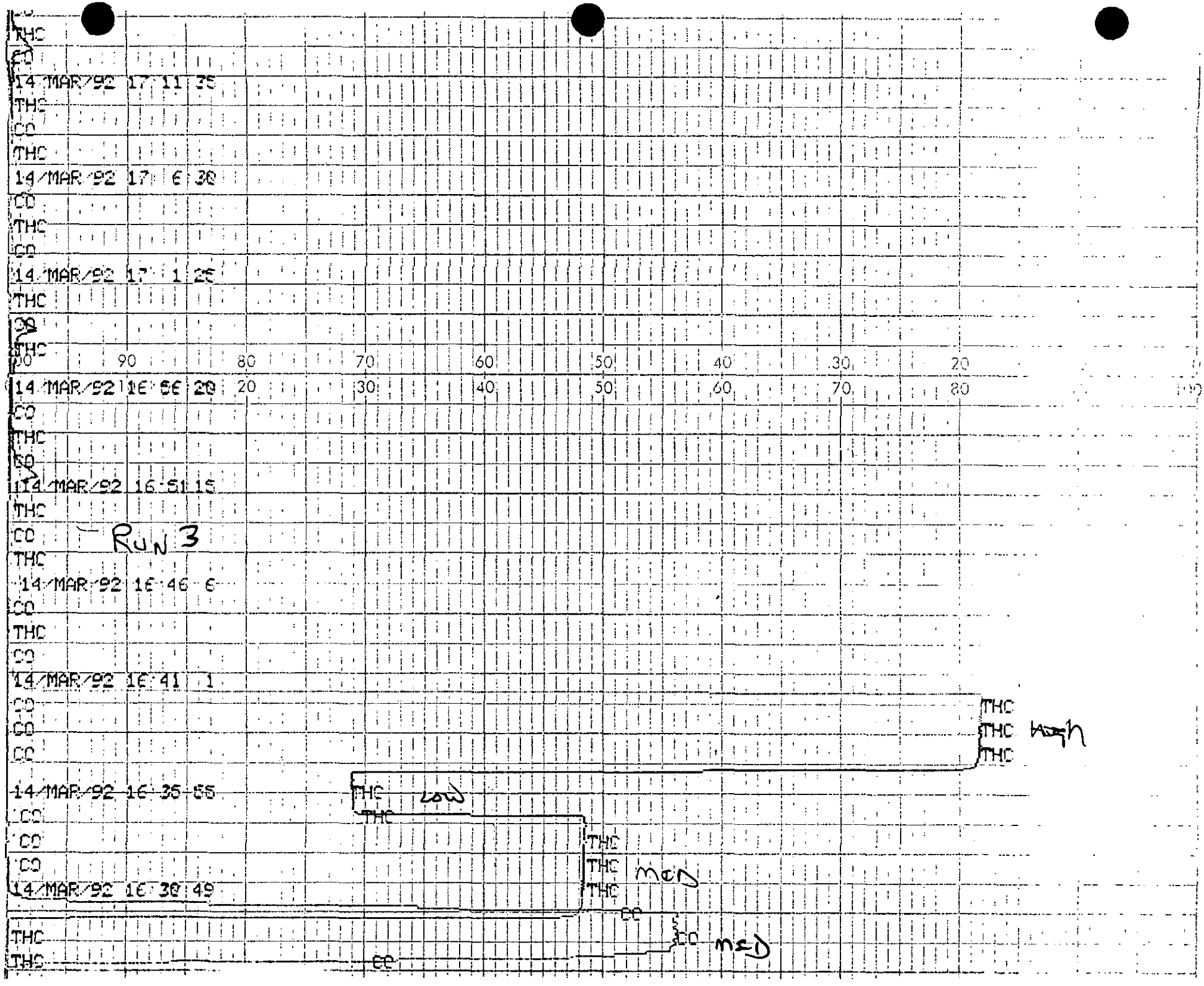
ZERO

SYSTEM DIS

14/MAR 15:34:49
CO
THC
CO
14/MAR/92 15:29:44
THC
CO
THC
14/MAR/92 15:24:39
CO
THC
CO
14/MAR/92 15:19:34
THC
CO
THC
— Run 2
14/MAR/92 15:14:25
CO
THC
CO
14/MAR/92 14:22:17
THC
CO
THC
14/MAR/92 14:17:12
CO
THC
CO
14/MAR/92 14:12:7
THC
CO
THC
14/MAR/92 14:6:58
CO
THC
CO
14/MAR/92 14:1:53
THC
CO

90 80 70 60 50 40 30 20
10 20 30 40 50 60 70 80

CO
THC
ZERO
CO
14/MAR/92 16 20 40
THC
CO
END RUN 2
THC
14/MAR/92 16 15 32
CO
THC
CO
14/MAR/92 16 10 28
THC
CO
THC
14/MAR/92 16 5 23
CO
THC
CO
14/MAR/92 16 0 18
THC
CO
THC
14/MAR/92 15 55 13
CO
THC
CO
14/MAR/92 15 50 8
THC
CO
THC
14/MAR/92 15 44 59
CO
THC
CO
14/MAR/92 15 39 54
THC
CO
THC


THC
CO
14 MAR/92 17 11 35
THC
CO
THC
14/MAR/92 17 6 30
CO
THC
CO
14 MAR/92 17 1 25
THC
CO
THC
90
80
70
60
50
40
30
20
14 MAR/92 16 56 20
CO
THC
CO
14/MAR/92 16 51 15
THC
CO
RUN 3
THC
14/MAR/92 16 46 6
CO
THC
CO
14/MAR/92 16 41 1
CO
CO
CO
THC
THC high
THC
14/MAR/92 16 35 55
CO
CO
CO
THC low
THC
THC
THC
THC med
14/MAR/92 16 30 49
CO
CO med
THC
THC
CO

CO

14/MAR/92 18 2 31

THC

THC

14/MAR/92 17 57 27

CO

THC

CO

14/MAR/92 17 52 18

THC

CO

THC

14/MAR/92 17 47 17

CO

THC

CO

14/MAR/92 17 42 8

THC

CO

THC

14/MAR/92 17 37 3

CO

THC

CO

14/MAR/92 17 31 58

THC

CO

THC

14/MAR/92 17 26 52

CO

THC

CO

14/MAR/92 17 21 46

THC

CO

THC

14/MAR/92 17 16 39

THC MED

THC

THC

CO

CO

CO MED

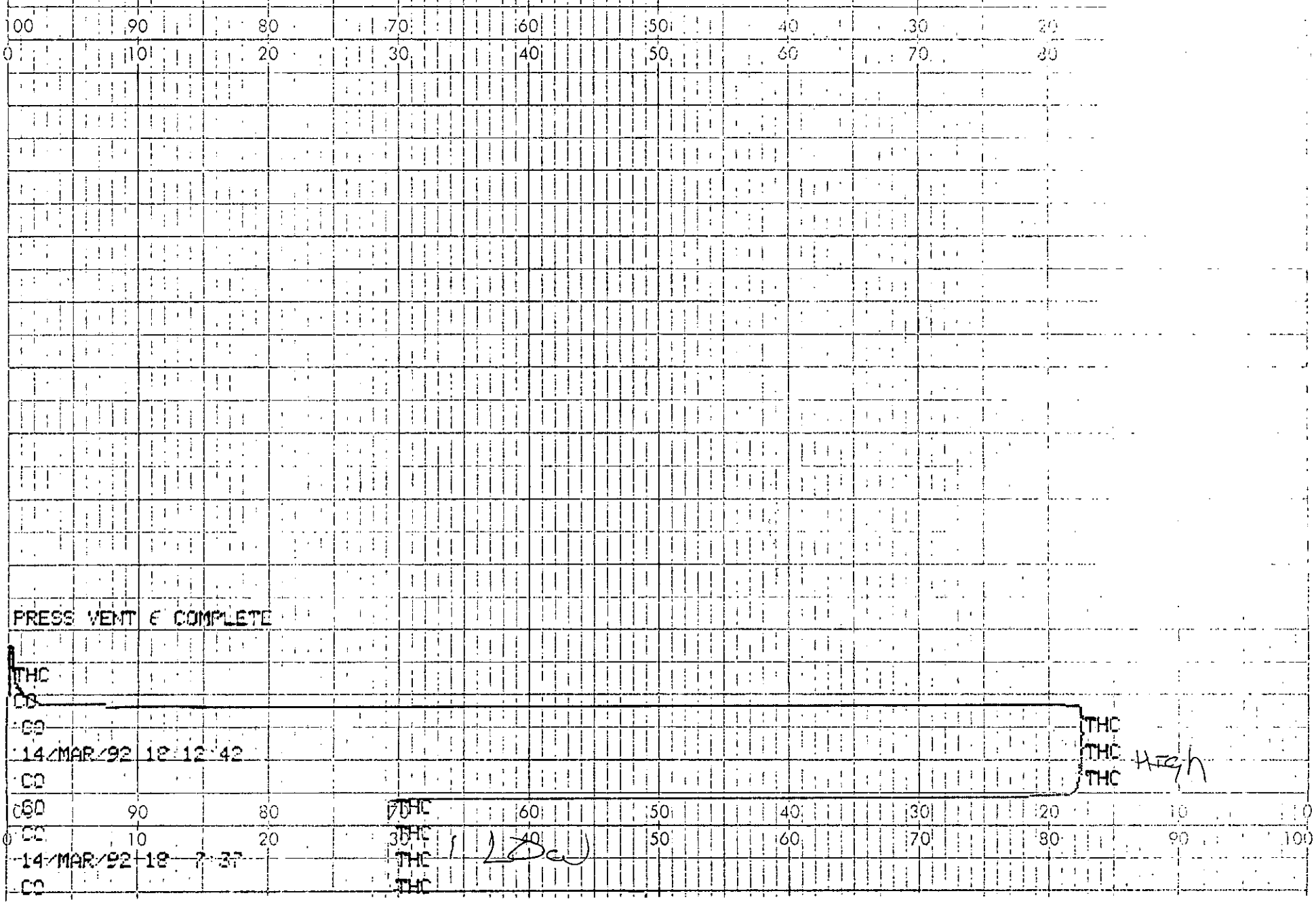
CO

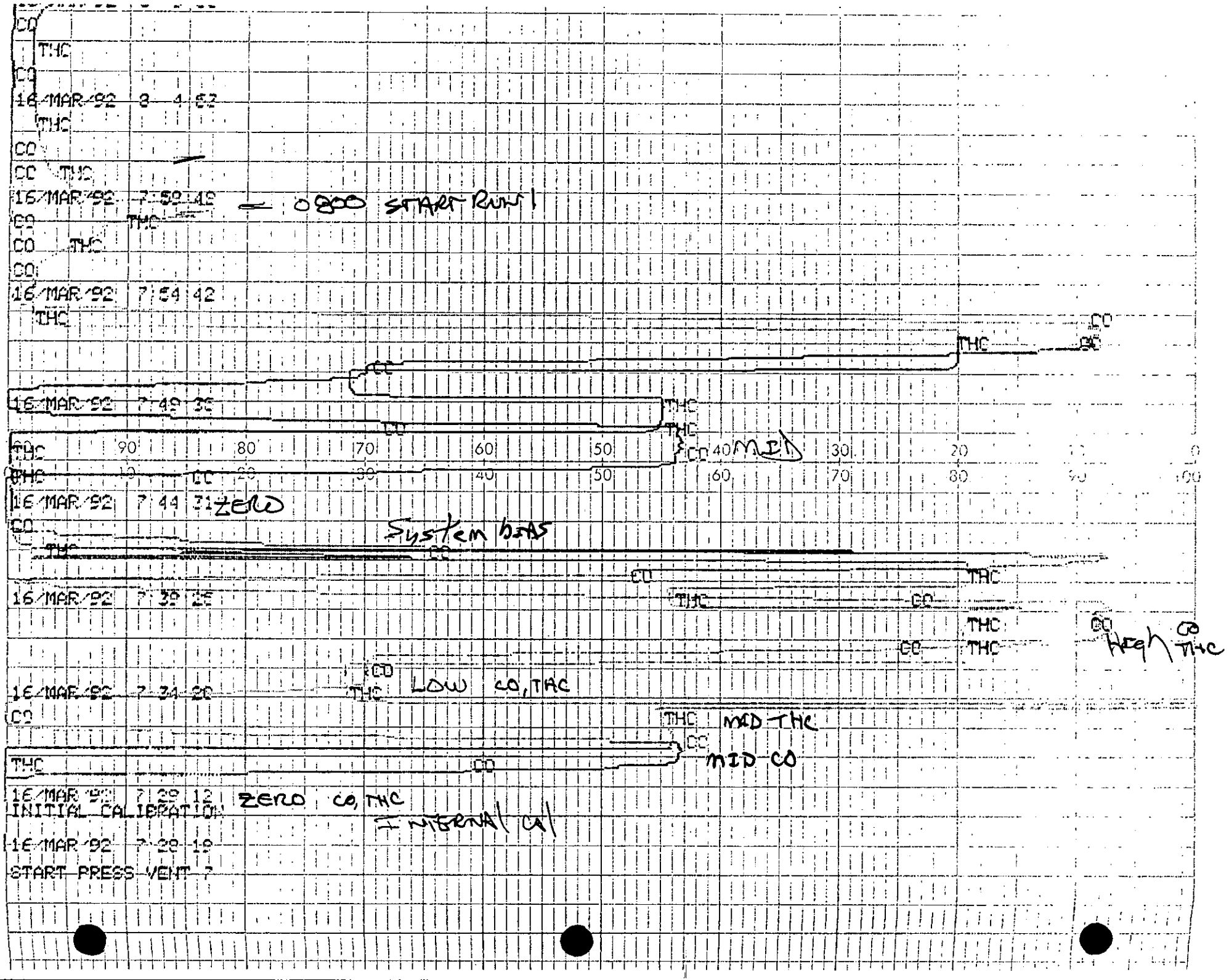
ZERO

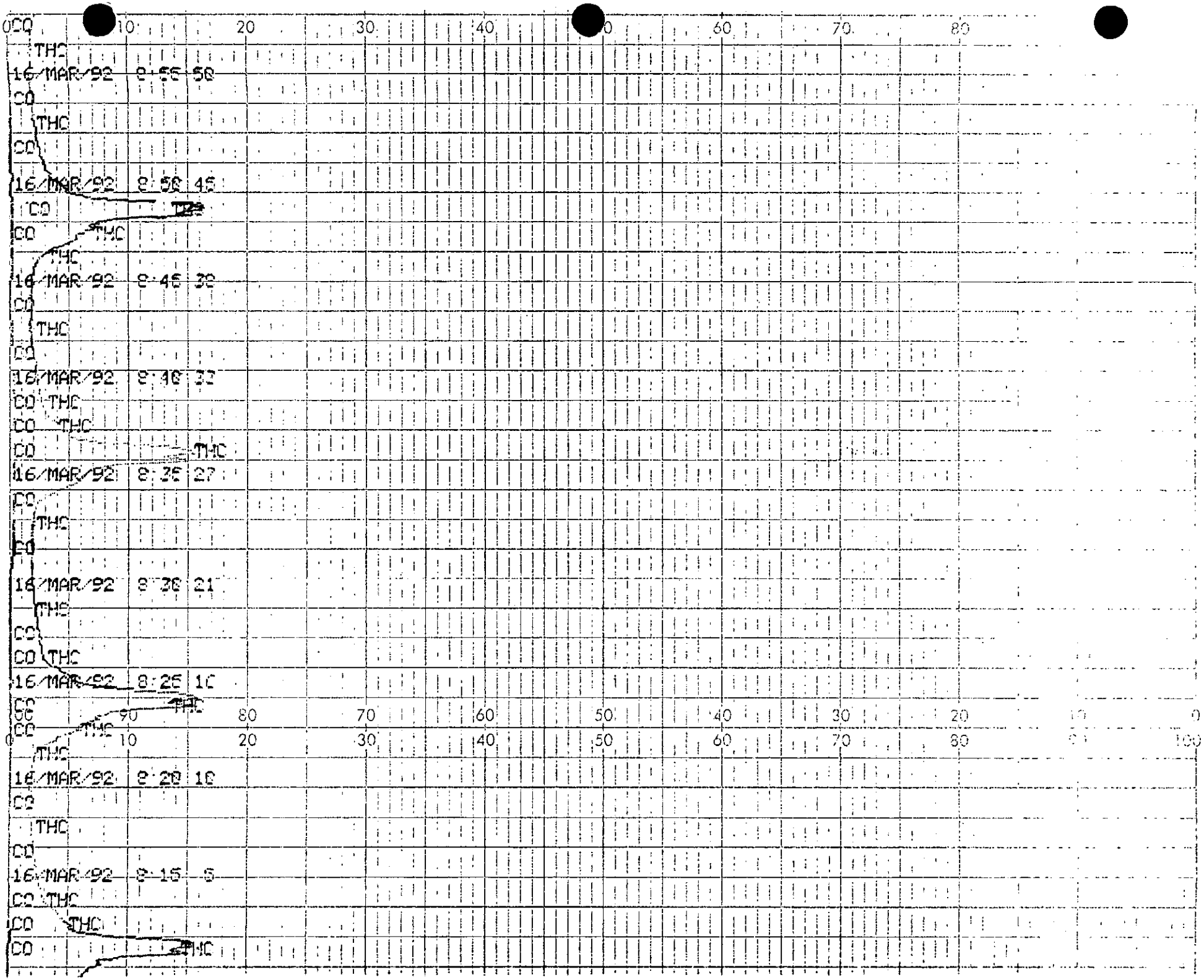
— 175 RUN3

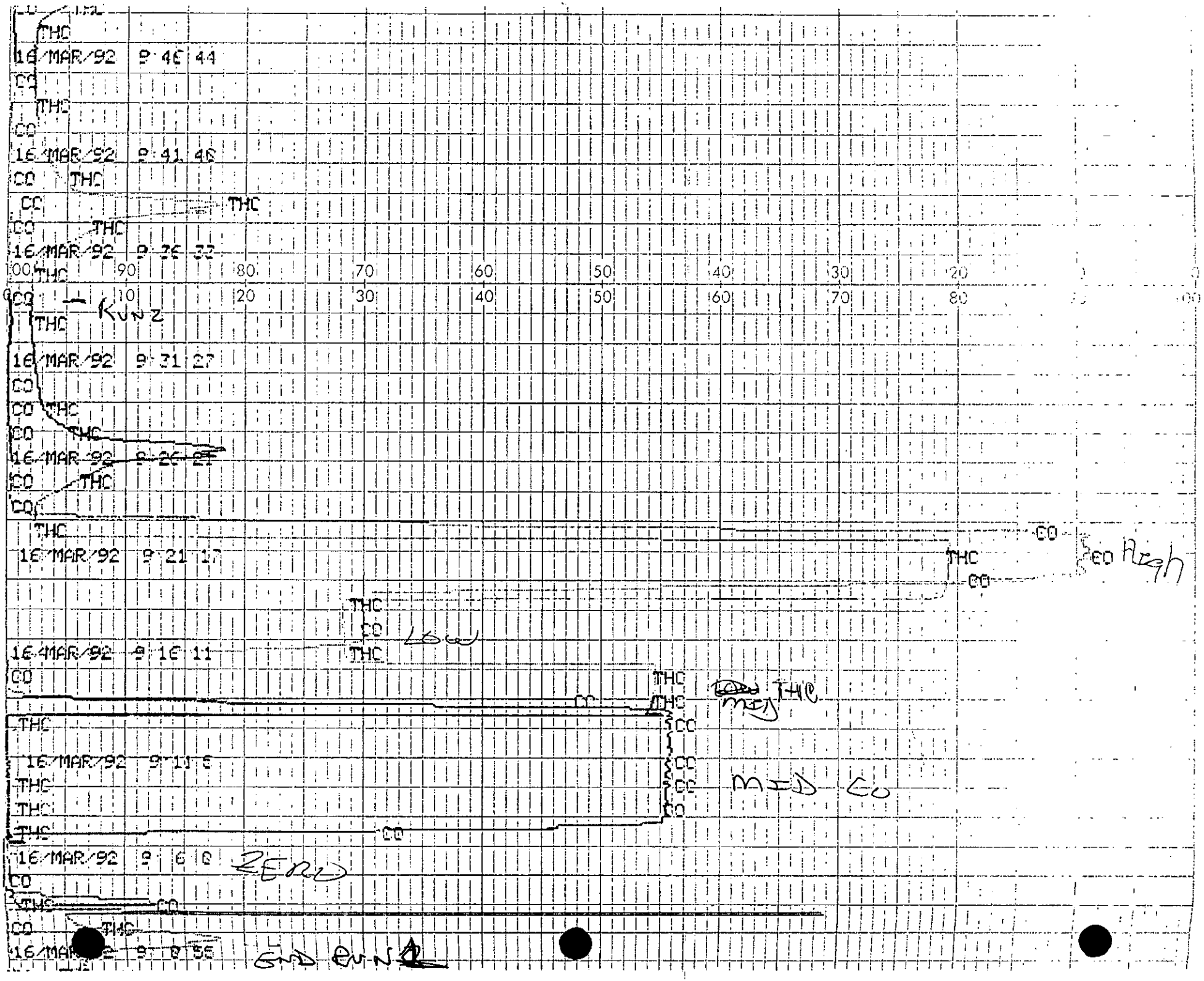
90 80 70 60 50 40 30 20 10 0

10 20 30 40 50 60 70 80 90 100


100 90 80 70 60 50 40 30 20
0 10 20 30 40 50 60 70 80
PRESS VENT & COMPLETE
THC
CO
CO
14/MAR/92 18 12 42
CO
THC
THC
THC
High
60 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
CO
14/MAR/92 18 7 37
CO
THC
THC
THC
Low


CO
THC
16 MAR 92 8 4 52
16 MAR 92 7 59 42
0800 START RUN 1
16 MAR 92 7 54 42
16 MAR 92 7 49 32
MID
90 80 70 60 50 40 30 20 10 0
10 20 30 40 50 60 70 80 90 100
16 MAR 92 7 44 31 ZERO
System bias
16 MAR 92 7 39 22
High CO THC
16 MAR 92 7 34 20
LOW CO, THC
MID THC
MID CO
16 MAR 92 7 29 12 ZERO CO, THC
INITIAL CALIBRATION
= INTERNAL CAL
16 MAR 92 7 28 19
START PRESS VENT 7


CO
THC
16/MAR/92 8:55 50
16/MAR/92 8:50 45
16/MAR/92 8:45 30
16/MAR/92 8:40 32
16/MAR/92 8:35 27
16/MAR/92 8:30 21
16/MAR/92 8:25 10
16/MAR/92 8:20 10
16/MAR/92 8:15 5
10 20 30 40 50 60 70 80
90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100

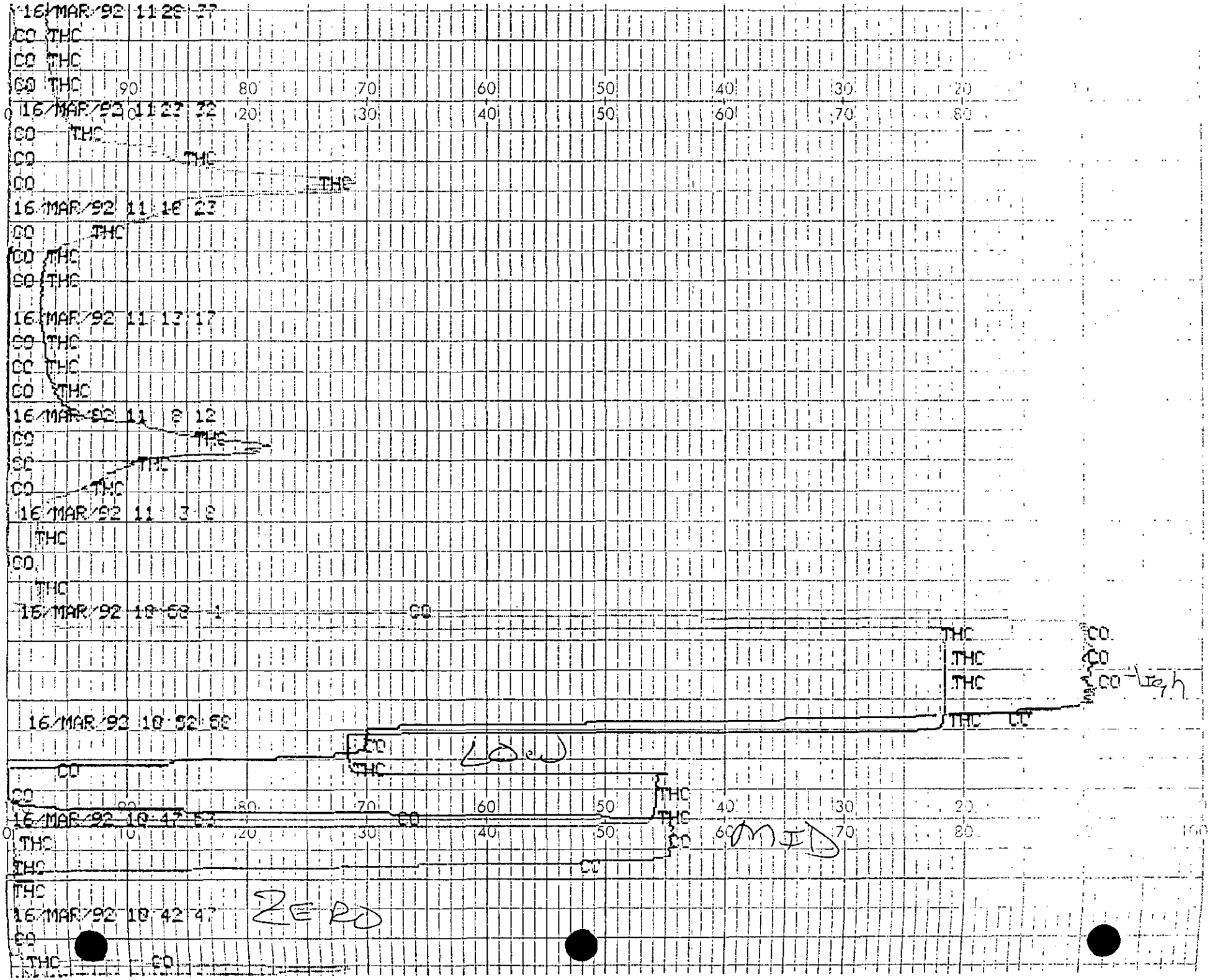

THC
16 MAR/92 9 46 44
CO
THC
CO
16 MAR/92 9 41 46
CO THC
CO THC
CO THC
16 MAR/92 9 36 32
100 THC 90 80 70 60 50 40 30 20
CO 10 20 30 40 50 60 70 80
KUNZ
THC
16 MAR/92 9 31 27
CO
CO THC
CO THC
16 MAR/92 9 26 21
CO THC
CO
THC
16 MAR/92 9 21 17
CO
THC
CO
THC
CO
Low
16 MAR/92 9 16 11
THC
CO
THC
THC
CO
THC
CO
CO
CO
MID CO
16 MAR/92 9 11 6
THC
THC
THC
CO
16 MAR/92 9 6 0
ZERO
CO
THC
CO
THC
16 MAR/92 9 0 55
END RUN

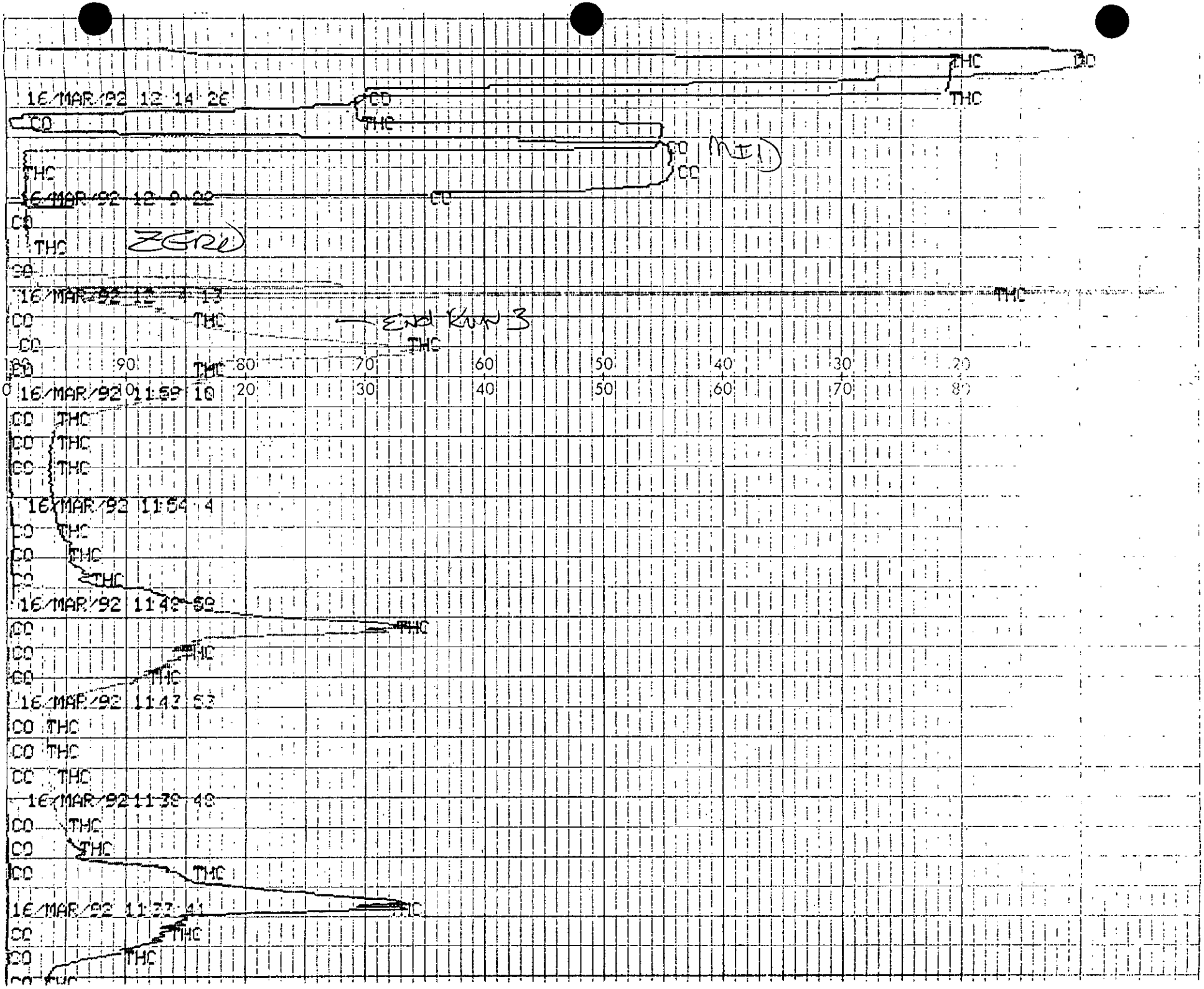
16 MAR 2 10 37 40
THC
CO
CO THC
End Run 2
16 MAR/92 10 32 35
CO THC
CO THC
CO THC
16 MAR/92 10 27 31
CO THC
CO THC
THC
16 MAR/92 10 22 26
CO
CO THC
CO THC
16 MAR/92 10 17 20
CO THC
CO THC
CO THC
16 MAR/92 10 12 11
CO
THC
CO
16 MAR/92 10 7 6
CO THC
CO THC
CO THC
16 MAR/92 10 2 2
THC
CO
THC
16 MAR/92 9 56 57
CO
CO THC
CO THC
16 MAR/92 9 51 51
CO THC

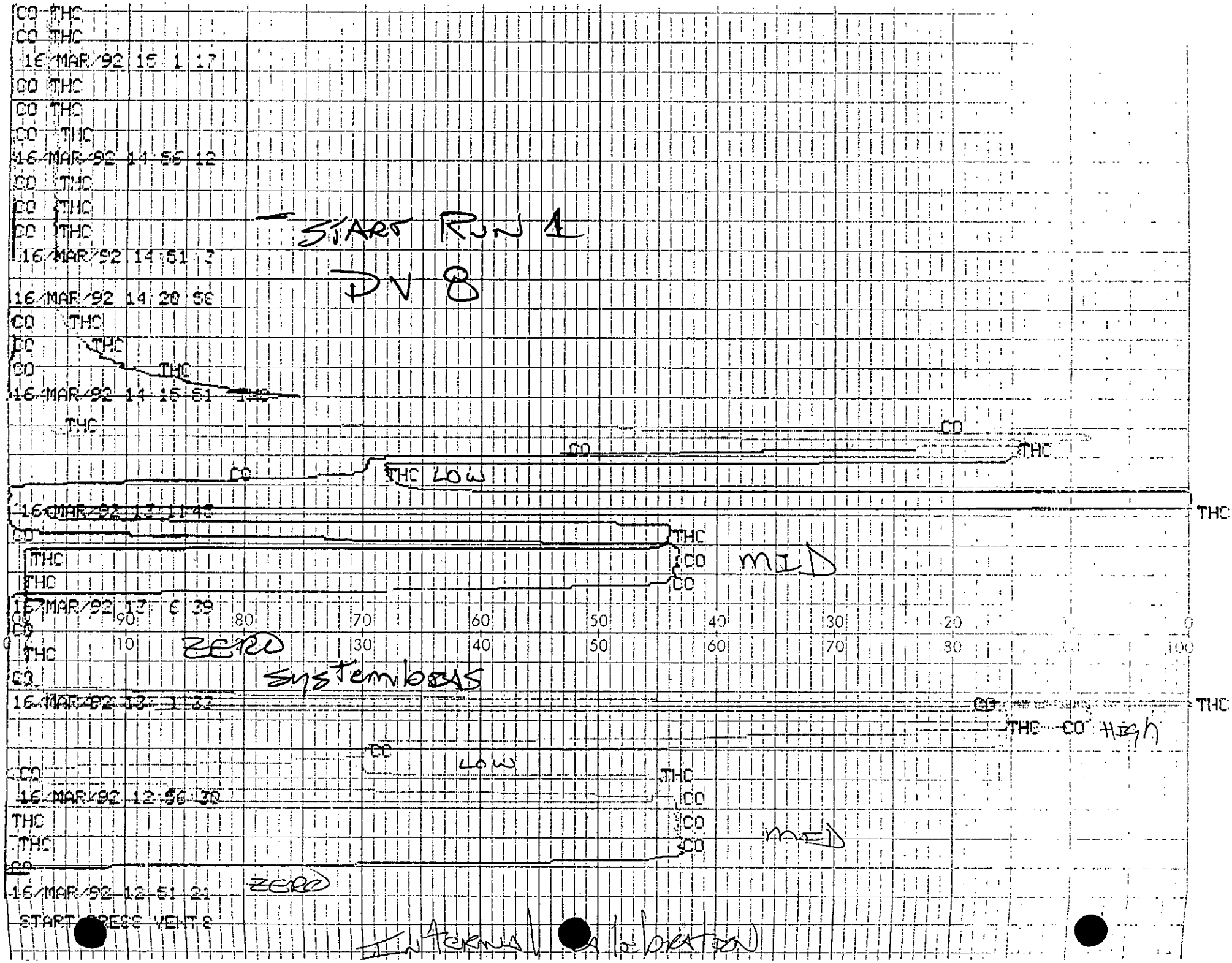
10 20 30 40 50 60 70 80

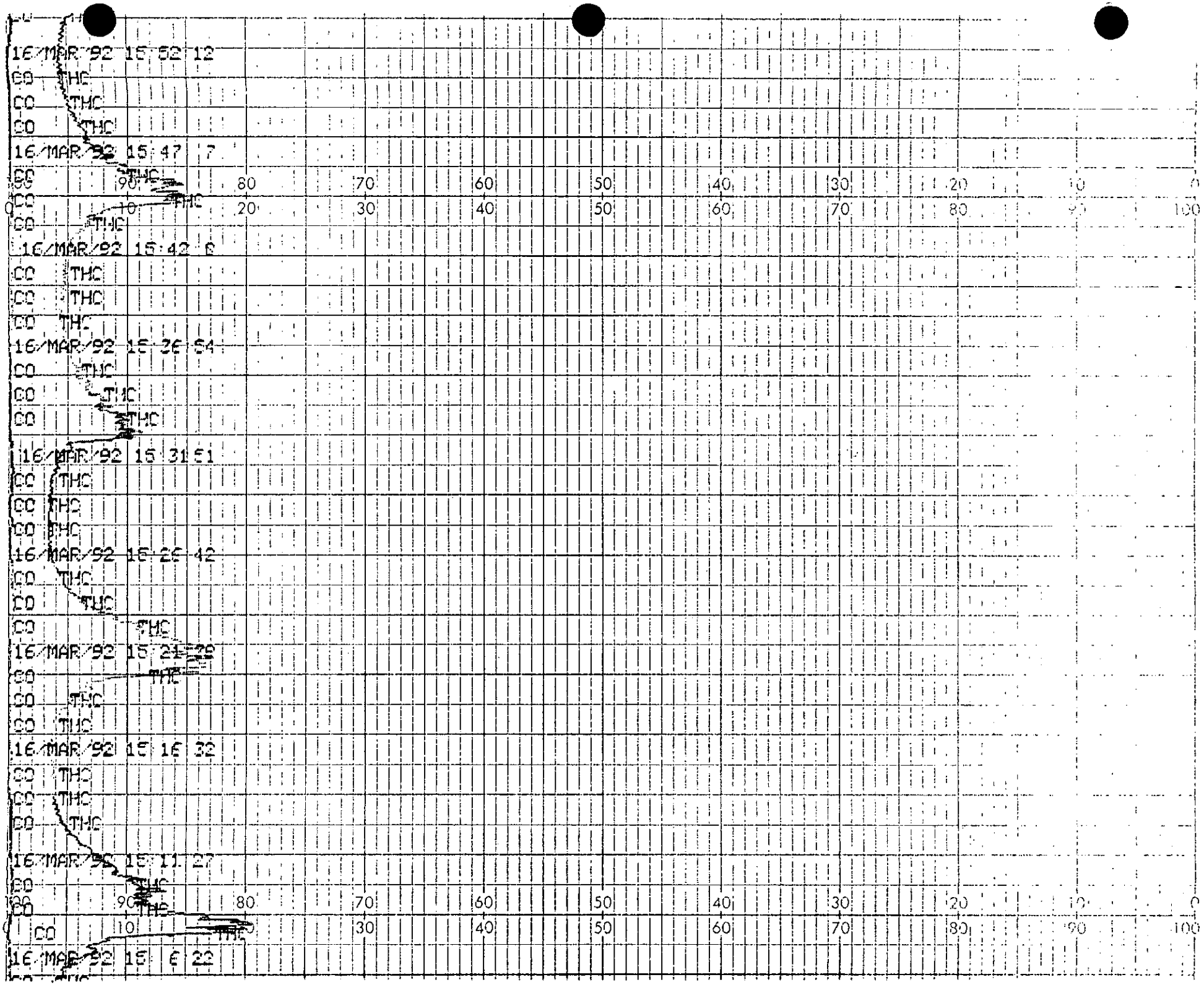
End Run 2

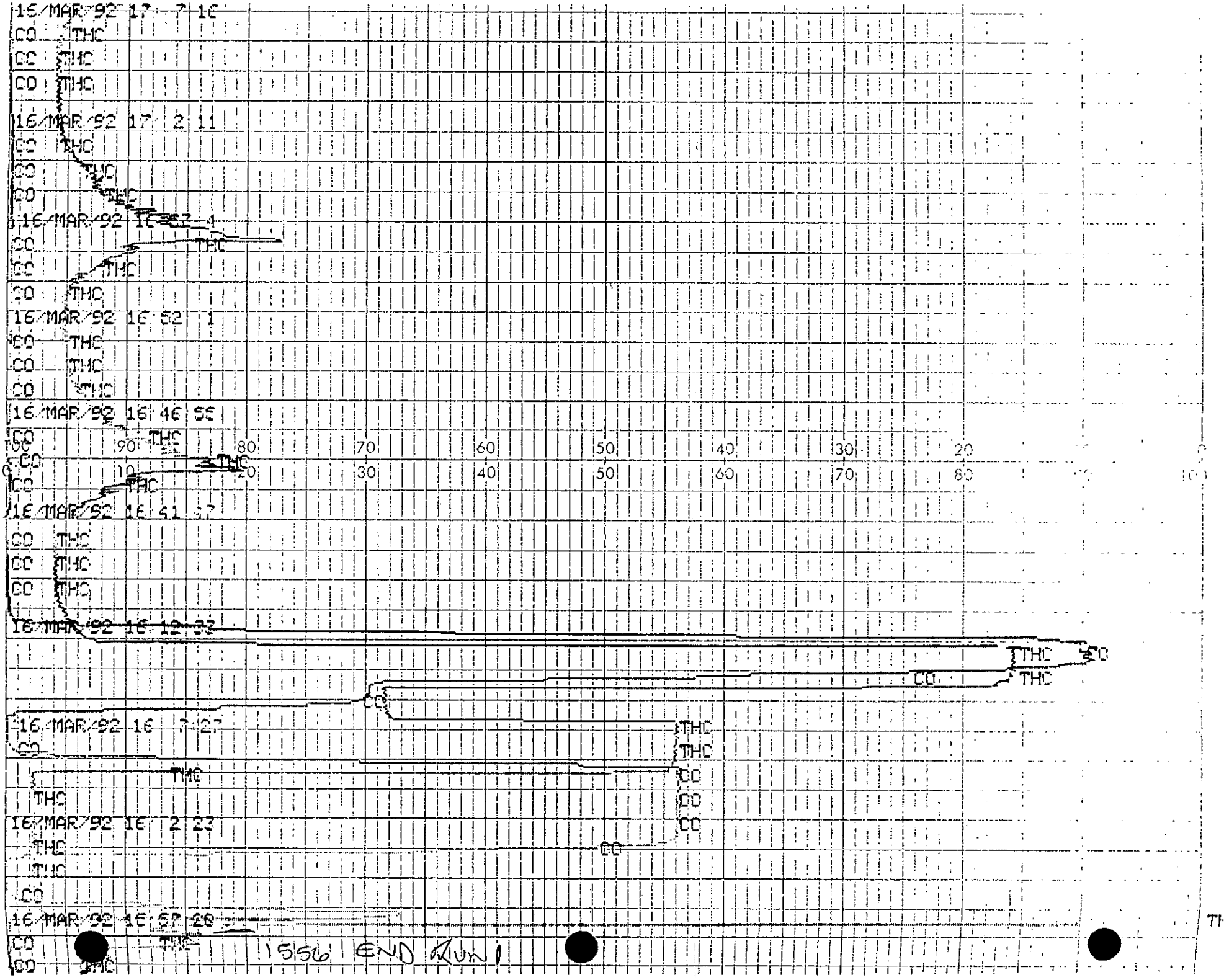
START SYSTEM BIAS

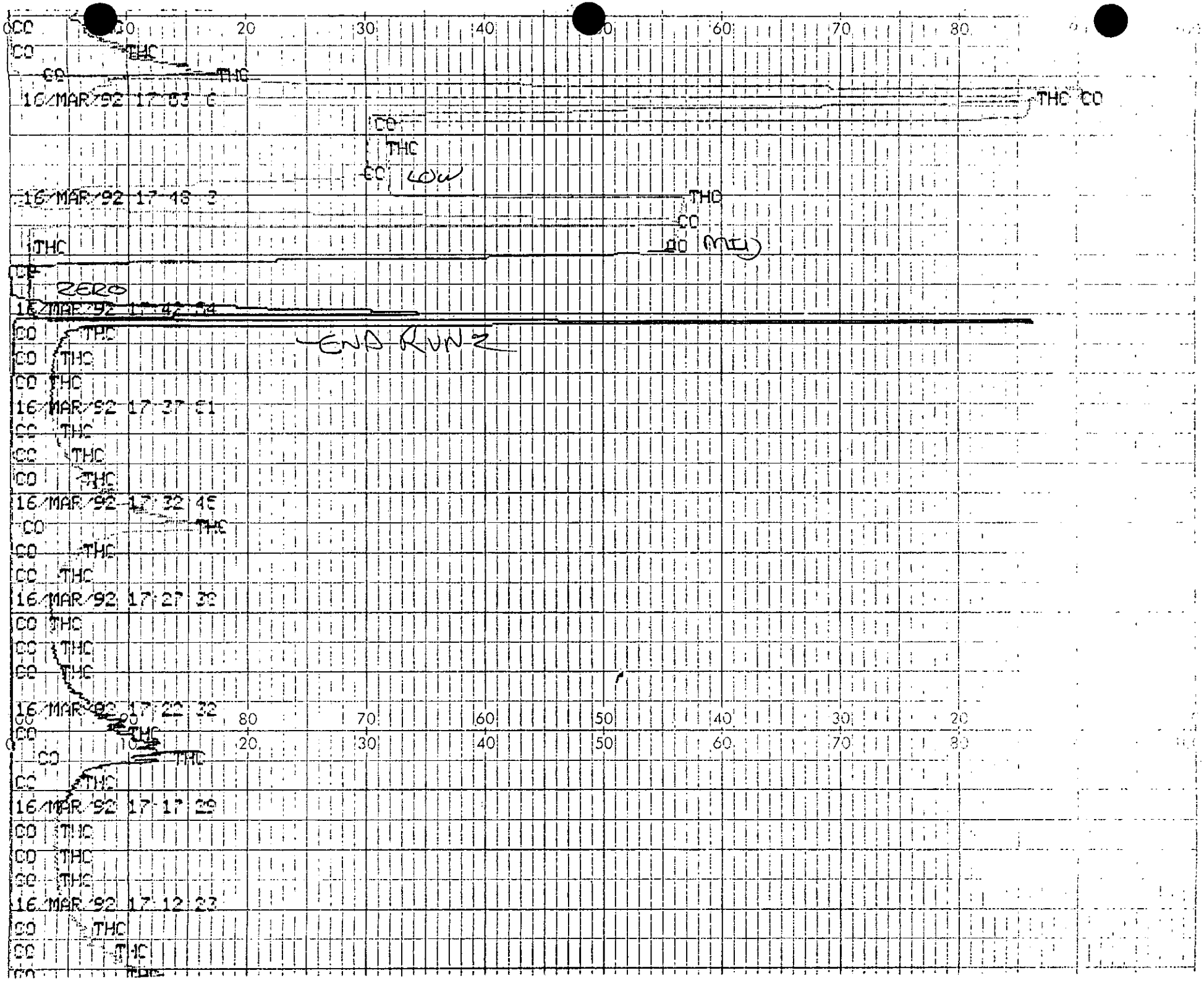

16/MAR/92 11 29 37
CO THC
CO THC
CO THC
90 80 70 60 50 40 30 20
16/MAR/92 11 27 32
0 20 30 40 50 60 70 80
CO THC
CO THC
CO THC
16/MAR/92 11 16 23
CO THC
CO THC
CO THC
16/MAR/92 11 13 17
CO THC
CO THC
CO THC
16/MAR/92 11 9 12
CO THC
CO THC
CO THC
16/MAR/92 11 3 8
THC
CO
THC
16/MAR/92 10 58 1
CO
THC
THC
THC
CO
CO
CO high
16/MAR/92 10 52 58
THC CO
CO
CO
THC
THC
16/MAR/92 10 47 53
CO
THC
THC
CO
THC
CO
THC
16/MAR/92 10 42 47
CO
THC CO
90 80 70 60 50 40 30 20
0 10 20 30 40 50 60 70 80 100
LOW
MID
ZERO


16/MAR/92 12:14:26
CO
THC
16/MAR/92 12:9:22
ZERO
16/MAR/92 12:4:13
END RUN 3
90
80
70
60
50
40
30
20
16/MAR/92 11:59:10
16/MAR/92 11:54:4
16/MAR/92 11:49:59
16/MAR/92 11:43:53
16/MAR/92 11:39:49
16/MAR/92 11:37:41


CO THC
CO THC
16 MAR 92 15 1 17
CO THC
CO THC
CO THC
16 MAR 92 14 56 12
CO THC
CO THC
CO THC
START RUN 1
PV 8
16 MAR 92 14 51 2
16 MAR 92 14 20 56
CO THC
CO THC
CO THC
16 MAR 92 14 15 51
THC
CO
CO
THC
CO
THC LOW
16 MAR 92 13 11 40
THC
CO
THC
THC
CO
MID
CO
16 MAR 92 13 6 39
90 80 70 60 50 40 30 20 0
0 10 30 40 50 60 70 80 100
CO
THC
ZERO
SYSTEM BIAS
16 MAR 92 13 1 32
CO
THC
THC CO HIGH
CO
LOW
CO
16 MAR 92 12 56 30
THC
THC
CO
CO
CO
MID
16 MAR 92 12 51 21
ZERO
START PRESS VENT 2
INTERNAL CALIBRATION


16/MAR/92 15 52 12
CO THC
CO THC
CO THC
16/MAR/92 15 47 7
CO THC
CO THC
CO THC
16/MAR/92 15 42 6
CO THC
CO THC
CO THC
16/MAR/92 15 36 54
CO THC
CO THC
CO THC
16/MAR/92 15 31 51
CO THC
CO THC
CO THC
16/MAR/92 15 26 42
CO THC
CO THC
CO THC
16/MAR/92 15 21 39
CO THC
CO THC
CO THC
16/MAR/92 15 16 32
CO THC
CO THC
CO THC
16/MAR/92 15 11 27
CO THC
CO THC
CO THC
16/MAR/92 15 6 22
90 80 70 60 50 40 30 20 10 0
10 20 30 40 50 60 70 80 90 100


15 MAR 92 17 7 16
CO
THC
16 MAR 92 17 2 11
16 MAR 92 16 52 1
16 MAR 92 16 46 55
16 MAR 92 16 41 37
16 MAR 92 16 12 33
16 MAR 92 16 7 27
16 MAR 92 16 2 23
16 MAR 92 16 57 20
90 80 70 60 50 40 30 20
10 20 30 40 50 60 70 80
1556 END Run!


CO
THC
16/MAR/92 17:03:6
CO
THC
LOW
16/MAR/92 17:18:2
THC
CO
20 MIN
THC
CO
ZERO
16/MAR/92 17:42:34
END RUN 2
CO
THC
16/MAR/92 17:27:51
16/MAR/92 17:32:45
16/MAR/92 17:27:39
16/MAR/92 17:22:32
16/MAR/92 17:17:29
16/MAR/92 17:12:23

CO THC
16/MAR/92 18:37:52
CO THC
CO THC
CO THC
16/MAR/92 18:52:46
CO THC
CO THC
CO THC
16/MAR/92 18:47:40
CO THC
CO THC
CO THC
16/MAR/92 18:42:34
CO THC
CO THC
CO THC
16/MAR/92 18:37:31
CO THC
CO THC
CO THC
16/MAR/92 18:32:26
CO THC
CO THC
CO THC
16/MAR/92 18:27:18
CO THC
CO THC
CO THC
16/MAR/92 18:22:13
CO THC
CO THC
CO THC
16/MAR/92 18:17:[illegible]
CO THC
CO THC
CO THC
16/MA[illegible]2 18:12:0

100 90 80 70 60 50 40 30 20
0 10 20 30 40 50 60 70 80

RUN 13

THC
CO ZERO

System BIAS

THC CO

17 MAR 92 7 31 52

THC CO HIGH
THC CO
THC

CO
CO LOW

17 MAR 92 7 26 48

MID
CO
THC CO MID
CO

17 MAR 92 7 21 41 ZERO

START INTERNAL CALIBRATION
START PRESS VENT 9
COMPLETED PRESS VENT 9

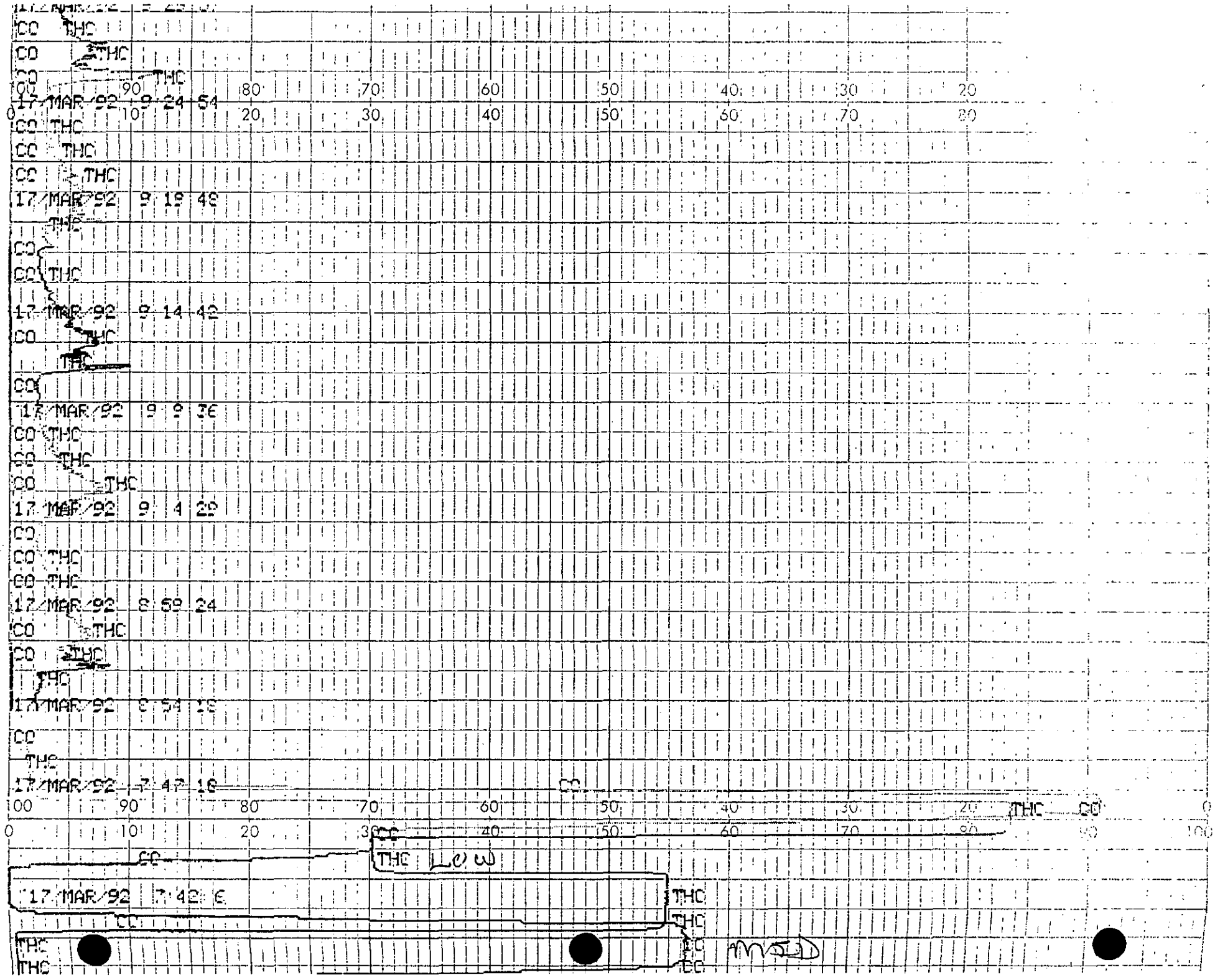
THC

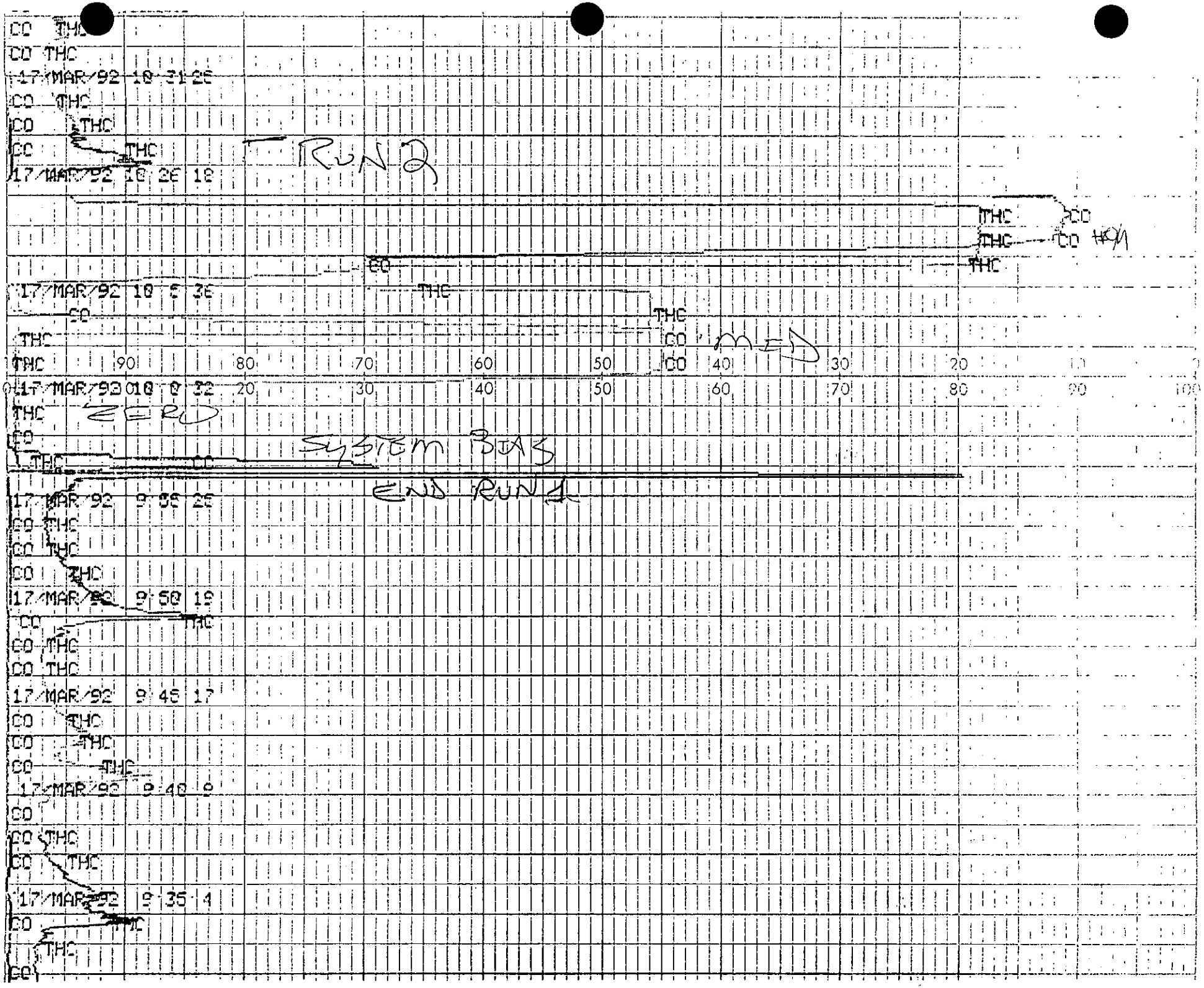
16 MAR 92 19 23 19 80 70 CO 60 50 40 30 20
0 CO 10 20 30 THC 40 50 60 70 80
CO
THC
THC
CO MID

16 MAR 92 19 18 13
CO
THC ZERO
CO

System BIAS

16 MAR 92 19 13 11
CO THC END RUN 3
CO THC
CO THC
16 MAR 92 19 8 4
CO THC
CO THC
CO THC
16 MAR 92 19 2 57
CO THC


CO
THC
17 MAR 92 9 24 54
17 MAR 92 9 19 48
17 MAR 92 9 14 42
17 MAR 92 9 9 36
17 MAR 92 9 4 29
17 MAR 92 8 59 24
17 MAR 92 8 54 18
17 MAR 92 7 42 6
90 80 70 60 50 40 30 20
0 10 20 30 40 50 60 70 80
100 90 80 70 60 50 40 30 20 0
0 10 20 30 40 50 60 70 80 90 100


CO THC
CO THC
17/MAR/92 10 31 26
CO THC
CO THC
CO THC
17/MAR/92 10 26 18
RUN 2
THC
CO
THC
CO HCN
THC
CO
17/MAR/92 10 8 36
THC
CO
THC
THC
CO
MED
THC
90
80
70
60
50
CO
40
30
20
10
0
17/MAR/92 10 0 32
20
30
40
50
60
70
80
90
100
THC
ZERO
CO
SYSTEM BIAS
THC
CO
END RUN 1
17/MAR/92 9 55 26
CO THC
CO THC
CO THC
17/MAR/92 9 50 19
CO
THC
CO THC
CO THC
17/MAR/92 9 45 17
CO THC
CO THC
CO THC
17/MAR/92 9 40 9
CO
CO THC
CO THC
17/MAR/92 9 35 4
CO
THC
THC
CO

CO THC

17/MAR/92 11 22 23

CO THC

CO THC

CO THC

17/MAR/92 11 17 17

CO THC

CO THC

CO THC

17/MAR/92 11 12 10

CO THC

CO THC

CO THC

17/MAR/92 11 7 2

CO THC

CO THC

CO THC

17/MAR/92 11 1 57

CO THC

CO THC

CO THC

17/MAR/92 10 56 53

CO THC

CO THC

CO THC

90 80 70 60 50 40 30 20

17/MAR/92 10 51 48

20 30 40 50 60 70 80 100

CO THC

CO THC

CO THC

17/MAR/92 10 46 41

CO THC

CO THC

CO THC

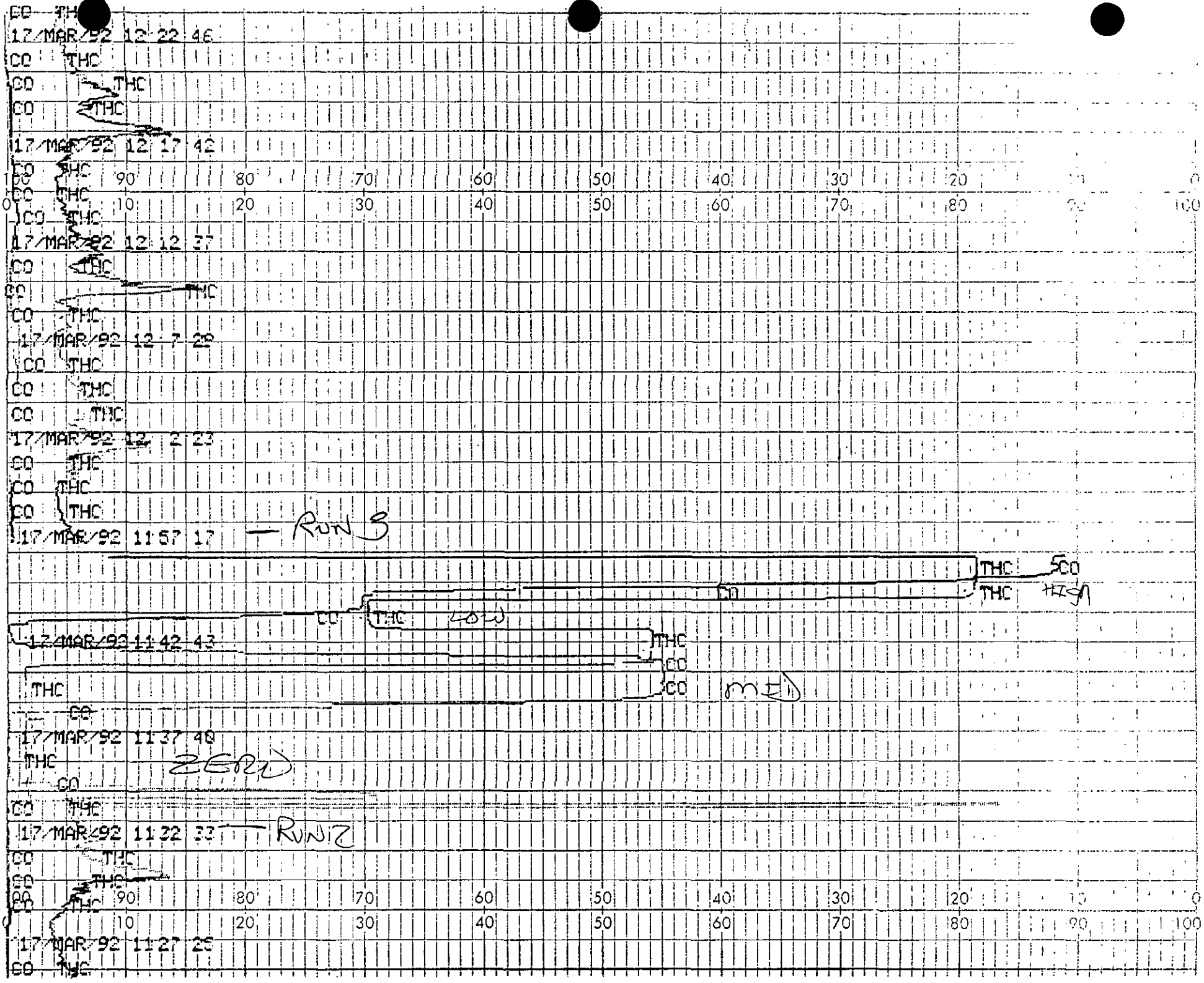
17/MAR/92 10 41 38

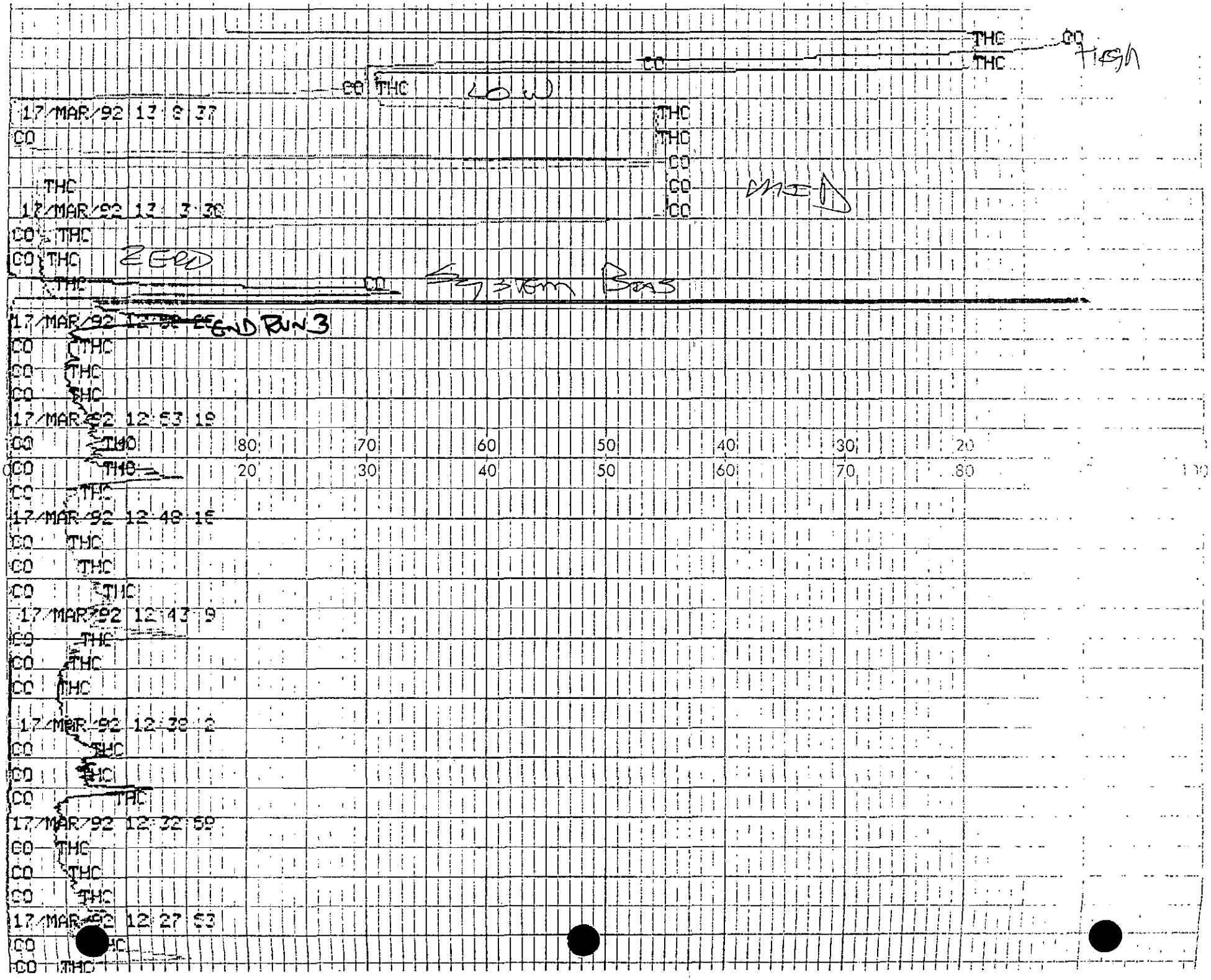
CO THC

CO THC

CO THC

17/MAR/92 10 36 32


CO THC
17/MAR/92 12 22 46
CO THC
CO THC
CO THC
17/MAR/92 12 17 42
CO THC
CO THC
CO THC
90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
17/MAR/92 12 12 37
CO THC
CO THC
CO THC
17/MAR/92 12 7 29
CO THC
CO THC
CO THC
17/MAR/92 12 2 23
CO THC
CO THC
CO THC
17/MAR/92 11 57 17
RUN 9
THC
CO
CO
THC
HIGH
CO
THC
LOW
17/MAR/92 11 42 43
THC
CO
CO
MID
THC
CO
17/MAR/92 11 37 40
THC
ZERO
CO
CO THC
17/MAR/92 11 32 33
RUN 12
CO THC
CO THC
CO THC
90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
17/MAR/92 11 27 26
CO THC


THC
CO
HIGH
CO
THC
LOW
17/MAR/92 12:8:37
CO
THC
THC
CO
CO
CO
CO
THC
17/MAR/92 12:3:30
CO THC
CO THC
ZERO
THC
CO
SYSTEM BIAS
17/MAR/92 12:38:55 END RUN 3
CO THC
CO THC
CO THC
17/MAR/92 12:53:19
CO THC
CO THC
CO THC
17/MAR/92 12:48:15
CO THC
CO THC
CO THC
17/MAR/92 12:43:9
CO THC
CO THC
CO THC
17/MAR/92 12:38:2
CO THC
CO THC
CO THC
17/MAR/92 12:32:59
CO THC
CO THC
CO THC
17/MAR/92 12:27:53
CO THC
CO THC
80 70 60 50 40 30 20
20 30 40 50 60 70 80 100

17/MAR/92 16 8 44

CO THC

CO THC

CO THC

17/MAR/92 16 3 38

CO THC

CO THC

CO THC

17/MAR/92 15 58 33

CO THC

CO THC

CO THC

17/MAR/92 15 53 27

CO THC

CO THC

CO THC

17/MAR/92 15 48 18

CO THC

CO THC

CO THC

17/MAR/92 15 43 16

CO THC

CO THC

CO THC

17/MAR/92 15 38 7

CO THC

CO THC

CO THC

17/MAR/92 15 33 1

CO THC

CO THC

CO THC

17/MAR/92 15 27 56

CO THC

CO THC

CO THC

17/MAR/92 15 22 50

START PRESS VENT 10

PRESS VENT 9 COMPLETE

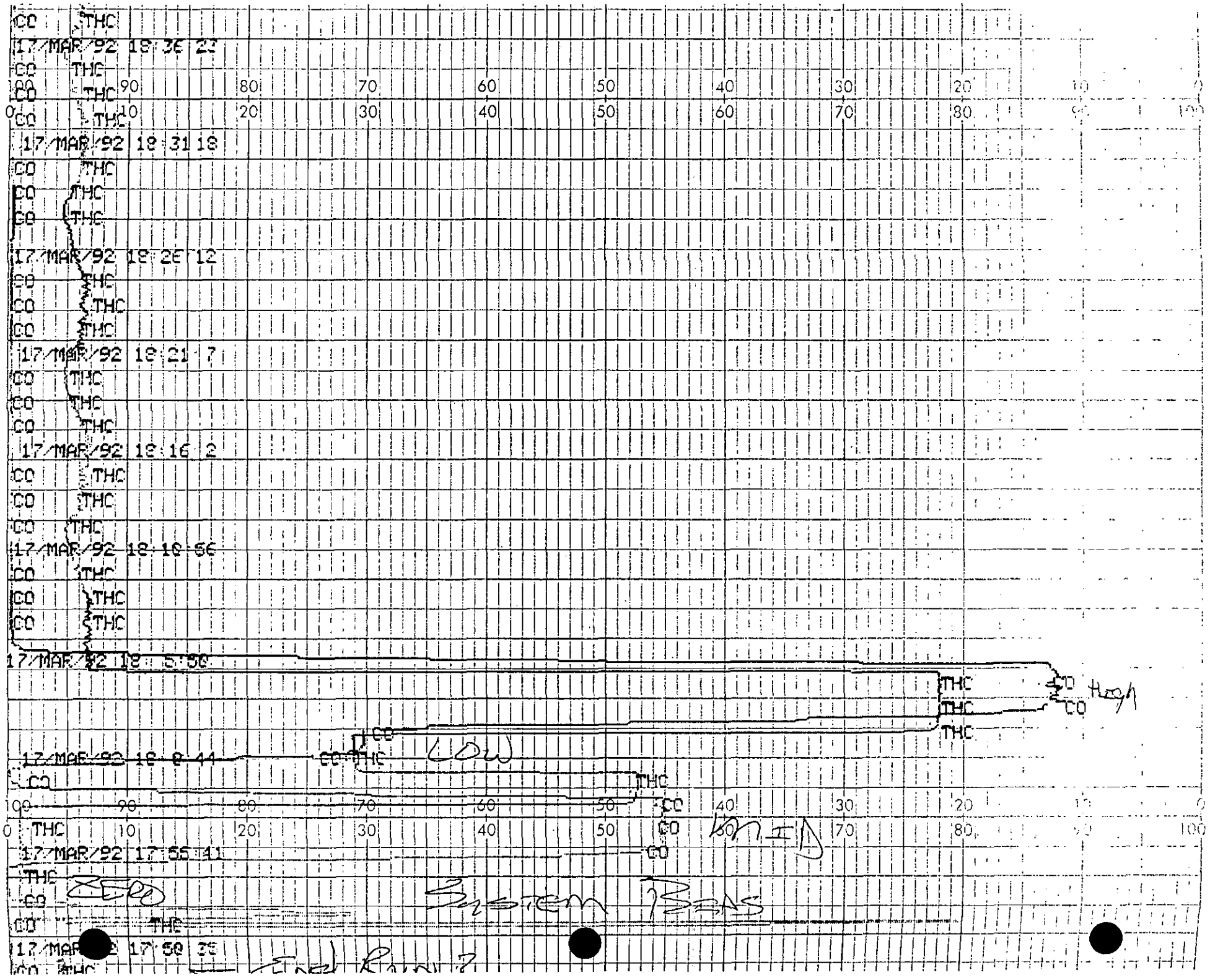
CO THC
CO THC
CO THC
17/MAR/92 16:54:24
CO THC
CO THC
CO THC
17/MAR/92 16:49:30 — Run 2
CO THC
THC

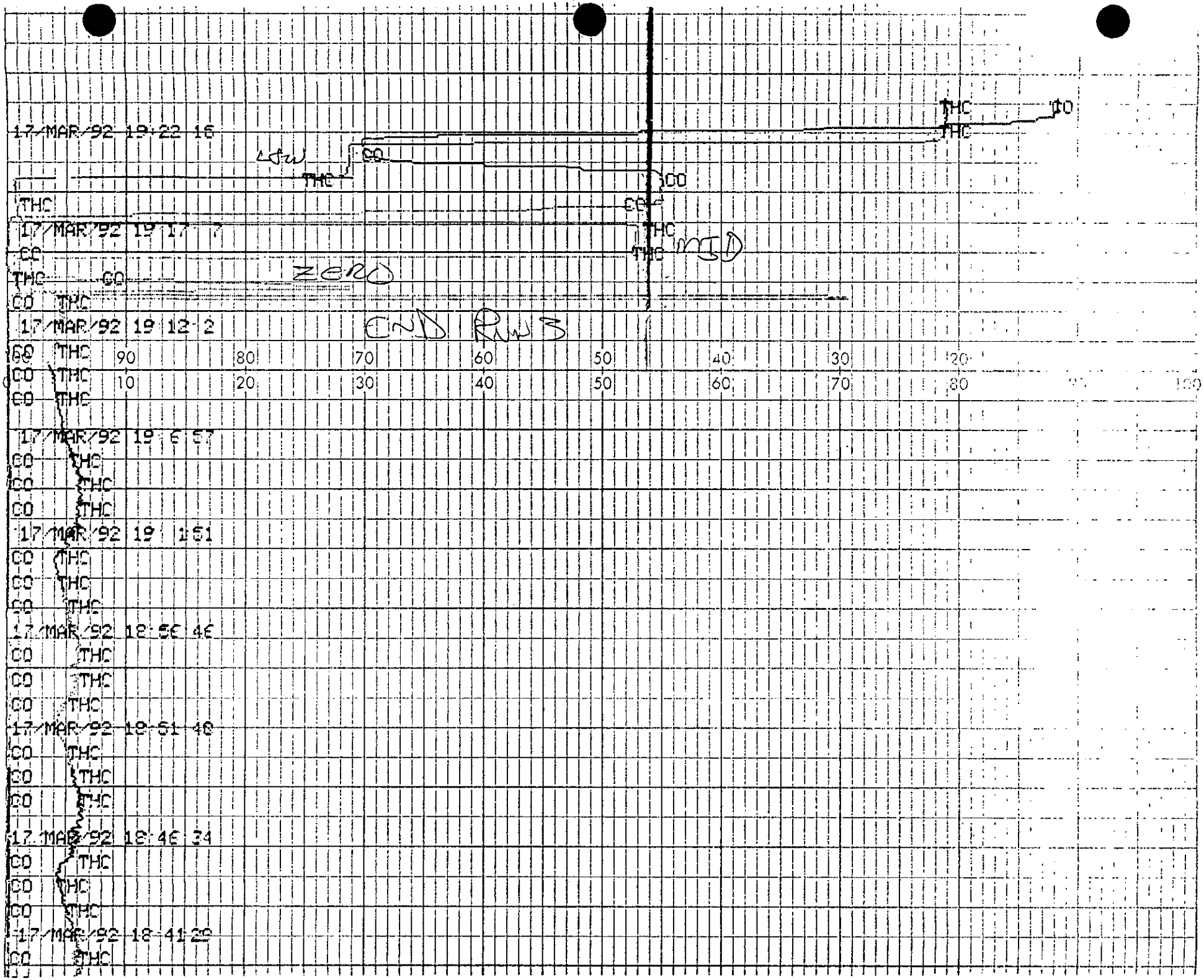
100 90 80 70 60 50 40 30 0
0 10 20 30 40 50 60 70 80 90 100

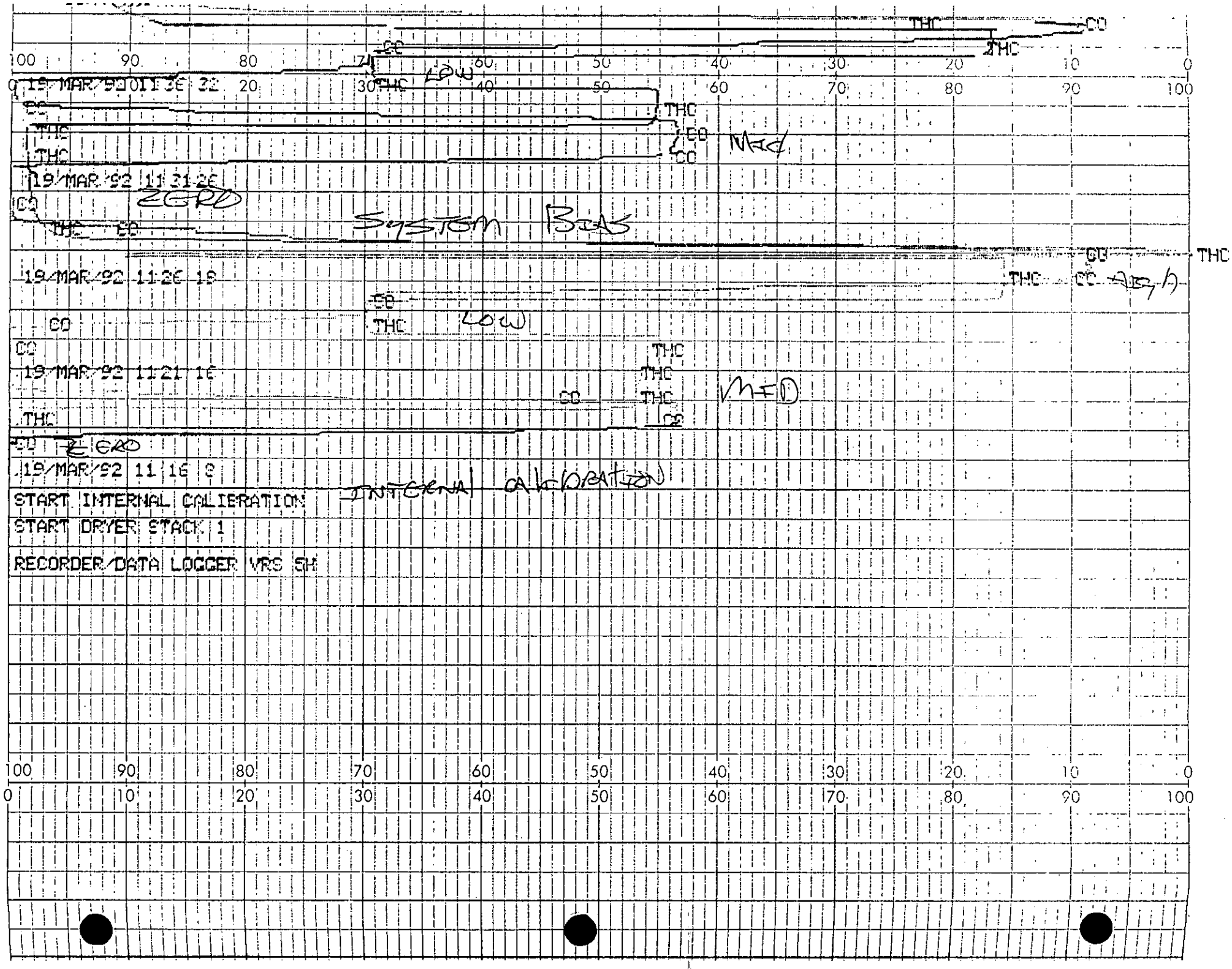
THC CO
17/MAR/92 16:44:22
CO 18W
CO THC
CO
CO
CO
THC
17/MAR/92 16:39:16 MOD
THC CO
THC
CO ZERO
17/MAR/92 16:34:10
CO THC
CO THC — System Bias
CO THC
17/MAR/92 16:29:6
CO THC
CO THC
CO THC
17/MAR/92 16:24:0 — Stop Run 1
CO THC
CO THC
CO THC
17/MAR/92 16:18:56
CO THC
CO THC
CO THC
17/MAR/92 16:13:49
CO THC
CO
CO THC

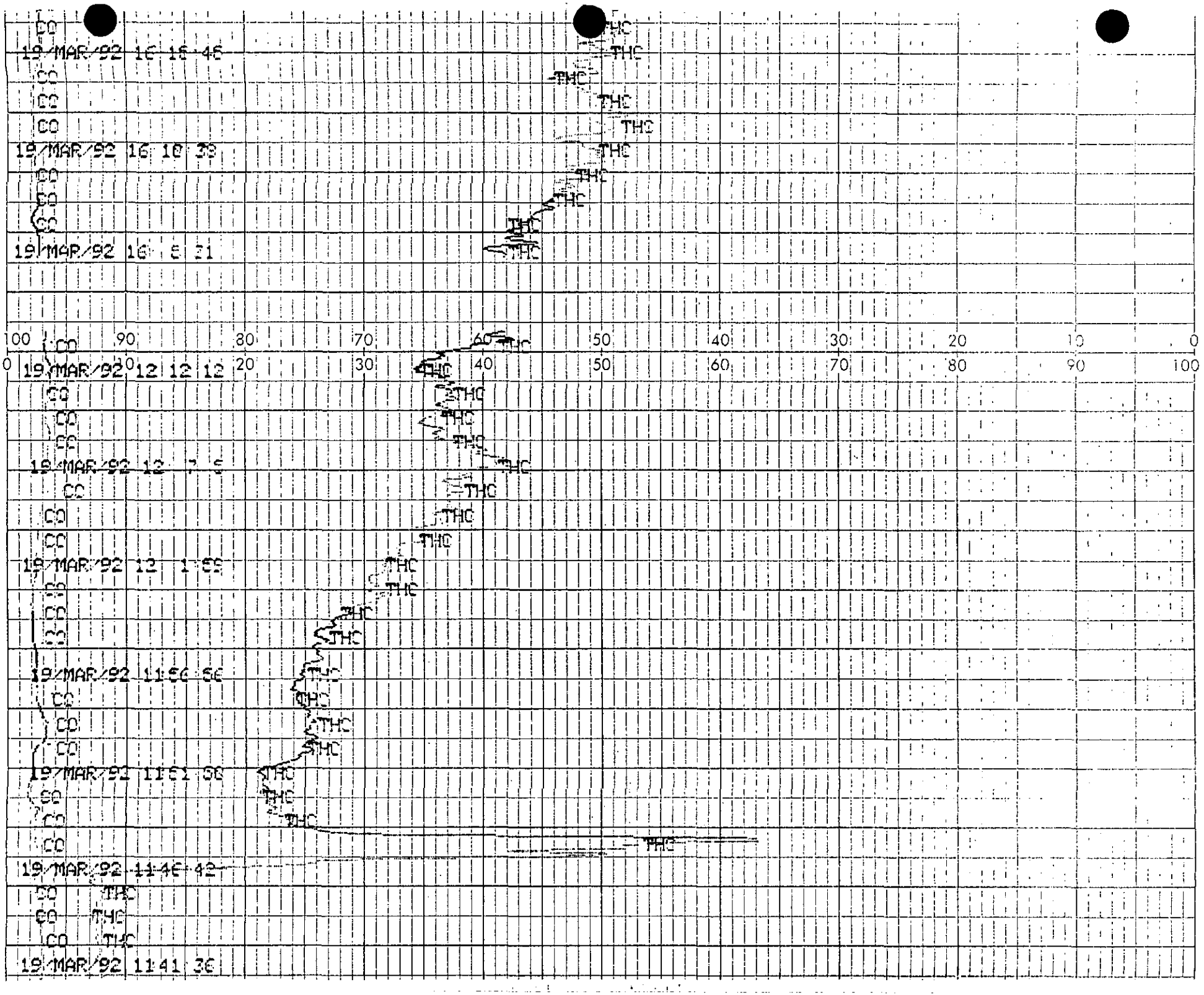
CO THC
CO THC
17/MAR/92 17 45 29
CO THC
CO THC
CO THC
17/MAR/92 17 40 23
CO THC
CO THC
CO THC
17/MAR/92 17 35 18
CO THC
CO THC
CO THC
17/MAR/92 17 30 12
CO THC
CO THC
CO THC
17/MAR/92 17 25 6
CO THC
CO THC
CO THC
17/MAR/92 17 20 1
CO THC
CO THC
CO THC
17/MAR/92 17 14 55
CO THC
CO THC
CO THC
17/MAR/92 17 9 50
CO THC
CO THC
CO THC
17/MAR/92 17 4 45
CO THC
CO THC
CO THC

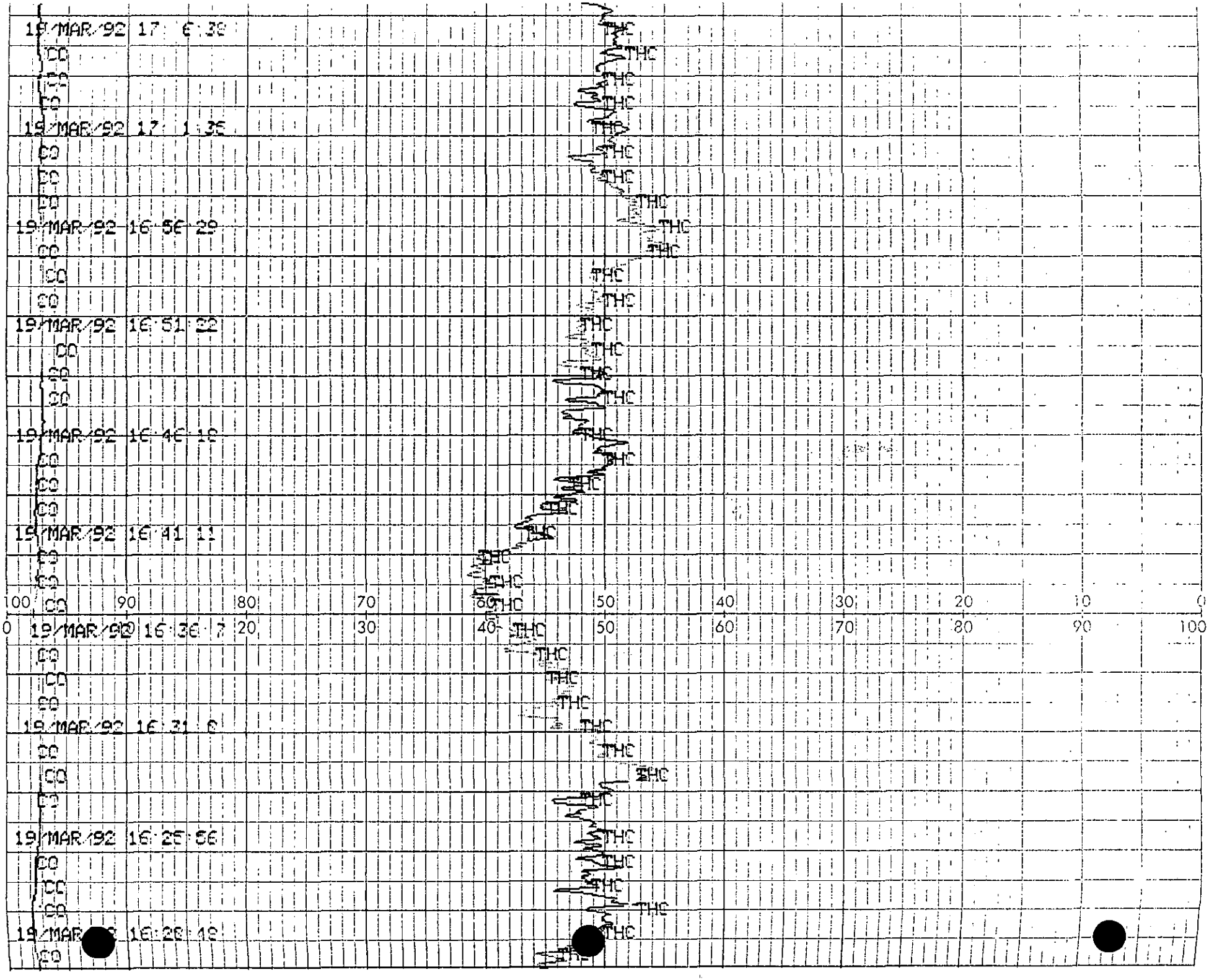
90 80 70 60 50 40 30 20 10 0
10 20 30 40 50 60 70 80 90 100

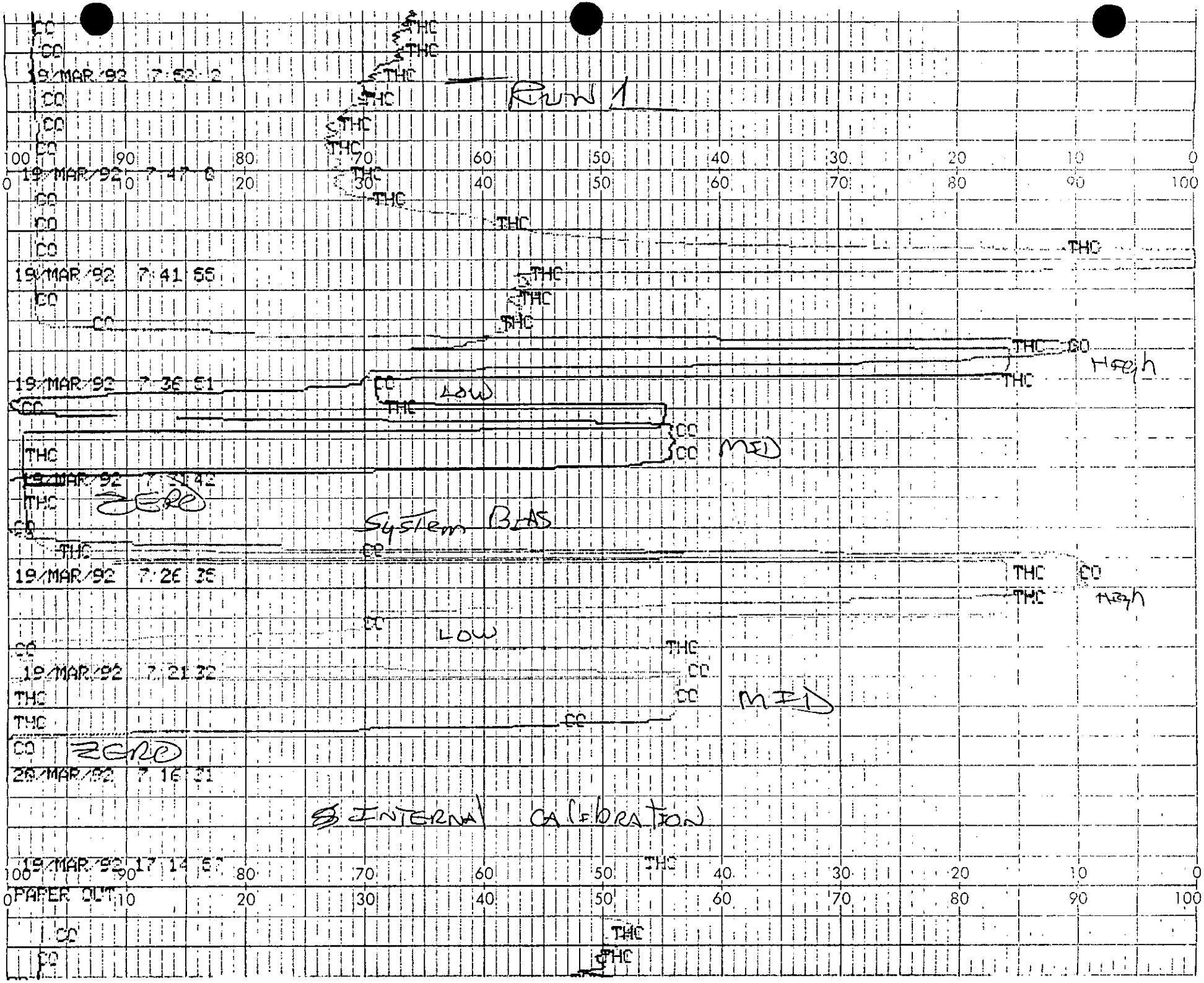

CO THC
17/MAR/92 18 36 22
CO THC
CO THC
CO THC
17/MAR/92 18 31 18
CO THC
CO THC
CO THC
17/MAR/92 18 26 12
CO THC
CO THC
CO THC
17/MAR/92 18 21 7
CO THC
CO THC
CO THC
17/MAR/92 18 16 2
CO THC
CO THC
CO THC
17/MAR/92 18 10 56
CO THC
CO THC
CO THC
17/MAR/92 18 5 50
THC
THC
THC
CO
CO
High
CO
17/MAR/92 18 0 44
CO THC
Low
CO
THC
CO
THC
CO
CO
Ran I D
17/MAR/92 17 55 41
CO
THC
CO
Zero
System Bias
CO THC
17/MAR/92 17 50 35
CO THC
Zero Point

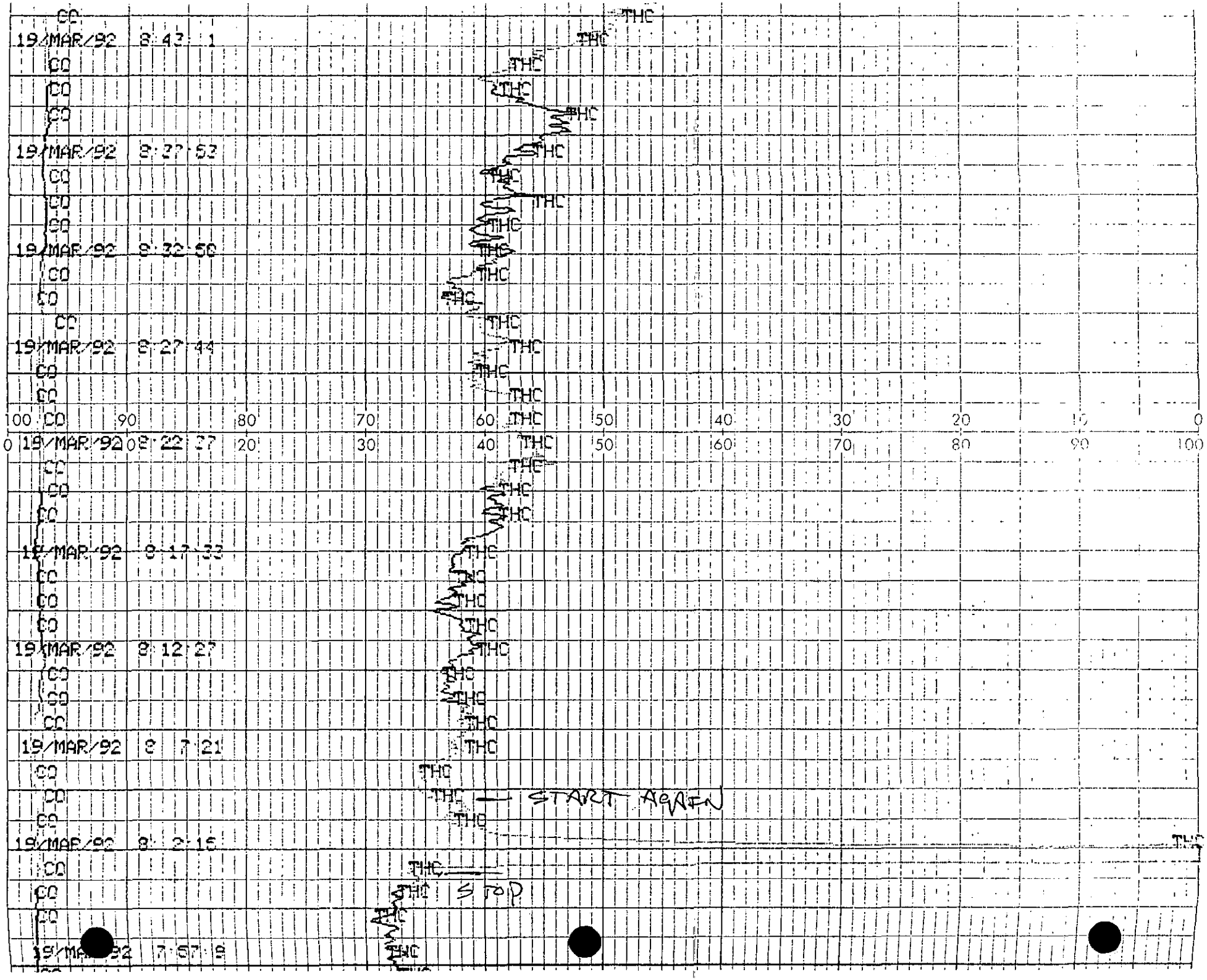

17/MAR/92 19:22:16
LOW
THC
CO
THC
CO
THC
CO
THC
17/MAR/92 19:17:
CO
THC
CO
THC
MID
ZERO
CO THC
17/MAR/92 19:12:2
2ND RUN
CO THC
CO THC
CO THC
90 80 70 60 50 40 30 20
10 20 30 40 50 60 70 80 90
17/MAR/92 19:6:57
CO THC
CO THC
CO THC
17/MAR/92 19:1:51
CO THC
CO THC
CO THC
17/MAR/92 18:56:46
CO THC
CO THC
CO THC
17/MAR/92 18:51:40
CO THC
CO THC
CO THC
17/MAR/92 18:46:34
CO THC
CO THC
CO THC
17/MAR/92 18:41:29
CO THC

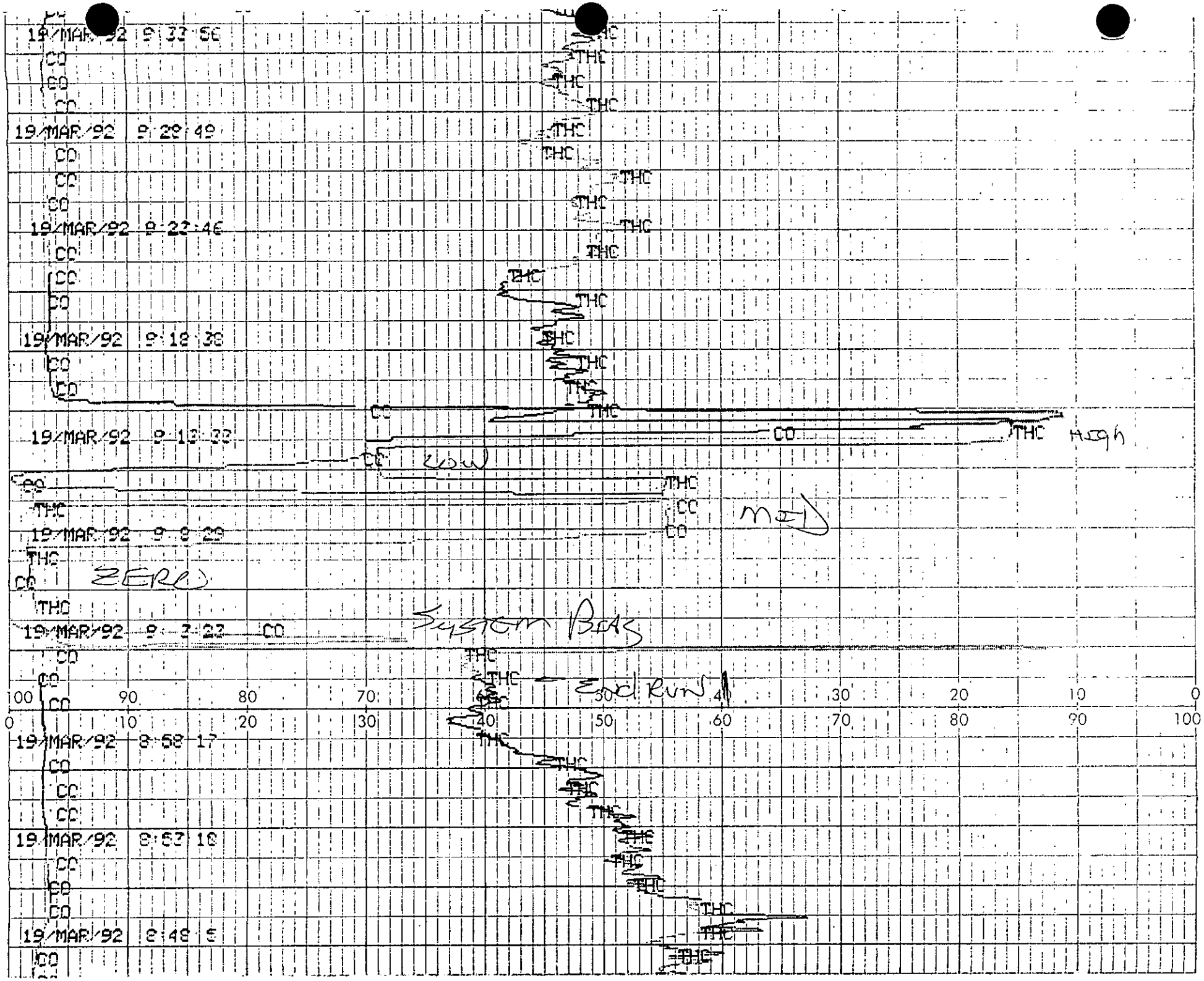

THC
CO
LOW
19/MAR/92 11:31:26
ZERO
SYSTEM BIAS
19/MAR/92 11:26:19
LOW
19/MAR/92 11:21:16
MED
ZERO
19/MAR/92 11:16:8
INTERNAL CALIBRATION
START INTERNAL CALIBRATION
START DRYER STACK 1
RECORDER/DATA LOGGER VRS SH

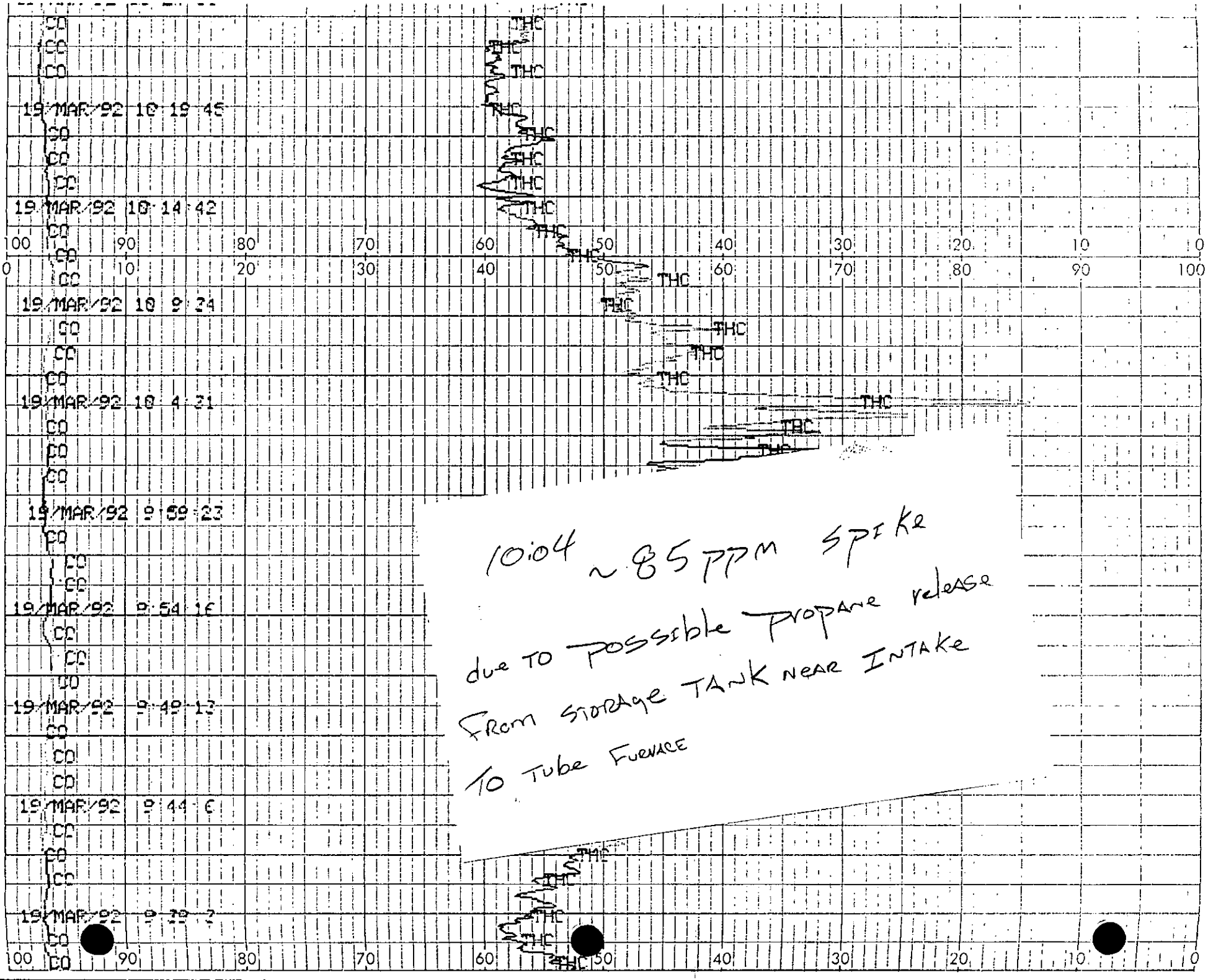

CO
19/MAR/92 16 16 46
CO
CO
CO
19/MAR/92 16 10 39
CO
CO
CO
19/MAR/92 16 5 21
THC
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
19/MAR/92 12 12 12
19/MAR/92 12 7 5
19/MAR/92 12 1 59
19/MAR/92 11 56 56
19/MAR/92 11 51 50
19/MAR/92 11 46 42
19/MAR/92 11 41 36

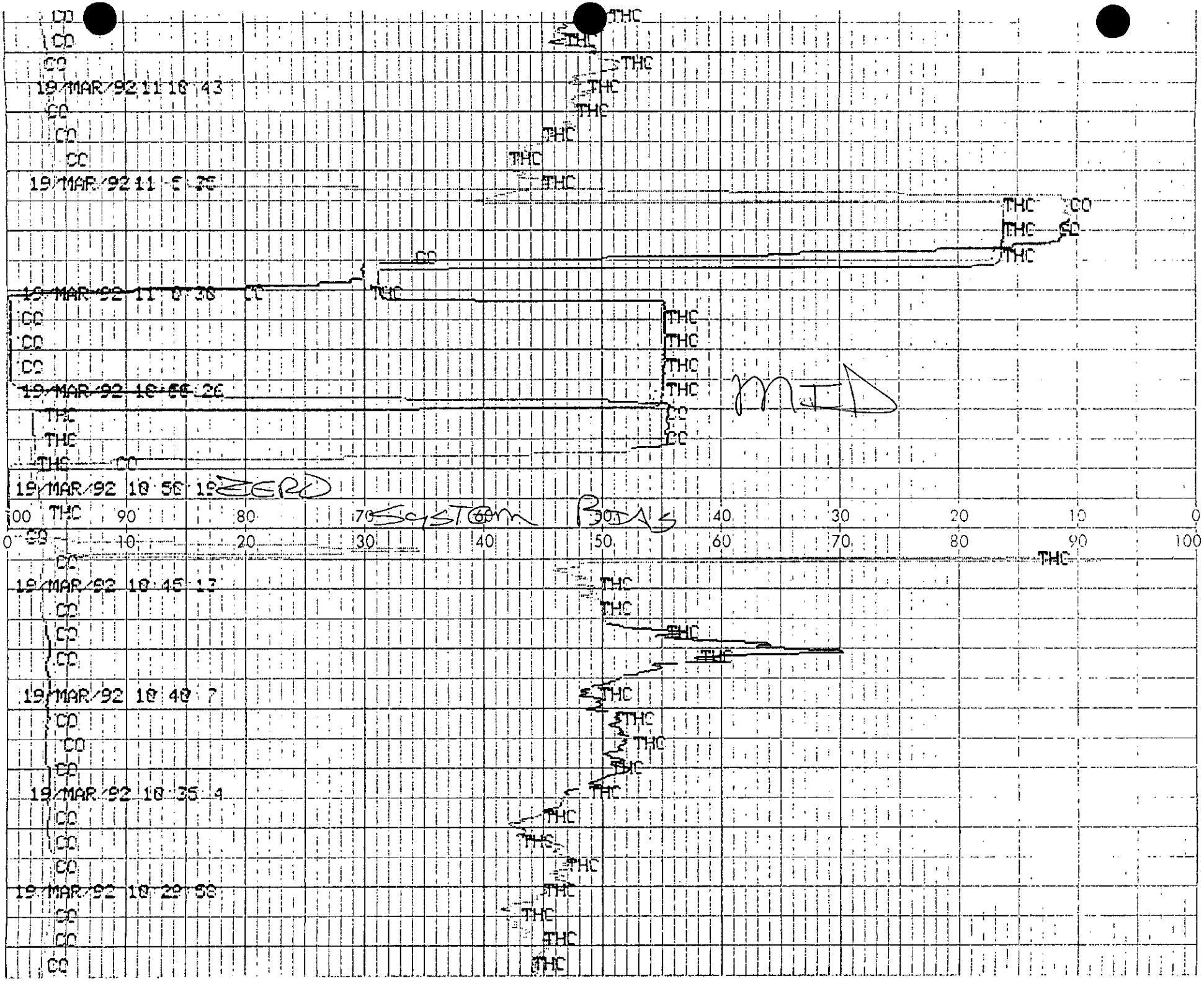

19/MAR/92 17 6 39
19/MAR/92 17 1 35
19/MAR/92 16 56 29
19/MAR/92 16 51 22
19/MAR/92 16 46 18
19/MAR/92 16 41 11
19/MAR/92 16 36 7
19/MAR/92 16 31 0
19/MAR/92 16 25 56
CO
THC
100 90 80 70 60 50 40 30 20 10 0
0 20 30 40 50 60 70 80 90 100

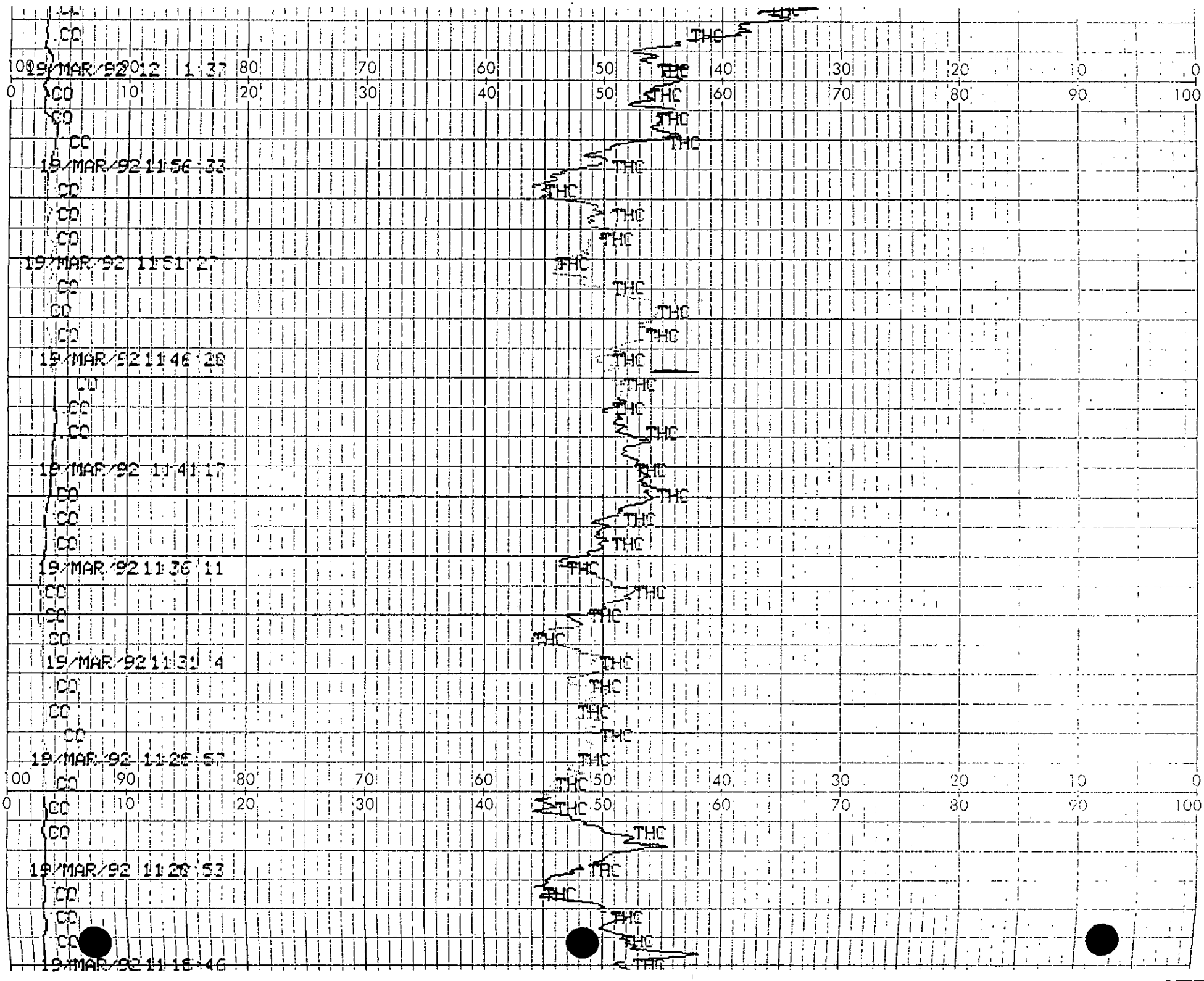

Run 1
19/MAR/92 7:52:12
19/MAR/92 7:47:0
19/MAR/92 7:41:55
19/MAR/92 7:36:51
High
LOW
MID
ZERO
System BIAS
19/MAR/92 7:26:36
High
LOW
19/MAR/92 7:21:32
MID
ZERO
20/MAR/92 7:16:21
INTERNAL CALIBRATION
19/MAR/92 17:14:57
PAPER OUT
THC
CO

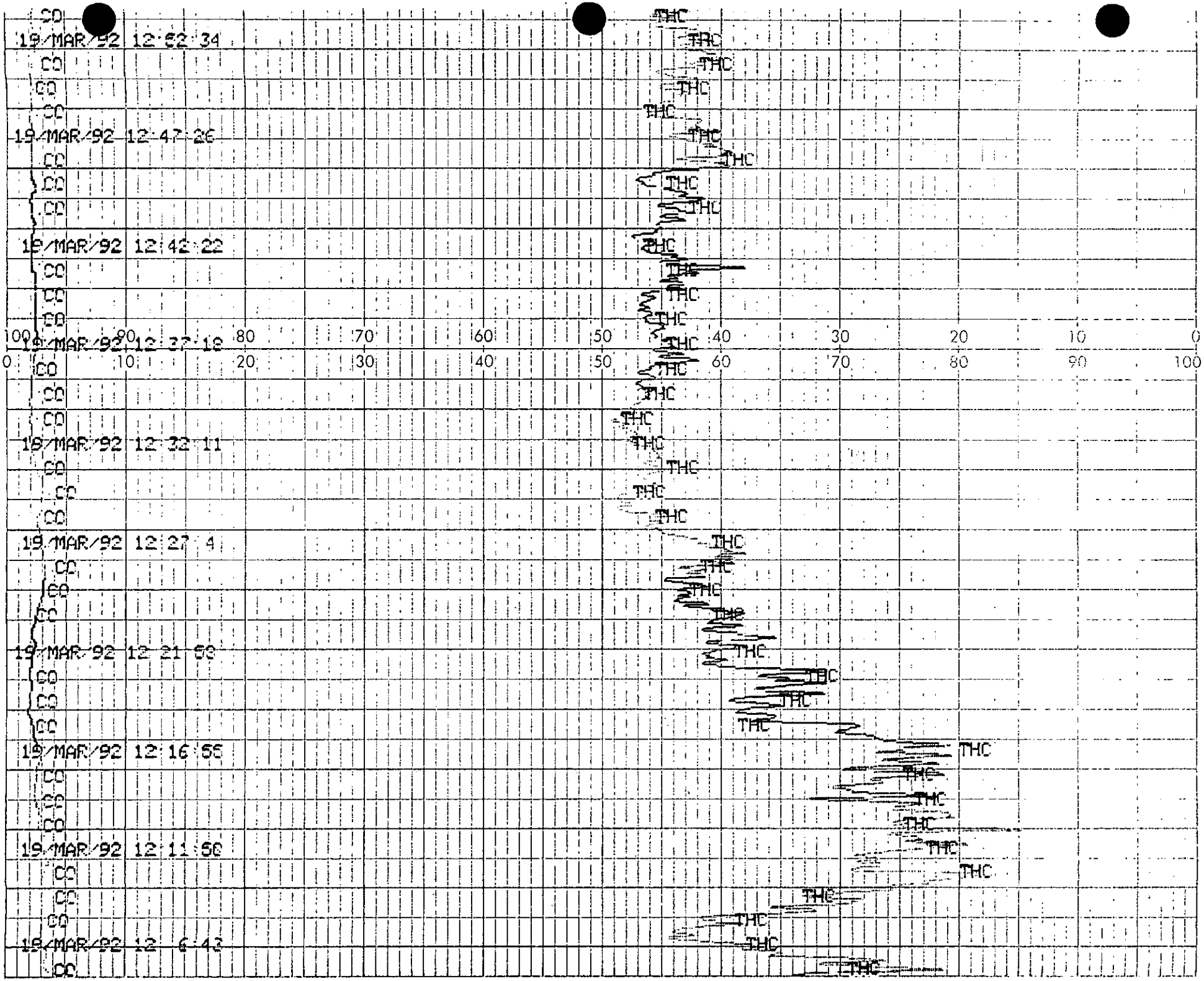

19/MAR/92 8:43: 1
19/MAR/92 8:37:53
19/MAR/92 8:32:50
19/MAR/92 8:27:44
19/MAR/92 8:22:37
19/MAR/92 8:17:33
19/MAR/92 8:12:27
19/MAR/92 8: 7:21
19/MAR/92 8: 2:15
19/MAR/92 7:57: 9
CO
THC
START AGAIN
STOP
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100

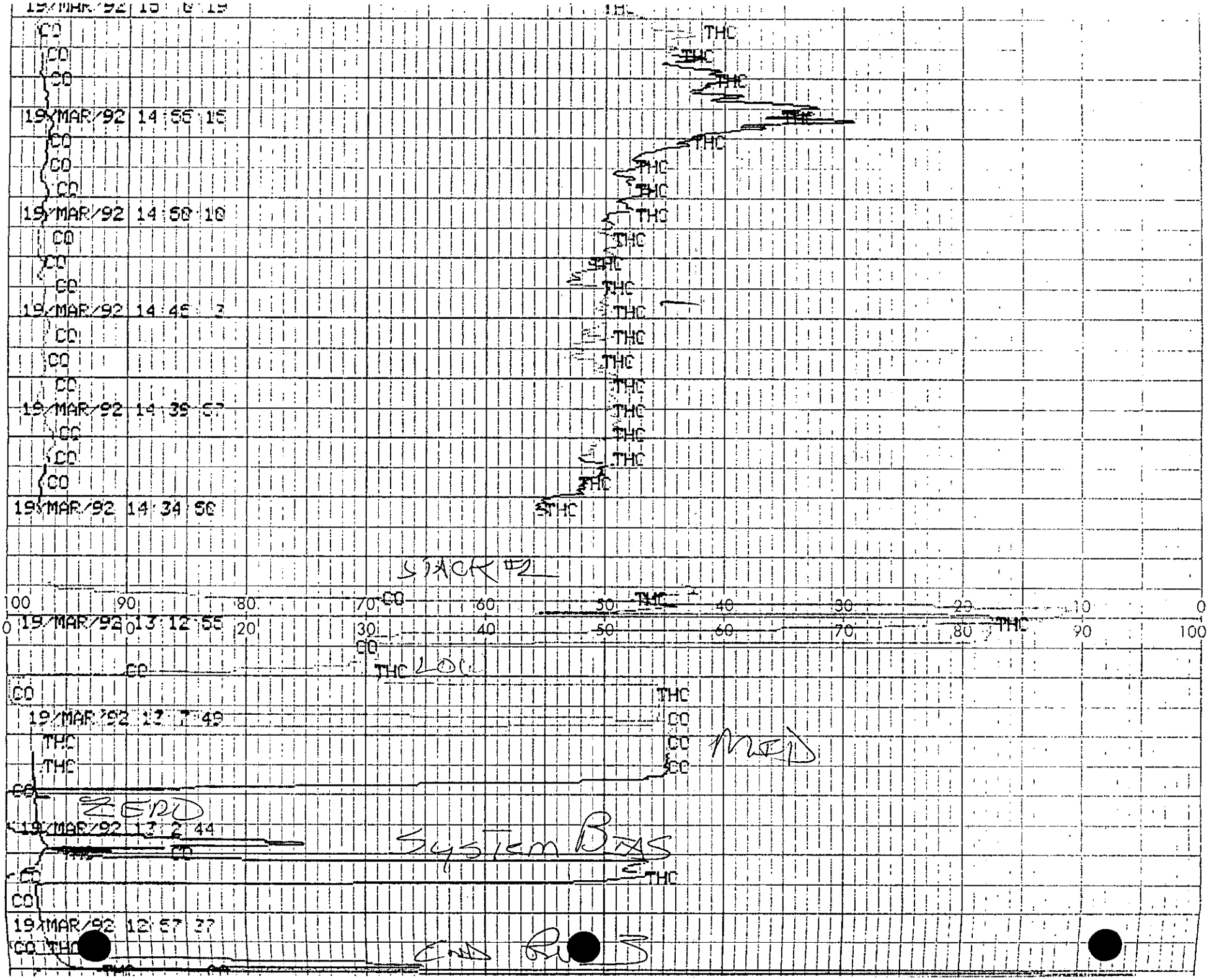

19/MAR/92 9:33:56
19/MAR/92 9:28:49
19/MAR/92 9:23:46
19/MAR/92 9:18:38
19/MAR/92 9:13:22
19/MAR/92 9:8:20
19/MAR/92 9:3:22
19/MAR/92 8:58:17
19/MAR/92 8:53:10
19/MAR/92 8:48:5
CO
THC
High
Low
Med
ZERO
System Bias
End Run
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100

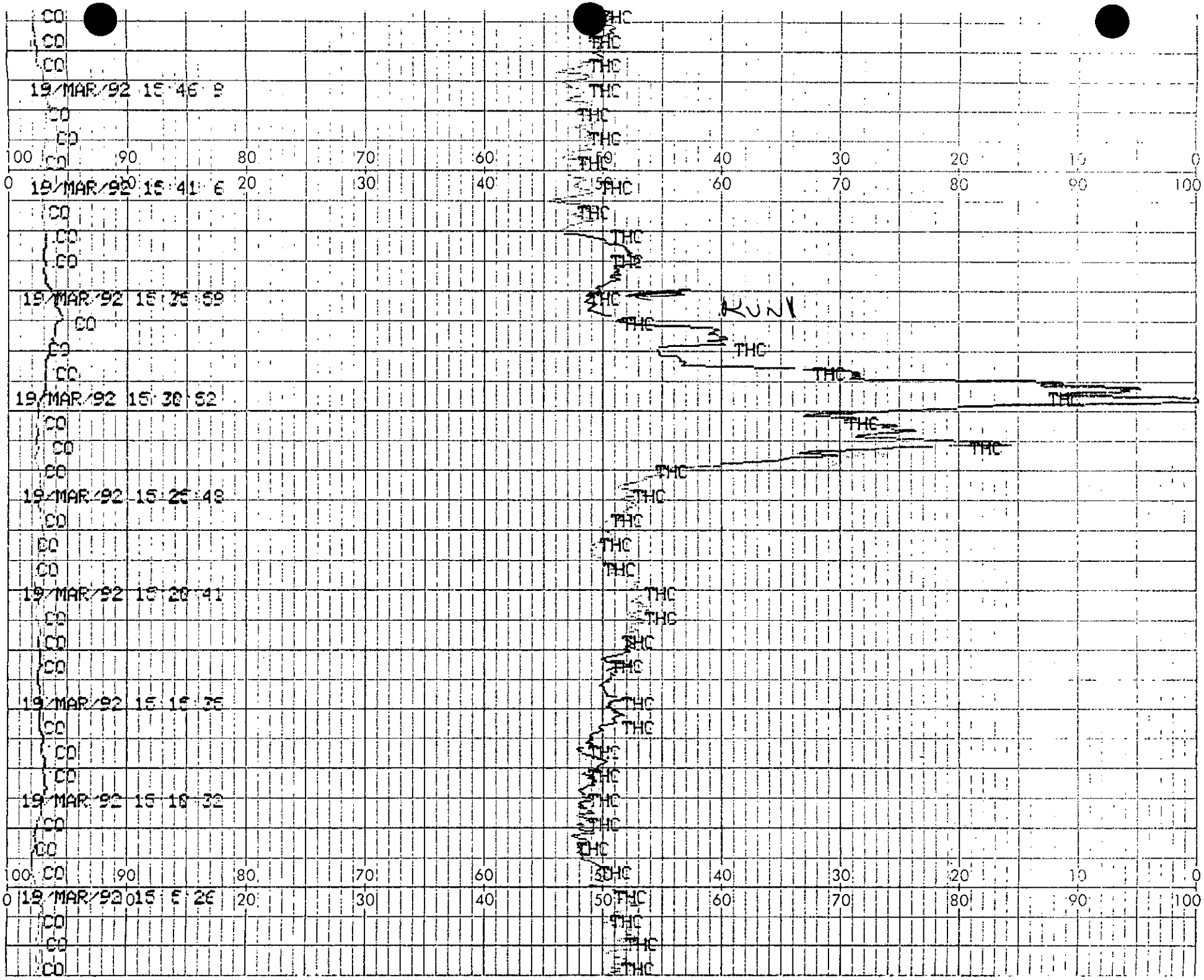

19/MAR/92 10 19 45
19/MAR/92 10 14 42
19/MAR/92 10 9 34
19/MAR/92 10 4 31
19/MAR/92 9 59 23
19/MAR/92 9 54 16
19/MAR/92 9 49 13
19/MAR/92 9 44 6
19/MAR/92 9 39 2
CO
THC
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
10:04 ~85 PPM SPIKE
due TO Possible Propane release
FROM STORAGE TANK NEAR INTAKE
TO Tube FURNACE

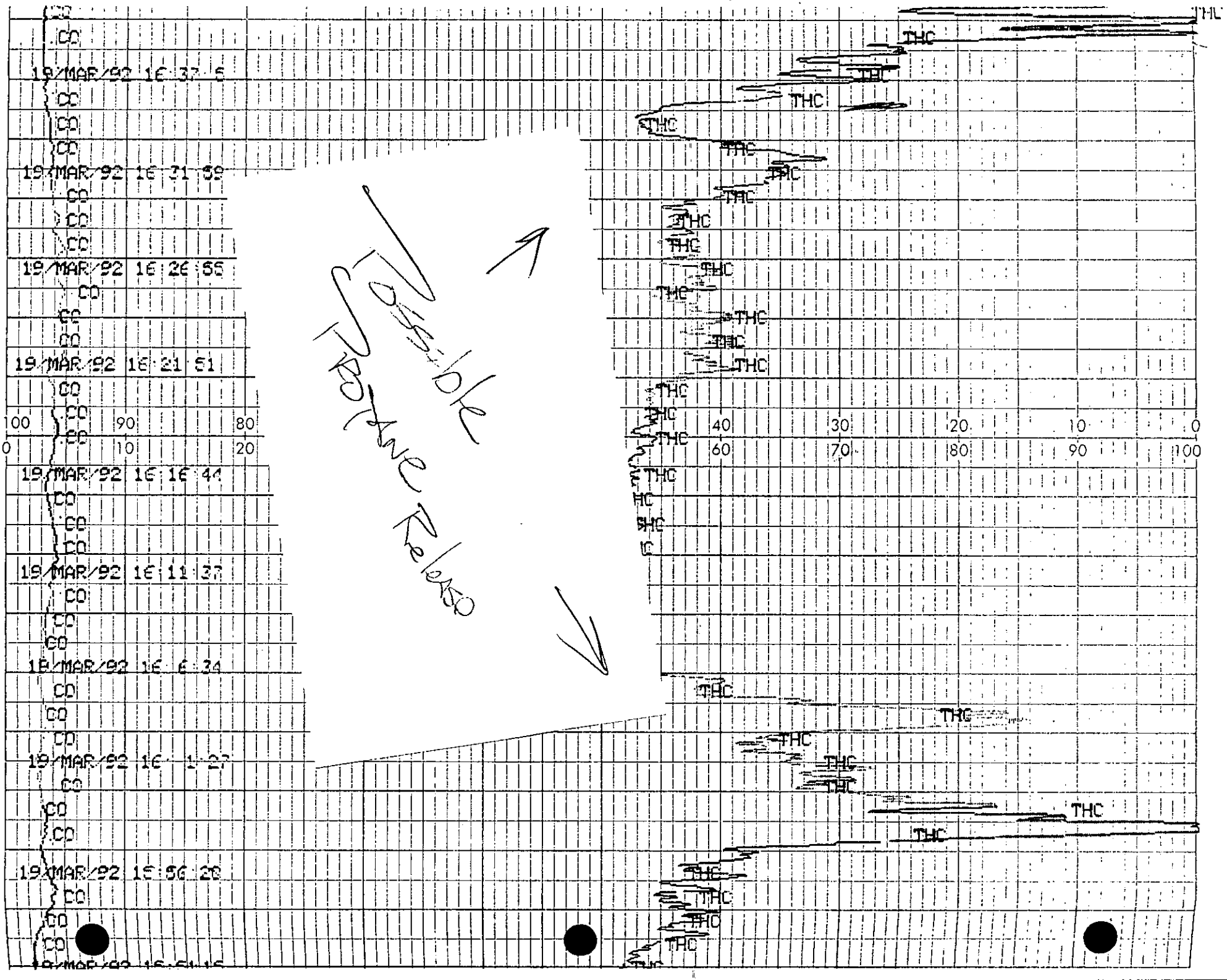

19/MAR/92 11 10 43
19/MAR/92 11 5 25
19/MAR/92 11 0 36
19/MAR/92 10 55 26
19/MAR/92 10 50 19
ZERO
SYSTEM BOLAS
MID
19/MAR/92 10 45 17
19/MAR/92 10 40 7
19/MAR/92 10 35 4
19/MAR/92 10 29 58
CO
THC
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100

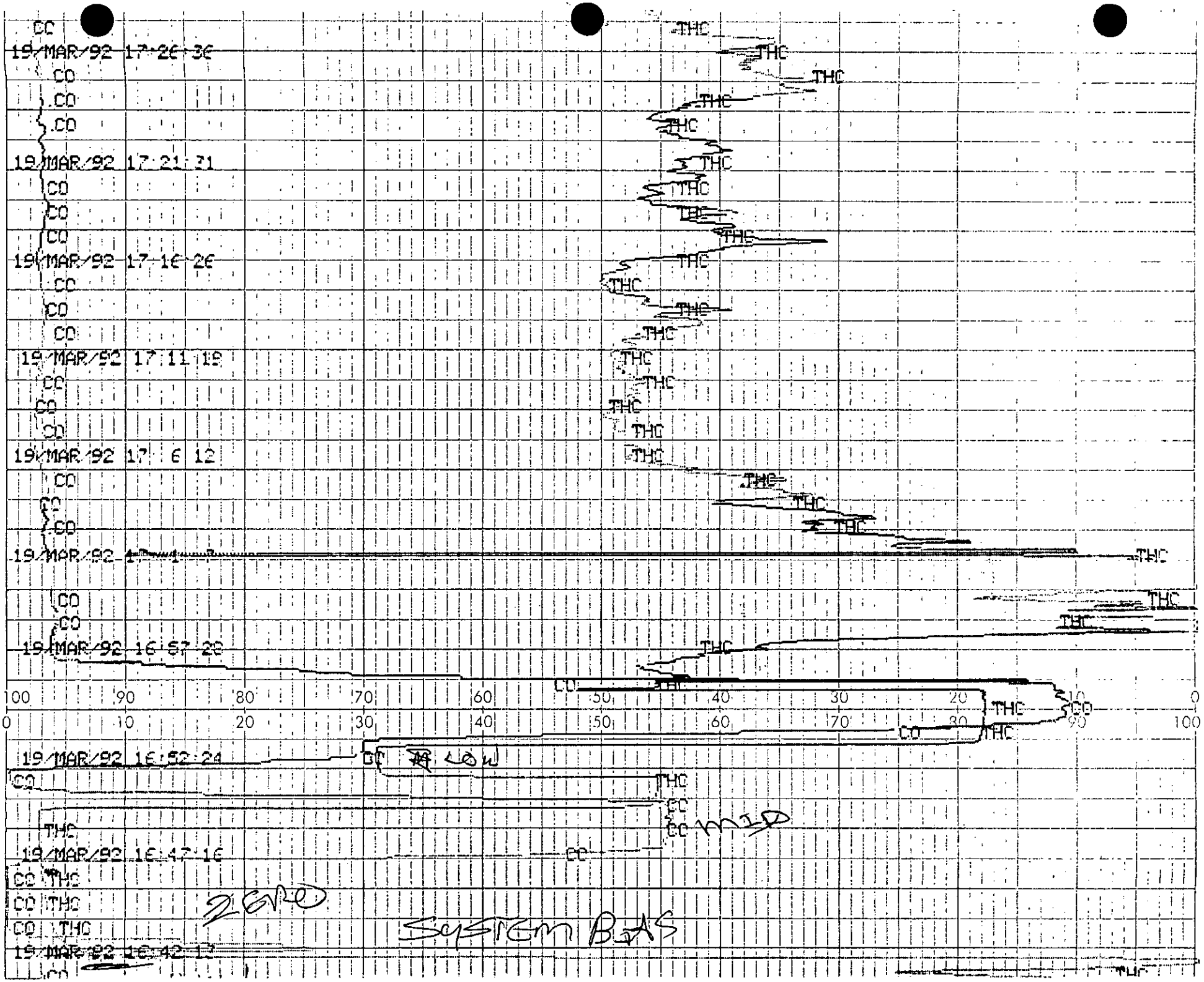

19/MAR/92 12 1 37
19/MAR/92 11 56 33
19/MAR/92 11 51 27
19/MAR/92 11 46 20
19/MAR/92 11 41 17
19/MAR/92 11 36 11
19/MAR/92 11 31 4
19/MAR/92 11 26 57
19/MAR/92 11 20 53
19/MAR/92 11 16 46
CO
THC
0 10 20 30 40 50 60 70 80 90 100

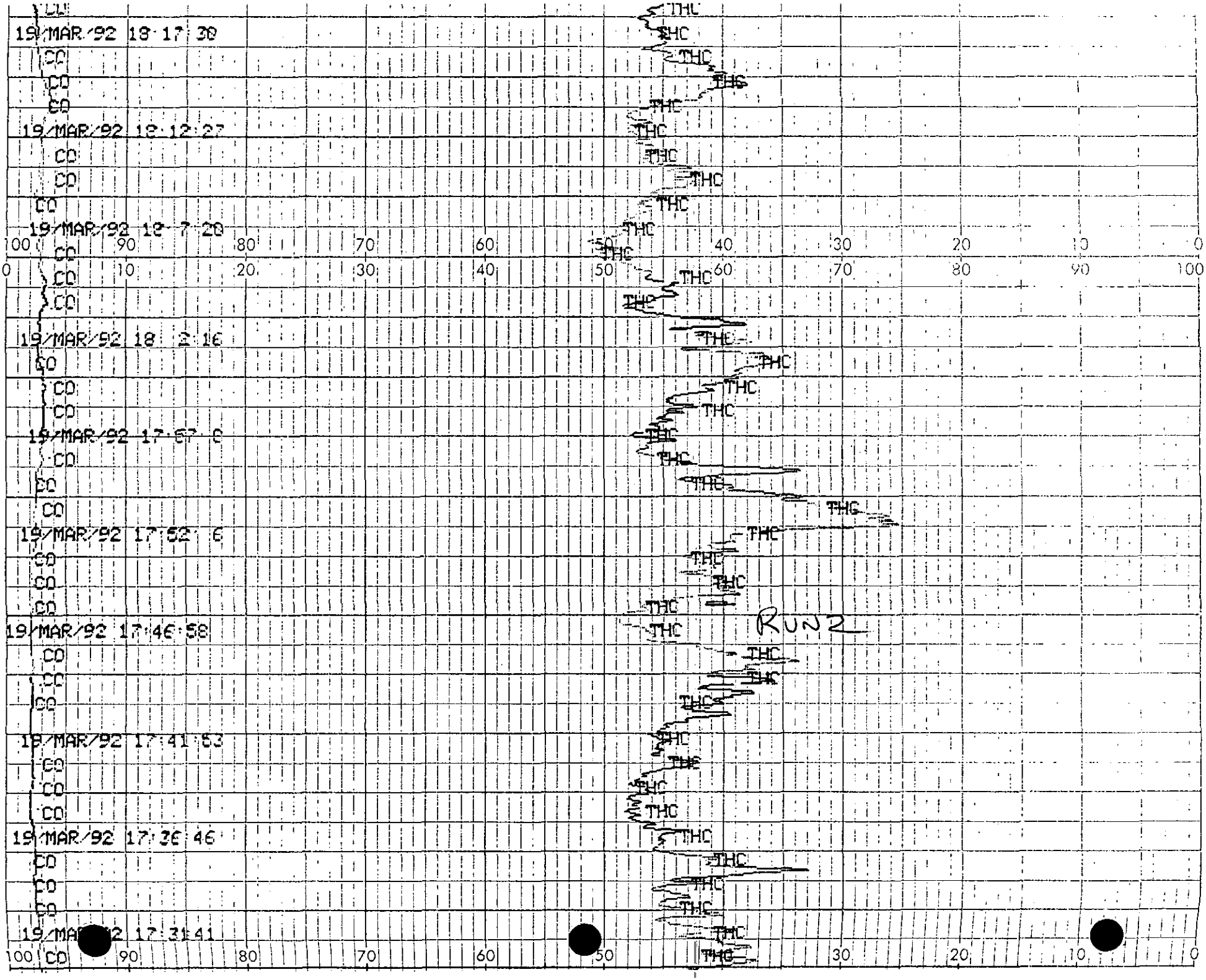

CO
19/MAR/92 12:52:34
19/MAR/92 12:47:26
19/MAR/92 12:42:22
19/MAR/92 12:37:18
19/MAR/92 12:32:11
19/MAR/92 12:27:4
19/MAR/92 12:21:59
19/MAR/92 12:16:55
19/MAR/92 12:11:50
19/MAR/92 12:6:43
THC
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100

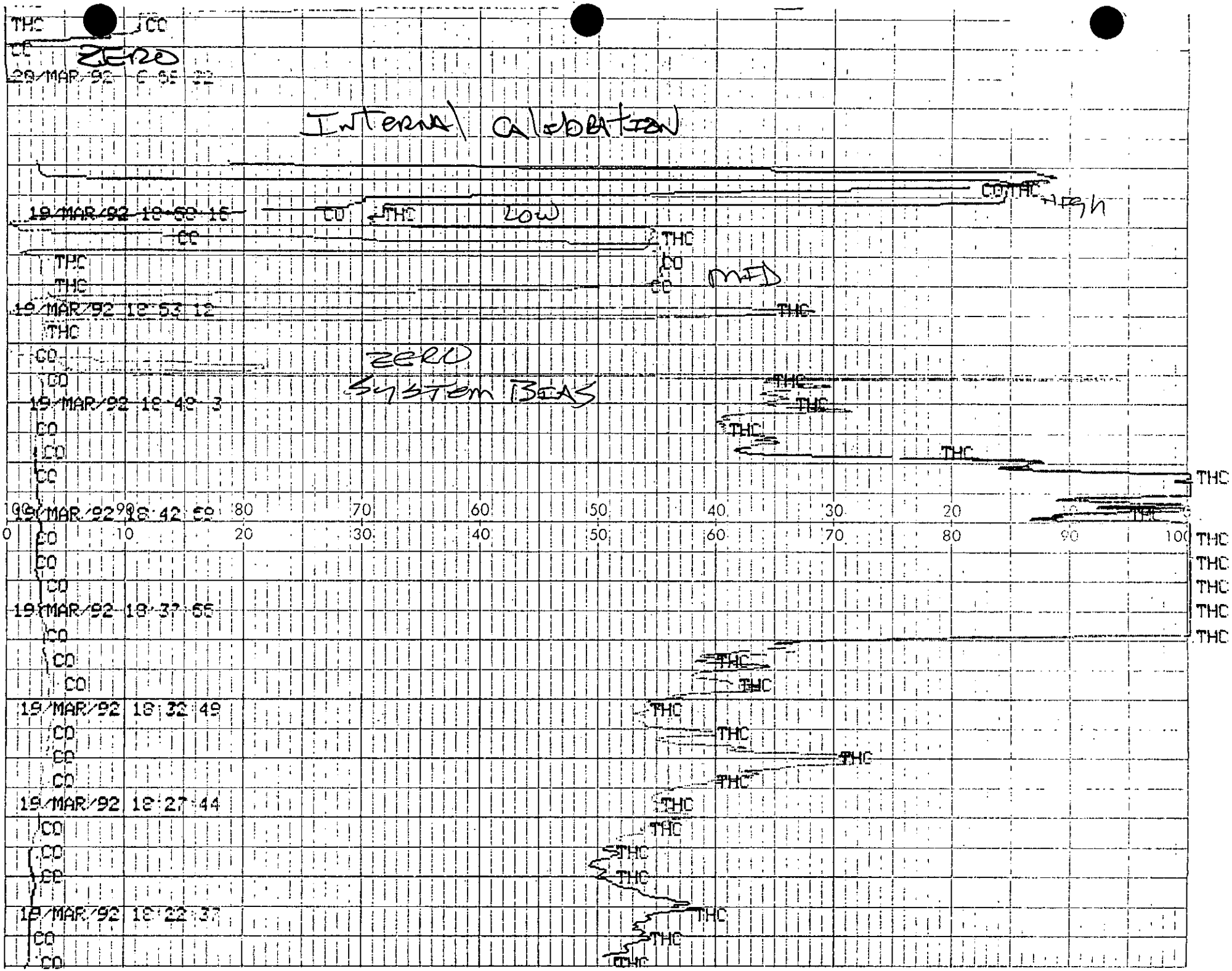

19/MAR/92 14:56:15
19/MAR/92 14:50:10
19/MAR/92 14:45:
19/MAR/92 14:39:57
19/MAR/92 14:34:50
STACK
100 90 80 70 60 50 40 30 20 10 0
19/MAR/92 13:12:55
LOW
19/MAR/92 13:7:49
MED
ZERO
19/MAR/92 13:2:44
SYSTEM BIAS
19/MAR/92 12:57:37
CO
THC

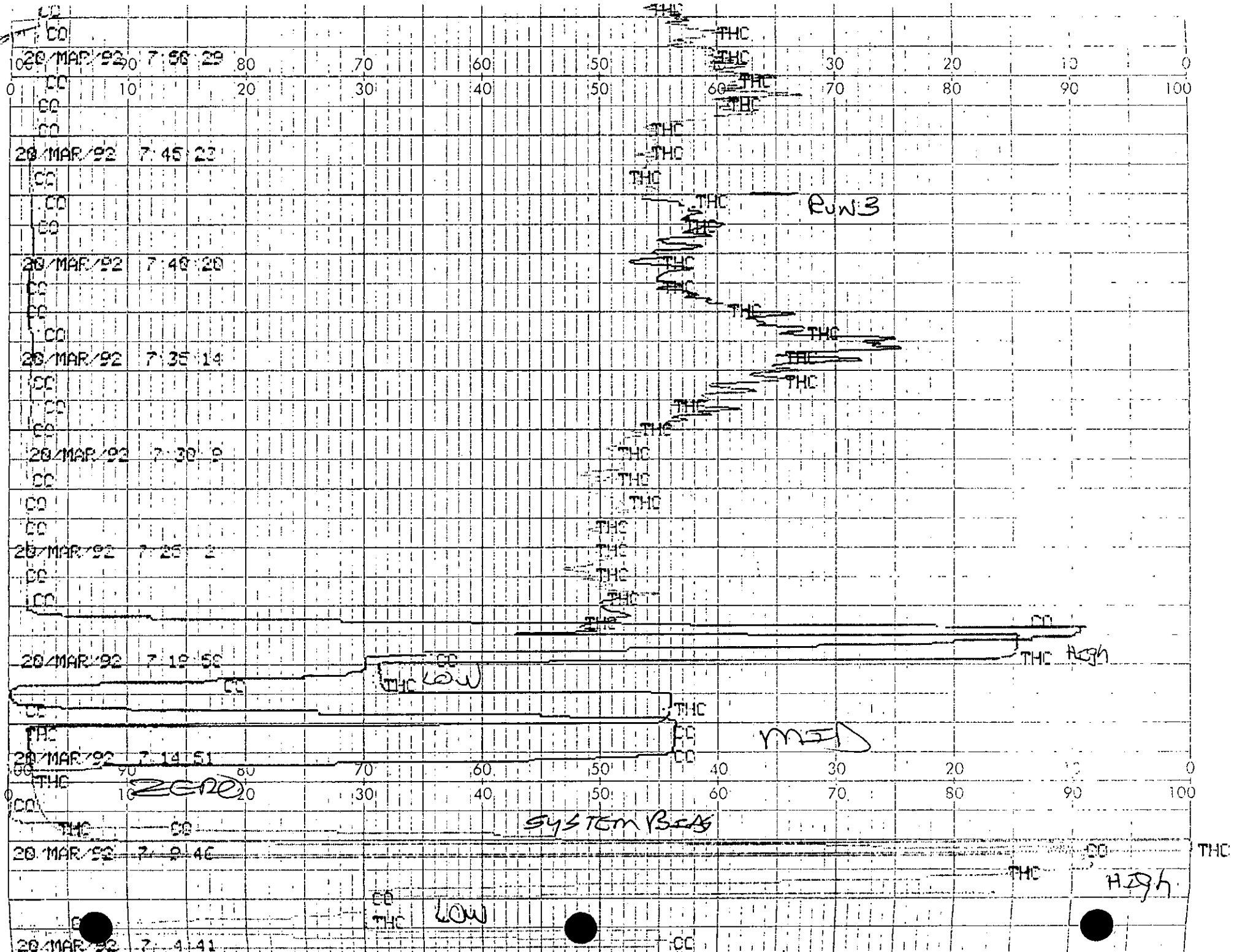

CO
THC
19/MAR/92 15 46 9
19/MAR/92 15 41 6
19/MAR/92 15 36 59
19/MAR/92 15 30 52
19/MAR/92 15 25 48
19/MAR/92 15 20 41
19/MAR/92 15 15 35
19/MAR/92 15 10 32
19/MAR/92 15 5 26
RUN1
100 90 80 70 60 50 40 30 20 10 0

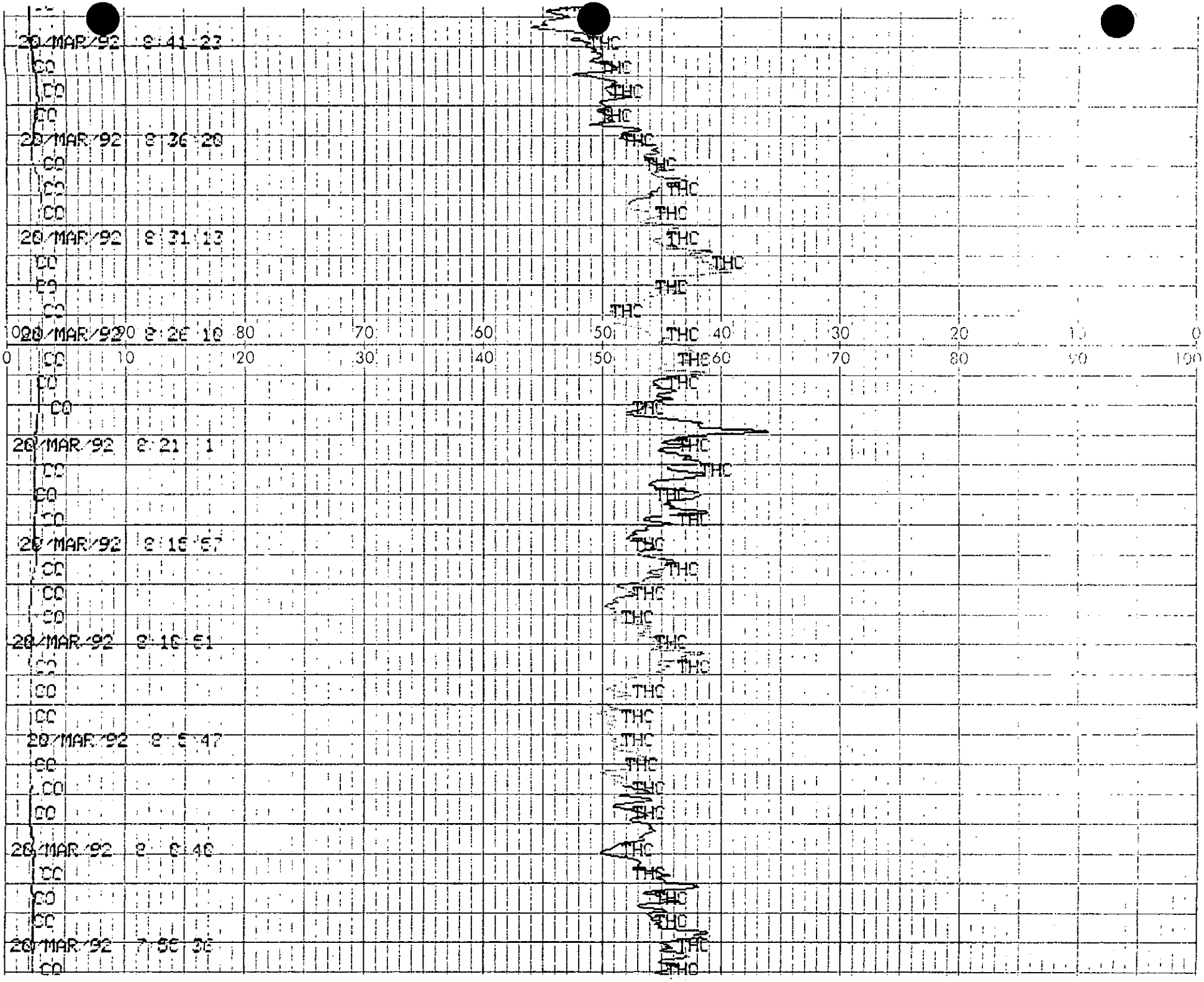

CO
19/MAR/92 16:37:5
19/MAR/92 16:31:39
19/MAR/92 16:26:55
19/MAR/92 16:21:51
19/MAR/92 16:16:44
19/MAR/92 16:11:37
19/MAR/92 16:6:34
19/MAR/92 16:1:27
19/MAR/92 15:56:20
THC
100 90 80 70 60 40 30 20 10 0
0 10 20 30 40 60 70 80 90 100
Possible Propane Release

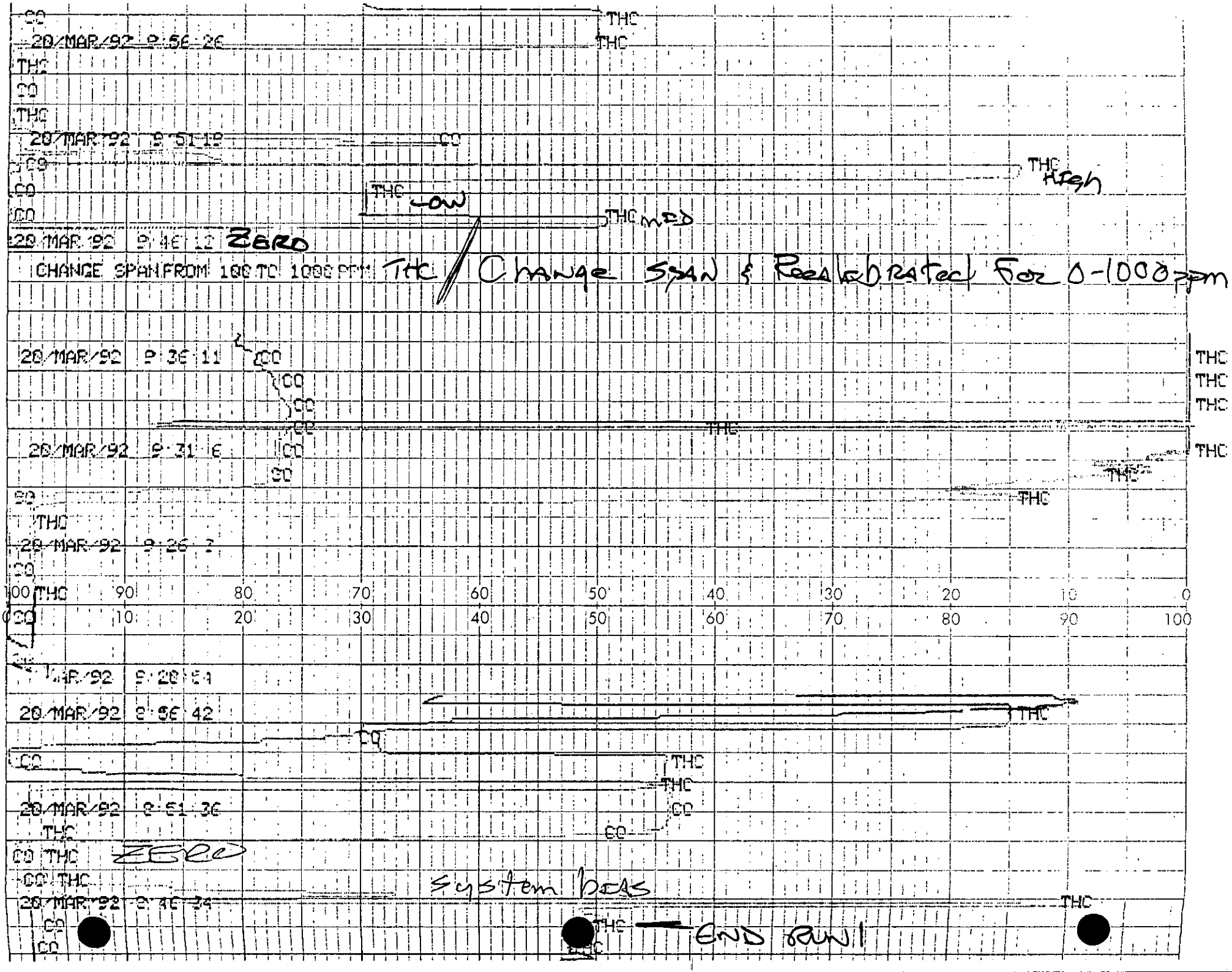

19/MAR/92 17:26:36
19/MAR/92 17:21:31
19/MAR/92 17:16:26
19/MAR/92 17:11:19
19/MAR/92 17:6:12
19/MAR/92 16:57:20
19/MAR/92 16:52:24
19/MAR/92 16:47:16
CO
THC
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
LOW
MID
ZERO
SYSTEM BIAS

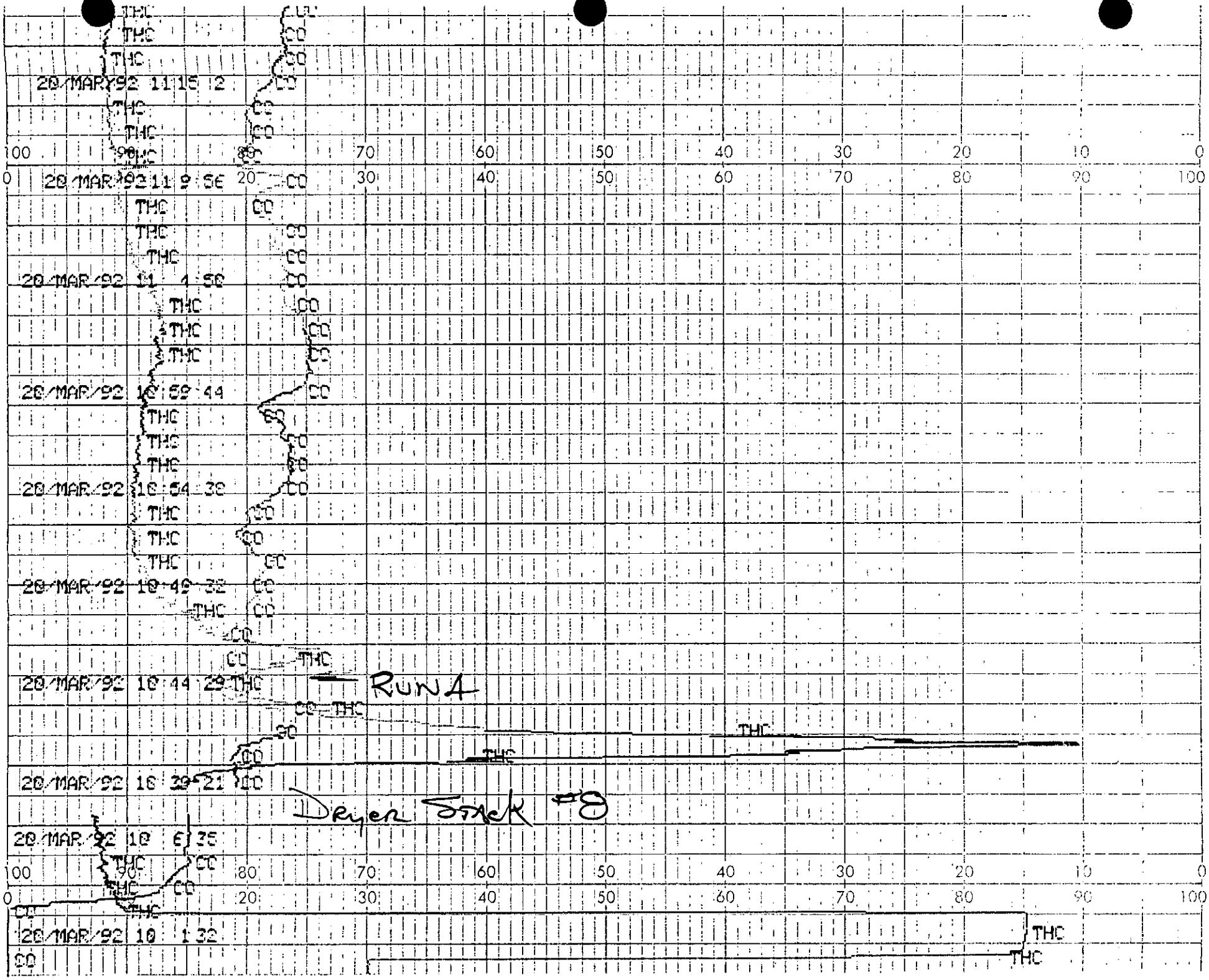

19/MAR/92 18:17:30
19/MAR/92 18:12:27
19/MAR/92 18:7:20
19/MAR/92 18:2:16
19/MAR/92 17:57:0
19/MAR/92 17:52:6
19/MAR/92 17:46:58
19/MAR/92 17:41:53
19/MAR/92 17:36:46
19/MAR/92 17:31:41
CO
THC
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
RUN2

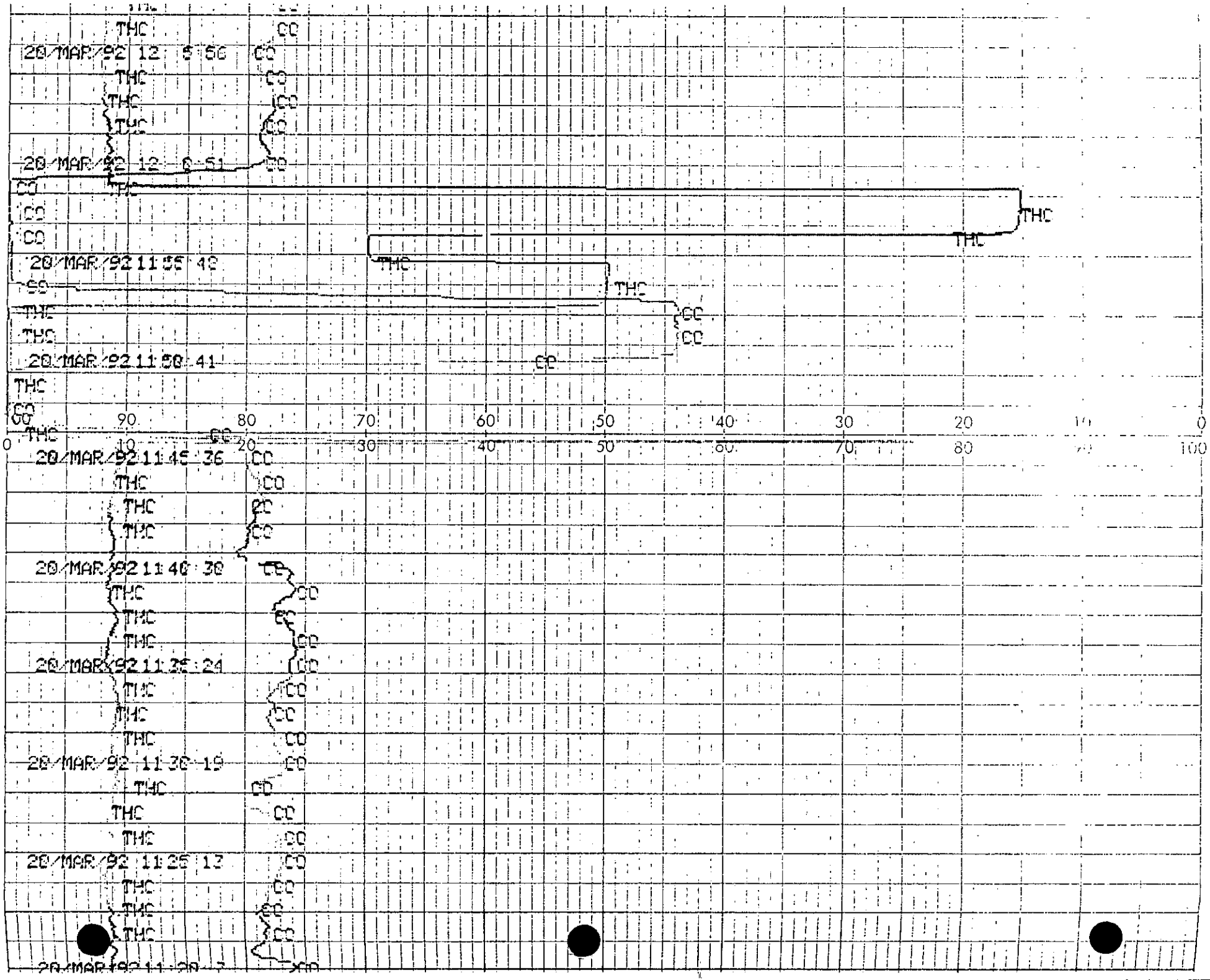

THC
CO
CO
ZERO
19/MAR/92 18 55 32
INTERNAL CALIBRATION
CO THC HIGH
19/MAR/92 18 50 16
CO
THC
LOW
CO
THC
THC
CO
CO
MED
19/MAR/92 18 53 12
THC
THC
CO
CO
ZERO
SYSTEM BIAS
THC
THC
19/MAR/92 18 49 3
CO
CO
CO
THC
THC
THC
19/MAR/92 18 42 59
CO
CO
CO
19/MAR/92 18 37 55
CO
CO
CO
THC
THC
THC
THC
THC
THC
THC
19/MAR/92 18 32 49
CO
CO
CO
THC
THC
THC
THC
19/MAR/92 18 27 44
CO
CO
CO
THC
THC
THC
THC
19/MAR/92 18 22 37
CO
CO
THC
THC
THC
0
10
20
30
40
50
60
70
80
90
100

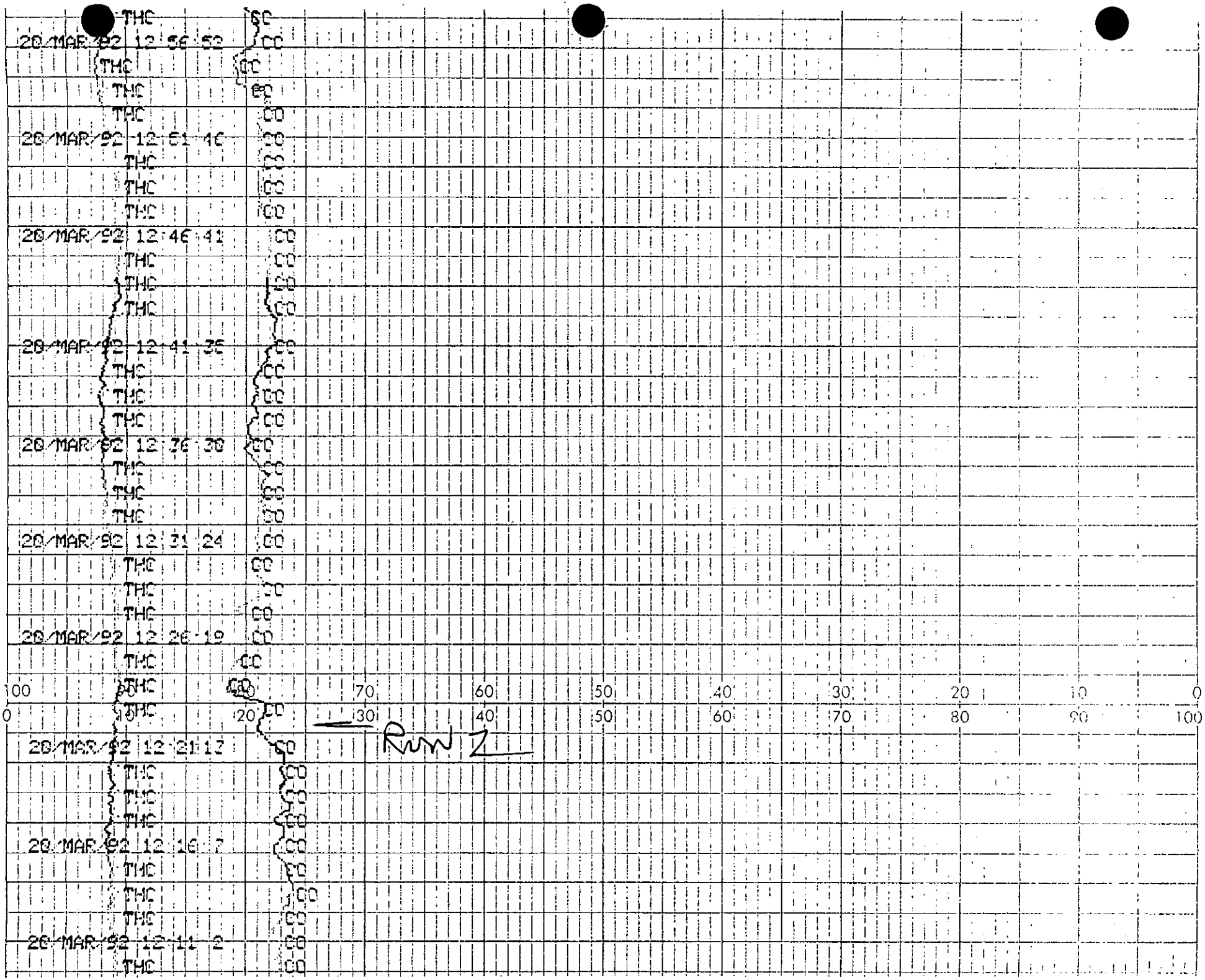

20/MAR/92 7:56:29
20/MAR/92 7:45:23
20/MAR/92 7:40:20
20/MAR/92 7:35:14
20/MAR/92 7:30:9
20/MAR/92 7:25:2
20/MAR/92 7:19:56
20/MAR/92 7:14:51
20/MAR/92 7:9:46
20/MAR/92 7:4:41
CO
THC
Run 3
High
Low
Mid
Zero
System Bias

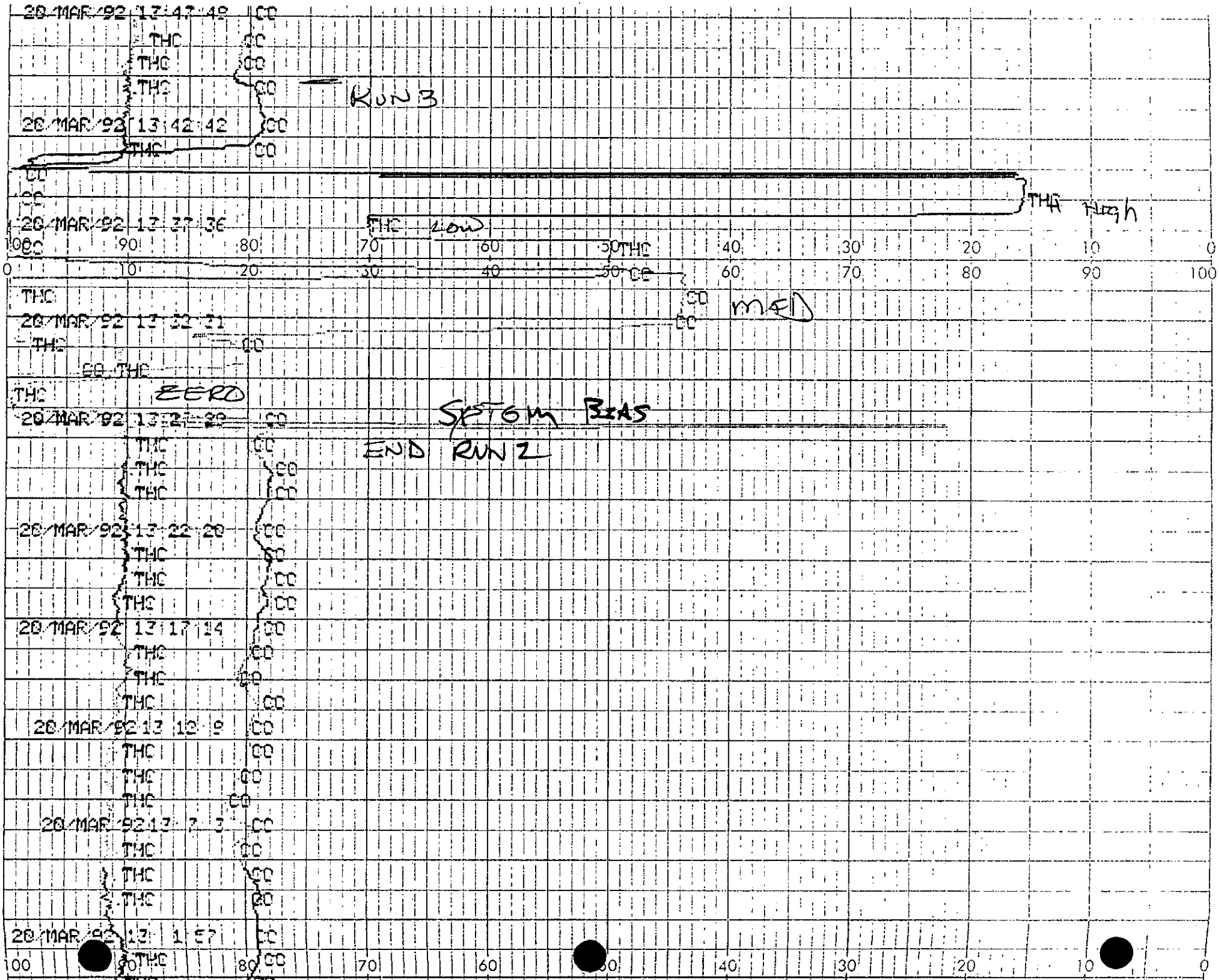

20/MAR/92 8:41:23
20/MAR/92 8:36:20
20/MAR/92 8:31:13
20/MAR/92 8:26:10
20/MAR/92 8:21:1
20/MAR/92 8:15:57
20/MAR/92 8:10:51
20/MAR/92 8:5:47
20/MAR/92 8:0:40
20/MAR/92 7:55:36
CO
THC
0 10 20 30 40 50 60 70 80 90 100

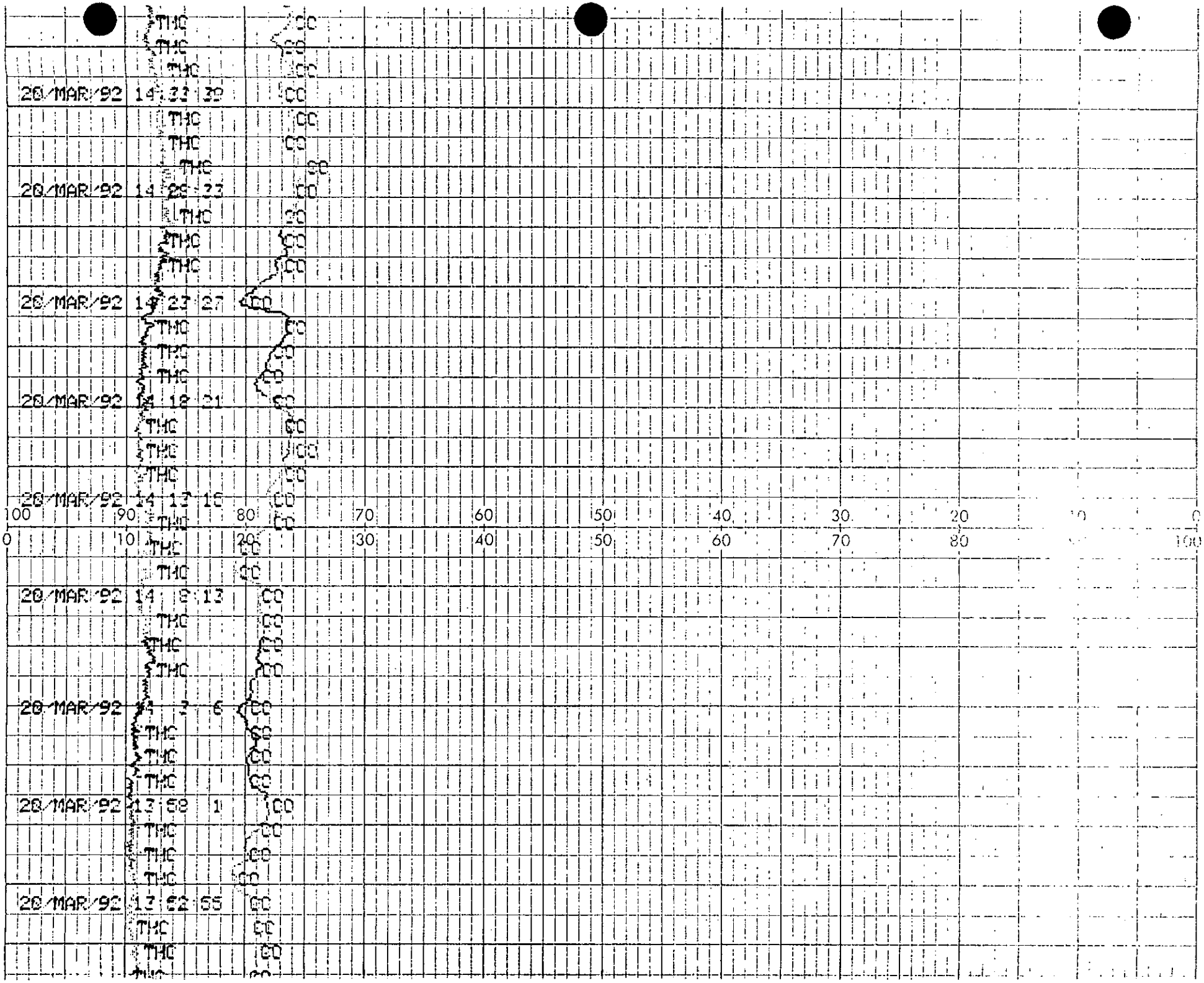

CO
20/MAR/92 8:56:26
THC
CO
THC
20/MAR/92 8:51:18
CO
CO
CO
CO
THC
THC LOW
THC MED
THC High
20 MAR 92 8:46:12 ZERO
CHANGE SPAN FROM 100 TO 1000 PPM THC / Change Span & Recalibrated for 0-1000 ppm
20/MAR/92 8:36:11
CO
CO
CO
CO
THC
THC
THC
THC
20/MAR/92 8:31:6
CO
CO
THC
THC
THC
CO
THC
20/MAR/92 8:26:7
CO
100 THC 90 80 70 60 50 40 30 20 10 0
CO 10 20 30 40 50 60 70 80 90 100
20/MAR/92 8:20:54
20/MAR/92 8:56:42
THC
CO
CO
THC
THC
CO
20/MAR/92 8:51:36
THC
CO
CO THC ZERO
CO THC
System BCAS
20/MAR/92 8:46:24
THC
CO
CO
THC
END RUN!

