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## **Background Report Reference**

**AP-42 Section Number:** 1.4

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**Title:** Emissions Source Test Report for  
Recirculation Gas By-Pass and Urea  
Compliance Testing Etiwanda Unit 3  
Permit Application No. 261513

Acurex Environmental

Acurex Environmental

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Section 1.4  
(BIO Ch. 2)

EMISSIONS SOURCE TEST REPORT FOR  
RECIRCULATION GAS BY-PASS AND UREA COMPLIANCE TESTING  
ETIWANDA UNIT 3  
PERMIT APPLICATION NO. 261513

Source Location:

Southern California Edison - Etiwanda Generating Station  
8996 Etiwanda Avenue  
Etiwanda, CA 91739

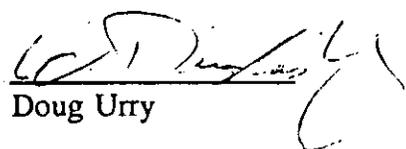
Submitted to:

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Environmental Affairs  
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## SECTION 1

### INTRODUCTION

Acurex Environmental was contracted by Southern California Edison Company (SCE) to conduct emissions source testing on Unit No. 3 located at Edison's Etiwanda Generating Station. This test program was conducted to quantify the effect of recirculation gas by-pass (RGB) and urea injection on various stack emissions as required in the South Coast Air Quality Management District (SCAQMD) Permit to Construct (PTC) No. 261513 (Condition 14B). Emissions measured were nitrogen oxides ( $\text{NO}_x$ ), carbon monoxide (CO), oxygen ( $\text{O}_2$ ), reactive organic gases (ROG), and ammonia ( $\text{NH}_3$ ).

This report summarizes results for the source tests performed as required by the PTC. Source tests were performed as specified in the conditionally approved Acurex Environmental source test protocol dated April 22, 1993; the conditional approval memorandum issued June 1, 1993 by the SCAQMD; and subsequent phone conversations between Mr. Michael Escarcega of Edison, and Mr. Darren Stroud and Mr. Glenn Kasai of the SCAQMD on January 18 and January 19, 1994, respectively. The most significant changes to the test scope as specified in the PTC, but approved by the SCAQMD were the elimination of particulate testing and the reduction of the ROG test requirement from all loads and test conditions to only full load baseline and full load RGB + Urea. A copy of the source test protocol, the District memorandum, and records of the referenced phone conversations are provided in Appendix A.

The results of this source test are summarized in Section 2. Section 3 provides a description of the SCE boiler and Sections 4 through 7 detail sampling and analysis procedures and results for each test parameter. Appendices B through H provide supporting documentation for data presented in Sections 4 through 7 and are specifically referenced where appropriate.

Key information pertaining to the emissions test series is summarized in Table 1-1, and the test matrix used at each of the three test loads (low, mid-, and high) is listed in Table 1-2.

Table 1-1. Etiwanda No. 3 Source Test Information

Source Tested	Southern California Edison's Etiwanda Generating Station, Utility Boiler No. 3
Test Location	8996 Etiwanda Ave. Etiwanda, CA 91739
Test Requested By	South Coast Air Quality Management District
Reason For Test	Addition of recirculation gas by-pass system (PTC Application No. 261513)
Test Dates	March 22-24, 1994
Tests Performed By	Acurex Environmental, Southwest Regional Office Project Engineer: Chad Garretson (714) 453-1264
Key Edison Contacts	Stafford Pease (818) 302-4034 Mike Escarcega (818) 302-4032

Table 1-2. Test Matrix for Etiwanda Unit No. 3

Boiler Operating Conditions		Test Parameter	Sampling Method	Analytical Method
Full Load	Baseline	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	<sup>a</sup> Various
		Moisture	SCAQMD 4.1	Gravimetric
		Flow Rate	SCAQMD 1.1-3.1	NA
		<sup>b</sup> ROG	SCAQMD 25.1	<sup>c</sup> TCA/FID
	RGB On	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various
		Moisture	SCAQMD 4.1	Gravimetric
		Flow Rate	SCAQMD 1.1-3.1	NA
	RGB and Urea Injection On	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various
		Flow Rate	SCAQMD 1.1-3.1	NA
		ROG	SCAQMD 25.1	TCA/FID
		Ammonia Slip/ Moisture	<sup>d</sup> SCAQMD Draft Method 207.1	Colorimetric
	Mid-Load	Baseline	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1
Moisture			SCAQMD 4.1	Gravimetric
Flow Rate			SCAQMD 1.1-3.1	NA
RGB On		NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various
		Moisture	SCAQMD 4.1	Gravimetric
		Flow Rate	SCAQMD 1.1-3.1	NA
RGB and Urea Injection On		NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various
		Ammonia Slip/ Moisture	SCAQMD Draft Method 207.1	Colorimetric
		Flow Rate	SCAQMD 1.1-3.1	NA

<sup>a</sup>Various: NO<sub>x</sub> - chemiluminescence  
 CO - non-dispersive infrared (NDIR)  
 O<sub>2</sub> - electrochemical

<sup>b</sup>SCAQMD Method 25.1 was performed at full load baseline and full load RGB plus urea injection conditions only

<sup>c</sup>TCA/FID - Total combustion analysis/flame ionization detector

<sup>d</sup>SCAQMD Draft Method 207.1 for Ammonia and Ammonium Compounds From Stationary Sources

NA - Not Applicable

Table 1-2. Test Matrix for Etiwanda Unit No. 3 (continued)

Boiler Operating Conditions		Test Parameter	Sampling Method	Analytical Method
Low Load	Baseline	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various
		Moisture	SCAQMD 4.1	Gravimetric
		Flow Rate	SCAQMD 1.1-3.1	NA
	RGB On	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various
		Moisture	SCAQMD 4.1	Gravimetric
		Flow Rate	SCAQMD 1.1-3.1	NA

NA - Not Applicable

## SECTION 2

### RESULTS SUMMARY

Boiler operating parameters (boiler output, fuel flow rate and air to fuel ratio), stack gas characteristics (flow rate, temperature and moisture content), and urea injection system data (urea injection rate and concentration) are summarized for each test condition in Table 2-1. Records of boiler operating parameters are provided in Appendix B.

NO<sub>x</sub>, CO, O<sub>2</sub>, ROG, and NH<sub>3</sub> emission measurement results are summarized in Table 2-2. No emission measurement results exceed PTC limits. For each test condition, Table 2-2 lists stack gas NO<sub>x</sub>, CO, O<sub>2</sub>, ROG, and NH<sub>3</sub> concentrations (corrected to 3 percent oxygen) and emission rates. ROG results presented in Table 2-2 represent an average of duplicate sampling and analysis results.

NO<sub>x</sub>, CO, NH<sub>3</sub>, and ROG mass emission rates were calculated based on measured concentration data and flow rate data collected during gaseous constituent concentration measurements. Documentation of NO<sub>x</sub>, CO, NH<sub>3</sub>, and ROG emission rate calculations is provided in Appendix D-7.

Table 2-1. Boiler Operating Conditions and Stack Gas Characteristics

Test Condition	Boiler Output (Net MW)	Fuel Flow Rate (mmscf/hr)	Air to Fuel Ratio	Urea		Stack Gas		
				Injection Rate (gal/hr)	Concentration (%)	Flow Rate (mmscf/hr)	Moisture Content (%)	Temperature (°F)
Full Load, Baseline	319	3.074	20.3	NA	NA	39.62	15.6	250
Full Load, RGB On	319	3.079	20.6	NA	NA	40.56	15.9	249
Full Load, RGB and Urea On	318	3.076	20.2	81	20	39.44	16.4	250
Mid-load, Baseline	249	2.376	20.0	NA	NA	30.97	15.3	225
Mid-load, RGB On	250	2.386	19.9	NA	NA	31.04	15.6	229
Mid-load, RGB and Urea On	250	2.389	19.6	39	20	30.85	16.0	230
Low Load, Baseline	122	1.266	17.3	NA	NA	15.50	14.7	182
Low Load, RGB On	123	1.271	17.5	NA	NA	15.72	15.0	182

Table 2-2. Source Test Results

Test Condition	Stack Gas O <sub>2</sub>		Stack Gas NO <sub>x</sub>		Stack Gas CO		Stack Gas ROG		Stack Gas NH <sub>3</sub>	
	percent	ppm	lb/hr	ppm	lb/hr	ppm	lb/hr	ppm	lb/hr	
Full Load, Baseline	3.1	62.0	297	197	574	130	217	NA	NA	
Full Load, RGB On	3.3	54.3	263	217	639	NA	NA	NA	NA	
Full Load, RGB and Urea On	3.2	46.3	219	206	595	160	265	6.6	12	
Mid-load, Baseline	3.6	44.4	161	151	334	NA	NA	NA	NA	
Mid-load, RGB On	3.7	32.5	118	150	330	NA	NA	NA	NA	
Mid-Load, RGB and Urea On	3.7	28.1	101	148	324	NA	NA	4.2	5.5	
Low Load, Baseline	4.8	23.1	39	0.8	1	NA	NA	NA	NA	
Low Load, RGB On	4.8	14.8	25	10.1	11	NA	NA	NA	NA	

NA - Not Applicable

ND - No Data

<sup>†</sup>ppm corrected to 3 percent O<sub>2</sub>, ROG concentrations are reported as methane

Note: Urea injection not used below mid-load.



## SECTION 3

### BOILER DESCRIPTION

Etiwanda Unit 3 is rated at 320 MW net generation and has a tangentially fired, controlled-circulation boiler designed by Combustion Engineering (CE) to burn gas or oil fuel. Maximum capacity of the boiler is 2,305,000 lb/hr steam. Design steam conditions are 2450 psig, 1050 °F superheat, and 1000 °F reheat.

This boiler is one of six similar CE tangentially fired boilers in the SCE system. All six are fired from the top and have division walls and three tiers of burners consisting of eight burners in each tier. Each burner contains an oil gun and two injectors. The boiler is equipped with burner tilts which can be varied from +10 to -30 degrees from horizontal.

Combustion air is supplied by two forced draft fans through primary and secondary air ducts. Air flow to individual burners is controlled by dampers. Existing controls regulate the position of all primary dampers and all secondary dampers separately.

Unit 3 has two flue gas recirculation fans that mix flue gas with the primary and secondary air supply. The recirculated gases are therefore mixed with the bulk gas fires that are characteristic of tangentially fired units.



## SECTION 4

### SCAQMD METHOD 100.1, NO<sub>x</sub>, CO, AND O<sub>2</sub> CONCENTRATION MEASUREMENTS

Section 4 summarizes SCAQMD Method 100.1 test procedures and results. A description of the sampling and analysis system is provided in Section 4.1. Method 100.1 concentration, stratification, and quality assurance/quality control (QA/QC) results are summarized in Sections 4.2, 4.3, and 4.4, respectively. Finally, SCAQMD Method 100.1 data reduction procedures are discussed in Section 4.5.

NO<sub>x</sub>, CO, and O<sub>2</sub> concentration measurements were performed with strict adherence to Method 100.1 sampling and analysis procedures. Each constituent concentration was monitored continuously for 60 minutes, and sampling was performed concurrent with all other gaseous constituent concentration measurements. All measurements were performed at existing sampling facilities on the stack. Sampling locations and stack dimensions are shown in Figure 4-1.

#### 4.1 Sampling System

Continuous emissions monitoring (CEM) instruments in the Acurex Environmental Mobile Laboratory were used to measure gaseous constituent concentrations present in the sample stream. The Acurex Environmental Mobile Laboratory is certified by the California Air Resources Board; a copy of the certificate is provided in Appendix I. A schematic of the CEM instrumentation is provided in Figure 4-2. The sample extraction and conditioning system consists of a stainless steel sampling probe connected to a heated teflon sample line located upstream of a Universal Analyzers gas sample conditioner. The sample line between the probe and the sample conditioner is heated to 250°F to maintain the gas stream temperature above the water dew point. The sampling system is constructed to avoid contact between the sample gas and moisture and therefore minimize nitrogen dioxide (NO<sub>2</sub>) absorption.

From the sample gas conditioner, the sample stream passes through a flexible teflon

sample line to a flow control system which meters the sample flow rate through the monitoring instruments. Sample flow rate is controlled with a bypass pressure regulator located at the instrument manifold. Flow to each monitoring instrument is controlled using individual flow control valves and meters. The CEM instrument specifications are summarized in Table 4-1. Instrument output is recorded by a strip chart recorder and an integrated data logging system. The logging device records 1 minute averages throughout each test.

All instrument calibrations were performed using National Bureau of Standards (NBS) traceable gas standards certified to  $\pm 1$  percent analytical accuracy. Copies of calibration gas certification sheets are provided in Appendix D-1.

