

AP42 Section:	9.12.2
Title:	Emission Factor Documentation for AP-42 Section 9.12. Wines And Brandy Final Report October 1995 APPENDICES ONLY

Emission Factor Documentation for AP-42
Section 9.12.2

Wines and Brandy

Final Report

For U. S. Environmental Protection Agency
Office of Air Quality Planning and Standards
Emission Factor and Inventory Group
Research Triangle Park, NC 27711

Attn: Mr. Dallas Safriet (MD-14)

Appendices only

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October 1995

APPENDIX A.

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STATE OF CALIFORNIA
AIR RESOURCES BOARD



EVALUATION TEST
TO MEASURE ETHANOL
EMISSIONS FROM A
106,000 GALLON FERMENTATION TANK

Stationary Source Control Division

ENGINEERING EVALUATION BRANCH
C-80-071
REPORT NO. _____

OCTOBER 1980

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SUMMARY

A 106,000 gallon fermentation tank filled with 90,000 gallons of must to produce a white blending wine was tested for 159 hours during which ethanol emissions were continuously monitored. Carbon dioxide (CO₂), oxygen (O₂), temperature, and exhaust gas volumes were also measured.

Fermentation exhaust gas temperatures were a constant 53°F.

The average ethanol concentration was 3,640 parts per million (ppm). Based on this concentration and a total measured gas volume of 310,060 ft³, the estimated mass of ethanol emitted to atmosphere was 137 lbs in 159 hours. This corresponds to a mass emission rate of approximately 0.86 lbs/hr. or, when expressed in terms of gallons of wine juice fermented, 1.52 lbs/10³ gal.

Other exhaust gas components and their determined concentrations are:

CO ₂	99.6%
H ₂ S	1.1 ppm
SO ₂	<.2 ppm
CH ₃ SH	<.006 ppm

No oxygen was detected in the exhaust gas.

IV. TEST METHODOLOGY & EQUIPMENT

All emission measurements were taken at the fermentation tank vent hatch. The hatch was fitted with an adaptor to which a turbine meter was attached. Ports on the adaptor accommodated (1) the sample line for continuous gaseous measurements, (2) a thermocouple for exhaust gas temperature measurements, and (3) a pitot tube for velocity pressure measurements. Exhaust gas volume was metered through the turbine and the volumetric rate determined by dividing the exhaust gas volume by the corresponding time interval during which the volume was measured. This was cross checked by pitot tube measurements and ARB Method 1-2, "Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)." Oxygen (O₂), carbon dioxide (CO₂), and ethanol (C₂H₅OH) concentrations were continuously measured by analyzers located inside a mobile van parked at the base of the fermentation tank. A heated sample line was used to prevent condensation as the sampled gas was being drawn from the vent hatch to the van.

The evaluation test equipment used and the sampling site where the measurements were taken are identified in Figure 4. The arrangement of the turbine meter and the adaptor is illustrated in Figure 5.

The parameters monitored and the measurement methods used are listed below:

Total Hydrocarbons: A Beckman Model 400 continuous analyzer measured hydrocarbon concentrations with a flame ionization detector (FID). The analyzer was calibrated with propane and a response factor to ethanol was determined.

Oxygen: Oxygen was measured with a Beckman Model F-3 continuous O₂ analyzer equipped with a paramagnetic detection system.

Carbon Dioxide: An Anarad Model 500 analyzer with a nondispersive infrared detector (NDIR) continuously monitored CO₂ concentrations.

Grab Samples: Grab samples of the exhaust gas were taken in 2 liter glass flasks and analyzed for total hydrocarbon, ethanol, CO₂, O₂, sulfur dioxide (SO₂), hydrogen sulfide (H₂S), and methyl mercaptan.

V. DISCUSSION OF RESULTS

The fermentation of 90,000 gallons of St. Emillion grape juice took 216.5 hours, starting on October 13, 1980 at 7:30 a.m. and ending on October 22, 1980 at 8:00 a.m. The fermentation process was initiated by the inoculation of the grape juice with yeast. The degrees Brix measured with a hygrometer at the time of inoculation was 20.5. The Brix scale is a measure of the concentration of sugar in solution as grams of sucrose per 100 grams of liquid. Two methods are typically used for making this determination: the hygrometer procedure and the refractometer procedure. The methodology involved with both procedures is presented in Appendix II. The fermentation was judged to be complete by United Vintner's winemaker when the degrees Brix was reduced to 2.

The ARB evaluation test began on October 15 at 5:00 p.m., 57.5 hours after the inoculum was introduced into the tanks. The duration of the evaluation test was 159 hours, representing data collection for 73 percent of the fermentation process. During the test period, the following parameters were monitored: CO_2 , O_2 , and ethanol concentrations in the exhaust gas; ambient and exhaust gas temperatures; exhaust gas volumetric flow rate.

The exhaust gas was predominately composed of carbon dioxide and ethanol, with trace amounts of hydrogen sulfide, sulfur dioxide and mercaptans. As expected from an anerobic process, measurable amounts of oxygen were not present. Table II lists

the exhaust gas components in descending order with respect to their measured concentrations averaged over the test period.

TABLE II
FERMENTATION TANK EXHAUST GAS COMPONENTS

Exhaust Gas Component	Concentration
CO ₂	99.6%
C ₂ H ₅ OH	0.4%
H ₂ S	1.1 ppm
SO ₂	< .2 ppm
CH ₃ SH	< .006 ppm

Analysis of the exhaust gas by continuous analyzers showed ethanol concentrations to increase steadily with respect to time while CO₂ remained constant. The ethanol concentration increased from 1,902 parts per million at the beginning of the test to 4,565 ppm at the end of the test. The end of the ARB's evaluation test coincided with the completion of the fermentation process. The average ethanol concentration over the 159 hour test period was approximately 3,640 ppm. Measured values of CO₂ concentration remained at over 99 percent throughout the test period while, in contrast, no oxygen was detected.

Based on an averaged ethanol concentration value of 3,640 ppm and a total measured exhaust gas volume of 310,060 ft³, the estimated

mass of ethanol emitted to atmosphere during the fermentation process was 137 pounds (lbs) in 159 hours. This corresponds to a mass emission rate of approximately 0.86 lbs/hr. Alternatively, when expressed in terms of gallons of wine juice fermented, the emission rate is approximately $1.52 \text{ lbs}/10^3 \text{ gal}$. This compared closely with an ethanol emission factor of $1.45 \text{ lbs}/10^3 \text{ gal}$ calculated per an equation cited in the Environmental Protection Agencies' publication entitled, "Compilation of Air Pollutant Emission Factors", commonly referred to as AP-42. The calculation and AP-42 equation are presented in Appendix III.

A composite plot of ethanol concentration and emission rate versus time is presented in Graph I. As previously mentioned, exhaust gas ethanol concentrations steadily increased during the test. Correspondingly, ethanol emission rates were decreasing. The diminishing emission rates were attributed to the dominance of declining exhaust gas volumetric flow over increasing concentrations as the fermentation process approached completion. Graph II illustrates the change in flow rates with respect to time.

Ambient and exhaust gas temperatures are plotted on Graph III. Ambient temperatures varied diurnally while the exhaust gas temperatures remained relatively constant. Exhaust gas temperatures reflected the constant tank temperatures to which the fermenting must was subjected.

APPENDIX B.

FINAL REPORT

CHARACTERIZATION OF ETHANOL EMISSIONS FROM WINERIES

Submitted to:

Research Division
California Air Resources Board

on

July 19, 1982

By:

EAL Corporation

Principal Investigators:

Mr. David R. Fielder (Technical Services Manager)
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Reference:

Mr. Joseph A. Pantalone (Contract Officer)
California Air Resources Board Agreement
No. AO-071-31

EAL Work Order No. 64-6003

METHODS

Sample Collection

An extraction method was employed in which a known volume of gas, withdrawn from the fermentation exhaust stream, was bubbled through a series of three large Greenburg-Smith impingers. The first two impinger collections were separated from the third in order to verify an acceptable collection efficiency.

EAL personnel had previously conducted a large scale emission test of an acetator tank in Oakland, California. The process involves heating a solution of 6% acetic acid and 6% ethanol to 86°F while blowing air through it at a rate of 170 m³ per hour over a 32 hour period. Oxidation of the ethanol occurs to produce an end product containing 12% acetic acid and 0.5% ethanol. These conditions closely approximate those of a wine fermentation tank.

Our sampling train for the acetator test consisted of a set of three impingers containing 100 mL each of a 0.1M NaOH solution (NaOH added to assist acetic acid absorption). Subsequently, the contents of the first two impingers were analyzed separately from that of the third to check absorption (capture) efficiency. The first four samples collected, during the initial high alcohol content portion of the cycle, had an average collection efficiency of 92% in the first two impingers. This information, coupled with the statistical evaluation of impinger collection efficiencies contained in the JAPCA article "Estimating Overall Sample Train Efficiency" demonstrates that for the complete three impinger train, an overall collection efficiency of greater than 99% was achieved⁽¹⁾.

A sample interface and all connections were made of glass and teflon. A thorough leak-check of the collection train was performed prior to each test at a 10" Hg vacuum for sixty seconds with a maximum tolerance of 0.02 ft³ of volume change. The sampling rate (cubic feet/min, cfm) test duration and dry gas meter conditions were carefully monitored (Ref. Figure 1). All the procedural items considered, the collection method had the advantage of simplicity, proximity to the source (minimizing ethanol wall losses and chances of leaks with a long sample line), and virtually no problem with entrained moisture.

Ethanol Analysis

The determination of ethanol concentrations (ppm v/v (aq)) in the impinger collections was accomplished by gas chromatography. An aliquot was directly injected onto an FFAP column and ethanol was quantified with a flame ionization detector operating at a lower detection limit of 5 ppm by weight, (Ref. Sample Calculations in Appendix). This lower detection limit corresponds to a 0.4 ppm by volume concentration in the gaseous phase.

Fermentation Exhaust Volumetric Flow Rate

The fermentation exhaust flow rates for the red and white wine tanks were measured with a turbine meter (totalizer) provided by the California Air Resources Board (CARB). Hourly readings were taken throughout the duration of the fermentation periods.

Quality Assurance

Sample integrity was maintained by strictly controlling containment, identification, and shipping of the samples. Directly following each impinger collection, the absorbing solution was transferred to clean polyethylene bottles. Oxidation of ethanol was prevented by purging the minimal head-space with carbon dioxide. The sample bottles were then labeled as to run number, time, location and finally refrigerated and/or placed on ice for shipment to EAL for immediate analysis.

Impinger collection train efficiency was monitored in the field by periodically obtaining a gas grab bag from the train exhaust and analyzing the contents with a Draeger tube. Ethanol breakthrough was not indicated at a lower detection limit of 2 ppm by volume.

The sampling and exhaust monitoring methods called for the use of only two measurement devices, which were the gas turbine and dry gas meters.

Fugitive Emissions

Samples were collected for fugitive ethanol emissions using the same impinger train illustrated in Figure 1, omitting the sample line and locating the train in selected sites for area sampling.

Analytical procedures were identical to those mentioned for source sampling.

A number of process handling procedures were evaluated and ethanol fugitive emissions estimated based on building ventilation and production activity during testing.

The United Vintners Madera facility was chosen for initial source testing. Mr. Kaz Sanbongi was extremely helpful in providing fermenter tank fitting adapters to facilitate connection of our test apparatus. In addition, both Mr. Sanbongi and Mr. Joe Rossi, winemaker, were able to arrange fermentation schedules and procedures which assisted our personnel with their tests.

The first tank tested was for white wine in number 576, a stainless steel tank with a capacity of 350,136 gallons. The major problem encountered with this test was that the record breaking prematurity of the crushing season throughout California, coupled with an unusually small harvest, meant that it was almost too late to get any white wine grapes to test⁽⁶⁾. Also, the daily amount of grapes crushed was so low that must was typically being added to fermentation tanks throughout the fermentation period to achieve a reasonable final fermentation volume. Adding fresh must during a test would have seriously jeopardized the usefulness of the data. This scheduling/production volume problem was a factor throughout the white wine testing phase. The testing team was faced with both an unexpected schedule and the necessity, through lack of choice, to test fermentation batches that were less than ideal due to accessibility and mechanical arrangement or because the batch subsequently did not follow ideal fermentation behavior. With the assistance of the U.V. personnel mentioned, we obtained a full tank of must by combining some cold unfermented must stored from the previous day's crush with ambient temperature must obtained that day. Testing commenced at 7 a.m. on September 9, 1981, and was completed at 12 noon on September 16, 1981. All samples were successfully shipped and analyzed.

The red wine fermentation tank chosen for testing had a capacity of 128,000 gallons. The tank was filled and inoculated on September 14, 1981, and testing commenced immediately. Due to our desire to measure the total emission volume from this tank, we attached the 6-inch ARB turbine meter to one of the 4-inch sampling ports, closed the 2-foot manhole cover, and relied on the remaining 4-inch pressure relief valve to protect the tank in case of over pressurization. Normally, the manhole is left open throughout the fermentation process. Our procedures and installation were observed by

U.V. personnel with no objections. We believed that in the event that the turbine meter flowrate capacity was exceeded, excess exhaust gas would escape through the pressure relief valve. However, instead of a relatively harmless release of vent gases, the fermenting must foamed over and shot out through both the turbine meter and pressure relief valve at approximately midnight Tuesday evening, September 15, 1981. An estimated 1,000 gallons of must were lost and U.V. personnel aborted the fermentation, and our test, the next morning. Subsequently, it became apparent that with the sudden release in pressure caused by the relief valve opening, the must acted like champagne and essentially "boiled over." This mishap placed a serious strain on our relations with U.V. personnel, although no one had foreseen this occurrence.

Joe Rossi felt committed to our achieving a successful red wine test and agreed to arrange a second attempt. A similar tank was fitted with both ARB turbine meters, one on the sampling port and one on the pressure relief valve port (with the valve removed). The second turbine meter had just become available due to completion of the white wine test. In addition, the manhole cover was to be opened periodically for a few seconds throughout the test to guard against the initiation of foaming. Exhaust flow measurements were taken frequently to allow interpolation of exhaust volumes over the brief periods that the hatch was lifted. This test was completed successfully.

Detailed results of these tests are contained in the following figures and tables.

TABLE 2
PHYSICAL PARAMETERS
Tank #576
White Wine Fermentation

Tank Material: Stainless Steel

Fermentation Tank Dimensions

12 inch bottom cone

24 inch top cone

480 inch shell (height)

Gallons per inch = 711.4

Total tank capacity = 350,110 gallons

Actual capacity = 280,000 gallons

Temperature Control

Chiller temperature set point (°F) = 57 in/56 out

Fermentation Period

Beginning September 9, 1981 ... through September 16, 1981

Total Hours = 172

Total volumetric exhaust flow = 1,549,940 actual cubic feet @ turbine meter.

TABLE 3

White Wine Fermentation Exhaust Ethanol Emissions

Tank No. 576

Capacity (gals): 350,110

Actual (gals): 280,000

Location: United Vintners(Madera facility)

Run	Time (Day/hrs)	Exhaust Flow (acfm)	Ethanol ppm-vol	Ethanol Emissions (lbs/hr)	Cumulative (lbs)	Run	Time (Day/hrs)	Exhaust Flow (acfm)	Ethanol ppm-vol	Ethanol Emissions (lbs/hr)	Cumulative (lbs)
1	1/0800	0.0	-- (1)	--	0	26	4/2009	243.7	3625	6.2	183.6
2	1/1123	0.0	27	0.0	0	27	4/2304	233.9	3882	6.3	205.6
3	1/1500	0.0	12	0.0	0	28	5/0200	225.9	3632	5.8	234.4
4	1/1730	0.0	36	0.0	0	29	5/0909	210.0	3582	5.3	255.5
5	1/2010	0.0	70	0.0	0	30	5/1030	223.2	3409	5.3	266.5
6	2/0019	0.0	152	0.0	0	31	5/1306	218.5	3886	5.9	283.9
7	2/0213	6.3	37 (1)	0.0	0	32	5/1600	223.8	3891	5.8	307.2
8	2/0800	44.5	735	0.2	0.2	33	5/2052	209.8	3775	5.7	327.0
9	2/1000	61.2	563	0.2	0.8	34	5/2300	208.6	3918	5.5	338.0
10	2/1300	70.7	768	0.4	1.9	35	6/0200	182.6	3918	5.1	263.3
11	2/1600	82.5	745	0.4	3.4	36	6/0834	198.3	4256	4.8	394.6
12	2/2020	93.9	822	0.5	5.3	37	6/1214	186.0	3796	4.9	406.9
13	2/2300	118.7	1065	0.9	8.0	38	6/1341	209.2	5416	7.8	418.6
14	3/0200	138.1	1156	1.1	13.0	39	6/1600	216.0	5847	8.8	457.8
15	3/0800	156.6	1346	1.5	19.7	40	6/2000	247.0	5662	9.7	486.8
16	3/1123	176.3	1543	1.9	24.4	41	6/2300	198.2	6422	8.8	504.4
17	3/1300	192.5	2354	3.2	30.7	42	7/0200	218.9	6987	10.6	557.6
18	3/1621	177.3	1787	2.2	41.7	43	7/0830	188.1	5861	7.6	595.7
19	3/2048	190.8	2122	2.8	50.2	44	7/1100	175.7	6483	7.8	611.3
20	3/2300	198.6	2407	3.4	56.9	45	7/1304	169.3	5914	6.9	642.2
21	4/0228	222.8	2692	4.2	82.3	46	7/1945	153.2	6131	6.4	677.4
22	4/0913	232.2	3431	5.6	118.4	47	7/2300	141.4	6490	6.3	696.5
23	4/1050	242.2	3409	5.5	135.0	48	8/0300	55.8	6050	2.5	708.3
24	4/1300	248.7	600 (1)	5.5 (2)	151.6 (2)	49	8/0833	28.8	5015	1.0	712.3
25	4/1600	231.3	3397	5.5	168.2	50	8/1200	19.8	4273	0.6	713.5

(1) Run is suspect.