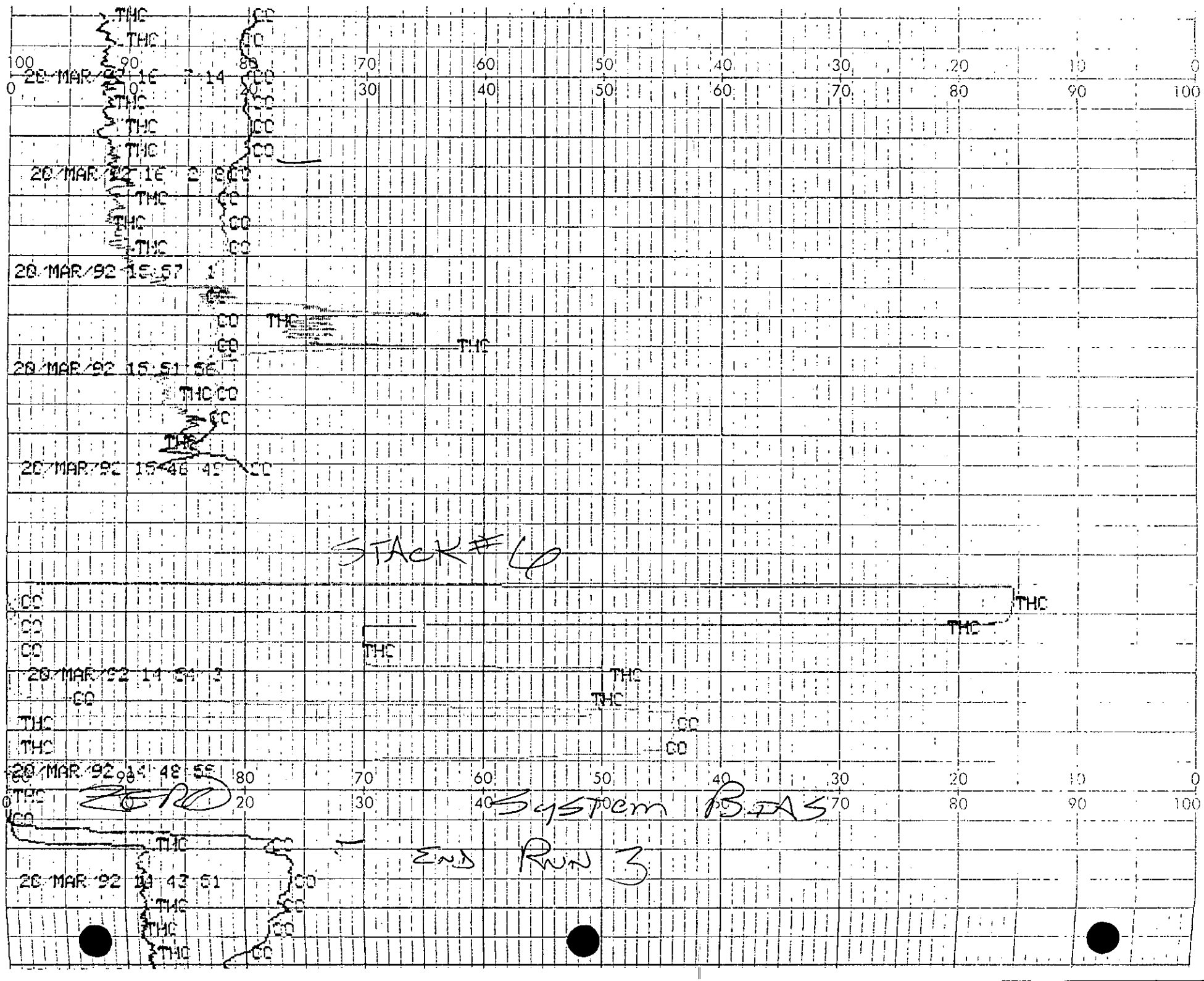

20/MAR/92 11 15 2
20/MAR/92 11 9 56
20/MAR/92 11 4 50
20/MAR/92 10 59 44
20/MAR/92 10 54 38
20/MAR/92 10 49 32
20/MAR/92 10 44 29
RUN 4
20/MAR/92 10 39 21
Dryer Stack #8
20/MAR/92 10 6 35
20/MAR/92 10 1 32
THC
CO

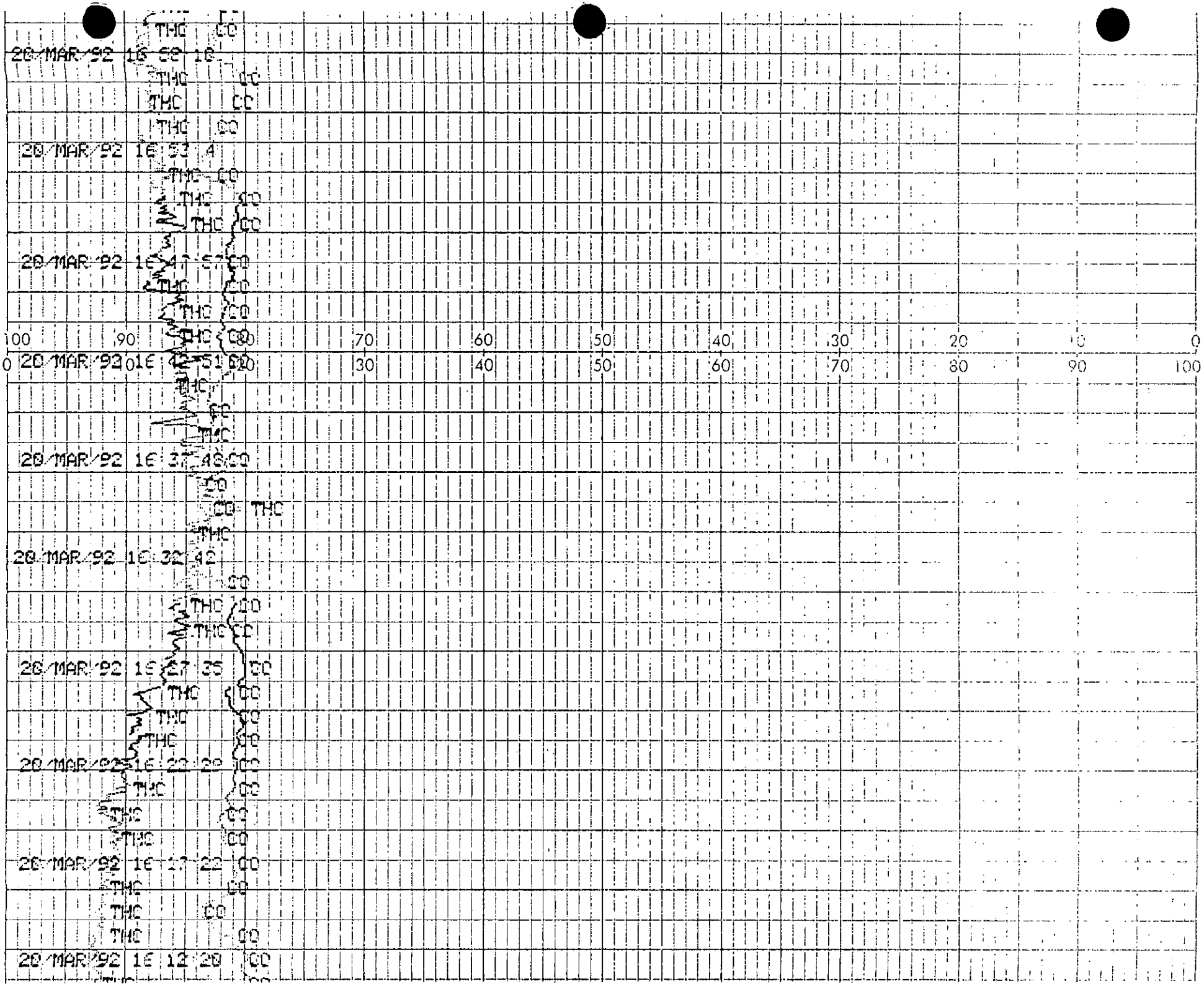

20/MAR/92 12 5 56
20/MAR/92 12 0 51
20/MAR/92 11 55 49
20/MAR/92 11 50 41
20/MAR/92 11 45 36
20/MAR/92 11 40 30
20/MAR/92 11 35 24
20/MAR/92 11 30 19
20/MAR/92 11 25 13
THC
CO
0
10
20
30
40
50
60
70
80
90
100

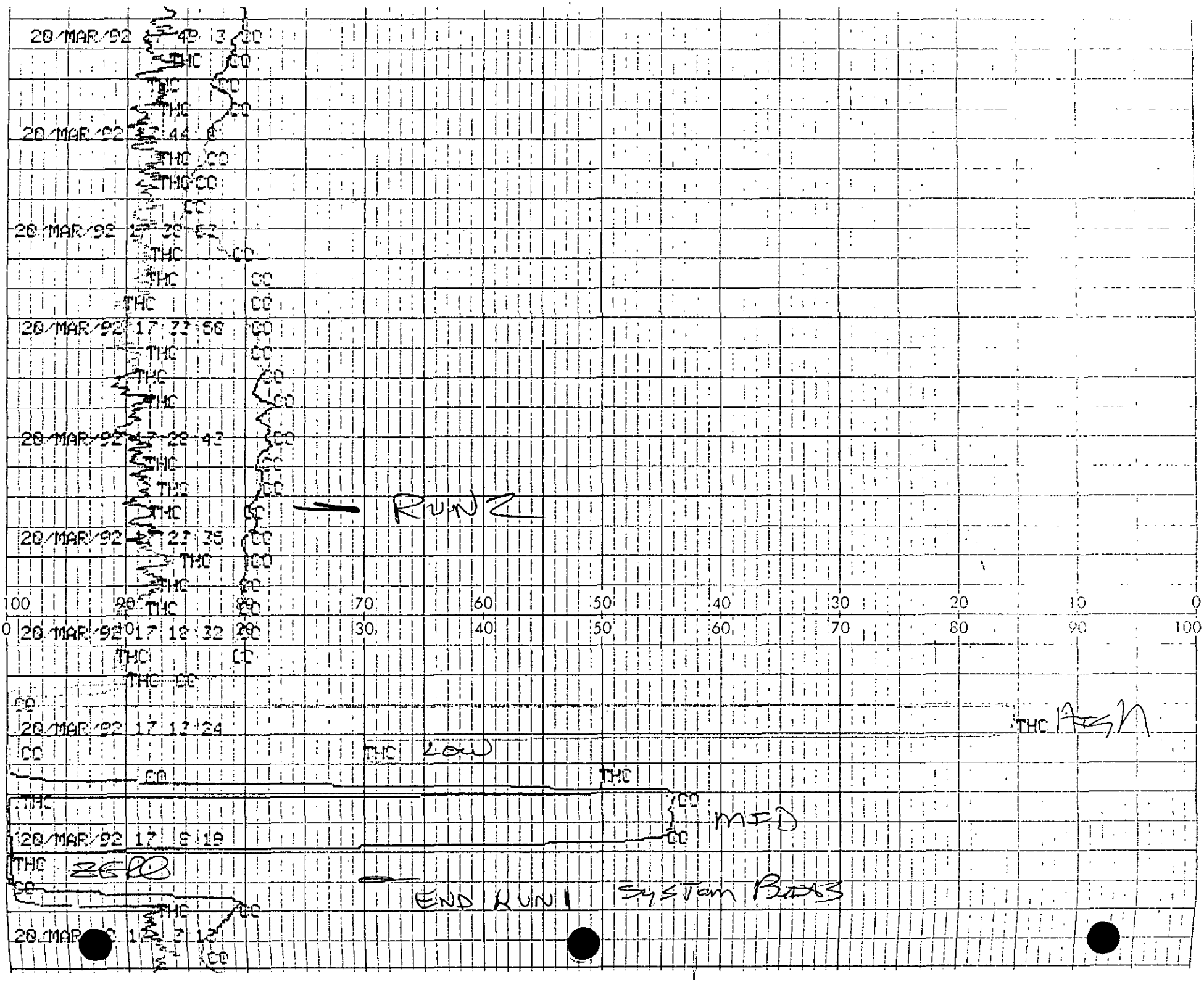

THC
CO
20/MAR/92 12:56:52
20/MAR/92 12:51:16
20/MAR/92 12:46:41
20/MAR/92 12:41:35
20/MAR/92 12:36:30
20/MAR/92 12:31:24
20/MAR/92 12:26:19
20/MAR/92 12:21:13
20/MAR/92 12:16:7
20/MAR/92 12:11:2
100
0
70
60
50
40
30
20
10
0
30
40
50
60
70
80
90
100
Run 1

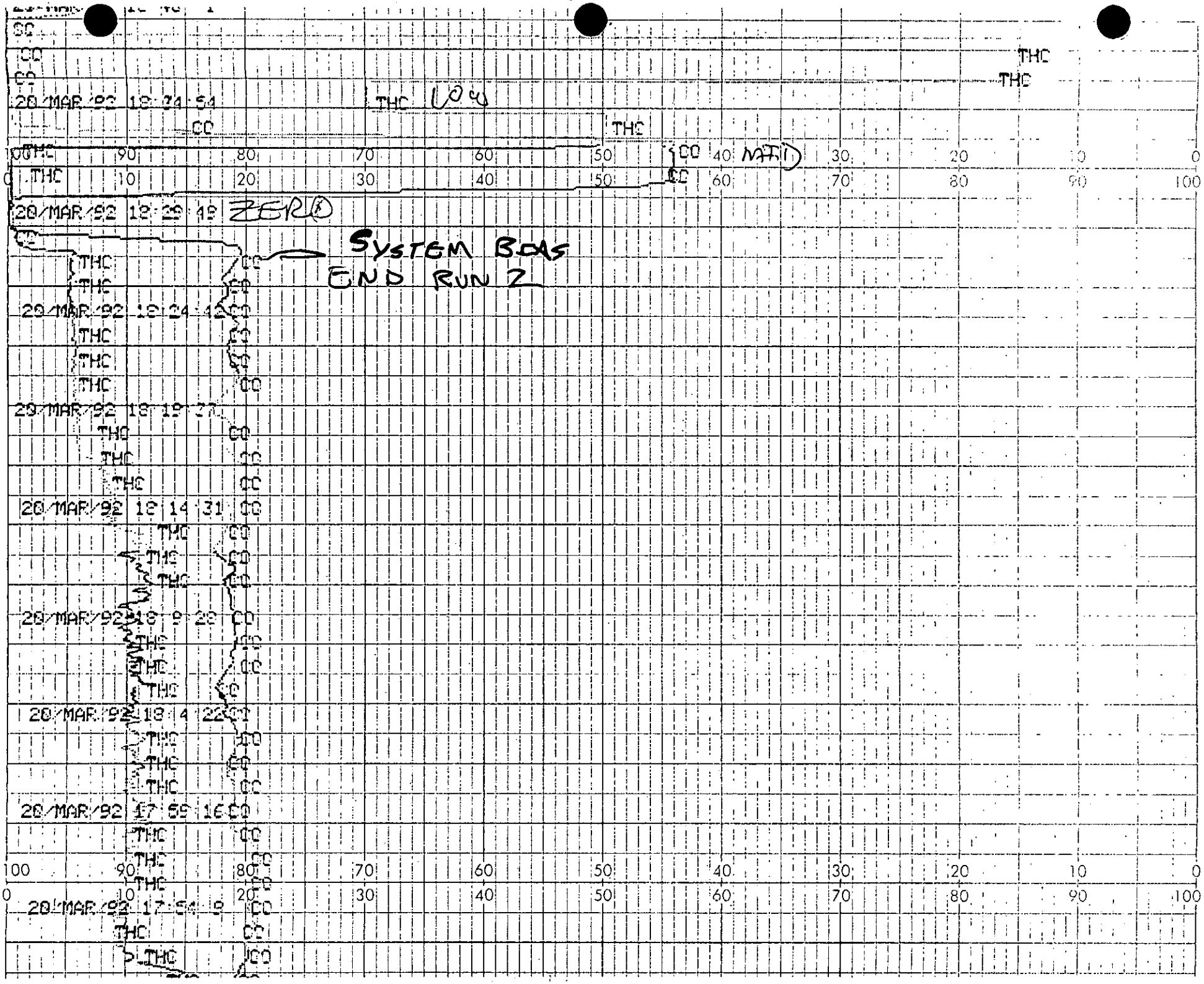

20 MAR 92 13 47 49
THC
CO
RUN 3
20 MAR 92 13 42 42
THC High
20 MAR 92 13 37 36
THC Low
THC
CO
MED
20 MAR 92 13 32 31
ZERO
SPAN BIAS
20 MAR 92 13 27 20
END RUN 2
20 MAR 92 13 22 20
20 MAR 92 13 17 14
20 MAR 92 13 12 9
20 MAR 92 13 7 3
20 MAR 92 13 1 57
100
90
80
70
60
50
40
30
20
10
0


THC
CO
20/MAR/92 14 33 39
20/MAR/92 14 28 23
20/MAR/92 14 23 27
20/MAR/92 14 18 21
20/MAR/92 14 13 16
20/MAR/92 14 8 13
20/MAR/92 14 2 6
20/MAR/92 13 58 1
20/MAR/92 13 52 55
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 100


THC
CO
20 MAR 92 16 14
20 MAR 92 16 2
20 MAR 92 15 57 1
20 MAR 92 15 51 56
20 MAR 92 15 46 49
STACK # 6
20 MAR 92 14 54 3
20 MAR 92 14 48 55
ZERO
SYSTEM BIAS
END RUN 3
20 MAR 92 14 43 51
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100


THC
CO
20 MAR 92 16 52 10
20 MAR 92 16 53 4
20 MAR 92 16 47 57
20 MAR 92 01 51
20 MAR 92 16 37 48
20 MAR 92 16 32 42
20 MAR 92 16 27 35
20 MAR 92 16 22 29
20 MAR 92 16 17 22
20 MAR 92 16 12 20
100 90 70 60 50 40 30 20 10 0
0 30 40 50 60 70 80 90 100


20/MAR/92
THC
CO
RUN 2
100
90
80
70
60
50
40
30
20
10
0
THC HIGH
THC LOW
MID
ZERO
END RUN 1
SYSTEM BIAS


20/MAR/92 18:24:54
THC
CO
LOW
MATID
20/MAR/92 18:29:49
ZERO
SYSTEM BIAS
END RUN 2
20/MAR/92 18:24:4
20/MAR/92 18:19:27
20/MAR/92 18:14:31
20/MAR/92 18:9:28
20/MAR/92 18:4:22
20/MAR/92 17:59:16
20/MAR/92 17:54:9
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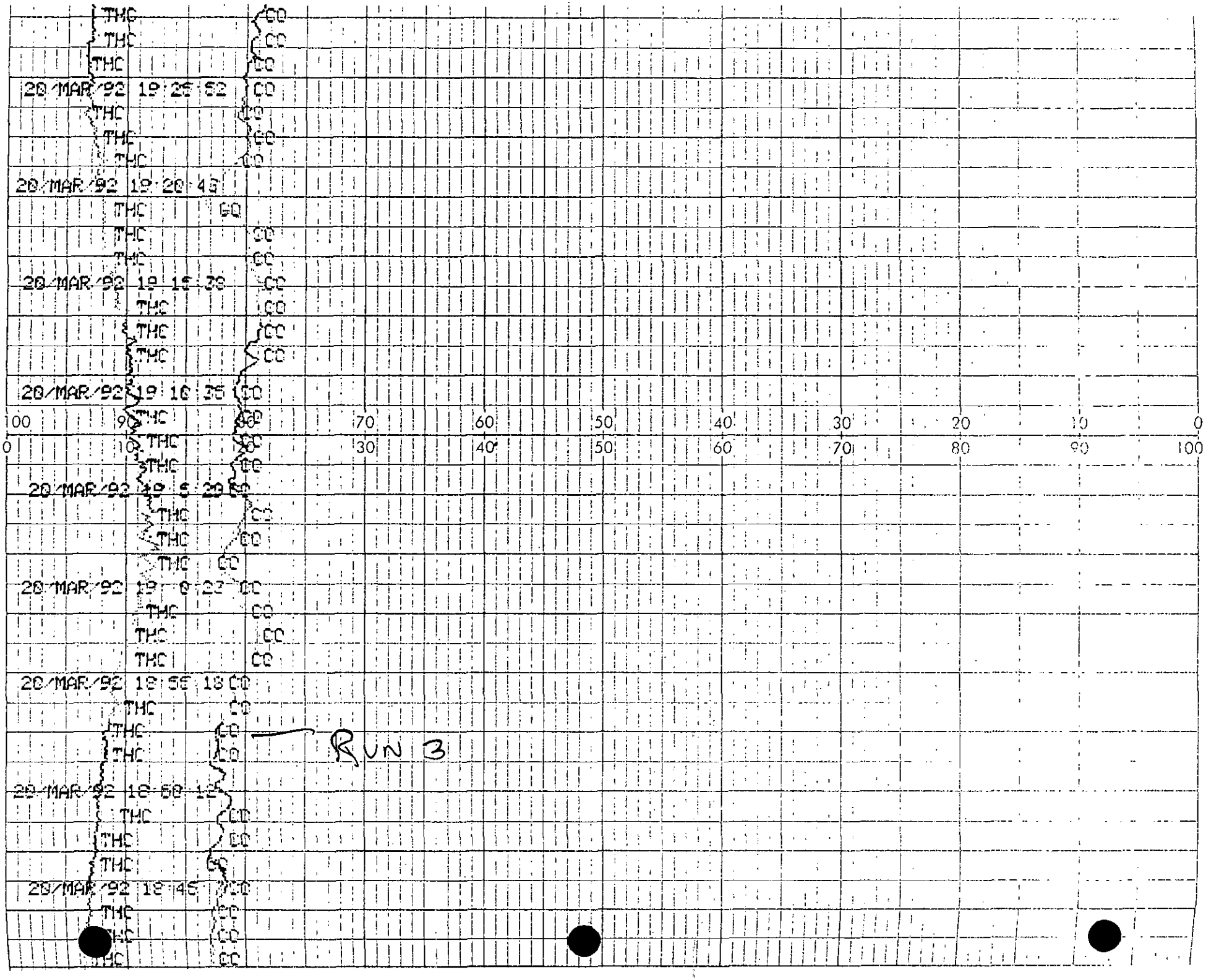
THC
CO
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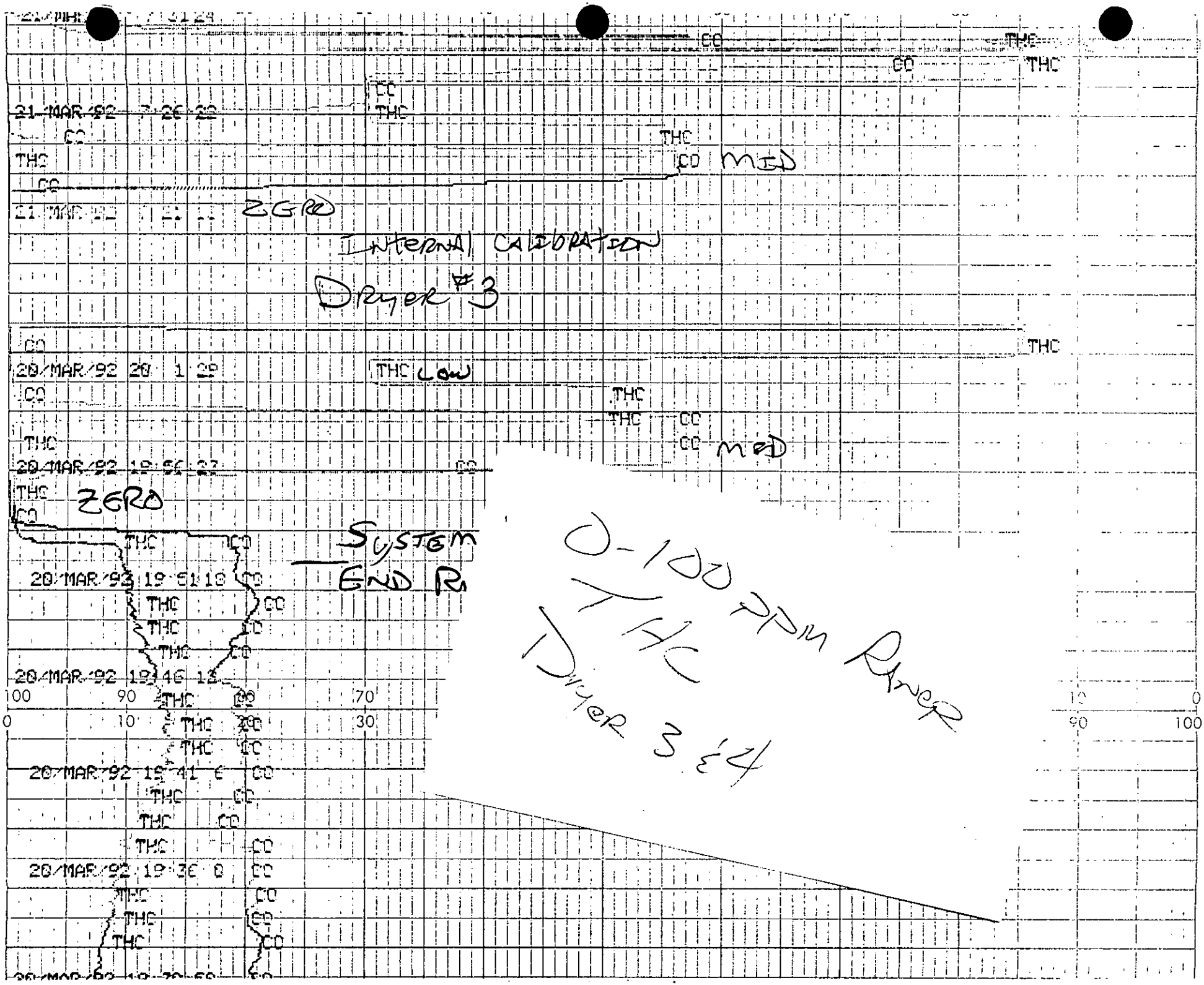
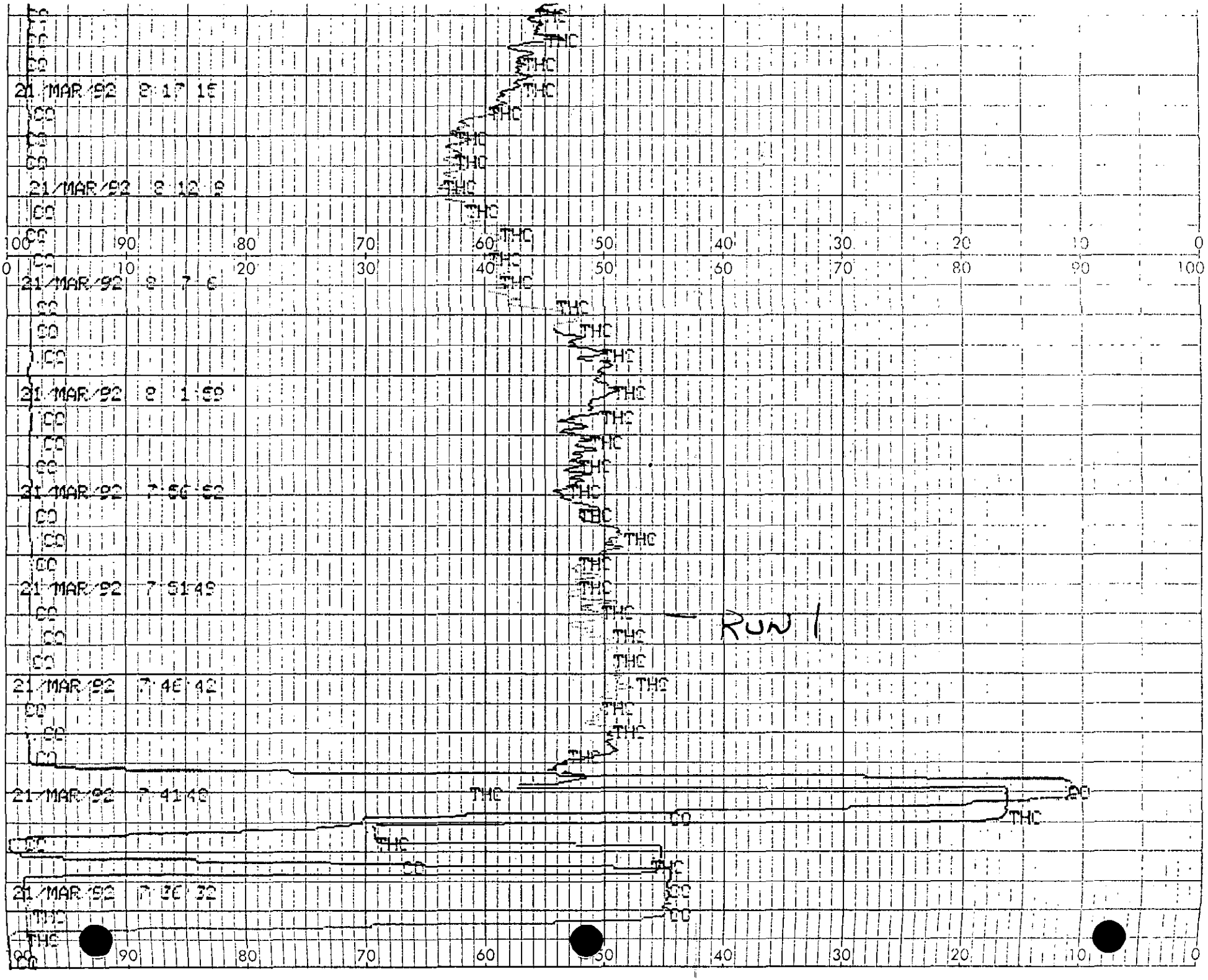
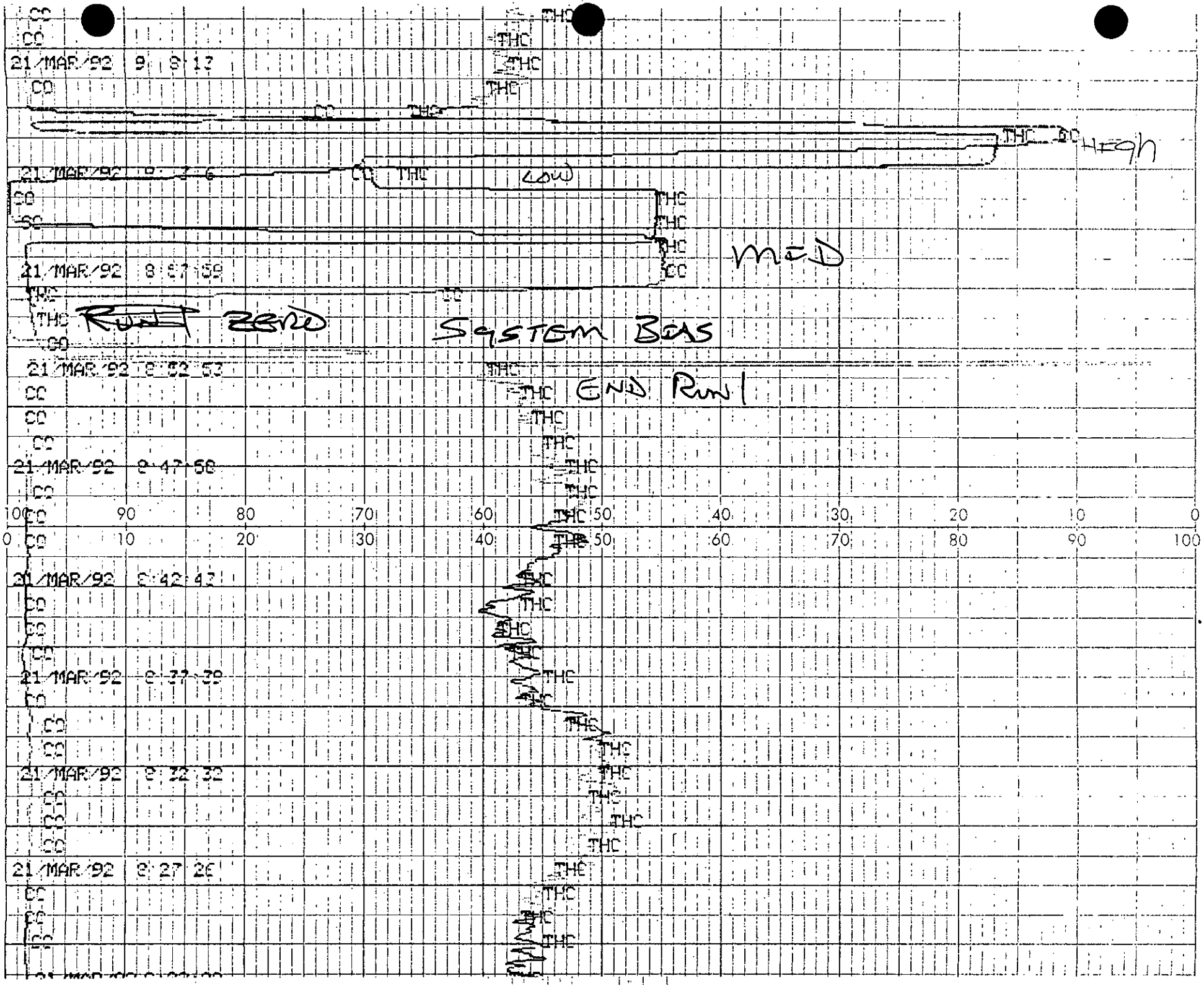
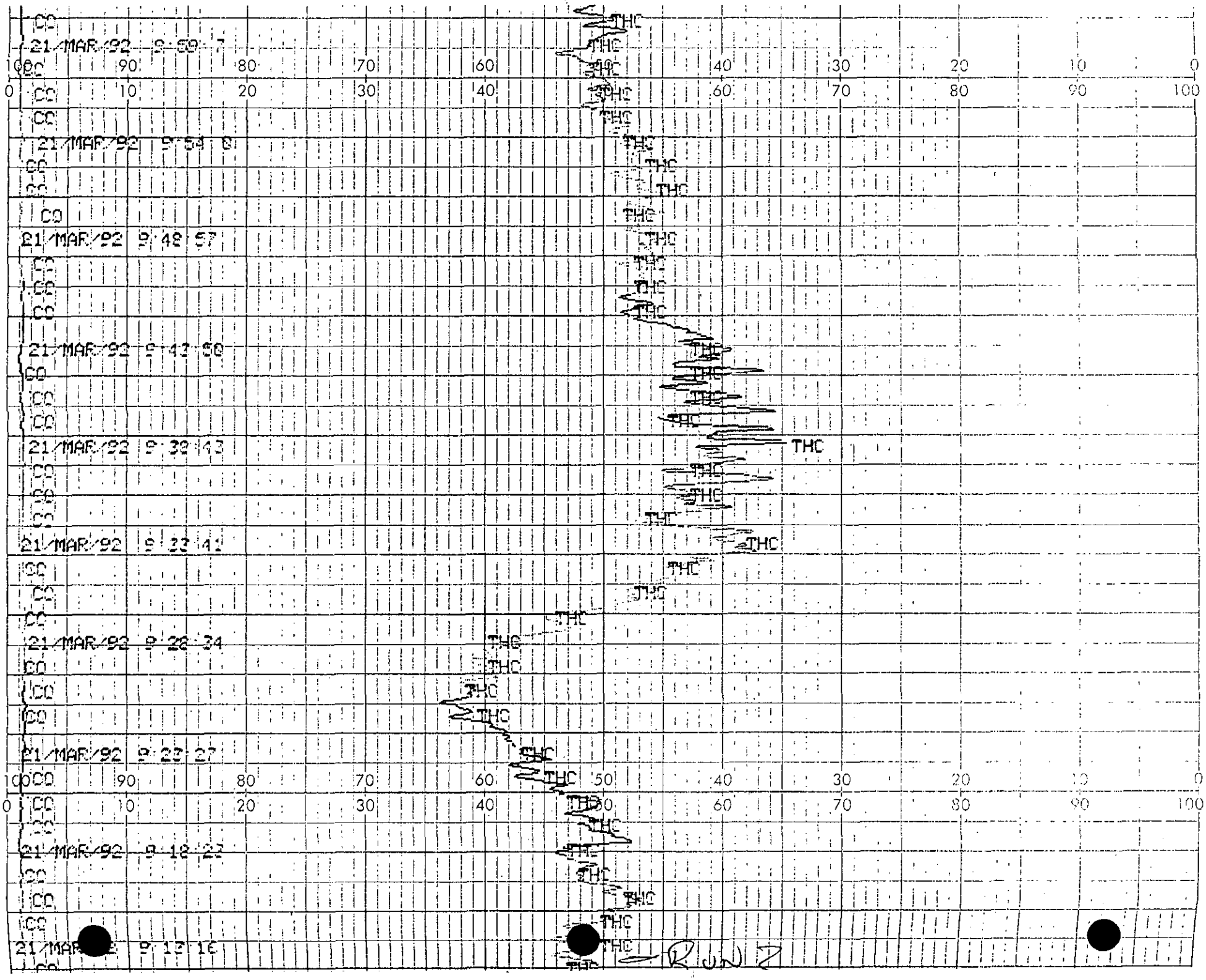
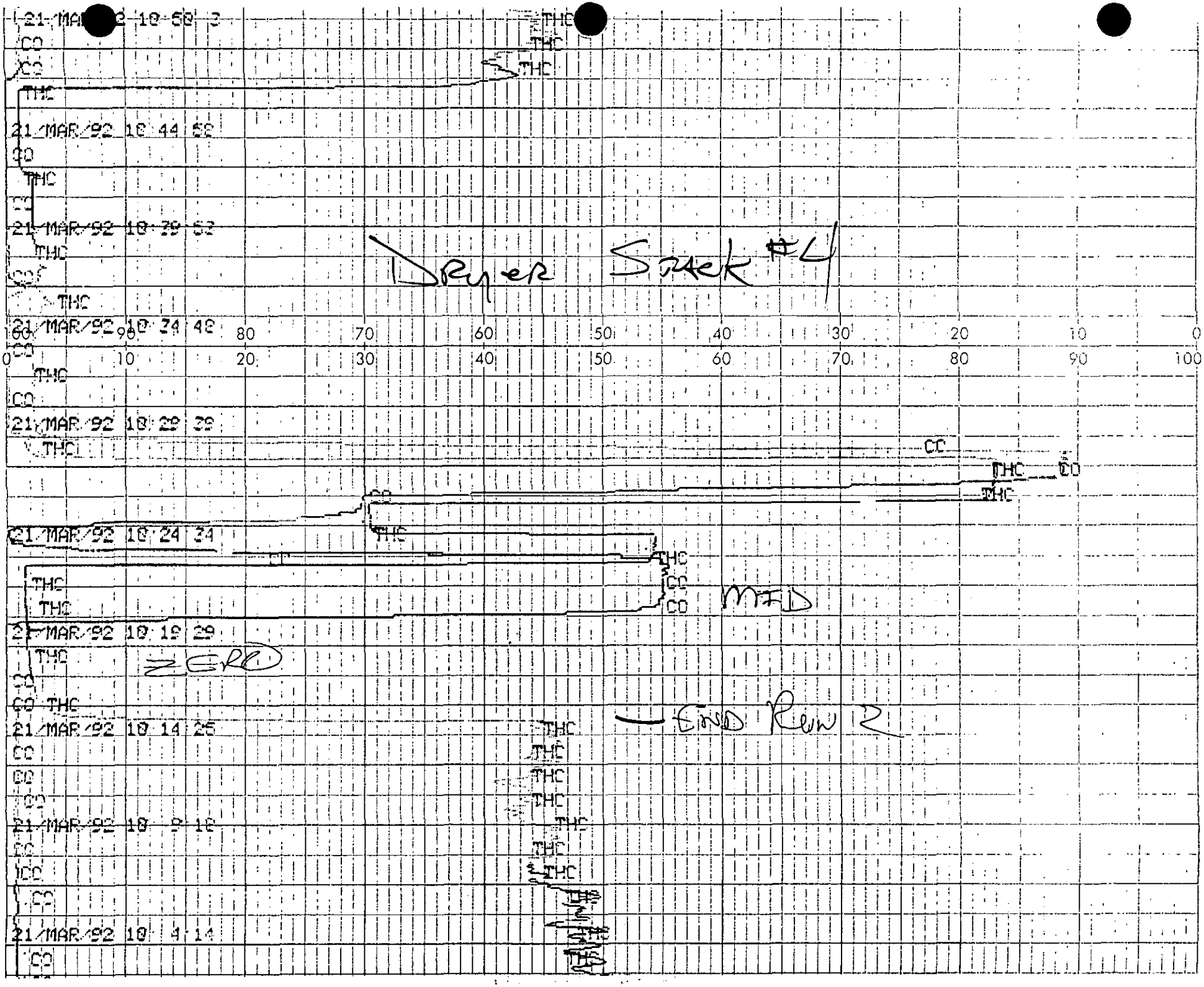
20/MAR/92 19:20:46
20/MAR/92 19:15:39
20/MAR/92 19:10:35
20/MAR/92 19:5:29
20/MAR/92 19:0:22
20/MAR/92 18:55:18
20/MAR/92 18:50:12
20/MAR/92 18:45:
100 90 70 60 50 40 30 20 10 0
0 10 30 40 50 60 70 80 90 100
RUN 3

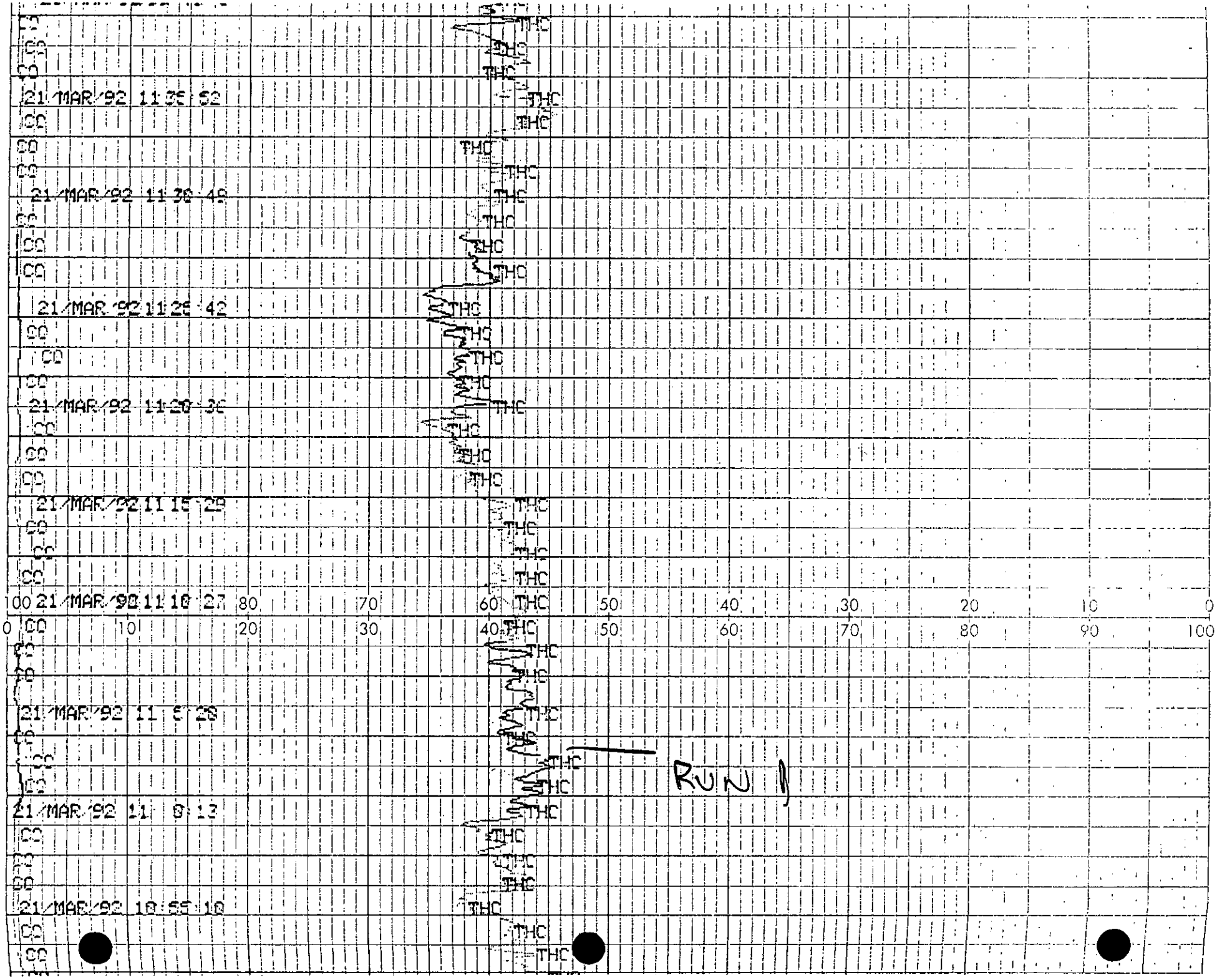

21 MAR 92 7 26 22
ZERO
INTERNAL CALIBRATION
Dryer #3
20 MAR 92 20 1 29
THC LOW
MID
20 MAR 92 19 56 27
ZERO
SYSTEM
END R
20 MAR 93 19 51 18
20 MAR 92 19 46 13
20 MAR 92 19 41 6
20 MAR 92 19 36 0
0-100 PPM RANGE
THC
Dryer 3 & 4
100
90
70
10
0
0
10
30
90
100

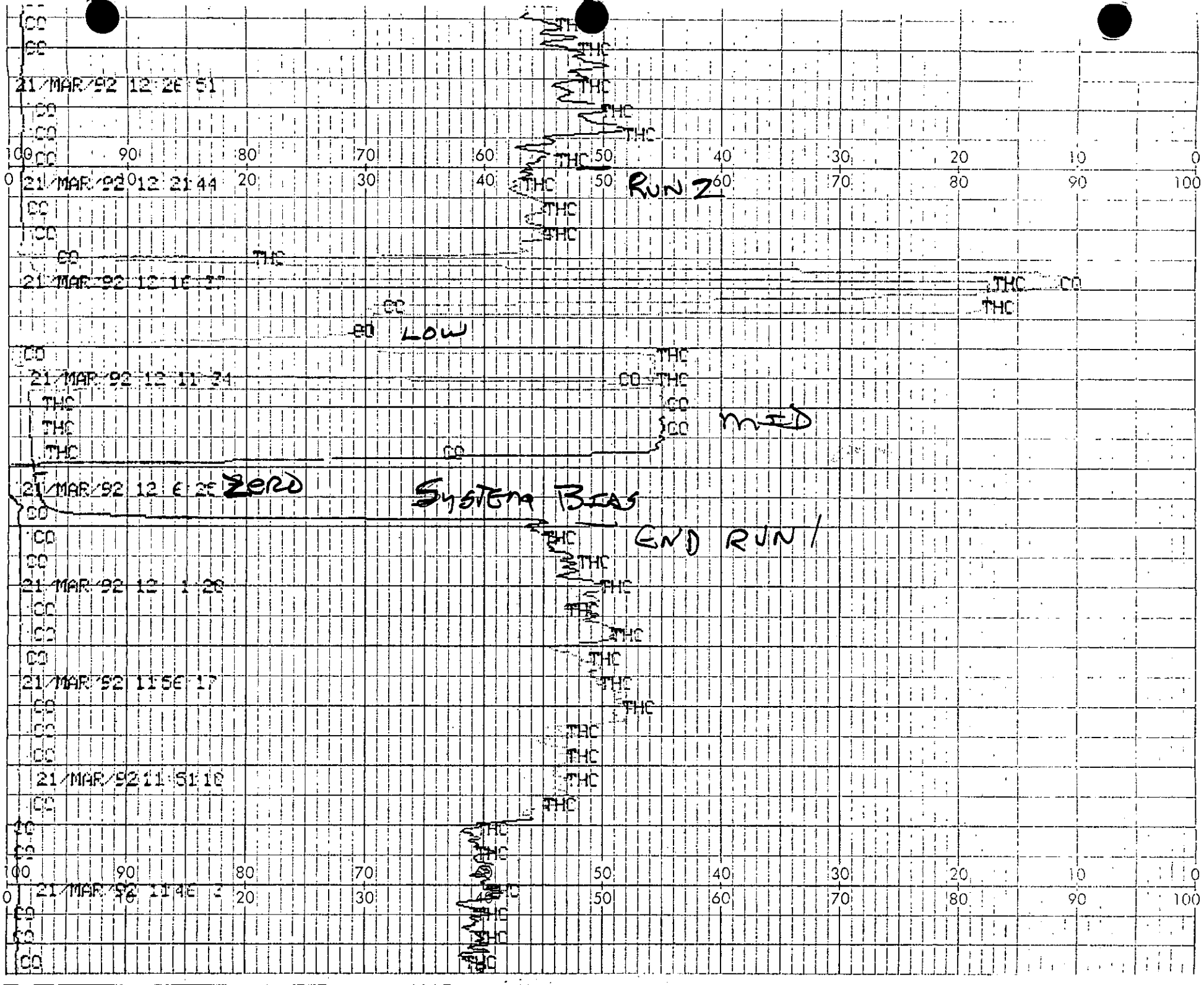

21/MAR/92 8:17:15
21/MAR/92 8:12:8
21/MAR/92 8:7:6
21/MAR/92 8:1:58
21/MAR/92 7:56:52
21/MAR/92 7:51:49
21/MAR/92 7:46:42
21/MAR/92 7:41:40
21/MAR/92 7:36:32
THC
CO
RUN 1
100 90 80 70 60 50 40 30 20 10 0

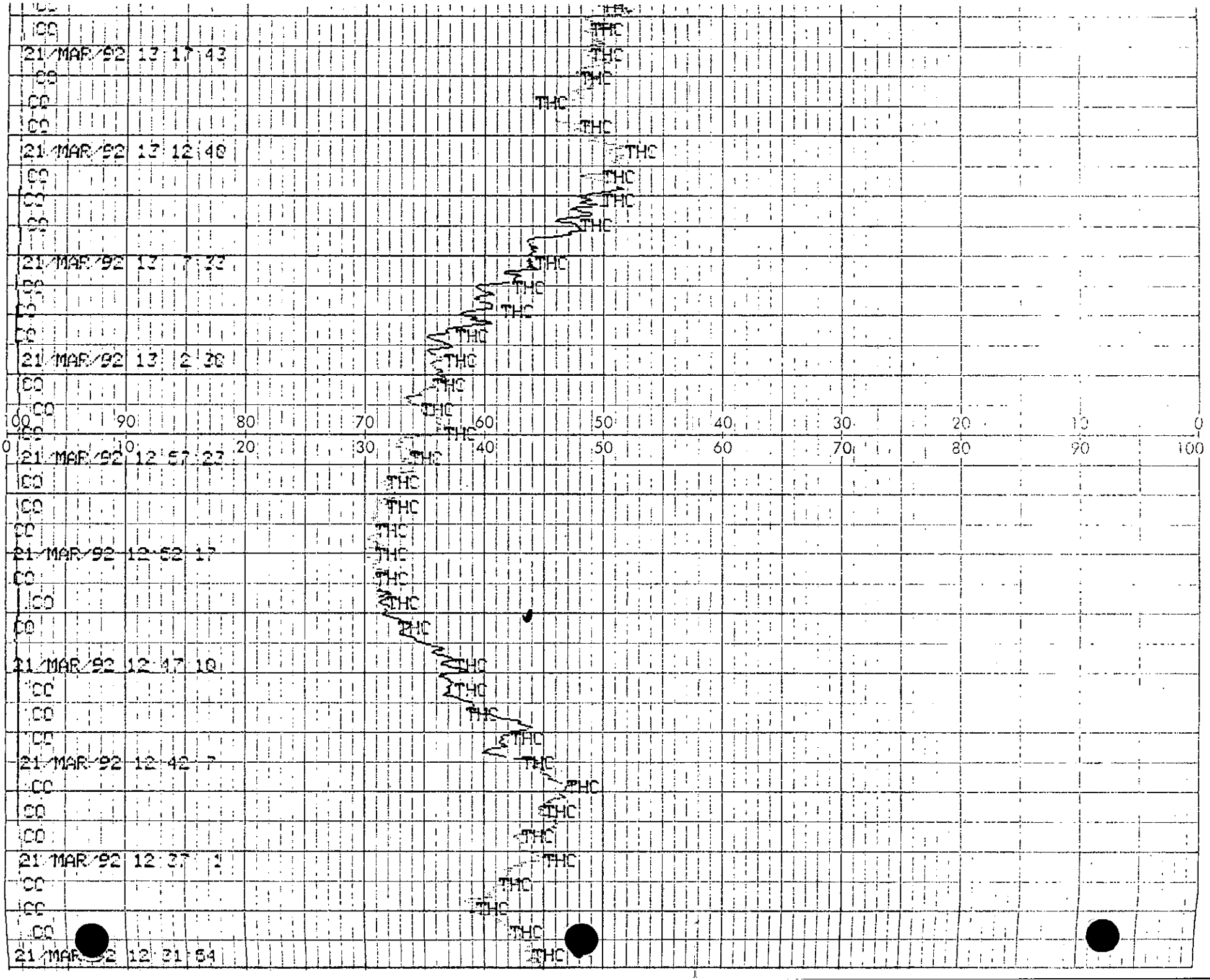

21/MAR/92 9 9 13
21/MAR/92 8 2 6
21/MAR/92 8 57 59
21/MAR/92 8 52 53
21/MAR/92 8 47 58
21/MAR/92 8 42 43
21/MAR/92 8 37 39
21/MAR/92 8 32 32
21/MAR/92 8 27 26
CO
THC
LOW
HIGH
MED
ZERO
SYSTEM BIAS
END RUN 1
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100

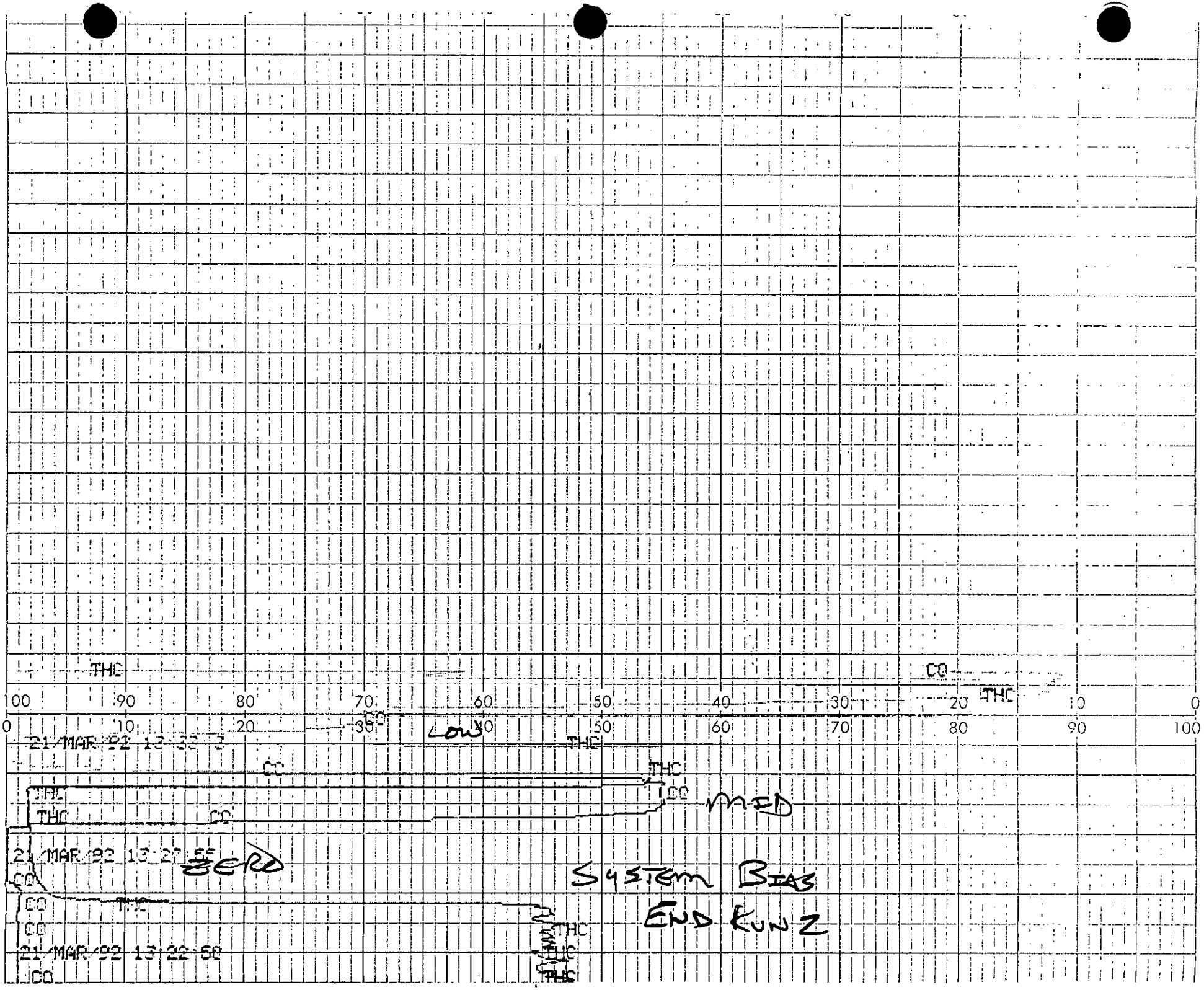

21/MAR/92 9:59:7
21/MAR/92 9:54:9
21/MAR/92 9:48:57
21/MAR/92 9:43:50
21/MAR/92 9:38:43
21/MAR/92 9:33:41
21/MAR/92 9:28:34
21/MAR/92 9:23:27
21/MAR/92 9:18:27
21/MAR/92 9:13:16
CO
THC
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
RUN 2


Dryer Stack #4
MID
ZERO
END Run 2
21/MAR/92 10:50:3
21/MAR/92 10:44:59
21/MAR/92 10:39:52
21/MAR/92 10:34:49
21/MAR/92 10:29:39
21/MAR/92 10:24:34
21/MAR/92 10:19:29
21/MAR/92 10:14:25
21/MAR/92 10:9:19
21/MAR/92 10:4:14
CO
THC
0 10 20 30 40 50 60 70 80 90 100


21 MAR 92 11 39 52
21 MAR 92 11 30 49
21 MAR 92 11 25 42
21 MAR 92 11 20 36
21 MAR 92 11 15 29
21 MAR 92 11 10 27
21 MAR 92 11 5 29
21 MAR 92 11 0 13
21 MAR 92 10 55 10
THC
RUN 1
100 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100


21/MAR/92 12 26 51
21/MAR/92 12 21 44
RUN 2
21/MAR/92 12 16 37
LOW
21/MAR/92 12 11 31
MID
21/MAR/92 12 6 25
ZERO
System Bias
END RUN 1
21/MAR/92 12 1 20
21/MAR/92 11 56 17
21/MAR/92 11 51 10
21/MAR/92 11 46 3
CO
THC


21 MAR 92 13 17 43
21 MAR 92 13 12 40
21 MAR 92 13 7 22
21 MAR 92 13 2 38
21 MAR 92 12 57 23
21 MAR 92 12 52 17
21 MAR 92 12 47 10
21 MAR 92 12 42 7
21 MAR 92 12 37 1
21 MAR 92 12 31 54
CO
THC
0 10 20 30 40 50 60 70 80 90 100
100 90 80 70 60 50 40 30 20 10 0


THC
CO
100 90 80 70 60 50 40 30 20 10 0
0 10 20 30 40 50 60 70 80 90 100
21 MAR 92 13 32 7
LOW
MID
ZERO
SYSTEM BIAS
END RUN 2
21 MAR 92 13 27 55
21 MAR 92 13 22 50

APPENDIX G

LABORATORY DATA AND CHAIN-OF-CUSTODY DOCUMENTATION

MERCURY RESEARCH LABORATORY, INC.

April 6, 1992

Mr. Jeff Burdett
Industrial & Environmental Analysis
P. O. Box 12846
Research Triangle Park
North Carolina 27709

RE: LOUISIANA PACIFIC, CLAYTON, AL
Your PO # 0050FS
Our Project No. 92-03-24

Dear Mr. Burdett:

On March 25, 1992, we received from your company, Fifty-four samples, related to the reference project. You requested that we determine the total amount of formaldehyde in these samples using high performance liquid chromatography (HPLC), and report our results to you.

The sample solutions were extracted three times separately with methylene chloride using a separatory funnel. The extracts for each sample were combined and evaporated to dryness under a vacuum system. Solid residues in the samples were reconstituted into acetonitrile. The final volumes of the acetonitrile for each sample were adjusted, and are listed in the attached Table 1.

A HPLC equipped with a UV detector set at 360 nm wavelength was used for the sample analysis. The analytical results, and the calibration curves are also summarized in the attached Table 1.

It is noted here that the concentration of formaldehyde in several samples were very high. Especially in the sample #28, all DNPH was consumed. The collection efficiency of the DNPH solution would decrease with the decreasing concentration of the reagent. When the total amount of formaldehyde exceeds 30 mg, it is recommended to have a third impinger, or 200 mL of DNPH solution should be added to each impinger.

Shouuld there be any questions concerning this report please do not hesitate to contact us at your convenience.

Respectfully submitted,
MERCURY RESEARCH LAB INC
1150-1 EXECUTIVE CIRCLE
PO BOX 996
CARY NC 27511
Mercury Research Laboratory, Inc.

April 6, 1992

LOUISIANA PACIFIC, CLAYTON, AL
Your PO No. 0050FS
Our Porject No. 92-03-24

Table 1. FORMALDEHYDE , TOTAL MG IN SAMPLE

Sample #	Counts	ppm as Hydrazone	Final Volumne	total mg Hydrazone	total mg Formaldehyde
#1 (PV3-RUN 1)	1,017 1,016	16.7	4,000 mL	66.8	9.6
#2 (PV3-RUN 2)	683 683	11.2	4,000 mL	44.8	6.4
#3 (PV3-RUN 3)	431 428	7.0	4,000 mL	28.0	4.0
#4 (PV4-RUN 1)	405 404	6.6	10,000 mL	66.0	9.4
#5 (PV4-RUN 2)	727 728	11.9	10,000 mL	119	17
#6 (PV4-RUN 3)	673 674	11.0	10,000 mL	110	16
#7 (PV5-RUN 1)	1,827 1,823	29.9	10,000 mL	299	43
#8 (PV5-RUN 2)	1,634 1,636	26.8	10,000 mL	268	38
#9. (PV5-RUN 3)	1,779 1,781	29.2	10,000 mL	292	42
#10 (Blank3/12)	42 42	0.7	2,000 mL	1	0.1
#11 (PV6-RUN 1)	1,708 1,710	28.0	10,000 mL	280	40
#12 (PV6-RUN 2)	1,306 1,304	21.4	10,000 mL	210	30
#13 (PV6-RUN 3)	812 813	13.3	10,000 mL	130	19

April 6, 1992

LOUISIANA PACIFIC. CLAYTON, AL
Your P.O. No. 0050FS
Our Porject No. 92-03-24

Table FORMALDEHYDE , TOTAL MG IN SAMPLE

Sample #	Counts	ppm as Hydrazone	Final Volumne	total mg Hydrazone	total mg Formaldehyde
#14	843	13.8	10,000 mL	138	20
(PV7-RUN1)	846				
#15	1,113	18.3	10,000 mL	183	26
(PV7-RUN2)	1,116				
#16	1,265	20.7	10,000 mL	207	30
(PV7-RUN3)	1,262				
#17	632	10.3	10,000 mL	103	15
(PV8-RUN 1)	630				
#18	670	11.0	10,000 mL	110	16
(PV8-RUN 2)	669				
#19	892	14.6	10,000 mL	146	21
(PV8-RUN 3)	889				
#20	16	0.26	2,000 mL	0.52	0.07
(Bk-3/13)	16				
#21	34	0.56	1,000 mL	0.56	0.08
(Bk-3/16)	35				
#22	608	10.0	10,000 mL	100	14
(PV9-RUN 1)	608				
#23	691	11.3	10,000 mL	113	16
(PV9-RUN 2)	693				
#24	745	12.2	10,000 mL	122	17
(PV9-RUN 3)	745				
#25	552	9.0	10,000 mL	90	13
(PV10-RUN 1)	552				
#26	638	10.5	10,000 mL	105	15
(PV10-RUN 2)	638				
#27	527	8.6	10,000 mL	86	12
(PV10-RUN 3)	527				

April 6, 1992

LOUISIANA PACIFIC, CLAYTON, AL
Your P. O. No. 0050FS
Our Porject No. 92-03-24

Table 1. FORMALDEHYDE , TOTAL MG IN SAMPLE

Sample #	Counts	ppm as Hydrazone	Final Volumne	total mg Hydrazone	total mg Formaldehyde
#28	3,198	52.4	10,000 mL	524	75
(PV11-RUN1)	3,200				
#29	2,448	40.1	10,000 mL	401	57
(PV11-RUN2)	2,448				
#30	2,336	38.3	10,000 mL	383	55
(PV11-RUN3)	2,338				
#31	N.D.		4,000 mL		N.D.*
(Bk 3/19)	N.D.				
#32	1,527	25.1	10,000 mL	251	36
(DS1-RUN 1)	1,533				
#33	1,424	23.3	10,000 mL	233	33
(DS1-RUN 2A)	1,422				
#34	N.D.		1,000 mL		N.D.*
(DS1-RUN 2B)	N.D.				
#35	1,270	20.8	10,000 mL	208	30
(DS1 RUN 3A)	1,273				
#36	67	1.1	1,000 mL	1.1	0.15
(DS1-RUN 3B)	67				
#37	1,703	28.0	10,000 mL	280	40
(DS2-RUN 1)	1,709				
#38	1,492	24.5	10,000 mL	245	35
(DS2-RUN 2)	1,494				
#39	1,057	17.4	10,000 mL	174	25
(DS2-RUN 3)	1,060				
#40	1,373	22.5	10,000 mL	225	32
(DS3-RUN 1)	1,373				
#41	1,411	23.1	10,000 mL	231	33
(DS3-RUN 2)	1,413				

April 6, 1992

LOUISIANA PACIFIC, CLAYTON, AL
Your P.O. No. 0050FS
Our Porject No. 92-03-24

Table 1. FORMALDEHYDE , TOTAL MG IN SAMPLE

Sample #	Counts	ppm as Hydrazone	Final Volumne	total mg Hydrazone	total mg Formaldehyde
#42 (DS4-RUN1)	1,602 1,602	26.3	10,000 mL	263	38
#43 (DS4-RUN2)	1,486 1,487	24.4	10,000 mL	244	35
#44 (Bk 3/20)	N.D. N.D.		1,000 mL		N.D.
#45 (Bk 3/21)	N.D. N.D.		4,000 mL		N.D.*
#46 (DS6-RUN 1)	426 425	7.0	20,000 mL	140	20
#47 (DS6-RUN 2)	447 447	7.3	20,000 mL	146	21
#48 (DS6-RUN 3)	468 466	7.6	20,000 mL	152	22
#49 (DS8 RUN 1)	506 513	8.3	20,000 mL	166	24
#50 (DS8-RUN 2)	461 469	7.6	20,000 mL	152	22
#51 (DS8-RUN 3)	789 789	12.9	20,000 mL	258	37
#52 (Bk 3/15)	1,274 1,274	20.9	2,000 mL	42	6
#53 (Bk 3/17)	20 21	0.3	5,000 mL	1.5	0.2
#54 (Bk 3/14)	109 110	1.8	5,000 mL	3.6	0.5

Standard Curves

		Pre-Sample Run		During Sample Run		Post-Sample Run	
5.0	ppm	303,	306,	295,	296,	300,	299.
10.0	ppm	604,	609,	602,	604,	605,	606
20.0	ppm	1,204,	1,206,	1,186,	1,197,	1,203,	1,200
50.0	ppm	3,064,	3,063,	3,047,	3,048	3,049,	3,040
100.0	ppm	6,475,	6,354,	6,327,	6,336	6,349,	6,348

Sample Calculation

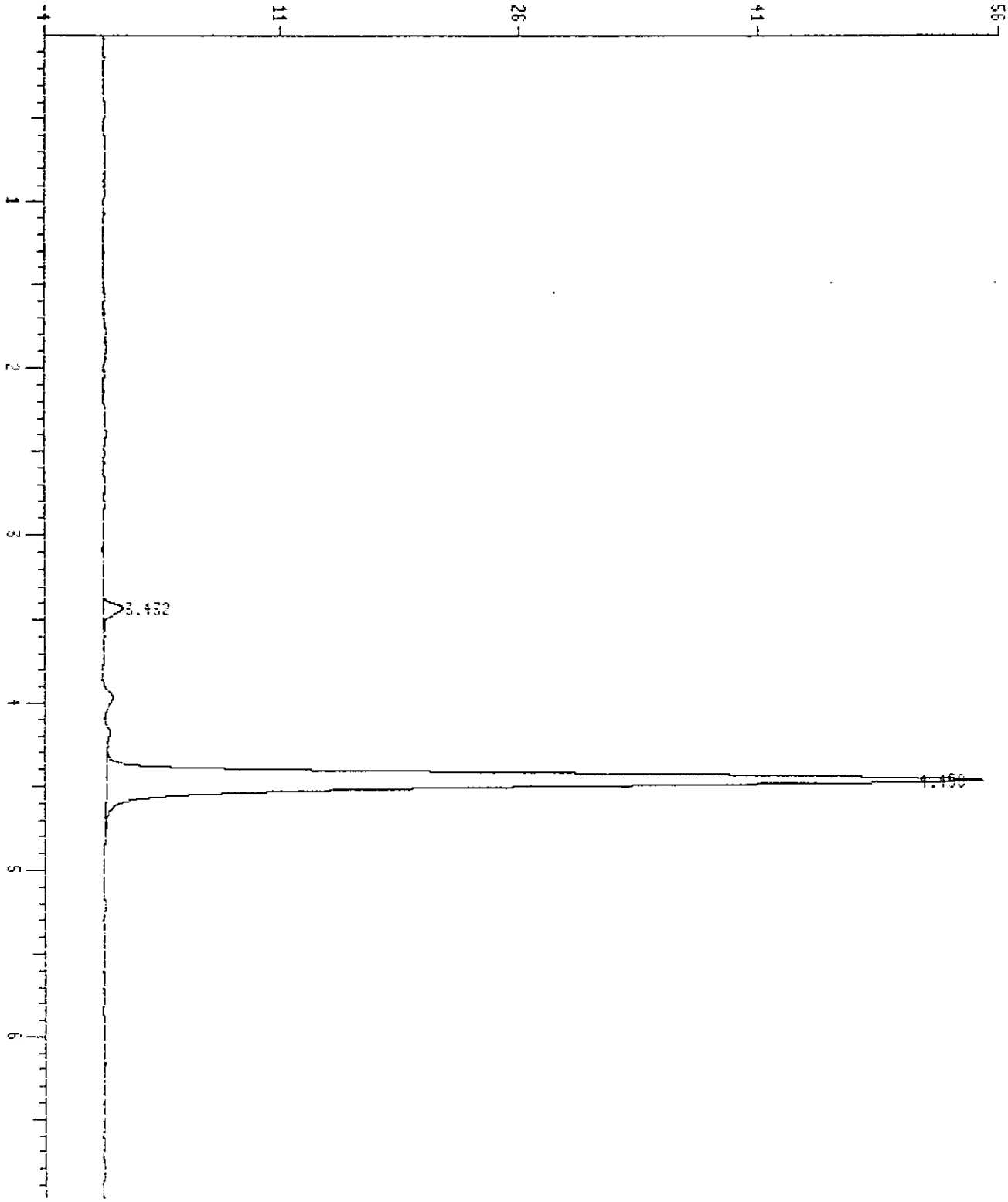
ppm of formaldehyde as hydrazone x final volume x .143/1000

= Total number of mg of formaldehyde in sample

Sample #1

16.7 ug/mL as hydrazone x 4000 mL x .143 (wt.% of formaldehyde in formaldehyde hydrazone) x 1 mg/1000 ug = 9.6 mg

1: LC A 360,4 550,100 of 0401A00A.D



N

*** Area Percent ***

Report by Signal

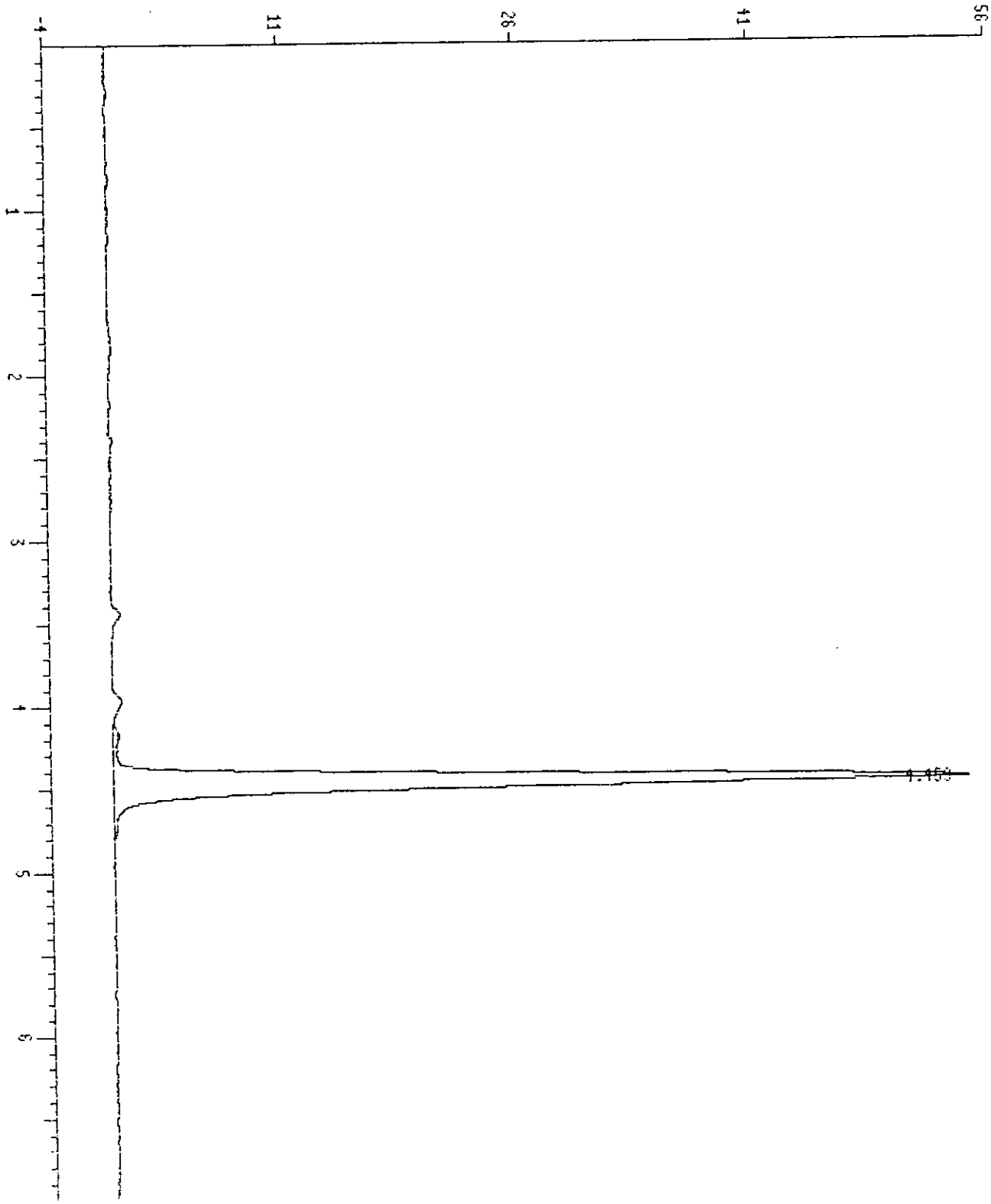
Operator: JCP 1 Apr 92 1:53 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 5 PPM
Misc Info:
Integration File Name : DATA:0401A00A.I
consisting of channels : 1. A 360,4 550,100 of 0401A00A.D
Sequence Index: 1 Bottle Number : 0 Repetition Number: 1

A 360,4 550,100 of 0401A00A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.432	BB	5.9937	1.2748	1.90	100.00	0.070	0.74
4.458	BB	302.99	55.2147	98.10	100.00	0.085	0.81

3

1: LC A 360,4 550,100 of 0401A009.D



4

*** Area Percent ***

Report by Signal

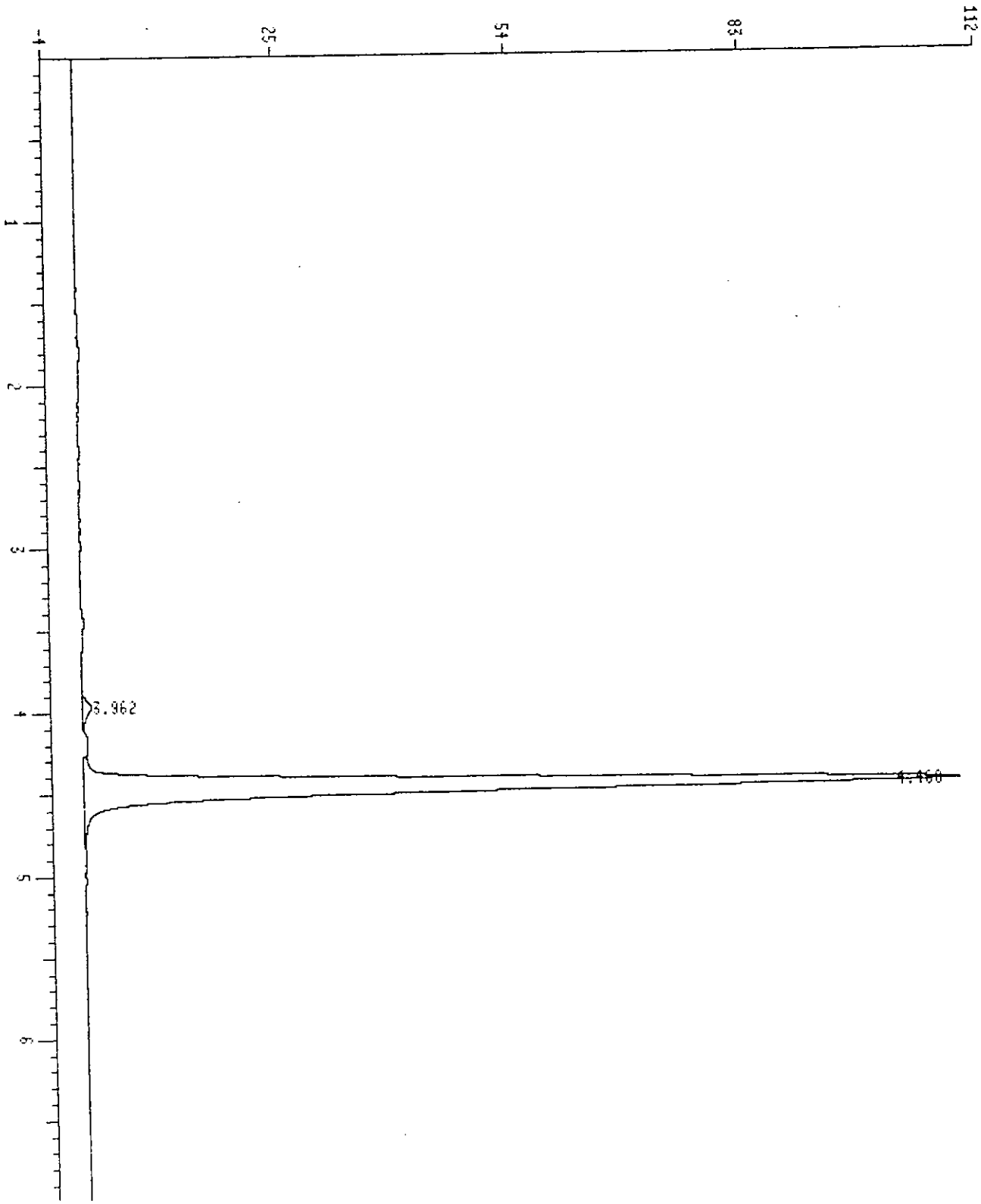
Operator: JCP 1 Apr 92 2:03 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 5 PPM
Misc Info:
Integration File Name : DATA:0401A00B.I
consisting of channels : 1. A 360,4 550,100 of 0401A00B.D
Sequence Index: 1 Bottle Number : 0 Repetition Number: 2

A 360,4 550,100 of 0401A00B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.459	VB	305.73	54.6020	100.00	100.00	0.086	0.83

5

1: LC A 360,4 550,100 of 0401A01A.D



*** Area Percent ***

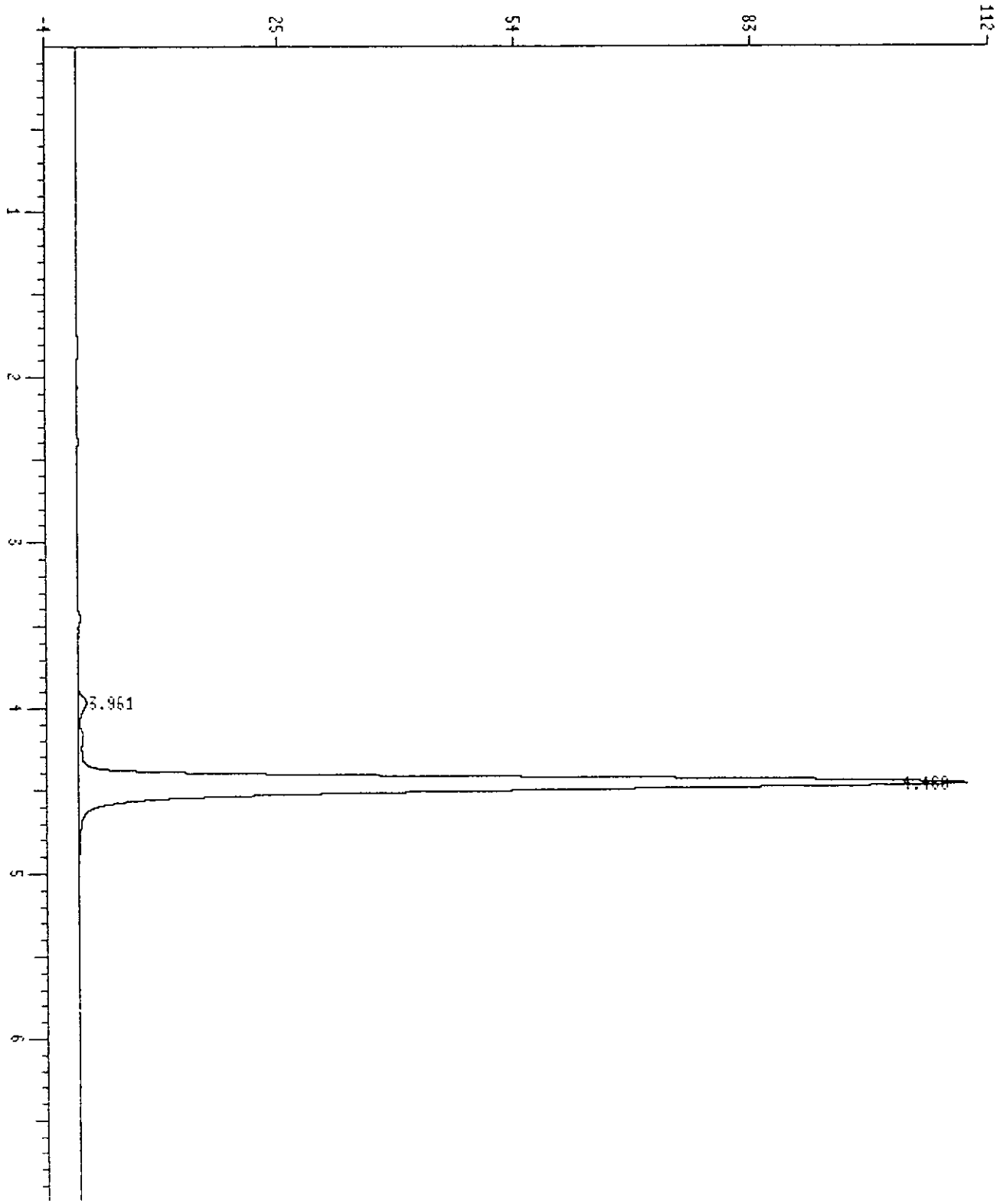
Report by Signal

Operator: JCP 1 Apr 92 2:13 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 10 PPM
Misc Info:
Integration File Name : DATA:0401A01A.I
consisting of channels : 1. A 360,4 550,100 of 0401A01A.D
Sequence Index: 1 Bottle Number : 1 Repetition Number: 1

A 360,4 550,100 of 0401A01A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.962	BV	7.8729	1.1389	1.29	100.00	0.103	0.69
4.460	VB	604.10	109.01	98.71	100.00	0.086	0.82

1: LC A 360,4 550,100 of 0401A01B.D



*** Area Percent ***

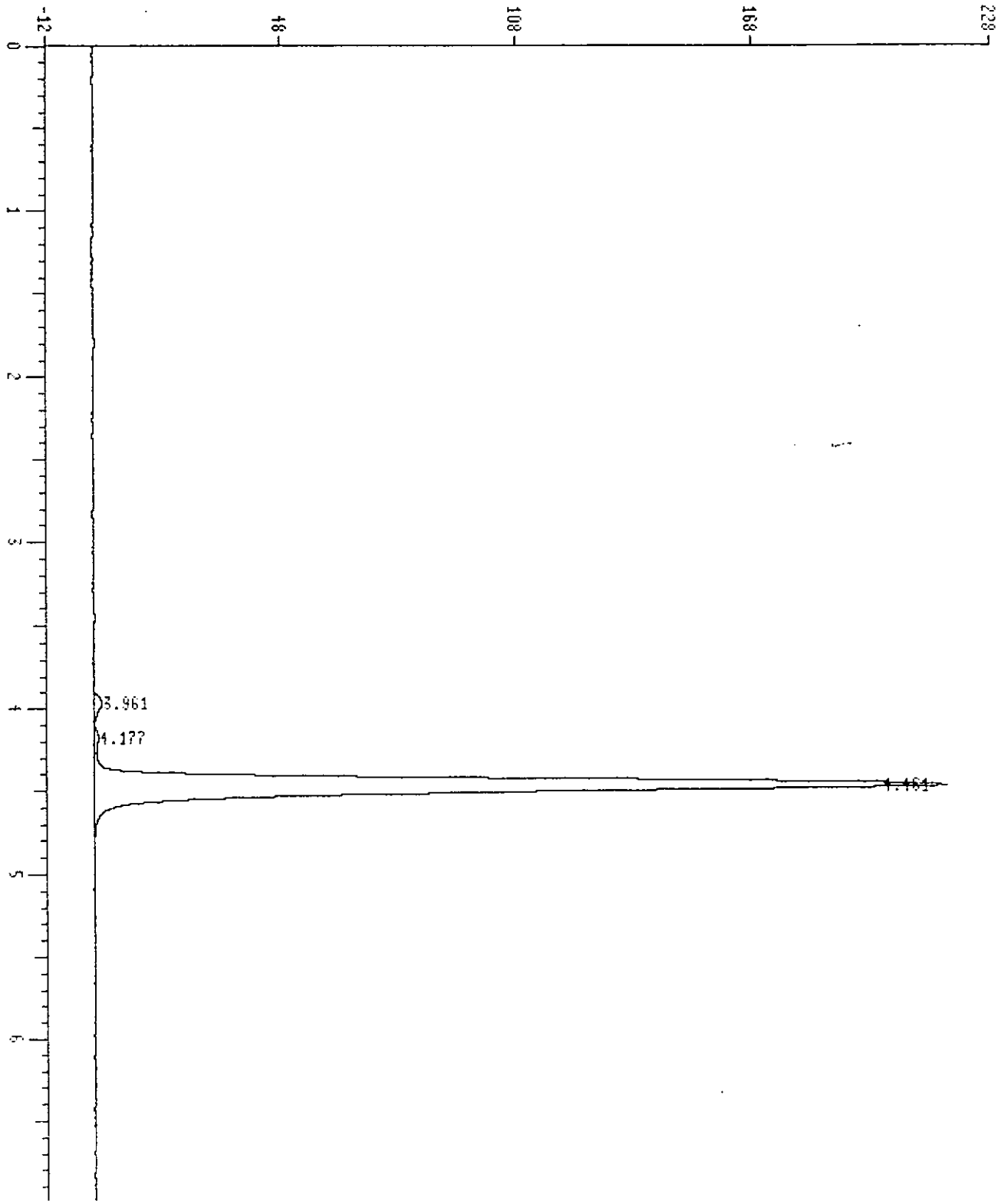
Report by Signal

Operator: JCP 1 Apr 92 2:22 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 10 PPM
Misc Info:
Integration File Name : DATA:0401A01B.I
consisting of channels : 1. A 360,4 550,100 of 0401A01B.D
Sequence Index: 1 Bottle Number : 1 Repetition Number: 2

A 360,4 550,100 of 0401A01B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.961	BV	7.5839	1.1204	1.23	100.00	0.102	0.72
4.460	VB	609.42	108.99	98.77	100.00	0.086	0.83

1: LC A 360,4 550,100 of 0401A02A.D



10

*** Area Percent ***

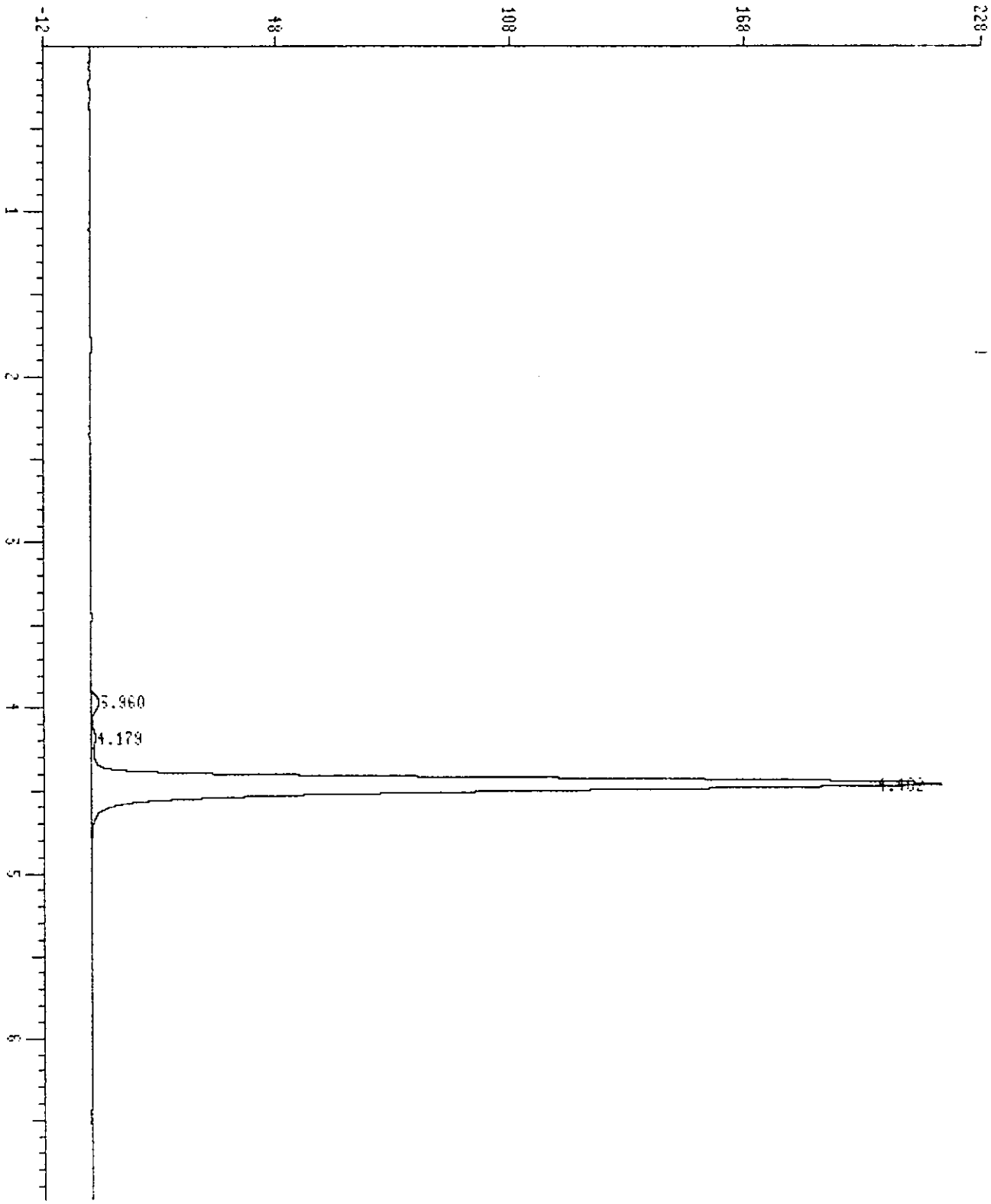
Report by Signal

Operator: JCP 1 Apr 92 2:32 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 20 PPM
Misc Info:
Integration File Name : DATA:0401A02A.I
consisting of channels : 1. A 360,4 550,100 of 0401A02A.D
Sequence Index: 1 Bottle Number : 2 Repetition Number: 1

A 360,4 550,100 of 0401A02A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.961	BV	15.2138	2.2442	1.24	100.00	0.101	0.67
4.177	VV	9.6593	1.2316	0.79	100.00	0.120	0.71
4.461	VB	1204.99	217.60	97.98	100.00	0.085	0.81

1: LC A 360,4 550,100 of 0401A02B.D



*** Area Percent ***

Report by Signal

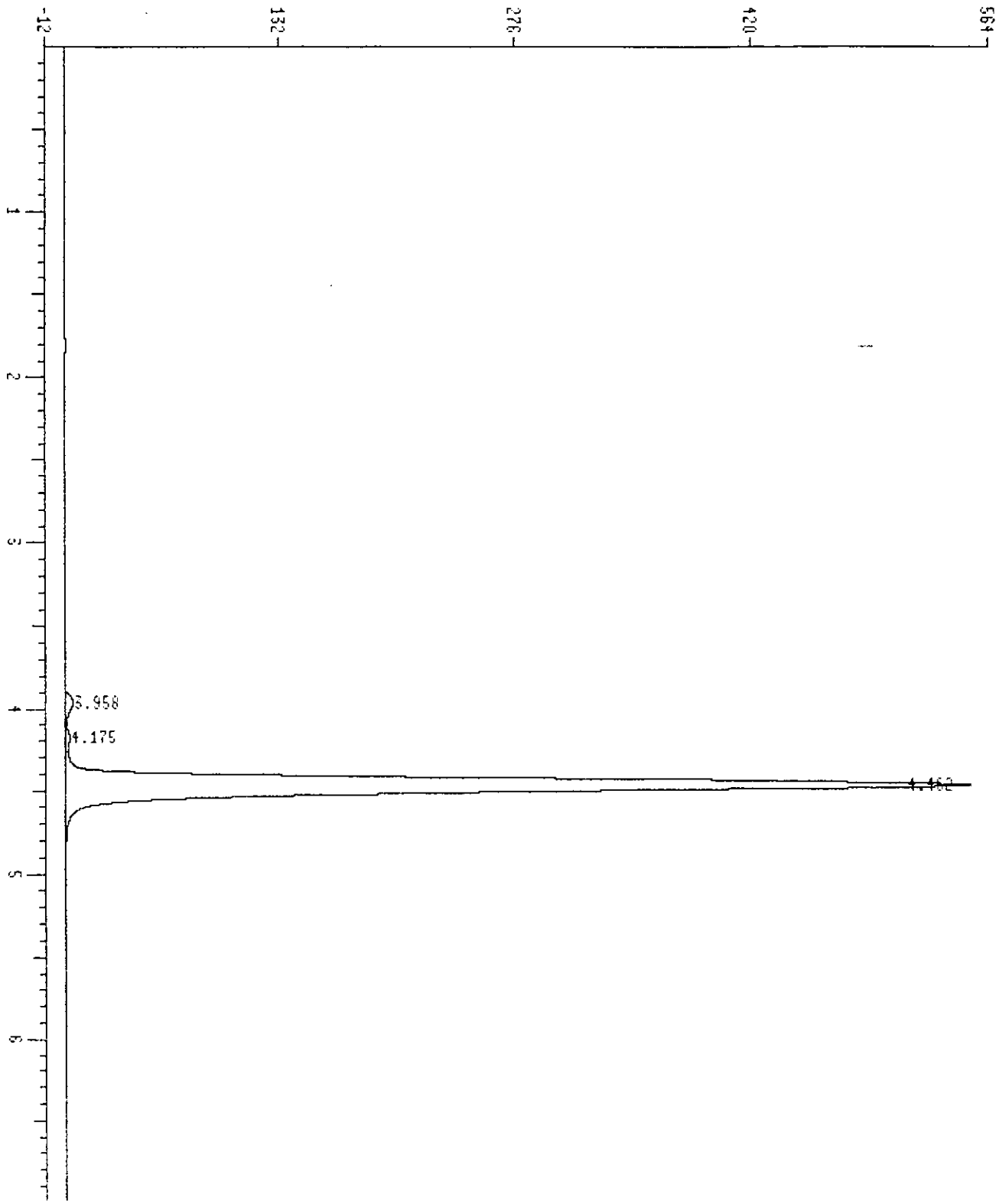
Operator: JCP 1 Apr 92 2:42 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 20 PPM
Misc Info:
Integration File Name : DATA:0401A02B.I
consisting of channels : 1. A 360,4 550,100 of 0401A02B.D
Sequence Index: 1 Bottle Number : 2 Repetition Number: 2

A 360,4 550,100 of 0401A02B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.960	BV	15.5088	2.2670	1.26	100.00	0.105	0.64
4.179	VV	9.1170	1.3270	0.74	100.00	0.102	0.94
4.462	VB	1205.70	217.37	98.00	100.00	0.085	0.82

13

1: LC A 360,4 550,100 of 0401A03A.D



14

*** Area Percent ***

Report by Signal

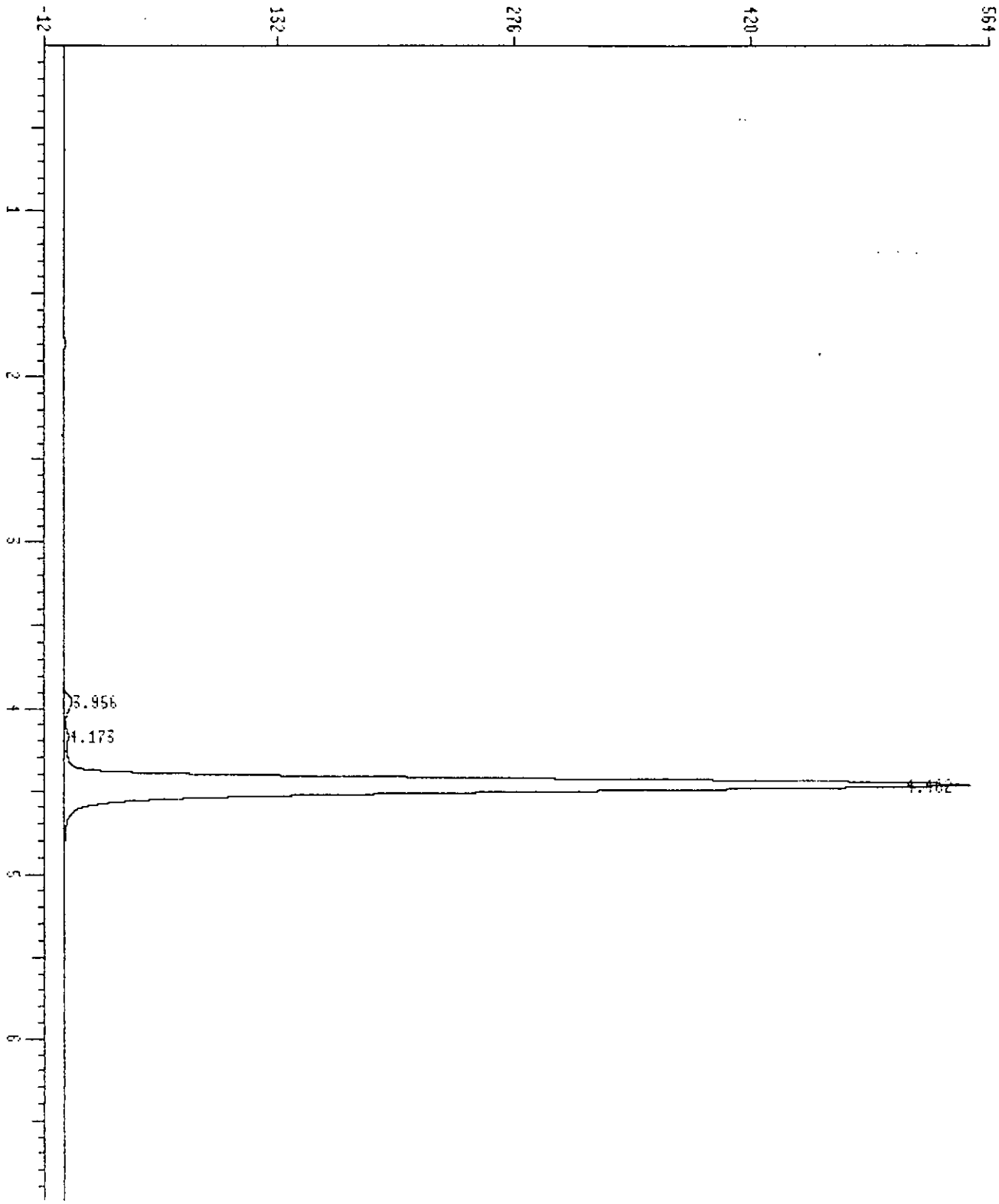
Operator: JCP 1 Apr 92 2:51 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 50 PPM
Misc Info:
Integration File Name : DATA:0401A03A.I
consisting of channels : 1. A 360,4 550,100 of 0401A03A.D
Sequence Index: 1 Bottle Number : 3 Repetition Number: 1

A 360,4 550,100 of 0401A03A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.958	BV	36.1707	5.2754	1.16	100.00	0.103	0.63
4.175	VV	23.5701	2.9559	0.75	100.00	0.116	0.73
4.462	VB	3064.06	553.03	98.09	100.00	0.085	0.81

15

1: LC A 360,4 550,100 of 0401A03B.D



*** Area Percent ***

Report by Signal

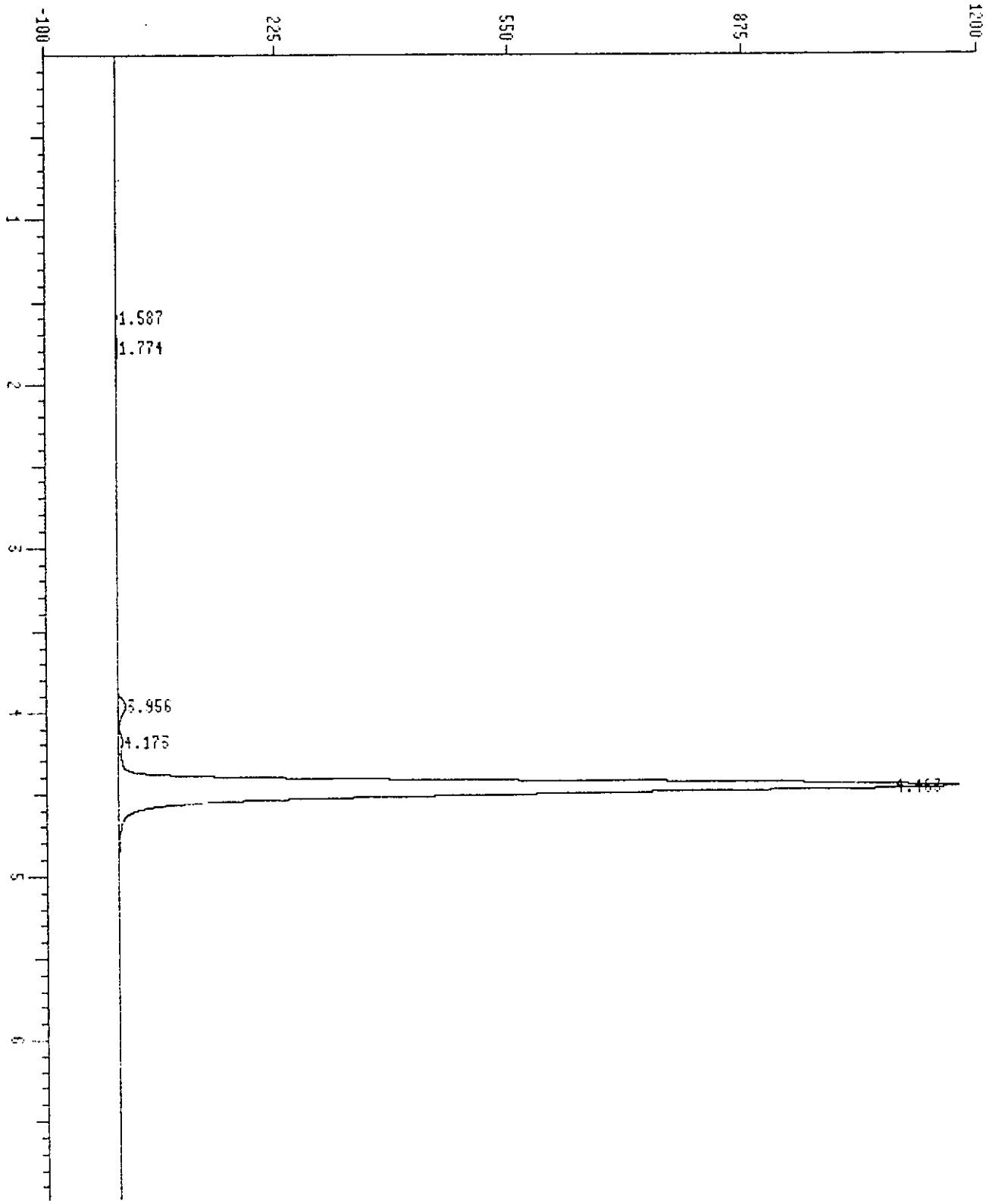
Operator: JCP 1 Apr 92 3:01 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 50 PPM
Misc Info:
Integration File Name : DATA:0401A03B.I
consisting of channels : 1. A 360,4 550,100 of 0401A03B.D
Sequence Index: 1 Bottle Number : 3 Repetition Number: 2

A 360,4 550,100 of 0401A03B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.956	BV	36.3299	5.3024	1.16	100.00	0.102	0.64
4.173	VV	22.5661	2.8870	0.72	100.00	0.112	0.75
4.462	VB	3063.82	552.77	98.11	100.00	0.085	0.81

14

1: LC A 360,4 550,100 of 0401A04A.D



*** Area Percent ***

Report by Signal

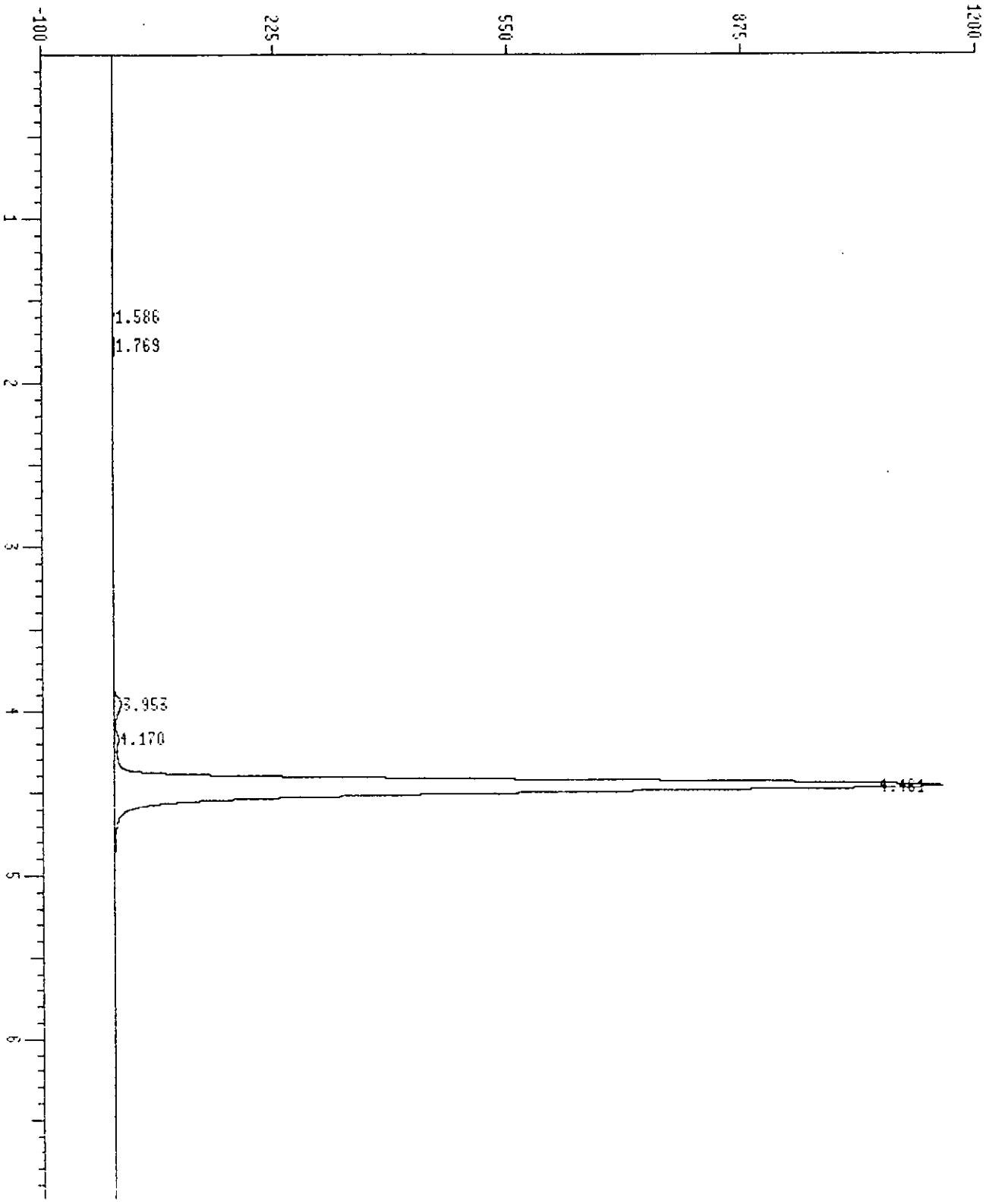
Operator: JCP 1 Apr 92 3:11 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 100 PPM
Misc Info:
Integration File Name : DATA:0401A04A.I
consisting of channels : 1. A 360,4 550,100 of 0401A04A.D
Sequence Index: 1 Bottle Number : 4 Repetition Number: 1

A 360,4 550,100 of 0401A04A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.587	BV	5.4638	1.1556	0.08	100.00	0.079	0.56
1.774	VB	15.4302	1.7221	0.23	100.00	0.129	1.05
3.956	BV	76.3053	11.1933	1.15	100.00	0.102	0.62
4.173	VV	46.1025	6.0390	0.70	100.00	0.110	0.81
4.463	VB	6475.69	1173.56	97.83	100.00	0.085	0.81

19

1: LC A 360,4 550,100 of 0401A04B.D



*** Area Percent ***

Report by Signal

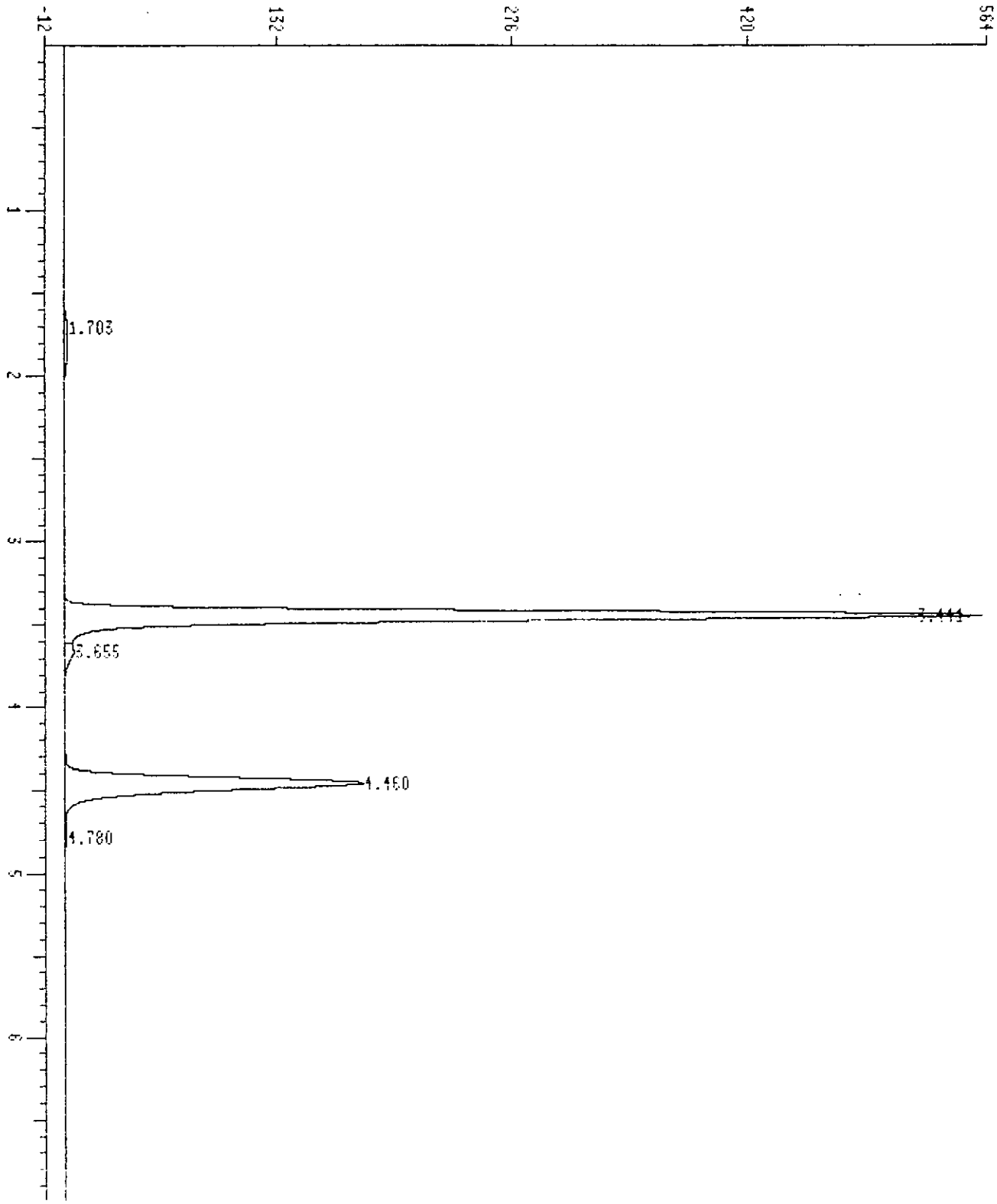
Operator: JCP 1 Apr 92 3:20 pm
Method File Name : DNPHIII.M
Sample Info : STANDARD; 100 PPM
Misc Info:
Integration File Name : DATA:0401A04B.I
consisting of channels : 1. A 360,4 550,100 of 0401A04B.D
Sequence Index: 1 Bottle Number : 4 Repetition Number: 2

A 360,4 550,100 of 0401A04B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.586	BV	5.8914	1.1233	0.09	100.00	0.087	0.51
1.769	VB	14.4444	1.6775	0.22	100.00	0.130	0.89
3.953	BV	74.9359	10.8665	1.15	100.00	0.103	0.62
4.170	VV	44.3150	5.9759	0.68	100.00	0.108	0.86
4.461	VB	6353.81	1151.90	97.85	100.00	0.085	0.81

82

1: LC A 360,4 550,100 of 0401A05A.D



*** Area Percent ***

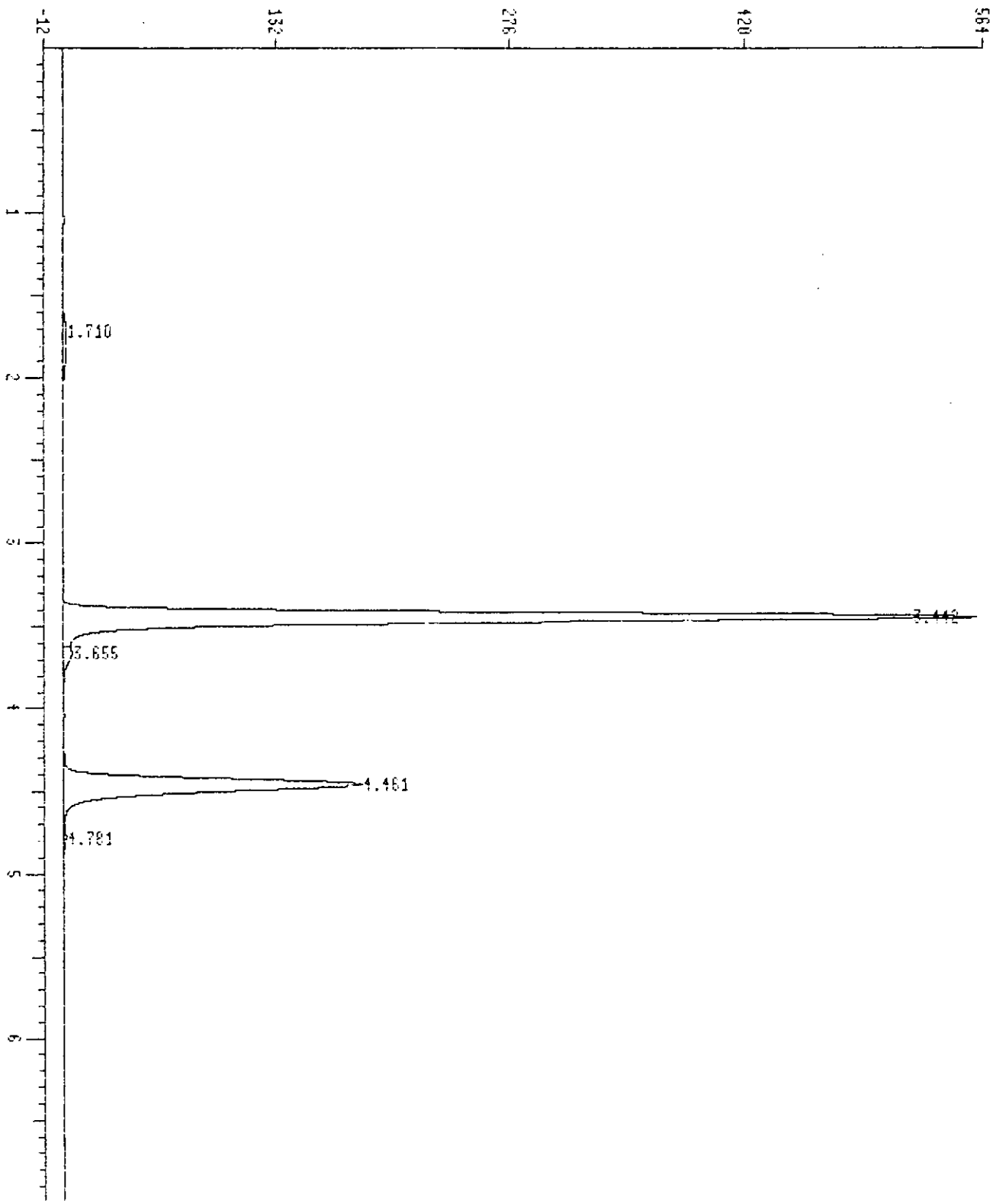
Report by Signal

Operator: JCP 1 Apr 92 3:30 pm
Method File Name : DNPHIII.M
Sample Info : #1
Misc Info:
Integration File Name : DATA:0401A05A.I
consisting of channels : 1. A 360,4 550,100 of 0401A05A.D
Sequence Index: 1 Bottle Number : 5 Repetition Number: 1

A 360,4 550,100 of 0401A05A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.703	BB	40.6853	2.1805	1.19	100.00	0.265	0.36
3.441	BV	2313.04	562.42	67.68	100.00	0.064	0.84
3.655	VB	35.9497	5.2266	1.05	100.00	0.103	0.56
4.460	BV	1018.65	183.76	29.75	100.00	0.085	0.81
4.780	VB	11.1509	1.5258	0.33	100.00	0.112	0.98

1: LC A 360,4 550,100 of 0401A05B.D



*** Area Percent ***

Report by Signal

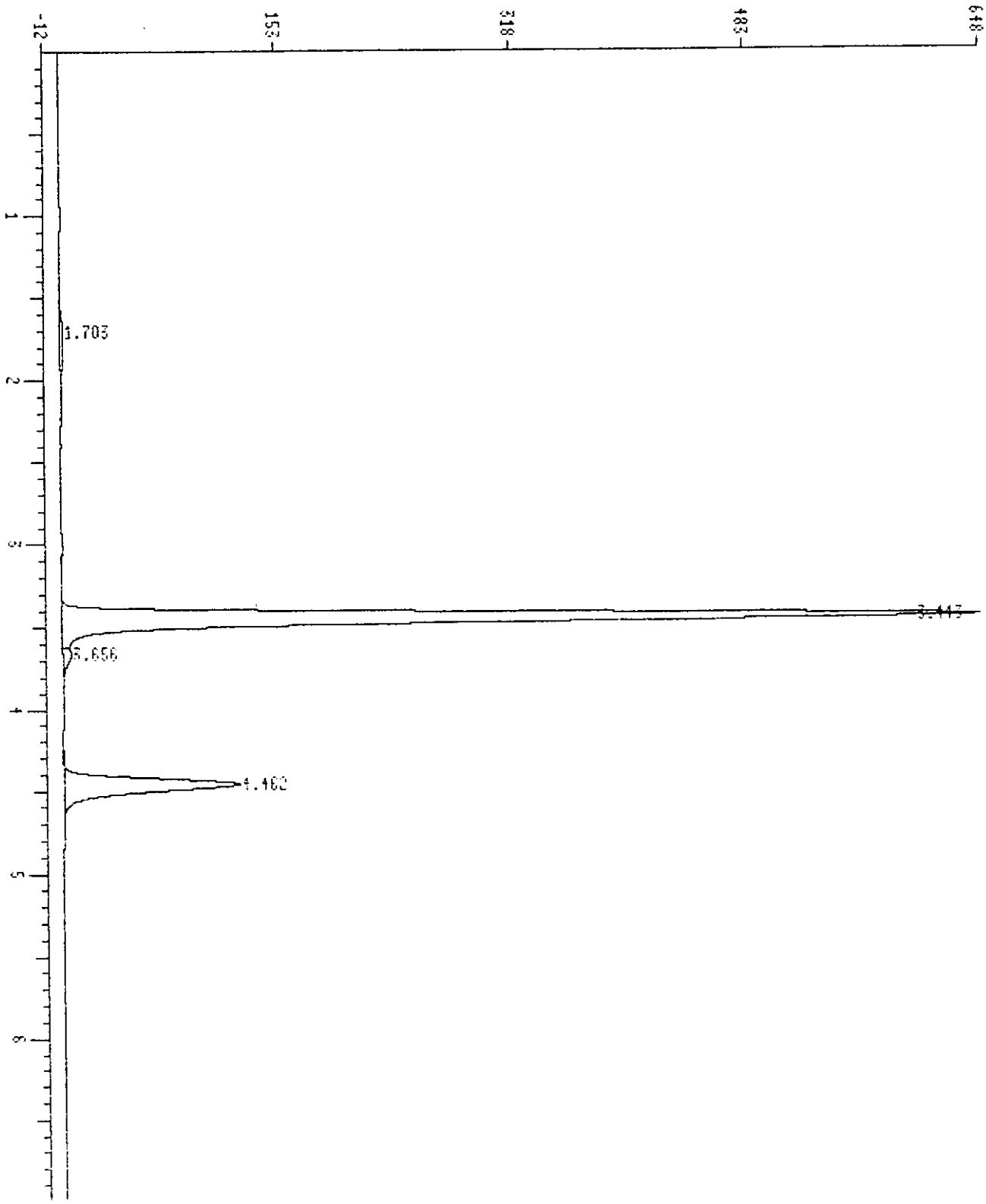
Operator: JCP 1 Apr 92 3:40 pm
Method File Name : DNPHIII.M
Sample Info : #1
Misc Info:
Integration File Name : DATA:0401A05B.I
consisting of channels : 1. A 360,4 550,100 of 0401A05B.D
Sequence Index: 1 Bottle Number : 5 Repetition Number: 2

A 360,4 550,100 of 0401A05B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.710	BB	35.0542	1.9847	1.02	100.00	0.255	0.41
3.442	BV	2323.12	563.34	67.91	100.00	0.064	0.83
3.655	VB	35.0851	5.1426	1.03	100.00	0.103	0.50
4.461	BV	1016.39	183.77	29.71	100.00	0.085	0.81
4.781	VB	11.2044	1.5505	0.33	100.00	0.108	0.97

52

1: LC A 360,4 550,100 of 0401A06A.D



26

*** Area Percent ***

Report by Signal

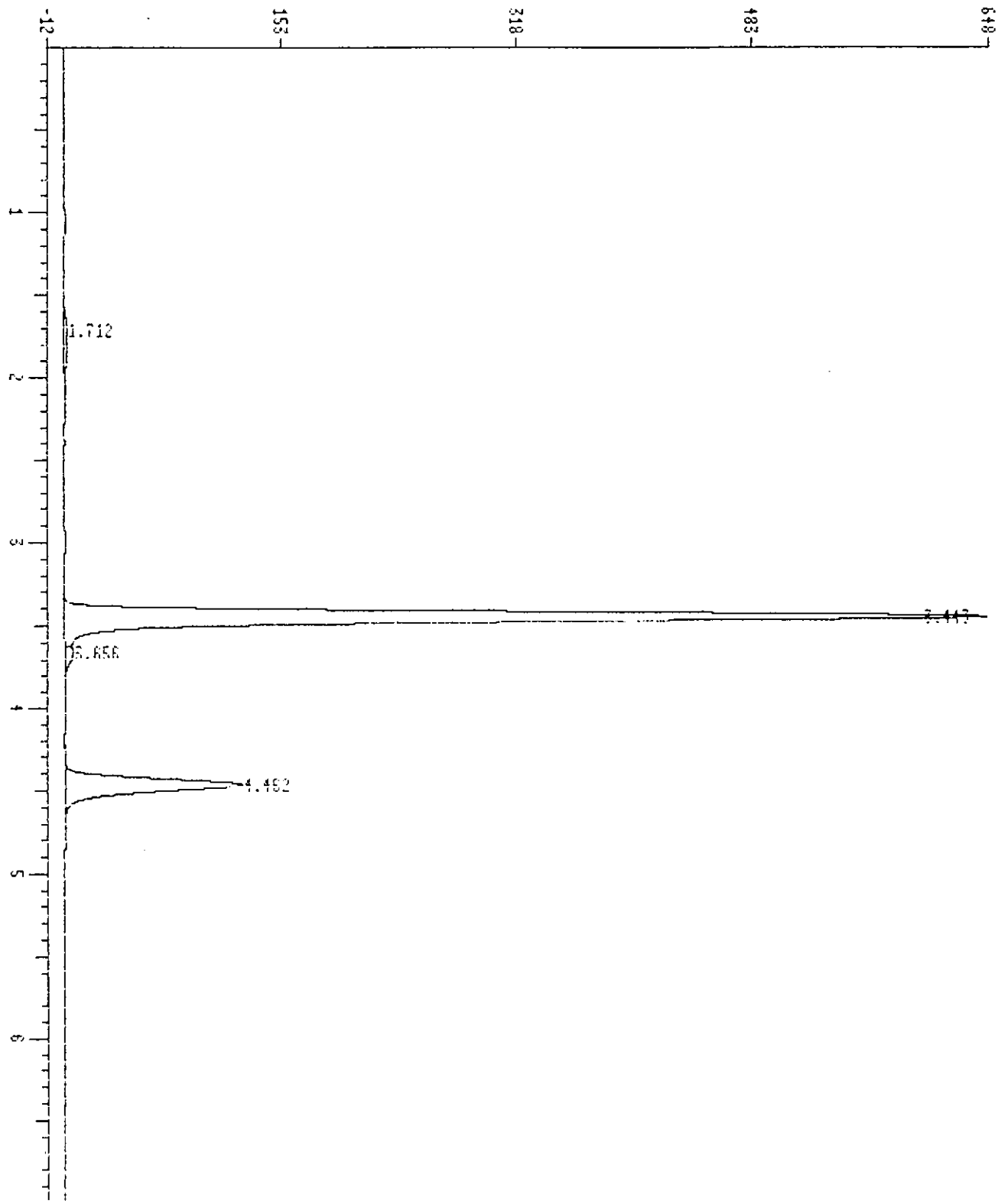
Operator: JCP 1 Apr 92 3:50 pm
Method File Name : DNPHIII.M
Sample Info : #2
Misc Info:
Integration File Name : DATA:0401A06A.I
consisting of channels : 1. A 360,4 550,100 of 0401A06A.D
Sequence Index: 1 Bottle Number : 6 Repetition Number: 1

A 360,4 550,100 of 0401A06A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.703	BB	35.3071	1.9539	1.03	100.00	0.257	0.39
3.443	BV	2676.29	647.54	77.92	100.00	0.064	0.83
3.656	VB	39.6031	5.7152	1.15	100.00	0.104	0.50
4.462	BV	683.46	124.57	19.90	100.00	0.085	0.82

27

1: LC A 360,4 550,100 of 0401A06B.D



\J
90

*** Area Percent ***

Report by Signal

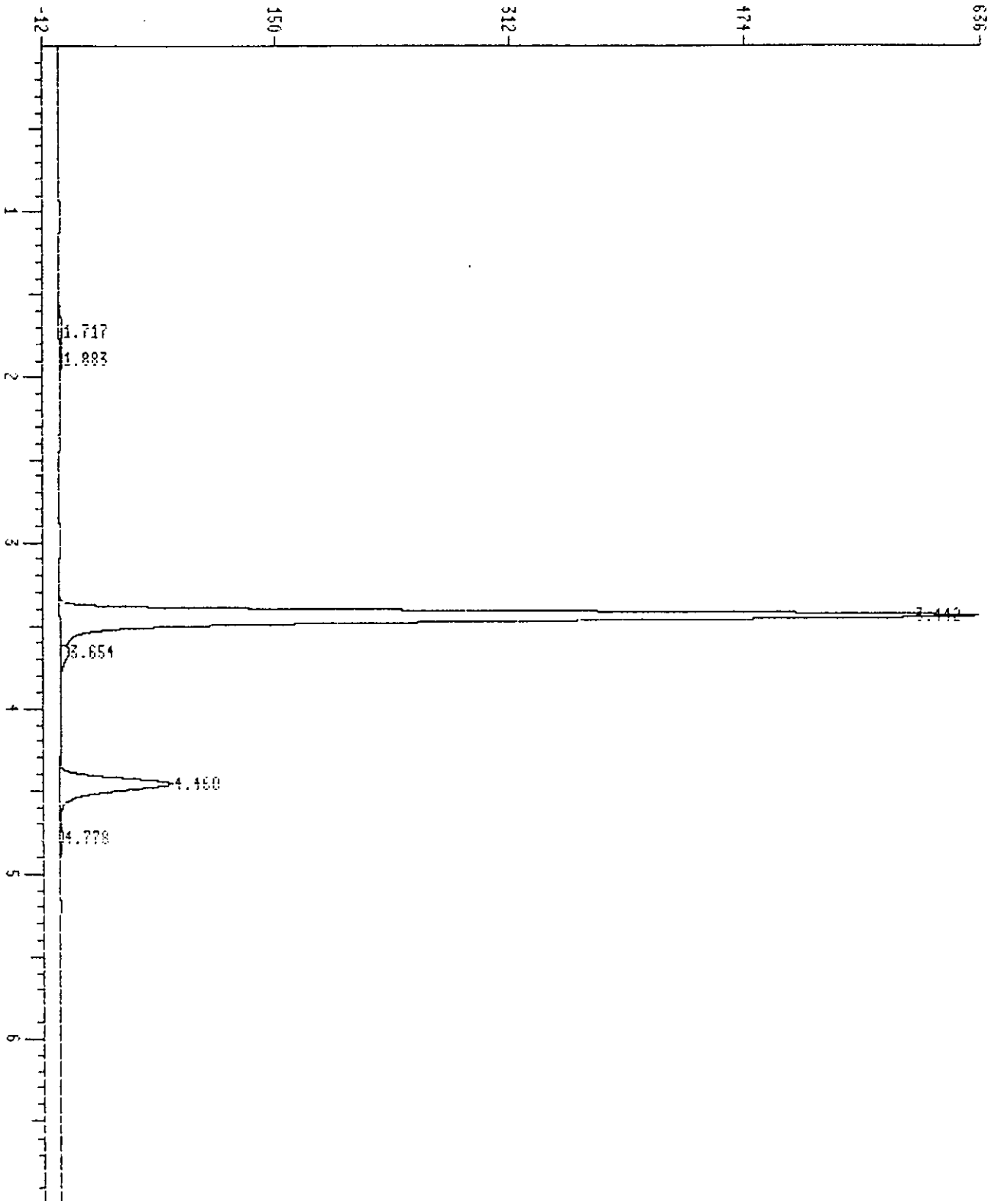
Operator: JCP 1 Apr 92 3:59 pm
Method File Name : DNPHIII.M
Sample Info : #2
Misc Info:
Integration File Name : DATA:0401A06B.I
consisting of channels : 1. A 360,4 550,100 of 0401A06B.D
Sequence Index: 1 Bottle Number : 6 Repetition Number: 2

A 360,4 550,100 of 0401A06B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.712	BB	37.1894	1.9842	1.09	100.00	0.273	0.44
3.443	BV	2679.53	649.24	77.95	100.00	0.064	0.93
3.656	VB	37.7752	5.5637	1.10	100.00	0.103	0.49
4.462	BV	682.79	124.52	19.86	100.00	0.085	0.82

29

1: LC A 360,4 550,100 of 0401A07A.D



*** Area Percent ***

Report by Signal

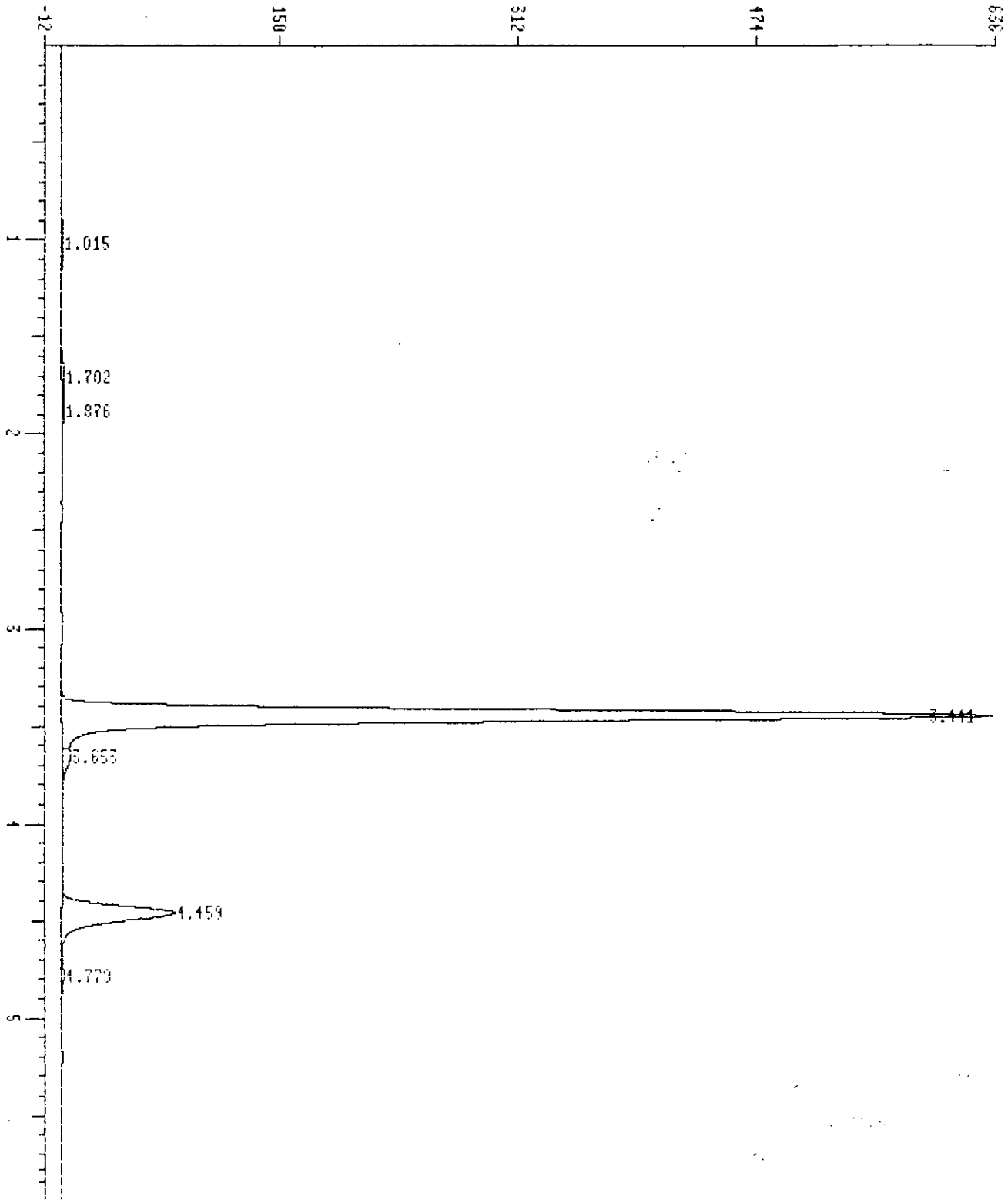
Operator: JCP 1 Apr 92 4:09 pm
Method File Name : DNPHIII.M
Sample Info : #3
Misc Info:
Integration File Name : DATA:0401A07A.I
consisting of channels : 1. A 350,4 550,100 of 0401A07A.D
Sequence Index: 1 Bottle Number : 7 Repetition Number: 1

A 350,4 550,100 of 0401A07A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.717	BV	22.5503	1.7941	0.72	100.00	0.191	0.97
1.983	VB	10.6341	1.3959	0.34	100.00	0.127	0.55
3.442	BV	2625.25	534.62	83.66	100.00	0.084	0.93
3.654	VB	37.0954	5.5245	1.18	100.00	0.112	0.49
4.460	BV	431.31	77.8143	13.75	100.00	0.095	0.91
4.778	VB	11.0599	1.5554	0.35	100.00	0.106	0.85

31

1: LC A 360,4 550,100 of 0401A07B.D



3
12

*** Area Percent ***

Report by Signal

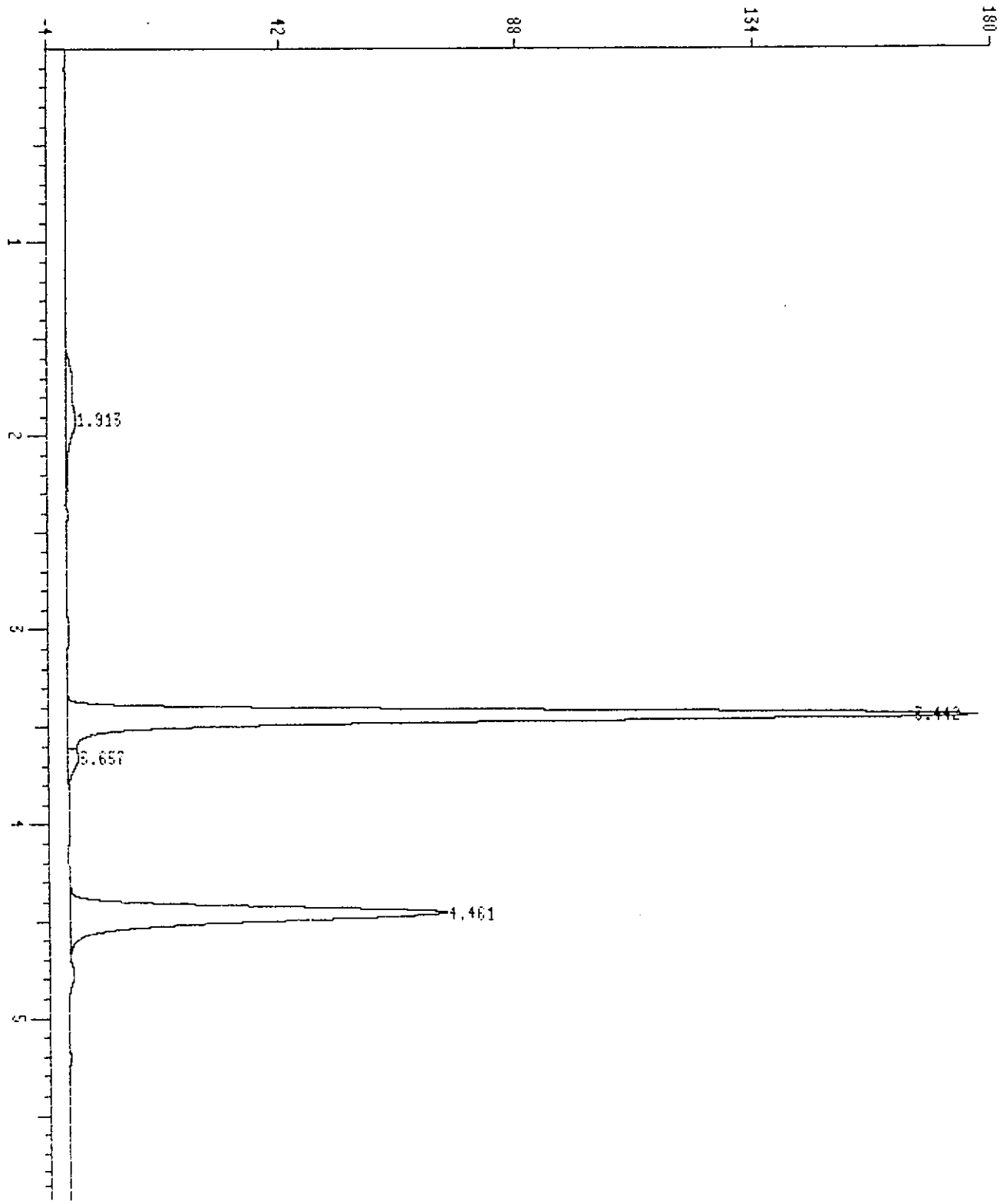
Operator: JCP 1 Apr 92 4:19 pm
Method File Name : DNPHIII.M
Sample Info : #3
Misc Info:
Integration File Name : DATA:0401A07B.I
consisting of channels : 1. A 360,4 550,100 of 0401A07B.D
Sequence Index: 1 Bottle Number : 7 Repetition Number: 2 .

A 360,4 550,100 of 0401A07B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.015	BB	12.5096	1.0210	0.40	100.00	0.177	1.08
1.702	BV	22.8823	1.8281	0.73	100.00	0.195	0.75
1.876	VB	8.9785	1.3049	0.29	100.00	0.115	0.43
3.441	BV	2625.86	634.16	83.48	100.00	0.065	0.83
3.653	VB	36.5853	5.3983	1.16	100.00	0.113	0.45
4.459	BV	428.18	77.6398	13.61	100.00	0.085	0.81
4.779	VB	10.5710	1.5338	0.34	100.00	0.107	0.97

33

1: LC A 360,4 550,100 of 0401A08A.D



34

*** Area Percent ***

Report by Signal

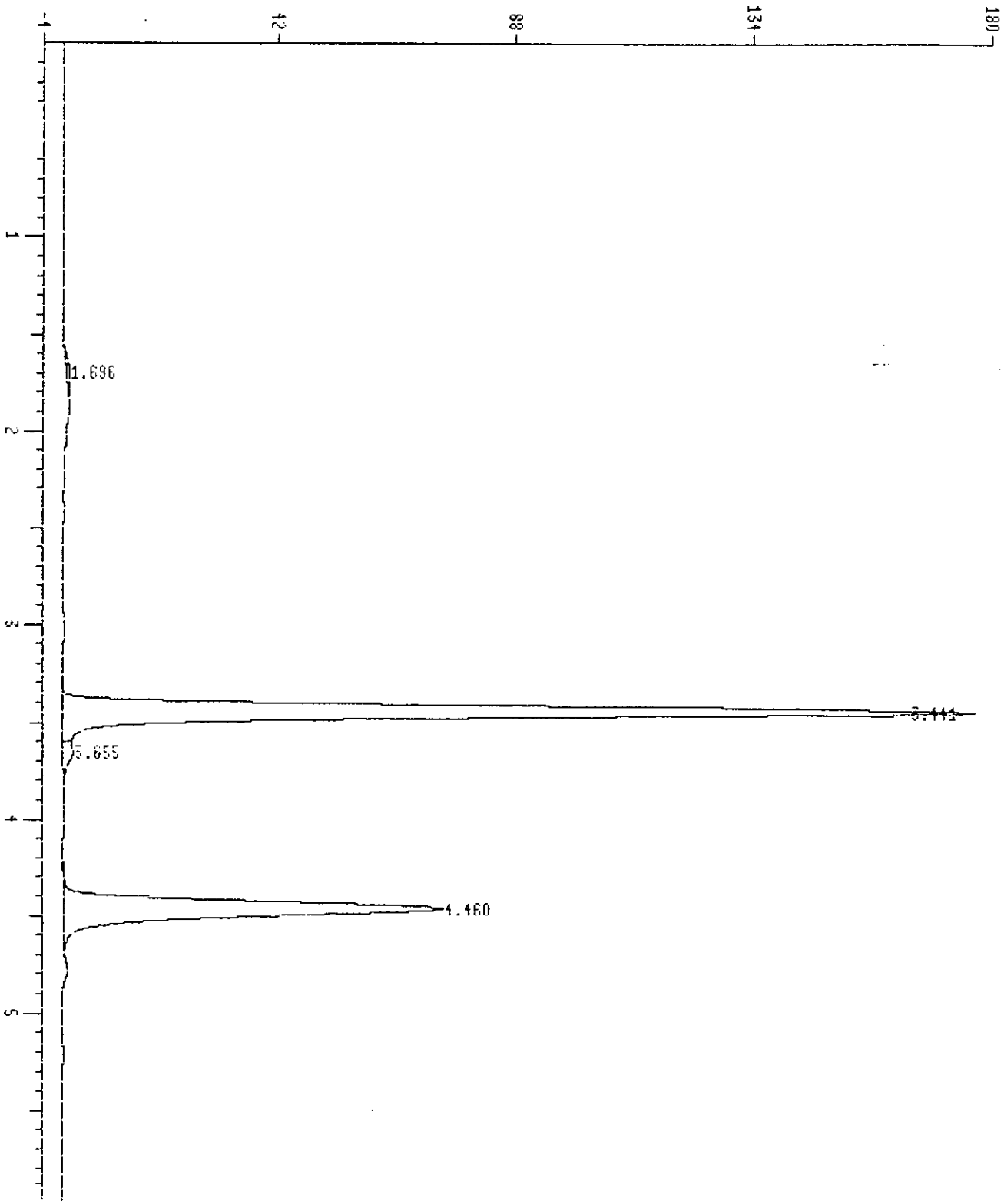
Operator: JCP 1 Apr 92 4:28 pm
Method File Name : DNPHIII.M
Sample Info : #4
Misc Info:
Integration File Name : DATA:0401A08A.I
consisting of channels : 1. A 360,4 550,100 of 0401A08A.D
Sequence Index: 1 Bottle Number : 8 Repetition Number: 1

A 360,4 550,100 of 0401A08A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.913	BB	36.0266	1.8766	3.05	100.00	0.257	1.87
3.442	BV	724.61	177.09	61.39	100.00	0.064	0.85
3.657	VB	14.3525	2.0295	1.22	100.00	0.108	0.61
4.461	BV	405.29	73.9268	34.34	100.00	0.085	0.82

35

1: LC A 360,4 550,100 of 0401A08B.D



3

*** Area Percent ***

Report by Signal

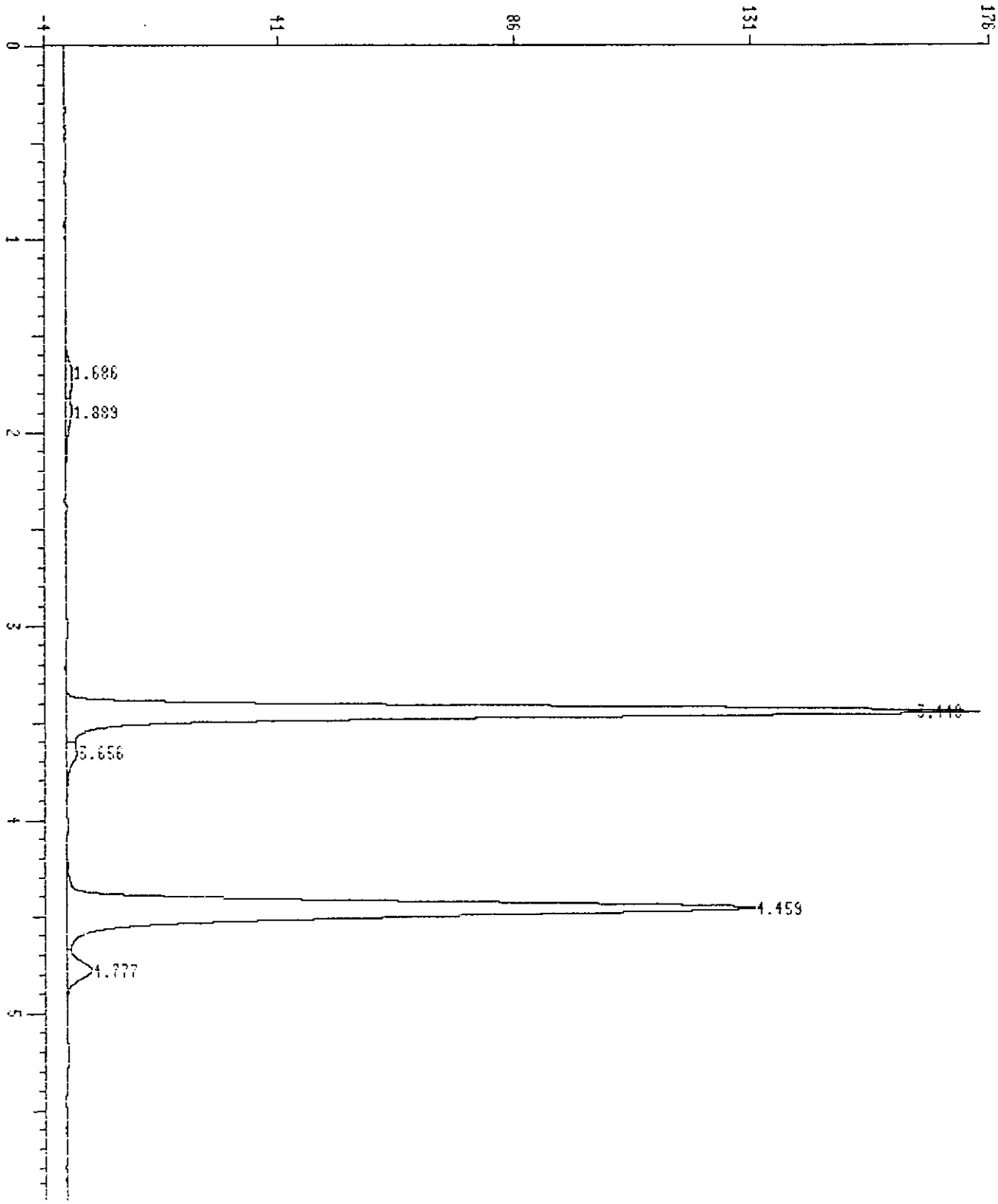
Operator: JCP 1 Apr 92 4:36 pm
Method File Name : DNPHIII.M
Sample Info : #4
Misc Info:
Integration File Name : DATA:0401A08B.I
consisting of channels : 1. A 360,4 550,100 of 0401A08B.D
Sequence Index: 1 Bottle Number : 8 Repetition Number: 2

A 360,4 550,100 of 0401A08B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.696	BV	6.1331	0.6480	0.53	100.00	0.169	1.08
3.441	BV	723.89	176.83	63.02	100.00	0.064	0.85
3.655	VB	13.6595	1.9092	1.19	100.00	0.107	0.70
4.460	BV	404.93	73.8308	35.25	100.00	0.085	0.82

37

1: LC A 350,4 550,100 of 0401A09A.D



3
8

*** Area Percent ***

Report by Signal

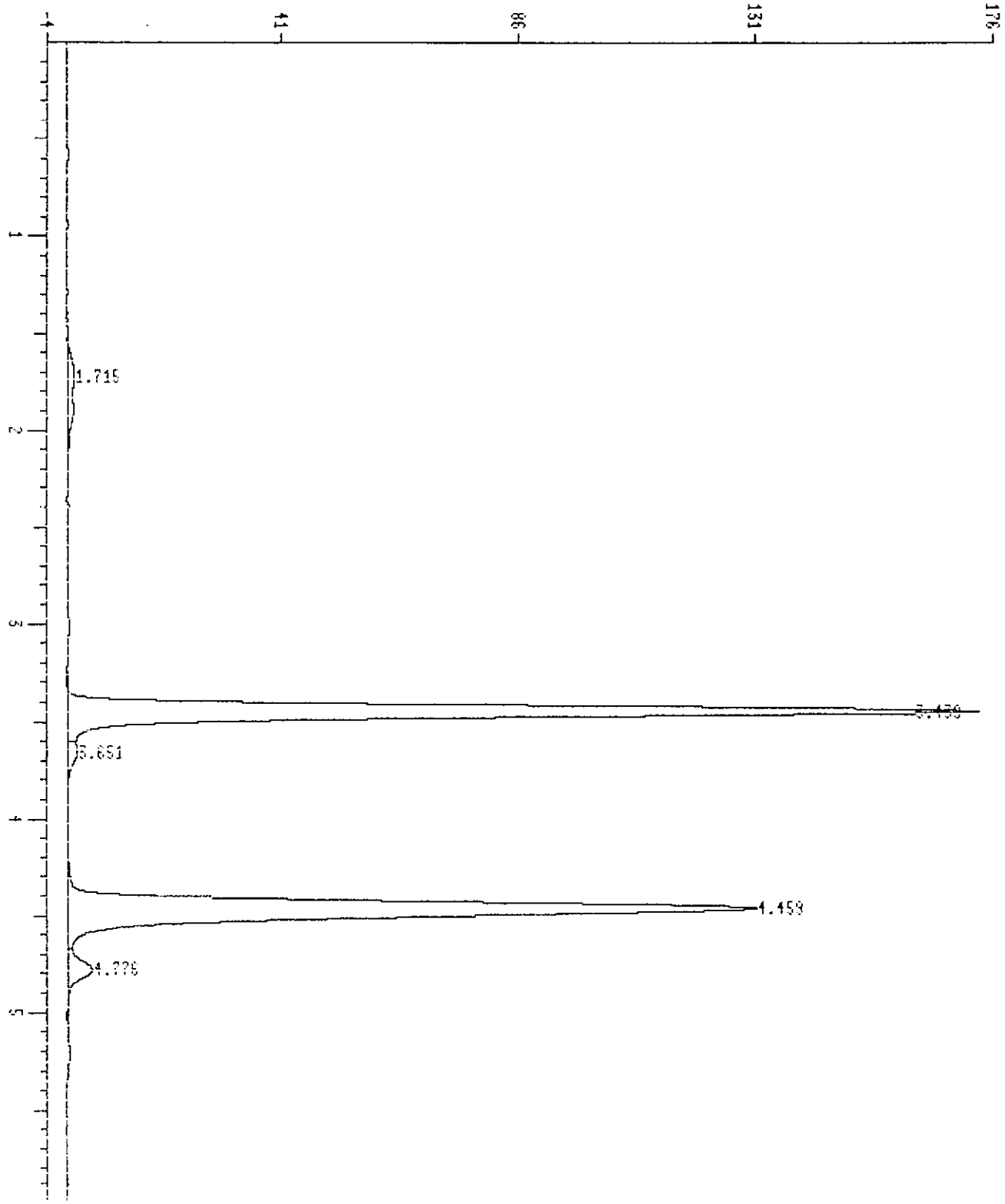
Operator: JCP 1 Apr 92 4:45 pm
Method File Name : DNPHIII.M
Sample Info : #5
Misc Info:
Integration File Name : DATA:0401A09A.I
consisting of channels : 1. A 360,4 550,100 of 0401A09A.D
Sequence Index: 1 Bottle Number : 9 Repetition Number: 1

A 360,4 550,100 of 0401A09A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.886	BV	15.3994	1.2913	1.02	100.00	0.206	0.66
1.889	VB	12.1693	1.2043	0.80	100.00	0.139	0.52
3.440	BV	713.44	174.02	47.10	100.00	0.064	0.85
3.656	VB	13.9496	1.9330	0.92	100.00	0.120	0.76
4.459	BV	727.09	131.24	48.00	100.00	0.086	0.81
4.777	VB	32.6833	4.7772	2.16	100.00	0.104	0.97

39

1: LC A 360,4 550,100 of 0401A09B.D



07

*** Area Percent ***

Report by Signal

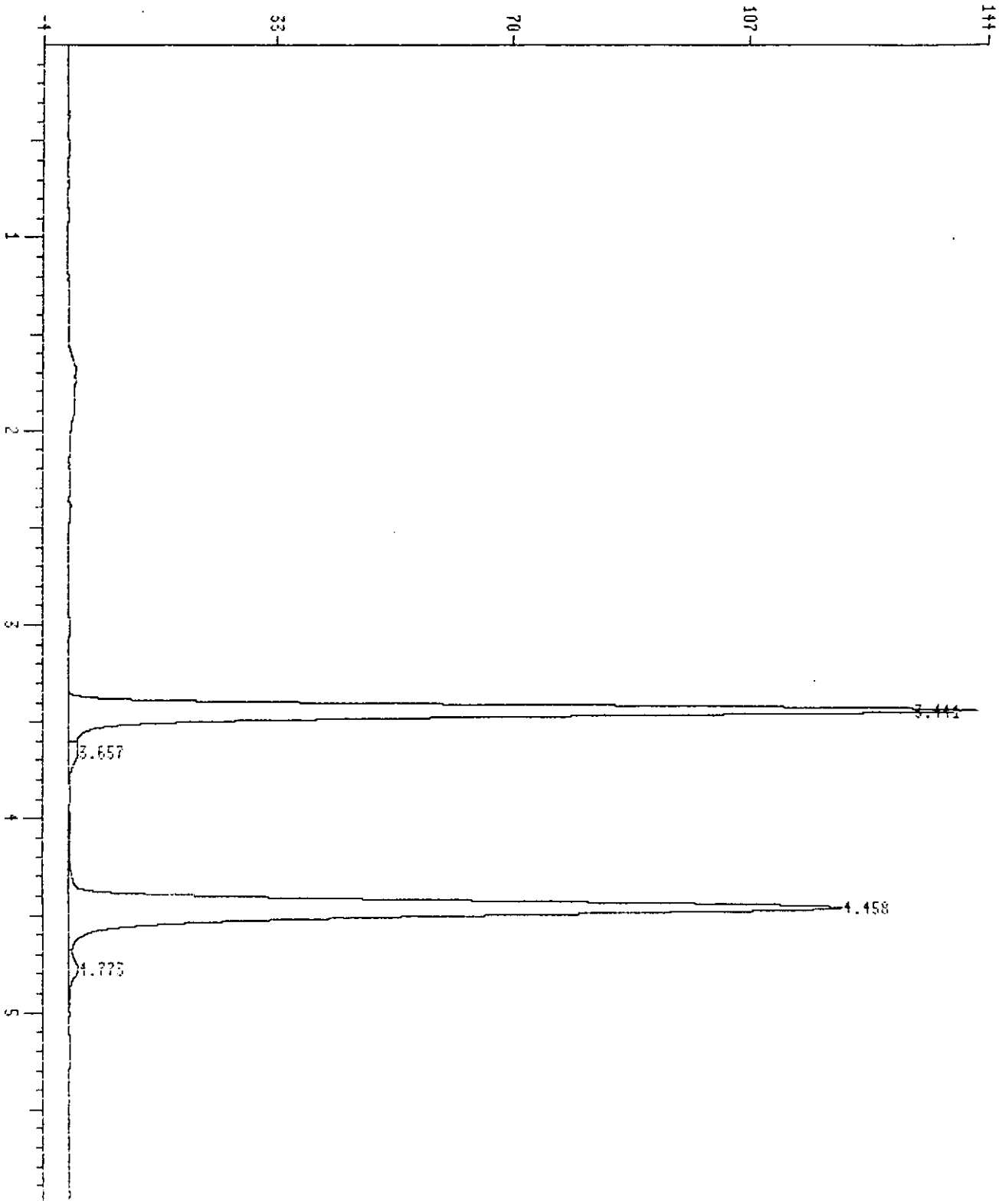
Operator: JCP 1 Apr 92 4:54 pm
Method File Name : DNPHIII.M
Sample Info : #5
Misc Info:
Integration File Name : DATA:0401A09B.I
consisting of channels : 1. A 360,4 550,100 of 0401A09B.D
Sequence Index: 1 Bottle Number : 9 Repetition Number: 2

A 360,4 550,100 of 0401A09B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.715	BB	26.9974	1.2432	1.79	100.00	0.344	0.42
3.439	BV	712.92	173.58	47.04	100.00	0.065	0.85
3.651	VB	13.7053	1.9161	0.90	100.00	0.119	0.62
4.459	PV	728.21	131.05	48.05	100.00	0.086	0.82
4.775	VV	33.7794	4.8225	2.23	100.00	0.107	0.99

17.