ETIWANDA UNIT 3

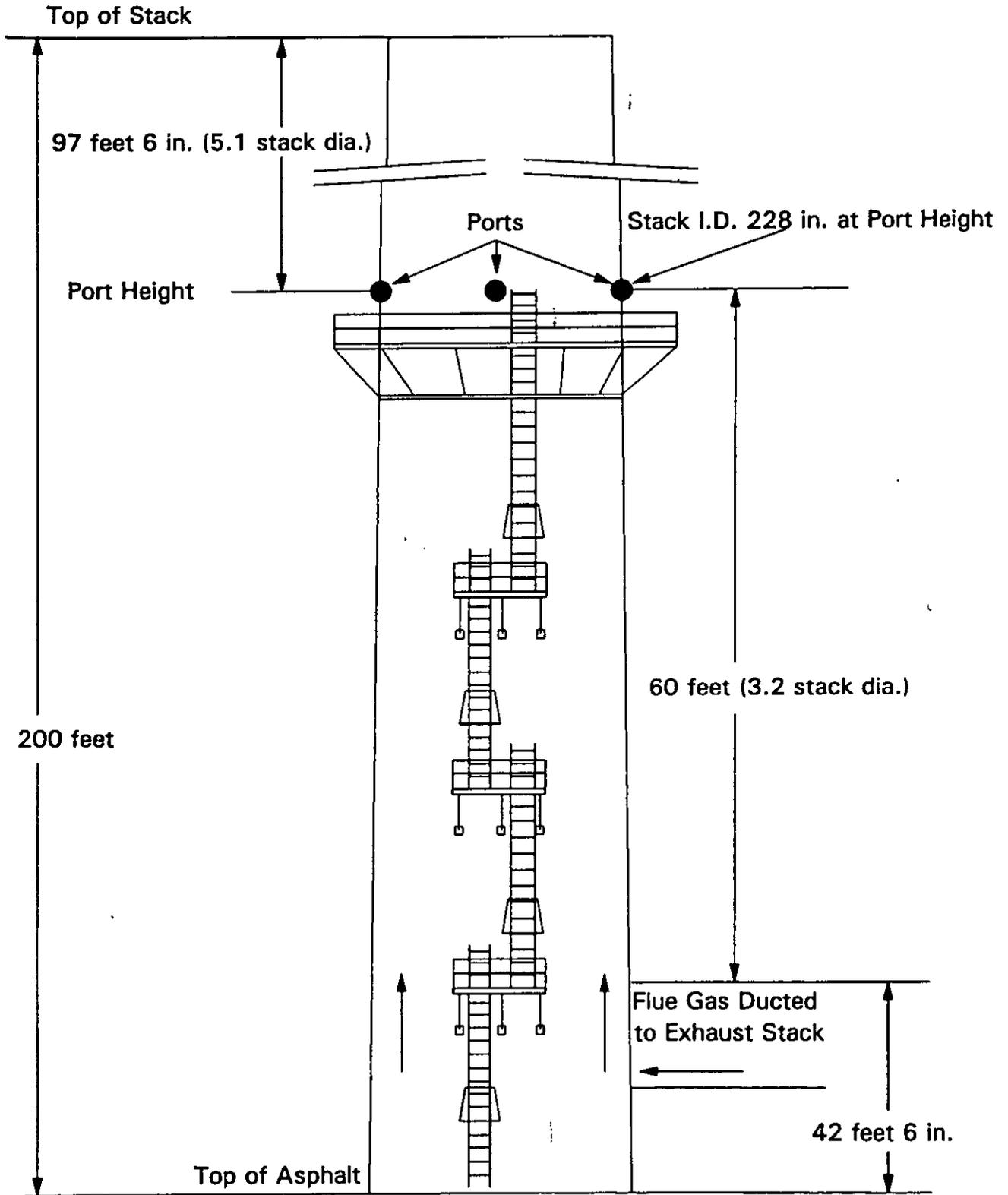


Figure 4-1. Diagram of Stack Dimensions and Sampling Locations

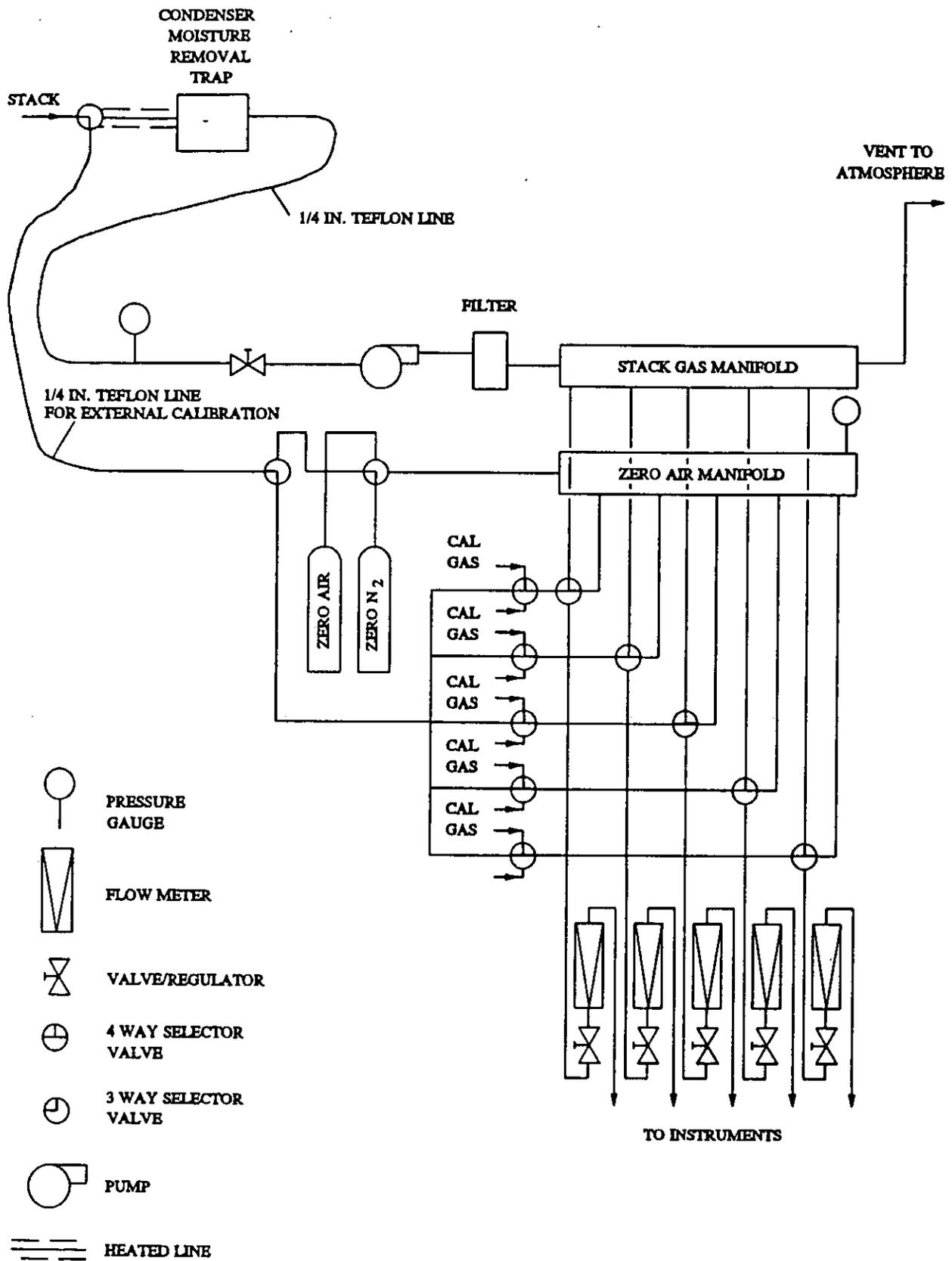


Figure 4-2. Schematic Diagram of CEM Instrumentation in the Acurex Environmental Mobile Laboratory

Table 4-1. Continuous Emissions Monitoring Instruments

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**NO<sub>x</sub> CHEMILUMINESCENT ANALYZER—THERMO ELECTRON MODEL 10A**

Response Time (0-95%)	3 sec—NO <sub>x</sub> mode
Zero Drift	Negligible after 1/2 hour warmup
Linearity	±1% of full scale
Accuracy	±1% of full scale
Output	0-10 V
Range	0-2.5, 10, 25, 100, 250, 1000, 2500, and 10,000 ppm
Sensitivity	0.1 ppm

**O<sub>2</sub> ANALYZER, FUEL TYPE—TELEDYNE MODEL 326A**

Response Time (0-95%)	30 sec
Accuracy	±1% of scale at constant temperature; ±1% of scale at ±5% of reading, whichever is greater, over the operating temperature range
Output	0-100 mV
Range	0-5, 10, 25 %

**CO INFRARED ANALYZER—TECO MODEL 48**

Response Time (0-95%)	30 sec
Zero Drift	±1%
Span Drift	±1%
Linearity	1%
Output	4-20 mA
Range	0-1, 2, 5, 10, 20, 50, 100, 200, 500, 1000 ppm

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#### 4.2 Method 100.1 Emissions Data

NO<sub>x</sub>, CO, O<sub>2</sub>, and carbon dioxide (CO<sub>2</sub>) emissions data are summarized in Table 4-2, which lists stack gas constituent concentrations, and concentrations corrected to 3% O<sub>2</sub> for NO<sub>x</sub> and CO, for each test condition. CO<sub>2</sub> concentration measurements were performed to provide data necessary to calculate stack gas molecular weight as prescribed in SCAQMD Method 3.1.

Table 4-2. Method 100.1 Test Results

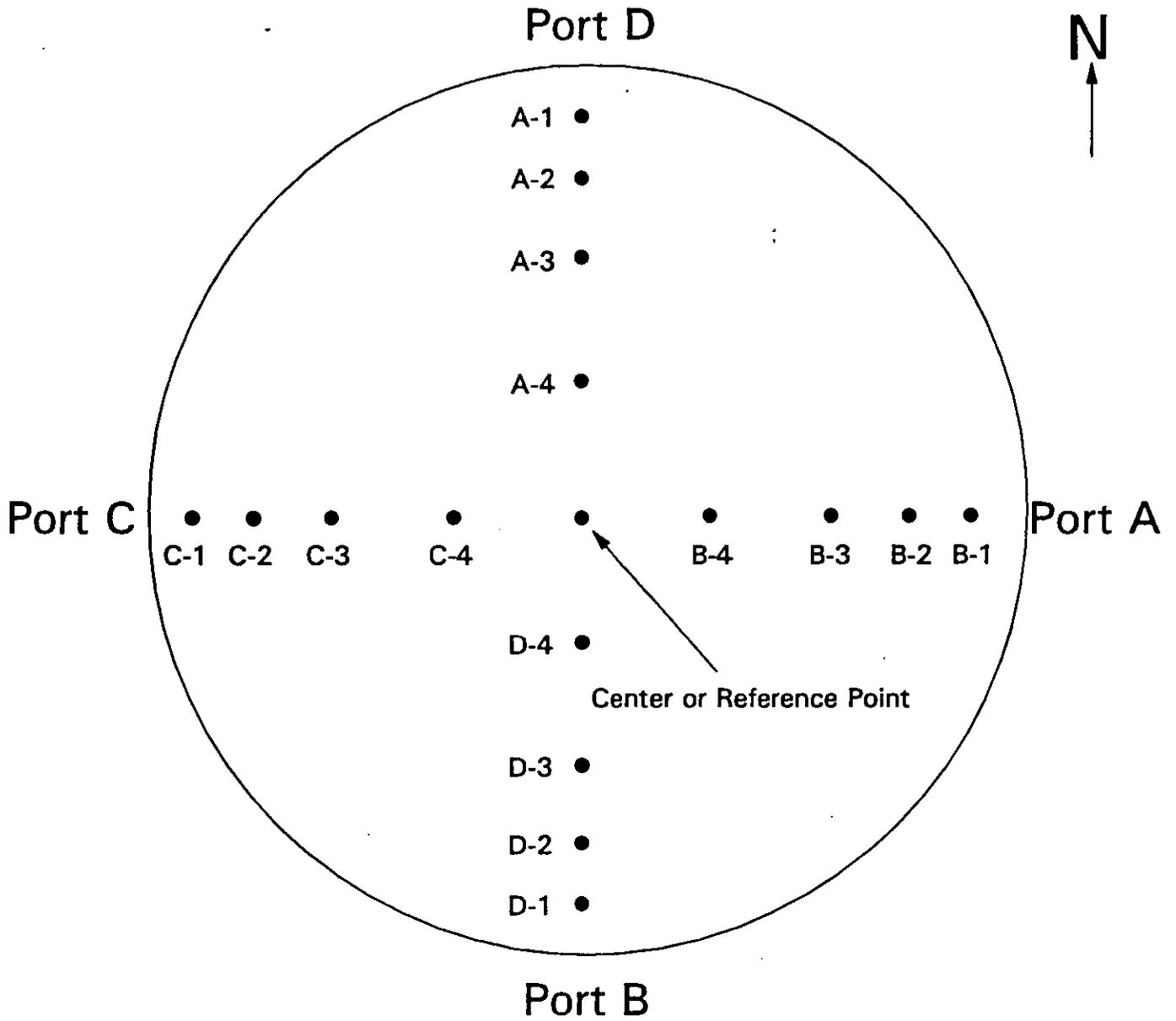
Test Condition	NO <sub>x</sub> (ppm)	NO <sub>x</sub> @ 3% O <sub>2</sub> (ppm)	CO (ppm)	CO @ 3% O <sub>2</sub> (ppm)	O <sub>2</sub> (%)	CO <sub>2</sub> (%)
Full Load, Baseline	61.7	62.0	196	197	3.1	10.0
Full Load, RGB On	53.4	54.3	213	217	3.3	10.0
Full Load, RGB and Urea On	45.8	46.3	204	206	3.2	10.0
Mid-load, Baseline	42.9	44.4	146	151	3.6	9.7
Mid-load, RGB On	31.2	32.5	144	150	3.7	9.7
Mid-load, RGB and Urea On	27.0	28.1	142	148	3.7	9.6
Low Load, Baseline	20.8	23.1	0.7	0.8	4.8	8.9
Low Load, RGB On	13.3	14.8	9.1	10.1	4.8	9.0

#### 4.3 Stratification Measurement Data

Constituent concentration stratification was assessed prior to performing Method 100.1 sampling at mid- and low operating loads. Per agreement with the SCAQMD (Appendix A-4), full load stratification testing was not performed. Stratification was determined following procedures submitted in the source test protocol.

Each stratification determination was performed by measuring NO<sub>x</sub> concentrations at the 16 traverse point locations illustrated in Figure 4-2. A copy of the field test data sheet documenting stratification test traverse point locations is provided in Appendix D-4. A stack diagram showing sampling port locations is provided in Appendix C. Through each sampling port, the sampling probe was first placed at the reference point (center point), followed by each traverse point, and then returned to the reference point. NO<sub>x</sub> concentrations were measured at

Figure 4-2. Stratification Test Traverse Point Locations



Traverse Point Locations (inches)

Stack I.D.	228 inches
Point 4	73 $\frac{5}{8}$ inches
Point 3	44 $\frac{1}{4}$ inches
Point 2	24 inches
Point 1	7 $\frac{1}{4}$ inches

each sample location for at least 3 minutes.

NO<sub>x</sub> concentration measurements performed to assess gaseous constituent stratification at mid- and low operating loads are summarized Tables 4-3 and 4-4, respectively. Stratification results were calculated following SCAQMD Source Test Manual, Chapter X, Section 13 procedures. Stratification was less than 10% at each operating load; therefore, all gaseous constituent concentration measurements, including ROG and NH<sub>3</sub>, were performed at the center point of the exhaust stack.

Copies of stratification field test data sheets and strip chart records are provided in Appendix D-2 and D-3, respectively

Table 4-3. Mid-load (250 MW) Stratification Test Results

Time	Traverse Point	Measured NOx Conc.			Time	Traverse Point	Measured NOx Conc.				
		Tx (ppm)	Kx	Txn			Tx (ppm)	Kx	Txn		
0744	reference	41.6			0850	reference			41.6		
0748	A-1	41.6	1.00	41.6	0854	C-1			41.4	1.00	41.4
0752	A-2	41.7	1.00	41.6	0859	C-2			41.7	1.00	41.8
0757	A-3	41.8	1.00	41.7	0903	C-3			41.2	0.99	41.2
0802	A-4	41.3	0.99	41.3	0908	C-4			41.1	0.99	41.1
0807	reference	41.7			0913	reference			41.5		
	reference avg:	41.7				reference avg:			41.6		
0816	reference	41.7			0921	reference			41.3		
0821	D-1	41.4	1.00	41.5	0926	B-1			41.0	0.99	41.0
0825	D-2	41.6	1.00	41.8	0930	B-2			41.2	0.99	41.2
0830	D-3	41.3	1.00	41.4	0934	B-3			41.3	0.99	41.3
0835	D-4	41.1	0.99	41.2	0938	B-4			41.8	1.00	41.8
0839	reference	41.2			0943	reference			41.6		
	reference avg:	41.5				reference avg:			41.5		

Stratification Test Results: Txn (average): 41.4  
 Txn (maximum): 41.8  
 Txn (minimum): 41.0  
 Stratification: 1.9%

Where: Kx = Proportionality Constant (conc. at traverse point x / avg. concentration at reference point)  
 Tx = Concentration at traverse point x  
 Txn = Normalized value of concentration at traverse point x

Table 4-4. Low load (120 MW) Stratification Test Results

Time	Traverse Point	Measured NOx Conc.			Time	Traverse Point	Measured NOx Conc.		
		Tx (ppm)	Kx	Txn			Tx (ppm)	Kx	Txn
2033	reference	20.1			2130	reference			
2037	B-1	20.3	1.00	20.1	2134	D-1	20.7	0.99	
2041	B-2	20.3	1.00	20.1	2138	D-2	20.9	1.01	
2045	B-3	20.4	1.00	20.2	2143	D-3	21.3	0.96	
2049	B-4	19.9	0.98	19.7	2149	D-4	20.2	1.01	
2054	reference	20.5			2153	reference	21.3		
	reference avg:	20.3				reference avg:	21.6		
						reference avg:	21.2		
2101	reference	20.5			2203	reference	21.1		
2105	A-1	20.6	1.00	20.1	2207	C-1	20.8	1.01	
2110	A-2	20.5	1.00	20.0	2211	C-2	20.7	1.01	
2114	A-3	20.7	1.00	20.2	2215	C-3	20.7	1.01	
2118	A-4	20.7	1.00	20.2	2219	C-4	20.6	1.00	
2122	reference	20.7			2224	reference	20.5		
	reference avg:	20.6				reference avg:	20.8		

Stratification Test Results: Txn (average): 20.1  
 Txn (maximum): 20.4  
 Txn (minimum): 19.2  
 Stratification: 6.0%

Where:  
 Kx = Proportionality Constant (conc. at traverse point x / avg. concentration at reference point)  
 Tx = Concentration at traverse point x  
 Txn = Normalized value of concentration at traverse point x

#### 4.4 Sampling System QA/QC

Sampling system and instrument performance measurements were recorded throughout this source test with strict adherence to Method 100.1 QA/QC procedures. Analyzer calibration error, instrument linearity, and system bias were assessed before and after each test run. Zero and calibration drift were assessed following each test run. In addition, sampling system leak checks were performed before and after each test run.