(2) Although the sample run was suspect, the emissions rate (lbs/hr) and cumulative values were generated using the best estimate between runs 23 & 25.

TABLE 4
PHYSICAL PARAMETERS
Tank No. 5
Red Wine Fermentation

Tank Material: Stainless Steel

Tank Dimensions: 24 inch bottom cone
12 inch top cone
480 inch shell (height)
gallons per inch = 288

Tank Capacity: 128,000 gallons

Actual Capacity: 44,000 gallons

Temperature Control: 1st 4 hrs @ 82°F
2nd 4 hrs @ 72°F
remaining 18 hrs 85°F

Fermentation Period:

Beginning September 17, 1981 through September 18, 1981

Total Hours = 26

Total Volumetric Exhaust Flow = 197380 actual cubic feet @ turbine meter

TABLE 5

Red Wine Fermentation Exhaust Ethanol Emissions

Tank No. 5
 Capacity (gals): 128,000
 Actual: 44,000
 Location: United Vintners, Madera

Run	Time Day/Hours	Exhaust Flow (acfm)	Ethanol (ppm.vol)	Ethanol Emissions (lbs/hr)	Cumulative (lbs)
1	1/1400	0.0	579	0.0	0.0
2	1/1600	71.0	1271	0.6	0.6
3	1/1945	144.0	1098	1.1	4.4
4	1/2300	225.0	3186	4.9	19.2
5	2/0200	250.0	10,094	16.5	101.7
6	2/0900	270.0	17,932	31	256.7
7	2/1145	209.0	14,916	20.4	307.7
8	2/1418	155.0	13,177	13.4	334.5
9	2/1609	94.0	11,147	7.1	341.6

sugar free, eliminating any further significant fermentation. The dried lees/pomace are sold for fertilizer or cattle feed. White wine must is extracted prior to fermentation to reduce skin contact. However, similar extraction procedures are employed and the final product is again dry and non-fermentable.

Because of the crushing season problems discussed earlier, it was vital to immediately commence fermentation tests at the Napa Valley winery. Mr. Al Del Bondio of United Vintner's Oakville facility had prepared suitable tank adapter fittings for our equipment. We arrived on site September 24, 1981. Mr. Del Bondio said that U.V. Oakville could not obtain sufficient white wine grapes to fill a tank prior to fermentation. Thus we would be required to use a tank being added to throughout the test. In addition, the expected fermentation period for white wines at this facility was 3-4 weeks and could not be significantly reduced. Those two factors prompted us, with the encouragement of our contract officer, to attempt to perform the white wine test at the Robert Mondavi winery located nearby.

The U.V. Oakville winery test program included two complete red wine fermentation tests. The first test failed to obtain measurable exhaust flow data, invalidating the test results. The second test was a Cabernet Sauvignon fermentation in a 9,000 gallons concrete tank. The tank was fitted with a gasketed hatch. During the two-day fermentation period, the hatch seal was supplemented by placing lead bricks on the hatch. The hatch was opened twice a day for pumping over the pomace cap. Testing was discontinued at those times until the hatch was replaced and pressurized conditions again obtained.

Fugitive emission testing was performed for various locations and processes at U.V. Oakville. Ambient ethanol levels in a barrel storage building were measured. In addition, a combined storage/fermentation building was monitored. Drag screen separation equipment, similar to that utilized at U.V. Madera, was monitored during operation as well as a conveyor assembly transporting fermented lees to the press. A bottling operation at the U.V. Inglenook Rutherford Winery was monitored for fugitive ethanol emissions. That facility was tested because U.V. Oakville does not have a bottling facility and R. Mondavi's was shut down for the season.

Detailed results of the United Vinters, Oakville source and fugitive emission tests are contained in the following figures and tables

TABLE 6
PHYSICAL PARAMETERS
Tank No. 198
Red Wine Fermentation
United Vintners (Oakville)

Tank Material: Concrete

Tank Dimensions: 144 inch height
140 gallons per inch

Tank Capacity: 9000 gallons

Actual Capacity: 8100 gallons

Temperature Control: 72°F Average

Fermentation Period:

Beginning October 7, 1981 through October 9, 1981

Total Hours: 77

Total volumetric exhaust flow = 80490 actual cubic feet @ turbine meter

TABLE 7

Red Wine Fermentation Exhaust Ethanol Emissions

Tank Number 198
 Capacity (gals) : 9000
 Actual (gals) : 8100
 Location: United Vintners (Oakville Facility)

Run	Time (Day/Hrs)	Exhaust Flow (adcfm)	Ethanol (ppm-vol)	Ethanol Emissions (lbs/hr)	Cumulative (lbs)
1	1/1000	53.5	5846	2.1	2.1
2	1/1400	65.5	5950	2.6	12.5
3	1/1800	57.5	12548	4.7	31.3
4	2/1020	21.0	13390	1.9	74.6
5	2/1210	19.0	13907	1.7	79.7
6	2/1610	14.5	14618	1.4	85.3
7	3/1100	0.0 ⁽¹⁾	10893	0.0	--(1)
8	3/1600	0.0 ⁽¹⁾	10730	0.0	--(1)

(1) volumetric flow undetectable.

TABLE 8

FUGITIVE EMISSIONS
UNITED VINTNERS (Oakville)

LOCATION	DATE, TIME (Hrs)	ETHANOL		COMMENTS	
		(mg/m ³)	(grams/hr) (ppm by vol)		
No. 1	9/25, 1000	0.04	0.003	0.02	Barrel Aging Area Samples (See Figure 8)
2	9/25, 1000	0.05	0.004	0.03	"
1	9/25, 1500	0.05	0.004	0.03	"
2	9/25, 1500	0.05	0.004	0.03	"
3	9/25, 1645	2.2	0.4	1.2	Fermentation area, Approx. 50,000 gals active, 20,000 being "racked out"
4	9/25, 1800	6.5 (1)	1	3.4	
5	9/26, 1300	0.04	0.003	0.02	Cold room storage (no fermentation)
6	9/26, 1430	0.08	0.007	0.04	
7	10/4, 1100	5429	923	2888	Drag Screen
8	10/6, 1000	1134	193	603	Pomace Press

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(1) Area approximately 3 ft. away from lees drag screen.

Sample Calculation: $Ethanol(grams/hr) = \frac{ETOHmg/m^3}{1000mg} \times 1.8 \times acfm \times 60 \frac{min}{hr} \times 1 \frac{m^3}{35.31 cf}$

acfm = actual cubic feet per minute

Dr. James Vahl assisted us in obtaining a tank with fittings suitable for the adapter Mr. Del Bondio had loaned to us. Also, a supply of Chardonnay grapes, requiring a shorter fermentation period, was available (the last of the season). Testing of a 6,000 gallon tank commenced on Saturday, September 26, 1981 and extended over a twenty-one day period. That test length resulted from the fermentation process "sticking" near the end, resulting in an unusually slow decrease in sugar content. In addition to the fermentation test, storage facility fugitive emissions were monitored as well as the process of aeration, used by quality vintners to remove undesired volatile flavor compounds such as excess H_2S or SO_2 . The fermented juice is allowed to splash from a hose into an open trough prior to storage.

Exhaust volumetric flow was undetectable with the turbine meter during the first four days of the twenty-one day fermentation period as a result of the comparatively small volume of fermenting juice (5,800 gals). Consequently, a method was employed in which the top of the meter was sealed, restricting exhaust release to the existing turbine meter sample ports (Ref. Figure 9). Gas flow was measured with a more sensitive dry test meter. Two dry test meters were used in order to provide twice the pressure relief during greater flow activity (Day 5 through Day 10). The tank headspace was permitted to reach a stable temperature/pressure condition before measuring gas flow per unit time (dry cubic feet/min). This procedure permitted reliable measurements while avoiding the "foaming-over" problem encountered at U.V. Madera. At peak fermentation activity, the juice is saturated or super-saturated with carbon dioxide. Increased pressure placed on the system (tank) may cause foaming-over in the event of an abrupt agitation. Although flow was measured on an actual dry basis with the dry test meters, moisture percent was negligible due to the small volume of juice and comparable to typical white wine fermentation exhaust data.

Detailed results of the Robert Mondavi source and fugitive emission tests are contained in the following figures and tables.

TABLE 10

PHYSICAL PARAMETERS
Tank #289
White Wine Fermentation
Robert Mondavi (Oakville)

Tank Material: Stainless Steel

Fermentation Tank Capacity:

Total Tank Capacity = 5,955 gallons

Actual Tank Capacity = 5,800 gallons

Temperature "Control"

Ambient (i.e., tank located outdoors)

Fermentation Period:

Beginning September 26, 1981 through October 16, 1981

Total Hours = 512

Total Volumetric Exhaust Flow = 149 cubic feet

Table 11

White Wine Fermentation Exhaust Ethanol Emissions

Tank No. 289
 Capacity (gal): 5,955
 Actual (gal): 5,800
 Location: Robert Mondavi (Oakville)
 Test Start Date: 9/26/81

RUN	Time (Day/Hours)	Exhaust Flow (1) (adcfm)	Ethanol PPM-vol	Ethanol Emissions (lbs/hr)	Cumulative (lbs)
1	1/1027	0.0 (2)	9	--	0.00
2	2/0200	0.0	4	--	0.00
3	2/0900	0.0	4	--	0.00
4	2/1214	0.0	6	--	0.00
5	2/1400	0.0	7	--	0.00
6	2/1624	0.0	31	--	0.00
7	2/2000	0.0	527	--	0.00
8	2/2200	0.0	650	--	0.00
9	3/0200	0.0	676	--	0.00
10	3/1000	0.0	663	--	0.00
11	3/1200	0.0	793	--	0.00
12	3/1600	0.0	765	--	0.00
13	3/1800	0.0	782	--	0.00
14	3/2200	0.0	833	--	0.00
15	4/0200	0.0	858	0.000 (5)	0.00
16	4/0800	0.0	1696	0.001	0.00
17	4/1200	0.0	2882	0.002	0.01
18	4/1610	0.0	2110	0.004	0.03
19	4/2000	0.0	3511	0.005	0.05
20	4/2300	0.0	1780	0.006	0.06

(1) Actual dry cubic feet per minute

(2) Exhaust flow undetectable with turbine meter.

(5) Interpolated values from chart. (Runs 15-20).

Table 11 (continued)

RUN	Time (Day/Hours)	Exhaust Flow (adcfm) (1)	Ethanol ppm-vol	Ethanol Emissions (lbs/hr)	Cumulative (lbs)
21	5/0200	0.0	1817	0.008 (5)	0.11
22	5/1042	0.0	2810(3)	0.011	0.17
23	5/1240	0.5	3416	0.012 (6)	0.19
24	5/1450	0.5	4071	0.014	0.23
25	5/1726	0.5	3484	0.013	0.26
26	5/2000	0.5	2660	0.010	0.29
27	5/2400	0.6	2888	0.011	0.34
28	6/0400	0.8	3337	0.014	0.42
29	6/1218	0.8	3895	0.021	0.56
30	6/1637	0.8	3701	0.020	0.65
31	6/2203	0.8	8089	0.042	0.86
32	7/0220	0.8	3313	0.018	0.98
33	7/1123	0.8	8684	0.045	1.23
34	7/1336	0.8	8440	0.041	1.37
35	7/1758	0.8	8986	0.046	1.57
36	7/2207	0.7	5733	0.028	1.68
37	8/0200	0.7	4286	0.020	1.79
38	8/0923	0.7	7282	0.031	1.91
39	8/1330	0.7	9129	0.042	2.04
40	8/1530	0.7	14568 (3)	0.063	2.39
41	8/2048	0.7	5631	0.026	2.50
42	8/2400	0.7	5717	0.026	2.58
43	9/0300	0.7	5762	0.025	2.74
44	9/1306	0.7	6984	0.031	2.94
45	9/1552	0.7	9046	0.040	3.09
46 (4)	9/2050	0.7	6891	0.034	3.23
47	9/2350	0.7	6765	0.034	3.32
48	10/0200	0.8	4210	0.022	3.45
49	10/1106	0.8	8895	0.050	3.73
50	10/1330	0.8	8013	0.045	3.86

(1) Actual dry cubic feet per minute.

(2) Exhaust flow undetectable with turbine meter.

(3) Run is suspect.

(4) Average of two samples taken simultaneously for Quality Assurance.

(5) Interpolated values from graph, (Runs 21-22).

(6) Measured values, (Runs 23-75).

Table 11 (continued)

RUN	Time (Day/Hours)	Exhaust Flow (1) (adcfm)	Ethanol ppm-vol	Ethanol Emissions (lbs/hr)	Cumulative (lbs)
51	10/1650	0.8	8700	0.048	4.03
52	10/2030	0.8	6646	0.035	4.14
53	10/2308	0.8	6451	0.032	4.23
54	11/0200	0.8	6608	0.030	4.46
55	11/1447	0.4	8446	0.024	4.64
56	11/1646	0.4	8123	0.023	4.73
57	11/2232	0.4	6415	0.018	4.83
58	12/0338	0.4	6021	0.017	4.94
59	12/1200	0.4	9871	0.028	5.09
60	12/1400	0.4	8216	0.022	5.16
61	12/1900	0.3	7030	0.015	5.32
62	13/1130	0.2	9676	0.017	5.49
63	13/1413	0.3	9155	0.019	5.55
64	13/1749	0.3	8705	0.018	5.76
65	14/1407	0.2	6827	0.010	5.87
66	14/1540	0.2	8118	0.012	6.03
67	15/1648	0.3	6968	0.015	6.41
68	16/1729	0.3	8616	0.018	6.84
69	17/1721	0.2	8335	0.009	7.05
70	18/1545	0.2	7409	0.013	7.36
71	19/1625	0.3	9246	0.018	7.79
72	20/1530	0.2	9316	0.012	7.93
73	20/1700	0.2	5382	0.007	8.02
74	21/1500	0.2	8968	0.013	8.17
75	21/1637	0.2	9532	0.012	8.18

(1) Actual dry cubic feet per minute.

SECTION III
SUMMARY AND CONCLUSIONS

Ethanol emission factors have been determined for the fermentation process. Additional measurements of ethanol fugitive emissions, generated from storage and handling during production, have been completed. Four fermentation tanks were monitored throughout their complete fermentation periods. The choice of tank location and type was made in an attempt to represent some of the variations in California wine production, given the time and budgetary limitations of the project. Final results listing ethanol fermentation emissions and emission factors are found in Table 13. Results for fugitive ethanol emissions and emission factors are detailed in Table 14.

The tabulated ethanol fermentation emissions (maximum lbs/hr and total lbs emitted) indicate a simple relationship between the volume of fermenting juice and wine type (i.e., red vs. white). Ethanol losses during red wine fermentation were higher than losses during white wine fermentation. The larger the volume of fermenting juice, the larger was the maximum quantity of ethanol emitted per unit time, or quantitatively, at the peak fermentation more CO₂ was produced and exhausted per unit time and thus more ethanol emitted through entrainment.

Ethanol emissions have been related to fermentation process conditions in order to generate emission factors, which in turn may be compared to historical data and theoretical attempts to characterize ethanol losses during fermentation.