1: LC A 350,4 550,100 of 0401A10A.D



42

*** Area Percent ***

Report by Signal

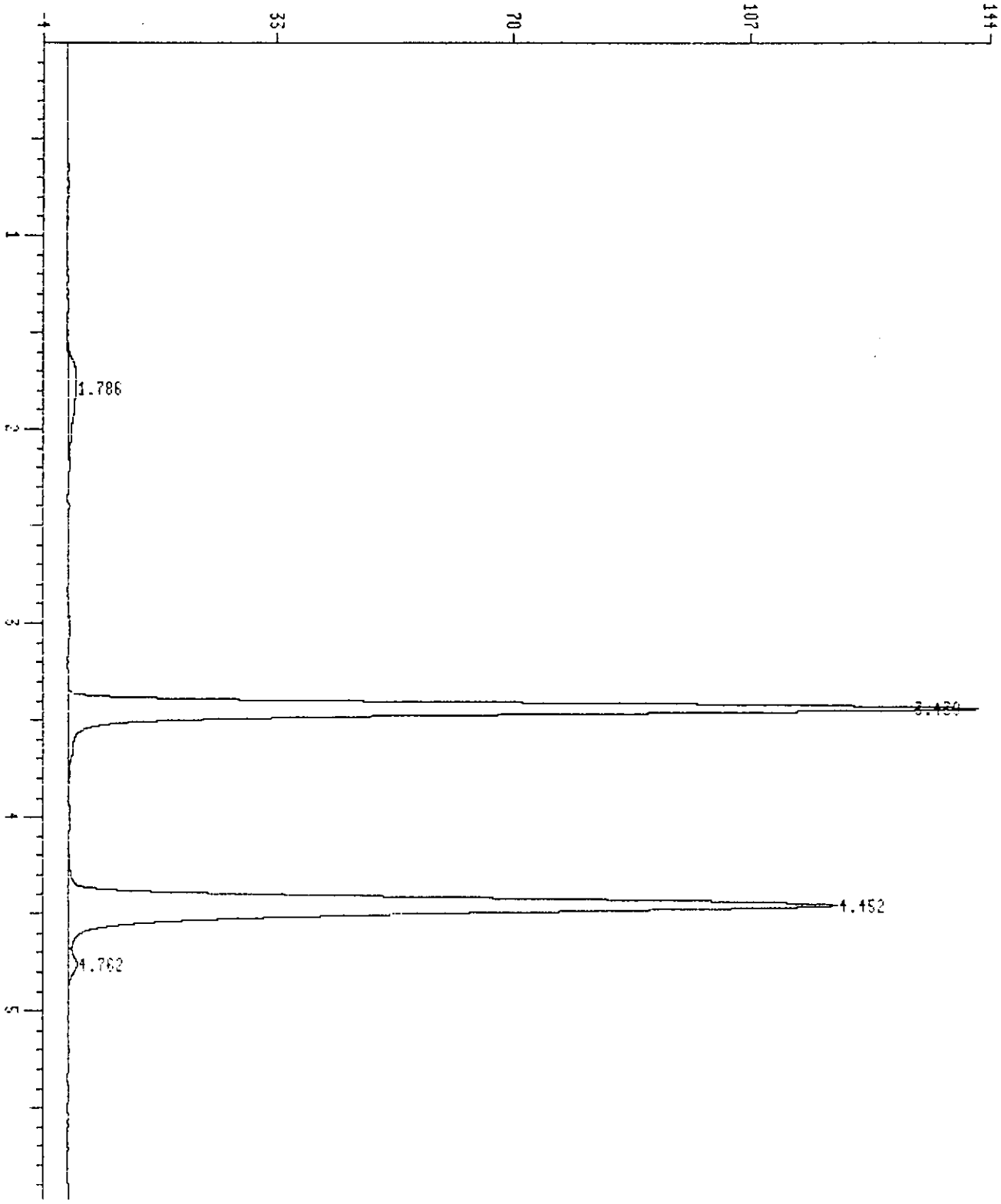
Operator: JCP 1 Apr-92 5:02 pm
Method File Name : DNPHIII.M
Sample Info : #5
Misc Info:
Integration File Name : DATA:0401A10A.I
consisting of channels : 1. A 360,4 550,100 of 0401A10A.D
Sequence Index: 1 Bottle Number : 10 Repetition Number: 1

A 360,4 550,100 of 0401A10A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.441	BV	585.54	142.68	45.74	100.00	0.064	0.85
3.657	VB	10.7619	1.4969	0.84	100.00	0.120	0.75
4.458	BV	673.53	121.35	52.61	100.00	0.086	0.81
4.773	VB	10.3312	1.4066	0.81	100.00	0.112	0.84

43

1: LC A 350,4 550,100 of 0401A10B.D



44

*** Area Percent ***

Report by Signal

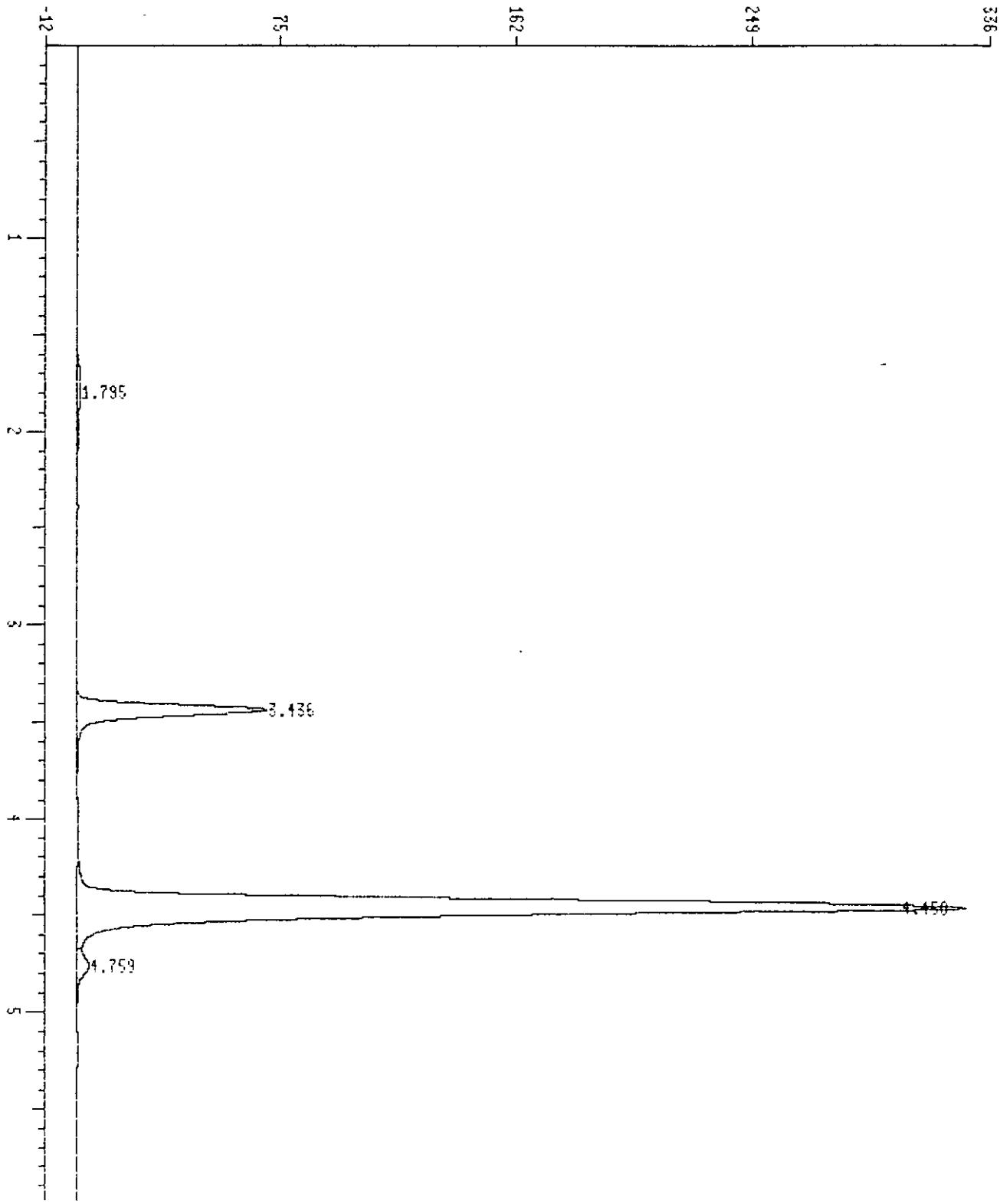
Operator: JCP 1 Apr 92 5:11 pm
Method File Name : DNPHIII.M
Sample Info : #6
Misc Info:
Integration File Name : DATA:0401A10B.I
consisting of channels : 1. A 360,4 550,100 of 0401A10B.D
Sequence Index: 1 Bottle Number : 10 Repetition Number: 2

A 360,4 550,100 of 0401A10B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.786	BB	26.2522	1.3113	2.02	100.00	0.288	0.77
3.438	BB	589.02	142.28	45.31	100.00	0.065	0.83
4.452	BV	674.44	120.18	51.88	100.00	0.087	0.80
4.762	VB	10.3418	1.4293	0.80	100.00	0.110	0.93

45

1: LC A 350,4 550,100 of 0401A11A.D



97

*** Area Percent ***

Report by Signal

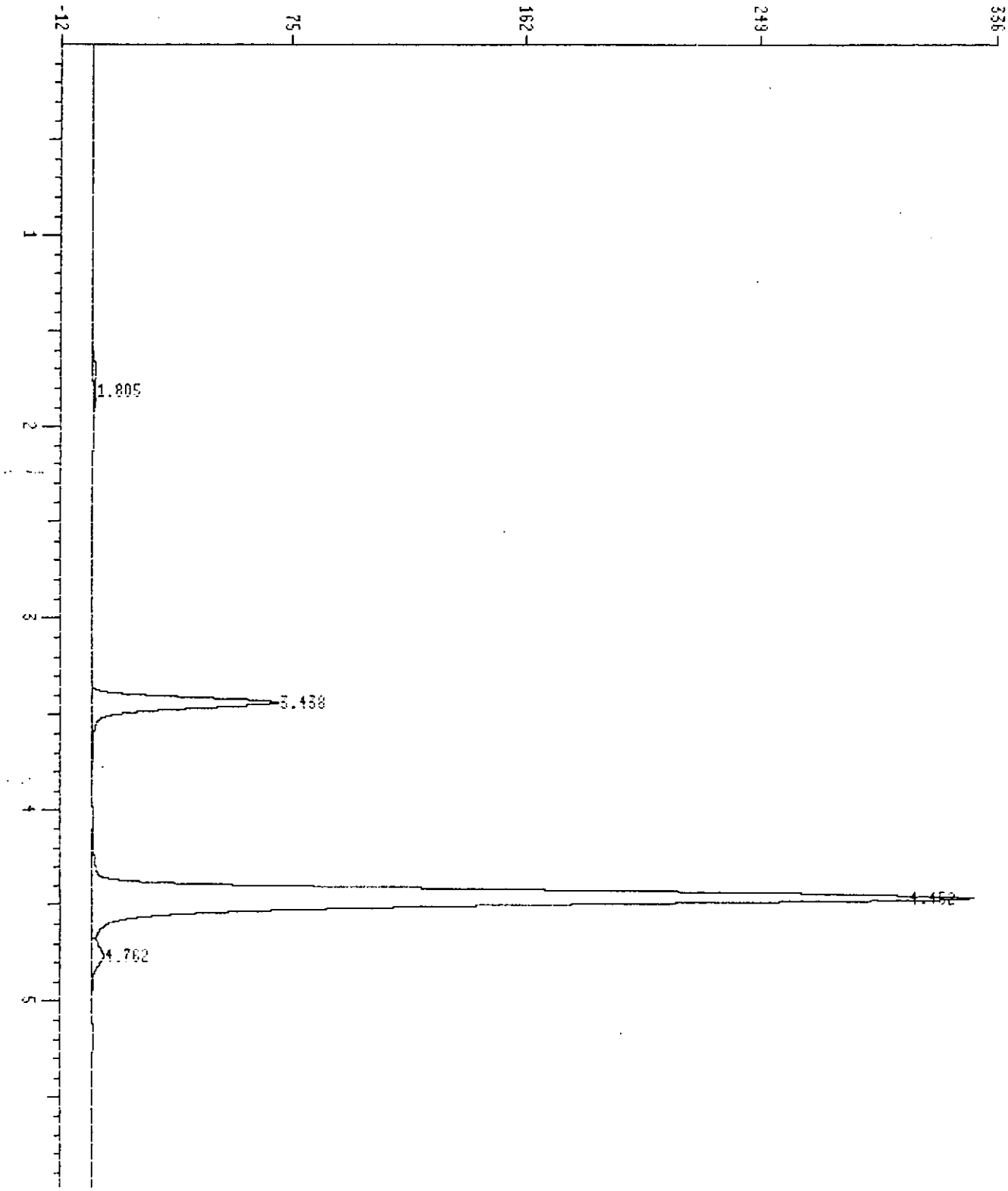
Operator: JCP 1 Apr 92 5:20 pm
Method File Name : DNPHIII.M
Sample Info : #7
Misc Info:
Integration File Name : DATA:0401A11A.I
consisting of channels : 1. A 360,4 550,100 of 0401A11A.D
Sequence Index: 1 Bottle Number : 11 Repetition Number: 1

A 360,4 550,100 of 0401A11A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.795	BB	21.5689	1.0819	0.99	100.00	0.289	0.85
3.436	BB	294.64	70.4519	13.55	100.00	0.065	0.83
4.450	BV	1827.55	326.98	84.05	100.00	0.086	0.80
4.759	VB	30.7191	4.2842	1.41	100.00	0.108	0.94

47

1: LC A 360,4 550,100 of 0401A11B.D



48

*** Area Percent ***

Report by Signal

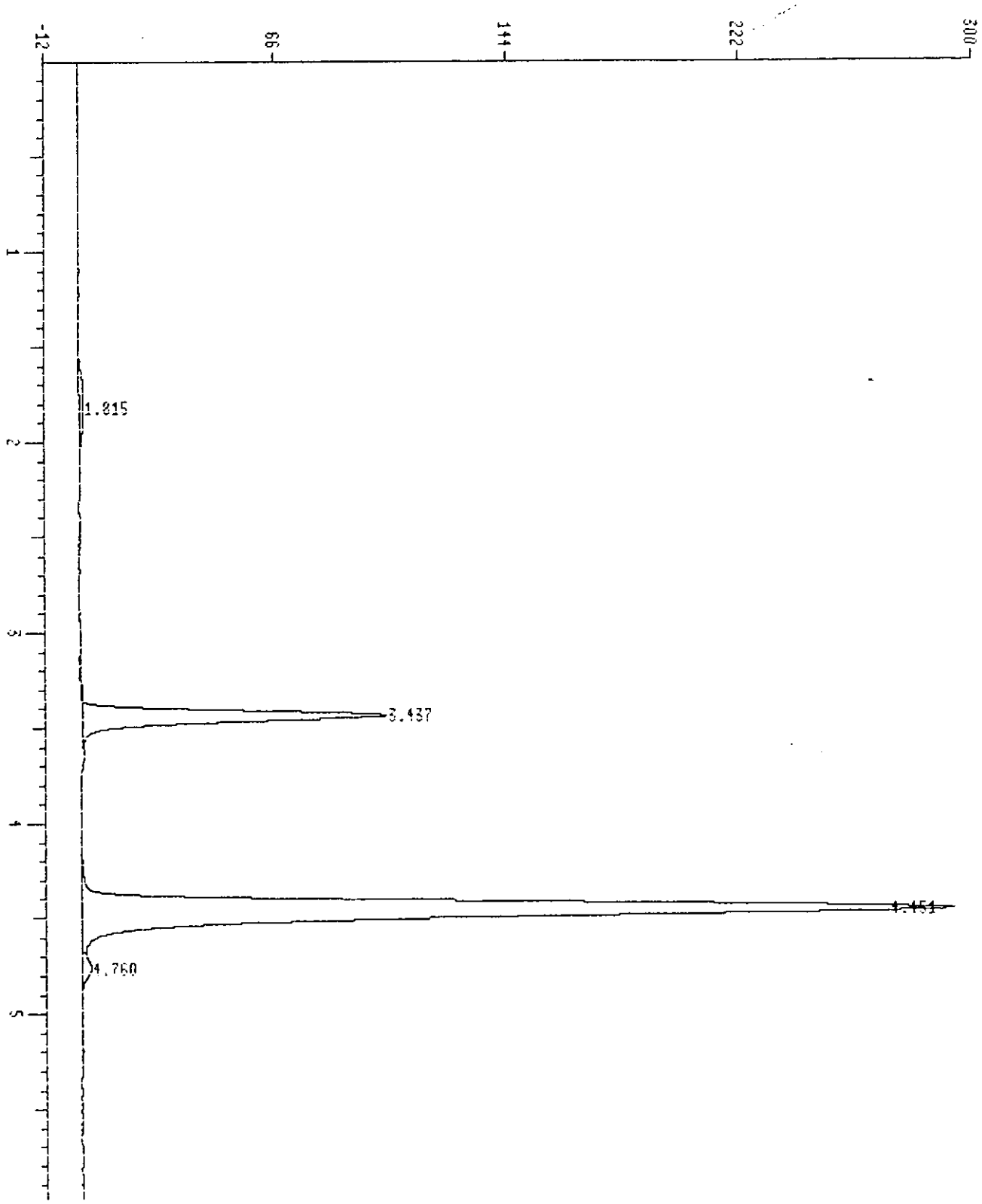
Operator: JCP 1 Apr 92 5:28 pm
Method File Name : DNPHIII.M
Sample Info : #7
Misc Info:
Integration File Name : DATA:0401A11B.I
consisting of channels : 1. A 360,4 550,100 of 0401A11B.D
Sequence Index: 1 Bottle Number : 11 Repetition Number: 2

A 360,4 550,100 of 0401A11B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.805	BV	13.1852	0.8855	0.61	100.00	0.195	1.96
3.438	BB	291.67	70.1727	13.52	100.00	0.065	0.82
4.452	BV	1823.29	327.38	84.49	100.00	0.086	0.80
4.762	VB	29.9527	4.2175	1.39	100.00	0.108	0.98

49

1: LC A 360,4 550,100 of 0401A12A.D



8

*** Area Percent ***

Report by Signal

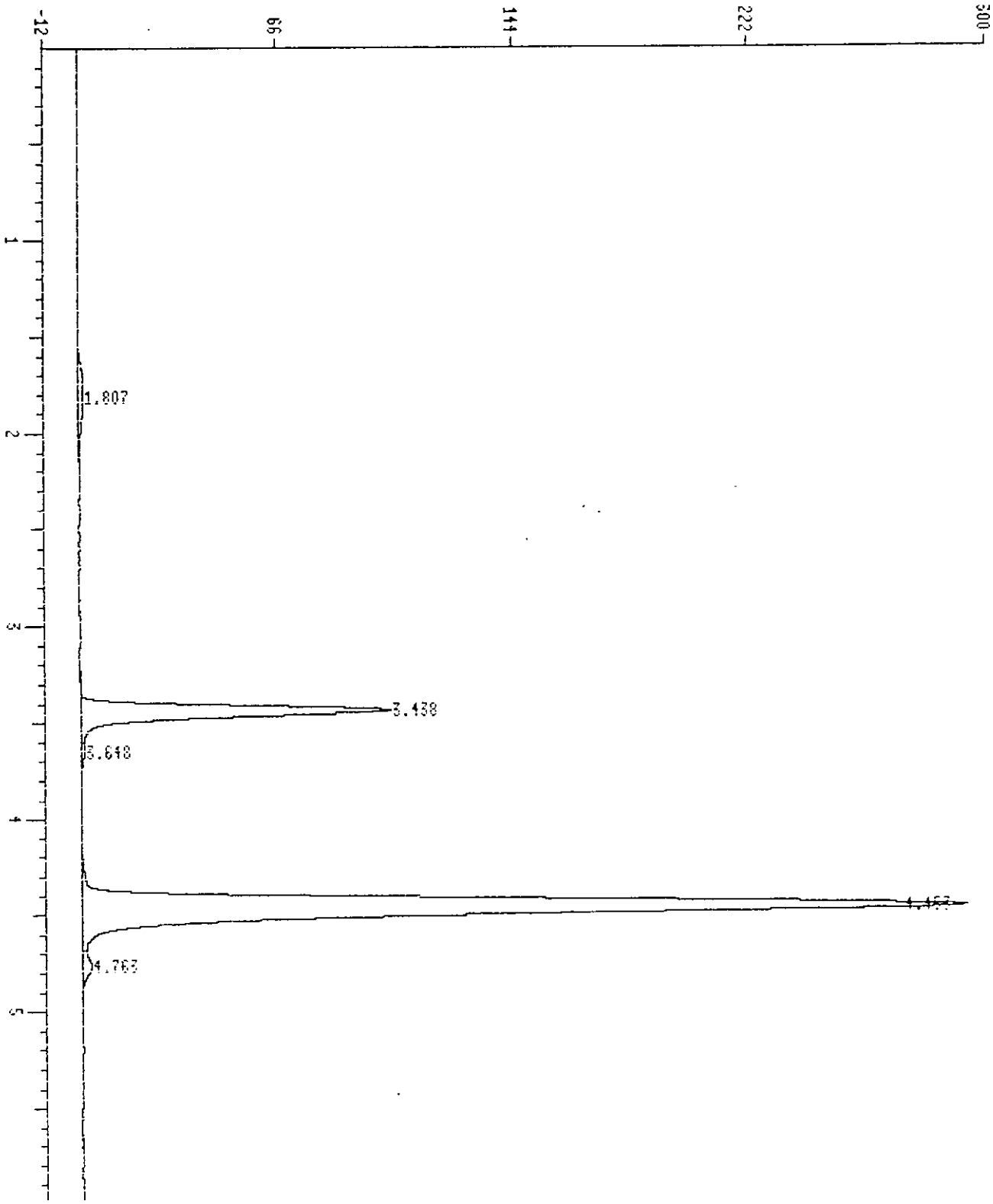
Operator: JCP 1 Apr 92 5:37 pm
Method File Name : DNPHIII.M
Sample Info : #8
Misc Info:
Integration File Name : DATA:0401A12A.I
consisting of channels : 1. A 360,4 550,100 of 0401A12A.D
Sequence Index: 1 Bottle Number : 12 Repetition Number: 1

A 360,4 550,100 of 0401A12A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.815	BB	30.0397	1.5101	1.43	100.00	0.275	0.92
3.437	BV	406.07	102.50	19.39	100.00	0.063	0.82
4.451	BV	1634.76	293.15	78.05	100.00	0.086	0.80
4.760	VB	23.6139	3.2287	1.13	100.00	0.110	0.93

15

1: LC A 350,4 550,100 of 0401A12B.D



*** Area Percent ***

Report by Signal

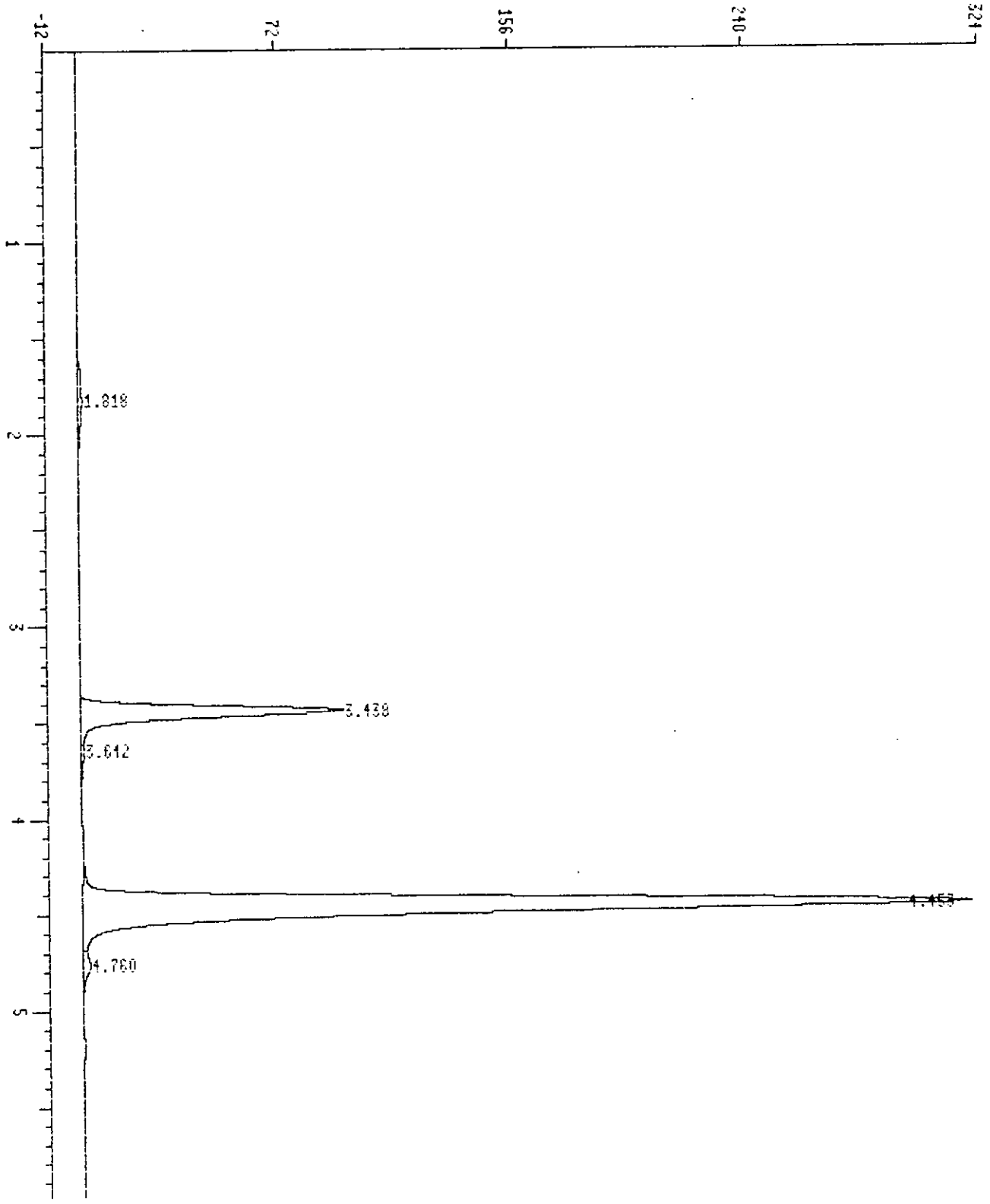
Operator: JCP 1 Apr 92 5:46 pm
Method File Name : DNPHIII.M
Sample Info : #8
Misc Info:
Integration File Name : DATA:0401A12B.I
consisting of channels : 1. A 360,4 550,100 of 0401A12B.D
Sequence Index: 1 Bottle Number : 12 Repetition Number: 2

A 360,4 550,100 of 0401A12B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.807	BB	30.5566	1.5195	1.44	100.00	0.276	0.93
3.438	BV	425.14	103.19	20.04	100.00	0.065	0.85
3.648	VB	7.7667	1.1792	0.37	100.00	0.110	0.73
4.453	BV	1635.47	293.29	77.09	100.00	0.086	0.81
4.763	VB	22.5970	3.1229	1.07	100.00	0.111	0.99

53

1: LC A 360,4 550,100 of 0401A13A.D



54

*** Area Percent ***

Report by Signal

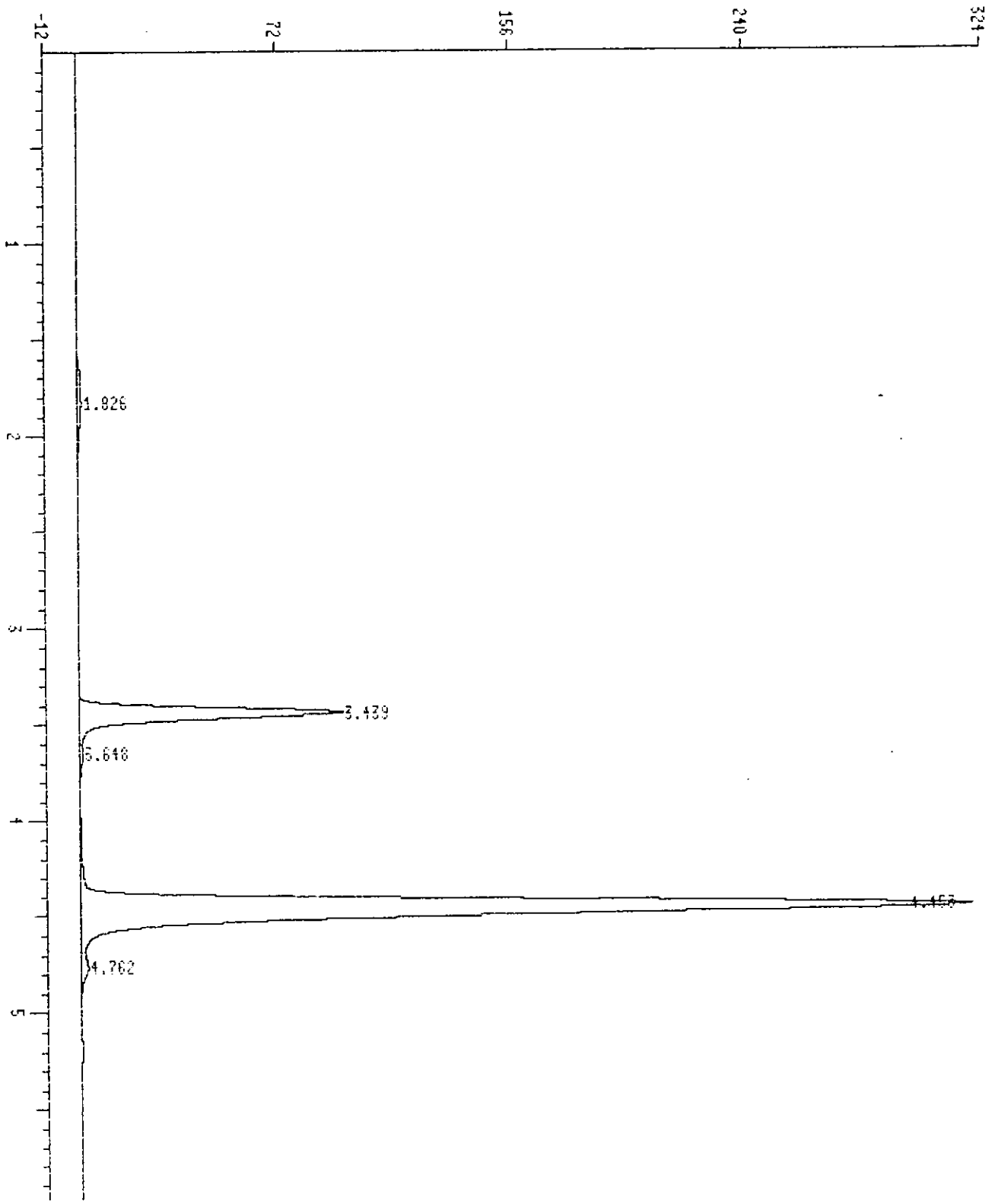
Operator: JCP 1 Apr 92 5:55 pm
Method File Name : DNPHIII.M
Sample Info : #9
Misc Info:
Integration File Name : DATA:0401A13A.I
consisting of channels : 1. A 360,4 550,100 of 0401A13A.D
Sequence Index: 1 Bottle Number : 13 Repetition Number: 1

A 360,4 550,100 of 0401A13A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.818	BB	29.2546	1.4604	1.32	100.00	0.279	1.01
3.438	BV	391.13	94.9617	17.59	100.00	0.065	0.84
3.642	VB	7.3758	1.1344	0.33	100.00	0.108	0.46
4.453	BV	1779.12	320.20	79.99	100.00	0.086	0.81
4.760	VB	17.3272	2.4237	0.78	100.00	0.109	0.94

55

1: LC A 360,4 550,100 of 0401A13B.D



46

*** Area Percent ***

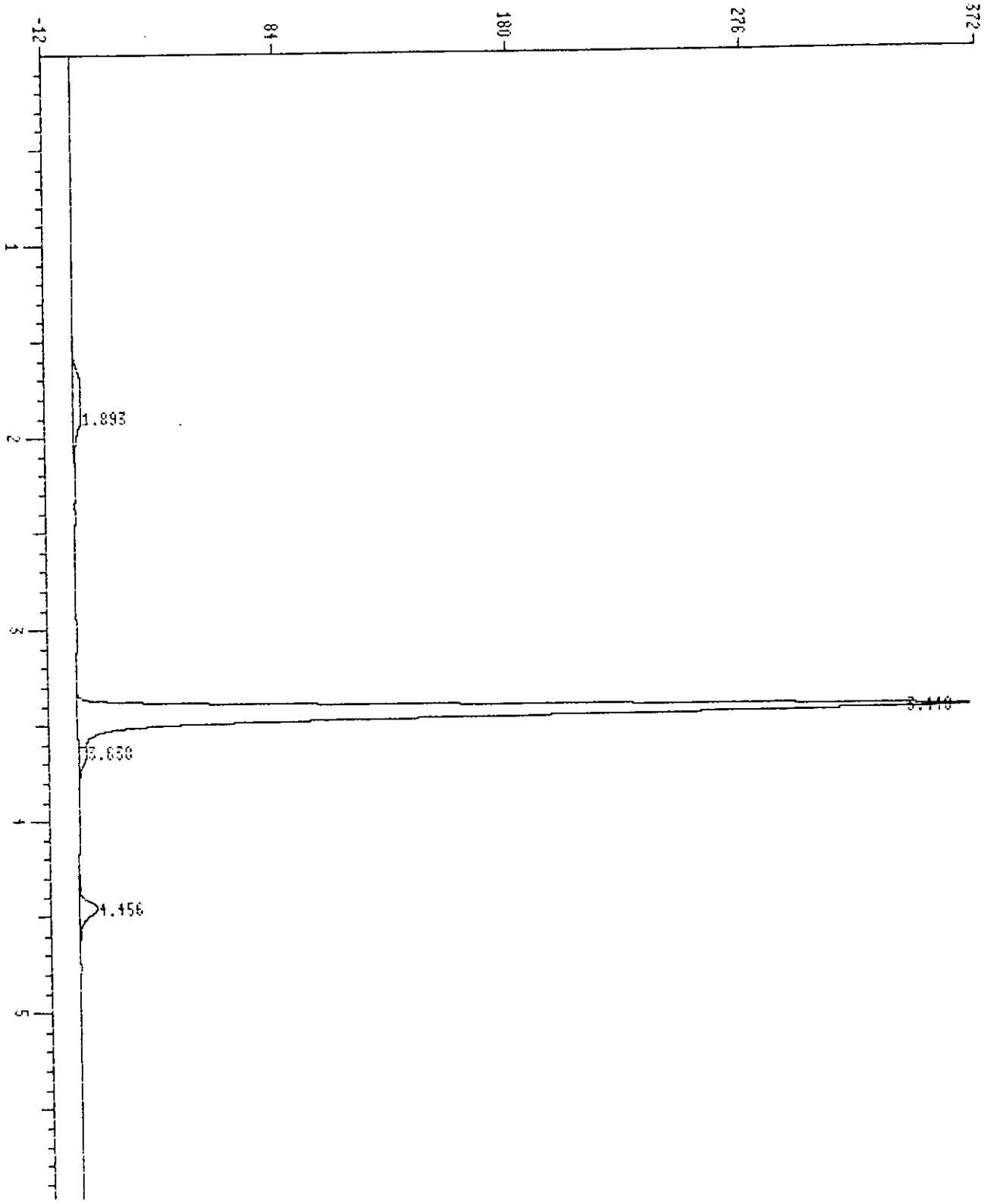
Report by Signal

Operator: JCP 1 Apr 92 6:03 pm
Method File Name : DNPHIII.M
Sample Info : #9
Misc Info:
Integration File Name : DATA:0401A13B.I
consisting of channels : 1. A 360,4 550,100 of 0401A13B.D
Sequence Index: 1 Bottle Number : 13 Repetition Number: 2

A 360,4 550,100 of 0401A13B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.826	BB	31.6097	1.4940	1.42	100.00	0.284	1.00
3.439	BV	390.92	95.0348	17.54	100.00	0.064	0.84
3.648	VB	8.0306	1.1811	0.36	100.00	0.113	0.61
4.453	BV	1781.04	320.85	79.93	100.00	0.086	0.81
4.762	VB	16.7373	2.3935	0.75	100.00	0.108	0.97

1: LC A 360,4 550,100 of 0401A15A.D



*** Area Percent ***

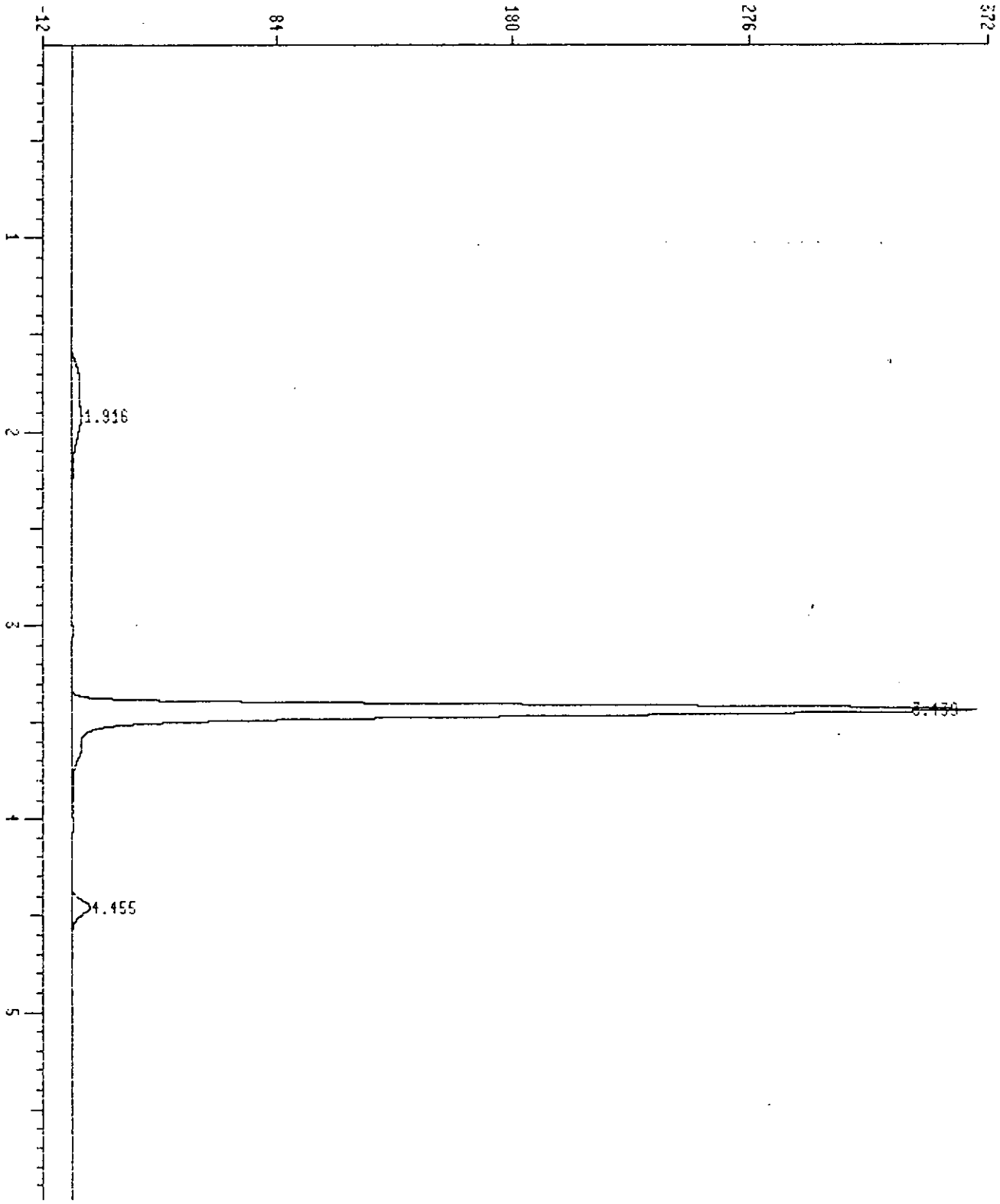
Report by Signal

Operator: JCP 1 Apr 92 6:29 pm
Method File Name : DNPHIII.M
Sample Info : #1b
Misc Info:
Integration File Name : DATA:0401A15A.I
consisting of channels : 1. A 360,4 550,100 of 0401A15A.D
Sequence Index: 1 Bottle Number : 15 Repetition Number: 1

A 360,4 550,100 of 0401A15A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.893	BB	66.0890	3.1262	4.03	100.00	0.268	2.46
3.440	BV	1506.77	367.46	91.99	100.00	0.064	0.84
3.638	VB	23.4151	3.4799	1.43	100.00	0.112	0.34
4.456	BB	41.7716	7.5726	2.55	100.00	0.086	0.81

1: LC A 360,4 550,100 of 0401A158.D



#160

*** Area Percent ***

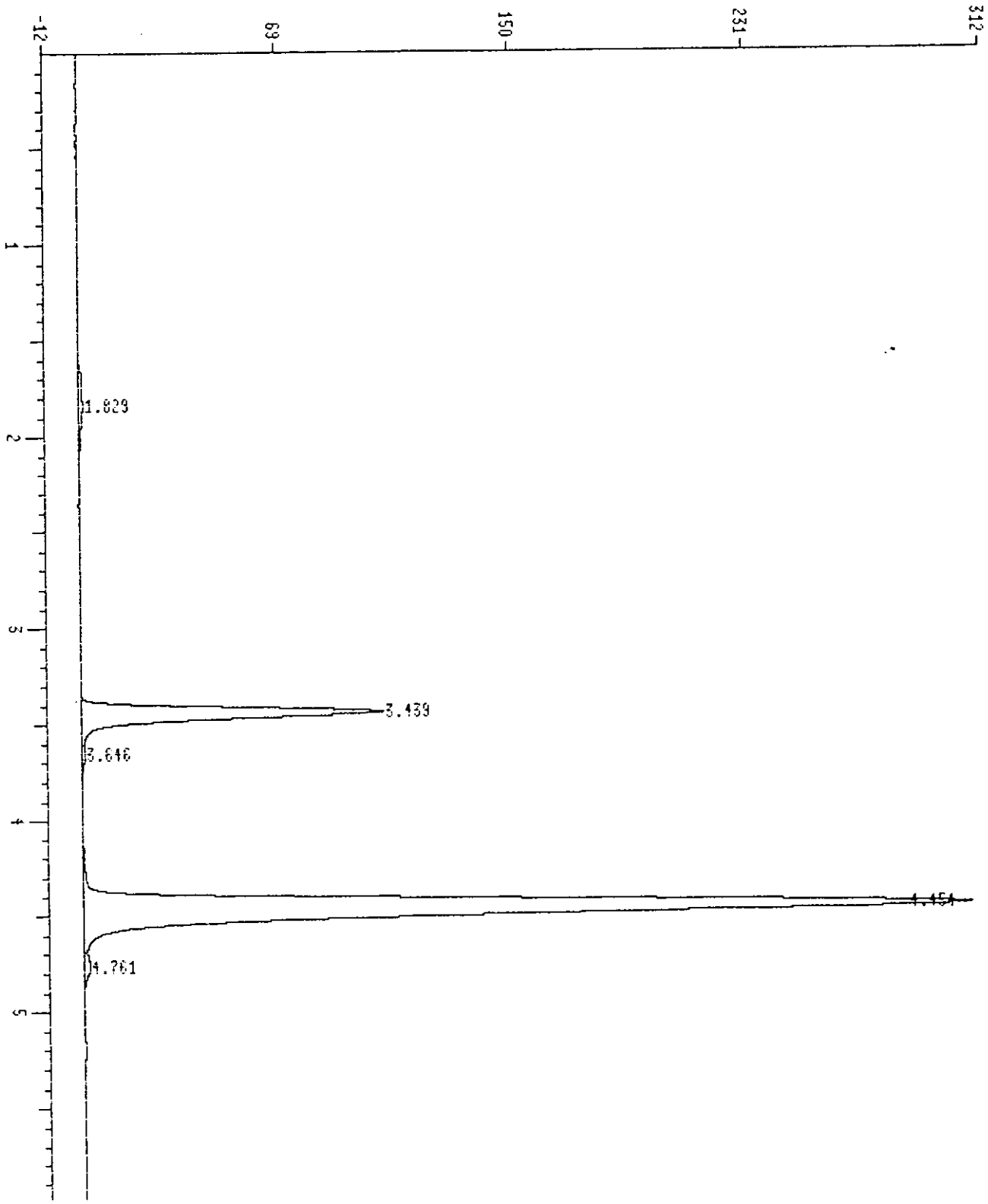
Report by Signal

Operator: JCP 1 Apr 92 6:38 pm
Method File Name : DNPHIII.M
Sample Info : #11
Misc Info:
Integration File Name : DATA:0401A15B.I
consisting of channels : 1. A 360,4 550,100 of 0401A15B.D
Sequence Index: 1 Bottle Number : 15 Repetition Number: 2

A 360,4 550,100 of 0401A15B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.916	BV	88.9381	4.1016	5.34	100.00	0.279	1.54
3.439	BB	1533.13	367.87	92.14	100.00	0.065	0.81
4.455	BB	41.9241	7.5137	2.52	100.00	0.086	0.80

1: LC A 360,4 550,100 of 0401A14A.D



*** Area Percent ***

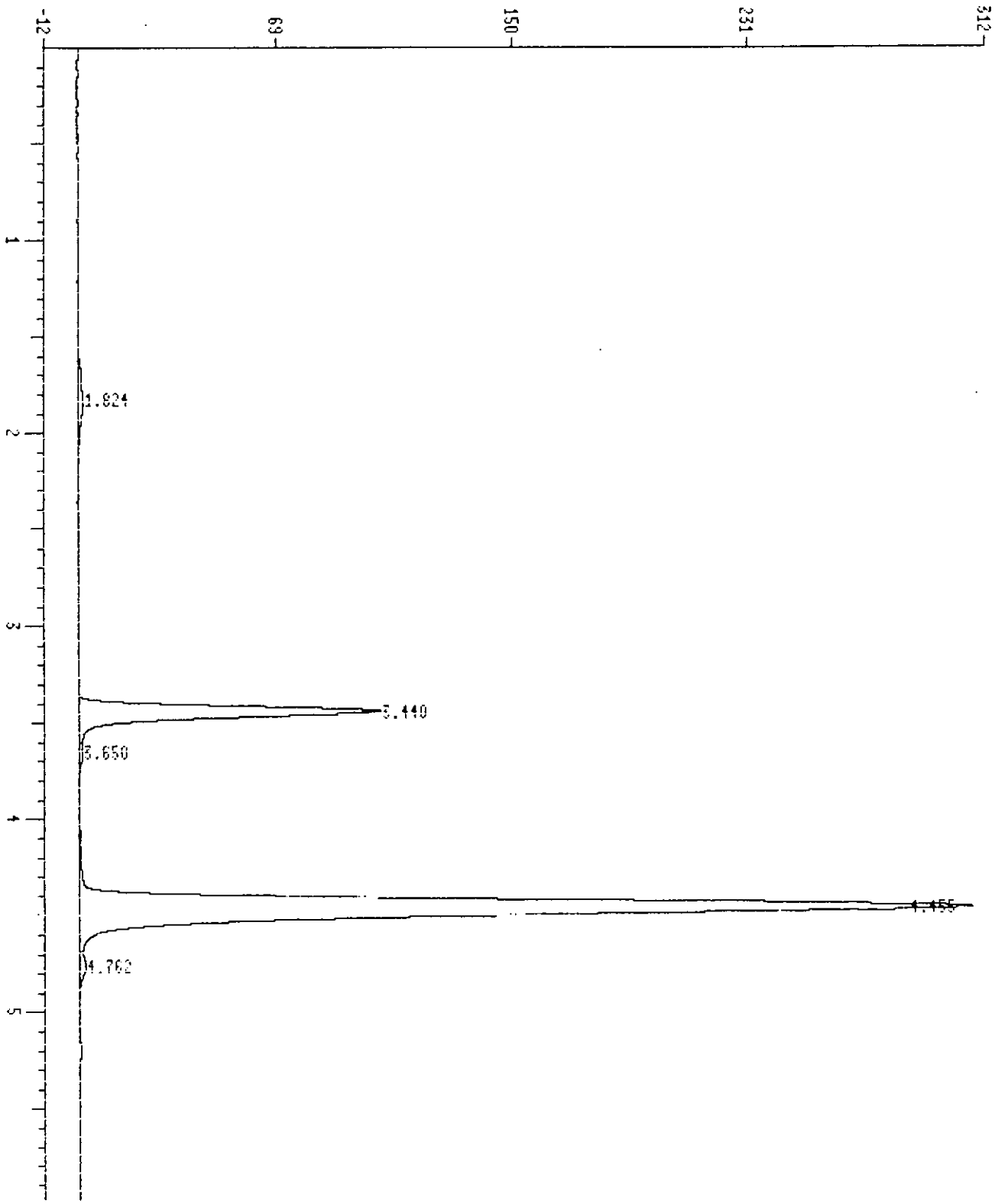
Report by Signal

Operator: JCP 1 Apr 92 5:12 pm
Method File Name : DNPHIII.M
Sample Info : #10
Misc Info:
Integration File Name : DATA:0401A14A.I
consisting of channels : 1. A 360,4 550,100 of 0401A14A.D
Sequence Index: 1 Bottle Number : 14 Repetition Number: 1

A 360,4 550,100 of 0401A14A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.829	BB	32.7223	1.5540	1.49	100.00	0.285	0.99
3.439	BV	429.56	104.63	19.57	100.00	0.064	0.85
3.546	VB	8.7112	1.2693	0.40	100.00	0.114	0.63
4.454	BV	1708.03	308.12	77.82	100.00	0.086	0.81
4.761	VB	15.7479	2.3100	0.72	100.00	0.104	0.94

1: LC A 350,4 550,100 of 0401A14B.D



*** Area Percent ***

Report by Signal

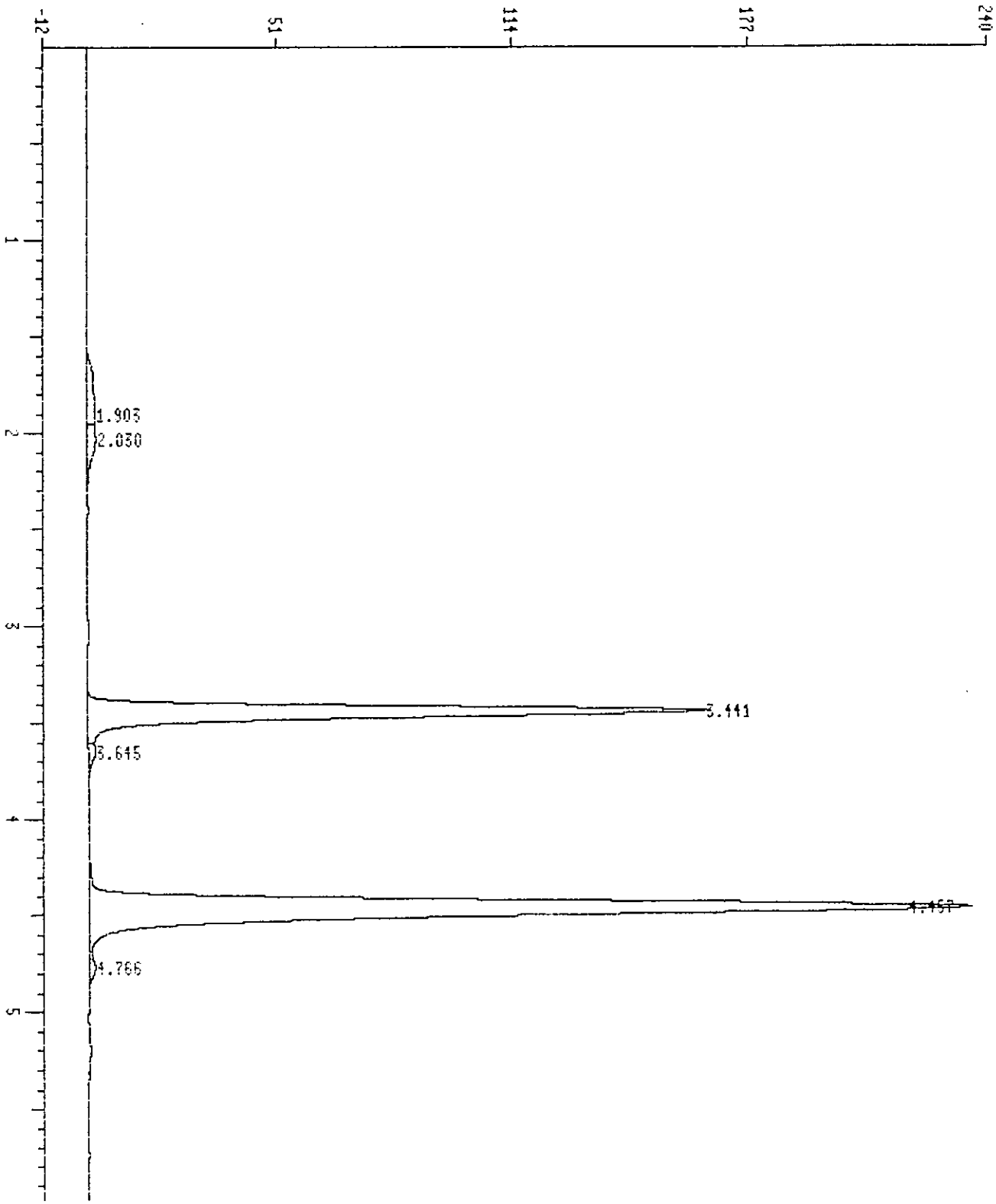
Operator: JCP 1 Apr 92 6:21 pm
Method File Name : DNPHIII.M
Sample Info : #10
Misc Info:
Integration File Name : DATA:0401A14B.I
consisting of channels : 1. A 360,4 550,100 of 0401A14B.D
Sequence Index: 1 Bottle Number : 14 Repetition Number: 2

A 360,4 550,100 of 0401A14B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.824	BB	33.6490	1.6031	1.53	100.00	0.279	0.97
3.440	BV	427.90	104.34	19.48	100.00	0.064	0.84
3.650	VB	8.0130	1.2474	0.36	100.00	0.107	0.70
4.455	BV	1710.77	308.03	77.90	100.00	0.086	0.81
4.762	VB	15.7526	2.2548	0.72	100.00	0.105	0.91

65

1: LC A 360,4 550,100 of 0401A16A.D



66

*** Area Percent ***

Report by Signal

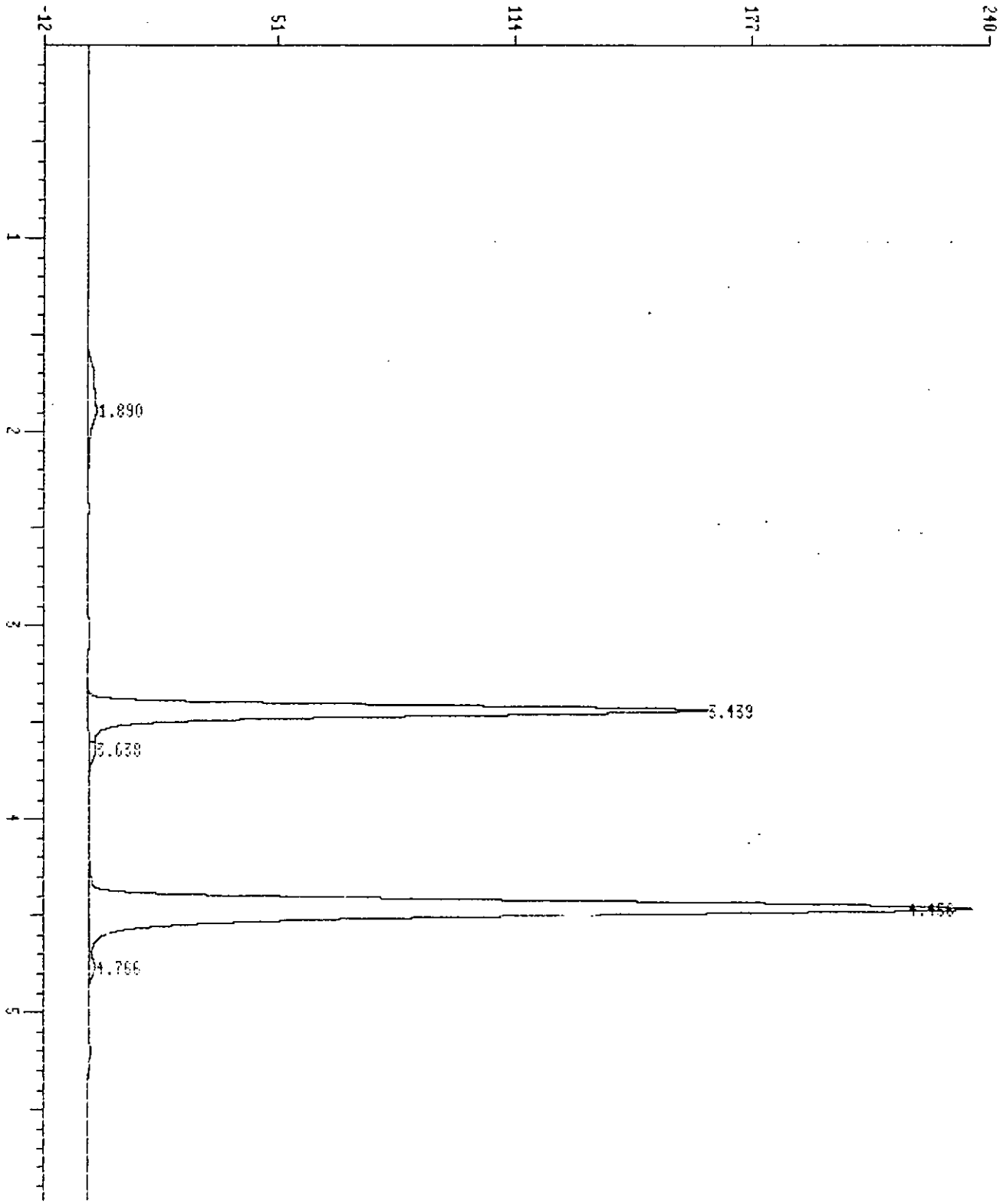
Operator: JCP 1 Apr 92 5:47 pm
Method File Name : DNPHIII.M
Sample Info : #12
Misc Info:
Integration File Name : DATA:0401A15A.I
consisting of channels : 1. A 360,4 550,100 of 0401A15A.D
Sequence Index: 1 Bottle Number : 15 Repetition Number: 1

A 360,4 550,100 of 0401A15A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.903	BV	35.4209	2.2098	1.76	100.00	0.275	5.12
2.030	VV	27.9965	2.3370	1.35	100.00	0.170	0.57
3.441	BV	677.47	165.49	32.71	100.00	0.054	0.84
3.645	VB	12.1080	1.8112	0.58	100.00	0.111	0.59
4.457	BV	1305.58	235.75	63.04	100.00	0.085	0.81
4.765	VB	11.6111	1.5753	0.56	100.00	0.107	0.91

67

1: LC A 360,4 550,100 of 0401A16B.D



*** Area Percent ***

Report by Signal

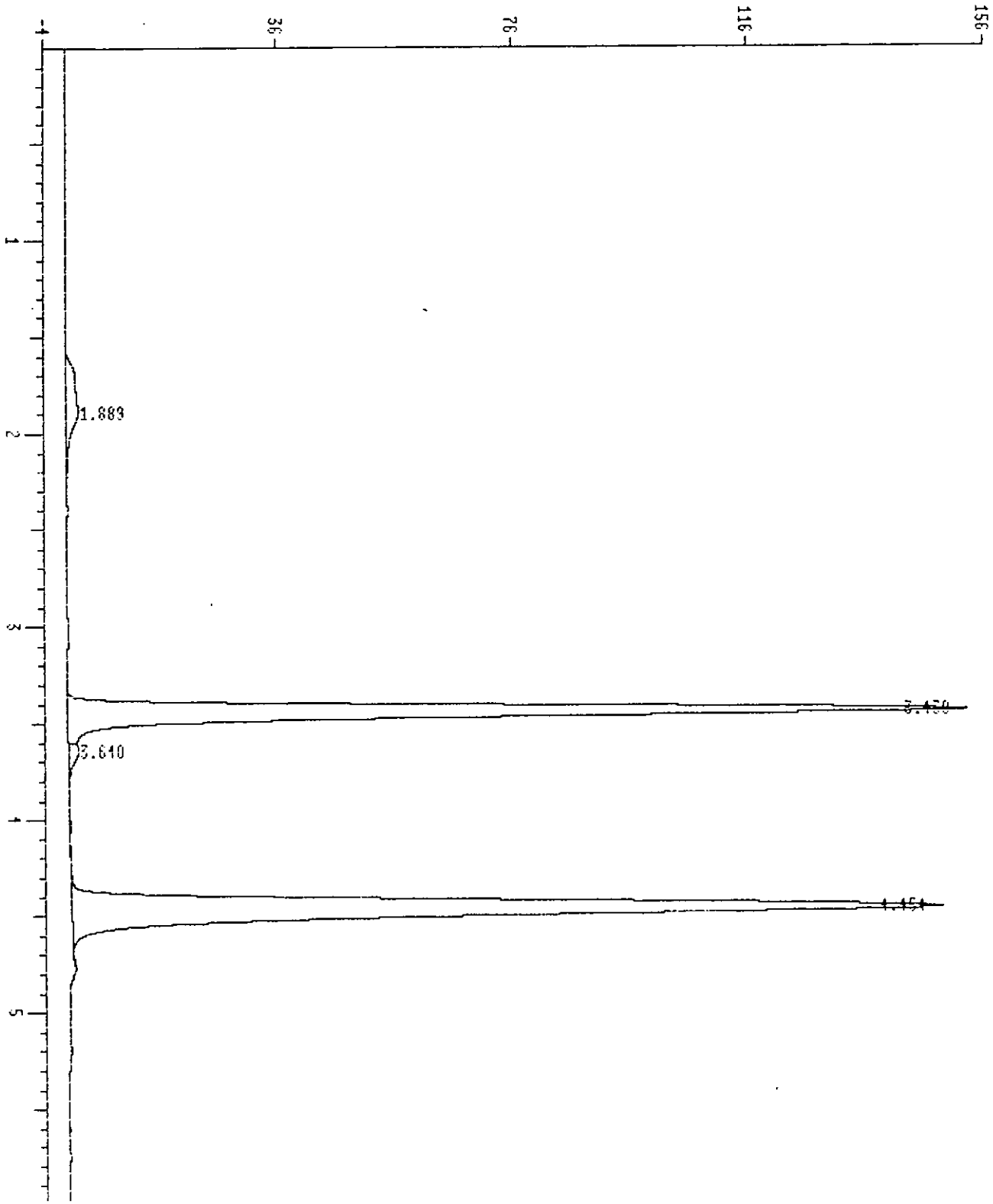
Operator: JCP 1 Apr 92 6:56 pm
Method File Name : DNPHIII.M
Sample Info : #12
Misc Info:
Integration File Name : DATA:0401A16B.I
consisting of channels : 1. A 360,4 550,100 of 0401A16B.D
Sequence Index: 1 Bottle Number : 16 Repetition Number: 2

A 360,4 550,100 of 0401A16B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.890	BV	49.0373	2.4354	2.39	100.00	0.264	1.59
3.439	BV	674.13	164.93	32.87	100.00	0.064	0.84
3.638	VB	12.8757	1.8270	0.63	100.00	0.117	0.48
4.456	BV	1303.58	235.57	63.55	100.00	0.085	0.80
4.766	VB	11.5137	1.6975	0.56	100.00	0.104	1.01

69

1: LC A 360,4 550,100 of 0401A17A.D



20

*** Area Percent ***

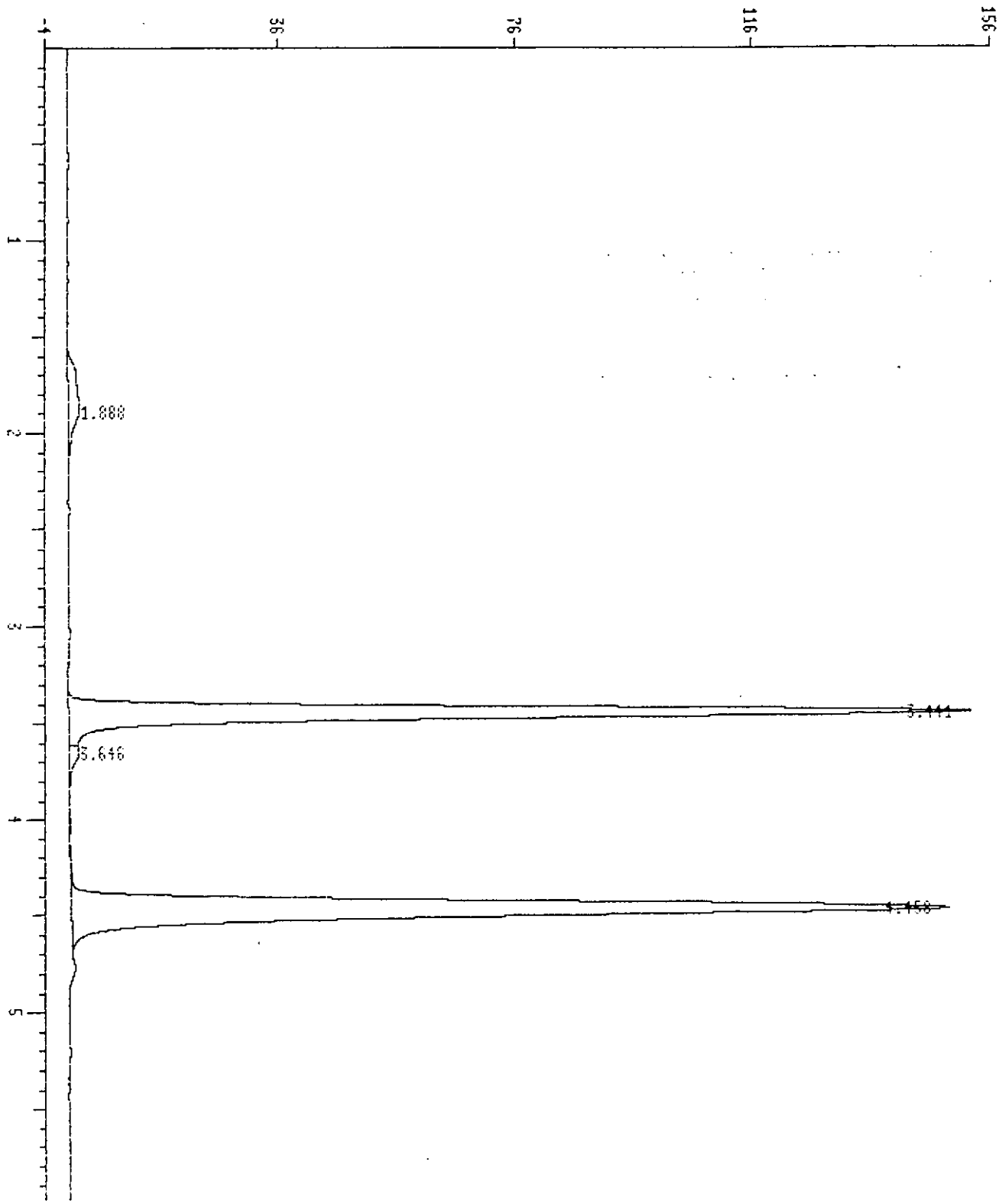
Report by Signal

Operator: JCP 1 Apr 92 7:04 pm
Method File Name : DNPHIII.M
Sample Info : #13
Misc Info:
Integration File Name : DATA:0401A17A.I
consisting of channels : 1. A 360,4 550,100 of 0401A17A.D
Sequence Index: 1 Bottle Number : 17 Repetition Number: 1

A 360,4 550,100 of 0401A17A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.889	BB	42.3264	2.1113	2.84	100.00	0.262	1.94
3.438	BV	626.42	153.12	41.98	100.00	0.064	0.85
3.640	VB	11.3284	1.6996	0.76	100.00	0.111	0.55
4.454	BV	812.08	148.54	54.42	100.00	0.085	0.81

1: LC A 360,4 550,100 of 0401A17B.D



22

*** Area Percent ***

Report by Signal

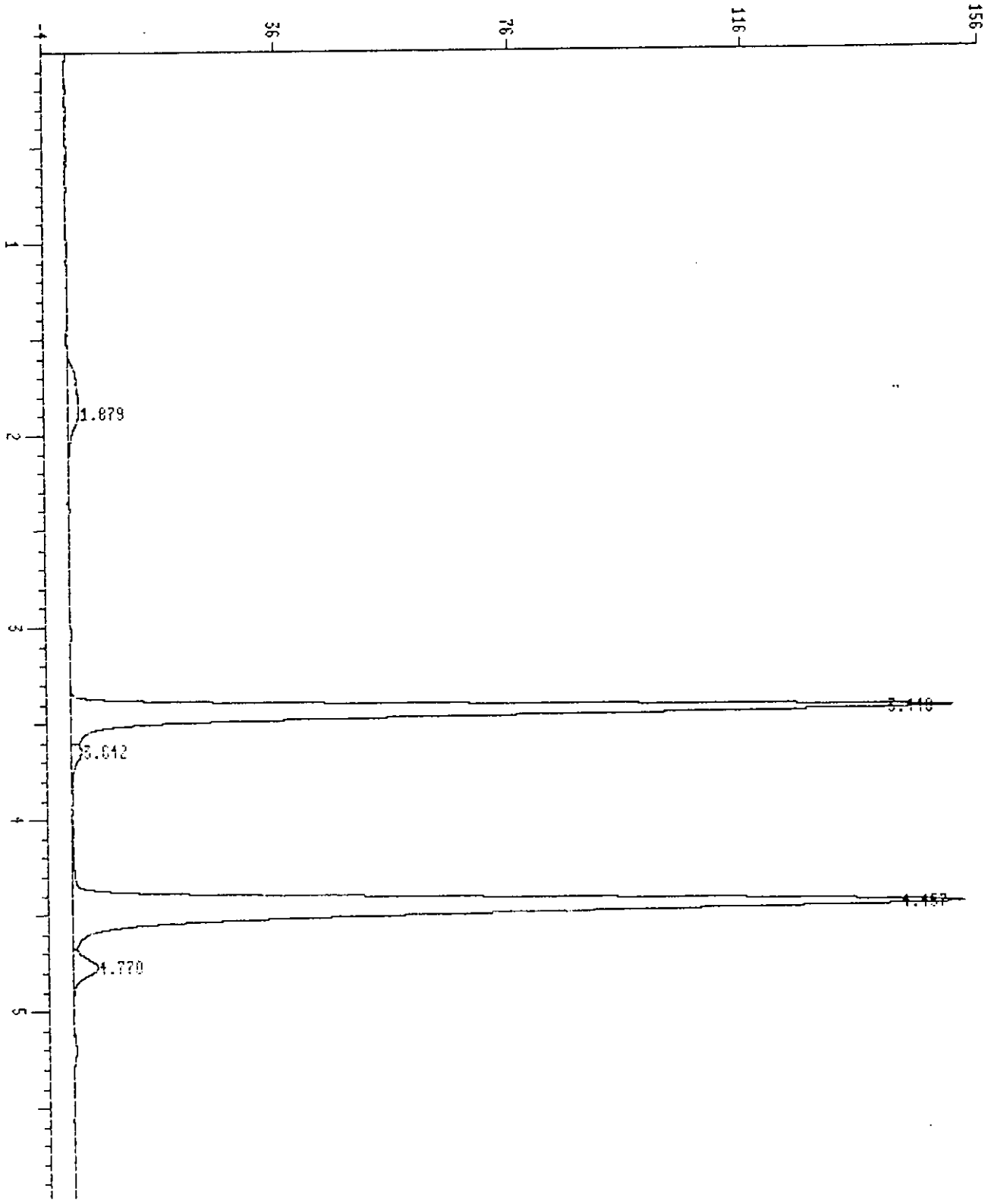
Operator: JCP 1 Apr 92 7:13 pm
Method File Name : DNPHIII.M
Sample Info : #13
Misc Info:
Integration File Name : DATA:0401A17B.I
consisting of channels : 1. A 360,4 550,100 of 0401A17B.D
Sequence Index: 1 Bottle Number : 17 Repetition Number: 2

A 360,4 550,100 of 0401A17B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.888	BB	38.3052	1.8955	2.57	100.00	0.256	2.17
3.441	BV	627.21	153.24	42.08	100.00	0.064	0.84
3.645	VB	11.3908	1.6947	0.76	100.00	0.112	0.50
4.458	BV	813.44	148.56	54.58	100.00	0.085	0.81

73

1: LC A 350,4 550,100 of 0401A18A.D



*** Area Percent ***

Report by Signal

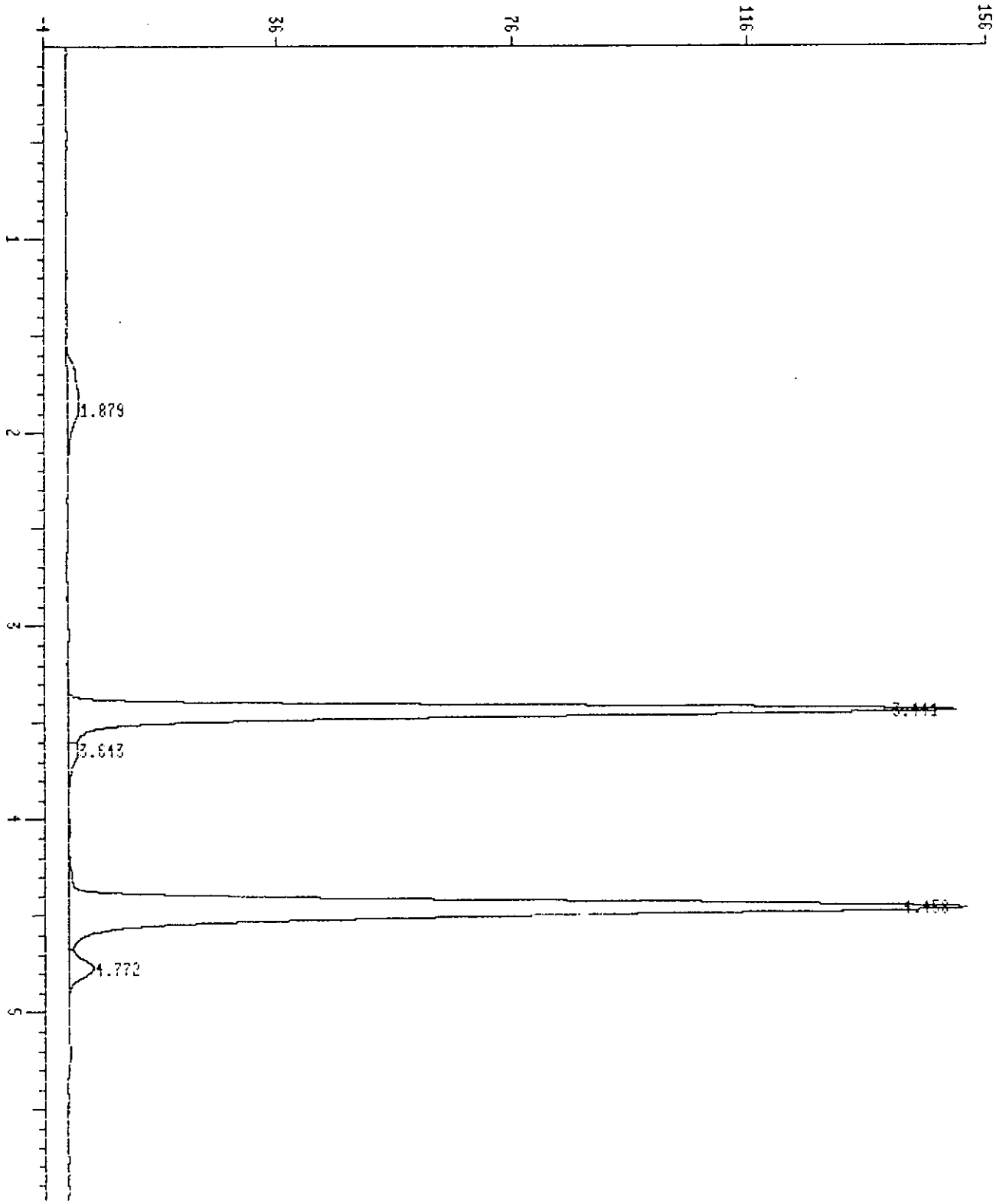
Operator: JCP 1 Apr 92 7:22 pm
Method File Name : DNPHIII.M
Sample Info : #14
Misc Info:
Integration File Name : DATA:0401A18A.I
consisting of channels : 1. A 360,4 550,100 of 0401A18A.D
Sequence Index: 1 Bottle Number : 18 Repetition Number: 1

A 360,4 550,100 of 0401A18A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.879	BB	38.9650	1.9683	2.53	100.00	0.251	1.96
3.440	BV	616.14	150.76	40.06	100.00	0.064	0.85
3.642	VB	11.7283	1.7062	0.76	100.00	0.115	0.55
4.457	BV	843.03	152.42	54.81	100.00	0.085	0.81
4.770	VB	28.1867	4.2445	1.83	100.00	0.102	1.00

75

1: LC A 360,4 550,100 of 0401A18B.D



*** Area Percent ***

Report by Signal

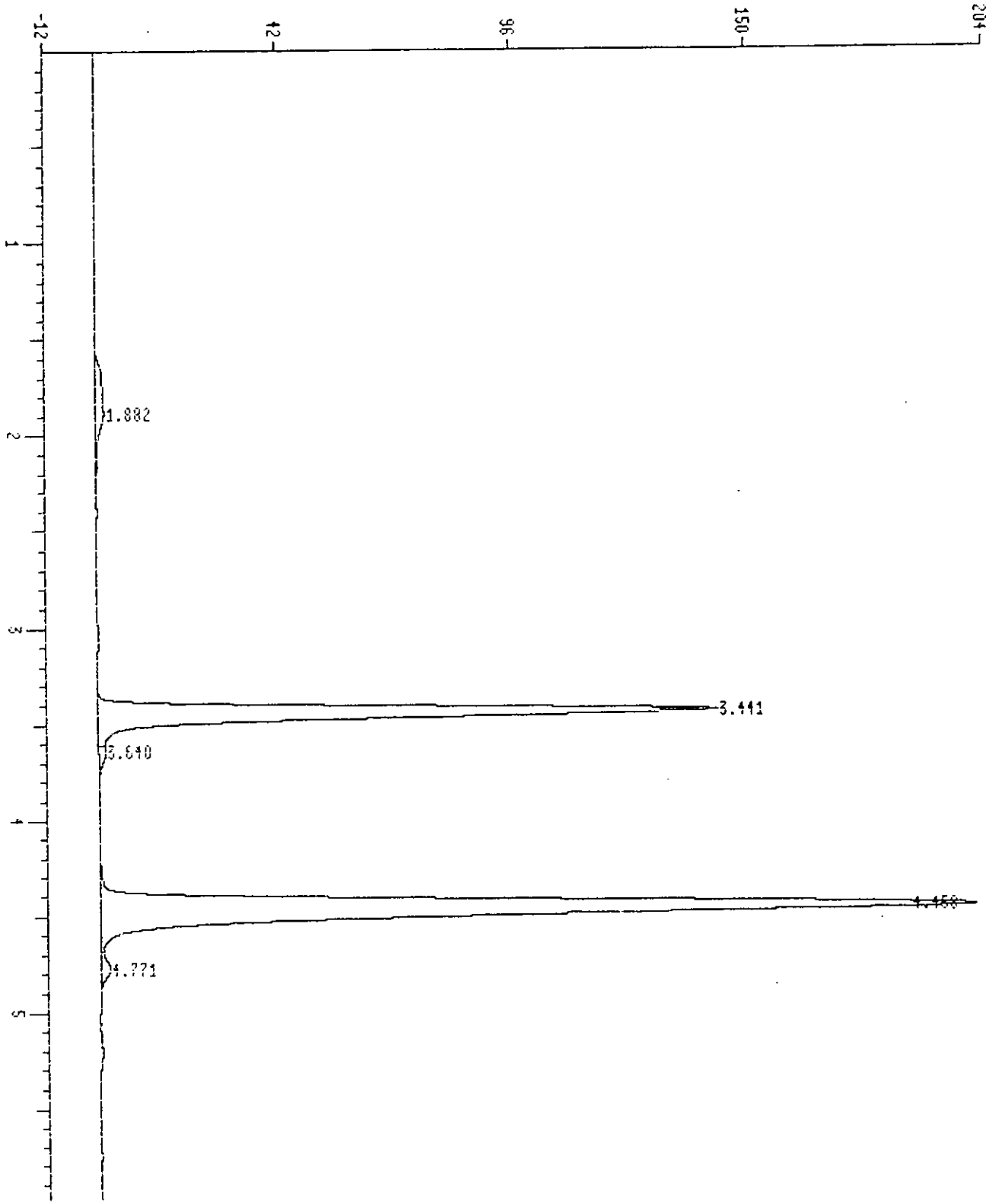
Operator: JCP 1 Apr 92 7:31 pm
Method File Name : DNPHIII.M
Sample Info : #14
Misc Info:
Integration File Name : DATA:0401A18B.I
consisting of channels : 1. A 360,4 550,100 of 0401A18B.D
Sequence Index: 1 Bottle Number : 18 Repetition Number: 2

A 360,4 550,100 of 0401A18B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.879	BB	38.4792	1.9269	2.49	100.00	0.255	2.05
3.441	BV	618.89	151.21	40.08	100.00	0.064	0.85
3.643	VB	11.9751	1.6840	0.78	100.00	0.119	0.48
4.458	BV	846.44	152.74	54.82	100.00	0.086	0.81
4.772	VB	28.3043	4.2548	1.83	100.00	0.103	1.04

77

1: LC A 350,4 550,100 of 0401A19A.D



*** Area Percent ***

Report by Signal

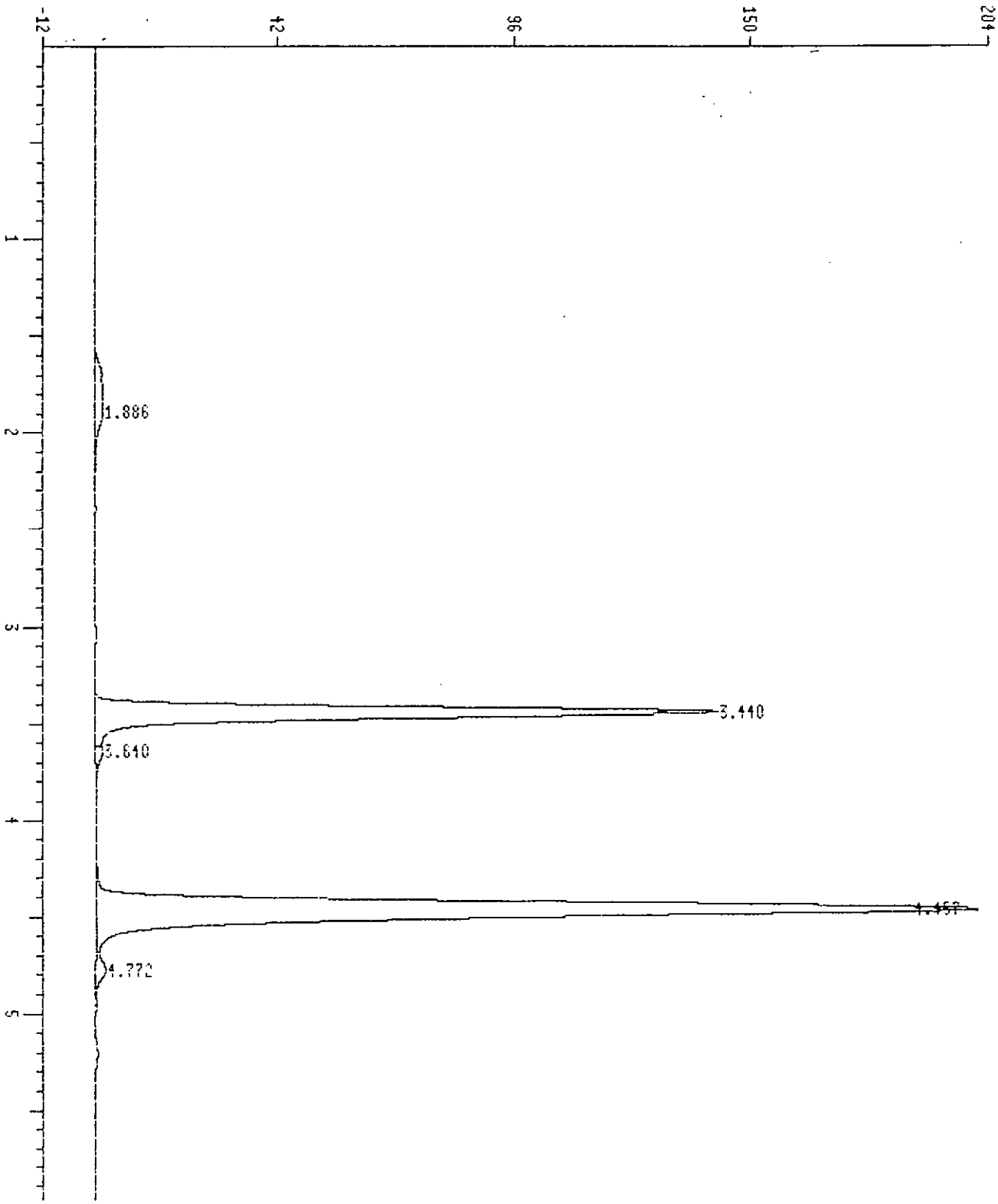
Operator: JCP 1 Apr 92 7:39 pm
Method File Name : DNPHIII.M
Sample Info : #15
Misc Info:
Integration File Name : DATA:0401A19A.I
consisting of channels : 1. A 360,4 550,100 of 0401A19A.D
Sequence Index: 1 Bottle Number : 19 Repetition Number: 1

A 360,4 550,100 of 0401A19A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.882	BB	38.2409	1.8925	2.17	100.00	0.260	2.05
3.441	BV	585.10	142.53	33.20	100.00	0.064	0.85
3.640	VB	11.1569	1.6319	0.63	100.00	0.114	0.43
4.458	BV	1112.79	201.87	63.14	100.00	0.085	0.80
4.771	VB	15.1438	2.2947	0.86	100.00	0.101	0.98

79

1: LC A 360,4 550,100 of 0401A198.D



*** Area Percent ***

Report by Signal

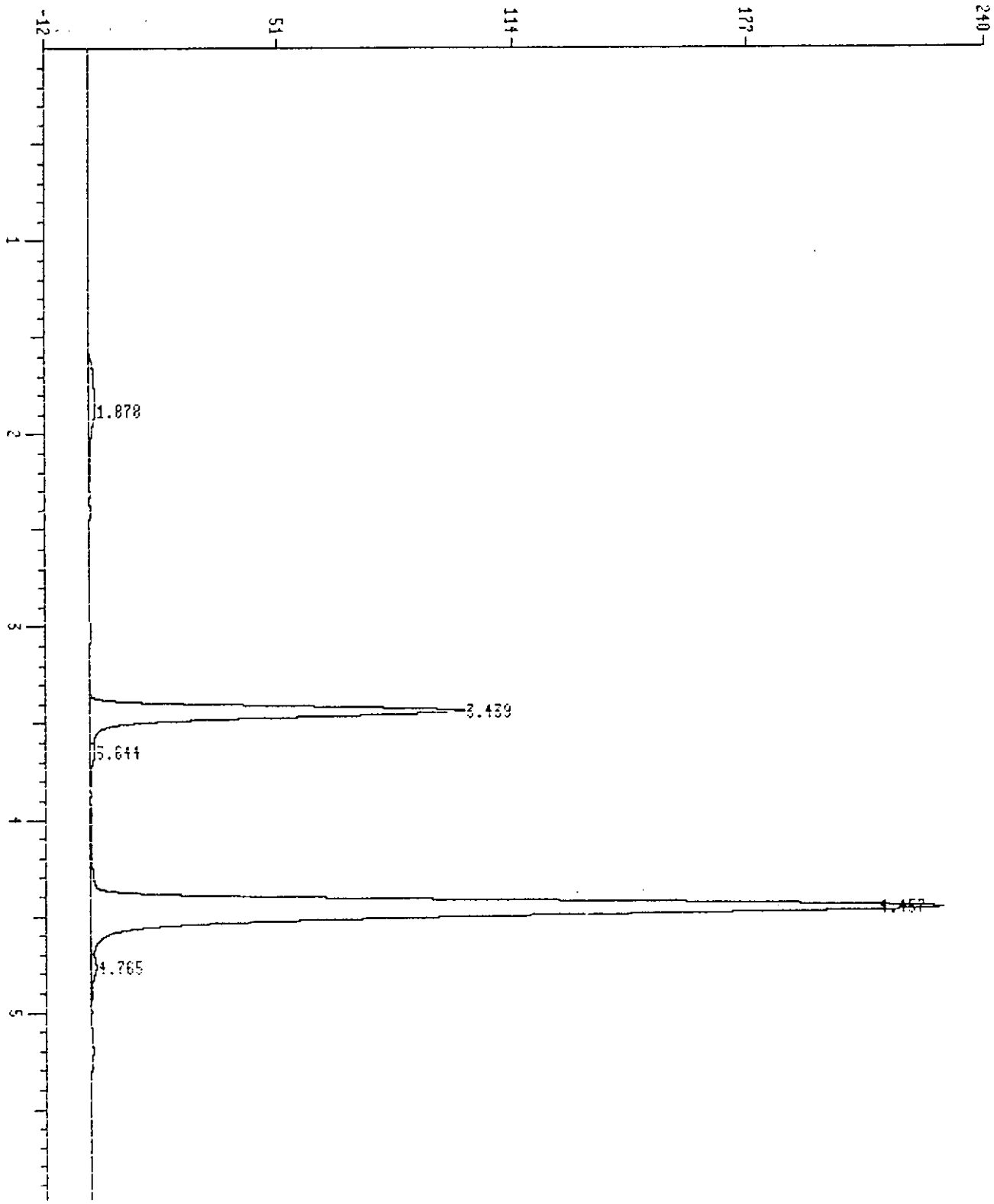
Operator: JCP 1 Apr 92 7:48 pm
Method File Name : DNPHIII.M
Sample Info : #15
Misc Info:
Integration File Name : DATA:0401A19B.I
consisting of channels : 1. A 360,4 550,100 of 0401A19B.D
Sequence Index: 1 Bottle Number : 19 Repetition Number: 2

A 360,4 550,100 of 0401A19B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.886	BB	39.6691	1.9232	2.25	100.00	0.260	2.12
3.440	BV	582.71	142.26	33.04	100.00	0.064	0.84
3.640	VB	9.1882	1.5311	0.52	100.00	0.100	0.39
4.457	BV	1116.27	201.90	63.29	100.00	0.085	0.81
4.772	VB	15.8644	2.2947	0.90	100.00	0.107	1.08

8

1: LC A 350,4 550,100 of 0401A20A.D



28

*** Area Percent ***

Report by Signal

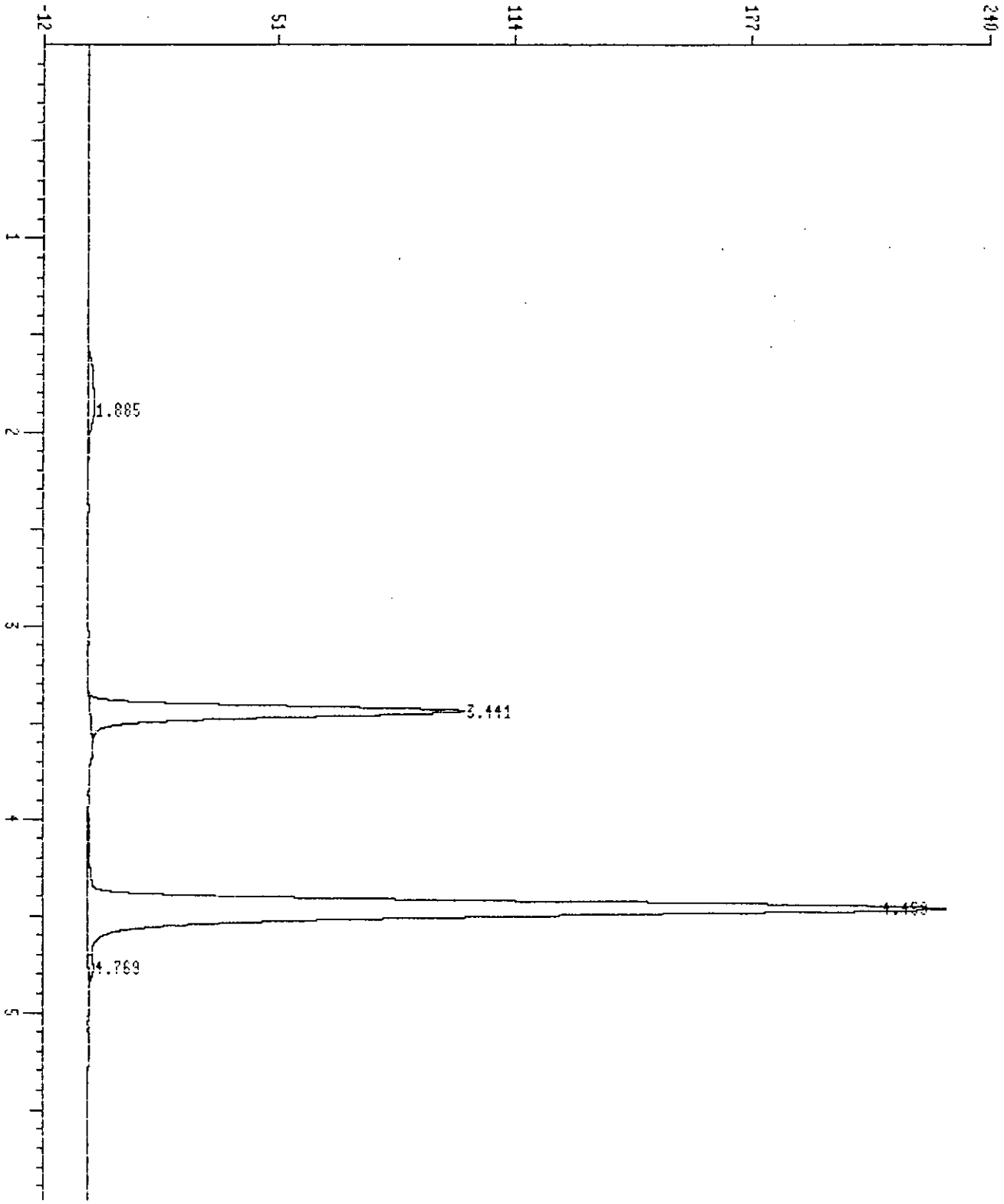
Operator: JCP 1 Apr 92 7:57 pm
Method File Name : DNPHIII.M
Sample Info : #16
Misc Info:
Integration File Name : DATA:0401A20A.I
consisting of channels : 1. A 360,4 550,100 of 0401A20A.D
Sequence Index: 1 Bottle Number : 20 Repetition Number: 1

A 360,4 550,100 of 0401A20A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.878	BV	32.8596	1.5208	1.90	100.00	0.307	1.66
3.439	BV	413.42	100.92	23.91	100.00	0.064	0.85
3.644	VB	7.9319	1.1810	0.46	100.00	0.112	0.69
4.457	BV	1265.13	228.70	73.17	100.00	0.085	0.81
4.765	VB	9.7110	1.3747	0.56	100.00	0.107	0.85

83

1: LC A 360,4 550,100 of 0401A20B.D



43

*** Area Percent ***

Report by Signal

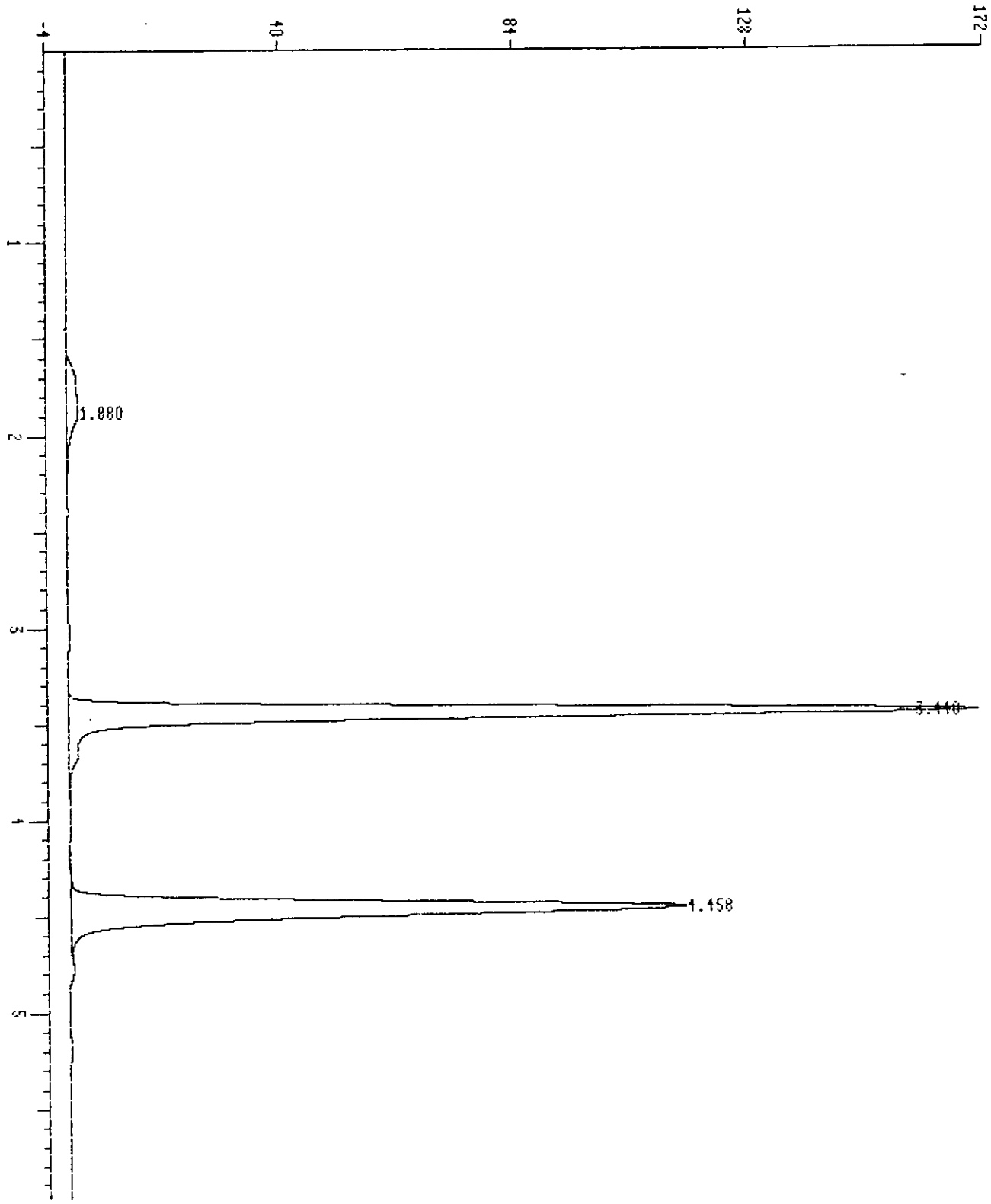
Operator: JCP 1 Apr 92 8:05 pm
Method File Name : DNPHIII.M
Sample Info : #15
Misc Info:
Integration File Name : DATA:0401A20B.I
consisting of channels : 1. A 360,4 550,100 of 0401A20B.D
Sequence Index: 1 Bottle Number : 20 Repetition Number: 2

A 360,4 550,100 of 0401A20B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.885	BB	33.2975	1.5468	1.95	100.00	0.270	1.93
3.441	BV	402.76	100.26	23.58	100.00	0.063	0.88
4.459	BV	1262.36	228.61	73.92	100.00	0.085	0.81
4.769	VB	9.3047	1.3337	0.54	100.00	0.102	0.81

85

1: LC A 360,4 550,100 of 0401A21A.D



98

*** Area Percent ***

Report by Signal

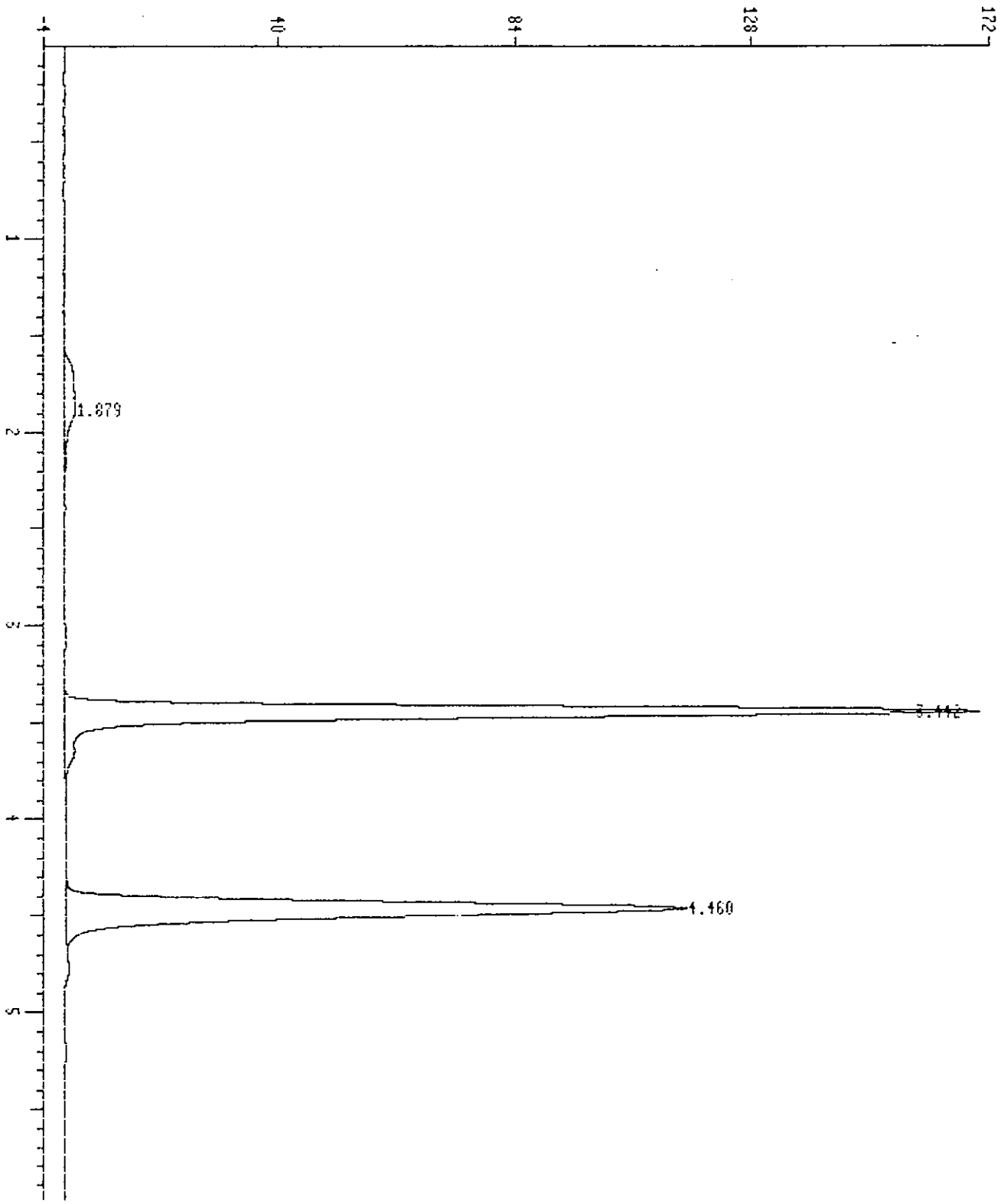
Operator: JCP 1 Apr 92 8:14 pm
Method File Name : DNPHIII.M
Sample Info : #17
Misc Info:
Integration File Name : DATA:0401A21A.I
consisting of channels : 1. A 360,4 550,100 of 0401A21A.D
Sequence Index: 1 Bottle Number : 21 Repetition Number: 1

A 360,4 550,100 of 0401A21A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.880	BB	43.5141	2.1369	3.14	100.00	0.262	1.94
3.440	BB	709.77	170.70	51.24	100.00	0.065	0.82
4.458	BV	631.97	115.39	45.62	100.00	0.085	0.81

87

1: LC A 350,4 550,100 of 0401A21B.D



88

*** Area Percent ***

Report by Signal

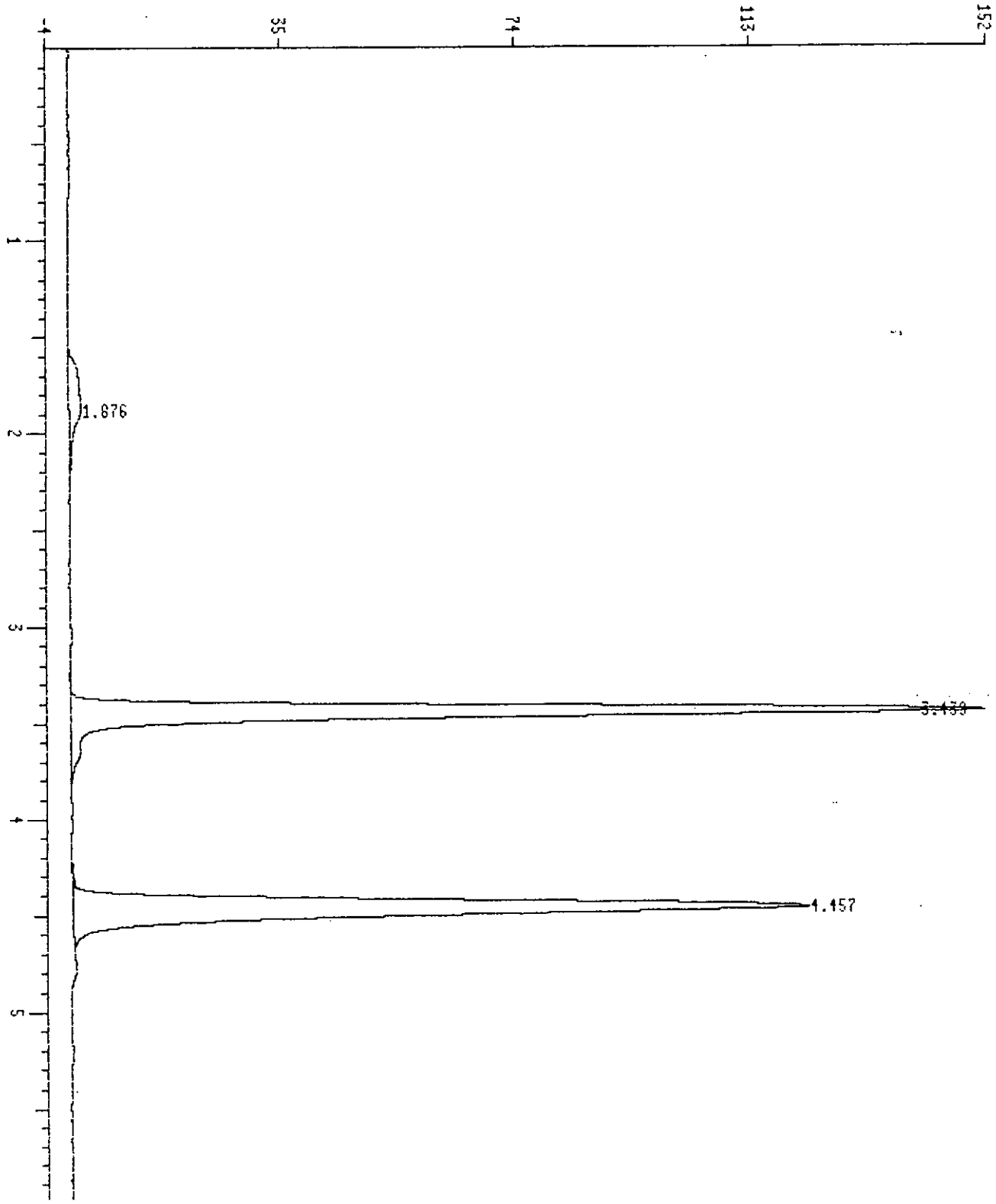
Operator: JCP 1 Apr 92 8:23 pm
Method File Name : DNPHIII.M
Sample Info : #17
Misc Info:
Integration File Name : DATA:0401A21B.I
consisting of channels : 1. A 360,4 550,100 of 0401A21B.D
Sequence Index: 1 Bottle Number : 21 Repetition Number: 2

A 360,4 550,100 of 0401A21B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.879	BB	46.9403	2.1862	3.39	100.00	0.274	1.60
3.442	BB	707.59	170.19	51.09	100.00	0.065	0.82
4.460	BV	630.53	115.32	45.52	100.00	0.085	0.81

89

1: LC A 360,4 550,100 of 0401A22A.D



90

*** Area Percent ***

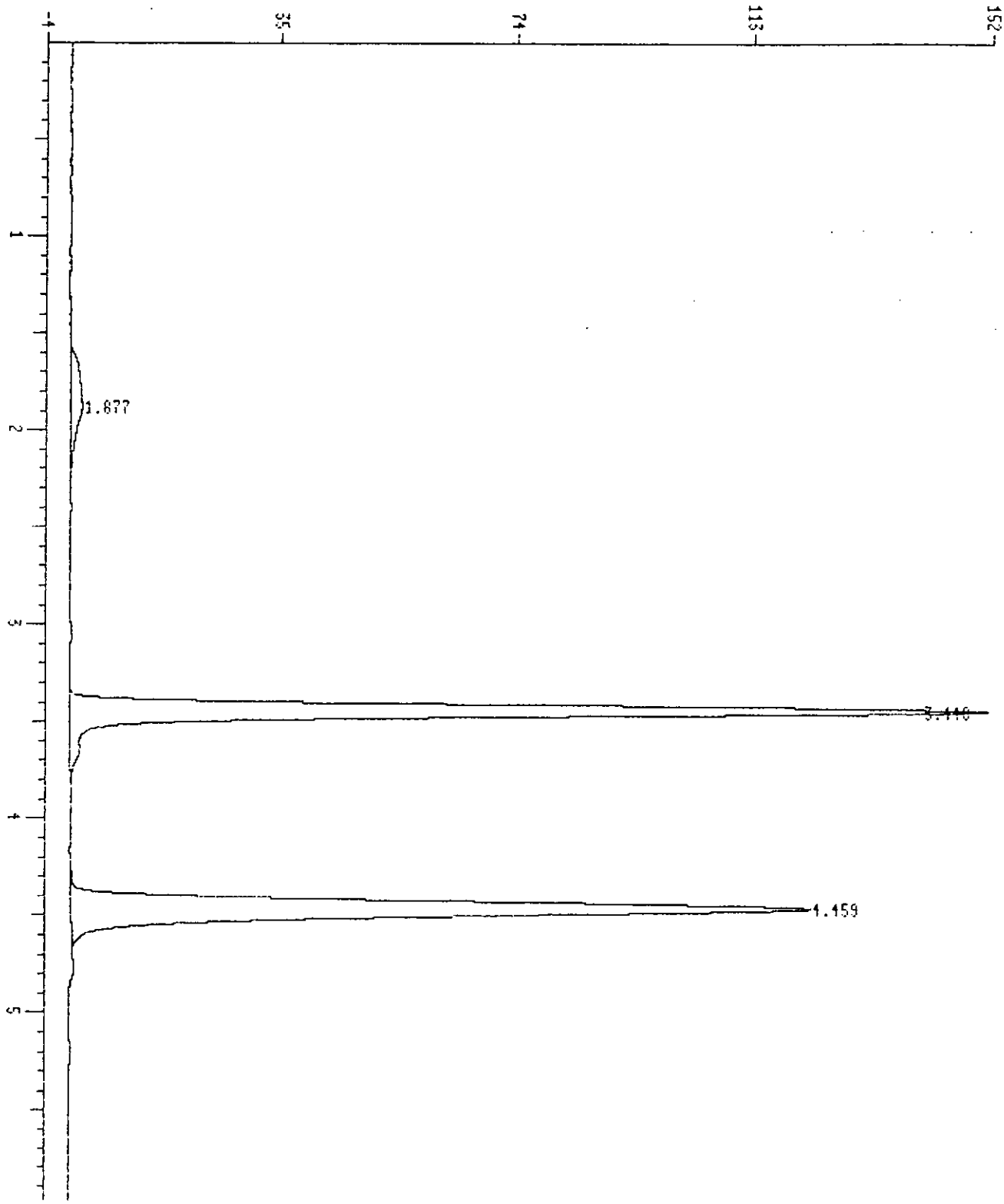
Report by Signal

Operator: JCP 1 Apr 92 8:32 pm
Method File Name : DNPHIII.M
Sample Info : #18
Misc Info:
Integration File Name : DATA:0401A22A.I
consisting of channels : 1. A 360,4 550,100 of 0401A22A.D
Sequence Index: 1 Bottle Number : 22 Repetition Number: 1

A 360,4 550,100 of 0401A22A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.876	BB	40.2984	1.8980	3.00	100.00	0.272	1.83
3.439	BB	634.27	152.18	47.18	100.00	0.065	0.82
4.457	BV	669.66	122.45	49.82	100.00	0.085	0.81

1: LC A 360,4 550,100 of 0401A22B.D



*** Area Percent ***

Report by Signal

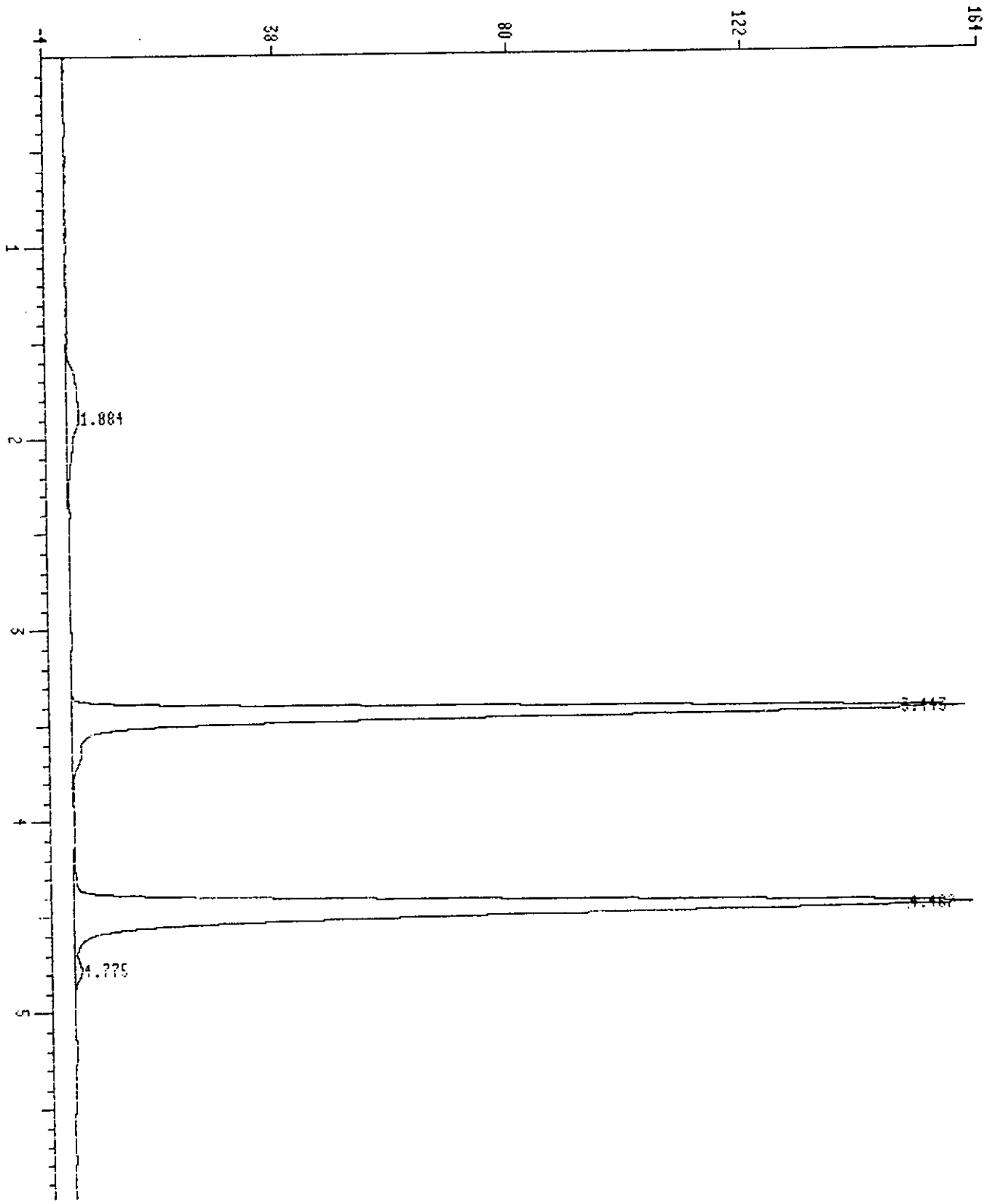
Operator: JCP 1 Apr 92 8:40 pm
Method File Name : DNPHIII.M
Sample Info : #18
Misc Info:
Integration File Name : DATA:0401A22B.I
consisting of channels : 1. A 360,4 550,100 of 0401A22B.D
Sequence Index: 1 Bottle Number : 22 Repetition Number: 2

A 360,4 550,100 of 0401A22B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.877	BV	47.3828	2.0565	3.52	100.00	0.299	1.31
3.440	BV	630.56	152.00	46.86	100.00	0.065	0.81
4.459	BV	667.80	122.29	49.62	100.00	0.085	0.81

43

1: LC A 350,4 550,100 of 0401A23A.D



7b

*** Area Percent ***

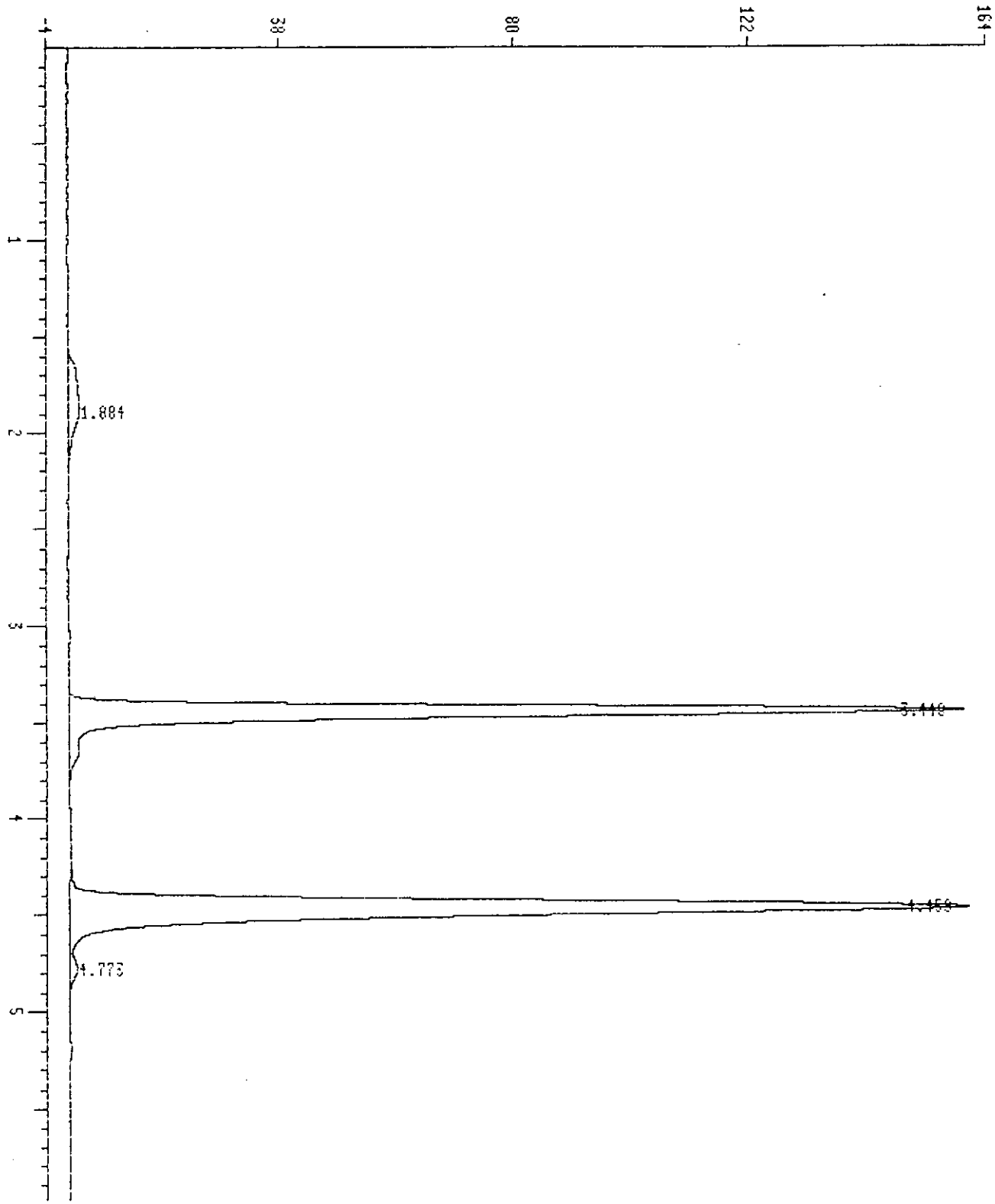
Report by Signal

Operator: JCP 1 Apr 92 8:49 pm
Method File Name : DNPHIII.M
Sample Info : #19
Misc Info:
Integration File Name : DATA:0401A23A.I
consisting of channels : 1. A 360,4 550,100 of 0401A23A.D
Sequence Index: 1 Bottle Number : 23 Repetition Number: 1

A 360,4 550,100 of 0401A23A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.884	BV	49.9253	2.1337	3.09	100.00	0.299	1.35
3.443	BB	667.98	160.63	41.28	100.00	0.065	0.81
4.462	BV	891.83	161.44	55.11	100.00	0.085	0.80
4.775	VB	8.6186	1.2639	0.53	100.00	0.104	1.03

1: LC A 360,4 550,100 of 0401A23B.D



96

*** Area Percent ***

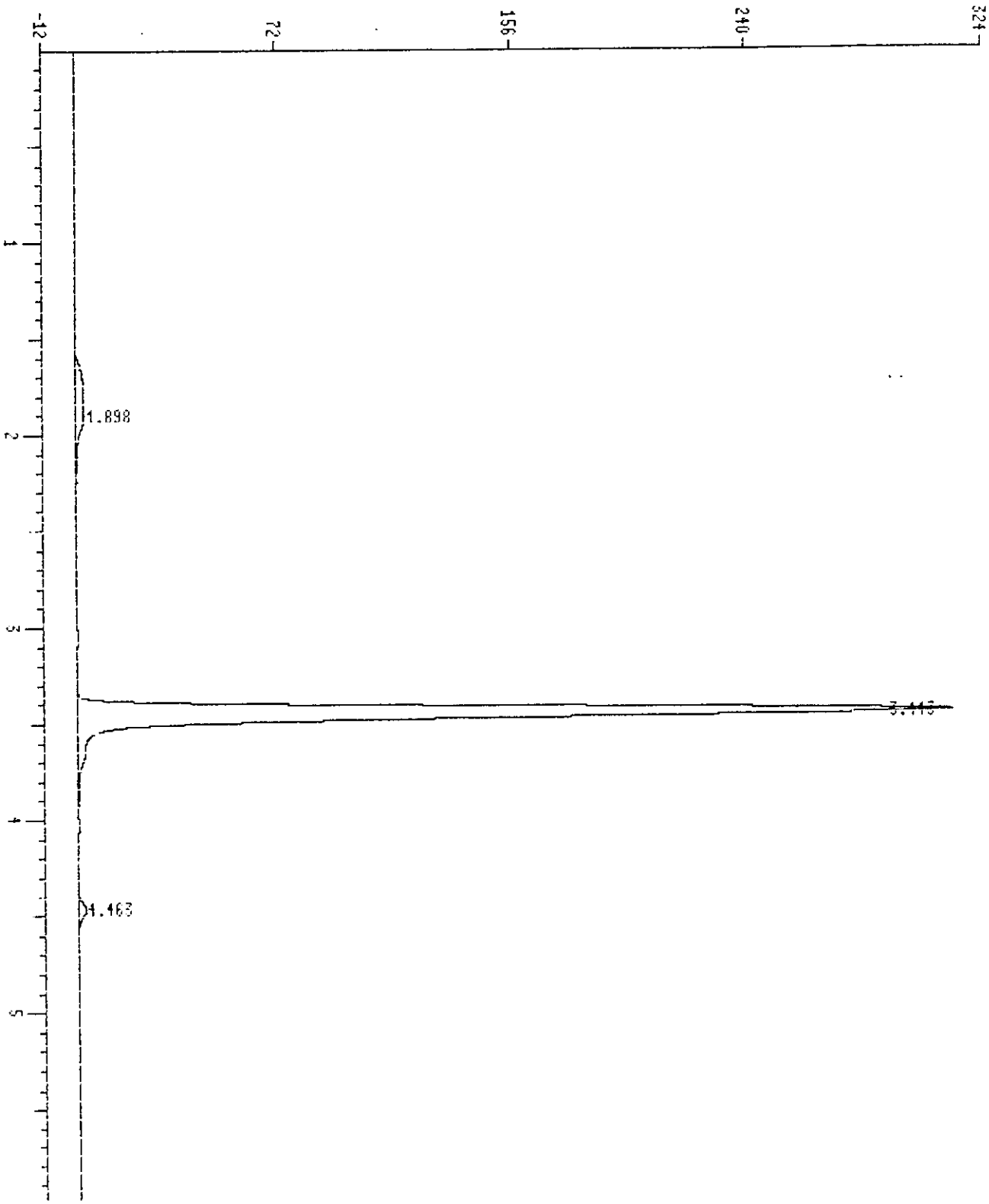
Report by Signal

Operator: JCP 1 Apr 92 8:58 pm
Method File Name : DNPHIII.M
Sample Info : #19
Misc Info:
Integration File Name : DATA:0401A23B.I
consisting of channels : 1. A 360,4 550,100 of 0401A23B.D
Sequence Index: 1 Bottle Number : 23 Repetition Number: 2

A 360,4 550,100 of 0401A23B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.884	BV	44.5711	2.1298	2.77	100.00	0.267	1.73
3.440	BB	668.43	150.70	41.48	100.00	0.065	0.91
4.459	BV	889.07	151.22	55.19	100.00	0.085	0.80
4.773	VB	9.2183	1.3335	0.57	100.00	0.109	0.90

1: LC A 350,4 550,100 of 0401A24A.D



98

*** Area Percent ***

Report by Signal

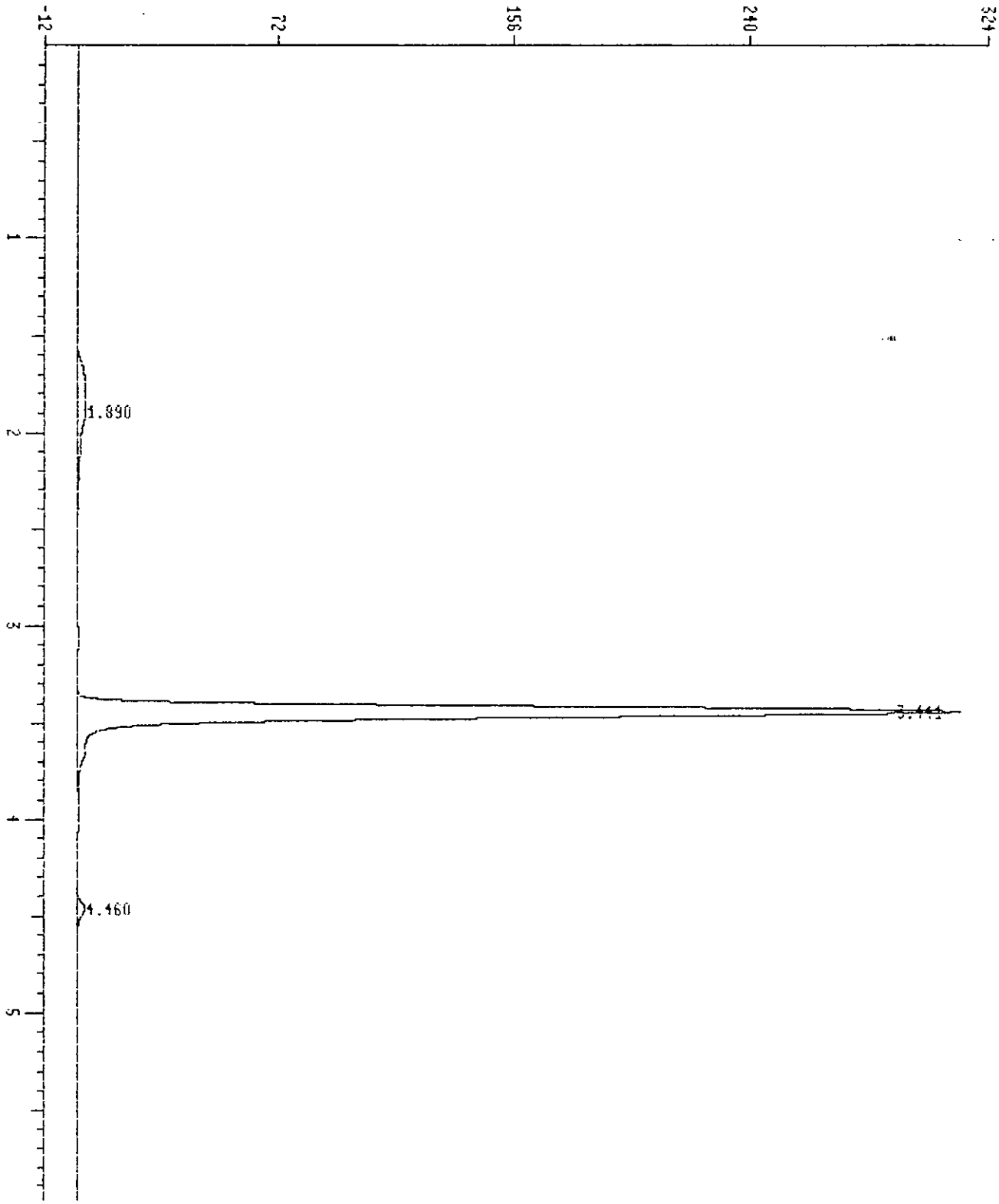
Operator: JCP 1 Apr 92 9:07 pm
Method File Name : DNPHIII.M
Sample Info : #20
Misc Info:
Integration File Name : DATA:0401A24A.I
consisting of channels : 1. A 350,4 550,100 of 0401A24A.D
Sequence Index: 1 Bottle Number : 24 Repetition Number: 1

A 350,4 550,100 of 0401A24A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.898	BV	69.4748	3.1373	5.00	100.00	0.286	1.85
3.443	BV	1304.02	313.72	93.84	100.00	0.065	0.82
4.453	BB	16.1153	2.9974	1.16	100.00	0.087	0.80

98

1: LC A 360,4 550,100 of 0401A24B.D



100

*** Area Percent ***

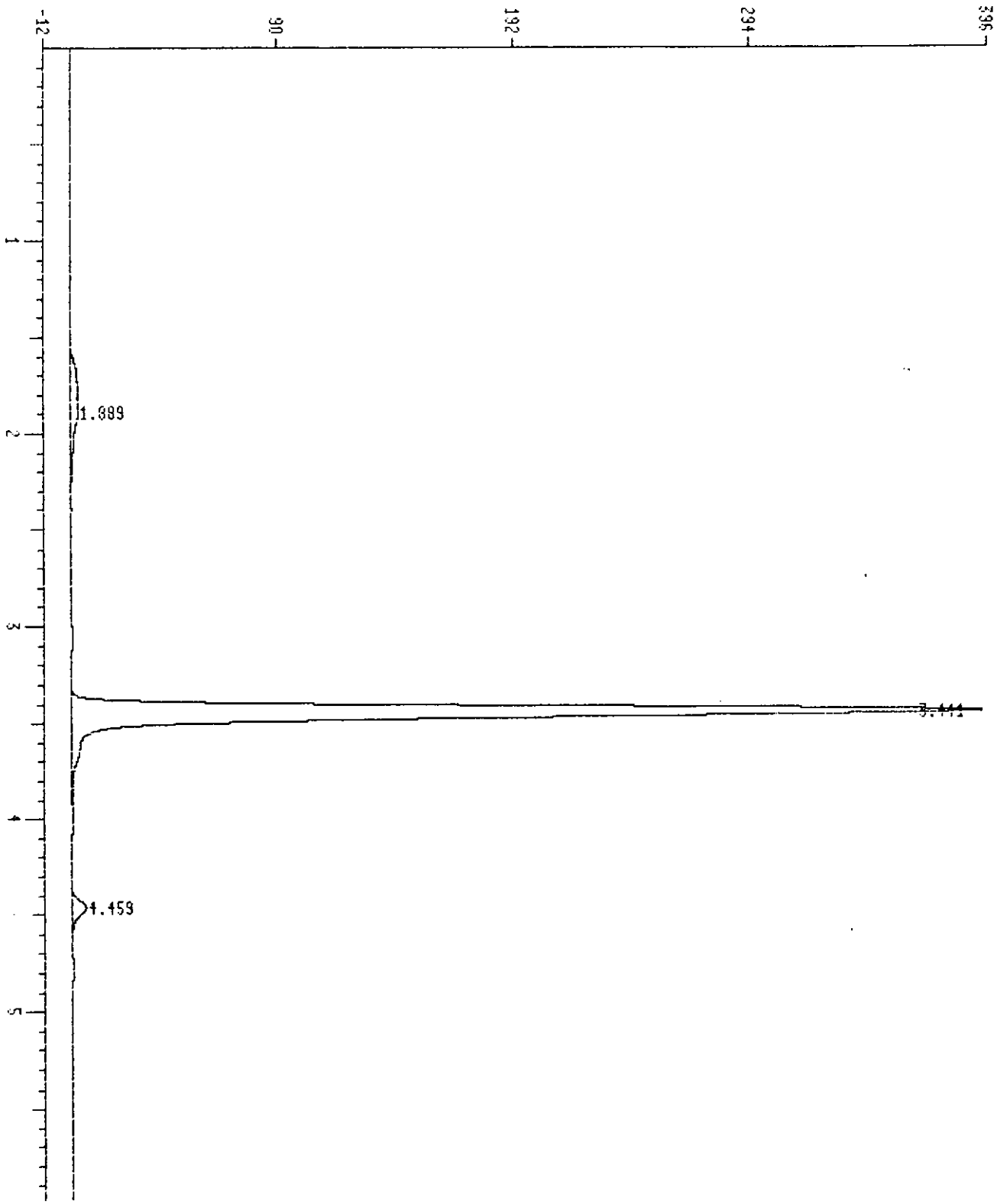
Report by Signal

Operator: JCP 1 Apr 92 9:15 pm
Method File Name : DNPHIII.M
Sample Info : #20
Misc Info:
Integration File Name : DATA:0401A24B.I
consisting of channels : 1. A 360,4 550,100 of 0401A24B.D
Sequence Index: 1 Bottle Number : 24 Repetition Number: 2

A 360,4 550,100 of 0401A24B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.890	BV	70.5923	3.0064	5.08	100.00	0.302	1.47
3.441	BB	1304.76	314.27	93.81	100.00	0.065	0.82
4.460	BB	15.5001	2.8650	1.11	100.00	0.085	0.77

1: LC A 360,4 550,100 of 0401A25A.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

*** Area Percent ***

Report by Signal

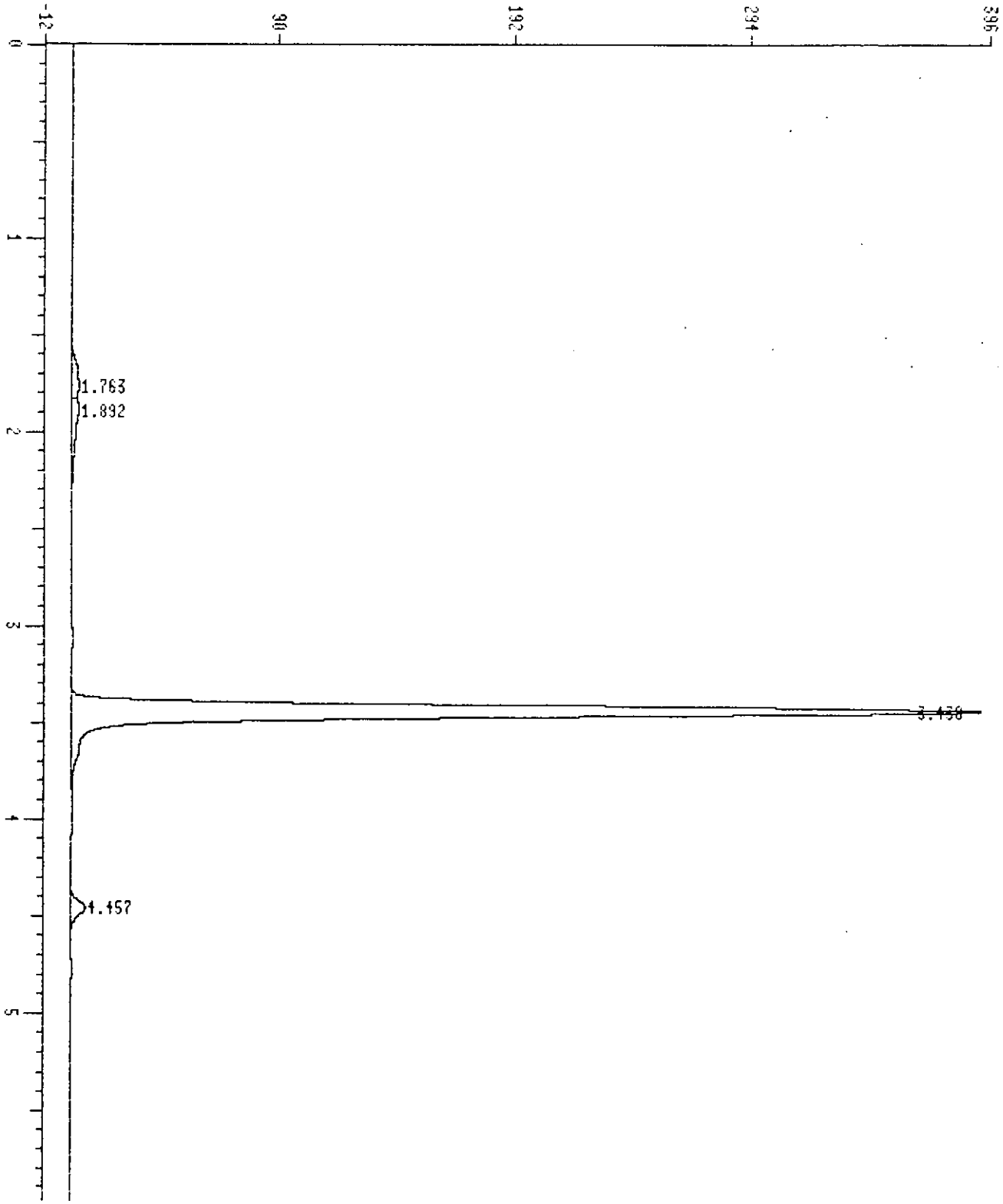
Operator: JCP 1 Apr 92 9:24 pm
Method File Name : DNPHIII.M
Sample Info : #21
Misc Info:
Integration File Name : DATA:0401A25A.I
consisting of channels : 1. A 360,4 550,100 of 0401A25A.D
Sequence Index: 1 Bottle Number : 25 Repetition Number: 1

A 360,4 550,100 of 0401A25A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.889	BV	78.9789	3.3384	4.51	100.00	0.298	1.56
3.441	PV	1638.47	394.59	93.54	100.00	0.065	0.92
4.459	BB	34.2538	6.3179	1.96	100.00	0.084	0.81

103

1: LC A 360,4 550,100 of 0401A259.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 7.77 cm/min

104

*** Area Percent ***

Report by Signal

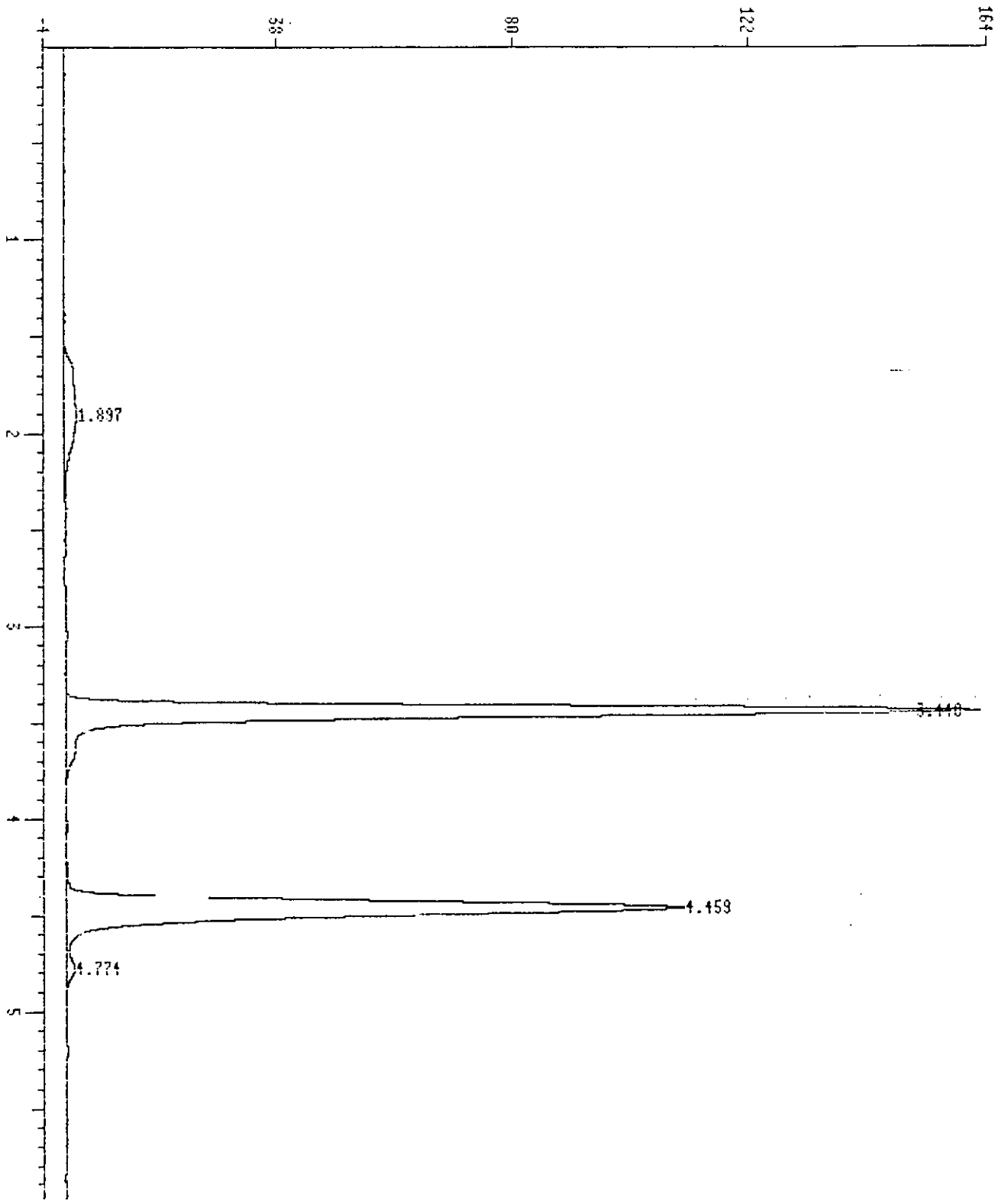
Operator: JCP 1 Apr 92 9:33 pm
Method File Name : DNPHIII.M
Sample Info : #21
Misc Info:
Integration File Name : DATA:0401A25B.I
consisting of channels : 1. A 360,4 550,100 of 0401A25B.D
Sequence Index: 1 Bottle Number : 25 Repetition Number: 2

A 360,4 550,100 of 0401A25B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.763	BV	38.4456	3.1435	2.19	100.00	0.169	2.24
1.992	VV	44.7591	3.3101	2.54	100.00	0.177	0.30
3.439	BV	1641.69	394.89	93.27	100.00	0.065	0.92
4.457	BV	35.2089	6.3831	2.00	100.00	0.086	0.82

10 5

1: LC A 360,4 550,100 of 0401A26A.D



End of plot Time = 0.00 to 5.99 minutes Chart speed = 7.77 cm/min

106

*** Area Percent ***

Report by Signal

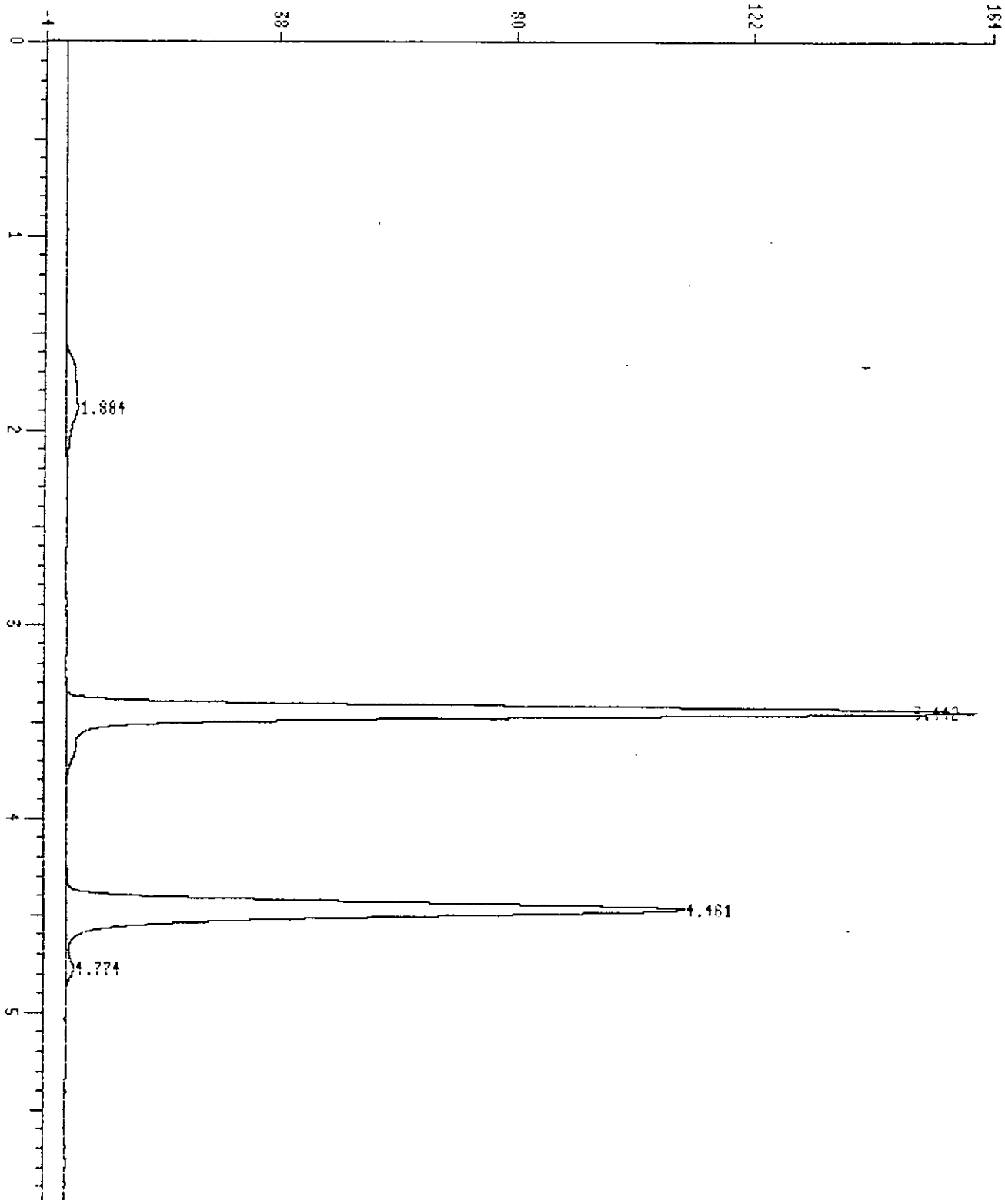
Operator: JCP 1 Apr 92 9:41 pm
Method File Name : DNPHIII.M
Sample Info : #22
Misc Info:
Integration File Name : DATA:0401A26A.I
consisting of channels : 1. A 360,4 550,100 of 0401A26A.D
Sequence Index: 1 Bottle Number : 26 Repetition Number: 1

A 360,4 550,100 of 0401A26A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.897	BV	55.8267	2.2041	4.12	100.00	0.313	1.25
3.440	BB	678.01	162.85	50.08	100.00	0.065	0.82
4.459	BV	608.90	110.11	44.99	100.00	0.096	0.80
4.774	VB	11.0089	1.5223	0.81	100.00	0.113	0.96

1 of 1

1: LC A 360,4 550,100 of 0401A26B.D



End of plot. Time = 0.00 to 5.99 minutes Chart speed = 3.33 cm/min

108

*** Area Percent ***

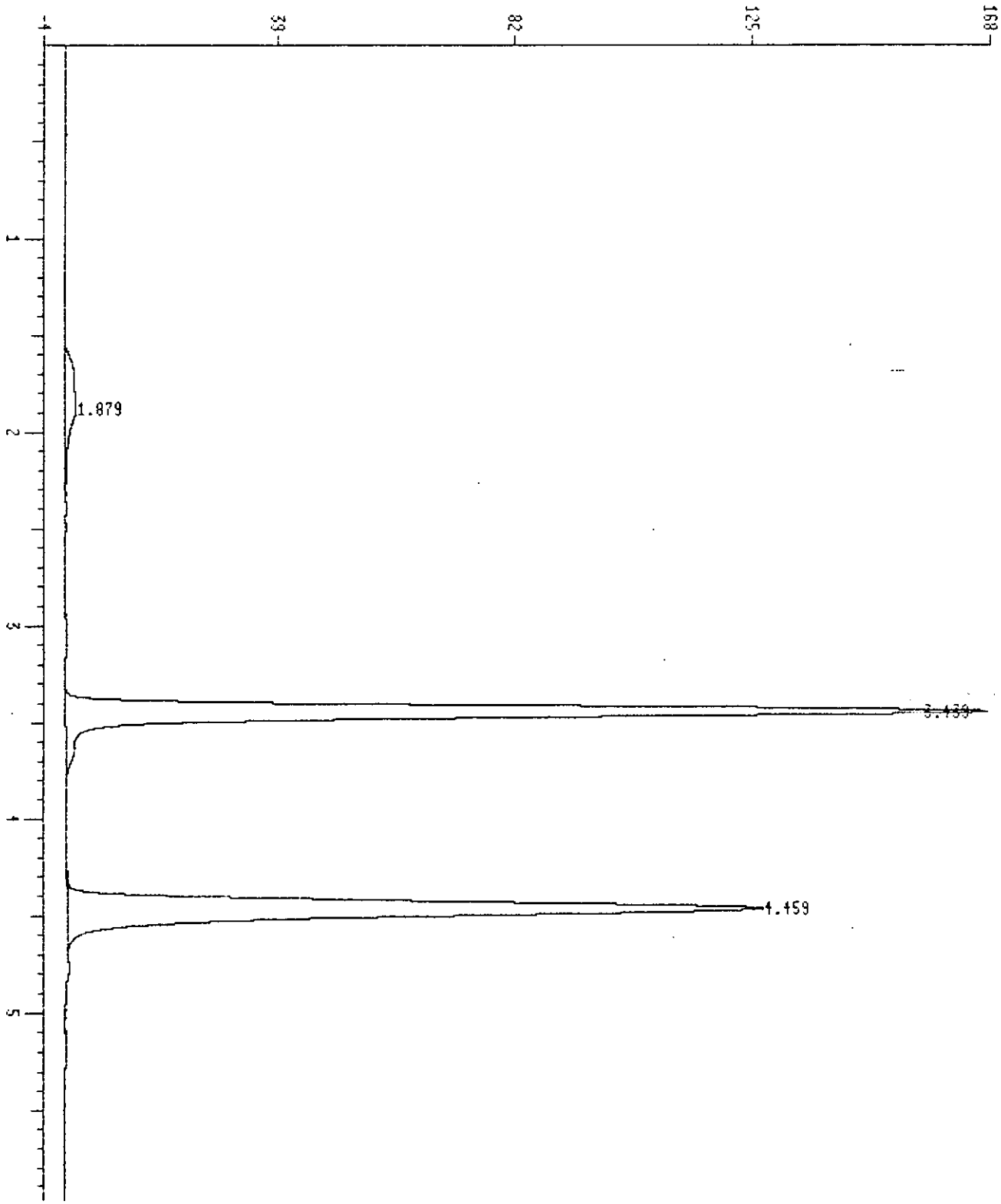
Report by Signal

Operator: JCP 1 Apr 92 9:50 pm
Method File Name : DNPHIII.M
Sample Info : #22
Misc Info:
Integration File Name : DATA:0401A26B.I
consisting of channels : 1. A 360,4 550,100 of 0401A26B.D
Sequence Index: 1 Bottle Number : 26 Repetition Number: 2

A 360,4 550,100 of 0401A26B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.884	BB	42.4788	2.0401	3.18	100.00	0.262	1.91
3.442	BB	673.91	162.29	50.50	100.00	0.065	0.82
4.461	BV	608.05	110.20	45.57	100.00	0.085	0.80
4.774	VB	9.9681	1.4495	0.75	100.00	0.106	1.02

1: LC A 360,4 550,100 of 0401A27A.D



End of plot Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

*** Area Percent ***

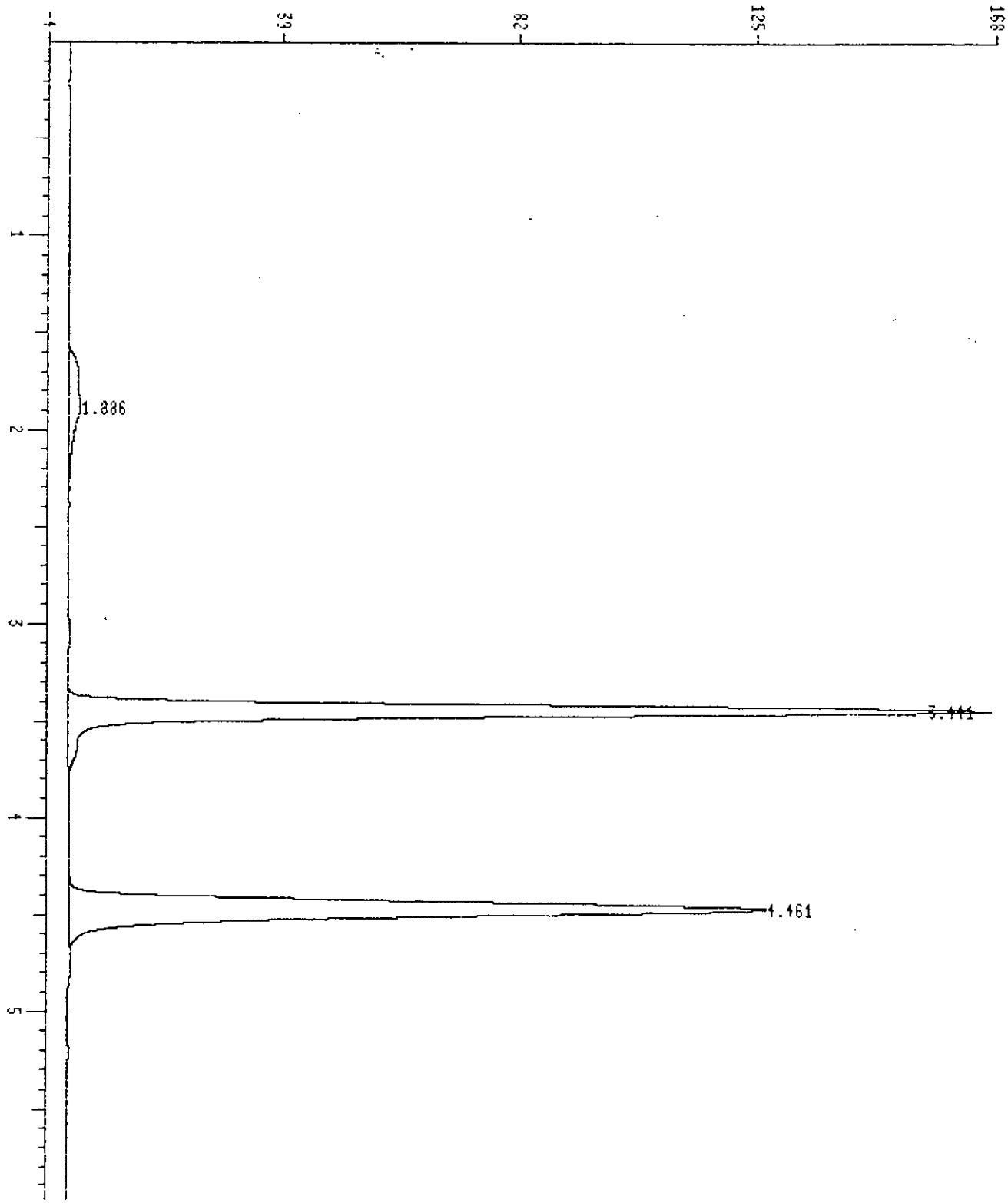
Report by Signal

Operator: JCP 1 Apr 92 9:59 pm
Method File Name : DNPHIII.M
Sample Info : #23
Misc Info:
Integration File Name : DATA:0401A27A.I
consisting of channels : 1. A 360,4 550,100 of 0401A27A.D
Sequence Index: 1 Bottle Number : 27 Repetition Number: 1

A 360,4 550,100 of 0401A27A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.879	BV	44.3692	2.0730	3.10	100.00	0.274	1.67
3.439	BB	697.72	157.90	48.69	100.00	0.065	0.92
4.459	BV	690.95	126.44	48.22	100.00	0.085	0.80

1: LC A 350,4 550,100 of 0401A27B.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

112

*** Area Percent ***

Report by Signal

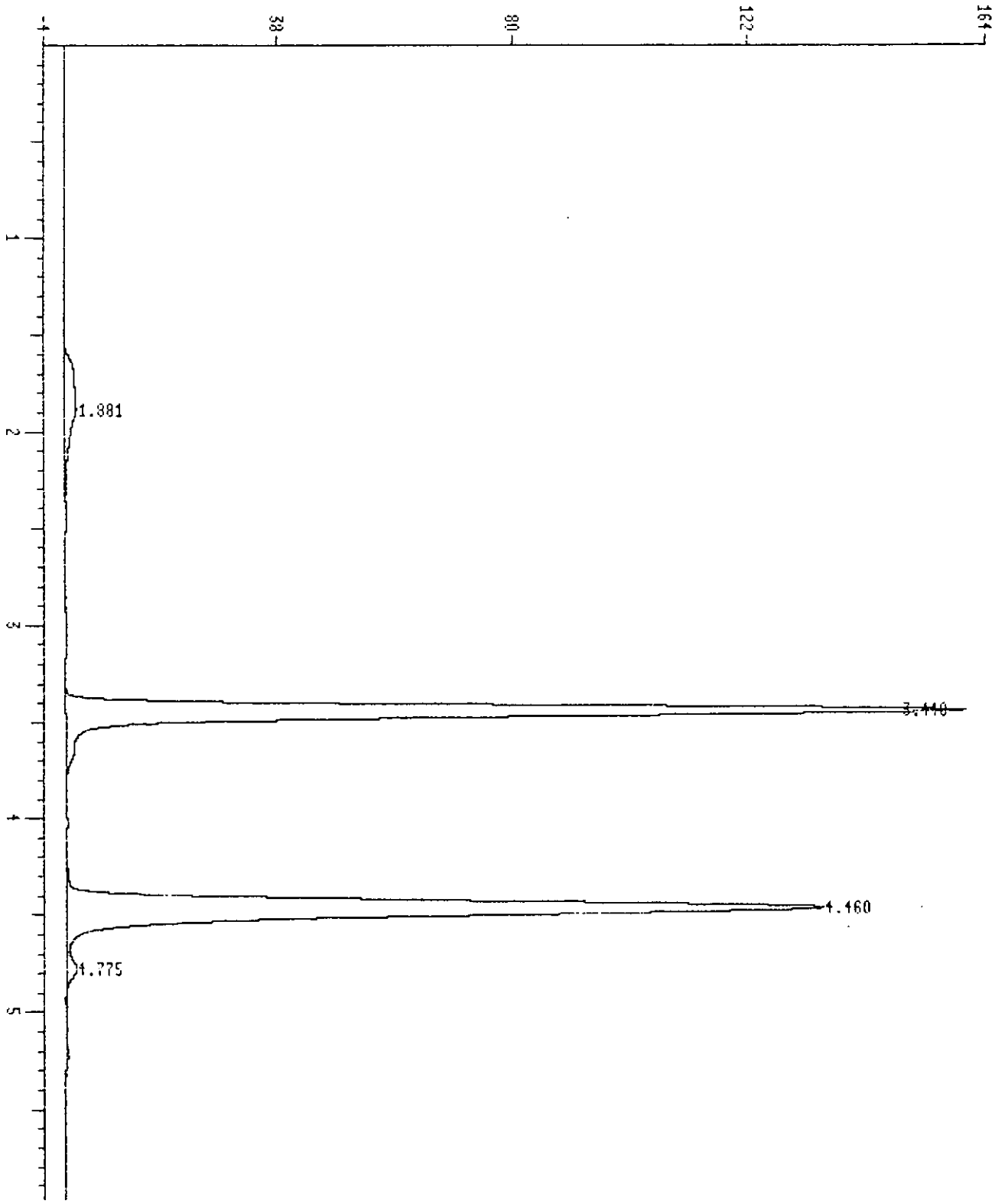
Operator: JCP 1 Apr 92 10:08 pm
Method File Name : DNPHIII.M
Sample Info : #23
Misc Info:
Integration File Name : DATA:0401A27B.I
consisting of channels : 1. A 360,4 550,100 of 0401A27B.D
Sequence Index: 1 Bottle Number : 27 Repetition Number: 2

A 360,4 550,100 of 0401A27B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.885	BV	48.3961	2.0995	3.36	100.00	0.298	1.46
3.441	BB	697.11	167.77	48.46	100.00	0.065	0.82
4.461	BV	693.09	126.64	48.18	100.00	0.085	0.81

113

1: LC A 360,4 550,100 of 0401A29A.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.34 cm/min

114

*** Area Percent ***

Report by Signal

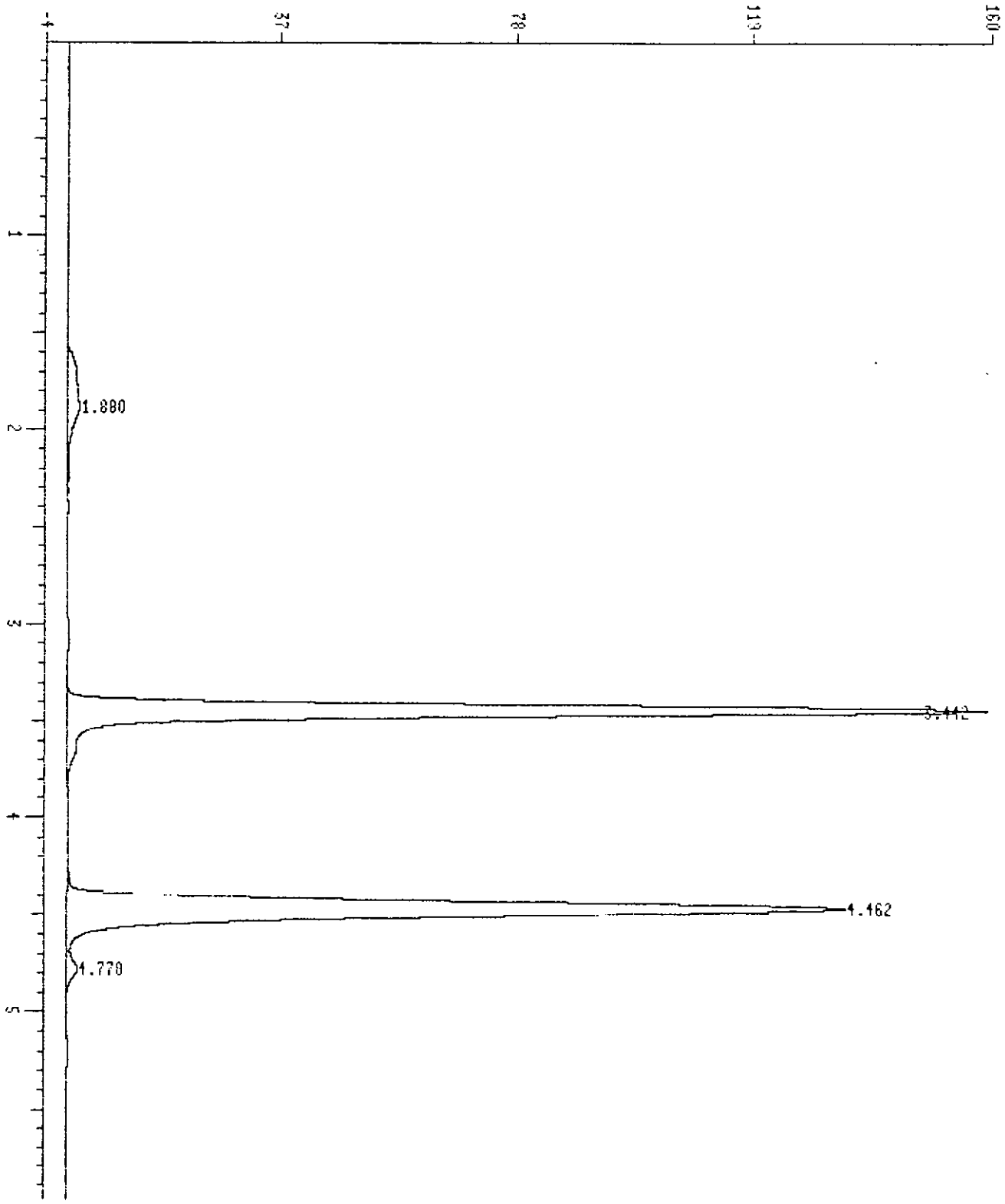
Operator: JCP 1 Apr 92 10:15 pm
Method File Name : DNPHIII.M
Sample Info : #24
Misc Info:
Integration File Name : DATA:0401A28A.I
consisting of channels : 1. A 360,4 550,100 of 0401A28A.D
Sequence Index: 1 Bottle Number : 28 Repetition Number: 1

A 360,4 550,100 of 0401A28A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.881	BV	47.1638	2.0500	3.20	100.00	0.290	1.41
3.440	BB	667.22	160.66	45.33	100.00	0.065	0.82
4.460	BV	744.82	135.28	50.61	100.00	0.085	0.80
4.775	VB	12.6100	1.8505	0.86	100.00	0.103	0.98