All NO<sub>x</sub>, CO, and O<sub>2</sub> analyzer and sampling system performance measurements were within error tolerances listed in Method 100.1 procedures with the following exceptions. The CO linearity error for the low load tests ranged from 1.2 to 1.4 percent instead of < 1.0 percent. This minor deviation in CO instrument linearity for low load tests does not impact the test results in demonstrating compliance with the 500 ppm CO limit as the results are < 10 ppm. The CO<sub>2</sub> linearity error for several tests ranged from 1.0 to 1.2 percent instead of < 1.0 percent, and the CO<sub>2</sub> post-test analyzer calibration error for the mid-load RGB plus urea injection test was 2.1 percent instead of < 2.0 percent, as specified in the method. The CO<sub>2</sub> measurements were used only to calculate stack gas molecular weight; therefore, these slight deviations from the performance tolerance requirements have negligible impact on test results.

Strip charts of the semi-annual analyzer certifications for response time and NO<sub>2</sub> to nitrous oxide (NO) converter efficiency are provided in Appendix D-5. The TECO Model 10AR NO<sub>x</sub> analyzer used for this test series was outfitted with a low temperature molybdenum (moly) converter. The moly converter demonstrated an acceptable NO<sub>2</sub> to NO conversion efficiency as evaluated following EPA Method 20, Section 5.6 procedures (see Appendix D-5).

#### 4.5 Data Reduction Procedures

CEM data were permanently recorded on multichannel strip chart recorders; in addition, a data logging system recorded 1 minute average constituent concentrations. The data stored in the logging system was downloaded and used to derive the test results. All CEM data were corrected for instrument drift and sampling system bias per Method 100.1. The calibration responses recorded by the data logger were used to correct the data logger information, and derive the final results presented in Table 4-2 (copies of data logger output are provided in Appendix D-6). The following calculation was used for the correction.

$$C_{gas} = (\bar{C} - C_o) \frac{C_{ma}}{C_m - C_o}$$

where:

$C_{gas}$  = Effluent gas concentration, dry basis, ppm

$\bar{C}$  = Average gas concentration indicated by gas analyzer, dry basis ppm

$C_{ma}$  = Actual concentration of the upscale calibration gas, ppm

$C_m$  = Average of initial and final system calibration bias check responses for the upscale calibration gas, ppm

$C_o$  = Average of initial and final system calibration bias check responses for the zero gas, ppm

Equations provided in Method 100.1, Section 3 were used to compute the  $NO_x$  and CO emission rates provided in Section 2.

## SECTION 5

### SCAQMD METHOD 25.1, ROG MEASUREMENTS

Section 5 provides a summary of SCAQMD Method 25.1 sampling and analysis procedures and results. An overview of the sampling and analysis procedures is provided in Section 5.1. ROG analytical and QA/QC data are summarized in Sections 5.2 and 5.3, respectively.

#### 5.1 Sampling and Analysis Procedures

ROG concentrations in the stack gas were measured following Method 25.1 sampling and analysis procedures. Method 25.1 samples were collected in duplicate at the center of the exhaust stack, concurrently with all other gaseous constituent concentration measurements. ROG samples were collected over a 60 minute test period.

Method 25.1 specifies that sample gas be withdrawn at a constant rate throughout the test duration. Condensibles are collected in a condensate trap chilled with dry ice located upstream of the evacuated tank. The gas phase ROG component is collected in the evacuated tank. Sample gases are withdrawn through a pre-cleaned  $\frac{1}{8}$  inch stainless steel sampling probe positioned at the center of the exhaust stack. Each sampling line is purged for approximately one minute before initiating sampling.

ROG concentrations are determined through independent analysis of the condensate in the traps and the gases in the tanks. The mass of ROG collected in each condensate trap is measured by first removing all  $\text{CO}_2$ , and then oxidizing the ROG in the condensate to  $\text{CO}_2$ . This  $\text{CO}_2$  fraction is collected in an evacuated cylinder and injected into the gas analysis module of the total combustion analyzer (TCA) and measured by a non-dispersive infrared (NDIR) detector.

ROG concentrations in the tanks are measured by injecting a portion of the sample gas into the gas analysis module of the TCA which uses a gas chromatograph (GC) column to

separate non-methane organics (NMO) from CO, CO<sub>2</sub>, and methane (CH<sub>4</sub>). The NMO elutes off the GC as fore-flush and back-flush, and is oxidized to CO<sub>2</sub>. A reduction catalyst is used to reduce this CO<sub>2</sub> fraction to CH<sub>4</sub>, and finally, the CH<sub>4</sub> is measured using a FID.

A Method 25.1 sampling system field blank was collected to assess sampling apparatus cleanliness and to determine potential sample contamination during set-up, sampling, and recovery activities. The field blank was collected by passing ultra-pure nitrogen gas through the sampling apparatus for approximately 60 minutes.

Method 25.1 sample analyses were performed by Horizon Air Measurements located in Newbury Springs, California. A portion of the analyses were subcontracted by Horizon to AAtmAA Laboratories, located in Calabasas, California.

## **5.2 Method 25.1 Analytical Data**

Method 25.1 analytical data are summarized in Table 5-1. For each test condition, duplicate analysis results are listed for ROG, CO, and CO<sub>2</sub>. Table 5-1 lists actual and corrected ROG concentrations; corrections are made to 3 percent O<sub>2</sub>. ROG emission rates (reported in pounds per hour as methane) are also included in Table 5-1. Emission rates were calculated based on volumetric flow rate data collected during the sampling period (Section 7). Copies of Method 25.1 analytical reports and field test data sheets are provided in Appendix E-1 and E-2, respectively.

The Method 25.1 post-test leak check for one of the tank/trap pairs did not pass during the full load RGB and Urea injection test, indicating that sample dilution occurred. The tank/trap pairs for this run were not analyzed and the entire test event was repeated. The results contained in this report for each parameter tested at this load and condition are from the second run. Field test data sheets for the invalid run are included in the appendices.

## **5.3 Method 25.1 QA/QC Results**

Field blank analytical results indicate 27 ppm residual ROG (as methane) was present in the apparatus. Data presented in Table 5-1 were blank corrected to account for residual ROG present in the Method 25.1 sampling equipment.

Table 5-1. Method 25.1 Test Results

Test Condition	Sample	ROG Concentration (ppm as methane)		ROG Emission Rate (lb/hr as CH <sub>4</sub> )	CO (ppm)	CO <sub>2</sub> (%)
		Actual	Corrected to 3 % O <sub>2</sub>			
Full Load, Baseline	*Tray 1	142	143	238	195	9.5
	Tray 2	117	118	196	181	9.4
	Average	130	131	217	188	9.4
Full Load, RGB and Urea On	Tray 1	158	160	264	188	9.0
	Tray 2	159	161	265	190	9.3
	Average	159	160	265	189	9.2

\*a tray constitutes one tank and condensate trap set



## SECTION 6

### DRAFT SCAQMD METHOD 207.1, AMMONIA CONCENTRATION MEASUREMENTS

Section 6 summarizes  $\text{NH}_3$  concentration sampling and analysis procedures and results. An overview of the sampling and analysis procedures is provided in Section 6.1.  $\text{NH}_3$  concentration results are summarized in Section 6.2.

#### 6.1 Sampling and Analysis Procedures

$\text{NH}_3$  samples were collected and analyzed following SCAQMD Draft Method 207.1, "Analytical Procedures for Determining Ammonia and Ammonium Compounds from Stationary Sources." A copy of this Method is provided in Appendix F-1.

$\text{NH}_3$  concentration measurements were performed only when the urea injection system was in service. For each test, sample gas was collected at the center of the exhaust stack for a 60 minute period.  $\text{NH}_3$  testing was performed concurrently with all other gaseous constituent concentration measurements.

$\text{NH}_3$  concentration samples are collected using a standard impinger train. Sample gas is withdrawn from the source at a constant rate through a  $\frac{1}{4}$  teflon sample line and four impingers by a sample pump. The first two impingers contain 100 ml of 0.1 N sulfuric acid, the third is empty, and the fourth contains silica gel. A sampling console controls sample flow rate, and records sample volume and TC measurements.

A sampling system leak check was performed immediately before and after each test. After each test, the teflon sample line was rinsed with 0.1 N sulfuric acid. This probe wash was combined with the impinger catch for analysis.

$\text{NH}_3$  samples were analyzed in strict accordance to Draft Method 207.1 procedures. This colorimetric method uses a spectrophotometer to measure the absorbance of a sample aliquot after reaction with Nessler reagent. The absorbance of the sample aliquot was compared to

calibration curve absorbencies developed by analyzing 6 standards of known concentration. The NH<sub>3</sub> concentration of the sample aliquot was interpolated from the calibration curve using linear regression.

### 6.2 Draft Method 207.1 Test Data

NH<sub>3</sub> concentration data are summarized in Table 6-1. For each urea test condition, Table 6-1 lists the analytical results, NH<sub>3</sub> concentration and NH<sub>3</sub> concentration corrected to 3 percent O<sub>2</sub>. Also listed are NH<sub>3</sub> emission rates calculated based on flow rate data collected during the test period (Section 7). Copies of NH<sub>3</sub> analytical reports and field test data sheets are provided in Appendix F-2 and F-3, respectively.

Table 6-1. NH<sub>3</sub> Test Data

Test Condition	Analytical Results (mg NH <sub>3</sub> /sample)	Stack Gas Concentration		Stack Gas Emission Rate (lb/hr)
		(ppm)	Corrected to 3 % O <sub>2</sub> (ppm)	
Full Load, RGB and Urea On	3.31	6.6	6.6	12
Mid-load, RGB and Urea On	2.07	4.0	4.2	5.5

### 6.3 Draft Method 207.1 QA/QC

Calibration curve results were within Draft Method 207.1 QA/QC requirements; the correlation coefficient for the 6 point calibration curve was 0.9997, exceeding the 0.9995 requirement. Also, the 40 µg control sample deviated 4.0 percent from the calculated curve, within the ± 5 percent requirement.

Sampling system calibration records are provided in Appendix H.

## SECTION 7

### SCAQMD METHOD 1.1, 2.1, 3.1, AND 4.1, STACK GAS VOLUMETRIC FLOW RATE MEASUREMENTS

Section 7 summarizes stack gas volumetric flow rate sampling procedures and results. Flow rate measurements were performed during each gaseous constituent concentration test run per requirements cited in Section 1. An overview of the sampling procedure is provided in Section 7.1. Stack gas flow rate data are summarized in Section 7.2.

#### 7.1 Volumetric Flow Rate Measurement Procedures

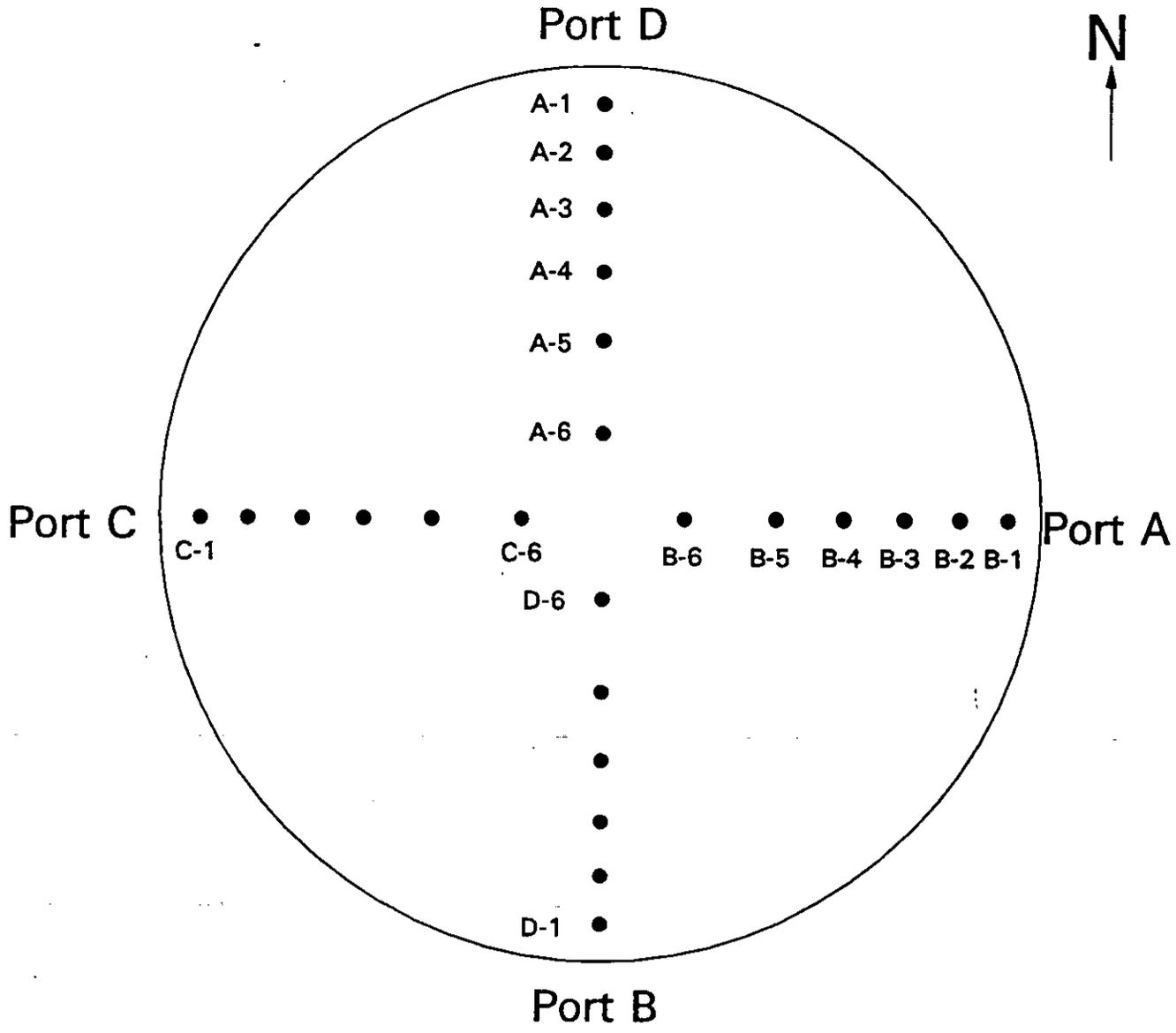
Traverse point locations and exhaust gas velocity, molecular weight, and moisture were determined following SCAQMD Methods 1.1, 2.1, 3.1, and 4.1, respectively. Data collected from Methods 1.1 through 4.1 were used to calculate stack gas volumetric flow rate. Method 1.1 outlines the procedures for choosing the proper traverse points, while Method 2.1 provides the methodology for measuring pressure differentials at each traverse point and calculating the stack gas velocity. For this test, exhaust gas molecular weight was determined from Method 100.1 data per Method 3.1. Exhaust gas moisture content was determined following SCAQMD Method 4.1 procedures.