Historical data representing ethanol emission factors as percent of total ethanol emitted versus fermentation temperature are graphed in Figure 13. Emission factors determined by EAL have been included in the graph and are in good agreement. In general, white wine fermentation emission factors are found at the lower end of the temperature range and red wine factors at the upper end. Comparison of EAL data to that of the California Air Resources Board (CARB) shows agreement for two separate white wine fermentations at approximately the same fermentation interval activity. Specifically, CARB reported an "ethanol concentration increase from 1,902 parts

TABLE 13

ETHANOL FERMENTATION EMISSIONS AND EMISSION FACTORS

SOURCE	LOCATION	FERMENTATION PARAMETERS				EMISSIONS Maximum Ethanol Emission Rate (Lbs/hr)	Total Ethanol Emitted (Lbs)	EMISSION FACTORS		
		Juice Volume (gal)	Average Temp. (°F)	Yeast Type	Duration (hours)			Ethanol Emitted (Lbs) 10 ³ Gal Juice	Ethanol ⁽¹⁾ Emitted (Lbs) Ton Grapes	% Ethanol Emitted Per Ethanol Produced
White Wine Fermentation Exhaust	United Vintners (Madera)	280,000	56	Montrachet	172	10.6	714	2.6	0.56	0.35
White Wine Fermentation Exhaust	Robert Mondavi (Oakville)	5,800	60	Montrachet	512	0.05	8.2	1.4	0.31	0.2
Red Wine Fermentation Exhaust	United Vintners (Madera)	44,000	83	Sacromices Servicia	26	31.0	342	7.8	1.7	1.3
Red Wine Fermentation Exhaust	United Vintners (Oakville)	8,100	72	Montrachet	77	4.7	85.3	10.5	2.3	0.82

(1) 220 Gallons Juice/Ton Grapes

TABLE 14
ETHANOL FUGITIVE EMISSIONS AND EMISSION FACTORS

Location: United Vintners, Oakville

<u>Area</u>	<u>(mg/m³)</u>	<u>(grams/hr)</u>	<u>(ppm by vol.)</u>
Storage (Locations 1, 2, 5, 6) Ref. Figure	0.04-0.08	0.003-0.007	0.02-0.04
Handling (Location 3)	2.2	0.4	1.4
Handling (Location 4, adjacent to drag screen)	6.5	1.0	3.4
Handling (Location 7, immediately above drag screen)	5429	923	2888
Handling (Location 8, immediately above pomace press)	1134	193	603

Location: Robert Mondavi, Oakville*

<u>Area</u>			
Handling (Location 1)	56	4.8	30
Storage (Location 2)	43	3.7	23
Storage (Location 3)	15	1.3	8

*The storage and handling areas at Robert Mondavi (Oakville) were undergoing final clean up operations of the crush season, possibly explaining the relatively higher ethanol values compared to those at United Vintners(Oakville).

TABLE 14 (continued)

Location: Inglenook (Rutherford), bottling process (i.e., handling)

<u>Area</u>	<u>(mg/m³)</u>	<u>(grams/hr)</u>	<u>(ppm by vol.)</u>
Room Air	32	-- *	17
Source, Corking Vent Outlet	654	1.8	348
Source, Filling Vent Outlet	3536	27.2	1881

ETHANOL FUGITIVE EMISSION FACTORS
HANDLING PROCESSES

<u>Process</u>	<u>Ethanol</u>
Drag Screen	0.5 lbs ethanol/10 ⁻³ gal juice
Pomace Press	0.02 lbs ethanol/ton of pomace
Wine Bottling	0.1 lbs ethanol/10 ⁻³ gal wine (white)

*No significant turbulence or air movement (i.e., ethanol dispersion).

APPENDIX C.

7 duplicate

State of California
AIR RESOURCES BOARD

ETHANOL EMISSIONS AND CONTROL
FOR WINE FERMENTATION TANKS

Engineering Evaluation Branch
Test Report

C-87-041

Report Date: April, 1988

APPROVED

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This report has been reviewed by the staff of the California Air Resources Board and approved for publication. Approval does not signify that the contents necessarily reflect the views and policies of the Air Resources Board, nor does mention of trade names or commercial products constitute endorsement or recommendation for use.

TABLE S.1

ETHANOL MASS EMISSION SUMMARY

FERMENTATION	TANK 1 CATALYTIC INCINERATOR		TANK 2 CARBON ADSORPTION UNIT		TANK 3 WATER SCRUBBER		TANK 4			
	POUNDS IN	POUNDS OUT OVERALL EFF	POUNDS IN	POUNDS OUT OVERALL EFF	POUNDS IN	POUNDS OUT OVERALL EFF	POUNDS OUT			
White Wine I ^{a/}	1.32	0.29	78%	1.48	0.15	90%	0.67	0.12	82%	0.58
Red Wine I ^{b/}	5.65	1.46	74%	8.92	3.91	56%	2.13	0.04	98%	1.33
Red Wine II	4.92	0.15	97%	4.64	0.27	94%	3.76	0.04	99%	2.56
White Wine II	3.71	0.04	99%	4.24	0.10	98%	3.71	0.06	98%	3.71

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a/ Catalytic incinerator experienced start-up difficulties during White Wine I

b/ Red Wine I data is limited due to foamover problems

TABLE 4.1

SUMMARY OF SAMPLING AND ANALYTICAL METHODS

<u>COMPONENT TO BE ANALYZED</u>	<u>SAMPLING METHOD</u>	<u>ANALYTICAL METHOD OR DETECTION PRINCIPLE</u>
O ₂	Continuous Analyzer	Paramagnetic
CO ₂	Continuous Analyzer	NDIR
CO	Continuous Analyzer	NDIR
Ethanol	Continuous Analyzer	FID
Moisture Content	Method 4	Volumetric
Volatile Organics	Grab Bag	GC/FID, GC/ECD
Liquid Catches	Grab (Specimen Jar)	GC/FID, GC/ECD

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V. TEST RESULTS

The test results are presented as follows:

- A. Continuous analyzer data and calculated control efficiency
- B. Flow rate and moisture content data
- C. Bag sample data
- D. Aqueous sample data
- E. Carbon tube data
- F. Calculation of Alcohol Loss

A. CONTINUOUS ANALYZER DATA

The continuous analyzer data for ethanol (EtOH), oxygen (O₂), and carbon dioxide (CO₂) gas concentrations is presented separately for each of the four fermentations. Each data point represents a time-averaged value for the time sampled at that tank. The continuous hydrocarbon analyzer measured the ethanol emissions as ppm propane. This has been converted to ppm ethanol based on a factor of 1.72 ppm EtOH = 1 ppm propane. This factor was obtained by observing the hydrocarbon analyzer response to a known EtOH concentration.

The percent ethanol control efficiency is calculated as follows:

$$\frac{(\text{EtOH In} - \text{EtOH out})}{(\text{EtOH In})} \times 100$$

Due to the difficulties inherent in measuring and comparing low ppm ethanol concentrations, the calculated control efficiencies near the start of the fermentations may not be representative of actual conditions.

F. CALCULATION OF ALCOHOL LOSS

Table 5.23 gives a summary of the mass of ethanol entering and leaving each control device for each fermentation. These values were obtained by integrating the ethanol concentration curves over the course of the fermentation. Details of this calculation can be found in Appendix B. Though the total amount of ethanol emitted may seem low, it should be kept in mind that only about 1000 gallons of grape must per tank were fermented in this pilot program.

Table 5.24 gives a summary of the data used to calculate the percent of ethanol lost by each tank. The data used to calculate the amount of total ethanol produced over the fermentation (gallons, % EtOH) were obtained from CSUF data summaries. The data for each tank is plotted in Figure 5.30 as a function of fermentation temperature. Also shown on Figure 5.30 are results from similar studies on fermentation tank emissions. The references are listed below the graph.

Most of the Phase I data are in fair agreement with previous work. Data scatter from Red Wine I is probably due to the limited number of data points available for this fermentation due to foamover problems. When the data from Red Wine I are removed from the graph, as in Figure 5.31, the plot shows an improved correlation.

Table 5.24

SUMMARY OF DATA USED TO CALCULATE PERCENT ETHANOL LOST

FERM	TANK	GALLONS	% ETOH	INITIAL SUGAR (DEG BRIX)	TEMP (DEG F)	AVAIL GALLONS ETOH	AVAIL GRAMS ETOH	GRAMS ETOH LOST	% OF TOTAL ETOH LOST
NW I	1	1086	10.3	20.1	59	112	3.3E+05	601	0.18
	2	1086	10.3	20.1	59	112	3.3E+05	672	0.20
	3	1086	10.3	20.1	57	112	3.3E+05	306	0.09
	4	1086	8.6	20.1	59	93	2.8E+05	264	0.09
RW I	1	736	14.11	24.1	78	104	3.1E+05	2567	0.83
	2	736	14.17	23.9	78	104	3.1E+05	4054	1.30
	3	736	14.3	23.9	79	105	3.1E+05	969	0.31
	4	736	13.65	24.3	75	100	3.0E+05	605	0.20
RW II	1	701	11.83	25.4	80	83	2.5E+05	2238	0.90
	2	701	13.00	24.8	78	91	2.7E+05	2108	0.77
	3	701	12.44	25.1	76	87	2.6E+05	1708	0.66
	4	701	12.54	25.5	81	88	2.6E+05	1162	0.44
NW II	1	1083	10.83	22.3	57	117	3.5E+05	1688	0.48
	2	1083	10.73	22.3	57	116	3.5E+05	1926	0.55
	3	1083	11.27	22.3	57	122	3.6E+05	1688	0.46
	4	1083	9.95	22.3	57	108	3.2E+05	1688	0.52

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TABLE

WHITE WINE 1 - EMISSION DATA FOR CATALYTIC HEATER

TANK	DATE	TIME	HOURS	TIME			ETOH		ETOH		FLOW (SCFM)	MASS ETOH	
				ETOH IN (PPM)	ETOH OUT (PPM)	INTERVAL (HOURS)	IN PPM AVG	IN PPM-HOUR	OUT PPM AVG	OUT PPM-HOUR		IN (GRAMS)	OUT (GRAMS)
1	19-Aug-87	11:30	0.0										
	20-Aug-87	13:00	25.5	3.44	3.44	25.5	1.7	43.9	1.7	43.9	7	1.0	1.0
	20-Aug-87	16:30	29.0	1.72	20.64	3.5	2.6	9.0	12.0	42.1	7	0.2	0.9
	21-Aug-87	07:00	43.5	86	1.72	14.5	43.9	636.0	11.2	162.1	7	14.2	3.6
	21-Aug-87	11:00	47.5	48.16	25.8	4.0	67.1	268.3	13.8	55.0	7	6.0	1.2
	21-Aug-87	14:30	51.0	34.4	20.64	3.5	41.3	144.5	23.2	81.3	7	3.2	1.8
	22-Aug-87	09:00	68.5	15.48	6.88	17.5	24.9	436.4	13.8	240.8	7	9.7	5.4
	22-Aug-87	10:00	70.5	25.8	15.48	2.0	20.6	41.3	11.2	22.4	7.25	1.0	0.5
	22-Aug-87	14:30	75.0	25.8	27.52	4.5	25.8	116.1	21.5	96.8	7	2.6	2.2
	23-Aug-87	10:30	95.0	189.2	149.64	20.0	107.5	2150.0	88.6	1771.6	7	48.0	39.6
	23-Aug-87	15:20	99.8	232.2	154.8	4.8	210.7	1018.4	152.2	735.7	7	22.7	16.4
	24-Aug-87	10:00	118.5	258	0	18.7	245.1	4575.2	77.4	1444.8	6.75	98.5	31.1
	24-Aug-87	13:15	121.7	412.8	51.6	3.2	335.4	1090.0	25.8	83.8	6.75	23.5	1.8
	24-Aug-87	17:10	125.7	430	43	3.9	421.4	1650.5	47.3	185.3	7	36.9	4.1
	26-Aug-87	07:00	163.5	86	3.44	37.8	258.0	9761.0	23.2	878.5	7	218.0	19.6
	26-Aug-87	17:00	173.5	146.2	1.72	10.0	116.1	1161.0	2.6	25.8	7	25.9	0.6
	27-Aug-87	08:30	189.0	68.8	1.72	15.5	107.5	1666.3	1.7	26.7	7	37.2	0.6
	27-Aug-87	17:00	197.5	120.4	8.6	8.5	94.6	804.1	5.2	43.9	7	18.0	1.0
	28-Aug-87	06:50	211.3	103.2	5.16	13.8	111.8	1546.6	6.9	95.2	7	34.5	2.1
											TOTAL GRAMS ETOH:	601.1	133.6
											OVERALL EFFICIENCY:		77.8%

WHITE WINE 1 - EMISSION DATA FOR CARBON ADSORPTION UNIT

TANK	DATE	TIME	HOURS	TIME			ETOH		ETOH		FLOW (SCFM)	MASS ETOH	
				ETOH IN (PPM)	ETOH OUT (PPM)	INTERVAL (HOURS)	IN PPM AVG	IN PPM-HOUR	OUT PPM AVG	OUT PPM-HOUR		IN (GRAMS)	OUT (GRAMS)
2	19-Aug-87	11:30	0.0										
	19-Aug-87	14:30	3.0	1.72	0	3.0	0.9	2.6	0.0	0.0	7	0.1	0.0
	20-Aug-87	14:00	26.5	3.44	1.72	23.5	2.6	60.6	0.9	20.2	7	1.4	0.5
	20-Aug-87	17:00	29.5	3.44	5.16	3.0	3.4	10.3	3.4	10.3	7	0.2	0.2
	21-Aug-87	08:00	44.5	86	1.72	15.0	44.7	670.8	3.4	51.6	7	15.0	1.2
	21-Aug-87	10:30	47.0	51.6	5.16	2.5	68.8	172.0	3.4	8.6	7	3.8	0.2
	21-Aug-87	11:30	48.0	60.2	12.04	1.0	55.9	55.9	8.6	8.6	7	1.2	0.2
	21-Aug-87	15:00	51.5	34.4	6.88	3.5	47.3	165.6	9.5	33.1	7	3.7	0.7
	21-Aug-87	17:00	53.5	13.76	8.6	2.0	24.1	48.2	7.7	15.5	7	1.1	0.3
	22-Aug-87	09:00	69.5	13.76	1.72	16.0	13.8	220.2	5.2	82.6	7	4.9	1.8
	22-Aug-87	10:45	71.2	24.08	0.86	1.7	18.9	33.1	1.3	2.3	7	0.7	0.1
	22-Aug-87	15:00	75.5	25.8	3.44	4.3	24.9	106.0	2.2	9.1	7	2.4	0.2
	23-Aug-87	07:30	92.0	103.2	0	16.5	64.5	1064.3	1.7	28.4	7	23.8	0.6
	23-Aug-87	11:15	95.7	232.2	6.88	3.8	167.7	628.9	3.4	12.9	7	14.0	0.3
	23-Aug-87	16:55	101.4	283.8	1.72	5.7	258.0	1462.0	4.3	24.4	7	32.6	0.5
	24-Aug-87	14:55	123.4	473	8.6	22.0	378.4	8324.8	5.2	113.5	7	185.9	2.5
	25-Aug-87	06:50	139.3	261.44	154.8	15.9	367.2	5844.9	81.7	1300.4	7	130.5	29.0
	25-Aug-87	11:45	144.2	275.2	1.72	4.9	268.3	1319.2	78.3	384.8	7	29.5	8.6
	26-Aug-87	08:00	164.5	154.8	2.58	20.3	215.0	4353.8	2.2	43.5	7	97.2	1.0
	26-Aug-87	14:30	171.0	189.2	3.44	6.5	172.0	1118.0	3.0	19.6	7	25.0	0.4
	27-Aug-87	11:00	191.5	120.4	72.24	20.5	154.8	3173.4	37.8	775.7	7	70.9	17.3
	27-Aug-87	11:30	192.0	120.4	1.72	0.5	120.4	60.2	37.0	18.5	7	1.3	0.4
	27-Aug-87	17:50	198.3	129	5.16	6.3	124.7	789.8	3.4	21.8	7	17.6	0.5
	28-Aug-87	07:40	212.2	60.2	1.72	13.8	94.6	1308.6	3.4	47.6	7	29.2	1.1
											TOTAL GRAMS ETOH:	671.6	65.7
											OVERALL EFFICIENCY:		90.2%