15

1: LC A 360,4 550,100 of 0401A29B.D



End of plot. Time = 0.01 to 5.98 minutes Chart speed = 3.34 cm/min

116

*** Area Percent ***

Report by Signal

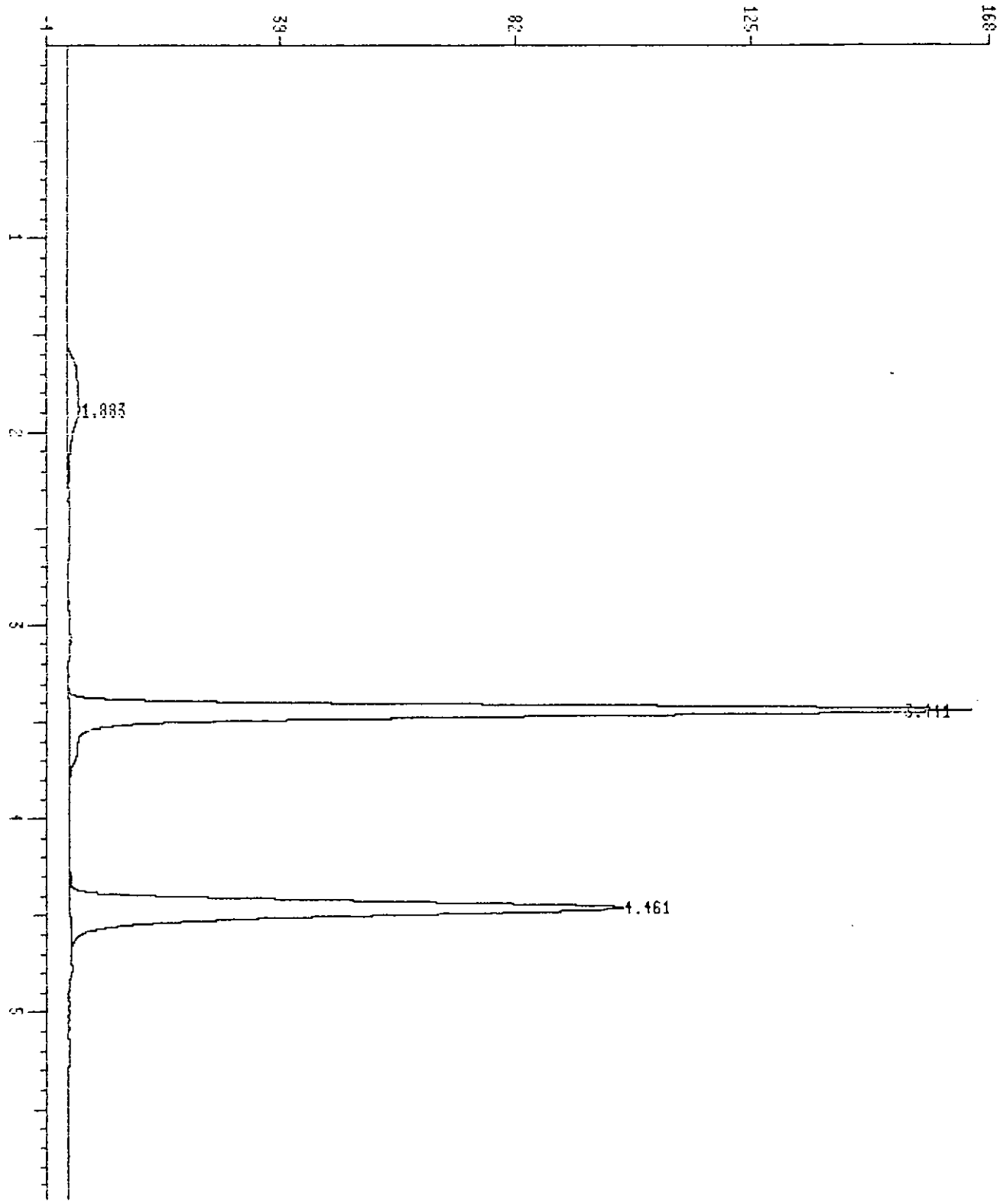
Operator: JCP 1 Apr 92 10:25 pm
Method File Name : DNPHIII.M
Sample Info : #24
Misc Info:
Integration File Name : DATA:0401A28B.I
consisting of channels : 1. A 360,4 550,100 of 0401A28B.D
Sequence Index: 1 Bottle Number : 28 Repetition Number: 2

A 360,4 550,100 of 0401A28B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.880	BB	43.3231	2.1282	2.95	100.00	0.263	1.75
3.442	BB	666.30	160.34	45.40	100.00	0.065	0.81
4.462	BV	745.00	135.24	50.77	100.00	0.085	0.90
4.778	VB	12.8502	1.8649	0.88	100.00	0.105	0.98

117

1: LC A 360,4 550,100 of 0401A23A.D



End of plot Time = 0.00 to 5.98 minutes Chart speed = 7.74 cm/min

*** Area Percent ***

Report by Signal

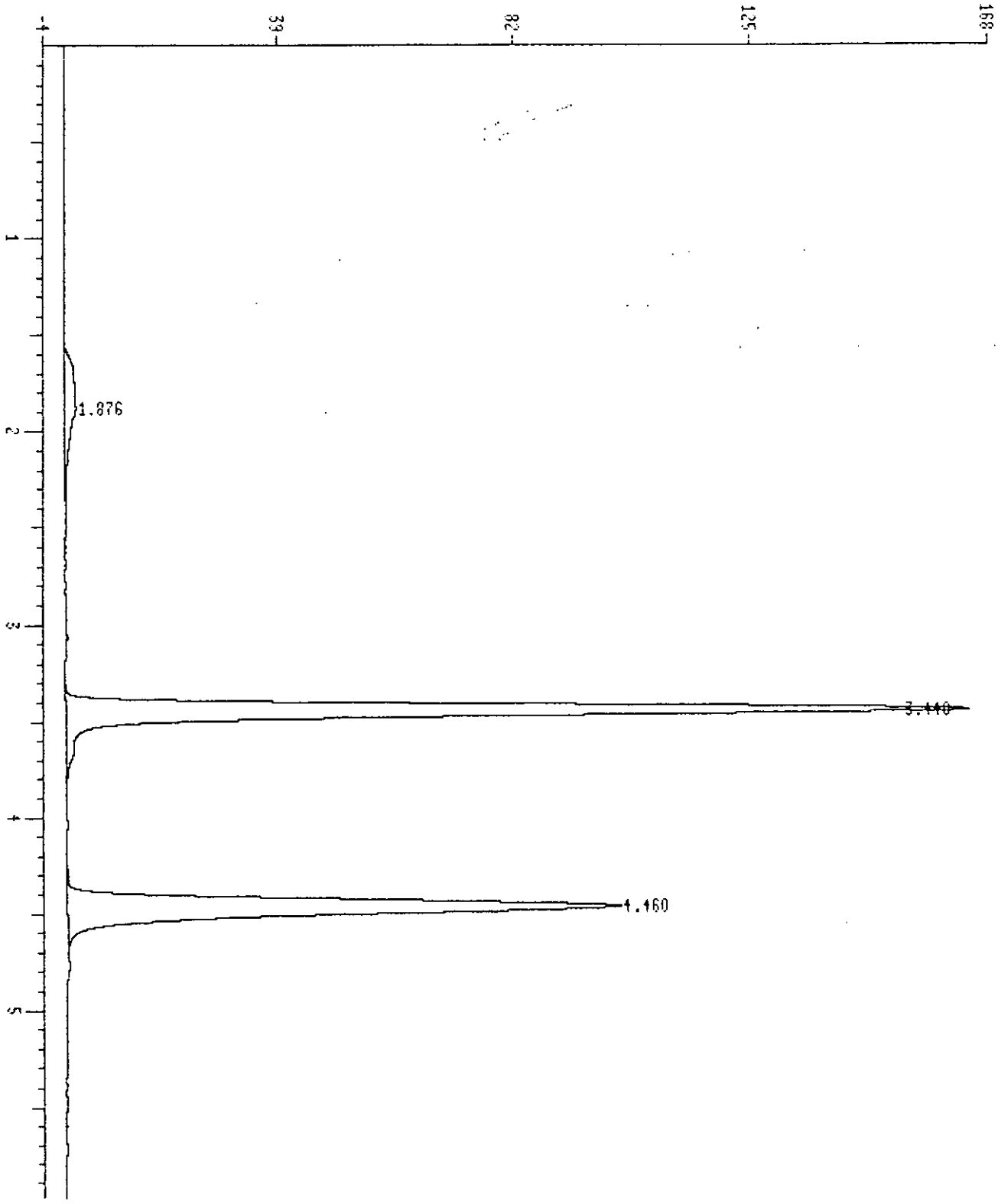
Operator: JCP 1 Apr 92 10:34 pm
Method File Name : DNPHIII.M
Sample Info : #25
Misc Info:
Integration File Name : DATA:0401A29A.I
consisting of channels : 1. A 360,4 550,100 of 0401A29A.D
Sequence Index: 1 Bottle Number : 29 Repetition Number: 1

A 360,4 550,100 of 0401A29A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.883	BV	45.5494	2.0752	3.56	100.00	0.278	1.83
3.441	BB	683.25	164.78	53.33	100.00	0.065	0.82
4.461	BV	552.41	101.07	43.12	100.00	0.085	0.81

119

1: LC A 360,4 550,100 of 0401A298.D



End of plot Time = 0.00 to 5.98 minutes Chart speed = 7.77 cm/min

120

*** Area Percent ***

Report by Signal

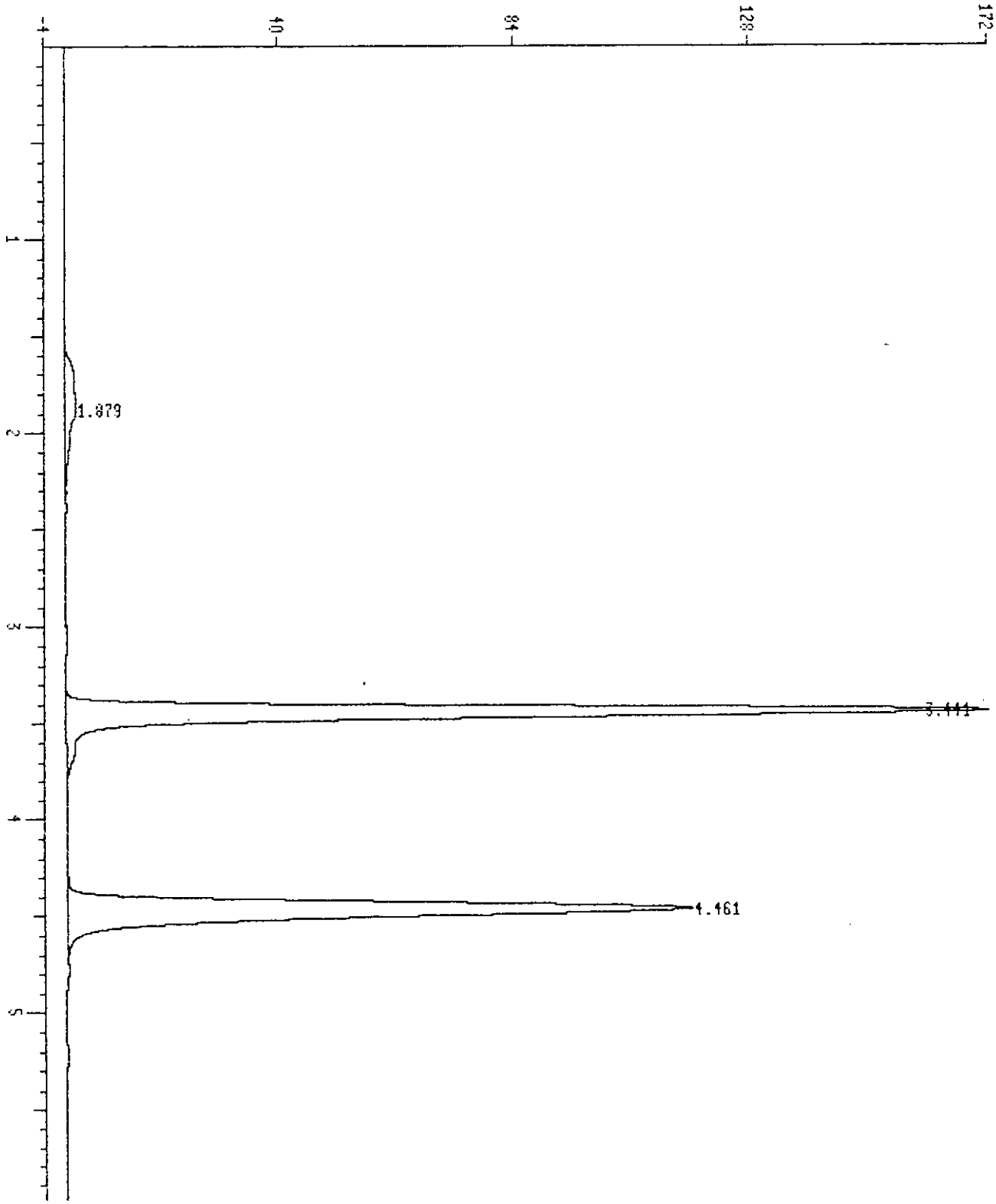
Operator: JCP 1 Apr 92 10:43 pm
Method File Name : DNPHIII.M
Sample Info : #25
Misc Info:
Integration File Name : DATA:0401A29B.I
consisting of channels : 1. A 360,4 550,100 of 0401A29B.D
Sequence Index: 1 Bottle Number : 29 Repetition Number: 2

A 360,4 550,100 of 0401A29B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym.
1.876	BV	48.0351	2.0464	3.74	100.00	0.294	1.38
3.440	BB	683.78	164.79	53.25	100.00	0.065	0.82
4.460	BV	552.37	100.93	43.01	100.00	0.085	0.81

121

1: LC A 360,4 550,100 of 0401A30A.D



End of plot. Time = 0.00 to 5.00 minutes. Chart speed = 7.77 cm/min

122

*** Area Percent ***

Report by Signal

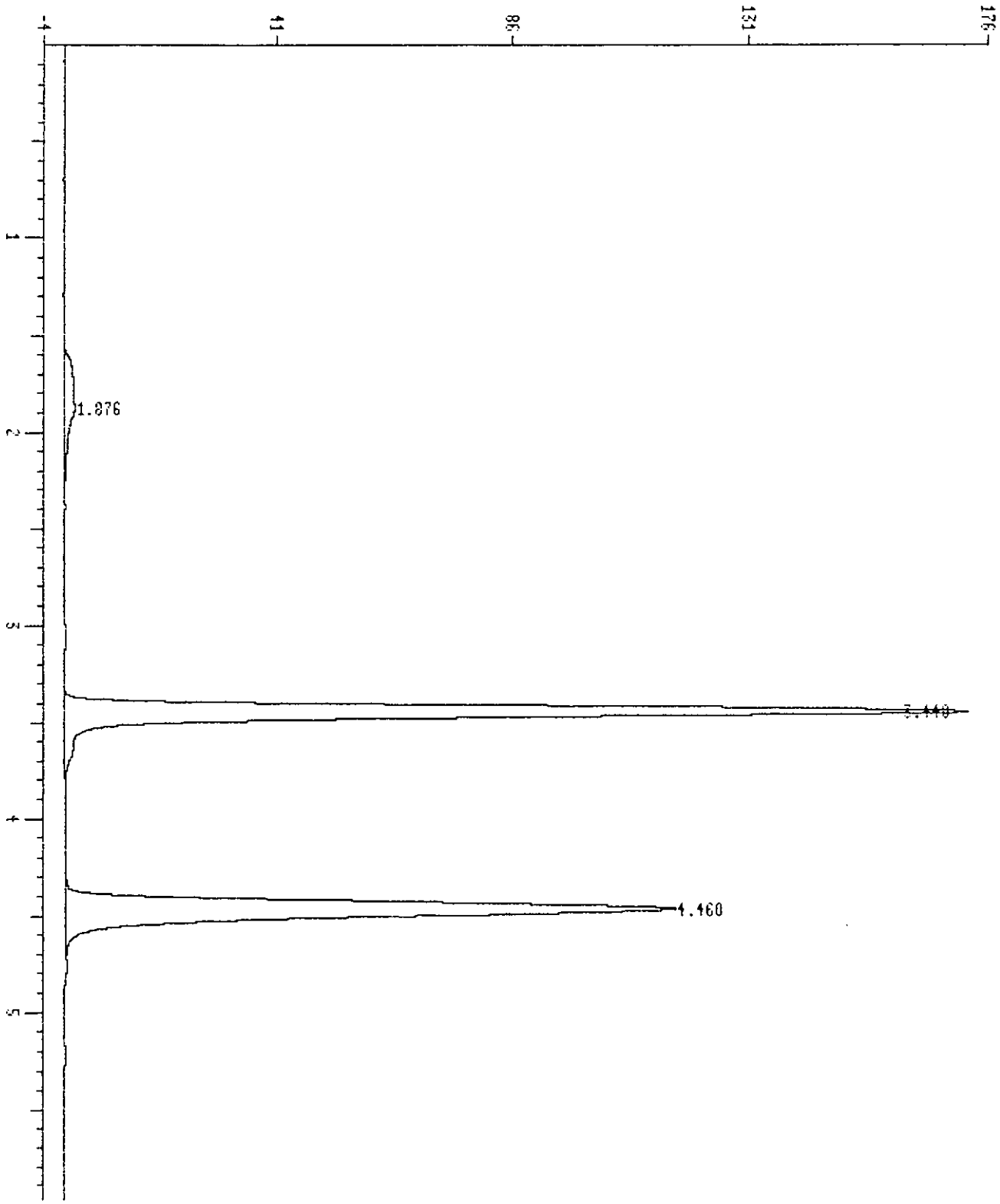
Operator: JCP 1 Apr 92 10:51 pm
Method File Name : DNPHIII.M
Sample Info : #26
Misc Info:
Integration File Name : DATA:0401A30A.I
consisting of channels : 1. A 360,4 550,100 of 0401A30A.D
Sequence Index: 1 Bottle Number : 30 Repetition Number: 1

A 360,4 550,100 of 0401A30A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.879	BV	47.0588	2.0510	3.36	100.00	0.291	1.43
3.441	BB	713.98	172.16	51.01	100.00	0.065	0.82
4.461	BV	638.64	116.57	45.63	100.00	0.085	0.81

123

1: LC A 360,4 S50,100 of 0401A30B.D



124

*** Area Percent ***

Report by Signal

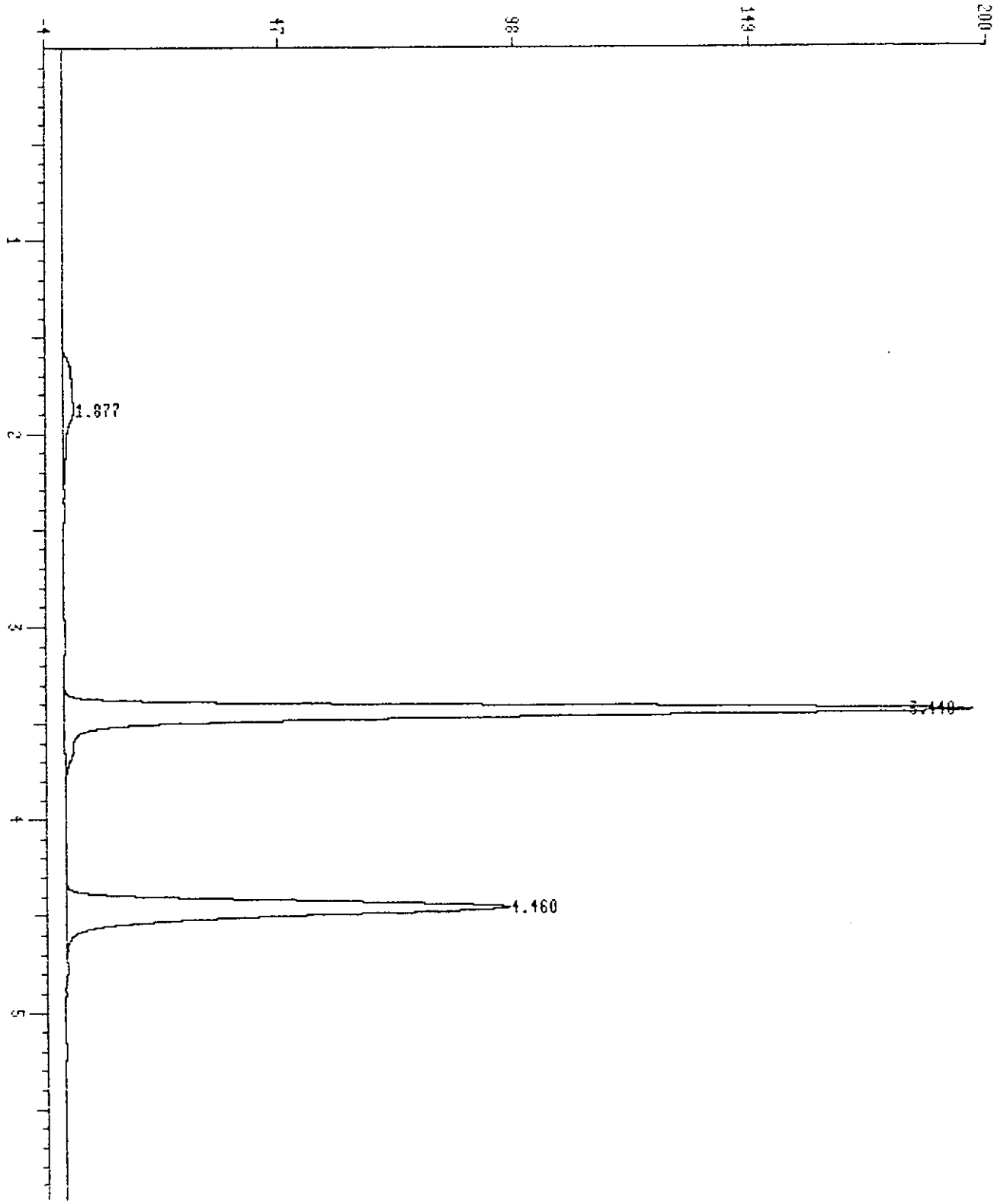
Operator: JCP 1 Apr 92 11:00 pm
Method File Name : DNPHIII.M
Sample Info : #26
Misc Info:
Integration File Name : DATA:0401A30B.I
consisting of channels : 1. A 360,4 550,100 of 0401A30B.D
Sequence Index: 1 Bottle Number : 30 Repetition Number: 2

A 360,4 550,100 of 0401A30B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.876	BV	48.3017	2.0982	3.45	100.00	0.290	1.45
3.440	BB	714.14	172.28	51.01	100.00	0.065	0.82
4.460	BV	637.50	116.43	45.54	100.00	0.085	0.80

125

1: LC A 360,4 550,100 of 0401A31A.D



End of plot Time = 0.00 to 5.99 minutes Chart speed = 7.74 cm/min

*** Area Percent ***

Report by Signal

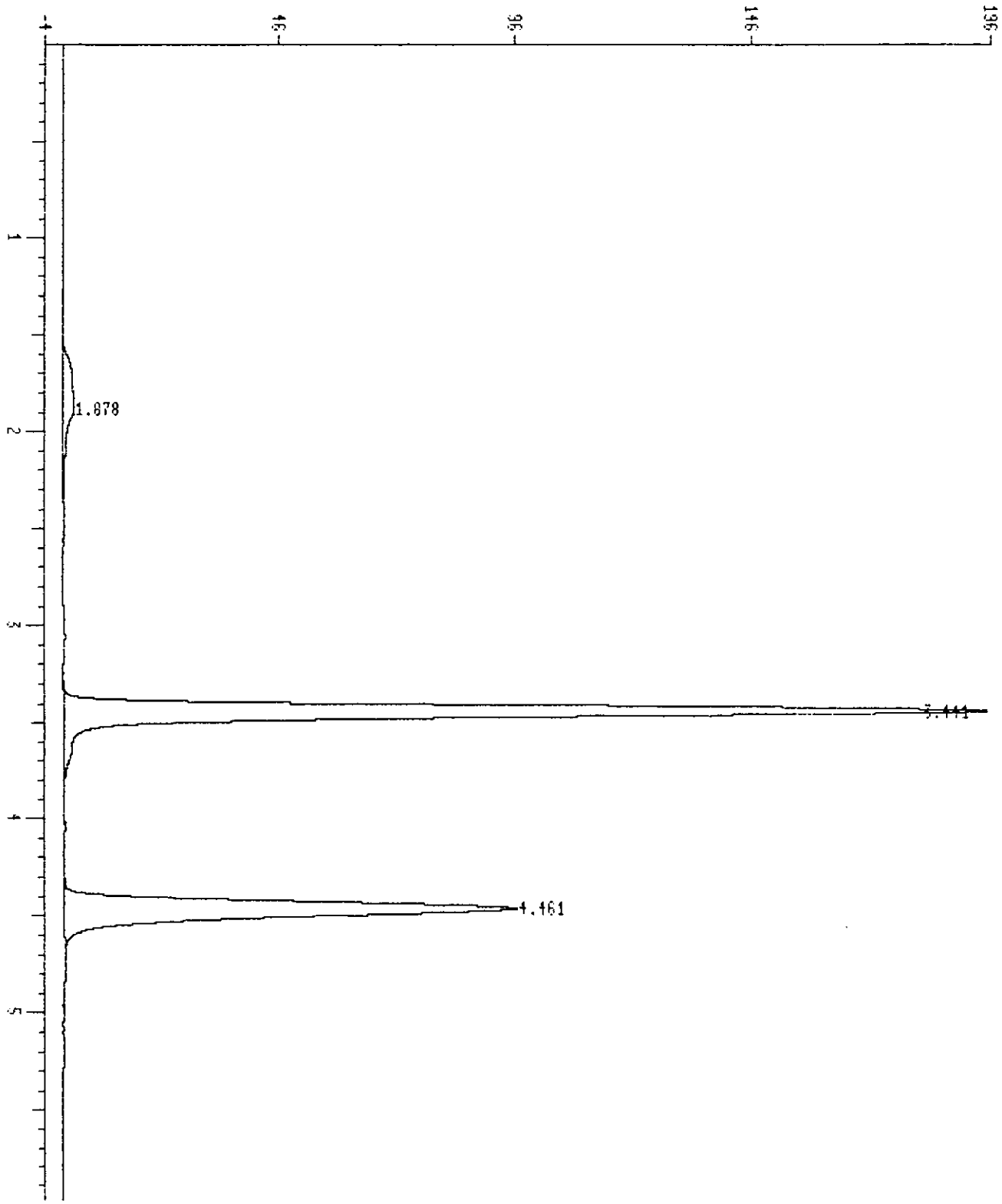
Operator: JCP 1 Apr 92 11:09 pm
Method File Name : DNPHIII.M
Sample Info : #27
Misc Info:
Integration File Name : DATA:0401A31A.I
consisting of channels : 1. A 360,4 550,100 of 0401A31A.D
Sequence Index: 1 Bottle Number : 31 Repetition Number: 1

A 360,4 550,100 of 0401A31A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.877	BB	48.3817	2.2297	3.48	100.00	0.276	1.77
3.440	BB	816.33	196.84	58.64	100.00	0.065	0.82
4.460	BV	527.38	96.4342	37.88	100.00	0.085	0.80

124

1: LC A 360,4 550,100 of 0401A31B.D



End of plot Time = 0.00 to 5.99 minutes Chart speed = 7.77 cm/min

128

*** Area Percent ***

Report by Signal

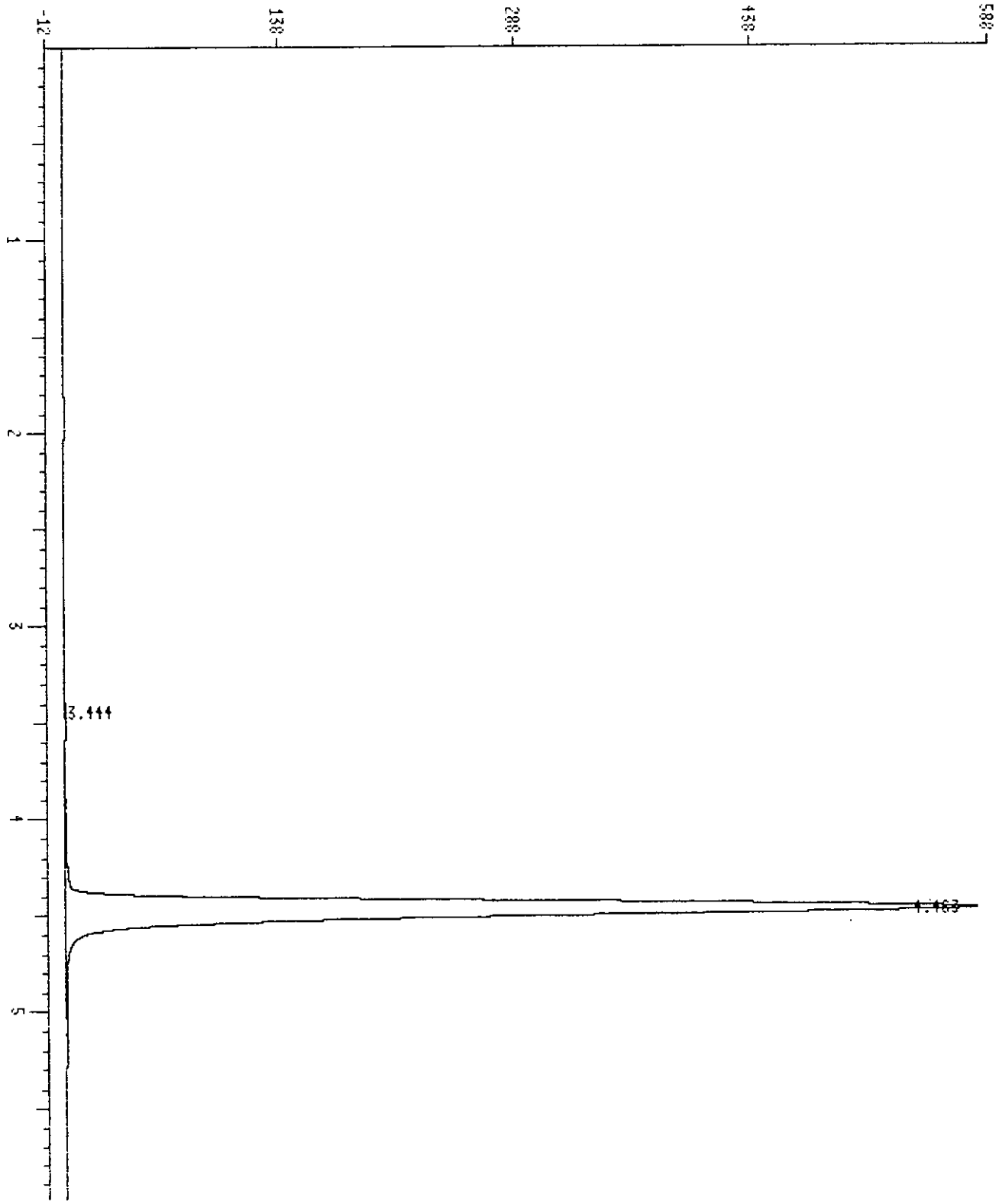
Operator: JCP 1 Apr 92 11:17 pm
Method File Name : DNPHIII.M
Sample Info : #27
Misc Info:
Integration File Name : DATA:0401A31B.I
consisting of channels : 1. A 360,4 550,100 of 0401A31B.D
Sequence Index: 1 Bottle Number : 31 Repetition Number: 2

A 360,4 550,100 of 0401A31B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.878	BV	48.7334	2.2536	3.50	100.00	0.279	1.70
3.441	BB	814.95	196.33	58.60	100.00	0.065	0.82
4.461	BV	526.98	98.2600	37.89	100.00	0.085	0.80

129

1: LC A 350,4 550,100 of 0401A32A.D



130

*** Area Percent ***

Report by Signal

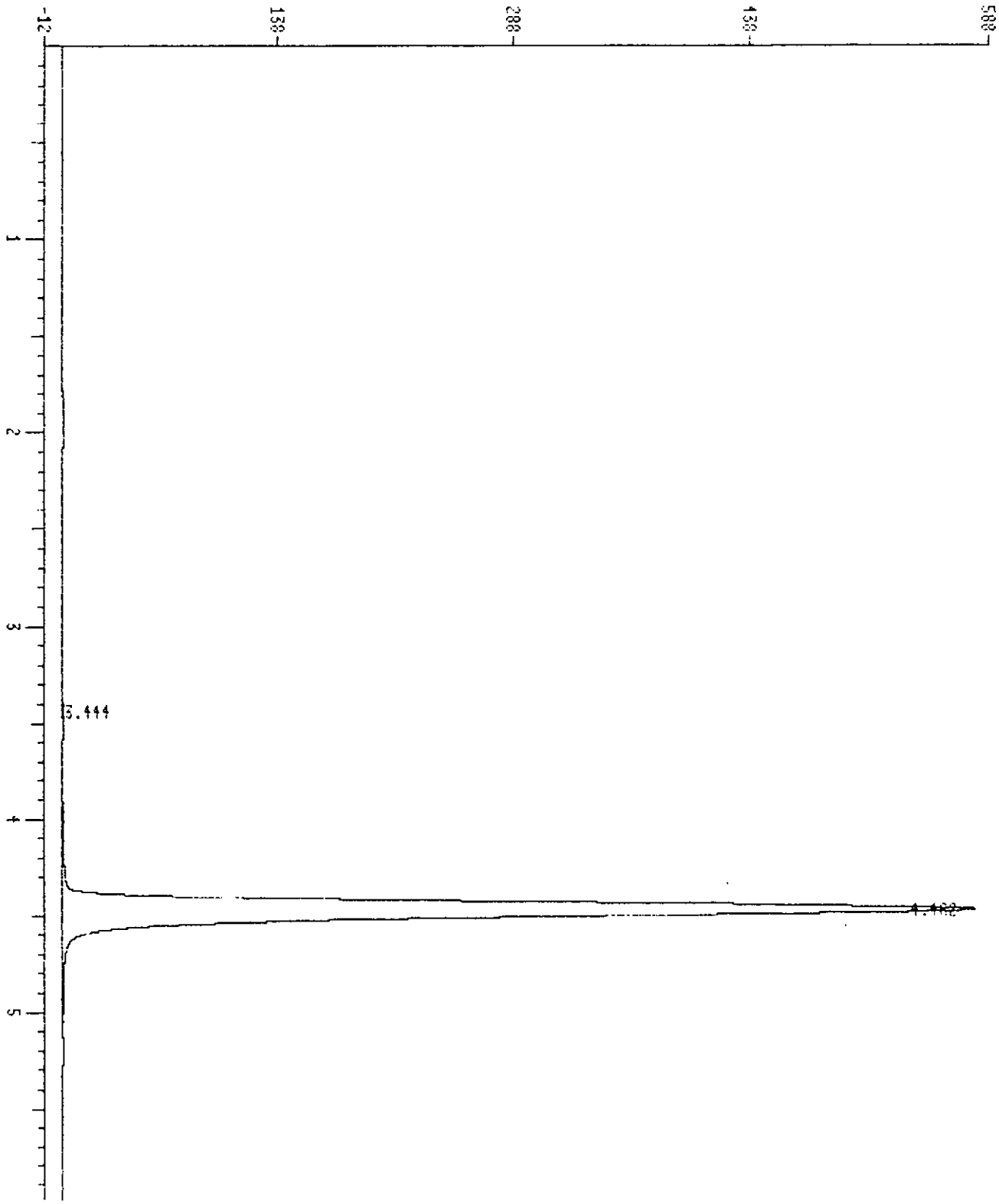
Operator: JCP 1 Apr 92 11:26 pm
Method File Name : DNPHIII.M
Sample Info : #28
Misc Info:
Integration File Name : DATA:0401A32A.I
consisting of channels : 1. A 360,4 550,100 of 0401A32A.D
Sequence Index: 1 Bottle Number : 32 Repetition Number: 1

A 360,4 550,100 of 0401A32A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.444	BV	3.3825	1.0153	0.11	100.00	0.057	0.86
4.463	BV	3199.75	590.02	99.89	100.00	0.085	0.81

131

1: LC A 360,4 550,100 of 0401A32B.D



End of plot Time = 0.00 to 5.00 minutes Chart speed = 7.77 cm/min

*** Area Percent ***

Report by Signal

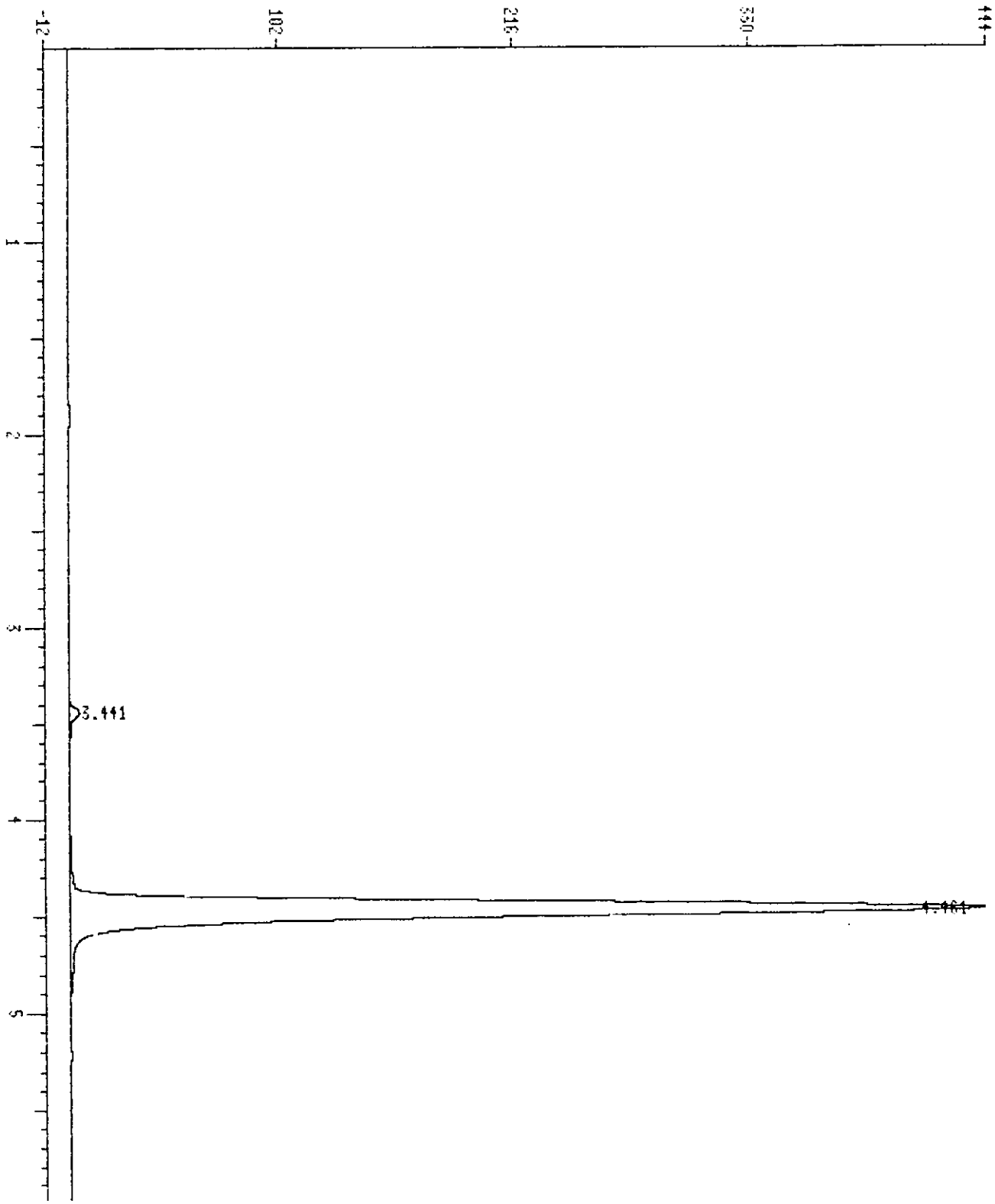
Operator: JCP 1 Apr 92 11:35 pm
Method File Name : DNPHIII.M
Sample Info : #28
Misc Info:
Integration File Name : DATA:0401A32B.I
consisting of channels : 1. A 360,4 550,100 of 0401A32B.D
Sequence Index: 1 Bottle Number : 32 Repetition Number: 2

A 360,4 550,100 of 0401A32B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.444	BV	3.6952	1.0111	0.12	100.00	0.060	1.07
4.462	BV	3200.24	580.35	99.88	100.00	0.085	0.81

133

1: LC A 360,4 550,100 of 0401A33A.D



End of plot Time = 0.00 to 5.00 minutes Chart speed = 7.77 cm/min

134

*** Area Percent ***

Report by Signal

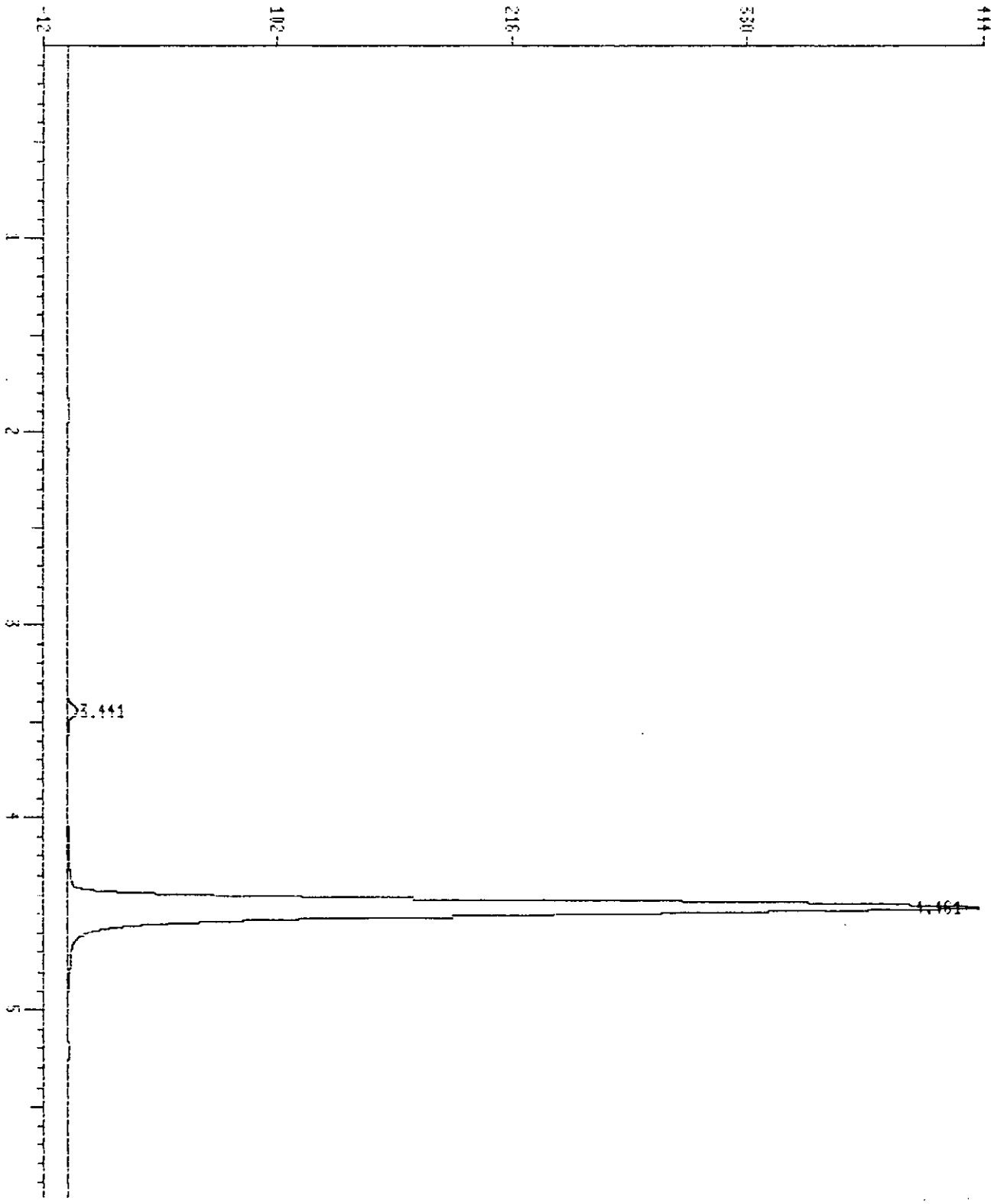
Operator: JCP 1 Apr 92 11:44 pm
Method File Name : DNPHIII.M
Sample Info : #29
Misc Info:
Integration File Name : DATA:0401A33A.I
consisting of channels : 1. A 360,4 550,100 of 0401A33A.D
Sequence Index: 1 Bottle Number : 33 Repetition Number: 1

A 360,4 550,100 of 0401A33A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.441	BB	21.0193	4.8406	0.85	100.00	0.057	0.79
4.461	BV	2447.97	443.45	99.15	100.00	0.095	0.80

135

1: LC A 360,4 550,100 of 0401A338.D



End of plot Time = 0.00 to 5.00 minutes Chart speed = 2.77 cm/min

136

*** Area Percent ***

Report by Signal

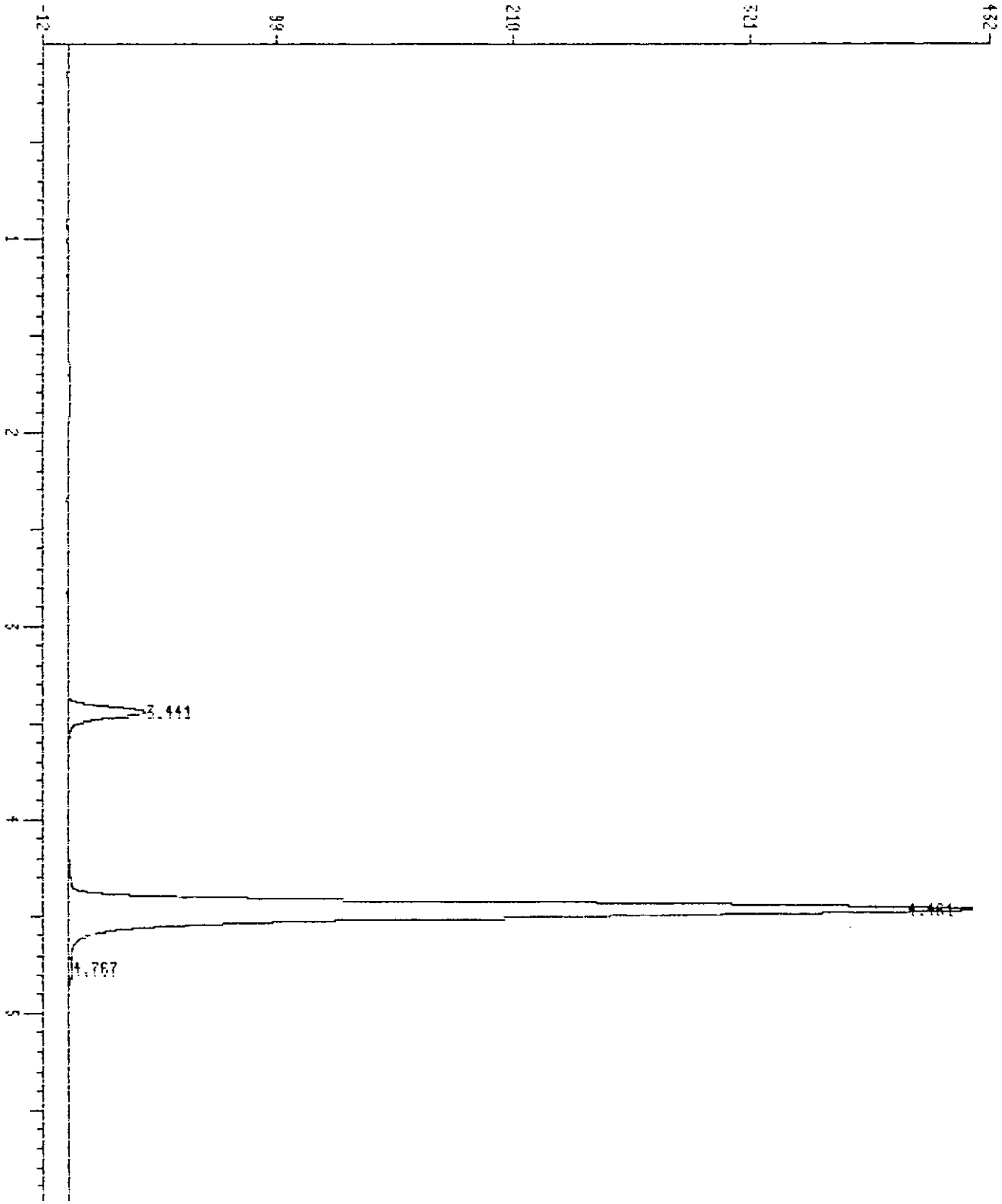
Operator: JCP 1 Apr 92 11:52 pm
Method File Name : DNPHIII.M
Sample Info : #29
Misc Info:
Integration File Name : DATA:0401A338.I
consisting of channels : 1. A 360,4 550,100 of 0401A338.D
Sequence Index: 1 Bottle Number : 33 Repetition Number: 2

A 360,4 550,100 of 0401A338.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.441	BB	22.8933	4.9538	0.93	100.00	0.071	0.79
4.461	BB	2449.14	443.06	99.07	100.00	0.095	0.80

137

1: LC A 350,4 550,100 of 0401A34A.D



End of plot Time - 0.00 to 5.98 minutes Chart speed - 7.77 cm/min

38

*** Area Percent ***

Report by Signal

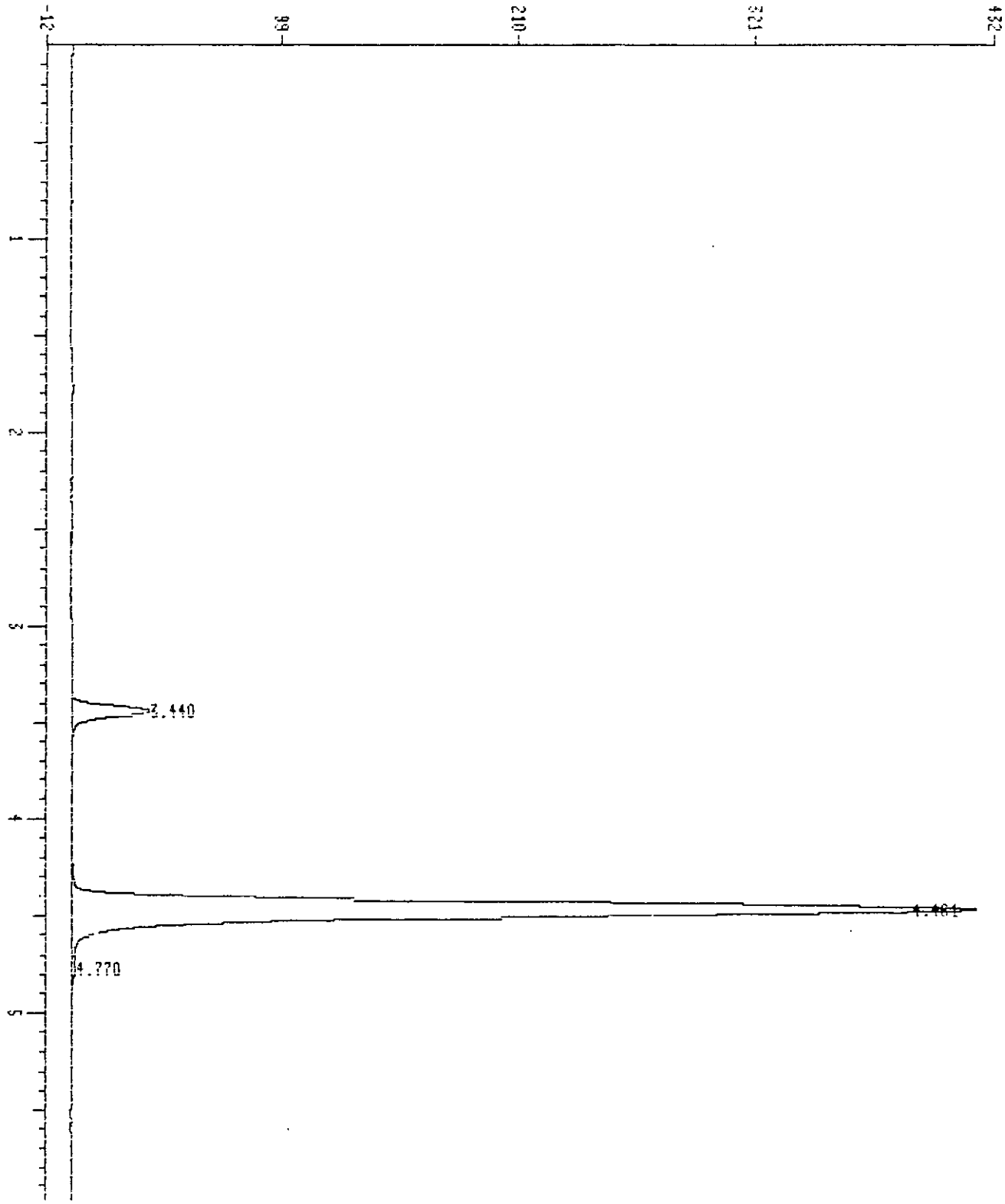
Operator: JCP 2 Apr 92 12:01 am
Method File Name : ONPHIII.M
Sample Info : #30
Misc Info:
Integration File Name : DATA:0401A34A.I
consisting of channels : 1. A 360,4 550,100 of 0401A34A.D
Sequence Index: 1 Bottle Number : 34 Repetition Number: 1

A 360,4 550,100 of 0401A34A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.441	BB	154.55	36.9352	6.17	100.00	0.065	0.93
4.451	BV	2336.08	424.67	93.31	100.00	0.085	0.81
4.767	VB	13.0101	1.8484	0.52	100.00	0.107	0.81

159

1: LC A 360,4 550,100 of 0401A348.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

140

*** Area Percent ***

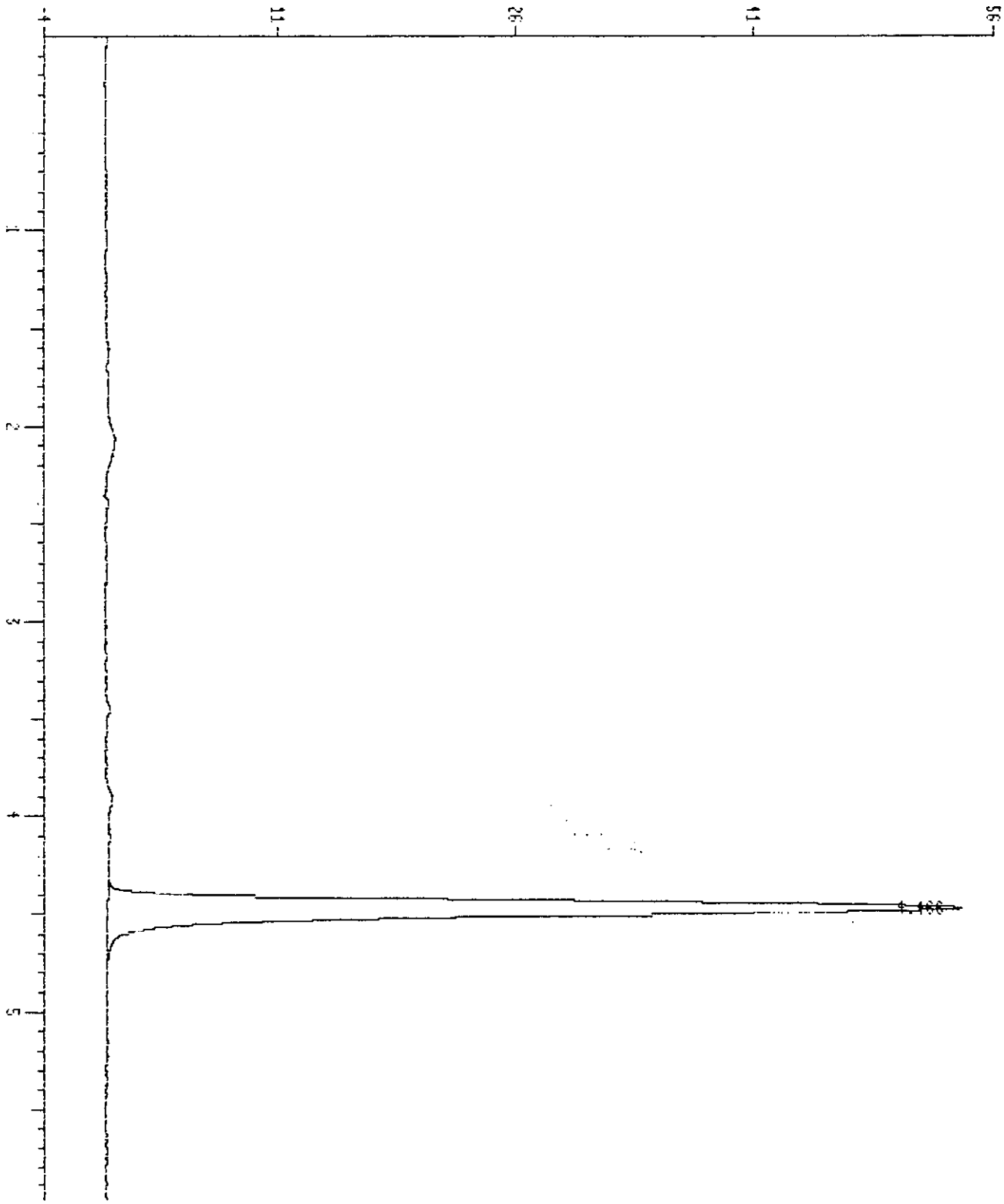
Report by Signal

Operator: JCP 2 Apr 92 12:10 am
Method File Name : DNPHIII.M
Sample Info : #30
Misc Info:
Integration File Name : DATA:0401A348.I
consisting of channels : 1. A 360,4 550,100 of 0401A348.D
Sequence Index: 1 Bottle Number : 34 Repetition Number: 2

A 360,4 550,100 of 0401A348.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.440	BB	155.19	37.0372	6.19	100.00	0.065	0.92
4.461	BV	2339.46	424.97	93.28	100.00	0.085	0.81
4.770	VB	13.3211	1.2500	0.53	100.00	0.109	0.93

1: LC A 350,4 550,100 of 0401A35A.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 7.74 cm/min

142

*** Area Percent ***

Report by Signal

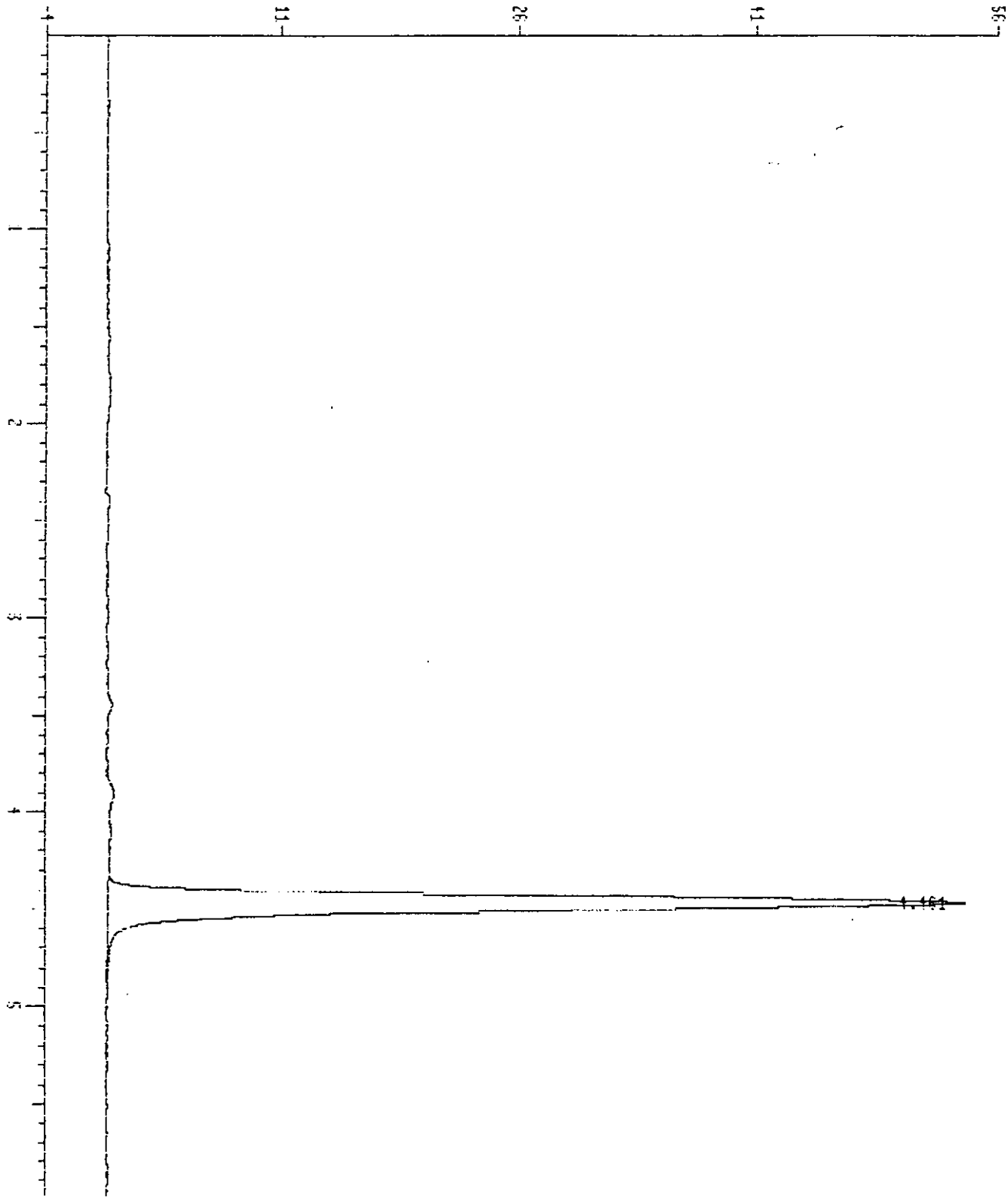
Operator: JCP 2 Apr 92 12:19 am
Method File Name : DNPHIII.M
Sample Info : STANDARD 5 PPM
Misc Info:
Integration File Name : DATA:0401A35A.I
consisting of channels : 1. A 360,4 550,100 of 0401A35A.D
Sequence Index: 1 Bottle Number : 35 Repetition Number: 1

A 360,4 550,100 of 0401A35A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.466	BB	294.71	54.0365	100.00	100.00	0.085	0.80

143

1: LC A 360,4 550,100 of 0401A35B.D



End of plot Time = 0.00 to 5.99 minutes Chart speed = 7.77 mm/min

1144

*** Area Percent ***

Report by Signal

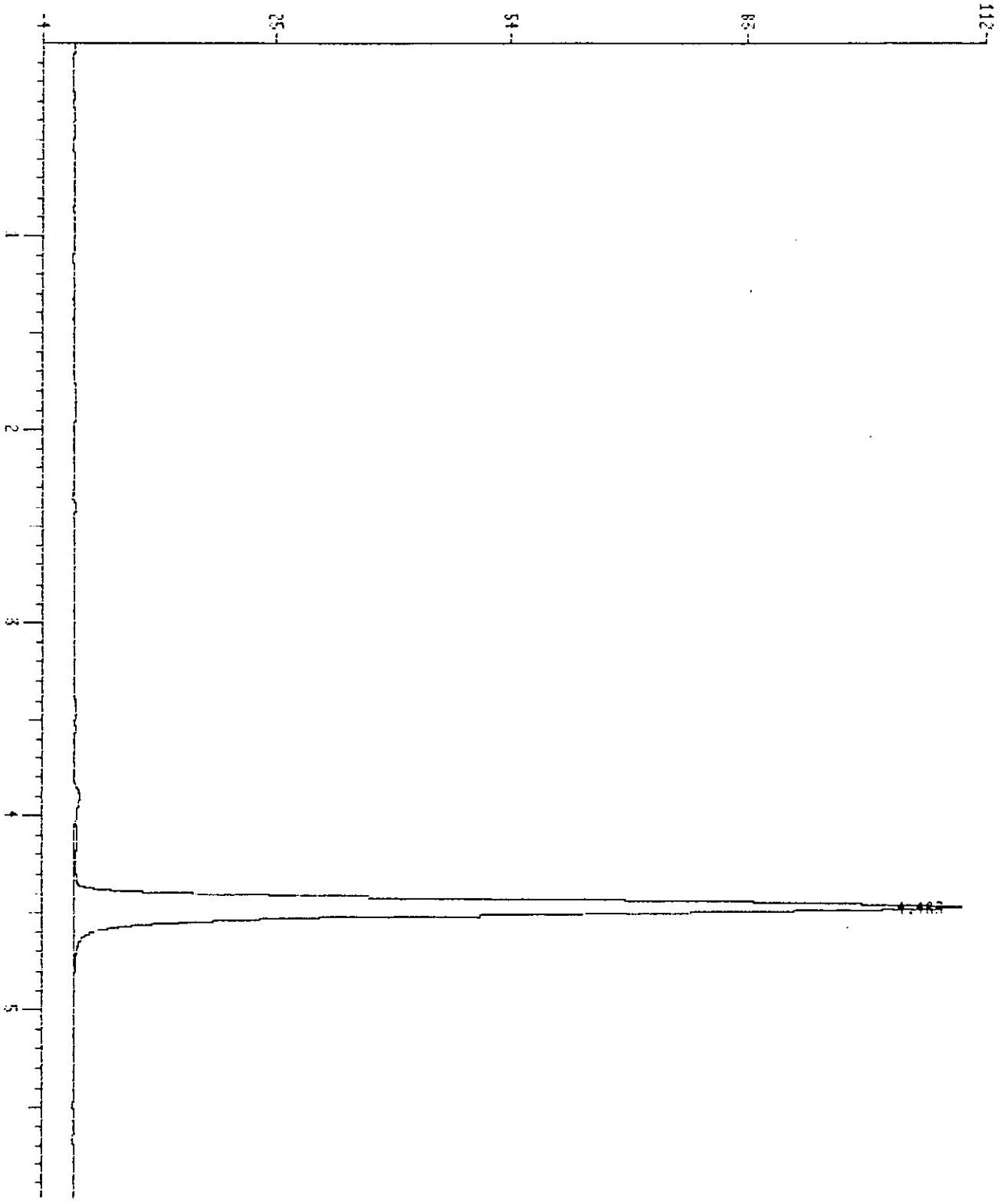
Operator: JCP 2 Apr 92 12:27 am
Method File Name : DNPHIII.M
Sample Info : STANDARD 5 PPM
Misc Info:
Integration File Name : DATA:0401A358.I
consisting of channels : 1. A 360,4 550,100 of 0401A358.D
Sequence Index: 1 Bottle Number : 35 Repetition Number: 2

A 360,4 550,100 of 0401A358.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.461	BB	298.10	53.9342	100.00	100.00	0.085	0.80

145

1: LC A 360,4 550,100 of 0401A35A.D



End of plot. Time = 0.00 to 5.99 minutes Chart speed = 3.33 cm/min

146

*** Area Percent ***

Report by Signal

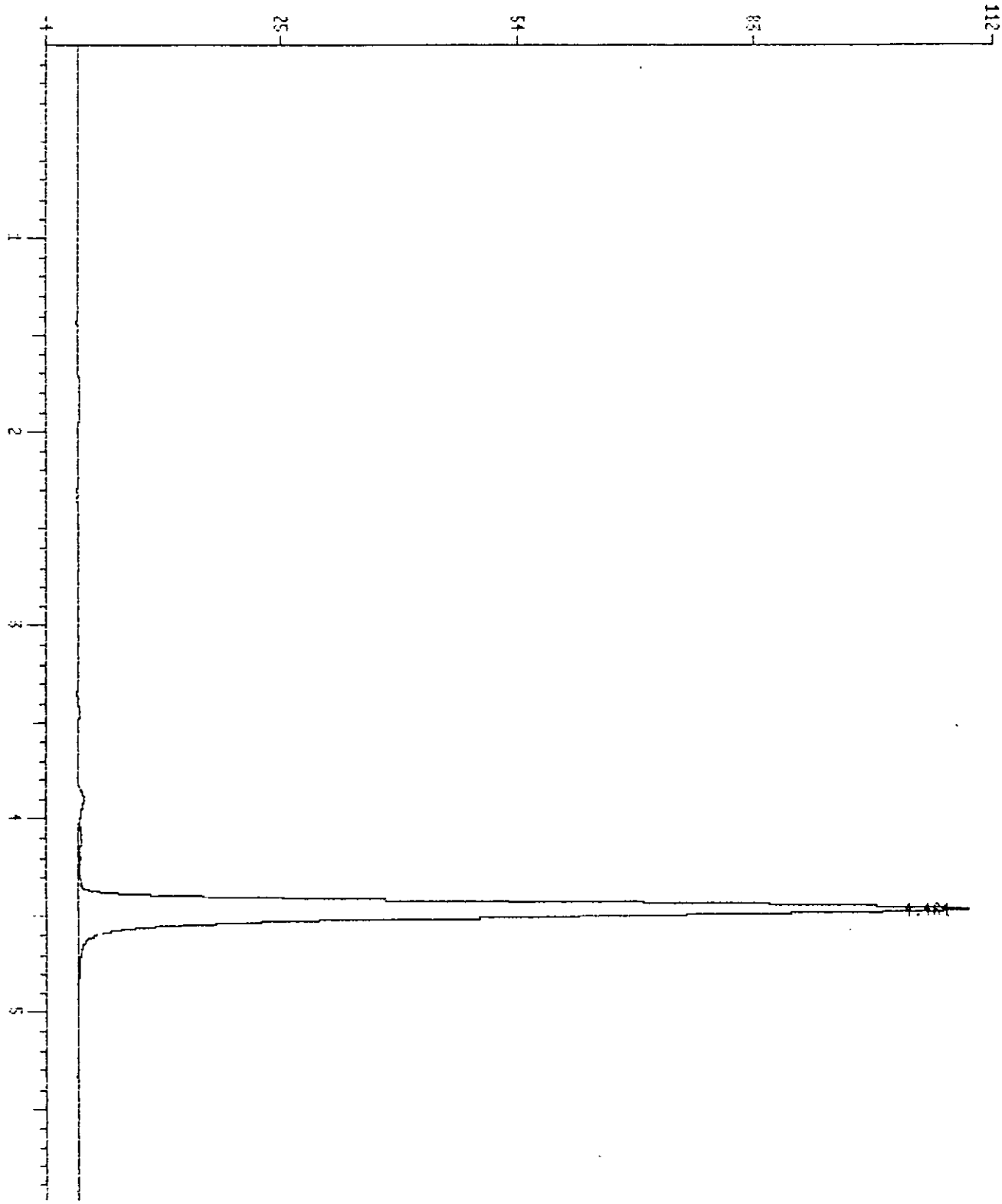
Operator: JCP 2 Apr 92 12:36 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 10 PPM
Misc Info:
Integration File Name : DATA:0401A36A.I
consisting of channels : 1. A 360,4 550,100 of 0401A36A.D
Sequence Index: 1 Bottle Number : 36 Repetition Number: 1

A 360,4 550,100 of 0401A36A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.463	VB	602.90	109.02	100.00	100.00	0.096	0.82

147

1: LC A 360,4 550,100 of 0401A368.D



End of plot Time = 0.00 to 5.99 minutes Chart speed = 3.33 cm/min

148

*** Area Percent ***

Report by Signal

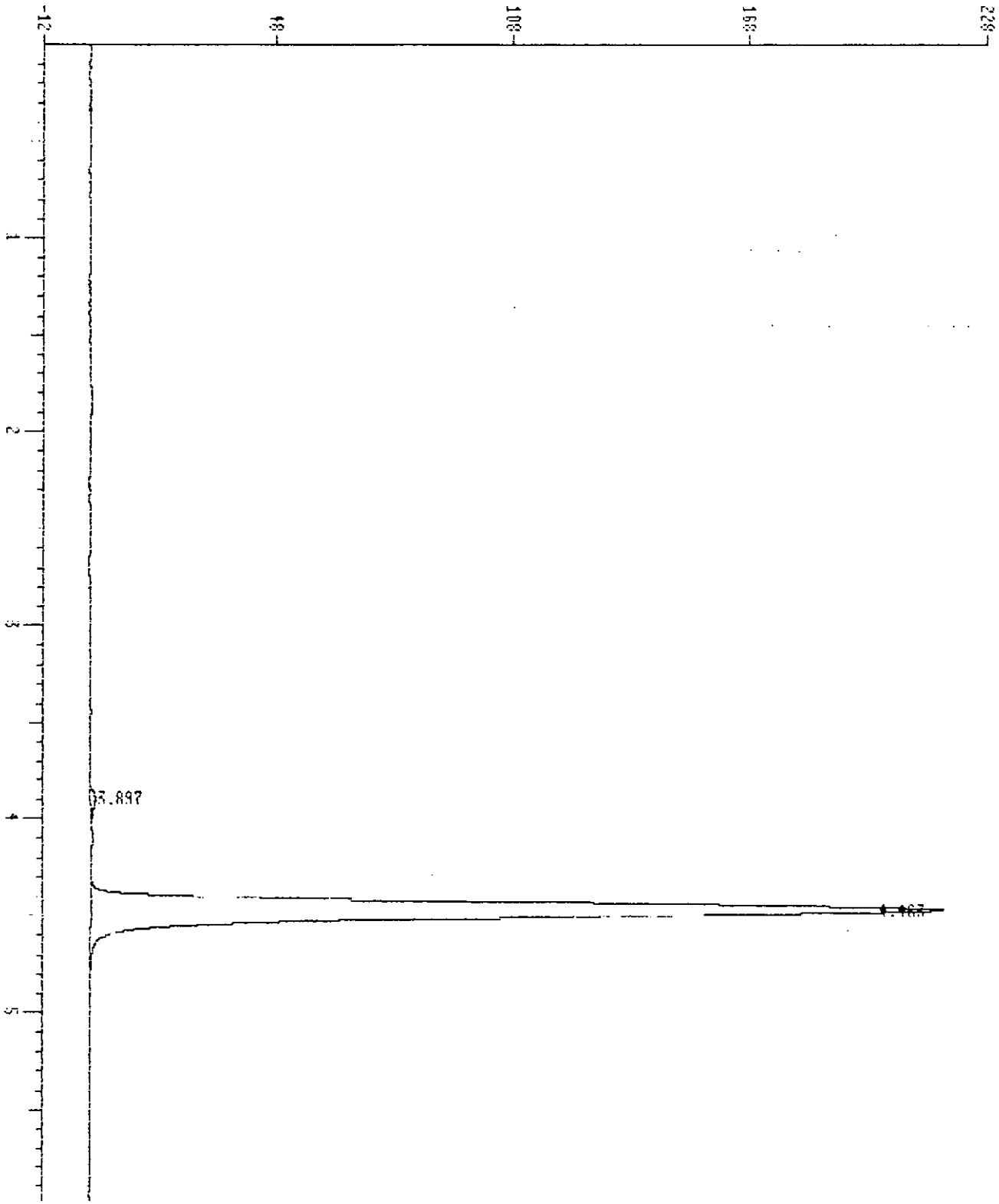
Operator: JCP 2 Apr 92 12:44 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 10 PPM
Misc Info:
Integration File Name : DATA:0401A36B.I
consisting of channels : 1. A 360,4 550,100 of 0401A36B.D
Sequence Index: 1 Bottle Number : 36 Repetition Number: 2

A 360,4 550,100 of 0401A36B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.461	VB	603.77	109.02	100.00	100.00	0.086	0.92

149

1: LC A 360,4 550,100 of 0401A37A.D



End of plot. Time - 0.00 to 5.98 minutes Chart speed - 3.33 cm/min

251

*** Area Percent ***

Report by Signal

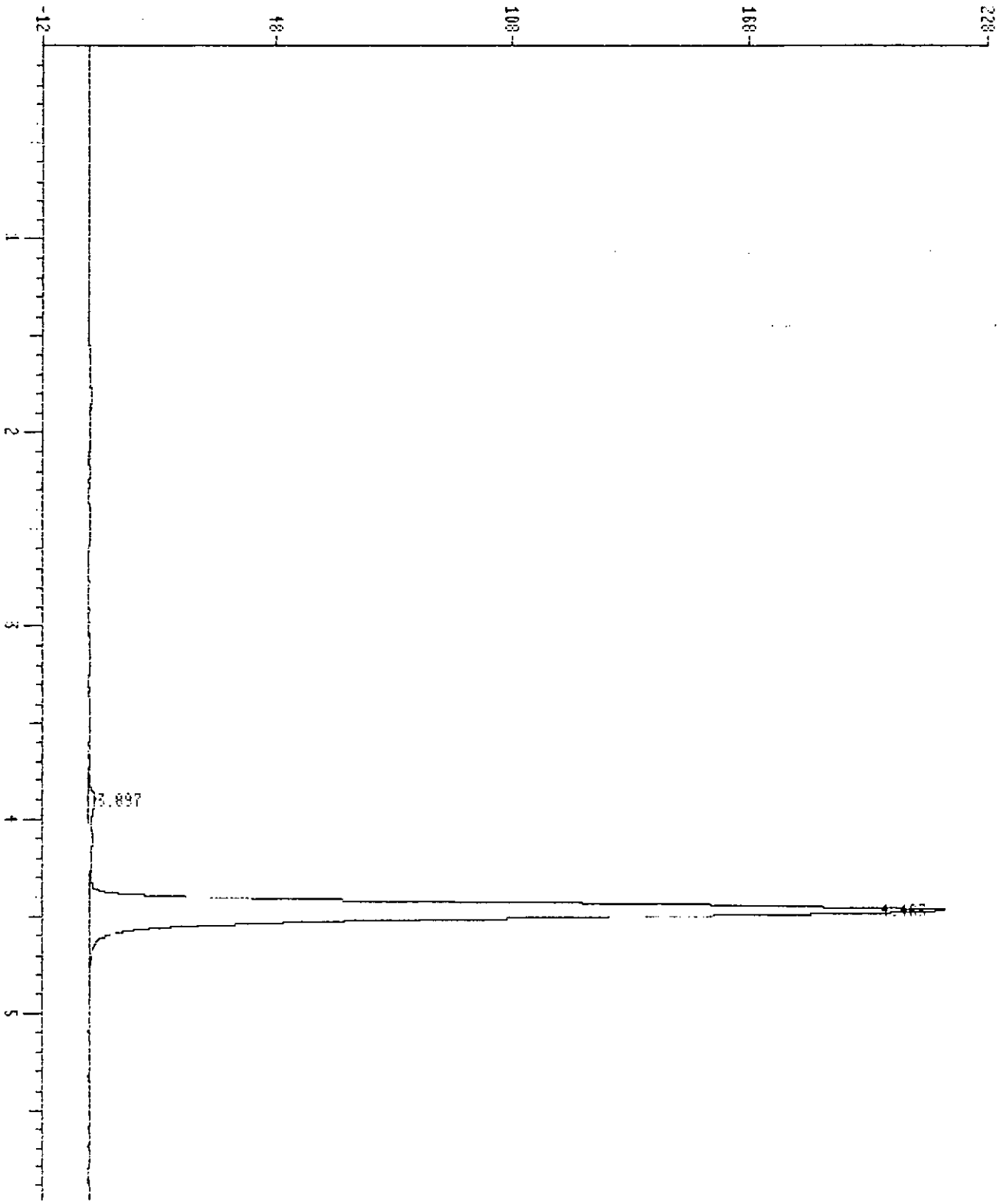
Operator: JCP 2 Apr 92 12:53 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 20 PPM
Misc Info:
Integration File Name : DATA:0401A37A.I
consisting of channels : 1. A 360,4 550,100 of 0401A37A.D
Sequence Index: 1 Bottle Number : 37 Repetition Number: 1

A 360,4 550,100 of 0401A37A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.897	BV	8.1243	1.2932	0.68	100.00	0.095	0.71
4.463	BB	1185.61	217.30	99.32	100.00	0.085	0.80

151

1: LC A 360,4 550,100 of 0401A37B.D



151

*** Area Percent ***

Report by Signal

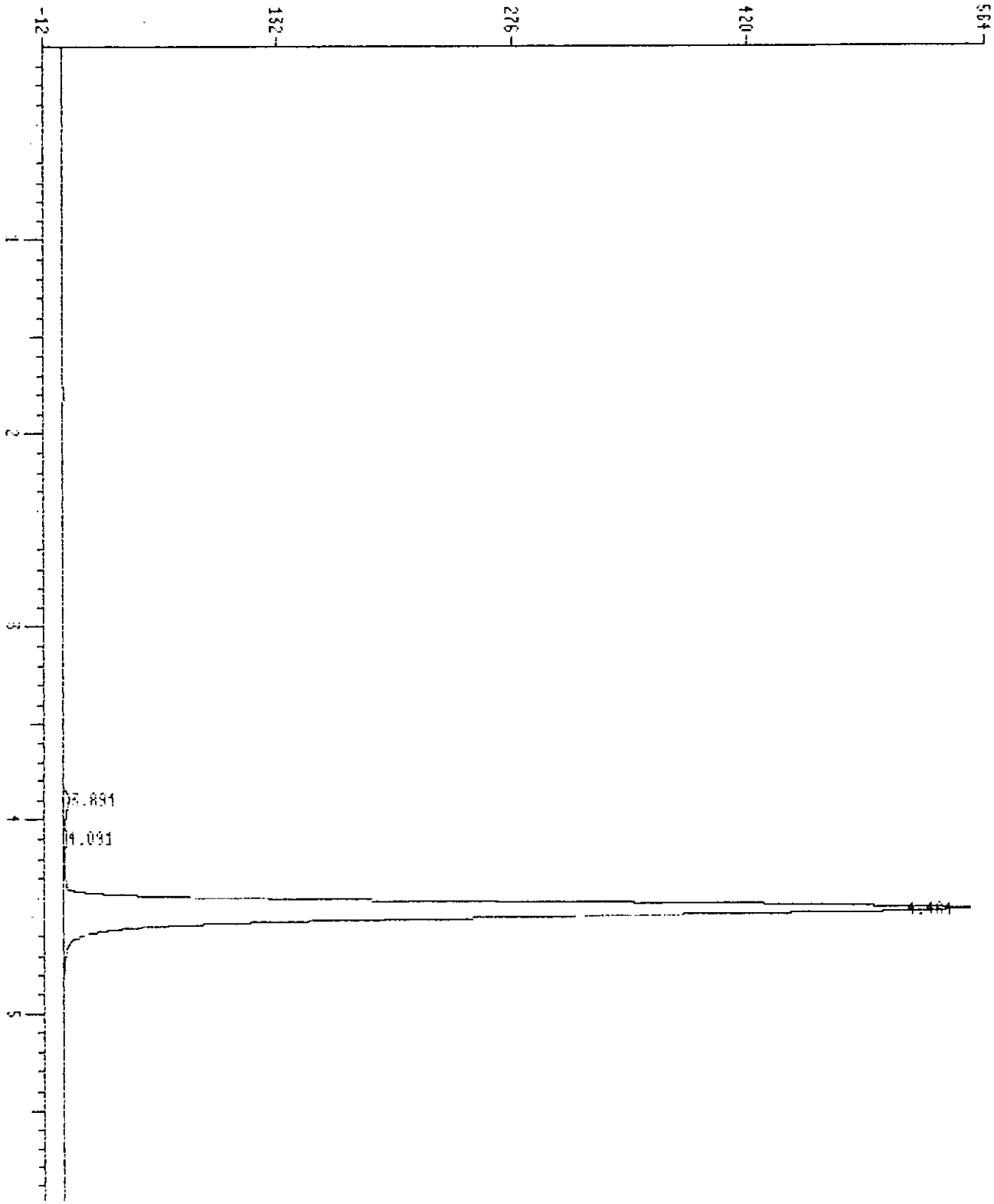
Operator: JCP 2 Apr 92 1:02 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 20 PPM
Misc Info:
Integration File Name : DATA:0401A37B.I
consisting of channels : 1. A 360,4 550,100 of 0401A37B.D
Sequence Index: 1 Bottle Number : 37 Repetition Number: 2

A 360,4 550,100 of 0401A37B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.897	BV	12.7800	1.5893	1.06	100.00	0.116	0.57
4.463	VB	1197.19	217.67	98.94	100.00	0.085	0.81

153

1: LC A 360,4 550,100 of 0401A39A.D



154

*** Area Percent ***

Report by Signal

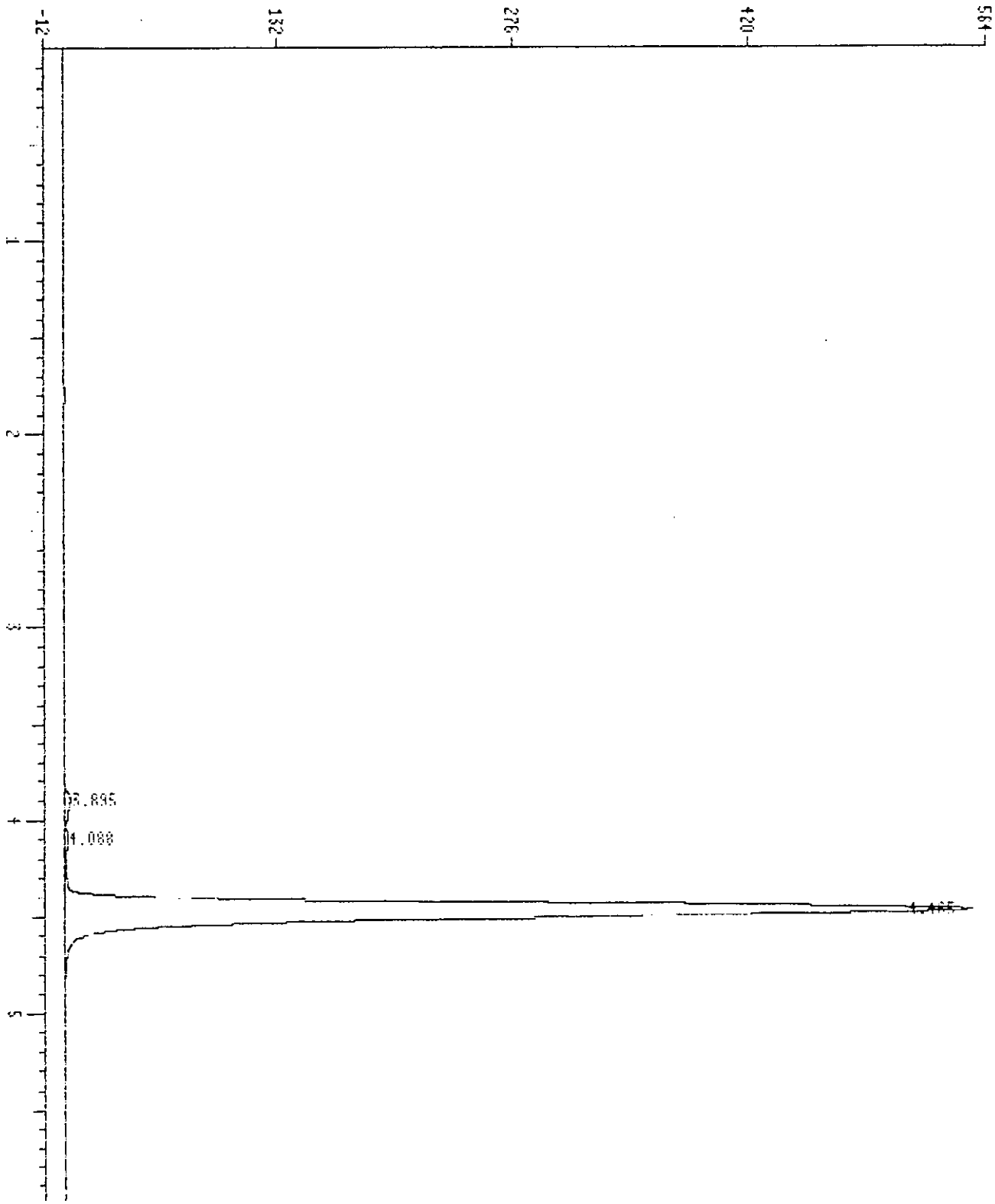
Operator: JCP 2 Apr 92 1:10 am
Method File Name : DNPHIII.M
Sample Info : STANDARD: 50 PPM
Misc Info:
Integration File Name : DATA:0401A38A.I
consisting of channels : 1. A 360,4 550,100 of 0401A38A.D
Sequence Index: 1 Bottle Number : 38 Repetition Number: 1

A 360,4 550,100 of 0401A38A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.991	BV	29.1851	3.6825	0.94	100.00	0.115	0.52
4.091	VV	21.4836	1.8958	0.69	100.00	0.153	0.42
4.461	VB	3046.53	554.81	98.36	100.00	0.085	0.80

155

1: LC A 360,4 550,100 of 0401A38B.D



158

*** Area Percent ***

Report by Signal

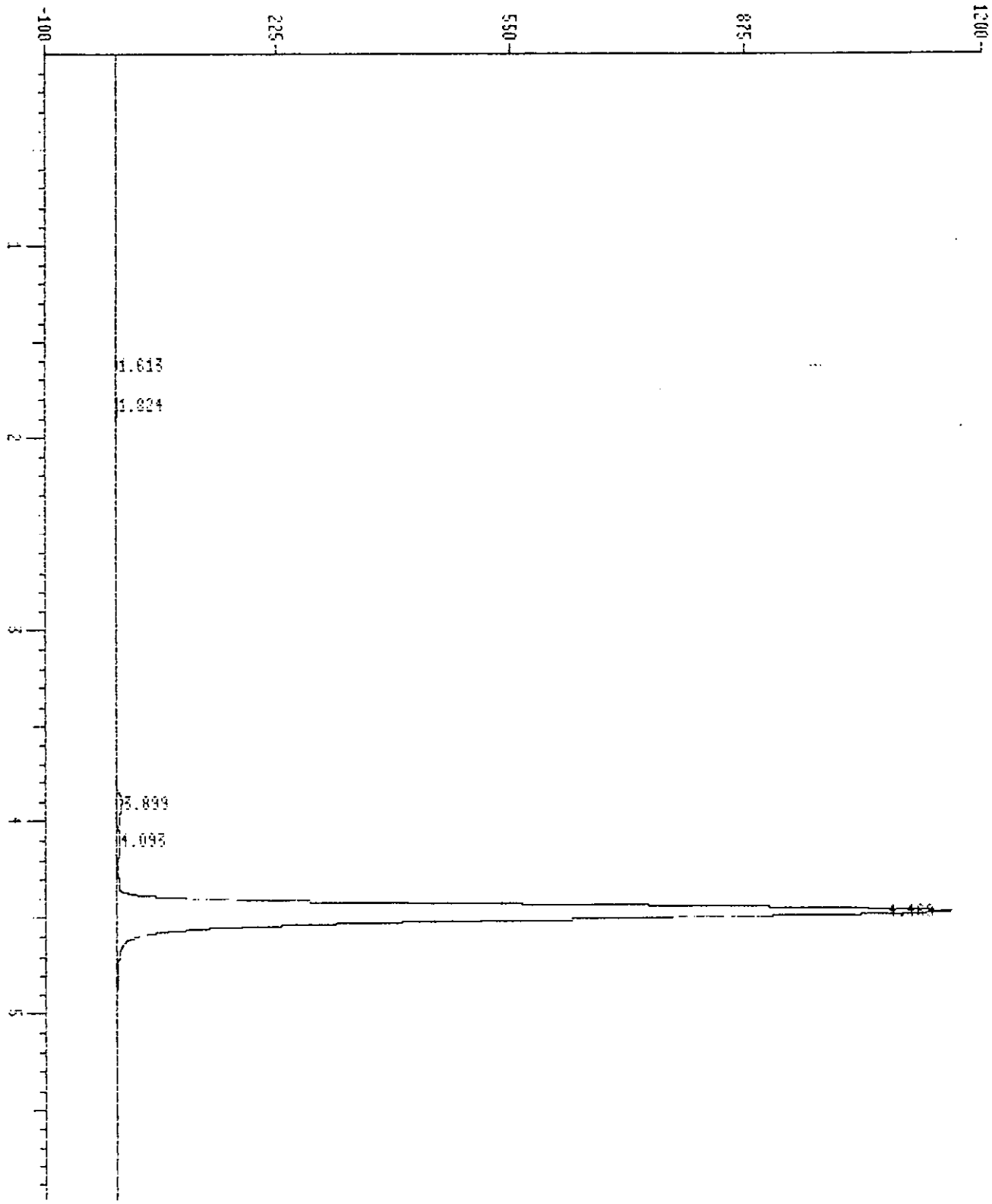
Operator: JCP 2 Apr 92 1:19 am
Method File Name : DNPHIII.M
Sample Info : STANDARD: 50 PPM
Misc Info:
Integration File Name : DATA:0401A38B.I
consisting of channels : 1. A 360,4 550,100 of 0401A38B.D
Sequence Index: 1 Bottle Number : 38 Repetition Number: 2

A 360,4 550,100 of 0401A38B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.895	BV	29.3045	3.6044	0.91	100.00	0.112	0.52
4.088	VV	19.4714	1.8355	0.63	100.00	0.153	0.42
4.465	VB	3048.02	554.43	98.46	100.00	0.085	0.80

157

1: LC A 360,4 550,100 of 0401A39A.D



*** Area Percent ***

Report by Signal

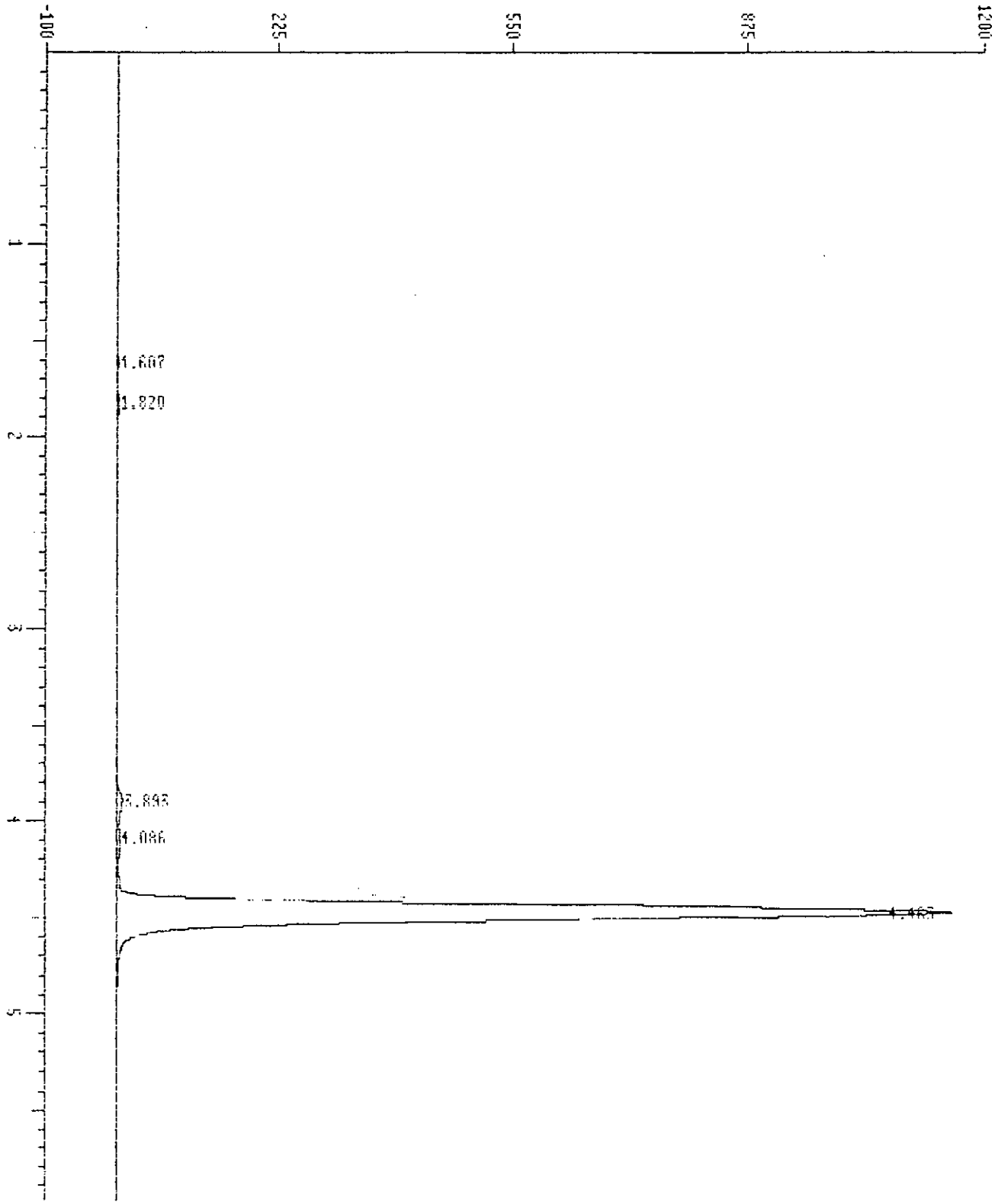
Operator: JCP 2 Apr 92 1:28 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 100 PPM
Misc Info:
Integration File Name : DATA:0401A39A.I
consisting of channels : 1. A 360,4 550,100 of 0401A39A.D
Sequence Index: 1 Bottle Number : 39 Repetition Number: 1

A 360,4 550,100 of 0401A39A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.613	BV	9.2249	1.3771	0.14	100.00	0.109	0.42
1.824	VB	22.3963	2.3538	0.35	100.00	0.129	0.45
3.899	BV	61.7687	7.6845	0.96	100.00	0.115	0.51
4.093	VV	42.8352	3.8752	0.66	100.00	0.148	0.38
4.459	VB	6327.20	1156.84	97.89	100.00	0.084	0.80

159

1: LC A 360,4 550,100 of 0401A39B.D



*** Area Percent ***

Report by Signal

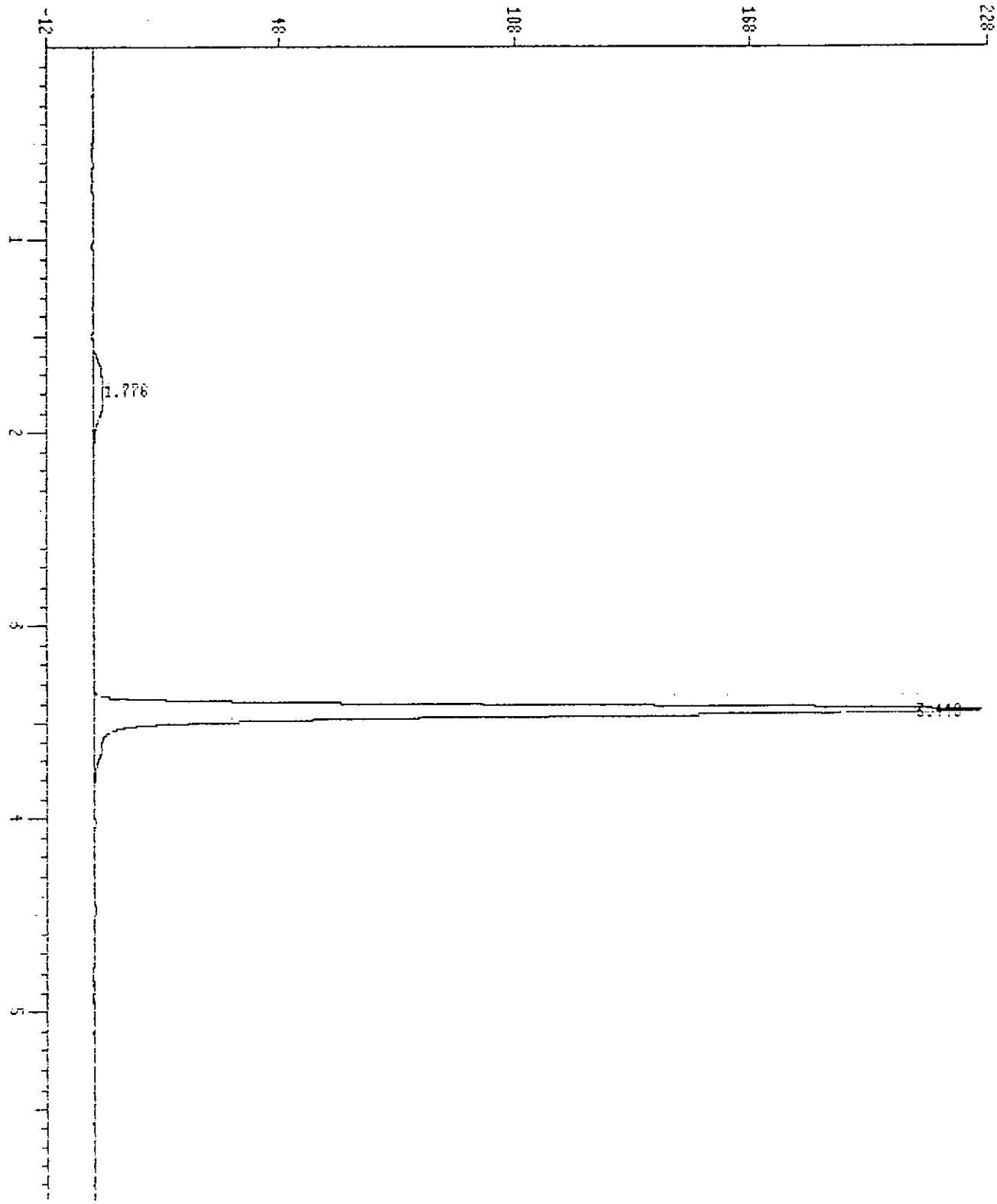
Operator: JCP 2 Apr 92 1:37 am
Method File Name : DNPHIII.M
Sample Info : STANDARD: 100 PPM
Misc Info:
Integration File Name : DATA:0401A39B.I
consisting of channels : 1. A 360,4 550,100 of 0401A39B.D
Sequence Index: 1 Bottle Number : 39 Repetition Number: 2

A 360,4 550,100 of 0401A39B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.607	BV	10.7299	1.4222	0.17	100.00	0.115	0.48
1.820	VB	21.5518	2.3732	0.33	100.00	0.123	0.39
3.893	BV	61.3057	7.6275	0.95	100.00	0.116	0.53
4.085	VV	44.4508	3.9386	0.69	100.00	0.163	0.39
4.463	VB	6336.20	1157.05	97.87	100.00	0.084	0.80

161

1: LC A 360,4 550,100 of 0401A40A.D



162

*** Area Percent ***

Report by Signal

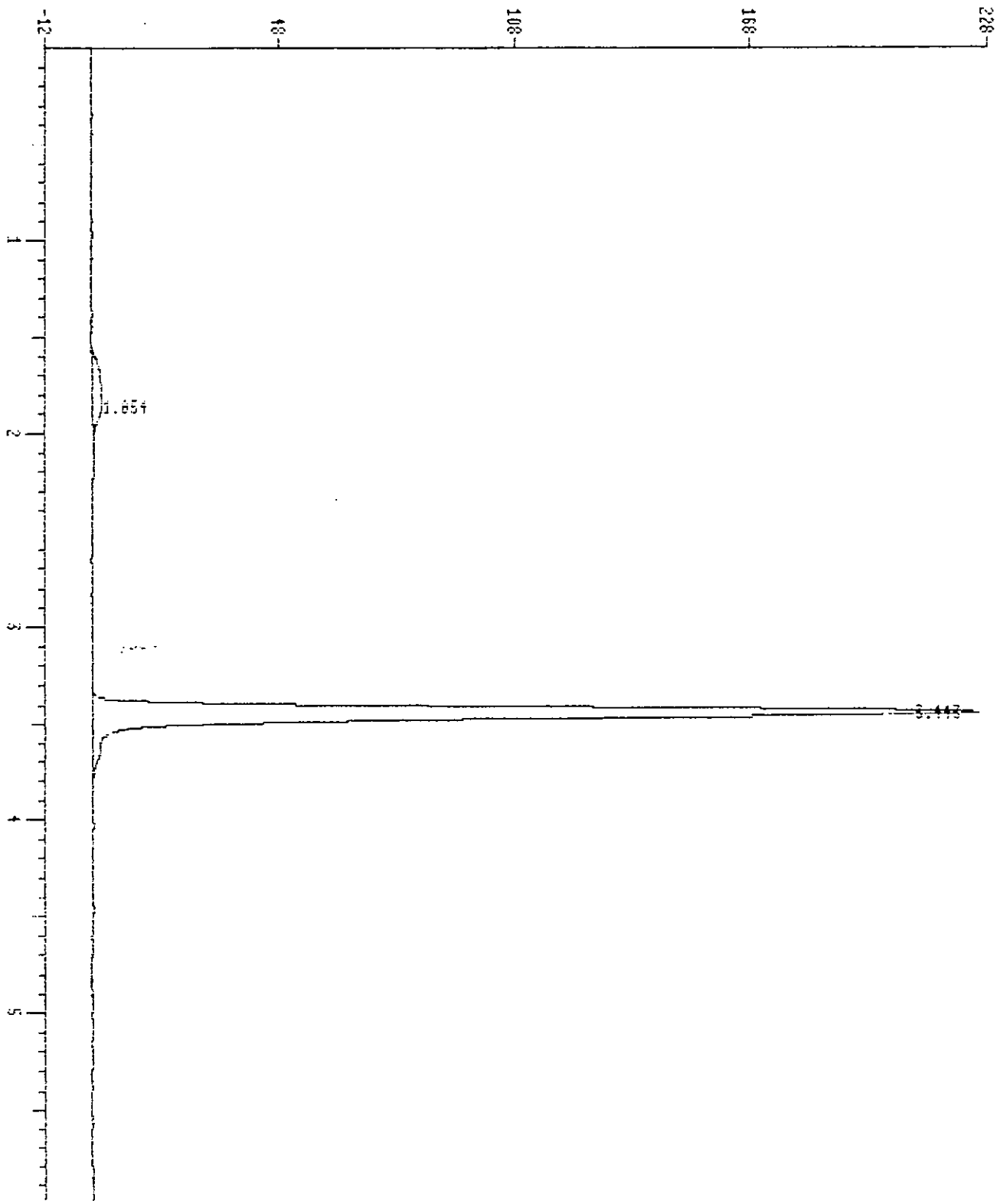
Operator: JCP 2 Apr 92 1:45 am
Method File Name : DNPHIII.M
Sample Info : #31
Misc Info:
Integration File Name : DATA:0401A40A.I
consisting of channels : 1. A 360,4 550,100 of 0401A40A.D
Sequence Index: 1 Bottle Number : 40 Repetition Number: 1

A 360,4 550,100 of 0401A40A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.776	BB	49.3751	2.4963	4.90	100.00	0.281	0.92
3.440	BB	938.61	226.27	95.10	100.00	0.065	0.83

167

1: LC A 360,4 550,100 of 0401A40B.D



164

*** Area Percent ***

Report by Signal

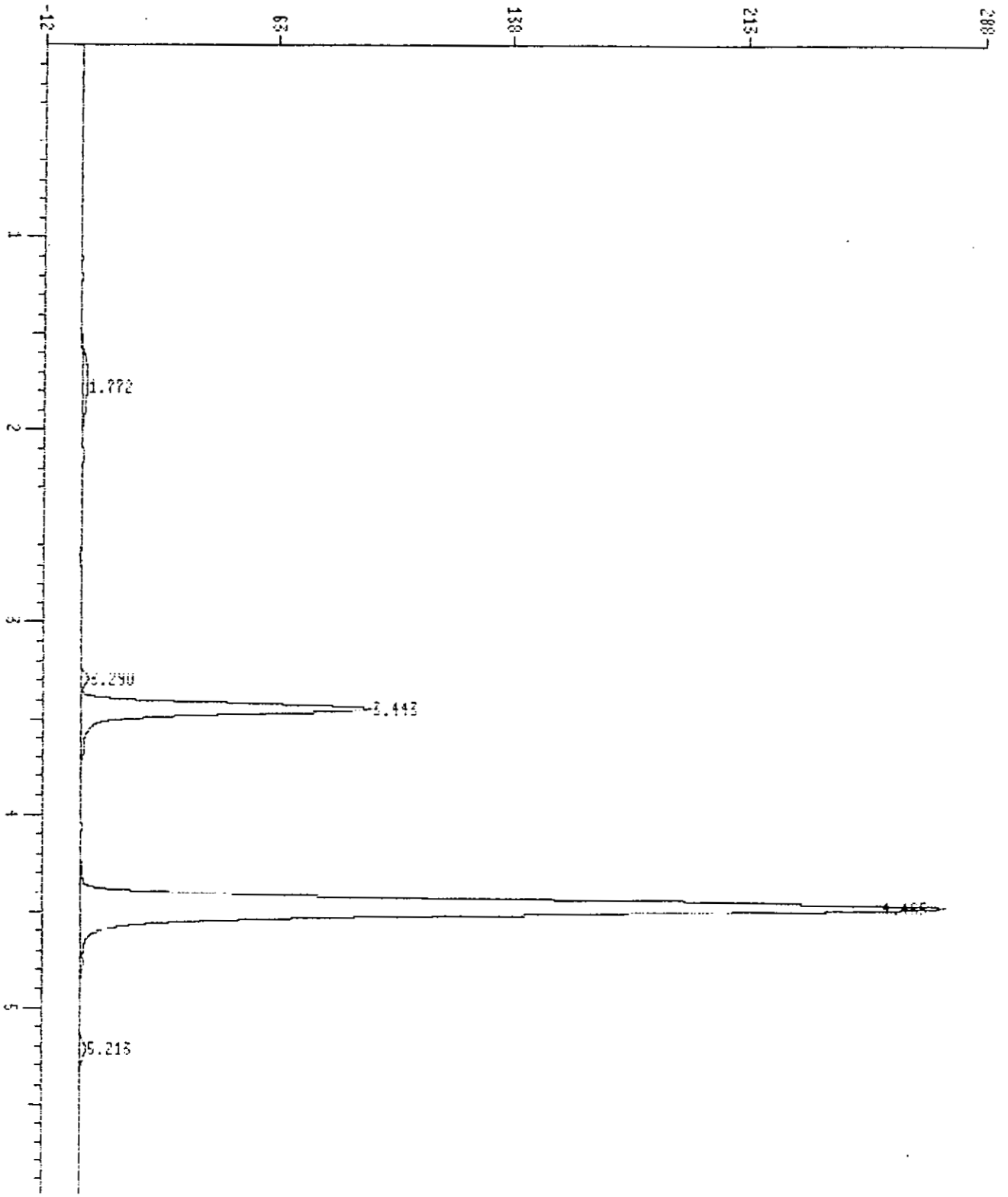
Operator: JCP 2 Apr 92 1:54 am
Method File Name : DNPHIII.M
Sample Info : #31
Misc Info:
Integration File Name : DATA:0401A40B.I
consisting of channels : 1. A 360,4 550,100 of 0401A40B.D
Sequence Index: 1 Bottle Number : 40 Repetition Number: 2

A 360,4 550,100 of 0401A40B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.854	BB	43.3677	2.2471	4.42	100.00	0.262	2.43
3.443	BB	937.85	226.30	95.58	100.00	0.065	0.83

165

1: LC A 380,4 550,100 of 0401A41A.D



166

*** Area Percent ***

Report by Signal

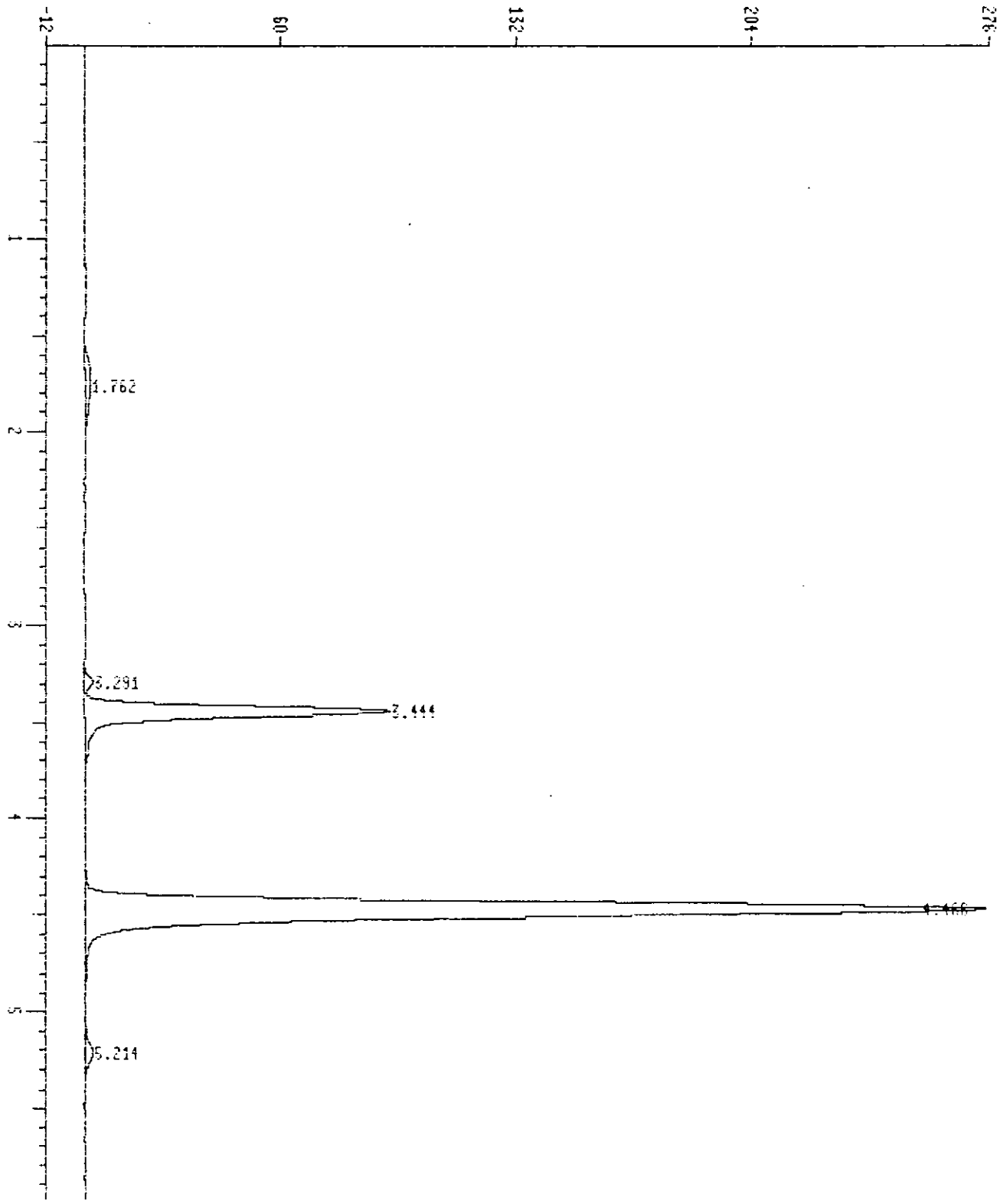
Operator: JCP 2 Apr 92 2:03 am
Method File Name : DNPHIII.M
Sample Info : #32
Misc Info:
Integration File Name : DATA:0401A41A.I
consisting of channels : 1. A 360,4 550,100 of 0401A41A.D
Sequence Index: 1 Bottle Number : 41 Repetition Number: 1

A 360,4 550,100 of 0401A41A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.772	BV	26.7362	1.4636	1.36	100.00	0.237	1.25
3.290	BV	10.2403	2.5130	0.52	100.00	0.064	0.89
3.443	VV	394.12	93.3704	19.99	100.00	0.066	0.80
4.455	VB	1527.48	276.22	77.47	100.00	0.085	0.80
5.213	BB	13.0925	2.0909	0.66	100:00	0.097	0.78

167

1: LC A 360,4 550,100 of 0401A41B.D



168

*** Area Percent ***

Report by Signal

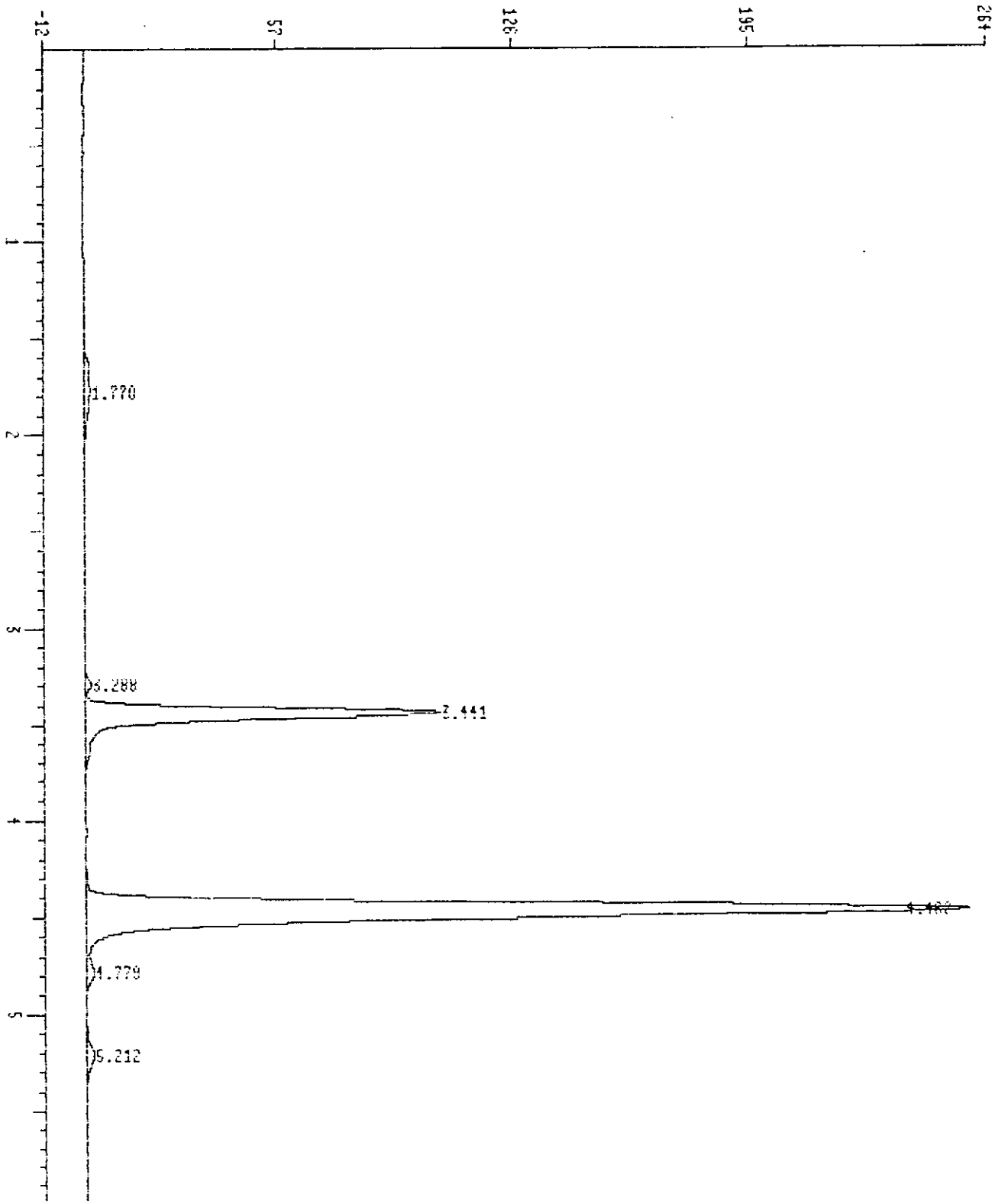
Operator: JCP 2 Apr 92 2:11 am
Method File Name : DNPHIII.M
Sample Info : #32
Misc Info:
Integration File Name : DATA:0401A41B.I
consisting of channels : 1. A 360,4 550,100 of 0401A41B.D
Sequence Index: 1 Bottle Number : 41 Repetition Number: 2

A 360,4 550,100 of 0401A41B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.762	BB	29.4159	1.5841	1.48	100.00	0.245	0.99
3.291	BV	10.5563	2.5503	0.53	100.00	0.065	0.92
3.444	VB	393.98	93.1949	19.79	100.00	0.066	0.80
4.465	BV	1533.19	276.20	77.00	100.00	0.086	0.80
5.214	VB	24.0388	2.7142	1.21	100.00	0.128	1.11

169

1: LC A 360,4 550,100 of 0401A42A.D



170

*** Area Percent ***

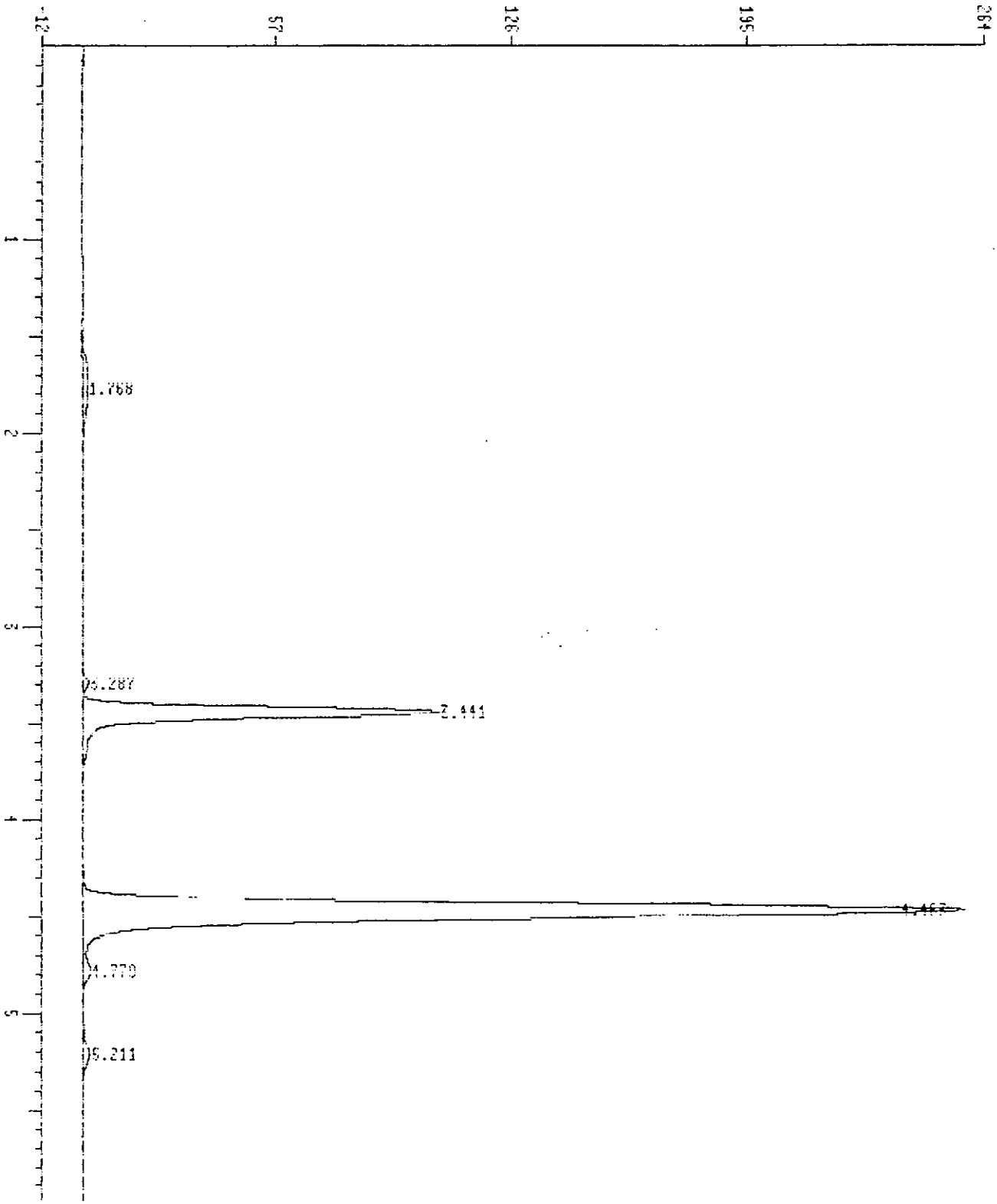
Report by Signal

Operator: JCP 2 Apr 92 2:20 am
Method File Name : DNPHIII.M
Sample Info : #33
Misc Info:
Integration File Name : DATA:0401A42A.I
consisting of channels : 1. A 350,4 550,100 of 0401A42A.D
Sequence Index: 1 Bottle Number : 42 Repetition Number: 1

A 350,4 550,100 of 0401A42A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.770	BB	37.4535	1.7584	1.93	100.00	0.274	1.22
3.299	BV	7.5557	1.8532	0.39	100.00	0.064	0.93
3.441	VV	439.06	104.67	22.59	100.00	0.065	0.90
4.482	BV	1423.56	258.92	73.25	100.00	0.085	0.80
4.778	VB	18.0373	2.3218	0.93	100.00	0.104	1.05
5.212	BB	19.6491	2.3583	1.01	100.00	0.121	0.98

1: LC A 360,4 550,100 of 0401A42B.D



172

*** Area Percent ***

Report by Signal

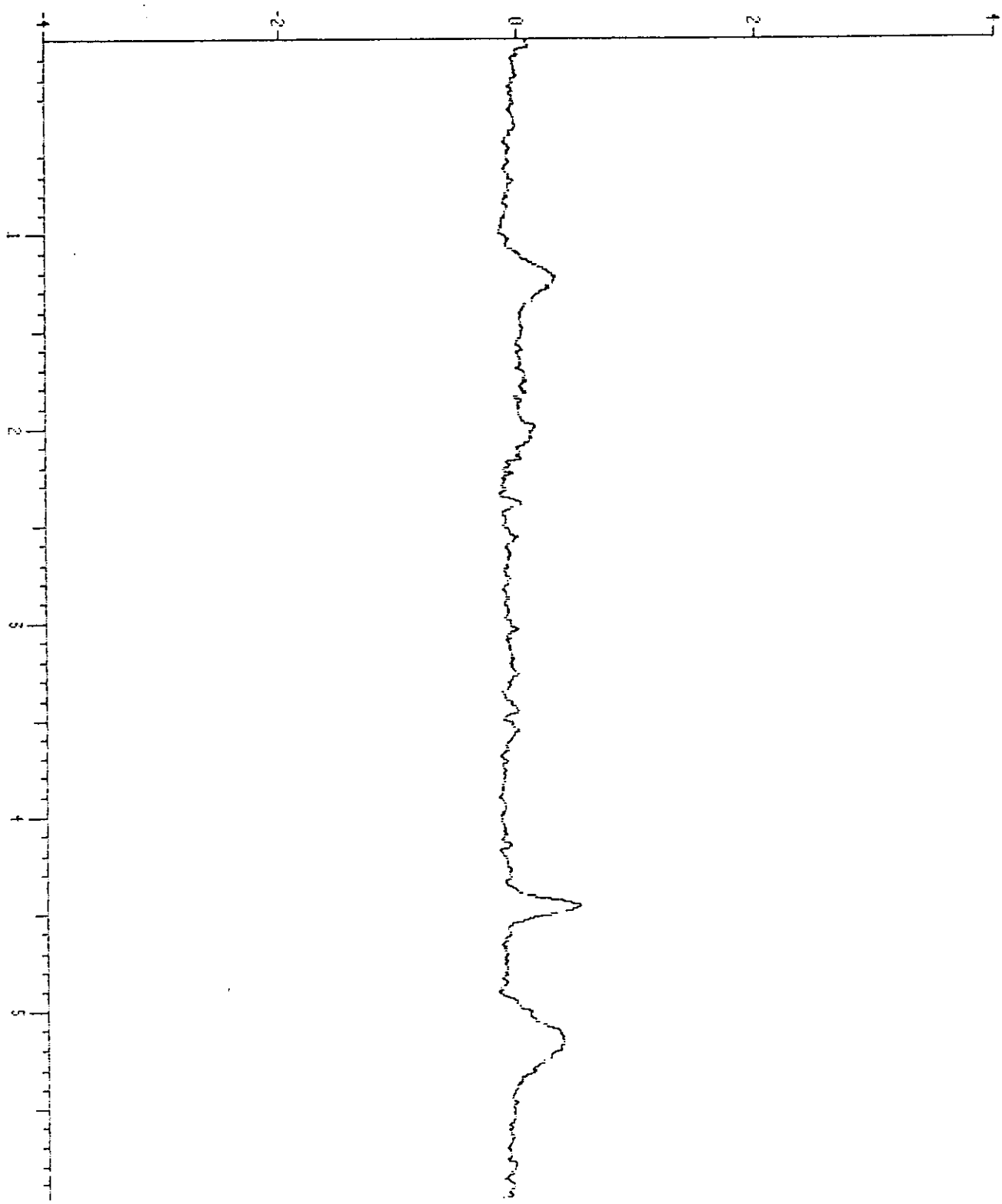
Operator: JCP 2 Apr 92 2:29 am
Method File Name : DNPHIII.M
Sample Info : #33
Misc Info:
Integration File Name : DATA:0401A42B.I
consisting of channels : 1. A 360,4 550,100 of 0401A42B.D
Sequence Index: 1 Bottle Number : 42 Repetition Number: 2

A 360,4 550,100 of 0401A42B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.758	BB	34.7559	1.6753	1.79	100.00	0.266	0.95
3.287	BV	7.5953	1.8494	0.39	100.00	0.064	0.93
3.441	VV	440.72	104.69	22.75	100.00	0.065	0.90
4.493	BV	1422.10	259.93	73.42	100.00	0.095	0.90
4.779	VB	15.3274	2.2470	0.79	100.00	0.104	1.09
5.211	BB	16.5149	2.0999	0.85	100.00	0.116	0.98

143

1: LC A 350,4 550,100 of 0401A43A.D



*** Area Percent ***

Report by Signal

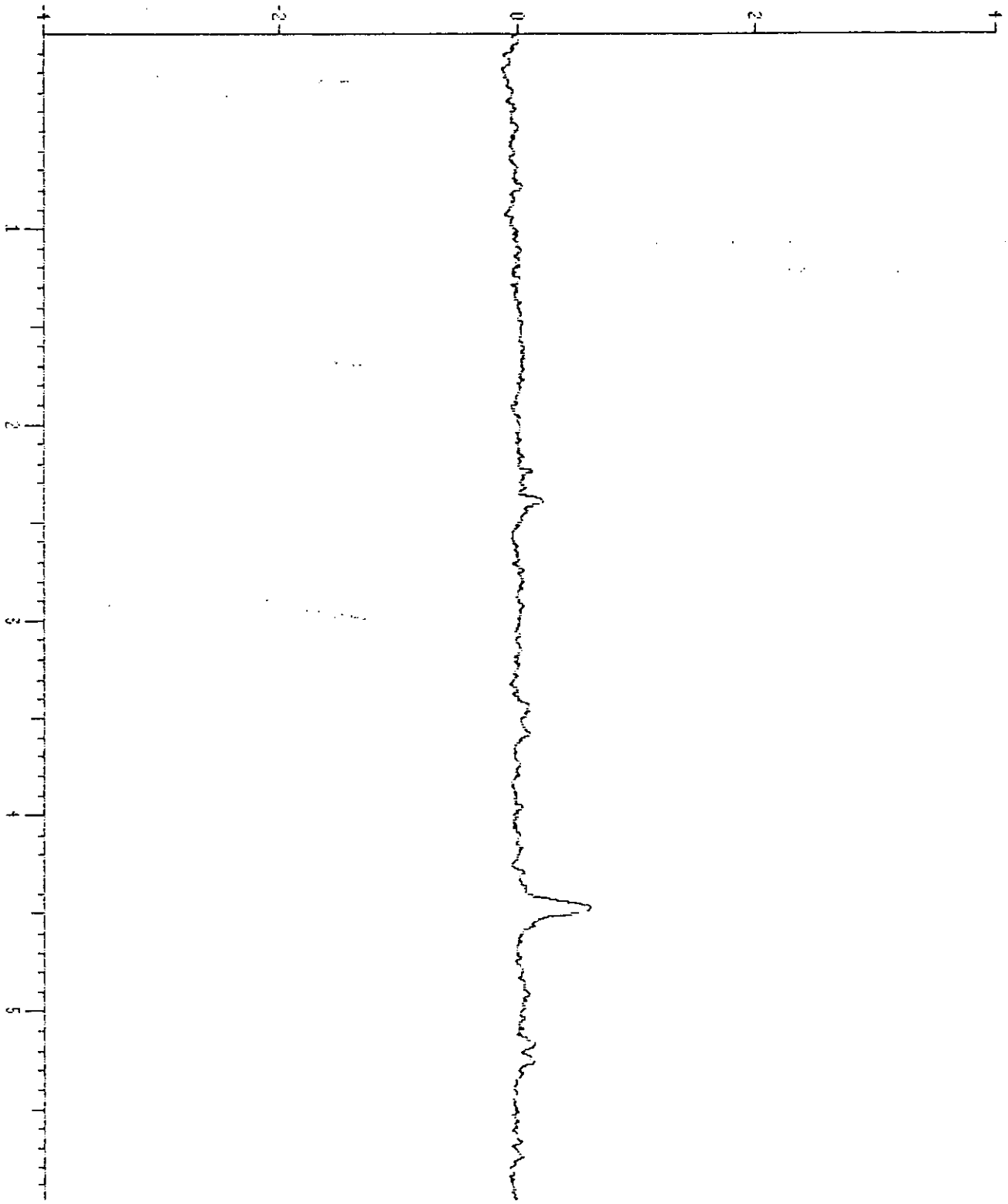
Operator: JCP 2 Apr 92 2:38 am
Method File Name : DNPHIII.M
Sample Info : #34
Misc Info:
Integration File Name : DATA:0401A43A.I
consisting of channels : 1. A 350,4 550,100 of 0401A43A.D
Sequence Index: 1 Bottle Number : 43 Repetition Number: 1

A 350,4 550,100 of 0401A43A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym

5+1

1: LC A 360,4 550,100 of 0401A43B.D



gtl

*** Area Percent ***

Report by Signal

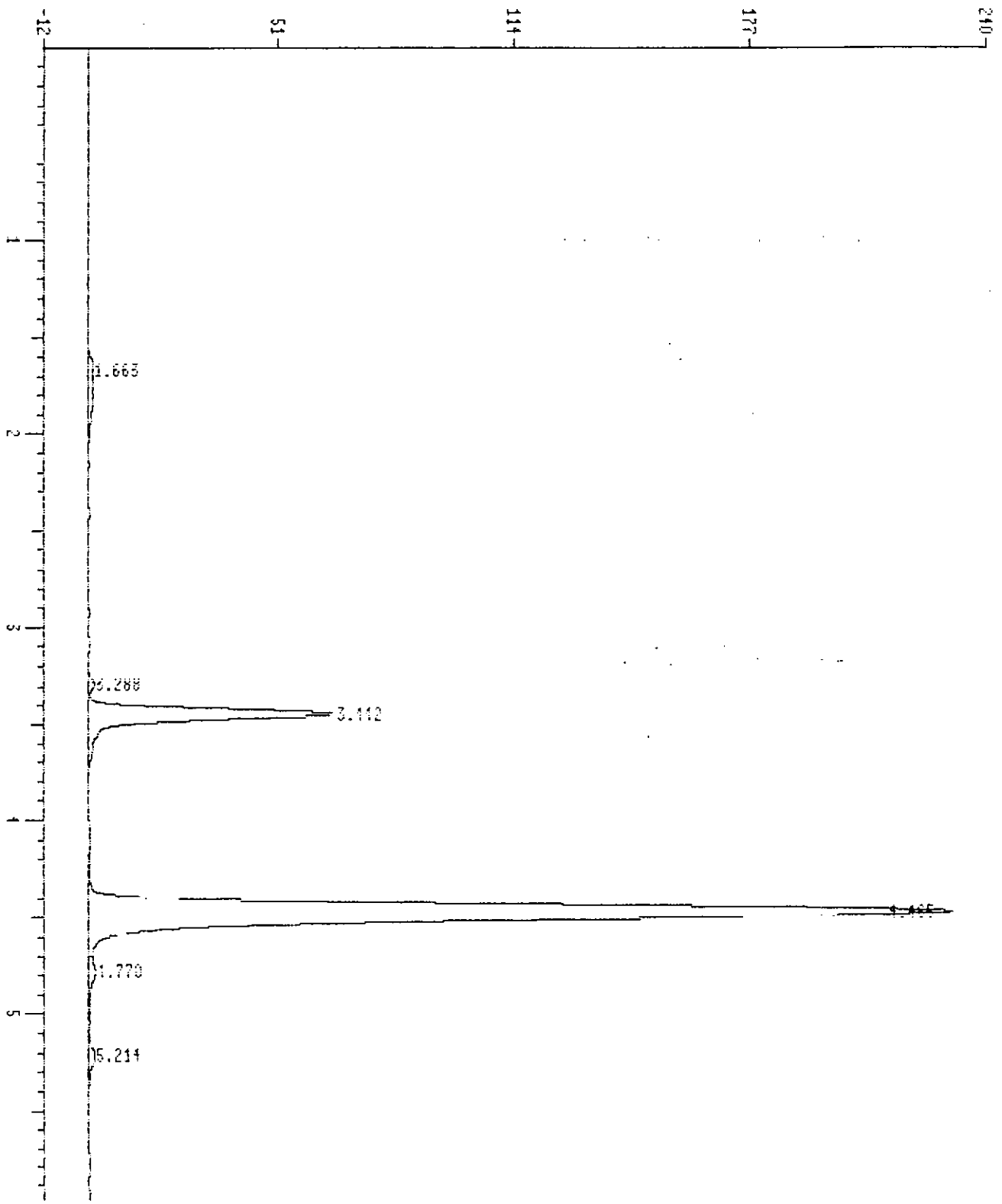
Operator: JCP 2 Apr 92 2:47 am
Method File Name : DNPHIII.M
Sample Info : #34
Misc Info:
Integration File Name : DATA:0401A438.I
consisting of channels : 1. A 360,4 550,100 of 0401A439.D
Sequence Index: 1 Bottle Number : 43 Repetition Number: 2

A 360,4 550,100 of 0401A439.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym

174

1: LC A 390,4 550,100 of 0401A44A.D



178

*** Area Percent ***

Report by Signal

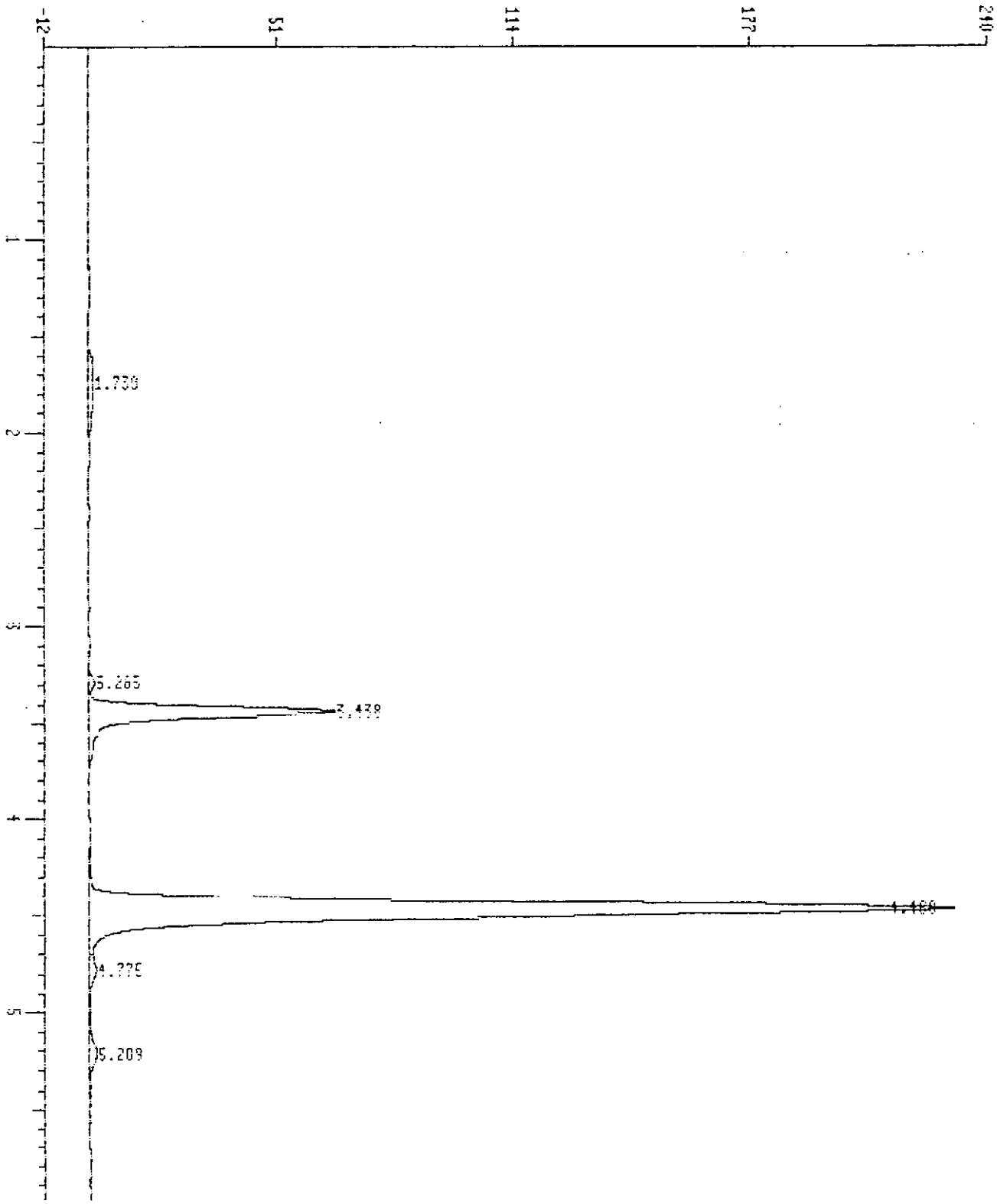
Operator: JCP 2 Apr 92 2:56 am
Method File Name : DNPHIII.M
Sample Info : #35
Misc Info:
Integration File Name : DATA:0401A44A.I
consisting of channels : 1. A 360,4 550,100 of 0401A44A.D
Sequence Index: 1 Bottle Number : 44 Repetition Number: 1

A 360,4 550,100 of 0401A44A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.693	BB	25.3956	1.3560	1.58	100.00	0.292	0.30
3.289	VV	5.2435	1.5160	0.39	100.00	0.064	0.95
3.442	VV	280.01	65.9007	17.45	100.00	0.066	0.79
4.455	VV	1269.25	230.99	79.09	100.00	0.095	0.91
4.778	VB	12.9957	1.7257	0.80	100.00	0.112	0.92
5.214	BV	11.1001	1.5410	0.69	100.00	0.105	0.72

179

1: LC A 350,4 550,100 of 0401A44B.D



*** Area Percent ***

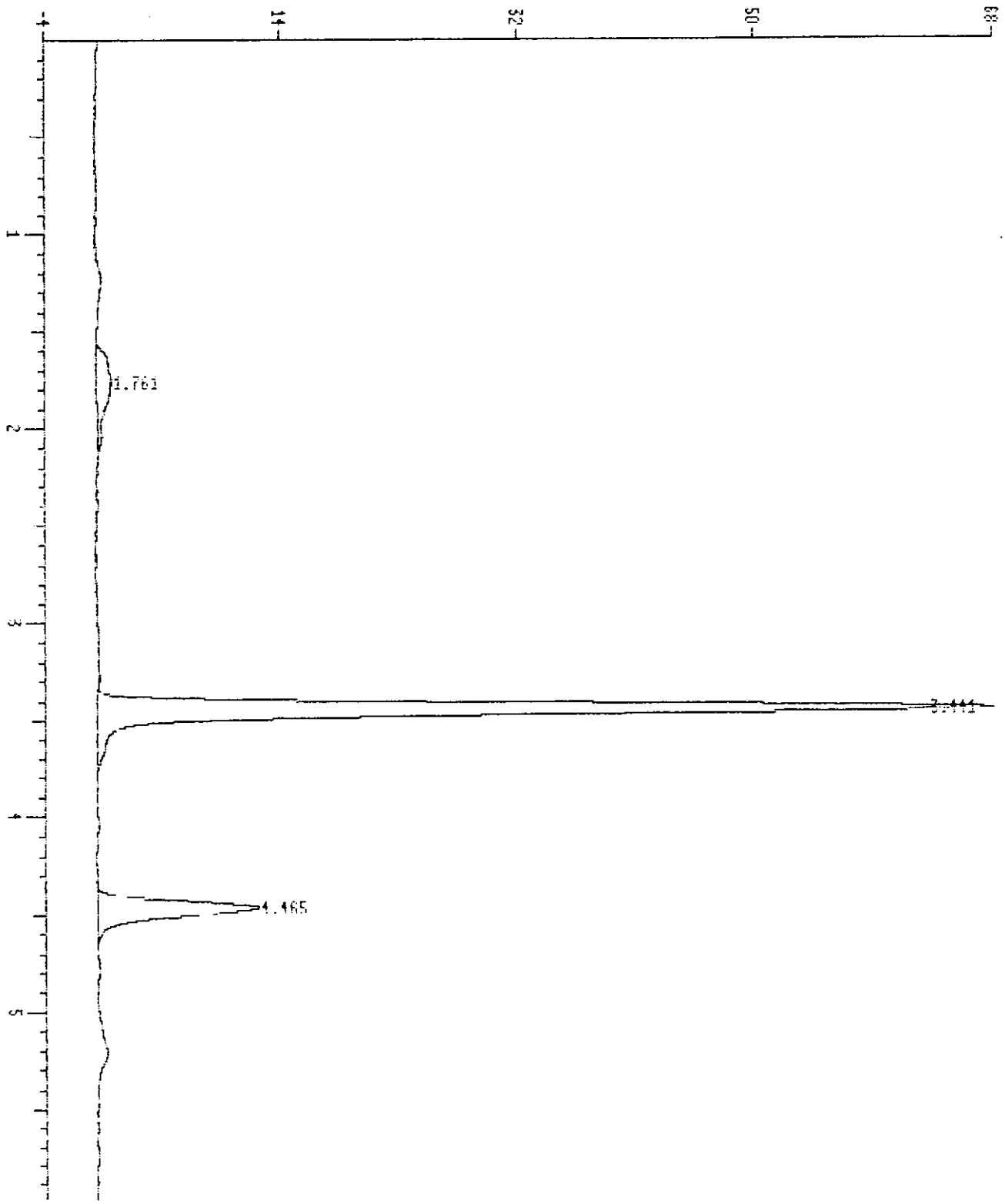
Report by Signal

Operator: JCP 2 Apr 92 3:05 am
Method File Name : DNPHIII.M
Sample Info : #35
Misc Info:
Integration File Name : DATA:0401A44B.I
consisting of channels : 1. A 350,4 550,100 of 0401A44B.D
Sequence Index: 1 Bottle Number : 44 Repetition Number: 2

A 350,4 550,100 of 0401A44B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.739	BB	26.9997	1.2951	1.65	100.00	0.322	0.70
3.285	BV	6.0259	1.5233	0.37	100.00	0.063	0.95
3.439	VV	280.44	55.0025	17.29	100.00	0.055	0.72
4.450	VV	1272.53	230.52	78.47	100.00	0.085	0.81
4.775	VV	14.8152	1.8434	0.91	100.00	0.115	0.79
5.209	VB	20.7977	2.1241	1.28	100.00	0.138	1.09

1: LC A 350,4 550,100 of 0401A45A.D



28

*** Area Percent ***

Report by Signal

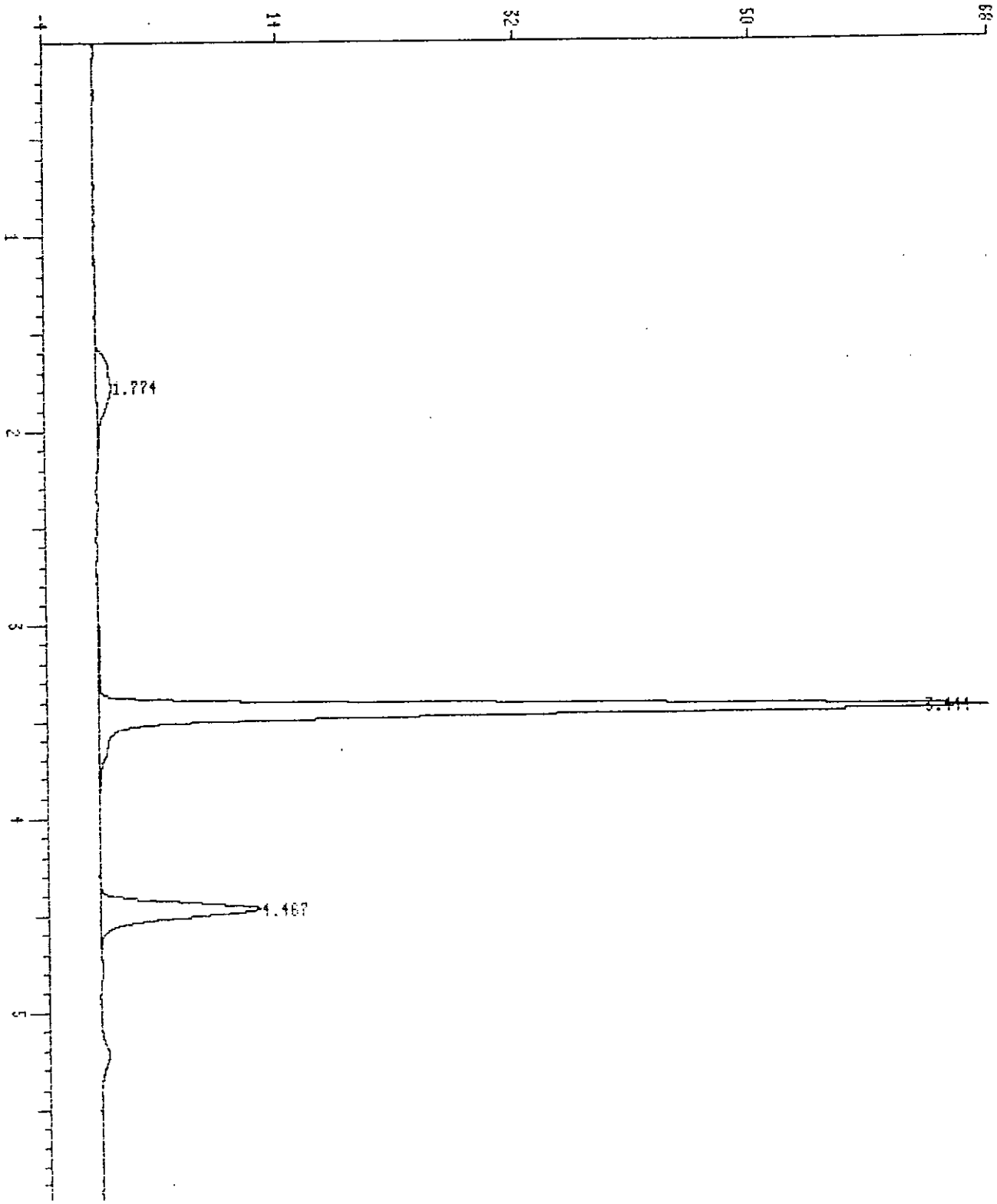
Operator: JCP 2 Apr 92 3:13 am
Method File Name : DNPHIII.M
Sample Info : #36
Misc Info:
Integration File Name : DATA:0401A45A.I
consisting of channels : 1. A 360,4 550,100 of 0401A45A.D
Sequence Index: 1 Bottle Number : 45 Repetition Number: 1

A 360,4 550,100 of 0401A45A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.761	BB	20.8347	1.0743	5.62	100.00	0.254	0.80
3.441	BB	282.62	68.0639	76.21	100.00	0.065	0.83
4.465	BV	67.3691	12.2816	18.17	100.00	0.085	0.80

183

1: LC A 360,4 550,100 of 0401A45B.D



184

*** Area Percent ***

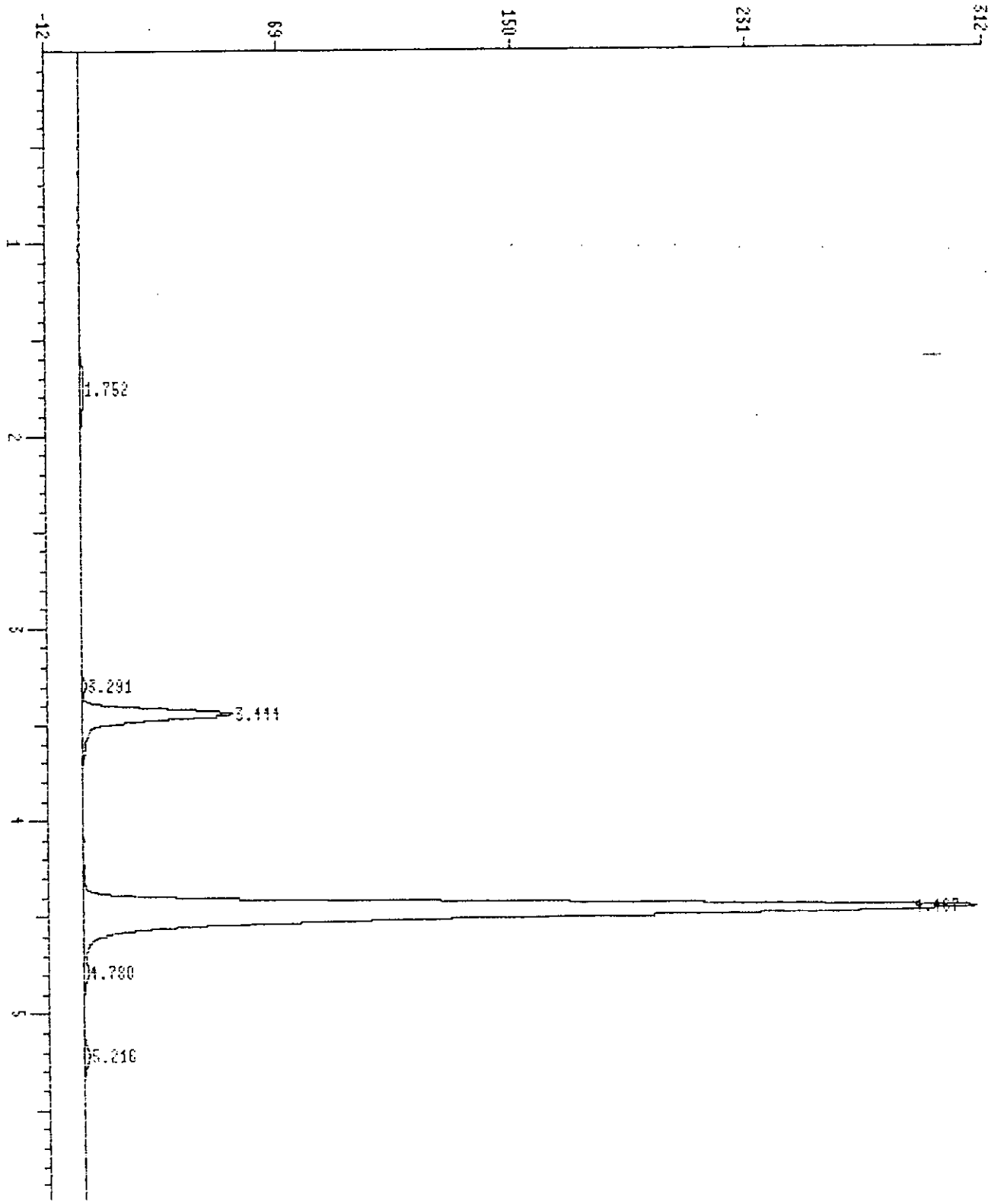
Report by Signal

Operator: JCP 2 Apr 92 3:22 am
Method File Name : DNPHIII.M
Sample Info : #36
Misc Info:
Integration File Name : DATA:0401A45B.I
consisting of channels : 1. A 360,4 550,100 of 0401A45B.D
Sequence Index: 1 Bottle Number : 45 Repetition Number: 2

A 360,4 550,100 of 0401A45B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.774	BB	18.8413	1.1197	5.08	100.00	0.231	1.13
3.444	BB	284.44	67.8780	76.74	100.00	0.065	0.85
4.467	BB	67.3809	12.3001	18.18	100.00	0.085	0.81

1: LC A 360,4 550,100 of 0401A46A.D



*** Area Percent ***

Report by Signal

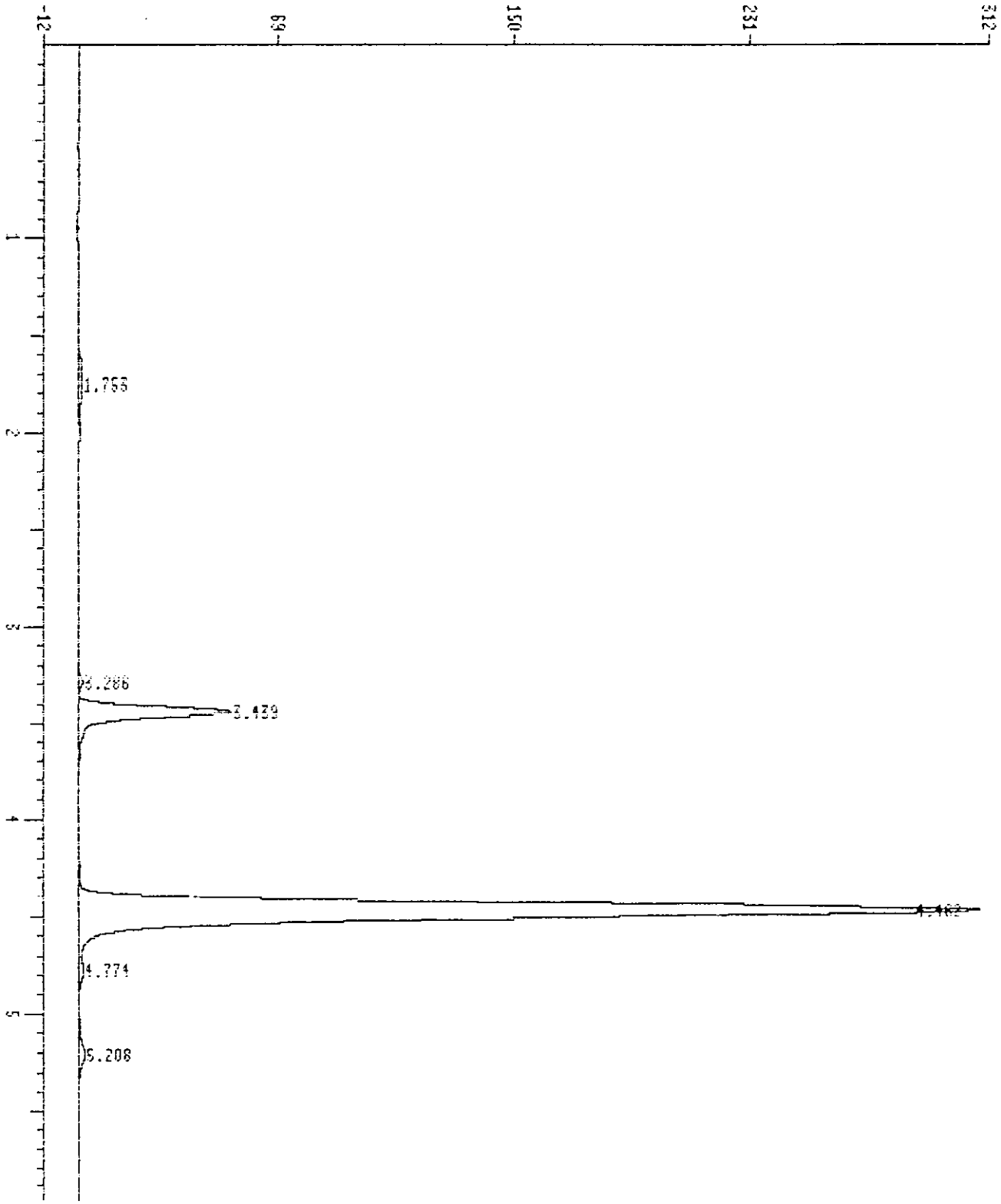
2 Apr 92 3:31 am

Operator: JCP
Method File Name : DNPHIII.M
Sample Info : #37
Misc Info:
Integration File Name : DATA:0401A46A.I
consisting of channels : 1. A 360,4 550,100 of 0401A46A.D
Sequence Index: 1 Bottle Number : 46 Repetition Number: 1

A 360,4 550,100 of 0401A46A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.752	BB	20.0663	1.1009	1.01	100.00	0.245	1.02
3.291	BV	7.1380	1.7334	0.36	100.00	0.064	0.90
3.444	VB	225.92	52.6615	11.40	100.00	0.066	0.78
4.467	BV	1702.84	309.61	85.95	100.00	0.085	0.81
4.780	VB	12.3894	1.5941	0.63	100.00	0.110	0.96
5.216	BB	12.9427	1.8526	0.65	100.00	0.106	0.77

1: LC A 350,4 550,100 of 0401A45B.D



8

*** Area Percent ***

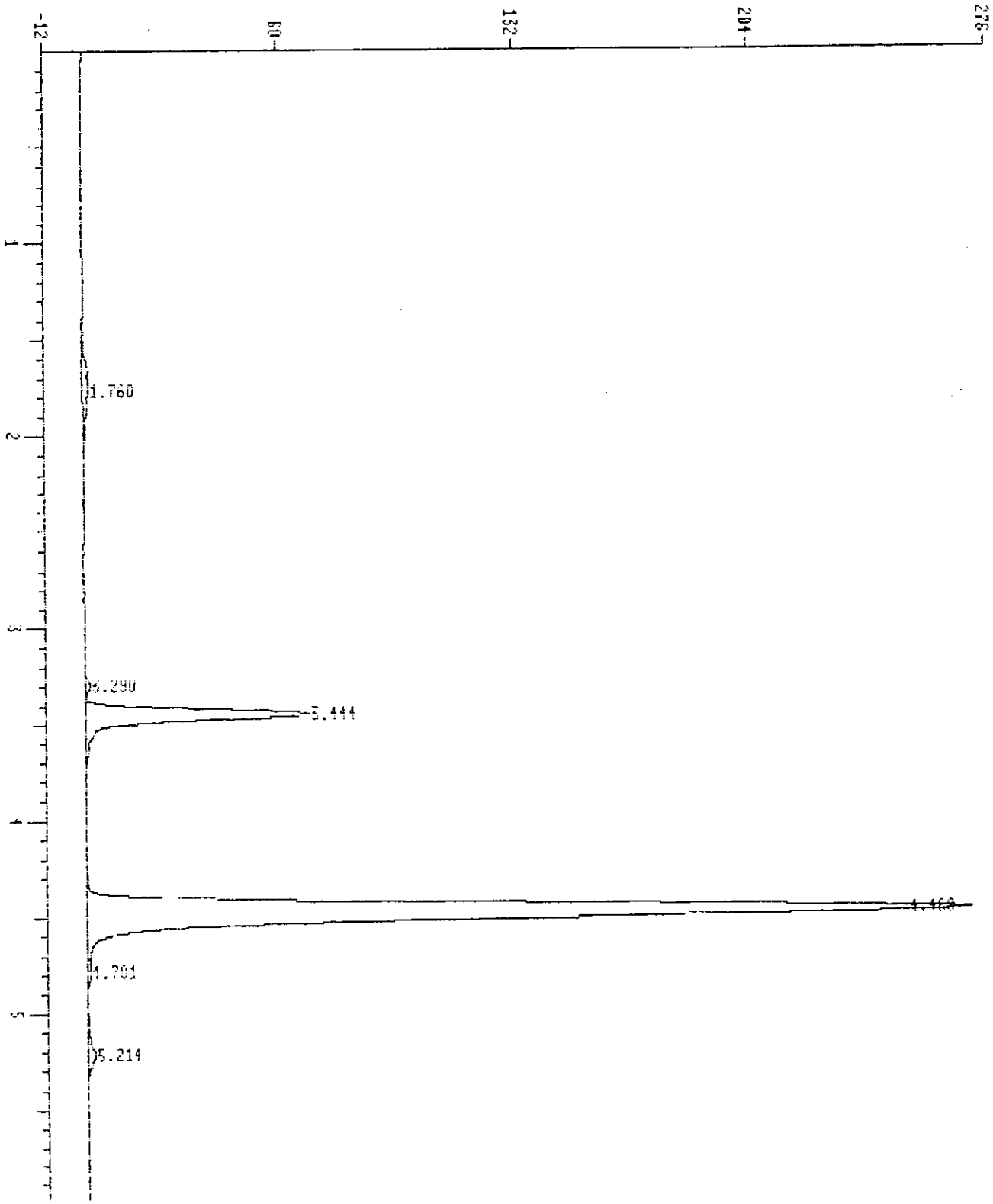
Report by Signal

Operator: JCP 2 Apr 92 3:40 am
Method File Name : DNPHIII.M
Sample Info : #37
Misc Info:
Integration File Name : DATA:0401A46B.I
consisting of channels : 1. A 360,4 550,100 of 0401A46B.D
Sequence Index: 1 Bottle Number : 46 Repetition Number: 2

A 360,4 550,100 of 0401A46B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.753	BB	16.6782	1.0010	0.83	100.00	0.219	1.44
3.285	BV	6.7502	1.7170	0.34	100.00	0.062	0.94
3.439	VV	226.47	52.6451	11.33	100.00	0.067	0.77
4.462	PV	1709.15	309.79	85.48	100.00	0.085	0.82
4.774	VV	14.7703	1.9157	0.74	100.00	0.115	0.74
5.208	VB	25.7340	2.4244	1.29	100.00	0.147	1.40

1: LC A 390,4 550,100 of 0401A47A.D



190

*** Area Percent ***

Report by Signal

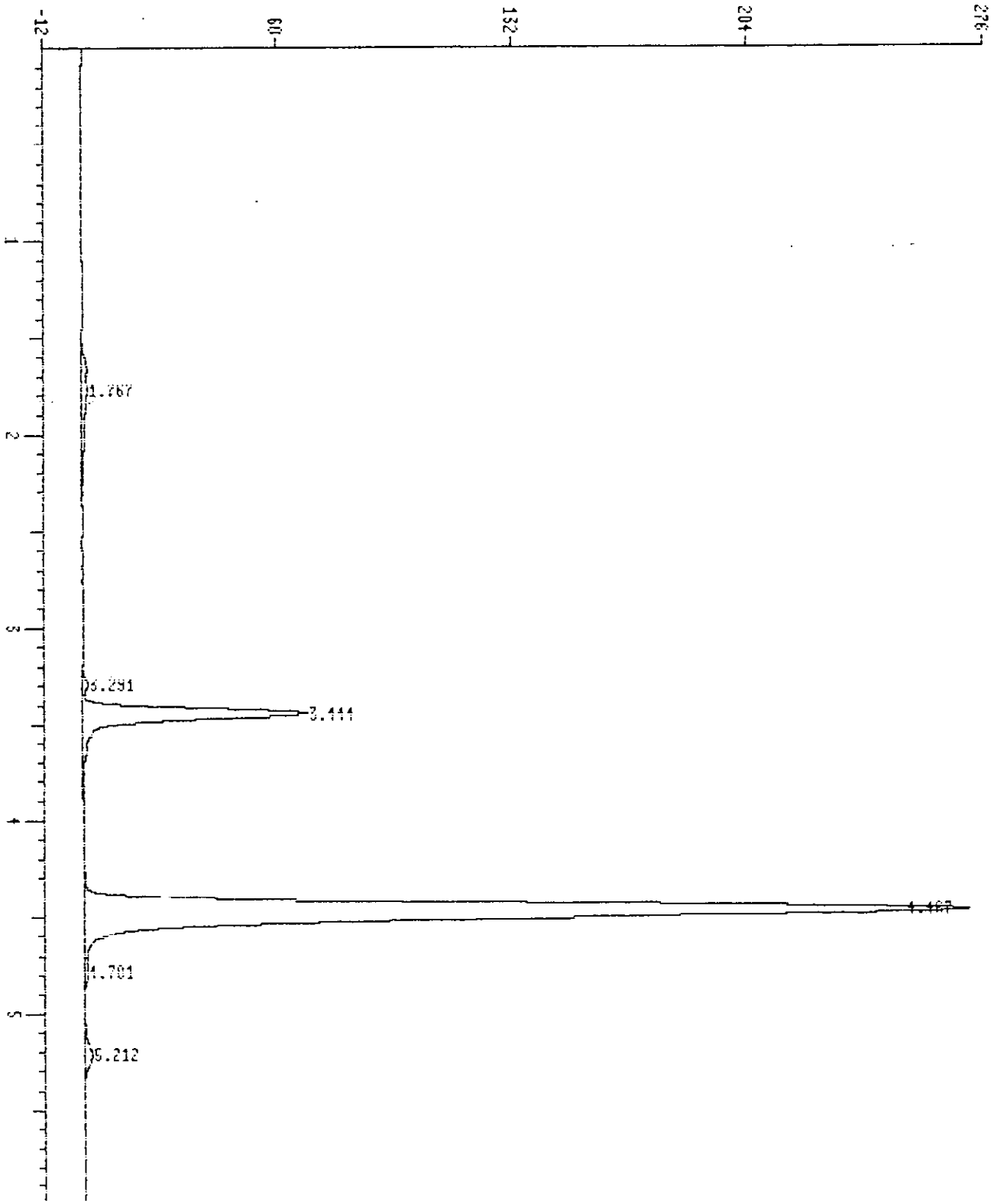
2 Apr 92 3:48 am

Operator: JCP
Method File Name : DNPHIII.M
Sample Info : #38
Misc Info:
Integration File Name : DATA:0401A47A.I
consisting of channels : 1. A 350,4 550,100 of 0401A47A.D
Sequence Index: 1 Bottle Number : 47 Repetition Number: 1

A 350,4 550,100 of 0401A47A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.750	BB	32.6471	1.4849	1.76	100.00	0.278	0.91
3.290	BV	7.6769	1.7811	0.41	100.00	0.066	1.10
3.444	VB	292.55	69.8493	15.75	100.00	0.065	0.79
4.459	VV	1492.09	271.59	80.29	100.00	0.095	0.91
4.781	VV	9.2287	1.2935	0.50	100.00	0.107	0.74
5.214	VB	24.1388	2.4293	1.30	100.00	0.141	1.53