For this test series, measurements were taken at 24 traverse points, exceeding the Method 1.1 requirement of 16 traverse points. Traverse point locations are illustrated in Figure 7-1. Exhaust stack cyclonic flow characteristics were assessed following SCAQMD Method 1.1, Section 2.4 for mid- and low load test conditions.

In accordance with Method 2.1, a calibrated Type S pitot tube and thermocouple were used in conjunction with a magnehelic gauge to measure stack gas velocity pressure and temperature. From these data, the exhaust gas velocity was calculated using standard equations.

Exhaust gas moisture content was measured according to Method 4.1 procedures. Using a standard impinger train, exhaust gas sample was collected at the center of the exhaust stack. During test conditions where the urea injection system was in service, moisture data was obtained from  $\text{NH}_3$  sampling and analysis procedures.

Figure 7-1. Particulate Test Traverse Point Locations



Traverse Point Locations (inches)

Stack I.D.	228 inches
Point 6	81 1/8 inches
Point 5	57 inches
Point 4	40 3/8 inches
Point 3	26 7/8 inches
Point 2	15 1/4 inches
Point 1	4 3/4 inches

## 7.2 Volumetric Flow Rate Test Data

Stack gas volumetric flow rate data are summarized in Table 7-1. For each test condition, stack gas flow rate, moisture content, temperature, and molecular weight is listed. Copies of flow rate and moisture calculation sheets, spreadsheets, and field data sheets are provided in Appendix G-1 and G-2, respectively. Copies of pitot and magnehelic calibration records are provided in Appendix H.

Table 7-1. Stack Gas Volumetric Flow Rate Results

Test Condition	Stack Gas Characteristics			
	Flow Rate (dscfm)	Moisture Content (%)	Temperature (°F)	Molecular Weight (lb/lb•mole)
Full Load, Baseline	660325	15.6	250	29.7
Full Load, RGB On	676063	15.9	249	29.7
Full Load, RGB and Urea On	657293	16.4	250	29.7
Mid-load, Baseline	516124	15.3	225	29.7
Mid-load, RGB On	517347	15.6	229	29.7
Mid-load, RGB and Urea On	514175	16.0	230	29.7
Low Load, Baseline	258370	14.7	182	29.6
Low Load, RGB On	262007	15.0	182	29.6

Exhaust stack cyclonic flow characteristics were assessed for mid- and low load test conditions. The average yaw angle results for mid- and low load test conditions are 7.9 and zero degrees, respectively, which is below the 20 degree method tolerance. Unstable yaw angles were observed at some traverse points nearest the stack wall (Point 1) for the mid-load test condition. Because Point 1 yaw angle measurement results are suspect and probably a result of air leakage at the port flange connector, Point 1 results were not included in the reported yaw angle average.

**APPENDIX A**  
**REFERENCED DOCUMENTS**



**APPENDIX A-1**  
**SOURCE TEST PROTOCOL**



**EMISSIONS SOURCE TEST PROTOCOL:**

**PERMIT APPLICATION NO. 261513**

**Source Location:**

**Southern California Edison - Etiwanda Generating Station  
8996 Etiwanda Avenue  
Etiwanda, CA 91739**

**Submitted to:**

**Southern California Edison Company  
Environmental Affairs  
2244 Walnut Grove Avenue  
Rosemead, California 91770**

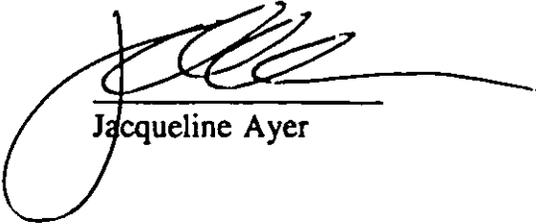
**Submitted by:**

**Acurex Environmental  
Southwest Regional Office  
4879 East La Palma Avenue, Suite 201  
Anaheim, California, 92817**

**Project Engineer**

  
**Chad Garretson**

**Quality Assurance**

  
**Jacqueline Ayer**



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**SECTION 1**  
**INTRODUCTION**

**1.1 Background**

Acurex Environmental was contracted by Southern California Edison Company (Edison) to conduct emissions source testing per the permit to construct (PTC) No. 261513. The source requiring emissions testing is Unit No. 3 located at Edison's Etiwanda Generating Station (Etiwanda #3). Key information for this project is summarized briefly in Table 1-1.

Table 1-1. Project Summary

Source Tested	Southern California Edison Etiwanda Generating Station, Unit No. 3
Test Location	8996 Etiwanda Avenue Etiwanda, CA 91739
Test Requested By	South Coast Air Quality Management District
Reason For Test	Alteration to Unit No. 3: addition of a recirculation gas by-pass system (RGB)
Tests To Be Performed By	Acurex Environmental, Southwest Regional Office Project Engineer: Chad Garretson (714) 970-5290
Key Edison Contacts	Stafford Pease (818) 302-4034 Michael Escarcega (818) 302-4032

This protocol summarizes source test procedures as required by PTC No. 261513. Section 2 presents the proposed test matrix. Section 3 describes sampling locations and procedures. Section 4 summarizes quality assurance (QA) procedures for the proposed test methods. The referenced PTC is provided in Appendix A. Acurex Environmental's California Air Resources Board (ARB) contractor's certification is provided in Appendix B.

## SECTION 2

### TEST MATRIX

#### 2.1 Test Matrix

The proposed test procedures are presented in Table 2-1. For each boiler operating condition, the table identifies the test parameters, sampling and analysis methods, number of runs, and sample duration of each run. The test procedures presented in Table 2-1 will be performed for each of the following boiler load conditions; 50 MW, 100 MW, 200 MW, 275 MW, and 320 MW. Urea emissions testing will only be performed if urea is used in conjunction with the RGB system. Fuel flow rate, air to fuel ratio, and net boiler output (MW) data will be recorded for each test condition. All emissions testing will be performed while the boiler fires natural gas. Particulate testing will be performed at full load conditions only (320 MW) because redistributing the gas recirculation is not expected to have any impact on particulate emissions. In addition, previous urea particulate compliance testing on a similar 320 MW unit demonstrated no significant increase in particulate emissions due to the injection of urea (Reference - Alamitos Unit 4, CARNOT Report No. 84015/R106B215.T).

For each operating condition involving urea injection, the urea injection rate and concentration will be recorded, and the urea/water solution injected will contain no more than 35 percent urea by weight. Ammonia slip testing will be performed only while the urea injection system is operating.

Table 2-1. Test Matrix

Boiler Operating Conditions	Test Parameter	Sampling Method	Analytical Method	Sample Duration (min)	No. of Runs
Baseline	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	*Various	60	1
	Moisture	SCAQMD 4.1	Gravimetric	30	1
	Flow Rate	SCAQMD 1.1-3.1	NA	30	2
	<sup>b</sup> Particulate	SCAQMD 5.2	Gravimetric	> 60	2
	ROG	SCAQMD 25.2	<sup>c</sup> TCA/FID	30	2
RGB	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various	60	1
	Moisture	SCAQMD 4.1	Gravimetric	30	1
	Flow Rate	SCAQMD 1.1-3.1	NA	30	2
	<sup>b</sup> Particulate	SCAQMD 5.2	Gravimetric	> 60	2
	ROG	SCAQMD 25.2	TCA/FID	30	2
RGB and Urea Injection	NO <sub>x</sub> , CO, O <sub>2</sub>	SCAQMD 100.1	Various	60	1
	Flow Rate	SCAQMD 1.1-4.1	Gravimetric	30	2
	<sup>b</sup> Particulate	SCAQMD 5.2	Gravimetric	> 60	2
	ROG	SCAQMD 25.2	TCA/FID	30	2
	Ammonia Slip/ Moisture	SCAQMD Draft Method 207.1	Colorimetric	30	2

\*Various: NO<sub>x</sub> - chemiluminescence  
 CO - non-dispersive infrared (NDIR)  
 O<sub>2</sub> - electrochemical

<sup>b</sup>SCAQMD Method 5.2 will be performed at full load conditions only (320 MW)

<sup>c</sup>TCA/FID - Total combustion analysis/flame ionization detector

<sup>d</sup>SCAQMD Draft Method 207.1 for Ammonia and Ammonium Compounds From Stationary Sources

NA - Not Applicable

## SECTION 3

### SAMPLING LOCATIONS AND PROCEDURES

#### 3.1 Sampling Locations

Extractive and integrated samples will be collected through four sample ports located on the Etiwanda #3 exhaust stack. A plan view illustrating the port locations is provided in Appendix C. The stack sampling location has been previously approved following SCAQMD Chapter X criteria for stratification and flow disturbance. Cross-sectional exhaust stack sampling locations are identified in Sections 3.2 through 3.6. General stack characteristics at the sampling port location follows:

Stack diameter	19 feet
Nearest upstream disturbance	3.2 diameters
Nearest downstream disturbance	5.1 diameters

#### 3.2 SCAQMD Method 100.1, Gaseous Constituent Concentration Measurements

Gaseous constituent concentrations present in the sample stream are measured using the continuous emissions monitoring (CEM) instruments in the Acurex Environmental Mobile Laboratory in general accordance with SCAQMD Method 100.1. A schematic of the CEM instrumentation is provided in Figure 3-1. The sample extraction and conditioning system consists of a stationary stainless steel sampling probe connected to a heated teflon sample line located upstream of a Universal Analyzers gas sample conditioner. The sample line between the probe and the sample conditioner is heated to 250°F to maintain the gas stream temperature above the water dew point. The sample gas cooler is constructed to minimize NO<sub>2</sub> absorption.

From the sample gas conditioner, the sample stream passes through flexible teflon sample line to a flow control system which meters the sample flow rate through the various monitoring

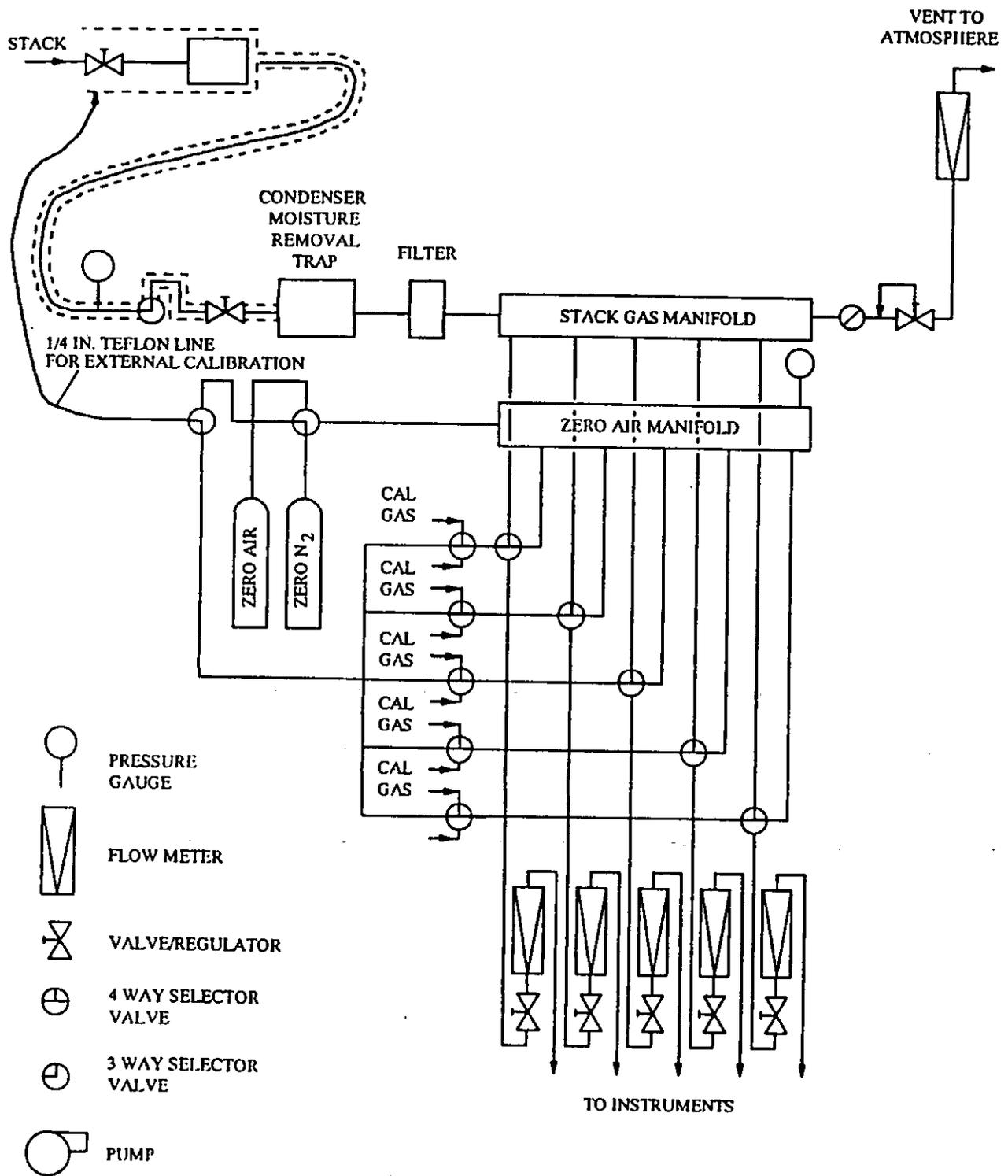


Figure 3-1. Schematic Diagram of CEM Instrumentation in the Acurex Environmental Mobile Laboratory

instruments. The sample flow rate is controlled using a bypass pressure regulator upstream of the instrument manifold. Flow to each instrument is controlled using individual flow control valves and meters. The CEM specifications are summarized in Table 3-1. Instrument output is recorded by a strip chart recorder and an integrated data logging system. The logging device records 1 minute averages throughout each test.

Gaseous constituent concentration measurements are measured in general accordance with SCAQMD Method 100.1 procedures. A leak check is performed prior to testing. Each CEM instrument is calibrated prior to performing system bias checks. System bias checks are performed before and after each test. Calibration results are recorded by both the stripchart instruments and the data logging system.

Extensive gaseous constituent stratification and flow disturbance tests have been previously performed at this test location following SCAQMD Chapter X guidelines (Reference - Etiwanda Unit No. 3, CARNOT Report No. 81915/R148B402.T). The test results show that the stack sampling location meets SCAQMD requirements by demonstrating that the stratification is less than 10 percent. Because the RGB and urea injection systems should have a negligible impact on gaseous stratification, Edison and Acurex Environmental propose the following for non-particulate tests:

- (1) conduct a 16 point  $\text{NO}_x$  or  $\text{O}_2$  traverse for the baseline condition of each load
- (2) if stratification from the 16 point traverse is less than 10 percent, select a representative sampling location and perform single point sampling for  $\text{NO}_x$ ,  $\text{O}_2$ , CO, ROG, ammonia, and moisture measurements for the RGB and RGB/urea test conditions at each load
- (3) if stratification is greater than 10 percent, sample gas will be collected along an 8-point traverse for the parameters identified above

CEM data are permanently recorded on multichannel strip chart recorders; in addition, a data logging system records 1 minute average constituent concentrations. The data stored in the logging system is downloaded and used to derive emissions results.  $\text{NO}_x$  and CO emission data are corrected to 3 percent  $\text{O}_2$ , and all CEM data are corrected for instrument drift and linearity per SCAQMD Method 100.1. The calibration responses recorded by the data logger are used to correct the data logger information. The following calculation is used for the correction.