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TABLE

WHITE WINE I - EMISSION DATA FOR WATER SCRUBBER

TANK	DATE	TIME	HOURS	TIME INTERVAL		ETOH IN (PPM AVG)	ETOH IN (PPM-HOUR)	ETOH OUT (PPM AVG)	ETOH OUT (PPM-HOUR)	FLOW (SCFM)	MASS ETOH		
				ETOH IN	ETOH OUT						IN (GRAMS)	OUT (GRAMS)	
3	19-Aug-87	11:30	0.0										
	19-Aug-87	15:00	3.5	2	0	3.5	0.9	3.0	0.0	0.0	4.6	0.0	0.0
	20-Aug-87	09:30	22.0	2	2	18.5	1.7	31.8	0.9	15.9	4.0	0.4	0.0
	20-Aug-87	14:30	27.0	5	3	5.0	3.4	17.2	2.6	12.9	3.5	0.2	0.0
	20-Aug-87	17:30	30.0	5	3	3.0	5.2	15.5	3.4	10.3	3.3	0.2	0.0
	21-Aug-87	08:30	45.0	258	3	15.0	131.6	1973.7	3.4	51.6	2.8	17.3	2.9
	21-Aug-87	12:30	49.0	103	7	4.0	180.6	722.4	5.2	20.6	3.8	8.6	0.6
	21-Aug-87	15:30	52.0	38	7	3.0	70.5	211.6	6.9	20.6	3.3	2.2	0.1
	21-Aug-87	17:30	54.0	15	9	2.0	26.7	53.3	7.7	15.5	3.3	0.6	0.0
	22-Aug-87	09:30	70.0	15	2	16.0	15.5	247.7	5.2	82.6	3.0	2.4	0.6
	22-Aug-87	11:30	72.0	28	0	2.0	21.5	43.0	0.9	1.7	3.0	0.4	0.0
	22-Aug-87	15:30	76.0	38	3	4.0	32.7	130.7	1.7	6.9	3.5	1.5	0.0
	23-Aug-87	08:30	93.0	120	2	17.0	79.1	1345.0	2.6	43.9	2.3	9.7	1.4
	23-Aug-87	11:48	96.3	258	7	3.3	189.2	624.4	4.3	14.2	2.8	5.5	0.2
	24-Aug-87	08:30	117.0	292	0	20.7	275.2	5696.6	3.4	71.2	2.5	45.4	10.3
	24-Aug-87	11:15	119.7	378	5	2.8	335.4	922.4	2.6	7.1	2.5	7.4	0.2
	24-Aug-87	15:45	124.2	564	4	4.5	471.3	2120.8	4.7	21.3	3.3	22.0	1.5
	25-Aug-87	08:00	140.5	550	10	16.2	557.3	9055.8	7.3	118.8	2.1	60.7	23.0
	25-Aug-87	14:00	146.5	433	3	6.0	491.9	2951.5	6.9	41.3	3.0	28.2	3.7
	26-Aug-87	09:00	165.5	52	2	19.0	242.5	4607.9	2.6	49.0	3.3	48.5	7.6
	26-Aug-87	15:30	172.0	258	2	6.5	154.8	1006.2	1.7	11.2	2.8	8.8	0.3
	27-Aug-87	06:30	187.0	172	3	15.0	215.0	3225.0	2.6	38.7	2.3	23.1	2.9
	27-Aug-87	13:00	193.5	120	3	6.5	146.2	950.3	3.4	22.4	4.3	12.9	0.9
											TOTAL GRAMS ETOH:	305.9	56.2
											OVERALL EFFICIENCY:		81.6%

WHITE WINE I - NO CONTROL EQUIPMENT

TANK	DATE	TIME	HOURS	ETOH	TIME INTERVAL		ETOH IN (PPM AVG)	ETOH IN (PPM-HOUR)	FLOW (SCFM)	MASS ETOH (GRAMS)	
					(HOURS)	(HOURS)					
4	19-Aug-87	11:30	0								
	19-Aug-87	15:30	4.0	36		4.0	18.1	72.2	0.0	0.0	
	20-Aug-87	16:00	28.5	636		24.5	336.3	8238.4	0.0	0.0	
	21-Aug-87	09:15	45.7	1462		17.3	1049.2	18098.7	0.0	0.0	
	21-Aug-87	13:30	50.0	1720		4.3	1591.0	6761.8	0.0	0.0	
	21-Aug-87	21:00	57.5	69		7.5	894.4	6708.0	0.0	0.0	
	22-Aug-87	13:45	74.2	146		16.7	107.5	1800.6	0.1	0.7	
	22-Aug-87	16:00	76.5	181		2.3	163.4	367.7	0.1	0.2	
	24-Aug-87	12:00	120.5	860		44.0	520.3	22893.2	1.1	80.3	
	24-Aug-87	16:25	124.9	1032		4.4	946.0	4178.2	1.0	13.3	
	25-Aug-87	09:15	141.7	860		16.8	946.0	15924.3	0.8	40.6	
	25-Aug-87	15:45	148.2	1032		6.5	946.0	6149.0	0.8	15.7	
	26-Aug-87	10:45	167.2	3354		19.0	2193.0	41667.0	0.5	66.5	
	27-Aug-87	14:15	194.7	1032		27.5	2193.0	60307.5	0.2	46.2	
										TOTAL GRAMS ETOH:	263.5

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TABLE

RED WINE I - EMISSION DATA FOR CATALYTIC HEATER

TANK	DATE	TIME	HOURS	ETOH IN	ETOH OUT	TIME INTERVAL (HOURS)	ETOH IN PPM AVG	ETOH IN PPM-HOUR	ETOH OUT PPM AVG	ETOH OUT PPM-HOUR	FLOW (SCFM)	MASS ETOH IN (GRAMS)	MASS ETOH OUT (GRAMS)	
1	31-Aug-87	12:00	0.0											
	01-Sep-87	19:00	31.0	2881	1075	31.0	1440.5	44655.5	537.5	16662.5	6.0	854.7	318.9	
	02-Sep-87	18:40	54.7	860	43	23.7	1870.5	44268.5	559.0	13229.7	7.8	1094.4	327.1	
	03-Sep-87	08:35	68.6	344	12	13.9	602.0	8377.8	27.5	383.0	7.0	187.1	8.6	
	03-Sep-87	14:50	74.8	1290	17	6.3	817.0	5106.3	14.6	91.4	7.0	114.0	2.0	
	04-Sep-87	06:45	90.8	292	10	15.9	791.2	12593.3	13.8	219.0	7.0	281.2	4.9	
	04-Sep-87	11:45	95.7	344	17	5.0	318.2	1591.0	13.8	68.8	7.0	35.5	1.5	
												TOTAL GRAMS ETOH:	2567.0	663.0
												OVERALL EFFICIENCY:		74.2%

RED WINE I - EMISSION DATA FOR CARBON ADSORPTION UNIT

TANK	DATE	TIME	HOURS	ETOH IN	ETOH OUT	TIME INTERVAL (HOURS)	ETOH IN PPM AVG	ETOH IN PPM-HOUR	ETOH OUT PPM AVG	ETOH OUT PPM-HOUR	FLOW (SCFM)	MASS ETOH IN (GRAMS)	MASS ETOH OUT (GRAMS)	
2	31-Aug-87	15:00	0											
	01-Sep-87	16:30	25.5	3784	1075	25.5	1892.0	48246.0	537.5	13706.3	7.0	1077.3	306.1	
	02-Sep-87	13:15	46.2	3354	2580	20.7	3569.0	74056.7	1827.5	37920.6	7.0	1653.7	846.8	
	03-Sep-87	09:10	66.2	722	163	19.9	2038.2	40594.1	1371.7	27319.7	7.0	906.5	610.0	
	03-Sep-87	13:35	70.6	1247	5	4.4	984.7	4349.1	84.3	372.2	7.0	97.1	8.3	
	04-Sep-87	07:35	88.6	344	26	18.0	795.5	14319.0	15.5	278.6	7.0	319.7	6.2	
												TOTAL GRAMS ETOH:	4054.3	1777.4
												OVERALL EFFICIENCY:		56.2%

RED WINE I - EMISSION DATA FOR WATER SCRUBBER

TANK	DATE	TIME	HOURS	ETOH IN	ETOH OUT	TIME INTERVAL (HOURS)	ETOH IN PPM AVG	ETOH IN PPM-HOUR	ETOH OUT PPM AVG	ETOH OUT PPM-HOUR	FLOW (SCFM)	MASS ETOH IN (GRAMS)	MASS ETOH OUT (GRAMS)	
3	31-Aug-87	17:00	0											
	02-Sep-87	09:20	40.3	860	0	40.3	430.0	17343.3	0.0	0.0	5.5	304.3	0.0	
	02-Sep-87	16:05	47.1	1600	17	6.8	1229.8	8301.2	8.6	58.1	4.5	119.2	0.8	
	03-Sep-87	12:00	67.0	826	52	19.9	1212.6	24151.0	34.4	685.1	4.8	365.9	10.4	
	04-Sep-87	08:00	87.0	301	5	20.0	563.3	11266.0	28.4	567.6	5.0	179.7	9.1	
												TOTAL GRAMS ETOH:	969.1	20.3
												OVERALL EFFICIENCY:		97.9%

RED WINE I - NO CONTROLS

TANK	DATE	TIME	HOURS	ETOH	TIME INTERVAL (HOURS)	ETOH PPM AVG	ETOH PPM-HOUR	FLOW (SCFM)	MASS ETOH (GRAMS)	
4	31-Aug-87	19:15	0							
	02-Sep-87	12:00	40.8	6880	40.8	3440.0	140180.0	1.6	715.5	
	03-Sep-87	16:30	69.3	7740	28.5	7310.0	208335.0	0.9	604.8	
	04-Sep-87	10:00	86.8	4300	17.5	6020.0	105350.0	0.6	198.3	
									TOTAL GRAMS ETOH:	1518.5

TABLE 5.6

RED WINE II - EMISSION DATA FOR CATALYTIC HEATER

TANK	DATE	TIME	HOURS	TIME			ETOH		ETOH		FLOW	MASS ETOH	
				ETOH IN	ETOH OUT	INTERVAL	IN	IN	OUT	OUT		IN	OUT
				(PPM)	(PPM)	(HOURS)	PPM AVG	PPM-HOUR	PPM AVG	PPM-HOUR	(SCFM)	(GRAMS)	(GRAMS)
1	10-Sep-87	13:00	0.0										
	11-Sep-87	11:20	22.3	1593	83	22.3	796.7	17792.7	41.7	930.4	7.0	397.3	20.8
	11-Sep-87	15:10	26.2	1044	64	3.8	1318.5	5054.3	73.9	283.2	7.0	112.9	6.3
	11-Sep-87	19:50	30.8	3194	53	4.7	2118.7	9887.2	58.6	273.3	7.0	220.8	6.1
	12-Sep-87	08:30	43.5	1781	18	12.7	2487.3	31505.9	35.1	445.2	7.0	703.5	9.9
	12-Sep-87	12:50	47.8	1932	49	4.3	1856.4	8044.5	33.2	143.9	7.0	179.6	3.2
	12-Sep-87	22:00	57.0	1093	65	9.2	1512.7	13866.2	56.9	521.9	7.0	309.6	11.7
	13-Sep-87	00:00	59.0	856	15	2.0	974.8	1949.5	40.1	80.2	7.0	43.5	1.8
	13-Sep-87	01:00	60.0	685	-1	1.0	770.7	770.7	7.1	7.1	7.0	17.2	0.2
PO	13-Sep-87	02:05	61.1	244	-4	1.1	464.8	503.5	-2.5	-2.7	7.0	11.2	-0.1
	13-Sep-87	04:00	63.0	455	-2	1.9	349.6	670.0	-3.0	-5.7	7.0	15.0	-0.1
	13-Sep-87	06:00	65.0	294	-1	2.0	374.7	749.3	-1.5	-3.0	7.0	16.7	-0.1
	13-Sep-87	14:55	73.9	382	36	8.9	338.1	3014.7	17.4	155.3	7.0	67.3	3.5
	13-Sep-87	19:40	78.7	649	28	4.7	515.2	2447.4	32.1	152.4	7.0	54.6	3.4
PO	13-Sep-87	20:10	79.2	233	22	0.5	441.0	220.5	25.0	12.5	7.3	5.1	0.3
	14-Sep-87	09:25	92.4	331	2	13.3	282.3	3740.8	11.7	154.6	7.0	83.5	3.5

TOTAL GRAMS ETOH: 2238.0 70.3

OVERALL EFFICIENCY: 96.9%

RED WINE II - EMISSION DATA FOR CARBON ADSORPTION UNIT

TANK	DATE	TIME	HOURS	TIME			ETOH		ETOH		FLOW	MASS ETOH	
				ETOH IN	ETOH OUT	INTERVAL	IN	IN	OUT	OUT		IN	OUT
				(PPM)	(PPM)	(HOURS)	PPM AVG	PPM-HOUR	PPM AVG	PPM-HOUR	(SCFM)	(GRAMS)	(GRAMS)
2	10-Sep-87	11:42	0.0										
	11-Sep-87	10:10	22.5	342	10	22.5	171.0	3842.7	5.2	115.8	7.3	88.9	2.7
	11-Sep-87	16:30	28.8	1144	17	6.3	743.2	4707.1	13.6	86.2	7.0	105.1	1.9
	11-Sep-87	20:50	33.1	2184	10	4.3	1664.3	7212.0	13.4	58.0	7.0	161.0	1.3
B1	12-Sep-87	08:55	45.2	1992	29	12.1	2088.1	25231.2	19.4	233.9	7.5	603.7	5.6
B2	12-Sep-87	09:30	45.8	1970	17	0.6	1980.9	1155.5	22.9	13.4	7.5	27.6	0.3
	12-Sep-87	13:55	50.2	1780	23	4.4	1874.7	8279.8	19.9	87.9	7.3	191.5	2.0
	13-Sep-87	10:00	70.3	749	278	20.1	1264.1	25387.9	150.2	3016.7	7.0	566.9	67.4
	13-Sep-87	17:15	77.6	1075	57	7.3	911.8	6610.7	167.1	1211.8	6.8	142.3	26.1
	13-Sep-87	20:45	81.1	562	47	3.5	818.7	2865.3	52.0	182.1	6.8	61.7	3.9
PO	13-Sep-87	21:45	82.1	265	29	1.0	413.7	413.7	38.4	38.4	6.8	8.9	0.8
	14-Sep-87	00:00	84.3	574	32	2.3	419.5	943.8	30.5	68.6	6.8	20.3	1.5
	14-Sep-87	02:00	86.3	689	32	2.0	631.4	1262.8	31.7	63.5	6.8	27.2	1.4
	14-Sep-87	03:25	87.7	896	33	1.4	792.6	1122.8	32.4	45.9	6.8	24.2	1.0
PO	14-Sep-87	05:15	89.6	489	29	1.8	692.5	1269.5	31.0	56.8	6.8	27.3	1.2
	14-Sep-87	06:30	90.8	374	28	1.2	431.1	538.9	28.7	35.9	6.8	11.6	0.8
	14-Sep-87	11:15	95.6	413	34	4.8	393.1	1867.3	31.4	149.0	6.8	40.2	3.2

TOTAL GRAMS ETOH: 2108.5 121.1

OVERALL EFFICIENCY: 94.3%

PO - Pumpover occurred during this sampling period.

TABLE 5.7

RED WINE II - EMISSION DATA FOR WATER SCRUBBER

TANK	DATE	TIME	HOURS	TIME			ETOH	ETOH	ETOH	ETOH	FLOW (SCFM)	MASS ETOH	MASS ETOH
				ETOH IN	ETOH OUT	INTERVAL	IN	IN	OUT	OUT		IN	OUT
				(PPM)	(PPM)	(HOURS)	PPM AVG	PPM-HOUR	PPM AVG	PPM-HOUR		(GRAMS)	(GRAMS)
3	10-Sep-87	10:10	0.0										
	11-Sep-87	12:15	26.1	471	8	26.1	235.3	6136.4	3.8	98.0	7.3	141.9	2.3
	11-Sep-87	17:25	31.3	368	4	5.2	419.3	2166.6	5.6	29.1	5.5	38.0	0.5
	11-Sep-87	23:50	37.7	434	7	6.4	401.0	2573.0	5.3	34.1	5.0	41.0	0.5
	12-Sep-87	02:00	39.8	1379	6	2.2	906.2	1963.3	6.6	14.3	5.0	31.3	0.2
	12-Sep-87	04:00	41.8	1657	6	2.0	1517.7	3035.5	6.3	12.6	5.0	48.4	0.2
	12-Sep-87	06:00	43.8	1486	6	2.0	1571.5	3143.0	6.2	12.5	5.0	50.1	0.2
	12-Sep-87	07:00	44.8	1269	7	1.0	1377.8	1377.8	6.4	6.4	6.5	28.6	0.1
	12-Sep-87	10:15	48.1	1808	5	3.2	1538.9	5001.6	6.0	19.4	7.0	111.7	0.4
	12-Sep-87	15:30	53.3	1584	5	5.3	1696.1	8904.7	5.3	27.7	6.8	191.7	0.6
	13-Sep-87	09:00	70.8	1155	6	17.5	1369.3	23962.8	5.7	100.3	7.5	573.3	2.4
	13-Sep-87	18:20	80.2	897	26	9.3	1025.8	9574.1	16.1	150.4	7.3	221.4	3.5
	14-Sep-87	08:10	94.0	364	4	13.8	630.5	8722.1	15.0	207.4	6.8	187.8	4.5
	14-Sep-87	12:00	97.8	597	24	3.8	480.4	1841.4	14.0	53.7	7.3	42.6	1.2

TOTAL GRAMS ETOH: 1708.0
OVERALL EFFICIENCY: 99.0%

RED WINE II - NO CONTROLS

TANK	DATE	TIME	HOURS	ETOH (PPM)	TIME			FLOW (SCFM)	MASS ETOH (GRAMS)
					INTERVAL (HOURS)	ETOH PPM AVG	ETOH PPM-HOUR		
4	10-Sep-87	09:30	0.0						
	10-Sep-87	15:55	6.4	7	6.4	3.6	23.2	0.0	0.0
	10-Sep-87	17:00	7.5	4	1.1	5.8	6.3	0.0	0.0
	10-Sep-87	18:00	8.5	3	1.0	3.9	3.9	0.0	0.0
	10-Sep-87	20:00	10.5	6	2.0	4.8	9.6	0.0	0.0
	10-Sep-87	22:00	12.5	4	2.0	5.4	10.8	0.0	0.0
	11-Sep-87	00:00	14.5	4	2.0	4.4	8.8	0.0	0.0
	11-Sep-87	02:00	16.5	30	2.0	17.0	34.1	0.0	0.0
	11-Sep-87	04:00	18.5	58	2.0	43.8	87.6	0.0	0.0
	11-Sep-87	06:00	20.5	74	2.0	65.7	131.4	0.0	0.0
	11-Sep-87	07:00	21.5	82	1.0	77.8	77.8	0.0	0.0
	11-Sep-87	12:45	27.3	44	5.8	63.2	363.5	0.0	0.0
	12-Sep-87	11:15	49.8	4214	22.5	2129.1	47905.9	2.0	305.6
PO	12-Sep-87	17:00	55.5	2978	5.7	3596.1	20677.8	2.9	191.3
	12-Sep-87	18:30	57.0	6171	1.5	4574.8	6862.2	2.9	63.5
	13-Sep-87	12:30	75.0	8789	18.0	7479.9	134638.8	1.4	601.3

TOTAL GRAMS ETOH: 1161.7

PO - Pumpover occurred during this sampling period.