1: LC A 350,4 550,100 of 0401A479.D



142

*** Area Percent ***

Report by Signal

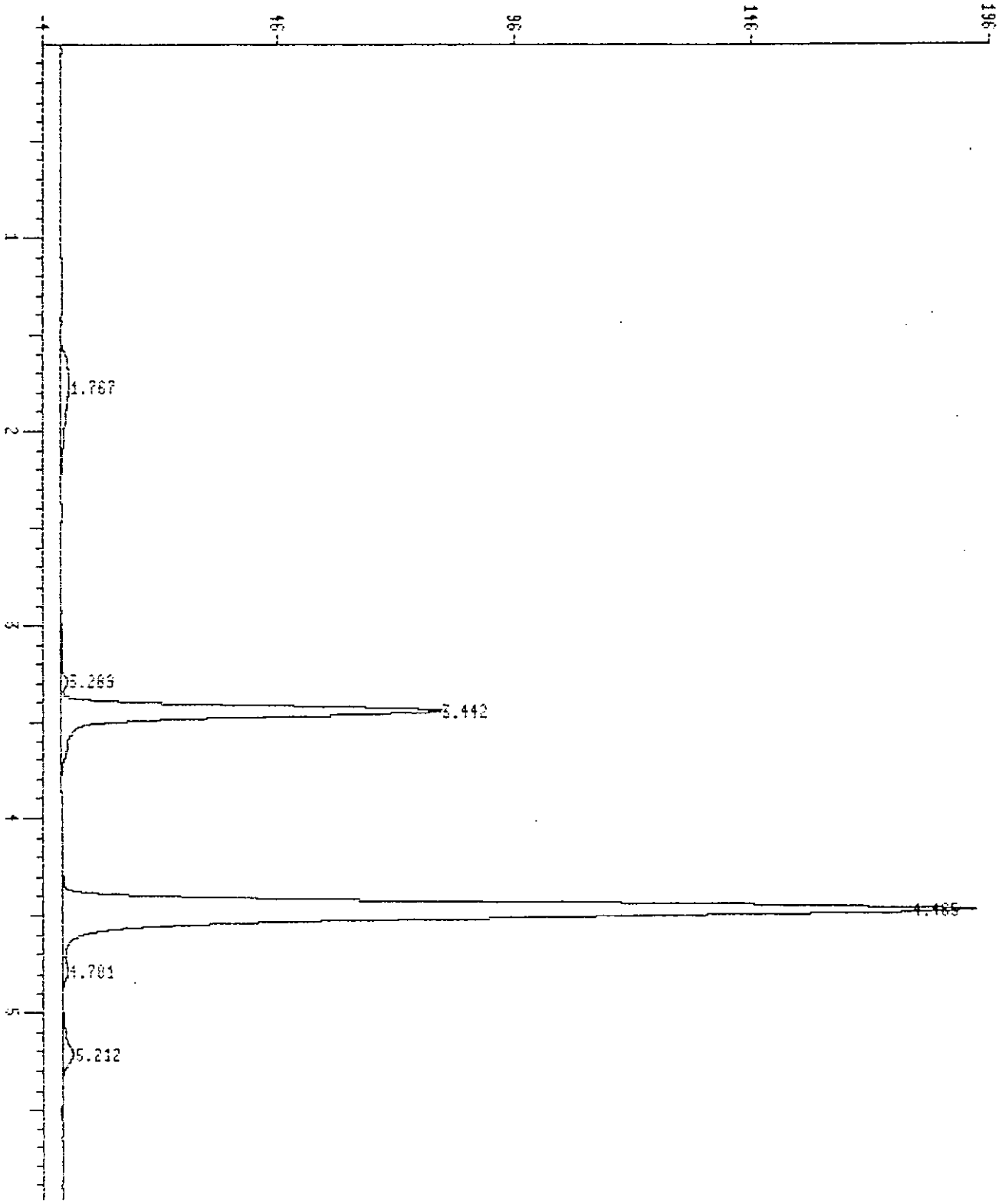
Operator: JCP 2 Apr 92 3:57 am
Method File Name : DNPHIII.M
Sample Info : #38
Misc Info:
Integration File Name : DATA:0401A47B.I
consisting of channels : 1. A 360,4 550,100 of 0401A47B.D
Sequence Index: 1 Bottle Number : 47 Repetition Number: 2

A 360,4 550,100 of 0401A47B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.767	BB	35.1565	1.5696	1.94	100.00	0.298	0.74
3.291	BV	7.2880	1.8103	0.39	100.00	0.063	0.93
3.444	VV	292.38	68.9524	15.72	100.00	0.066	0.79
4.467	PV	1493.71	271.75	80.32	100.00	0.085	0.81
4.781	VB	8.4637	1.1706	0.46	100.00	0.109	1.05
5.212	BB	21.6149	2.5295	1.16	100.00	0.124	1.05

195

1: LC A 360,4 550,100 of 0401A48A.D



194

*** Area Percent ***

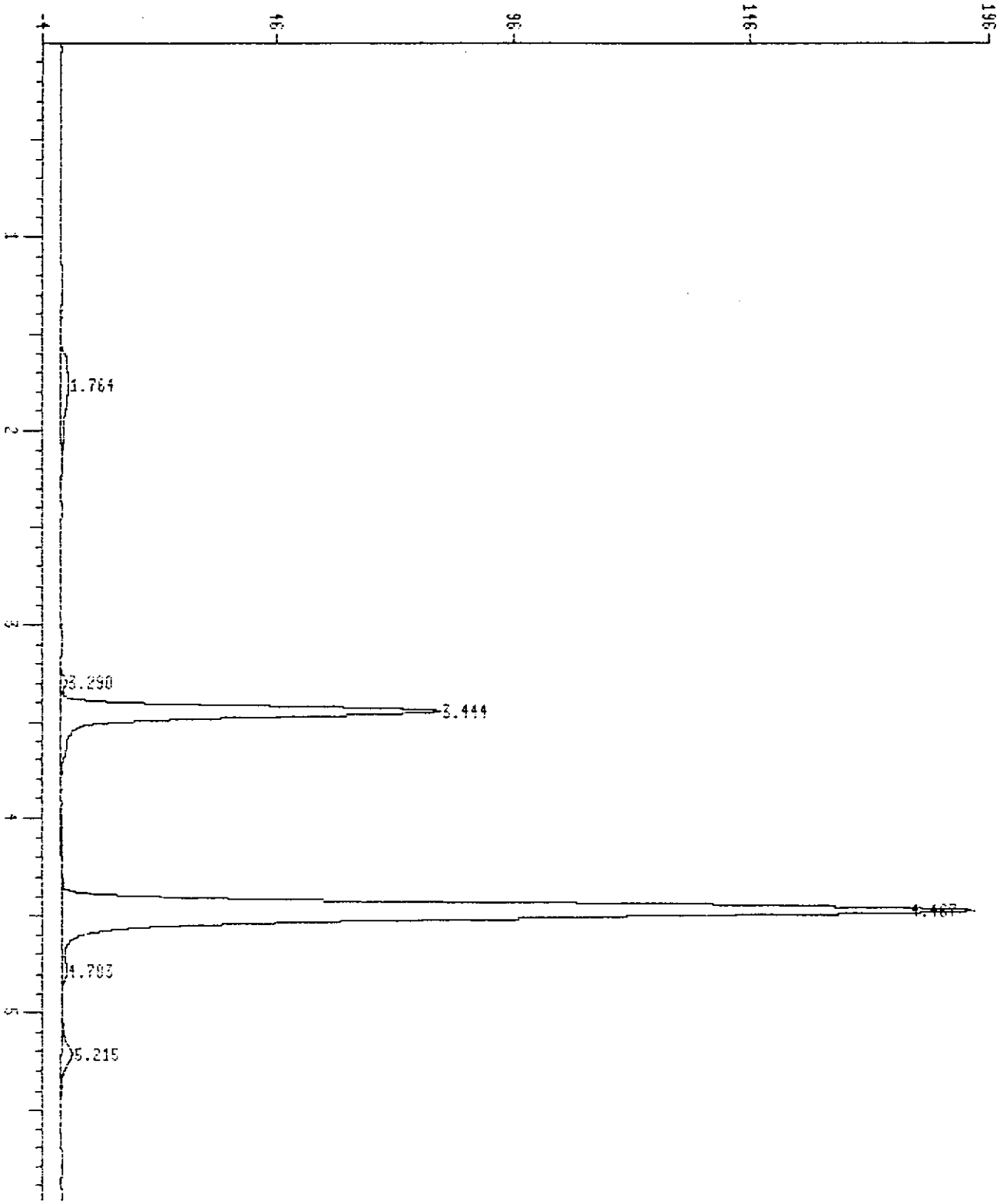
Report by Signal

Operator: JCP 2 Apr 92 4:06 am
Method File Name : DNPHIII.M
Sample Info : #39
Misc Info:
Integration File Name : DATA:0401A48A.I
consisting of channels : 1. A 360,4 550,100 of 0401A48A.D
Sequence Index: 1 Bottle Number : 48 Repetition Number: 1

A 360,4 550,100 of 0401A48A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.757	BB	39.6386	1.6349	2.69	100.00	0.301	0.65
3.289	BV	6.8130	1.3392	0.46	100.00	0.075	1.67
3.442	VV	339.40	80.5805	23.01	100.00	0.065	0.80
4.465	BV	1057.38	193.12	71.68	100.00	0.085	0.80
4.781	VV	8.7719	1.2565	0.59	100.00	0.106	0.97
5.212	VB	23.0871	2.3229	1.57	100.00	0.140	1.45

1: LC A 360,4 550,100 of 0401A48B.D



*** Area Percent ***

Report by Signal

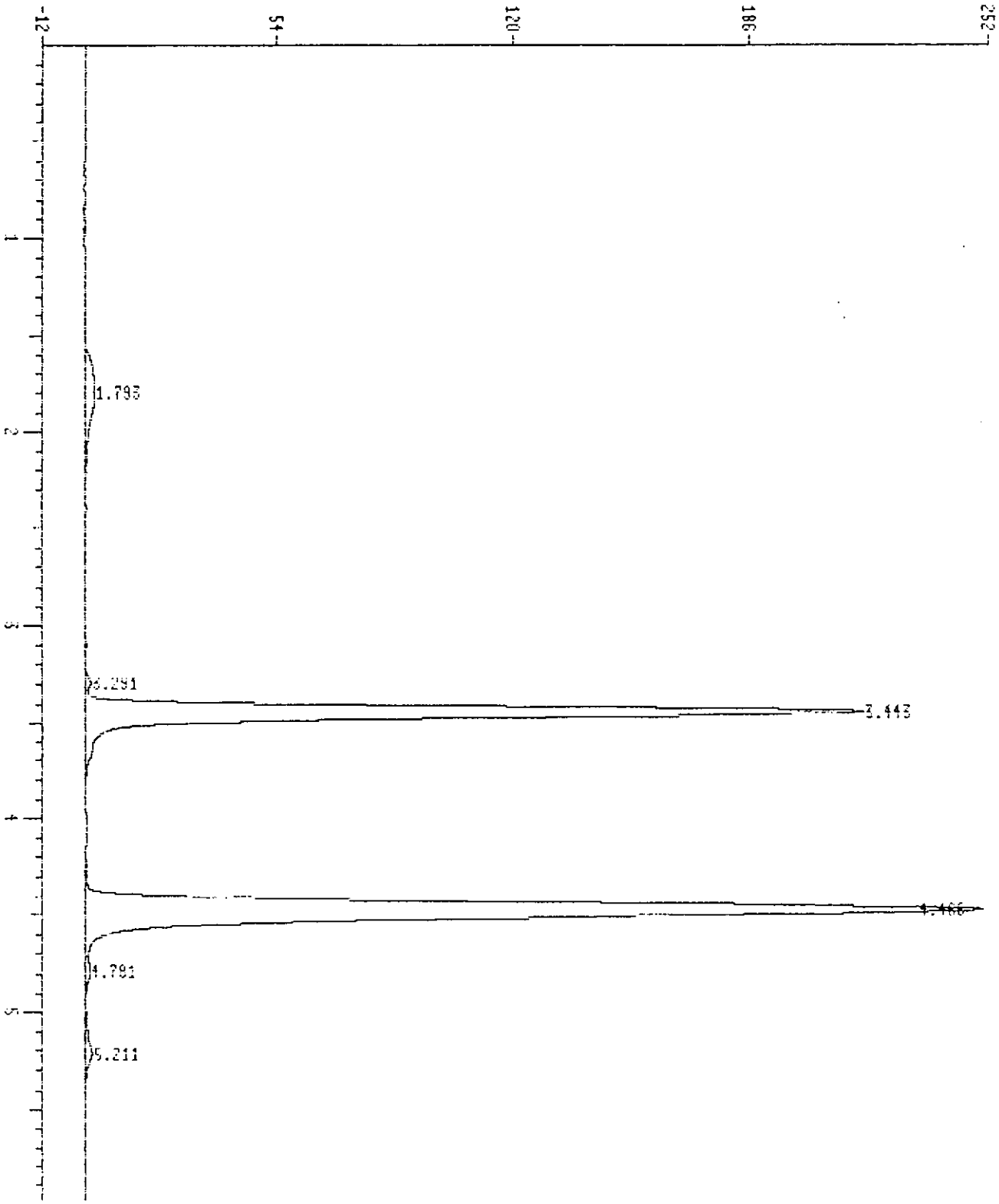
Operator: JCP 2 Apr 92 4:15 am
Method File Name : DNPHIII.M
Sample Info : #39
Misc Info:
Integration File Name : DATA:0401A48B.I
consisting of channels : 1. A 360,4 550,100 of 0401A48B.D
Sequence Index: 1 Bottle Number : 48 Repetition Number: 2

A 360,4 550,100 of 0401A48B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.764	BB	31.2778	1.5387	2.14	100.00	0.259	0.79
3.290	BV	5.0059	1.3074	0.34	100.00	0.061	0.91
3.444	VB	338.84	80.4747	23.14	100.00	0.065	0.80
4.457	BV	1059.67	193.17	72.37	100.00	0.085	0.81
4.783	VB	9.5654	1.2510	0.59	100.00	0.106	1.00
5.215	BB	20.8047	2.3232	1.42	100.00	0.128	1.12

194

1: LC A 350,4 550,100 of 0401A49A.D



*** Area Percent ***

Report by Signal

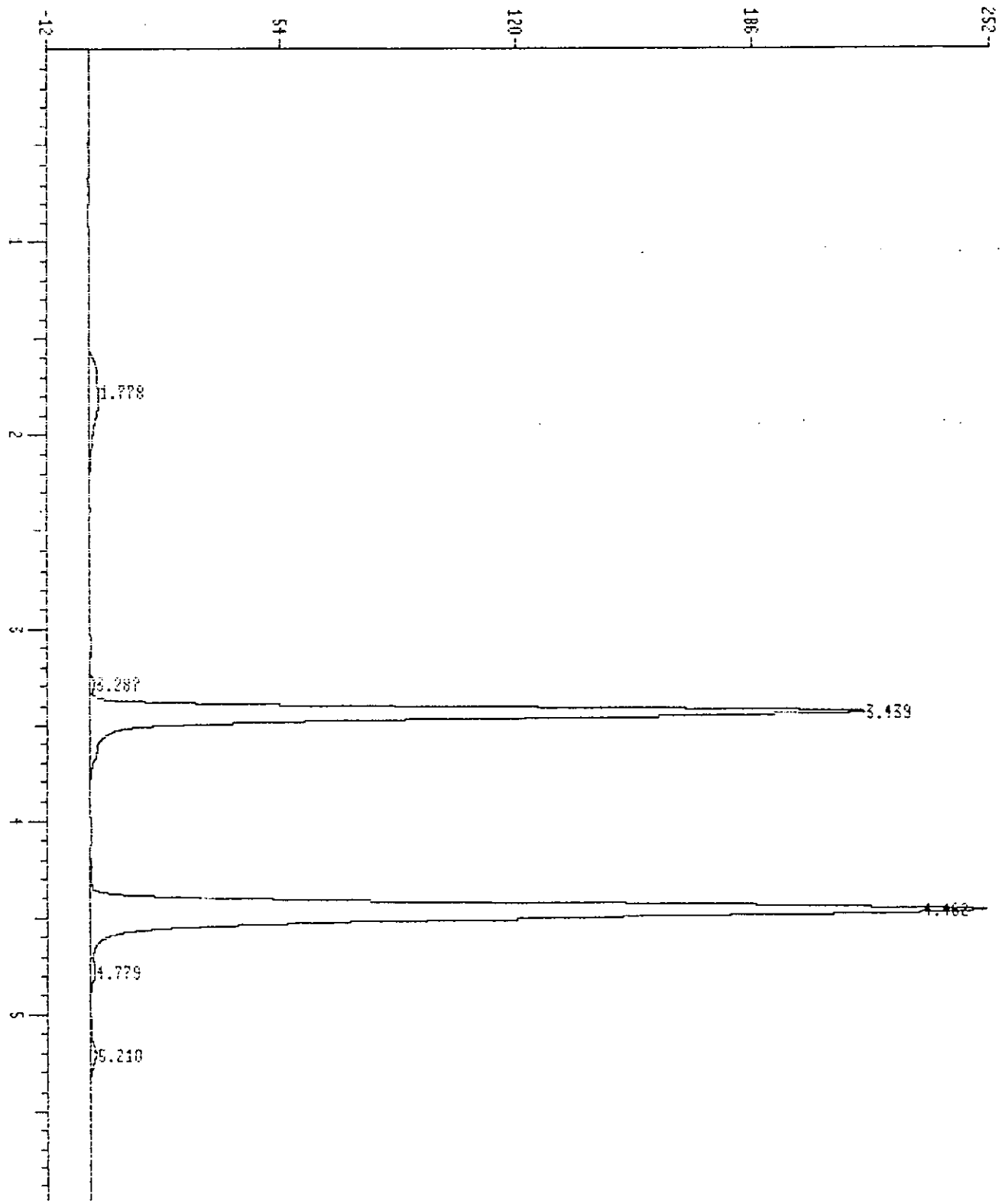
Operator: JCP 2 Apr 92 4:23 am
Method File Name : DNPHIII.M
Sample Info : #40
Misc Info:
Integration File Name : DATA:0401A49A.I
consisting of channels : 1. A 360,4 550,100 of 0401A49A.D
Sequence Index: 1 Bottle Number : 49 Repetition Number: 1

A 360,4 550,100 of 0401A49A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.793	BV	61.3052	2.6603	2.59	100.00	0.307	0.95
3.291	BV	8.1311	1.5446	0.34	100.00	0.077	2.03
3.443	VB	905.95	217.69	38.16	100.00	0.065	0.83
4.466	BV	1372.94	250.93	57.77	100.00	0.085	0.81
4.791	VB	9.5012	1.3592	0.40	100.00	0.105	0.96
5.211	BB	17.8127	1.9035	0.75	100.00	0.134	1.40

188

1: LC A 360,4 550,100 of 0401A498.D



280

*** Area Percent ***

Report by Signal

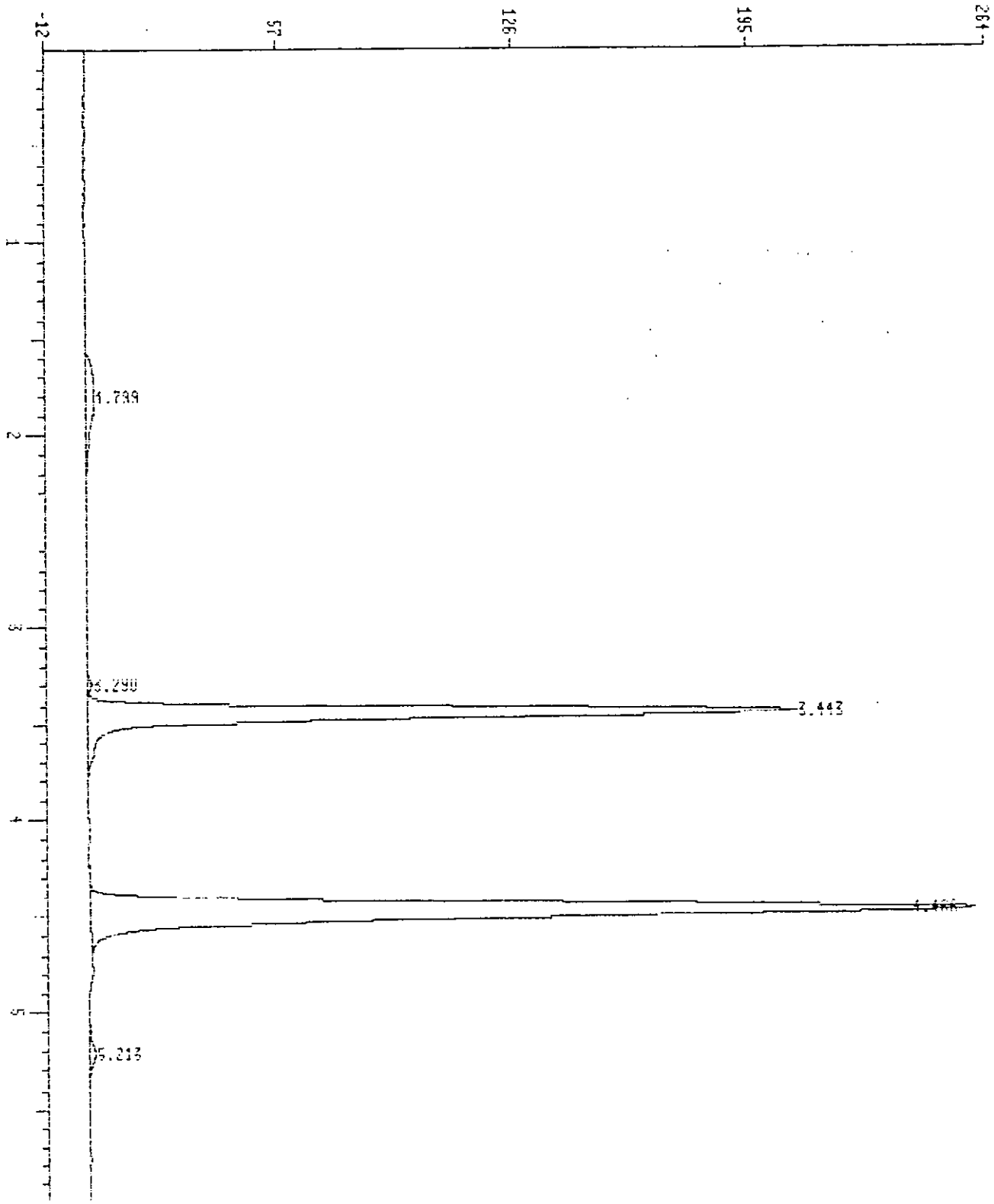
Operator: JCP 2 Apr 92 4:32 am
Method File Name : DNPHIII.M
Sample Info : #40
Misc Info:
Integration File Name : DATA:0401A49B.I
consisting of channels : 1. A 360,4 550,100 of 0401A49B.D
Sequence Index: 1 Bottle Number : 49 Repetition Number: 2

A 360,4 550,100 of 0401A49B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.778	BV	63.5475	2.6043	2.67	100.00	0.334	0.68
3.287	VV	5.9039	1.4953	0.25	100.00	0.061	0.92
3.439	VB	907.54	217.50	38.17	100.00	0.065	0.83
4.462	BV	1373.43	251.08	57.76	100.00	0.085	0.81
4.779	VV	10.6486	1.4452	0.45	100.00	0.111	0.90
5.210	VB	16.7224	1.7123	0.70	100.00	0.138	1.34

20

1: LC A 360,4 550,100 of 0401A50A.D



22

*** Area Percent ***

Report by Signal

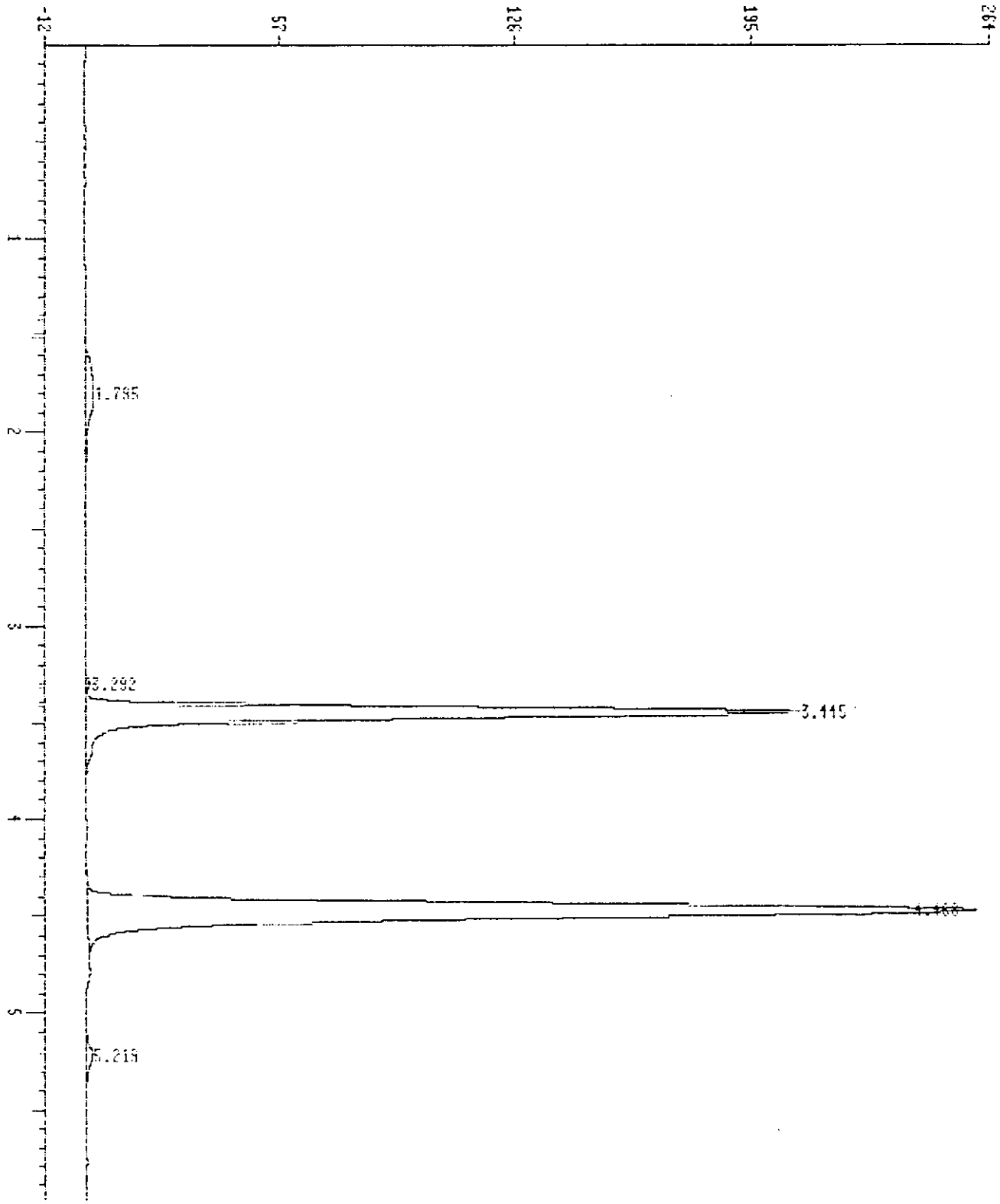
Operator: JCP 2 Apr 92 4:41 am
Method File Name : DNPHIII.M
Sample Info : #41
Misc Info:
Integration File Name : DATA:0401A50A.I
consisting of channels : 1. A 360,4 550,100 of 0401A50A.D
Sequence Index: 1 Bottle Number : 50 Repetition Number: 1

A 360,4 550,100 of 0401A50A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.799	BV	57.7960	2.4159	2.45	100.00	0.325	0.95
3.290	PV	4.9921	1.2936	0.21	100.00	0.061	1.02
3.443	VB	869.53	208.45	36.88	100.00	0.065	0.82
4.456	BV	1411.15	260.00	59.85	100.00	0.084	0.81
5.213	BB	14.2228	1.8474	0.60	100.00	0.115	0.97

203

1: LC A 350,4 550,100 of 0401A50B.D



204

*** Area Percent ***

Report by Signal

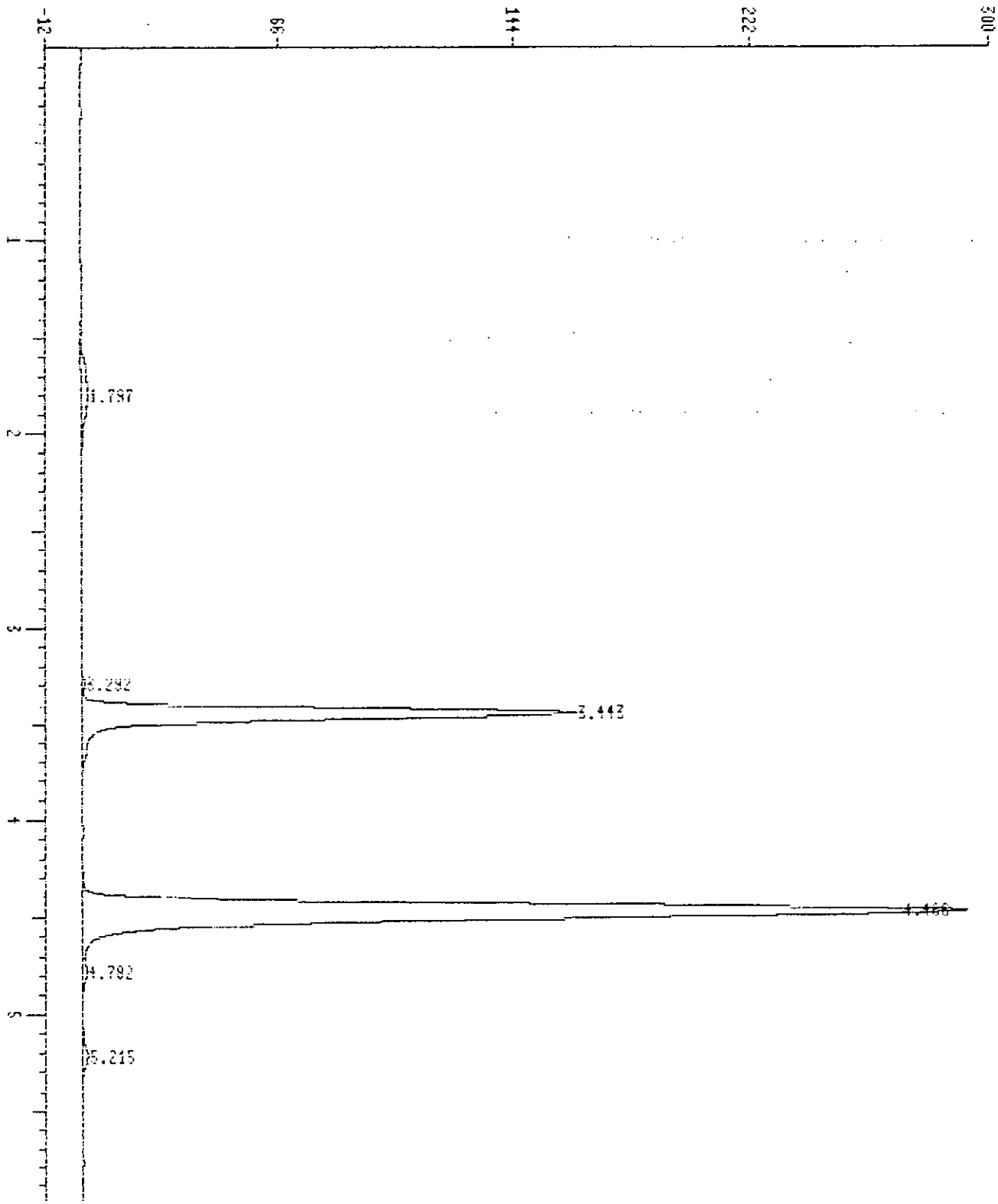
Operator: JCP 2 Apr 92 4:50 am
Method File Name : DNPHIII.M
Sample Info : #41
Misc Info:
Integration File Name : DATA:0401A50B.I
consisting of channels : 1. A 360,4 550,100 of 0401A50B.D
Sequence Index: 1 Bottle Number : 50 Repetition Number: 2

A 360,4 550,100 of 0401A50B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.794	BB	50.7480	2.4192	2.16	100.00	0.299	0.99
3.292	BV	5.0080	1.2919	0.21	100.00	0.061	0.98
3.445	VB	869.39	208.43	36.92	100.00	0.065	0.93
4.468	BV	1412.70	260.14	60.00	100.00	0.094	0.91
5.219	BB	16.6932	2.0397	0.71	100.00	0.122	0.90

2 of

1: LC A 360,4 550,100 of 0401A51A.D



206

*** Area Percent ***

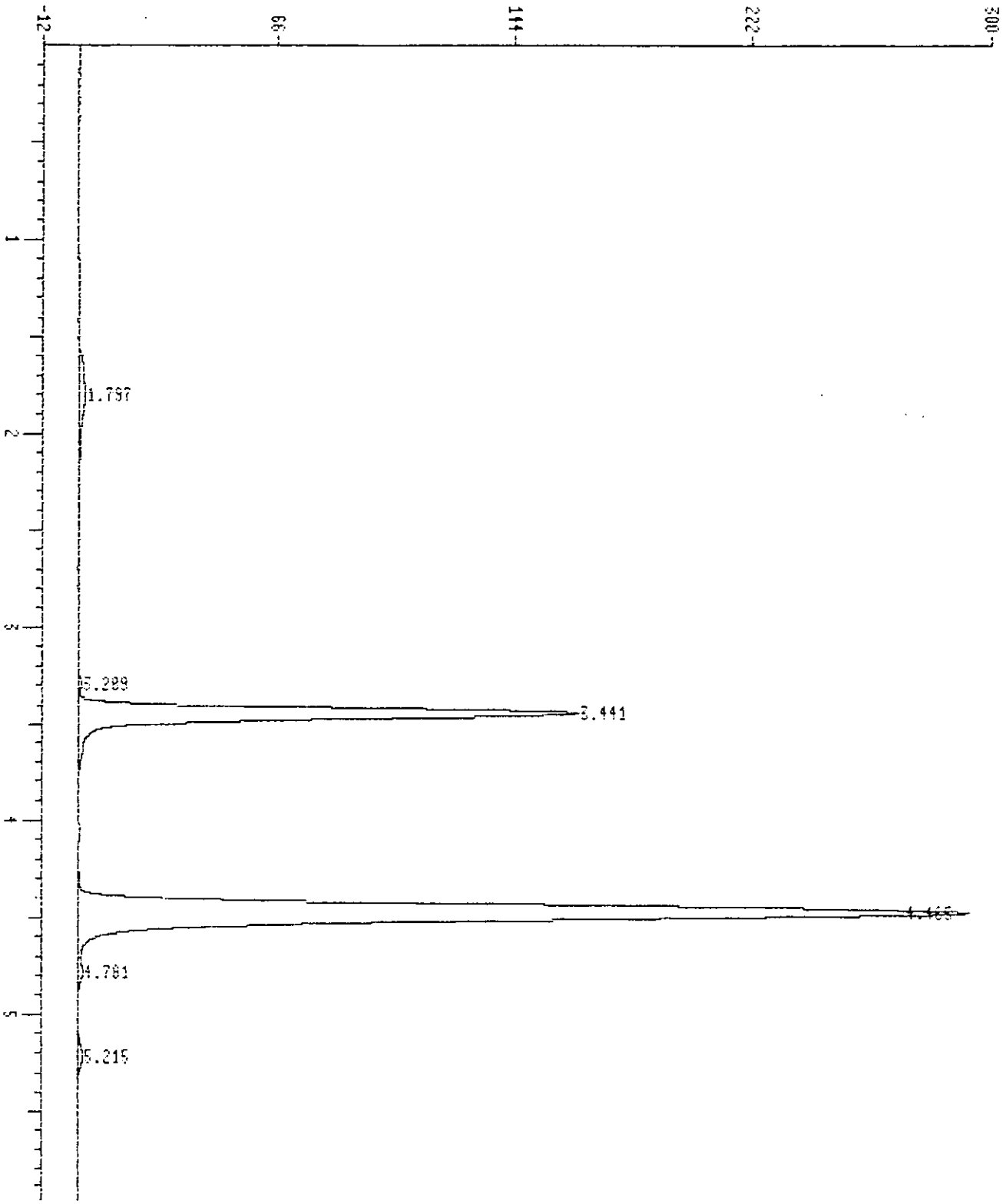
Report by Signal

Operator: JCP 2 Apr 92 4:58 am
Method File Name : DNPHIII.M
Sample Info : #42
Misc Info:
Integration File Name : DATA:0401A51A.I
consisting of channels : 1. A 360,4 550,100 of 0401A51A.D
Sequence Index: 1 Bottle Number : 51 Repetition Number: 1

A 360,4 550,100 of 0401A51A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.797	BV	47.4981	2.1543	2.00	100.00	0.289	0.96
3.292	BV	5.0786	1.3294	0.21	100.00	0.060	0.96
3.443	VV	687.05	165.02	29.00	100.00	0.065	0.82
4.466	BV	1602.05	293.08	67.61	100.00	0.085	0.80
4.782	VV	10.9336	1.5193	0.46	100.00	0.107	0.90
5.215	VB	16.8922	1.9320	0.71	100.00	0.126	1.05

1: LC A 360,4 550,100 of 0401A51B.D



208

*** Area Percent ***

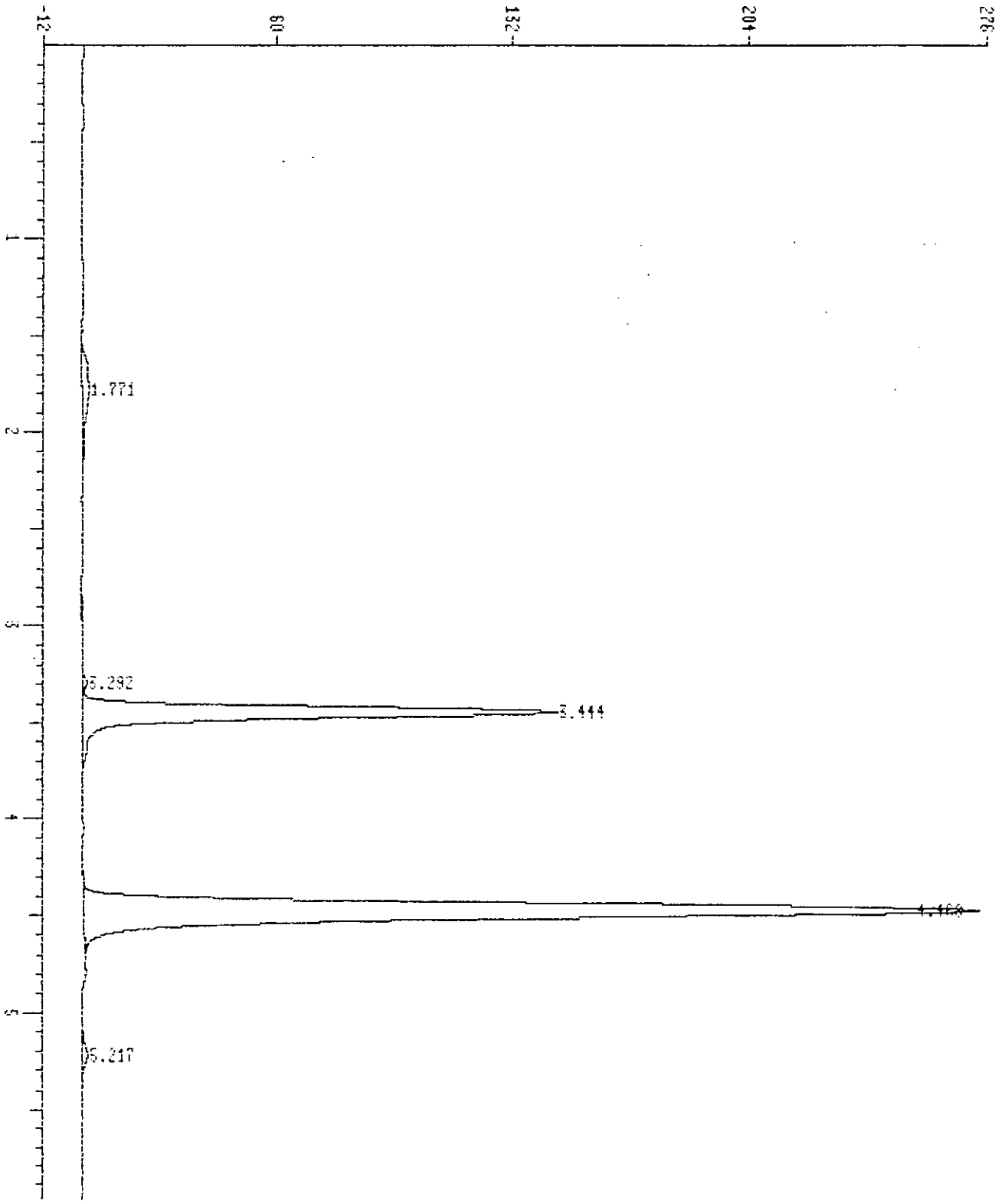
Report by Signal

Operator: JCP 2 Apr 92 5:07 am
Method File Name : DNPHIII.M
Sample Info : #42
Misc Info:
Integration File Name : DATA:0401A51B.I
consisting of channels : 1. A 360,4 550,100 of 0401A51B.D
Sequence Index: 1 Bottle Number : 51 Repetition Number: 2

A 360,4 550,100 of 0401A51B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.797	BV	50.9811	2.1199	2.14	100.00	0.322	0.82
3.289	PV	5.6327	1.4037	0.24	100.00	0.062	0.95
3.441	VV	689.82	164.80	29.07	100.00	0.065	0.82
4.485	BV	1601.69	293.08	67.50	100.00	0.085	0.80
4.781	VB	10.5897	1.5413	0.45	100.00	0.104	0.99
5.215	BB	14.3254	1.8248	0.60	100.00	0.113	1.02

1: LC A 360,4 550,100 of 0401A52A.D



210

*** Area Percent ***

Report by Signal

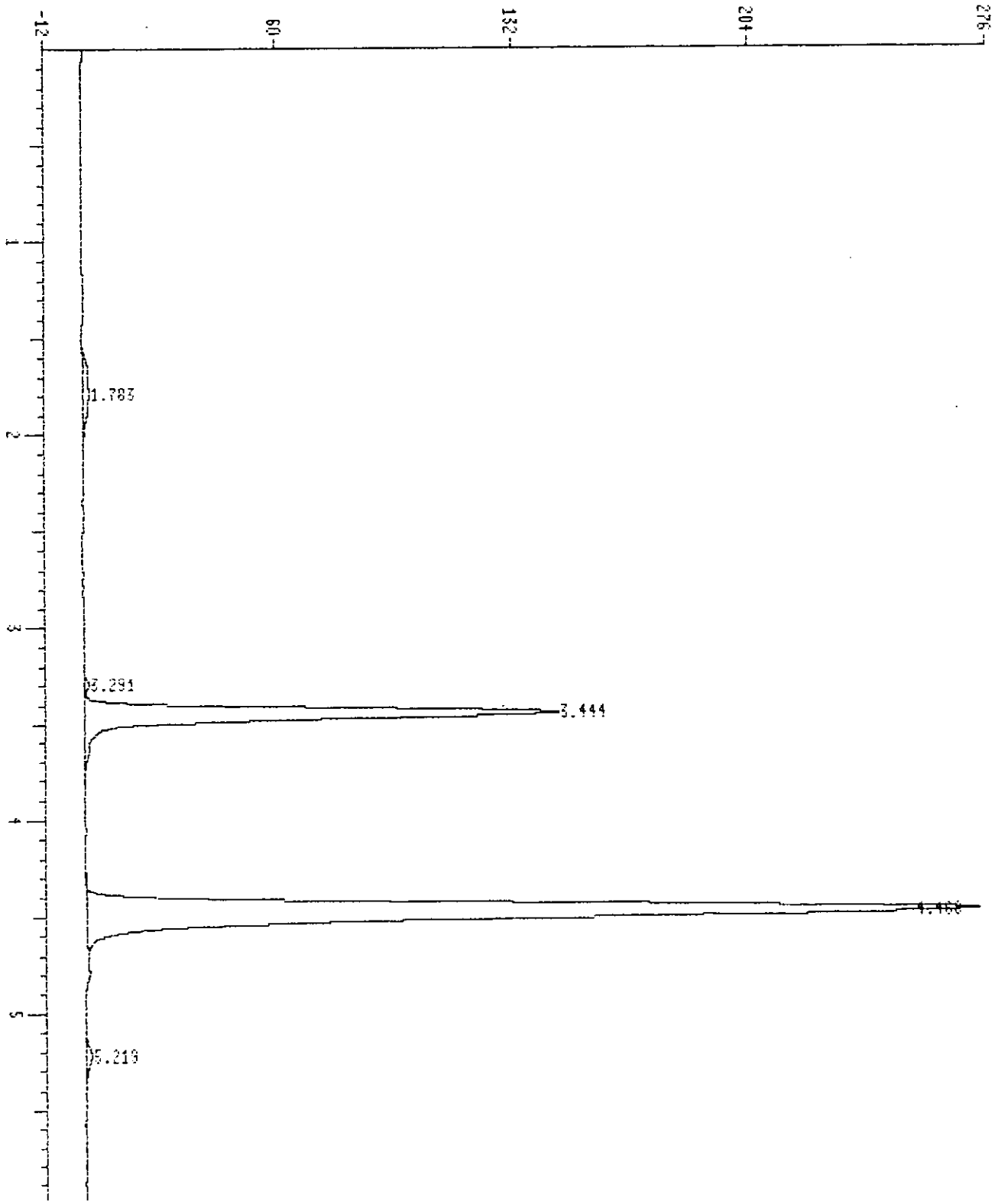
Operator: JCP 2 Apr 92 5:16 am
Method File Name : DNPHIII.M
Sample Info : #43
Misc Info:
Integration File Name : DATA:0401A52A.I
consisting of channels : 1. A 360,4 550,100 of 0401A52A.D
Sequence Index: 1 Bottle Number : 52 Repetition Number: 1

A 360,4 550,100 of 0401A52A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.771	BB	44.2290	1.9964	2.04	100.00	0.289	0.73
3.292	BV	8.0583	1.5507	0.37	100.00	0.076	1.80
3.444	VB	611.96	145.29	28.28	100.00	0.065	0.82
4.468	BV	1485.59	273.94	68.65	100.00	0.084	0.81
5.217	BB	14.2865	1.8541	0.66	100.00	0.113	1.10

211

1: LC A 360,4 550,100 of 0401A52B.D



212

*** Area Percent ***

Report by Signal

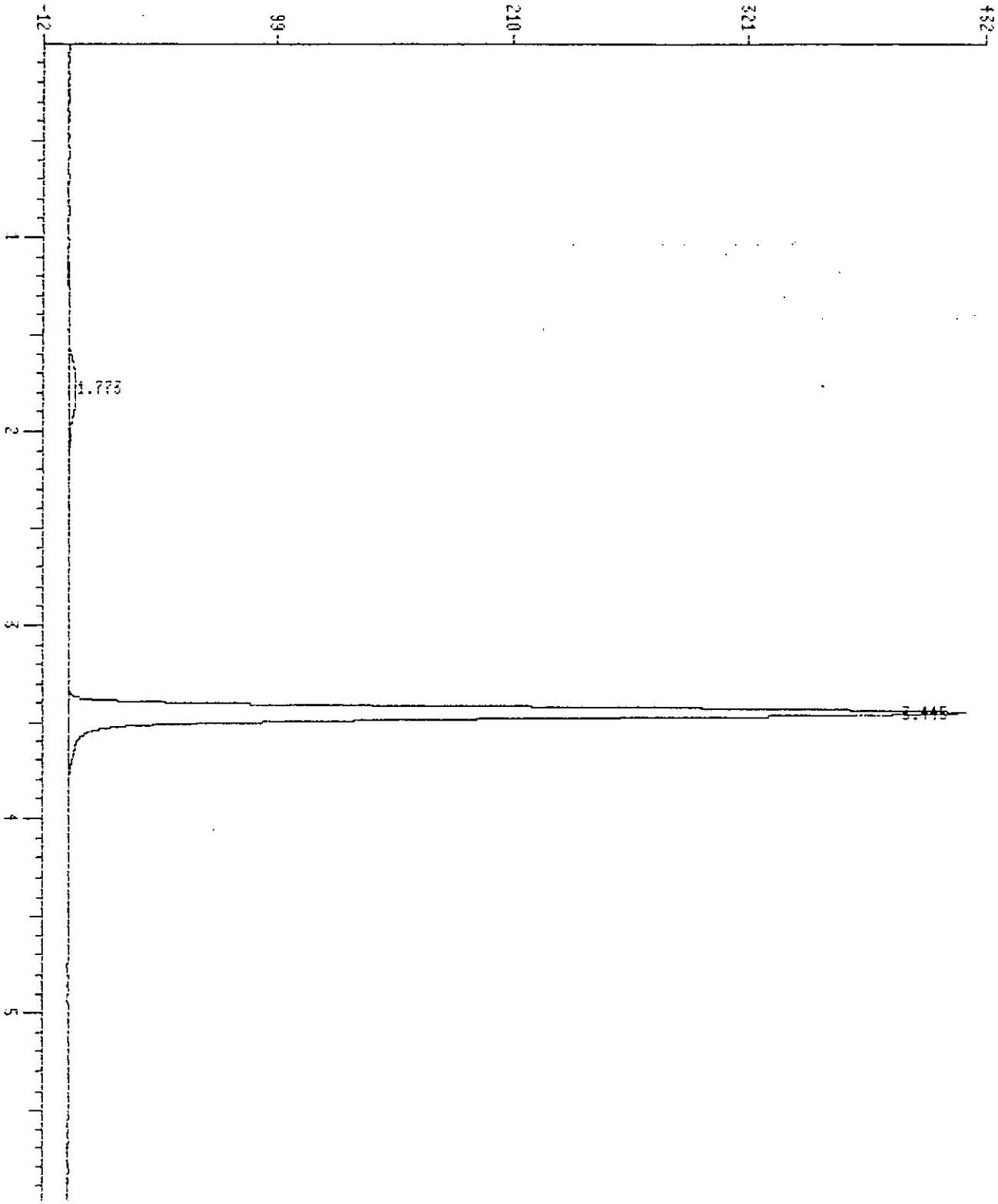
Operator: JCP 2 Apr 92 5:25 am
Method File Name : DNPHIII.M
Sample Info : #43
Misc Info:
Integration File Name : DATA:0401A52B.I
consisting of channels : 1. A 360,4 550,100 of 0401A52B.D
Sequence Index: 1 Bottle Number : 52 Repetition Number: 2

A 360,4 550,100 of 0401A52B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.783	BB	36.9565	1.8893	1.71	100.00	0.282	1.04
3.291	BV	5.2464	1.6241	0.29	100.00	0.060	0.96
3.444	VB	611.78	146.03	28.35	100.00	0.065	0.82
4.468	BV	1486.96	273.75	68.92	100.00	0.084	0.81
5.219	BB	15.6939	1.8944	0.73	100.00	0.122	0.78

213

1: LC A 360,4 550,100 of 0401A53A.D



314

*** Area Percent ***

Report by Signal

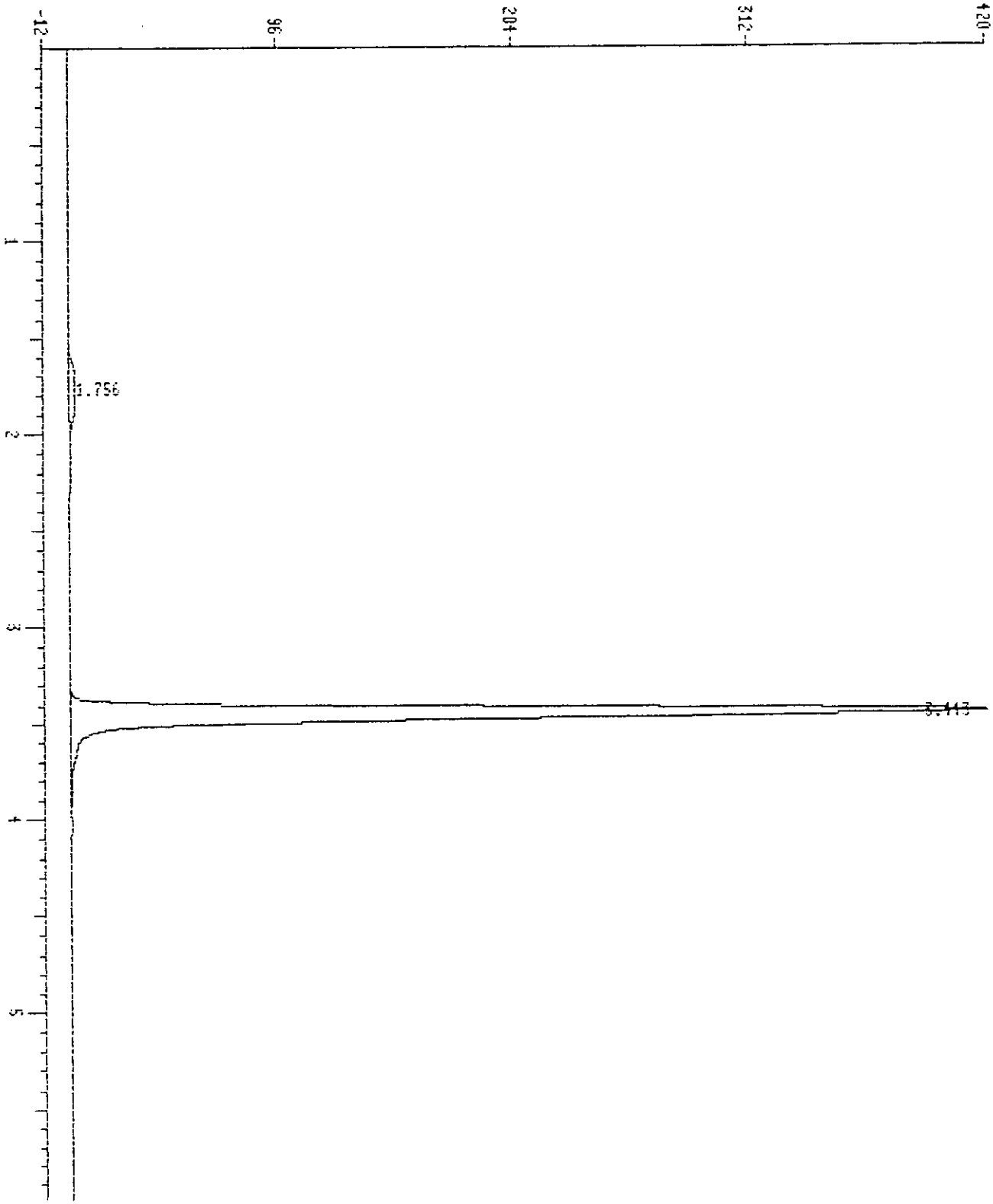
Operator: JCP 2 Apr 92 5:33 am
Method File Name : DNPHIII.M
Sample Info : #44
Misc Info:
Integration File Name : DATA:0401A53A.I
consisting of channels : 1. A 360,4 550,100 of 0401A53A.D
Sequence Index: 1 Bottle Number : 53 Repetition Number: 1

A 360,4 550,100 of 0401A53A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.773	BB	66.4397	3.1512	3.64	100.00	0.308	0.83
3.445	BV	1756.99	422.36	96.36	100.00	0.065	0.83

215

1: LC A 360,4 550,100 of 0401A53B.D



2-2

*** Area Percent ***

Report by Signal

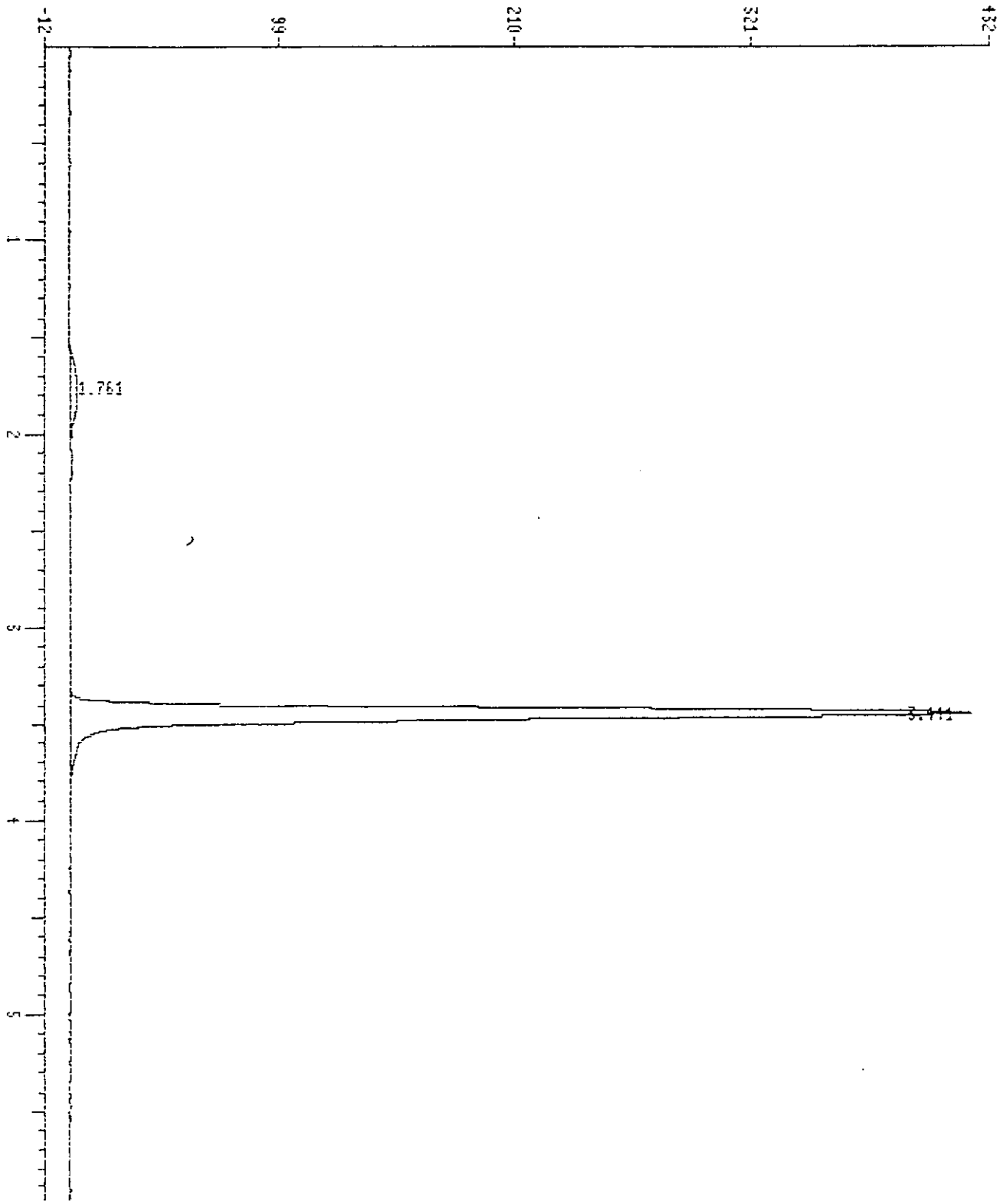
Operator: JCP 2 Apr 92 5:42 am
Method File Name : DNPHIII.M
Sample Info : #44
Misc Info:
Integration File Name : DATA:0401A53B.I
consisting of channels : 1. A 360,4 550,100 of 0401A53B.D
Sequence Index: 1 Bottle Number : 53 Repetition Number: 2

A 360,4 550,100 of 0401A53B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.756	BV	56.0034	3.0073	3.09	100.00	0.303	0.77
3.443	PV	1753.65	419.73	96.91	100.00	0.065	0.82

214

1: LC A 360,4 550,100 of 0401A54A.D



2-08

*** Area Percent ***

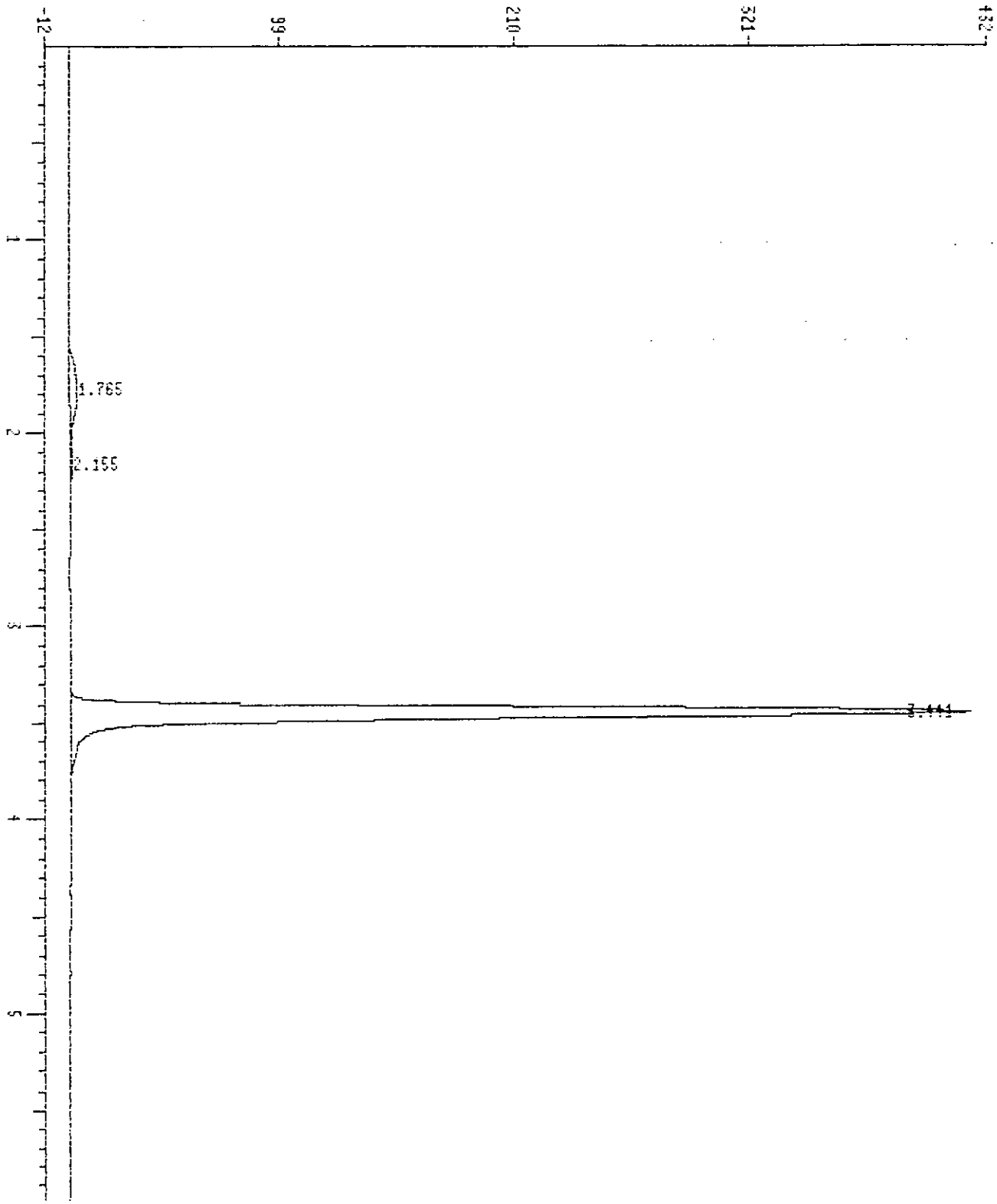
Report by Signal

Operator: JCP 2 Apr 92 5:51 am
Method File Name : DNPHIII.M
Sample Info : #45
Misc Info:
Integration File Name : DATA:0401A54A.I
consisting of channels : 1. A 360,4 550,100 of 0401A54A.D
Sequence Index: 1 Bottle Number : 54 Repetition Number: 1

A 360,4 550,100 of 0401A54A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.761	BV	54.6729	2.9851	2.99	100.00	0.294	0.84
3.441	PV	1771.76	423.20	97.01	100.00	0.065	0.82

1: LC A 360,4 550,100 of 0401A54B.D



220

*** Area Percent ***

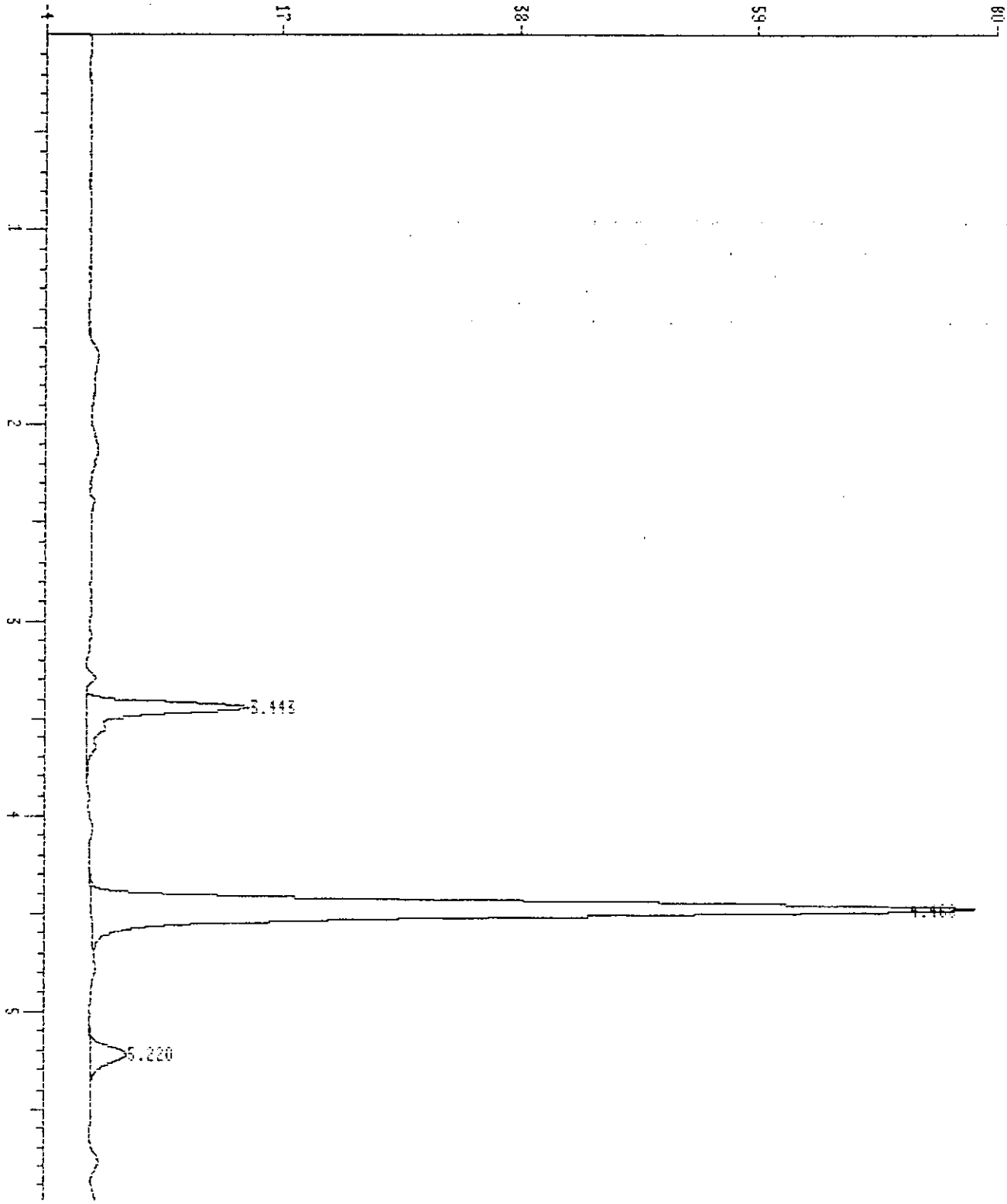
Report by Signal

Operator: JCP 2 Apr 92 5:59 am
Method File Name : DNPHIII.M
Sample Info : #45
Misc Info:
Integration File Name : DATA:0401A54B.I
consisting of channels : 1. A 360,4 550,100 of 0401A54B.D
Sequence Index: 1 Bottle Number : 54 Repetition Number: 2

A 360,4 550,100 of 0401A54B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.765	BV	61.9440	3.1939	3.35	100.00	0.310	0.81
2.155	VV	12.5145	1.0055	0.68	100.00	0.183	1.06
3.441	BV	1772.83	424.39	95.97	100.00	0.065	0.82

1: LC A 360,4 550,100 of 0401A55A.D



2
2
2

*** Area Percent ***

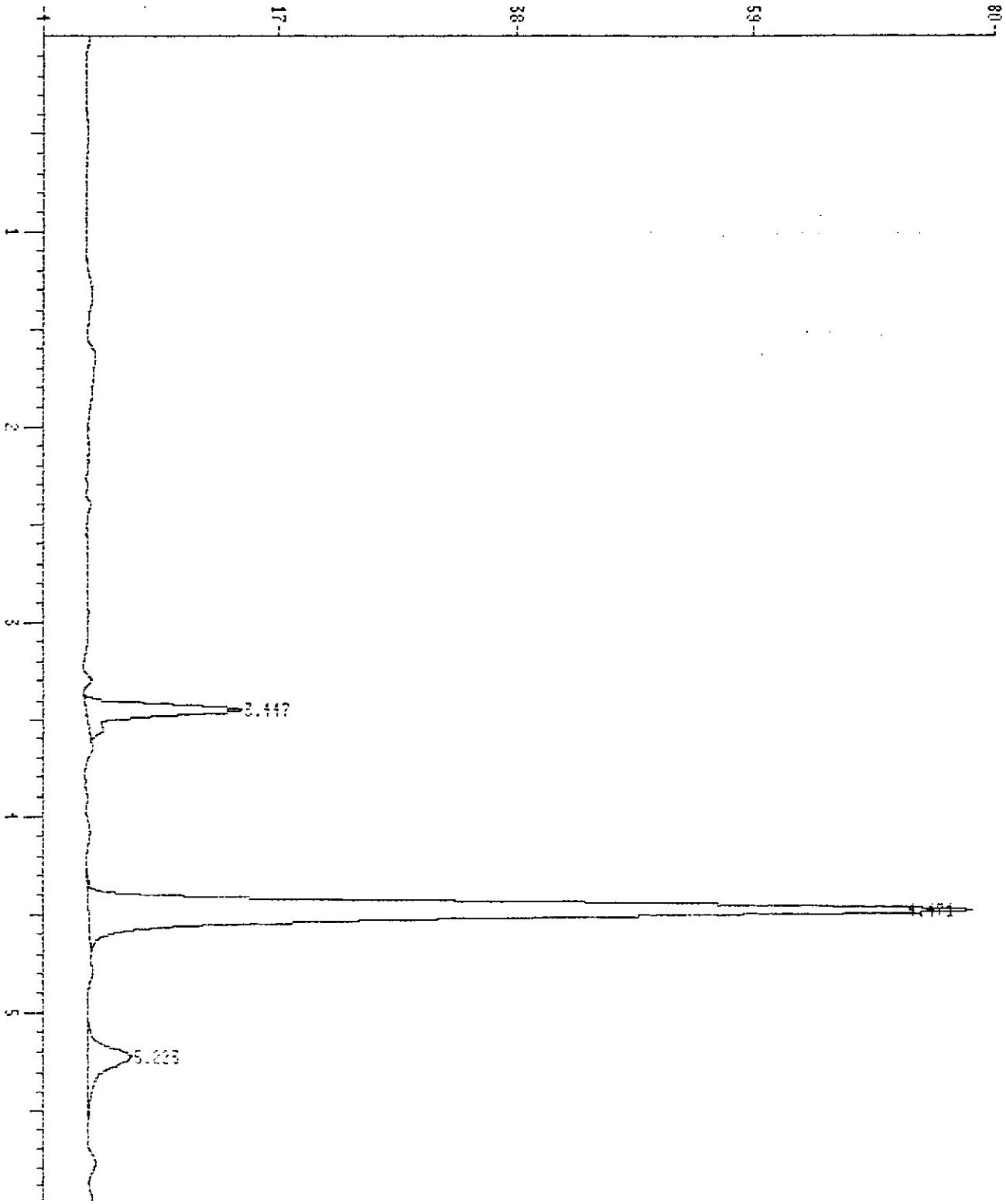
Report by Signal

Operator: JCP 2 Apr 92 6:08 am
Method File Name : DNPHIII.M
Sample Info : #46
Misc Info:
Integration File Name : DATA:0401A55A.I
consisting of channels : 1. A 360,4 550,100 of 0401A55A.D
Sequence Index: 1 Bottle Number : 55 Repetition Number: 1

A 360,4 550,100 of 0401A55A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.443	PB	68.3634	14.3998	13.31	100.00	0.072	0.60
4.468	BV	425.49	78.2557	82.82	100.00	0.085	0.81
5.220	BB	19.9272	3.2492	3.88	100.00	0.095	0.81

1: LC A 360,4 550,100 of 0401A55B.D



*** Area Percent ***

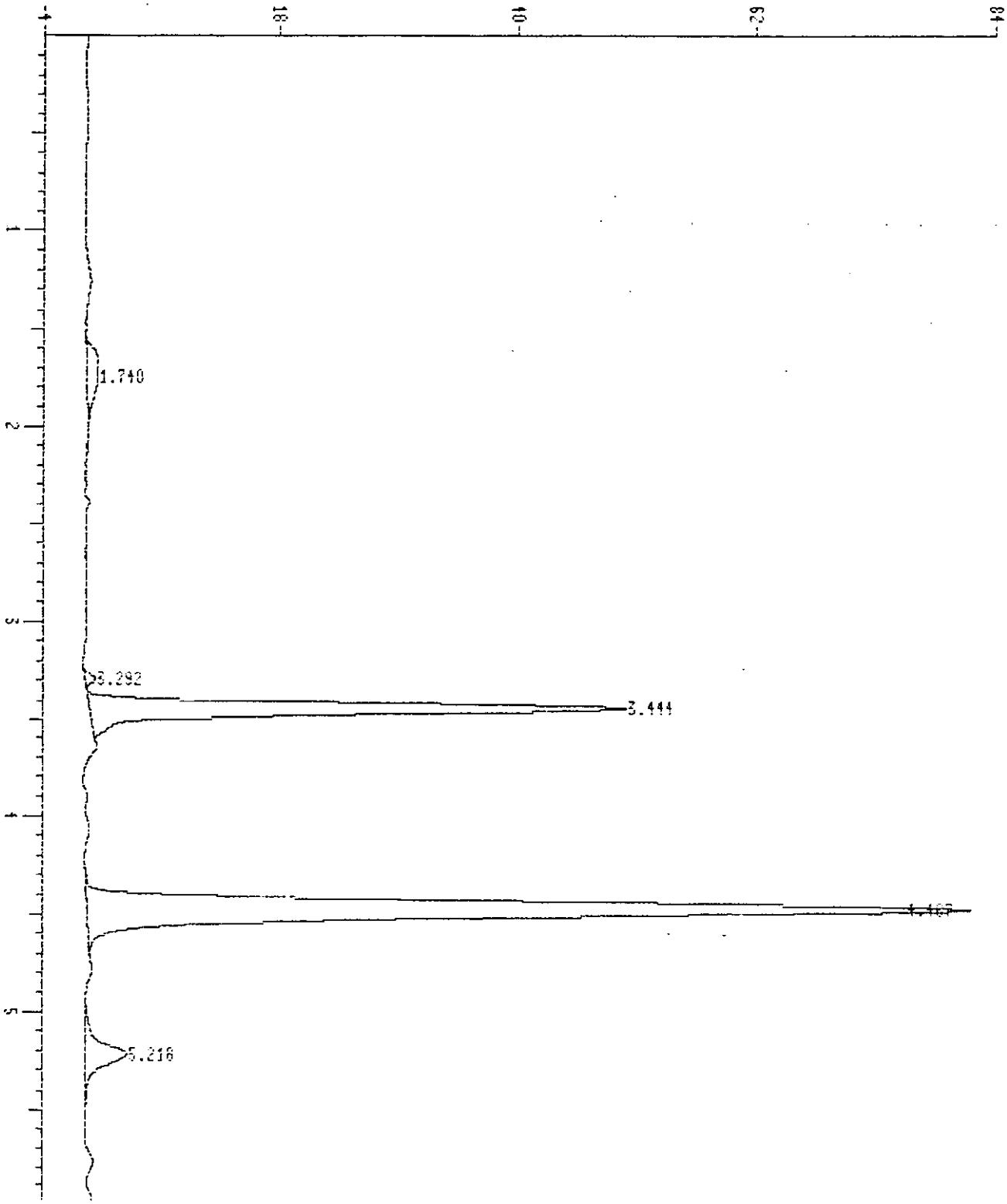
Report by Signal

Operator: JCP 2 Apr 92 6:17 am
Method File Name : DNPHIII.M
Sample Info : #46
Misc Info:
Integration File Name : DATA:0401A55B.I
consisting of channels : 1. A 360,4 550,100 of 0401A55B.D
Sequence Index: 1 Bottle Number : 55 Repetition Number: 2

A 360,4 550,100 of 0401A55B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.447	PV	59.1919	14.0018	11.46	100.00	0.066	0.76
4.471	BV	425.06	78.0264	82.28	100.00	0.085	0.81
5.223	BB	32.3799	3.9614	6.27	100.00	0.122	0.71

1: LC A 360,4 550,100 of 0401A56A.D



229

*** Area Percent ***

Report by Signal

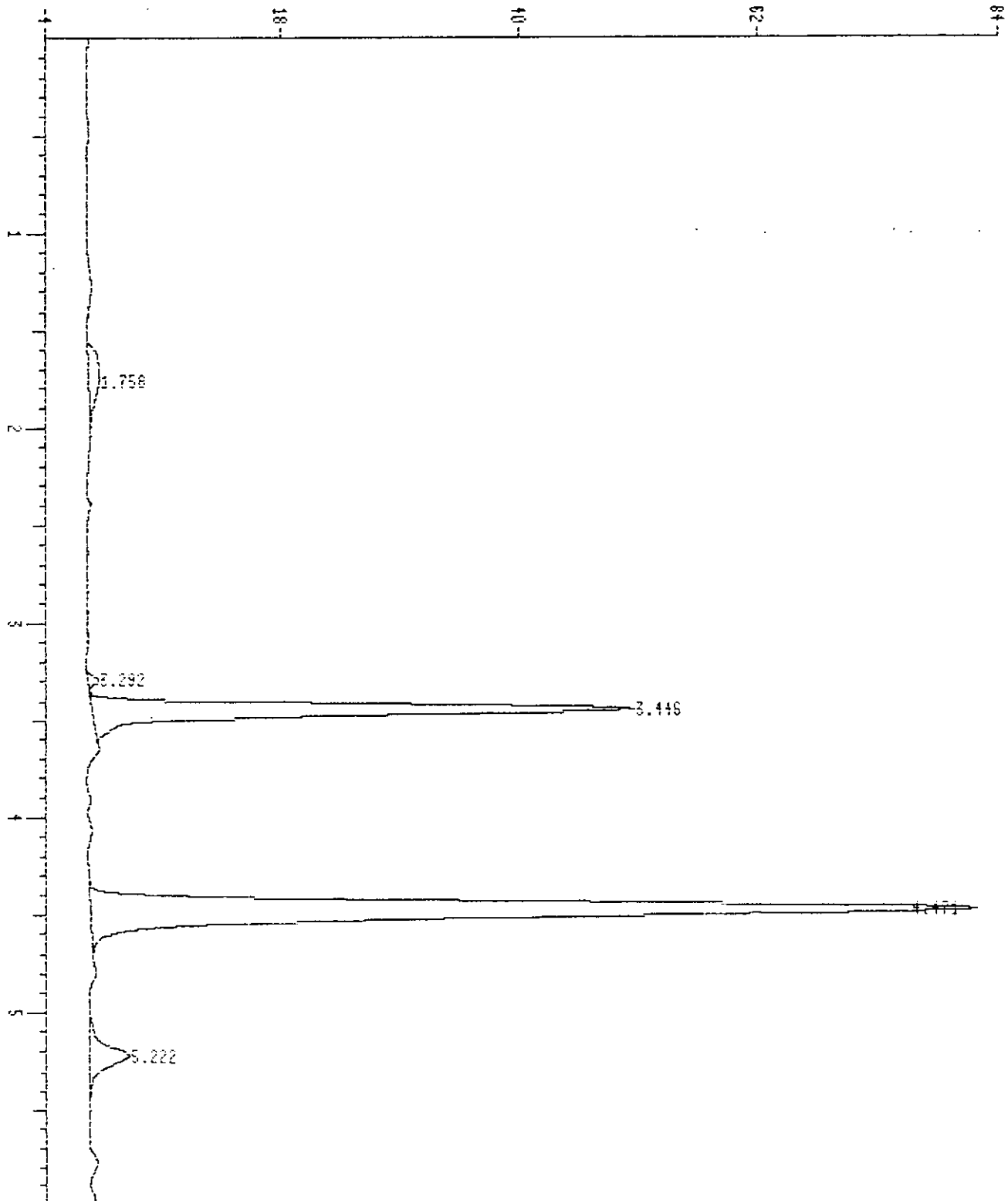
Operator: JCP 2 Apr 92 6:25 am
Method File Name : ONPHIII.M
Sample Info : #47
Misc Info:
Integration File Name : DATA:0401A56A.I
consisting of channels : 1. A 360,4 550,100 of 0401A56A.D
Sequence Index: 1 Bottle Number : 56 Repetition Number: 1

A 360,4 550,100 of 0401A56A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.740	BB	17.4990	1.0385	2.50	100.00	0.226	1.12
3.292	BV	3.1541	0.9562	0.45	100.00	0.055	1.13
3.444	VV	202.20	49.7949	28.92	100.00	0.064	0.86
4.467	BV	446.61	81.8736	63.89	100.00	0.085	0.82
5.218	BB	29.6065	3.8101	4.24	100.00	0.116	1.02

227

1: LC A 360,4 550,100 of 0401A56B.D



228

*** Area Percent ***

Report by Signal

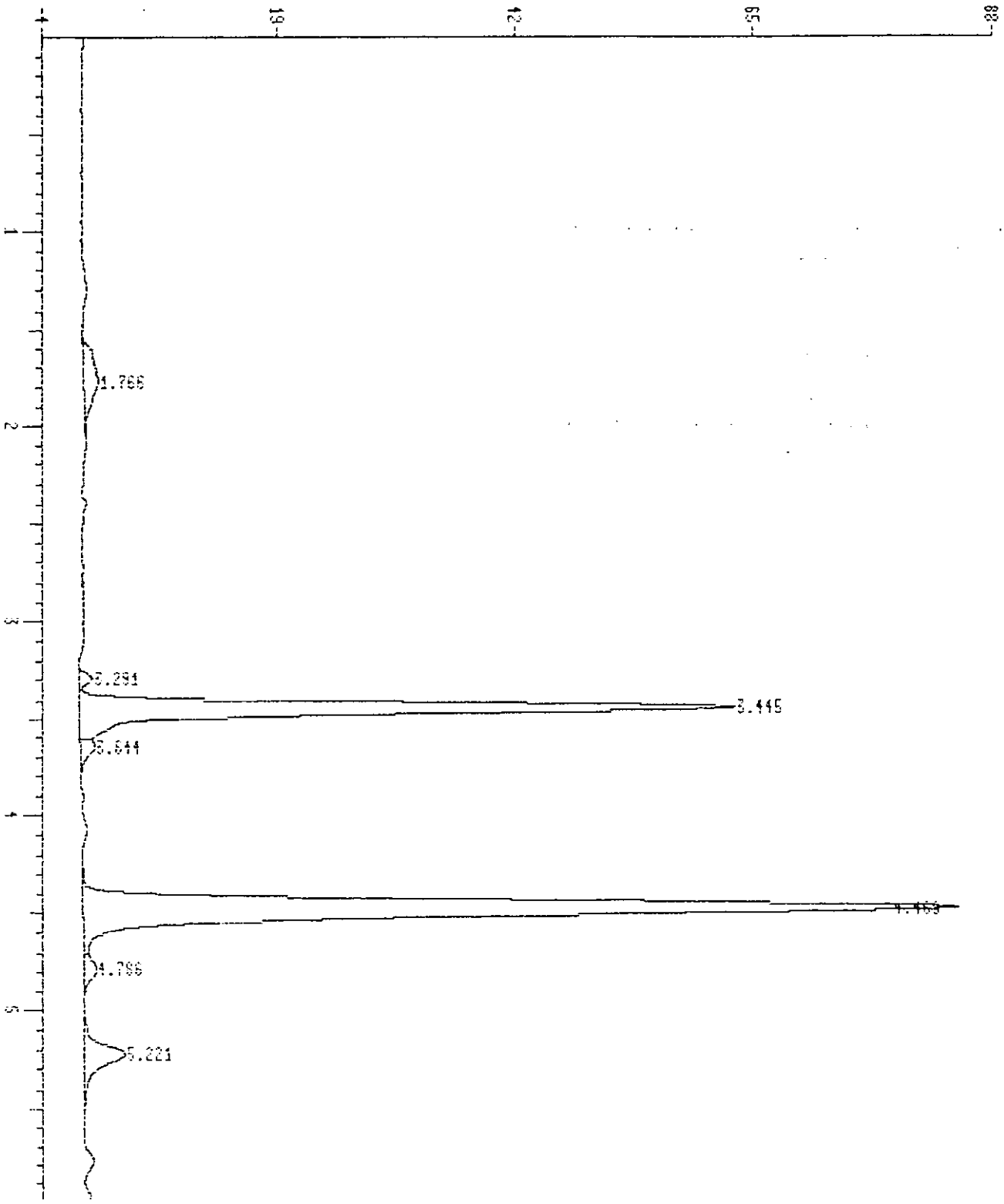
Operator: JCP 2 Apr 92 6:34 am
Method File Name : DNPHIII.M
Sample Info : #47
Misc Info:
Integration File Name : DATA:0401A56B.I
consisting of channels : 1. A 360,4 550,100 of 0401A56B.D
Sequence Index: 1 Bottle Number : 56 Repetition Number: 2

A 360,4 550,100 of 0401A56B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.758	BB	16.1847	0.9875	2.32	100.00	0.216	1.60
3.292	BV	3.3378	1.0137	0.48	100.00	0.054	1.04
3.446	PV	203.39	50.0499	29.12	100.00	0.064	0.86
4.471	BV	446.79	81.7831	63.96	100.00	0.085	0.82
5.222	BB	28.8743	3.7593	4.13	100.00	0.113	0.94

229

1: LC A 360,4 550,100 of 0401A57A.D



230

*** Area Percent ***

Report by Signal

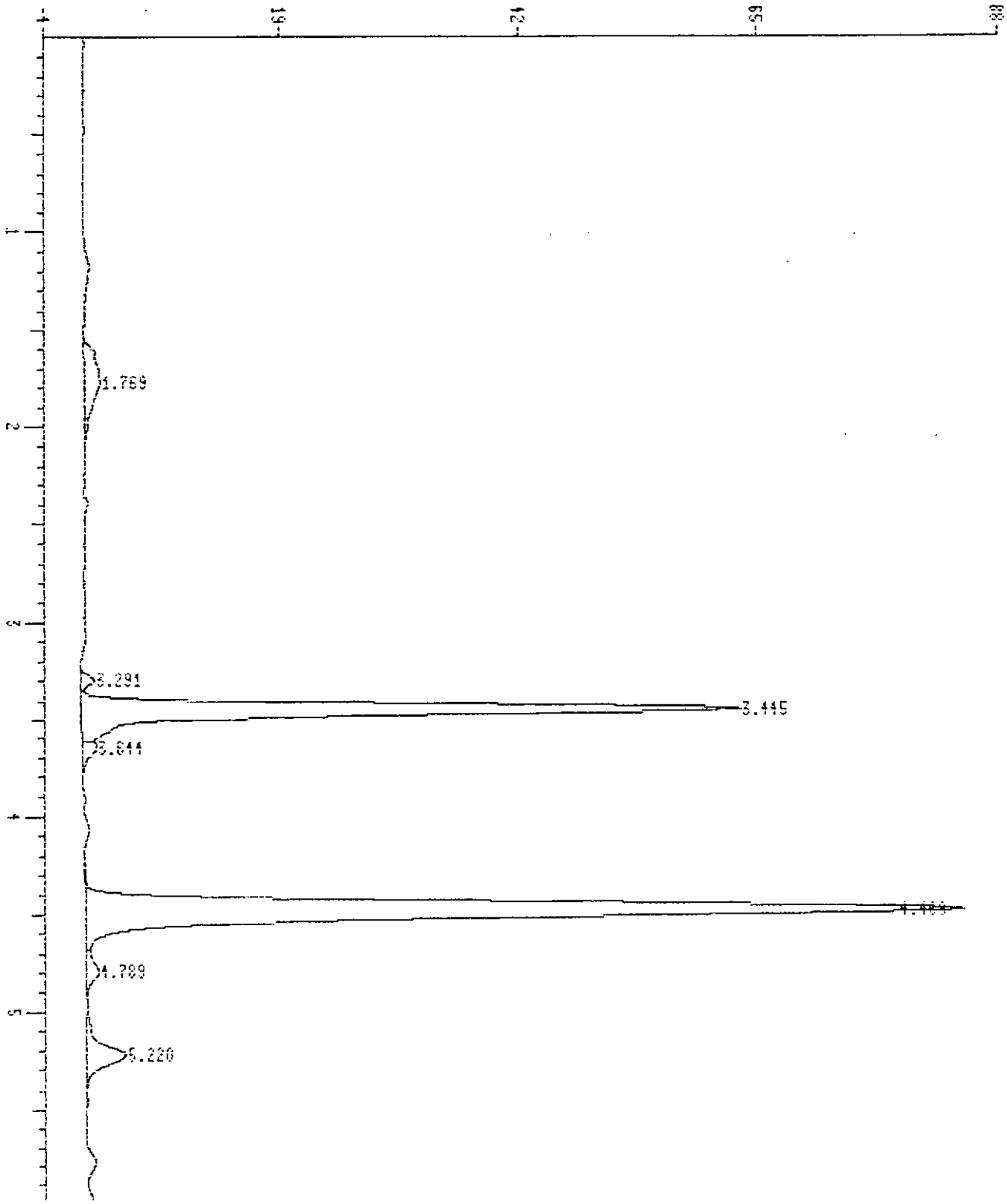
Operator: JCP 2 Apr 92 6:43 am
Method File Name : DNPHIII.M
Sample Info : #48
Misc Info:
Integration File Name : DATA:0401A57A.I
consisting of channels : 1. A 360,4 550,100 of 0401A57A.D
Sequence Index: 1 Bottle Number : 57 Repetition Number: 1

A 360,4 550,100 of 0401A57A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.766	BB	22.5071	1.4249	2.77	100.00	0.208	1.32
3.291	PV	4.9226	1.3129	0.61	100.00	0.061	0.95
3.445	VV	269.02	63.6026	33.11	100.00	0.066	0.81
3.644	VB	8.1476	1.4723	1.00	100.00	0.092	0.51
4.469	BV	467.71	84.8760	57.57	100.00	0.085	0.81
4.786	VB	8.9392	1.2696	1.10	100.00	0.108	0.96
5.221	BB	31.2145	4.1155	3.84	100.00	0.114	0.77

236

1: LC A 360,4 550,100 of 0401A57B.D



232

*** Area Percent ***

Report by Signal

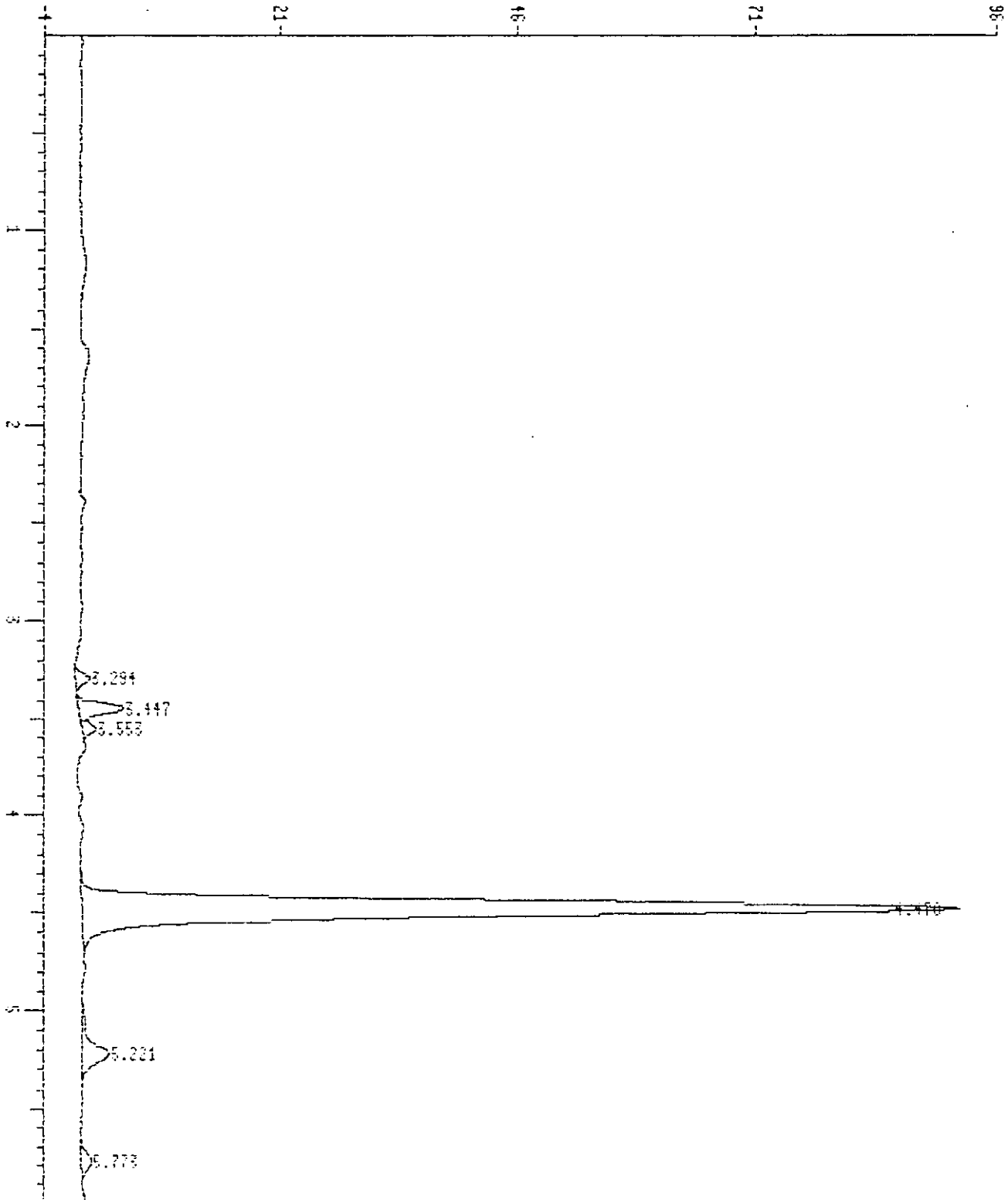
Operator: JCP 2 Apr 92 6:52 am
Method File Name : DNPHIII.M
Sample Info : #48
Misc Info:
Integration File Name : DATA:0401A57B.I
consisting of channels : 1. A 360,4 550,100 of 0401A57B.D
Sequence Index: 1 Bottle Number : 57 Repetition Number: 2

A 360,4 550,100 of 0401A57B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.759	BB	26.8315	1.5542	3.30	100.00	0.215	1.15
3.291	BV	4.9793	1.3242	0.61	100.00	0.060	0.90
3.445	VV	269.82	63.6311	33.22	100.00	0.066	0.81
3.644	VB	7.8672	1.4639	0.97	100.00	0.090	0.50
4.459	BV	465.87	84.7762	57.36	100.00	0.085	0.81
4.789	VB	8.7222	1.2119	1.07	100.00	0.104	1.25
5.220	BB	28.0759	3.8923	3.46	100.00	0.108	1.08

233

1: LC A 360,4 550,100 of 0401A58A.D



234

*** Area Percent ***

Report by Signal

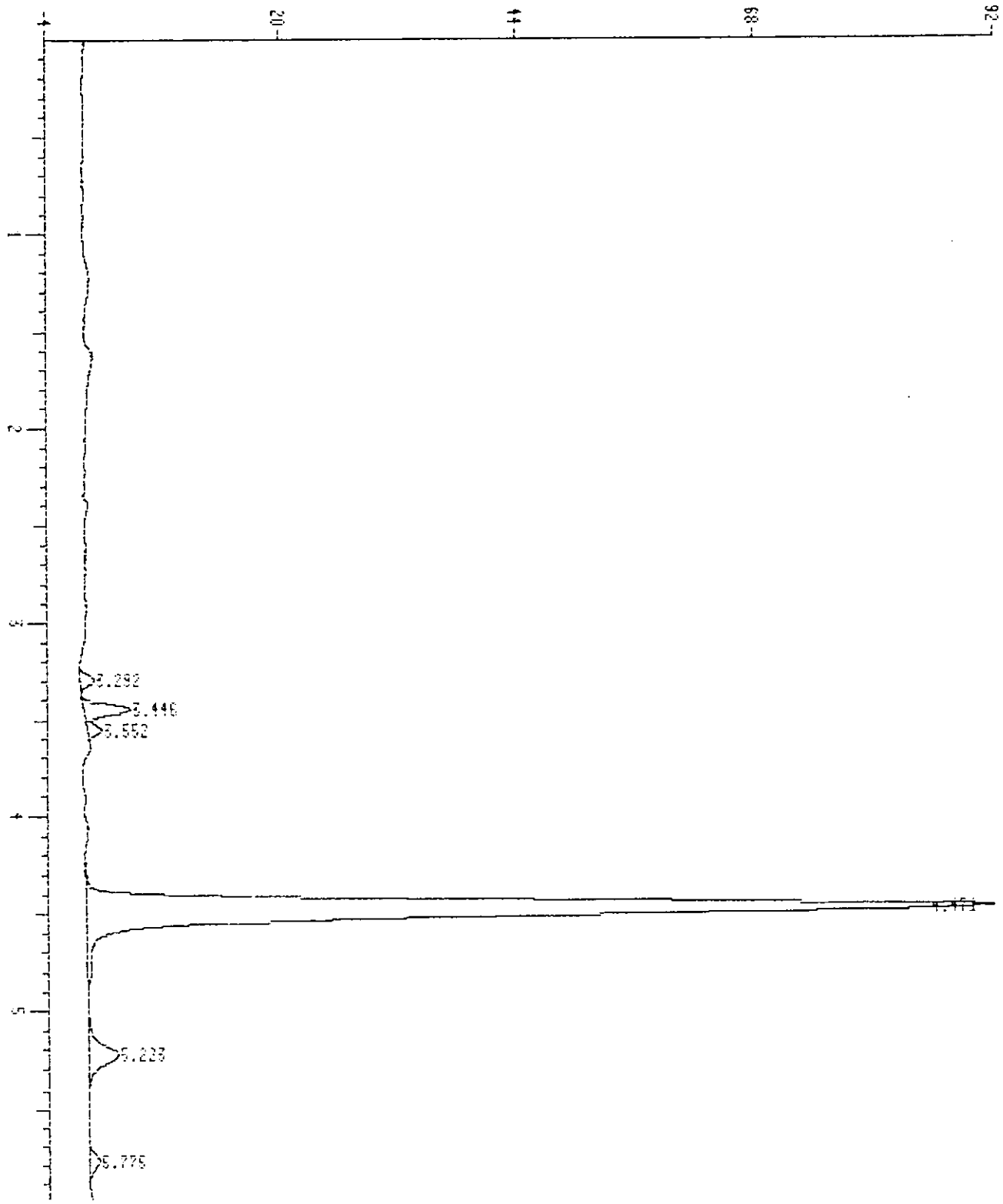
Operator: JCP 2 Apr 92 7:01 am
Method File Name : DNPHIII.M
Sample Info : #49
Misc Info:
Integration File Name : DATA:0401A58A.I
consisting of channels : 1. A 360,4 550,100 of 0401A58A.D
Sequence Index: 1 Bottle Number : 58 Repetition Number: 1

A 360,4 550,100 of 0401A58A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.294	PV	5.8664	1.5311	1.04	100.00	0.062	0.95
3.447	PV	18.6113	4.8941	3.29	100.00	0.061	0.95
3.553	VV	5.2361	1.4819	0.93	100.00	0.056	1.14
4.470	BV	506.42	92.2463	89.49	100.00	0.085	0.81
5.221	BB	22.5926	2.9627	3.99	100.00	0.113	1.28
5.773	BV	7.1738	1.1093	1.27	100.00	0.101	0.92

235

1: LC A 360,4 550,100 of 0401A58B.D



236

*** Area Percent ***

Report by Signal

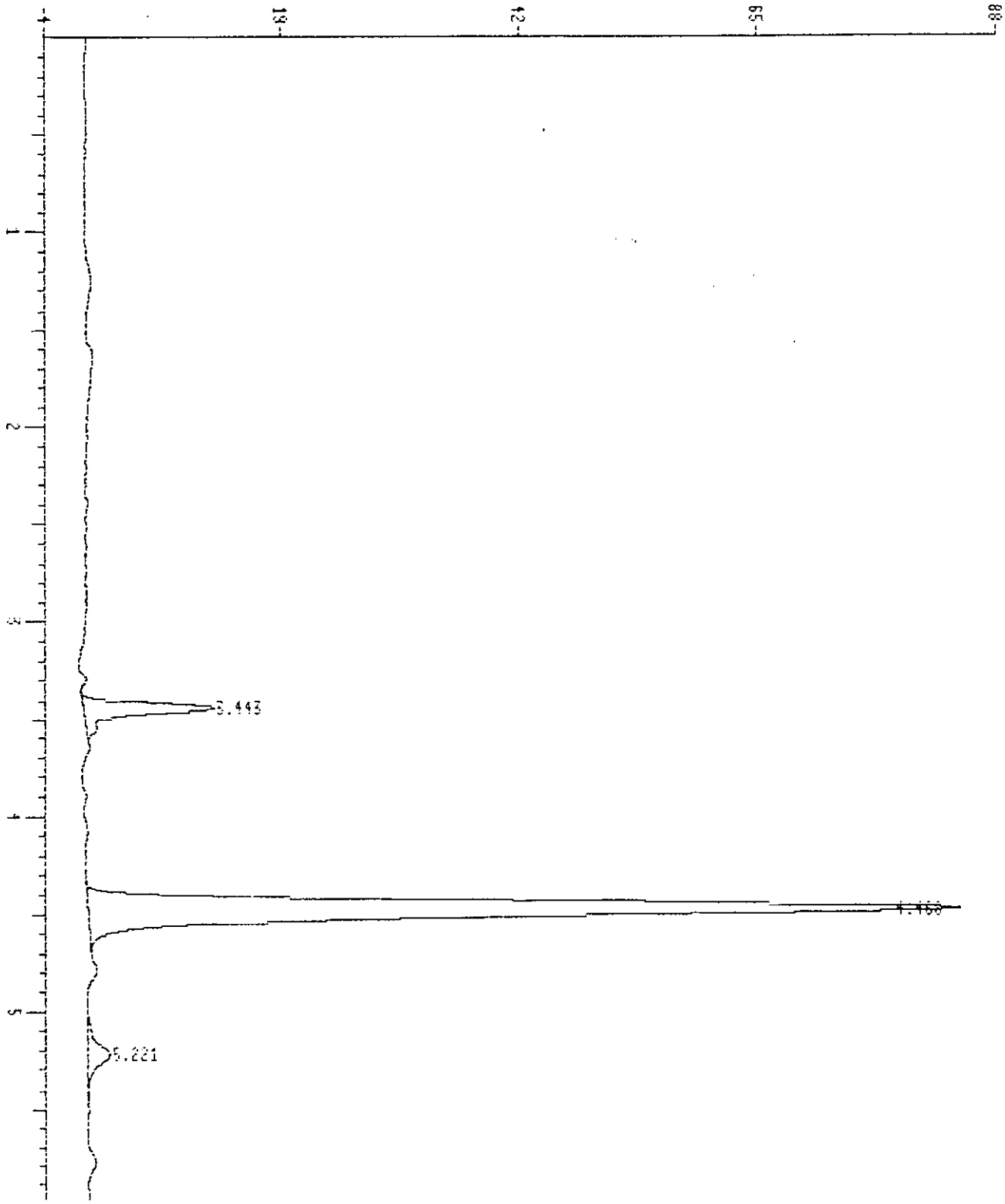
Operator: JCP 2 Apr 92 7:09 am
Method File Name : DNPHIII.M
Sample Info : #49
Misc Info:
Integration File Name : DATA:0401A58B.I
consisting of channels : 1. A 360,4 550,100 of 0401A58B.D
Sequence Index: 1 Bottle Number : 58 Repetition Number: 2

A 360,4 550,100 of 0401A58B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.292	BV	5.8608	1.5569	1.02	100.00	0.060	0.89
3.446	PV	18.3618	4.8856	3.21	100.00	0.060	0.95
3.552	VV	5.1566	1.4682	0.90	100.00	0.056	1.08
4.471	BB	513.28	92.2934	89.61	100.00	0.086	0.80
5.223	BB	23.5528	3.1455	4.11	100.00	0.110	1.01
5.775	BV	6.5787	1.1211	1.15	100.00	0.090	0.95

232

1: LC A 360,4 550,100 of 0401A59A.D



238

*** Area Percent ***

Report by Signal

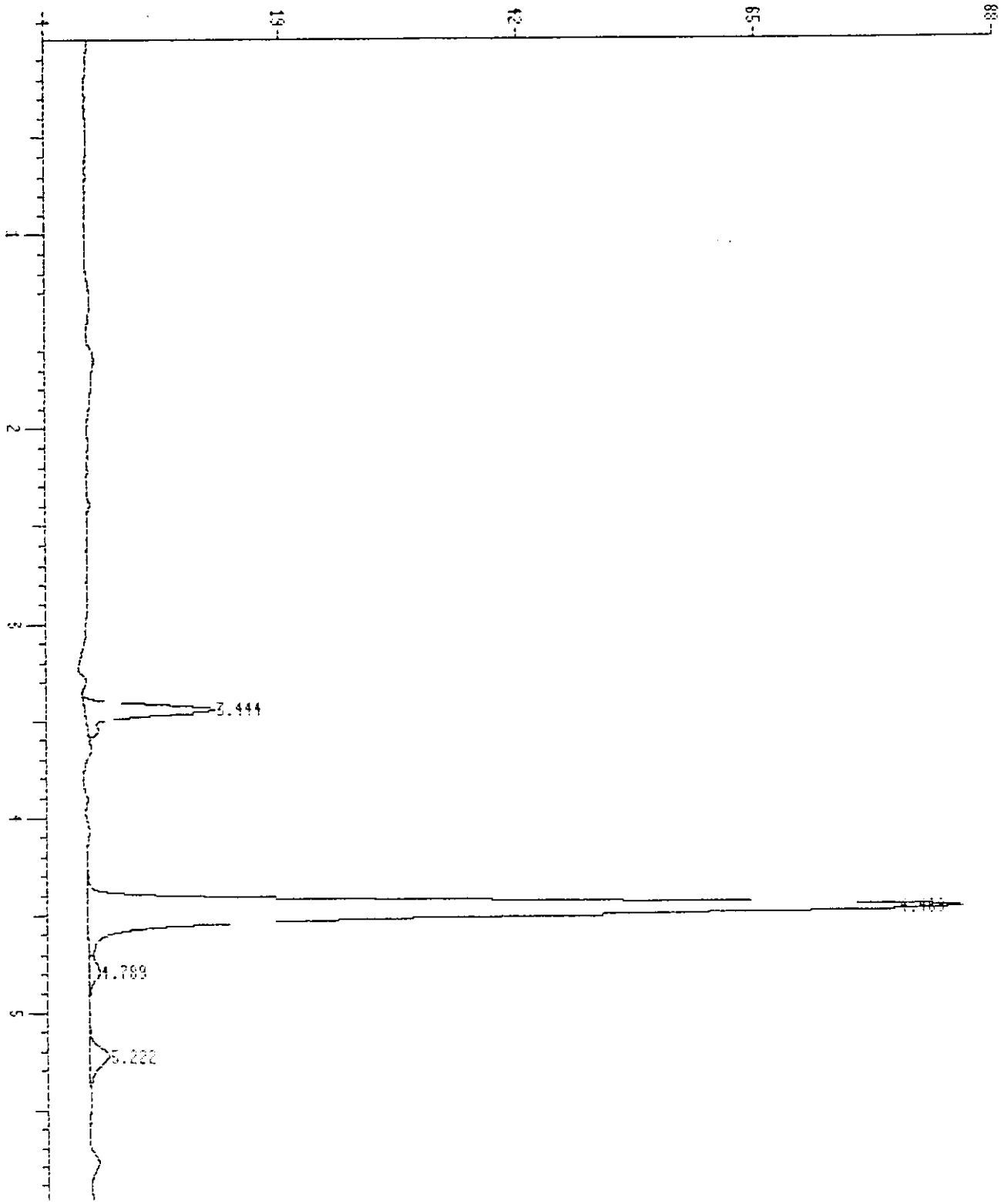
Operator: JCP 2 Apr 92 7:18 am
Method File Name : DNPHIII.M
Sample Info : #50
Misc Info:
Integration File Name : DATA:0401A59A.I
consisting of channels : 1. A 360,4 550,100 of 0401A59A.D
Sequence Index: 1 Bottle Number : 59 Repetition Number: 1

A 360,4 550,100 of 0401A59A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.443	PV	53.7760	12.7868	10.09	100.00	0.065	0.78
4.468	BV	461.03	84.5078	86.53	100.00	0.085	0.82
5.221	BB	17.9867	2.2042	3.38	100.00	0.119	1.06

239

1: LC A 360,4 550,100 of 0401A59B.D



240

*** Area Percent ***

Report by Signal

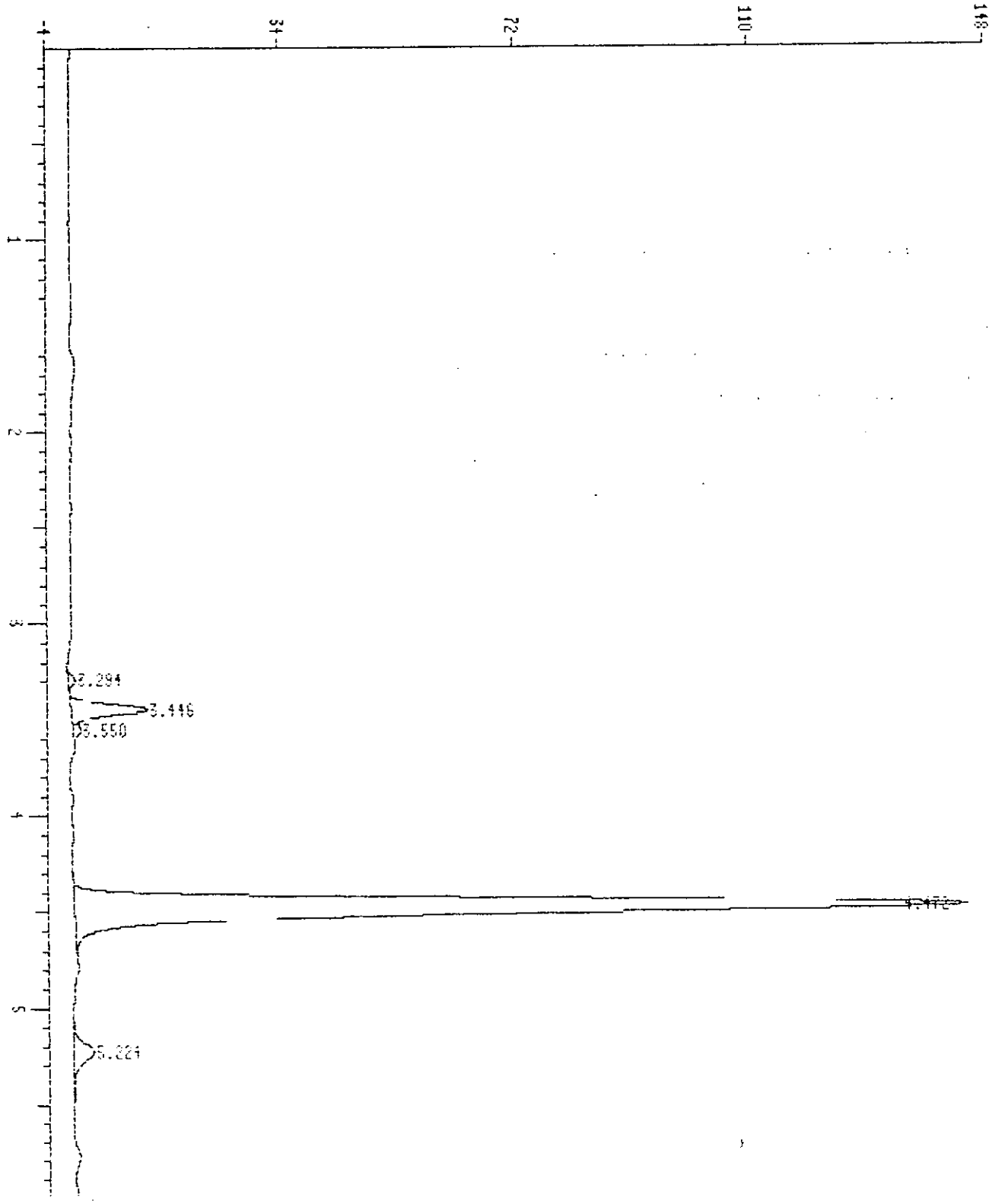
Operator: JCP 2 Apr 92 7:27 am
Method File Name : DNPHIII.M
Sample Info : #50
Misc Info:
Integration File Name : DATA:0401A59B.I
consisting of channels : 1. A 360,4 550,100 of 0401A59B.D
Sequence Index: 1 Bottle Number : 59 Repetition Number: 2

A 360,4 550,100 of 0401A59B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.444	PV	53.6309	12.7678	9.85	100.00	0.065	0.79
4.469	BV	469.03	84.9903	86.13	100.00	0.086	0.81
4.789	VB	7.7663	1.0988	1.43	100.00	0.107	1.07
5.222	BB	14.1451	1.9731	2.60	100.00	0.111	0.81

24

1: LC A 360,4 550,100 of 0401A60A.D



242

*** Area Percent ***

Report by Signal

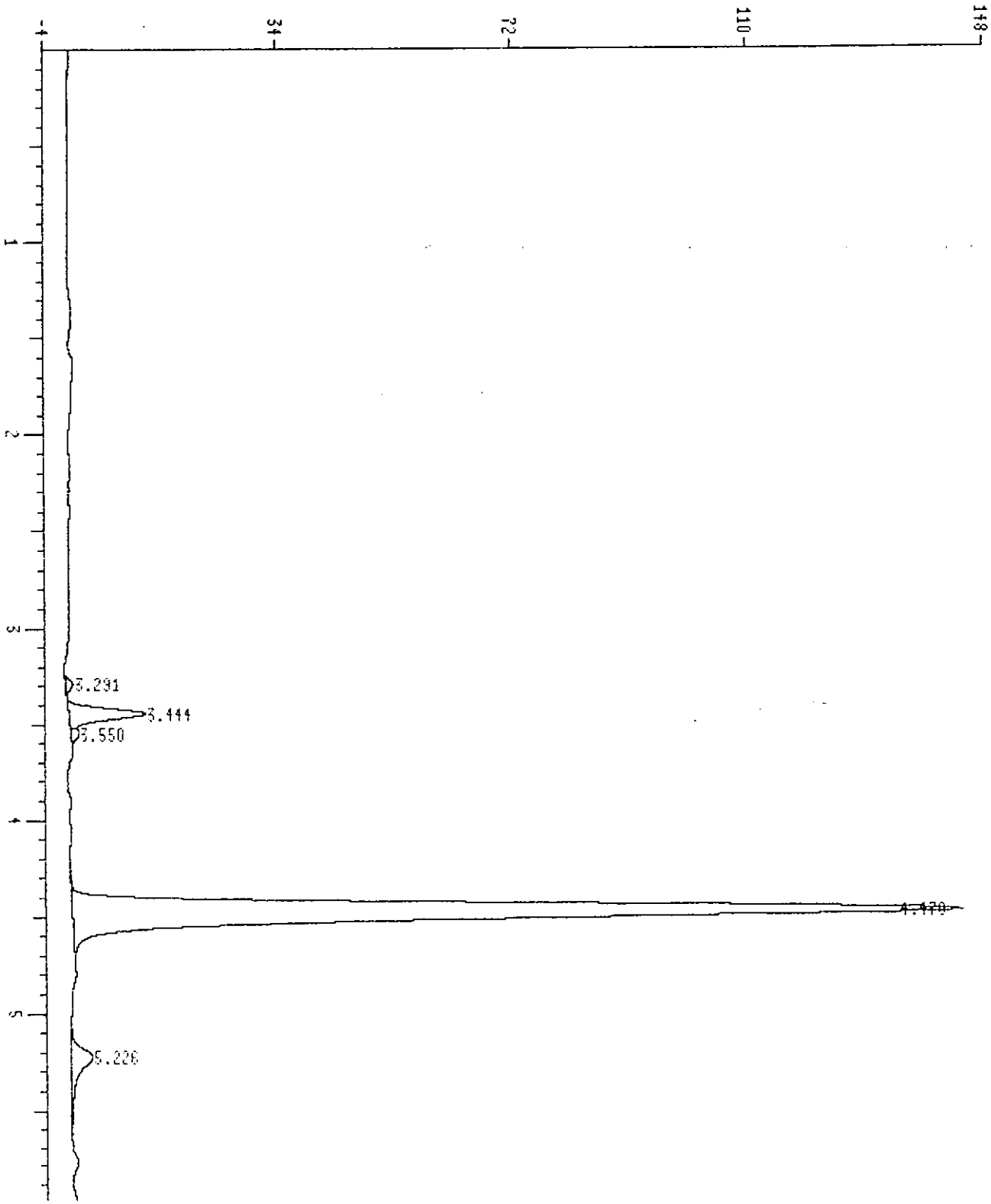
Operator: JCP 2 Apr 92 7:36 am
Method File Name : DNPHIII.M
Sample Info : #51
Misc Info:
Integration File Name : DATA:0401A60A.I
consisting of channels : 1. A 360,4 550,100 of 0401A60A.D
Sequence Index: 1 Bottle Number : 60 Repetition Number: 1

A 360,4 550,100 of 0401A60A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.294	BV	4.2155	1.1585	0.48	100.00	0.059	1.09
3.446	PV	49.4824	12.6702	5.68	100.00	0.062	0.91
3.550	VV	4.2058	1.3160	0.48	100.00	0.053	0.87
4.472	BV	789.11	144.62	90.60	100.00	0.085	0.82
5.224	BB	23.9455	3.3324	2.75	100.00	0.107	0.82

243

1: LC A 360,4 550,100 of 0401A60B.D



244

*** Area Percent ***

Report by Signal

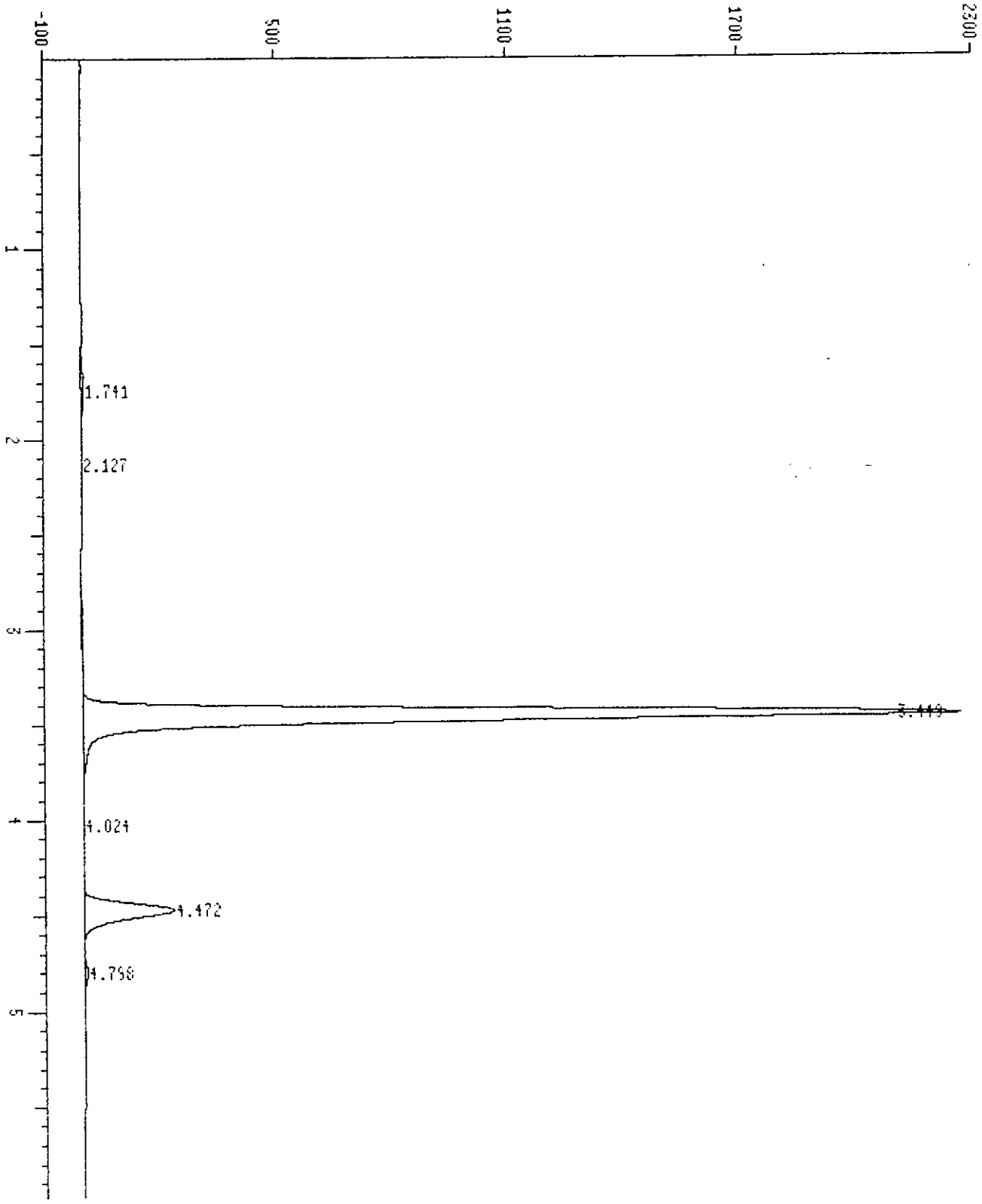
Operator: JCP 2 Apr 92 7:44 am
Method File Name : DNPHIII.M
Sample Info : #51
Misc Info:
Integration File Name : DATA:0401A60B.I
consisting of channels : 1. A 360,4 550,100 of 0401A60B.D
Sequence Index: 1 Bottle Number : 60 Repetition Number: 2

A 360,4 550,100 of 0401A60B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.291	BV	4.2844	1.1650	0.49	100.00	0.060	1.00
3.444	PV	49.6947	12.6181	5.67	100.00	0.062	0.91
3.550	VV	4.5082	1.3554	0.51	100.00	0.055	0.87
4.470	BV	788.54	144.20	89.99	100.00	0.085	0.82
5.226	BB	29.2389	3.4631	3.34	100.00	0.123	0.61

245

1: LC A 360,4 550,100 of 0401A61A.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

246

*** Area Percent ***

Report by Signal

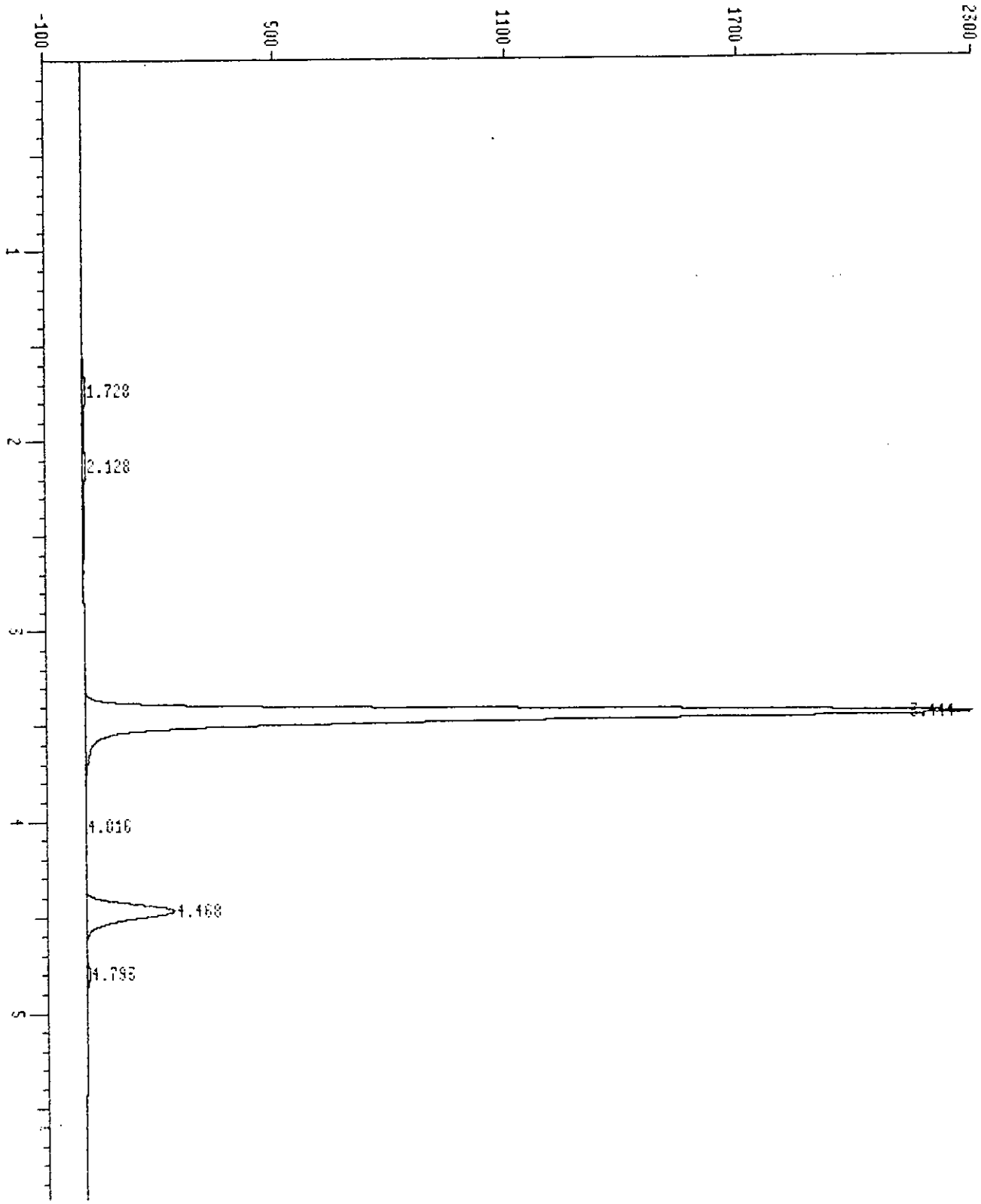
Operator: JCP 2 Apr 92 7:53 am
Method File Name : DNPHIII.M
Sample Info. : #52
Misc Info:
Integration File Name : DATA:0401A61A.I
consisting of channels : 1. A 360,4 550,100 of 0401A61A.D
Sequence Index: 1 Bottle Number : 61 Repetition Number: 1

A 360,4 550,100 of 0401A61A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.741	PV	90.3601	5.2049	0.80	100.00	0.256	0.73
2.127	VV	12.9326	1.0181	0.11	100.00	0.178	0.67
3.449	BV	9875.83	2273.25	87.14	100.00	0.067	0.81
4.024	VB	10.9337	1.5789	0.10	100.00	0.098	0.77
4.472	BV	1274.97	232.05	11.25	100.00	0.085	0.81
4.798	VV	68.7130	9.8215	0.61	100.00	0.109	0.93

247

1: LC A 360,4 550,100 of 0401A61B.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

248

*** Area Percent ***

Report by Signal

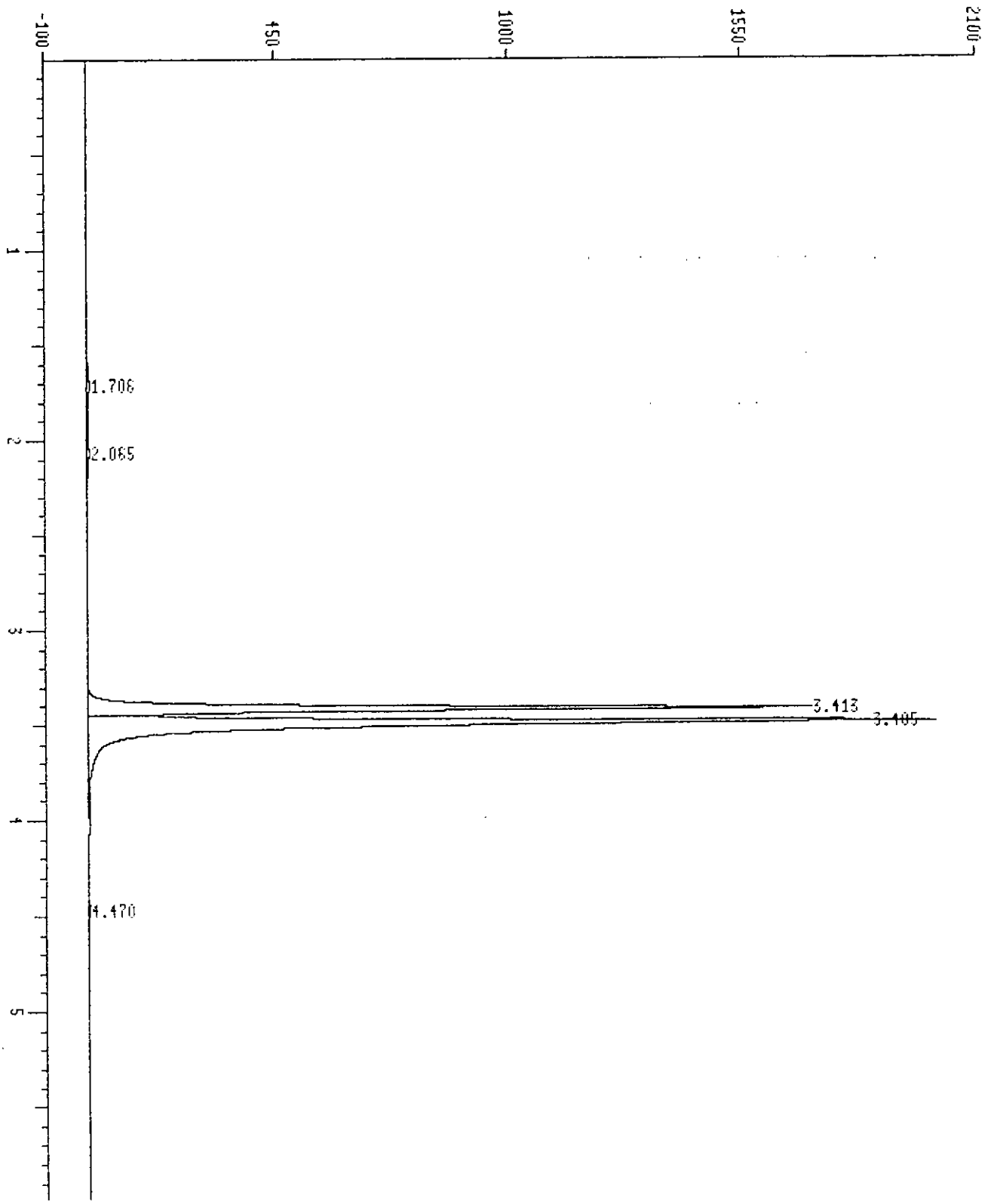
Operator: JCP 2 Apr 92 8:02 am
Method File Name : DNPHIII.M
Sample Info : #52
Misc Info:
Integration File Name : DATA:0401A61B.I
consisting of channels : 1. A 360,4 550,100 of 0401A61B.D
Sequence Index: 1 Bottle Number : 61 Repetition Number: 2

A 360,4 550,100 of 0401A61B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.728	BV	82.6255	4.8063	0.72	100.00	0.276	0.71
2.128	VB	83.5139	6.1638	0.72	100.00	0.197	0.80
3.444	BV	10018	2302.67	86.85	100.00	0.067	0.81
4.016	VB	8.4701	1.4914	0.07	100.00	0.085	0.41
4.468	BV	1273.73	232.01	11.04	100.00	0.085	0.81
4.793	VB	68.6017	9.9146	0.59	100.00	0.107	0.93

249

1: LC A 360,4 550,100 of 0401A62A.D



End of plot. Time = 0.01 to 5.98 minutes Chart speed = 3.33 cm/min

212

*** Area Percent ***

Report by Signal

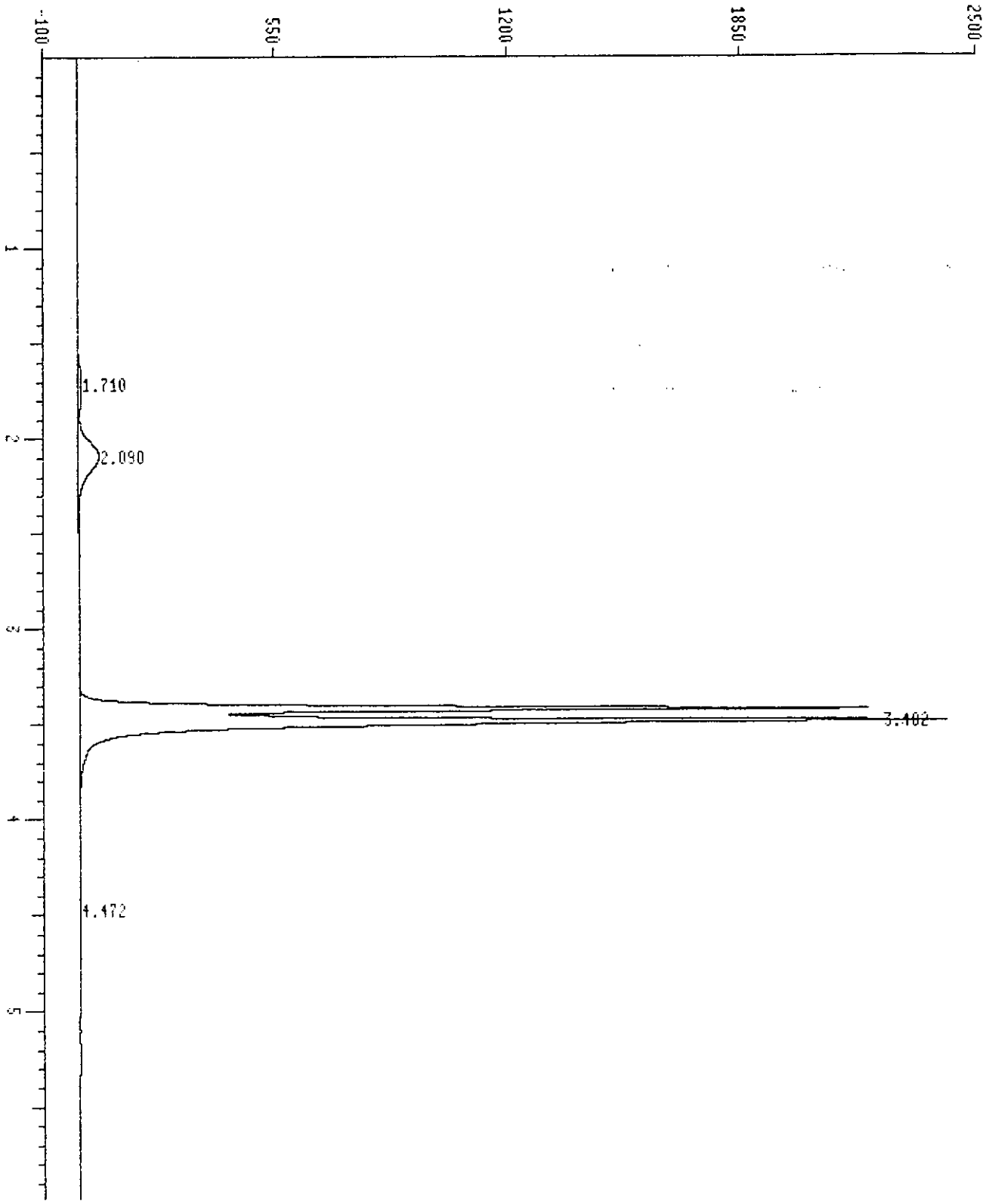
Operator: JCP 2 Apr 92 8:10 am
Method File Name : DNPHIII.M
Sample Info : #53
Misc Info:
Integration File Name : DATA:0401A62A.I
consisting of channels : 1. A 360,4 550,100 of 0401A62A.D
Sequence Index: 1 Bottle Number : 62 Repetition Number: 1

A 360,4 550,100 of 0401A62A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.706	BV	100.84	6.4777	1.21	100.00	0.225	0.62
2.065	VB	94.0536	6.3954	1.13	100.00	0.212	0.68
3.413	BV	3084.52	1767.31	37.05	100.00	0.029	1.18
3.485	VV	5024.98	1983.30	60.36	100.00	0.039	0.55
4.470	VB	20.2315	3.3786	0.24	100.00	0.091	0.95

152

1: LC A 360,4 550,100 of 0401A62B.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

22

*** Area Percent ***

Report by Signal

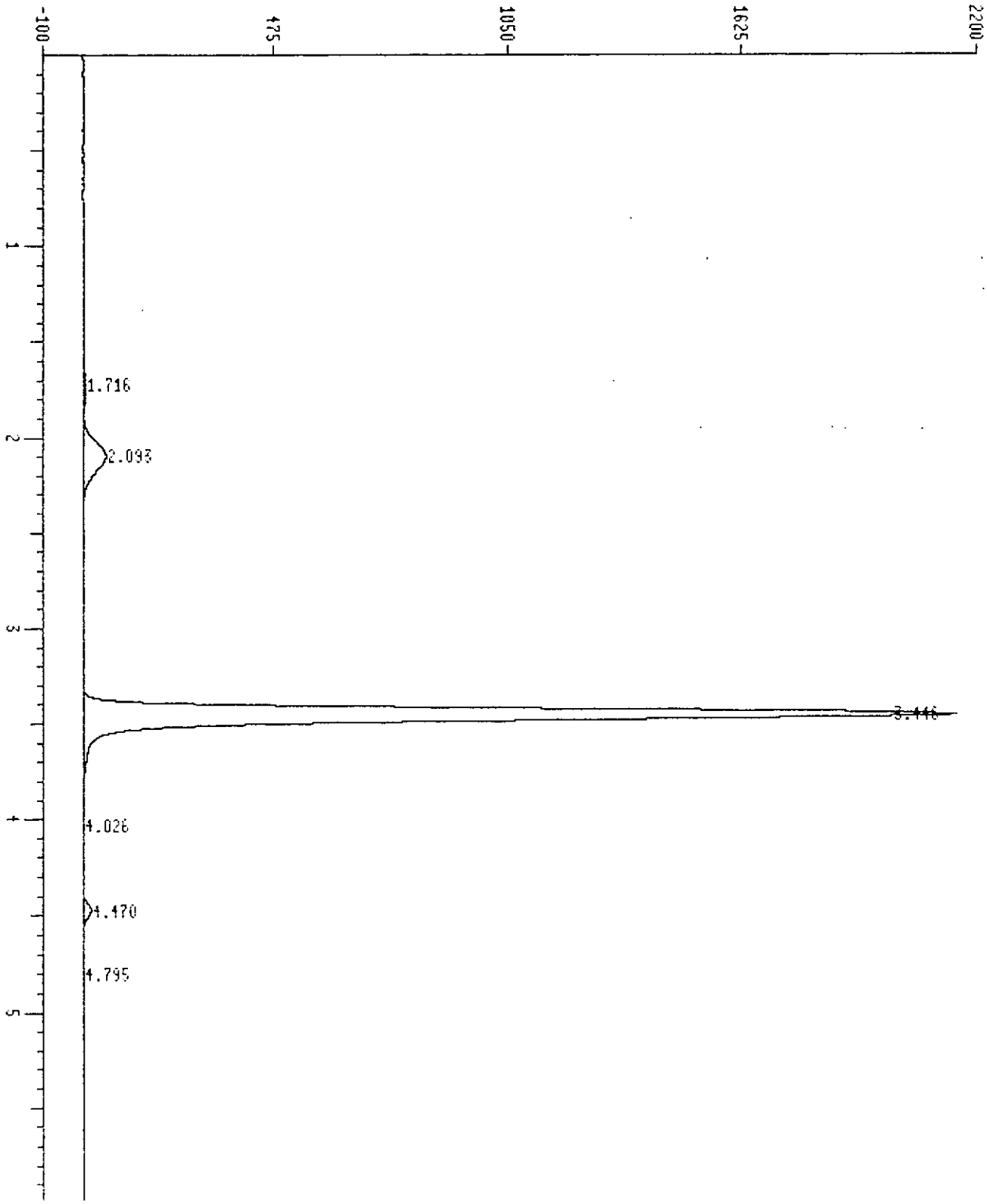
Operator: JCP 2 Apr 92 8:19 am
Method File Name : DNPHIII.M
Sample Info : #53
Misc Info:
Integration File Name : DATA:0401A62B.I
consisting of channels : 1. A 360,4 550,100 of 0401A62B.D
Sequence Index: 1 Bottle Number : 62 Repetition Number: 2

A 360,4 550,100 of 0401A62B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.710	BV	95.5050	6.5222	0.88	100.00	0.207	0.77
2.090	VB	681.49	57.5846	6.28	100.00	0.179	0.85
3.482	BV	10057	2364.89	92.65	100.00	0.078	1.54
4.472	VV	20.6430	3.3957	0.19	100.00	0.093	0.83

213

1: LC A 360,4 550,100 of 0401A63A.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.34 cm/min

254

*** Area Percent ***

Report by Signal

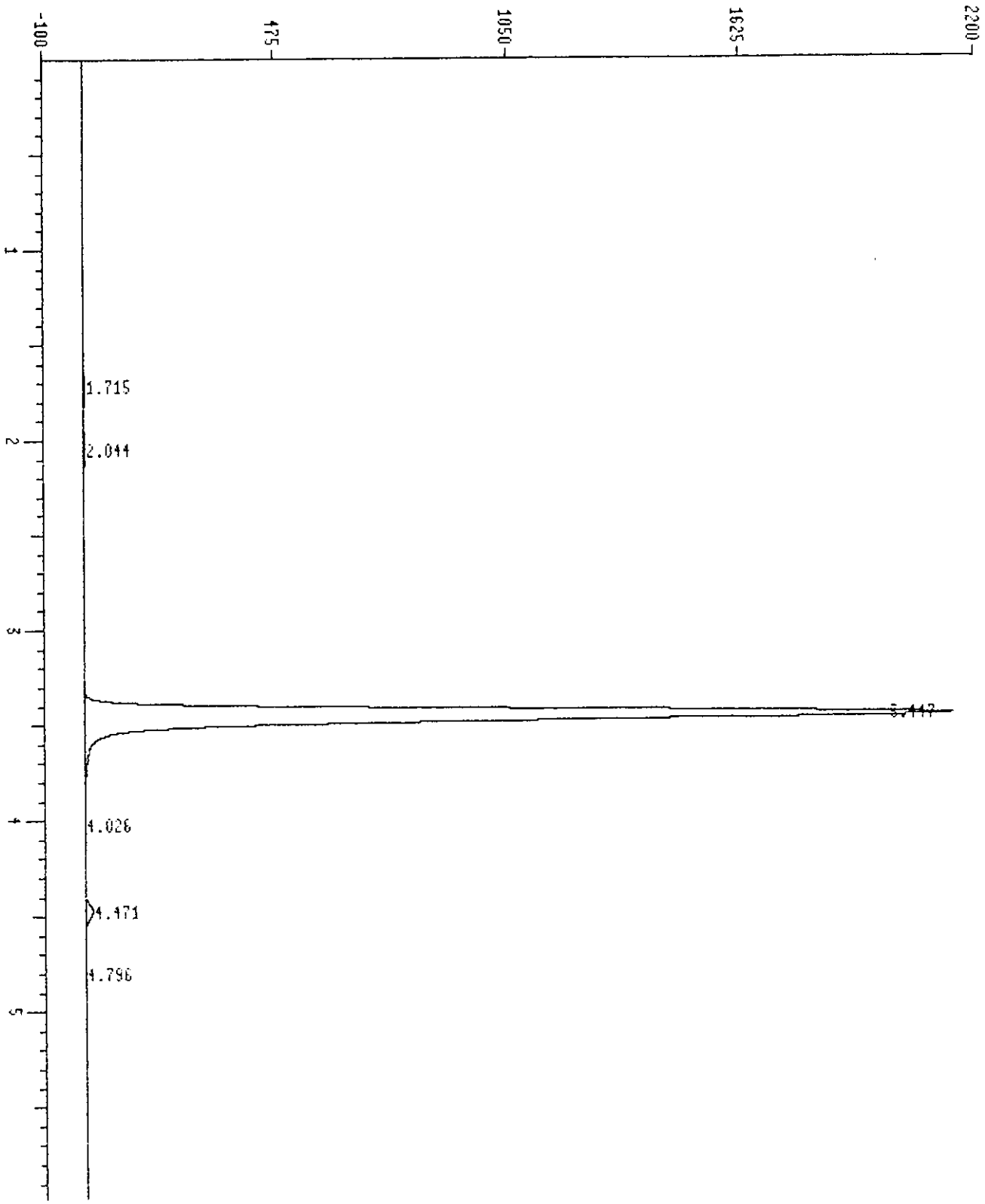
Operator: JCP 2 Apr 92 8:28 am
Method File Name : DNPHIII.M
Sample Info : #54
Misc Info:
Integration File Name : DATA:0401A63A.I
consisting of channels : 1. A 360,4 550,100 of 0401A63A.D
Sequence Index: 1 Bottle Number : 63 Repetition Number: 1

A 360,4 550,100 of 0401A63A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.716	BV	65.1995	4.3364	0.63	100.00	0.216	0.76
2.093	VB	671.13	57.1312	6.53	100.00	0.183	0.86
3.446	BV	9391.93	2154.09	91.41	100.00	0.067	0.80
4.026	VB	14.0433	1.7720	0.14	100.00	0.111	0.63
4.470	BV	109.36	19.9748	1.06	100.00	0.085	0.82
4.795	VB	22.7098	3.2853	0.22	100.00	0.107	0.89

242

1: LC A 360,4 550,100 of 0401A63B.D



End of plot. Time = 0.00 to 5.98 minutes Chart speed = 3.33 cm/min

242

*** Area Percent ***

Report by Signal

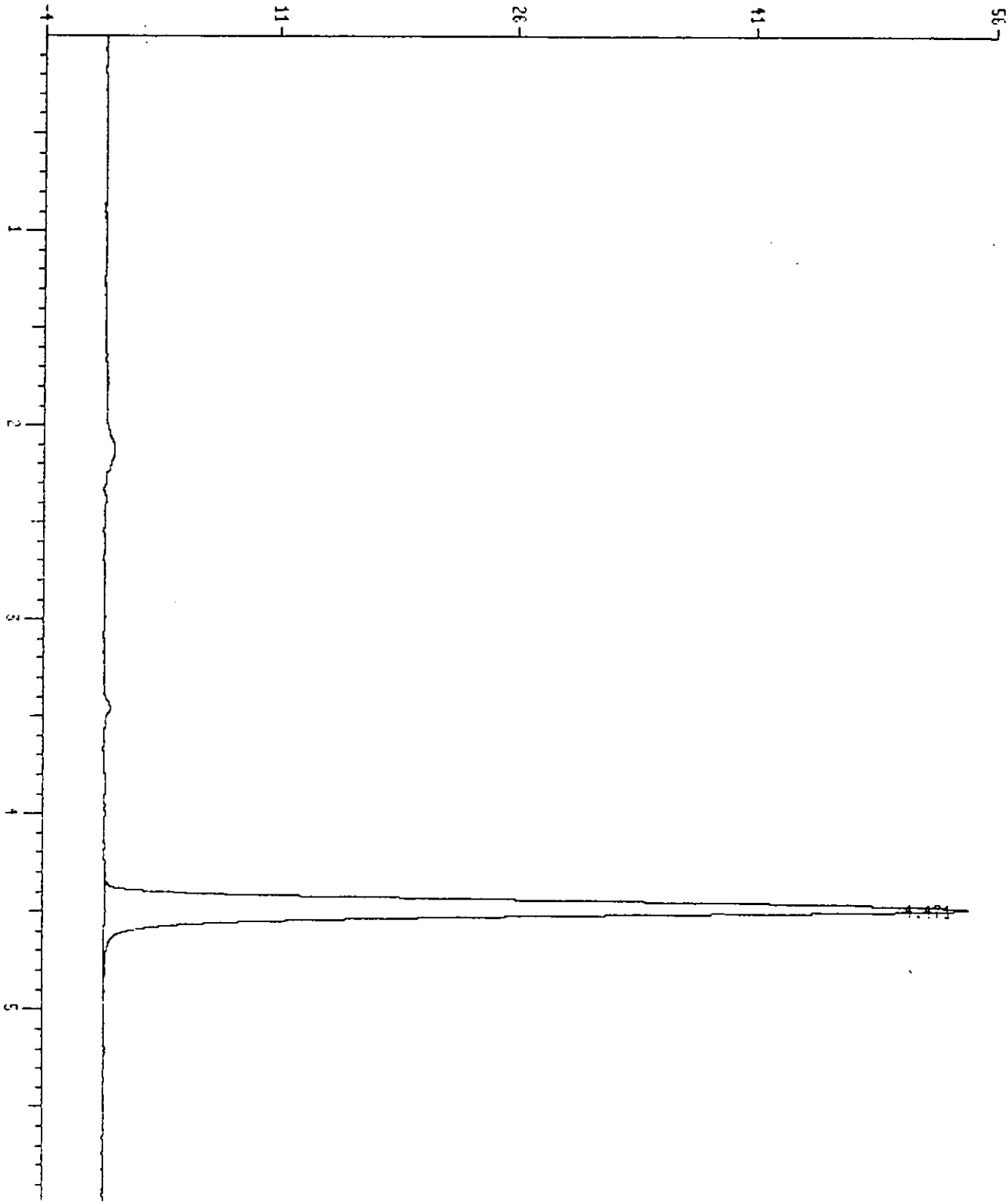
Operator: JCP 2 Apr 92 8:37 am
Method File Name : DNPHIII.M
Sample Info : #54
Misc Info:
Integration File Name : DATA:0401A63B.I
consisting of channels : 1. A 360,4 550,100 of 0401A63B.D
Sequence Index: 1 Bottle Number : 63 Repetition Number: 2

A 360,4 550,100 of 0401A63B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.715	BV	64.8016	3.9685	0.67	100.00	0.232	0.65
2.044	VV	74.4376	5.8630	0.77	100.00	0.193	0.84
3.447	BV	9386.32	2152.32	97.07	100.00	0.067	0.81
4.026	VB	12.0513	1.7129	0.12	100.00	0.104	0.67
4.471	BV	109.69	20.0165	1.13	100.00	0.085	0.82
4.796	PB	22.2901	3.3028	0.23	100.00	0.105	0.88

257

1: LC A 360,4 550,100 of 0401A68A.D



250

*** Area Percent ***

Report by Signal

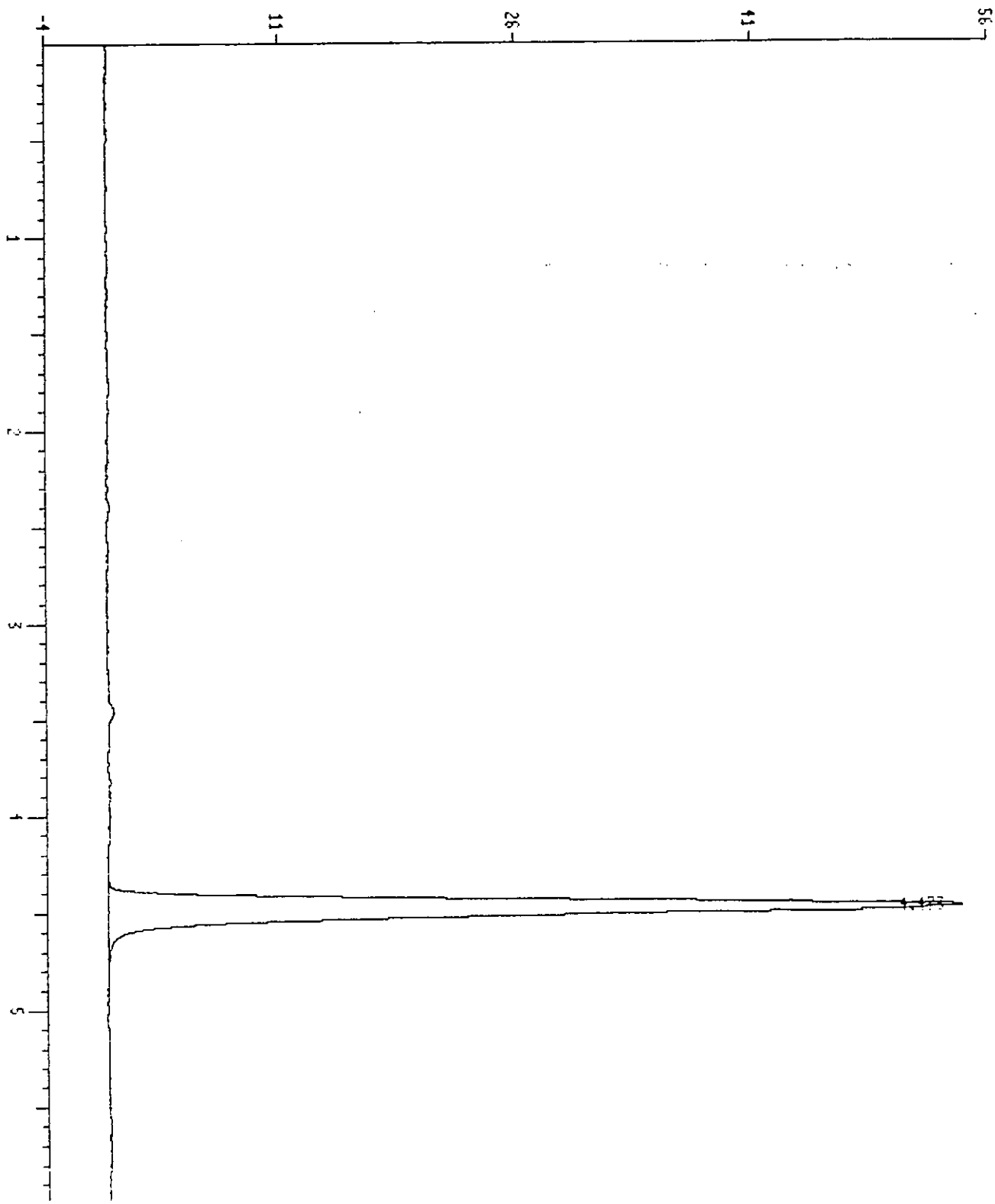
Operator: JCP 2 Apr 92 9:56 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 5 PPM
Misc Info:
Integration File Name : DATA:0401A68A.I
consisting of channels : 1. A 360,4 550,100 of 0401A68A.D
Sequence Index: 1 Bottle Number : 68 Repetition Number: 1

A 360,4 550,100 of 0401A68A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.471	BB	299.81	54.4754	100.00	100.00	0.085	0.81

259

1: LC A 360,4 550,100 of 0401A68B.D



260

*** Area Percent ***

Report by Signal

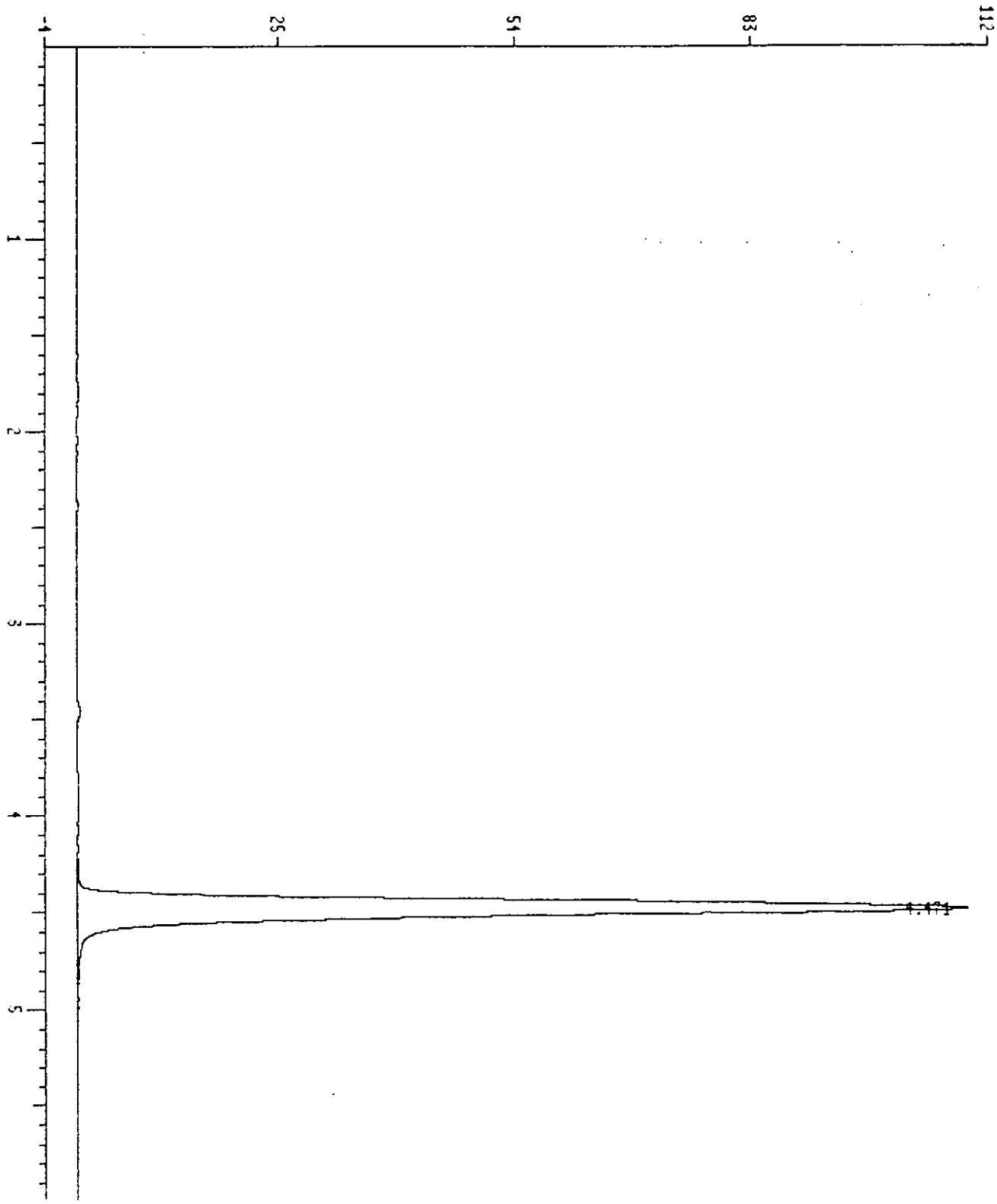
Operator: JCP 2 Apr 92 10:04 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 5 PPM
Misc Info:
Integration File Name : DATA:0401A68B.I
consisting of channels : 1. A 360,4 550,100 of 0401A68B.D
Sequence Index: 1 Bottle Number : 68 Repetition Number: 2

A 360,4 550,100 of 0401A68B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.473	BB	298.93	54.4860	100.00	100.00	0.085	0.82

261

1: LC A 360,4 550,100 cf 0401A69A.D



22

*** Area Percent ***

Report by Signal

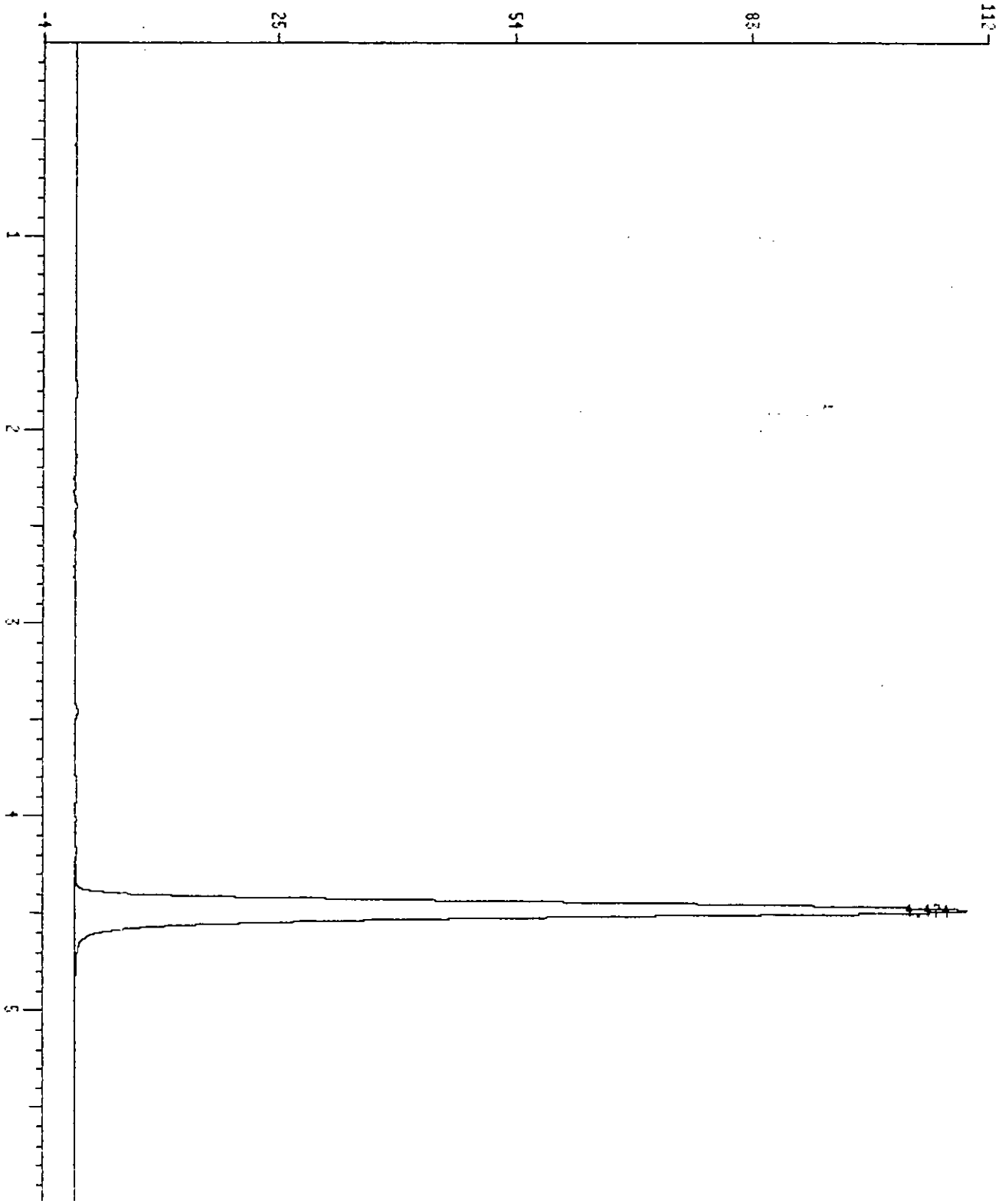
Operator: JCP 2 Apr 92 10:13 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 10 PPM
Misc Info:
Integration File Name : DATA:0401A69A.I
consisting of channels : 1. A 360,4 550,100 of 0401A69A.D
Sequence Index: 1 Bottle Number : 69 Repetition Number: 1

A 360,4 550,100 of 0401A69A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.471	BB	605.04	109.74	100.00	100.00	0.086	0.82

263

1: LC A 360,4 550,100 of 0401A69B.D



264

*** Area Percent ***

Report by Signal

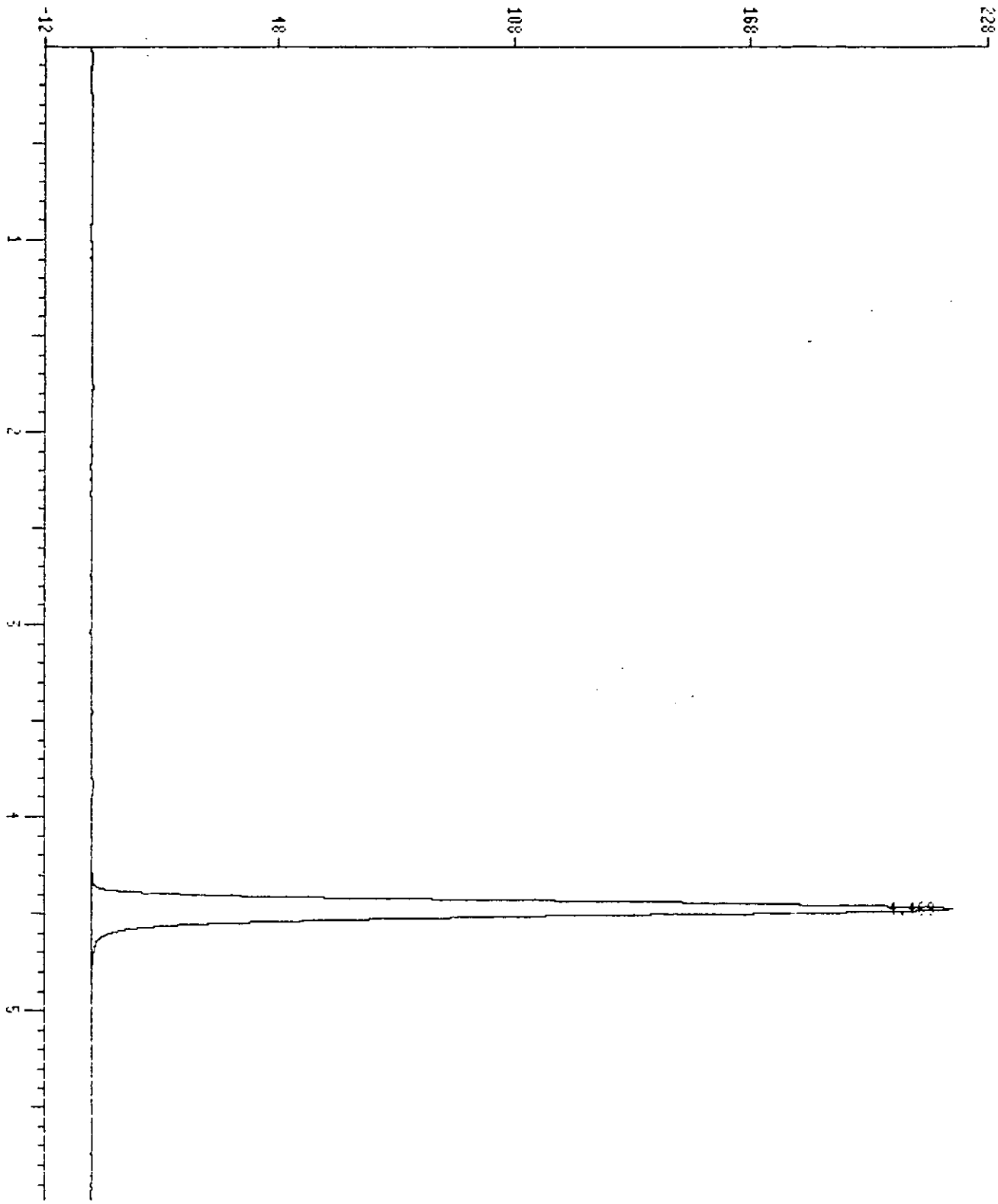
Operator: JCP 2 Apr 92 10:22 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 10 PPM
Misc Info:
Integration File Name : DATA:0401A69B.I
consisting of channels : 1. A 360,4 550,100 of 0401A69B.D
Sequence Index: 1 Bottle Number : 69 Repetition Number: 2

A 360,4 550,100 of 0401A69B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.474	BB	605.86	109.84	100.00	100.00	0.086	0.82

2655

1: LC A 360,4 550,100 of 0401A70A.D



266

*** Area Percent ***

Report by Signal

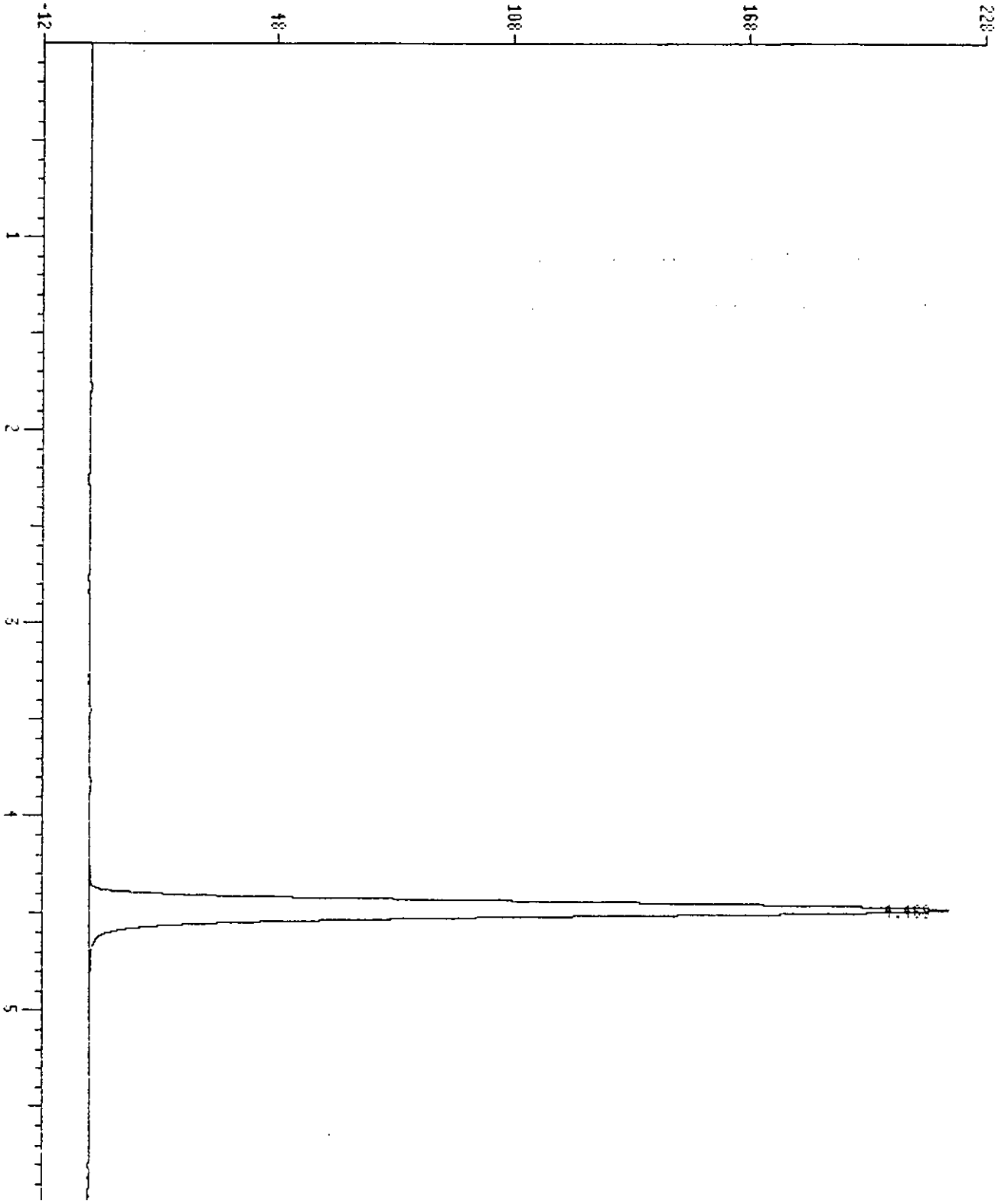
Operator: JCP 2 Apr 92 10:30 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 20 PPM
Misc Info:
Integration File Name : DATA:0401A70A.I
consisting of channels : 1. A 360,4 550,100 of 0401A70A.D
Sequence Index: 1 Bottle Number : 70 Repetition Number: 1