Table 3-1. Continuous Emissions Monitoring Instruments

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**NO<sub>x</sub> CHEMILUMINESCENT ANALYZER—THERMO ELECTRON MODEL 10A**

Response Time (0-90%)	1.5 sec—NO mode 1.7 sec—NO <sub>x</sub> mode
Zero Drift	Negligible after 1/2 hour warmup
Linearity	±1% of full scale
Accuracy	±1% of full scale
Output	0-10 V
Range	0-2.5 ppm, 0-10 ppm, 0-25 ppm, 0-100 ppm, 0-250 ppm, 0-1000 ppm, 0-2500 ppm, and 0-10,000 pm
Sensitivity	0.1 ppm

**O<sub>2</sub> ANALYZER, FUEL TYPE—TELEDYNE MODEL 326A**

Response Time (0-90%)	60 sec
Accuracy	±1% of scale at constant temperature; ±1% of scale at ±5% of reading, whichever is greater, over the operating temperature range
Output	0-100 mV
Range	0-5, 0-10, and 0-25% O <sub>2</sub>

**CO INFRARED ANALYZER—HORIBA MODEL PIR 2000**

Response Time (0-90%)	5 sec
Zero Drift	±1%
Span Drift	±1%
Linearity	1%
Resolution	Less than 1% of full scale
Output	0-100 mV
Range	0-500, 0-1500, 0-2500

---

$$C_{gas} = (\bar{C} - C_o) \frac{C_{ma}}{C_m - C_o} \quad (4-1)$$

where:

- $C_{gas}$  = Effluent gas concentration, dry basis, ppm
- $\bar{C}$  = Average gas concentration indicated by gas analyzer, dry basis ppm
- $C_{ma}$  = Actual concentration of the upscale calibration gas, ppm
- $C_m$  = Average of initial and final system calibration bias check responses for the upscale calibration gas, ppm
- $C_o$  = Average of initial and final system calibration bias check responses for the zero gas, ppm

### 3.3 SCAQMD Methods 1.1, 2.1, 3.1, and 4.1, Flow Rate Measurements

Traverse point locations and exhaust gas velocity, molecular weight, and moisture are determined following SCAQMD Methods 1.1, 2.1, 3.1, and 4.1, respectively. Data collected from SCAQMD Methods 1.1 through 4.1 are used to calculate stack gas flow rate. Method 1.1 outlines the procedures for selecting the proper traverse points, while Method 2.1 provides the methodology for performing the actual traverse. The exhaust gas molecular weight is determined per Method 3.1 using Method 100.1 data. Exhaust gas moisture content is determined following SCAQMD Method 4.1 procedures.

Velocity is measured during the test at selected discrete sample points at a cross section of the stack according to SCAQMD Method 1.1 requirements. The cross section is divided into equal areas, to allow measurement of velocity and temperature profiles across the stack. Pressure differential measurements will be performed at 24 traverse point locations, exceeding the Method 1.1 requirements of 16 traverse point locations.

In Method 2.1, a calibrated Type S pitot tube and thermocouple are used, in conjunction with an inclined manometer or magnehelic gauge to measure exhaust gas velocity pressure and temperature. From these data, the exhaust gas velocity is calculated using standard equations.

Exhaust gas moisture content will be measured gravimetrically following Method 4.1 procedures. With a standard impinger train, exhaust gas sample will be collected within a 3 foot radius of the center of the stack. For each moisture test, at least 21 standard cubic feet of sample gas will be collected at a rate less than 0.75 cubic foot per minute.

### 3.4 SCAQMD Method 5.2, Particulate Emissions Measurements

SCAQMD Method 5.2 is used to measure flue gas particulate concentration and emission rates. A sample is withdrawn isokinetically from the source. Particulate matter and condensable material (such as water vapor, organic compounds, and/or sulfuric acid) are collected in impingers and on a glass fiber filter maintained at  $248 \pm 25^{\circ}\text{F}$ . The quantity of solid particulate collected in the probe, impingers, connecting tubing and on the filter is determined gravimetrically.

A schematic of the Method 5.2 sample train is illustrated in Figure 3-2. The sample is collected using a stainless steel goose-necked, sharp-edged nozzle attached to a stainless steel probe. A stainless steel sheathed Type K thermocouple (TC) is used to measure stack temperature, while a stainless-steel S-type pitot and magnehelic gauge is used to measure stack gas velocity. The impingers are placed in an ice bath to maintain the sample gas temperature exiting the last impinger at  $60^{\circ}\text{F}$  or less. The first two impingers contain deionized water, the third impinger is empty, and the fourth impinger contains silica gel.

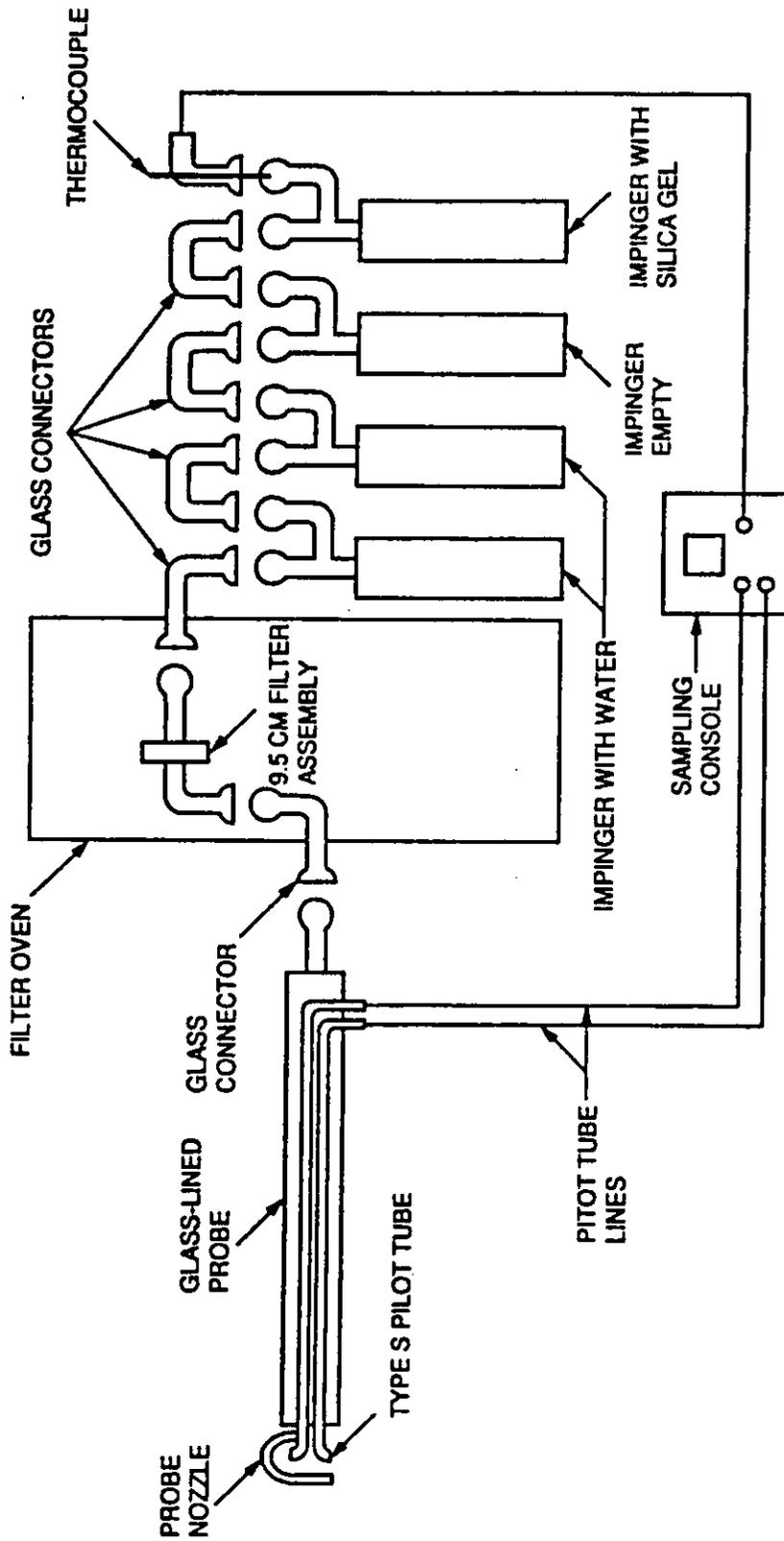
An air-tight pump equipped with a bypass and a shut-off valve maintains a controlled sample flow rate through the system. Sample flow rate is measured using a sharp-edged orifice with upstream and downstream pressure taps. The sample volume is measured using a dry gas meter.

All measurement devices (TC, TC readout, nozzle, pitot, balance for weighings, dry gas meter, orifice, and magnehelic gauges) are calibrated using National Bureau of Standards (NBS) traceable or equivalent techniques. The sample is collected isokinetically at each sample point by adjusting the sample flow rate according to the stack gas velocity and temperature conditions measured at that point.

The flue gas is sampled during the test at selected discrete sample points at a cross section of the stack, according to SCAQMD Method 1.1 requirements. The cross section is divided into 24 equal areas, and the sample is collected at the centroid of each equal area. This method is used to obtain a representative particulate sample across the stack cross section.

Pre-test and post-test leak checks are conducted for the sample train and pitot lines. The probe, sample line, and impingers are capped for return to the recovery area.

Figure 3-2. Particulate sampling train, Method 5.2



### **3.5 SCAQMD Draft Method 25.2, ROG Measurements**

ROG exhaust gas concentrations will be determined as per SCAQMD Method 25.2. A copy of this method is submitted in Appendix D. This method requires duplicate exhaust gas samples to be withdrawn at a constant rate and collected in Tedlar bags. Draft Method 25.2 samples will be collected over a one hour period at a single point within a 3 foot radius of the center of the exhaust stack.

As specified by Draft Method 25.2, the integrated samples are analyzed via TCA/FID. In this procedure, an aliquot of the sample gas is injected into a gas chromatograph/flame ionization detector (GC/FID) unit which separates the CO, carbon dioxide (CO<sub>2</sub>), and methane from the ROG present in the sample stream. The methane concentration is determined by the FID. The GC is then back-flushed to recover the ROG, which is subsequently oxidized and reduced to methane. The concentration of ROG (now in the form of methane) is then measured with an FID). Laboratory analyses will be performed by Truesdail Laboratories, Tustin, California, within 72 hours following sample collection.

### **3.6 SCAQMD Draft Method 207.1, Ammonia Slip Measurements**

Ammonia slip samples will be collected and analyzed following SCAQMD "Draft Method 207.1, Analytical Procedures for Determining Ammonia and Ammonium Compounds from Stationary Sources." A copy of this method is submitted in Appendix E. To collect the ammonia slip sample, Acurex Environmental will follow the general sampling procedures specified in SCAQMD Method 5.2, with the following exceptions:

- No heated filter or probe will be used. Instead, a teflon sampling probe will run directly for the source to the first impinger.
- Immediately following the post-test leak check, the impingers will be capped and the sample line rinsed with 0.1 N sulfuric acid or hydrochloric acid (i.e. the absorbing solution). The probe wash will be added to the impinger catch and rinsate for analysis.
- Exhaust gas will be collected for 60 minutes at a rate of 0.5 cubic feet per minute.
- Exhaust gas will be collected at a single point in the stack. The sampling point will be located within a 3 foot radius of the center of the stack.

Ammonia slip analyses will be performed as specified in the draft method.

## **SECTION 4**

### **ACUREX ENVIRONMENTAL QUALITY ASSURANCE PROCEDURES**

There are several internal quality control/quality assurance (QA/QC) procedures that Acurex Environmental routinely implements to ensure accurate and representative results. These procedures are discussed briefly here, and include stringent internal QA audits and data validation requirements, rigorous sample chain of custody procedures, and the collection of adequate QA samples. QA procedures for SCAQMD Method 100.1 are discussed in Section 3.1.

#### **4.1 Internal QA Auditing and Data Validation Procedures**

Key elements of the standard Environmental QA auditing procedures include: field sample recovery and data sheet QA audits (conducted in the field); mandatory pre- and post-test equipment calibration checks; thorough QA reviews of the reduced field data and the chemistry laboratory sample analysis reports for completeness; and finally, a QA and peer review of the draft and final source test report. Data validation procedures include calculating relevant data quality indicators such as measurement precision and accuracy, and evaluating these indicators in terms of data quality requirements specified by the applicable method.

#### **4.2 Sample QA and Chain of Custody Procedures**

The key elements of the standard Acurex Environmental chain of custody procedures are:

- Recovery of the sample in an appropriate work area using sample containers appropriate to the method
- Collection of all completed field data sheets by the Project Engineer
- Sample identification using a two part sample label; each part is stamped with the same sample identification number. The large label is affixed to the sample and the small label is affixed to the field data sheet

- Completion of the chain of custody (COC) forms, which identify the sample type, identification number, and the required analytical procedures. The COC form accompanies the samples to the analytical laboratory, and are signed at each transfer point
- Examination of the samples at each transfer point for integrity (i.e. broken seals or damaged containers)

Upon completion of the analyses, the analytical laboratory returns the COC forms with the results to Acurex Environmental. All samples are accounted for by the project engineer.

#### **4.3 QA Samples**

In addition to the standard QA procedures discussed above, Acurex Environmental will include the collection of various QA samples (field and solution blanks) that are typically included in source test events of this type. For all integrated sampling methods, one field blank will be collected and analyzed for every 10 test events. A reagent blank will be collected and analyzed for each lot of chemicals used.

**APPENDIX A**  
**PERMIT TO CONSTRUCT, APPLICATION NO. 261513**

*i*



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**Legal Owner  
or Operator:**

SO. CALIFORNIA EDISON COME  
P. O. BOX 800  
ROSEMEAD, CALIFORNIA 91770  
ATTN: PETER R. WELSTING

**Equipment Location:** 8998 ETIWANDA AVENUE, ETIWANDA, CA. 91739

The equipment described below and as shown on the approved plans and specifications are subject to the special condition, or conditions listed.

**Equipment Description:**

ALTERATION TO AN EXISTING UTILITY BOILER NO. 3, PERMIT NO. 11202B, BY THE ADDITION OF A RECIRCULATION GAS BYPASS (RGB) SYSTEM:

- 1.) A 4.5 FEET LONG BYPASS DUCT INSTALLED BETWEEN THE RECIRCULATION DUCT AND THE PRIMARY AIR DUCT.
- 2.) A BYPASS DAMPER LOCATED IN THE BYPASS DUCT.

**Conditions:**

1. OPERATION OF THIS BOILER SHALL BE CONDUCTED IN COMPLIANCE WITH ALL THE DATA, DRAWINGS, AND SPECIFICATIONS SUBMITTED WITH THE APPLICATION FOR ETIWANDA UNIT 3 UNLESS OTHERWISE NOTED BELOW.
2. THIS BOILER SHALL BE PROPERLY MAINTAINED AND KEPT IN GOOD CONDITION AT ALL TIMES.
3. THIS BOILER SHALL FIRE NATURAL GAS ONLY, EXCEPT AS ALLOWED BY RULE 1135 WHEN FUEL OIL SHALL BE FIRED.
4. FUEL OIL SUPPLIED AT THE BURNERS OF THIS BOILER SHALL CONTAIN 0.25 PERCENT OR LESS SULFUR BY WEIGHT.
5. THE MAXIMUM CONCENTRATION OF OXIDES OF NITROGEN (NO<sub>2</sub>) EMISSIONS, AT THE EXHAUST STACK, AVERAGED OVER ONE HOUR, SHALL NOT EXCEED 110 PPM WHEN FIRING NATURAL GAS AND 200 PPM WHEN FIRING FUEL OIL, DRY AND CORRECTED TO 3% OXYGEN (O<sub>2</sub>).