+ - Extrapolated value (off the calibrated scale of 0-25%)

TABLE
WHITE WINE II - EMISSION DATA FOR CATALYTIC HEATER

TANK	DATE	TIME	HOURS	TIME			ETOH	ETOH	ETOH	ETOH	FLOW (SCFM)	MASS ETOH	MASS ETOH
				ETOH IN (PPM)	ETOH OUT (PPM)	INTERVAL (HOURS)	IN PPM AVG	IN PPM-HOUR	OUT PPM AVG	OUT PPM-HOUR		IN (GRAMS)	OUT (GRAMS)
1	15-Sep-87	11:00	0.0										
	16-Sep-87	16:45	29.8	13.0	7.4	29.8	6.5	192.8	3.7	110.7	6.8	4.2	2.4
	17-Sep-87	08:15	45.3	0.9	5.7	15.5	6.9	107.2	6.6	101.9	7.0	2.4	2.3
	17-Sep-87	11:55	48.9	2.2	0.0	3.7	1.5	5.6	2.9	10.5	7.0	0.1	0.2
	17-Sep-87	16:35	53.6	3.9	4.8	4.7	3.1	14.3	2.4	11.3	7.0	0.3	0.3
	18-Sep-87	08:35	69.6	2.3	3.1	16.0	3.1	50.3	3.9	63.2	7.0	1.1	1.4
	18-Sep-87	13:30	74.5	18.7	4.5	4.9	10.5	51.8	3.8	18.7	7.0	1.2	0.4
	19-Sep-87	02:00	87.0	48.4	1.1	12.5	33.6	419.5	2.8	35.5	7.0	9.4	0.8
	19-Sep-87	04:00	89.0	57.5	0.7	2.0	53.0	105.9	0.9	1.9	7.0	2.4	0.0
	19-Sep-87	06:00	91.0	70.4	0.7	2.0	64.0	128.0	0.7	1.4	7.0	2.9	0.0
	19-Sep-87	08:15	93.3	76.6	0.4	2.3	73.5	165.4	0.5	1.1	6.8	3.6	0.0
	20-Sep-87	13:40	122.7	1782.9	5.6	29.4	929.7	27349.8	3.0	86.9	6.8	593.3	1.9
	20-Sep-87	22:00	131.0	1079.7	6.8	8.3	1431.3	11927.4	6.2	51.4	6.8	258.7	1.1
	21-Sep-87	00:00	133.0	806.4	2.5	2.0	943.1	1886.1	4.7	9.3	6.8	40.9	0.2
	21-Sep-87	02:00	135.0	748.3	1.2	2.0	777.3	1554.7	1.9	3.7	7.0	34.7	0.1
	21-Sep-87	04:00	137.0	661.8	0.2	2.0	705.1	1410.1	0.7	1.4	7.0	31.5	0.0
	21-Sep-87	07:00	140.0	524.1	5.8	3.0	593.0	1779.0	3.0	9.0	7.0	39.7	0.2
	21-Sep-87	11:05	144.1	869.9	6.0	4.1	697.0	2846.2	5.9	24.2	7.0	63.6	0.5
	21-Sep-87	19:30	152.5	615.9	0.0	8.4	742.9	6252.7	3.0	25.4	7.0	139.6	0.6
	22-Sep-87	12:00	169.0	473.2	7.5	16.5	544.5	8984.4	3.7	61.8	7.0	200.6	1.4
	22-Sep-87	15:00	172.0	383.7	7.9	3.0	428.4	1285.2	7.7	23.1	7.0	28.7	0.5
	23-Sep-87	09:35	190.6	284.9	2.2	18.6	334.3	6212.4	5.1	93.9	7.0	138.7	2.1
	23-Sep-87	13:30	194.5	269.2	1.3	3.9	277.0	1085.1	1.7	6.8	7.0	24.2	0.2
	24-Sep-87	08:15	213.3	47.2	0.6	18.8	158.2	2965.8	1.0	17.8	7.0	66.2	0.4
											TOTAL GRAMS ETOH:	1688.0	17.0
											OVERALL EFFICIENCY:		99.0%

WHITE WINE II - EMISSION DATA FOR CARBON ADSORPTION UNIT

TANK	DATE	TIME	HOURS	TIME			ETOH	ETOH	ETOH	ETOH	FLOW (SCFM)	MASS ETOH	MASS ETOH
				ETOH IN (PPM)	ETOH OUT (PPM)	INTERVAL (HOURS)	IN PPM AVG	IN PPM-HOUR	OUT PPM AVG	OUT PPM-HOUR		IN (GRAMS)	OUT (GRAMS)
2	15-Sep-87	11:00	0.0										
	17-Sep-87	18:30	55.5	0.8	0.9	55.5	0.4	22.7	0.4	24.9	7.0	0.5	0.6
	18-Sep-87	09:30	70.5	9.8	2.9	15.0	5.3	79.8	1.9	28.6	7.0	1.8	0.6
	18-Sep-87	17:45	78.8	21.4	10.8	8.3	15.6	129.0	6.9	56.6	7.0	2.9	1.3
	19-Sep-87	12:25	97.4	141.8	5.5	18.7	81.6	1523.7	8.2	152.2	6.8	33.1	3.3
	20-Sep-87	14:25	123.4	2037.3	20.8	26.0	1089.5	28328.2	13.2	342.2	7.0	632.6	7.6
	21-Sep-87	10:00	143.0	896.2	5.3	19.6	1466.8	28723.9	13.1	255.6	7.0	641.4	5.7
	21-Sep-87	12:20	145.3	948.6	6.8	2.3	922.4	2152.3	6.1	14.1	7.0	48.1	0.3
	21-Sep-87	17:10	150.2	901.8	113.1	4.8	925.2	4471.9	60.0	289.8	7.0	99.9	6.5
	21-Sep-87	22:00	155.0	426.2	1.9	4.8	664.0	3209.4	57.5	278.0	7.0	71.7	6.2
	22-Sep-87	00:00	157.0	365.8	0.6	2.0	396.0	792.0	1.3	2.5	7.0	17.7	0.1
	22-Sep-87	02:00	159.0	363.6	1.1	2.0	364.7	729.4	0.8	1.7	7.0	16.3	0.0
	22-Sep-87	04:00	161.0	366.5	0.6	2.0	365.1	730.1	0.9	1.7	7.0	16.3	0.0
	22-Sep-87	06:30	163.5	364.2	0.5	2.5	365.4	913.4	0.6	1.4	7.0	20.4	0.0
	22-Sep-87	13:45	170.8	520.3	6.4	7.3	442.2	3206.1	3.4	25.0	7.0	71.6	0.6
	22-Sep-87	16:50	173.8	401.9	12.6	3.1	461.1	1421.6	9.5	29.3	7.0	31.7	0.7
	23-Sep-87	11:05	192.1	272.6	6.4	18.3	337.3	6154.8	9.5	173.8	7.0	137.4	3.9
	23-Sep-87	15:10	196.2	239.8	14.7	4.1	256.2	1046.1	10.5	43.0	7.0	23.4	1.0
	24-Sep-87	00:00	205.0	136.7	27.7	8.8	188.3	1663.0	21.2	187.3	7.0	37.1	4.2
	24-Sep-87	02:00	207.0	162.1	20.9	2.0	149.4	298.8	24.3	48.6	7.0	6.7	1.1
	24-Sep-87	04:00	209.0	147.9	16.6	2.0	155.0	310.0	18.7	37.4	7.0	6.9	0.8
	24-Sep-87	06:40	211.7	126.9	13.6	2.7	137.4	366.5	15.1	40.2	7.0	8.2	0.9
											TOTAL GRAMS ETOH:	1925.5	45.3
											OVERALL EFFICIENCY:		97.6%

TABLE

WHITE WINE II - EMISSION DATA FOR WATER SCRUBBER

TANK	DATE	TIME	HOURS	TIME			ETOH		ETOH		FLOW (SCFM)	MASS ETOH	
				ETOH IN (PPM)	ETOH OUT (PPM)	INTERVAL (HOURS)	IN PPM AVG	IN PPM-HOUR	OUT PPM AVG	OUT PPM-HOUR		IN (GRAMS)	OUT (GRAMS)
3	15-Sep-87	11:00	0.0										
	17-Sep-87	09:45	46.8	1.3	0.0	46.8	0.6	30.2	0.0	0.0	7.3	0.7	0.0
	17-Sep-87	15:10	52.2	2.8	3.1	5.4	2.0	11.1	1.5	8.4	7.0	0.2	0.2
	17-Sep-87	19:45	56.8	0.0	0.8	4.6	1.4	6.4	1.9	8.9	7.0	0.1	0.2
	18-Sep-87	10:30	71.5	15.0	2.8	14.8	7.5	110.7	1.8	26.9	7.0	2.5	0.6
	18-Sep-87	22:00	83.0	64.9	1.3	11.5	40.0	459.4	2.1	23.8	7.0	10.3	0.5
	18-Sep-87	23:00	84.0	79.7	0.0	1.0	72.3	72.3	0.6	0.6	7.0	1.6	0.0
	19-Sep-87	16:15	101.3	448.0	3.5	17.3	263.9	4551.8	1.7	30.1	6.8	98.7	0.7
	20-Sep-87	16:20	125.3	2139.8	7.9	24.1	1293.9	31161.1	5.7	137.7	6.3	621.3	2.7
	21-Sep-87	08:30	141.5	437.9	5.2	16.2	1288.8	20835.8	6.6	106.4	7.5	498.5	2.5
	22-Sep-87	16:00	173.0	361.1	23.8	31.5	399.5	12583.7	14.5	457.8	7.0	281.0	10.2
	23-Sep-87	11:45	192.8	311.8	22.5	19.7	336.5	6645.0	23.2	457.6	7.0	148.4	10.2
	23-Sep-87	16:15	197.3	174.7	5.4	4.5	243.3	1094.7	14.0	62.8	7.0	24.4	1.4
											TOTAL GRAMS ETOH:	1687.8	29.3
											OVERALL EFFICIENCY:		98.3%

WHITE WINE II - NO CONTROLS

TANK	DATE	TIME	HOURS	TIME			ETOH		FLOW (SCFM)	MASS ETOH		
				ETOH IN (PPM)	ETOH OUT (PPM)	INTERVAL (HOURS)	IN PPM AVG	IN PPM-HOUR		IN (GRAMS)	OUT (GRAMS)	
4	15-Sep-87	11:00	0.0									
	16-Sep-87	15:30	28.5	24.1	22.5	28.5	12.1	344.0	0.0	0.0		
	16-Sep-87	19:45	32.8	0.7	-0.4	4.3	12.4	52.7	0.0	0.0		
	16-Sep-87	22:00	35.0	0.7	2.3	2.3	0.7	1.6	0.0	0.0		
	17-Sep-87	00:00	37.0	0.5	2.0	2.0	0.6	1.2	0.0	0.0		
	17-Sep-87	02:00	39.0	4.5	3.8	2.0	2.5	5.0	0.0	0.0		
	17-Sep-87	04:00	41.0	4.5	3.2	2.0	4.5	9.0	0.0	0.0		
	17-Sep-87	06:30	43.5	3.8	3.0	2.5	4.2	10.4	0.0	0.0		
	17-Sep-87	11:00	48.0	4.1	3.4	4.5	3.9	17.7	0.0	0.0		
	17-Sep-87	16:00	53.0	8.5	9.4	5.0	6.3	31.5	0.0	0.0		
	17-Sep-87	22:00	59.0	11.5	11.5	6.0	10.0	60.2	0.0	0.0		
	18-Sep-87	00:00	61.0	18.2	18.1	2.0	14.9	29.7	0.0	0.0		
	18-Sep-87	02:00	63.0	27.2	27.2	2.0	22.7	45.4	0.0	0.0		
	18-Sep-87	04:00	65.0	34.2	31.1	2.0	30.7	61.4	0.0	0.0		
	18-Sep-87	06:45	67.8	35.0	30.6	2.8	34.6	95.1	0.0	0.0		
	18-Sep-87	11:45	72.8	123.7	117.7	5.0	79.4	396.8	0.0	0.0		
	20-Sep-87	18:40	127.7	5568.0	5564.5	54.9	2845.9	156285.7	1.4	678.0		
	21-Sep-87	14:30	147.5	5126.0	---	19.8	5347.0	106049.1	0.8	270.6		
	22-Sep-87	08:30	165.5	4298.7	4573.3	18.0	4712.3	84822.0	0.8	216.5		
	22-Sep-87	09:30	166.5	4934.4	5114.0	1.0	4616.5	4616.5	0.8	11.8		
	22-Sep-87	18:30	175.5	5122.9	5123.3	9.0	5028.7	45258.0	0.8	115.5		
	22-Sep-87	20:05	177.1	4626.0	4742.4	1.6	4874.5	7717.9	0.8	19.7		
	22-Sep-87	22:00	179.0	4190.9	4025.6	1.9	4408.4	8449.5	0.8	21.6		
	23-Sep-87	00:00	181.0	3958.7	4121.8	2.0	4074.8	8149.6	0.8	20.8		
	23-Sep-87	02:00	183.0	4297.5	4560.5	2.0	4128.1	8256.3	0.8	21.1		
	23-Sep-87	04:00	185.0	4260.1	4548.5	2.0	4278.8	8557.6	0.8	21.8		
	23-Sep-87	06:45	187.8	4218.9	4501.1	2.8	4239.5	11658.5	0.8	29.8		
	23-Sep-87	18:45	199.8	5020.3	5668.7	12.0	4619.6	55435.1	0.8	141.5		
	24-Sep-87	09:15	214.3	1425.4	---	14.5	3222.8	46731.2	0.8	119.3		
										TOTAL GRAMS ETOH:	1687.9	

C-87-041

APPENDIX D.

Ethanol Emissions Control
from
Wine Fermentation Tanks
Using Charcoal Adsorption
A Pilot Study

March 5, 1990

by
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SECTION II. EQUIPMENT

Fermentation

The pilot plant installation where this work was performed is located at the CSU, Fresno enology facility. This fermentation line is provided with a bin dumper, a Demoisie Model D-8 crusher stemmer, and ancillary 3-inch diameter stainless steel must lines. Pomace pressing was performed on a Bucher RPL 18 press.

The fermentation line itself consists of four 1,412 gallon (shell volume) (1,467 nominal volume) jacketed, stainless steel fermentors (8 feet high x 5.5 feet diameter). The tanks are provided with manholes on the side at the bottom of the tank and on the conical top. In addition, each tank has a 6-inch diameter lidded hand hole on top. A 2-inch diameter vent is located at the center of the conical top. The tank shells are insulated with 3-inch thick polyurethane - aliphatic coating. Only tanks 1 and 2 were used for this experiment. Both tanks are provided with 2-inch diameter pumpover lines which extend to about 1-inch below the uppermost height of the tank shell. At this point, the pipe enters semi-tangentially into the tank to allow for as even a spray as possible. In addition, the pumpover lines are provided with a sight glass to allow for visual determination of pumpover rate and, when pumpover is not being conducted, with a means to indicate if a foamover occurs. This device permits must pumpover in what is essentially a "closed" system without the need to open either the manhole or hand hole.

Each tank is also provided with an anti-foam injector which consists of a silastic gland fitting located midway between the upper manhole and the tank vent. Each tank also has a sampling tap located 4 inches above the bottom manhole. Tank 1 was termed "reference" and tank 2 was termed "controlled." The vent of tank 1 was affixed to measuring devices to determine gas characteristics and flow. The vent of tank 2 was provided with a stainless steel capture hood which was piped to the emissions control device through 1-inch diameter piping as described below.

Cooling water (44 degrees Fahrenheit) for the tank jackets and condenser unit was provided by a 25-ton, chilled water refrigeration unit. Tank temperatures were thermostatically controlled by UE800 controllers in conjunction with Red Hat solenoid valves.