A 360,4 550,100 of 0401A70A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.469	BB	1203.79	219.12	100.00	100.00	0.085	0.82

202

1: LC A 360,4 550,100 of 0401A70B.D



2928

*** Area Percent ***

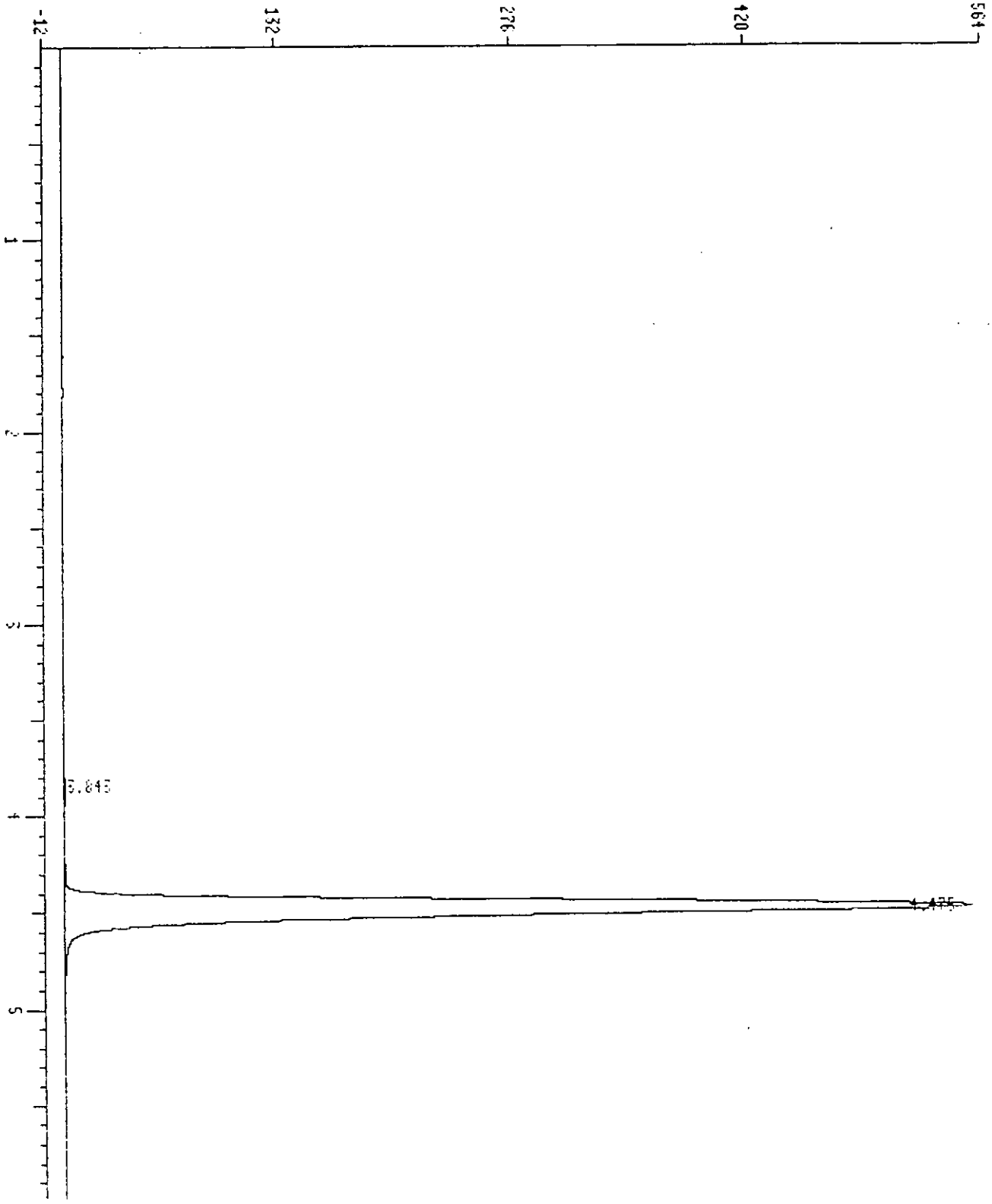
Report by Signal

Operator: JCP 2 Apr 92 10:39 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 20 PPM
Misc Info:
Integration File Name : DATA:0401A70B.I
consisting of channels : 1. A 360,4 550,100 of 0401A70B.D
Sequence Index: 1 Bottle Number : 70 Repetition Number: 2

A 360,4 550,100 of 0401A70B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
4.469	BB	1200.09	219.18	100.00	100.00	0.085	0.82

1: LC A 360,4 550,100 of 0401A71A.D



270

*** Area Percent ***

Report by Signal

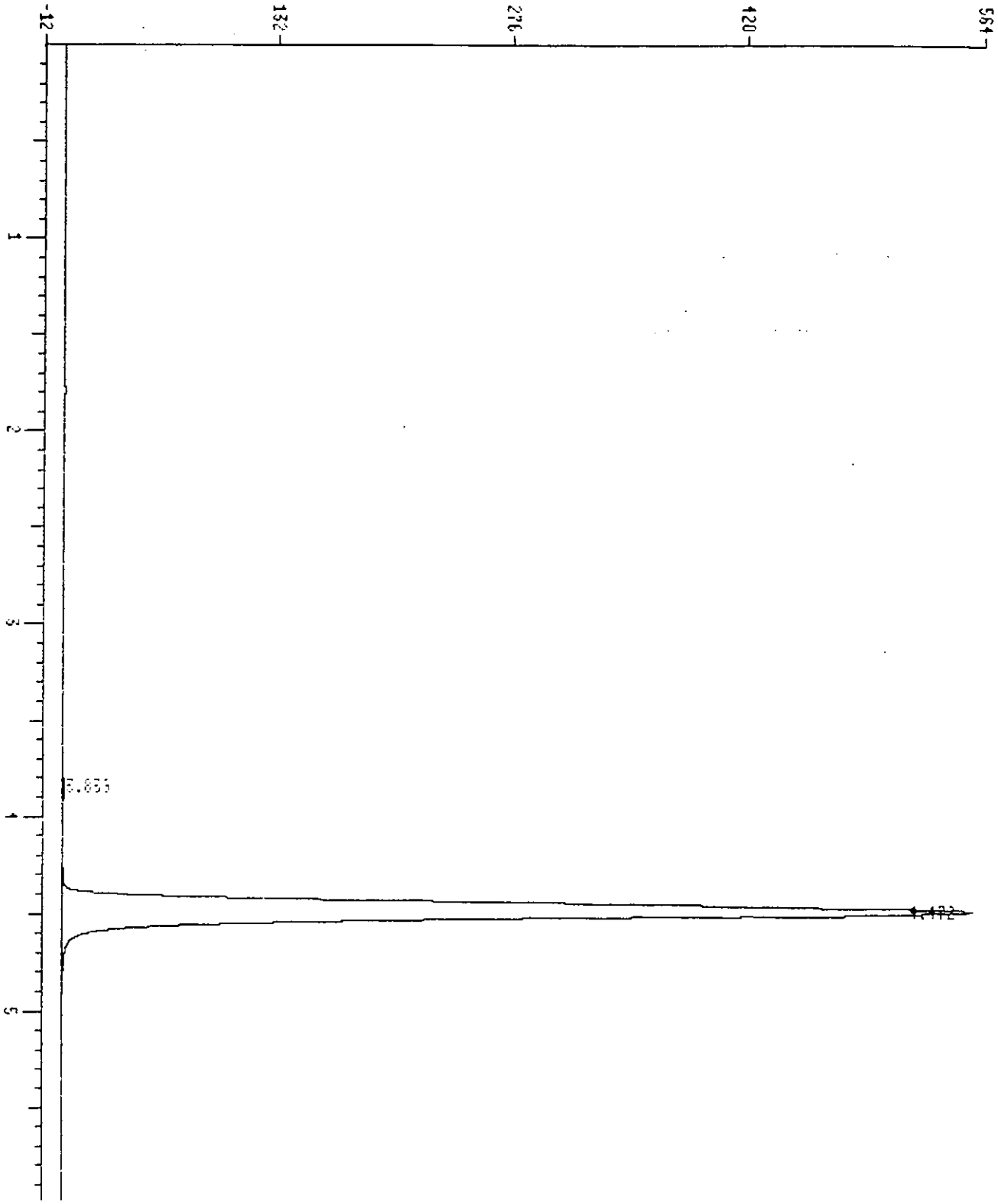
Operator: JCP 2 Apr 92 10:48 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 50 PPM
Misc Info:
Integration File Name : DATA:0401A71A.I
consisting of channels : 1. A 360,4 550,100 of 0401A71A.D
Sequence Index: 1 Bottle Number : 71 Repetition Number: 1

A 360,4 550,100 of 0401A71A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.843	BB	4.5558	0.7204	0.15	100.00	0.101	0.87
4.475	BB	3048.75	557.65	99.85	100.00	0.085	0.82

271

1: LC A 360,4 550,100 of 0401A71B.D



272

*** Area Percent ***

Report by Signal

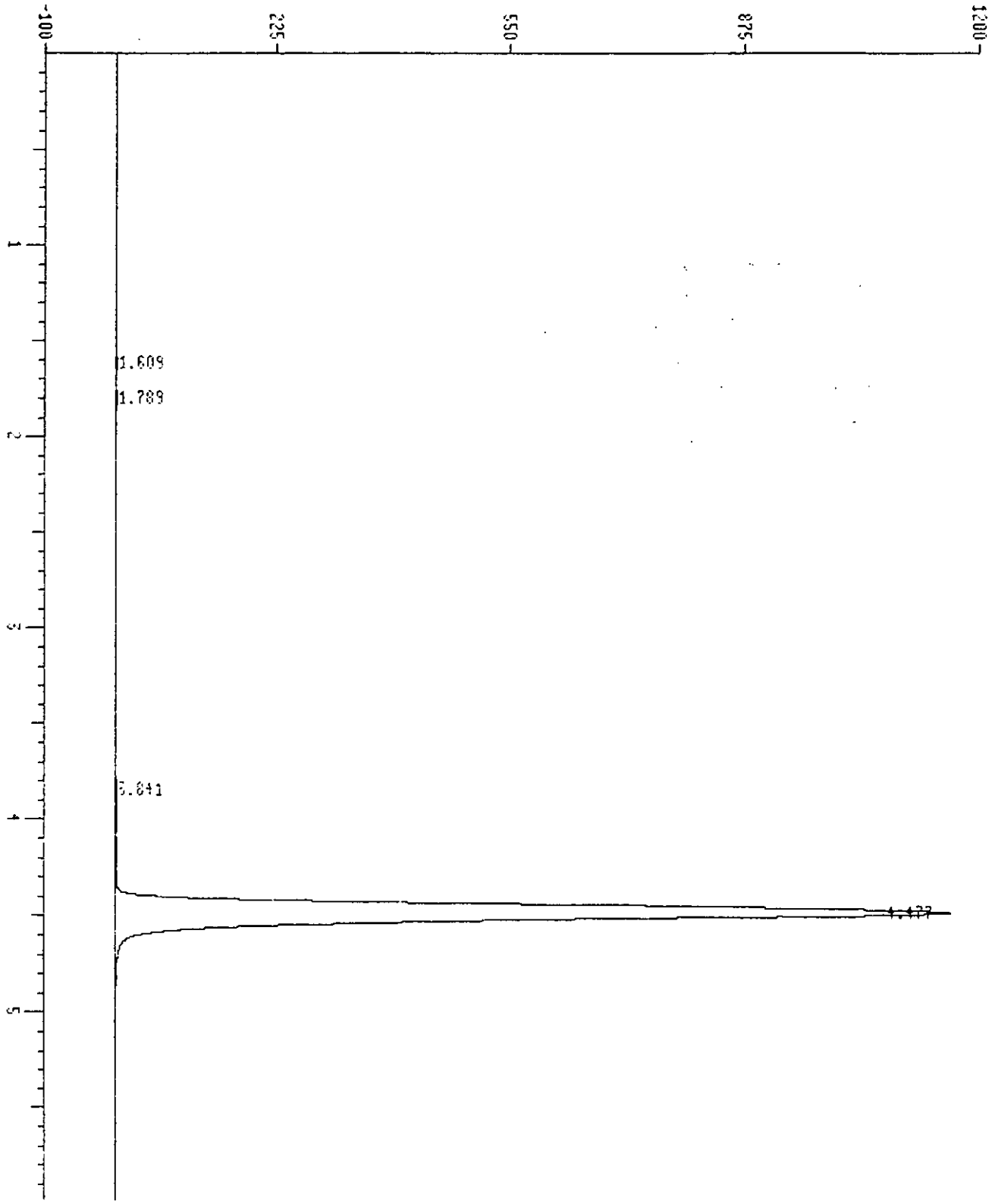
Operator: JCP 2 Apr 92 10:57 am
Method File Name : DNPHIII.M
Sample Info : STANDARD; 50 PPM
Misc Info:
Integration File Name : DATA:0401A71B.I
consisting of channels : 1. A 360,4 550,100 of 0401A71B.D
Sequence Index: 1 Bottle Number : 71 Repetition Number: 2

A 360,4 550,100 of 0401A71B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
3.839	BB	7.2330	0.8703	0.24	100.00	0.129	0.46
4.472	BB	3040.21	557.91	99.76	100.00	0.084	0.82

272

1: LC A 360,4 550,100 of 0401A72A.D



274

*** Area Percent ***

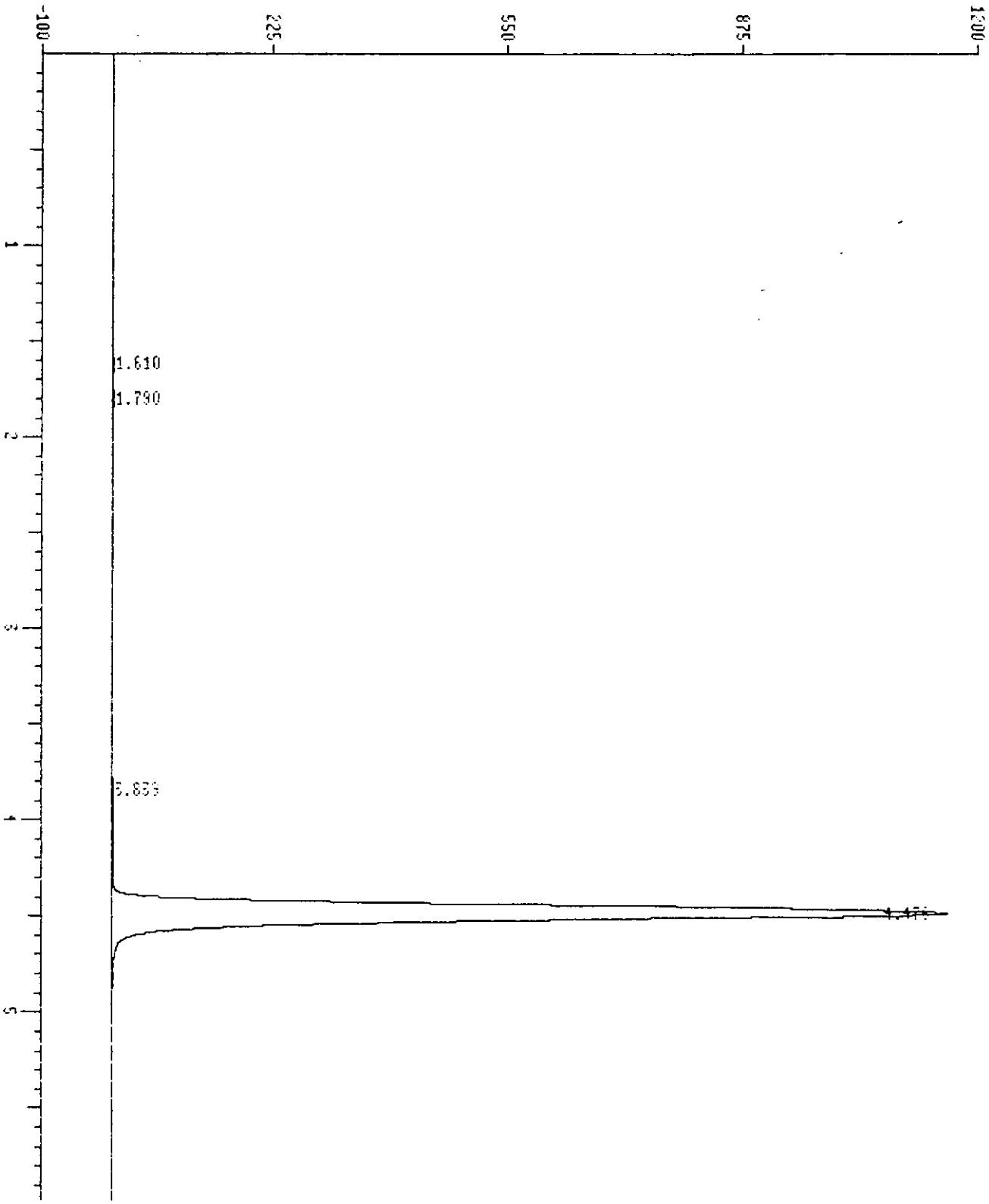
Report by Signal

Operator: JCP 2 Apr 92 11:05 am
Method File Name : DNPHIII.M
Sample Info : STANDRAD; 100 PPM
Misc Info:
Integration File Name : DATA:0401A72A.I
consisting of channels : 1. A 360,4 550,100 of 0401A72A.D
Sequence Index: 1 Bottle Number : 72 Repetition Number: 1

A 360,4 550,100 of 0401A72A.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.609	BV	9.8382	1.6560	0.15	100.00	0.085	0.46
1.789	VB	14.5814	1.7805	0.23	100.00	0.112	0.54
3.841	BV	26.8164	2.1492	0.42	100.00	0.166	0.31
4.477	VB	6349.14	1159.95	99.20	100.00	0.085	0.82

1: LC A 360,4 550,100 of 0401A72B.D



276

*** Area Percent ***

Report by Signal

Operator: JCP
Method File Name : DNPHIII.M 2 Apr 92 11:14 am
Sample Info : STANDRAD; 100 PPM
Misc Info:
Integration File Name : DATA:0401A72B.I
consisting of channels : 1. A 360,4 550,100 of 0401A72B.D
Sequence Index: 1 Bottle Number : 72 Repetition Number: 2

A 360,4 550,100 of 0401A72B.D

Ret Time	Type	Area	Height	Area %	Ratio %	Width	Sym
1.610	BV	9.6306	1.6458	0.15	100.00	0.084	0.46
1.790	VB	16.3017	1.8648	0.25	100.00	0.116	0.50
3.839	BV	27.9583	2.1685	0.44	100.00	0.174	0.30
4.476	VB	6348.11	1160.93	99.16	100.00	0.084	0.82

Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP Clayton Alabama Run number M5-Run 1

Sample Location Boiler Stack #1 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	BS1-M5-1-FH	✓
filter(s)	BS1-M5-1-PF	✓

Acetone rinse beaker #337 rinse volume ($V_a w$) 350 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (350) = 1.67×10^{-4} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 114.6649 g

Date/time/RH of wt 4/13/92 - 0930 - 34% RH Gross wt 114.6633 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 114.6643 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 114.6676 g

4/22/92 - 1300 - 44% RH Gross wt 114.6673 Average Gross wt 114.6675 g

Tare wt 114.6166 g

Less acetone blank wt (W_a) 1.67×10^{-4} g

Weight of particulate in acetone rinse (m_a) ~~44 wt~~ DKP 0.0507 g

Filter(s) container number F350

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 4.0600 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 4.0594 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 4.0592 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 4.0593 g

Tare wt 3.8452 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) 0.2140 g

Weight of particulate in acetone rinse(m_a) 0.0507 g

Total weight of particulate (m_n) ~~0.2647~~ 0.2647 DKP g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Alabama Run number M5-R2

Sample Location Boiler Stack #1 Run 2 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	BS1 - M5 - 2-FH	✓
filter(s)	BS1-M5-2-PF	✓

Acetone rinse beaker #352 rinse volume ($V_a w$) 350 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (350) = 1.67×10^{-4} g

Date/time/RH of wt 4/10/92 - 0845 - 35% A.H. Gross wt 105.2749 g

Date/time/RH of wt 4/11/92 - 0930 - 41% AH. Gross wt 105.2758 g

Date/time/RH of wt 4/13/92 - 1130 - 34% AH Gross wt 105.2735 g

Date/time/RH of wt 4/15/92 - 1330 - 30% AH Gross wt 105.2740 g

Average Gross wt 105.2738 g

Tare wt 105.1878 g

Less acetone blank wt (W_a) 1.67×10^{-4} g

Weight of particulate in acetone rinse (m_a) .0858 g

Filter(s) container number F351

Date/time/RH of wt 4/11/92 - 1100 - 43% AH Gross wt 4.0977 g

Date/time/RH of wt 4/13/92 - 0930 - 36% AH Gross wt 4.0970 g

Date/time/RH of wt 4/13/92 - 1530 - 30% AH Gross wt 4.0972 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 4.0971 g

Tare wt 3.8325 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.2646~~ 0.2645 g

Weight of particulate in acetone rinse(m_a) 0.0858 g

0.3503 DKP

Total weight of particulate (m_n) ~~0.3504~~ g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K. Pennock

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Alabama Run number M5 - R3

Sample Location Boiler stack #1 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	BS1 - M5 - 3 - FH	✓
filter(s)	BS1 - M5 - 3 - PF	✓

Acetone rinse beaker #357 rinse volume ($V_a w$) 235 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (235) = 1.12×10^{-4} g

Date/time/RH of wt 4/11/92 - 0930 — 41% RH Gross wt 107. 2393 g

Date/time/RH of wt 4/13/92 - 0930 - 34% RH Gross wt 107. 2376 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 107. 2379 g

Date/time/RH of wt 4/29/92 - 0830 31% Gross wt 107. 2320 g

4/29/92 1445 31% 107. 2323 Average Gross wt DKP ~~107. 2378~~ g 107. 2322

Tare wt 107. 1987 g

Less acetone blank wt (W_a) 1.12×10^{-4} g

Weight of particulate in acetone rinse (m_a) DKP ~~0.0390~~ g 0.0334

Filter(s) container number F355

Date/time/RH of wt 4/11 - 1100 - 43% Gross wt 4. 0225 g

Date/time/RH of wt 4/13 - 0930 - 36% RH Gross wt 4. 0218 g

Date/time/RH of wt 4/13 - 1600 HRS - 30% RH Gross wt 4. 0220 g

Date/time/RH of wt Gross wt g

Average Gross wt 4. 0219 g

Tare wt 3. 8264 g

Less filter blank wt (F_a) 0. 0001 g

Weight of particulate on filter(s) (m_f) ~~0.1955~~ 0.1954 g DKP

Weight of particulate in acetone rinse (m_a) DKP ~~0.0390~~ g 0.0334

Total weight of particulate (m_n) DKP ~~0.2345~~ g DKP ~~0.2289~~ 0.2288

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K. Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Alabama Run number M5-R1

Sample Location Boiler Stack #2 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	BS2-M5-1-FH	✓
filter(s)	BS2-M5-1-PF	✓

Acetone rinse beaker # 314 rinse volume ($V_a w$) 220 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(220) = 1.05 \times 10^{-4}$ g

Date/time/RH of wt 4/11/92 - 0830 - 41% RH. Gross wt 104.6474 g

Date/time/RH of wt 4/13/92 - 0830 - 34% RH Gross wt 104.6460 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 104.6473 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 104.6492 g

Gross wt 104.6491g 4/22/92 1300 44% RH Average Gross wt 104.6492 g

Tare wt 104.5935 g

Less acetone blank wt (W_a) 1.05×10^{-4} g

Weight of particulate in acetone rinse (m_a) 0.0556 g

Filter(s) container number F 352

Date/time/RH of wt 4/11 - 1130 - 43% Gross wt 3.9893 g

Date/time/RH of wt 4/13 - 0830 - 36% Gross wt 3.9888 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.9890 g

Tare wt 3.7863 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) DKP ~~0.2027~~ 0.2026 g

Weight of particulate in acetone rinse(m_a) 0.0556 g

Total weight of particulate (m_n) DKP 0.2582 ~~0.2583~~ g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Ronnie K Pennock

Signature of Reviewer: _____

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Alabama Run number MM5 -R2

Sample Location Boiler Stack # 2 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	BS2 - M5 - 2 - FH	✓
filter(s)	BS2 - M5 - 2 - PF	✓

Acetone rinse beaker 364 rinse volume ($V_a w$) 270 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (270) = 1.29×10^{-4} g

Date/time/RH of wt 4/11/92 - 0930 - 4% RH Gross wt 106.8661 g

Date/time/RH of wt 4/13/92 - 0930 - 34% RH Gross wt 106.8646 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.8650 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 106.8648 g

Tare wt 106.8307 g

Less acetone blank wt (W_a) 1.29×10^{-4} g

Weight of particulate in acetone rinse (m_a) .0339 g

Filter(s) container number F 353

Date/time/RH of wt 4/11 - 1130 - 43% RH Gross wt 4.0493 g

Date/time/RH of wt 4/13 - 0930 - 36% RH Gross wt 4.0489 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 4.0491 g

Tare wt 3.8285 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~.2206~~ .2205 g DKP

Weight of particulate in acetone rinse(m_a) .0339 g

Total weight of particulate (m_n) ~~.2545~~ .2544 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Denise K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala Run number M5 - R3

Sample Location Boiler stack # 2 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	BS2 - M5 - 3 - FH	✓
filter(s)	BS2 - M5 - 3 - PF	✓

Acetone rinse beaker 344 rinse volume ($V_a w$) 350 ml ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(350) = 1.67 \times 10^{-4}$ g

Date/time/RH of wt 4/11/92 - 0930 - 41%RH Gross wt 106.2970 g

Date/time/RH of wt 4/13/92 - 0930 - 34%RH Gross wt 106.2956 g

Date/time/RH of wt 4/15/92 - 1330 - 30%RH Gross wt 106.2960 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 106.2958 g

Tare wt 106.2534 g

Less acetone blank wt (W_a) 1.67×10^{-4} g

Weight of particulate in acetone rinse (m_a) 0.0422 g

Filter(s) container number F 354

Date/time/RH of wt 4/11/92 - 1130 - 43%RH Gross wt 4.0610 g

Date/time/RH of wt 4/13/92 - 0930 - 36%RH Gross wt 4.0604 g

Date/time/RH of wt 4/13/92 - 1600 - 30%RH Gross wt 4.0605 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 4.0605 g

Tare wt 3.7970 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.2635~~ .2634 g

Weight of particulate in acetone rinse(m_a) 0.0422 g DKP

Total weight of particulate (m_n) ~~0.3057~~ .3056 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K. Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Former R1

Sample Location Former Exhaust

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	FE1-M5-1-FH	✓
filter(s)	FE1-M5-1-PF	✓

Acetone rinse beaker 345 rinse volume ($V_a w$) 235 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (235) = 1.12×10^{-4} g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 108.0482 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 108.0356 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 108.0571 g

Date/time/RH of wt 4/22/92 - 1300 - 44% RH Gross wt 108.0652 g

Gross wt 108.0388 4/23/92 0820 - 39% RH Average Gross wt 108.0490 g

Tare wt 106.4598 g

Less acetone blank wt (W_a) ~~1.5892~~ DKP g 1.12×10^{-4}

Weight of particulate in acetone rinse (m_a) 1.5891 g

Filter(s) container number F 337

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 5.4923 * g Not in Avg

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 5.4773 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 5.4781 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 5.4716 g

Gross wt 5.4651 g 4/21/92 - 1115 - 43% RH Average Gross wt 5.4730 g

Tare wt 3.8092 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~1.6640~~ 1.6639 g

Weight of particulate in acetone rinse(m_a) 1.5891 g DKP

Total weight of particulate (m_n) ~~3.2531~~ 3.2530 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks - Lt orange color to rinse - Solid matter present

Signature of analyst: Donna K Parish

Signature of Reviewer:

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton ala Run number Former R2

Sample Location Former Exhaust Run 2

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	Fe1 – M5 – 2 – FH	✓
filter(s)	Fe1 – M5 – 2 – PF	✓

Acetone rinse beaker 356 rinse volume ($V_a w$) 240 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (240) = 1.14×10^{-4} g

Date/time/RH of wt 4/15/92 – 1330 – 30% RH Gross wt 109.7714 g

Date/time/RH of wt 4/21/92 – 1115 – 43% RH Gross wt 109.7921 g

Date/time/RH of wt 4/22/92 – 1300 – 44% RH Gross wt 109.7711 g

Date/time/RH of wt 4/23/92 – 0820 – 39% RH Gross wt 109.7751 g

4/24/92 – 0830 – 36% RH Gross wt 109.7722 Average Gross wt 109.7764 g

Tare wt 108.3682 g

Less acetone blank wt (W_a) DKP ~~1.4082~~ g 1.14×10^{-4}

Weight of particulate in acetone rinse (m_a) 1.4081 g

Filter(s) container number F338

Date/time/RH of wt 4/11 – 1130 – 43% RH Gross wt 4.9816 * Not used in Avg g

Date/time/RH of wt 4/13 – 0930 – 36% RH Gross wt 4.9698 g

Date/time/RH of wt 4/13 – 1600 – 30% RH Gross wt 4.9712 g

Date/time/RH of wt 4/15 – 1330 – 30% RH Gross wt 4.9660 g

Gross wt 4.9645g 4/21 – 1115 – 43% RH Average Gross wt 4.9679 g

Tare wt 3.7752 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~1.1927~~ 1.1926 g

Weight of particulate in acetone rinse(m_a) 1.4081 g DKP

Total weight of particulate (m_n) ~~2.6008~~ 2.6007 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks Lt Orange Color w/ Solid matter present in Rinse

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Former R3

Sample Location Former Exhaust Run 3 3/12/91

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	Fe1-M5-3-FH	✓
filter(s)	Fe1-M5-3-PF	✓

Acetone rinse beaker #370 rinse volume ($V_a w$) 300 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(300) = 1.43 \times 10^{-4}$ g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 109.6851 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 109.6853 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 109.6852 g

Tare wt 108.1652 g

Less acetone blank wt (W_a) 1.43×10^{-4} g

Weight of particulate in acetone rinse (m_a) ~~1.520~~ DKP 1.5200 g

Filter(s) container number F339

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 5.1537 g * out of avg

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 5.1441 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 5.1453 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 5.1405 g

Gross wt 5.1381g 4/21/92 - 1115 - 43% RH Average Gross wt 5.1420 g

Tare wt ~~F339~~ 3.8096 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~1.3324~~ 1.3323 g

Weight of particulate in acetone rinse(m_a) 1.5200 g DKP

Total weight of particulate (m_n) ~~2.8524~~ 2.8523 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parnell

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Alabama Run number PV 7-M5-R1

Sample Location Press Vent #7 3/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	Press Vent #7 PV7-M5-1-FH	✓
filter(s)	PV7-M5-1-PF	✓

Acetone rinse beaker #373 rinse volume ($V_a w$) 90 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(90) = 4.28 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 105.7512 g

Date/time/RH of wt 4/11/92 - 1130 - 34% RH Gross wt 105.7508 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 105.7513 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 105.7510 g

Tare wt 105.7473 g

Less acetone blank wt (W_a) 4.28×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0037 g

Filter(s) container number F374

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7715 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7717 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7716 g

Tare wt 3.7703 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0013~~ .0012 g

Weight of particulate in acetone rinse(m_a) 0.0037 g DKP

Total weight of particulate (m_n) ~~0.0050~~ .0049 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number PV7-M5-#2

Sample Location Press Vent #7 3/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV7-M5-2-FH	✓
filter(s)	PV7-M5-2-PF	✓

Acetone rinse beaker 353 rinse volume ($V_a w$) 110 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (110) = 5.24×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH Gross wt 106.8206 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 106.8212 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 106.8192 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.8204 g

Gross wt 106.8223 g 4/21/92 11.15 43% RH Average Gross wt 106.8207 g

Tare wt 106.8132 g

Less acetone blank wt (W_a) 5.24×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0074 g

Filter(s) container number F377

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8047 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8047 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8047 g

Tare wt 3.8034 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0013~~ .0012 g

Weight of particulate in acetone rinse(m_a) 0.0074 g DKP

Total weight of particulate (m_n) ~~0.0087~~ .0086 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 3 PV7

Sample Location Press Vent #7

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV7- M5- 3 - FH	✓
filter(s)	PV7- M5- 3 - PF	✓

Acetone rinse beaker 340 rinse volume ($V_a w$) 120 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (120) = 5.71×10^{-5} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH. Gross wt 115.2999 g

Date/time/RH of wt 4/13/92 - 1130 - ~~[illegible]~~ 34% RH Gross wt 115.2983 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 115.2983 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 115.2983 g

Tare wt 115.2925 g

Less acetone blank wt (W_a) 5.71×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0057 g

Filter(s) container number F379

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8019 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8018 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8019 g

Tare wt 3.7987 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0032~~ .0031 g

Weight of particulate in acetone rinse(m_a) 0.0057 g DKP

Total weight of particulate (m_n) ~~0.0089~~ .0088 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala Run number Run 1 PV8

Sample Location Press Vent #8 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV8 - M5 - 1 - FH	✓
filter(s)	PV8 - M5 - 1 - PF	✓

Acetone rinse beaker 331 rinse volume ($V_a w$) 100 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (100) = 4.76×10^{-5} g

Date/time/RH of wt 4/13/92 - 1130HRS - 34% RH Gross wt 105.7804 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 105.7803 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 105.7804 g

Tare wt 105.7773 g

Less acetone blank wt (W_a) 4.76×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0031 g

Filter(s) container number F 366

Date/time/RH of wt 4/13/92 - 1130 - 43% RH Gross wt 3.8114 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8112 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8113 g

Tare wt 3.8098 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0015~~ .0014 g DKP

Weight of particulate in acetone rinse(m_a) 0.0031 g

Total weight of particulate (m_n) ~~0.00446~~ .0045 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP — Clayton Ala Run number Run 2 PV8

Sample Location Press Vent #8 3/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV8-M5-2-FH	✓
filter(s)	PV8-M5-2-PF	✓

Acetone rinse beaker #363 rinse volume ($V_a w$) 110 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (110) = 5.24×10^{-5} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 105.7878 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 105.7875 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 105.7875 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 105.7875 g

Tare wt 105.7820 g

Less acetone blank wt (W_a) 5.24×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0054 g

Filter(s) container number F367

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7972 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7969 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7971 g

Tare wt 3.7968 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0003~~ .0002 g

Weight of particulate in acetone rinse(m_a) 0.0054 g DICP

Total weight of particulate (m_n) ~~0.0057~~ .0056 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Nimra K Parish

Signature of Reviewer: _____

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number PV8 R-3

Sample Location Press Vent #8 3/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV8-M5-3-FH	✓
filter(s)	PV8-M5-3-PF	✓

Acetone rinse beaker #320 rinse volume ($V_a w$) 80 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (80) = 3.81×10^{-5} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 105.7041 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 105.7031 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 105.7032 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 105.7032 g

Tare wt 105.6965 g

Less acetone blank wt (W_a) 3.81×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0067 g

Filter(s) container number F 371

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8116 g

Date/time/RH of wt 4/13/92 - 0930 - 36 RH Gross wt 3.8116 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8116 g

Tare wt 3.8104 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0012~~ .0011 g

Weight of particulate in acetone rinse(m_a) 0.0067 g DKP

Total weight of particulate (m_n) ~~0.0079~~ .0078 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parnell

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton ala Run number R1- PV9

Sample Location Press Vent #9

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV9- M5-1-FH	✓
filter(s)	PV9- M5-1-PF	✓

Acetone rinse beaker #346 rinse volume ($V_a w$) 150 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (150) = 7.14×10^{-5} g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 112.0462 g

Date/time/RH of wt 4/13/92 - 1130 34% RH Gross wt 112.0452 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 112.0451 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 112.0452 g

Tare wt 112.0442 g

Less acetone blank wt (W_a) 7.14×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0009 g

Filter(s) container number F357

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8105 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8104 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8105 g

Tare wt 3.8091 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0014~~ .0013 g

Weight of particulate in acetone rinse(m_a) 0.0009 g PRP

Total weight of particulate (m_n) ~~0.0023~~ .0022 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 2 PV9

Sample Location Press Vent #9 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV9-M5-2-FH	✓
filter(s)	PV9-M5-2-PF	✓

Acetone rinse beaker #333 rinse volume ($V_a w$) 200 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(200) = 9.52 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 105.7043 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 105.7029 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 105.7031 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 105.7030 g

Tare wt 105.7000 g

Less acetone blank wt (W_a) 9.52×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0029 g

Filter(s) container number F 359

Date/time/RH of wt 4/11/92 - 1130 HRS - 43% RH Gross wt 3.8342 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8343 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8343 g

Tare wt 3.8331 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0012~~ .0011 g

Weight of particulate in acetone rinse(m_a) 0.0029 g DKP

Total weight of particulate (m_n) ~~0.0041~~ .0040 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parnell

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number PV9 - R3

Sample Location Press Vent #9 Run 3 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV9 - M5 - 3 - FH	✓
filter(s)	PV9 - M5 - 3 - PF	✓

Acetone rinse beaker 336 rinse volume ($V_a w$) 155 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (155) = 7.4×10^{-5} g

Date/time/RH of wt 4/11/92 - 1130 - 43% Gross wt 111.4263 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 111.4256 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 111.4261 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 111.4258 g

Tare wt 111.4228 g

Less acetone blank wt (W_a) 7.4×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0029 g

Filter(s) container number F361

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7908 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7906 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7907 g

Tare wt 3.7896 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) 0.0010 g

Weight of particulate in acetone rinse(m_a) 0.0029 g

Total weight of particulate (m_n) ~~0.0040~~ .0039 DKP g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala Run number Run 1

Sample Location Press Vent #10

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV10 - M5-1-FH	✓
filter(s)	PV10 - M5-1-PF	✓

Acetone rinse beaker 342 rinse volume ($V_a w$) 100 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (100) = 4.76×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH Gross wt 106.4510 g

Date/time/RH of wt 4/11/92 - 0930 - 40% RH Gross wt 106.4518 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 106.4498 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.4507 g

Gross wt 106.4523g 4/21/92 - 1115 - 43% RH Average Gross wt 106.4511 g

Tare wt 106.4490 g

Less acetone blank wt (W_a) 4.76×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0021 g

Filter(s) container number F 363

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7923 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7921 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7922 g

Tare wt 3.7899 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0023~~ .0022 g

Weight of particulate in acetone rinse(m_a) 0.0021 g DKP

Total weight of particulate (m_n) ~~0.0044~~ .0043 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 2

Sample Location Press Vent #10 3/18/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV10 - m5 - 2 - FH	✓
filter(s)	PV10 - M5 - 2 - PF	✓

Acetone rinse beaker #301 rinse volume ($V_a w$) 95 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (95) = 4.52×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH. Gross wt 111.9367 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 111.9373 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 111.9350 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 111.9365 g

Gross wt 111.9378 g 4/21/92 - 1115 - 43% RH Average Gross wt 111.9367 g

Tare wt 111.9309 g

Less acetone blank wt (W_a) 4.52×10^{-5} g

Weight of particulate in acetone rinse (m_a) ~~8~~ 0.0058 g DKP

Filter(s) container number F 368

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7822 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7820 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7821 (DKP) g

Tare wt 3.7780 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0041~~ .0040 g

Weight of particulate in acetone rinse(m_a) 0.0058 g DKP

Total weight of particulate (m_n) ~~0.0099~~ .0098 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 3

Sample Location Press Vent 10 3/18/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV 10 - M5 - 3-FH	✓
filter(s)	PV10 - M5 - 3-PF	✓

Acetone rinse beaker 341 rinse volume ($V_a w$) 120 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (120) = 5.71×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 HAS - 35% RH Gross wt 106.3591 g

Date/time/RH of wt 4/11/92 - 0930 HAS - 41% RH Gross wt 106.3599 g

Date/time/RH of wt 4/13/92 - 1130 HAS - 34% RH Gross wt 106.3582 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.3591 g

Gross wt 106.3606 4/21/92 - 1115 - 43% RH Average Gross wt 106.3594 g

Tare wt 106.3543 g

Less acetone blank wt (W_a) 5.71×10^{-5} g

Weight of particulate in acetone rinse (m_a) 5.04×10^{-3} g
0.0050

Filter(s) container number F 370

Date/time/RH of wt 4/11/92 - 1130 HAS - 43% RH Gross wt 3.7917 g

Date/time/RH of wt 4/13/92 - 0930 HAS - 36% RH Gross wt 3.7917 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7917 g

Tare wt 3.7896 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0021~~ .0020 g

Weight of particulate in acetone rinse(m_a) 0.0050 g

DKP

Total weight of particulate (m_n) ~~0.0071~~ .0070 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton ala. Run number Run 1

Sample Location Dryer Stak #1 3/13/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	051- M5-1-FH	✓
filter(s)	051- M5-1-PF	✓

Acetone rinse beaker 351 rinse volume ($V_a w$) 195 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(195) = 9.28 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 110. 8962 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH. Gross wt 110. 8939 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 110. 8949 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 110. 8970 g

Gross wt 110.8951 4/23/92 0820 39% RH Average Gross wt 110. 8954 g

Tare wt 110. 8452 g

Less acetone blank wt (W_a) 9.28×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0501 g

Filter(s) container number F340

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3. 8860 g

Date/time/RH of wt 4/13/92 - 0930 - 34% RH Gross wt 3. 8841 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3. 8856 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3. 8835 g

Gross wt 3.8857g 4/21/92 - 1115 - 43% RH Average Gross wt 3. 8850 g

Tare wt 3. 7651 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.1179~~ .1198

Weight of particulate in acetone rinse(m_a) 0.0501 g

DKP

Total weight of particulate (m_n) ~~0.1700~~ .1699 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 2 DS1

Sample Location Dryer Stack #1 3/13/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS1-M5-2-FH	✓
filter(s)	DS1-M5-2-PF	✓

Acetone rinse beaker #360 rinse volume ($V_a w$) 170 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (170) = 8.09×10^{-5} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 108.6814 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 108.6792 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 108.6792 g

Date/time/RH of wt Gross wt g

Average Gross wt 108.6792 g

Tare wt 108.6177 g

Less acetone blank wt (W_a) 8.09×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0614 g

Filter(s) container number F 342

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.9339 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.9310 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.9325 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.9304 g

Gross wt 3.9327g 4/21/92 - 1115 - 43% RH Average Gross wt 3.9321 g

Tare wt 3.7656 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.1665~~ .1664 g DKP

Weight of particulate in acetone rinse(m_a) 0.0614 g

Total weight of particulate (m_n) ~~0.2279~~ .2278 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Nanne K Parrish

Signature of Reviewer:

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant L.P. - Clayton Ala. Run number Run 3 051

Sample Location Dryer Stack #1 3/13/92 Run 3

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	051-M5-3-FH	✓
filter(s)	051-M5-3-PF	✓

Acetone rinse beaker #361 rinse volume ($V_a w$) 205 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(205) = 9.76 \times 10^{-5}$ g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH. Gross wt 102.6348 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 102.6346 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 102.6347 g

Tare wt 102.5506 g

Less acetone blank wt (W_a) 9.76×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0240 g

Filter(s) container number F341

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.9661 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.9632 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.9646 g

Date/time/RH of wt 4/15/92 - 1300 - 30% RH Gross wt 3.9626 g

Gross wt 3.9649 g 4/21/92 - 1115 - 43% RH Average Gross wt 3.9643 g

Tare wt 3.7986 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.1657~~ .1656 g

Weight of particulate in acetone rinse(m_a) 0.0240 g DKP

Total weight of particulate (m_n) ~~0.2497~~ .2496 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala. Run number Run 1 DS2

Sample Location Dryer Stack #2 Run 1 3/14/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS2 - M5 - 1 - FH	✓
filter(s)	DS2 - M5 - 1 - PF	✓

Acetone rinse beaker #366 rinse volume ($V_a w$) 175 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (175) = 8.33×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 HRS - 36% RH Gross wt 111. 2389 g

Date/time/RH of wt 4/11/92 - 0930 - 43% RH Gross wt 111. 2408 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 111. 2378 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 111. 2383 g

Average Gross wt 111. 2381 g

Tare wt 111. 1727 g

Less acetone blank wt (W_a) 8.33×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0653 g

Filter(s) container number F343

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.9775 * g * Not used in avg.

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.9758 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.9768 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.9756 g

Gross wt 3.9764 g 4/21/92 - 1115 - 43% RH Average Gross wt 3.9762 g

Tare wt 3.8334 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.1428~~ .1427 g

Weight of particulate in acetone rinse(m_a) 0.0653 g

DKP

Total weight of particulate (m_n) ~~0.2081~~ .2080 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Dianne K Parrish

Signature of Reviewer:

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Control No.

METHOD 5
SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 2 DS2

Sample Location Dryer Stack # 2 Run 2

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS2 - M5-2-FH	✓
filter(s)	DS2 - M5- 2 - PF	✓

Acetone rinse beaker #316 rinse volume ($V_a w$) 180 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (180) = 8.57×10^{-5} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 107.6501 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 107.6475 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 107.6474 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 107.6475 g

Tare wt 107.5522 g

Less acetone blank wt (W_a) 8.57×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0954 ~~42~~ DKP g

Filter(s) container number F 344

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.9855 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.9822 g

Date/time/RH of wt 4/13/92 - 1600 HRS - 30% RH Gross wt 3.9842 g

Date/time/RH of wt 4/15/92 - 1330 HRS - 30% RH Gross wt 3.9810 g

Gross wt 3.9846g 4/21/92 - 1115 - 43% RH Average Gross wt 3.9835 g

Tare wt 3.7750 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.2085~~ .2884 DKP

Weight of particulate in acetone rinse(m_a) 0.0952 g

Total weight of particulate (m_n) ~~0.3037~~ .3036 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton ala Run number Run 3 4S2

Sample Location Dryer Stack #2 Run 3

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	0S2-M5-3-FH	✓
filter(s)	0S2-M5-3-PF	✓

Acetone rinse beaker #355 rinse volume ($V_a w$) 205 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (205) = 9.76×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 HRS - 35% RH Gross wt 108.4755 g

Date/time/RH of wt 4/11/92 - 0930 HRS - 48% RH Gross wt 108.4768 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% RH Gross wt 108.4731 g

Date/time/RH of wt 4/15/92 - 1330 HRS - 30% RH Gross wt 108.4741 g

Gross wt 108.4768 4/21/92 - 1115 - 43% RH Average Gross wt 108.4753 g

Tare wt 108.4027 g

Less acetone blank wt (W_a) 9.76×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0725 g

Filter(s) container number F345

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.9625 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.9608 ✓ g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.9612 ✓ g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.9603 g

Average Gross wt 3.9610 g

Tare wt 3.8222 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.1388~~ .1387 g

Weight of particulate in acetone rinse(m_a) 0.0725 g

DKP

Total weight of particulate (m_n) ~~0.2113~~ .2112 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number DS3 Run 1

Sample Location Dryer Stack #3 3/14/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS 3 - M5 - 1 - FH	✓
filter(s)	DS 3 - M5 - 1 - PF	✓

Acetone rinse beaker #304 rinse volume ($V_a w$) 200 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(200) = 9.52 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 109.0485 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 109.0459 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 109.0472 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 109.0494 g

4/23/92 - 0820 - 39% RH Gross wt 109.0469 Average Gross wt 109.0476 g

Tare wt 108.9738 g

Less acetone blank wt (W_a) 9.52×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0737 g

Filter(s) container number F346

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.9767 g * Not used in avg wt

Date/time/RH of wt 4/13/92 - 0830 - 36% RH Gross wt 3.9740 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.9750 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.9733 g

Gross wt 3.9748g 4/21/92 - 1115 - 43% RH Average Gross wt 3.9743 g

Tare wt 3.7780 g

Less filter blank wt (F_a) 0.001 g

Weight of particulate on filter(s) (m_f) ~~0.1963~~ .1962 g

Weight of particulate in acetone rinse(m_a) 0.0737 g DKP

Total weight of particulate (m_n) ~~0.2700~~ .2699 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant CP- Clayton Run number Run 2 DS3

Sample Location Dryer Stack # 3 3/18/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS3- M5-2-FH	✓
filter(s)	DS3-M5-2-PF	✓

Acetone rinse beaker #375 rinse volume ($V_a w$) 200 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (200) = 9.52×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 HRS - 35% RH Gross wt 110.3351 g

Date/time/RH of wt 4/11/92 - 0930 HRS - 43% RH Gross wt 110.3361 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% RH Gross wt 110.3330 g

Date/time/RH of wt 4/15/92 - 1330 HRS - 30% RH Gross wt 110.3337 g

Gross wt 110.3355g 4/21/92 - ~~1115~~ 1115 DKP - 43% RH Average Gross wt 110.3347 g

Tare wt 110.2608 g

Less acetone blank wt (W_a) 9.52×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.7380 g

Filter(s) container number F 347

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 4.0280 g * Not used in Avg.

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 4.0201 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 4.0215 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 4.0195 g

Gross wt 4.0216g 4/21/92 - 1115 - 43% RH Average Gross wt 4.0207 g

Tare wt 3.8351 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.1844~~ .1843 g

Weight of particulate in acetone rinse(m_a) 0.7380 g DKP

Total weight of particulate (m_n) ~~0.9224~~ .9223 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parish

Signature of Reviewer:

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 1 DS'4

Sample Location Dryer Stack # 4 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS4- M5- 1-FH	✓
filter(s)	DS4- M5- 1- PF	✓

Acetone rinse beaker #365 rinse volume ($V_a w$) 235 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (235) = 1.12×10^{-4} g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 105.2940 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 105.2912 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 105.2920 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 105.2945 g

Gross wt 105.2918g 4/23/92 0820 39% RH Average Gross wt 105.2927 g

Tare wt 105.1962 g

Less acetone blank wt (W_a) 1.12×10^{-4} g

Weight of particulate in acetone rinse (m_a) 0.0964 g

Filter(s) container number F 348

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 4.0005 g * Not used in Avg

Date/time/RH of wt 4/13/92 - 0830 - 36% RH Gross wt 3.9969 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.9981 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.9965 g

Gross wt 3.9988g 4/21/92 - 1115 - 43% RH Average Gross wt 3.9976 g

Tare wt 3.7786 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.2190~~ g 2189

Weight of particulate in acetone rinse(m_a) 0.0964 g DKP

Total weight of particulate (m_n) ~~0.3154~~ .3153 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant Dryer Stack #4 LP-Clayton Run number Run 2 DS4

Sample Location DS 4 — 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS4-M5-2-FH	✓
filter(s)	DS4-M5-2-PF	✓

Acetone rinse beaker #350 rinse volume ($V_a w$) 225 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(225) = 1.07 \times 10^{-4}$ g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH Gross wt 110.8823 g

Date/time/RH of wt 4/11/92 - 0930 - 38% RH Gross wt 110.8836 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 110.8803 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 110.8808 g

Average Gross wt 110.8806 g

Tare wt 110.7987 g

Less acetone blank wt (W_a) 1.07×10^{-4} g

Weight of particulate in acetone rinse (m_a) 0.0818 g

Filter(s) container number F 349

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.9995 g

Date/time/RH of wt 4/13/92 - 0930 - 34% RH Gross wt 3.9962 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.9976 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.9957 g

Gross wt 3.9923 g 4/21/92 - 1115 - 43% RH Average Gross wt 3.9975 g

Tare wt 3.7814 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.2161~~ .2160 g DKP

Weight of particulate in acetone rinse(m_a) 0.0818 g

Total weight of particulate (m_n) ~~0.2979~~ .2978 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 1 DS6

Sample Location Dryer Stack #6 M5-

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	086 - M5 - 1 - PH	✓
filter(s)	086 - M5 - 1 - PF	✓

Acetone rinse beaker # 359 rinse volume ($V_a w$) 200 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (200) = 9.52×10^{-5} g

Date/time/RH of wt 4/11/92 - 1130 - 43% AH. Gross wt 109. 3666 g

Date/time/RH of wt 4/13/92 - 1130 - 34% AH Gross wt 109. 3603 g

Date/time/RH of wt 4/13/92 - 1330 - 30% AH Gross wt 109. 3612 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 109. 3645 g

Gross wt 109.3604 4/23/92 - 0820 - 39% RH Average Gross wt 109. 3626 g

Tare wt 109. 1058 g

Less acetone blank wt (W_a) 9.52×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.2567 g

Filter(s) container number F 334

Date/time/RH of wt 4/11/92 - 1130 HRS - 43% AH. Gross wt 3. 8619 g

Date/time/RH of wt 4/13/92 - 0930 - 36% AH Gross wt 3. 8598 g

Date/time/RH of wt 4/13/92 - 1600 - 30% AH Gross wt 3. 8602 g

Date/time/RH of wt 4/15/92 - 1330 - 30% AH Gross wt 3. 8600 g

Average Gross wt 3. 8601 g

Tare wt 3. 7806 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0795~~ .0794 g

Weight of particulate in acetone rinse(m_a) 0.2567 g DKP

Total weight of particulate (m_n) ~~0.3362~~ .3361 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Pembl

Signature of Reviewer:

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number R2 056

Sample Location Dryer Stack #6 Run 2

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	056 - M5 - 2 - FH	✓
filter(s)	056 - M5 - 2 - PF	✓

Acetone rinse beaker #358 rinse volume ($V_a w$) 220 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (220) = 1.05×10^{-4} g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 110.1644 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 110.1608 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 110.1589 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 110.1658 g

Gross wt 110.1667g 4/22/92 - 1300 - 44% RH Average Gross wt 110.1633 g

Tare wt 109.9081 g

Less acetone blank wt (W_a) 1.05×10^{-4} g

Weight of particulate in acetone rinse (m_a) 0.2551 g

Filter(s) container number F 335

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8780 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8764 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.8773 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.8763 g

Gross wt 3.8774g 4/21/92 - 1115 - 43% RH Average Gross wt 3.8771 g

Tare wt 3.8065 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0706~~ .0705 g

Weight of particulate in acetone rinse(m_a) 0.2551 g DKP

Total weight of particulate (m_n) ~~0.3257~~ .3256 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala. Run number OS6 - R3

Sample Location Dryer Stack #6 M5 - Run 3 3/12/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	OS6 - M5 - 3 - FH	✓
filter(s)	OS6 - M5 - 3 - PF	✓

Acetone rinse beaker #372 rinse volume ($V_a w$) 220 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(220) = 1.05 \times 10^{-4}$ g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 109.6064 g

Date/time/RH of wt 4/13/92 - 1130 — 34% RH Gross wt 109.6023 g

Date/time/RH of wt 4/15/92 - 1330 — 30% RH Gross wt 109.6002 g

Date/time/RH of wt 4/21/92 - 1115 — 43% RH Gross wt 109.6071 g

Gross wt 109.6014 g 4/22/92 - 1300 - 44% RH Average Gross wt 109.6035 g

Tare wt 109.3860 g

Less acetone blank wt (W_a) 1.05×10^{-4} g

Weight of particulate in acetone rinse (m_a) 0.2174 g

Filter(s) container number F 336

Date/time/RH of wt 4/11/92 - 1130 - 43% RH. Gross wt 3.8294 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8283 g

Date/time/RH of wt 4/13/92 - 1600 — 30% RH Gross wt 3.8289 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.8281 g

Gross wt 3.8287 g 4/21/92 - 1115 - 43% RH Average Gross wt 3.8287 g

Tare wt 3.7716 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0571~~ g .0570

Weight of particulate in acetone rinse(m_a) 0.2174 g DKP

Total weight of particulate (m_n) ~~0.2745~~ g .2744

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Anne K Parish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala Run number Run 1 DS8

Sample Location Dryer Stack #8 Run 1 3/10/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS8-M5-1-FH	✓
filter(s)	DS8-M5-1-PF	✓

Acetone rinse beaker #369 rinse volume ($V_a w$) ~~369~~ 225 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(225) = 1.07 \times 10^{-4}$ g

Date/time/RH of wt 4/11/92 - 0930 HAS - 41% RH Gross wt 112.3032 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 112.3014 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 112.3022 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 112.3045 g

Gross wt 112.3024 4/23/92 0820 39% RH Average Gross wt 112.3027 g

Tare wt 112.2196 g

Less acetone blank wt (W_a) 1.07×10^{-4} g

Weight of particulate in acetone rinse (m_a) 0.0830 g

Filter(s) container number F 331

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8279 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8269 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.8273 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.8267 g

Gross wt 3.8275g 4/21/92 - 1115 - 43% RH Average Gross wt 3.8273 g

Tare wt 3.8021 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0252~~ .0251 g

Weight of particulate in acetone rinse(m_a) 0.0830 g DKP

Total weight of particulate (m_n) ~~0.1082~~ .1081 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Run 2 DS 8

Sample Location Dryer Stack #8 Run 2 3/10/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS8 – M5-2-FH	✓
filter(s)	DS8- M5-3-PF	✓

Acetone rinse beaker # 334 rinse volume ($V_a w$) 170 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (170) = 8.09×10^{-5} g

Date/time/RH of wt 4/11/92 – 0930 – 41% RH Gross wt 107.5615 g

Date/time/RH of wt 4/13/92 – 1130 – 31% RH Gross wt 107.5600 g

Date/time/RH of wt 4/15/92 – 1330 – 30% RH Gross wt 107.5600 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 107.5600 g

Tare wt 107.5144 g

Less acetone blank wt (W_a) 8.09×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0455 g

Filter(s) container number F 332

Date/time/RH of wt 4/11/92 – 1130 – 43% RH Gross wt 3.8404 * Not used in Avg

Date/time/RH of wt 4/13/92 – 0930 – 34% RH Gross wt 3.8388 g

Date/time/RH of wt 4/13/92 – 1600 – 30% RH Gross wt 3.8398 g

Date/time/RH of wt 4/15/92 – 1300 – 30% RH Gross wt 3.8389 g

Gross wt 3.8399 g 4/21/92 - 1115 - 43% RH Average Gross wt 3.8394 g

Tare wt 3.7909 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0485~~ .0484 g

Weight of particulate in acetone rinse(m_a) 0.0455 g DKP

Total weight of particulate (m_n) ~~0.0940~~ .0939 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 3 058

Sample Location Dryer Stack #8 Run 3 3/11/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	058 - M5 - 3 - FH	✓
filter(s)	058 - M5 - 3 - PF	✓

Acetone rinse beaker #349 rinse volume ($V_a w$) 175 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (175) = 8.33×10^{-5} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 107.7076 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 107.7055 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 107.7056 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 107.7056 g

Tare wt 107.6355 g

Less acetone blank wt (W_a) 8.33×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0700 g

Filter(s) container number F333

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8459 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8448 g

Date/time/RH of wt 4/13/92 - 1600 - 30% RH Gross wt 3.8455 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 3.8447 g

Gross wt 3.8451g 4/21/92 - 1115 - 43% RH Average Gross wt 3.8452 g

Tare wt 3.8144 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0308~~ g .0307

Weight of particulate in acetone rinse(m_a) 0.0700 g DKP

Total weight of particulate (m_n) ~~0.1008~~ g .1007

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Run 1 PV3

Sample Location Press Vent #3 Run 1 3/18/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV 3-M5-1-FH	✓
filter(s)	PV3-M5-1-PF	✓

Acetone rinse beaker #310 rinse volume ($V_a w$) 125 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(125) = 5.95 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 0930 - 41% AM Gross wt 104.8138 g

Date/time/RH of wt 4/13/92 - 1130 - 34% AM Gross wt 104.8127 g

Date/time/RH of wt 4/15/92 - 1330 - 30% AM Gross wt 104.8130 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 104.8129 g

Tare wt 104.8107 g

Less acetone blank wt (W_a) 5.95×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0021 g

Filter(s) container number F362

Date/time/RH of wt 4/11/92 - 1130 - 43% AM Gross wt 3.8072 g

Date/time/RH of wt 4/13/92 - 0930 - 36% AM Gross wt 3.8071 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8072 g

Tare wt 3.8073 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0001~~ .0002 g

Weight of particulate in acetone rinse(m_a) 0.0021 g

DKP

.0019

Total weight of particulate (m_n) ~~0.0020~~ g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 2 PV 3

Sample Location Preservent # 3 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV 3 - M5 - 2 - FH	✓
filter(s)	PV3 - M5 - 2 - PF	✓

Acetone rinse beaker #376 rinse volume ($V_a w$) 125 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(125) = 5.95 \times 10^{-5}$ g

Date/time/RH of wt 4/13/92 - 1130 - 34% AH Gross wt 104.9137 g

Date/time/RH of wt 4/15/92 - 1330 - 30% AH Gross wt 104.9141 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 104.9139 g

Tare wt 104.9094 g

Less acetone blank wt (W_a) 5.95×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0044 g

Filter(s) container number F364

Date/time/RH of wt 4/11/92 - 1130 - 43% AH Gross wt 3.7996 g

Date/time/RH of wt 4/13/92 - 0930 - 36% AH Gross wt 3.7997 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7997 g

Tare wt 3.7978 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0019~~ .0018 g

Weight of particulate in acetone rinse(m_a) 0.0044 g

DKP

Total weight of particulate (m_n) ~~0.0063~~ .0062 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 3 PU 3

Sample Location Press Vent #3 Run 3 3/18/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PU3 - M5 - 3 - FH	✓
filter(s)	PU3 - M5 - 3 - PF	✓

Acetone rinse beaker # 391 rinse volume ($V_a w$) 120 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(120) = 5.71 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 0930 - 46% RH Gross wt 112.4342 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 112.4332 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 112.4337 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 112.4335 g

Tare wt 112.4275 g

Less acetone blank wt (W_a) 5.71×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0059 g

Filter(s) container number F 369

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8056 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8055 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8056 g

Tare wt 3.8041 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0015~~ .0014 DKP g

Weight of particulate in acetone rinse(m_a) 0.0059 g

Total weight of particulate (m_n) ~~0.0074~~ .0073 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala Run number PV4 Run 1

Sample Location Press Vent #4 Run 1 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV4-M5-1-FH	✓
filter(s)	PV4-M5-1-PF	✓

Acetone rinse beaker # 383 rinse volume ($V_a w$) 90 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(90) = 4.28 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 106.7518 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 106.7511 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.7628 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 106.7641 g

Gross wt 106.7625 - 0820 - 4/23/92 39% RH

Average Gross wt 106.7585 g

Tare wt 106.7491 g

Less acetone blank wt (W_a) 4.28×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0094 g

Filter(s) container number F356

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8068 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8069 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8069 g

Tare wt 3.8038 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0031~~ .0030 g

Weight of particulate in acetone rinse(m_a) 0.0094 g DKP

Total weight of particulate (m_n) ~~0.0125~~ .0124 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala. Run number PV4 R2

Sample Location Press Vent #4 Run 2

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV4-M5-2-FH	✓
filter(s)	PV4-M5-2-PF	✓

Acetone rinse beaker 385 rinse volume ($V_a w$) 100 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(100) = 4.76 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 112.5695 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 112.5681 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 112.5685 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 112.5683 g

Tare wt 112.5662 g

Less acetone blank wt (W_a) 4.76×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0021 g

Filter(s) container number F358

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8144 g

Date/time/RH of wt 4/13/92 - 0830 HRS - 36% RH Gross wt 3.8144 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8144 g

Tare wt 3.8123 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0021~~ .0020 g

Weight of particulate in acetone rinse(m_a) 0.0021 g DKP

Total weight of particulate (m_n) ~~0.0042~~ .0041 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Run 3 PV4

Sample Location Precipitent #4 3/17/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV4 - M5 - 3 - FH	✓
filter(s)	PV4 - M5 - 3 - PF	✓

Acetone rinse beaker 388 rinse volume ($V_a w$) 90 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(90) = 4.28 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH. Gross wt 111.3322 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 111.3313 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 111.3316 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 111.3315 g

Tare wt 111.3294 g

Less acetone blank wt (W_a) 4.28×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0021 g

Filter(s) container number F360

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8223 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8223 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8223 g

Tare wt 3.8209 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0014~~ .0013 g

Weight of particulate in acetone rinse(m_a) 0.0021 g DICP

Total weight of particulate (m_n) ~~0.0035~~ .0034 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Cola Run number Run 1 PV5

Sample Location Press Vent #5 Run 1 5/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV5-M5-1-FH	✓
filter(s)	PV5-M5-1-PF	✓

Acetone rinse beaker #378 rinse volume ($V_a w$) 70 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(70) = 3.33 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 - 0845 - 35%RH Gross wt 107.9954 g

Date/time/RH of wt 4/11/92 - 0930 - 41%RH Gross wt 107.9962 g

Date/time/RH of wt 4/13/92 - 1130 - 34%RH Gross wt 107.9942 g

Date/time/RH of wt 4/15/92 - 1330 - 30%RH Gross wt 107.9954 g

Gross wt 107.9969 g 4/21/92 - 1115 - 43% RH Average Gross wt 107.9956 g

Tare wt 107.9924 g

Less acetone blank wt (W_a) 3.33×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0032 g

Filter(s) container number F 372

Date/time/RH of wt 4/11/92 - 1130 - 43%RH Gross wt 3.8064 g

Date/time/RH of wt 4/13/92 - 0930 - 36%RH Gross wt 3.8066 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8065 g

Tare wt 3.8049 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0016~~ .0015 g

Weight of particulate in acetone rinse(m_a) 0.0032 g DICP

Total weight of particulate (m_n) ~~0.0048~~ .0047 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Denise K Parnell

Signature of Reviewer: _____

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant Press Vent 5 Run 2 Run number Run 2 PV5

Sample Location LP – Clayton Alabama 3/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV5 – M5 – 2 – FH	✓
filter(s)	PV5 – M5 – 2 – PF	✓

Acetone rinse beaker 379 rinse volume ($V_a w$) 90 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (90) = 4.28×10^{-5} g

Date/time/RH of wt 4/10/92 – 0845 HRS – 35% RH Gross wt 111.8747 g

Date/time/RH of wt 4/11/92 – 0930 – 41% RH Gross wt 111.8755 g

Date/time/RH of wt 4/13/92 – 1130 – 34% RH Gross wt 111.8735 g

Date/time/RH of wt 4/15/92 – 1330 – 30% RH Gross wt 111.8740 g

Average Gross wt 111.8738 g

Tare wt 111.8730 g

Less acetone blank wt (W_a) 4.28×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0008 g

Filter(s) container number F373

Date/time/RH of wt 4/11/92 – 1130 – 43% RH Gross wt ~~3.8074~~ 3.8111 g

Date/time/RH of wt Gross wt 3.8111 g

Date/time/RH of wt 4/13/92 – 0930 – 36% RH Gross wt 3.8109 g

Date/time/RH of wt Gross wt g

Average Gross wt 3.8110 g

Tare wt 3.8074 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0036~~ .0035 g

Weight of particulate in acetone rinse(m_a) 0.0008 g DKP

Total weight of particulate (m_n) ~~0.0044~~ .0043 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant Press Vent #5 Run number Run 3 PV5

Sample Location LP - Clayton Ala. 3/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV 5 - M5 - 3-FH	✓
filter(s)	PV5 - M5 - 3-PF	✓

Acetone rinse beaker 381 rinse volume ($V_a w$) 160 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (160) = 7.62×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 HRS - 35% RH. Gross wt 110.3424 g

Date/time/RH of wt 4/11/92 - 0930 HRS - 41% RH Gross wt 110.3427 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% RH Gross wt 110.3414 g

Date/time/RH of wt 4/15/92 - 1330 HRS - 30% RH Gross wt 110.3421 g

Gross wt 110.3440g 4/21/92 - 1115 - 43% RH Average Gross wt 110.3425 g

Tare wt 110.3378 g

Less acetone blank wt (W_a) 7.62×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0046 g

Filter(s) container number F 375

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.8106 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8104 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.8105 g

Tare wt 3.8049 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0056~~ .0055 g

Weight of particulate in acetone rinse(m_a) 0.0046 g DKP

Total weight of particulate (m_n) ~~0.0102~~ .0101 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna R Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala. Run number Run 1 PV6

Sample Location Press Vent #6 3/19/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV6 - M5-1-FH	✓
filter(s)	PV6 - M5-1-PF	✓

Acetone rinse beaker #387 rinse volume ($V_a w$) 75 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (75) = 3.57×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845HRS - 35% RH Gross wt 107.0475 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 107.0484 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 107.0460 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 107.0474 g

Gross wt 107.04889 4/21/92 1115 - 43% RH Average Gross wt 107.0476 g

Tare wt 107.0429 g

Less acetone blank wt (W_a) 3.57×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0047 g

Filter(s) container number F376

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7724 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7724 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7724 g

Tare wt 3.7717 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0007~~ .0006 g

Weight of particulate in acetone rinse(m_a) 0.0047 g

Total weight of particulate (m_n) ~~0.0054~~ .0053 DKP g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 2 PV6

Sample Location Press Vent #6 Run 2 3/20/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV6-M5-2-FH	✓
filter(s)	PV6-M5-2-PF	✓

Acetone rinse beaker #386 rinse volume ($V_a w$) 90 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (90) = 4.28×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845HRS - 35% RH Gross wt 103.7126 g

Date/time/RH of wt 4/11/92 - 0930HR - 41% RH Gross wt 103.7138 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% RH Gross wt 103.7119 g

Date/time/RH of wt 4/15/92 - 1330HRS - 30% RH Gross wt 103.7125 g

Gross wt 103.7143g 4/21/92 -1115 - 43% RH Average Gross wt 103.7130 g

Tare wt 103.7102 g

Less acetone blank wt (W_a) 4.28×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0028 g

Filter(s) container number F378

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7643 g

Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7639 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7641 g

Tare wt 3.7628 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0013~~ .0012 g

Weight of particulate in acetone rinse(m_a) 0.0028 g DICP

Total weight of particulate (m_n) ~~0.0041~~ .0040 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parnish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Run 3 PV6

Sample Location Press Vent #6 Run 3 3/20/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	PV6 – M5 – 3 – FH	✓
filter(s)	PV6 – M5 – 3 – PF	✓

Acetone rinse beaker #396 rinse volume ($V_a w$) 170 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(170) = 8.09 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 – 0845 HRS – 35% RH Gross wt 104.5893 g

Date/time/RH of wt 4/11/92 – 0930 HRS – 42% RH Gross wt 104.5903 g

Date/time/RH of wt 4/13/92 – 1130 HRS – 34% RH Gross wt 104.5888 g

Date/time/RH of wt 4/13/92 – 1330 HRS – 30% RH Gross wt 104.5895 g

Gross wt 104.5908 4/21/92 1115 – 45% RH

Average Gross wt 104.5912 g

Tare wt 104.5870 g

Less acetone blank wt (W_a) 8.09×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0041 g

Filter(s) container number F 380

Date/time/RH of wt 4/11/92 – 1130 – 43% RH Gross wt 3.7789 g

Date/time/RH of wt 4/13/92 – 0930 – 36% RH Gross wt 3.7789 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 3.7789 g

Tare wt 3.7780 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0009~~ .0008 g

Weight of particulate in acetone rinse(m_a) 0.0041 g

Total weight of particulate (m_n) ~~0.0050~~ .0049 g DKP

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donnie K Pennington

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala. Run number Run 1

Sample Location Dryer Stack 1 PM10 Run 1 3/13/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	081 - PM10 - 1 - CYAce	✓
filter(s)	051 - PM10 - 1 - PF	✓

Acetone rinse beaker # 392 rinse volume ($V_a w$) 170 ml ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(170) = 8.09 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH Gross wt 109.6526 g

Date/time/RH of wt 4/11/92 - 0830 - 41% RH. Gross wt 109.6535 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 109.6511 g

Date/time/RH of wt 4/13/92 - 1330 - 30% RH Gross wt 109.6515 g

Average Gross wt 109.6513 g

Tare wt 109.6072 g

Less acetone blank wt (W_a) 8.09×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0440 g

Filter(s) container number 620 007

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1929 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1927 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1928 g

Tare wt 0.1857 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0071~~ .0070 g

Weight of particulate in acetone rinse(m_a) 0.0440 g

Total weight of particulate (m_n) ~~0.0511~~ .0510 DKP g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No.

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala. Run number Run 2 PM10.

Sample Location Dryer Stack #1 - PM10 Run 2 3/13/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS1 - PM10 - 2 - CYACC	✓
filter(s)	DS1 - PM10 - 2 - PF	✓

Acetone rinse beaker #393 rinse volume ($V_a w$) 60 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (60) = 2.86×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 HRS - 35% AH Gross wt 106.2166 g

Date/time/RH of wt 4/11/92 - 0930 HRS - 41% AH Gross wt 106.2172 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% AH Gross wt 106.2153 g

Date/time/RH of wt 4/15/92 - 1330 HRS - 30% AH Gross wt 106.2164 g

Gross wt 106.2176 g - 4/21/92 - 1115 43% RH Average Gross wt 106.2166 g

Tare wt 106.2156 g

Less acetone blank wt (W_a) 2.86×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0010 g

Filter(s) container number 62Q008

Date/time/RH of wt 4/13/92 - 1300 - 32% RH Gross wt 0.2035 g

Date/time/RH of wt 4/15/92 - 1330 - 30% AH Gross wt 0.2033 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.2034 g

Tare wt 0.1860 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0174~~ .0173 g

Weight of particulate in acetone rinse(m_a) 0.0010 g DKP

Total weight of particulate (m_n) ~~0.0184~~ .0183 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K. Parnell

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant CP- Clayton Run number Run 3 PM10

Sample Location Dryer Stack # 3 PM-10 3/14/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	0S1 - PM10 - 3-CyAcc	✓
filter(s)	0S1 - PM10 - 3-PF	✓

Acetone rinse beaker # 395 rinse volume ($V_a w$) 85 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(85) = 4.05 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 - 0845HRS - 35% R.H. Gross wt 109.4262 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 109.4271 g

Date/time/RH of wt 4/13/92 - 1130HRS - 34% RH Gross wt 109.4252 g

Date/time/RH of wt 4/15/92 - 1330HRS - 30% RH Gross wt 109.4255 g

Average Gross wt 109.4254 g

Tare wt 109.4152 g

Less acetone blank wt (W_a) 4.05×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0102 g

Filter(s) container number 620609

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1953 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1952 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1953 g

Tare wt 0.1839 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0114~~ .0113 g

Weight of particulate in acetone rinse(m_a) 0.0102 g DKP

Total weight of particulate (m_a) ~~0.0210~~ .0215 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Dana K Parash

Signature of Reviewer: _____

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Control No. 001302

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala. Run number Run 1 PM10

Sample Location Dryer Stack #2 PM10 Run 1

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	OS2 - PM10 - 1 - CYACE	✓
filter(s)	OS2 - PM10 - 1 - PF	✓

Acetone rinse beaker # 418 rinse volume ($V_a w$) 100 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(100) = 4.76 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 105.3102 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 105.3092 g

Date/time/RH of wt 4/15/92 - 1330 - 30% Gross wt 105.3097 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 105.3113 g

Gross wt 105.3098 4/23/92 0820 - 39% RH Average Gross wt 105.3100 g

Tare wt 105.2905 g

Less acetone blank wt (W_a) 4.76×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0195 g

Filter(s) container number 62Q010

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1913 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1912 g

Date/time/RH of wt Gross wt g

Date/time/RH of wt Gross wt g

Average Gross wt 0.1913 g

Tare wt 0.1855 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0056~~ .0057 g

Weight of particulate in acetone rinse(m_a) 0.0195 g DKP

Total weight of particulate (m_a) ~~0.0253~~ .0252 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Parrish

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number PS2 - R2

Sample Location Drum Stack #2 - PM10 - Run 2 3/14/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS2 - PM10 - 2 - CYACE	✓
filter(s)	DS2 - PM10 - 2 - PF	✓

Acetone rinse beaker #417 rinse volume ($V_a w$) 80 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(80) = 3.81 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 - 0845HRS - 35% RH. Gross wt 98.5725 g

Date/time/RH of wt 4/11/92 - 0930HRS - 41% RH Gross wt 98.5731 g

Date/time/RH of wt 4/13/92 - 1130HRS - 34% RH. Gross wt 98.5713 g

Date/time/RH of wt 4/15/92 - 1330HRS - 30% RH Gross wt 98.5723 g

Gross wt 98.5737 g 4/21/92 1115 - 43% RH Average Gross wt 98.5726 g

Tare wt 98.5644 g

Less acetone blank wt (W_a) 3.81×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0082 g

Filter(s) container number 629 011

Date/time/RH of wt 4/13 - 1300 - 32% RH. Gross wt 0.1926 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1926 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1926 g

Tare wt 0.1787 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0139~~ .0138 g

Weight of particulate in acetone rinse(m_a) 0.0082 g

DKP

Total weight of particulate (m_n) ~~0.0221~~ .0220 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Lamsh

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant CP – Clayton Ala Run number Run 3 PM10

Sample Location Dryer Stack #2 – PM10 Run 3/14/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	OS2 – PM10 – 3 – CYRE	✓
filter(s)	DS2 – PM10 – 3 – PF	✓

Acetone rinse beaker # 302 rinse volume ($V_a w$) 120 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(120) = 5.71 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 – 0845 HRS – 35% RH Gross wt 109.8644 g

Date/time/RH of wt 4/11/92 – 0930 HRS – 41% RH Gross wt 109.8651 g

Date/time/RH of wt 4/13/92 – 1130 HRS – 34% RH Gross wt 109.8631 g

Date/time/RH of wt 4/15/92 – 1330 HRS – 30% RH Gross wt 109.8641 g

Gross wt 109.8659 4/21/92 – 1115 – 43% RH Average Gross wt 109.8645 g

Tare wt 109.8615 g

Less acetone blank wt (W_a) 5.71×10^{-5} g

Weight of particulate in acetone rinse (m_a) ~~2.9~~ DKP 0.0029 g

Filter(s) container number 62Q 012

Date/time/RH of wt 4/13 – 1300 – 32% RH Gross wt 0.1923 g

Date/time/RH of wt 4/15 – 1330 – 30% RH Gross wt 0.1922 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1923 g

Tare wt 0.1788 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0135~~ .0134 g

Weight of particulate in acetone rinse(m_a) 0.0029 g DKP

Total weight of particulate (m_n) ~~0.0164~~ .0163 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Run 1 PM 10

Sample Location 3/14/92 Dryer Stack #3 PM 10 Run 1

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	OS 3 – PM 10 – 1 – CYACC	✓
filter(s)	OS 3 – PM10 – 1 – PF	✓

Acetone rinse beaker #318 rinse volume ($V_a w$) 75 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(75) = 3.57 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 – 1130 HRS – 43% RH. Gross wt 104.5158 g

Date/time/RH of wt 4/13/92 – 1130 HRS – 34% RH Gross wt 104.5153 g

Date/time/RH of wt 4/15/92 – 1330 HRS – 30% RH Gross wt 104.5170 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 104.5156 g

Tare wt 104.5155 g

Less acetone blank wt (W_a) 3.57×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0001 g

Filter(s) container number 62Q013

Date/time/RH of wt 4/13 – 1300 – 32% RH Gross wt 0.1891 g

Date/time/RH of wt 4/15 – 1330 – 30% RH Gross wt 0.1890 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1891 g

Tare wt 0.1778 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0113~~ .0112 g

Weight of particulate in acetone rinse(m_a) 0.0001 g DKP

Total weight of particulate (m_n) ~~0.0114~~ .0113 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. 001300

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala Run number PM10 Run 2

Sample Location Dryer Stack # 3 3/16/92 Run 2

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS3 - PM10 - 2 - CY ACE	✓
filter(s)	DS3 - PM10 - 2 - PM	✓

Acetone rinse beaker #305 rinse volume ($V_a w$) 70 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(70) = 3.33 \times 10^{-5}$ g

Date/time/RH of wt 4/10 - 0845 - 35% RH Gross wt 107.5552 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 107.5557 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 107.5538 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 107.5549 g

Gross wt 107.5564 4/21/92 - 1115 - 43% RH Average Gross wt 107.5552 g

Tare wt 107.5502 g

Less acetone blank wt (W_a) 3.33×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0050 g

Filter(s) container number 62Q 014

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.2089 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.2082 g

Date/time/RH of wt 4/21 - 1115 - 43% RH Gross wt 0.2083 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.2083 g

Tare wt 0.1782 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0301~~ .0300 g

Weight of particulate in acetone rinse(m_a) 0.0050 g DKP

Total weight of particulate (m_n) ~~0.0351~~ .0350 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna R Parnell

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala. Run number Run 1 PM10

Sample Location Dryer Stack #4 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	084-PM10-1-CYACE	✓
filter(s)	084-PM10-1-PF	✓

Acetone rinse beaker #380 rinse volume ($V_a w$) 95 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(95) = 4.52 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH Gross wt 106.4171 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 106.4178 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH. Gross wt 106.4154 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.4164 g

Gross wt 106.4181g 4/21/92 -1115 - 43% RH Average Gross wt 106.4170 g

Tare wt 106.4057 g

Less acetone blank wt (W_a) 4.52×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0113 g

Filter(s) container number 620015

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1983 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1982 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1983 g

Tare wt 0.1786 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0197~~ .0194 g

Weight of particulate in acetone rinse(m_a) 0.0113 g DKP

Total weight of particulate (m_n) ~~0.0310~~ .0309 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K. Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Run 2 PM10

Sample Location Dryer Stack #4 PM10 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	054 - PM10-2-CYACE	✓
filter(s)	054 - PM10-2-PF	✓

Acetone rinse beaker A 390 rinse volume ($V_a w$) 80 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(80) = 3.81 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 - 0845 - 35% A.H. Gross wt 109.5785 g

Date/time/RH of wt 4/11/92 - 0930 - 41% AH Gross wt 109.5792 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% AH Gross wt 109.5768 g

Date/time/RH of wt 4/15/92 - 1330 HRS - 30% AH Gross wt 109.5782 g

Gross wt 109.5794 g 4/21/92 -1130 -43% RH Average Gross wt 109.5784 g

Tare wt 109.5725 g

Less acetone blank wt (W_a) 3.81×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0059 g

Filter(s) container number 62Q 016

Date/time/RH of wt 4/13 - 1300 - 32% AH Gross wt 0.1966 g

Date/time/RH of wt 4/15 - 1330 - 30% AH Gross wt 0.1979 g

Date/time/RH of wt Gross wt 0.1981 g

Date/time/RH of wt Gross wt ~~0~~ DKP g

Average Gross wt 0.1980 g

Tare wt ~~0.1786~~ 0.1764 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0216~~ .0215 g

Weight of particulate in acetone rinse(m_a) 0.0059 g DKP

Total weight of particulate (m_n) ~~0.0275~~ .0274 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks

Signature of analyst: Donna K Pennock

Signature of Reviewer:

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 1 PM10

Sample Location Dryer Stack #6 PM10 - 3/12/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS6 - PM10 - 1-CVACC	✓
filter(s)	DS6 - PM10 - 1-PF	✓

Acetone rinse beaker #382 rinse volume ($V_a w$) 75 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (75) = 3.57×10^{-5} g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH Gross wt 101.2672 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 101.2680 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 101.2660 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 101.2669 g

Gross wt 101.2683 g 4/21/92 - 1115 - 43% RH Average Gross wt 101.2673 g

Tare wt 101.2634 g

Less acetone blank wt (W_a) 3.57×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0039 g

Filter(s) container number 620 004

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.2025 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.2024 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.2025 g

Tare wt 0.1862 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0163~~ .0162 g

Weight of particulate in acetone rinse(m_a) 0.0039 g DKP

Total weight of particulate (m_n) ~~0.0202~~ .0201 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala Run number Run 2 PM10

Sample Location Dryer stack #6 PM10 Run 2 3/12/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	056 - PM10 - 2 - CYACE	✓
filter(s)	056 - PM10 - 2 - PF	✓

Acetone rinse beaker #384 rinse volume ($V_a w$) 75 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (75) = 3.57×10^{-5} g

Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 106.8821 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 106.8810 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.8813 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 106.8812 g

Tare wt 106.8800 g

Less acetone blank wt (W_a) 3.57×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0012 g

Filter(s) container number 620 005

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1917 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1917 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1917 g

Tare wt 0.1860 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0057~~ .0056 g

Weight of particulate in acetone rinse(m_a) 0.0012 g

.00668 DKP

Total weight of particulate (m_n) ~~0.0069~~ g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Ala. Run number Run 3 PM10

Sample Location Dryer STACK #6 — 3/12/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS-6 - PM10 - 3-CYACE	✓
filter(s)	DS6 - PM10 - 3-PF	✓

Acetone rinse beaker # 389 rinse volume ($V_a w$) 80 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(80) = 3.81 \times 10^{-5}$ g

Date/time/RH of wt 4/10/92 - 0845 - 35% RH Gross wt 106.2778 g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 106.2786 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 106.2765 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 106.2777 g

Gross wt 106.2793g 4/21/92 1115 43% RH

Average Gross wt 106.2780 g

Tare wt 106.2755 g

Less acetone blank wt (W_a) 3.81×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0025 g

Filter(s) container number 62Q006

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1945 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1940 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1945 g

Tare wt 0.1858 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0087~~ .0086 g

Weight of particulate in acetone rinse(m_a) 0.0025 g

.0111 DKP

Total weight of particulate (m_n) ~~0.0112~~ g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Lanier

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala. Run number Run 1 PM10

Sample Location Dryer Stack #8 PM10 Run 1 3/11/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS8 - PM10 - 1 - CYACE	✓
filter(s)	DS8 - PM10 - 1 - PF	✓

Acetone rinse beaker #312 rinse volume ($V_a w$) 85 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10)^{7} (\ 85\ ) = 4.05 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 0930 HRS - 41% RH Gross wt 110.8303 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% RH. Gross wt 110.8292 g

Date/time/RH of wt 4/15/92 - 1330 HRS - 30% RH Gross wt 110.8299 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 110.8311 g

Gross wt 110.8310 g 4/22/92 1300 - 44% RH Average Gross wt 110.8303 g

Tare wt 110.8289 g

Less acetone blank wt (W_a) 4.05×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0014 g

Filter(s) container number 62Q002

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1930 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1929 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1930 g

Tare wt 0.1860 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0070~~ .0069 g

Weight of particulate in acetone rinse(m_a) 0.0014 g

DKP

Total weight of particulate (m_a) ~~0.0084~~ .0083 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. [illegible]

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP - Alabama Run number Run 2 PM10

Sample Location Dryer Stack #8 PM10 - 3/11/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	DS8 - PM10 - 2 - CYACE	✓
filter(s)	DS8 - PM10 - 2 - PF	✓

Acetone rinse beaker #399 rinse volume ($V_a w$) 65 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.75 \times 10^{-7})$ (65) = 3.09×10^{-5} g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 110.9005 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 110.8992 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 110.8994 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 110.8993 g

Tare wt 110.8982 g

Less acetone blank wt (W_a) 3.09×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0011 g

Filter(s) container number 62 Q 001

Date/time/RH of wt 4/13 - 1300 - 32% RH Gross wt 0.1908 g

Date/time/RH of wt 4/15 - 1330 - 30% RH Gross wt 0.1906 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1907 g

Tare wt 0.1851 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0056~~ .0056 g

Weight of particulate in acetone rinse(m_a) 0.0011 g

Total weight of particulate (m_n) ~~0.0067~~ .0066 DKP g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K Parrish

Signature of Reviewer: _____

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Control No. 001314

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Ala Run number Run 3 PM10

Sample Location Dryer Stack #8 PM10 R3 - 3/11/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse	088-PM10-3-CYACE	✓
filter(s)	088-PM10-3-PF	✓

Acetone rinse beaker #416 rinse volume ($V_a w$) 70 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})$ (70) = 3.33×10^{-5} g

Date/time/RH of wt 4/11/92 - 1130 HRS - 43% RH Gross wt 99.5562 g

Date/time/RH of wt 4/13/92 - 1130 HRS - 34% RH Gross wt 99.5554 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 99.5559 g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 99.5557 g

Tare wt 99.5514 g

Less acetone blank wt (W_a) 3.33×10^{-5} g

Weight of particulate in acetone rinse (m_a) 4.27×10^{-3} g

0.0043

Filter(s) container number 62Q003

Date/time/RH of wt 4/13/92 - 1300 - 32% RH Gross wt 0.1915 g

Date/time/RH of wt 4/15/ - 1330 - 30% RH Gross wt 0.1913 g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt 0.1914 g

Tare wt 0.1856 g

Less filter blank wt (F_a) 0.0001 g

Weight of particulate on filter(s) (m_f) ~~0.0058~~ .0057 g

Weight of particulate in acetone rinse(m_a) 0.0043 g

Total weight of particulate (m_n) ~~0.0101~~ .0100 DKP g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: Donna K. Parrish

Signature of Reviewer: _____

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Control No. 001315

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP – Clayton Ala Run number Run 2 PM10 ≥10μ

Sample Location Dryer Stack 2 greater than PM10

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse filter(s)	DS2 – ≥PM10 – 2 – CYAce	✓

Acetone rinse beaker 397 rinse volume ($V_a w$) 100 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(100) = 4.76 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 – 0930 – 46% RH Gross wt 108.5001 g

Date/time/RH of wt 4/13/92 – 1130 – 34% RH Gross wt 108.4979 g

Date/time/RH of wt 4/21/92 – 1115 – 43% RH Gross wt 108.5009 g

Date/time/RH of wt 4/22/92 – 1130 – 44% RH Gross wt 108.5008 g

Average Gross wt 108.5009 g

Tare wt 108.4071 g

Less acetone blank wt (W_a) 4.76×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0938 g

Filter(s) container number _____

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt _____ g

Tare wt _____ g

Less filter blank wt (F_a) _____ g

Weight of particulate on filter(s) (m_f) _____ g

Weight of particulate in acetone rinse(m_a) _____ g

Total weight of particulate (m_n) _____ g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: _____

Signature of Reviewer: _____

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Control No. 001316

METHOD 5

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number Run 2 DS3 PM10

Sample Location Dryer Stack 3 PM10 greater than 10um 3/16/92

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Acetone rinse filter(s)	DS3 - PM10 - 2 - CYACE - B	✓

Acetone rinse beaker 398 rinse volume ($V_a w$) 140 ml

Acetone blank residue concentration (C_a) 4.76×10^{-7} g/ml

$W_a = C_a V_a w = (4.76 \times 10^{-7})(140) = 6.66 \times 10^{-5}$ g

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 109.1152 g

Date/time/RH of wt 4/13/92 - 1130 - 38% RH Gross wt 109.1133 g

Date/time/RH of wt 4/21/92 - 1115 - 43% RH Gross wt 109.1158 g

Date/time/RH of wt ~~4/20/92~~ - 1130 - 44% RH Gross wt 109.1160 g

DKP 4/22/92

Average Gross wt 109.1159 g

Tare wt 109.0163 g

Less acetone blank wt (W_a) 6.66×10^{-5} g

Weight of particulate in acetone rinse (m_a) 0.0995 g

Filter(s) container number _____

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Date/time/RH of wt _____ Gross wt _____ g

Average Gross wt _____ g

Tare wt _____ g

Less filter blank wt (F_a) _____ g

Weight of particulate on filter(s) (m_f) _____ g

Weight of particulate in acetone rinse(m_a) _____ g

Total weight of particulate (m_n) _____ g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of acetone used to subtracted from the sample weight.

Remarks _____

Signature of analyst: _____ Signature of Reviewer: _____

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Control No. 100806

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number R2 - PV2

Sample location Press Vent #8 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	P08-M201-2-MCL	✓
Aqueous rinse	P08-M201-2-H2O	✓

Methylene Chloride rinse container number 432

Methylene Chloride rinse volume ($V_a w$) 220 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = 0.0 g

Date and time of wt 4/23/92 0850 3970 Gross wt 104.8966 g

Date and time of wt 4/23/92 1400 Gross wt 104.8970 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.8968 g

Tare wt 104.8903 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0065 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 440

Aqueous rinse volume ($V_a w$) 410 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/29/92 0830 3170 Gross wt 105.7245 g

Date and time of wt 4/29/92 1445 3170 Gross wt 105.7244 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.7245 g

Tare wt 105.7189 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0056 g

Total weight of particulate (m_n) 0.0121 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number A1-PV8

Sample location President #8 Run 1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV8-M202-1-MCL	✓
Aqueous rinse	PV8-M202-1-H_2O	✓

Methylene Chloride rinse container number 437

Methylene Chloride rinse volume ($V_a w$) 215 ml

Methylene Chloride blank residue concentration (C_a) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 3770 Gross wt 108.4224 g

Date and time of wt 4/23/92 1400 Gross wt 108.4228 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 108.4224 g

Tare wt 108.4156 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0070 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 441

Aqueous rinse volume ($V_a w$) 260 ml

Aqueous blank residue concentration (C_a) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0830 3770 Gross wt 104.1984 g

Date and time of wt 4/23/92 1600 Gross wt 104.1979 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.1987 g

Tare wt 104.1927 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0060 g

Total weight of particulate (m_n) 0.0130 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dianne Parrish

Signature of reviewer

Control No. 100802

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number R3-PV7

Sample location PressVent 7 Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV7-M202-3-MC	✓
Aqueous rinse	PV7-M202-3-H_2O	✓

Methylene Chloride rinse container number 423

Methylene Chloride rinse volume (V_aw) 225 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = 0.0 g

Date and time of wt 4/23/92 0850 3170 Gross wt 106.5368 g

Date and time of wt 4/23/92 1400 Gross wt 106.5372 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 106.5370 g

Tare wt 106.5332 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0038 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 454

Aqueous rinse volume (V.w) 265 ml

Aqueous blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/29/92 0830 3170 Gross wt 104.1858 g

Date and time of wt 4/29/92 1445 3170 Gross wt 104.1860 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.1859 g

Tare wt 104.1831 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0028 g

Total weight of particulate (m_n) 0.0066 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parnell

Signature of reviewer

Control No. 100893

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number A2 -PV7

Sample location President #7 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV7-M202-2-MCL	✓
Aqueous rinse	PV7-M202-2-H20	✓

Methylene Chloride rinse container number 107

Methylene Chloride rinse volume ($V_a w$) 175 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = 0.0 g

Date and time of wt 4/23/92 0850 3970 Gross wt 112.0543 g

Date and time of wt 4/23/92 1400 Gross wt 112.0542 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 112.0543 g

Tare wt 112.0510 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0033 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 447

Aqueous rinse volume ($V_a w$) 400 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/29/92 0830 3170 Gross wt 103.5962 g

Date and time of wt 4/29/92 1445 3170 Gross wt 103.5961 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 103.5962 g

Tare wt 103.5944 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0018 g

Total weight of particulate (m_n) 0.0051 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dianne Parrish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number R1-PV7

Sample location Press Vent #7 Run 1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV7-M202-1-MCL	✓
Aqueous rinse	PV7-M201-1-H2O	✓

Methylene Chloride rinse container number 430

Methylene Chloride rinse volume ($V_a w$) 210 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 39% Gross wt 110.7754 g

Date and time of wt 4/23/92 1400 Gross wt 110.7758 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 110.7756 g

Tare wt 110.7722 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0034 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 439

Aqueous rinse volume (V w) 480 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 102.3185 g

Date and time of wt 4/30/92 1415 Gross wt 102.3186 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 102.3186 g

Tare wt 102.3148 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0038 g

Total weight of particulate (m_n) 0.0072 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dennis K Parrish

Signature of reviewer

Control No. 100605

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number R3 PV6

Sample location Press Vent #6 Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV6-M202-3-MCL	✓
Aqueous rinse	PV6-M202-3-H2O	✓

Methylene Chloride rinse container number 46

Methylene Chloride rinse volume ($V_a w$) 200 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 3970 Gross wt 106.1182 g

Date and time of wt 4/23/92 1400 Gross wt 106.1185 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 106.1184 g

Tare wt 106.1158 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0026 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 426

Aqueous rinse volume ($V w$) 460 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 101.5962 g

Date and time of wt 4/30/92 1415 Gross wt 101.5963 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 101.5963 g

Tare wt 101.5939 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0024 g

Total weight of particulate (m_n) 0.0050 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dianne K Parrish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number Run 2

Sample location Press Vent #6 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV6-M202-2-MCL	✓
Aqueous rinse	PV6-M202-2-H2O	✓

Methylene Chloride rinse container number 425

Methylene Chloride rinse volume ($V_a w$) 225 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 3970 Gross wt 104.6063 g

Date and time of wt 4/23/92 1400 Gross wt 104.6067 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.6065 g

Tare wt 104.6042 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0023 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 456

Aqueous rinse volume (V w) ~~235~~ 475 ml ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = 0.0 g

Date and time of wt 4/29/92 0830 3170 Gross wt 102.2840 g

Date and time of wt 4/29/92 1445 3170 Gross wt 102.2841 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 102.2841 g

Tare wt 102.2817 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0024 g

Total weight of particulate (m_n) 0.0047 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Pearson

Signature of reviewer

Control No. 100897

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 1

Sample location Preconvert #6 R1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV6 - M 202 - 1 - MCL	—
Aqueous rinse	PV6 - M 202 - 1 - H_2O	—

Methylene Chloride rinse container number 236

Methylene Chloride rinse volume (V_aw) 200 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 3140 Gross wt 120.9475 g

Date and time of wt 4/23/92 1400 Gross wt 120.9479 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 120.9477 g

Tare wt 120.9449 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0028 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 466

Aqueous rinse volume (V_w) 225 + 165 → 390 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/29/92 0850 3170 Gross wt 108.5615 g

Date and time of wt 4/29/92 1445 3170 Gross wt 108.5615 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 108.5615 g

Tare wt 108.5586 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0029 g

Total weight of particulate (m_n) 0.0057 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No. 10[illegible]B

SAMPLE ANALYTICAL FORM

Plant LP-Clayton. Run number R3-PV5

Sample location Press Vent #5 Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV5-M202-3-MCL	✓
Aqueous rinse	PV5-M202-3-H2O	✓

Methylene Chloride rinse container number 438

Methylene Chloride rinse volume ($V_a w$) 225 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 3970 Gross wt 110.0513 g

Date and time of wt 4/23/92 1400 3770 Gross wt 110.0517 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 110.0515 g

Tare wt 110.0443 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0072 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 430

Aqueous rinse volume (V w) 225 + 135 → 360 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 107.0485 g

Date and time of wt 4/28/92 1600 Gross wt 107.0478 g

Date and time of wt 4/29/92 0830 3170 Gross wt 107.0473 g

Date and time of wt Gross wt g

Average gross wt 107.0476 g

Tare wt 107.0453 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0023 g

Total weight of particulate (m_n) 0.0095 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Vince K Powell

Signature of reviewer

Control No. 100099

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number R2-PV5

Sample location Press Vent 5 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV5-M202-R2-mcl	—
Aqueous rinse	PV5-M202-R2-H2O	—

Methylene Chloride rinse container number 445

Methylene Chloride rinse volume ($V_a w$) 175 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 DKP 0850 5970 Gross wt 107.8804 g

Date and time of wt 4/23/92 1400 Gross wt 107.8807 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.8806 g

Tare wt 107.8752 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0054 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 451

Aqueous rinse volume (V_w) 370 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 3670 Gross wt 108.0072 g

Date and time of wt 4/27/92 0830 3470 Gross wt 108.0055 g

Date and time of wt 4/27/92 1600 3470 Gross wt 108.0053 g

Date and time of wt Gross wt g

Average gross wt 108.0054 g

Tare wt 108.0015 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) .0039 g

Total weight of particulate (m_n) 0.0093 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Pernash

Signature of reviewer

Control No. 100010

SAMPLE ANALYTICAL FORM

Plant CP-Clayton Run number R1-PV5

Sample location Preservent # 5 Run 1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV5-M202-1-MCL	✓
Aqueous rinse	PV5-M202-1-H2O	✓

Methylene Chloride rinse container number 93

Methylene Chloride rinse volume ($V_a w$) 200 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 39% Gross wt 113.5132 g

Date and time of wt 4/23/92 1400 Gross wt 113.5137 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 113.5135 g

Tare wt 113.5083 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0052 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 427

Aqueous rinse volume (V w) 400 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 59% Gross wt 106.4034 g

Date and time of wt 4/28/92 1600 Gross wt 106.4035 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 106.4034 g

Tare wt 106.4016 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0020 g

Total weight of particulate (m_n) 0.0072 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number R3-PU4

Sample location Press Vent 4 R3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PU4-M202-3-MCC	✓
Aqueous rinse	PU4-M202-3-H_2O	✓

Methylene Chloride rinse container number 452

Methylene Chloride rinse volume ($V_a w$) 170 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 Gross wt 104.7067 g

Date and time of wt 4/23/92 1400 Gross wt 104.7070 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.7069 g

Tare wt 104.7060 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0029 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 465

Aqueous rinse volume (V_w) 395 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 107.8190 g

Date and time of wt 4/28/92 1600 Gross wt 107.8185 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.8188 g

Tare wt 107.8165 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0023 g

Total weight of particulate (m_n) 0.0052 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dennis Parrish

Signature of reviewer

Control No. 100[illegible]2

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number R2-PV4

Sample location Press Vent #4 R2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV4-M202-2-MCL	✓
Aqueous rinse	PV4-M202-2-H_2O	✓

Methylene Chloride rinse container number 442

Methylene Chloride rinse volume ($V_a w$) 180 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/23/92 0850 3/10 Gross wt 101.8844 g

Date and time of wt 4/23/92 1400 Gross wt 101.8847 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 101.8846 g

Tare wt 101.8826 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0020 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 443

Aqueous rinse volume (V w) 225+25+65 → 315 ml ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = 4c g

Date and time of wt 4/23/92 0850 3/10 Gross wt 106.8919 g

Date and time of wt 4/23/92 1400 Gross wt 106.8924 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 106.8922 g

Tare wt 106.8901 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) .0021 g

Total weight of particulate (m_n) 0.0041 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Pernak

Signature of reviewer

Control No. 100613

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number R1 PV4

Sample location Press Vent #4 R1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV4-M202-1-MCL	✓
Aqueous rinse	PV4-M202-1-H_2O	—

Methylene Chloride rinse container number 434

Methylene Chloride rinse volume ($V_a w$) 190 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 1400 HRS 37% Gross wt 110.5095 g

Date and time of wt 4/24/92 0830 36% Gross wt 110.5090 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 110.5093 g

Tare wt 110.5076 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0017 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 435

Aqueous rinse volume (V_w) 225 + 120 → 345 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 39% Gross wt 109.7085 g

Date and time of wt 4/28/92 1400 Gross wt 109.7085 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 109.7085 g

Tare wt 109.7060 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0025 g

Total weight of particulate (m_n) 0.0042 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Pernsh

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant CP-Clayton Run number R3-PV3

Sample location Press Vent #3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV3-M202-3-MCL	✓
Aqueous rinse	PV3-M202-3-H2O	✓

Methylene Chloride rinse container number 449

Methylene Chloride rinse volume ($V_a w$) 200 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 39% Gross wt 105.6740 g

Date and time of wt 4/23/92 1400 Gross wt 105.6745 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.6743 g

Tare wt 105.6727 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0016 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 453

Aqueous rinse volume (V w) 225 + 275 → 500 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 Gross wt 113.4261 g

Date and time of wt 4/28/92 1600 Gross wt 113.4258 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 113.4260 g

Tare wt 113.4236 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) .0024 g

Total weight of particulate (m_n) 0.0040 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Perich

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant CP-Clayton Run number R2-PV3

Sample location Press Vent #3 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV3-M202-2-MCL	
Aqueous rinse	PV3-M202-2-H2O	✓

Methylene Chloride rinse container number 428

Methylene Chloride rinse volume ($V_a w$) 200 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 1400 HRS 37% Gross wt 107.2792 g

Date and time of wt 4/24/92 0830 HRS 59% Gross wt 107.2789 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.2791 g

Tare wt 107.2766 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0025 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 446

Aqueous rinse volume ($V w$) 225 + 105 → 100 → 430 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 39% Gross wt 109.5790 g

Date and time of wt 4/28/92 1600 Gross wt 109.5785 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 109.5788 g

Tare wt 109.5768 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0020 g

Total weight of particulate (m_n) 0.0045 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Perrot

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number R3-Fe1

Sample location Former Exhaust #1 - Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	Fe1-M202-3-MCL	✓
Aqueous rinse	Fe1-M202-3-H2O	✓

Methylene Chloride rinse container number 411

Methylene Chloride rinse volume ($V_a w$) 130 mL ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 1400 3770 Gross wt 104.8307 g

Date and time of wt 4/24/92 0830 3670 Gross wt 104.8310 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.8309 g

Tare wt 104.8172 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0137 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 444

Aqueous rinse volume ($V_a w$) 200 + 40 → 240 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 Gross wt 103.3720 g

Date and time of wt 4/23/92 1400 Gross wt 103.3724 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 103.3722 g

Tare wt 103.3701 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0021 g

Total weight of particulate (m_n) 0.0158 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Pernak

Signature of reviewer

Control No. 100039

SAMPLE ANALYTICAL FORM

Plant CP-Clayton Run number _____

Sample location Former Exhaust #

Relative humidity _____

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	FC1-M202-2-MCC	✓
Aqueous rinse	FC1-M202-2-H2O	✓

Methylene Chloride rinse container number 422

Methylene Chloride rinse volume ($V_a w$) 275 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/23/92 1400 HRS 37% Gross wt 103.2727 g

Date and time of wt 4/24/92 0830 36% Gross wt 103.2722 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 103.2725 g

Tare wt 103.2562 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0163 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 458

Aqueous rinse volume (V_w) 225 + 75 + 90 → 390 mL ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/23/92 0850 37% Gross wt 102.8441 g

Date and time of wt 4/23/92 1400 Gross wt 102.8446 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 102.8444 g

Tare wt 102.8408 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0036 g

Total weight of particulate (m_n) 0.0199 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks _____

Signature of analyst Dianne Perrault

Signature of reviewer _____

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP- Clayton Run number R1-FE1

Sample location Former exhaust

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	FE1-M202-1-MCL	✓
Aqueous rinse	FE1-M202-1-H2O	✓

Methylene Chloride rinse container number 106

Methylene Chloride rinse volume ($V_a w$) 220 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 1400HRS 3770 Gross wt 118.8295 g

Date and time of wt 4/24/92 0830 3470 Gross wt 118.8291 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 118.8293 g

Tare wt 118.8163 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0130 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 455

Aqueous rinse volume (V w) 225+90+ 315 mr ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 3670 Gross wt 107.1164 g

Date and time of wt 4/27/92 0830 3470 Gross wt 107.1150 g

Date and time of wt 4/27/92 1600 3470 Gross wt 107.1146 g

Date and time of wt Gross wt g

Average gross wt 107.1148 g

Tare wt 107.1117 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0031 g

Total weight of particulate (m_n) 0.0161 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number R2-BS2

Sample location Boiler Stack #2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	BS2-M202-2-MCL	✓
Aqueous rinse	BS2-M202-2-H20	✓

Methylene Chloride rinse container number 448

Methylene Chloride rinse volume (V_aw) 205 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 1400 HRS 3970 Gross wt 101.7510 g

Date and time of wt 4/24/92 0830 3970 Gross wt 101.7511 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 101.7511 g

Tare wt 101.7478 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0033 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 457

Aqueous rinse volume (V_w) 225 + 120 + 155 → 500 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 106.1732 g

Date and time of wt 4/28/92 1600 Gross wt 106.1733 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 106.1733 g

Tare wt 106.1688 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0045 g

Total weight of particulate (m_n) 0.0078 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Pamph

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number R3-BS2

Sample location Boiler Stack #2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	BS2-M202-3-MCL	✓
Aqueous rinse	BS2-M202-3-H2O	✓

Methylene Chloride rinse container number 354

Methylene Chloride rinse volume ($V_a w$) 160 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 1400 Hrs 37°C Gross wt 113.0392 g

Date and time of wt 4/24/92 0830 36°C Gross wt 113.0348 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 113.0350 g

Tare wt 113.0335 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0015 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 431

Aqueous rinse volume (V w) 225 + 150 + 75 → 450 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 36°C Gross wt 103.2230 g

Date and time of wt 4/27/92 0830 34°C Gross wt 103.8220 g

Date and time of wt 4/27/92 1600 34°C Gross wt 103.8216 g

Date and time of wt Gross wt g

Average gross wt 103.8218 g

Tare wt 103.8192 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0026 g

Total weight of particulate (m_n) 0.0041 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No. 100[illegible]

SAMPLE ANALYTICAL FORM

Plant C P Clayton Run number R1-BS2

Sample location Boiler Stack #2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	BS2-M202-1-MC	✓
Aqueous rinse	BS2-M202-1-H2O	✓

Methylene Chloride rinse container number 460

Methylene Chloride rinse volume (V_aw) 225 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/23/92 1400 HRS 3770 Gross wt 108.6703 g

Date and time of wt 4/24/92 0830 3670 Gross wt 108.6701 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 108.6702 g

Tare wt ~~118.6694~~ DKP g 108.6694

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0008 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 462

Aqueous rinse volume (V w) 225 + 140 + 40 → 405 mL ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/28/92 0830 3970 Gross wt 107.5542 g

Date and time of wt 4/28/92 1600 Gross wt 107.5539 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 107.5541 g

Tare wt 107.5515 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0026 g

Total weight of particulate (m_n) 0.0034 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP-Clayton Run number R3-BS1

Sample location Boiler Stack #1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	BS1-M202-3-MCL	✓
Aqueous rinse	BS1-M202-3-H2O	✓

Methylene Chloride rinse container number 429

Methylene Chloride rinse volume ($V_a w$) 200 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 1400HRS 3770 Gross wt 100.0179 g

Date and time of wt 4/24/92 0830 3770 Gross wt 100.0176 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 100.0178 g

Tare wt 100.0163 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0015 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 9

Aqueous rinse volume (V w) 200 + 120 + 85 = 405 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0832 3970 Gross wt 113.2071 g

Date and time of wt 4/28/92 1600 Gross wt 113.2071 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 113.2071 g

Tare wt 113.2041 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0030 g

Total weight of particulate (m_n) 0.0045 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No. L0[illegible]

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 2 BS1

Sample location Boiler Stack #1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	BS1 - M202-2-MeCl2	✓
Aqueous rinse	BS1 - M202-2-H2O	✓

Methylene Chloride rinse container number 420

Methylene Chloride rinse volume ($V_a w$) 240 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 Gross wt 102.6755 g

Date and time of wt 4/23/92 1400 Gross wt 102.6758 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 102.6757 g

Tare wt 102.6677 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0080 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 394

Aqueous rinse volume (V w) 190 + 100 + 160 → 450 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 3670 Gross wt 103.9930 g

Date and time of wt 4/27/92 0830 3470 Gross wt 103.9922 g

Date and time of wt 4/27/92 1600 3470 Gross wt 103.9915 g

Date and time of wt 4/28/92 0830 3970 Gross wt 103.9928 g

4/28/92 1600 Average gross wt 103.9923 g

103.9920

Tare wt 103.9083 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0840 g

Total weight of particulate (m_n) 0.0920 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP - Clayton Run number Run 1 BS1

Sample location Boiler Stack #1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	BS1 - M202 - 1 - MCL	✓
Aqueous rinse	BS1 - M202 - 1 - H2O	✓

Methylene Chloride rinse container number 464

Methylene Chloride rinse volume (V_w) 180 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/23/92 0850 Gross wt 100.3323 g

Date and time of wt 4/23/92 1400 Gross wt 100.3326 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 100.3325 g

Tare wt 100.3302 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0023 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 377

Aqueous rinse volume (V_w) 220 + 120 + 150 → 490 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 367o RH Gross wt 103.8167 g

Date and time of wt 4/27/92 0830 347o Gross wt 103.8158 g

Date and time of wt 4/27/92 1600 347o Gross wt 103.8156 g

Date and time of wt Gross wt g

Average gross wt 103.8157 g

Tare wt 103.8134 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0023 g

Total weight of particulate (m_n) 0.0046 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Pesak

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number R-3

Sample location Stack 1 Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS1 M202-3-MCL	yes
Aqueous rinse	DS1 M202-3-H20	yes

Methylene Chloride rinse container number 512

Methylene Chloride rinse volume (V_aw) 120 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 3470 Gross wt 106.4910 g

Date and time of wt 4/27/92 0830 3470 Gross wt 106.4889 g

Date and time of wt 4/27/92 1600 3470 Gross wt 106.4887 g

Date and time of wt Gross wt g

Average gross wt 106.4888 g

Tare wt 106.4849 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0039 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 477

Aqueous rinse volume (V w) 360 ml

Aqueous blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/29/92 0830 3170 Gross wt 105.8667 g

Date and time of wt 4/29/92 1445 3170 Gross wt 105.8669 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.8668 g

Tare wt 105.8620 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) .0048 g

Total weight of particulate (m_n) 0.0087 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna Parrish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number R-2

Sample location Stack 1 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DSI M202-2 MCL	yes
Aqueous rinse	DSI M202-2 H_2O	yes

Methylene Chloride rinse container number 468

Methylene Chloride rinse volume ($V_a w$) 50 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 3470 Gross wt 109.4042 g

Date and time of wt 4/27/92 0830 3470 Gross wt 109.4021 g

Date and time of wt 4/27/92 1600 3470 Gross wt 109.4021 g

Date and time of wt Gross wt g

Average gross wt 109.4021 g

Tare wt 109.3941 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0080 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 493

Aqueous rinse volume (V_w) 360 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 106.1934 g

Date and time of wt 4/30/92 1415 Gross wt 106.1939 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 106.1937 g

Tare wt 106.1919 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0018 g

Total weight of particulate (m_n) 0.0098 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number _____

Sample location _____

Relative humidity _____

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DSI M202-1 MCL	yes
Aqueous rinse	DSI M202-1-H2O	yes

Methylene Chloride rinse container number 515

Methylene Chloride rinse volume ($V_a w$) 60 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/24/92 1300 3670 Gross wt 106.2187 g

Date and time of wt 4/27/92 0830 3470 Gross wt 106.2138 g

Date and time of wt 4/27/92 1600 3470 Gross wt 106.2136 g

Date and time of wt _____ Gross wt _____ g

Average gross wt 106.2137 g

Tare wt 106.2088 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0049 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 487

Aqueous rinse volume ($V_a w$) 470 ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/30/92 0815 Gross wt 102.6514 g

Date and time of wt 4/30/92 1415 Gross wt 102.6517 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 102.6516 g

Tare wt 102.6488 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0028 g

Total weight of particulate (m_n) 0.0077 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks _____

Signature of analyst Donna K Parrish

Signature of reviewer _____

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant L. P. Clayton Run number R-3

Sample location Stack 2 Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS2-M202-3-MCL	yes
Aqueous rinse	DS2-M202-3-H2O	yes

Methylene Chloride rinse container number 478

Methylene Chloride rinse volume ($V_a w$) 100 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 104.1836 g

Date and time of wt 4/28/92 1600 Gross wt 104.1832 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.1834 g

Tare wt 104.1751 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0083 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 469

Aqueous rinse volume ($V_a w$) 370 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 107.5901 g

Date and time of wt 4/30/92 1415 Gross wt 107.5902 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.5902 g

Tare wt 107.5848 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0054 g

Total weight of particulate (m_n) 0.0137 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number R-2

Sample location Stack 2 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS2-M202-2MCL	yes
Aqueous rinse	DS2 M202-2 H2O	yes

Methylene Chloride rinse container number 508

Methylene Chloride rinse volume ($V_a w$) 80 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 3670 Gross wt 103.0767 g

Date and time of wt 4/27/92 0830 3470 Gross wt 103.0706 g

Date and time of wt 4/27/92 1600 3470 Gross wt 103.0701 g

Date and time of wt Gross wt g

Average gross wt 103.0704 g

Tare wt 103.0612 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0092 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 513

Aqueous rinse volume (V w) 480 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 104.7655 g

Date and time of wt 4/30/92 1415 Gross wt 104.7660 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.7658 g

Tare wt 104.7605 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0053 g

Total weight of particulate (m_n) 0.0145 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dianne K Parrish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number R-1

Sample location Stack 2 Run 1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS2M202-1MCL	yes
Aqueous rinse	DS2M202-1 H2O	yes

Methylene Chloride rinse container number 498

Methylene Chloride rinse volume ($V_a w$) 75 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 367o Gross wt 104.9670 g

Date and time of wt 4/27/92 0830 347o Gross wt 104.9614 g

Date and time of wt 4/27/92 1600 347o Gross wt 104.9609 g

Date and time of wt Gross wt g

Average gross wt 104.9612 g

Tare wt 104.9540 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0072 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 490

Aqueous rinse volume ($V_a w$) 360 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 337o Gross wt 109.1624 g

Date and time of wt 4/30/92 1415 Gross wt 109.1628 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 109.1626 g

Tare wt 109.16202 g DKP

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0006 g

Total weight of particulate (m_n) 0.0078 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number R-1

Sample location Stack 3 Run 1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS3M2021 MCL	yes
Aqueous rinse	DS3M2021 H2O	yes

Methylene Chloride rinse container number 506

Methylene Chloride rinse volume ($V_a w$) 75 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 5670 Gross wt 106.3557 g

Date and time of wt 4/27/92 0830 3470 Gross wt 106.3520 g

Date and time of wt 4/27/92 1600 3470 Gross wt 106.3516 g

Date and time of wt Gross wt g

Average gross wt 106.3518 g

Tare wt 106.3450 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0068 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 499

Aqueous rinse volume (V_w) 480mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 107.5646 g

Date and time of wt 4/30/92 1415 Gross wt 107.5651 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.5649 g

Tare wt 107.5617 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0032 g

Total weight of particulate (m_n) 0.0100 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

SAMPLE ANALYTICAL FORM

Control No. 100.35

Plant i P Clayton Run number

Sample location Stack 6 Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	P56 - M202-3MCL	yes
Aqueous rinse	D56 - M202-3 H2O	yes

Methylene Chloride rinse container number 503

Methylene Chloride rinse volume ($V_a w$) 150 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 5970 Gross wt 103.0550 g

Date and time of wt 4/28/92 1600 Gross wt 103.0548 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 103.0549 g

Tare wt 103.0460 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0089 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 502

Aqueous rinse volume (V w) 460 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 103.8518 g

Date and time of wt 5/1/92 1415 Gross wt 103 8513 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 103.8514 g

Tare wt 103.8414 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0100 g

Total weight of particulate (m_n) 0.0189 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Pennish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number Run 1

Sample location Stack 4 Run 1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS4 M202-1 MCL	yes
Aqueous rinse	DS4 M202-1 H2O	yes

Methylene Chloride rinse container number 485

Methylene Chloride rinse volume ($V_a w$) 95 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 39% Gross wt 105.0053 g

Date and time of wt 4/28/92 1600 Gross wt 105.0057 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.0055 g

Tare wt 104.9954 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0101 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 489

Aqueous rinse volume (V w) 460 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 104.9173 g

Date and time of wt 4/30/92 1415 Gross wt 104.9178 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.9176 g

Tare wt 104.9120 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0056 g

Total weight of particulate (m_n) 0.0157 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dianne K Parrish

Signature of reviewer

Control No. 100[illegible]

SAMPLE ANALYTICAL FORM

Plant L.P. Clayton Run number R-2

Sample location Stack 4 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS4M202-2-MCl	yes
Aqueous rinse	DS4M202-2 H2O	yes

Methylene Chloride rinse container number 476

Methylene Chloride rinse volume ($V_a w$) 110 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 106.8327 g

Date and time of wt 4/28/92 1600 Gross wt 106.8327 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 106.8327 g

Tare wt 106.8218 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0109 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 483

Aqueous rinse volume (V w) 110 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 105.7403 g

Date and time of wt 4/30/92 1415 Gross wt 105.7406 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.7405 g

Tare wt 105.7350 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0055 g

Total weight of particulate (m_n) 0.0164 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dianne K Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number _____

Sample location Stack 6 Run 2

Relative humidity _____

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS6-M202-2-MC	yes
Aqueous rinse	DS6-M202-2 H_2O	yes

Methylene Chloride rinse container number 475

Methylene Chloride rinse volume ($V_a w$) 130 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/28/92 0830 39% Gross wt 103.9758 g

Date and time of wt 4/28/92 1600 Gross wt 103.9756 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 103.9757 g

Tare wt 103.9632 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0125 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 488

Aqueous rinse volume (V w) 370 ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 5/4/92 0830 42% Gross wt 105.7780 g

Date and time of wt 5/4/92 1600 35% Gross wt 105.7781 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 105.7781 g

Tare wt 105.7737 g

Less aqueous blank wt (W_a) _____ g

Weight of particulate in aqueous rinse (m_a) _____ g

Total weight of particulate (m_n) _____ g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks _____

Signature of analyst _____

Signature of reviewer _____

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant L. P. Clayton Run number R-2

Sample location Stack 3 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS3-M202-2MCL	yes
Aqueous rinse	DS3-M202-2H2O	yes

Methylene Chloride rinse container number 500

Methylene Chloride rinse volume ($V_a w$) 120 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/24/92 1300 3470 Gross wt 103.7433 g

Date and time of wt 4/27/92 0830 3470 Gross wt 103.7408 g

Date and time of wt 4/27/92 1600 3470 Gross wt 103.7405 g

Date and time of wt Gross wt g

Average gross wt 103.7407 g

Tare wt 103.7360 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0047 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 470

Aqueous rinse volume (V w) 420 ml ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 105.1006 g

Date and time of wt 4/30/92 1415 Gross wt 105.1011 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.1009 g

Tare wt 105.0955 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0054 g

Total weight of particulate (m_n) 0.0101 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number _____

Sample location Press Vent 8 Run 3

Relative humidity _____

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	P V8 - M202 - 3 MU	yes
Aqueous rinse	PV8 - M202 - 3 H2O	yes

Methylene Chloride rinse container number 480

Methylene Chloride rinse volume ($V_a w$) 110 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/28/92 0830 3970 Gross wt 106.0379 g

Date and time of wt 4/28/92 1600 Gross wt 106.0375 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 106.0377 g

Tare wt 106.0369 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0008 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 494

Aqueous rinse volume (V w) 440 ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 5/1/92 0815 Gross wt 111.3749 g

Date and time of wt 5/1/92 1415 Gross wt 111.3748 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 111.3749 g

Tare wt 111.3728 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0021 g

Total weight of particulate (m_n) 0.0029 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks _____

Signature of analyst Denise K Parrish

Signature of reviewer _____

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number _____

Sample location Stack 6 Run 1

Relative humidity _____

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DSG M202-1 MCL	yes
Aqueous rinse	DSG M202-1 H2O	yes

Methylene Chloride rinse container number 517

Methylene Chloride rinse volume ($V_a w$) 150 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/28/92 0830 39% Gross wt 107.0002 g

Date and time of wt 4/28/92 1600 Gross wt 107.0002 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 107.0002 g

Tare wt 106.9852 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0150 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 501

Aqueous rinse volume ($V_a w$) 385 ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 5/1/92 0815 Gross wt 105.1196 g

Date and time of wt 5/1/92 1415 Gross wt 105.1196 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 105.1196 g

Tare wt 105.1130 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0066 g

Total weight of particulate (m_n) 0.0216 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks _____

Signature of analyst Donna K Parnell

Signature of reviewer _____

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number

Sample location Press Vent 9 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV9-M202-2MCL	yes
Aqueous rinse	PV9-M202-2H2O	yes

Methylene Chloride rinse container number 481

Methylene Chloride rinse volume ($V_a w$) 110 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 39% Gross wt 109.5548 g

Date and time of wt 4/28/92 1600 Gross wt 109.5550 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 109.5549 g

Tare wt 109.5551 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) ~~0.002~~ 0.0002 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 482

Aqueous rinse volume ($V_a w$) 470 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 105.5515 g

Date and time of wt 4/30/92 1415 Gross wt 105.5518 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.5517 g

Tare wt 105.5496 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0021 g

Total weight of particulate (m_n) 0.0019 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No. 10041

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number

Sample location Press Vent #10 Run #2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV10-M202-2MCL	yes
Aqueous rinse	PV10-M202-2H2O	yes

Methylene Chloride rinse container number 492

Methylene Chloride rinse volume ($V_a w$) 80 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 107.2307 g

Date and time of wt 4/28/92 1600 Gross wt 107.2307 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.2307 g

Tare wt 107.2314 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) -0.0007 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 526

Aqueous rinse volume (V w) 430 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/30/92 0815 Gross wt 105.8037 g

Date and time of wt 4/30/92 1415 Gross wt 105.8044 g

Date and time of wt 5/1/92 0815 Gross wt 105.8038 g

Date and time of wt 5/1/92 1415 Gross wt 105.8041 g

Average gross wt 105.8040 g

Tare wt 105.8027 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0013 g

Total weight of particulate (m_n) 0.0006 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K. Parrish

Signature of reviewer

Control No. 100[illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number

Sample location Press Vent 10 Run #1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV10-M202-1MCL	yes
Aqueous rinse	PV10-M202-1H2O	yes

Methylene Chloride rinse container number 467

Methylene Chloride rinse volume ($V_a w$) 120 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 105.6451 g

Date and time of wt 4/28/92 1600 Gross wt 105.6455 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.6453 g

Tare wt 105.6462 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) -0.0009 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 524

Aqueous rinse volume ($V_a w$) 420 mL ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 105.9319 g

Date and time of wt 5/1/92 1415 Gross wt 105.9324 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.9322 g

Tare wt 105.9312 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0010 g

Total weight of particulate (m_n) 0.0001 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No. 10049

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number

Sample location Press Vent 9 Run #1

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV9-M202-1MCL	yes
Aqueous rinse	PV9-M202-1H2O	yes

Methylene Chloride rinse container number 522

Methylene Chloride rinse volume (V_aw) 90 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 3970 Gross wt 104.6742 g

Date and time of wt 4/28/92 1400 Gross wt 104.6631 g

Date and time of wt 4/29/92 0830 3170 Gross wt 104.6628 g

Date and time of wt Gross wt g

Average gross wt 104.6630 g

Tare wt 104.6632 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) -0.0002 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 509

Aqueous rinse volume (Vw) 350 ml

Aqueous blank residue concentration (C) ml

$W_a = C_aV_aw$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 108.7720 g

Date and time of wt 5/1/92 1415 Gross wt 108.7723 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 108.7722 g

Tare wt 108.7708 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0014 g

Total weight of particulate (m_n) 0.0012 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Dianne K Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number

Sample location Press Vent 9 Run # 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV9-M202-3MCL	yes
Aqueous rinse	PV9-M202-3H2O	yes

Methylene Chloride rinse container number 484

Methylene Chloride rinse volume ($V_a w$) 70 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0330 3970 Gross wt 105.5330 g

Date and time of wt 4/28/92 1600 Gross wt 105.5332 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 105.5331 g

Tare wt 105.5329 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0002 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 521

Aqueous rinse volume ($V_a w$) 340 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 103.7581 g

Date and time of wt 5/1/92 1415 Gross wt 103.7585 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 103.7583 g

Tare wt 103.7578 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0005 g

Total weight of particulate (m_n) 0.0007 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number

Sample location Press Vent 10 Run #3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	PV10-M202-3MCL	yes
Aqueous rinse	PV10-M202-3H2O	yes

Methylene Chloride rinse container number 495

Methylene Chloride rinse volume ($V_a w$) 95 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 0830 39% Gross wt 107.2807 g

Date and time of wt 4/28/92 1600 Gross wt 107.2812 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.2810 g

Tare wt 107.2787 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0023 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 473

Aqueous rinse volume (V_w) ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/4/92 0830 42% Gross wt 107.2165 g

Date and time of wt 5/4/92 1600 35% Gross wt 107.2168 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.2167 g

Tare wt 107.2135 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) g

Total weight of particulate (m_n) g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number R-3

Sample location Stack 8 Run 3

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS8-M202-3MCL	✓
Aqueous rinse	DS8-M202-3 H_2O	✓

Methylene Chloride rinse container number 486

Methylene Chloride rinse volume ($V_a w$) 125 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 4/28/92 1600 Gross wt 106.0693 g

Date and time of wt 4/29/92 0830 3170 Gross wt 106.0682 g

Date and time of wt 4/29/92 1445 3170 Gross wt 106.0681 g

Date and time of wt Gross wt g

Average gross wt 106.0682 g

Tare wt 106.0633 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0049 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 471

Aqueous rinse volume (V w) 345 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 107.9293 g

Date and time of wt 5/1/92 1415 Gross wt 107.9296 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 107.9295 g

Tare wt 107.9245 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0050 g

Total weight of particulate (m_n) 0.0099 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K Parrish

Signature of reviewer

Control No.

SAMPLE ANALYTICAL FORM

Plant L. P. Clayton Run number R-2

Sample location Stack 8 Run 2

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS8 M202-2 MCL	✓
Aqueous rinse	DS8 M202-2 H2O	✓

Methylene Chloride rinse container number 520

Methylene Chloride rinse volume ($V_a w$) 95 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = 1 g

Date and time of wt 4/28/92 0830 3970 Gross wt 104.8525 g

Date and time of wt 4/28/92 1400 Gross wt 104.8525 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 104.8525 g

Tare wt 104.8482 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0043 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 474

Aqueous rinse volume ($V_a w$) 330 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 108.4239 g

Date and time of wt 5/1/92 1415 Gross wt 108.4243 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 108.4241 g

Tare wt 108.4137 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0104 g

Total weight of particulate (m_n) 0.0147 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna R Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number R-1

Sample location Stack 8 R4

Relative humidity

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse	DS8 M202-1 MCl	✓
Aqueous rinse	DS8 M202-1 H_2O	✓

Methylene Chloride rinse container number 491

Methylene Chloride rinse volume ($V_a w$) 140 ml

Methylene Chloride blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 106.8488 g

Date and time of wt 5/1/92 1415 Gross wt 106.8490 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 106.8489 g

Tare wt 106.8457 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) 0.0032 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 523

Aqueous rinse volume (V w) 300 ml

Aqueous blank residue concentration (C) ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = g

Date and time of wt 5/1/92 0815 Gross wt 103.2506 g

Date and time of wt 5/1/92 1415 Gross wt 103.2507 g

Date and time of wt Gross wt g

Date and time of wt Gross wt g

Average gross wt 103.2507 g

Tare wt 103.2458 g

Less aqueous blank wt (W_a) 0.0 g

Weight of particulate in aqueous rinse (m_a) 0.0049 g

Total weight of particulate (m_n) 0.0081 g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks

Signature of analyst Donna K. Parrish

Signature of reviewer

Control No. [illegible]

SAMPLE ANALYTICAL FORM

Plant LP Clayton Run number _____

Sample location BLANK H_2O

Relative humidity _____

Sample type	Sample identifiable	Liquid level marked and/or container sealed
Methylene Chloride rinse		
Aqueous rinse		

Methylene Chloride rinse container number 570

Methylene Chloride rinse volume ($V_a w$) 150 ml

Methylene Chloride blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 4/28/92 0830 3970 Gross wt 103.6118 g

Date and time of wt 4/28/92 1600 Gross wt 103.6119 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt _____ g

Average gross wt 103.6119 g

Tare wt 103.6122 g

Less Methylene Chloride blank wt (W_a) 0.0 g

Weight of particulate in Methylene Chloride rinse (m_a) -0.0003 g

Note: In no case should a blank residue >0.01 mg/g or 0.001% of the weight of Methylene Chloride used be subtracted from the sample weight.

Aqueous rinse container number 479

Aqueous rinse volume ($V_a w$) 500 ml

Aqueous blank residue concentration (C) _____ ml

$W_a = C_a V_a w$ = ( ) ( ) ( ) = _____ g

Date and time of wt 5/4/92 0830 4270 Gross wt 109.4847 g

Date and time of wt 5/4/92 1600 3572 Gross wt 109.4851 g

Date and time of wt _____ Gross wt _____ g

Date and time of wt _____ Gross wt 109.4849 g

Average gross wt 109.4849 g

Tare wt _____ g

Less aqueous blank wt (W_a) _____ g

Weight of particulate in aqueous rinse (m_a) _____ g

Total weight of particulate (m_n) _____ g

Note: In no case should a blank residue >1.00 mg/l of the weight of aqueous used be subtracted from the sample weight.

Remarks _____

Signature of analyst _____

Signature of reviewer _____

Control No.

METHOD 5
BLANK ANALYTICAL FORM

Plant LP- Clayton Ala. Run number acetone Blank.
Sample Location
Blank Identification # Acetone Blank. Rinse Breaker # 313
Liquid level marked and container sealed ✓
Blank volume (V_a) 210 ml.
Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 102.1841 g
Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 102.1832 g
Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 102.1836 g
Date/time/RH of wt Gross wt g
Average Gross wt 102.1834 g
Tare wt 102.1833 g
Weight of blank (m_a) 0.0001 g
$C_a = M_a/V_a$ = (0.0001) / (210) = 4.76×10^{-7} g/ml

Note: In no case should a blank residue >0.001 mg/g of the blank weight be subtracted from the sample weight.

Filter(s) identification Filter number F 382
Date/time/RH of wt 4/11/92 - 1130 - 43% RH Gross wt 3.7721 g
Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.7716 g
Date/time/RH of wt Gross wt g
Date/time/RH of wt Gross wt g
Average Gross wt 3.7719 g
Tare wt 3.7718 g
Difference +0.0001 g

Note: Average difference must be less than ± 5 mg or 2% of total sample weight whichever is greater.

Remarks

Signature of analyst: Signature of Reviewer:

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Control No. [illegible]

METHOD 5
BLANK ANALYTICAL FORM

Plant LP- Clayton Run number H_2O Blank
Sample Location
Blank Identification # H_2O Blank Rinse Breaker # 421
Liquid level marked and container sealed ✓
Blank volume (V_a) 200 ml.
Date/time/RH of wt 4/11/92 - 1130 - 43%RH Gross wt 103.8195 g
Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 103.8190 g
Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 103.8193 g
Date/time/RH of wt Gross wt g
Average Gross wt 103.8193 g
Tare wt 103.8131 g
Weight of blank (m_a) .0062 g
$C_a = M_a/V_a$ = (.0062) / (200) = 3.1×10^{-5} g/ml
* Do not subtract from sample wt.

Note: In no case should a blank residue >0.001 mg/g of the blank weight be subtracted from the sample weight.

Filter(s) identification Filter number F381
Date/time/RH of wt 4/11/92 - 1130 - 43%RH Gross wt 3.8237 g
Date/time/RH of wt 4/13/92 - 0930 - 36% RH Gross wt 3.8234 g
Date/time/RH of wt Gross wt g
Date/time/RH of wt Gross wt g
Average Gross wt 3.8236 g
Tare wt 3.8236 g
Difference 0 g

Note: Average difference must be less than ± 5 mg or 2% of total sample weight whichever is greater.

Remarks

Signature of analyst: Dianne Parrish

Signature of Reviewer:

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Control No.

METHOD 5
BLANK ANALYTICAL FORM

Plant LP- Clayton Run number MeCl2 Blank

Sample Location

Blank Identification # methylen chloride Blank Rinse Breaker # 419

Liquid level marked and container sealed

Blank volume (V_a) 200 ml.

Date/time/RH of wt 4/11/92 - 0930 - 41% RH Gross wt 103.3560 g

Date/time/RH of wt 4/13/92 - 1130 - 34% RH Gross wt 103.3560 g

Date/time/RH of wt 4/15/92 - 1330 - 30% RH Gross wt 103.3564 g

Date/time/RH of wt Gross wt g

Average Gross wt 103.3560 g

Tare wt 103.3490 g

Weight of blank (m_a) 0.0070 g

$C_a = M_a/V_a$ = (0.0070) / (200) = 3.5×10^{-5} g/ml

* Do not subtract from sample wt.

Note: In no case should a blank residue >0.001 mg/g of the blank weight be subtracted from the sample weight.

PM10 Blank filters

Filter(s) identification Q049 & Q050 Filter number Q049 / Q050

Date/time/RH of wt 4/13/92 - 1300 - 32% RH Gross wt .1790 / .1780 g

Date/time/RH of wt 4/15/92 - 1300 - 30% RH Gross wt .1794 / .1772 g

Date/time/RH of wt 4/24/92 - 0830 - 36% RH Gross wt DKP ~~.1792~~ / .1769 g

Date/time/RH of wt Gross wt g

Average Gross wt .1792 / .1771 g

Tare wt ~~.4069~~ 0.1791 / ~~.4145~~ 0.1776 DKP g

Difference 0.0001 / 0.0005 g

Note: Average difference must be less than ± 5 mg or 2% of total sample weight whichever is greater.

Remarks

Signature of analyst: Donna Parrish

Signature of Reviewer:

c:\airdiv\form\b-analyt.frm

Analyst: B. RAYFIELD Balance I.D.: METTLER L58883

Client Name: LOUISIANA-PACIFIC Location(s):

Humidity %'s:	30%	28%			
Filter I.D.:	1 3/7/92 17:10	2 3/8/92 6:30	3	4	AVERAGE:
62Q001	0.1851	0.1851			
62Q002	0.1859	0.1860			
62Q003	0.1856	0.1856			
62Q004	0.1862	0.1861			0.1862
62Q005	0.1860	0.1860			0.1860
62Q006	0.1858	0.1858			0.1858
62Q007	0.1857	0.1857			
62Q008	0.1860	0.1860			
62Q009	0.1838	0.1839			
62Q010	0.1855	0.1854			
62Q011	0.1787	0.1787			
62Q012	0.1788	0.1787			
62Q013	0.1777	0.1778			
62Q014	0.1782	0.1782			
62Q015	0.1785	0.1786			
62Q016	0.1764	0.1764			
62Q017	0.1795	0.1795			
62Q018	0.1800	0.1799			
62Q019	0.1796	0.1796			
62Q020	0.1788	0.1788			
62Q021	0.1776	0.1776			
62Q022	0.1791	0.1790			
62Q023	0.1814	0.1813			
62Q024	0.1815	0.1815			
62Q025	0.1814	0.1817			

Include date of each tare in columns numbered 1 through 4. The average value is the mean of two consecutive weighings that agree within 0.5 milligrams (0.0005 grams).

Analyst: J. SOKASH Balance I.D.: METTLER L58883

Client Name: LOUISIANA-PACIFIC Location(s):

Humidity %'s:	18%	18%			
Filter I.D.:	1 2/5/92 14:30	2 2/6/92 9:30	3	4	AVERAGE:
F331	3.8021	3.8020			3.8021
F332	3.7909	3.7908			3.7909
F333	3.8144	3.8143			3.8144
F334	3.7806	3.7806			3.7806
F335	3.8065	3.8065			3.8065
F336	3.7715	3.7716			3.7716
F337	3.8092	3.8092			3.8092
F338	3.7752	3.7752			3.7752
F339	3.8096	3.8095			3.8096
F340	3.7650	3.7651			3.7651
F341	3.7985	3.7986			3.7986
F342	3.7657	3.7655			3.7656
F343	3.8333	3.8334			3.8334
F344	3.7750	3.7750			3.7750
F345	3.8222	3.8222			3.8222
F346	3.7780	3.7781			3.7780
F347	3.8351	3.8351			3.8351
F348	3.7785	3.7786			3.7786
F349	3.7814	3.7814			3.7814
F350	3.8452	3.8452			3.8452
F351	3.8325	3.8325			3.8325
F352	3.7863	3.7863			3.7863
F353	3.8284	3.8285			3.8285
F354	3.7970	3.7970			3.7970
F355	3.8264	3.8264			3.8264

Include date of each tare in columns numbered 1 through 4. The average value is the mean of two consecutive weighings that agree within 0.5 milligrams (0.0005 grams).

Analyst: J. SOKASH Balance I.D.: METTLER L58883

Client Name: LOUISIANA - PACIFIC Location(s):

Humidity %'s:	18%	18%			
Filter I.D.:	1 2/5/92 14:30	2 2/6/92 9:40	3	4	AVERAGE:
F356	3.8037	3.8038			3.8038
F357	3.8090	3.8092			3.8091
F358	3.8121	3.8124			3.8123
F359	3.8330	3.8332			3.8331
F360	3.8208	3.8209			3.8209
F361	3.7894	3.7897			3.7896
F362	3.8072	3.8073			3.8073
F363	3.7898	3.7900			3.7899
F364	3.7978	3.7978			3.7978
F365	3.7913	3.7913			3.7913
F366	3.8097	3.8099			3.8098
F367	3.7967	3.7968			3.7968
F368	3.7778	3.7781			3.7779
F369	3.8039	3.8042 BR			3.8041
F370	3.7895	3.7897			3.7896
F371	3.8102	3.8105			3.8104
F372	3.8047	3.8050			3.8049
F373	3.8072	3.8075			3.8074
F374	3.7704	3.7702			3.7703
F375	3.8048	3.8049			3.8049
F376	3.7718	3.7716			3.7717
F377	3.8034	3.8033			3.8034
F378	3.7628	3.7627			3.7628
F379	3.7987	3.7987			3.7987
F380	3.7780	3.7780			3.7780

Include date of each tare in columns numbered 1 through 4. The average value is the mean of two consecutive weighings that agree within 0.5 milligrams (0.0005 grams).

Analyst: J. SOKASH Balance I.D.: METTLER L58883

Client Name: LOUISIANA-PACIFIC Location(s):

Humidity %'s:	18%	20%			
Filter I. D.:	1 2/5/92 14:00	2 2/6/92 10:20	3	4	AVERAGE:
F381	3.8235	3.8236			3.8236
F382	3.7717	3.7719			3.7718
~~F383~~					
F383	3.8259	3.8260			3.8260
F384	3.7600	3.7600			3.7600
F385	3.8108	3.8110			3.8109
F386	3.7806	3.7804			3.7805
F387	3.8232	3.8232			3.8232
F388	3.7739	3.7741			3.7740
F389	3.8122	3.8125			3.8124
F390	3.7763	3.7764			3.7764
F391	3.8014	3.8016			3.8015
F392	3.7761	3.7761			3.7761
F393	3.8051	3.8053			3.8052
F394	3.7775	3.7776			3.7776
F395	3.8137	3.8139			3.8138
F396	3.7745	3.7748			3.7747
F397	3.8100	3.8103			3.8102
F398	3.7816	3.7818			3.7817
F399	3.8206	3.8210			3.8208
F400	3.7862	3.7865			3.7864

Include date of each tare in columns numbered 1 through 4. The average value is the mean of two consecutive weighings that agree within 0.5 milligrams (0.0005 grams).

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25744

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449-001	Louisiana Pacific - Clayton

SAMPLERS: *(SIGNATURE)*

~~SAMPLE~~ BOX I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS: 0011a
3	~~3/19~~ 3/20				Blank 3-20-92	1			X
3	3/21				Blank 3-21-92	1			X
10	3/21				DS3-HCHO-1-DNPH	1			X
10	3/21				DS3-HCHO-2-DNPH	1			X
	~~3/21~~				~~DS3-HCHO-3-DNPH~~				~~X~~
10	3/21				DS4-HCHO-1-DNPH	1			X
3	3/21				DS4-HCHO-2-DNPH	1			X
10	3/21				DS6-HCHO-3-DNPH	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
[signature]	3/25/92		Jimmy Pan	3/25/92	
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

iea

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25795

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449-001	LOUISIANA PACIFIC

SAMPLERS: *(SIGNATURE)*

~~SAMPLE~~ BOX I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS: 0011A
11	3/20/92				DS8-HCHO-1-DNPH	1			X
11	3/20/92				DS8-HCHO-2-DNPH	1			X
11	3/20/92				DS8-HCHO-3-DNPH	1			X

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
B Rayfield	3/25/92		Jimmy C. Paul	3/25/92	
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

NO: 20034

PROJECT #	PROJECT NAME
1449-001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

BOX

~~SAMPLE~~ I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS: DO11a
8	3/17				PV9-HCHO-1-DNPH	1			X
7	3/17				PV9-HCHO-2-DNPH	1			X
7	3/17				PV9-HCHO-3-DNPH	1			X
7	3/17				PV10-HCHO-1-DNPH	1			X
7	3/17				PV10-HCHO-2-DNPH	1			X
7	3/17				PV10-HCHO-3-DNPH	1			X
2	3/13				PV11-HCHO-1-DNPH	1			X
2	3/13				PV11-HCHO-2-DNPH	1			X
2	3/13				PV11-HCHO-3-DNPH	1			X
5	3/19				Blank 3/19	1			X
5	3/19				DS1-HCHO-1-DNPH	1			X

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
[signature]	3/25/92		Jimmy C. Pau	3/25/92	
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

iea an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 20048

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT # 1449-001

PROJECT NAME Louisiana Pacific

SAMPLERS: (SIGNATURE)

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS 8011a
6	3/17				Blank 3-17-92	1			X
6	3/14				Blank 2 - HCHO-6-DNPH	1			X
9	3/20				DS6-HCHO-1-DNPH	1			X
6	3/20				DS6-HCHO-2-DNPH	1			X
6	3/19				DS2-HCHO-1-DNPH	1			X
9	3/19				DS2-HCHO-2-DNPH	1			X
6	3/19				DS2-HCHO-3-DNPH	1			X
9	3/19				DS1-HCHO-2A-DNPH	1			X
9	3/19				DS1-HCHO-2B-DNPH	1			X
9	3/19				DS1-HCHO-3A-DNPH	1			X
3	3/19				DS1-HCHO-3B-DNPH	1			X

RELINQUISHED BY (SIGNATURE)	DATE	TIME	RECEIVED BY	DATE	TIME
[signature]	3/25/92		Jimmy C. Pau	3/25/92	
RELINQUISHED BY (SIGNATURE)	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	P.O. NO.

IEA REMARKS

Dryer Stack #1 (DS1) Runs 2 + 3 have 2 bottles

FIELD REMARKS

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 20035

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449-001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

~~SAMPLE~~ BOX I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS 8011a											
4	3/14				PV6-HCHO-1-DNPH	1			X											
4	3/14				PV6-HCHO-2-DNPH	1			X											
4	3/14				PV6-HCHO-3-DNPH	1			X											
4	3/16				PV7-HCHO-1-DNPH	1			X											
4	3/16				PV7-HCHO-2-DNPH	1			X											
8	3/16				PV7-HCHO-3-DNPH	1			X											
8	3/16				PV8-HCHO-1-DNPH	1			X											
8	3/16				PV8-HCHO-2-DNPH	1			X											
8	3/16				PV8-HCHO-3-DNPH	1			X											
5	3/13				Blank-1-HCHO-1-DNPH	1			X											
2	3/16				Blank-3-HCHO-1-DNPH	1			X											

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME	IEA QUOTE NO.	IEA RUSH NO.
[signature]	3/23/92		Jimmy C. Paul				
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**	**PROJECT MANAGER (PLEASE PRINT)**	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

iea

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

NO: 20036

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

BX

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS 0811a
1	3/12				PV3-HCHO-1-DNPH	1			X
1	3/12				PV3-HCHO-2-DNPH	1			X
1	3/12				PV3-HCHO-3-DNPH	1			X
1	3/11				PV4-HCHO-1-DNPH	1			X
1	3/11				PV4-HCHO-2-DNPH	1			X
1	3/11				PV4-HCHO-3-DNPH	1			X
1	3/11				PV5-HCHO-1-DNPH	1			X
1	3/11				PV5-HCHO-2-DNPH	1			X
1	3/11				PV5-HCHO-3-DNPH	1			X
5	3/12				Blank 3/12	1			X
1	3/15				Blank 3/15	1			X

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
[signature]	3/25/92		Jimmy C. Pay	3/25/92	
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25770

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				DS2-m5-3-FH	1			
F 346					DS3-m5-1-PF	1			
					DS3-m5-1-FH	1			
F 347					DS3-m5-2-PF	1			
					DS3-m5-2-FH	1			
F 348					DS4-m5-1-PF	1			
					DS4-m5-1-FH	1			
F 349					DS4-m5-2-PF	1			
					DS4-m5-2-FH	1			
F 334					DS6-m5-1-PF	1			
					DS6-m5-1-FH	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Moh	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			[illegible]	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

(2)

iea an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25771

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT # 1449,001

PROJECT NAME Louisiana Pacific

SAMPLERS: (SIGNATURE)

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
F335	3/20/92				DS6-m5-2-PF	1			
					DS6-m5-2-FH	1			
F336					DS6-m5-3-PF	1			
					DS6-m5-3-FH	1			
F331					DS8-m5-1-PF	1			
					DS8-m5-1-FH	1			
F332					DS8-m5-2-PF	1			
					DS8-m5-2-FH	1			
F333					DS8-m5-3-PF	1			
					DS8-m5-3-FH	1			

RELINQUISHED BY (SIGNATURE)	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Mah	3/20/92				
RELINQUISHED BY (SIGNATURE)	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			[illegible]	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	P.O. NO.

IEA REMARKS

FIELD REMARKS

3

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25766

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449-001	LOUISIANA PACIFIC

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
F340	3/20/92				DS1-M5-1-PF				
					DS1-M5-1-FH				
F342					DS1-M5-2-PF				
					DS1-M5-2-FH				
F341					DS1-M5-3-PF				
					DS1-M5-3-FH				
F343					DS2-M5-1-PF				
					DS2-M5-1-FH				
F344					DS2-M5-2-PF				
					DS2-M5-1-FH				
F345					DS2-M5-3PF				

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
Thomas E Thompson	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			[illegible]	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

iea

n environmental
esting company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 5776

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				DS2-PM10-3-CYACE	1			
					DS3-PM10-1-PF	1			
					DS3-PM10-1-CYACE	1			
					DS3-PM10-2-PF	1			
					DS3-PM10-2-CYACE	1			
					DS4-PM10-1-PF	1			
					DS4-PM10-1-CYACE	1			
					DS4-PM10-2-PF	1			
					DS4-PM10-2-CYACE	1			
					DS6-PM10-1-PF	1			
					DS6-PM10-1-CYACE	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S Malon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			[illegible]	7/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

5

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25775

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				DS1-PM10-1-PF	1			
					DS1-PM10-1-CYACE	1			
					DS1-PM10-2-PF	1			
					DS1-PM10-2-CYACE	1			
					DS1-PM10-3-PF	1			
					DS1-PM10-3-CYACE	1			
					DS2-PM10-1-PF	1			
					DS2-PM10-1-CYACE	1			
					DS2-PM10-2-PF	1			
					DS2-PM10-2-CYACE	1			
					DS2-PM10-3-PF	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**
			T H Sobieski	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

6

iea an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25772

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				DS1-M202-1-H20	1			
					DS1-M202-1-MCL	1			
					DS1-M202-2-H20	1			
					DS1-M202-2-MCL	1			
					DS1-M202-3-H20	1			
					DS1-M202-3-MCL	1			
					DS2-M202-1-H20	1			
					DS2-M202-1-MCL	1			
					DS2-M202-2-H20	1			
					DS2-M202-2-MCL	1			
					DS2-M202-3-H20	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
[signature]	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			[signature]	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

7

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25773

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				DS2-M202-3-MCL	1			
					DS3-M202-1-H2O	1			
					DS3-M202-1-MCL	1			
					DS3-M202-2-H2O	1			
					DS3-M202-2-MCL	1			
					DS4-M202-1-H2O	1			
					DS4-M202-1-MCL	1			
					DS4-M202-2-H2O	1			
					DS4-M202-2-MCL	1			
					DS6-M202-1-H2O	1			
					DS6-M202-1-MCL	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Melo	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			T A Schaub	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

8

iea an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 5774

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				DS6-M202-2-H2O	1			
					DS6-M202-2-MCL	1			
					DS6-M202-3-H2O	1			
					DS6-M202-3-MCL	1			
					DS8-M202-1-H2O	1			
					DS8-M202-1-MCL	1			
					DS8-M202-2-H2O	1			
					DS8-M202-2-MCL	1			
					DS8-M202-3-H2O	1			
					DS8-M202-3-MCL	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			T A Schank	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

9

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25732

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				BS1-M202-1-H2O	1			
					BS1-M202-1-MCL	1			
					BS1-M202-2-H2O	1			
					BS1-M202-2-MCL	1			
					BS1-M202-3-H2O	1			
					BS1-M202-3-MCL	1			
					BS2-M202-1-H2O	1			
					BS2-M202-1-MCL	1			
					BS2-M202-2-H2O	1			
					BS2-M202-2-MCL	1			
					BS2-M202-3-H2O	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			M Schank	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

10

iea

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25778

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449,001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				BS1-m5-1-PF	1			
					BS1-m5-1-FH	1			
					BS1-m5-2-PF	1			
					BS1-m5-2-FH	1			
					BS1-m5-3-PF	1			
					BS1-m5-3-FH	1			
					BS2-m5-1-PF	1			
					BS2-m5-1-FH	1			
					BS2-m5-2-PF	1			
					BS2-m5-2-FH	1			
					BS2-m5-3-PF	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malan	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			M Sohah	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

11

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25730

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				BS2-M5-3-FH	1			
F337					FE1-M5-1-PF	1			
					FE1-M5-1-FH	1			
F338					FE1-M5-2-PF	1			
					FE1-M5-2-FH	1			
F339					FE1-M5-3-PF	1			
					FE1-M5-3-FH	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S Mah	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			M A Schuch	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

(12)

iea

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25731

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				BS2-M202-3-MCL	1			
					FE1-M202-1-H2O	1			
					FE1-M202-1-MCL	1			
					FE1-M202-2-H2O	1			
					FE1-M202-2-MCL	1			
					FE1-M202-3-H2O	1			
					FE1-M202-3-MCL	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Mala	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			[illegible]	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

13

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25739

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV3-M202-1-H2O	1			
					PV3-M202-1-MCL	1			
					PV3-M202-2-H2O	1			
					PV3-M202-2-MCL	1			
					PV3-M202-3-H2O	1			
					PV3-M202-3-MCL	1			
					PV4-M202-1-H2O	1			
					PV4-M202-1-MCL	1			
					PV4-M202-2-H2O	1			
					PV4-M202-2-MCL	1			
					PV4-M202-3-H2O	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Mahon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**
			T A Schenk	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

14

iea an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25740

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV4-M202-3-MCL	1			
					PV5-M202-1-H20	1			
					PV5-M202-1-MCL	1			
					PV5-M202-2-H20	1			
					PV5-M202-2-MCL	1			
					PV5-M202-3-H20	1			
					PV5-M202-3-MCL	1			
					PV6-M202-1. H20	1			
					PV6-M202-1. MCL	1			
					PV6-M202-2-H20	1			
					PV6-M202-2-MCL	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Mal[illegible]	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			M Schaub	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

15

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25741

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV6-M202-3-H2O	1			
					PV6-M202-3-MCL	1			
					PV7-M202-1-H2O	1			
					PV7-M202-1-MCL	1			
					PV7-M202-2-H2O	1			
					PV7-M202-2-MCL	1			
					PV7-M202-3-H2O	1			
					PV7-M202-3-MCL	1			
					PV8-M202-1-H2O	1			
					PV8-M202-1-MCL	1			
					PV8-M202-2-H2O	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			J. A. Sohash	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

iea

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 5742

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV8-M202-2-MCL	1			
					PV8-M202-3-H20	1			
					PV8-M202-3-MCL	1			
					PV9-M202-1-H20	1			
					PV9-M202-1-MCL	1			
					PV9-M202-2-H20	1			
					PV9-M202-2-MCL	1			
					PV9-M202-3-H20	1			
					PV9-M202-3-MCL	1			
					PV10-M202-1-H20	1			
					PV10-M202-1-MCL	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Mahon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**
			M Sohah	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

17

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25743

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
		3/20/92			PU10-M202-2-H2O	1			
					PU10-M202-2-MCL	1			
					PU10-M202-3-H2O	1			
					PU10-M202-3-MCL	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			J A Schank	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

iea

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25737

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV8-M5-2-FH	1			
					PV8-M5-3-PF	1			
					PV8-M5-3-FH	1			
					PV9-M5-1-PF	1			
					PV9-M5-1-FH	1			
					PV9-M5-2-PF	1			
					PV9-M5-2-FH	1			
					PV9-M5-3-PF	1			
					PV9-M5-3-FH	1			
					PV10-M5-1-PF	1			
					PV10-M5-1-FH	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Maher	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			J H Schenk	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

19

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25738

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV10-M5-2-PF	1			
					PV10-M5-2-FH	1			
					PV10-M5-3-PF	1			
					PV10-M5-3-FH	1			
					BLANK-H20-A	1			
					BLANK-H20-B	1			
					BLANK ACETONE	1			
					DS3-PM10-2-CYACE-B	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malon	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**
			J A Schaub	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

20

iea

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25733

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV3-m5-1-PF	1			
					PV3-m5-1-FH	1			
					PV3-m5-2-PF	1			
					PV3-m5-2-FH	1			
					PV3-m5-3-PF	1			
					PV3-m5-3-FH	1			
					PV4-m5-1-PF	1			
					PV4-m5-1-FH	1			
					PV4-m5-2-PF	1			
					PV4-m5-2-FH	1			
					PV4-m5-3-PF	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Moler	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	**DATE**	**TIME**	**RECEIVED FOR LAB BY**	**DATE**	**TIME**
			VA Solinski	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

21

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25735

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT # 1449.001

PROJECT NAME Louisiana Pacific

SAMPLERS: (SIGNATURE)

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV4-m5-3-FH	1			
					PV5-m5-1-PF	1			
					PV5-m5-1-FH	1			
					PV5-m5-2-PF	1			
					PV5-m5-2-FH	1			
					PV5-m5-3-PF	1			
					PV5-m5-3-FH	1			
					PV6-m5-1-PF	1			
					PV6-m5-1-FH	1			
					PV6-m5-2-PF	1			
					PV6-m5-2-FH	1			

RELINQUISHED BY (SIGNATURE)	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Malon	3/20/92				
RELINQUISHED BY (SIGNATURE)	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			[illegible]	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	P.O. NO.

IEA REMARKS

FIELD REMARKS

22

an environmental testing company
3000 WESTON PKWY.
CARY, N.C. 27513

CHAIN OF CUSTODY RECORD

NO: 25736

REGULATORY CLASSIFICATION - PLEASE SPECIFY

☐ NPDES ☐ DRINKING WATER ☐ RCRA ☐ OTHER _____

PROJECT #	PROJECT NAME
1449.001	Louisiana Pacific

SAMPLERS: *(SIGNATURE)*

SAMPLE I.D.	DATE	TIME	COMP	GRAB	STATION LOCATION	# OF CONTAINERS	MATRIX SOIL	MATRIX WATER	REQUESTED PARAMETERS
	3/20/92				PV6-M5-3-PF	1			
					PV6-M5-3-FH	1			
					PV7-M5-1-PF	1			
					PV7-M5-1-FH	1			
					PV7-M5-2-PF	1			
					PV7-M5-2-FH	1			
					PV7-M5-3-PF	1			
					PV7-M5-3-FH	1			
					PV8-M5-1-PF	1			
					PV8-M5-1-FH	1			
					PV8-M5-2-PF	1			

RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED BY	DATE	TIME
John S. Mola	3/20/92				
RELINQUISHED BY *(SIGNATURE)*	DATE	TIME	RECEIVED FOR LAB BY	DATE	TIME
			J A Schank	3/24	

IEA QUOTE NO.	IEA RUSH NO.
PROJECT MANAGER (PLEASE PRINT)	**P.O. NO.**

IEA REMARKS

FIELD REMARKS

23

APPENDIX H

INSTRUMENT CALIBRATION AND CERTIFICATION DATA

DRY GAS METER INITIAL CALIBRATION

DATE: 3-6-92

CALIBRATOR: MR

METER BOX ID.: M5 DGM SERIAL #: 462147

BAROMETRIC PRESSURE (Pb): 29.97 in. Hg

REFERENCE METER ID: 008759 GAMMA: 1.007

Leak Checks:

Positive (minimum 5 in. H2O) : 0.0

Negative (within 3 in. Hg of absolute) : 0.00 cfm* 27 in. Hg

* Not to exceed 0.005 cfm.

Orifice manometer setting ΔH in. H2O	Volume reference meter Vw ft³	Volume dry gas meter Vd ft³	Temperatures: Reference meter Tw °F	Temperatures: Dry gas meter Td °F	Test duration min	Calibration Factor Y	H@ in. H2O
0.5	stop 159.927	stop 715.205	stop 75	stop 76	17	0.999	1.861
	start 153.350	start 708.579	start 74	start 74			
≥ 5 ft³	diff 6.577	diff 6.626	avg 74.5	avg 75			
1.0	stop 166.039	stop 721.360	stop 75	stop 78	10	0.996	1.896
	start 160.619	start 715.879	start 75	start 76			
≥ 5 ft³	diff 5.415	diff 5.481	avg 75	avg 77			
1.5	stop 172.566	stop 727.965	stop 75	stop 79	9	0.997	1.952
	start 166.692	start 722.016	start 75	start 78			
≥ 10 ft³	diff 5.874	diff 5.949	avg 75	avg 78.5			
2.0	stop 179.708	stop 735.190	stop 75	stop 81	8	0.999	1.974
	start 173.726	start 729.125	start 74	start 79			
≥ 10 ft³	diff 5.982	diff 6.064	avg 74.5	avg 80			
2.5	stop 187.009	stop 742.582	stop 75.5	stop 82	7	1.001	1.899
	start 181.040	start 736.545	start 75	start 81			
≥ 10 ft³	diff 5.969	diff 6.037	avg 75	avg 81.5			
					Average Values	0.998	1.916

Provide calculations of the back side of this page

Y must not deviate by more than +/-0.02 Y.

H@ must not deviate by more than 0.15 in. H2O.

QC Review by: [signature] Date: 3/6/92

DRY GAS METER INITIAL CALIBRATION

DATE: 3-5-92

CALIBRATOR: MR

METER BOX ID.: M-6 DGM SERIAL #: 462141

BAROMETRIC PRESSURE (Pb): 30.08 in. Hg

REFERENCE METER ID: 008759 GAMMA: 1.0073

Leak Checks:

Positive (minimum 5 in. H2O) : _____

Negative (within 3 in. Hg of absolute) : _____ cfm* _____ in. Hg

* Not to exceed 0.005 cfm.

Orifice manometer setting ΔH in. H2O		Volume reference meter Vw ft³	Volume dry gas meter Vd ft³	Temperatures: Reference meter Tw °F	Temperatures: Dry gas meter Td °F	Test duration min	Calibration Factor Y	H@ in. H2O
0.5	stop	55.495	581.886	73	76	13	0.9937	1.843
	start	50.470	576.770	73	76			
≥ 5 ft³	diff	5.025	5.116	73	76			
1.0	stop	60.759	587.246	72	75	9.5	0.9919	1.893
	start	55.640	582.031	72	75			
≥ 5 ft³	diff	5.119	5.215	72	75			
1.5	stop	67.060	593.640	72	78	8	0.9951	1.946
	start	61.862	588.350	72	76			
≥ 10 ft³	diff	5.198	5.290	72	77			
2.0	stop	78.160	604.937	72	80	14	0.9952	1.930
	start	67.626	594.200	72	77			
≥ 10 ft³	diff	10.539	10.737	72	78.5			
2.5	stop	110.155	637.406	74	79	6	0.9934	1.9665
	start	105.141	632.302	74	80			
≥ 10 ft³	diff	5.014	5.104	74	79.5			
						Average Values	0.9939	1.938

Provide calculations of the back side of this page

Y must not deviate by more than +/-0.02 Y.

H@ must not deviate by more than 0.15 in. H2O.

QC Review by: _____ *Date:* _____

DRY GAS METER INITIAL CALIBRATION

DATE: 3/6/92

CALIBRATOR: MR

METER BOX ID.: M-7 DGM SERIAL #: 677163

BAROMETRIC PRESSURE (Pb): 29.97 in. Hg

REFERENCE METER ID: 008759 GAMMA: 1.0073

Leak Checks:

Positive (minimum 5 in. H2O) : 0.0

Negative (within 3 in. Hg of absolute) : 0.00 cfm* 27 in. Hg

* Not to exceed 0.005 cfm.

Orifice manometer setting ΔH in. H2O	Volume reference meter Vw ft³	Volume dry gas meter Vd ft³	Temperatures: Reference meter Tw °F	Temperatures: Dry gas meter Td °F	Test duration min	Calibration Factor Y	H@ in. H2O
0.5	stop 200.174	stop 346.092	stop 74	stop 77	13	1.002	1.758
	start 195.008	start 340.891	start 74	start 74			
≥ 5 ft³	diff 5.166	diff 5.201	avg 74	avg 75.5			
1.0	stop 205.914	stop 351.912	stop 74	stop 79	10	0.994	1.82
	start 200.388	start 346.300	start 74	start 76			
≥ 5 ft³	diff 5.526	diff 5.612	avg 73	avg 77.5			
1.5	stop 212.059	stop 358.116	stop 74	stop 80	8	0.997	1.95
	start 206.848	start 352.819	start 74	start 79			
≥ 10 ft³	diff 5.211	diff 5.297	avg 74	avg 79.5			
2.0	stop 218.966	stop 365.085	stop 74	stop 82	8	1.009	1.92
	start 212.905	start 358.990	start 74	start 80			
≥ 10 ft³	diff 6.061	diff 6.095	avg 74	avg 81			
2.5	stop 225.726	stop 371.934	stop 73	stop 83	6	1.007	1.905
	start 220.646	start 366.796	start 73	start 82			
≥ 10 ft³	diff 5.080	diff 5.138	avg 73	avg 82.5			
					Average Values	1.002	1.871

Provide calculations of the back side of this page

Y must not deviate by more than +/-0.02 Y.

H@ must not deviate by more than 0.15 in. H2O.

QC Review by: CJ Date: 3-5-92

DRY GAS METER INITIAL CALIBRATION

DATE: 3-6-92

CALIBRATOR: MR

METER BOX ID.: M-8 DGM SERIAL #: 66153

BAROMETRIC PRESSURE (Pb): 29.97 in. Hg

REFERENCE METER ID: 008759 GAMMA: 1.0073

Leak Checks:

Positive (minimum 5 in. H2O) : _____

Negative (within 3 in. Hg of absolute) : _____ cfm* _____ in. Hg

* Not to exceed 0.005 cfm.

Orifice manometer setting ΔH in. H2O	Volume reference meter Vw ft³	Volume dry gas meter Vd ft³	Temperatures: Reference meter Tw °F	Temperatures: Dry gas meter Td °F	Test duration min	Calibration Factor Y	H@ in. H2O
0.5	stop 118.602	stop 284.492	stop 73	stop 74	16	1.004	1.802
	start 112.338	start 278.192	start 70	start 73			
≥ 5 ft³	diff 6.264	diff 6.300	avg 71.5	avg 73.5			
1.0	stop 129.126	stop 294.950	stop 73	stop 77	10	1.004	1.85
	start 123.658	start 289.449	start 73	start 75			
≥ 5 ft³	diff 5.468	diff 5.501	avg 73	avg 76			
1.5	stop 134.675	stop 300.563	stop 73	stop 78	8	1.004	1.93
	start 129.435	start 295.282	start 73	start 77			
≥ 10 ft³	diff 5.240	diff 5.281	avg 73	avg 77.5			
2.0	stop 141.751	stop 307.689	stop 73	stop 80	9	1.005	1.94
	start 134.978	start 300.859	start 73	start 78			
≥ 10 ft³	diff 6.773	diff 6.830	avg 73	avg 79			
2.5	stop 147.835	stop 313.820	stop 73	stop 81	7	1.008	1.90
	start 141.896	start 307.839	start 73	start 80			
≥ 10 ft³	diff 5.939	diff 5.981	avg 73	avg 80.5			
					Average Values	1.005	1.88

Provide calculations of the back side of this page

Y must not deviate by more than +/-0.02 Y.

H@ must not deviate by more than 0.15 in. H2O.

QC Review by: [signature] Date: 3/6/92

DRY GAS METER AND ORIFICE SYSTEM CALIBRATION

DATE 9-25-91 OPERATOR CJ Metering System Identification M-2

* Orifice Manometer Setting ΔH " H_2O	Minimum Volume of Gas ft³	Stand WET TEST METER GAS VOLUMES AND TEMPERATURES: Initial ft³ V_{w_i}	Initial Temp. °F T_{w_i}	Final ft³ V_{w_f}	Final Temp. °F T_{w_f}	Net Volume ft³ V_w	Avg. Temp. °F T_w	DRY TEST METER GAS VOLUMES AND TEMPERATURES: Initial ft³ V_{d_i}	Initial Temp. of T_{d_i}	FINAL ft³ V_{d_f}	FINAL Temp. °F T_{d_f}	Net Volume ft³ V_d	Avg. Temp. °F T_d	Total Test Time Minutes θ	Barometer Reading, Inches Hg P_b
0.5	5	173.240	71	~~494.058~~ 180.866	71	7.626	71	494.058	71	501.728	73	7.670	72	20	29.88
1.00	5	181.160	71	188.630	71	7.470	71	502.048	71	509.556	75	7.508	73	14	29.88
2.00	5	188.886	71	196.233	71	7.347	71	509.815	75	517.165	75	7.350	75	10	29.88
3.00	5	202.004	71	208.261	71	6.257	71	522.915	76	529.175	76	6.256	76	7	29.88

* Check at least every 2 minutes and adjust if needed.