THESE NO<sub>x</sub> LIMITS ARE VALID THROUGH THE ENTIRE PERMIT TO CONSTRUCT PHASE. SUBSEQUENT NO<sub>x</sub> LIMITS WILL BE ESTABLISHED AT THE PERMIT TO OPERATE PHASE DEPENDING ON SOURCE TESTING RESULTS.

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6. THE MAXIMUM CONCENTRATION OF CARBON MONOXIDE (CO) EMISSIONS, AT THE EXHAUST STACK, AVERAGED OVER ONE HOUR, SHALL NOT EXCEED 500 PPM WHEN FIRING NATURAL GAS AND 500 PPM WHEN FIRING FUEL OIL, DRY AND CORRECTED TO 3% OXYGEN (O<sub>2</sub>).

THESE CO LIMITS ARE VALID THROUGH THE ENTIRE PERMIT TO CONSTRUCT PHASE. SUBSEQUENT CO LIMITS WILL BE ESTABLISHED AT THE PERMIT TO OPERATE PHASE DEPENDING ON SOURCE TESTING RESULTS.

7. ONCE THE INSTALLATION AND TESTING OF THE RECIRCULATION GAS BYPASS (RGB) SYSTEM HAS BEEN COMPLETED, THE SOUTHERN CALIFORNIA EDISON (SCE) SHALL SUBMIT TO THE DISTRICT BY DECEMBER 30, 1992, A FINAL REPORT CONSISTING OF THE FOLLOWING INFORMATION:

- A) A DETAILED DESCRIPTION OF HOW THE RGB MODIFICATION HAS REDUCED NO<sub>x</sub> AND THE AMOUNT OF NO<sub>x</sub> REDUCTION ACHIEVED OVER THE FULL BOILER LOAD RANGE OF OPERATION.
- B) A QUANTITATIVE ANALYSIS DISCUSSING THE EFFECT OF THE INSTALLATION RGB SYSTEM ON THE EMISSIONS OF CO, NO<sub>x</sub>, ROG, AND PARTICULATE MATTER AT VARIOUS BOILER LOADS AND OPERATING CONDITIONS. THIS ANALYSIS SHALL INCLUDE SOURCE TESTS CONDUCTED UNDER THE FOLLOWING CRITERIA:
- I) SOURCE TESTING SHALL BE CONDUCTED WITHIN 60 CALENDAR DAYS AFTER NORMAL OPERATION OF THIS BOILER HAS BEEN ESTABLISHED, BUT NO LATER THAN 180 DAYS AFTER INITIAL START-UP OF THE BOILER.
- II) THE SOURCE TEST SHALL MEASURE CO, NO<sub>x</sub>, AND O<sub>2</sub> BY USING DISTRICT METHOD 100.1; ROG BY USING DISTRICT METHOD 25.1; AND PARTICULATE MATTER BY USING DISTRICT METHOD 5.1.
- III) THE SOURCE TESTS FOR MEASURING CO, NO<sub>x</sub>, O<sub>2</sub>, ROG, AND PARTICULATE MATTER SHALL BE CONDUCTED AT BOILER LOADS OF 50 MW, 100 MW, 200 MW, 275 MW AND 320 MW WHEN THE RGB IS IN OPERATION AND WHEN THE RGB IS NOT IN OPERATION. THE SAMPLING TIME AT EACH LOAD SHALL BE AT A MINIMUM FOR ONE CONSECUTIVE HOUR.
- IV) A SOURCE TEST PROTOCOL SHALL BE SUBMITTED TO THE DISTRICT NOT LATER THAT 45 DAYS BEFORE THE PROPOSED TEST DATE AND SHALL BE APPROVED BY THE DIRECTOR OF ENGINEERING BEFORE THE SOURCE TESTS COMMENCE.



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- V) A TESTING LABORATORY CERTIFIED BY THE CALIFORNIA AIR RESOURCES BOARD AND IN COMPLIANCE WITH DISTRICT RULE 304 (NO CONFLICT OF INTEREST) SHALL CONDUCT THE TEST.
- VI) DURING SOURCE TESTING, THE FOLLOWING DATA SHALL BE COLLECTED FOR EACH TEST LOAD:
- a) FUEL FLOW RATE (MMSCF/HR FOR GAS AND GAL/HR FOR OIL) AT EACH LOAD,
  - b) AIR/FUEL RATIO AT EACH LOAD,
  - c) FLUE GAS FLOW RATE (MMSCF/HR) AT EACH LOAD,
  - d) MOISTURE CONTENT (%) AT EACH LOAD,
  - e) BOILER EXHAUST STACK TEMPERATURE (°F) AT EACH LOAD,
  - f) BOILER OUTPUT (NET MW) AT EACH LOAD,
- VII) THE SOURCE TEST REPORT SHALL PRESENT ALL EMISSION DATA IN UNITS OF POUNDS PER HOUR (LB/HR), AND PARTS PER MILLION (PPM), ON A DRY BASIS CORRECTED TO 3% OXYGEN.
- C) A QUANTITATIVE ANALYSIS OF NO<sub>x</sub> AND CO EMISSIONS BEFORE AND AFTER THE INSTALLATION OF THE RGB WHILE FIRING NATURAL GAS AND FIRING FUEL OIL, (IF FUEL OIL IS AVAILABLE). SUCH AN ANALYSIS SHALL COMPARE THE NO<sub>x</sub> AND CO EMISSIONS DATA, IN PPM (DRY CORRECTED TO 3 PERCENT OXYGEN), OVER A ONE HOUR BASIS, FOR ANY SEVEN (7) DAYS OF OPERATION BEFORE AND AFTER THE INSTALLATION OF THE UREA INJECTION SYSTEM. EACH DAY OF OPERATION SHALL BE FOR A TWENTY-FOUR (24) HOUR PERIOD. THE AVERAGE UTILITY BOILER LOAD SHALL ACCOMPANY EACH NO<sub>x</sub> AND CO DATA POINT. THE DATA SHALL BE SUBMITTED IN TABULAR FORM CONTAINED ON A 3.5" DISKETTE THAT IS FORMATTED FOR LOTUS 123.
8. IF THE UREA INJECTION SYSTEM IS OPERATED IN CONJUNCTION WITH THE RGB SYSTEM, THE MAXIMUM CONCENTRATION OF AMMONIA (NH<sub>3</sub>) SLIP AT THE EXHAUST DUCT, SHALL NOT EXCEED 20 PPM, CORRECTED TO 3% DRY OXYGEN (O<sub>2</sub>) AND AVERAGED OVER ONE HOUR, FOR BOTH GASEOUS FUEL AND FUEL OIL FIRING.
- THIS NH<sub>3</sub> LIMIT IS VALID THROUGH THE ENTIRE PERMIT TO CONSTRUCT PHASE. A SUBSEQUENT NH<sub>3</sub> LIMIT WILL BE ESTABLISHED AT THE PERMIT TO OPERATE PHASE DEPENDING ON SOURCE TESTING RESULTS.
9. IF THE UREA INJECTION SYSTEM IS OPERATED IN CONJUNCTION WITH THE RGB SYSTEM, THE CONCENTRATION OF UREA IN THE UREA/WATER SOLUTION INJECTED INTO THIS UTILITY BOILER SHALL CONTAIN NO MORE THAN THIRTY-FIVE (50) PERCENT UREA BY WEIGHT.



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10. IF THE UREA INJECTION SYSTEM IS OPERATED IN CONJUNCTION WITH THE RGB INJECTION SYSTEM, THE UREA/WATER SOLUTION RATE OF INJECTION INTO THIS BOILER SHALL NOT EXCEED THIRTY (30) GALLONS PER MINUTE (GPM) FOR EACH OF THE THREE INJECTION LOOPS.
11. IF THE UREA INJECTION SYSTEM IS OPERATED IN CONJUNCTION WITH THE RGB SYSTEM, THE OPERATOR OF THIS UTILITY BOILER SHALL INSTALL FLOW METERS THAT MEASURE THE UREA/WATER SOLUTION FLOW RATE IN GALLONS PER MINUTE.
12. IF THE UREA INJECTION SYSTEM IS OPERATED IN CONJUNCTION WITH THE RGB SYSTEM, THE OPERATOR OF THIS UTILITY BOILER SHALL MAINTAIN RECORDS OF THE CONCENTRATION OF UREA IN THE UREA/WATER SOLUTION AND THE UREA/WATER SOLUTION INJECTION FLOW RATES FOR THE VARIOUS BOILER LOADS. THE MANNER OF RECORD KEEPING SHALL BE APPROVED IN WRITING BY THE DIRECTOR OF THE COMPLIANCE DIVISION. ALL RECORDS SHALL BE RETAINED FOR A PERIOD OF TWO YEARS AND BE MADE AVAILABLE TO DISTRICT PERSONNEL UPON REQUEST.
13. IF THE UREA INJECTION SYSTEM IS OPERATED IN CONJUNCTION WITH THE RGB SYSTEM, THE FLOW RATE OF THE UREA/WATER SOLUTION SHALL BE REGULATED ACCORDING TO THE LOAD OF THE BOILER VIA A FULLY MODULATING AUTOMATIC CONTROL SYSTEM.
14. ONCE THE INSTALLATION AND TESTING OF THE RGB SYSTEM HAS BEEN COMPLETED AND IF THE UREA INJECTION SYSTEM IS OPERATED IN CONJUNCTION WITH THE RGB SYSTEM, SCE SHALL SUBMIT TO THE DISTRICT BY DECEMBER 30, 1992, A FINAL REPORT CONSISTING OF THE FOLLOWING INFORMATION:
  - A) A DESCRIPTION OF HOW THE UREA/WATER SOLUTION FLOW IS CONTROLLED AND REGULATED WHEN USED IN CONJUNCTION WITH THE RGB SYSTEM FOR VARIOUS BOILER LOADS.
  - B) A QUANTITATIVE ANALYSIS OF THE EFFECT OF UREA INJECTION ON THE EMISSIONS OF CO, NO<sub>x</sub>, NH<sub>3</sub>, ROG, AND PARTICULATE MATTER AT WHEN USED IN CONJUNCTION WITH THE RGB SYSTEM AT VARIOUS BOILER LOADS. THIS ANALYSIS SHALL INCLUDE SOURCE TESTS CONDUCTED UNDER THE FOLLOWING CRITERIA:
    - 1) SOURCE TESTING SHALL BE CONDUCTED WITHIN 60 CALENDAR DAYS AFTER NORMAL OPERATION OF THIS BOILER HAS BEEN ESTABLISHED WITH ITS ASSOCIATED UREA INJECTION SYSTEM, BUT NO LATER THAN 180 DAYS AFTER INITIAL START-UP OF THE BOILER WITH ITS ASSOCIATED UREA INJECTION SYSTEM.

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- II) THE SOURCE TEST SHALL MEASURE CO, NO<sub>x</sub>, AND O<sub>2</sub> BY USING DISTRICT METHOD 100.1; ROG BY USING DISTRICT METHOD 25.1; PARTICULATE MATTER BY USING DISTRICT METHOD 5.1; AND NH<sub>3</sub> SAMPLE EXTRACTION BY USING EPA METHOD 17 AND NH<sub>3</sub> ANALYSIS BY USING EPA METHOD 350.2.
- III) THE SOURCE TESTS FOR MEASURING CO, NO<sub>x</sub>, O<sub>2</sub>, ROG, NH<sub>3</sub> AND PARTICULATE MATTER SHALL BE CONDUCTED AT BOILER LOADS OF 50 MW, 100 MW, 200 MW, 275 MW AND 320 MW WHEN THE UREA INJECTION SYSTEM IS USED IN CONJUNCTION WITH THE RGB SYSTEM. THE SAMPLING TIME AT EACH LOAD SHALL BE AT A MINIMUM FOR ONE CONSECUTIVE HOUR.
- IV) A SOURCE TEST PROTOCOL SHALL BE SUBMITTED TO THE DISTRICT NOT LATER THAN 45 DAYS BEFORE THE PROPOSED TEST DATE AND SHALL BE APPROVED BY THE DIRECTOR OF ENGINEERING BEFORE THE SOURCE TESTS COMMENCE.
- V) A TESTING LABORATORY CERTIFIED BY THE CALIFORNIA AIR RESOURCES BOARD AND IN COMPLIANCE WITH DISTRICT RULE 304 (NO CONFLICT OF INTEREST) SHALL CONDUCT THE TEST.
- VI) DURING SOURCE TESTING, THE FOLLOWING DATA SHALL BE COLLECTED FOR EACH TEST LOAD WHEN THE UREA INJECTION SYSTEM IS USED IN CONJUNCTION WITH THE RGB SYSTEM:
- a) FUEL FLOW RATE (MMSCF/HR FOR GAS AND GAL/HR FOR OIL) AT EACH LOAD,
  - b) AIR/FUEL RATIO AT EACH LOAD,
  - c) FLUE GAS FLOW RATE (MMSCF/HR) AT EACH LOAD,
  - d) UREA INJECTION FLOW RATE (GAL/HR) AT EACH LOAD,
  - e) UREA CONCENTRATION (%) BY WEIGHT AT EACH LOAD
  - f) MOISTURE CONTENT (%) OF THE FLUE GASES AT EACH LOAD,
  - g) BOILER EXHAUST DUCT TEMPERATURE (°F) AT EACH LOAD,
  - h) BOILER OUTPUT (NET MW) AT EACH LOAD,
- VII) THE SOURCE TEST REPORT SHALL PRESENT ALL EMISSION DATA IN UNITS OF POUNDS PER HOUR (LB/HR), AND PARTS PER MILLION (PPM), ON A DRY BASIS AT 3% OXYGEN.



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- C) A QUANTITATIVE ANALYSIS OF NO<sub>x</sub> EMISSIONS BEFORE AND AFTER THE INSTALLATION OF THE RGB SYSTEM WHEN USED IN CONJUNCTION WITH THE RGB SYSTEM WHILE FIRING GASEOUS FUEL AND FIRING FUEL OIL (IF FUEL OIL IS AVAILABLE). SUCH AN ANALYSIS SHALL COMPARE THE NO<sub>x</sub> EMISSIONS DATA, IN PPM (DRY CORRECTED TO 3 PERCENT OXYGEN), OVER A ONE HOUR BASIS, FOR ANY SEVEN (7) DAYS OF OPERATION BEFORE AND AFTER THE INSTALLATION OF THE UREA INJECTION SYSTEM. EACH DAY OF OPERATION SHALL BE FOR A TWENTY-FOUR (24) HOUR PERIOD. THE AVERAGE UTILITY BOILER LOAD SHALL ACCOMPANY EACH NO<sub>x</sub> DATA POINT. THE DATA SHALL BE SUBMITTED IN TABULAR FORM CONTAINED ON A 3.5" DISKETTE THAT IS FORMATTED FOR LOTUS 123.
15. THE OWNER OR OPERATOR OF THIS BOILER SHALL INSTALL, OPERATE, AND MAINTAIN IN CALIBRATION AS REQUIRED BY RULE 1135, A CONTINUOUS EMISSION MONITORING SYSTEM (CEMS) FOR NO<sub>x</sub> AND A REMOTE TERMINAL UNIT (RTU) FOR DATA GATHERING THAT HAVE BEEN APPROVED BY THE DIRECTOR OF THE APPLIED SCIENCE AND TECHNOLOGY DIVISION TO DEMONSTRATE COMPLIANCE WITH THE DISTRICT-WIDE DAILY LIMITS AS STIPULATED IN RULE 1135.

Approval or denial of this application for permit to operate the above equipment will be made after an inspection to determine if the equipment has been constructed in accordance with the approved plans and specifications and if the equipment can be operated in compliance with all Rules of the South Coast Air Quality Management District.

Please notify D. W. STROUD at 714/396-2526 when construction of equipment is complete.