Emission Control

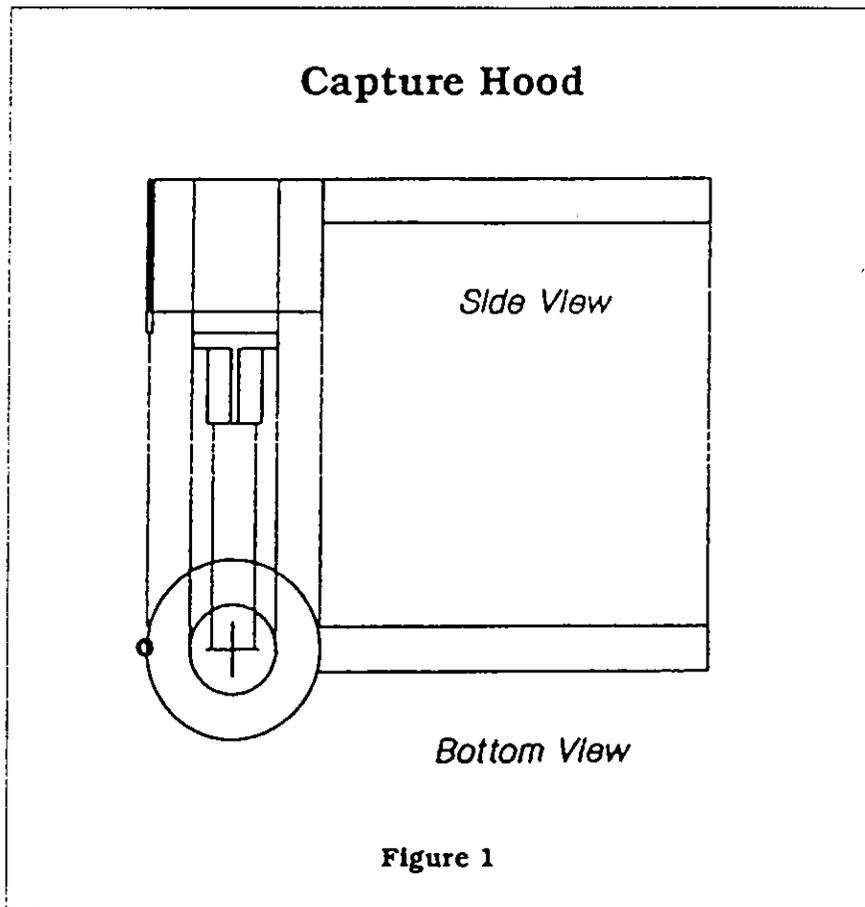
Fermentation emissions were collected from fermentation tank 2 which is fitted with a cylindrical stainless steel capture hood provided with a slitted plastic skirt that extends to the top of the tank. The purpose of this skirt is to allow some air to be drawn into the control piping. Also, this slitted skirt acts as protection should a foamover occur.

The capture hood (See Fig. 1) is connected with 1-inch stainless steel square tubing to a foamover pot. A rotameter and valve are located at the exit of this vessel. From there the line goes into a tube-in-tube chiller cooled by 44 degrees Fahrenheit water. At the exit of this chiller there is a condensate collection vessel (300 mL volume). The purpose of this chiller and condensate trap is to remove as much water as possible before passing the gas stream through a charcoal adsorption bed. The gas stream is then pumped through appropriate piping and valving into either one of two

charcoal adsorption beds enclosed in insulated 6-inch diameter x 3-foot stainless steel cylinders. After passage through the charcoal bed the stream is ducted into the atmosphere (See Fig. 2).

Each charcoal adsorption bed is also connected to a source of dry, filtered steam for purposes of regeneration. In normal operation, one bed is adsorbing volatiles while the other bed is either in the process of being regenerated or is idle.

Adsorbed volatiles freed from the charcoal upon steam regeneration are condensed into a stainless steel reservoir cooled by chilled water at 44 degrees Fahrenheit. The vent from this system is provided with an additional condenser in order to prevent the escape of volatiles into the atmosphere.



Instrumentation

The instruments for determining ethanol concentrations and gas flows out of the fermentation tanks and through the charcoal adsorption unit are listed in Table 1. The specifics of the instrumentation are noted below.

Table 1. Summary of Sampling and Analytical Methods

<u>Control to be Analyzed</u>	<u>Sampling Method</u>	<u>Analytical Method or Detection Principle</u>
Ethanol	Continuous Analyzer	FID
Gas Flows	Rotameter	Balanced Forces
Gas Volume	Positive Displacement	Positive Displacement
Gas Volume	Gas Test Meter	Expansion of Diaphragms

1. Ethanol Concentrations

Ethanol concentrations were measured with Beckman 400 flame ionization detectors (FID). The sensor is a burner. A regulated flow of sample gas passes through a flame sustained by regulated flows of zero air and hydrogen (fuel gas). Hydrocarbon compounds, such as ethanol, contained in the sample gas undergo a complex ionization producing electrons and positive ions. Polarized electrodes collect these ions, causing current to flow through electronic measuring circuitry. Current flow is proportional to the rate at which carbon atoms enter the burner.

An FID does not respond to carbon dioxide (CO_2) or water vapor which is present in the fermentation gas stream with the ethanol. An FID will respond to other hydrocarbons in the gas stream, but previous studies indicated that the concentrations of other hydrocarbons in the gas stream are insignificant relative to the concentration of ethanol.

2. Gas Flow and Volume Measurement

a. Rotameters

Rotameters measure fluid flow. They are variable-area, constant-head, rate-of-flow meters. As fluid flows upward through a tapered tube, a shaped weight within the tapered tube is lifted upward until the upward fluid force balances its weight.

b. Positive Displacement Meter

Positive displacement meters measure total gas volume. Two figure-8 shaped (two-lobed) impellers counter-rotate within a rigid casing. Gas enters and exhausts on opposite sides of the casing. The impellers are accurately produced so that a continuous seal without contact is formed at all positions during rotation. As a result the impellers rotate with very little pressure and the gas on the inlet side is effec-

tively isolated from the outlet. In rotating, an impeller traps a known specific volume of gas between its lobes and the adjacent semi-circular portion of the meter casing. Rotation of the impellers is measured by a magnetically coupled counter.

c. Test Meter

The test meter measures total volume. Gas enters one half of a double-diaphragm contained in a molded port and pan. Expansion of the diaphragm causes the metering unit to move. When one diaphragm is fully expanded, then it begins to deflate and the other diaphragm begins to expand. Expansion of the second diaphragm causes the metering unit to continue to move.

SECTION III. METHODS

Fermentations

Four fermentations were carried out in this study as follows:

- (1) Red I - Carignane grapes from CSU, Fresno vineyard, 918 gallons per tank (65 percent fill); 80 degrees Fahrenheit nominal fermentation temperature. Started 12:00 noon September 2, 1988. (Results for Red I are not presented in this report due to problems in measuring the volume of gas vented from the reference tank and collecting the ethanol captured by the charcoal adsorption unit.)
- (2) Red II - Carignane grapes from CSU, Fresno vineyards, 918 gallons per tank (65 percent fill); 80 degrees Fahrenheit nominal fermentation temperature. Started 12:00 noon September 7, 1988.
- (3) White I - Clarified French Colombard juice (provided by Gallo Winery) (2 percent solids), 918 gallons per tank (65 percent fill); 80 degrees Fahrenheit nominal fermentation temperature. This wine was fermented as a red. Started 12:00 noon September 14, 1988.
- (4) White II - Clarified juice as above, 1130 gallons per tank (80 percent fill); 55 degrees Fahrenheit nominal fermentation temperature. Started 12:00 noon September 19, 1988.

Saccharomyces cerevisiae var. Montrachet yeast was used. Zero time for each experiment (fermentation) was inoculation time. Both "reference" and "controlled" tanks were filled simultaneously. Fermentation progress was followed by measuring Balling and alcohol content (v/v by GC) at 8-hour intervals. For purposes of this study, the fermentations were considered complete when the Balling reached 2 degrees. Fermentation progress in each case may be seen in Figures 3, 4, and 5.

a. Gaseous Emissions

Sampling for ethanol in the fermentation tanks exhausts was performed in accordance with California Air Resources Board stationary source sampling method, "Method 100 - Procedures for Continuous Emission Stack Sampling." This test method is used for determining gaseous emissions from stationary sources.

For this particular study three gaseous hydrocarbon sampling instruments were available to sample the inlet and outlet of the charcoal control unit and the vent of the reference tank simultaneously. Total hydrocarbon concentration (mostly ethanol) was measured by an analyzer equipped with a flame ionization detector (FID). The gas samples were drawn through separate Teflon sampling lines by three sampling pumps and exhausted into the analyzers. Data from the three instruments were recorded on strip charts and a computer data acquisition system. The analyzers were calibrated at the ARB Sacramento facilities before the emissions test, and in the field before, during, and after each fermentation.

b. Flows

Flow rates into the control unit and analyzers were measured with rotameters. The analyzers and the control device required specific constant flows for optimum performance. The rotameters, at a glance, were able to indicate if the flows were correct. Any flow adjustment could be made quickly with the rotameters. The fermentation period was timed so total flows could be calculated.

A test gas meter and positive displacement meter measured total volume at a variety of flow rates. The test gas meter measured the gas from the reference tank to the analyzers. The positive displacement meter measured the amount of gas from the reference tank in excess of that needed by the sampling instruments. At the beginning and end of each fermentation, gas production from the reference tank was less than that required for the instruments. At those times the positive displacement meter was reversed to measure the dilution air going to the instruments.

Flow volumes out of the reference tank and flow rates through the control unit were periodically recorded during each fermentation.

SECTION IV. RESULTS

Fermentations

As mentioned above, all fermentations were considered complete for the purposes of this experiment when the Balling decreased to or below 2 degrees. Figures 3, 4, and 5 show progress for each fermentation. All fermentations were typical as shown by the decrease in Balling and the concomitant increase in alcohol content.

Since White Wine I was fermented as a red (80 degrees Fahrenheit), its fermentation curve is accelerated as compared to that of White Wine II which was fermented at 55 degrees Fahrenheit in the traditional manner.

Emissions

For each fermentation, ethanol emissions from both tanks and the charcoal adsorption unit are shown graphically in Figures 7 through 12. The figures for the reference tank (tank 1) show the ethanol concentrations in parts per million (ppm) for the different periods of time plus the cumulative ethanol emission in pounds. The figures for the controlled tank (tank 2) show ethanol concentrations in ppm into and out of the control unit and the cumulative ethanol emission in pounds into and out of the control unit. The controlled tank shows lower ethanol concentrations than the reference tank because dilution air is being drawn into the charcoal adsorption unit in order to maintain 7 cubic feet per minute flow through the unit.

The total mass emissions, in pounds of ethanol from both fermentation tanks for each fermentation are shown on Table 2 below. The range is between 1.60 and 4.14 pounds of ethanol.

Table 2. Ethanol Emissions (Uncontrolled)

<u>Fermentation</u>	¹ Reference Tank, <u>lbs. of Ethanol</u>	² Controlled Tank, 1/ <u>lbs. of Ethanol</u>
1. Red II	3.93	4.14
2. White I	3.56	3.04
3. White II	1.75	1.60

1/ Emissions from controlled tank to charcoal adsorption unit.

Table 3 below shows the total ethanol emissions into and out of the charcoal adsorption unit during each fermentation. This table also shows the control adsorption unit during each fermentation. As indicated, the control efficiency of the charcoal unit was better than 98 percent for the three fermentations.

Table 3. Control Efficiency of Ethanol Control Unit (Charcoal Adsorption)

<u>Fermentation</u>	<u>Ethanol In,</u> lbs.	<u>Ethanol Out,</u> lbs.	Control Efficiency, 1/ %	<u>Ethanol Collected 2/ from Control Unit</u> lbs.
1. Red II	4.14	0.0653	98.4	4.76 <i>5189 gms</i>
2. White I	3.04	0.00421	99.9	2.96 <i>313 gms</i>
3. White II	1.60	0.0311	98.1	1.89 <i>1130 gms</i>

1/ Efficiency = [(In-Out)/In] * 100
2/ Ethanol collected is ethanol recovered from the charcoal adsorption unit.

APPENDIX E.

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1990 DEMONSTRATION PROGRAM
ETHANOL EMISSIONS CONTROL
FROM
WINE FERMENTATION TANKS
UTILIZING CARBON ADSORPTION TECHNOLOGY

Issued: June 24, 1991

RECEIVED
AUG 2 1993

SAN JOAQUIN VALLEY
UNIFIED A.P.C.D.
NO. REGION

By: Akton Associates
737 Arnold Drive
Martinez, California

200 pounds per hour at initial steam pressures of 10 to 14 psig measured at the boiler. Outlet bed temperatures of greater than 230°F were obtained during "normal" regeneration cycles.

Condensed regeneration steam (condensate), including recovered ethanol, was collected, measured and analyzed for ethanol content prior to disposal.

Operation of the system was continuously monitored and all pertinent operations were logged at least once per hour. Logged data for all eight fermentation cycles are shown in the "Field Data" section. The duties of the emission test operators are attached as Appendix 2.

Both inlet and outlet ethanol concentrations were monitored by CARB personnel during runs 6, 7 & 8. Chart data for these tests are attached as Appendix 4.

FERMENTATION CYCLES

A total of eight fermentation cycles were conducted between August 29 and September 28, 1990. Fermentation cycles 1, 2 and 8 were conducted with clarified juice at fermentation temperature of approximately 58°F. Initial Ballings (% sugar w/w) were approximately 20° and final alcohol contents were approximately 12%. Tank fill was a nominal 170,000 gallons.

The remaining fermentation cycles 3 through 7, were red fermentations at nominal fermentation temperatures of 73°F. Initial Ballings were approximately 23°, and final alcohol contents varied from 8.6 to 10.2 % before transfer to other tanks.

All fermentation practices utilized were normal E. & J. Gallo Winery operating procedures. Exhibits 1 through 8 show relationships between time, sugar content, alcohol content and fermentation temperature for each cycle.

All sampling procedures, analysis and record keeping were conducted by E. & J. Gallo Winery personnel in accordance with normal winery operation, and as required by appropriate governmental agencies.

RESULTS OF FERMENTATIONS

Combined average results of fermentation conditions and quantities and composition of carbon regeneration condensate are shown in Tables 1 and 2.

A carbon activity analysis was conducted on a composite sample of carbon removed from the carbon beds after the final regeneration of the carbon at the conclusion of the tests. The reported "slight loss of activity" was judged by the equipment manufacturer to be typical for carbon which has been in service. A report of these tests is included as Appendix 3.

Results of "wipe tests" on inside surfaces of ducting to judge sanitation conditions were negative. Minimal carryover of foam or juice from the tank was noted. Significant

discoloring of the hood was noted. No significant foam-over was detected during the program. It was reported that on one occasion, carryover required more extensive cleaning than simply wiping the duct interior. This was not thought to be significant enough to require recording, and the cleaning was completed by operating personnel.

Pressure drop through the carbon beds, (fan discharge to carbon bed outlet), remained constant at approximately 12.0 inches water column at low CO₂ concentrations. Internal fermentation tank pressures of 0.025 inches water column were measured at maximum red fermentation rates and with the adsorption system in normal operation.

The calculated amount of fuel required for the boiler during a normal red wine fermentation cycle requiring an average of 14 regenerations was 6.4 million BTU. Cooling water volume was not measured, but cooling must be supplied at a rate of 25,000 BTU per hour to condense regeneration steam and alcohol.

1990 DEMONSTRATION PROGRAM FERMENTATION CONDITIONS

TABLE 1

No.	Fermentation Type	Date	Volume Fermented (Gallons)	Total Hours	Avg. Temp. (*F)	Initial Balling	Final Balling	Final Alcohol (% v/v)
1	White	8/29-9/3	172,000	164	59	20.0	≤0.2*	12.0
2	White	9/5-9/11	170,000	148	56	20.0	≤0.1*	12.0
3	Red	9/12-9/13	164,000	32	72	23.2	6.5	9.5
4	Red	9/14-9/15	164,000	28	74	23.0	6.2	9.3
5	Red	9/16-9/17	164,000	32	73	23.0	5.0	9.6
6	Red	9/18-9/19	160,000	36	73	22.8	7.0	8.9
7	Red	9/20-9/22	160,000	48	74	22.6	4.6	10.2
8	White	9/23-9/28	170,000	128	57	21.6	≤0.7*	11.7

* Residual Sugar

Note: Fermentation Tank 30'-0" φ X 207,000 gallons

1990 DEMONSTRATION PROGRAM
CONDENSATE QUANTITIES AND ANALYSIS
TABLE 2

Fermentation Number	Condensate Collected (Gallons)	Alcohol Content (% v/v)	Alcohol (Pounds)	Pounds Alcohol Per 1000 Gals. Fermented
1	383	9.45	238.3	1.39(a)
2	775	7.75	395.5	2.33
3	275	25.45	460.8	2.80
4	220	24.55	355.6	2.16(b)
5	325	21.85	467.6	2.85(b)
6	352	21.85	506.4	3.17
7	454	21.30	636.7	3.98
8	339	12.50	279.0	1.64

(a) Programming and fan problems resulted in significant unit down-time

(b) Wet carbon beds noted

DISCUSSION OF OPERATIONS

Several major operational problems were encountered during the program. While all were corrected without disturbing the normal fermentation cycle, significant down-time was experienced and, therefore, the overall capture of emitted alcohol was reduced. Since only one fermentation tank was connected to the system, the quantity of ethanol not captured would be variable with the type of wine fermenting and the point in the fermentation cycle. Operational problems included:

- 1) Excessive fan vibration resulting from failed bearing and distorted shaft. Unit was shut-down and parts replaced.
- 2) Shut-down of analyzer system on several occasions due to:
 - a) loss of fuel
 - b) loss of ignition

c) moisture in inlet line

d) sample pump failure

Adsorption unit was bypassed in all cases and analyzer system problems corrected. Time loss was variable from 30 minutes to three hours on each occasion.