Vacuum System Leak Check ✓
Pressure Leak Check of Meter Box ✓
System Operated 15 min. Prior to Calibration ✓

CALCULATIONS

$$Y = \frac{(w_r)(V_w)(P_b)(T_d + 460)}{(V_d)(P + \frac{\Delta H}{13.6})(T_w + 460)}$$

$$\Delta H@ = \frac{0.0317\ (\Delta H)}{(P_b)(T_d + 460)} \left[\frac{(T_w + 460)\ \theta}{(w_r)(V_w)}\right]^2$$

Calc. By:
Checked By:
Date:

ΔH	GAMMA CALCULATIONS	Y	ΔH@ CALCULATIONS	ΔH@
0.5	$\frac{1.007\ (7.626)(29.88)(72 + 460)}{(7.670)(29.88 + \frac{0.5}{13.6})(71 + 460)}$	1.002	$\frac{0.0317\ (0.5)}{(29.88)(72 + 460)} \frac{(71 + 460)(20)^2}{1.007\ (7.626)}$	1.912
1.00	$\frac{1.007\ (7.470)(29.88)(73 + 460)}{(7.508)(29.88 + \frac{1.0}{13.6})(71 + 460)}$	1.003	$\frac{0.0317\ (1.0)}{(29.88)(73 + 460)} \frac{(71 + 460)(14)^2}{1.007\ (7.470)}$	1.953
2.00	$\frac{1.007\ (7.347)(29.88)(75 + 460)}{(7.350)(29.88 + \frac{2.0}{13.6})(71 + 460)}$	1.009	$\frac{0.0317\ (2.0)}{(29.88)(75 + 460)} \frac{(71 + 460)(10)^2}{1.007\ (7.347)}$	2.060
3.00	$\frac{1.007\ (6.257)(29.88)(76 + 460)}{(6.256)(29.88 + \frac{3.0}{13.6})(71 + 460)}$	1.009	$\frac{0.0317\ (3.0)}{(29.88)(76 + 460)} \frac{(71 + 460)(7)^2}{1.007\ (6.257)}$	2.088
	AVERAGE	1.0057	AVERAGE	2.003

(Y) Gamma = ratio of reading of wet test meter to dry test meter
Tolerance = ± 0.02 from average

ΔH@ = orifice pressure differential that gives 0.75 cfm of air at 68°F and 29.92" Hg.
Average ΔH@ value between 1.59-2.09 is acceptable. In addition, the ΔH@ must not vary by more than ±0.20 over the ΔH range of calibration of 0.5-3.00" H_2O.

THERMOCOUPLE DIGITAL INDICATOR
MONROE AUTO CALIBRATION DATA FORM

Date 12-31-91 Calibrator Name TOM DRAKE

Indicator No. _____ Serial No. M 1

Calibration Device No CL-300-2100 F Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	0	0
2		100	98	0.36
3		200	201	0.15
4		300	301	0.13
5		400	398	0.23
6		500	499	0.10
7		600	602	0.19
8		700	701	0.09
9		800	802	0.16
10		900	901	0.07

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

DRY GAS METER POST-TEST CALIBRATION USING REFERENCE METER

DATE: 12-31-91 METER BOX NO. M 1

CALIBRATOR: TOM DRAKE BAROMETRIC PRESSURE (Pb) 30.21 in. Hg

INITIAL CALIBRATION Y: 0.999 ΔH@: 1.913

PLANT: MONROE PROJECT NO.: 985-002

AVERAGE ΔH DURING TESTING: 2 MAXIMUM VACUUM 10 in. Hg

Orifice manometer setting* ΔH in. H2O	Volume reference meter Vw ft3	Volume dry gas meter Vd ft3	Temperatures: Ref Meter Tw °F	Ref Meter Avg Tw °F	Dry gas meter Td °F	Dry gas meter Avg Td °F	Test duration θ min	Vacuum setting ** in. Hg	Calibr Factor Y	ΔH@ in. H2O
2	start 258.748 stop 269.910 diff 11.162	435.126 446.343 11.217	start 74 stop 75	74.5	start 72 stop 74	73	15	10	0.993	2.007
2	start 269.910 stop 281.014 diff 11.104	446.343 457.550 11.207	start 75 stop 75	75	start 74 stop 77	75.5	15	10	0.993	2.023
2	start 281.014 stop 292.130 diff 11.116	457.550 468.802 11.252	start 75 stop 76	75.5	start 77 stop 78	77.5	15	10	0.993	2.016
								Post-test Average***	0.993	2.015

* To be the average ΔH used during test series.

** To be the highest vacuum used during test series.

*** Post-test Y must be within the range, pre-test Y +/- 5% OK? ☒

Post-test ΔH@ should be within the range of the initial or pre-test ΔH@ +/- 0.20 in. H2O. OK? ☒

$$Y = \frac{(1.006)\,(Vw)\,(Pbar)\,(Td + 460)}{(Vd)\,(Pbar + \Delta H / 13.6)\,(Tw + 460)}$$

$$\Delta H@ = \frac{(0.0317)\,(\Delta H)}{(Pbar)\,(Td + 460)} \left[\frac{(Tw + 460)\,(\theta)}{(Vw)(1.006)} \right]^2$$

$$\text{Percent difference} = \frac{(\text{Avg inital } Y) - (\text{Post-test } Y)}{(\text{Avg initial } Y)}$$

dgmptcal.wk1

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Meter Box 4

Date 2/19/92 Calibrator Name [illegible]

Indicator No. CL-300-2100F Serial No. 009

Calibration Device No. Temp Chamber #1 Manufacturer Omega

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		100	100	
2		500	502	
3		900	904	
4		1300	1305	
5		1700	1699	
6		zero	zero	
7		200	202	
8		400	400	
9		800	804	
10		1200	1203	

Percent difference must be less than or equal to 0.5%

Percent Difference:

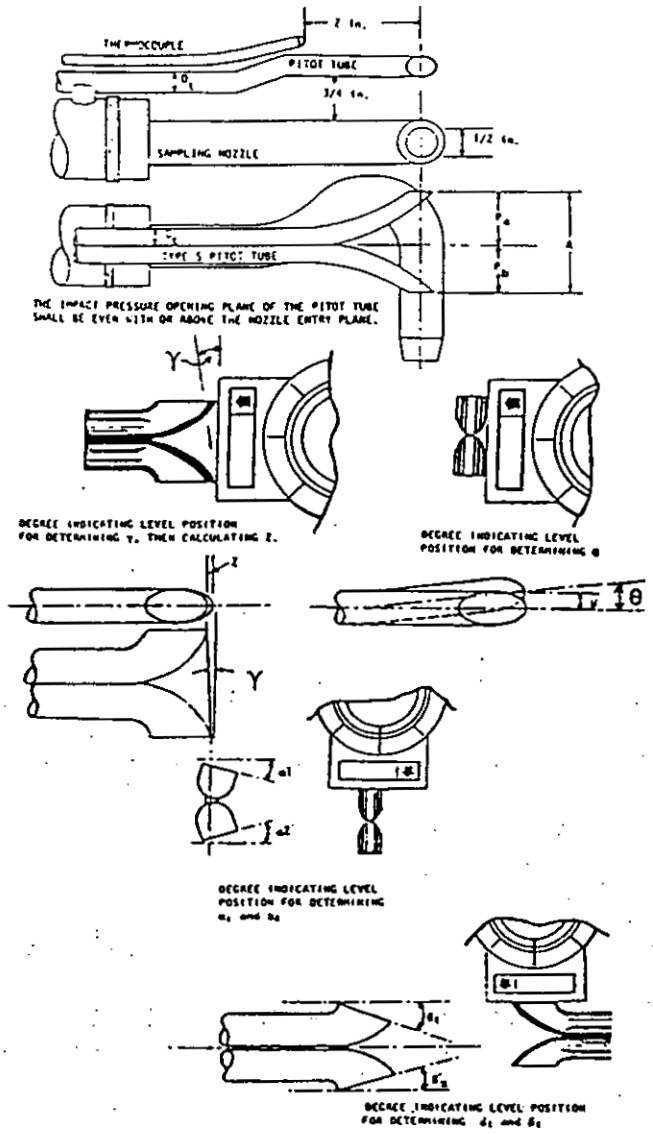
$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

PITOT TUBE INSPECTION DATA SHEET

Company Name: IEA

Pre-sample Date 2/21/92

Post Sample Date _____



YES	level?	
NO	obstructions?	
NO	damaged?	
0	$-10° < \alpha_1 < +10°$	
0	$-10° < \alpha_2 < +10°$	
0	$-5° < \beta_1 < +5°$	
0	$-5° < \beta_2 < +5°$	
0	γ	
0	θ	
0.919	A	
0.457	$1.05\ D_t < P_a < 1.5\ D_t$	
0.457	$1.05\ D_t < P_b < 1.5\ D_t$	
0.403	$3/16" \leq D_t \leq 3/8"$	
0	$A \tan \gamma < 0.125"$	
0	$A \tan \theta < 0.03125"$	
yes	$P_a = P_b$	

Comments: _____

Pitot tube/probe number 5A meets or exceeds all specifications criteria and/or applicable design features* and is hereby assigned a pitot tube calibration factor of 0.84.

Signature [signature]

Date 2/21/92

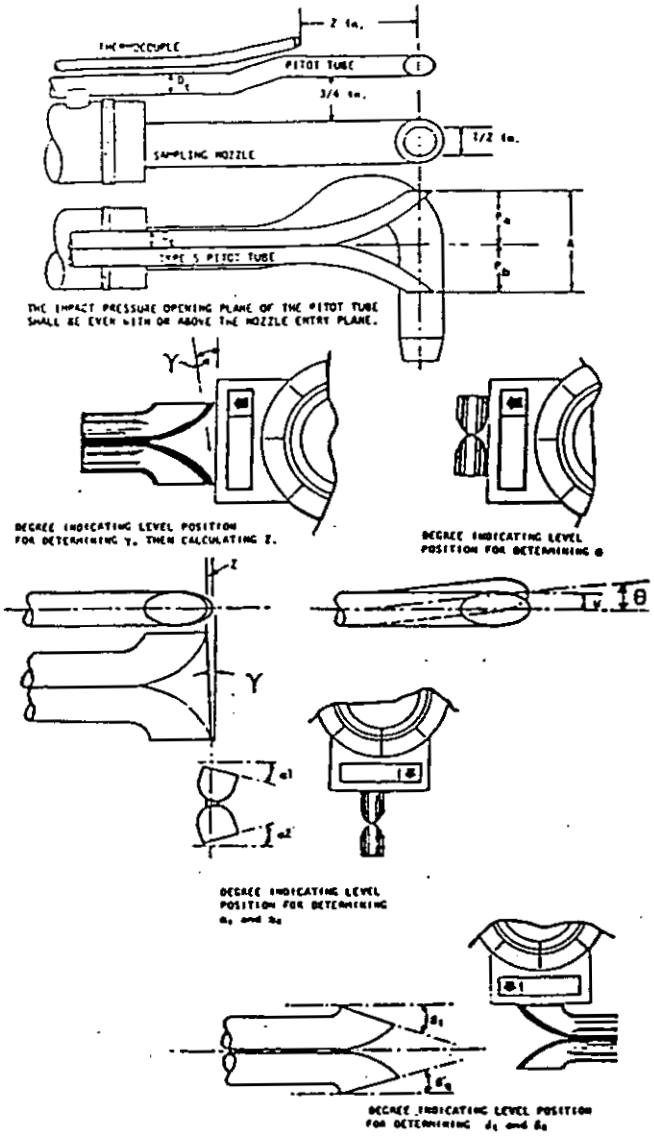
*See 40 CFR 60, Vol. 42, No. 160, Method 2. Verify the minimum 2 inch setback of the thermocouple and the minimum 3/4 inch separation between the pitot tube and the nozzle as shown at the top of this page.

PITOT TUBE INSPECTION DATA SHEET

Company Name: UNION CAMP SAVANNAH

Pre-sample Date 11-5-91

Post Sample Date _____



yes	level?	yes
NO	obstructions?	NO
NO	damaged?	NO
O	$-10° < \alpha_1 < +10°$	O
O	$-10° < \alpha_2 < +10°$	O
O	$-5° < \beta_1 < +5°$	O
O	$-5° < \beta_2 < +5°$	O
O	γ	O
O	θ	O
0.942	A	0.943
0.471	$1.05\ D_t < P_a < 1.5\ D_t$	0.471
0.471	$1.05\ D_t < P_b < 1.5\ D_t$	0.472
0.375	$3/16" \leq D_t \leq 3/8"$	0.382
O	$A \tan \gamma < 0.125"$	O
O	$A \tan \theta < 0.03125"$	O
yes	$P_a = P_b$	—

(within tolerances)

Comments: No longer ATTACHED TO PROBE #10A
USED at UNION CAMP SAVANNAH

Pitot tube/probe number PT-10 meets or exceeds all specifications criteria and/or applicable design features* and is hereby assigned a pitot tube calibration factor of 0.84.

Signature [signature]

Date 1-6-91

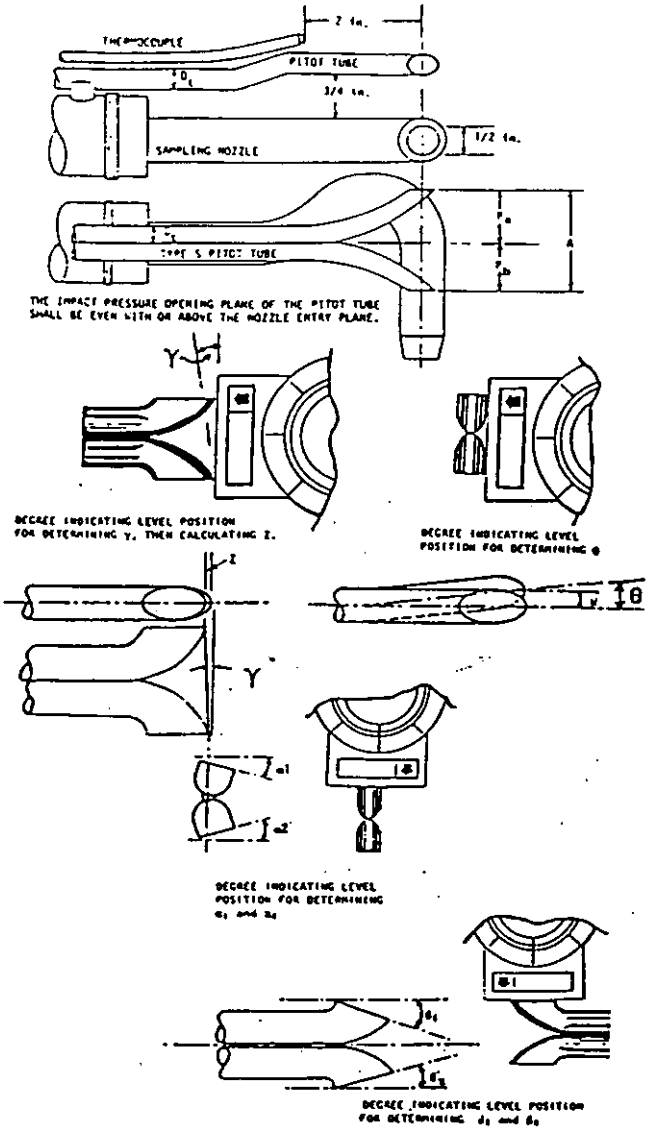
*See 40 CFR 60, Vol. 42, No. 160, Method 2. Verify the minimum 2 inch setback of the thermocouple and the minimum 3/4 inch separation between the pitot tube and the nozzle as shown at the top of this page.

PITOT TUBE INSPECTION DATA SHEET

Company Name: IEA / GP Woodland, ~~Lincoln~~, ME

Pre-sample Date 12/16/91

Post Sample Date NOT USED AT GP WOODLAND



yes	level?	
no	obstructions?	
no	damaged?	
2°	$-10° < \alpha_1 < +10°$	
0°	$-10° < \alpha_2 < +10°$	
1°	$-5° < \beta_1 < +5°$	
0°	$-5° < \beta_2 < +5°$	
0°	γ	
0°	θ	
0.938"	A	
yes 0.47"	$1.05\ D_t < P_a < 1.5\ D_t$	
yes 0.47"	$1.05\ D_t < P_b < 1.5\ D_t$ 0.38	
0.380	3/16" 0.19 $\leq D_t \leq$ 3/8"	
0 / yes	$A \tan \gamma < 0.125"$	
0 / yes	$A \tan \theta < 0.03125"$	
0.47 = 0.47 yes	$P_a = P_b$	

Comments: within spec.

Pitot tube/probe number ~~PT 98~~ PT 14 meets or exceeds all specifications criteria and/or applicable design features* and is hereby assigned a pitot tube calibration factor of 0.84.

Signature M Rousseau

Date 12/16/91

*See 40 CFR 60, Vol. 42, No. 160, Method 2. Verify the minimum 2 inch setback of the thermocouple and the minimum 3/4 inch separation between the pitot tube and the nozzle as shown at the top of this page.

18 2 47 71

PITOT TUBE INSPECTION DATA SHEET

Company Name: INLAND ROME

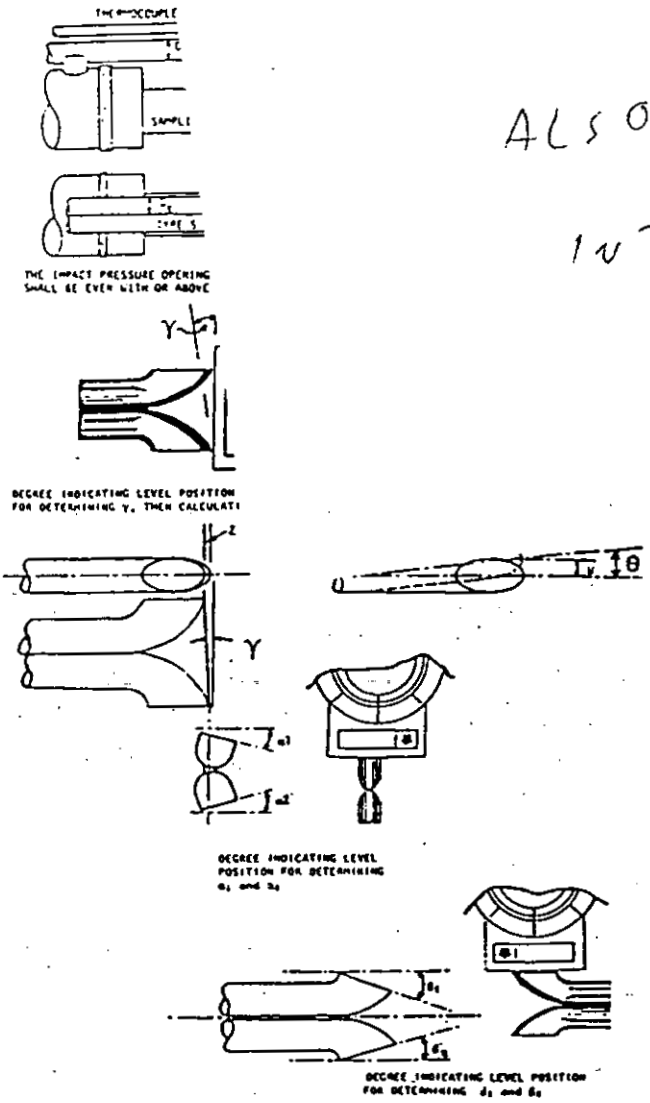
Pre-

Post Sample

e

ALSO COPY

INTRS TRAILER



0	γ
0	θ
0.938	A
0.469	1.05 D_t < P_a < 1.5 D_t
0.469	1.05 D_t < P_b < 1.5 D_t
0.372	3/16" ≤ D_t ≤ 3/8"
N/A	A tan γ < 0.125"
N/A	A tan θ < 0.03125"
yes	P_a = P_b

Comments: _____

Pitot tube/probe number TRSPT6 meets or exceeds all specifications criteria and/or applicable design features* and is hereby assigned a pitot tube calibration factor of 0.84.

Signature _____

Date _____

*See 40 CFR 60, Vol. 42, No. 160, Method 2. Verify the minimum 2 inch setback of the thermocouple and the minimum 3/4 inch separation between the pitot tube and the nozzle as shown at the top of this page.

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.730 cm ~~(in.)~~

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.365 cm (in.) P_b 0.330 cm (in.)

D_t = 0.303 cm (in.)

Comments: 10-8-91
Checked by R.S.
CR-4

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes ____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 1.0 °, θ = 0 °, A = (0.951) cm (in.)

z = A sin γ = 0.017 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0.0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.474 cm (in.) P_b 0.477 cm (in.)

D_t = 0.375 cm (in.)

Comments: Calib by MCR 7/19/91

Calibration required? ____ yes X no

Probe # 4-D

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? _____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.945 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.472 cm (in.) P_b 0.473 cm (in.)

D_t = 0.375 cm (in.)

Comments: Check by MCR 7/19/91
probe 4C

Calibration required? _____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 1.5 °, θ = 0.0 °, A = 0.916 (cm) (in.)

z = A sin γ = 0.024 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.458 cm (in.) P_b 0.458 cm (in.)

D_t = 0.377 cm (in.)

Comments: checked Calib by MCR 7/19/91

Probe # 4A

Calibration required? _____ yes X no

3

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? _____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.947 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.471 cm (in.) P_b 0.471 cm (in.)

D_t = 0.375 cm (in.)

Comments: Check by MCR 7/19/91
Probe #: 3B

Calibration required? _____ yes X no

8

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = _____ °, θ = 0 °, A = 0.644 (cm) ~~(in.)~~

z = A sin γ = _____ cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = _____ cm (in.); <.08 cm (<1/32 in.)

P_A 0.375 (cm) ~~(in.)~~ P_b 0.371 (cm) ~~(in.)~~

D_t = 0.289 (cm) ~~(in.)~~

Comments: 10-8-91
Checked by P.S.
CR-03

Calibration required? _____ yes _____ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 3.70 (cm) (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.435 cm (in.) P_b 0.435 cm (in.)

D_t = 0.382 cm (in.)

Comments: Inspected 10-9-91 by [illegible]
Probe #3A

Calibration required? ____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? _____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 1.0 °, θ = 0 °, A = 0.937 cm ~~(in.)~~

z = A sin γ = 0.016 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.469 cm (in.) P_b 0.468 cm (in.)

D_t = 0.374 cm (in.)

Comments: Checked by MR 7/19/91

probe - 1-A

Calibration required? _____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.970 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.47 cm (in.) P_b 0.47 cm (in.)

D_t = 0.940 cm (in.)

Comments: checked by TO 8-14-91
PROBE #1B

Calibration required? _____ yes X no

QA Sect 3.1, 3.2, 3.3 7.1

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? _____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 1.0 °, θ = 0 °, A = 0.940 cm (in.)

z = A sin γ = 0.016 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.470 cm (in.) P_b 0.470 cm (in.)

D_t = 0.375 cm (in.)

Comments: Checked by MCP 7/19/91

probe # 4-B

Calibration required? _____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.942 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.470 cm (in.) P_b 0.472 cm (in.)

D_t = 0.373 cm (in.)

Comments: Checked by MCK 7/19/91
probe # 5A

Calibration required? _____ yes X no

6

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.942 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.471 cm (in.) P_b 0.471 cm (in.)

D_t = 0.373 cm (in.)

Comments: ~~Calib.~~ Checked by MCR 7/9/91

Probe #: 5-C

Calibration required? ____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0.75 °, θ = 1.0 °, A = 0.943 cm (in.)

z = A sin γ = ~~0.75~~ 0.012 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = ~~1.0~~ 0.016 cm (in.); <.08 cm (<1/32 in.)

P_A 0.471 cm (in.) P_b 0.472 cm (in.)

D_t = 0.371 cm (in.)

Comments: ~~Calib~~ checked by MCR 7/19/91

Probe # 6-A

Calibration required? ____ yes ✗ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 1 °, θ = 0 °, A = 0.940 cm (in.)

z = A sin γ = 0.016 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.470 cm (in.) P_b 0.470 cm (in.)

D_t = 0.373 cm (in.)

Comments: Checked by MCR

7/19/91

Probe # 6-C

Calibration required? ____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? _____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = .942 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.475 cm (in.) P_b 0.475 cm (in.)

D_t = 0.375 cm (in.)

Comments: Checked by MCR 7/9/91

Probe 7A

Calibration required? _____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✗ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.944 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.472 cm (in.) P_b 0.472 cm (in.)

D_t = 0.278 cm (in.)

Comments: PT #7 on PROBE #7B
checked by TFD on 11-5-91

Calibration required? _____ yes ✗ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? 0 yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.944 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.472 cm (in.) P_b 0.472 cm (in.)

D_t = 0.375 cm (in.)

Comments: Checked by MCP
probe # 7B 7/19/91

Calibration required? _____ yes ~~X~~ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? ____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.944 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.472 cm (in.) P_b 0.472 cm (in.)

D_t = 0.376 cm (in.)

Comments: PT 11 on PROBE #9A
checked by TFD on 11-5-91

Calibration required? ____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ___X___ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ___X___ no

α_1 = ___0___ ° (<10°), α_2 = ___0___ ° (<10°), β_1 = ___0___ ° (<5°),

β_2 = ___0___ ° (<5°)

γ = ___0___ °, θ = ___0___ °, A = ___0.945___ cm (in.)

z = A sin γ = ___0___ cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = ___0___ cm (in.); <.08 cm (<1/32 in.)

P_A ___0.472___ cm (in.) P_b ___0.473___ cm (in.)

D_t = ___0.375___ cm (in.)

Comments: Checked by MCK 7/19/91

Probe #: 9-A

Calibration required? ____ yes ___X___ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? _____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.942 cm (~~in.~~)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.471 cm (~~in.~~) P_b 0.471 cm (~~in.~~)

D_t = 0.375 cm (~~in.~~)

Comments: PT-10 on PROBE # 10A
checked by TFD on 11-5-91

Calibration required? _____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.948 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.474 cm (in.) P_b 0.474 cm (in.)

D_t = 0.373 cm (in.)

Comments: Calib. by MCR 7/19/91

Probe # 10 A

Calibration required? ____ yes ✓ no

2

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? ____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.945 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.473 cm (in.) P_b 0.472 cm (in.)

D_t = 0.375 cm (in.)

Comments: PT-9 For Probe #11-A
checked by TFO. 11-5-91

Calibration required? ____ yes X no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? X yes _____ no

Pitot tube openings damaged? _____ yes (explain below) X no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 0.942 cm (in)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.470 cm (in) P_b 0.472 cm (in.)

D_t = 0.375 cm (in.)

Comments: checked by MCK 7/19/91

probe # 11A

Calibration required? _____ yes / no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = ~~6.860~~ 0.686 cm ~~(in.)~~

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 0.360 cm (in.) P_b 0.356 cm (in.)

D_t = 0.285 cm (in.)

Comments: 10-8-91
Checked by PS.
CL-5

Calibration required? ____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 3.70 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 4.35 cm (in.) P_b 4.35 cm (in.)

D_t = 3.82 cm (in.)

Comments: Inspected by P. Slater

June 28, 1991

Pitot IEA 3A

Calibration required? ____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 357 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 4.15 cm (in.) P_b 4.15 cm (in.)

D_t = 3.93 cm (in.)

Comments: Inspected by P. Slater
June 28, 1991
Pitot 1EA 3B

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 3.75 cm (in)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 4.21 cm (in) P_b 4.21 cm (in.)

D_t = 355 cm (in.)

Comments: Inspected by P. Slater
28 June 1991
Pitot IEA 4C

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 3.94 cm (in)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 4.83 cm (in.) P_b 4.83 cm (in.)

D_t = 3.98 cm (in)

Comments: Inspected by P. Slater
28 June 1991
Pitot IEA 4D

Calibration required? ____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 3.58 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 4.40 cm (in.) P_b 4.40 cm (in.)

D_t = 4.07 cm (in.)

Comments: Inspected by P. Slater
28 June 1991
Pitot 1EA 5A

Calibration required? ____ yes ____ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 347 cm (in)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 302 cm (in) P_b 302 cm (in.)

D_t = 380 cm (in)

Comments: Inspected by P. Slater
28 June 1991
Pitot 1EA 5C

Calibration required? ____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 3.52 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 4.60 cm (in.) P_b 4.60 cm (in.)

D_t = 3.72 cm (in.)

Comments: Inspected by P. Slater
28 June 1991
Pitot 1EA 6B

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 3.53 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 3.93 cm (in.) P_b 5.52 cm (in.)

D_t = 4.08 cm (in.)

Comments: Inspected by P. Slater
June 28, 1991
Pitot 1EA 6C

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 244 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 122 cm (in.) P_b 122 cm (in.)

D_t = 96 cm (in.)

Comments: Inspected by David A. Prater
1 May 1990
Pitot #IEA PT6-A

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? ✓ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 244 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 122 cm (in.) P_b 122 cm (in.)

D_t = 96 cm (in.)

Comments: Inspected By David A. Prater
1 May 1990
Pitot # IEA PT 5-A

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),

β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 244 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),

w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 122 cm (in.) P_b 122 cm (in.)

D_t = 96 cm (in.)

Comments: Inspected by DAVID PRATER
1 MAY 1990
PITOT #IEA PT 7-A

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 244 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 122 cm (in.) P_b 122 cm (in.)

D_t = 96 cm (in.)

Comments: CALIBRATED BY DAVID A. PRATER
DATE 1 MAY 1990
PITOT # IEA PT 4A (FOUR FOOT PROBE)

Calibration required? _____ yes ✓ no

TYPE S PITOT TUBE INSPECTION DATA FORM

Pitot tube assembly level? ✓ yes _____ no

Pitot tube openings damaged? _____ yes (explain below) ✓ no

α_1 = 0 ° (<10°), α_2 = 0 ° (<10°), β_1 = 0 ° (<5°),
β_2 = 0 ° (<5°)

γ = 0 °, θ = 0 °, A = 244 cm (in.)

z = A sin γ = 0 cm (in.); <0.32 cm (<1/8 in.),
w = A sin θ = 0 cm (in.); <.08 cm (<1/32 in.)

P_A 122 cm (in.) P_b 122 cm (in.)

D_t = 96 cm (in.)

Comments: CALIBRATED BY DAVID A. PRATER
DATE 1 MAY 1990
PITOT # IEA PT 1

Calibration required? _____ yes ✓ no

TEMPERATURE CALIBRATION DATA FORM

Date 1-28-92 Calibrator Name P. SLATER

Ambient Temperature 68°F Barometric Pressure _____ in. Hg

Reference: Hg-in-glass _____

Other Fluke 52

Thermocouple No.	Source (specify)	Reference thermometer temperature °F	Thermocouple indicator temperature °F	Percent error %
7-A	AMBIENT	67.0	67.0	0.0
	ICE BATH	34.2	39.0	0.971
	Boiling H2O	214.4	215.0	0.089

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 12/16/91 Calibrator Name MCR

Ambient Temp 68° F Barometric Pressure 29.76 in. Hg

Reference: Mercury-in-glass ________

Other FLUKE 52

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
PT 14	Ambient	67.8	66.8	0.19
	Ice	32.4	32.6	0.06
	Boiling	213.8	212.0	0.27

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 11-6-91

Calibrator Name T. D RAKE

Ambient Temp 65°

Barometric Pressure 29.805 in. Hg

Reference: Mercury-in-glass

Other Fluke

Probes used AT UNION CAMP, SAVANNAH

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
9 A	AMBIENT	68.4	71	0.50
	ICE H_2O	34.5	37	0.60
	Boiling H_2O	214.2	212	0.33
11 A	AMBIENT	70.2	68	0.40
	ICE H_2O	37.0	38	0.20
	Boiling H_2O	212.8	211	0.20

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 11-5-91

Calibrator Name T. DRAKE

Ambient Temp 57

Barometric Pressure 29.875 in. Hg

Reference: Mercury-in-glass

Other FLUKE

For probe used AT P&G Oglethorpe

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
10A	AMBIENT	57.6	56	0.30
	ICE	35.6	37	0.28
	Boiling	214.6	213	0.24

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 10/23/91 Calibrator Name MCR

Ambient Temp 74°F Barometric Pressure 30.07 in. Hg

Reference: Mercury-in-glass

Other FLUKE 52

PROBES USED @ GE

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
4A	AMBIENT	72.4	72.4	0.0
	ICE	32.6	32.8	0.04
	BOILING H2O	211.6	212.4	0.12
3B	Ambient	72.6	75.4	0.53
	Ice	33.2	34.0	0.16
	Boiling H2O	211.6	212.0	0.06
4C	Ambient	76.0	77.2	0.22
	Ice	39.8	38.4	0.28
	Boil	211.8	211.8	0.0
5C	Amb	73.2	71.8	0.26
	Ice	36.8	37.0	0.04
	Boil	210.6	211.2	0.09
CR-3	Amb.	81.0	81.6	0.11
	Ice	32.2	33.2	0.20
	Boil	211.4	211.8	0.06
CR4	Amb.	76.4	76.2	0.03
	Ice	32.8	32.8	0.0
	Boil	211.6	211.8	0.03

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

3A
4D

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 10/23/91 Calibrator Name MIC R

Ambient Temp 74°F Barometric Pressure 30.07 in. Hg

Reference: Mercury-in-glass _____

Other FLUKE 52

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
3A	Amb.	76.0	76.6	0.11
	Ice	31.8	32.2	0.08
	Boil	211.6	212.6	0.15
4D	Amb.	81.0	83.0	0.37
	ICE	33.0	35.2	0.45
	BOIL	211.0	211.0	0.0

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 10/2/91

Calibrator Name JS.

Ambient Temp 76°

Barometric Pressure 30.25 in. Hg

Reference: Mercury-in-glass —

Other Fluke

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
3 A	Ambient	75.2	75.0	0.4
	ICE	34.5	35.0	1.0
	Boiling H_2O	208.9	210.0	1.6
3 B	Ambient	75.2	75.0	0.4
	ICE	34.3	35.0	1.4
	Boiling H_2O	210.4	211.0	0.9
4-A	Ambient	75.0	75.0	0.0
	ICE	34.4	35.0	1.2
	Boiling H_2O	212.8	213	0.03
4-C	Ambient	75.9	76.0	0.2
	ICE	33.1	33.0	0.2
	Boiling H_2O	208.8	209.0	0.3
4-D	Ambient	76.6	76.0	1.1
	ICE	33.8	34.0	0.4
	Boiling H_2O	208.0	209.0	1.4

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

$$\frac{(208 + 460) - (209 + 460)}{208 + 460} = .14$$

TEMPERATURE CALIBRATION DATA FORM

Date 10/7/91 Calibrator Name B.

Ambient Temp 72.0°F Barometric Pressure 29.98 in. Hg

Reference: Mercury-in-glass —

Other Fluke 52

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
CR-3	Ambient	72.8°	71.4°	0.08
	Ice	40.6°	41.4°	0.09
	Boiling H_2O	211.3°	211.5°	0.02
CR-4	Ambient	72.8°	71.2°	0.11
	ICE	43.2°	43.5°	0.04
	boiling H_2O	210.6°	211.5°	0.09
CR5	Ambient	72.8°	71.2°	0.11
	ICE	35.6°	36.0°	0.04
	boiling H_2O	211.6°	211.3°	0.04

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 7/17/91 Calibrator Name MCR

Ambient Temp 74° F Barometric Pressure 29.824 in. Hg

Reference: Mercury-in-glass FLUKE

Other *

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
4A	AMBIENT	72	72	0
	BOILING	212.4	213	0.03
* 4B	AMBIENT	77.4	78	0.11
	BOILING	212.0	213	0.15
4C	AMBIENT	78.0	78	0
	BOILING	211.8	211	0.12
4D	AMBIENT	77.2	78	0.15
	BOILING	212.6	213	0.06
5A	AMBIENT	78.8	79	0.04
	BOILING	212.2	213	0.12
5B	DEFECTIVE			
		DO NOT USE		
5C	AMBIENT	78.0	78	0
	BOILING	212.0	214	0.30

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 8-13-91 Calibrator Name T. DRAKE

Ambient Temp 73 Barometric Pressure 29.96 in. Hg

Reference: Mercury-in-glass _____

Other Fluke S/N 4970142

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
11A	Ambient	72.8°F	73°F	0.04
	Ice Bath	32.2°F	33	~~1.6~~ 0.16
	Boiling H_2O	211.4	213	
1B	Ambient	72.0	72°F	0
	Ice BATH	32.2	33	~~0.16~~ 0.16
	Boiling H_2O	211.8	212	0.03

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 8/23/91 Calibrator Name MCR

Ambient Temp 74° F Barometric Pressure 29.93 in. Hg

Reference: Mercury-in-glass _____

Other FLUKE 52

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
Probe # 7B #1 (TC)	*Ambient H_2O	78.6	78	0.11
	ICE H_2O	34.6	35	0.08
	Boiling H_2O	213.6	214	0.08
Probe 3A #1 TC	AMBIENT H_2O	75.4	76	0.13
	ICE "	40.2	40	0.04
	BOILING "	211.2	211	0.04
PROBE 7A #1 TC	AMBIENT H_2O	75.6	76	0.08
	ICE "	41.4	42	0.13
	BOILING "	211.6	212	0.08
9A #1 TC	Ambient Air	76.4	77	0.13
	ICE H_2O	43.4	43	0.08
	BOILING "	212.4	212	0.08

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 3/4/91 Calibrator Name MCR

Ambient Temp 71 Barometric Pressure 29.89 in. Hg

Reference: Mercury-in-glass Fluke 52

Other

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
9A	Ambient Air	71.8	71	0.15
	Boiling H_2O	211.6	212	0.06
4A	Ambient Air	72.2	71	0.23
	Boiling H_2O	211.8	211	0.12

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 6/28/91 Calibrator Name P.S.

Ambient Temp 76° Barometric Pressure 30.25 in. Hg

Reference: Mercury-in-glass ✓

Other

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
6A	Ice Bath	1.8°C / 35.2°F	36°	1.6
	Ambient Air	24.2°C / 75.5°F	75°	0.9
	Boiling H_2O	97.4°C / 207.3°F	208°	1.0
6C	Ice Bath	1.9°C / 35.4°F	36°	1.2
	Ambient Air	24.2°C / 75.5°F	75°	0.9
	Boiling H_2O	96.2°C / 205.2°F	206°	1.2

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 6-28-91 Calibrator Name P.S.

Ambient Temp 76° Barometric Pressure 30.25 in. Hg

Reference: Mercury-in-glass ✓

Other

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
4C	Ice Bath	0.6°C / 33.1°F	33°	0.2
	Ambient Air	24.4°C / 75.9°F	76°	0.2
	Boiling H_2O	98.2°C / 208.8°F	209°	0.3
4D	Ice Bath	0.8°C / 33.8°F	34°	0.4
	Ambient Air	24.8°C / 76.6°F	76°	1.1
	Boiling H_2O	97.8°C / 208.0°F	209°	1.4
5C	Ice Bath	0.4°C / 32.7°F	33°	0.6
	Ambient Air	24.2°C / 75.5°F	75°	0.9
	Boiling H_2O	99.4°C / 210.9°F	212°	1.6
6B	Ice Bath	1.2°C / 34.2°F	35°	1.6
	Ambient Air	24.0°C / 75.2°F	75°	0.4
	Boiling H_2O	98°C / 208.4°F	210°	2.4
3A	Ice Bath	1.4°C / 34.5°F	35°	1.0
	Ambient Air	24.0°C / 75.2°F	75°	0.4
	Boiling H_2O	98.3°C / 208.9°F	210	1.6
3B	Ice Bath	1.3°C / 34.3°F	35°	1.4
	Ambient Air	24.0°C / 75.2°F	75°	0.4
	Boiling H_2O	99.1°C / 210.4°F	211°	0.9

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 9/20/91 Calibrator Name MCR

Ambient Temp 71.8 Barometric Pressure 29.92 in. Hg

Reference: Mercury-in-glass ✓

Other PRINCO 453 also

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
CR-5	Ambient	71.8	71.2	0.11
	Ice	35.6	36.0	0.04
Chrom 6 PROBE	Boiling	211.6	211.3	0.04
CR-3	Ambient	71.8	71.4	0.08
	Ice	40.6	41.4	0.09
Chr. 6 Prb.	Boil	211.3	211.5	0.02
CR-4	Ambient	71.8	71.2	0.11
	Ice	43.2	43.5	0.04
Chr. 6 - Prb.	Boil	210.6	211.5	0.09
4B	Amb.	72.5	72.1	0.08
	Ice	32.4	32.7	0.03
	Boil	213.44	211.5	0.29
5A	Amb	69.8	71.2	0.26
	Ice	32.9	32.7	0.04
	Boil	210.9	212.0	0.16
6-A	Amb.	71.6	72.7	0.21
	Ice	32.5	32.7	0.04
	Boil	212.2	214.2	0.30

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 5/30/911 Calibrator Name R.S.

Ambient Temp 92° Barometric Pressure 29.90 in. Hg

Reference: Mercury-in-glass ✓

Other

Thermocouple No.	Source (specify)	Reference thermometer temperature deg C / deg F	Thermocouple indicator temperature deg F	Percent error %
4B	Ice Bath	.1°C / 32.4°F	33°	1.8
	Ambient Air	24.0°C / 75.2°F	75°	0.3
	Boiling H_2O	98.0°C / 208.4°F	210°	0.8
4A	Ice Bath	0.7°C / 33.3°F	35°	5.1
	Ambient Air	23.7°C / 74.6°F	74°	0.8
	Boiling H_2O	98.8°C / 209.8°F	211°	0.6
5A	Ice Bath	0.2°C / 32.3°F	34°	5.3
	Ambient Air	23.6°C / 74.5°F	74°	0.7
	Boiling H_2O	98.2°C / 208.8°F	210°	0.6
• Bad Thermocouple 5B	~~Ice Bath~~	~~0.3°C / 32.5°F~~	~~34°~~	
	~~Ambient Air~~			
	~~Boiling H_2O~~	~~98.1°C / 208.6°F~~	~~210°~~	

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 9/30/91 Calibrator Name [illegible]

Ambient Temp 74° Barometric Pressure 30.33 in. Hg

Reference: Mercury-in-glass _____

Other Fluke Thermometer

Thermocouple No.	Source (specify)	Reference thermometer temperature deg F	Thermocouple indicator temperature deg F	Percent error %
1A	Ambient	69.8°	69.08	0.001
	Ice Bath	32.36°	32.36°	0.0
	Boiling H_2O	212.4°	212.6°	0.008
1B	Ambient	70.5°	70.7°	0.003
	Ice Bath	33.4°	32.8°	0.001
	Boiling H_2O	212.6°	212.8°	0.0002

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 1-30-92 Calibrator Name D. Slater

Ambient Temperature 68° F Barometric Pressure 29.80 in. Hg

Reference: Hg-in-glass

Other Fluke 52

Thermocouple No.	Source (specify)	Reference thermometer temperature °F	Thermocouple indicator temperature °F	Percent error %
6B	Ambient	66.2	67.8	0.3
	Ice Bath	32.2	33.4	0.24
	Boiling H_2O	211.0	211.4	0.06
5A	Ambient	68.6	67.6	0.19
	Ice Bath	32.2	32.4	0.04
	Boiling H_2O	211.4	211.6	0.03
5C	Ambient	68.4	67.8	0.11
	Ice Bath	32.2	31.6	0.12
	Boiling H_2O	211.2	212.2	0.15
6A	Ambient	68.8	67.6	0.23
	Ice Bath	32.2	32.0	0.04
	Boiling H_2O	211.2	211.6	0.06

Source: ice bath, ambient air, boiling H2O, hot oil

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

TEMPERATURE CALIBRATION DATA FORM

Date 2/21/92 Calibrator Name P. Slater

Ambient Temperature 72° F Barometric Pressure 30.02 in. Hg

Reference: Hg-in-glass

Other Fluke 52

Thermocouple No.	Source (specify)	Reference thermometer temperature °F	Thermocouple indicator temperature °F	Percent error %
6C	Ambient	71.4	71.0	0.08
	Ice Bath	31.8	31.0	0.16
	Boiling H_2O	214.2	213.8	0.06
5A	Ambient	71.2	71.4	0.04
	Ice Bath	31.6	31.8	0.04
	Boiling H_2O	212.6	212.2	0.06
7B	Ambient	71.8	71.8	0.0
	Ice Bath	31.8	31.0	0.16
	Boiling H_2O	212.6	212.8	0.04

Source: ice bath, ambient air, boiling H2O, hot oil

iea

$$\% \text{ error} = \frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 1.5\%$$

tempcal.wk1

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-2-92 Calibrator Name CJ

Indicator No. _____ Serial No. 007

Calibration Device No. M-2 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	002	
2		200	203	
3		400	401	
4		600	604	
5		800	804	
6		100	99	
7		300	302	
8		500	500	
9		700	701	
10		900	901	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-2-92 Calibrator Name [illegible]

Indicator No. _____ Serial No. 007

Calibration Device No. M-3 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	004	
2		200	204	
3		400	401	
4		600	603	
5		800	801	
6		100	100	
7		300	302	
8		500	499	
9		700	699	
10		900	898	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-2-92 Calibrator Name CJ

Indicator No. _____ Serial No. 007

Calibration Device No. M-5 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	005	
2		200	205	
3		400	400	
4		600	602	
5		800	800	
6		100	101	
7		300	302	
8		500	499	
9		700	699	
10		900	897	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-3-92 Calibrator Name CJ.

Indicator No. _____ Serial No. 007

Calibration Device No. M-6 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	004	
2		200	205	
3		400	402	
4		600	604	
5		800	804	
6		100	100	
7		300	303	
8		500	501	
9		700	702	
10		900	901	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-2-92 Calibrator Name [illegible]

Indicator No. _____ Serial No. 007

Calibration Device No. M-7 Manufacturer Omega

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	005	
2		200	204	
3		400	399	
4		600	601	
5		800	800	
6		100	100	
7		300	301	
8		500	498	
9		700	698	
10		900	896	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-2-92 Calibrator Name [illegible]

Indicator No. _____ Serial No. 007

Calibration Device No. M-8 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	0.003	
2		200	204	
3		400	400	
4		600	604	
5		800	803	
6		100	100	
7		300	302	
8		500	499	
9		700	701	
10		900	900	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

NOZZLE CALIBRATION

Date 15 May 1990 Calibrated by David Prater
Jerry Bowser

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
#3 A	.084	.085	.086	.002	.085
#4 A	.118	.118	.118	.000	.118
#5 A	.150	.149	.148	.002	.149
#6 A	.173	.172	.173	.001	.173
#7 A	.218	.217	.217	.001	.217

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 2 APR 90 Calibrated by DAVID PRATER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
IEA #8A	0.250	0.249	0.250	0.001	0.250

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 5/15/90 Calibrated by JERRY BOWSER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
# 8 A	.250	.250	.250	.000	.250
# 9 A	.279	.281	.282	.003	.281
# 10 A	.312	.312	.312	000	.312
# 11 A	.338	.338	.338	.000	.338
# 12 A	.374	.374	3.73	.001	.374

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 5/15/90

Calibrated by DAVID PRATER
JERRY BOWSER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
#13A	.395	.398	.398	.003	.397
#14A	.445	.445	.445	.000	.445
#15A	.470	.472	.471	.002	.471
#16A	.490	.490	.489	.001	.490
* #20A	.613	.621	.615	.008	

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

* EXCEEDS MAXIMUM TOLERANCE

NOZZLE CALIBRATION

Date 5/15/90

Calibrated by DAVID PRATER
JERRY BOWSER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
#24A	.752	.753	.753	.001	.753

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 5/5/90

Calibrated by DAVID PRATER
GERALD BROWSER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
# 3 B	.089	.091	.090	.002	.090
# 4 B	.118	.118	.118	.000	.118
# 5 B	.150	.148	.149	.002	.149
# 6 B	.171	.174	.173	.003	.173
# 7 B	.215	.217	.217	.002	.216

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 5/15/90 Calibrated by DAVID PRATER
GERALD BOWSER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
# 8 B	.242	.242	.243	.001	.242
# 9 B	.281	.281	.281	.000	.281
# 10 B	.311 ~~.339~~	.310 ~~.339~~	.311 ~~.339~~	.001 ~~.000~~	.311 ~~.339~~
# 11 B	.339	.339	.339	.000	.339
# 12 B	.369	.369	.368	.001	.369

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 5/15/90 Calibrated by DAVID PRATER
GERALD BOWSER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
# 13 B	.397	.399	.398	.002	.398
# 14 B	.438	.438	438	.000	.438
# 15 B	.472	.473	.473	.001	.473
# 16 B	.492	.492	.492	.000	.492
# 20 B	610	.617	6.10		

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 5/15/90 Calibrated by DAVID PRATER
GERALD BOWSER

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
#24B	.756	.756	.755	001	.756

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET G

NOZZLE CALIBRATION

Date 6/26/91 Calibrated by MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
G.19	0.196	0.195	0.197	0.002	0.196
G.25	0.235	0.234	0.234	0.001	0.234
G.28	0.276	0.277	0.277	0.001	0.277
G.31	0.310	0.310	0.309	0.001	0.310
G.38	0.394	0.396	0.395	0.002	0.395

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET G

NOZZLE CALIBRATION

Date 6/26/91 Calibrated by MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
G.41	0.395	0.395	0.396	0.001	0.395
G.44	0.429	0.427	0.430	0.003	0.429
G.50	0.494	0.491	0.493	0.003	0.493
G.63	0.620	0.622	0.624	0.004	0.622
G.75	0.746	0.745	0.742	0.004	0.744

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET H

NOZZLE CALIBRATION

Date 6/28/91 Calibrated by MCK

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
H.19	0.197	0.197	0.196	0.001	0.197
H.25	0.236	0.235	0.236	0.001	0.236
H.28	0.278	0.277	0.277	0.001	0.277
H.31	0.309	0.309	0.309	0.000	0.309
H.38	0.375	0.371	0.373	0.004	0.373

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET H

NOZZLE CALIBRATION

Date 6/25/91 Calibrated by MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
H.42	0.431	0.433	0.430	0.003	0.431
H.44	0.431	0.429	.430	0.003	0.429
H.50	0.496	0.492	0.494	0.004	0.494
H.63	0.623	0.621	0.622	0.002	0.622
H.75	0.746	0.744	0.743	0.003	0.744

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET J

NOZZLE CALIBRATION

Date 7/23/91 Calibrated by MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	D, in.	Davg
J.19	0.193	0.193	0.192	0.001	0.193
J.24	0.236	0.236	0.236	0.000	0.236
J.25	0.238	0.238	0.238	0.000	0.238
J.44	0.430	0.430	0.428	0.002	0.429
J.31	0.309	0.310	0.310	0.001	0.310
J.38	0.377	0.377	0.378	0.001	0.377
J.40	0.394	0.393	0.394	0.001	0.394
J.50	0.495	0.494	0.495	0.001	0.495
J.63	0.622	0.623	0.625	0.003	0.623
J.75	0.746	0.742	0.742	0.004	0.743

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET K

NOZZLE CALIBRATION

Date 6/25/91 Calibrated by MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
K.20	0.197	0.194	0.194	0.003	0.195
K.25	0.235	0.235	0.236	0.001	0.235
K.28	0.272	0.270	0.272	0.002	0.271
K.31	0.310	0.309	0.311	0.002	0.310
K.38	0.376	0.377	0.375	0.002	0.376

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET K

NOZZLE CALIBRATION

Date 6/25/91 Calibrated by MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	delta D, in.	Davg
K.40	0.393	0.393	0.394	0.001	0.393
K.50	0.494	0.493	0.495	0.002	0.494
K.44	0.430	0.430	0.430	0.000	0.430
K.63	0.625	0.626	0.625	0.001	0.625
K.75	0.740	0.742	0.744	0.004	0.742

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

delta D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

SET L

NOZZLE CALIBRATION

Date 6/30/91 Calibrated by MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	D, in.	Davg
L.20	0.195	0.194	0.195	0.001	0.195
L.25	0.263	0.263	0.263	0.000	0.263
L.25	.235 ~~0.275~~	.236 ~~0.274~~	.236 ~~0.274~~	0.001	0.236 ~~0.274~~ MR
L.38	0.375	0.371	0.371	0.004	0.372
L.40	0.392	0.393	0.393	0.001	0.373
L.47	0.471	0.472	0.474	0.003	0.472
L.50	0.496	0.495	0.497	0.002	0.496
L.44	0.430	0.430	0.430	0.000	0.430
L.63	0.625	0.624	0.623	0.002	0.624
L.75	0.743	0.746	0.745	0.003	0.745

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 6/26/91

Calibrated by: MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	D, in.	Davg
G.19	0.196	0.195	0.197	0.002	0.196
G.25	0.235	0.234	0.234	0.001	0.234
G.28	0.276	0.277	0.277	0.001	0.277
G.31	0.310	0.310	0.309	0.001	0.310
G.38	0.394	0.396	0.395	0.002	0.395
G.41	0.395	0.395	0.396	0.001	0.395
G.50	0.494	0.491	0.493	0.003	0.493
G.63	0.620	0.622	0.624	0.004	0.622
G.75	0.746	0.745	0.742	0.004	0.744

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 6/26/91

Calibrated by: MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	D, in.	Davg
H.19	0.197	0.197	0.196	0.001	0.197
H.25	0.236	0.235	0.236	0.001	0.236
H.28	0.278	0.277	0.277	0.001	0.277
H.31	0.309	0.309	0.309	0.000	0.309
H.38	0.375	0.371	0.373	0.004	0.373
H.42	0.431	0.433	0.430	0.003	0.431
H.50	0.496	0.492	0.494	0.004	0.494
H.63	0.623	0.621	0.622	0.002	0.622
H.75	0.746	0.744	0.743	0.003	0.744

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 6/26/91 Calibrated by: MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	D, in.	Davg
J.19	0.193	0.193	0.192	0.001	0.193
J.24	0.236	0.236	0.236	0.000	0.236
J.26	0.259	0.260	0.259	0.001	0.259
J.27	0.274	0.273	0.273	0.001	0.273
J.31	0.309	0.310	0.310	0.001	0.310
J.38	0.377	0.377	0.378	0.001	0.377
J.50					
J.75	0.746	0.742	0.742	0.004	0.743

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 6/26/91 Calibrated by: MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	D, in.	Davg
K.20	0.197	0.194	0.194	0.003	0.195
K.25	0.235	0.235	0.236	0.001	0.235
K.28	0.272	0.270	0.272	0.002	0.271
K.31	0.310	0.309	0.311	0.002	0.310
K.38	0.376	0.377	0.375	0.002	0.376
K.50	0.494	0.493	0.495	0.002	0.494

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

NOZZLE CALIBRATION

Date 6/25/91 Calibrated by: MCR

Nozzle identification number	D1, in.	D2, in.	D3, in.	D, in.	Davg
L.20	0.195	0.194	0.195	0.001	0.195
L.28	0.275	0.274	0.274	0.001	0.274
L.50	0.496	0.495	0.497	0.002	0.496
L.38	0.375	0.371	0.371	0.004	0.372

where:

D1, D2, D3 = nozzle diameter measured on a different diameter, in.
Tolerance = measure within 0.001 in.

D = maximum difference in any two measurements, in.
Tolerance = 0.004 in.

Davg = average of D1, D2, and D3.

I-CHEM

CERTIFICATE OF ANALYSIS

Analysis of Lot 2002022 January 02, 1992

Lot 2002022 has been cleaned in accordance with I-CHEM's Performance-Based Specifications. Randomly selected samples from this lot were analyzed using ICP/Mass Spectroscopy, ICP/Atomic Emission Spectroscopy, Furnace Atomic Absorption, Flame Atomic Absorption, and Cold Vapor Atomic Absorption. The following analytical results were obtained.

Element	Concentration (ug/L)	Element	Concentration (ug/L)	Element	Concentration (ug/L)
Aluminum	< 80	Antimony	< 5	Arsenic	< 2
Barium	< 20	Beryllium	< 0.5	Cadmium	< 1
Calcium	< 500	Chromium	< 10	Cobalt	< 10
Copper	< 10	Iron	< 50	Lead	< 2
Magnesium	< 100	Manganese	< 10	Mercury	< 0.2
Nickel	< 20	Potassium	< 750	Selenium	< 2
Silver	< 5	Sodium	< 5000	Thallium	< 5
Vanadium	< 10	Zinc	< 10		

Selected samples from this lot were also analyzed for semivolatiles by GC/Mass Spectroscopy and pesticides by GC/Electron Capture Detector. The following analytical results were obtained.

Compound	Concentration (ug/L)	Compound	Concentration (ug/L)	Compound	Concentration (ug/L)
Acenaphthene	< 5	Acenaphthylene	< 5	Anthracene	< 5
Benzo(a)anthracene	< 5	Benzo(a)pyrene	< 5	Benzo(b)fluoranthene	< 5
Benzo(k)fluoranthene	< 5	Benzo(g,h,i)perylene	< 5	Benzoic Acid	< 20
Benzyl Alcohol	< 5	4-Bromophenyl-phenylether	< 5	Butylbenzylphthalate	< 5
4-Chloroaniline	< 5	4-Chloro-3-methylphenol	< 5	bis-(2-Chloroethoxy)methane	< 5
bis-(2-Chloroethyl)ether	< 5	bis-(2-Chloroisopropyl)ether	< 5	2-Chloronaphthalene	< 5
2-Chlorophenol	< 5	4-Chlorophenyl-phenylether	< 5	Chrysene	< 5
Di-n-butylphthalate	< 5	Di-n-octylphthalate	< 5	Dibenzo(a,h)anthracene	< 5
Dibenzofuran	< 5	1,2-Dichlorobenzene	< 5	1,4-Dichlorobenzene	< 5
1,3-Dichlorobenzene	< 5	3,3'-Dichlorobenzidine	< 5	2,4-Dichlorophenol	< 5
Diethylphthalate	< 5	Dimethylphthalate	< 5	2,4-Dimethylphenol	< 5
4,6-Dinitro-2-methylphenol	< 20	2,4-Dinitrophenol	< 20	2,4-Dinitrotoluene	< 5
2,6-Dinitrotoluene	< 5	bis-(2-Ethylhexyl)phthalate	< 5	Fluoranthene	< 5
Fluorene	< 5	Hexachlorobenzene	< 5	Hexachlorobutadiene	< 5
Hexachlorocyclopentadiene	< 5	Hexachloroethane	< 5	Indeno(1,2,3-cd)pyrene	< 5
Isophorone	< 5	2-Methylnaphthalene	< 5	2-Methylphenol	< 5
4-Methylphenol	< 5	2-Nitroaniline	< 20	3-Nitroaniline	< 20
4-Nitroaniline	< 20	N-Nitroso-di-n-propylamine	< 5	N-Nitrosodimethylamine	< 5
N-Nitrosodiphenylamine	< 5	Naphthalene	< 5	Nitrobenzene	< 5
2-Nitrophenol	< 5	4-Nitrophenol	< 20	Pentachlorophenol	< 20
Phenanthrene	< 5	Phenol	< 5	Pyrene	< 5
1,2,4-Trichlorobenzene	< 5	2,4,5-Trichlorophenol	< 20	2,4,6-Trichlorophenol	< 5
1,2-Diphenylhydrazine	< 5	Benzidine	< 40	Aldrin	< 0.01
4,4'-DDD	< 0.02	Endosulfan II	< 0.02	Alpha-BHC	< 0.01
4,4'-DDE	< 0.02	Endosulfan Sulfate	< 0.02	Beta-BHC	< 0.01
4,4'-DDT	< 0.02	Endrin	< 0.02	Delta-BHC	< 0.01
Dieldrin	< 0.02	Endrin Aldehyde	< 0.02	Gamma-BHC	< 0.01
Endosulfan I	< 0.01	Heptachlor	< 0.01	Heptachlor Epoxide	< 0.01
Methoxychlor	< 0.10	Endrin Ketone	< 0.02	Alpha-Chlordane	< 0.01
Gamma-Chlordane	< 0.01	Toxaphene	< 1.00	Aroclor-1016	< 0.20
Aroclor-1221	< 0.20	Aroclor-1232	< 0.40	Aroclor-1242	< 0.20
Aroclor-1248	< 0.20	Aroclor-1254	< 0.20	Aroclor-1260	< 0.20
Aroclor-1262	< 0.20	Aroclor-1268	< 0.20		

Please keep this certificate for your records and to facilitate any necessary correspondence regarding this lot.

If additional information is required, contact our Technical Service Department at (800) 443-1689, outside CA, and (800) 262-5006, inside CA.

Randy E. Benson
Corporate Quality Assurance Manager

printed on recycled paper

Control No. 000002

ANALYTICAL BALANCE CALIBRATION FORM

Balance METTLER AE240 Serial Number L58883

Class of standard weights CLASS S #2511

Date	Analyst	0.500 g	1.0000 g	10.0000 g	50.0000 g	100.0000 g
8/5/91	BHR	0.500g	1.0001g	10.0000g	50.0000g	100.0000g
8/7/91	JWB	0.5000	1.0001	10.0001	50.0004	100.0002
8/9/91	JWB	0.5001	1.0002	10.0002	50.0005	100.0002
8/13/91	MCR	0.5001	1.0002	10.0002	50.0003 (MC)	100.0002
8/22/91	MCR	0.5000	1.0000	10.0000	50.0003	100.0000
	(CONTINUED FROM PAGE 0001)					
12-12-91	T.Drake	0.5000	1.0000	20.0001	50.0003	
12-13-91	T Drake	0.4999	1.0001	20.0002	50.0005	
12-14-91	T. DRAKE	0.5001	1.0002	20.0002	50.0002	
1/22/92	TASchank	0.5000	1.0000	10.0000	50.0002	99.9998
1/23/92	TASchank	0.5000	1.0000	10.0000	50.0003	99.9998
1/29/92	TASchank	0.5000	1.0000	10.0000	50.0002	99.9998
1/30/92	TASchank	0.5000	1.0001	10.0000	50.0003	99.9998
1/31/92	TASchank	0.5000	1.0001	10.0001	50.0004	100.0000
2/3/92	TASchank	0.5000	1.0000	10.0000	50.0002	99.9997
2/4/92	TASchank	0.5000	1.0000	10.0000	50.0002	99.9997
2/5/92	TASchank	0.5001	1.0000	10.0001	50.0002	99.9997
3/7/92	B. RAYFIELD	0.5000	1.0000	10.0001	50.0002	99.9998

c:\airdiv\form\balcal.frm

FIELD BALANCE CALBRATION DATA SHEET

Balance No.	Date	Calibrator	Mass determined for 295 g					
			5 g	Error	50 g	Error	~~100~~ g	Error
BB3000	3/10/92	B. RAYFIELD					297.6	0.4 g
"	3/11/92	B. RAYFIELD					297.7	0.3 g
"	3/12/92	B. RAYFIELD					297.7	0.3 g
"	3/13/92	B. RAYFIELD					297.7	0.3 g

Error must not exceed 0.5 grams at each point.

DRY GAS METER POST-TEST CALIBRATION
USING REFERENCE METER

DATE: 3-31-92 METER BOX NO. M-8

CALIBRATOR: CY BAROMETRIC PRESSURE (Pb) 29.50 in. Hg

INITIAL CALIBRATION Y: 1.005 ΔH@: 1.88

PLANT: L.A. Pacific PROJECT NO.:

AVERAGE ΔH DURING TESTING: 1.0 MAXIMUM VACUUM 1.0 in. Hg

Orifice manometer setting* ΔH in. H2O	Volume reference meter Vw ft3	Volume dry gas meter Vd ft3	Temperatures: Ref Meter Tw °F	Ref Meter Avg Tw °F	Dry gas meter Td °F	Dry gas meter Avg Td °F	Test duration θ min	Vacuum setting ** in. Hg	Calibr Factor Y	ΔH@ in. H2O
1.0	start 615.533 stop 621.083 dif 5.550	133.912 139.501 5.589	start 71 stop 72	71.5	start 72 stop 73	72.5	10	1.0	0.999	1.82
1.0	start 621.083 stop 626.632 dif 5.549	139.501 145.096 5.595	start 72 stop 70	71	start 73 stop 75	73	10	1.0	1.000	1.82
1.0	start 626.632 stop 632.173 dif 5.541	145.096 150.721 5.625	start 70 stop 71	70.5	start 75 stop 75	75	10	1.0	1.007	1.82
								Post-test Average***	1.002	1.82

* To be the average ΔH used during test series.

** To be the highest vacuum used during test series.

*** Post-test Y must be within the range, pre-test Y +/- 5% OK? ☒

Post-test ΔH@ should be within the range of the initial or pre-test ΔH@ +/- 0.20 in. H2O. OK? ☒

$$Y = \frac{(1.006)\,(Vw)\,(Pbar)\,(Td + 460)}{(Vd)\,(Pbar + \Delta H / 13.6)\,(Tw + 460)}$$

$$\Delta H@ = \frac{(0.0317)\,(\Delta H)}{(Pbar)\,(Td + 460)} \left[\frac{(Tw + 460)\,(\theta)}{(Vw)(1.006)} \right]^2$$

$$\text{Percent difference} = \frac{(\text{Avg inital Y}) - (\text{Post-test Y})}{(\text{Avg initial Y})}$$

dg[illegible]ptcal.wk1

THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-31-92 Calibrator Name CJ.

Indicator No. _____ Serial No. 107

Calibration Device No. M-8 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	003	
2		200	204	
3		400	400	0.00
4		600	604	
5		800	803	
6		100	99	
7		300	301	
8		500	499	
9		700	701	
10		900	900	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

DRY GAS METER POST-TEST CALIBRATION
USING REFERENCE METER

DATE: 4-1-92 METER BOX NO. M7

CALIBRATOR: CJ BAROMETRIC PRESSURE (Pb) 29.49 in. Hg

INITIAL CALIBRATION Y: 1.002 ΔH@: 1.87

PLANT: L.A. PACIFIC PROJECT NO.:

AVERAGE ΔH DURING TESTING: 1.0 MAXIMUM VACUUM 10 in. Hg

Orifice manometer setting* ΔH in. H2O	Volume reference meter Vw ft3	Volume dry gas meter Vd ft3	Temperatures: Ref Meter Tw °F	Ref Meter Avg Tw °F	Dry gas meter Td °F	Dry gas meter Avg Td °F	Test duration θ min	Vacuum setting ** in. Hg	Calibr Factor Y	ΔH@ in. H2O
1.0	start 667.054 stop 672.584 diff 5.530	630.697 636.273 5.576	start 75 stop 75	75	start 75 stop 77	76	10	10	1.001	1.85
1.0	start 672.584 stop 678.099 diff 5.515	636.273 641.825 5.552	start 75 stop 74	74.5	start 77 stop 78	77.5	10	10	1.003	1.85
1.0	start 678.099 stop 683.598 diff 5.499	641.825 647.395 5.570	start 74 stop 74	74	start 78 stop 78	78	10	10	0.999	1.86
								Post-test Average***	1.001	1.85

* To be the average Δ H used during test series.

** To be the highest vacuum used during test series.

*** Post-test Y must be within the range, pre-test Y +/- 5% OK? ☒

Post-test Δ H@ should be within the range of the initial or pre-test Δ H@ +/- 0.20 in. H2O. OK? ☒

$$Y = \frac{(1.006)\,(Vw)\,(Pbar)\,(Td + 460)}{(Vd)\,(Pbar + \Delta H / 13.6)\,(Tw + 460)}$$

$$\Delta H@ = \frac{(0.0317)\,(\Delta H)}{(Pbar)\,(Td + 460)} \left[\frac{(Tw + 460)\,(\theta)}{(Vw)(1.006)} \right]^2$$

$$\text{Percent difference} = \frac{(\text{Avg inital Y}) - (\text{Post-test Y})}{(\text{Avg initial Y})}$$

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THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 4-1-92 Calibrator Name C.J.

Indicator No. _____ Serial No. 007

Calibration Device No. M7 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	004	
2		200	203	
3		400	399	
4		600	600	
5		800	798	
6		100	99	
7		300	300	
8		500	497	
9		700	697	
10		900	895	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

DRY GAS METER POST-TEST CALIBRATION
USING REFERENCE METER

DATE: 3-30-92 METER BOX NO. M-5

CALIBRATOR: CJ BAROMETRIC PRESSURE (Pb) 29.50 in. Hg

INITIAL CALIBRATION Y: 0.998 ΔH@: 1.92

PLANT: L.A. Refi PROJECT NO.:

AVERAGE ΔH DURING TESTING: 10 MAXIMUM VACUUM 10 in. Hg

Orifice manometer setting* ΔH in. H2O	Volume reference meter Vw ft3	Volume dry gas meter Vd ft3	Temperatures: Ref Meter Tw °F	Ref Meter Avg Tw °F	Dry gas meter Td °F	Dry gas meter Avg Td °F	Test duration θ min	Vacuum setting ** in. Hg	Calibr Factor Y	ΔH@ in. H2O
1.0	start 598.216 stop 603.680 diff 5.464	914.843 920.379 5.536	start 71 stop 71	71	start 73 stop 75	74	10	10	0.997	1.874
1.0	start 603.680 stop 609.136 diff 5.456	920.379 925.931 5.552	start 71 stop 71	71	start 75 stop 76	75.5	10	10	0.996	1.874
1.0	start 609.136 stop 614.606 diff 5.470	925.931 931.464 5.533	start 71 stop 71	71	start 76 stop 77	76.5	10	10	1.003	1.861
								Post-test Average***	0.9987	1.87

* To be the average ΔH used during test series.

** To be the highest vacuum used during test series.

*** Post-test Y must be within the range, pre-test Y +/- 5% OK? ☒

Post-test ΔH@ should be within the range of the initial or pre-test ΔH@ +/- 0.20 in. H2O. OK? ☒

$$Y = \frac{(1.009)\,(Vw)\,(Pbar)\,(Td + 460)}{(Vd)\,(Pbar + \Delta H / 13.6)\,(Tw + 460)}$$

$$\Delta H@ = \frac{(0.0317)\,(\Delta H)}{(Pbar)\,(Td + 460)} \left[\frac{(Tw + 460)\,(\theta)}{(Vw)\,(1.009)} \right]^2$$

$$\text{Percent difference} = \frac{(\text{Avg inital } Y) - (\text{Post-test } Y)}{(\text{Avg initial } Y)}$$

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THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 3-31-92 Calibrator Name CJ

Indicator No. Serial No. 007

Calibration Device No. M-5 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	004	
2		200	204	
3		400	400	
4		600	602	
5		800	800	
6		100	100	
7		300	302	
8		500	498	
9		700	699	
10		900	897	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

DRY GAS METER POST-TEST CALIBRATION
USING REFERENCE METER

DATE: 4-1-92 METER BOX NO. M-2

CALIBRATOR: CJ BAROMETRIC PRESSURE (Pb) 29.49 in. Hg

INITIAL CALIBRATION Y: 1.01 ΔH@: 2.00

PLANT: L.A. Pacific PROJECT NO.:

AVERAGE ΔH DURING TESTING: 1.0 MAXIMUM VACUUM 10 in. Hg

Orifice manometer setting* ΔH in. H2O	Volume reference meter Vw ft3	Volume dry gas meter Vd ft3	Temperatures: Ref Meter Tw °F	Ref Meter Avg Tw °F	Dry gas meter Td °F	Dry gas meter Avg Td °F	Test duration θ min	Vacuum setting ** in. Hg	Calibr Factor Y	ΔH@ in. H2O
1.0	start 683.913 stop 690.279 diff 6.366	175.420 181.779 6.359	start 71 stop 71	71	start 68 stop 73	70.5	12	10	1.004	2.002 ~~1.981~~
1.0	start 690.279 stop 695.580 diff 5.301	181.779 187.081 5.302	start 71 stop 70	70.5	start 73 stop 75	74	10	10	1.010	1.990
1.0	start 695.580 stop 700.871 diff 5.291	187.081 192.427 5.346	start 70 stop 68	69	start 75 stop 75	75	10	10	1.010	1.981
								Post-test Average***	1.010	1.991

* To be the average ΔH used during test series.

** To be the highest vacuum used during test series.

*** Post-test Y must be within the range, pre-test Y +/- 5% OK? [X]

Post-test ΔH@ should be within the range of the initial or pre-test ΔH@ +/- 0.20 in. H2O. OK? [X]

$$Y = \frac{(1.007)\,(Vw)\,(Pbar)\,(Td + 460)}{(Vd)\,(Pbar + \Delta H / 13.6)\,(Tw + 460)}$$

$$\Delta H@ = \frac{(0.0317)\,(\Delta H)}{(Pbar)\,(Td + 460)} \left[\frac{(Tw + 460)\,(\theta)}{(Vw)\,(1.007)} \right]^2$$

$$\text{Percent difference} = \frac{(\text{Avg inital Y}) - (\text{Post-test Y})}{(\text{Avg initial Y})}$$

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THERMOCOUPLE DIGITAL INDICATOR
CALIBRATION DATA FORM

Date 4-1-92 Calibrator Name CJ

Indicator No. _____ Serial No. 007

Calibration Device No. M-2 Manufacturer OMEGA

Test Point No.	Millivolt Signal	Equivalent Temperature deg. F	Digital Indicator Temperature deg. F	Percent difference %
1		0	001	
2		200	203	
3		400	399	
4		600	603	
5		800	803	
6		100	98	
7		300	300	
8		500	499	
9		700	700	
10		900	900	

Percent difference must be less than or equal to 0.5%

Percent Difference:

$$\frac{(\text{Ref temp} + 460) - (\text{Test temp} + 460)}{(\text{Ref temp} + 460)} \times 100\% \text{ should be} < 0.5\%$$

APPENDIX I

PROCESS INFORMATION

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-10-92 Shift A Pressing Cycle

Foreman Mickey Davis Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
13/2	49 7/8 x 2.45	38	638	0		638
15/2	49 7/8 x 2.45	1	16	0		16

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-2		-15	1:05-1:50 Repair conveyor dryer
	-4			2:02-2:06 : Put loader belt on F-4D tray after it had pulled out of gear
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	-12		-15	-27

Comments: 911

Furnish: 70,~~594~~

Resin: 91.5 gallons/1000 sq. ft. 3/4

Wax: 9390 hourly rate 8

Sup. 3/4

Ammonate dumped in pit.

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-10-92 Shift C Pressing Cycle

Foreman Mickey-Mike Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
15/32	49½ x 245	5	80	0		80
1 1/16	49½ x 245	9	144	0		144
1"	49½ x 245	31	496	0		496

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	11			3:19-3:30 Pin came out of master link on flying saw chain
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	11			11

Comments:

Footage: 71,004

NO [illegible] Pesin: 604

Pulp: 8488

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-10 92 Shift B Pressing Cycle

Foreman Robert Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1"	52¼x267	2	32			32
1"	52¼x277	1	16			16
1"	52¼x280	1	16			16
1"	52¼x286	2	32			32
1"	52¼x293	4	64			64
1"	51x295	2	32			32

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				594

Comments:

Footage 69,8[illegible]

Usage 926

Rate 5725

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location _____

Date _____ Shift _____ Pressing Cycle _____

Foreman _____ Hours _____ Total Cycle _____

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
.984	51 x 295	4	64			64
7/8	52 1/4 x 280	6	96			96
7/8	49 7/8 x 245	6	96			96
7/8	47 1/4 x 245	12	192			192
3/4	51 1/2 x 295	4	64			64

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments: _____

SD 5344

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-9-98

FT A-7-3

OPERATOR Ben Lee

BOARD THICKNESS 13/16

BOARD SIZE [illegible]

BOARD TYPE D.P

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	~~LINE TEMP.~~ Spec. 2	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	10:00	310	708	720		Pot 60	Time :45	780 340	80	12	
2			720	732					71	12	
3			732	744					68	12	
4			744	756					72	12	
C 5			756	808					71	12	
6			808	819					77	11	
7			819	830					74	11	
8			830	842					75	12	
9			842	854					79	12	
10			854	906					84	12	
11			906	918					78	12	
12			918	930					74	12	
13			930	942					71	12	
14			942	954					74	12	
C 15			954	1006					73	12	
16			1006	1018					71	12	
17			1018	1030					70	12	
18			1030	1042					70	12	
19			1042	1054					67	12	
C 20			1054	1105					70	11	
21			1105	1116					69	11	
22			1116	1128					65	12	
23			1128	1139					61	11	
24			1139	1150					62	11	
C 25			1150	1201					63	11	
26			1201	1213					61	12	
27			1213	1224					62	11	
28			1224	1235					60	11	
[illegible]			1235	1247					62	12	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-10-92

SHIFT A 7-3

OPERATOR Ben Lee

BOARD THICKNESS 1 3/16 - 1 5/32

BOARD SIZE 48 7/8 x 245

BOARD TYPE D.P.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	CYCLE ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~[illegible]~~	INTERMEDIATE ~~[illegible]~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	10:00	310	1247	1259		Pot 60	Timer 1:45	780 340	60	12	
C 31			1259	111					65	12	
32			111	131					65	20	
Shop 33	Shop		131	149					63	18	
34			149	202					66	13	-4) 2:02-2:06 Put loader
35			206	218					65	12	belt on F4 tray after
36			218	230					64	12	I had pulled mat out
37			230	243					64	13	of press
38			243	255					64	12	
39			255	307					65	12	

1 3/16 x 48 7/8 x 245

1 5/32 x 48 7/8 x 245

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-10-92

SHIFT C 3-11

OPERATOR Ben-Mickey

BOARD THICKNESS 1 5/32-1 1/16-1"

BOARD SIZE 49 7/8 x 8'

BOARD TYPE D.P.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE/Position HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	10:00	310	307	319		HOT 60	45	800 500	64	12	-11 3:19-3:30 Pin Curve
2			330	342					63	12	out of [illegible] link in
3			342	354					65	12	flying Saw Chain
4			354	405					64	11	
5			405	417					63	12	
6	9:40		417	429				700 250	[illegible]	10	
7			429	439					[illegible]	10	
8			439	449					67	10	
9			449	500					62	11	
10			500	512					70	12	
11			512	523					71	12	
12			523	534					78	11	
13			534	545					74	11	
14			545	556					75	11	
[illegible]			556	606				700 250	62	10	
16			606	616					60	10	
17			616	625					58	9	
18			625	635					59	10	
19			635	645					56	10	
20			645	655					58	10	
21			655	705					60	10	
22			705	716					59	11	
23			716	726					66	10	
24			726	736					70	10	
25			736	746					78	10	
26			746	756					77	10	
27			756	806					78	10	
28			806	816					79	10	
29			816	826					77	10	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-10-1992

SHIFT C 3-11

OPERATOR Ben-Mickey

BOARD THICKNESS

BOARD SIZE

BOARD TYPE D.P.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE PSI	PRESSURE PSI	PRESSURE PSI	PRESSURE PSI
MIN	MIN	MIN	MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~PRESS~~	INTERMEDIATE ~~TIMER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	820	310	826	836	640	Poi 60	Timer 15	190	69	10	
31			836	846					72	10	
32			846	856					74	10	
33			856	906					72	10	
34			906	916					71	10	
35			916	926					67	10	
36			926	936					67	10	
37			936	945					74	9	
38			945	954					74	9	
39			954	1003					67	9	
40			1003	1014					71	11	
41			1014	1024					66	10	
42			1024	1034					68	10	
43			1034	1044					72	10	
44			1044	1053					80	9	
45			1053						31		

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-10-1992

SHIFT B 11-7

OPERATOR Mickey Gilmore

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	~~LINE TEMP.~~ CYC 2	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1		310	1104	1117		POT 60	TIMER 15		81	13	
2			1117	1128					84	11	
3			1128	1138					86	10	
4			1138	1149					85	11	
5			1149	1159					86	10	
6			1159	1210					83	11	
7			1210	1222					67	12	
8			1222	1234					62	12	
9			1234	1245					73	11	
10			1245	1256					73	11	
11			1256	109					82	14	
12			109	122					74	13	
13			122	135					88	13	
14			135	148					90	13	
15			148	200					85	12	
16			200	211					74	11	
17			211	222					80	11	
18			222	232					82	10	
19			232	242					[illegible]	10	
20			242	253					75	11	
21			253	304					78	11	
22			304	314					80	10	
23			314	325					77	11	
24			325	336					79	11	
25			336	346					78	10	
26			346	356					77	10	
27			356	407					76	11	
28			407	417					74	10	
29			417	427					72	10	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-10-92

SHIFT B-11-7

OPERATOR Micky

BOARD THICKNESS 1

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	Cycle ~~TIME~~ ~~TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	Position ~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	820	310	427	438		Pot 60	Timer 15		72	11	
31			438	448					71	10	
32			448	458					73	10	
33			458	508					72	10	
34			508	518					66	10	
35			518	529					68	11	
36			529	538					66	9	
37			538	550					65	12	
38			550	600					72	10	
39			600	612					72	12	
40			612	621					70	9	
41			621	631					72	10	
42			631	641					73	10	
43			641	651					71	10	
44			651						87		

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-11-92 Shift A Pressing Cycle

Foreman Mickey Davis Hours 7-3 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
[illegible]	3/4	51½x295	8	128	0		128
[illegible]	3/4	51½x295	5	80	0		80
[illegible]	3/4	51½x295	13	208	0		208
[illegible]	3/4	51½x295	24	384	0		384

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-20			11:34-11:54 Put #2 B' loader [illegible]
				belt on & start up
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	-20			-20

Comments:

No mats dumped in pit

Footage: 76,800

Pieces: 84.6

[illegible]: 10,017

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-11-1992 Shift C Pressing Cycle

Foreman Mike Bloom Hours 3-11 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
[illegible]	3/4	51½x295	29	464	0		464
Stock	3/4	51½x295	24	384	0		384

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No down time
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: No [illegible] Recorded.

Footage: 81,408

Press: 84.5

Pack: 10,176

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 2-11-92 Shift D Pressing Cycle

Foreman George Hours 11-7 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
S.W	3/4	51½x295	20	320	0		320
H.11	3/4	51½x297	1	16	0		16
	3/4	51½x257	1	16	0		16
L.P.	.708	51½x295	12	192	0		192
.01.	9/16	51½x259	25	400	0		400
	7/16	51½x[illegible]		16	0		16

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
- 3				5:49 - 5:52 Down at press #8
				pressure switch stuck.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
- 3				- 3

Comments: No [illegible] Dumped

Eng. Hr. 77,352 ✓

Hrs. 898

Prod. 9791

SD 5344

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-11-1992

SHIFT A 7-3

OPERATOR Ben Lee

BOARD THICKNESS 3/4

BOARD SIZE 51 1/2 x 295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	~~CONE TEMP.~~ Cycle	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
	7:40	305	701	710		Pot 30	Timer :45	680 260	86	9	
2			710	719					89	9	
3			719	728					86	9	
4			728	737					85	10	
5			737	745					85	10	
6			745	759					83	11	
7			759	810					84	11	
8			810	821					79	11	
9			821	832					80	11	
10			832	843					83	11	
11			843	854					82	11	
12			854	905					84	11	
13	7:20		905	914					85	9	
14			914	924					94	10	
15			924	933				650 230	89	9	
16			933	942					88	9	
17			942	951					87	9	
18			951	1000					85	9	
19			1000	1009					79	9	
20			1009	1019					81	10	
21			1019	1029					83	10	
22			1029	1038					84	9	
23			1038	1047					85	9	
24			1047	1056					86	9	
25			1056	1105					80	9	
26			1105	1115					80	10	
27			1115	1124					88	9	
28			1124	1124					79	0	
29			1124	1134					90	10	-20 11:34-11:54 Put loader belt on (#2 X') + start up

Pattison off Nashville

United

Stack

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-11-92

SHIFT A 23

OPERATOR Ben Lee

BOARD THICKNESS 3/4

BOARD SIZE 51½1295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE (PSI) Line ~~HIGH~~ Feed	INTERMEDIATE ~~UPPER~~ POT	INTERMEDIATE ~~LOWER~~ TIME	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	7:00	310	1154	1203	44	POT 60	TIME 145	650 230	86	9	
31			1203	1212					86	9	
32			1212	1221					84	9	
33			1221	1230					82	9	
34			1230	1239					83	9	
35			1239	1249					84	9	
36			1249	1256					85	8	
37			1256	106					87	8	
38			106	115					84	9	
39			115	124					86	9	
40			124	133					84	9	
41			133	142					85	9	
42			142	151					86	9	
43			151	200					86	9	
44			200	209					84	9	
45			209	218					85	9	
46			218	227					86	9	
47			227	236					87	9	
48			236	245					86	9	
49			245	254					85	9	
50			254	303					84		
51											

3/4 51½ x 295 STOCK

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-11-92

SHIFT C-3-11

OPERATOR Ben + Anthony

BOARD THICKNESS 3/4

BOARD SIZE 51½ x 295

BOARD TYPE M.O.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

	LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
3/4	1	700	310	3:03	3:12	650	Pet :10	Timer :45	230	87	9	
51½ x 295	2			3:12	3:21					86	9	
L.P.	3			3:21	3:30					86	9	
L.W	4			3:30	3:38	610			190	85	8	
	5			3:38	3:47					87	9	
	6			3:47	3:57					85	10	
3/4	7 c			3:57	4:06	590			170	89	9	
51½ x 295	8			4:06	4:15					85	9	
	9			4:15	4:24					84	9	
stock	10			4:24	4:33					82	9	
	11			4:33	4:42					86	9	
	12			4:42	4:51					85	9	
	13			4:51	5:00					84	9	
	14 c			5:00	5:09					83	9	
	15			5:09	5:18					84	9	
	16			5:18	5:27					89	9	
	17			5:27	5:36					89	9	
	18			5:36	5:45					90	9	
	19			5:45	5:54					90	9	
	20 c			5:54	6:03					89	9	
	21			6:03	6:12					95	9	
	22			6:12	6:21					83	9	
	23			6:21	6:30					82	9	
	24			6:30	6:39					83	9	
	25			6:39	6:48					84	9	
	26			6:48	6:57					86	9	
	27 c			6:57	7:05					87	8	
	28			7:05	7:14					89	9	
51½ x 295	29			7:14	7:24					85	10	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-11-1992

SHIFT C 3:11

OPERATOR Ben-Anthony

BOARD THICKNESS 3/4

BOARD SIZE 51½x8.25

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

3/4
51½ x 8.25
..P.
..W.

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	700	910	7:24	7:32	590	pot :60	Timer :45	170	89	8	
31			7:32	7:41					84	9	
32			7:41	7:51	650			230	86	10	
33			7:51	8:01					88	10	
34 C			8:01	8:11					86	10	
35			8:11	8:20					84	9	
36			8:20	8:29					88	9	
37			8:29	8:37					86	8	
38			8:37	8:46					85	9	
39			8:46	8:55					88	9	
40 C			8:55	9:04					87	9	
41			9:04	9:13					89	9	
42			9:13	9:22					88	9	
43			9:22	9:31					86	9	
44			9:31	9:40					84	9	
45			9:40	9:49					88	9	
46			9:49	9:58					86	9	
47 C			9:58	10:07					85	9	
48			10:07	10:15					89	8	
49			10:15	10:23					87	8	
50			10:23	10:32					86	9	
51			10:32	10:42					85	10	
52			10:42	10:52					87	10	
53 C			10:52						88		
54											
55											
56											
57											
58											

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-11-92

SHIFT D 11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE PSI	PRESSURE PSI	PRESSURE PSI	PRESSURE PSI
MIN	MIN	MIN	MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	cycle ~~CINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE, Station HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	700	310	11:02	11:12	650	pot :60	Timer :45	220	86	10	
2			11:12	11:20					84	8	
3			11:20	11:29					86	9	
4			11:29	11:38					95	9	
5			11:38	11:47					84	9	
6			11:47	11:55					86	8	
7 C			11:55	12:05					84	10	
8			12:05	12:14					86	9	
9			12:14	12:24					86	10	
10			12:24	12:32					85	8	
11			12:32	12:41					84	9	
12			12:41	12:50					86	9	
13			12:50	12:59					86	9	
14			12:59	1:08					85	9	
15 C			1:08	1:17					86	9	
16			1:17	127					85	10	
17			127	136					84	9	
18			136	145					85	9	
19			145	154					86	9	
20			154	2:03					87	9	
297 21 C			2:03	212					85	9	
259 22			212	2:20					88	8	
.708 23	700		2:20	2:29	590			170	87	9	
51½ 24			2:29	2:38					86	9	
195 25			2:38	2:46					87	8	
.P. 26			2:46	2:55					85	9	
27 C			2:55	3:03					88	8	
28			3:03	3:1[illegible]					84	9	
29			3:1[illegible]	3:19					81	7	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-11-1992

SHIFT D 11-7

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~GAGE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	630	310	3:19	3:26	590	560	Timer	170	84	7	
31			3:26	3:35					81	9	
32			3:35	3:43					82	8	
33			3:43	3:51					79	8	
34			3:51	3:59					81	8	
35 C			3:59	4:06	790			400	84	7	
36			4:06	4:13					82	7	
37			4:13	4:20					81	7	
38			4:20	4:27					84	7	
39			4:27	4:34	850			460	82	7	
40			4:34	4:40					81	6	
41			4:40	4:46					80	6	
42			4:46	4:52					82	6	
43			4:52	5:00					81	8	
44 C			5:00	5:07					84	7	
45			5:07	5:14					80	7	
46			5:14	5:21					78	7	
47			5:21	5:28					76	7	
48			5:28	5:35					75	7	
49			5:35	5:42					81	7	
50			5:42	5:49					82	7	5:49-5:52 Down at press
51			5:52	6:00					86	8	=8 pressure switch stuck
52 C			6:00	6:07					85	7	
53			6:07	6:14					84	7	
54			6:14	6:21					85	7	
55			6:21	6:28					85	7	
56			6:28	6:35					80	7	
57			6:35	6:42					77	7	
58			6:42	6:49					76	7	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-11-92

SHIFT D-11.7

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
59	500	3:10	[illegible]	6:56	850	At -60	timer -45	460	82	7	
EEC			6:56						84		

SD 5343

Louisiana-Pacific Co. oration

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-12-92 Shift A Pressing Cycle

Foreman Mickey Davis Hours 7-3 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
Kni.	3/4	[illegible]	6	96	0		96
	3/4	51½x295	48	768	0		768
	3/4 (F.R.)	51½x295	6	96	0		96

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-4		-15	12:10-12:44 Re-Face + clean tube dryer
		-7		12:33-12:40 mats breaking up at speed up
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	-4	-7	15	-26

Comments:

Footage: 69,120

No mats dumped in pit

Resin: 94.6

Paper: 9,135

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-12-1992 Shift C Pressing Cycle

Foreman Mike Brooks Hours 3-11 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
ains FRD	3/16	51½ x 295	9	144	0		144
TT	3/16	51½ x 295	34	544	0		544
..l.	1/16	51½ x 297	10	160	0		160
Col.	1/16	51½ x 295	4	64	0		64

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			-12	4:55-5:06 Rey. Co... & Cleaned dryer
-20				6:00-6:20 Down on line #1 #2
				burners went down
-3				6:20-6:25 Down on Face burner's
				down
-3				
				6:40-6:45 Down on core burner's
				down.
	-5			6:29-6:34 pre press conveyer belt
				tracked off.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
-26	-5		-12	-43

Comments:

Footage: 69,245'

No mats dumped in pit

Resin: 8.1

Total: 9000

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-12-92 Shift D Pressing Cycle

Foreman Cotton Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
col. 11/16	51½ x 295	63	1008	0		1008

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No down time
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				-0

Comments: No Mats Dumped

Footage: 88,704 ✓

Resin: 71.9

Rate: 11,205

SD 5344

Louisiana-Pacific Corpora 7

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-92

SHIFT A-7-3

OPERATOR Ben

BOARD THICKNESS 9/16

BOARD SIZE 51½/297-295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	cycle ~~LINE~~ TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	5:00	310	701	709		POT 60	Timer :45	850 460	77	8	
2			709	717					73	8	
3			717	725					76	8	
4			725	733					75	8	
5			733	741					74	8	
6			741	749					76	8	
7			749	757					78	8	
8			757	804					80	7	
9			804	812					83	8	
10			812	820					84	8	
11			820	828					84	8	
12			828	836					90	8	
13			836	844					91	8	
14			844	853					92	9	
15			853	901					91	8	
16			901	909					93	8	
17			909	917					86	8	
18			917	925					85	8	
19			925	933					84	8	
20			933	941					82	8	
21			941	949					83	8	
22			949	957					84	8	
23			957	1004					82	7	
24			1004	1012					81	8	
25			1012	1019					80	7	
26			1019	1026					81	7	
27			1026	1034					83	8	
28			1034	1041					84	7	
29			1041	1049					82	8	

Col. + McKnight

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-1992

SHIFT A 7-3

OPERATOR Ben Lee

BOARD THICKNESS 9/16

BOARD SIZE 51 1/2 x 295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	~~EMP. TEMP.~~ Gauge	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position: ~~HIGH~~ Line Speed	INTERMEDIATE ~~UPPER~~ Pot Bar	INTERMEDIATE ~~LOWER~~ Trach Bar	~~LOW~~ 810 420	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	5.20	300	1049	1056	54	60	45		93	7	
C 31			1056	1103					92	7	
32			1103	1110					89	7	
33			1110	1118					83	8	
34			1118	1126					85	8	
35			1126	1133					84	7	
36			1133	1140					82	7	
37			1140	1147					53	7	
38			1147	1155					54	8	
39			1155	1202					85	7	
40			1202	1209					85	7	
41			1209	1217					80	8	
42			1217	1233					85	16	-7 12:33-12:40 mats
43			1240	1256					83	16	breaking up at speed
44			1256	104					83	8	up
45			104	111					79	7	
46			111	118					79	7	
47			118	126					81	8	
48			126	134					82	8	
49			134	141					80	7	
50			141	148					81	7	
51			148	155					80	7	
C 52			155	203					85	8	
53			203	210					83	7	
54			210	217					80	7	
55			217	[illegible]					84	[illegible]	
56			225	232					80	7	
57			232	240					82	8	
58			240	247					73	7	

1/16 51 1/2 x 295 Finished Panel

1/16 51 1/2 x 295 Plained Panel

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-92

SHIFT A 7-3

OPERATOR Ben

BOARD THICKNESS 9/16

BOARD SIZE 51½x295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	~~OVEN TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~ Position	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
59	5:20	300	247	255		POT 60	TIMER :45	780 400	82	8	
60			255	302					86	7	
61											

SD 5343

Louisiana-Pacific Corporation
SOUTHERN DIVISION
FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-1992
SHIFT C 3-11
OPERATOR Ben-Anthony

BOARD THICKNESS 9/16
BOARD SIZE 51 1/2 x 295
BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position: Line ~~HIGH~~ speed	INTERMEDIATE ~~UPPER~~	~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	5:20	305	302	310	52	pot 60	Timer 45	780 400	85	8	
2			310	318					89	8	
3			318	326					87	8	
4			326	334					86	8	
5			334	342					85	7	
6			342	349					82	7	
7			349	356					84	7	
C 8			356	403					85	7	
9			403	411					81	8	
10			411	418					83	7	
11			418	425					83	7	
12			425	433					84	8	
13			433	440					83	7	
14			440	447					87	7	
15			447	455					84	8	
C 16			455	503					83	8	
17			503	515					82	12	Pos Size
18			515	528					82	13	
19			528	536					81	8	
20			536	545					81	9	
21			545	554					82	9	
22			554	600					81	9	-17 6:03-6:20 Down on
23			600	608					83	9	both systems OT M+D.
24			634	642					84	8	(burner went down)
25			642	650					82	8	-5 6:29-6:34 Pre-press
26			650	700					70	10	Convert of bolt tracks off
27 C			700	7:10					79	10	
28			7:10	7:18					76	8	
29			7:18	7:25					75	7	

1/16 51 1/2 x 295 Pine (F.F.)

1/16 51 1/2 x 295 Colt + McKnight

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-92

SHIFT C 3-11

OPERATOR Ben-Anthony

BOARD THICKNESS 9/16

BOARD SIZE 51½/295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

	LOAD NO.	~~GAUGE TEMP.~~ Cycle	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position HIGH	INTERMEDIATE ~~UPPER~~ Pot	INTERMEDIATE ~~LOWER~~ Timer	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
9/16	30	520	300	7:25	7:35	790	.60	.45	400	78	10	
51½	31			7:35	7:44					76	9	
	32			7:44	7:50					91	6	
	33			7:50	7:57					85	7	
	34 C			7:57	8:05					86	8	
	35			8:05	8:12					84	7	
	36			8:12	8:19					87	7	
	37			8:19	8:26					95	7	
	38			8:26	8:35					81	9	
	39			8:35	8:42					81	7	
	40			8:42	8:50					85	8	
	41			8:50	8:56					84	6	
	42			8:56	9:04					81	8	
	43 C			9:04	9:12					81	8	
11/16	44	650		9:12	9:20	696			270	84	8	
51½	45			9:20	9:29					81	9	
	46			9:29	9:36					84	7	
	47			9:36	9:44					81	8	
	48			9:44	9:51					85	7	
	49			9:51	9:59					82	8	
	50 C			9:59	10:07					84	8	
	51			10:07	10:15					81	8	
	52			10:15	10:23					85	8	
	53			10:23	10:30					82	7	
11/16	54			10:30	10:39					85	8	
51½	55			10:39	10:46					82	8	
	56			10:46	10:54					84	8	
	57 C			10:54						80		
	58											

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-92

FT D 11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	Cycle ~~Line Temp.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position: HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	600	300	11:01	11:09	690	Pot :60	Timer :45	270	82	8	
2			11:09	11:17					79	8	
3			11:17	11:25					77	8	
4			11:25	11:33					79	8	
5			11:33	11:41					77	8	
6			11:41	11:48					76	8	
7			11:48	11:56					79	8	
8 C			11:56	12:04					78	8	
9			12:04	12:11					79	7	
10			12:11	12:18					81	7	
11			12:18	12:25					84	7	
12			12:25	12:33					86	8	
13			12:33	12:40					81	7	
14			12:40	12:48					82	8	
15			12:48	12:55					80	7	
16 C			12:55	1:03					82	8	
17			1:03	1:11					83	8	
18			1:11	1:19					85	8	
19			1:19	1:27					85	8	
20			1:27	1:35					86	8	
21			1:35	1:43					85	8	
22			1:43	1:51					84	8	
23			1:51	1:59					86	8	
24 C			1:59	2:07					87	8	
25			2:07	2:16					85	9	
26			2:16	2:25					83	9	
27			2:25	2:33					85	8	
28			2:33	2:40					84	7	
29			2:40	2:47					86	7	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-92

SHIFT D 11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

11/16 51½ x 295 Col.

LOAD NO.	Cycle ~~TIME~~ ~~TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE/position HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	600	300	2:47	2:55	690	Pot .60	Timer .45	270	81	8	
31 C			2:55	3:02					84	7	
32			3:02	3:10					86	8	
33			3:10	3:18					83	8	
34			3:18	3:25					86	7	
35			3:25	3:33					85	8	
36			3:33	3:41					82	8	
37			3:41	3:49					86	8	
38			3:49	3:56					84	7	
39 C			3:56	4:04					82	8	
40			4:04	4:11					86	7	
41			4:11	4:19					83	8	
42			4:19	4:26					85	7	
43			4:26	4:34					82	8	
44			4:34	4:41					85	7	
45			4:41	4:49					86	8	
46			4:49	4:56					83	7	
47 C			4:56	5:04					84	8	
48			5:04	5:12					86	8	
49			5:12	5:20					85	8	
50			5:20	5:29					82	9	
51			5:29	5:37					86	8	
52			5:37	5:44					84	7	
53			5:44	5:51					88	7	
54			5:51	5:58					87	7	
55 C			5:58	6:05					86	7	
56			6:05	6:13					85	7	
57			6:13	6:20					84	7	
58			6:20	6:27					86	7	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-92

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	cyclic ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Pot. HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
11/16 59	600	300	627	6:34	690	Pot =40	Timer =45	270	79	7	
:15 60			6:34	6:41					82	7	
:95 61			6:41	6:48					82	7	
Col. 62			6:48	6:55					86	7	
63C			6:55						81		
64											

SD 5343

Louisiana-Pacific Co., oration

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-13-92 Shift A Pressing Cycle

Foreman Mickey Davis Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1/16	5½x[illegible]	37	592	0		592
1/16	5½x[illegible]	11	176	0		176
1/16	5½x[illegible]	4	64	0		64

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
-20				9:05-9:44 Down on face: lost
				control power on #1 & 2 presses
-39				9:02-10:25 Down on Core: lost contin.
				power on #1 & 2 presses + #1 boiler
				went down
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
-59				-59

Comments:

No mats dumped

Inventory 73,216

Begin: 75.3

Prod: 10,434

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-13-1992 Shift B Pressing Cycle

Foreman Robert Hamin Hours 3:11 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
Col.	11/16	51½x295	42	672	0		672
Col.	11/16	51½x259	14	224	0		224

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
-3				7:22-7:26 = changed out
				motor on = 3 phase off Nr.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
-3				-3

Comments: NO Wire Dumped

Footage: 76,384

Resin: 88.7

Pate: 954.8

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-13-92 Shift D Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
11/16	51½ x 295	56	896	0		896

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No down time
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				- 0

Comments: No Mats Burned

Sq. Ft. 78,848

Pcs 863

Gen 9960

SD 5344

Louisiana-Pacific Corporat 7

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-13-92

SHIFT A-7-3

OPERATOR Ben

BOARD THICKNESS 7/16

BOARD SIZE 5 1/2 [illegible]

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	~~TIME TEMP.~~ 3/10-12	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	6:00	300	702	710		Pot :60	Finer :45	690 [illegible]	90	8	
2			710	715					91	5	
3			715	725					92	7	
4			725	732					97	7	
5			732	739					96	7	
6			739	747					91	8	
7			747	754					93	7	
8			754	802					95	8	
9			802	809					94	7	
10			809	817					93	8	
11			817	825					91	8	
12			825	832					87	7	
13			832	840					88	8	
14			840	848					88	8	
15			848	905					82	7	
16			905	913					81	8	
17			913	921					80	8	9:21-10:00 Down
18			1000	1014					82	14	on line because of
19			1014	1028					87	14	trouble at MDF
20			1028	1039					90	11	
21			1039	1050					92	11	
22			1050	1059					91	9	
23			1059	1108					92	9	
24			1108	1116					93	8	
25			1116	1124					92	8	
26			1124	1133					90	9	
27			1133	1141					97	8	
28			1141	1150					98	9	
29			1150	1156					[illegible]	6	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-13-92

SHIFT A 7-3

OPERATOR BEN

BOARD THICKNESS 11/16

BOARD SIZE 51 1/2 x 225 - 52 1/2 x 225

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~GAUGE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Actual HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	6:00	300	1158	1205		pot 60	Timer :45	620 250	78	7	
31			1205	1214					81	9	
32			1214	1223					82	9	
33			1223	1231					84	8	
34			1231	1239					83	8	
35			1239	1247					82	8	
36			1247	1254					81	7	
37			1254	101					85	7	
38			101	109					85	8	
39			109	117					84	8	
40			117	125					85	8	
41			125	133					85	8	
42			133	141					86	8	
43			141	149					86	8	
44			149	158					85	9	
45			158	206					84	8	
46			206	214					87	8	
47			214	223					86	9	
48			223	231					89	8	
49			231	239					85	8	
50			239	247					86	8	
51			247	255					84	8	
52			255	303					85	8	

Whiteville

11/16 Harris Col.

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-13-92

SHIFT B 3-11

OPERATOR Ben-Anthony

BOARD THICKNESS 11/16

BOARD SIZE 57½ x295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	CYCLE ~~TIME~~ ~~TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position: HIGH	INTERMEDIATE ~~[illegible]~~	INTERMEDIATE ~~[illegible]~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	6:00	300	303	311		HOT 60	TIMER :45	720 290	86	8	
2			3:11	3:20					85	9	
3			3:20	[illegible]					85	7	
4			[illegible]	3:27					86	9	
5			[illegible]	3:41					82	7	
6			3:41	3:52					84	8	
7			3:52	4:01					91	9	
C 8			4:01	410					90	9	
9			410	419					76	9	
10			419	428					91	9	
11			428	437					90	9	
12			437	445					89	8	
13			445	454					88	9	
14			454	502					85	8	
15			502	510					84	8	
C 16			510	519					81	9	
17			519	527					82	8	
18			527	535					84	8	
19			535	544					75	9	
20			544	553					86	9	
21			553	602					84	9	
22			602	611					91	9	
23			611	6:20					92	9	
24			6:20	6:28					92	8	
25			6:27	6:37					88	9	
26			6:37	6:46					87	9	
27			6:46	6:55					87	9	
28			6:55	7:03					86	8	
29			7:03	7:14					84	11	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-13-92

SHIFT B 3-11

OPERATOR Ben-Anthony

BOARD THICKNESS 11/16

BOARD SIZE 51½x295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	600	300	7:14	7:23	720	Pot :60	Timer :45	290	81	9	7:23-7:26
31			7:26	7:35					84	9	
32			7:35	7:43					82	8	
33			7:43	7:50					85	7	
34			7:50	7:57					84	7	
35			7:57	8:04					86	7	
36 C			8:04	8:13					81	9	
37			8:13	8:21					84	8	
38			8:21	8:30					86	9	
39			8:30	8:39					84	9	
40			8:39	8:47					86	8	
41			8:47	8:54					84	7	
42			8:54	9:01					81	7	
43 C			9:01	9:10					85	9	
44			9:10	9:17					82	7	
45			9:17	9:25					84	8	
46			9:25	9:33					81	8	
47			9:33	9:42					84	9	
48			9:42	9:51					82	9	
49			9:51	10:00					85	9	
50 C			10:00	10:09					81	9	
51			10:09	10:18					83	9	
52			10:18	10:27					84	9	
53			10:27	10:37					81	10	
54			10:37	10:46					83	9	
55			10:46	10:55					85	9	
56 C			10:55						82		

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-13-92

SHIFT D 11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	~~LINE TEMP.~~ PLATE	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~ Position	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	660	300	11:04	11:14	700	Pot :66	Time :45	270	81	10	
2			11:14	11:24					84	10	
11/16 3			11:24	11:34					86	10	
4			11:34	11:44					82	10	
5 1/2 5			11:44	11:51					81	7	
x 295 6			11:51	12:00					84	9	
501 7 C			12:00	12:09					82	9	
8			12:09	12:19					85	10	
9			12:19	12:27					81	8	
10			12:27	12:37					84	10	
11			12:37	12:45					82	8	
12			12:45	1:53					82	8	
13			1:53	2:03					85	10	
14 C			2:03	2:11					86	8	
15			2:11	2:20					87	9	
16			2:20	2:28					82	8	
17			2:28	2:37					87	9	
18			2:37	2:47					84	10	
19			2:47	2:55					86	8	
20			2:55	3:03					82	8	
21 C			3:03	3:11					85	8	
22			3:11	3:19					86	8	
23			3:19	3:29					85	10	
24			3:29	3:36					87	7	
25			3:36	3:44					84	8	
26			3:44	3:50					81	6	
27			3:50	3:57					79	7	
28 C			3:57	4:05					83	8	
29			4:05	4:15					86	10	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-12-92

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	cycle LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	660	200	3:15	3:24	700	Pot :40	timer :45	270	82	9	
31			3:24	3:32					86	8	
32			3:32	3:40					84	8	
33			3:40	3:49					81	9	
34			3:49	3:57					84	8	
35 C			3:57	4:05					86	8	
36			4:05	4:14					82	9	
37			4:14	4:23					84	9	
38			4:23	4:31					81	8	
39			4:31	4:39					84	8	
40			4:39	4:47					82	8	
41			4:47	4:55					85	8	
42 C			4:55	5:04					83	9	
43			5:04	5:13					81	9	
44			5:13	5:21					85	8	
45			5:21	5:30					84	9	
46			5:30	5:38					79	8	
47			5:38	5:47					82	9	
48			5:47	5:55					83	8	
49 C			5:55	6:04					81	9	
50			6:04	6:12					82	8	
51			6:12	6:20					84	8	
52			6:20	6:29					80	9	
53			6:29	6:37					81	8	
54			6:37	6:45					83	8	
55			6:45	6:53					85	8	
56 C			6:53						82		
57											
58											

11/6

5 1/2

.75

.1.

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-14-92 Shift 2 Pressing Cycle

Foreman Mike Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
7/16	51½ x 8[illegible]	5	80	0		80
5/8	51½ x 8[illegible]	14	224	0		224
5/8	51½ x 8[illegible]	14	224	0		224
5/8	51½ x 8[illegible]	25	400	0		400

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			-38	805-920 #1 Down to [illegible]
				Plates
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			-38	-38

Comments: No mats dumped

Footage [illegible]

Issue 8/13

Date 10/[illegible]

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-14-92 Shift B Pressing Cycle

Foreman Robert Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
5/8	51½x395	23	368	0		368
5/8	51½x296	39	624	0		624

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				NO down time.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				-0

Comments: NO mats Empty.

Footage 79360

Used 807

Rate 9920

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-14-92 Shift D Pressing Cycle

Foreman George Hours 11-7 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
Sden	5/8	51½ x 296	3	48	0		48
Sden	7/8	51½ x 296	48	768	0		768
Sol.	11/16	51½ x 295	13	208	0		208

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-7			6:28-6:35 Down at Flying saw
				Pin broke.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	-7			-7

44

Comments: No Mats Dumped

Left . 73,360

RH . 86.1

Right . 9,228

SD 5344

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-13-92

SHIFT C-7-3

OPERATOR Gary

BOARD THICKNESS 11/16 - 5/8

BOARD SIZE 51 1/2 x 275

BOARD TYPE 7[illegible] D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

	LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
11/16	1	660	300	702	711	700	pot	timer	270	86	9	
5/8	2			711	720		100	115		86	9	
col.	3			720	729					85	9	
	4			729	738					84	9	
	5			738	746					84	8	
5/8	6			746	754	740			310	87	8	
5/8	7			754	803					84	9	
[illegible]	8			803	814					80	11	
	9			814	826					82	12	
	10			826	840					85	14	
	11			840	854					92	14	
	12			854	906					101	12	
	13			906	920					99	14	
	14			920	930					87	10	
	15			930	938					82	8	
	16			938	946					85	8	
	17			946	954					86	8	
	18			954	1001					80	7	
	19			1001	1008					73	7	
5/8	20			1008	1016					74	8	
275	21			1016	1024					72	8	
[illegible]	22			1024	1031					72	7	
	23			1031	1038					73	7	
	24			1038	1045					74	7	
	25			1045	1053					77	8	
	26			1053	1101					80	8	
	27			1101	1108					79	7	
	28			1108	1116					84	8	
	29			1116	1123					80	7	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-14-92

SHIFT C-7-3

OPERATOR Gary

BOARD THICKNESS 5/8

BOARD SIZE 51½ x 295

BOARD TYPE M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

5/19 295 timer

timer

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	600	300	1122	1131	740	Port	Timer	310	85	8	
31			1123	1138		100	15		84	7	
32			1132	1145					84	7	
33			1145	1152					85	7	
34			1152	1200					84	8	
35			1200	1208					83	8	
36			1208	1215					86	7	
37			1215	1222					82	7	
38			1222	1229					80	7	
39			1229	1237					83	8	
40			1237	1245					83	8	
41			1245	1252					86	7	
42			1252	1259					83	7	
43			1259	106	710			280	80	7	
44			106	114					80	8	
45			114	122					82	8	
46			122	129					81	7	
47			129	137					81	8	
48			137	144					83	7	
49			144	151					82	7	
50			151	159					82	8	
51			159	207					84	8	
52			207	214					83	7	
53			214	221					82	7	
54			221	227					85	8	
55			227	236					85	7	
56			236	244					86	8	
57			244	252					86	8	
58			252						55		

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-14-92

SHIFT E-3-11

OPERATOR [illegible]

BOARD THICKNESS 5/3

BOARD SIZE 51½ x 295

BOARD TYPE M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	600	300	300	3:08	710	POT	Timer	280	88	8	
2			3:08	3:16		100	:15		84	8	
3			3:16	3:24					87	10	
4			3:24	3:32					81	8	
5			3:32	3:40					83	8	
6			3:40	3:48					82	8	
7			3:48	3:56					82	7	
8			3:56	4:03					81	7	
9			4:03	4:11					83	8	
10			4:11	4:19					82	8	
11			4:19	427					80	8	
12			427	434					78	7	
13			434	442					79	8	
14			442	449					82	7	
15			449	456					84	7	
16			456	503	780			390	83	7	
17			503	511					87	8	
18			511	519					89	8	
19			519	527					84	8	
20			527	534					85	7	
21			534	542					86	8	
22			542	549					84	7	
23			549	556					86	7	
24			556	604					85	8	
25			604	612					83	8	
26			612	620					84	8	
27			620	628					86	8	
28			628	636					84	8	
29			636	643					81	7	

5/3 25 insert

5/8 26

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-14-92

SHIFT B-3-11

OPERATOR Gary + Anthony

BOARD THICKNESS 5/2

BOARD SIZE 51½ x 296

BOARD TYPE M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
5/8 30	600	300	6:43	6:50	780	POT	Timer	390	82	7	
296 31			6:50	6:58		100	:15		81	8	
loaden 32			6:58	7:06					83	8	
33			7:06	7:14					86	8	
34			7:14	7:21					84	7	
35			7:21	7:29					81	8	
36			7:29	7:36					84	7	
37			7:36	7:44					81	8	
38			7:44	7:51					83	7	
39			7:51	7:59					84	8	
40			7:59	8:07					81	8	
41C			8:07	8:15					83	8	
42			8:15	8:22					80	7	
43			8:22	8:30					81	8	
44			8:30	8:39					84	9	
45			8:39	8:47					86	8	
46			8:47	8:55					84	8	
47			8:55	9:02					81	[illegible]	
48C			9:[illegible]	9:10					[illegible]	8	
49			9:10	9:20					54	10	
50			9:20	9:30					81	10	
51			9:30	9:39					84	9	
52			9:39	9:47					83	8	
53			9:47	9:54					84	7	
54			9:54	10:01					84	7	
55C			10:01	10:09					81	8	
56			10:09	10:19					82	10	
57			10:19	10:26					81	7	
58			10:26	10:34					89	8	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-14-92

SHIFT B-3-11

OPERATOR Gary + Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
59	600	300	10:34	10:41	780	Pet 150	Timer 2:45	390	82	7	
60			10:41	10:49					84	8	
61			10:49	10:56					86	7	
62c			10:56						82		

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-14-92

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Posi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	580	300	11:02	11:12	810	Pot 260	timer 245	420	79	10	
2			11:12	11:22					81	10	
3			11:22	11:30					84	8	
4			11:30	11:39					84	9	
5			11:39	11:47					81	8	
6			11:47	11:54					82	7	
7			11:54	12:01	890			500	85	7	
8 C			12:01	12:09					81	8	
9			12:09	12:16					84	7	
10			12:16	12:24					85	8	
11			12:24	12:31					87	7	
12			12:31	12:39					84	8	
13			12:39	12:45					85	6	
14			12:45	12:52					82	7	
15			12:52	12:59					84	7	
16 C			12:59	1:06					81	7	
17			1:06	1:13					84	7	
18			1:13	1:20					81	7	
19			1:20	1:27					85	7	
20			1:27	1:34					84	7	
21			1:34	1:41					82	7	
22			1:41	1:49					84	8	
[illegible]			1:49	1:55					81	6	
24			1:55	2:02					84	7	
25			2:02	2:10					80	8	
26			2:10	2:17					81	7	
27			2:17	2:24					83	7	
28			2:24	2:31					79	7	
29			2:31	2:38					78	7	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-14-93

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	580	300	2:38	245	890	Pot :60	timer :15	500	78	7	
31			2:45	253					76	8	
32			253	3:00					78	7	
33 C			3:00	3:07					74	7	
34			3:07	3:14					76	7	
35			3:14	3:21					78	7	
36			3:21	3:27					79	6	
37			3:27	3:34					81	7	
38			3:34	3:41					82	7	
39			3:41	3:48					84	7	
[illegible]			3:48	3:55					81	7	
[illegible]			3:55	4:02					80	7	
[illegible] C			4:02	4:09					79	7	
[illegible]			4:09	4:16					81	7	
[illegible]			4:16	4:24					84	8	
45			4:24	4:31					81	7	
46			4:31	4:38					83	7	
47			4:38	4:45					85	7	
48			4:45	4:52					83	7	
[illegible]			4:52	5:00					81	8	
50 C			5:00	5:08					84	8	
51			5:08	5:18					82	10	
52	630		5:18	5:26	720			300	85	8	
53			5:26	5:34					84	8	
54			5:34	5:42					81	8	
55			5:42	5:50					84	8	
56			5:50	5:58					82	8	
57 C			5:58	6:06					81	9	
58			6:06	6:19					82	8	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-14-92

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

11/16

51½ x 25 col.

LOAD NO.	~~LINE TEMP.~~ Cyl. 1	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
59	630	300	6:14	6:21	720	Pot 720	tmr 545	300	82	7	
60			6:21	6:28					80	7	6:28–6:35 Down at
61			6:35	6:42					84	7	Flying saw.
62			6:42	6:50					86	8	
63			6:50	6:58					85	8	
64			6:58						84		

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3-15-82 Shift 2 Pressing Cycle

Foreman [illegible] Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 1/16	[illegible]	21	336	0		336
1 1/8	[illegible]	20	320	0		320

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-8		-45	715-900 = 2 [illegible]
	-8			1015-1020 Pin [illegible]
				[illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	-16		-45	-61

Comments: Dumped 12 [illegible] Footage [illegible]

Lot them out Usage [illegible]

[illegible] 960

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-15-92 Shift B Pressing Cycle

Foreman Robert Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 1/8	49 7/8 x 245	16	256			256
1 1/8	50 1/4 x 267	1	16			16
1 1/8	50 1/4 x 277	2	32			32
1 1/8	50 1/4 x 280	1	16			16
1 1/8	50 1/4 x 286	6	96			96

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
-2				#8 Pressure Switch hung up. Press wouldn't open.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
-2				-2

Comments:

Footage 73,412

Usage 86.9

Rate 9177

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Claxton

Date 3-15-92 Shift B Pressing Cycle

Foreman Robert Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 1/8	50 1/4 x 293	1	16			16
1 1/8	47 1/4 x 245	2	32			32
1 3/16	49 7/8 x 245	11	176			176

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments:

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-15-92 Shift 0 Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 3/16	49 3/8 x 245	41	656	0		656

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-7			11:12-11:20 Down a.- Flying saw pin broke.

Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total	
	-7			-7	QD

Comments: No Mate Downed.

Eff. . 74.57%

Eff. . 88.4

Eff. . 9440

SD 5344

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-15-92

SHIFT C-7-3

OPERATOR Gary

BOARD THICKNESS 11/16

BOARD SIZE 51 1/2 x 225

BOARD TYPE M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
11/16 1	610	300	706	714	720	POT	Timer	300	81	8	
245 2			714	724		100	:15		79	10	
3			724	744	670			250	81	20	
4			744	808					74	24	
5			808	833	620			200	76	25	
6			833	858					79	25	
7			858	912					82	14	
8			912	920					89	8	
9			920	929					91	9	
10			929	938					89	9	
11			938	946					85	8	
12			946	954					86	8	
13			954	1002					89	8	
14			1002	1010					88	8	
15			1010	1018					89	8	1018 - 1026 Pin broke
16			1026	1034					84	8	on Flying Saw
17			1034	1042					86	8	
18			1042	1049					85	7	
19			1049	1057					85	8	
20			1057	1106					84	9	
21			1106	1119					87	13	
1/3 22			1119	1130					81	11	
245 23			1130	1141					77	11	
24			1141	1152	620			240	75	11	
25			1152	1203					80	11	
26			1203	1215					77	12	
27			1215	1226					67	11	
28			1226	1237					67	11	
29			1237	1248					69	11	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-15-92

SHIFT C-7-2

OPERATOR Gary

BOARD THICKNESS 1/8

BOARD SIZE [illegible]

BOARD TYPE [illegible]

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1/8 30	980	310	1248	1259	620	POT	TIMER	240	69	11	
5 31			1259	112		100	115		77	13	
32			112	125					80	13	
33			125	136					81	11	
34			136	147					83	11	
35			147	152					80	11	
36			152	207					78	1.	
37			207	220					74	11	
38			220	232					72	12	
39			232	244					73	12	
40			244	255					75	11	
41			255						74		

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-15-92

SHIFT B-3-11

OPERATOR [illegible]

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	980	310	306	318	620	60	15	240	66	12	
2			318	330					67	12	
3			330	342					69	12	
4			342	354					71	12	
5			354	407					71	13	
6			407	420					67	13	
7			420	433					72	13	
8			433	445					79	12	
9			445	457					81	12	
10			457	508					79	11	
11			508	519					76	11	
12			519	530					76	11	
13			530	542					74	12	
14			542	553					76	11	
15			553	604					78	11	
16			604	615					79	11	
17			615	628					89	13	
18			628	640					89	12	
19			640	653					88	13	
20			653	705					85	13	
21			705	718					89	13	
22			718	730					84	12	
23			730	742					81	12	
24			742	754					76	12	
25			754	807					77	13	
26			807	820					86	13	
27			820	831					89	11	
28			831	842					73	11	
29			842	853					74	11	

SD 5343

Louisiana-Pacific Corpora n

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-15-92

FT B-3-11

OPERATOR Micky

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	1000	310	853	904	780	60	15	340	74	11	
31			904	916					74	12	
32			916	927					71	11	
33			927	939					70	12	
34			939	950					71	11	
35			950	1002					74	12	
36			1002	1014					70	12	-2 " Pressure Switch
37			1016	1027					73	12	
38			1027	1039					71	11	
39			1039	1051					81	12	
40			1051						82		
41											
42											

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-15-88

SHIFT D-11-7

OPERATOR [illegible]

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
	970	310	11:01	11:13	760	Pot :60	timer :45	340	71	12	11:13 - 11:20 Down at
1 7/16			11:20	11:32					73	12	Flying saw pin broke.
49 7/8 x 2.5 3			11:32	11:44					75	12	
4			11:44	11:56					76	12	
5 C			11:56	12:08					74	12	
6			12:08	12:20					76	12	
7			12:20	12:31					78	11	
8			12:31	12:43	800			380	73	12	
9			12:43	12:54					75	11	
10 C			12:54	105					76	11	
11			105	117					74	12	
12			117	1:29					74	12	
13			1:29	1:41					78	12	
14			1:41	1:52					76	11	
15 C			1:52	2:04					75	12	
16			2:04	2:15					78	11	
17			2:15	2:26					76	11	
18			2:26	2:37					75	11	
19			2:37	2:49					76	12	
20			2:49	3:01					79	12	
21 C			3:01	3:12					76	11	
22			3:12	3:24					72	12	
23			3:24	3:36					75	12	
24			3:36	3:48					78	12	
25			3:48	3:59					75	11	
26 C			3:59	4:09					77	10	
27			4:09	4:20					75	11	
28			4:20	4:32					76	12	
29			4:32	4:44					78	12	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-15-92

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	1000	310	4:44	4:55	800	psi :60	psi :45	380	84	11	
31 C			4:55	5:06					81	11	
32			5:06	5:17					85	11	
33			5:17	5:29					83	12	
34			5:29	5:41					77	12	
35			5:41	5:52					76	11	
36			5:52	6:05					77	13	
37 C			6:05	6:17					74	12	
38			6:17	6:29					75	12	
39			6:29	6:42					72	13	
40			6:42	6:54					71	12	
41 C			6:54						75		
42											
43											
44											
45											

1 3/16

19 1/2

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date [illegible] Shift [illegible] Pressing Cycle _____

Foreman [illegible] Hours [illegible] Total Cycle _____

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
[illegible]	[illegible]	19	304	0		304
1 3/16	52¼x267	1	16	0		16
1 3/16	52¼x[illegible]	3	48	0		48
1 3/16	52¼x280	3	48	0		48
1 3/16	52¼x[illegible]	4	64	0		64

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-28			22E - 253 Pin broke on
				flying saw, Change out
				[illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	-28			-28

Comments: No mats [illegible]

Footage 63 [illegible] 4%

[illegible] 90.5

[illegible] 2625

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-16-92 Shift C Pressing Cycle

Foreman MIKE Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 3/16	24¼x292	3	48	0		48
1 5/32	49⅞x245	2	32	0		32

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments:

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-16-92 Shift B Pressing Cycle

Foreman Robert Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 5/32	49 7/8 x 245	27	432			432
1 5/32	52 1/4 x 267	3	48			48
1 5/32	52 1/4 x 277	2	32			32
1 5/32	52 1/4 x 280	4	64			64
1 5/32	52 1/4 x 286	3	48			48

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
3				#8 Pressure Switch hung up - Press wouldn't open.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
3				3

Comments: Footage 72,912

Usage 87.1

Rate 9268

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-16-92 Shift D Pressing Cycle

Foreman George Hours 7-3 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
P	1 5/32	52¼ x 286	3	48	0		48
	1 5/32	52¼ x 293	2	32	0		32
P.	1¼	49⅞ x 245	2	32	0		32
P.	1"	49⅞ x 245	4	60	0		60
P.	1"	49⅞ x 245	31	496			496

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			-22	5:05 550 Down on core to Roy
				clean up and go on.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			-22	-22

Comments: No Mats Dumped

Sq ft . 68,369

Pll . 97.2

Pcs . 8955

SD 5344

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-16-92

SHIFT C-7-3

OPERATOR Gary

BOARD THICKNESS 1 3/16

BOARD SIZE 49 7/8 X 245

BOARD TYPE D.P.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

	LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
3/16	1	1000	310	706	720	8.00	Pot	Time	350	76	14	
245	2			720	732		100	15		73	12	
	3			732	744					72	12	
	4			744	756					69	12	
	5			756	808					69	12	
	6			808	821					72	13	
	7			821	834	770			350	74	13	
	8			834	847					73	13	
	9			847	859					76	12	
	10			859	912					75	13	
	11			912	924					77	12	
	12			924	936					77	12	
	13			936	949					75	13	
	14			949	1001					75	12	
	15			1001	1014					77	13	
	16			1014	1026					76	12	
	17			1026	1038					75	12	
	18			1038	1049					73	11	
	19			1049	1100					75	13	
367	20			1100	1118					78	16	
	21			1118	1133					78	15	
79	22			1133	1146					76	13	
	23			1146	1157					84	13	
	24			1157	1214					81	15	
330	25			1214	1228					79	14	
	26			1228	1242					86	15	
	27			1242	1255					86	12	
36	28			1255	109					82	14	
	29			109	124					82	15	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 2-16-92

SHIFT 3-7-3

OPERATOR Gary

BOARD THICKNESS 1 3/16

BOARD SIZE 52 1/4 X 286-288

BOARD TYPE D.P.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	10:90	310	124	136	770	POT	Timer	350	86	12	
31			136	149		100	145		85	13	
32			149	201					87	12	
33			201	214					86	13	
34			214	225	930			510	77	11	225-253 pin
35			253						75		brake on flying
											saw, chang bearing
											in pin block

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-16-92

SHIFT B-3-11

OPERATOR TILCKY

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	1050	310	306	317	930	60	15	510	80	11	
2			317	330					78	13	
3			330	342					61	12	
4			342	353					56	11	
5			353	405					54	12	
6			405	417					62	12	-3 #2 pressure switch
7			420	430					58	10	
8			430	442					58	12	
9			442	453					59	11	
10			453	505					72	12	
11			505	517					64	12	
12			517	529					62	12	
13			529	540					62	11	
14			540	552					60	12	
15			552	603					61	11	
16			603	615					62	12	
17			615	626					55	11	
18			626	637					52	11	
19			637	649					52	12	
20			649	700					55	11	
21			700	712					58	12	
22			712	724					61	12	
23			724	735					62	11	
24			735	747					58	12	
25			747	758					58	11	
26			758	810					56	12	
27			810	822					58	12	
28			822	834					61	12	
29			834	846					64	12	

SD 5343

Louisiana-Pacific Corpora)

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-16-92

SHIFT P - 3-11

OPERATOR Mickey

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
[illegible]	[illegible]	210	846	859	940	62	5	480	66	13	
[illegible]			859	912					57	13	
[illegible]			912	925					56	13	
[illegible]			925	938					57	13	
[illegible]			938	951					56	13	
[illegible]			951	1004					58	13	
[illegible]			1004	1017					59	13	
[illegible]			1017	1032					60	15	
[illegible]			1032	1047					60	15	
[illegible]			1047						62		

SD 5343

Louisiana-Pacific Corpora

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-16-88

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

	LOAD NO.	Cycle LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1 5/32 5-1/4 x 226	1	1050	310	11:00	11:14	920	Pot :60	tiner :45	480	79	14	
	2	1100		11:14	11:26					82	12	
	3			11:26	11:41					80	15	
5/32 5-1/4 x 243	4			11:41	11:54					82	13	
	5			11:54	12:09					81	15	
5	6 C	1050		12:09	12:21	720			280	84	12	
	7			12:21	12:34					82	13	
	8	860		12:34	12:45	640			200	65	11	
49 3/8 x 245	9			12:45	12:55					61	10	
	10 C			12:55	1:05					62	10	
Shop	11			1:05	1:15					65	10	
	12			1:15	1:25					74	10	
	13			1:25	1:35					73	10	
	14			1:35	1:45					76	10	
	15			1:45	1:55					72	10	
	16 C			1:55	2:05					69	10	
	17			2:05	2:17					74	12	
	18			2:17	2:28					72	11	
	19			2:28	2:38					73	10	
	[illegible]			2:38	2:48					72	10	
	[illegible]			2:48	2:58					76	10	
	[illegible] C			2:58	3:08					73	10	
	[illegible]			3:08	3:18					77	10	
	24			3:18	3:30					74	12	
	25			3:30	3:40					78	10	
	26			3:40	3:52					73	12	
	[illegible]			3:52	4:02					74	10	
	[illegible] C			4:02	4:14					76	12	
	[illegible]			4:14	4:24					75	10	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-16-92

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE (DES) HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	860	310	4:24	4:35	640	Pit -60	timer :45	200	72	11	
31			4:35	4:45					78	10	
32			4:45	4:55					74	10	
33			4:55	5:05					76	10	
34 C			5:05	5:15					74	10	
35			5:15	5:35					71	20	
36			5:35	5:55					75	20	
37 C			5:55	6:09					89	14	
38			6:09	6:19					84	10	
39			6:19	6:30					78	11	
40			6:30	6:41					75	11	
41			6:41	6:52					78	11	
42 C			6:52						76		
43											
44											

1" 9 7/8 .5

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clarion

Date 3-17-93 Shift 2 Pressing Cycle

Foreman [illegible] Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1"	49 7/8 x 245	2	32	0		32
1"	52 1/4 x 217	1	16	0		16
11/16	51 1/2 x 225	56	896	0		896

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: NO mats dumped

Footage 83,712

Usage 83.6

Rate 10,464

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-17-92 Shift B Pressing Cycle

Foreman Tank Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
11/16	51½ x 295	37	592			592
7/8	47½ x 245	18	288			288
		69.10				

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				4

Comments: Footage - 75,356

Usage - 92.0

Rate

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-17-92 Shift D Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
7/8	47 1/4 x 245	12	192	0		192
7/8	49 7/8 x 245	5	80	0		80
7/8	52 1/4 x 280	4	64	0		64
1"	52 1/4 x 280	2	32	0		32
1"	52 1/4 x 226	3	48	0		48

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	- 12		- 15	4:30-5:22 Down on Face to Row
				clean dryer + dump zone changed
				out Resin header.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	- 12		- 15	- 27

Comments: No Mats Dropped

Gas . 65,668

Oil . 985

Nat . 8,678

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-17-92 Shift D Pressing Cycle

Foreman George Hours 11-7 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
.P.	1"	51×295	3	48	0		48
.P.	1"	49 7/8×245	5	80	0		80
.l.	11/16	51 1/2×295	10	160	0		160

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments:

SD 5344

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-19-92

SHIFT C-7-3

OPERATOR Gary

BOARD THICKNESS 1" + 11/16

BOARD SIZE 49 7/8 x 245 - 58 MX277 / 51 1/4 x 245

BOARD TYPE 1/2 M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	9:00	316	706	718	640	Pot :60	timer :45	200	86	12	
2			718	732					85	14	
3			732	744					89	12	
4			744	753	650			310	88	11	
5			753	801					90	8	
6			801	809					90	8	
7			809	817					92	8	
8			817	824					96	7	
9			824	831					94	7	
10			831	839					91	8	
11			839	847					90	8	
12			847	854	730			390	92	7	
13			854	902					90	8	
14			902	910					96	8	
15			910	917					92	7	
16			917	924					92	7	
17			924	931					90	7	
18			931	939					87	8	
19			939	947					89	8	
20			947	954					89	7	
21			954	1001					87	7	
22			1001	1009					86	8	
23			1009	1017					89	8	
24			1017	1025					86	8	
25			1025	1033					86	8	
[illegible]			1033	1041					85	8	
[illegible]			1041	1049					86	8	
[illegible]			1049	1057					87	8	
[illegible]			1057	1105					89	8	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 5-7-96

SHIFT 6-7-3

OPERATOR Gary

BOARD THICKNESS 7/16

BOARD SIZE 51½x[illegible]

BOARD TYPE [illegible]

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
11/10 30	580	300	1105	1113	730	Pot	Timer	390	85	8	
1:35 31			1113	1120		100	115		84	8	
1:01 32			1120	1127					86	8	
33			1128	1137					85	9	
34			1137	1145					87	8	
35			1145	1152					70	7	
36			1152	1200					72	8	
37			1200	1208					85	8	
38			1208	1216					86	8	
39			1216	1224					84	8	
40			1224	1232					86	8	
41			1232	1240					86	8	
42			1240	1248					87	8	
43			1248	1256					85	8	
44			1256	104					87	8	
45			104	112					86	8	
46			112	120					86	8	
47			120	128					84	8	
48			128	136					84	8	
49			136	144					80	8	
50			144	152					82	8	
51			152	200					79	8	
52			200	208					86	8	
53			208	216					84	8	
54			216	224					86	8	
55			224	232					84	8	
56			232	240					70	8	
57			240	248					92	8	
58			248	255					90	7	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-17-92

SHIFT 2-7-3

OPERATOR Gary

BOARD THICKNESS 11/16

BOARD SIZE 51½ x 225

BOARD TYPE M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
59	600	300	255		730	Pot	Timer	390	89		
						100	15				

11/16
295
Col.

SD 5343

Louisiana-Pacific Corpora)

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-17-93

SHIFT 3-3-11

OPERATOR WICKY

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	600	300	304	313	730	60	15	370	91	9	
2			313	322					92	9	
3			322	330					95	8	
4			330	340					92	10	
5			340	349					91	9	
6			349	357					93	8	
7			357	407					92	10	
8			407	415					92	8	
9			415	424					92	9	
10			424	432					93	8	
11			432	441					93	9	
12			441	449					92	8	
13			449	457					92	8	
14			457	505					92	8	
15			505	514					90	9	
16			514	521					91	7	
17			521	529					91	8	
18			529	537					89	8	
19			537	545					87	8	
20			545	552					86	7	
21			552	600					87	8	
22			600	608					88	8	
23			608	617					90	9	
24			617	624					90	7	
25			624	632					89	8	
26			632	[illegible]					87	7	
27			[illegible]	[illegible]					87	5	
28			[illegible]	[illegible]					87	8	
29				706					89	10	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-17-92

SHIFT B-3-11

OPERATOR micky

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	600	300	706	715	720	60	15	390	92	9	
31			715	723					89	8	
32			723	731					89	8	
33			731	739					89	8	
34			739	747					89	8	
35			747	754					89	7	
36			754	803					90	7	
11/16 37			803	815					90	12	
7/8 38			815	825					72	10	
39			825	834					72	9	
40			834	843					82	9	
41			843	852					80	9	
42			852	902					79	10	
43			902	911					78	9	
44			911	920					76	9	
45			920	930					77	10	
46			930	939					77	9	
47			939	948					78	9	
48			948	957					73	9	
49			957	1006					76	9	
50			1006	1016					80	10	
51			1016	1025					80	9	
52			1025	1034					83	9	
53			1034	1043					81	9	
54			1043	1052					82	9	
55			1052						83		

SD 5343

Louisiana-Pacific Corpora

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-17-90

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

	LOAD NO.	Cycle ~~LINE TEMP~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
7/3	1	780	310	11:01	11:11	710	Pit :60	Finer :45	290	74	10	
	2			11:11	11:20					71	9	
7¼ x	3			11:20	11:29					76	9	
	4			11:29	11:39					74	10	
45	5			11:39	11:49					78	10	
	6			11:49	11:57					76	8	
	7C			11:57	12:06					79	9	
	8			12:06	12:15					75	9	
	9			12:15	12:24					72	9	
	10			12:24	12:34					74	10	
	11			12:34	12:44					72	10	
	12			12:44	12:54					76	10	
7/8	13			12:54	1:04					75	10	
19 7/8 x	14C			1:04	1:14					76	10	
145	15			1:14	1:22					75	8	
	16			1:22	1:32					73	10	
	17			1:32	1:45					75	13	
7/8	19	840		1:45	1:55	650			230	79	10	
7¼ x	19C			1:55	2:07					76	12	
80	20			2:07	2:19					74	12	
	21			2:19	2:32					78	13	
52 7/8 x	22			2:32	2:46	600			180	76	14	
280	23			2:46	3:00					79	14	
52¼ x	24C			3:00	3:11					76	11	
36	25			3:11	3:24					78	13	
	26			3:24	3:37					79	13	
51 x	27			3:37	3:50					74	13	
295	28			3:50	4:04					78	14	
	29			4:04	4:16					74	12	

SD 5343

Louisiana-Pacific Corpora

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-17-92

SHIFT D-11-7

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

	LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Psi. HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1"	30C	860	310	4:16	4:30	600			190	71	14	
49 7/8	31			4:30	4:44					75	14	
2:5	32			4:44	5:06					76	20	
	33 C			5:06	5:26					74	20	
	34			5:26	5:41					73	15	
11/16	35	700	300	5:41	5:50	710			290	78	9	
	36			5:50	5:59					81	9	
5 1/2	37 C			5:59	6:08					80	9	
2:5	38			6:08	6:16					83	8	
Col.	39			6:16	6:24					84	8	
	40			6:24	6:32					81	8	
	41			6:32	6:40					85	8	
	42			6:40	6:48					78	8	
	43			6:48	6:56					81	8	
	44 C			6:56						84		
	45											
	46											
	47											
	48											
	49											
	50											

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-19-92 Shift C Pressing Cycle

Foreman Mike Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
11/16	51½ x 395	59	944	0		944

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: Dumped 2) 11/16 - 395 Footage 83,072 ✓

Sent them out Usage 81.1

Date 10 38 ✓

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-18-92 Shift B Pressing Cycle

Foreman Tank Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
11/16	51 1/2 x 295	47	752			752

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	55			6:34 - 7:29 Prepress belt broke
		5		10:10 - 10:20 #1 infeed belt shut off
				Plugged Cyclone
		20		10:20 - 11:00 #1 plug feeder stalled
				out
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	55	25		80

Comments: Footage - 66 1/2 %

Usage - 86 %

Rate - 99 %

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-18-1992 Shift A Pressing Cycle

Foreman Mickey Davis Hours 11-7 Total Cycle

	Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
ob	1/16	51½x295	50	800	0		800
certif	3/16	51½x295	2	32	0		32

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
		-33		11:00-12:05 down on core from last shift. Plug feeder screw stalled out. Drilled cap off of plug feeder splitter.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
		-33		-33

Comments:

Footage: 73,472

Resin: 521

Rate: 7263

10 mats dumped in pit.

SD 5344

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-18-92

SHIFT C-7-3

OPERATOR Gary

BOARD THICKNESS 11/16

BOARD SIZE 51 1/2 x 225

BOARD TYPE 100 D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	[illegible]	330	707	717	710	Pat	Timer	350	93	10	
2			717	726		[illegible]	[illegible]		93	9	
3			726	735					90	9	
4			735	744					90	9	
5			744	[illegible]					91	9	
6			[illegible]	[illegible]					89	9	
7			[illegible]	810	670			310	90	8	
8			810	818					93	8	
9			818	826					91	8	
10			826	834					91	8	
11			834	842					90	8	
12			[illegible]	849					90	7	
13			849	856					89	7	
14			856	864					90	8	
15			864	872					92	8	
16			[illegible]	920					91	8	
17			920	928					91	8	
18			928	936					90	8	
19			936	944					87	8	
20			944	954					90	10	
21			954	1003					89	9	
22			1003	1011					91	8	
23			1011	1018					92	7	
24			1018	1025					93	7	
25			1025	1033					96	8	
26			1033	1041					96	8	
27			1041	1049					95	8	
28			1049	1057					93	8	
29			1057	1105					93	8	

11/16 225 .01.

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE [illegible]

SHIFT [illegible]

OPERATOR [illegible]

BOARD THICKNESS [illegible]

BOARD SIZE [illegible]

BOARD TYPE [illegible]

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	6:00	[illegible]	1105	1112	670	[illegible]	[illegible]	310	88	7	
31			1112	1120		100	115		[illegible]	8	
[illegible]			1120	1128					89	8	
[illegible]			1128	1136					87	8	
[illegible]	X		1136	1144	870			510	85	8	
[illegible]			1144	1152					87	8	
[illegible]			1152	[illegible]					87	8	
[illegible]			[illegible]	[illegible]					86	8	
[illegible]			[illegible]	1216					85	8	
[illegible]			1216	[illegible]					87	8	
40			[illegible]	1232					89	8	
[illegible]		Y	1232	1240	970			610	86	8	
[illegible]			1240	1248					87	8	
[illegible]			1248	1256					89	8	
[illegible]			1256	[illegible]					90	8	
[illegible]			[illegible]	[illegible]					92	8	
[illegible]			112	[illegible]					[illegible]	8	
47			[illegible]	128					[illegible]	8	
[illegible]			128	136					[illegible]	8	
[illegible]			136	144					[illegible]	8	
50			144	152					[illegible]	8	
51			152	200	570			210	95	8	
[illegible]			200	209	[illegible]			140	93	9	
[illegible]			209	217	470			110	101	8	
54	X	[illegible]	217	225					100	8	
55			225	233					102	8	
[illegible]			233	240	430			60	93	7	
[illegible]			240	248					92	8	
[illegible]			248	256					93	8	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-18-76

SHIFT 1-7-3

OPERATOR Gary

BOARD THICKNESS 11/16

BOARD SIZE [illegible]

BOARD TYPE [illegible]

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

11/16
275
201

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
59	600	300	2516			Pr.	Time		9.4		
						100	15				

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-[illegible]-92

FT [illegible]

OPERATOR [illegible]

BOARD THICKNESS 11/16

BOARD SIZE 51½ X 295

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	[illegible]	300	303	312	[illegible]	[illegible]	[illegible]	[illegible]	100	9	
2			312	320					100	8	
3			320	329					103	9	
4			329	337					115	8	
5			337	346					124	9	
6			346	355					125	9	
7			355	404					122	9	
8			404	414					117	10	
9			414	422					116	8	
10			422	430					114	8	
11			430	439					114	9	
12			439	448					123	9	
13			448	456					123	8	
14			456	505					116	9	
15			505	514					107	9	
16			514	522					101	8	
17			522	531					92	9	
18			531	540					94	9	
19			540	549					102	9	
20			549	558					101	9	
21			558	6:07					102	9	
22			6:07	6:16					111	9	
23			6:16	625					113	9	
24			6:25	634					112	9	
25			729	738					115	9	
26			738	746					115	9	
27			746	754					113	9	
28			754	803					109	9	
29			803	812					109	9	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-17-96

SHIFT B-3-11

OPERATOR [illegible]

BOARD THICKNESS 11/16

BOARD SIZE 51 1/2 x 225

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	620	305	812	821	400	60	15	130	104	9	
31			821	830					102	8	
32			830	838					99	9	
33			838	847					95	9	
34			847	856					[illegible]	9	
35			856	905					77	9	
36			905	914					92	8	
37			914	922					92	8	
38			922	930					94	9	
39			930	939					94	9	
40			939	948					94	9	
41			948	957					95	9	
42			957	1006					102	10	down of Core
43			1006	1016					93	13	
44			1016	1026					89	10	
45			1026	1044					93		
46			1044	1059					91		
47			1059						96		
48											

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-18-92

FT A-11-7

OPERATOR Pouloc

BOARD THICKNESS 11/16

BOARD SIZE 51½ x 225

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	Cycle ~~TIME TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE POSITION HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	7:10	300	1114	1130		Pot 40	Timer 1:45	330 70	91	16	
2	7:50		1130	1146			2:00		100	16	
3			1146	1202					111	16	
4			1202	1216					102	14	
5			1216	1226					99	10	
6			1226	1235					99	9	
7			1235	1244					120	9	
8			1244	1253					113	9	
9			1253	102					105	9	
10			102	112					104	10	
11			112	122					101	10	
12			122	131					100	9	
13			131	140					101	9	
14			140	149					94	9	
15			149	158					91	9	
C 16			158	207					93	9	
17			207	215					99	8	
18			215	223					102	8	
19			223	231					107	8	
20	6:50		231	239					106	8	
21			239	247					106	8	
22			247	255					104	8	
C 23			255	303					110	8	
24			303	312					125	9	
25			312	321					120	9	
26			321	329					119	8	
27			329	337					99	8	
28			337	345					97	8	
29			345	354					104	9	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-18-1992

SHIFT A 11-7

OPERATOR Ben Lee

BOARD THICKNESS 11/16-3/4

BOARD SIZE 51½x295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
C 30	6:40	300	354	402		Pot 60	Timer 145	300 40	101	8	
31			402	410					100	8	
32			410	419					99	9	
33			419	427					114	8	
34			427	435					104	8	
35			435	444					102	9	
36			444	452					100	8	
37			452	500					101	8	
38			500	508					102	7	
39			508	516					100	8	
40			516	524					103	8	
41			524	533					101	9	
42			533	541					101	9	
43			541	550					102	9	
44			550	559					103	9	
C-45			559	608					101	9	
46			608	616					100	8	
47			616	624					103	8	
48			624	632					110	8	
49			632	640					109	8	
50			640	649					111	8	
51			649	657					103	8	
52			657	706					110	9	

Average

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-19-93 Shift 3 Pressing Cycle

Foreman Mike Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/4	51½x295	7	112	0		112
3/4	51½x295	4	64	0		64
3/4	51½x295	7	112	0		112
(SW) 3/4	51½x295	33	528	0		528

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
		-8		832-840 Lost Control Down
				It from on #2 Station
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
		-8		-8

Comments: No mats dumped

Footage 78,336

Usage 50.0

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SD 5344

Louisiana-Pacific Co.,.oration

PRESS ..EPORT AND DOWNTIME

Location Clayton

Date 3-19-92 Shift B Pressing Cycle

Foreman Robert Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/4	51 1/2 x 275	42	672			672
11/16	51 1/2 x 275	12	192			192

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments:

Footage 81,408

Usage 849

Rate 10,176

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-19-92 Shift A Pressing Cycle

Foreman Mickey Jones Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1/2	[illegible]	57	912	0		912

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			-13	4:35-4:10 Rev. Coil + cleaned [illegible]
				Loader - main hydraulic pump [illegible]
				4 times loose wire in [illegible]
				but no down time
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			-13	-13

Comments:

Footage: 8055

No mats damaged in pit

Resin: 52.7

Paper: 10.423

SD 5344

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-19-1992

SHIFT C 7-3

OPERATOR Gary Knight

BOARD THICKNESS 3/4

BOARD SIZE 51½ 12?

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

	LOAD NO.	cycle ~~TEMP~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE		~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
3/4	1	700	300	706	716	330	Pot	Time:	70	102	10	
35	2			716	725		100	15		107	9	
Drift	3			725	734					110	9	
	4		290	734	744					115	10	
	5			744	754					127	10	
	6			754	804					124	10	
	7			804	814					135	10	
3/4	8			814	823					107	9	
35	9			823	832					100	9	830-500 Loss-
ap	10			832	845					113	13	Control power at
	11			845	904					159	9	forming on #2
3/4	12			904	913					116	9	System
295	13			913	922					110	9	
35	14			922	930					106	8	
	15			930	938					106	8	
	16			938	947					107	9	
	17			947	956					109	9	
	18			956	1005					113	9	
3/4	19			1005	1014					126	9	
35	20			1014	1023					132	9	
220	21			1023	1031					129	8	
210	22			1031	1040					127	9	
	23			1040	1049					130	9	
	24			1049	1057					128	8	
	25			1057	1106					132	9	
	26			1106	1115					117	9	
	27			1115	1124					136	9	
	28		x	1124	1133					135	9	
	29		x	1133	1142					127	9	

SD 5343

Louisiana-Pacific Corporation

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-19-92

SHIFT C-7-3

OPERATOR Gary

BOARD THICKNESS 3/4"

BOARD SIZE 5½" x 0.25

BOARD TYPE M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	700	270	1142	1151	330	POT.	Timer	70	124	9	
31			1151	1200		100	115		122	9	
32			1200	1209					122	9	
33			1209	1218					125	9	
34			[illegible]	1227					124	9	
35			[illegible]	1235					124	8	
36			1235	[illegible]					125	9	
37			[illegible]	[illegible]					[illegible]	9	
38			[illegible]	[illegible]					125	9	
39			[illegible]	[illegible]					100	9	
40			[illegible]	[illegible]					102	9	
41			[illegible]	129					117	9	
42			129	132					122	9	
[illegible]			132	147					126	9	
[illegible]			147	156					124	9	
45			156	205					124	9	
46			205	214					129	9	
47			214	223					152	9	
48			223	233					153	10	
49			233	243					129	10	
50			243	253					133	10	
51			253						130		

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-9-90

SHIFT B-3-11

OPERATOR [illegible]

BOARD THICKNESS 3/4

BOARD SIZE 51 1/2 X 295

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	700	290	301	310	330	40	15	.70	109	9	
2			310	318					108	8	
3			318	326					106	8	
4			326	335					102	9	
5			335	343					87	8	
6			343	352					85	9	
7			352	400					104	8	
8			400	409					126	9	
9			409	417					127	8	
10			417	425					134	8	
11			425	434					149	9	
12			434	443					148	9	
13			443	452					124	9	
14			452	501					115	9	
15			501	510					112	9	
16			510	519					92	9	
17			519	528					106	9	
18			528	538					149	10	
19			538	548					182	10	
20			548	558					138	10	
21			558	6:08					118	10	
22			6:08	6:18					137	10	
23			6:18	6:28					168	10	
24			6:28	6:38					169	10	
25			6:38	6:47					167	9	
26			6:47	656					169	9	
27			656	705					165	9	
28			705	715					177	10	
29			715	724					174	9	

SD 5343

Louisiana-Pacific Corpora 7

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-19-88

SHIFT 7-3-11

OPERATOR Micky

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	800	290	724	734	320	40	15	100	168	10	
31			734	743					169	9	
32			743	753					179	10	
33			753	802					164	9	
34			802	812					140	10	
35			812	821					140	9	
36			821	830					162	9	
37			830	8:40					142	10	
38			8:40	8:49					143	9	
39			8:49	8:58					141	9	
40			8:58	908					146	10	
41			908	917					158	9	
3/4 42			917	926					162	9	
11/16 43			926	935					117	9	
44			935	944					106	9	
45			944	954					97	10	
46			954	1002					97	8	
47			1002	1010					98	8	
48			1010	1018					97	8	
49			1018	1025					102	7	
50			1025	1034					100	9	
51			1034	1042					99	8	
52			1042	1049					108	7	
53			1049	1056					118	7	
54			1056						110		

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-19-96

SHIFT A-11-7

OPERATOR [illegible]

BOARD THICKNESS 11/16

BOARD SIZE 5'[illegible]

BOARD TYPE UCF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~TIME PEND~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE/Position HIGH	INTERMEDIATE [redacted]	[redacted]	[redacted]	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	6:00	[illegible]	1104	112[illegible]		Pot 60	Timer :45	280 60.[illegible]	102	8	
2			1112	1120					119	8	
3	6:20		1120	1128					125	8	
4			1128	1136					127	8	
5			1136	1144					126	8	
6			1144	1152					127	8	
7			1152	1159					124	7	
C 8			1159	1206					124	7	
9			1206	1215					126	9	
10			1215	1223					122	8	
11			1223	1231					103	8	
12			1231	1239					97	8	
13			1239	1246					100	7	
14			1246	1254					112	8	
C 15			1254	101					110	7	
16			101	109					117	8	
17			109	117					113	8	
18			117	125					111	8	
19			125	133					115	8	
20			133	141					119	8	
21			141	149					113	8	
22			149	158					101	9	
C 23			158	206					100	8	
24			206	215					99	9	
25			215	223					109	8	
26			223	231					102	8	
27			231	239					101	8	
28			239	248					103	9	
29			248	256					105	8	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE _____

SHIFT _____

OPERATOR Ben Lee

BOARD THICKNESS 11/16

BOARD SIZE 51 1/2 x 295

BOARD TYPE MDP

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position. HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
C 30	6:20	300	255	304		Pot 20	Timer 14		97	8	
31			304	313					99	9	
32			313	321					98	8	
33			321	329					99	8	
34			329	337					100	8	
35			337	345					103	8	
36			345	352					107	7	
37			352	400					112	8	
38			400	408					113	8	
39			408	416					110	8	
40			416	425					97	9	
41			425	434					90	9	
42			434	444					97	10	
43			444	458					127	14	
C 44			458	512					113	14	
45			512	523					113	11	
46			523	531					109	8	
47			531	539					105	8	
48			539	548					100	9	
49			548	557					104	9	
C 50			557	605					112	8	
51			605	613					110	8	
52			613	621					111	8	
53			621	629					113	8	
54			629	638					109	9	
55			638	646					111	8	
56			646	654					119	8	
57			654	702					123	8	

SD 5343

Louisiana-Pacific Co.,oration

PRESS ..EPORT AND DOWNTIME

Location Clayton

Date 2-[illegible]-7[illegible] Shift C Pressing Cycle

Foreman [illegible] Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
[illegible]	[illegible]	9	144	0		144
[illegible]	[illegible]	7	112	0		112
[illegible]	[illegible]	33	528	0		528

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
		-7		7:2-7:4 [illegible]
				[illegible]
		-6		9:32-9:39 " " " "
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
		-13		-13

Comments: NO mats dumped

Footage 71,855

Hours 95.1

Rate 923.4

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-20-92 Shift D Pressing Cycle

Foreman George Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
11/16	51½ x 295	60	960	0		960

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No down time
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				- 0

Comments: No Mat'l Dumped

Eq. Eff. . 84,480 ✓

P.U. . 81.7

Pcf . 10,500

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-20-92 Shift A Pressing Cycle

Foreman Mickey Davis Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
11/16	51½x245	52	832	0		832
1 3/16	49 7/8x245	1	16	0		16

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	-3		-15	3:30-4:05 Rev. Core & cleaned dryer. Replaced ref. feeder packing & fixed leak on high pressure water line while reversing
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	-3		-15	-18

Comments:

No mats dumped in pit

Footage: 75,035

Resin: 47.3

Rate: 9745

SD 5344

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-20-1992

FT C 7-3

OPERATOR Gary Knight

BOARD THICKNESS 11/16

BOARD SIZE 51½ by 295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE (psi) HIGH	INTERMEDIATE ~~PRESS~~ POT	INTERMEDIATE ~~TIME~~ Timer	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
11/16 1	650	300	703	712	310			90	89	9	712 - 719 Ejector
2			719	728		100	15		89	9	Cont. Came off
3			728	737					91	9	
4			737	745					90	8	
5			745	753					93	8	
6			753	801					94	8	
7			801	809					97	8	
8			809	817					96	8	
9			817	833					92	16	
3/16 10	1020		833	849	950			550	90	16	
11			849	903					89	14	903 - 909 Ejector
12	1140		909	924					89	15	Cont. Came off
13			924	940					86	16	
14			940	956					89	16	
15			956	1011					79	15	
16			1011	1025					80	14	
17			1025	1033	310			90	79	8	
18			1033	1041					82	8	
19			1041	1049					89	8	
20			1049	1057					87	8	
21			1057	1105					89	8	
22			1105	1113					89	8	
23			1113	1121					93	8	
24			1121	1129					92	8	
25			1129	1136					86	7	
26			1136	1144					80	8	
27			1144	1151					80	7	
28			1151	1158					82	7	
29			1158	1206					84	8	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-20-9

SHIFT 2-7-3

OPERATOR [illegible]

BOARD THICKNESS 11/16

BOARD SIZE 51½ x 295

BOARD TYPE M.D.F.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
[illegible]	[illegible]	[illegible]	1206	1216	310	[illegible]	[illegible]	90	89	10	
[illegible]			1216	1225		[illegible]	[illegible]		93	9	
[illegible]			1225	1235	360			140	89	10	
[illegible]			1235	[illegible]					100	9	
[illegible]			[illegible]	1253					[illegible]	9	
[illegible]			1253	102	400			180	114	9	
[illegible]			102	111					107	[illegible]	
[illegible]			111	[illegible]					97	9	
[illegible]			[illegible]	129					100	9	
[illegible]			129	137					98	8	
[illegible]			137	145					96	8	
41		/	145	154					94	9	
42			154	202					92	8	
43			202	211	450			230	94	9	
44			211	219					94	8	
45			219	227					97	8	
46			227	235					96	8	
47			235	243					97	8	
48			243	252					99		
[illegible]			252						97		

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-20-96

FT [illegible]

OPERATOR [illegible]

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	~~LINE TEMP.~~ Cycle	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Posi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
11/16 1	620	290	3:00	3:08	450	Pot :60	timer :45	230	98	8	
51½ 2			3:08	3:16					96	8	
29.5 3			3:16	3:24					94	8	
4			3:24	3:32					98	8	
5			3:32	3:40	350			130	95	8	
6			3:40	3:48					92	8	
7			3:48	3:56					94	8	
8 C			3:56	4:04					91	8	
9			4:04	4:12					92	8	
10			4:12	4:20					96	8	
11			4:20	4:28					94	8	
12			4:28	4:36					95	8	
13			4:36	4:44					92	8	
14			4:44	4:52					94	8	
15			4:52	5:00					91	8	
16 C			5:00	5:08					94	8	
17			5:08	5:16					92	8	
18			5:16	5:24					96	8	
Loader			5:24	5:32					94	8	
20			5:32	5:40					96	8	
21			5:40	5:48					94	8	
22			5:48	5:56					92	8	
23 C			5:56	6:06					95	10	
24			6:06	6:14					91	8	
25			6:14	6:22					94	8	
26			6:22	6:30					92	8	
27			6:30	6:38					95	8	
28			6:38	6:46					92	8	
29			6:46	6:54					95	8	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-20-92

SHIFT D-3-11

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30 C	620	290	6:54	7:02	350	Pot .60	timer :45	130	94	8	
31			7:02	7:10					91	8	
32			7:10	7:19					94	9	
33			7:19	7:27					96	8	
34			7:27	7:35					94	8	
35			7:35	7:43					92	8	
36			7:43	7:51					94	8	
37			7:51	7:59					96	8	
38 C			7:59	8:07					94	8	
39			8:07	8:15					92	8	
40			8:15	8:24					94	9	
41			8:24	8:32					90	8	
42			8:32	8:40					91	8	
43			8:40	8:48					93	8	
44			8:48	8:56					91	8	
45			8:56	9:04					94	8	
46 C			9:04	9:13					91	9	
47			9:13	9:21					94	8	
48			9:21	9:29					94	8	
49			9:29	9:37					96	8	
50			9:37	9:45					94	8	
51			9:45	9:53					92	8	
52			9:53	10:01					92	8	
53			10:01	10:09					94	8	
54 C			10:09	10:17					92	8	
55			10:17	10:25					98	8	
56			10:25	10:34					99	9	
57			10:34	10:41					102	7	
58			10:41	10:49					109	8	

11/16 51½ x .95 Col.

SD 5343

Louisiana-Pacific Corpora

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-20-92

SHIFT D-2-11

OPERATOR Anthony

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	~~LINE TEMP.~~ Cycle	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
59	620	290	10:49	10:57	350	Pot :60	timer :15	130	111	8	
60c			10:57						113		

SD 5343

Louisiana-Pacific Corpora

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-20-92

SHIFT A-11-7

OPERATOR Ben

BOARD THICKNESS 11/16

BOARD SIZE 57 1/2 x 8'0"

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	~~TIME TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE ~~UPPER~~	INTERMEDIATE ~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	2:00	30	1104	1112		60 50	Timer	350 130	101	8	
2			1112	1120					107	8	
3			1120	1128					110	8	
4			1128	1136					117	8	
5			1136	1144					127	8	
6			1144	1152					124	8	
7			1152	1201					127	9	
C 8			1201	1210					127	9	
9			1210	1219					124	9	
10			1219	1228					124	9	
11			1228	1236					123	8	
12			1236	1244					113	8	
13			1244	1252					123	8	
14			1252	100					120	8	
C 15			100	109					115	9	
16			109	117					109	8	
17			117	125					119	8	
18			125	133					108	8	
19			133	141					111	8	
20			141	149					117	8	
21			149	157					124	8	
C 22			157	205					121	8	
23			205	213					123	8	
24			213	222					120	9	
25			222	230					123	8	
26			230	238					119	8	
27			238	246					120	8	
28			246	255					119	9	
29			255	304					114		

SD 5343

Louisiana-Pacific Corpora

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-20-92

SHIFT A 11-7

OPERATOR Ben Lee

BOARD THICKNESS 11/16 - 13/16

BOARD SIZE 51 1/2 x 295 - 44 x 295

BOARD TYPE MDF

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	CYCLE ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Position HIGH	INTERMEDIATE ~~UPPER~~	~~LOWER~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	520	500	304	313		HOT 60	Time 145	350 130	114	9	
31			313	322					112	9	
32			322	331					112	9	
33			331	341					113	10	
34			341	358					110	17	
35			358	415					113	17	
36			415	424					112	9	
37			424	432					108	8	
38			432	441					94	9	
39			441	449					94	8	
40			449	458					93	9	
41			458	506					92	8	
42			506	514					94	8	
43			514	523					99	9	
44			523	531					93	8	
45			531	539					91	8	
46			539	548					96	9	
47			548	556					99	8	
48			556	605					101	9	
49			605	614					102	9	
50			614	624					103	10	
51			624	638					100	14	
52			638	653					99	15	
53			653	706					101	13	
54											
55											
56											
57											
58											

SD 5343

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-21-92 Shift B Pressing Cycle

Foreman Robert Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 3/16	49 7/8 x 245	23	368			368
1 3/16	52 1/4 x 267	1	16			16
1 3/16	52 1/4 x 277	3	48			48
1 3/16	52 1/4 x 280	3	48			48
1 3/16	52 1/4 x 286	4	64			64
1 3/16	52 1/4 x 293	2	32			32

DOWNTIME REPORT

Record in Minutes				
Elect.	Mech.	Operators	Other	7:19-7:35 Explain-Reasons
	6			Speed up's broke mate's
				and Raw into pre-press
				9:12-9:26
		13		-16 moisture got dry, mates
				pulled out of press
				210 213
3				-3 #8 pressure switch
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
3	6	13		22

Comments: Dumped two mate's in pit 1 3/16 49 1/8 x 245

got them out

Footage 70,207

Usage 955

Rate 8776

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-21-92 Shift D Pressing Cycle

Foreman George Hours 3-11 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 3/16	52 1/4 x 293	1	16	0		16
1 1/8	49 7/8 x 245	41	656	0		656

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No down time.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0 35

Comments: No Mats Pumped

Z. 1x . 72,948

P.U . 95.0

Pots . 9118

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3-21-92 Shift A Pressing Cycle

Foreman Mickey Davis Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 1/8	49 7/8x245	8	128	0		128
1 1/8	50 1/4x267	2	32	0		32
1 1/2	50 1/4x277	1	16	0		16
1 1/2	50 1/4x287	4	64	0		64
1 1/2	50 1/4x286	1	16	0		16
1 1/2	50 1/4x293	5	80	0		80

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				-0

Comments: 086

Footage: 74,~~604~~

no mats dumped in pit

Resin: 98.3

Psto: 9,271

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location _____

Date _____ Shift _____ Pressing Cycle _____

Foreman _____ Hours _____ Total Cycle _____

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1 1/8	47 1/4 x 245	3	48	0		42
13/16	49 7/8 x 245	3	48	0		42
15/32	49 7/8 x 245	10	160	0		50
1 1/4	[illegible]	3	48	0		42

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments: _____

SD 5344

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-21-92

SHIFT B-7-3

OPERATOR micky

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE PSI	PRESSURE PSI	PRESSURE PSI	PRESSURE PSI
MIN	MIN	MIN	MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	1060	290	705	717	350	60	15	130	71	12	
2			717	729					69	12	
3			735	747					77	12	-6 Speed up's brake made
4			747	759					76	12	and ran into pressure
5			759	811					80	12	
6			811	823					84	12	
7			823	835					87	12	
8			835	847					92	12	
9			847	859					100	12	
10			859	912					100	13	
11			926	942					102	16	-13 premature action
12			942	957					87	15	panel pulled out of press
13			957	1012					89	15	
14			1012	1025					85	13	
15			1025	1038					82	13	
16			1038	1050					72	12	
17			1050	1102					76	12	
18			1102	1114					74	12	
19			1114	1126					78	12	
20			1126	1138					81	12	
21			1138	1150					81	12	
22			1150	1202					77	12	
23			1202	1214					79	12	
24			1214	1225					86	11	
25			1225	1237					88	12	
26			1237	1250					93	13	
27			1250	102					95	12	
28			102	115					94	13	
29			115	126					89	13	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 5-21-72

FT P-7-3

OPERATOR [illegible]

BOARD THICKNESS

BOARD SIZE

BOARD TYPE

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS

TOTAL TIME

LOAD NO.	LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	1040	290	1:28	1:42	460	610	15	210	89	14	
31			1:42	1:56					91	14	
32			1:56	210					91	14	-3 7/8 pressure switch
33			213	224					92	11	
34			224	238					90	14	
35			238	256					92		
36			256						94		
37											
38											
39											
40											

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-21-92

SHIFT D-3-11

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

1 2/16 52 7/8 x 293

1 1/8 49 7/8 x 225

LOAD NO.	Cycle ~~LINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	1040	290	3:12	3:24	460	Pst :60	timer :45	210	91	12	
2			3:24	3:36					75	12	
3			3:36	3:49					79	14	
4			3:49	4:00					82	11	
5 C			4:00	4:10					81	10	
6			4:10	4:20	340			90	79	10	
7			4:20	4:30					76	10	
8			4:30	4:42					78	12	
9			4:42	4:55					79	13	
10 C			4:55	5:07					84	12	
11			5:07	5:19					81	12	
12			5:19	5:30					84	11	
13			5:30	5:41					82	11	
14			5:41	5:52					85	11	
15 C			5:52	6:04	390			130	81	12	
16			6:04	6:15					80	11	
17			6:15	6:26					78	11	
18			6:26	6:39					75	13	
19			6:39	6:49					78	10	
20			6:49	7:00					76	11	
21 C			7:00	7:11					73	11	
22			7:11	7:23					70	12	
[illegible]			7:23	7:35					74	12	
[illegible]			7:35	7:46					85	11	
[illegible]			7:46	7:57					84	11	
[illegible] C			7:57	8:09					82	12	
[illegible]			8:09	820					84	11	
[illegible]			820	8:31					81	11	
[illegible]			8:31	8:42					84	11	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-21-92

SHIFT D-3-11

OPERATOR Anthony

BOARD THICKNESS _____

BOARD SIZE _____

BOARD TYPE _____

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

	LOAD NO.	Cycle LINE TEMP.	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1 1/8	30	1000	290	8:42	8:53	380	pot :50	timer :02	130	84	11	
19 7/8	31			8:53	9:04					82	12	
x	32 C			9:04	9:16					83	12	
15	33			9:16	9:26					85	12	
	34			9:26	9:39					84	12	
	35			9:39	9:50					81	12	
	36			9:50	10:02					84	12	
	37 C			10:02	10:13					80	12	
	38			10:13	10:25					79	12	
	39			10:25	10:36					78	11	
	40			10:36	10:46					74	10	
	41			10:46	10:56					76	10	
	42 C			10:56						71		

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 3-21-77

SHIFT A-11-7

OPERATOR Ben

BOARD THICKNESS 1 1/8 - 1 3/16 - 5/32

BOARD SIZE 49 3/8 [illegible] 50 1/4 1267 [illegible]

BOARD TYPE D.P. 286-293

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI	PRESSURE ____ PSI
____ MIN	____ MIN	____ MIN	____ MIN

TIME TO STOPS ____ TOTAL TIME ____

LOAD NO.	CYCLE ~~GINE TEMP.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE psi HIGH	INTERMEDIATE UPPER	INTERMEDIATE LOWER	LOW	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
1	10:00	290	1109	1120		pot :60	timer :45	420 130	82	11	
2			1120	1131					85	11	
3			1131	1143					94	[illegible]	
4			[illegible]	1154				380 130	83	11	
5C			1154	1205					94	11	
6			1205	1217					90	12	
7			1217	1229					84	12	
8			1229	1240					83	11	
9			1240	1253					81	13	
10			1253	105					74	12	
11			105	118					93	13	
12			118	131					90	13	
13			131	144					91	13	
14			144	158					93	14	
15			158	212					92	14	
16			212	226					91	14	
17			226	239					94	13	
18			239	253					93	14	
[illegible]			253	306					92	13	
[illegible]			306	319					93	13	
[illegible]			319	331					94	12	
[illegible]			331	342					96	11	
[illegible]			342	353					85	11	
[illegible]			353	404					84	11	
[illegible]	10:00		404	415				990 420	84	11	
[illegible]			415	[illegible]					[illegible]	11	
[illegible]			[illegible]	437					[illegible]	11	
[illegible]			437	449				430 [illegible]	84	12	
[illegible]			449	501					85	12	

SD 5343

Louisiana-Pacific Corpora 1

SOUTHERN DIVISION

FLAKEBOARD

HOT PRESS REPORT

DATE 7-31-82

SHIFT A 11-7

OPERATOR Ben

BOARD THICKNESS 1 5/32 - 1 1/4

BOARD SIZE 49 7/8 x 45

BOARD TYPE D.8.