This Permit to Construct is based on the plans, specifications, and data submitted as it pertains to the release of air contaminants and control measures or reduce air contaminants. No approval or opinion concerning safety and other factors in design, construction or operation of the equipment is expressed or implied.

This Permit to Construct shall serve as a temporary Permit to Operate provided the Executive Officer is given prior notice of such intent to operate.

This Permit to Construct will become invalid if the Permit to Operate is denied or if this application is cancelled. THIS PERMIT TO CONSTRUCT SHALL EXPIRE ONE YEAR FROM THE DATE OF ISSUANCE unless an extension is granted by the Executive Officer.

*Dorris M. Bailey*

By  
DORRIS M. BAILEY  
Principal Office Assistant

DMB/eb

ORIGINAL

**APPENDIX A-2**  
**SCAQMD CONDITIONAL APPROVAL MEMORANDUM**



SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT  
APPLIED SCIENCE & TECHNOLOGY  
SOURCE TESTING & ENGINEERING BRANCH

PROTOCOL REVIEW

S/T I.D.: P93072

COMPANY: Southern California Edison  
P.O. Box 800  
Rosemead, CA 91770

EQUIPMENT: Etiwanda Boiler #3  
(A/N 261513)

LOCATION: 8998 Etiwanda Avenue  
Etiwanda, CA 91739

EVALUATE: NOx, CO, O2, ROG, Particulate Matter

REQUESTOR: Ben Shaw/ Darren Stroud

TYPE EVAL:	<input type="checkbox"/>	CEMS	<input type="checkbox"/>	CEMS	<input type="checkbox"/>	CEMS
		APPL.		PROT.		RPRT.
	<input checked="" type="checkbox"/>	PERF.	<input type="checkbox"/>	PERF.	<input type="checkbox"/>	OTHER:
		PROT.		RPRT.		

The document indicated above has been reviewed by the Evaluations Unit staff and has been determined to contain sufficient information, as presented (see Discussion/ Remediation below for specific instructions, if any).

The document indicated above has been reviewed by the Evaluations Unit staff and has been determined to contain insufficient information, or requires further explanation, in the following area(s) (see complete Discussion/Remediation below):

- Completeness of Application/Protocol/Report.
- Representativeness of Data & Process.
- Rule/Permit Fulfillment.
- Sampling & Analytical Methods.
- Quality Assurance
- Calculations.

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DISCUSSION

Representativeness of Data & Process

- OK 1) Procedures and schedule for calibrating thermocouples, pressure measurement devices, pitot tubes, and gas meters shall in accordance with Chapter III of the District Source Test Manual.
- Talk to District S. 2) Acurex offers to test for particulates at full load conditions only since gas recirculation redistribution and urea injection is not expected to impact particulate emissions. It is the District's experience however, that urea injection may cause excessive particulate emissions. Particulate measurements shall be measured at each test condition as required by the Permit Conditions.
- OK 3) NOx, CO, O2, and ROG shall be sampled concurrently. Moisture content shall be measured during the gas sampling.
- OK 4) The sensitivity of the differential pressure gauge for the velocity measurement device shall conform with Section 2.1.2 of District Method 2.1.  
AP < .05

Rule/Permit Fulfillment

- Mike E. To respond. 5) The protocol does not test for NOx and CO District Permit limits when firing fuel oil.
- OK 6) ROG and ammonia slip measurements shall be sampled for one consecutive hour to satisfy Permit Condition 7.B.III, rather than for 30 minutes as proposed by the protocol.
- OK \* 7) ROG shall be sampled using SCAQMD Method 25.1 to satisfy Permit Condition 7.B.II, rather than using SCAQMD Draft Method 25.2 as proposed by the protocol. In addition to ROG, the gas sample shall be analyzed and reported for carbon dioxide and carbon monoxide as outlined by SCAQMD Method 25.1.

Sampling & Analytical Methods

- ? 8) Exhaust flow shall be calculated using the Flue Factor Method (District Source Test Manual, Chapter 10, Section 2). Reference point velocities shall be recorded at five minute intervals.
- OK 9) The District requires a strict adherence, rather than a "general" accordance, to SCAQMD Method 100.1.
- ? OK 10) Since ammonia is present in the exhaust, a molybdenum NO2 to NO converter will be necessary.
- Be discussed in 29 minutes 100 response to District letter. 11) The method for determining stratification, according to District Procedures, requires 48 points for stacks greater than 107.6 ft<sup>2</sup> in cross sectional area. The sampling procedure of alternating between a traverse point and a sampling point is mid & low

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to be observed. Refer to District Source Test Manual, Chapter 10, Section 13) for sampling and calculation procedures.

*See memo 10/13/93  
1 to 2 response*

12) In addition to testing for stratification, a test for the absence of cyclonic flow should be performed per District Method 1.1.

13) Should stratification using the above method prove to be greater than 10 percent, gaseous concentrations may be calculated on a weighted average basis, but only in the absence of cyclonic flow. For example, the following procedure would be acceptable:

At every traverse point, the concentration of each gaseous constituent (excluding moisture) and velocity will be determined. Moisture may be determined at each point by the following relation:

$$\%H_2O = \left[ 1 - \frac{1}{1 + 0.018 (\%CO_2 + \%CO)} \right] \times 100$$

The total mass flow rate of the constituent may then be calculated by :

$$\text{Lbs/hr} = (1.583 \times 10^{-7})(MW) \sum (\text{Flow})_i (\text{ppm})_i$$

where "i" denotes a traverse point, and "Flow" is flue factor corrected flow in units of dry standard cubic feet per minute.

If average flow rate is determined by dividing the summation of the traverse flow rates by the number of traverse points, then the average concentration is calculated by:

$$\text{Avg ppm} = \frac{\text{Total Mass Flow Rate}}{(1.583 \times 10^{-7})(MW)(\text{Avg Flow Rate})}$$

? \* 14) For particulate sampling using District Method 5.2, the glass fiber filter is to be maintained between 180°-200° F, rather than 248 ± 25° F as specified in the protocol.

OK 15) Permit Condition 14.A.II requires EPA Method 17 for sampling ammonia. Traverse sampling however, is not required for non-stratified conditions.

General Continuous Gas Monitoring Requirements

\* The District requires continuous gas monitoring equipment employing sample extraction and conditioning, and electronic detection, to be conducted strictly according to District Method 100.1, with the emphasis upon representativeness, documentation, and quality assurance. This includes, in part:

✓ OK 1. Gas analyzers must meet minimum acceptable standards for method of detection, sensitivity, noise, precision, linearity, and interference (see TABLE 100.1-1 for

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details). Also, the gas sample extraction and conditioning equipment (probe, filter, pump, conditioner, connective plumbing, etc., and data acquisition and logging equipment shall meet minimum acceptable specifications, as described in Method 100.1.

OK (2)

2. The entire sampling system for continuous gas monitoring instruments should be leak checked before and after each test run by evacuating the system to a minimum of 20" in. Hg vacuum, and plugging for a period of five minutes. The resultant loss of vacuum can not exceed 1" Hg during this period.

J OK

3. Calibration of all analyzers must be accomplished at zero, mid span (40-60% of full scale range), and high span (80-95% of full scale range). The lowest practicable range should be selected for monitoring, so that the measured emission values are within 20-95% of the range. If a significant amount of the data are outside of this range, the data may be rejected, depending upon the application.

Check with Bruce for... OK

The calibration gases must be certified according to EPA Protocol Number 1, or certified to an analytical accuracy of + 1% and be NIST traceable (except cal gases used for system bias check). Generally, if cal gases are more than 18 months old, they must be recertified (superblends, 6 months).

OK

5. A calibration error check, and zero/span drift check must be performed before and after each test run. Calibration error must be less than + 2% of the range of measurement for zero, mid, and high range calibration gases. Zero/span drift must be less than + 3% of the range of measurement.

OK

6. A system bias check must be performed before and after each test run by alternately introducing cal gases to the entire sampling system, then to the gas analyzer(s), for comparison. The difference can not exceed + 5% of the analyzer range.

? OK

(7)

7. Semi-annual analyzer certifications consisting of linearity plot, calibration curve, response time, interference response, and NO<sub>2</sub> to NO converter efficiency, must be furnished with the other calibrations to satisfy Q/A documentary requirements.

? OK

8. NOx measurement must be performed in the NOx mode of the analyzer. An NO<sub>2</sub> to NO converter is required if NO<sub>2</sub> constitutes 5% or more of the total NOx in the sample stream, or the rule or permit condition requires "NOx" monitoring. The NO<sub>2</sub> to NO converter must be at least 90% efficient (as demonstrated by EPA Method 20, Sect. 5.6). The converter should be high temperature (650°C) stainless steel, if no NH<sub>3</sub> is present. If NH<sub>3</sub> is present in the sample stream, then a low temperature (350°C) molybdenum catalyst must be used in the converter.

? OK

9. The connective tubing from the probe to the sample conditioner must be heated above the dewpoint and the dewpoint reported. The sample conditioner must be able to maintain a dewpoint temperature below 35° F. A particulate filter, as described by District Method 100.1, shall also be installed.

? OK

10. Data recorder resolution must be at least 0.5% of the range of measurement. A data point for each contaminant/diluent monitored must be recorded at least once/minute. Analog chart recorders must have a minimum 10-inch chart width.

## PROTOCOL REVIEW

PAGE 5 OF 6

- OK
11. All facets of testing must be continuously recorded. This includes the 3-point calibration, system bias, calibration error, and zero/span drift checks, which must precede and conclude each test run.
- OK
12. All chart traces, or digital printouts, must be included in the final report and must be clearly identified as to:
- |                       |                                 |
|-----------------------|---------------------------------|
| -location/source      | -range changes                  |
| -operator initials    | -range of measurement           |
| -date/running times   | -calibrations                   |
| -actual test interval | -cal gas concentration/cyl. no. |
| -contaminant/diluent  | -range of calibration           |

When more than one gas trace is shown on a chart, the individual traces must be distinguishable by color coding or some other means (original charts may be submitted, and returned following evaluation). If a gas measurement range has been "offset" from zero, or zero has been "transposed to the right side of the recorder chart, it must be clearly identified.

- OK
13. Gaseous measurements must be conducted a minimum of 60 continuous minutes at each load or specified condition, after the readings have stabilized.

### Final Test Report

The final Source Test Report must include the following data:

1. A summary of the Source Test results, including applicable rules and permit conditions (show allowable standards) and source test data computed so as to satisfy these requirements.
2. A brief process description. Indicate equipment operation during testing, as well as any other information which may influence the final report.
3. A simple schematic diagram of the process, showing the sampling location, with respect to the upstream and downstream flow disturbances. Also include a cross-sectional diagram of the stack or duct at the sampling location, depicting the sampling points with respect to compass direction.
4. The sampling and analytical procedures. Be specific about all aspects of sampling and analysis. Include diagrams of test equipment and methods.
5. Complete raw field data, including production data indicative of the testing interval, lab analyses, and the test results (show all calculations).
6. Calibration data regarding all sampling and measuring equipment utilized during testing (see District Source Testing Manual, Chapter III or "Quality Assurance Handbook For Air Pollution Measurement Systems", Vol. III, U.S. EPA-600/4-77-0276).
7. A detailed chain-of-custody sheet containing all pertinent test equipment documentation from lab to field and back to the lab, including any change of hand in between.

PROTOCOL REVIEW

PAGE 6 OF 6

REMEDIATION

Testing may proceed as described in the protocol with the implementation of the measures discussed in this evaluation.

The above measures must be implemented in the test protocol prior to testing.

Modifications to the approved protocol, without written consent from the District, may result in rejection of the final report.

EVALUATOR: Glenn Kasai EXT: 2271 DATE: June 1, 1993

P93072.DOC

**APPENDIX A-3**

**COMMUNICATION MEMO DATED JANUARY 18, 1994**



# TELEPHONE CONFERENCE RECORD

TIME	DATE
7:55 AM	1/18/94

PROJECT  
ETIWANDA UNIT 3 FGR + UREA COMPLIANCE TESTING

SUBJECT  
SOURCE TEST DETAILS A/N 261513

CONFEREES SCE TELEPHONE AGENCY  
MIKE ESCARCEGA DARREN STROUD (SCAQMD)  
(909) 396-2526

CONFERENCE HIGHLIGHTS

SUMMARY

THE BELOW ITEMS WERE DISCUSSED & AGREED TO :

- NO PARTICULATE TESTING IS REQUIRED AT ANY OF THE TEST LOADS (LOW, MID & HIGH) OR TEST CONDITIONS (BASELINE, FGR ON, FGR + UREA) AS FGR & UREA ARE EXPECTED TO HAVE NEGLIGIBLE IMPACTS.
- ROGS - BECAUSE FGR IS EXPECTED TO HAVE NEGLIGIBLE IMPACTS ON ROGS & BECAUSE PREVIOUS ROG TESTS ON OTHER SCE UNITS WITH UREA HAVE DEMONSTRATED NEGLIGIBLE IMPACTS, IT WAS AGREED THAT ROGS WOULD ONLY BE SAMPLED AT THE HIGH LOAD FGR + UREA CONDITION AND THE HIGH LOAD BASELINE.

NOTE: THE ABOVE TWO AGREED UPON ITEMS SUPERCEDE

ADDITIONAL COMMENTS

ITEMS 2 & 6 OF MY LETTER TO YOU DATED OCT. 21, 1993 RE. SOURCE TEST DETAILS.

ACTION REQUIRED

---



---

CC: P.R. WELSHING  
S.D. PEASE  
DARREN STROUD (SCAQMD)  
GLENN KASAI (SCAQMD)

PREPARED BY  
Michael J. Garman  
(818) 302-4032

PAX



**APPENDIX A-4**

**COMMUNICATION MEMO DATED JANUARY 19, 1994**



TELEPHONE CONFERENCE RECORD

TIME 3:30 PM

DATE 1/19/94

PROJECT ETIWANDA UNIT 3 FGR+UREA COMPLIANCE TESTING

SUBJECT SOURCE TEST DETAILS AIN 261513

CONFEREES SCE MIKE ESCARCEGA

TELEPHONE AGENCY GLENN KASAI (SCAQMD) (909) 396-2271

CONFERENCE HIGHLIGHTS

SUMMARY

THE BELOW ITEM WAS DISCUSSED & AGREED TO:

- SIXTEEN POINT ABBREVIATED STRATIFICATION & CYCLONIC FLOW TESTS AT LOW AND MID-LOADS WOULD BE ACCEPTABLE INSTEAD OF THE FULL CHAPTER X 48-POINT TESTS. ALSO, THE FULL LOAD REQUIREMENT WOULD BE MET BY A PREVIOUS 48-POINT STRATIFICATION & CYCLONIC FLOW TEST THAT WAS PERFORMED AS PART OF THE RULE 1135 COMPLIANCE PROGRAM.

NOTE: THE ABOVE AGREED UPON ITEM SUPERCEDES ITEMS 11 & 12 OF MY LETTER TO DARREN STROUD DATED OCT. 21, 1993 REGARDING SCE'S RESPONSE TO YOUR PROTOCOL REVIEW.