3) Initial programming problems of regeneration cycle controller resulted in delayed start-up of unit during initial fermentation cycle.

4) Plugging of condensate withdrawal lines resulting in incomplete regeneration cycles during fermentation cycles 4 and 5. Carbon fines migrated through support screens and plugged drain piping, resulting in an inability to achieve desired regeneration cycles. The unit was shut down and lines cleared. This problem, which was assumed to be a result of new carbon, resulted in both lost unit availability during repair and inefficient operation during period before repair.

Minor operational difficulties were also encountered, but resulted in minimal disruption of unit availability. These include:

Failure of pressure gauges

Adjustment of rental boiler steam pressure controls

Carbon Efficiency - Calculations based on average carbon adsorber outlet gas ethanol concentrations and total amounts of alcohol condensed indicate that alcohol removal efficiencies of greater than 98% were achieved for red wine fermentation cycles 6 and 7 and greater than 97% for white wine fermentation 8. Comparison of inlet versus outlet VOC concentrations as measured by CARB staff confirms that these results were achieved on an overall basis. Analyzer data for three fermentation runs, included herein as Appendix 4, confirms the overall efficiencies noted above. It should be noted that these efficiencies are for the carbon adsorber units only, and do not reflect overall system capture and abatement efficiency. As addressed above, total capture may have been less than 90% during short periods of red wine fermentation.

Overall Efficiency - Overall efficiency is also effected by pumpover and sampling practice. The fermentation tank utilized had facilities which allowed both sampling and pumpover without requiring the removal of tank top opening covers. Capture of gases evolved from the tank during fermentation was, therefore, primarily limited by hood capture efficiency and system flow rate capacity.

Ethanol to Carbon Ratios - The amount of ethanol adsorbed per pound of carbon for each regeneration cycle was within the normally expected range of alcohol concentrations and bed temperatures experienced. Calculated averages were 0.052 pounds ethanol per pound of carbon for red wines and 0.025 pounds per pound of carbon for white wine.

Ethanol Content of Condensate - Condensate ethanol concentrations of 21 to 25% (v/v) for red wine fermentations and 8 to 12% for white wine were observed. These values are

WINE III, FERMENTATION 6

Date	Time	THC, ppm C3 In	Out	Recovery, percent
	1030	1300	22	98.3
	1100	1350	23	98.3
	1130	1300	12	99.1
	1200	1800	14	99.2
	1230	1950	20	99.0
	1300	1850	22	98.8
	1330	1800	15	99.2
	1400	1900	16	99.2
	1430	2050	21	99.0
	1500	2100	14	99.3
	1530	1750	13	99.3
	1600	1800	15	99.2
	1630	1650	14	99.2
	1700	1550	11	99.3
	1730	1500	12	99.2
	1800	1500	14.5	99.0
	1830	1450	11	99.2
	1900	1400	11	99.2
	1930	1450	12	99.2
	2000	1450	15	99.0
	2030	1500	13	99.1
	2100	1500	11	99.3
	2130	1500	11	99.3
	2200	1550	13	99.2
	2230	1550	10	99.4
	2300	1600	11	99.3
	2330	1650	9	99.5
9/20/90	2400	1700	9	99.5
	0030	1800	9	99.5
	0100	1800	8	99.6
	0130	1800	7	99.6
	0200	1800	7	99.6
	0230	750	7.5	99.0
	0300	1800	8	99.6
	0330	1800	7	99.6
END	0400	1650	6.5	99.6
AVERAGES		1093	12	97.0
(Ferm. only)		Overall	Eff. =>	98.9
Emptying	0430	1150	6.5	99.4
Tank	0500	800	6	99.3
	0530	700	6	99.1
	0600	600	5.5	99.1

WINE III, FERMENTATION 7

Date	Time	THC, ppm C3 In	Out	Recovery, percent
	1200	1400	14	99.0
	1230	1350	18	98.7
	1300	1300	12	99.1
	1330	1250	8	99.4
	1400	1200	11	99.1
	1430	1250	13	99.0
	1500	1350	10	99.3
	1530	1400	9	99.4
	1600	1450	12	99.2
	1630	1450	14	99.0
	1700	1450	10	99.3
	1730	1425	13	99.1
	1800	1500	18	98.8
	1830	1500	11	99.3
	1900	1500	11	99.3
	1930	1550	18	98.8
	2000	1500	14	99.1
	2030	1350	6	99.6
	2100	1300	14	98.9
	2130	1350	19	98.6
	2200	1350	8	99.4
	2230	1325	8	99.4
	2300	1400	13	99.1
	2330	1500	22	98.5
9/22/90	2400	1550	11	99.3
	0030	1450	10	99.3
	0100	1450	19	98.7
	0130	1450	22	98.5
	0200	1450	8	99.4
	0230	1450	10	99.3
	0300	1525	14	99.1
	0330	1550	23	98.5
	0400	1550	11	99.3
	0430	1475	13	99.1
	0500	1350	27	98.0
	0530	1425	20	98.6
	0600	1500	9	99.4
	0630	1450	14	99.0
	0700	1500	19	98.7
	0730	1500	23	98.5
	0800	1575	23	98.5
	0830	1000	18	98.2
	0900	850	29	96.6
	0930	800	22	97.3
	1000	550	8	98.5
	1030	400	10	97.5
	1100	350	10	97.1
End	1130	250	13	94.8
AVERAGES		960	13	97.2
		Overall Eff. =>		98.6

WINE III, FERMENTATION 8

Date	Time	THC, ppm In	C3 Out	Recovery, percent
	0700	310	11	96.5
	0800	280	19	93.2
	0900	290	6	97.9
	1000	290	4	98.6
	1100	300	5	98.3
	1200	330	13	96.1
	1300	320	20	93.8
	1400	300	34	88.7
	1500	280	4	98.6
	1600	270	6	97.8
	1700	260	27	89.6
	1800	270	3	98.9
	1900	260	4	98.5
	2000	270	9	96.7
	2100		19	
	2200		29	
	2300		42	
9/28/90	2400		59	
	0100		1	
	0200		2	
	0300		5	
	0400		8	
	0500		14	
	0600			
	0700			
	0800	280	65	76.8
	0900	290	2	99.3
	1000	290	4	98.6
	1100	340	5	98.5
	1200	350		100.0
	1300	360	37	89.7
	1400	320	27	91.6
AVERAGES		213	16	88.0
		Overall Eff. =>		92.5

APPENDIX F.



E. & J. GALLO WINERY

Modesto, California

December 14, 1992

RECEIVED

DEC 18 1992

San Joaquin Valley Unified
Air Pollution Control District

Maria Lima
S.J.U.V.A.P.C.D.
1999 Tuolumne Street
Fresno, CA 93721

Dear Ms. Lima:

Enclosed is the protocol for, and results of, the full scale fermentation emission tests conducted at E. & J. Gallo's Fresno Winery. As the attached documentation shows, these tests were devised in conjunction with the staff of the California Air Resources Board, and monitored by members of the staff. The primary purpose was to develop emission factors for ethanol during fermentation. This could be done very accurately since all of the emissions during each of eight fermentations were trapped on granular activated carbon, then steamed off and condensed. The volume of the condensate was measured in each case, and a comprehensive chemical analysis performed by gas chromatography. Although the chief objective was to obtain an accurate measurement of ethanol content, other constituents, including acetaldehyde, were also quantitated. This provided the basis for our estimate of total acetaldehyde emissions. The average acetaldehyde emitted during the red and white fermentations was calculated in pounds per thousand gallons and then applied to the total amount of wine fermented that year in each category.

Copies of the analytical data sheets, the volume of condensate for each test fermentation, the calculations of the average acetaldehyde content for the red and white fermentations, and (as confidential information) the total gallons of red and white wine fermented that year are included.

These should give the background on the whole ethanol emission measurement history, and the information taken from those experiments which were used to quantitate the acetaldehyde emissions and to give a rough estimate of the H₂S levels based on frequent sampling using Dräger tubes. (We realize that Dräger

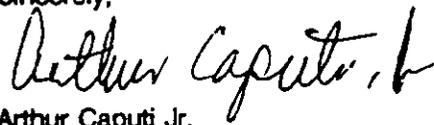
- continued -

Maria Lima
Page 2

December 14, 1992

tubes are not sanctioned for official measurement, but we were able to take measurements throughout a fermentation cycle to get an idea of the amounts emitted and if those emissions varied within the duration of the fermentation. As the results showed, H₂S quantities varied tremendously; some fermentations had none, and those which tested positive did not show a consistent pattern of emission.

Sincerely,



Arthur Caputi Jr.

ACJ:el

In accordance with our proposed inventory plan for the Emission Inventory Criteria and Guidelines Regulation for the Administration of the Air Toxics "Hot Spots" Information and Assessment Act of 1987, Gallo formulated a source test to determine the amount of acetaldehyde emitted from our fermenters. During the fermentation, condensate was collected and the acetaldehyde concentration was determined by gas chromatography. The following calculations were used to determine the total amount of acetaldehyde emitted from the fermentations during our 1990 crushing season.

Acetaldehyde Calculations

(Modesto Lab Results)

Fermentation #1

(White)
(170,016 gals)

383 gal. condensate x 3.78 L = 1,447.7 L
 22 mg/L x 1,447.7 = 31,849.4 mg = 31.8 g
 31.8g + 453.5 g/lb = 0.07 lb
 0.07 lb + 170.0 = 0.00041 lb/1000 gals.

Fermentation #2

(White)
(172,322 gals)

484 gal. condensate (fraction #1) x 3.78 L = 1,829.5 L
 20 mg/L x 1,829.5 = 36,590 mg = 36.6 g
 36.6 g + 453.5 g/lb = 0.08 lb

291 gal. condensate (fraction #2) x 3.78 L = 1,100 L
 23 mg/L x 1,100 = 25,300 mg = 25.3 g
 25.3 g + 453.5 g/lb = 0.06 lb

0.08 lb + 0.06 lb = 0.14 lb
 0.14 lb + 172.3 = 0.00081 lb/1000 gals.

Fermentation #3

(Red)
(157,120 gals)

275 gal. condensate x 3.78 L = 1,039.5 L
 84 mg/L x 1,039.5 = 87,318 mg = 87.3 g
 87.3 g + 453.5 g/lb = 0.19 lb
 0.19 lb + 157.1 = 0.0012 lb/1000 gals.

Fermentation #4

(Red)
(152,740 gals)

220 gal. condensate x 3.78 = 831.6 L
 87 mg/L x 831.6 L = 72,349 mg = 72.3 g
 72.3 g + 453.5 g/lb = 0.16 lb
 0.16 lb + 152.7 = 0.001 lb/1000 gals.

Fermentation #5
(Red)
(145,280 gals)

$$\begin{aligned} 325 \text{ gal. condensate} \times 3.78 &= 1,228.5 \text{ L} \\ 114 \text{ mg/L} \times 1,228.5 \text{ L} &= 140,009 \text{ mg} = 140.0 \text{ g} \\ 140.0 \text{ g} + 453.5 \text{ g/lb} &= 0.31 \text{ lb} \\ 0.31 \text{ lb} + 145.3 &= \underline{0.0021 \text{ lb/1000 gals.}} \end{aligned}$$

Fermentation #6
(Red)
(146,145 gals)

$$\begin{aligned} 352 \text{ gal. condensate} \times 3.78 &= 1,330.6 \text{ L} \\ 169 \text{ mg/L} \times 1,330.6 &= 224,871.4 \text{ mg} = 224.9 \text{ g} \\ 224.9 \text{ g} + 453.5 \text{ g/lb} &= 0.50 \text{ lb} \\ 0.50 \text{ lb} + 146.1 &= \underline{0.0034 \text{ lb/1000 gals.}} \end{aligned}$$

Fermentation #7
(Red)
(144,475 gals)

$$\begin{aligned} 454 \text{ gal. condensate} \times 3.78 &= 1,716 \text{ L} \\ 226 \text{ mg/L} \times 1,716.1 &= 387,838.6 \text{ mg} = 387.8 \text{ g} \\ 387.8 \text{ g} + 453.5 \text{ g/lb} &= 0.86 \text{ lb} \\ 0.86 \text{ lb} + 144.5 &= \underline{0.0060 \text{ lb/1000 gals.}} \end{aligned}$$

Fermentation #8
(White)
(169,028 gals)

$$\begin{aligned} 339 \text{ gal. condensate} \times 3.78 &= 1,281.4 \text{ L} \\ 58 \text{ mg/L} \times 1,281.4 &= 74,321.2 \text{ mg} = 74.3 \text{ g} \\ 74.3 \text{ g} + 453.5 \text{ g/lb} &= 0.16 \text{ lb} \\ 0.16 \text{ lb} + 169.0 &= \underline{0.0009 \text{ lb/1000 gals.}} \end{aligned}$$

$$\begin{aligned} \text{Average lb acetaldehyde (white)} &= 0.00041 + 0.00081 + 0.0009 + 3 \\ &= 0.00071 \text{ lb/1000 gals} \end{aligned}$$

$$\begin{aligned} \text{Average lb acetaldehyde (red)} &= 0.0012 + 0.001 + 0.0021 + 0.0034 + 0.0060 + 5 \\ &= 0.00274 \text{ lb/1000 gals} \end{aligned}$$

A. CAPUTI-RES

ID: RES

TANK: ART

3100=60=0358 EXP. RUN #1

173 REQ 07Sep90 1120 DRAW 04Sep90 0000 C B

	22			
ALC	11.75	MG/L	acetal	
ALC	11.75	VOL %		
ALD	40.	MG/L		
FD	281.	MG/L		
FSO2	5.	MG/L	free SO ₂	
ISOA	149.	MG/L	isoamyl alc.	
ISO3	23.	MG/L	isoethyl "	
MEOH	47.	MG/L		
NBUT	UND	MG/L	n-butanol	UNDETECTABLE
NPRO	87.	MG/L	n-propyl alc.	
PH	3.56			
RSLC	0.04	GM/100ML	reducing sugar by liq. chrom.	
SEC3	UND	MG/L	sec-butanol	UNDETECTABLE
TA	0.64	G/100ML	total acids	
TSO2	65.	MG/L	total SO ₂	
VA	0.023	G/100ML	volatile acid	

Fermentation #1

10-10-90 07:17 AM

RESEARCH SUMMARY

ID: RES

TANK: AC

0000=00=0000

9798 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #7

ACTA	226.	MG/L	<i>acetal</i>
ALC	21.35	VOL %	<i>EtOH</i>
ALD	170.	MG/L	<i>aldehyde</i>
FO	1558.	MG/L	<i>fuel oil</i>
ISOA	1010.	MG/L	
ISOB	217.	MG/L	
MEOH	88.	MG/L	
NBUT	2.	MG/L	
NPRO	100.	MG/L	
SECB	2.	MG/L	
VA	0.019	G/100ML	

9799 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #5

ACTA	114.	MG/L	
ALC	21.95	VOL %	
ALD	260.	MG/L	
FO	1082.	MG/L	
ISOA	631.	MG/L	
ISOB	193.	MG/L	
MEOH	119.	MG/L	
NBUT	2.	MG/L	
NPRO	140.	MG/L	
SECB	UND	MG/L	
VA	0.009	G/100ML	

UNDETECTABLE

ACC 9800 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B RUN #6

ACTA	169.	MG/L	
ALC	21.80	VOL %	
ALD	180.	MG/L	
FO	1298.	MG/L	
ISOA	793.	MG/L	
ISOB	217.	MG/L	
MEOH	109.	MG/L	
NBUT	2.	MG/L	
NPRO	114.	MG/L	
SECB	3.	MG/L	
VA	0.011	G/100ML	