DESIRED PRESSING CONDITIONS

HIGH	UPPER INTERMEDIATE	LOWER INTERMEDIATE	LOW
PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI	PRESSURE _____ PSI
_____ MIN	_____ MIN	_____ MIN	_____ MIN

TIME TO STOPS _____ TOTAL TIME _____

LOAD NO.	Cycle ~~Time~~ ~~Temp.~~	PRESS TEMP.	TIME PRESS CLOSED	TIME PRESS OPENED	GAUGE PRESSURE Psi. HIGH	INTERMEDIATE ~~[illegible]~~	INTERMEDIATE ~~[illegible]~~	~~LOW~~	TIME TO STOPS	TOTAL PRESSING TIME	REMARKS
30	10:00	290	501	514		Pot 60	Timer :45	530 330	86	13	
31			514	526					81	12	
32			526	538					84	12	
33			538	549					80	11	
34			549	600					78	11	
35			600	612					79	12	
36			612	623					80	11	
37			623	635					81	12	
38			635	647					82	12	
39			647								
40											

SD 5343

DRYER TEST DATA

DRYER NO. 1 STACK #3 TEST #1

TEST TYPE: FORM., CO, THC

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner (MAGNA HELIC %OUT / FUEL RATE) PD	mA	~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
7:55	42	174	111	5.0	67.3/9.0	104			155°			WOOD FUEL COUNTER - 693285 ~~ACCUMULATOR OF GAS~~
8:10	42	174	110	5.0	65.6/8.5	109		10.0	160°			693355
8:25	42	172	110	4.5	66.1/8.5	99	39.0		164°			693434
8:40	42	174	109	5.0	66.3/9.0	107		10.0	164°			693503
8:55	42	171	109	4.5	68.8/8.5	109			166°			693583

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST Date 3-21-92
LP
Customer

TEST TYPE: FORM., CO, THC

TEST LOCATION: DRYER 1 - STACK #3

TEST #1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-21-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	7:55	8:10	8:25	8:40	8:55	THAYER SCALES 11650
Forming Line Speed	17.0	17.0	17.0	17.0	17.0	10180
Board Thickness	5/8"	5/8"	5/8"	5/8"	5/8"	10690
Press ~~Cycle Time~~ ZONE 1	218°	218°	218°	217°	217°	9840
Control Oil Temp. ~~Setpoint (Press)~~ 2	217°	217°	217°	217°	217°	9980
~~Press Circ. Pump #1 Motor Load~~ 3	220°	220°	220°	220°	220°	10300
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.4	10.2	10.6	10.5	10.6	10130
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	8140
RAW MATL MIX DRY BIN LEVEL	Hi Hi	Hi Hi	Hi Hi	Hi Hi	Hi Hi	9260
						8220

3 CHIPS 2 SHAVINGS

FLOW RATE 24,509 LBS/HR

TOTAL 98390

AVG. 19678

HEATER OPERATION

TIME					
Return Oil Temperature INLET	448	449	448	448	448
Feed Oil Temperature OUTLET	490	490	489	490	490
Heater Inlet Temperature HOT GAS	906	910	904	908	904
Heater Disch. Temperature COIL	642	642	640	642	641
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output %	81.6	72.4	76.9	70.1	80.4
Wood Fuel Delivery, Volts	151	126	144	135	140
Wood Air Signal, mA	13.0	12.0	12.5	11.5	11.5
Wood Burner Shell Temp.	189°	194°	148°	148°	150°
Wood Fuel Counter	257926	258080	258125	258212	258329
PD MAGNAHELIC	7.5	8.0	7.5	7.0	7.0

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT LP Date 3-21-92
Customer

DRYER TEST DATA

DRYER NO. 1 STACK #3 TEST # 2

TEST TYPE: FORM., CO, THC

Tomb, °F:
PBAR, "Hg:

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNA HELIC %OUT / FUEL RATE)	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
												WOOD FUEL COUNTER – 693700 ~~RECEIVING HOPPER GATE~~
9:20	42	161	106	4.5	71.2 / 8.0	99			174°			693764
9:35	42	163	106	4.5	71.8 / 8.5	97		10.0	176°			693835
9:50	42	161	106	4.5	71.3 / 8.0	90	34.0		185°			693891
10:05	42	161	106	5.0	71.3 / 8.5	88		10.0	190°			693971
10:20	42	158	105	5.0	71.7 / 8.5	96			189°			

TEST TYPE: FORM., CO, THC

TEST LOCATION: DRYER 1 - STACK # 3

TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-21-92

SHT. 2 OF 2

PROCESS INFORMATION

	TIME						THAYER SCALES
	Forming Line Speed	17.0	17.0	17.0	17.3	17.3	9930
	Board Thickness	5/8"	5/8"	5/8"	5/8"	5/8"	9020
	Press Cycle Time	217°	217°	217°	217°	217°	10080
	Control Oil Temp. Setpoint (Press)	217°	217°	217°	217°	217°	9660
	Press Circ. Pump #1 Motor Load	220°	220°	220°	220°	220°	10930
GPM	Press Circ. Pump #2 Motor Load RESIN	10.6	10.5	10.5	10.5	10.5	10160
MLPM	Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	11650
RAW MAT'L MIX	DRY BIN LEVEL	HI HI	HI HI	HI	HI	HI	10230
3 CHIPS 2 SHAVINGS							12840
							9420

FLOW RATE 24650 LBS/HR

TOTAL 103920

AVG. 20784

HEATER OPERATION

TIME					
Return Oil Temperature INLET	448	448	448	448	448
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	904	904	902	904	902
Heater Disch. Temperature COIL	642	641	642	642	642
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output %	84.7	87.2	93.6	91.8	84.0
Wood Fuel Delivery, Volts	131	136	144	129	123
Wood Air Signal, mA	12.0	11.0	11.5	12.0	11.0
Wood Burner Shell Temp.	160°	158°	166°	167°	168°
Wood Fuel Counter	258483	258577	258687	258766	258878
PD MAGNAHELIC	7.5	7.0	7.5	7.5	7.5

P.O. Box 330 / Neodesha, Kansas 66757, U.S.A. / Telephone: 316-325-2673 / Telex: 43-6402 / Telefax: 316-325-2670

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST LP Date 3-21-92
Customer

DRYER TEST DATA

DRYER NO. 1 STACK #4 TEST #1

TEST TYPE: Form, CO, THC

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNA HELIC %OUT / FUEL RATE)	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2~~ °F	AIR FLOW ACFM	REMARKS
11:05	42	158	103	4.5	69.4 / 7.5	89		10.4	191°			WOOD FUEL COUNTER - 694177 ~~RECEIVING THE DRYER~~
11:20	42	159	106	4.5	68.9 / 8.0	91			186°			694243
11:35	42	159	106	4.0	69.3 / 7.5	92	37.6		190°			694306
11:50	42	162	107	4.5	71.4 / 7.5	88			194°			694367
12:05	42	159	105	4.5	70.7 / 7.5	95		10.0	188°			694430

TEST TYPE: FORM, CO, THC

TEST LOCATION: DRYER 1 - STACK #4

TEST #1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-21-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	11:05	11:20	11:35	11:50	12:05	THAYER SCALES
Forming Line Speed	17.3	17.3	17.3	17.3	17.6	10280
Board Thickness	5/8"	5/8"	5/8"	5/8"	5/8"	12270
Press ~~Cycle Time~~ ZONE 1	217°	217°	217°	217°	217°	9440
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	217°	217°	217°	217°	217°	10630
~~Press Circ. Pump #1 Motor Load~~ 3	220°	220°	220°	220°	220°	9280
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.6	10.6	10.8	10.6	10.8	10190
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	10170
RAW MATL MIX 3 CHIPS 2 SHAVINGS — DRY BIN LEVEL	HI	HI	HI	HI	HI	12820
						1176°

FLOW RATE 25,390 LBS/HR

TOTAL 108130

AVG. 21626

HEATER OPERATION

TIME					
Return Oil Temperature INLET	448	448	448	448	448
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	898	897	899	895	898
Heater Disch. Temperature COIL	642	641	641	641	640
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output	83.9	86.7	79.8	41.0	87.7
Wood Fuel Delivery, Volts	121	132	117	136	137
Wood Air Signal, mA	11.0	11.5	10.0	12.0	11.5
Wood Burner Shell Temp.	167°	164°	165°	166°	165°
Wood Fuel Counter	259158	259277	259367	259469	259573
PD MAGNAHELIC	6.5	6.5	6.0	6.0	7.0

DRYER TEST DATA

DRYER NO. 1 STACK #4 TEST # 2

TEST TYPE: FORM., CO, THC

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNA HELIC %OUT / FUEL RATE)	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
12:25	42	159	103	4.5	70.1 / 8.5	101		10.4	185°			WOOD FUEL COUNTER - 694509 ~~REGENERATIVE THERMAL OXIDIZER~~
12:40	42	159	103	4.5	69.8 / 8.0	97	34.6		185°			694571
12:55	42	159	102	5.0	69.9 / 8.0	98			184°			694636
1:10	42	158	102	4.0	67.6 / 8.0	89		10.7	184°			694701
1:25	42	159	103	4.0	69.5 / 7.5	93			182°			694767

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT Date 3-21-92

Customer LP

TEST TYPE: FORM., CO, THC

TEST LOCATION: DRYER 1 - STACK #4

TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-21-92

SAT. 2 OF 2

PROCESS INFORMATION

TIME	12:25	12:40	12:55	1:10	1:25	THAYER SCALES
Forming Line Speed	17.6	17.6	17.6	17.6	17.6	10350
Board Thickness	5/8	5/8	5/8	5/8	5/8	12760
Press Cycle Time ZONE 1	217°	217°	217°	217°	217°	11430
Control Oil Temp. Setpoint (Press) 2	217°	217°	217°	217°	217°	11710
~~Press Circ. Pump #1 Motor Load~~ 3	220°	220°	220°	220°	220°	9580
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.8	11.0	11.0	10.9	11.0	11660
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	10240
RAW MATL MIX DRY BIN LEVEL	Hi	Hi Hi	Hi Hi	Hi Hi	Hi Hi	12050
						10540

3 CHIPS 2 SHAVINGS

FLOW RATE 25,390 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET	448	448	453	451	496
Feed Oil Temperature OUTLET	490	490	491	491	488
Heater Inlet Temperature HOT GAS	899	897	895	889	893
Heater Disch. Temperature COIL	641	639	655	625	633
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

112400
22480

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output %	80.6	81.1	79.8	79.7	79.0
Wood Fuel Delivery, Volts	129	126	123	128	116
Wood Air Signal, mA	11.5	11.5	11.0	12.0	11.0
Wood Burner Shell Temp.	162°	164°	164°	162°	164°
Wood Fuel Counter	259682	259686	259690	259958	260097
PD MAGNAHELIC	6.5	7.0	6.5	7.0	6.5

DRYER TEST DATA

DRYER NO. 2 STACK# 2 TEST# 3

TEST TYPE: FORM., CO, THC

Tomb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNA HELIC %OUT / FUEL RATE)	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
7:45	46.0	185	110	8.5	82.1 / 14.0	174			139°			WOOD FUEL COUNTER - 247656 ~~RECEIVING HOT OIL OKT~~
8:00	46.0	187	111	8.5	79.5 / 14.0	155		11.2	138°			247757
8:15	46.0	191	112	8.5	81.1 / 14.5	163			137°			247866
8:30	46.0	193	115	8.0	81.8 / 14.0	158	31.0		138°			247998
8:45	46.0	181	112	8.5	84.6 / 14.5	153		11.0	139°			248113

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT Date 3-20-92

Customer LP

TEST TYPE: Form., CO, THC

TEST LOCATION: DRYER 2 - STACK #2

TEST # 3

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-20-92

SHT. 2 OF 2

PROCESS INFORMATION

	TIME	7:45	8:00	8:15	8:30	8:45	THAYER SCALES
	Forming Line Speed	17.5	17.5	17.5	17.5	17.5	10110
	Board Thickness	5/8"	5/8"	5/8"	5/8"	5/8"	9440
	Press ~~Cycle Time~~ 1	217°	217°	217°	217°	217°	11710
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	213°	213°	213°	214°	214°	9720
	~~Press Circ. Pump #1 Motor Load~~ 3	221°	221°	221°	221°	221°	12540
MLPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	10.6	10.6	10.8	10.8	10.8	9820
GPM	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	16480
	DRY BIN LEVEL	HI	HI HI	HI HI	HI HI	HI HI	10490
							11800
							10680
						TOTAL	112790
						AVG.	22558

RAW MATL MIX
3 CHIPS 2 SHAVINGS

FLOW RATE 25,282 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	448	448	448	448	448
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	919	917	918	917	918
Heater Disch. Temperature COIL	644	644	644	644	646
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output %	69.3	68.2	67.6	67.7	69.8
Wood Fuel Delivery, Volts	119	122	120	117	115
Wood Air Signal, mA	9.0	9.5	10.0	9.5	9.5
Wood Burner Shell Temp.	160°	160°	160°	159°	160°
Wood Fuel Counter	685768	685896	685920	686012	686078
PD MAGNAHELIC	5.0	5.5	5.5	5.5	5.0

STACKS 5 & 6 — RPM — CORE / FACE — STACKS 7 & 8

DRYER TEST DATA

PRESS LINE ~~DRYER~~ NO. 1 FACE STACK #8 TEST # 1

TEST TYPE: FORM., CO, THC

Tomb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~ RPM	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2~~ °F	AIR FLOW ACFM	REMARKS DRY BIN WINDOWS
10:45	72	212	129	~	—	925/800			~	~	~	2
11:00	72	209	131	~	—	900/800		10.0	—	—	—	2
11:15	72	210	130	~	—	875/800			—	—	—	1½
11:30	72	210	128	~	—	875/800	20.2	11.4	—	—	—	1½
11:45	72	206	128	~	—	925/800			—	—	—	2

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST LP Date 3-20-92

Customer

TEST TYPE: FORM., CO, THC

TEST LOCATION: ~~PRESS LINE 1~~ - STACK #8

TEST #1

THIS SHOULD BE DRYER STACK 8

MEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-20-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	10:45	11:00	11:15	11:30	11:45		THAYER SCALES
Forming Line Speed	52	52	52	52	52		
Board Thickness	11/16"	11/16"	11/16	11/16	11/16		
Press Cycle Time	6:00	6:00	6:00	6:00	6:00		
Control Oil Temp. Setpoint (Press)	290	290	290	290	290		
GPM ~~Press Circ. Pump #1 Motor Load~~ RESIN	7.9	7.9	7.9	7.8	7.8		
LPM ~~Press Circ. Pump #2 Motor Load~~ WAX			1500				
~~Press Circ. Pump #3 Motor Load~~							
RAW MAT'L MIX ~~DRY BIN LEVEL~~							

1 CHIPS 3 SHAVINGS 1/4 SAW TRIM

FLOW RATE 47551 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET					
Feed Oil Temperature OUTLET					
Heater Inlet Temperature HOT GAS					
Heater Disch. Temperature COIL					
Control Temperature Setpoint					
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

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DRYER TEST DATA

PRESS LINE ~~DRYER~~ NO. 1 ~~FAE~~ STACK # 8

TEST TYPE: FORM., CO, THC

TEST # 2

Tomb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~ RPM / ~~FUEL RATE~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
12:25	72	207	129	—	—	925 / 800			—	—	—	~~LOSSO FUEL COUNTER~~ ~~ACCUMULATOR~~	2
12:40	72	208	129	—	—	900 / 800	22.0	10.4	—	—	—		2
12:55	80	213	131	—	—	900 / 800			—	—	—		1
1:10	80	212	130	—	—	900 / 800		10.8	—	—	—		1
1:25	84	206	129	—	—	900 / 800			—	—	—		2

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

Customer _____

By DB/RST / LP Date 3-20-92

TEST MTL · FORM., CO, THC

TEST LOCATION: ~~PRESS~~ LINE 1 - STACK #8

TEST # 2

DRYER STACK #8

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-20-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	12:25	12:40	12:55	1:10	1:25	THAYER SCALES
Forming Line Speed	45	45	45	45	45	
Board Thickness	11/16	11/16	11/16	11/16	11/16	
Press Cycle Time	6:00	6:00	6:00	6:00	6:00	
Control Oil Temp. Setpoint (Press)	290	290	290	290	290	
CPM ~~Press Circ. Pump #1 Motor Load~~ RESIN	7.8	7.9	8.1	8.1	8.1	
NLPM ~~Press Circ. Pump #2 Motor Load~~ WAX		1500				
~~Press Circ. Pump #3 Motor Load~~						
RAW MATL MIX ~~DRY BIN LEVEL~~						
1 CHIPS 3 SHAVINGS 1/4 SAW TRIM						

FLOW RATE 39,068 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET					
Feed Oil Temperature OUTLET					
Heater Inlet Temperature HOT GAS					
Heater Disch. Temperature COIL					
Control Temperature Setpoint					
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

DRYER TEST DATA

PRESS LINE ~~DRYER~~ NO. 1 ~~FACE~~ STACK #8

TEST TYPE: FORM., CO, THC

TEST #3

Tomb, °F: _____

PBAR, "Hg: _____

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

Customer _____ By DB/RST Date 3-..-92
LP

TIME	FEED %	TG_1 °F	TG_2 °F	~~ALAGNA HCCS~~ Wood Burner PD	~~% BOIL~~ Wood Burner mA	RPM ~~FACE RATE~~ Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2~~ °F	AIR FLOW ACFM	REMARKS DRY BIN WINDOWS
1:45	84	205	129	—	—	900/800		10.4	—	—	—	~~DOSE FOR CONTROL~~ ~~RECYCLING HOT DIG GAS~~ 1
2:00	84	223	129	—	—	925/800	20.0			—	—	1
2:15	84	221	129	—	—	925/800				—	—	1
2:30	84	221	129	—	—	900/800		10.2		—	—	1
2:45	84	219	129	—	—	925/800				—	—	1

TEST TYPE: FORM., CO, THC

TEST LOCATION: ~~PRESS LINE~~ 1 - STACK #8

TEST # 3

DRYER STACK #8

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-20-92

SHT. 2 OF 2

PROCESS INFORMATION

	TIME	1:45	2:00	2:15	2:30	2:45	THAYER SCALES
	Forming Line Speed	48	48	48	48	48	
	Board Thickness	11/16	11/16	11/16	11/16	11/16	
	Press Cycle Time	6:00	6:00	6:00	6:00	6:00	
	Control Oil Temp. Setpoint (Press)	290	290	290	290	290	
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	8.4	8.1	8.1	8.1	8.1	
MLPM	~~Press Circ. Pump #2 Motor Load~~ WAX		1500				
	~~Press Circ. Pump #3 Motor Load~~						
	~~DRY BIN LEVEL~~						

RAW MATL MIX

81 CHIPS 3 SHAVINGS 14 SAW TRIM

FLOW RATE 43,123 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET					
Feed Oil Temperature OUTLET					
Heater Inlet Temperature HOT GAS					
Heater Disch. Temperature COIL					
Control Temperature Setpoint					
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

DRYER TEST DATA

PRESS LINE ~~DRYER~~ NO. 1 CORE STACK #6

TEST TYPE: FORM., CO, THC

TEST # 1

Tomb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~ ~~MAGNA HELIC~~ ~~%OUT~~ / RPM ~~FUEL RATE~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2~~ °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
4:05	90	178	125	—	—	1025/800		11.2	—	—	—	~~WOOD FUEL COUNTER~~ ~~RECEIVING NOT ON SITE~~	1
4:20	90	177	127	—	—	1000/800	19.2		—	—	—		1
4:35	90	178	128	—	—	1000/800		10.0	—	—	—		1
4:50	90	177	129	—	—	1000/800			—	—	—		1
5:05	90	176	129	—	—	1000/800		9.8	—	—	—		1

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST LP Date 3-20-92

Customer

MEC COMPANY
Neodesha, Kansas U.S.A.

TEST TYPE: FORM., CO, THC

TEST LOCATION: ~~PRESS LINE~~ 1- STACK #6

TEST # 1

Dryer Stack #6

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-20-92

SHT. 2 OF 2

PROCESS INFORMATION

	TIME	4:05	4:20	4:35	4:50	5:05	THAYER SCALES
	Forming Line Speed	48	48	48	48	48	
	Board Thickness	11/16	11/16	11/16	11/16	11/16	
	Press Cycle Time	6:20	6:20	6:20	6:20	6:20	
	Control Oil Temp. Setpoint (Press)	290	290	290	290	290	
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIGN	6.1	6.2	6.0	6.1	6.1	
HL PM	~~Press Circ. Pump #2 Motor Load~~ WAX	1200	—	—	—	1200	
	~~Press Circ. Pump #3 Motor Load~~						
RAW MATL MIX	~~DRY BIN LEVEL~~						

1 CHIPS 3 SHAVINGS 4 SAW TRIM

FLOW RATE 42839 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET					
Feed Oil Temperature OUTLET					
Heater Inlet Temperature HOT GAS					
Heater Disch. Temperature COIL					
Control Temperature Setpoint					
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA	—	—	—	NA
Flowing Gas/Oil Pressure After Reg.	NA	—	—	—	NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

DRYER TEST DATA

PRESS LINE ~~DRYER~~ NO. 1 CORE STACK # 6 TEST # 2

TEST TYPE: FORM., CO, THC

Tomb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~ RPM	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2~~ °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
5:25	90	175	128	—	—	1000/800		9.8	—		—	~~1000 FUEL COUNTER~~ ~~RECEIVING HOT OIL OFF~~	2
5:40	90	176	127	—	—	1050/800	23.3		—		—		2
5:55	90	173	128	—	—	1000/800		10.2	—		—		2
6:10	90	172	127	—	—	1000/800			—		—		2
6:25	90	173	127	—	—	1025/800		10.4	—		—		1½

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MAF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT LP Date 3-2092

Customer

TEST TYPE: FORM., CO, TMC

TEST LOCATION: ~~PRESS LINE~~ 1 - STACK #6

TEST # 2

DRYER STACK #6

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-20-92

SHT. 2 OF 2

PROCESS INFORMATION

	TIME	5:25	5:40	5:55	6:10	6:25	THAYER SCALES
	Forming Line Speed	48	48	48	48	48	
	Board Thickness	11/16	11/16	11/16	11/16	11/16	
	Press Cycle Time	6:20	6:20	6:20	6:20	6:20	
	Control Oil Temp. Setpoint (Press)	290°	290°	290°	290°	290°	
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.1	6.1	6.1	6.0	6.1	
MLPM	~~Press Circ. Pump #2 Motor Load~~ WAX		1200				
	~~Press Circ. Pump #3 Motor Load~~						
	~~DRY BIN LEVEL~~						

RAW MATL MIX

1 CHIPS 3 SHAVINGS 4 SAW TRIM

FLOW RATE 43,838 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET					
Feed Oil Temperature OUTLET					
Heater Inlet Temperature HOT GAS					
Heater Disch. Temperature COIL					
Control Temperature Setpoint					
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
ΔP MAGNAHELIC					

DRYER TEST DATA

PRESS LINE ~~DRYER~~ NO 1 CORE STACK #6 TEST #3

TEST TYPE:

Tomb, °F: _____

PBAR, "Hg: _____

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~ ~~TATAGION HELIX~~ ~~% BOOST~~ / RPM ~~FAN RATE~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS DRY BIN WINDOWS
6:55	90	172	134	—	—	1075/800		9.4	—	—	—	~~WOOD FUEL GRAPHITE~~ ~~ACCELERATOR DECAYS~~ 1
7:10	90	181	132	—	—	1075/800			—	—	—	1
7:25	90	182	131	—	—	1075/800	17.2		—	—	—	1
7:40	90	181	132	—	—	1100/800		9.0	—	—	—	1
7:55	90	180	130	—	—	1100/800			—	—	—	1

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

MEC COMPANY
Neodesha, Kansas U.S.A.

By DB/RST Date 3-20-92

Customer LP

TEST TYPE: FORM., CO, THC

TEST LOCATION: ~~PRESS LINE 1~~ - STACK #6

TEST #3

Dryer Stack #6

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-20-92

SAT. 2 OF 2

PROCESS INFORMATION

THAYER SCALES

	TIME	6:55	7:10	7:25	7:40	7:55	
	Forming Line Speed	48	48	48	48	48	
	Board Thickness	11/16	11/16	11/16	11/16	11/16	
	Press Cycle Time	6:20	6:20	6:20	6:20	6:20	
	Control Oil Temp. Setpoint (Press)	290°	290°	290°	290°	290°	
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.0	6.0	6.0	6.0	6.1	
1LPM	~~Press Circ. Pump #2 Motor Load~~ WAX			1200			
	~~Press Circ. Pump #3 Motor Load~~						
	~~DRY BIN LEVEL~~						

RAW MATL MIX

#1 CHIPS 3 SHAVINGS 4 SAW TRIM

FLOW RATE 43,19 LBS/HR

HEATER OPERATION

TIME						TOTAL GAS
Return Oil Temperature INLET						
Feed Oil Temperature OUTLET						
Heater Inlet Temperature HOT GAS						
Heater Disch. Temperature COIL						
Control Temperature Setpoint						
Oil Differential Pressure	NA	NA	NA	NA	NA	
Heater Differential Press. Setpoint						
Tee Section Static Pressure						
Main Circulating Pump Motor Load						
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA	

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

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mEC COMPANY

TEST TYPE: PART, CPM, O_2 & CO_2
" LOCATION: PRESS VENT # 6
" NO.: 1

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL
Plant Description: M.D.F
Date: 3/19/92

MC, 32.0
CORE MC2 10.2, 9.0
FACE MC2 9.6, 9.6

PROCESS INFORMATION

	TIME	12:21	12:36	12:51	1:06	1:21
FPM	Forming Line Speed	45.0	45.0	45.0	45.0	45.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control Temp. (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.5 | 7.7	6.5 | 7.7	6.8 | 7.7	6.5 | 7.7	6.3 | 7.7
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ALPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1900	1900	1900	1900	1900
	DRY BIN LEVELS (WINDOWS) CORE	4	4	4	4	4
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 43738 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: PART. CPM, O_2 & CO_2
" LOCATION: PRESS VENT #6
" NO.: 2

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL.
Plant Description: M.D.F.
Date: 3/19/92

MC, 30.0
PRE MC, 8.8, 10.2
FACE MC, 9.0, 10.4

PROCESS INFORMATION

	TIME	2:13	2:28	2:43	2:58	3:13
FPM	Forming Line Speed	42.0	42.0	42.0	42.0	42.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control ~~Set~~ Temp. ~~Setpoint~~ (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.5 | 7.7	6.6 | 7.7	6.6 | 7.7	6.7 | 7.7	6.6 | 7.7
MAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
LPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	3	2 1/2	3	3	2
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 42,144 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: PART. CPM, O_2 & CO_2
" LOCATION: PRESS VENT #6
" NO.: 3

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL.
Plant Description: M.D.F.
Date: 3/19/92

MC, 32
CORE MC, 9.6, 10.4
FACE MC, 10.4, 10.2

PROCESS INFORMATION

	TIME	3:59	4:14	4:29	4:44	4:59
FPM	Forming Line Speed	46.0	46.0	46.0	43.0	43.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control ~~Set~~ Temp. ~~Setpoint~~ (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.6 / 7.7	6.9 / 7.7	6.6 / 7.7	6.6 / 7.7	6.5 / 7.7
MAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ALPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	2	2	1 1/2	1	1
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 43,300 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE: PART, CPM, O_2 & CO_2
" LOCATION: PRESS VENT #7
" NO.: 1

Owner: L.P.

Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL

Plant Description: M.D.F.

Date: 3/19/92

MC, 33.0
CORE MC2 9.2, 10.2
FACE MC2 9.6, 9.6

PROCESS INFORMATION

	TIME	12:06	12:21	12:36	12:51	1:06
FPM	Forming Line Speed	45.0	45.0	45.0	45.0	45.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control ~~Set~~ Temp. ~~Setpoint~~ (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.5 | 7.7	6.5 | 7.7	6.6 | 7.7	6.5 | 7.7	6.5 | 7.7
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ILPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	4	4	4	4	4
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAWTRIM

HEATER OPERATION FLOW RATE 43.348 gal/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE: PART, CPM, O_2 & CO_2
" LOCATION: PRESS VENT #7
" NO.: 2

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL.
Plant Description: M.D.F.
Date: 3/19/92

MC, 30.0
CORE MC_2 9.2, 8.8
FACE MC_2 9.6, 9.0

PROCESS INFORMATION

	TIME	1:45	1:00	2:15	2:30	2:45
FPM	Forming Line Speed	44.0	44.0	42.0	42.0	42.0
IN.	Board Thickness	3/4"	3/4	3/4"	3/4"	3/4"
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control [redacted] Temp. [redacted] (Press)	290	290	290	290	290
IPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.6 | 7.7	6.7 | 7.7	6.6 | 7.7	6.6 | 7.7	6.7 | 7.7
MAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
LPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	3	3	3	2 1/2	3
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 40,559 ft/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: PART, CPM, O_2 & CO_2
" LOCATION: PRESS VENT #7
" NO.: 3

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL.
Plant Description: M.D.F
Date: 3/19/92

MC, 30
CORE MC_2 10.0, 9.6
FACE MC_2 10.6, 10.4

PROCESS INFORMATION

	TIME	3:23	3:38	3:53	4:08	4:23
FPM	Forming Line Speed	46.0	46.0	46.0	46.0	46.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control Temp. (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.6 / 7.7	6.4 / 7.7	6.5 / 7.7	6.4 / 7.7	6.6 / 7.7
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ALPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	2	2	2	2	1/2
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 44,481 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE PART, CPM, O_2 & CO_2
" LOCATION PRESS VENT #8
" NO. 1

Owner: L.P. Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL Plant Description: M.D.F.

Date: 3/18/92

MC, 29.0
CORE MC_2 9.8, 11.6
FACE MC_2 10.9, 10.9

PROCESS INFORMATION

	TIME	12:35	12:50	1:05	1:20	1:35
FPM	Forming Line Speed	50.0	50.0	50.0	50.0	50.0
IN.	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN.	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control [redacted] Temp. [redacted] (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.1/7.8	6.2/7.8	6.2/7.6	6.1/7.6	6.2/7.6
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ILPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	3	3	3	3	2 1/2
	DRY BIN LEVELS (WINDOWS) FACE	2	2	2	2	1 1/2

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 43893 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: PART. CPM, O_2 & CO_2
" LOCATION: PRESS VENT #8
" NO.: 2

Owner: L.P.

Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL.

Plant Description: M.D.F.

Date: 3/19/92

MC, 30.0
CORE MC_2 9.6, 9.6
FACE MC_2 10.4, 11.0

TEST ON HOLD 8:32
RESTART 8:55
LAST CONTROL PANEL READINGS
(PRECEDENTAL ESSM)

PROCESS INFORMATION

	TIME	7:50	8:05	8:20	8:58	9:13
FPM	Forming Line Speed	43.0	43.0	45.0	45.0	45.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control ~~Circ~~ Temp. ~~Setpoint~~ (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.5/7.5	6.5/7.5	6.4/7.5	6.7/7.2	6.8/7.4
AMAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ILPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	3	3	3	3	4
	DRY BIN LEVELS (WINDOWS) FACE	2	2	2	3	2

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/6 SAW TRIM

HEATER OPERATION FLOW RATE 42,205 ft/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE: PART, CPM, O_2 & CO_2
" LOCATION: PRESS VENT #8
" NO.: 3

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL.
Plant Description: M.D.F.
Date: 3/19/92

MC, 30.0
CORE MC2 9.8, 8.0
FACE MC2 9.3, 9.4

PROCESS INFORMATION

	TIME	9:52	10:07	10:22	10:37	10:52
FPM	Forming Line Speed	45.0	45.0	45.0	45.0	45.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control Temp. (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.3 | 7.4	6.2 | 7.4	6.3 | 7.3	6.2 | 7.4	6.3 | 7.4
MAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
LPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	3	4	4	4	4
	DRY BIN LEVELS (WINDOWS) FACE	2	2	2	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 40,525 ft/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoiht					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE : PART, CPM, O_2 & CO_2
" LOCATION : PRESS VENT #10
" NO. : 1

LINE 1

Owner: L.P. Test Personnel: R.G.T & D.B.

Location: CLAYTON, AL Plant Description: M.D.F.

Date: 3/18/92

MC, 29.8
CORE MC_2 11.6, 10.0
FACE MC_2 10.0, 11.0

PROCESS INFORMATION

	TIME	9:14	9:29	9:44	9:59	10:14
FPM	Forming Line Speed	50.0	50.0	50.0	50.0	50.0
IN.	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN.	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control ~~[illegible]~~ Temp. ~~[illegible]~~ (Press)	300	300	300	300	300
AMPS	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.2/7.6	6.2/7.6	6.4/7.8	6.3/7.8	6.3/7.8
AMPS	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
AMPS	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	2	2	2	2	2
	DRY BIN LEVELS (WINDOWS) FACE	2	2	2	2	2

RAW MATERIAL MIX
[illegible] SHAVINGS
1. CHIPS
1/4 SAW TRIM

~~[illegible]~~ FLOW RATE 43,599 ft³/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: PART, CPM, O_2 & CO_2
" LOCATION: PRESS VENT # 10
" NO.: 2

LINE 1

Owner: L.P.

Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL.

Plant Description: M.D.F.

Date: 3/19/92

MC, 35.0
CORE MC_2 10.2, 9.6
FACE MC_2 9.6, 10.9

PROCESS INFORMATION

	TIME	7:32	7:47	8:02	8:17	8:32
FPM	Forming Line Speed	43.0	43.0	45.0	45.0	4
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control Temp. (Press)	290	290	290	290	290
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.5 | 7.5	6.5 | 7.5	6.5 | 7.5	6.5 | 7.5	6.5 | 7.5
MAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ILPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	2	2	3	3	3
	DRY BIN LEVELS (WINDOWS) FACE	1	1	2	2	2

RAW MATERIAL MIX
3 SHAVINGS
1 " CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 41,423 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoiht					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: PART, CPM, O_2 & CO_2
" LOCATION: PRESS VENT #10
" NO.: 3

LINE 1

Owner: L.P

Test Personnel: R.G.T. & D.B

Location: CLAYTON, AL

Plant Description: M.D.F.

Date: 3/19/92

MC, 30.0
CORE MC2 9.8, 8.0
FACE MC2 9.7, 9.4

PROCESS INFORMATION

	TIME	9:39	9:54	10:09	10:24	10:39
FPM	Forming Line Speed	45.0	45.0	45.0	45.0	45.0
IN.	Board Thickness	3/4	3/4	3/4	3/4	3/4
MIN.	Press Cycle Time	7.0	7.0	7.0	7.0	7.0
°F	Control ~~[illegible]~~ Temp. ~~Setpoint~~ (Press)	290	290	290	290	290
PM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.3/7.4	6.2/7.4	6.3/7.4	6.3/7.4	6.3/7.4
AX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
PM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	4	3	4	4	4
	DRY BIN LEVELS (WINDOWS) FACE	2	2	2	2	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 42,146 #/HR

TIME					
~~Return Oil Temperature~~					
~~Feed Oil Temperature~~					
~~Heater Inlet Temperature~~					
~~Heater Disch. Temperature~~					
~~Control Temperature Setpoint~~					
~~Oil Differential Pressure~~					
~~Heater Differential Press. Setpoint~~					
~~Tee Section Static Pressure~~					
~~Main Circulating Pump Motor Load~~					
~~Aux. Circulating Pump Motor Load~~					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
~~Gas/Oil Heat Controller Output~~					
~~Flowing Gas/Oil Pressure After Reg.~~					
~~Wood Heat Controller Output~~					
~~Wood Fuel Delivery, Volts~~					
~~Wood Air Signal, mA~~					
~~Wood Burner Shell Temp.~~					
~~Wood Fuel Counter~~					

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DRYER TEST DATA

DRYER NO. 2 STACK # 1 TEST # 1

TEST TYPE: [redacted] FORM, CO, THC

Tomb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNA HELIC %OUT / FUEL RATE)	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
7:55	44.0			9.5	76.7 / 13.5	151		10.6	148°			WOOD FUEL COUNTER - 236549 ~~RECEIVING HOT OIL GAS~~
					—	STOP		TEST	8:01			RESTART 8:04
8:10	44.0			9.5	73.3 / 12.0	163			148°			236651
8:25	44.0			9.0	76.6 / 13.5	160	39.2		148°			236750
8:40	44.0			8.5	75.9 / 14.0	167		11.2	148°			236846
8:55	44.0			8.5	81.0 / 14.0	169			149°			236961

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

Customer _____ By DB/RST LP Date 3-19-92

FORM, CO, THC

TEST LOCATION: DRYER #2 - STACK # 1

TEST # 1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-19-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	7:55	8:10	8:25	8:40	8:55	THAYER SCALES
Forming Line Speed	22.0	22.0	22.0	22.0	22.0	12420
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	14900
Press ~~Cycle Time~~ ZONE 1	217°	217°	217°	217°	217°	13520
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	214°	214°	214°	12260
~~Press Circ. Pump #1 Motor Load~~ 3	214°	214°	214°	214°	214°	13060
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.2	10.4	10.5	10.4	10.3	12370
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	11170
DRY BIN LEVEL	HI	HI	HI	HI HI	HI	11660
						13650
						12320
TOTAL						123330
AVG.						24666

RAW MATL MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,445 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	449	449	449	448	449
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	918	915	917	915	914
Heater Disch. Temperature COIL	634	634	634	634	633
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output %	71.8	71.6	70.2	69.9	68.0
Wood Fuel Delivery, Volts	143	132	135	129	130
Wood Air Signal, mA	10.0	10.5	10.0	10.5	10.0
Wood Burner Shell Temp.	165°	166°	163°	164°	165°
Wood Fuel Counter	677518	677610	677802	677788	677901
PD MAGNAHELIC	6.0	6.0	6.0	5.5	5.5

TEST LOCATION: PRESS LINE 2-VENT #5

TEST #1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-19-92

PROCESS INFORMATION

TIME	8:30	8:45	9:00	9:15	9:30	THAYER SCALES
Forming Line Speed	22.0	22.0	22.0	22.0	22.0	13060
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	12370
Press ~~Cycle Time~~ ZONE 1	217	217	217	217	217	12450
~~Control~~ Oil Temp. Setpoint (Pr[illegible] 2	214	214	214	214	214	10[illegible]
~~Press Circ. Pump #1 Motor Load~~ 3	214	214	214	214	214	11570
~~Press~~ Circ. Pump ~~#2 Motor Load~~ RESIN	10.5	10.[illegible]	10.2	10.3	10.3	12740
Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	12160
DRY BIN LEVEL	HI	HI	HI	HI HI	HI HI	11110
						11370

RAW MATL MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,445 LBS/HR

TOTAL 120,490
AVG 24,098

HEATER OPERATION

TIME					AVG
Return Oil Temperature INLET	449	449	449	449	450
Feed Oil Temperature OUTLET	490	490	490	490	[illegible]
Heater Inlet Temperature HOT GAS	915	916	914	916	[illegible]
Heater Disch. Temperature COIL	634	633	633	634	634
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "H")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

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TEST LOCATION: PRESS LINE 2 - VENT #5

TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-19-92

PROCESS INFORMATION

TIME	10:00	10:15	10:30	10:45	11:00	THAYER SCALES 11250
Forming Line Speed	22.0	22.0	22.3	22.3	22.3	11420
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	10350
Press ~~Cycle Time~~ ZONE 1	217°	217°	217	217	217	14110
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	215	215	215	10460
~~Press. Circ. Pump #1 Motor Load~~ 3	[illegible]	214°	214	214	215	10660
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.2	10.2	10.3	10.5	10.2	11040
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	11670
DRY BIN LEVEL	HI	HI	HI	HI	HI	09430
						12320

RAW MAT'L MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,916 LBS/HR

TOTAL 112,730
AVG 22,546

HEATER OPERATION

TIME					
Return Oil Temperature INLET	450	450	450	450	450
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	915	914	915	912	914
Heater Disch. Temperature COIL	634	632	634	633	632
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "H")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

DRYER TEST DATA

DRYER NO. 2 STACK #1

TEST TYPE: [redacted]

FORM, CO, THC

TEST #2

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VOC~~ MAGNA HELIC %OUT / FUEL RATE	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2~~ °F	AIR FLOW ACFM	REMARKS
10:00	45.0	230	124	9.0	88.3 / 14.5	175		11.4	155°			WOOD FUEL COUNTER - 237566 ~~READING NOT UPDATE~~
10:15	45.0	228	123	9.0	90.1 / 13.5	179			154°			237684
10:30	45.0	228	123	9.5	88.4 / 15.0	171	41.0		154°			237808
10:45	45.0	229	123	9.0	89.4 / 14.0	163			155°			237941
11:00	45.0	230	123	9.0	88.4 / 15.0	172		11.0	155°			238071

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST LP Date 3-19-92

Customer

TEST LOCATION: DRYER #2 STACK #1

TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-19-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	10:00	10:15	10:30	10:45	11:00	THAYER SCALES
Forming Line Speed	22.0	22.0	22.3	22.3	22.3	10020
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	11860
Press Cycle Time 1	217°	217°	217°	217°	217°	9340
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	215°	215°	215°	10380
~~Press Circ. Pump #1 Motor Load~~ 3	214°	214°	214°	214	215°	10190
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.2	10.2	10.0	10.4	10.2	11200
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	10730
DRY BIN LEVEL	HI	HI	HI	HI	HI	12650
						11440
						11630

RAW MATL MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,916 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG
Return Oil Temperature INLET	449	450	450	450	450
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	915	914	915	914	913
Heater Disch. Temperature COIL	633	633	634	632	632
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output %	72.2	71.8	73.2	74.3	71.9
Wood Fuel Delivery, Volts	134	134	131	135	130
Wood Air Signal, mA	10.0	10.0	10.5	10.5	10.0
Wood Burner Shell Temp.	173°	173°	174°	174°	175°
Wood Fuel Counter	678319	678348	678474	678583	678681
PD MAGNAHELIC	5.5	6.0	6.0	6.0	6.0

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DRYER TEST DATA

DRYER NO. 2 STACK # 1

TEST #3

TEST TYPE: [redacted]

FORM., CO, THC

Tamb, °F: _____

PBAR, "Hg: _____

MAGNA HELIC %OUT / FUEL RATE

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
11:50	45.0	238	124	9.0	90.9 / 15.0	178			157°			WOOD FUEL COUNTER - 238487 ~~RECEIVING NOT ON-SITE~~
12:05	45.0	221	123	9.0	97.0 / 14.0	180		11.2	160°			238642
12:20	45.0	225	122	9.5	78.3 / 13.0	157			160°			238758
12:35	45.0	222	121	8.5	78.9 / 12.5	156	41.3		160°			238859
12:50	45.0	222	121	8.0	78.2 / 12.5	144		11.2	160°			238958

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST LP Date 3-19-92

Customer

[redacted]

TEST LOCATION: DRYER #2 STACK #1

TEST #3

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-19-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	11:50	12:05	12:20	12:35	12:50	THAYER SCALES 10980
Forming Line Speed	22.3	22.3	22.3	22.3	22.3	10900
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	11060
Press ~~Cycle Time~~ ZONE 1	217°	217°	217°	217°	217°	17640
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	214°	214°	215°	13910
~~Press~~ Circ. ~~Pump #1 Motor Load~~ 3	214°	214°	214°	214°	215°	15350
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.2	10.3	10.3	10.4	10.1	14540
~~Press~~ Circ. ~~Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	14280
DRY BIN LEVEL	HI	HI	HI	HI	HI HI	12620
						12580

RAW MATL MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,640 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET	450	450	450	450	450
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	912	910	915	911	907
Heater Disch. Temperature COIL	631	632	633	630	630
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output %	71.4	72.4	72.8	71.6	72.7
Wood Fuel Delivery, Volts	12.5	12.0	12.9	12.3	12.6
Wood Air Signal, mA	10.0	9.5	9.5	10.0	10.0
Wood Burner Shell Temp.	176°	172°	180°	179°	181°
Wood Fuel Counter	67398	67904	67956	67947	67997
PD MAGNAHELIC	6.0	6.0	5.5	6.0	5.5

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PRESS LINE 2
TEST LOCATION: PRESS VENT #5
TEST # 3

mEC COMPANY

Owner: LP
Test Personnel: DB/RGT
Location: CLAYTON, AL
Plant Description: MDF
Date: 3-19-92
SHT. 2 OF 2

PROCESS INFORMATION

TIME	11:35	11:50	12:05	12:20	12:35	11990
Forming Line Speed	22.3	22.3	22.3	22.3	22.3	11890
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	10470
Press ~~Cycle Time~~ ZONE 1	217	217	217	217°	217	12020
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214	214	214	214°	215	14010
~~Press Circ. Pump #1 Motor Load~~ 3	214	214	214	214°	215	15510
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.1	10.2	10.3	10.2	10.1	13020
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	14430
DRY BIN LEVEL	HI	HI	HI	HI	HI	14470
						10950

RAW MATL MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,640 LBS/HR

TOTAL 128,750
AVG 25,750

HEATER OPERATION

TIME					
Return Oil Temperature INLET	450	450	450	450	450
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	911	911	910	914	904
Heater Disch. Temperature COIL	632	632	632	631	629
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					
PD MAGNAHELIC					

DRYER TEST DATA

DRYER NO. 2 STACK #2 TEST #1

TEST TYP[redacted]
FORM., CO, THC

Tamb, °F: _____

PBAR, "Hg: _____

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST Date 3-19-92

Customer LP

MEC COMPANY
Neodesha, Kansas U.S.A.

TIME	FEED %	TG_1 °F	TG_2 °F	MAGNA HPLC Wood Burner PD	mA	~~VDC~~	FUEL RATE %OUT/	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2~~ ~~°F~~	AIR FLOW ACFM	REMARKS
													WOOD FUEL COUNTER - 240341
3:40	43.0	216	117	8.0	87.2 / 13.5	157				167°			~~DEVICE WAS NOT ON STAT~~
													240442
3:55	43.0	205	115	8.0	81.3 / 12.0	144	45.6			166°			
													240558
4:10	43.0	207	115	8.5	92.6 / 13.5	175		11.8		166°			
													240679
4:25	43.0	217	115	8.5	97.9 / 14.0	169				166°			
													240804
4:40	43.0	215	117	8.5	94.1 / 14.0	163				166°			

TEST [redacted] FORM, CO, THC

TEST LOCATION: DRYER 2- STACK #2

TEST # 1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-19-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	3:40	3:55	4:10	4:25	4:40	THAYER SCALES
Forming Line Speed	22.6	22.6	22.6	22.6	22.6	12390
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	10610
Press Cycle Time 1	217°	217°	217°	217°	217°	11360
Control Oil Temp. Setpoint (Press) 2	215°	215°	215°	215°	215°	12180
Press Circ. Pump #1 Motor Load 3	214°	214°	214°	214°	214°	12140
Press Circ. Pump #2 Motor Load RESIN	10.2	10.0	10.2	10.2	10.0	11860
Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	13470
DRY BIN LEVEL	HI	MED	MED	MED	HI	12930
						12100
						12950
TOTAL						110350
AVG						22070

RAW MATL MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,685 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	450	450	450	450	450
Feed Oil Temperature OUTLET	490	490	490	490	489
Heater Inlet Temperature HOT GAS	894	895	896	898	897
Heater Disch. Temperature COIL	629	630	630	632	629
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output %	72.2	72.9	73.2	76.4	75.1
Wood Fuel Delivery, Volts	124	121	118	115	123
Wood Air Signal, mA	9.5	9.5	9.5	9.0	9.5
Wood Burner Shell Temp.	177°	187°	189°	190°	190°
Wood Fuel Counter	680314	680396	680481	680585	680659
PD MAGNAHELIC	5.5	5.0	5.5	5.0	5.5

DRYER TEST DATA

DRYER NO. 2 STACK# 2 TEST# 2

TEST TYPE [redacted] FORM., CO, THC

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	MAGNA HELIC Wood Burner PD	mA	~~VDC~~	FUEL RATE	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
													WOOD FUEL COUNTER - 241556 ~~DEGREESING NOT DUCTS~~
5:50	43.0	212	116	8.0	84.2 / 13.5	159				165°			
													241450
6:05	43.0	210	116	8.5	93.1 / 13.5	164			12.0	165°			
													241570
6:20	43.0	210	115	7.5	85.5 / 13.0	158				165°			
													241693
6:35	43.0	219	116	8.5	85.1 / 13.5	153	39.4			160°			
													241801
6:50	43.0	217	116	8.0	73.9 / 12.0	139			12.0	159°			

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST/LP Date 3-19-92

Customer

MEC COMPANY
Neodesha, Kansas U.S.A.

TEST LOCATION: DRYER 2 - STACK #2

TEST # 1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-19-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	5:50	6:05	6:20	6:35	6:50	THAYER SCALES
Forming Line Speed	22.6	22.6	22.6	22.6	22.6	13080
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	12640
Press ~~Cycle Time~~ ZONE 1	217°	217°	217°	217°	217°	12080
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	214°	214°	214°	10940
~~Press Circ. Pump #1 Motor Load~~ 3	214°	214°	214°	214°	214°	10210
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.4	10.3	10.2	10.2	10.4	12740
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	13650
DRY BIN LEVEL	HI	HI	HI	HI-HI	HI	14040
						12300

RAW MAT'L MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,848 LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET	450	450	450	450	450
Feed Oil Temperature OUTLET	490	491	490	489	490
Heater Inlet Temperature HOT GAS	904	905	908	905	911
Heater Disch. Temperature COIL	634	635	634	634	635
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output 90	70.3	72.6	70.9	72.1	69.5
Wood Fuel Delivery, Volts	119	114	116	122	116
Wood Air Signal, mA	9.5	9.5	9.5	10.0	9.0
Wood Burner Shell Temp.	186°	188°	186°	183°	181°
Wood Fuel Counter	681057	681155	681235	681313	681410
PD MAGNAHELIC	5.5	5.0	5.5	5.5	5.5

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mEC COMPANY

TEST TYPE: PARTICULATE, CPM, CO_2, O_2
TEST LOCATION: PRESSLINE 2 VENT #3
TEST# 1

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-18-92

PROCESS INFORMATION

	TIME	9:45	10:00	10:15	10:30	10:45	THAYER SCALES
	Forming Line Speed	25.0	25.0	25.0	25.0	25.3	11860
	Board Thickness	7/16"	7/16"	7/16"	7/16"	7/16"	11420
	Press ~~Cycle Time~~ ZONES 1	220°	220°	220°	220°	220°	14170
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	214°	215°	215°	12520
	Press ~~Circ. Pump #1 Motor Load~~ 3	215°	215°	215°	216°	216°	14080
GPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	10.4	10.4	10.4	10.4	10.4	10630
LPM	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	12860
	FIBER BIN LEVEL	Hi Hi	Hi Hi	Hi Hi	Hi-Hi	Hi Hi	10020
							11120
							9580
						TOTAL	106992
						AVG	21398

RAW MATL. MIX
3 CHIPS 1 SHAVINGS

FLOW RATE 27,764 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	447	447	447	447	447
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	913	913	911	905	912
Heater Disch. Temperature COIL	640	639	639	640	639
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "X")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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TEST TYPE: PARTICULATE, CFM, CO_2, O_2

TEST LOCATION: PRESS LINE 2 VENT # 3
TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-18-92

PROCESS INFORMATION

	TIME	1:40	1:55	2:10	2:25	2:40	THAYER SCALES
	Forming Line Speed	22.5	22.5	22.5	22.5	22.5	14300
	Board Thickness	½"	½"	½"	½"	½"	12370
	Press ~~Cycle Time~~ 1	219°	219°	219°	219°	219°	12680
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	214°	219°	214°	11750
	~~Press Circ. Pump #1 Motor Load~~ 3	216°	216°	216°	216°	216°	14530
GPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	10.2	10.2	10.2	10.4	10.4	14810
MLPM	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	12210
	FIBER	MED	HI	HI	HI HI	HI HI	11240
							10930
							10140

RAW MATL. MIX
3 CHIPS / SHAVINGS
FLOW RATE 27,988 LBS/HR

TOTAL 124960
AVG 24992

HEATER OPERATION

TIME					
Return Oil Temperature	448	448	448	448	448
Feed Oil Temperature	490	490	489	490	491
Heater Inlet Temperature	908	909	910	911	906
Heater Disch. Temperature	636	637	635	637	639
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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TEST TYPE: PARTICULATE, CPM, CO_2, O_2

TEST LOCATION: PRESS LINE 2 VENT #3
TEST #3.

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON

Plant Description: MDF

Date: 3-18-92

PROCESS INFORMATION

TIME	4:01	4:16	4:31	4:45	5:01	THAYER SCALES
Forming Line Speed	22.5	22.5	22.5	22.5	22.5	12580
Board Thickness	1/2"	1/2"	1/2"	1/2"	1/2"	11220
Press ~~Cycle Time~~ ZONE 1	219°	219°	219°	219°	219°	12260
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	214°	214°	214°	214°	214°	10830
~~Press Circ. Pump #1 Motor Load~~ 3	216°	216°	216°	216°	216°	12600
GPM ~~Press Circ. Pump #2 Motor Load~~ RESIN	10.2	10.2	10.2	10.4	10.4	9820
GPM ~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	12210
RAW MAT'L. MIX FIBER BIN LEVEL	HI HI	HI HI	HI HI	HI	HI	10780
3 CHIPS / SHAVINGS						12700
						10980

TOTAL 115980
AVG 23196

FLOW RATE 27,589 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	447	448	448	448	448
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	903	905	904	905	906
Heater Disch. Temperature COIL	635	635	636	637	637
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE FORM, CO, THC
" LOCATION PRESS VENT #9
" NO. 1

LINE 1

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL. **Plant Description:** M.D.F.

Date: 3/17/92

MC, 29.2
CORE MC2 10.4, 10.2
FACE MC2 10.9, 10.8

PROCESS INFORMATION

	TIME	8:55	9:10	9:25	9:40	9:55
FPM	Forming Line Speed	53.0	53.0	53.0	53.0	53.0
IN	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN	Press Cycle Time	5.8	5.8	5.8	5.8	5.8
°F	Control ~~[illegible]~~ Temp. ~~Setpoint~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.3 | 7.8	6.4 | 7.8	6.4 | 7.8	6.4 | 7.8	6.3 | 7.8
WAX	Press Circ. Pump #2 Motor Load CORE	1200	1200	1200	1200	1200
MLPM	Press Circ. Pump #3 Motor Load FACE	1400	1400	1400	1400	1400
	DRY BIN LEVEL (WINDOWS) CORE	1.5	1.5	1.0	1.0	1.0
	DRY BIN LEVEL (WINDOWS) FACE	1.5	1.5	2.0	2.0	2.0

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 46,663 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoiht					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE FORM., CO, THC
" LOCATION PRESS VENT #7
" NO. 2

LINE 1

Owner: L.P. Test Personnel: R.G.T. & D.B

Location: CLAYTON, AL. Plant Description: M.D.F.

Date: 3/17/92

MC, 30.0
CORE MC2 9.8, 9.6
FACE MC2 10.2, 10.2

PROCESS INFORMATION

	TIME	10:27	10:42	10:57	11:12	11:27
FPM	Forming Line Speed	50.0	50.0	50.0	50.0	50.0
IN	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN	Press Cycle Time	5.8	5.8	5.8	5.8	5.8
OF	Control ~~Oil~~ Temp. ~~Setpoint~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.9/7.7	6.9/7.7	6.9/7.7	6.5/7.7	6.5/7.7
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MLPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1900	1900	1900	1900	1900
	DRY BIN LEVELS (WINDOWS) CORE	2	2	1	1	1
	DRY BIN LEVELS (WINDOWS) FACE	2	2	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/9 SAW TRIM

HEATER OPERATION FLOW RATE 49,883 #/HR

TIME					
Return Oil Temperature					
~~Feed Oil Temperature~~					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE FORM, CO, THC
" LOCATION PRESS VENT #9
" No. 3
LINE 1

Owner: L.P. Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL Plant Description: M.D.F.

Date: 3/17/92

MC, 9.8
CORE MC, 9.6, 9.8
FACE MC, 10.9, 10.0

PROCESS INFORMATION

	TIME	11:52	12:13	12:22	12:43	12:52
FPM	Forming Line Speed	50.00	50.0	50.0	50.0	50.0
IN.	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN.	Press Cycle Time	5.8	5.8	5.8	5.8	5.8
°F	Control ~~Oil~~ Temp. ~~Setpoint~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.5|7.7	6.4|7.7	6.6|7.7	6.8|7.7	6.7|7.7
MAX.	Press Circ. Pump #2 Motor Load CORE	1200	1200	1200	1200	1200
MLPM	Press Circ. Pump #3 Motor Load FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	1	1	1	1	1
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAWTRIM

HEATER OPERATION FLOW RATE 42,820 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoiht					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood-Burner Shell Temp.					
Wood Fuel Counter					

P.O. Box 330 · Muscotah, Kansas 66757, U.S.A. / Telephone: 316-335-2673 / Telex: 43-6402 / Telefax: 316-335-2678

(METHOD 5) TEST TYPE PARTICULATE, O_2, CO_2, CFM
" LOCATION PRESS VENT #9
" NO. 1

mEC COMPANY

LINE 1

Owner: L. P. Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL. Plant Description: M.D.F.

Date: 3/17/92

mC_1 36.0
CORE mC_2 10.2, 9.8
FACE mC_2 10.0, 9.9

PROCESS INFORMATION

	TIME	2:56	3:11	3:26	3:41	3:56
FPM	Forming Line Speed	44.0	44.0	44.0	44.0	44.0
IN.	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control ~~RTD~~ Temp. ~~Setpoint~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.6 | 7.7	6.7 | 7.8	6.6 | 7.2	6.7 | 7.8	6.6 | 7.8
MAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ALPM	Press Circ. Pump #3 Motor Load FACE	1400	1400	1400	1400	1400
	DRYER LEVELS (WINDOWS) CORE	1	1	1	1	1
	DRYER LEVELS (WINDOWS) FACE	1	1	1	1	2

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 37,947 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner-Shell Temp.					
Wood Fuel Counter					

P.O. Box 330 / Hutchinson, Kansas 67767, U.S.A. / Telephone: 316-325-2672 / Telex: 40-6402 / Telefax: 316-325-2678

(METHOD 5) TEST TYPE PARTICULATE, O_2, CO_2, CFM
" LOCATION PRESS VENT # 2
" NO. 2

mEC COMPANY

LINE 1

Owner: L.P **Test Personnel:** R.G.T. & D.B

Location: CLAYTON, AL **Plant Description:** M.D.F

Date: 3/17/92

MC_1 30
CORE MC_2 10.2, 9.8
FACE MC_2 10.0, 10.2

PROCESS INFORMATION

	TIME	4:36	4:51	5:06	5:21	5:36
FPM	Forming Line Speed	49.0	49.0	49.0	49.0	49.0
IN.	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control ~~Set~~ Temp. ~~Setpoint~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.6 | 7.7	6.7 | 7.7	6.7 | 7.8	6.7 | 7.8	6.7 | 7.8
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MLPM	Press Circ. Pump #3 Motor Load FACE	1400	1400	1400	1400	1400
	DRY BIN LEVEL (WINDOWS) CORE	2	2	2	1	1
	DRY BIN LEVEL (WINDOWS) FACE	1.25	1	1	1.25	1.25

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION

FLOW RATE 42,281 #/HR

TIME					
~~Return Oil~~ Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE PART, O_2, CO_2, CPM
" LOCATION PRESS VENT #9
" NO. 3

LINE 1

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL **Plant Description:** M.D.F.

Date: 3/17/92

MC, 27
CORE MC_2 10.2, 10.6
FACE MC_2 10.8, 11.2

PROCESS INFORMATION

	TIME	6:06	6:21	6:36	6:51	7:06
FPM	Forming Line Speed	49.0	49.0	49.0	49.0	49.0
IN.	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN.	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control Temp. (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.7 | 7.8	6.7 | 7.8	6.7 | 7.7	6.7 | 7.8	6.7 | 7.7
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
ALFM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1900	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	1	1	1	1	1
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1.25	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 40,605 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE FORM, CO. THC
" LOCATION PRESSVENT #10
" NO. 1

LINE 1

Owner: L.P. Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL. Plant Description: M.D.F.

Date: 3/17/92

MC1 36.0
CORE MC2 9.8 9.8
FACE MC2 9.4 10.0

PROCESS INFORMATION

	TIME	3:23	3:38	3:53	4:08	4:22
FPM	Forming Line Speed	44.0	44.0	44.0	44.0	44.0
IN.	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN.	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control ~~Oil~~ Temp. ~~Setpoint~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.6 | 7.8	6.7 | 7.8	6.6 | 7.8	6.6 | 7.7	6.7 | 7.8
WAX	~~Press. Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MLPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	1	1	1	1	1
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	2	2

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 38,656 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

LINE 1

TEST TYPE FORM, CO, THC
" LOCATION PRESS VENT #10
" NO. 2

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL **Plant Description:** MDF

Date: 3/17/92

MC, 30
CORE MC2 10.2, 9.8
FACE MC2 10.0, 10.2

PROCESS INFORMATION

	TIME	4:49	5:09	5:19	5:34	5:49
FPM	Forming Line Speed	49.0	49.0	49.0	49.0	49.0
IN	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control ~~Set~~ Temp. ~~Surface~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.6 | 7.7	6.8 | 7.8	6.8 | 7.8	6.7 | 7.8	6.7 | 7.7
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MLFM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	2	2	1	1	1
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1.25	1.25	1.

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 41,925 #/HR

TIME					
~~Return Oil Temperature~~					
~~Feed Oil Temperature~~					
~~Heater Inlet Temperature~~					
~~Heater Disch. Temperature~~					
~~Control Temperature Setpoint~~					
~~Oil Differential Pressure~~					
~~Heater Differential Press. Setpoint~~					
~~Tee Section Static Pressure~~					
~~Main Circulating Pump Motor Load~~					
~~Aux. Circulating Pump Motor Load~~					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
~~Gas/Oil Heat Controller Output~~					
~~Flowing Gas/Oil Pressure After Reg.~~					
~~Wood Heat Controller Output~~					
~~Wood Fuel Delivery, Volts~~					
~~Wood Air Signal, mA~~					
~~Wood Burner Shell Temp.~~					
~~Wood Fuel Counter~~					

mEC COMPANY

LINE 1

TEST TYPE FORM CO. THC
" LOCATION PRESS VENT #10
" No. 3

Owner: L.P Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL. Plant Description: M.D.F.

Date: 3/17/92

MC1 27
CORE MC2 10.2, 10.6
FACE MC2 10.8, 11.2

PROCESS INFORMATION

	TIME	6:12	6:27	6:42	6:57	7:12
FPM	Forming Line Speed	49.0	49.0	49.0	49.0	49.0
"	Board Thickness	11/16	11/16	11/16	11/16	11/16
MIN.	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
°F	Control ~~Oil~~ Temp. ~~Setpoint~~ (Press)	300	300	300	300	300
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.8 | 7.8	6.7 | 7.8	6.7 | 7.7	6.8 | 7.8	6.7 | 7.8
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MCFM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	1	1	1	1	1
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1.25	1	1

RAW MATERIAL MIX
~~3~~ SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 40,605 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

Neodesha, Kansas U.S.A.

By DB/RGT Date 3-17-92

Customer LP

Job No. M.D.F. Location CLAYTON, AL Sht. No. ____ of ____

BOILER STACK # 1 TEST # 3

TIME	10:50	11:05	11:20	11:35	11:50	
STEAM PRESSURE	257	257	257	257	257	PSIG
STEAM PRODUCED	19.0	20.0	20.0	19.5	19.0	LBS/HR x 1000
AIR HEATER TEMP.	430°	440°	425°	435°	440°	
BURNER FUEL FEED RPMS	800	850	800	750	800	

PARTICULATE ONLY

BOILER STACK # 2 TEST # 3

TIME	8:50	9:05	9:20	9:35	9:50	
STEAM PRESSURE	257	257	257	257	257	PSIG
STEAM PRODUCED	20.0	20.0	19.0	20.0	20.0	LBS/HR x 1000
AIR HEATER TEMP.	465°	470°	475°	475°	475°	
BURNER FUEL FEED RPM	875	900	900	950	850	

mEC COMPANY

Neodesha, Kansas U.S.A.

By DB/RGT Date 3-17-92

Customer LP

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. ____ of ____

BOILER STACK # 1 TEST # 2

TIME	8:35	8:50	9:05	9:20	9:35	
STEAM PRESSURE	257	257	257	257	257	PSIG
STEAM PRODUCED	20.0	20.0	19.5	20.0	19.5	LBS/HR x 1000
AIR HEATER TEMP.	420°	425°	425°	425°	425°	
BURNER FUEL FEED RPMS	850	825	850	825	850	

PARTICULATE ONLY

BOILER STACK # TEST #

TIME					
STEAM PRESSURE					
STEAM PRODUCED					
AIR HEATER TEMP.					
BURNER FUEL FEED RPM					

mEC COMPANY

PRESS LINE #2 VENT #4 TEST #1
CPM, PARTICULATE, CO_2, O_2

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL.

Plant Description: MDF

Date: 3-17-92

PROCESS INFORMATION

TIME	1:40	1:55	2:10	2:25	2:40	THAYER SCALES
Forming Line Speed	25.0	25.0	25.0	25.0	25.0	13160
Board Thickness	7/16"	7/16"	7/16"	7/16"	7/16"	10120
Press ~~Cycle Time~~ 1	220°	220°	220°	220°	220°	13520
~~Control~~ Oil Temp. ~~Setpoint~~ (Press) 2	215°	215°	215°	215°	215°	9980
~~Press Circ. Pump #1 Motor Load~~ 3	216°	216°	216°	216°	216°	12120
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.0	10.0	10.2	10.0	10.0	9020
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	12080
DRY BIN LEVEL	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	11370
						11150
						9020
					TOTAL	111540
					AVG.	22308

RAW MAT'L. MIX
3 CHIPS / SHAVING

FLOW RATE 28,055 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	448	448	448	448	448
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	907	911	907	905	904
Heater Disch. Temperature COIL	634	636	635	633	634
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

PRESS LINE #2 VENT #4 TEST #2
CPM, PARTICULATE, CO_2, O_2

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-17-92

PROCESS INFORMATION

TIME	3:10	3:25	3:40	3:55	4:10	THAYER SCALES
Forming Line Speed	25.0	25.0	25.0	25.0	25.0	10950
Board Thickness	7/16"	7/16"	7/16"	7/16"	7/16"	14760
Press ~~Cycle Time~~ 1	220°	220°	220°	220°	220°	9820
~~Control~~ Oil Temp. ~~Setpoint~~ (Press) 2	215°	215°	215°	215°	215°	11860
~~Press Circ. Pump #1 Motor Load~~ 3	216°	216°	216°	216°	216°	9440
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.0	10.2	10.0	10.2	10.0	12460
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	10930
DRY BIN LEVEL	HI-HI	HI-HI	HI	HI	HI	12490
						10550
					TOTAL	116670
					AVG.	23334

RAW MAT'L. MIX
3 CHIPS / SHAVINGS
FLOW RATE 28,176 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	448	448	448	448	448
Feed Oil Temperature OUTLET	489	490	490	490	490
Heater Inlet Temperature HOT GAS	901	906	903	907	904
Heater Disch. Temperature COIL	632	634	633	633	634
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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PRESS LINE #2 VENT #4 TEST #3
CPM, PARTICULATE, CO_2, O_2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-17-92

PROCESS INFORMATION

TIME	4:55	5:10	5:25	5:40	5:55	THAYER SCALES
Forming Line Speed	25.3	25.3	25.3	25.3	25.3	15650
Board Thickness	7/16	7/16	7/16	7/16	7/16	9280
Press ~~Cycle Time~~ 1	220°	220°	220°	220°	220°	13240
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	215°	215°	215°	215°	215°	9450
~~Press Circ. Pump #1 Motor Load~~ 3	216°	216°	216°	216°	216°	13320
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.0	10.2	10.0	10.0	10.0	10190
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	13690
DRY BIN LEVEL	HI	HI	HI	MED	MED	9280
						13900
						8820
					TOTAL	116320
					AVG	23264

RAW MAT'L. MIX
3 CHIPS / SHAVINGS

FLOW RATE 28,112 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature	448	448	448	448	448
Feed Oil Temperature	490	490	490	490	490
Heater Inlet Temperature	905	913	907	906	907
Heater Disch. Temperature	634	634	634	633	636
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

P.O. Box 330 / Hoodesana, Kansas 66757, U.S.A. / Telephone: 316-325-2673 / Telex: 43-6402 / Telefax: 316-325-2678

mEC COMPANY

TEST TYPE FORM, CO, THC
" LOCATION PRESS VENT #7
" NO. 1

LINE 1

Owner: L.P. Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL. Plant Description: M.D.F.

Date: 3/16/92

19.0 MC1
11.6 MC2 CORE 12.9
10.2 MC2 FACE 12.3

PROCESS INFORMATION

	TIME		8:00	8:15	8:30	8:45	9:00
FPM	Forming Line Speed		26.0	26.0	26.0	26.0	26.0
	Board Thickness		1 3/16"	1 3/16"	1 3/16"	1 3/16"	1 3/16"
	Press Cycle Time		10.9 min	10.9	10.9	10.9	10.9
	Control [redacted] Temp. ~~Setpoint~~ (Press)		310°F	310°F	310°F	310°F	310°F
GPM	~~Press Circ. Pump #1 Motor Load~~	RESIN	6.7 6.9	6.6 7.0	6.6 7.0	6.7 6.9	6.7 6.9
MAX	~~Press Circ. Pump #2 Motor Load~~	CORE	1600	1600	1600	1600	1600
PM	~~Press Circ. Pump #3 Motor Load~~	FACE	1600	1600	1600	1600	1600
	DRY BIN LEVEL (WINDOWS)	CORE	3	3	3	3	3
		FACE	3.5	3.5	3.5	3.5	3.5

RAW MATERIAL MIX
1 SHAVINGS
0 CHIPS
0 SAWTRIM

HEATER OPERATION FLOW RATE 35,373 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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MEC COMPANY

LINE 1

TEST TYPE FORM, CO, THC
" LOCATION PRESS VENT #7
" NO. 2

Owner: L.P.

Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL.

Plant Description: M.D.F

Date: 3/16/92

19.6 MC_1
9.6 MC_2 CORE 9.8 / 10.0
10.0 MC_2 FACE

PROCESS INFORMATION

	TIME	9:32	9:47	10:02	10:17	10:32
FPM	Forming Line Speed	26.0	26.0	26.0	26.0	26.0
	Board Thickness	1 3/16"	1 3/16"	1 3/16"	1 3/16"	1 3/16"
MIN	Press Cycle Time	10.9	10.9	10.9	10.9	10.9
	Control [redacted] Temp. [redacted] (Press)	310°F	310°F	310°F	310°F	310°F
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.8 | 6.8	6.9 | 6.8	6.8 | 6.8	6.8 | 6.8	6.9 | 6.8
DAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1600	1600	1600	1600	1600
ILPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1600	1600	1600	1600	1600

RAW MATERIAL MIX
1 SHAVINGS
0 CHIPS
0 SAW TRIM

DRY BIN LEVELS (WINDOWS)						
	CORE	3	3	3	3	3.5
	FACE	3	3	2	2	2

HEATER OPERATION FLOW RATE 35,775 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
~~Gas/Oil~~ Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE FORM, CO, THC
" LOCATION PRESS VENT #7
" NO. 3

LINE 1

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL **Plant Description:** M.D.F.

Date: 3/16/92

19.4 MC1
9.8 MC2 CORE 10.0
16.0 MC2 FACE 9.8

PROCESS INFORMATION

	TIME	11:00	11:15	11:30	11:45	12:00
FPM	Forming Line Speed	26.0	26.0	26.0	26.0	26.0
	Board Thickness	1 3/16"	1 3/16"	1 3/16"	1 3/16"	1 3/16"
	Press Cycle Time	10.9	10.9	10.9	10.9	10.9
°F	Control [redacted] Temp. [redacted] (Press)	310	310	310	310	310
GPM	Press Circ. Pump #1 Motor Load RESIN	6.5 | 6.9	6.5 | 7.0	6.6 | 7.0	6.6 | 7.0	6.5 | 6.9
WAX	Press Circ. Pump #2 Motor Load CORE	1600	1600	1600	1600	1600
ILPM	Press Circ. Pump #3 Motor Load FACE	1600	1600	1600	1600	1600
	DRY BIN LEVELS (WINDOWS) CORE	4	4	4	4	4
	DRY BIN LEVELS (WINDOWS) FACE	2	2	2	2	2

RAW MATERIAL MIX
1 SHAVINGS
0 CHIPS
0 SAWTRIM

HEATER OPERATION FLOW RATE 36,408 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoiht					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

LINE 1

TEST TYPE FORM., CO, THC
" LOCATION PRESS VENT #8
" NO. 1

Owner: L.P.

Test Personnel: RGT & D.B.

Location: CLAYTON, AL.

Plant Description: M.D.F.

Date: 3/16/92

MC 1 13
CORE MC2 9.8, 10.6
FACE MC2 8.0, 9.6

PROCESS INFORMATION

	TIME	2:57	3:12	3:27	3:42	3:57
PM	Forming Line Speed	25.0	25.0	25.0	25.0	25.0
	Board Thickness	1 5/32"	1 5/32"	1 5/32"	1 5/32"	1 5/32"
MIN.	Press Cycle Time	10.5	10.5	10.5	10.5	10.5
°F	Control ~~Out~~ Temp. ~~[illegible]~~ (Press)	310	310	310	310	310
°m	Press Circ. Pump #1 Motor Load RESIN	6.6 | 6.8	6.5 | 6.8	6.5 | 6.8	6.5 | 6.8	6.5 | 6.8
MAX	Press Circ. Pump #2 Motor Load CORE	1600	1600	1600	1600	1600
PM	Press Circ. Pump #3 Motor Load FACE	1600	1600	1600	1600	1600
	DRY BIN LEVELS (WINDOWS) CORE	3	3	3	3	3
	DRY BIN LEVELS (WINDOWS) FACE	3	4	4	4	4

RAW MATERIAL MIX
1 SHAVINGS
0 CHIPS
0 SAW TRIM

HEATER OPERATION FLOW RATE 34,599 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoiht					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE Form, CO, THC
" LOCATION Press Vent #8
" No. 2

LINE 1

Owner: L.P. Test Personnel: RGT & D.B.

Location: Clayton, AL. Plant Description: M.D.F.

Date: 3/16/92

Mc, 15.0
CORE MC2 9.8, 9.8
FACE MC2 7.6, 9.8

PROCESS INFORMATION

	TIME	4:10	4:55	5:10	5:25	5:40
FPM	Forming Line Speed	25.0	25.00	25.0	25.0	25.0
	Board Thickness	1 5/32"	1 5/32"	1 5/32"	1 5/32"	1 5/32"
MIN	Press Cycle Time	10.5	10.5	10.5	10.5	10.5
°F	Control ~~Oil~~ Temp. ~~Setpoint~~ (Press)	310	310	310	310	310
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.5/6.9	6.4/6.9	6.5/6.9	6.4/6.8	6.4/6.8
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1600	1600	1600	1600	1600
LPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1600	1600	1600	1600	1600
	DRY BIN LEVELS (WINDOWS) CORE	4	4	4	4	4
	DRY BIN LEVELS (WINDOWS) FACE	2	2	2	3	3

RAW MATERIAL MIX
1 SHAVINGS
0 CHIPS
0 SAW TRIM

HEATER OPERATION FLOW RATE 36,363 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
~~Heater Inlet Temperature~~					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil ~~Pressure After Reg.~~					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE FORM, CO, THC
" LOCATION PRESS VENT #8
" NO. 3

LINE 1

Owner: L.P.

Test Personnel: R.G.T. & D.B.

Location: CLAYTON, AL.

Plant Description: M.D.F

Date: 3/16/92

MC, 16.0

CORE MC2 10.0, 9.8

FACE MC2 10.4, 10.8

PROCESS INFORMATION

	TIME	6:10	6:25	6:40	6:55	7:10
FPM	Forming Line Speed	26.0	26.0	26.0	26.0	26.0
	Board Thickness	1 5/32"	1 5/32"	1 5/32"	1 5/32"	1 5/32"
MIN.	Press Cycle Time	10.20	10.2	10.2	10.2	10.2
°F	Control ~~Set~~ Temp. ~~Setpoint~~ (Press)	310	310	310	310	310
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	6.1 | 7.1	6.9 | 7.1	6.9 | 7.1	6.5 | 7.0	6.9 | 7.1
MAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1600	1600	1600	1600	1600
LPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1600	1600	1600	1600	1600
DRY BIN LEVEL (WINDOWS)	CORE	1	2	1	1	1
	FACE	3	3	3	3	3

RAW MATERIAL MIX
1 SHAVINGS
0 CHIPS
0 SAW TRIM

HEATER OPERATION FLOW RATE 35,317 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoiht					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

MEC COMPANY
Neodesha, Kansas U.S.A.

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST Date 3-16-92
LP Customer

DRYER TEST DATA

DRYER NO. 1 STACK #4

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST #1

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	MAGNA HELIC % OUT / FUEL RATE Wood Burner PD	mA	~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
9:03	40.0	201	116	5.5	57.5/10.0	124	35.6		135°			WOOD FUEL COUNTER - ~~RECHECKING THE DAY AFTE~~ 655491
9:25	40.0	206	118	5.5	57.4/10.0	121		11.2	136°			TEST STOP 9:15 TO 9:25 655611
9:40	40.0	204	118	5.5	59.7/10.0	120			138°			655704
9:55	40.0	203	117	5.5	60.9/10.5	129			140°			655789
10:10	40.0	201	116	5.5	58.3/9.5	117		10.4	140°			655867

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO

TEST LOCATION: DRYER # 1 - STACK # 4

TEST # 1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-16-92

SAT. 2 OF 2

PROCESS INFORMATION

TIME						THAYER SCALES
Forming Line Speed	38.0	38.0	38.0	38.0	38.0	13160
Board Thickness	1/4"	1/4"	1/4"	1/4"	1/4"	10760
Press Cycle Time	219°	219°	219°	219°	219°	15890
Control Oil Temp. Setpoint (Press)	214°	214°	214°	214°	214°	11080
Press Circ. Pump #1 Motor Load	210°	210°	210°	210°	210°	15120
Press Circ. Pump #2 Motor Load RESIN	10.0	10.0	9.8	10.0	10.0	12090
Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	14720
DRY BIN LEVEL	HI	HI	HI	HI	HI	12330
						15310
						11480
TOTAL						131940
AVG.						26388

RAW MAT'L. MIX
3 CHIPS 1 SHAVING

FLOW RATE 39,016 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	444	444	444	444	444
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	917	918	918	917	917
Heater Disch. Temperature COIL	667	666	667	669	668
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "H")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output	63.2	64.2	65.1	64.9	64.8
Wood Fuel Delivery, Volts	152	157	149	155	157
Wood Air Signal, mA	13.5	13.5	13.0	13.0	13.0
Wood Burner Shell Temp.	142°	141°	144°	145°	147°
Wood Fuel Counter	205942	206081	206221	206325	206437
PD MAGNAHELIC	8.0	8.0	8.0	8.0	8.0

DRYER TEST DATA

DRYER NO. 1 STACK #4

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST #2

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	MAGNA HELIC Wood Burner PD	mA	~~%OUT~~ / FUEL RATE	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
11:55	40.0	190	115	5.0	62.4/9.0	111			146°			WOOD FUEL COUNTER - ~~RECEIVING HOPPER~~ 656164
11:10	40.0	186	113	5.0	61.0/9.0	110		11.0	148°			656203
11:25	40.0	182	111	5.0	61.3/9.0	113			150°			656278
11:40	40.0	184	112	5.0	61.5/9.0	114			154°			656348
11:55	40.0	185	112	5.0	61.6/9.0	112	33.2	10.8	154°			656422

MEC COMPANY
Neodesha, Kansas U.S.A.

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST Date 3-16-92

Customer LP

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO

TEST LOCATION: DRYER # 1 - STACK #4

TEST # 2

mtc COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-14-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME						THAYER SCALES
Forming Line Speed	38.0	38.0	38.0	38.0	38.0	14950
Board Thickness	1/4"	1/4"	1/4"	1/4"	1/4"	11750
Press Cycle Time 1	219°	220°	220°	220°	219°	14040
Control Oil Temp. Setpoint (Press) 2	215°	215°	215°	215°	214°	12300
~~Press Circ. Pump #1 Motor Load~~ 3	210°	211°	211°	211°	210°	13820
~~Press Circ. Pump #2 Motor Load~~ RESIN	9.8	10.0	10.0	9.8	10.0	13060
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	14720
RAW MAT'L. MIX / DRY BIN LEVEL	HI	HI	HI	HI-HI	HI-HI	10870
3 CHIPS / SHAVINGS						14630
						12550
TOTAL						149763
AVG.						29953

FLOW RATE 28,791 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	444	444	444	443	443
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	916	916	914	913	915
Heater Disch. Temperature COIL	667	668	668	666	666
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output	68.3	69.8	70.7	76.7	76.9
Wood Fuel Delivery, Volts	138	146	143	166	152
Wood Air Signal, mA	12.5	12.8	13.0	13.5	13.0
Wood Burner Shell Temp.	153°	155°	154°	164°	161°
Wood Fuel Counter	206778	206879	206978	207086	207197
PD MAGNAHELIC	7.5	7.5	7.5	7.5	8.0

mEC COMPANY

Neodesha, Kansas U.S.A.

By DB/RGT Date 3-16-92

Customer LP

~~Job No.~~ MDF Location CLAYTON, AL. Sht. No. ____ of ____

BOILER STACK # 1 TEST # 1

TIME	3:20	3:35	3:50	6:05	6:20	
STEAM PRESSURE	255	255	255	255	255	PSIG
STEAM PRODUCED	20.0	19.0	19.0	20.0	19.5	LBS/HR X 1000
AIR HEATER TEMP.	440°	445°	425°	425°	425°	
BURNER FUEL FEED RPMS	850°	850°	825°	800°	825°	

PARTICULATE ONLY

BOILER STACK # 2 TEST # 1

TIME	5:20	5:35	5:50	6:05	6:20	
STEAM PRESSURE	255	255	255	255	255	PSIG
STEAM PRODUCED	19.0	18.5	19.0	18.5	19.0	LBS/HR. X 1000
AIR HEATER TEMP.	445°	450°	450°	450°	460°	
BURNER FUEL FEED RPM	975	975	950	950	850°	

mtc COMPANY

Neodesha, Kansas U.S.A.

By DB/RGT Date 3-16-92

Customer LP

~~Job No.~~ MDF Location CLAYTON, AL. Sht. No. ____ of ____

BOILER STACK # TEST #

TIME						
STEAM PRESSURE						PSIG
STEAM PRODUCED						LBS/HR
AIR HEATER TEMP.						
BURNER FUEL FEED RPMS						

PARTICULATE ONLY

BOILER STACK # 2 TEST # 2

TIME	5:20	5:35	5:50	6:05	6:20	
STEAM PRESSURE	255	255	255	255	255	PSIG
STEAM PRODUCED	20.5	20.0	20.5	21.0	21.0	LBS/HR X1000
AIR HEATER TEMP.	475°	475°	475°	475°	475°	
BURNER FUEL FEED RPM	800	800	850	850	875	

DAVE PRATER
JERRY PAYFIELD

GARY 228

mEC COMPANY

LINE 1

TEST TYPE FORM., CO, THC
" LOCATION PRESS VENT #6
" No. 1

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL. **Plant Description:** M.D.F.

Date: 3/14/92

28% MC1
9.4 MC2 FACE 9.6
9.0 MC2 CORE 9.4

PROCESS INFORMATION

	TIME	11:55	12:10	12:25	12:40	12:55
FPM	Forming Line Speed	52.0	52.0	52.0	52.0	52.0
	Board Thickness	5/8"	5/8"	5/8"	5/8"	5/8"
	Press Cycle Time	6.0 MIN.	6.0 MIN.	6.0 MIN.	6.0 MIN.	6.0 MIN.
	Control ~~MC~~ Temp. ~~Supplied~~ (Press)	300°F	300°F	300°F	300°F	300°F
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	5.8 / 8.0	5.8 / 8.0	5.8 / 7.9	5.8 / 8.0	5.9 / 8.0
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MLPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1900	1900	1900	1900	1900
	DRYBINS LEVELS (WINDOWS) CORE	2	2	2	2	2
	DRYBINS LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION

FLOW RATE 12,839 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE FORM., CO, THC
" LOCATION PRESS VENT #6
" NO. 2

Owner: L.P

Test Personnel: RGT & D.B.

Location: CLAYTON, AL.

Plant Description: MDF

Date: 3/14/92

11 MC1
9.8 MC2 CORE 9.6
10.4 MC2 FACE 9.6

PROCESS INFORMATION

	TIME	3:15	3:30	3:45	4:00	4:15
FPM	Forming Line Speed	48.0	48.0	48.0	48.0	48.0
	Board Thickness	5/8"	5/8"	5/8"	5/8"	5/8"
	Press Cycle Time	6.0	6.0	6.0	6.0	6.0
	Control ~~Set~~ Temp. ~~Setpoint~~ (Press)	300°F	300°F	300°F	300°F	300°F
GPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	5.5 | 8.0	5.5 | 8.0	5.6 | 8.0	5.5 | 80	5.1 | 7.9
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MLPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRYBIN LEVELS (WINDOWS) CORE	1	1	1	1	1
	DRYBIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAWTRIM

HEATER OPERATION

FLOW RATE 37,196 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE Form, CO, THC
" LOCATION PRESS VENT #6.
" NO. 3

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL. **Plant Description:** M.D.F.

Date: 3/14/92

24% MC_1
9.8 MC_2 CORE 9.8
9.8 MC_2 FACE 10.2

PROCESS INFORMATION

	TIME	1:46	5:01	5:16	5:31	5:46
FPM	Forming Line Speed	48.0	48.0	48.0	48.0	48.0
	Board Thickness	5/8"	5/8"	5/8"	5/8"	5/8"
	Press Cycle Time	6.0 MIN	6.0 MIN	6.0 MIN	6.0 MIN	6.0 MIN
	Control ~~Zone~~ Temp. ~~Setpoint~~ (Press)	300°F	300°F	300°F	300°F	300°F
CPM	~~Press Circ. Pump #1 Motor Load~~ RESIN	5.6 | 8.0	5.6 | 8.0	5.6 | 8.0	5.5 | 8.1	5.6 | 8.0
WAX	~~Press Circ. Pump #2 Motor Load~~ CORE	1200	1200	1200	1200	1200
MLPM	~~Press Circ. Pump #3 Motor Load~~ FACE	1400	1400	1400	1400	1400
	DRY BIN LEVELS (WINDOWS) CORE	1	1	1	1/2	1
	DRY BIN LEVELS (WINDOWS) FACE	1	1	1	1	1

RAW MATERIAL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

HEATER OPERATION FLOW RATE 41,232 #/HR

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

MEC COMPANY
Neoulesha, Kansas U.S.A.

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST LP Date 3-14-92
Customer

DRYER TEST DATA

DRYER NO. 2 STACK #2

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2
TEST #2

Tamb, °F: _____
PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	MAGNA HELIC % OUT / FUEL RATE Wood Burner PD	mA	~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
8:55	45.0	189	109	7.0	69.1/12.0	138			154°			WOOD FUEL COUNTER - 185243 ~~RECEIVING HOT OIL GAS~~
9:10	45.0	183	110	7.0	72.7/12.0	142		10.4	158°			185354
9:25	45.0	187	109	7.0	74.5/12.5	153			158°			185470
9:40	44.0	186	109	7.0	72.1/12.5	141	20.8		160°			185579
9:55	44.0	186	109	7.0	78.6/15.0	147		10.0	160°			185677

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST LOCATION: DRYER #2 - STACK #2

TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-14-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	8:55	9:10	9:25	9:40	9:55	THAYER SCALES
Forming Line Speed	28.3	28.3	28.3	28.3	28.3	10700
Board Thickness	3/8"	3/8"	3/8"	3/8"	3/8"	10760
Press Cycle Time 1	220°	220°F	220°	220°	220°	12220
Control Oil Temp. Setpoint (Press) 2	216°	216°F	216°	216°	216°	11950
Press Circ. Pump #1 Motor Load 3	214°	214°F	214°	214°	214°	11240
Press Circ. Pump #2 Motor Load RESIN	9.8	9.8	9.8	9.8	10.0	9820
Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	12880
RAW MATL. MIX DRY BIN LEVEL	HI-HI	HI-HI	HI-HI	HI-HI	HI-HI	11210
						13240
						11330

3 CHIPS / SHAVINGS

FLOW RATE 27,755 LBS/HR

TOTAL 115,350

AVG. 23,0

HEATER OPERATION

TIME					
Return Oil Temperature INLET	445	445	446	446	445
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	904	900	898	900	898
Heater Disch. Temperature COIL	654	653	652	653	651
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output %	62.5	63.3	62.7	63.9	63.2
Wood Fuel Delivery, Volts	107	103	101	105	107
Wood Air Signal, mA	9.0	9.0	8.5	8.5	9.0
Wood Burner Shell Temp.	150°	155°	156°	157°	158°
Wood Fuel Counter	640801	640871	640962	641027	641103
PD MAGNAHELIC	5.0	5.0	5.0	5.0	5.0

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DRYER TEST DATA

DRYER NO. 2 STACK #2

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST # 3

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner (MAGNA HELIC %OUT / FUEL RATE) PD	mA	~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
12:25	44.0	186	115	7.5	67.8/12.0	137		11.0	161°			WOOD FUEL COUNTER - 186694 ~~BEGINNING NAT GAS~~
12:40	44.0	202	113	7.5	67.5/12.5	141			161°			186856
12:55	44.0	199	113	7.5	68.0/12.5	138		10.8	164°			186967
1:10	44.0	199	113	7.0	64.4/11.0	127	29.0		165°			187025
1:25	44.0	199	112	7.0	72.9/12.5	149			164°			187121

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT LP Date 3-14-92

Customer

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST LOCATION: DRYER #2 - STACK #2

TEST # 3

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-14-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	12:25	12:40	12:55	1:10	1:25	THAYER SCALES
Forming Line Speed	29.7	29.7	29.7	29.7	29.7	12570
Board Thickness	3/8"	3/8"	3/8"	3/8"	3/8"	11060
Press Cycle Time 1	219°	219°	220°	220°	220°	15090
Control Oil Temp. Setpoint (Press) 2	215°	215°	215°	215°	215°	13660
Press Circ. Pump #1 Motor Load 3	215°	215°	214°	214°	214°	13230
Press Circ. Pump #2 Motor Load RESIN	10.2	10.2	10.2	10.2	10.2	11440
Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	13600
DRY BIN LEVEL	HI	HI	HI-HI	HI-HI	HI-HI	10820
						11260
						10140

RAW MAT'L. MIX
3 CHIPS 1 SHAVING

FLOW RATE 29,573 LBS/HR

TOTAL 129,890
AVG 24,9

HEATER OPERATION

TIME					
Return Oil Temperature INLET	448	448	447	447	447
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	884	886	888	898	885
Heater Disch. Temperature COIL	634	641	644	643	645
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output %	62.2	62.9	61.5	63.2	62.2
Wood Fuel Delivery, Volts	114	110	112	120	103
Wood Air Signal, mA	9.0	9.5	9.0	9.0	9.0
Wood Burner Shell Temp.	162°	160°	160°	161°	164°
Wood Fuel Counter	641799	641898	641982	642055	642129
PD MAGNAHELIC	5.0	5.0	5.0	5.0	5.0

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DRYER TEST DATA

DRYER NO. 1 STACK #3

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST #1

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~ (MAGNA HELIC %OUT / FUEL RATE)	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2~~ ~~°F~~	AIR FLOW ACFM	REMARKS
3:15	40.0	178	109	7.0	61.6/8.0	99		10.4	171°			WOOD FUEL COUNTER - 642671 ~~RECYCLING MC SPLITTER~~
3:30	40.0	178	109	7.0	63.9/8.5	95			173°			642724
3:45	40.0	177	109	7.0	63.6/8.0	101			175°			642805
4:00	40.0	175	108	7.0	62.7/8.5	94	38.8		175°			642868
4:15	40.0	174	108	7.0	62.9/8.0	97		10.9	175°			642925

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RST Date 3-14-92

Customer LP

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST LOCATION: DRYER #1 - STACK #3

TEST # 1

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-14-92

SHT. 2 OF 2

PROCESS INFORMATION

15/16 15/23

TIME	3:15	3:30	3:45	4:00	4:15	THAYER SCALES
Forming Line Speed	30.3	30.3	30.3	30.3	30.3	11720
Board Thickness	3/8"	3/8"	3/8"	3/8"	3/8"	10770
Press Cycle Time 1	219°	219°	219°	219°	219°	13180
Control Oil Temp. Setpoint (Press) 2	216°	216°	216°	216°	216°	11530
Press Circ. Pump #1 Motor Load 3	214°	214°	214°	214°	214°	13290
Press Circ. Pump #2 Motor Load RESIN	10.2	10.2	10.2	10.4	10.4	12910
Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	14270
RAW MAT'L. MIX / DRY BIN LEVEL	HI	HI	HI	HI	HI	12200
3 CHIPS / SHAVINGS						13690
						12540
					TOTAL	126200
					AVG	2520

FLOW RATE 29,589 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	447	447	446	447	447
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	888	888	885	887	888
Heater Disch. Temperature COIL	645	645	645	646	647
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "H")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output %	73.1	72.6	73.5	76.2	74.8
Wood Fuel Delivery, Volts	128	132	138	141	135
Wood Air Signal, mA	11.0	11.5	11.5	12.0	11.5
Wood Burner Shell Temp.	175	175	176°	176°	176°
Wood Fuel Counter	187907	187985	188046	188169	188271
PD MAGNAHELIC	4.5	4.5	4.5	4.5	4.5

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DRYER TEST DATA

DRYER NO. 1 STACK #3

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST #2

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner (MAGNA HELIC %OUT / FUEL RATE) PD	mA	~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
												WOOD FUEL COUNTER - 643344 ~~RECYCLING INT. GAS~~
5:45	40.0	182	109	7.0	61.1 / 8.5	99	35.2		172°			
												643410
6:00	40.0	179	108	7.0	62.5 / 8.0	95			174°			
												643472
6:15	40.0	177	108	7.5	61.3 / 8.5	100		11.4	172°			
												643542
6:30	40.0	184	109	7.5	59.4 / 8.0	100			170°			
												643626
6:45	40.0	185	110	7.5	59.7 / 8.0	97		11.5	167°			

MEC COMPANY
Neodesha, Kansas U.S.A.

~~Job No.~~ MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT Date 3-14-92
LP

Customer

TEST TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

TEST LOCATION: DRYER #1 - STACK #3

TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-14-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	5:45	6:00	6:15	6:30	6:45	THAYER SCALES
Forming Line Speed	30.7	30.7	31.0	31.0	31.0	15820
Board Thickness	3/8"	3/8"	3/8"	3/8"	3/8"	11900
Press ~~Cycle Time~~ 1	219°	219°	219°	219°	219°	16620
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	215°	215°	215°	215°	215°	14020
~~Press Circ. Pump #1 Motor Load~~ 3	213°	213°	213°	213°	213°	15570
~~Press Circ. Pump #2 Motor Load~~ RESIN	10.2	10.2	10.2	10.2	10.4	14350
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	14380
RAW MAT'L. MIX DRY BIN LEVEL	HI	HI	HI	HI	HI-HI	13530
						15140
						13140
TOTAL						142670
AVG.						285

3 CHIPS 1 SHAVINGS

FLOW RATE 30,426 LBS/HR

HEATER OPERATION

TIME					
Return Oil Temperature INLET	447	447	446	446	446
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	892	894	893	895	894
Heater Disch. Temperature COIL	647	648	648	647	648
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output %	69.7	71.0	73.8	72.3	75.0
Wood Fuel Delivery, Volts	139	138	147	141	144
Wood Air Signal, mA	11.5	11.5	12.5	12.5	13.0
Wood Burner Shell Temp.	171°	171°	170°	169°	165°
Wood Fuel Counter	188844	188954	189033	189141	189257
PD MAGNAHELIC	4.5	4.5	4.5	4.5	4.5

MEC COMPANY

TEST TYPE: FORM, CO, THC
" LOCATION: PRESS VENT #11
" No.: 1

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL.
Plant Description: M.D.F.
Date: 3/13/92

PROCESS INFORMATION

	TIME	10:24	10:39	10:54	11:09	11:24	THAYER SCALE
FPM	Forming Line Speed	37.0	37.0	37.0	37.0	37.0	12880
	Board Thickness	3/16"	3/16"	3/16"	3/16"	3/16"	11160
	Press ~~Cycle Time~~ ZONE 1	219°F	219°F	219°F	219°F	220°F	10120
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	213°F	213°F	213°F	213°F	214°F	9230
	Press ~~Circ. Pump #1 Motor Load~~ 3	211°F	211°F	211°F	211°F	212°F	11040
GPM	Press ~~Circ. Pump #2 Motor Load~~ RESIN	9.4	9.4	9.4	9.5	9.4	9380
MLPM	Press ~~Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	11,750
	DRY BIN LEVEL	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	9,140
							12,240
							8,890
							106,910
							21,382

RAW MATERIAL MIX 1 SHAVINGS / 3 CHIPS FLOW RATE 22,700 #/HR

T.O. HEATER OPERATION

TIME	10:24	10:39	10:54	11:09	11:24
Return Oil Temperature	446	446	446	446	446
Feed Oil Temperature	490	490	490	490	490
Heater Inlet Temperature	879	883	881	884	880
Heater Disch. Temperature	655	656	656	656	653
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure	↓	↓	↓	↓	↓
Main Circulating Pump Motor Load	↓	↓	↓	↓	↓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
~~Gas/Oil Heat Controller Output~~					
~~Flowing Gas/Oil Pressure After Reg.~~					
~~Wood Heat Controller Output~~					
~~Wood Fuel Delivery, Volts~~					
~~Wood Air Signal, mA~~					
~~Wood Burner Shell Temp.~~					
~~Wood Fuel Counter~~					

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mEC COMPANY

TEST TYPE: FORM, CO, THC
" LOCATION: PRESS VENT #11
" No.: 2

Owner: L.P **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL **Plant Description:** M.D.F.

Date: 3/13/92

PROCESS INFORMATION

	TIME	12:44	12:59	1:14	1:29	1:44	THAYER SCALES 10250
FPM	Forming Line Speed	43.0	43.0	43.0	43.0	43.0	10320
	Board Thickness	3/16"	3/16"	3/16"	3/16"	3/16"	11,580
	Press ~~Cycle Time~~ ZONE 1	220°F	220°F	219°F	219°F	219°F	9940
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	215°F	215°F	215°F	215°F	215°F	11,970
	~~Press Circ. Pump #1 Motor Load~~ 3	212°F	212°F	210°F	210°F	210°F	10,020
GPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	9.5	9.6	9.7	9.6	9.6	12240
MLPM	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	11420
	DRY BIN LEVEL	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	11900
	RAW MATERIAL MIX 1 SHAVINGS / 3 CHIPS — FLOW RATE 26,442 #/HR						9110

108,750
21,750

T.O. HEATER OPERATION

TIME	12:44	12:59	1:14	1:29	1:44
Return Oil Temperature	446	446	446	445	445
Feed Oil Temperature	490	490	490	490	490
Heater Inlet Temperature	879	880	880	879	877
Heater Disch. Temperature	656	655	657	657	656
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load	✓	✓	✓	✓	✓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
~~Gas/Oil Heat Controller Output~~					
~~Flowing Gas/Oil Pressure After Reg.~~					
~~Wood Heat Controller Output~~					
~~Wood Fuel Delivery, Volts~~					
~~Wood Air Signal, mA~~					
~~Wood Burner Shell Temp.~~					
~~Wood Fuel Counter~~					

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mEC COMPANY

TEST TYPE: FORM, CO, THC
" LOCATION: PRESS VENT #11
" NO. : 3

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL **Plant Description:** M.D.F.

Date: 3/13/92

Start 14:40

PROCESS INFORMATION

	TIME	2:43	2:58	3:13	3:28	3:43	THAYER SCALE
FPM	Forming Line Speed	43	—	—	—	43	14830 1
	Board Thickness	3/16	—	—	—	3/16	12550 2
	Press ~~Cycle Time~~ ZONE 1	219°F	219°F	219°F	219°F	219°F	14810
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	215°F	215°F	215°F	215°F	215°F	12100
	Press ~~Circ. Pump #1 Motor Load~~ 3	210°F	210°F	210°F	210°F	210°F	15730
GPM	Press ~~Circ. Pump #2 Motor Load~~ RESIN	9.5	10.0	9.7	9.6	9.6	12730
MLPM	Press ~~Circ. Pump #3 Motor Load~~ WAX	1700	—	—	—	1700	14140
	DRY BIN LEVEL	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	11,120
	FLOW RATE 27,335 #/HR						12,870
							9,760

RAW MATERIAL MIX 1 SHAVINGS / 3 CHIPS

130,690
24128

T.O. HEATER OPERATION

TIME	2:43	2:58	3:13	3:28	3:43
Return Oil Temperature Inlet	445	444	444	444	444
Feed Oil Temperature pre-heat	490	490	490	490	490
Heater Inlet Temperature the gas	845	879	879	878	879
Heater Disch. Temperature Coil Temp	657	659	657	657	658
Control Temperature Setpoint	490	—	—	—	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure	↓	↓	↓	↓	↓
Main Circulating Pump Motor Load	↓	↓	↓	↓	↓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

DRYER TEST DATA

DRYER NO. FACE

FIRST FORMER LINE #1

PARTICULATE ONLY

Tamb, °F: _____

PBAR, "Hg: _____

TEST #3

TIME	FEED % (REFINER)	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~ %OPT/RPM (GAS ASSIST)	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
7:30	97	177	152	~	~	1000/800		9.0	~	~	~	~~WOOD FUEL COUNTER~~ ~~RECYCLING HOT OIL GAS~~	2
7:45	97	175	132	~	~	1000/875		9.2	~	~	~		2
8:00	97	184	133	~	~	975/925	21.1		~	~	~		2
8:15	97	173	129	~	~	950/925		8.4	~	~	~		2
8:30	97	176	129	~	~	950/925	22.3	9.8	~	~	~		2

PRODUCTION RATE
45,219 LBS/HR.
FACE & CORE

RAW MATL. MIX
3 SHAVINGS
1 CHIP
1/4 SAWTRIM

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

Customer LP By DB/RGT Date 3/13/92

MEC COMPANY
Neodesha, Kansas U.S.A.

PARTICULATE ONLY

mEC COMPANY

RAW MAT'L. MIX
3 SHAVINGS
1 CHIP
1/4 SAW TRIM

PRODUCTION RATE
45,219 LBS/HR.
FACE & CORE

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: MARCH 13, 1992

SHT. 2 OF 2

FACE DRYER
FIRST FORMER LINE #1
TEST #3

PROCESS INFORMATION

TIME						
Forming Line Speed	51					
Board Thickness	11/16					
Press Cycle Time	6:00					
Control Oil Temp. Setpoint (Press)	300°					
~~Press Circ. Pump #1 Motor Load~~ RESIN	7.9					GPM
~~Press Circ. Pump #2 Motor Load~~ WAX	1430					MLPM
~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME						
Return Oil Temperature						
Feed Oil Temperature						
Heater Inlet Temperature						
Heater Disch. Temperature						
Control Temperature Setpoint						
Oil Differential Pressure						
Heater Differential Press. Setpoint						
Tee Section Static Pressure						
Main Circulating Pump Motor Load						
Aux. Circulating Pump Motor Load						

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME						
Gas/Oil Heat Controller Output						
Flowing Gas/Oil Pressure After Req.						
Wood Heat Controller Output						
Wood Fuel Delivery, Volts						
Wood Air Signal, mA						
Wood Burner Shell Temp.						
Wood Fuel Counter						

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DRYER TEST DATA

DRYER NO. 2 STACK 1

TEST NO. 1

TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNA HELIC)	Wood Burner ~~VDC~~ (% OUT / FUEL RATE)	MC_1 %	MC_2 %	PRODUCT ~~TPS~~ °F SHELL	PRODUCT TP °F	AIR FLOW ACFM	REMARKS
11:00	40.0	157	101	7.0	67.7 / 11.5	134			155°F			TOTALIZER WOOD FUEL COUNTER THRU-PUT ~~RECYCLING HOT OIL GAS~~ 176312
11:15	40.0	148	99	7.0	70.6 / 11.0	126			160°F			176387
11:30	40.0	146	97	6.5	71.0 / 11.5	133		11.4	157°F			176472
11:45	42.0	154	100	7.0	70.3 / 11.0	129			155°			176562
12:00	42.0	147	97	7.0	71.5 / 11.5	133	31.8	10.8	159°		56,045	176653 LBS/HR = 23,049

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT Date 3/13/92

Customer LP

AEC COMPANY

Neodesha, Kansas U.S.A.

mEC COMPANY

TEST TYPE PARTICULATE, PM10, CPM, O_2, CO_2

TEST LOCATION DRYER 2 - STACK 1

TEST # 1

Owner: LP **Test Personnel:** DB/RGT

Location: CLAYTON, AL **Plant Description:** MDF

Date: 3-13-92

SHT. 2 OF 2

PROCESS INFORMATION

	TIME						THAYER SCALE 1
							8971
FPM	Forming Line Speed	37.0	37.0	37.0	37.0	37.0	8840
	Board Thickness	3/16"	3/16"	3/16"	3/16"	3/16	10130
	Press ~~Cycle Time~~ 1	219°F	220°F	220°F	220°F	220°F	9420
	~~Control~~ Oil Temp. ~~Setpoint~~ (Press) 2	213°F	214°F	214°F	214°F	214°F	9170
	Press Circ. Pump ~~#1 Motor Load~~ 3	211°F	212°F	212°F	212°F	212°F	9390
GPM	Press Circ. Pump ~~#2 Motor Load~~ RESIN	9.4	9.4	9.4	9.6	9.4	11051
TALPM	Press Circ. Pump #3 Motor Load WAX	1700	1700	1700	1700	1700	10650
	RAW MATERIAL MIX / SHAVINGS 3 CHIPS — DRY BIN LEVEL	HI-HI	HI-HI	HI-HI	HI-HI	HI	9980
							9590

FLOWRATE 23049 #/HR

TOTAL 97,140
AVG. 19,428

T.O. HEATER OPERATION

TIME					
Return Oil Temperature INLET	446	446	446	446	446
Feed Oil Temperature OUTLET	490	490	490	489	490
Heater Inlet Temperature HOT GAS	882	879	882	878	880
Heater Disch. Temperature COIL	654	654	654	652	655
Control Temperature Setpoint	490	490	490	490	490
~~Oil Differential Pressure~~	~~NA~~	~~NA~~	~~NA~~	~~NA~~	~~NA~~
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure	↓	↓	↓	↓	↓
Main Circulating Pump Motor Load	↓	↓	↓	↓	↓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Reg.	NA				NA
Wood Heat Controller Output 90 OUT	59.4	61.3	59.9	61.3	59.6
Wood Fuel Delivery, Volts	90	97	94	99	98
Wood Air Signal, mA	8.0	8.0	8.5	8.0	8.0
Wood Burner Shell Temp.	150°	155°	155°	154°	155°
Wood Fuel Counter TOTALIZER	634426	634449	634510	634573	634644
MAGNAHELIC PD	4.5	4.5	4.5	4.5	4.5

DRYER TEST DATA

DRYER NO. 2 STACK 1
TEST NO. 2

TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

Tamb, °F: _____
PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNA HELIC / % OUT)	Wood Burner ~~VDC~~ (FUEL RATE)	MC_1 %	MC_2 %	PRODUCT °F SHELL	PRODUCT TP_e °F	AIR FLOW ACFM	REMARKS (TOTALIZER)
~~1:34~~	~~44.0~~	~~166~~	~~102~~	~~6.5~~	~~68.5 / 11.0~~	~~128~~			~~162°~~			~~WOOD FUEL QUANTITY 177261 THRU-PUT RECYCLING NOT ALL GAS~~
1:47			STOP					TEST				PRESS DOWN
2:25	44.0	156	107	6.5	67.4 / 11.0	120		11.6	162°			RESTART @ 2:25 177521
2:40	44.0	169	105	7.0	67.2 / 11.5	132		11.0	161°			177602
2:55	44.0	174	105	7.0	72.7 / 12.5	143	31.6		160°			177718
3:10	44.0	173	104	7.5	74.9 / 13.0	149		12.0	160°			177845
3:25	44.0	174	104	7.0	73.4 / 12.5	145			160°		56045	177952

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

Customer LP By DB/RGT Date 3/13/92

DEC COMPANY
Neodesha, Kansas U.S.A.

TEST TYPE PARTICULATE, PM10, CPM, O2 & CO2

TEST LOCATION DRYER 2-STACK 1

TEST # 2

mEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-13-92

SHT. 2 OF 2

PROCESS INFORMATION

TIME	1:34	2:25	2:40	2:55	3:10	THAYER SCALES
Forming Line Speed	43.0	43.0	43.0	43.0	43.0	12640
Board Thickness	3/16	3/16	3/16	3/16	3/16	11340
Press ~~Cycle Time~~ 1	219°F	219°F	219°F	219°F	219°F	13460
~~Control~~ Oil Temp. ~~Setpoint~~ (Press) 2	218°F	215°F	215°F	215°F	215°F	13050
~~Press Circ. Pump #1 Motor Load~~ 3	210°F	210°F	210°F	210°F	210°F	14300
GPM ~~Press Circ. Pump #2 Motor Load~~ RESIN	9.6	9.6	9.6	9.7	9.6	12190
MLPM ~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	14640
DRY BIN LEVEL	HI-HI	HI	HI-HI	HI-HI	HI-HI	10790
						14590
						10660

RAW MAT'L. MIX

3 CHIPS / SHAVINGS

FLOW RATE

HEATER OPERATION

TIME						3:25
Return Oil Temperature INLET	445	445	445	444	444	444
Feed Oil Temperature OUTLET	490	489	490	490	490	490
Heater Inlet Temperature HOT GAS	878	871	876	879	880	879
Heater Disch. Temperature COIL	657	648	657	658	657	658
Control Temperature Setpoint	490	490	490	490	490	490
~~Oil Differential Pressure~~	NA	NA	NA	NA	NA	
Heater Differential Press. Setpoint						
Tee Section Static Pressure						
Main Circulating Pump Motor Load						
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA	

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME						
Gas/Oil Heat Controller Output	NA				NA	
Flowing Gas/Oil Pressure After Req.	NA				NA	
Wood Heat Controller Output	58.6	58.1	56.6	57.7	59.4	58.9
Wood Fuel Delivery, Volts	96	100	97	97	93	90
Wood Air Signal, mA	8.0	8.0	8.0	8.0	8.5	8.0
Wood Burner Shell Temp.	156°	158°	156°	156°	155°	156°
Wood Fuel Counter	635070	635251	635322	635394	635476	635550
MAGNAHELIC PD	4.5	4.5	4.5	4.5	4.5	4.5

MEC COMPANY
Neodesha, Kansas U.S.A.

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT Date
Customer LP

DRYER TEST DATA

DRYER NO. 2 STACK # 2

TEST # 1

TEST TYPE: PARTICULATE, PM10, CFM, O_2, CO_2

Tomb, °F: _____

PBAR, "Hg: _____

MASNA-HELIC % 0027 / FUEL RATE

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
6:36	40.0	154	98	7.0	72.7/11.5	139			160°			~~WOOD FUEL COUNTER~~ 179104 ~~RECYCLING NOT ON GAS~~
6:51	40.0	158	100	7.0	69.0/11.5	125	34.3		155°			179195
7:06	40.0	155	99	6.5	68.1/11.5	130		12.2	151°			179321
7:21	40.0	153	98	6.5	68.7/11.5	131			150°			179397
7:36	40.0	164	100	7.0	66.1/11.5	130		12.4	149°		55,210	179491

mEC COMPANY

TEST TYPE PARTICULATE, PM10, CFM, O_2, CO_2
TEST LOCATION DRYER #2 - ~~STACK #2~~
TEST #1

Owner: LP
Test Personnel: DB/RGT
Location: CLAYTON, AL
Plant Description: MDF
Date: 3-13-92

PROCESS INFORMATION

TIME						THAYER SCALES
Forming Line Speed	43.0	43.0	43.0	43.0	43.0	12190
Board Thickness	3/16"	3/16"	3/16"	3/16"	3/16"	10610
Press ~~Cycle Time~~ 1	219°F	219°	219°	219°	219°	11080
~~Control~~ Oil Temp. ~~Setpoint~~ (Press) 2	215°F	215°	215°	215°	215°	11030
~~Press Circ. Pump #1 Motor Load~~ 3	210°F	210°	210°	210°	210°	10640
~~Press Circ. Pump #2 Motor Load~~ RESIN	9.6	9.4	9.4	9.4	9.4	11050
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	12420
RAW MATL. MIX DRY BIN LEVEL	HI	HI	HI	HI	HI	10720
3 CHIPS 1 SHAVINGS						11860
						9450

FLOW RATE LBS/HR

HEATER OPERATION

TIME					TOTAL AVG.
Return Oil Temperature INLET	445	445	445	445	445
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	883	886	885	887	886
Heater Disch. Temperature COIL	657	656	658	657	658
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output	59.6	59.7	59.3	59.1	57.0
Wood Fuel Delivery, Volts	95	88	87	92	102
Wood Air Signal, mA	8.0	8.0	8.0	8.0	8.0
Wood Burner Shell Temp.	157°	153°	152°	151°	150°
Wood Fuel Counter	636351	636418	636501	636559	636614
MAGNAHELIC ΔP	4.5	4.5	4.5	4.5	4.5

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DRYER TEST DATA

DRYER NO. 2 STACK 1

TEST NO. 3

TYPE: PARTICULATE, PM10, CPM, O_2, CO_2

Tamb, °F: _____

PBAR, "Hg: _____

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA (MAGNAHELIC)	Wood Burner ~~VDC~~ (% OUT / FUEL RATE)	MC_1 %	MC_2 %	PRODUCT TP_1 °F SHELL	PRODUCT ~~TP_2 °F~~	AIR FLOW ACFM	REMARKS
4:25	40.0	152	99	6.5	83.7 / 120	143		12.1	166°			TOTALIZER WOOD FUEL COUNTER - THRU-PUT 178330
4:40	40.0	154	99	6.5	74.9 / 11.5	124	39.2		166°			178426
4:55	40.0	157	99	6.0	68.5 / 10.5	118		12.2	164°			178531
5:10	40.0	146	98	6.0	75.1 / 10.5	123			164°			178611
5:25	40.0	144	96	6.5	74.5 / 10.5	122		12.0	161°		56045	178701

Job No. MDF Location CLAYTON, NC Sht. No. 1 of 2

By DB/RGT Date 3/13/92

Customer LP

MEC COMPANY
Neodesha, Kansas U.S.A.

O_2, CO_2

TEST TYPE PARTICULATE, PM10, CPM,

TEST LOCATION DRYER 2-STACK 1

TEST # 3

MEC COMPANY

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: 3-13-92

PROCESS INFORMATION

	TIME						THAYER SCALES
	Forming Line Speed	41.0	41.0	41.0	41.0	41.0	9660
	Board Thickness	3/16	3/16	3/16	3/16	3/16	10470
	Press ~~Cycle Time~~ TEMP. 1	220°F	220°	220°	220°	220°	11830
	~~Control~~ Oil Temp. ~~Setpoint~~ (Press) 2	216°F	216°	216°	216°	216°	10160
	~~Press Circ. Pump #1 Motor Load~~, 3	211°F	211°	211°	211°	211°	11220
GPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	9.4	9.4	9.2	9.2	9.2°	10190
MLPM	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	1700	1700	1700	1700	11940
	DRY BIN LEVEL	HI-HI	HI-HI	HI-HI	HI-HI	HI-HI	10460
							9930
							9710

RAW MAT'L. MIX
3 CHIPS 1 SHAVINGS
FLOW RATE 25/17

HEATER OPERATION

TIME					
Return Oil Temperature INLET	445	444	444	444	445
Feed Oil Temperature OUTLET	490	490	490	490	490
Heater Inlet Temperature HOT GAS	880	876	878	875	877
Heater Disch. Temperature COIL	659	656	657	656	656
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

OTHER BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output	NA				NA
Flowing Gas/Oil Pressure After Req.	NA				NA
Wood Heat Controller Output %	61.6	62.9	60.5	64.6	62.5
Wood Fuel Delivery, Volts	91	96	90	85	86
Wood Air Signal, mA	7.5	8.0	8.0	8.0	8.0
Wood Burner Shell Temp.	162°	162°	160°	160°	162°
Wood Fuel Counter	635821	635879	635942	635994	636062
MAGNAHELIC PD	4.0	4.5	4.5	4.0	4.0

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JEFF - 255

mEC COMPANY

TEST TYPE: FORM, CO, THC
LOCATION: PRESS VENT #4
NO.: 2

Owner: L.P. **Test Personnel:** F.G.T. & D.B.

Location: CLAYTON, AL. **Plant Description:** M.D.F

Date: 3/12/92

PROCESS INFORMATION

	TIME	7:50	8:05	8:20	8:35	8:50	THAYER SCALES
FPM	Forming Line Speed	35.0	35.0	[illegible]	35.0	35.0	13040
	Board Thickness	1/4"	1/4"	1/4"	1/4"	1/4"	11100
	Press ~~Cycle Time~~ ZONE 1	218°F	218°F	218°F	219°F	218°F	13,000
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	217°F	217°F	217°F	217°F	217°F	11,210
	~~Press. Circ. Pump #1 Motor Load~~ 3	219°F	219°F	219°F	219°F	219°F	9,030
GPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	9.4	9.6	9.6	9.3	9.3	7,600
MLPM	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	—	1700	—	1700	13,090
	DRY BIN LEVEL	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	10,120
							8,360
							9260
							108,810
							21,762

RAW MATERIAL MIX 1 SHAVINGS / 3 CHIPS

FLOW RATE 26,595 #/HR

565 [illegible]

T.O. HEATER OPERATION

TIME	7:50	8:05	8:20	8:35	8:50
Return Oil Temperature	447	446	446	446	446
Feed Oil Temperature	487	490	490	490	490
Heater Inlet Temperature	879	883	888	889	888
Heater Disch. Temperature	635	646	652	656	655
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load	✓	✓	✓	✓	✓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: FORM, CO, THC
" LOCATION: PRESS VENT #4
" NO.: 3

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL. **Plant Description:** M.D.F.

Date: 3/12/92

9:54 BACK RUNNING
951 PRESS DOWN

PROCESS INFORMATION

	TIME	9:20	9:35	9:50	10:08	10:28	THAYER SCALES
FPM	Forming Line Speed	35.0	35.0	35.0	35.0	35.0	11,170
	Board Thickness	1/4"	1/4"	1/4"	1/4"	1/4"	10,260
	Press ~~Cycle Time~~ ZONE 1	219°F	219°F	219°F	221°F	221°F	11,250
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	216°F	216°F	216°F	217°F	216°F	10,610
	~~Press Circ. Pump #1 Motor Load~~ 3	211°F	211°F	212°F	212°F	211°F	12,650
GPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	9.4	9.3	9.4	9.4	9.3	10,990
MLPM	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	—	1700	—	1700	12,820
	DRY BIN LEVEL	Hi	Hi	Hi	Hi-Hi	Hi	10,240
							11,590
	FLOW RATE 26,614 #/HR						10,020
							111,550
							22,310

RAW MATERIAL MIX 1 SHAVINGS / 3 CHIPS

562 - 281

T.O. HEATER OPERATION

TIME	9:20	9:35	9:50	10:08	10:28
Return Oil Temperature	445	445	445	447	445
Feed Oil Temperature	490	490	490	490	490
Heater Inlet Temperature	887	888	887	885	885
Heater Disch. Temperature	658	659	657	653	655
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure	↓	↓	↓	↓	↓
Main Circulating Pump Motor Load	↓	↓	↓	↓	↓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE: FORM, CO, THC
" LOCATION: PRESS VENT #3
" NO.: 1

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL. **Plant Description:** M.D.F.

Date: 3/12/92

PROCESS INFORMATION

THAYER SCALES

	TIME	1:30	1:45	2:00	2:15	2:30	15,060
FPM	Forming Line Speed	38.0	38.0	38.0	38.0		11,350
	Board Thickness	1/4"	1/4"	1/4"	1/4"		14,550
	Press ~~Cycle Time~~ ZONE 1	221° F	221° F	220° F	220° F		12,280
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	216° F	216° F	215° F	216° F		14,270
	Press ~~Circ. Pump #1 Motor Load~~ 3	210° F	210° F	210° F	210° F		12,170
GPM	Press ~~Circ. Pump #2 Motor Load~~ RESIN	9.9	9.7	9.8	9.8	9.9	15,190
MLPM	Press ~~Circ. Pump #3 Motor Load~~ WAX	1700	—	1700	—	1700	11,170
	DRY BIN LEVEL	Hi	Hi	Hi	Hi	Hi	13,800
	FLOWRATE			28,272		#/HR	12,200
							132,040
							26,408

RAW MATERIAL MIX 1 SHAVINGS / 3 CHIPS

589-296

T.O. HEATER OPERATION

TIME	1:30	1:45	2:00	2:15	2:30
Return Oil Temperature	445	440	442	445	445
Feed Oil Temperature	490	480	490	490	490
Heater Inlet Temperature	888	886	896	892	891
Heater Disch. Temperature	657	627	656	652	650
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure	↓	↓	↓	↓	↓
Main Circulating Pump Motor Load	↓	↓	↓	↓	↓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

RUN SOOT BLOWERS

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter		✓			

MEC COMPANY

TEST TYPE: FORM. CO. THC
" LOCATION: PRESS VENT #3
" NO.: 2

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL
Plant Description: M.D.F.
Date: 3/12/92

PROCESS INFORMATION

THAYER SCALES

TIME	3:02	3:17	3:32	3:47	4:02	15,550
Forming Line Speed	38.0	38.0	38.0	38.0	38.0	12,480
Board Thickness	1/4"	1/4"	1/4"	1/4"	1/4"	13,890
Press ~~Cycle Time~~ ZONE 1	220°F	220°F	220°F	220°F	220°F	12,210
~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	216°F	216°F	216°F	215°F	215°F	14,490
Press Circ. ~~Pump #1 Motor Load~~ 3	216°F	210°F	210°F	210°F	212°F	12,210
Press Circ. ~~Pump #2 Motor Load~~ RESIN	9.9	9.7	9.9	9.8	9.8	13,800
Press ~~Circ. Pump #3 Motor Load~~ WAX	1700	—	1700	—	1700	11,800
DRY BIN LEVEL	Hi	Hi	Hi-Hi	Hi	Hi	14,180
FLOW RATE	28,703				#/HR	11,520

RAW MATERIAL MIX 1 SHAVINGS 3 CHIPS
587.2 - 295

132,130
26,426

T.O. HEATER OPERATION

TIME	3:02	3:17	3:32	3:47	4:02
Return Oil Temperature	495	495	444	444	444
Feed Oil Temperature	490	490	490	490	490
Heater Inlet Temperature	889	890	888	889	889
Heater Disch. Temperature	650	651	649	651	652
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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mEC COMPANY

TEST TYPE: FORM. CO THC
" LOCATION: PRESS VENT #3
" No. : 3

Owner: L.P. **Test Personnel:** R.G.T. & D.S.

Location: CLAYTON, AL. **Plant Description:** MDF

Date: 3/12/92

PROCESS INFORMATION

TIME	4:28	4:43	4:58	5:13	5:28	THAYER SCALES 13320
Forming Line Speed	38.0	38.0	38.0	38.0	38.0	11480
Board Thickness	1/4"	1/4"	1/4"	1/4"	1/4"	14400
~~Press Cycle Time~~ ZONE 1	220°F	220°F	220°F	220°F	219°F	11,780
~~Control~~ Oil Temp. ~~[illegible]~~ (Press) 2	215°F	215°F	215°F	215°F	215°F	15,110
~~Press Circ. Pump #1 Motor Load~~ 3	210°F	210°F	210°F	210°F	209°F	12,830
~~Press Circ. Pump #2 Motor Load~~ MELT	9.9	9.7	9.8	9.8	9.8	15,520
~~Press Circ. Pump #3 Motor Load~~ WAX	1700	—	1700	—	1700	12,540
DRY BIN LEVEL	Hi	Hi	Hi	Hi	Hi	16,990
FLOW RATE			28,395		#/HR	12,600
						136,070
						27,214

RAW MATERIAL MIX 1 SHAVINGS / 3 CHIPS
588 - 299

T.O. HEATER OPERATION

TIME	4:28	4:43	4:58	5:13	5:28
Return Oil Temperature	444	444	444	444	444
Feed Oil Temperature	490	490	490	490	490
Heater Inlet Temperature	887	892	891	895	898
Heater Disch. Temperature	651	652	651	653	651
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

DRYER TEST DATA
DRYER NO. CORE
PRESS LINE #1

PM 10 PARTICULATE & CONDENSABLES

Tamb, °F: _____
PBAR, "Hg: _____

TEST #1

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	RPM ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
8:45	94	159	121	~	~	750/1050	20.3	7.9	~	~	~	~~WOOD FUEL (CONT.)~~ ~~RECYCLING HOT OIL GAS~~	1
9:00	94	159	121	~	~	750/1150		9.0	~	~	~		1
9:15	94	161	121	~	~	750/975	23.0	9.0	~	~	~		1
9:30	94	161	121	~	~	750/1100		9.2	~	~	~		1
9:45	94	161	121	~	~	750/1250		8.6	~	~	38,125		1

PRODUCTION RATE
36,646 LBS/HR.
CORE & FACE

RAW MATL. MIX
3 SHAVINGS
1 CHIP
1/4 SAW TRIM

MEC COMPANY
Neodesha, Kansas U.S.A.

Job No. MDF Location CORE CLAYTON, AL Sht. No. ____ of ____
Customer L/P By DB/RGT Date 3/12/92

MEC COMPANY PM10 PARTICULATE & CONDENSABLES	RAW MAT'L. MIX 3 SHAVINGS 1 CHIP 1/4 SAW TRIM	PRODUCTION RATE 36,646 LBS./HR. CORE & FACE

Owner: L/P Test Personnel: DB/RGT

Location: CLAYTON, AL Plant Description: MDF

Date: MARCH 12, 1992 SHT. 2 OF 2

CORE DRYER
PRESS LINE #1
TEST #1

PROCESS INFORMATION

TIME						
Forming Line Speed	48					
Board Thickness	9/16					
Press Cycle Time	5:20					
Control Oil Temp. Setpoint (Press)	300°					
~~Press Circ. Pump #1 Motor Load~~						
~~Press Circ. Pump #2 Motor Load~~ RESIN	6.2					GPM
~~Press Circ. Pump #3 Motor Load~~ WAX	1,200					MLPM

HEATER OPERATION

TIME						
Return Oil Temperature						
Feed Oil Temperature						
Heater Inlet Temperature						
Heater Disch. Temperature						
Control Temperature Setpoint						
Oil Differential Pressure						
Heater Differential Press. Setpoint						
Tee Section Static Pressure						
Main Circulating Pump Motor Load						
Aux. Circulating Pump Motor Load						

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME						
Gas/Oil Heat Controller Output						
Flowing Gas/Oil Pressure After Reg.						
Wood Heat Controller Output						
Wood Fuel Delivery, Volts						
Wood Air Signal, mA						
Wood Burner Shell Temp.						
Wood Fuel Counter						

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DRYER TEST DATA
DRYER NO. CORE
PRESS LINE #1

PM10 PARTICULATE & CONDENSABLES

Tamb, °F: _____
PBAR, "Hg: _____

TEST #2

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	RPM ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
10:45	100	163	121	~	~	750/1150		8.0	~	~	~	~~WOOD FUEL COUNTER~~ ~~RECYCLING HOT OIL GAS~~	1
11:00	100	160	120	~	~	750/900	20.0	8.6	~	~	~		1
11:15	100	158	119	~	~	750/650			~	~	~		1
11:30	100	161	119	~	~	750/750		9.6	~	~	~		1
11:45	100	161	120	~	~	750/800		9.0	~	~	~		1
12:00	100	163	120	~	~	750/950	20.0		~	~	38,417		1

PRODUCTION RATE
38,036 LBS./HR
CORE & FACE

RAW MATL MIX
3 SHAVINGS
1 CHIPS
1/4 SAW TRIM

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

CORE

MEC COMPANY
Neodesha, Kansas U.S.A.

Customer _____ By DB/RGT/LP Date 3/12/92

PM10 PARTICULATE & CONDENSABLES

mEC COMPANY

RAW MAT'L. MIX
3 SHAVINGS
1 CHIP
1/4 SAW TRIM

PRODUCTION RATE
38,036 LBS./HR
CORE & FACE

Owner: LP **Test Personnel:** DB/RGT

Location: CLAYTON, AL **Plant Description:** MDF

Date: MARCH 12, 1992 SHT. 2 OF 2

CORE DRYER
PRESS LINE #1
TEST #2

PROCESS INFORMATION

TIME						
Forming Line Speed	59					
Board Thickness	9/16					
Press Cycle Time	5:20					
Control Oil Temp. Setpoint (Press)	300°					
~~Press Circ. Pump #1 Motor Load~~ RESIN	6.3					GPM
~~Press Circ. Pump #2 Motor Load~~ WAX	1,200					MLPM
~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME						
Return Oil Temperature						
Feed Oil Temperature						
Heater Inlet Temperature						
Heater Disch. Temperature						
Control Temperature Setpoint						
Oil Differential Pressure						
Heater Differential Press. Setpoint						
Tee Section Static Pressure						
Main Circulating Pump Motor Load						
Aux. Circulating Pump Motor Load						

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME						
Gas/Oil Heat Controller Output						
Flowing Gas/Oil Pressure After Reg.						
Wood Heat Controller Output						
Wood Fuel Delivery, Volts						
Wood Air Signal, mA						
Wood Burner Shell Temp.						
Wood Fuel Counter						

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DRYER TEST DATA

DRYER NO. CORE

PRESS LINE #1

PM10 PARTICULATE & CONDENSABLES

Tamb, °F: _____

PBAR, "Hg: _____

TEST # 3

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	RPM ~~DDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
1:15	100	161	122	~	~	750/800		9.4	~	~	~	~~WOOD FUEL COUNTER~~ ~~RECYCLING HOT OIL GAS~~	1
1:30	100	161	123	~	~	750/750	9.0	8.8	~	~	~		1
1:45	100	159	123	~	~	750/550			~	~	~		1
2:00	100	162	123	~	~	750/525		8.4	~	~	~		1
2:15	100	157	120	~	~	750/525	20.0		~	~	38,191		1

PRODUCTION RATE
39,301 LBS/HR
CORE & FACE

RAW MATL. MIX
3 SHAVINGS
1 CHIP
1/4 SAWTRIM

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT Date 3/12/92

Customer LP

MEC COMPANY
Neodesha, Kansas U.S.A.

PM10 PARTICULATE & CONDENSABLES	RAW MAT'L. MIX 3 SHAVINGS 1 CHIP 1/4 SAW TRIM	PRODUCTION RATE 39,301 LBS./HR. CORE & FACE

Owner: LP **Test Personnel:** DB/RGT

Location: CLAYTON, AL **Plant Description:** MDF

Date: MARCH 12, 1992 SHT. 2 OF 2

CORE DRYER PRESS LINE #1 TEST #3

PROCESS INFORMATION

TIME						
Forming Line Speed	52					
Board Thickness	9/16					
Press Cycle Time	5:20					
Control Oil Temp. Setpoint (Press)	300°					
~~Press Circ. Pump #1 Motor Load~~ RESIN	6.2	6.3	6.5	6.2		GPM
~~Press Circ. Pump #2 Motor Load~~ WAX	1200					MLPM
~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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DRYER TEST DATA

DRYER NO. FACE

FIRST FORMER LINE #1

PARTICULATE ONLY

Tamb, °F: _____

PBAR, "Hg: _____

TEST #1

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	RPM ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
3:30	91	164	125	~	~	725/800		9.6	~	~	~	~~WOOD FUEL COLLECTOR~~ RECYCLING HOT OIL GAS	1
3:45	91	162	126	~	~	725/525	25.2	10.0	~	~	~		1
4:00	91	155	123	~	~	725/875		9.6	~	~	~		1
4:15	91	157	124	~	~	725/550		9.8	~	~	~		1
4:30	91	165	125	~	~	725/800			~	~	~		1
4:45	91	166	127	~	~	725/700			~	~			1

PRODUCTION RATE
38,331 LBS./HR.
FACE & CORE

RAW MATL. MIX
3 SHAVINGS
1 CHIPS
1/4 SAWTRIM

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

By DB/RGT/LP Date 3/12/92

Customer

MEC COMPANY
Neodesha, Kansas U.S.A.

FACE

mEC COMPANY PARTICULATE ONLY	RAW MATERIAL 3 SHAVINGS 1 CHIP 1/4 SAWTRIM	PRODUCTION RATE 38,331 LBS./HR. FACE & CORE

Owner: LP

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: MARCH 12, 1992

PROCESS INFORMATION

TIME						
Forming Line Speed	52					
Board Thickness	9/16					
Press Cycle Time	5:20					
Control Oil Temp. Setpoint (Press)	300°					
~~Press Circ. Pump #1 Motor Load~~ RESIN	8.0					GPM
~~Press Circ. Pump #2 Motor Load~~ WAX	1,400					MLPM
~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME						
Return Oil Temperature						
Feed Oil Temperature						
Heater Inlet Temperature						
Heater Disch. Temperature						
Control Temperature Setpoint						
Oil Differential Pressure						
Heater Differential Press. Setpoint						
Tee Section Static Pressure						
Main Circulating Pump Motor Load						
Aux. Circulating Pump Motor Load						

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME						
Gas/Oil Heat Controller Output						
Flowing Gas/Oil Pressure After Req.						
Wood Heat Controller Output						
Wood Fuel Delivery, Volts						
Wood Air Signal, mA						
Wood Burner Shell Temp.						
Wood Fuel Counter						

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DRYER TEST DATA

DRYER NO. FACE

FIRST FORMER LINE #1

PARTICULATE ONLY

Tamb, °F: _____

PBAR, "Hg: _____

~~Sect~~ RPM

TEST #2

TIME	FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner ~~VDC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS
5:30	91	137	120	~	~	125/150			~	~	~	~~DOG FUEL COUNTER~~ ~~RECYCLING HOT OIL GAS~~ 1
5:45	91	167	124	~	~	132.5/—			~	~	~	LOST #2 BURNER #1 BURNER TO AUTO 1
5:55 6:12	OUT IN			STOP		TEST						LOST #1 BURNER REFIRE #1 ON GAS
6:15	90	165	132	~	~	GAS/1147°		STOP		TEST		PRESS TROUBLE 6:23 OUT 1
6:30	90	146	122	~	~	GAS/1043			~	~	~	6:27 IN 2
				STOP		TEST						LOST #1 BURNER 6:38 OUT
IN 6:46	90	138	122	~	~	GAS/904			~	~	~	
7:00	90	137	120	~	~	GAS/890	25.0	9.0	~	~	~	
7:10	DONE											PRODUCTION RATE 37,583 LBS./HR. FACE + CORE
												RAW MATL. MIX 3 SHAVINGS 1 CHIP 14 SAWTRIM

Job No. MDF Location CLAYTON, AL Sht. No. 1 of 2

Customer _____ By DB/RGT LP Date 3/12/92

FACE

MEC COMPANY Neodesha, Kansas U.S.A.

PARTICULATE ONLY

mEC COMPANY

RAW MATL. MIX	PRODUCTION RATE
3 SHAVINGS	1 LBS./HR.
1 CHIP	FACE & CORE
1/4 SAW TRIM	

Owner: LP **Test Personnel:** DB/RGT

Location: CLAYTON, AL **Plant Description:** MDF

Date: MARCH 12, 1992 SHT. 2 OF 2

FACE DRYER
FIRST FORMER LINE #1
TEST #2

PROCESS INFORMATION

TIME	5:30	6:12	6:18	6:27	6:35	
Forming Line Speed	46	38	24	52	42	
Board Thickness	9/16					
Press Cycle Time	5:20					
Control Oil Temp. Setpoint (Press)	300°					
~~Press Circ. Pump #1 Motor Load~~ RESIN	8.0	7.9	8.1			GPM
~~Press Circ. Pump #2 Motor Load~~ WAX	1400					MLPM
~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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DAVID PRATER

PRESS 255 - LEE [illegible]

mEC COMPANY

TEST TYPE: FORM., CO, THC

LOCATION: PRESS VENT #2

No.: 1

Owner: L.P. **Test Personnel:** RGT & D.B.

Location: CLAYTON, AL. **Plant Description:** MDF

Date: 3/11/92

PROCESS INFORMATION

								THAYER SCALES
	TIME		6:00	6:15	6:30	6:45	7:00	13040
FPM	Forming Line Speed		28.0	28.0	28.0	28.0	28.0	10120
	Board Thickness		3/8"	3/8"	3/8"	3/8"	3/8"	12640
	Press ~~Cycle Time~~	ZONE 1	219°F	219°F	219°F	219°F	219°F	10,050
	~~Control Oil~~ Temp. ~~Setpoint (Press)~~	2	219°F	218°F	219°F	218°F	218°F	15,060
	~~Press Circ. Pump #1 Motor Load~~	3	216°F	216°F	218°F	219°F	219°F	10,000
GPM	~~Press Circ. Pump #2 Motor Load~~	RESIN	9.8	9.5	9.6	9.6	9.7	15,170
MLPM	~~Press Circ. Pump #3 Motor Load~~	WAX	1700	—	1700	—	1700	12,130
	DRY BIN LEVEL		Hi	Hi	Hi	Hi	Hi	14,120
								11,000
								123,900
								24,780

RAW MATERIAL MIX = 1 SHAVINGS / 1 CHIPS

FLOW RATE 27,764 #/HR

578

T.O. HEATER OPERATION

TIME	6:00	6:15	6:30	6:45	7:00
Return Oil Temperature	449	448	447	447	446
Feed Oil Temperature	489	490	495	490	490
Heater Inlet Temperature	882	888	887	886	884
Heater Disch. Temperature	626	639	642	644	644
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load	✓	✓	✓	✓	✓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Req.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

234 CONT 1
227 CONT 2
255 LINE 2

LAB -
PRESS OPER. - JEFF HARRISON

IEA -
DAVID PRATER
BARRY RAYFIELD

mEC COMPANY

TEST TYPE: FORM, CO, THC
TEST LOCATION: PRESS VENT #-5
TEST No.: 1

Owner: L.P. **Test Personnel:** R.G.T. & D.B.

Location: CLAYTON, AL. **Plant Description:** M.D.F.

Date: 3-11-92

PROCESS INFORMATION

TIME	10:00A	10:15	10:30	10:45	11:00	THRU SCALES
Forming Line Speed	28.5	28.5	28.5	28.5	28.5	13050
Board Thickness	3/8	3/8	3/8	3/8	3/8	11010
~~Press Cycle Time~~ PRESS TEMP ZONE 1	220	220	220	220	220	13800
Control Oil Temp. ~~Setpoint~~ (~~Press~~) 2	217	217	217	217	217	11550
~~Press Circ. Pump #1 Motor Load~~ ZONE 3	212	212	212	212	212	13200
GPM ~~Press Circ. Pump #2 Motor Load~~ RESIN	9.8	9.8	9.6	9.6	9.6	11250
MLPM ~~Press Circ. Pump #3 Motor Load~~ WAX	1700	—	1700	—	1700	12960
BIN LEVEL	HI-HI	HI-HI	HI	HI	HI	10900
RAW MATERIAL MIX = 1 SHAVINGS TO 1 CHIPS LINE 2						13210
						11940

T.O. HEATER OPERATION FLOW RATE 27,565 #/HR 122,270 24,574

TIME	10:00	10:15	10:30	10:45	11:00	
Return Oil Temperature	445	446	445	440	445	
Feed Oil Temperature	490	490	490	490	490	
Heater Inlet Temperature	890	896	888	891	890	
Heater Disch. Temperature	656	657	655	656	656	
Control Temperature Setpoint	490	490	490	490	490	
Oil Differential Pressure	NA	X	X	X	X	X
Heater Differential Press. Setpoint	NA	X	X	X	X	X
Tee Section Static Pressure	X	X	X	X	X	X
Main Circulating Pump Motor Load	X	X	X	X	X	X
Aux. Circulating Pump Motor Load	X	X	X	X	X	X

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

mEc COMPANY

TEST TYPE: FORM., CO, THC
LOCATION: PRESSVENT #5
No.: 2

Owner: L.P.
Test Personnel: R.G.T. & D.B.
Location: CLAYTON, AL
Plant Description: MDF
Date: 3-11-92

PROCESS INFORMATION

	TIME	11:14	12:27	12:44	12:59	1:14	THRUPUT SCALES
	Forming Line Speed FPM	28.8	28.8	28.8	28.8	28.8	13,550
	Board Thickness	3/8"	3/8"	3/8"	3/8"	3/8"	11,240
	Press ~~Cycle Time~~ ZONE 1	217°F	218°F	220°F	220°F	220°F	13,880
	~~Control~~ Oil Temp. ~~Setpoint (Press)~~ 2	217°F	217°F	217°F	217°F	217°F	11,540
	~~Press Circ. Pump #1 Motor Load~~ 3	213°F	213°F	213°F	213°F	213°F	13,200
GPM	~~Press Circ. Pump #2 Motor Load~~ RESIN	9.6	9.7	9.6	9.7	9.6	10620
1L P m	~~Press Circ. Pump #3 Motor Load~~ WAX	1700	—	1700	—	1700	14,780
	BIN LEVEL	HI	HI	HI	HI	HI	11,310
							15550
	FLOW RATE 28,429 #/HR						12,520
							128,210
							25,642

RAW MIX = 1 SHAVINGS / 1 CHIPS

5.74 257
578 257

HEATER OPERATION

TIME	12:14	12:27	12:44	12:59	1:14
Return Oil Temperature	445	445	446	445	445
Feed Oil Temperature	490	489	490	490	487
Heater Inlet Temperature	889	890	892	890	892
Heater Disch. Temperature	655	654	655	656	658
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure	↓	↓	↓	↓	↓
Main Circulating Pump Motor Load	↓	↓	↓	↓	↓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood/Burner Shell Temp.					
Wood Fuel Counter					

mEC COMPANY

TEST TYPE: FORM, CO, THC
LOCATION: PRESS VENT #5
No.: 3

Owner: L.P **Test Personnel:** RGT + O.B.

Location: CLAYTON, AL. **Plant Description:** MDF

Date: 3-11-92

PROCESS INFORMATION

	TIME	1:45	2:00	~~2:15~~	2:30	2:45	TRAYER SCALES
FPM	Forming Line Speed	~~28.8~~	~~28.8~~	28.8	28.8	28.8	14460
	Board Thickness	~~3/8"~~	~~3/8"~~	3/8"	3/8"	3/8"	11220
	~~Press Cycle Time~~ PRESS TEMP ZONE 1	~~219°F~~	219°F	219°F	219°F	219°F	19610
	~~Control Oil Temp. Setpoint (Press)~~ 2	~~217°F~~	217°F	217°F	217°F	217°F	13,000
	Press Circ. Pump #1 Motor Load 3	213°F	213°F	213°F	213°F	213°F	13,560
GPM	Press Circ. Pump #2 Motor Load	9.6	9.5	9.8	9.8	9.5	12,160
MLPM	Press Circ. Pump #3 Motor Load	1700	—	1700	—	1700	13,590
	DRY BIN LEVEL	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	Hi-Hi	10,050
	RAW MATERIAL MIX 1 SHAVINGS / 1 CHIPS					FLOW RATE 28,437 #/HR	12,220 / 11,230

578 ÷ 2 = 289

126,050 ÷ 5 = 25,225

HEATER OPERATION

TIME	1:45	2:00	2:15	2:30	2:45
Return Oil Temperature	495	495	496	496	496
Feed Oil Temperature	490	490	490	489	490
Heater Inlet Temperature	892	892	893	889	889
Heater Disch. Temperature	697	648	648	697	696
Control Temperature Setpoint	490	490	490	490	490
Oil Differential Pressure	NA	NA	NA	NA	NA
Heater Differential Press. Setpoint	↓	↓	↓	↓	↓
Tee Section Static Pressure	↓	↓	↓	↓	↓
Main Circulating Pump Motor Load	↓	↓	↓	↓	↓
Aux. Circulating Pump Motor Load	NA	NA	NA	NA	NA

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
~~Gas/Oil Heat Controller Output~~					
~~Flowing Gas/Oil Pressure After Req.~~					
~~Wood Heat Controller Output~~					
~~Wood Fuel Delivery, Volts~~					
~~Wood Air Signal, mA~~					
~~Wood Burner Shell Temp.~~					
Wood Fuel Counter					

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DRYER TEST DATA

DRYER NO. FACE

PRESS LINE #1

PM 10 PARTICULATE & CONDENSABLES

Tamb, °F: _____

PBAR, "Hg: _____

TEST #1

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	RPM Wood Burner VDC	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
10:15	78	160	124	~	~	925/1100			~	~	~	~~WOOD CHIPS COMBUSTION~~ ~~RECYCLING HOT OIL GAS~~	3
10:30	78	157	125	~	~	950/1050	21.0	8.8	~	~	~		2½
10:45	69	158	125	~	~	950/750			~	~	~		2
11:00	69	157	125	~	~	950/750	22.0	8.8	~	~	~		2
11:15	69	158	126	~	~	925/775			~	~	~		2
11:30	69	141	126	~	~	950/825			~	~	~		2

RAW MATL. MIX
3 SHAVINGS
1 CHIP
¼ SAW TRIM

PRODUCTION RATE
39,796 LBS./HR
FACE & CORE

Job No. _____ Location FACE CLAYTON, AL. Sht. No. 1 of 2

Customer LP

By RGT & D.B. Date 3-11-92

MEC COMPANY
Neodesha, Kansas U.S.A.

PM10 PARTICULATE & CONDENSABLES

mEC COMPANY

RAW MATL. MIX
3 SHAVINGS
1 CHIP
1/4 SAW TRIM

PRODUCTION RATE
39,796 LBS/HR.
FACE & CORE

Owner: L/P

Test Personnel: DB/RGT

Location: CLAYTON AL

Plant Description: MDF

Date: MARCH 11 1992

SHT. 2 OF 2

FACE DRYER
PRESS LINE #1
TEST #1

PROCESS INFORMATION

TIME						
✓ Forming Line Speed		42				
✓ Board Thickness		3/4				
✓ Press Cycle Time	10 MIN	7:20				
✓ Control Oil Temp. Setpoint (Press)		310				
✓ ~~Press Circ. Pump #1 Motor Load~~	RESIN	7.8			7.8	GPM
✓ ~~Press Circ. Pump #2 Motor Load~~	WAX	1400			1400	MLPM
~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

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DRYER TEST DATA
DRYER NO. FACE
PRESS LINE #1

PM 10 PARTICULATE & CONDENSABLES

Tamb, °F: _____
PBAR, "Hg: _____

TEST # 2

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	Wood Burner RPM VDC	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS DRY BIN WINDOWS
1:00	69	151	125	~	~	850/1050	25.0	8.6	~	~	~	~~WOOD FUEL CONDITION~~ ~~RECYCLING HOT OIL GAS~~ 2
1:15	69	144	123	~	~	850/700			~	~	~	2
1:30	69	147	123	~	~	850/600		8.4	~	~	~	1½
1:45	69	143	122	~	~	850/900			~	~	~	1
2:00	69	145	123	~	~	850/800	24.8	8.6	~	~	~	1
2:15	69	146	123	~	~	850/775			~	~	41,300	1

PRODUCTION RATE
39,525 LBS/HR
FACE & CORE

RAW MATL. MIX
3 SHAVINGS
1 CHIP
¼ SAWTRIM

MEC COMPANY
Neodesha, Kansas U.S.A.

Job No. MDF Location FACE CLAYTON AL Sht. No. 1 of 2
Customer LP
By DB/RGT Date 3/11/93

mEC COMPANY

PM 10 PARTICULATE & CONDENSABLES

RAW MATL. MIX
3 SHAVINGS
1 CHIP
1/4 SAW TRIM

PRODUCTION RATE
39,525 LBS./HR.
FACE & CORE

Owner: L/P

Test Personnel: DB/RGT

Location: CLAYTON, AL

Plant Description: MDF

Date: MARCH 11, 1992

SHT. 2 OF 2

FACE DRYER
PRESS LINE #1
TEST #2

PROCESS INFORMATION

	TIME						
✓	Forming Line Speed	44					
✓	Board Thickness	34					
✓	Press Cycle Time	7:00					
✓	Control Oil Temp. Setpoint (Press)	310					
✓	~~Press Circ. Pump #1 Motor Load~~ RESIN	7.8					GPM
✓	~~Press Circ. Pump #2 Motor Load~~ WAX	1,400					MLPM
	~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME						
Return Oil Temperature						
Feed Oil Temperature						
Heater Inlet Temperature						
Heater Disch. Temperature						
Control Temperature Setpoint						
Oil Differential Pressure						
Heater Differential Press. Setpoint						
Tee Section Static Pressure						
Main Circulating Pump Motor Load						
Aux. Circulating Pump Motor Load						

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME						
Gas/Oil Heat Controller Output						
Flowing Gas/Oil Pressure After Reg.						
Wood Heat Controller Output						
Wood Fuel Delivery, Volts						
Wood Air Signal, mA						
Wood Burner Shell Temp.						
Wood Fuel Counter						

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DRYER TEST DATA

DRYER NO. FACE

PRESS LINE #1

PM10 PARTICULATE & CONDENSABLES

Tamb, °F: _____

PBAR, "Hg: _____

TEST # 3

TIME	REFINER FEED %	TG_1 °F	TG_2 °F	Wood Burner PD	Wood Burner mA	RPM ~~VBC~~	MC_1 %	MC_2 %	PRODUCT TP_1 °F	PRODUCT TP_2 °F	AIR FLOW ACFM	REMARKS	DRY BIN WINDOWS
3:15	69	150	123	~	~	850/65	25.6	10.2	~	~	~	~~WOOD FUEL CONVEYOR~~ ~~RECYCLING HOT OIL GAS~~	1
3:30	69	142	122	~	~	850/1050		9.8	~	~	~		1
3:45	69	155	124	~	~	850/60			~	~	~		1
4:00	67	145	122	~	~	850/550	25.4	9.6	~	~	~		1
4:15	68	151	123	~	~	900/550		10.0	~	~	~		1
4:30	69	159	124	~	~	900/575		10.0	~	~	40,800		1

RAW MAT'L. MIX
3 SHAVINGS
1 CHIP
1/4 SAW TRIM

PRODUCTION RATE
41,506 LBS/HR
FACE & CORE

Job No. MDF Location FACE CLAYTON, AL Sht. No. 1 of 2

By DB/RGT Date 3/11/92

Customer L/P

MEC COMPANY
Neodesha, Kansas U.S.A.

mEC COMPANY

PM10 PARTICULATE & CONDENSABLES

RAW MATL. MIX	PRODUCTION RATE
3 SHAVINGS	41,506 LBS./HR.
1 CHIP	FACE & CORE
1/4 SAWTRIM	

Owner: L/P **Test Personnel:** DB/RGT

Location: CLAYTON, AL. **Plant Description:** MDF

Date: MARCH 11, 1992 SHEET 2 OF 2

FACE DRYER PRESS LINE #1 TEST #3

PROCESS INFORMATION

TIME						
✓ Forming Line Speed	44					
✓ Board Thickness	3/4					
✓ Press Cycle Time	7:00					
✓ Control Oil Temp. Setpoint (Press)	310°					
✓ ~~Press Circ. Pump #1 Motor Load~~ RESIN	7.9	7.8	7.8	7.9	7.8	GPM
✓ ~~Press Circ. Pump #2 Motor Load~~ WAX	1440					MLPM
~~Press Circ. Pump #3 Motor Load~~						

HEATER OPERATION

TIME					
Return Oil Temperature					
Feed Oil Temperature					
Heater Inlet Temperature					
Heater Disch. Temperature					
Control Temperature Setpoint					
Oil Differential Pressure					
Heater Differential Press. Setpoint					
Tee Section Static Pressure					
Main Circulating Pump Motor Load					
Aux. Circulating Pump Motor Load					

BURNER OPERATION (Automatic Control Unless Noted "M")

TIME					
Gas/Oil Heat Controller Output					
Flowing Gas/Oil Pressure After Reg.					
Wood Heat Controller Output					
Wood Fuel Delivery, Volts					
Wood Air Signal, mA					
Wood Burner Shell Temp.					
Wood Fuel Counter					

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3-10-92 Shift A [illegible] Pressing Cycle

Foreman [illegible] Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
7/16	49x04	AIF	22[illegible]			22[illegible]

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			100	7-15 [illegible]
				[illegible]
				Back [illegible] Press [illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			118	118

Comments: Footage - 42,078.5

[illegible] 86.7

[illegible] 0

[illegible] 0

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton AL

Date 3-10-92 Shift C-2 Pressing Cycle

Foreman Mike Hours 3:00 - 11:00 Total Cycle

Lee

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
7/16	49 X 97	AIF	2336			2336
7/16	49 X 85	DAnville	178			178
7/16	49 X 73	DAY	430			430
7/16	61 X 97	Component	103			103

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				NO DOWN TIME
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	0	0	0

Comments: Footage - 54,933.5

R/u - 87.0

Metal mat -

Mat weight

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clifton Ark

Date 3-11-92 Shift B2 Pressing Cycle

Foreman Robert Hours 11:00 - 7:00 Total Cycle

Derek

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
7/16	61x97	Component	615			615
.472	49x97	L.P.	495			495
3/8	61x97	Harden	1240			1240

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			14	12:47-1:01 - Changed Wedges To .472
			17	2:37-2:54 - Changed Wedges To 3/8
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			31	31

Comments:

Footage - 49,117.9

R/U - 86.5

Net Weight - 0

Metal Net - 0

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton Ala.

Date 3-11-92 Shift A-2 Pressing Cycle

Foreman Mickel Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/8	[illegible]	Hardboard	2425			2425
3/8	[illegible]	VTI	172			172

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	6			12-52 - 2-55 Trouble at saw Line
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				6

Comments: Footage - 51,252 ✓

[illegible] - 89.8

[illegible] - 0

[illegible] - 0

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton Al.

Date 3-11-92 Shift 3-2 Pressing Cycle

Foreman Mike Lee Hours 3:00 - 11:00 Total Cycle

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
3/8	49X97	V.T.I.	3260			3260

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
		15		5:35-5:50 Went Down to
				Come Back UP on Both Sides.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	15	0	15

Comments: Footage - 52,160

R/u - 86.6

Metal Mat -

Mat Weight -

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3,11,90 Shift D-2 Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Mark Martin

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/5	49 X 97	VTI	1716			1716
3/8	49 X 100	Mobilsaff	1036			1036
3.5	49X121	VTI	286			286
3/8	49X145	VTI	162			162

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				None

Comments: Sq. ft. 54,158 ✓
RM 86.0

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location Clanton Ala

Date 3-12-92 Shift H 2 Pressing Cycle

Foreman [illegible] Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
5/8	49 X 145	VTI	128			128
.354	49 x 9[illegible]	L.P.	118			118
[illegible]	[illegible]	ALF + [illegible]	1580			1580
1/4	49 x 97	mills	1646			1646

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			14	7:23-7:37 [illegible]
				[illegible] 1/4
	4			9:51-9:55 SERVO [illegible]
		5		12:41-12:46 [illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	4	5	14	23

Comments: Footage - 43,474.8

[illegible] - 101.3

[illegible] 11

[illegible]

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton Fl.

Date 5-12-92 Shift C-2 Pressing Cycle

Foreman Mike Lee Hours 3:00-11:00 Total Cycle

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
1/4	49 X 97	Mills	664			664
1/4	49 X 97	Domtar	1062			1062
1/4	61 X 97	AIF & United	1574			1574
1/4	61 X 97	Domtar	304			304
5/16	49 X 97	Danville	110			110

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			11	10:11-[illegible] Changed [illegible] to 5/16
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			11	11

Comments: Footage - 44,918

R/u - 759

Metal mat -

Mat weight - 1

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3,12,92 Shift D-2 Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Mark Martin

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
5/16	49 x 97	Danville	1940			1940
5/16	49 x 95	Colwood	234			234
3/16	49 x 97	Dual	1,116			1,116
3/16	61 x 97	Hardi	437			437

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			18	2:57 to 3:15 Closed [illegible]
				to 3/16, [illegible]
				[illegible] limits.
			43	4:59 to 5:42 Reversed the
				Refiner and went to SNE System.
				welded one crack.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			61	61

Comments: Sq ft = 41,~~804~~ 778

Sq ft - 995

Attachment-1

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clanton Ala.

Date 3-13-92 Shift A-2 Pressing Cycle

Foreman Mickey Hall Hours 7-3 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/16	61 X 94	Hardin	2366			2366
3/16	50 X 98	Columbia	1166			1166

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			6	7-25-731 Went Down to repair [illegible]
				[illegible]
			19	1-41-200 Emergency stop
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			25	25

33,282

Comments: Footage - ~~32,988~~

R/u - 128.9

mat weight -

metal prep -

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clifton, AZ

Date 3-13-92 Shift B Pressing Cycle

Foreman Robert Hours ~~11:40-2:00~~ 3- Total Cycle

Derek

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
3/16	50x98	Columbia	1272			1272
3/16	49x97	Dai	3600			3600

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			20	5:26-5:46 - Adjusted wedges on 3/16
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			20	20

Comments: Footage - 39,796

F/s - 111.6

Not wait - 4.0

Not ~~4.4~~ .0

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Chester

Date 3/13/92 Shift 6-2 Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Mark Martin

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/16	49x97	Day	1,817			1,817
3/16	49x97	AKIMSTIM	3,051			3,051

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			15	6:26 to 6:41 Changed inverter's to 3/8.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			15	15

Comments: Sq. ft. 38,944
RU - 114.9

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton Al.

Date 3-14-92 Shift 2-3 Pressing Cycle

Foreman Mike Hours 7:00 - 3:00 Total Cycle

Thickness & Density	Rough Size	~~Loads Produced~~ Lee	Panels Produced	Waste	Test	Net Panels Produced
3/16	49 X 97	Arnstion	44			44
3/8	49 X 97	Harden	3010			3010

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	25			10:23 - 10:48 Down Chain Came
				off Dry Bin Leveling Screws +
				Pump & Weight Belt
3				10:50 - 10:53 Bottom Press Belt
				Tracked off Two Time
		13		11:51 - 12:04 Went Down to
				Come up on Both Systems
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
3	25	13	0	41

Comments: Footage - 48 : 2

R/A - 91.9

Metal Mat -

Mat [illegible] -

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton, Ala

Date 3-14-92 Shift B2 Pressing Cycle

Foreman Robert Derek Hours 3:00-11:00 Total Cycle

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
3/8	49X97	Harden	873			873
3/8	49X121	H&K	386			386
3/8	49X145	H&K	360			360
3/8	61X97	Harden	1414			1414

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No Down Time
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: Footage - 58,608

Bin - 84.7

Net Weight - 0

Metal Wt - 0

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3.[illegible] Shift [illegible] Pressing Cycle

Foreman [illegible] Hours [illegible] Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/8	61x97	Hardon	1,351			1,351
3/16	49x97	[illegible]	356			356
3/16	49x[illegible]	Dry	1,370			1,370
3/16	49x121	Capitoline	302			302
3/16	49x145	Capitoline	174			174

DOWNTIME REPORT

Record in Minutes				
Elect.	Mech.	Operators	Other	Explain-Reasons
			21	2:34 to 2:55 [illegible]
				[illegible]
				[illegible]
	2			2:57 to 2:59 Too [illegible]
				belt tracked off.
7				5:31 to 5:38 Trouble [illegible]
				burner head plugged
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
7	2		21	30

Comments:

[illegible] - 44.6[illegible]

[illegible] - 97.2

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton Al.

Date 3-15-92 Shift C-2 Pressing Cycle

Foreman Mike Hours 7:00-3:00 Total Cycle

Lee

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
3/16	49 X 145	Capitoline	134			134
3/16	55 X 128	Panel	740			740
3/16	42 X 128	Panel	732			732
3/16	61 X 81	Panel	1026			1026
3/16	37 X 81	Panel	1031			1031

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
		2		2:12-2:15 Photo EYE Press mat too High
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	2	0	2

36,378

Comments: Footage - ~~37,778~~

R/u - 130.5

Metal mat-

mat [illegible]

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location Clayton AL

Date 2-15-92 Shift C-2 Pressing Cycle

Foreman mike Hours 7:00-3:00 Total Cycle

Lee

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/16	61 X 76	PANEL	451			451
3/16	37 X 76	PANEL	451			451

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments: Footage -

R/u -

Metal mat -

Mat weight -

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location Clayton N.P.

Date 3-15-92 Shift B2 Pressing Cycle

Foreman Robert Hours 7 A.M.-11:00 Total Cycle

Derek

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
3/16	61 X 76	Panel	149			149
3/16	37 X 76	Panel	149			149
7/32	49 X 97	Sequoia	484			484
7/32	49 X 85	Constitution	1802			1802
7/32	50 X 98	Temple	2390			2390

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No Down Time
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: Footage - 44,172

Plu - 105.1

Net Weight - 0

Metal Wt. - 0

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3,15,92 Shift D-3 Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Nick Fleetin

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
7/32	50x94	Temple	756			756
.225	49x121	Panel	1,350			1,350
.275	49x157	Land	1,020			1,020
.225	49x97	Willamette	578			578

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
7				2:36 to 2:43 Printer, Emerson
				STR[illegible]
				C[illegible]
				[illegible] before press
				would start
	3			5:48 to 7:01 Tec [illegible]
				press hall [illegible] off
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
7	3			10

Comments: Sq. ft. 45,030

DM - 1036

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton AL

Date 3-16-92 Shift C-2 Pressing Cycle

Foreman Mike Hours 7:00-3:00 Total Cycle

Lee

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
225	49X97	Willamette	396			396
1/4	49X97	Donsco	3728			3728

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			39	7:21 - 7:00 (hanged [illegible] to 1/4 + [illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	0	39	39

Comments: Footage - 43,568

R/U - 97.5

Metal mat -

mat [illegible] -

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3-16-92 Shift R2 Pressing Cycle

Foreman Mike Kedrge Hours 3:00-11:00 Total Cycle

Dennis

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
1/4	49X97	PONSCO	2444			2444
1/4	49X85	WOODTEK	2000			2000

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			8	10:08-10:16 - Run out of food
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			8	8

Comments: Footage - 44,738

B/U - 102.8

Metal Detect - 0

Metal Mat - 0

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton

Date 3/16/87 Shift D-2 Pressing Cycle

Foreman George Hours 11-7 Total Cycle

Mark Martin

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1/4	49 x 45	Hardtek	495			495
1/4	61 x 97	Hardtek	1,730			1730
7/16	49 x 97	AIF	872			872

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			14	3:35 to 3:49 Changed [illegible] to 7/16.
	2			3:52 to 3:54 bottom [illegible] 6-4 [illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	2		14	16

Comments: Sq. ft - 43,824

M - 965

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton, Ill.

Date 3-17-92 Shift C-2 Pressing Cycle

Foreman Mike Hours 7:00 - 3:00 Total Cycle

Lee

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
7/16	49 x 97	A-E	2876			2876

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				NO DOWN TIME
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	0	0	0

Comments: Footage - 53,655

R/u - 879

Metal mat -

Mat [illegible] -

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton, Ala

Date 3-17-92 Shift B2 Pressing Cycle

Foreman Nathan Hours 3:00-11:00 Total Cycle

Derek

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
7/16	49x97	AIF	2668			2668
7/16	49x110	AIF	278			278

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No Downtime
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: Footage - 55,695

Plies - 881

Metal Wet - 0

Metal Dry - 0

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date [illegible] Shift [illegible] Pressing Cycle [illegible]

Foreman George Hours [illegible] Total Cycle [illegible]

Nick Martin

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
7/16	[illegible]	HIF	1508			1508
7/16	49 x 73	AIF	946			946

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			100	5:20 to 7:00 Down to [illegible]
				Mew plate in the [illegible]
				included two [illegible] also.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			100	100

Comments: Sq. ft - 45,255

DLL - 83.2

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3-18-92 Shift C-2 Pressing Cycle

Foreman Mike Hours 7:00-3:30 Total Cycle

Lee

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
7/16	49 X 73	A.I.E.	282			282
7/16	49 X 85	Whiteville	360			360
7/16	49 X 121	OBM	[illegible]			[illegible]
7/16	49 X 145		90			90
1/2	49 X 97	Donsco	648			[illegible]

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			[illegible]	7:30-7:31 Down From [illegible]
				Shift Changed Plates
		8		[illegible] Mat Weight Trouble
				Current Diff. too High Press
			15	12:15-12:30 Changed [illegible] to 1/2
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	8	46	54

Comments: Footage - 46,935'

[illegible] - 924

[illegible]

[illegible] - 1

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Citronelle, Ala.

Date 3-18-92 Shift B2 Pressing Cycle

Foreman Nathan Hours 3:00-11:00 Total Cycle

Derek

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
1/2	49x97	Dwsco	2725			2725

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No Downtime
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total

Comments: Entage - 56.13%

Rlu - 87.6

Mat Defect - 0

Total Mat - 0

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton Ala.

Date 3-18-92 Shift A-2 Pressing Cycle

Foreman Nathan Stone Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1/2	49x97	Donsco	2260			2260

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	70			1:33-2:43 [illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	70			70

Comments: Footage - [illegible]

Rip - 89.4

mat weight -

metal mats -

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton [illegible]

Date 3-19-92 Shift C-2 Pressing Cycle

Foreman Mike Hours 7:00 - 3:00 Total Cycle

Lee

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
1/2	49 X 97	Dongco	2650			2650

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				NO DOWN TIME.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	0	0	0

Comments: Footage - [illegible]

R/U - 873

[illegible]

[illegible]

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3-19-92 Shift [illegible] Pressing Cycle _____

Foreman [illegible] Hours [illegible] Total Cycle _____

[illegible]

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
1/2	49x97	Dawsco	324			324
1/2	49x98	Southern	162			162
1/2	49x85	Whitmyle	264			264
1/2	49x109	Plains	740			740
1/2	49x97	R. Weed	1030			1030

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				[illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: [illegible] 55.06%

[illegible] 89.8

[illegible]

[illegible]

SD 5344

Louisiana-Pacific Co.,oration

PRESS REPORT AND DOWNTIME

Location [illegible]

Date [illegible] Shift A-2 Pressing Cycle

Foreman [illegible] Hours [illegible] Total Cycle

Jeff

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
1/2	[illegible]	R. Weed	1514			1514
5/8	49 x 121	AIF	292			292
5/8	[illegible]	Frisco	334			334

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			16	[illegible] 5:26 crossed [illegible] to -
				5/8.
11				4:54-5:05 · #2 Wood Bunker
				flamed out, wouldn't start Sor's
				Dust screw tripped out.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
11			16	27

Comments: Employee - 50.939

R/U - 96.1

[illegible] - 0

[illegible] - 1

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clayton Al

Date 3-20-92 Shift C-2 Pressing Cycle

Foreman Mike Lee Hours 7:00 - 3:00 Total Cycle

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
5/8	49 X 97	Frisco	2078			2078

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				NO DOWN TIME.
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
0	0	0	0	0

Comments: Footage - 55 ft

R/U - 94.3

Metal mat -

Mat weight -

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3.20.92 Shift [illegible] Pressing Cycle _____

Foreman [illegible] Hours 3-11 Total Cycle _____

Mark Martin

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
5/8	49 x 97	Frisco	2,068			2,068

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
	8			6:09 to 6:17 Flying Saw [illegible]
				[illegible]
				[illegible]
				[illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
	8			8

Comments: Sq. ft. - 55,144
RM - 965

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location Clarion Ala.

Date 3-20-92 Shift A-2 Pressing Cycle

Foreman [illegible] Hours [illegible] Total Cycle

Jeff

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
5/8	49 x 97	Frisco	326			326
5/8	49 x 98	Sequoia	126			126
5/8	49 x 115	Mason	210			210
5/8	49 x 121	AIF	584			584
5/8	61 x 97	Frisco	370			370

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			30	5:21 - 5:31 Went down to reverse
				refiner.
9				5:32-5:41 current diff. too
				high press. (short matin press)
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
9			30	39

Comments: Footage - 50,537

R/U - 91.9

mat [illegible] - D

[illegible] - D

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3-2-92 Shift Pm Pressing Cycle

Foreman Robert Shift Hours 7m-3:00 Total Cycle

Derek

Thickness & Density	Rough Size	~~Loads Produced~~	Panels Produced	Waste	Test	Net Panels Produced
5/8	61X97	FRISCO	1625			1625

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
				No Down Time
				Ø
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: Footage 54.16$

[illegible] 947

[illegible] Wash

Metal Mfr

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date [illegible] Shift [illegible] Pressing Cycle _____

Foreman [illegible] Hours [illegible] Total Cycle _____

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/8	[illegible]	[illegible]	702			702
3/4	[illegible]	[illegible]	[illegible]			[illegible]

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
			[illegible]	[illegible]
				[illegible]
				[illegible]
				[illegible]
				[illegible]
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
			[illegible]	[illegible]

Comments: Sq. ft. 51,238 RU 96.4

SD 5344

Louisiana-Pacific Corporation

PRESS REPORT AND DOWNTIME

Location [illegible]

Date 3-21-92 Shift A-2 Pressing Cycle

Foreman [illegible] Hours 11-7 Total Cycle

Thickness & Density	Rough Size	Loads Produced	Panels Produced	Waste	Test	Net Panels Produced
3/4	61 X 97	Frisco	1097			1097
3/4	61 X 109	Darling	72			72
3/4	[illegible]	[illegible]	72			72
3/4	[illegible]	Stevens	48			48
3/[illegible]	[illegible]	Stevens	48			48

DOWNTIME REPORT

Record in Minutes				Explain-Reasons
Elect.	Mech.	Operators	Other	
Total Elect.	Total Mech.	Total Operators	Total Other	Grand Total
				0

Comments: Footage - 52,[illegible]

3/4 - 98.9

[illegible] weights - 0

[illegible] - 0

SD 5344

APPENDIX J

PROJECT PARTICIPANTS

Louisiana Pacific

James T. Boswell, Corporate Director of Environmental Controls
Billy Adams, Plant Contact

Industrial & Environmental Analysts, Inc.

Jeff Burdette, Project Manager
Tommy Thompson, Field Team Manager
David Prater, Team Leader
Jay Morgan, Technician
Rodney Morgan, Technician
Barry Rayfield, Team Leader
John Malone, Technician
Steve Terll, Technician