ACC 9801 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B

ACTA	169.	MG/L	
ALC	7.10	VOL %	
ALD	105.	MG/L	
FO	259.	MG/L	
ISOA	143.	MG/L	
ISOB	22.	MG/L	
MEOH	22.	MG/L	
NBUT	UND	MG/L	
NPRO	74.	MG/L	
SECB	UND	MG/L	
VA	0.013	G/100ML	

fermentation #2A

UNDETECTABLE

UNDETECTABLE

10-10-90 07:17 AM

RESEARCH SUMMARY

CC: A CAPUTI-RES

CC: A. CAPUTI-RES

L ID: RES

TANK: AC

0000=00=0000

ACC 9795 REG 09Oct90 1526 DRAW 09Oct90 0000 C B

		MG/L
ALC	9.15	VOL %
ALD	95.	MG/L
FO	324.	MG/L
ISDA	189.	MG/L
ISOB	23.	MG/L
MEOH	19.	MG/L
NBUT	UND	MG/L
NPRO	89.	MG/L
SECB	UND	MG/L
VA	0.006	Q/100ML

fermentation #2 B

UNDETECTABLE

UNDETECTABLE

ACC 9796 REG 09Oct90 1526 DRAW 09Oct90 0000 C B

RUN #3

ACTA	84.	MG/L
ALC	25.05	VOL %
ALD	745.	MG/L
FO	1212.	MG/L
ISDA	632.	MG/L
ISOB	152.	MG/L
MEOH	230.	MG/L
NBUT	5.	MG/L
NPRO	338.	MG/L
SECB	UND	MG/L
VA	0.010	Q/100ML

UNDETECTABLE

ACC 9797 REG 09Oct90 1526 DRAW 09Oct90 0000 C B

RUN #4

ACTA	87.	MG/L
ALC	24.60	VOL %
ALD	550.	MG/L
FO	1299.	MG/L
ISDA	671.	MG/L
ISOB	165.	MG/L
MEOH	199.	MG/L
NBUT	6.	MG/L
NPRO	369.	MG/L
SECB	2.	MG/L
VA	0.011	Q/100ML

10-10-90 07:17 AM

RESEARCH SUMMARY

A. CAPUTI-RES

CC: A. CAPUTI-RES

ID: RES

TANK: AC

0000=00=0000

9795 REG 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #28

ACTA	23.	MG/L
ALC	9.15	VOL %
ALD	55.	MG/L
FO	324.	MG/L
ISOA	189.	MG/L
ISOB	23.	MG/L
MEOH	19.	MG/L
NBUT	UND	MG/L
NPRO	89.	MG/L
SECB	UND	MG/L
VA	0.006	Q/100ML

UNDETECTABLE

UNDETECTABLE

ACC 9796 REG 09Oct90 1526 DRAW 09Oct90 0000 C B

94

ALC	25.05	MG/L
ALD	745.	MG/L
FO	1212.	MG/L
ISOA	632.	MG/L
ISOB	152.	MG/L
MEOH	230.	MG/L
NBUT	5.	MG/L
NPRO	338.	MG/L
SECB	UND	MG/L
VA	0.010	Q/100ML

Fermentation #3

UNDETECTABLE

ACC 9797 REG 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #4

ACTA	87.	MG/L
ALC	24.60	VOL %
ALD	550.	MG/L
FO	1299.	MG/L
ISOA	671.	MG/L
ISOB	165.	MG/L
MEOH	199.	MG/L
NBUT	6.	MG/L
NPRO	369.	MG/L
SECB	2.	MG/L
VA	0.011	Q/100ML

CC: A. CAPUTI-RES

CC: A. CAPUTI-RES

L ID: RES

TANK: AC

0000=00=0000

ACC 9795 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #2B

ACTA	23.	MG/L	
ALC	9.15	VOL %	
ALD	55.	MG/L	
FD	324.	MG/L	
ISOA	189.	MG/L	
ISOB	23.	MG/L	
MEOH	19.	MG/L	
NBUT	UND	MG/L	UNDETECTABLE
NPRO	89.	MG/L	
SECB	UND	MG/L	UNDETECTABLE
VA	0.006	G/100ML	

ACC 9796 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #3

ACTA	84.	MG/L	
ALC	25.05	VOL %	
ALD	745.	MG/L	
FD	1212.	MG/L	
ISOA	632.	MG/L	
ISOB	152.	MG/L	
MEOH	230.	MG/L	
NBUT	5.	MG/L	
NPRO	338.	MG/L	
SECB	UND	MG/L	UNDETECTABLE
VA	0.010	G/100ML	

ACC 9797 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B

87

ALC	24.60	VOL %	
ALD	550.	MG/L	
FD	1299.	MG/L	
ISOA	671.	MG/L	
ISOB	165.	MG/L	
MEOH	199.	MG/L	
NBUT	6.	MG/L	
NPRO	369.	MG/L	
SECB	2.	MG/L	
VA	0.011	G/100ML	

fermentation #4

10-10-90 07:17 AM

RESEARCH SUMMARY

L ID: RES

TANK: AC

0000=00=0000

ACC 9798 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #7

ACTA	226.	MG/L
ALC	21.35	VOL %
ALD	170.	MG/L
FO	1558.	MG/L
ISOA	1010.	MG/L
ISOB	217.	MG/L
MEOH	88.	MG/L
NBUT	2.	MG/L
NPRO	100.	MG/L
SECB	2.	MG/L
VA	0.019	G/100ML

ACC 9799 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B

114

ALC	21.95	VOL %
ALD	260.	MG/L
FO	1082.	MG/L
ISOA	631.	MG/L
ISOB	193.	MG/L
MEOH	119.	MG/L
NBUT	2.	MG/L
NPRO	140.	MG/L
SECB	UND	MG/L
VA	0.009	G/100ML

fermentation #5

UNDETECTABLE

ACC 9800 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B RUN #6

ACTA	169.	MG/L
ALC	21.80	VOL %
ALD	180.	MG/L
FO	1298.	MG/L
ISOA	793.	MG/L
ISOB	217.	MG/L
MEOH	109.	MG/L
NBUT	2.	MG/L
NPRO	114.	MG/L
SECB	3.	MG/L
VA	0.011	G/100ML

ACC 9801 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B

RUN #2A

ACTA	20.	MG/L
ALC	7.10	VOL %
ALD	105.	MG/L
FO	259.	MG/L
ISOA	143.	MG/L
ISOB	22.	MG/L
MEOH	22.	MG/L
NBUT	UND	MG/L
NPRO	74.	MG/L
SECB	UND	MG/L
VA	0.013	G/100ML

UNDETECTABLE

UNDETECTABLE

L ID: RES

TANK: AC

0000=00=0000

ACC 9798 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #7

ACTA	226.	MG/L
ALC	21.35	VOL %
ALD	170.	MG/L
FO	1558.	MG/L
ISOA	1010.	MG/L
ISOB	217.	MG/L
MEOH	88.	MG/L
NBUT	2.	MG/L
NPRO	100.	MG/L
SECB	2.	MG/L
VA	0.019	G/100ML

ACC 9799 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #5

ACTA	114.	MG/L
ALC	21.95	VOL %
ALD	260.	MG/L
FO	1082.	MG/L
ISOA	631.	MG/L
ISOB	193.	MG/L
MEOH	119.	MG/L
NBUT	2.	MG/L
NPRO	140.	MG/L
SECB	UND	MG/L
VA	0.009	G/100ML

UNDETECTABLE

ACC 9800 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B ~~1527~~

169

ALC	21.80	VOL %
ALD	180.	MG/L
FO	1298.	MG/L
ISOA	793.	MG/L
ISOB	217.	MG/L
MEOH	109.	MG/L
NBUT	2.	MG/L
NPRO	114.	MG/L
SECB	3.	MG/L
VA	0.011	G/100ML

Fermentation #6

ACC 9801 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B RUN #2A

ACTA	20.	MG/L
ALC	7.10	VOL %
ALD	103.	MG/L
FO	259.	MG/L
ISOA	143.	MG/L
ISOB	22.	MG/L
MEOH	22.	MG/L
NBUT	UND	MG/L
NPRO	74.	MG/L
SECB	UND	MG/L
VA	0.013	G/100ML

UNDETECTABLE

UNDETECTABLE

10-10-90 07:17 AM

RESEARCH SUMMARY

L ID: RES

TANK: AC

0000=00=0000

ACC 9798 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B

226

		MG/L
ALC	21.35	VOL %
ALD	170.	MG/L
FO	1558.	MG/L
ISOA	1010.	MG/L
ISOB	217.	MG/L
MEOH	88.	MG/L
NBUT	2.	MG/L
NPRO	100.	MG/L
SECB	2.	MG/L
VA	0.019	G/100ML

fermentation #7

ACC 9799 REQ 09Oct90 1526 DRAW 09Oct90 0000 C B RUN #5

ACTA	114.	MG/L
ALC	21.95	VOL %
ALD	260.	MG/L
FO	1082.	MG/L
ISOA	631.	MG/L
ISOB	193.	MG/L
MEOH	119.	MG/L
NBUT	2.	MG/L
NPRO	140.	MG/L
SECB	UND	MG/L
VA	0.009	G/100ML

UNDETECTABLE

ACC 9800 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B RUN #6

ACTA	169.	MG/L
ALC	21.80	VOL %
ALD	180.	MG/L
FO	1298.	MG/L
ISOA	793.	MG/L
ISOB	217.	MG/L
MEOH	109.	MG/L
NBUT	2.	MG/L
NPRO	114.	MG/L
SECB	3.	MG/L
VA	0.011	G/100ML

ACC 9801 REQ 09Oct90 1527 DRAW 09Oct90 0000 C B RUN #2A

ACTA	20.	MG/L
ALC	7.10	VOL %
ALD	105.	MG/L
FO	259.	MG/L
ISOA	143.	MG/L
ISOB	22.	MG/L
MEOH	22.	MG/L
NBUT	UND	MG/L
NPRO	74.	MG/L
SECB	UND	MG/L
VA	0.013	G/100ML

UNDETECTABLE

UNDETECTABLE

10-03-90 07:12 AM

RESEARCH SUMMARY

CC: A. CAPUTI-RES

L ID: RES

TANK: ART

0000-00-0000 EXP. RUN #8

ACC 7645 REQ 02Oct90 0858 DRAW 28Sep90 0000 C 4 TK: 2930 CONDENSATE

ACTA	58.	MG/L
ALC	12.35	VOL %
ALD	105.	MG/L
FO	638.	MG/L
ISOA	388.	MG/L
ISOB	47.	MG/L
MEOH	16.	MG/L
NBUT	UND.	MG/L
NPRO	145.	MG/L
SECB	UND.	MG/L
VA	0.020	0/100ML

fermentation #8

UNDETECTABLE
UNDETECTABLE

Hydrogen Sulfide Emission Factors

Red Fermentations:

Fermentation No.	Lbs. H ₂ S Produced	Gallons Fermented	<i>lbs./1,000gal</i>
<i>77°F 20'3</i> 3	0	157,120	0
<i>77°F 20'3</i> 4	0	152,740	0
<i>77°F 20'3</i> 5	0.42	145,280	<i>0.0029</i>
<i>77°F 20'3</i> 6	0.33	146,145	<i>0.0023</i>
<i>77°F 20'3</i> 7	0.51	144,475	<i>0.0035</i>
Totals	1.26	745,760	

Factor = 0.0017 lbs. H₂S/1,000 gallons (1.26/745,760)

White Fermentation:

Fermentation No.	Lbs. H ₂ S Produced	Gallons Fermented	<i>lbs./1,000gal</i>
<i>57°F 21.6'3</i> 8	0.24	169,028	<i>0.0014</i>

Factor = 0.0014 lbs. H₂S/1,000 gallons (0.24/169,028)

Hydrogen Sulfide Calculations

1990 Fermentation - Fresno¹

Fermentation #3
(Red)

0 Hydrogen Sulfide

Fermentation #4
(Red)

0 Hydrogen Sulfide

Fermentation #5
(Red)*

Portion of ferm. with measurable H₂S = 16 hours
Average H₂S = 4 + 5 + 2 = 4.5 ppm
(4.5 ppm + 10⁶) x (66,000 x 16 hrs) = 4.75 ft³
4.75 ft³ + 11.23 ft³/lb = 0.42 lb H₂S

Fermentation #6
(Red)

Portion of ferm. with measurable H₂S = 8 hours
Average H₂S = 7 ppm
(7 ppm + 10⁶) x (66,000 x 8 hrs) = 3.7 ft³
3.7 ft³ + 11.23 ft³/lb = 0.33 lb H₂S

Fermentation #7
(Red)

Portion of ferm. with measurable H₂S = 17 hours
Average H₂S = (6 + 4 + 6 + 5 + 4.5) + 5 = 5.1 ppm
(5.1 ppm + 10⁶) x (66,000 x 17) = 5.72 ft³
5.72 ft³ + 11.23 ft³/lb = 0.51 lb H₂S

1. Factors Used in the Following Calculations:

1,100 cfm x 60 = 66,000 cfh

To calculate the number of volumes of gas: ppm H₂S is
divided by 1,000,000

H₂S = 11.23 ft³/lb

Fermentation #8
(White)

Portion of ferm. with measurable H₂S = 16 hours
Average H₂S = (4 + 1.25) ÷ 2 = 2.6 ppm
(2.6 ppm ÷ 10⁶) x (66,000 x 16) = 2.75 ft³
2.75 ft³ ÷ 11.23 ft³/lb = 0.24 lb H₂S

Hydrogen Sulphide Concentration - 1990 Fermentations

Hydrogen Sulphide Concentration - Fermentation #3 (Red)

time/ date	0710	1020	1100	1425	1500	1600	2300
9/12	0		0		0		0
9/13		0		0		0	

Hydrogen Sulphide Concentration - Fermentation #4 (Red)

time/ date	0710	1210	1315	1600	1700
9/14			0	0	
9/15	0	0			0

Hydrogen Sulphide Concentration - Fermentation #5 (Red)

time/date	1130	1855	2300
9/16			0
9/17	4	5	0

Hydrogen Sulphide Concentration - Fermentation #6 (Red)

time/date	0640	1200	1530	2330	2355
9/18			0		0
9/19	0	7		0	

Hydrogen Sulphide Concentration - Fermentation #7 (Red)

time/date	0640	0720	1220	1505	2345
9/20				0	0
9/21	6	4	6	5	4.5

Hydrogen Sulphide Concentration - Fermentation #8 (White)

time/date	0630	0640	0645	0705	1205	1210	1230	1320	1530	2330	2345
9/23									0	4	
9/24				0	0						0
9/25			0			0					0
9/26	0						0				
9/27		0						Trace		0	
9/28				1.25							

Hydrogen Sulphide Concentration (ppm) - Fermentations 72 - 79 - 1990 (Frey)

date/hm	9/12	9/13	9/14	9/15	9/16	9/17	9/18	9/19	9/20	9/21	9/23	9/24	9/25	9/26	9/27	9/28
0630																
0640								0		6			0		0	
0650																
0700												0				
0710	0			0						4						1.23
1020		0														
1100	0															
1130						4										
1200								7								
1210				0												
1220									0					0		
1230															0	
1315			0													
1320															Tr.	
1425		0														
1515	0								0	5						
1530							0							0		
1800			0	0												
1700					0											
1740																
1855						5										
1920																
2000	0							0								
2030																
2345							0	0	0	4.5	4	0	0		0	

APPENDIX G.

AIR RESOURCES BOARD

2020 L STREET
P.O. BOX 2815
SACRAMENTO, CA 95814-2815



November 1, 1994

Mark Boese
Deputy Air Pollution Control Officer
San Joaquin Valley Unified Air Pollution Control District
1990 Tuolumne Street, Suite 200
Fresno, California 93721

Dear Mr. Boese:

As discussed during our recent telephone conversation, I am writing to provide you with a summary of our analysis of the data collected during the pilot studies conducted at the California State University, Fresno, and the full scale demonstration study conducted at the Gallo Winery in Fresno. Based on our analysis, we intend to revise our emission inventory for wineries and revise our original estimate of cost effectiveness for controlling winery emissions.

Winery Emission Inventory

Based on the most recent source test data, the emission factors for white wine fermentation is about 1.9 pounds of ethanol emitted per 1,000 gallons of wine fermented. The emission factor for red wine is about 4.7 pounds of ethanol emitted per 1,000 gallons of wine fermented. These new emission factors are approximately 30 percent less than the emission factors that were presented in the technical support document for the Air Resources Board's suggested control measure for winery emissions. Therefore, we recommend that the new emission factors be used to revise the winery emission inventory.

Cost Effectiveness to Control Winery Emissions

Based on the new emission factors and our winery tank usage survey, we have recalculated the cost effectiveness to control winery emissions. The new cost effectiveness ranges from about \$40,000 to \$120,000 per ton of emissions reduced.

Mr. Mark Boese

November 1, 1994

Page Two

If you have any questions regarding the information that I have provided or need further assistance, please call me at (916) 322-6020, or have your staff call Mr. Gary Yee, Manager, Industrial Section, Criteria Pollutants Branch, Stationary Source Division, at (916) 327-5986.

Sincerely,



Dean C. Simeroth, Chief
Criteria Pollutants Branch

cc: Michael H. Scheible
Deputy Executive Officer
Air Resources Board

Arthur Caputi
E & J Gallo Winery
Post Office Box 1130
Modesto, California 95353