ACTION REQUIRED

CC: P.R. WELSING  
 S.D. PEASE  
 GLENN KASAI (SCAQMD)  
 DARREN STROUD (SCAQMD)

PREPARED BY Mike D. Escarcega  
 (818) 302-4032



**APPENDIX B**  
**RECORDS OF BOILER OPERATING PARAMETERS**





Test No.	Time	Load	Aux. Power	BOOS	Steam Flow	FD Water Flow	S. H. Temp.	R. H. Temp.	Total Fuel Flow	Air Flow	O2 North - East	O2 South - West	FD Fans Amps - E/W	FGR Amps - E/W	APH Outlet Temp E/W	FGR Dampers E/W	FGR O2 E/W	Water Flow	Water Pressure	KVB Reference Time	KVB Fuel Flow	KVB Stack Flow	KVB O2	KVB NOx raw.	KVB NOx corr.	KVB NOx	KVB Lead	
	3/22/94	3*																										
	1315	320	9.2	None	1883	1998	1053	1003/1003	73.6	79.2	1.2	0.9	214/218	83/78	240/272	105/105	17.4/17.7	1.4	4.7	60.2	1330	3078.3	575.1	3.85	43.1	45.2	179	318.4
	1515	320	9.1	None	1889	2005	1053	1002/1004	73.6	79.4	1.0	1.0	214/212	82/77	237/268	0.77				1400	1515	3072.9	569.4	3.71	57.4	59.6	234	318.8
	1545	320	9.0	None	1889	2002	1056	1003/1002	23.7	79.3	0.8	0.9	214/214	82/76	237/267	0.77				1520	1545	3075.4	569.5	3.70	58.0	60.3	236	319.5
	1600																			1600								

\* test rerun due to a bad Rob test during first run (1100 - 1200)

1.05

Test Description:		Flue Gas Recirc. Bypass Compliance Test									
Unit:		St. Wendel Unit #3									
Data By:		S. Reese / M. Wilson									
Date	Time	im/d	hr	min	sec	min	sec	min	sec	min	sec
		3/23/94	5								
Test No.											6
Time		07:45				08:45					10:30
Load		250				250					250
Aux. Power		7.9				7.9					7.9
BOOS		None				None					None
Steam Flow		1439				1429				1433	1432
FD Water Flow		1576				1569				1559	1561
S. H. Temp.		1053				1052				1051	1053
R.H. Temp.		1005				1004				1003	1003
Total Fuel Flow		54.7				54.3				55.2	54.6
Air Flow		61.8				61.4				61.9	61.5
O2 North - East		1.5				1.2				1.2	1.2
O2 South - West		1.0				1.0				0.9	1.0
FD Fans - E/W		160/150				160/150				160/150	160/150
FGR - E/W		82/79				82/79				83/79	82/79
APH Outlet Temp. E/W		214/226				217/223				219/234	220/236
FBR Dampers - E/W		-				-				-	-
FBR O2 - E/W		-				-				-	-
Urea Flow		-				-				-	-
Water Flow		-				-				-	-
Water Pressure		-				-				-	-
KVB Reference Time		08:00				08:15				09:15	11:15
KVB Fuel Flow		2384.3				2384.9				2375.5	2377.1
KVB Stack Flow		462.1				461.4				458.2	460.4
KVB O2		4.46				4.43				4.38	4.45
KVB NOx raw.		40.9				40.6				40.5	41.3
KVB NOx corr.		44.5				44.2				43.8	45.0
KVB NOx		135				134				133	136
KVB Lead		250.5				250.4				249.3	249.6

Unit Spun 1-05  
 Consent 2070

Flasbas Recin. Bypass Compliance Test  
 5. Please

Test Description:	Flasbas Recin. Bypass Compliance Test		3/23/94	
Unit:	St. Vincent Unit # 3			
Data By:	S. Please			
Date	3/23/94	3/23/94	3/23/94	3/23/94
Test No.	7	8	8	8
Time	12:30	13:30	14:17	15:17
Load	250	250	250	250
Aux. Power	7.9	7.9	7.9	7.9
BOOS	None	None	None	None
Steam Flow	1439	1432	1433	1435
FD Water Flow	1545	1541	1545	1534
S. H. Temp.	1052	1052	1053	1052
R.H. Temp.	1010	1013	1013	1012
Total Fuel Flow	55.5	55.2	55.0	55.4
Air Flow	62.2	62.2	62.1	62.4
O2 North - East	1.2	1.1	1.1	1.0
O2 South - West	1.0	.9	1.0	.7
FD Fans - E/W	160/150	160/150	160/150	160/150
FGR - E/W	85/82	85/82	85/82	85/82
APH Outlet Temp. E/W	224/238	226/239	226/240	227/240
FGR Dampers E/W	105	105	105	105
FGR O2 E/W	16.8/16.7	16.6/7.0	16.5/16.7	16.6/16.9
Urea Flow	-	-	.7	.6
Water Flow	-	-	5.8	5.7
Water Pressure	-	-	54.8	54.6
KVB Reference Time	12:45	13:15	14:30	15:30
KVB Fuel Flow	2386.3	2386.1	2386.9	2385.3
KVB Stack Flow	460.9	460.5	461.9	459.8
KVB O2	4.41	4.39	4.44	4.37
KVB NOx raw.	24.1	29.2	25.2	25.8
KVB NOx corr.	31.6	31.7	27.4	27.9
KVB NOx	96	96	83	85
KUB Load	250.4	250.2	249.8	249.6



Date	mm/dd/yyyy	3/23/94						
Test No.	hrs	9						
Time	mm	2:00						2:00
Load	MW	118						120
Aux. Power	MW	6.8						6.8
BOOS		None						None
Steam Flow	kKlbs/hr	713						720
FD Water Flow	kKlbs/hr	773						802
S. H. Temp.	deg F	1052						1052
R.H. Temp.	deg F	1003/1006						1003/1001
Total Fuel Flow	%	28.9						28.6
Air Flow	%	29.6						29.7
O2 North - East	%	0.8						0.9
O2 South - West	%	1-2						1-3
FD Fans <del>N/S</del> - E/W	Amps	103/90						103/90
FGR <del>N/S</del> - E/W	Amps	80/80						81/79
APH Outlet Temp Ek		201/189						198/188
FGR Dampers E/W		OFF						OFF
FGR O <sub>2</sub> E/W								
Urea Flow								
Water Flow								
Water Pressure								
KVB Reference Time	hrs	2:05						2:15
KVB Fuel Flow	KSCFH	1262.7						1266.8
KVB Stack Flow	KSCFMI	260.2						260.6
KVB O <sub>2</sub>	%	5.45						5.42
KVB NOx raw.	ppm	19.5						20.3
KVB NOx corr.	ppm	22.4						23.5
KVB NOx	lbs/hr	37						37
KVB Lead		121.4						123.8

Flue Gas Recirc. Bypass Compliance Test  
 St. Joseph's Unit #3  
 S. Pease

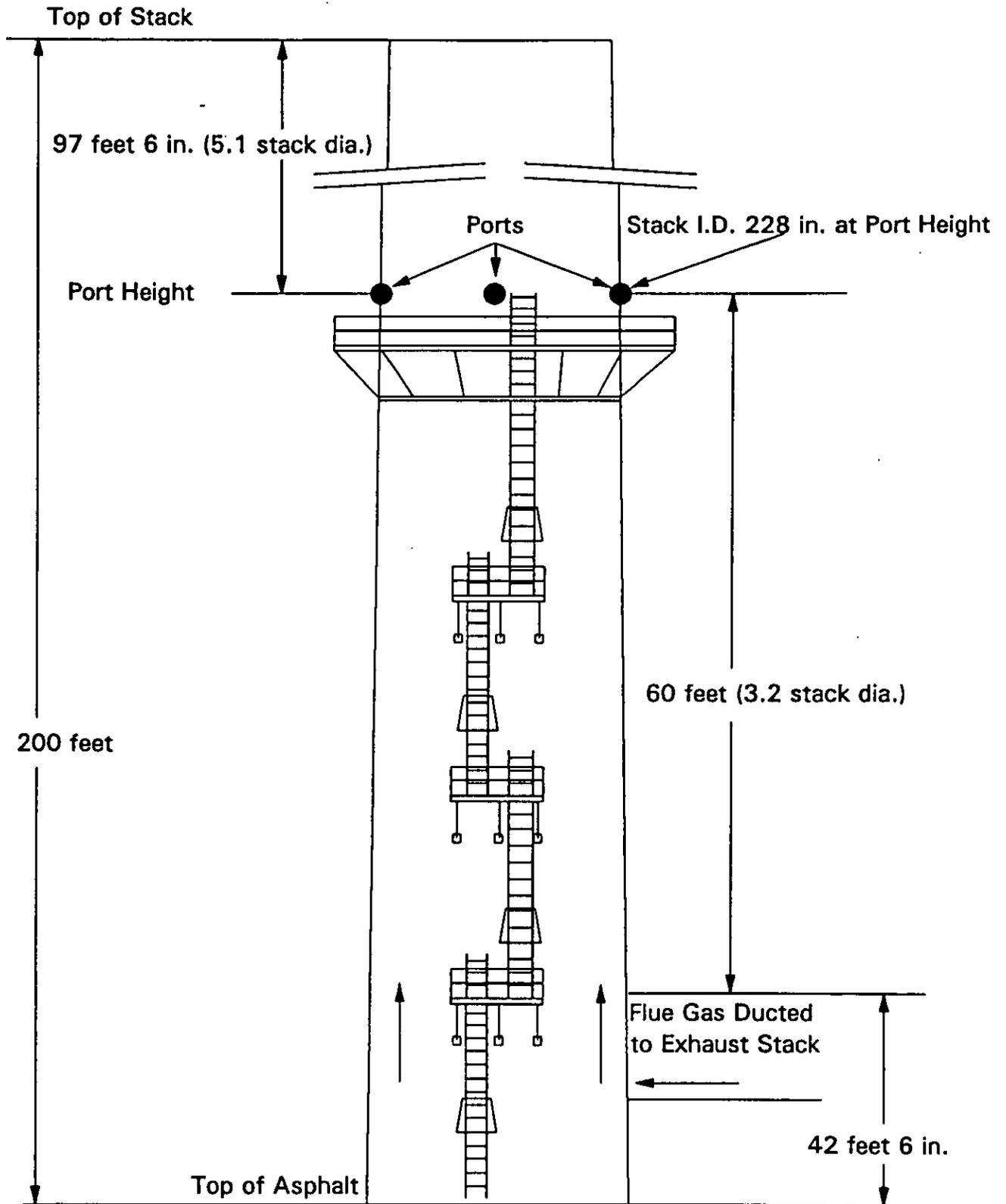
Date	3/23/94	3/24/94	3/24/94
Test No.	10	Run (1830-0030)	Run (0115-0215)
Time	2330	0000	0115
Load	119	119	120
Aux. Power	6.8	6.8	6.8
BOOS	None	None	None
Steam Flow	713	714	717
FD Water Flow	790	790	773
S. H. Temp.	1053	1058	1054
R.H. Temp.	1000/1002	1000/1003	1005/1003
Total Fuel Flow	290	286	287
Air Flow	298	293	298
O2 North - East	1.1	1.0	1.1
O2 South - West	1.0	0.9	0.9
FD Fans Amps - E/W	103/90	105/90	103/89
FGR Amps - E/W	81/79	81/79	81/79
APH Outlet Temp. E/W	155/188	152/187	191/191
Flue Dampers E/W	OFF	OFF	60/60
Flue O <sub>2</sub> E/W			16.1/16.3
Urea Flow			OFF
Water Flow			
Water Pressure			
KVB Reference Time	2345	0015	0130
KVB Fuel Flow	1264.8	1265.4	1270.0
KVB Stack Flow	260.3	260.3	261.6
KVB O <sub>2</sub>	5.42	5.41	5.42
KVB NOx raw.	19.2	19.1	12.9
KVB NOx corr.	22.2	22.1	14.9
KVB NOx	36.0	36	24
KVB Lead	1219	1220	1227
			122.7
			123.0
			122.7
			122.7

**APPENDIX C**

**STACK DIAGRAM ILLUSTRATING SAMPLING PORT LOCATIONS**



ETIWANDA UNIT 3





**APPENDIX D**

**RECORDS SUPPORTING SCAQMD METHOD 100.1 MEASUREMENTS**



**APPENDIX D-1**  
**CALIBRATION GAS CERTIFICATION SHEETS**





# SCOTT-MARRIN, INC.

6531 BOX SPRINGS BLVD. • RIVERSIDE, CA 92507  
TELEPHONE (714) 653-6780 • FAX (714) 653-2430

## REPORT OF ANALYSIS NIST TRACEABLE GAS MIXTURES

ACUR01  
TO: CHAD GARRETTSON  
ACUREX  
4879 E LA PALMA AVE  
STE 201  
ANAHEIM, CA 92807-

DATE: 02/19/93

CUSTOMER ORDER NUMBER: EV40239Z

PAGE 1

CYLINDER NUMBER	COMPONENT	CONCENTRATION (v/v)	NIST TRACEABLE REFERENCE STANDARD
CC66796	Oxygen Nitrogen	17.04 ± 0.17 % Balance	SRM 2659
CC51254	Oxygen Nitrogen	9.14 ± 0.09 % Balance	SRM 2658a
CC28267	Oxygen Nitrogen	4.20 ± 0.04 % Balance	SRM 2658a

ppm = umole/mole

% = mole-%

The above analyses are traceable to the National Institute of Standards and Technology by intercomparison with the reference standards listed above. Where indicated, volumetric and gravimetric reference standards are traceable thru use of our analytical balance. NIST Report No. MMAP 232.09/202491.

Analyst:

-----  
M.S. Calhoun

Approved:

-----  
J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS



# Scott Specialty Gases, Inc.

2600 CAJON BOULEVARD, SAN BERNARDINO, CA 92411

(909) 887-2671 FAX: (909) 887-0540

## CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS RECERTIFICATION

**Customer**  
ACUREX CORPORATION  
CHAD GARRETSON  
4879 E LA PALMA AVE  
SUITE 201  
ANAHEIM CA 92807

**Assay Laboratory**  
Scott Specialty Gases  
2600 Cajon Boulevard  
San Bernardino, CA 92411

**Purchase Order** NV30371SC  
**Scott Project #** 0227883#002

### ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure #G1, Section Number 3.0.4

**Cylinder Number** AAL5362  
**Cylinder Pressure** 950PSIG

**Certification Date** 10-05-93  
**Previous Certification Dates** 12-30-91

**Acid Rain Exp.**  
**General Exp.** 10-05-95

### ANALYZED CYLINDER

**Components**  
NITRIC OXIDE

**Certified Concentration**  
91.87PPM

**Analytical Uncertainty\***  
±1% NIST Traceable

**Balance Gas:** Nitrogen  
NOX

92.18PPM

\*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes.

### REFERENCE STANDARD

**Type** GMIS  
**Expiration Date** 09-94

**Cylinder Number**  
ALM33883

**Concentration**  
99.20PPM

### INSTRUMENTATION

**Instrument/Model/Serial #**  
TECO / 10AR-38644-258

**Last Date Calibrated**  
07-26-93

**Analytical Principle**  
Chemi-Luminescent

### ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

Components	Previous Certification	Third Triad Analysis	Calibration Curve
NITRIC OXIDE	<b>Date:</b> 12-30-91 <b>Response Units:</b> mv Z1=                  R1=                  T1= R2=                  Z2=                  T2= Z3=                  T3=                  R3= <b>Avg. Conc. of Cust Cyl.</b> 91.42PPM	<b>Date:</b> 10-05-93 <b>Response Units:</b> mv Z1= 0.00              R1= 96.6              T1= 89.2 R2= 96.6              Z2= 0.00              T2= 89.2 Z3= 0.00              T3= 89.2              R3= 96.6 <b>Avg. Conc. of Cust Cyl.</b> 91.87PPM	<b>Concentration=</b> Ax + B A = 1.026289 B = 0.328756
	<b>Date:</b> <b>Response Units:</b> Z1=                  R1=                  T1= R2=                  Z2=                  T2= Z3=                  T3=                  R3= <b>Avg. Conc. of Cust Cyl.</b>	<b>Date:</b> <b>Response Units:</b> Z1=                  R1=                  T1= R2=                  Z2=                  T2= Z3=                  T3=                  R3= <b>Avg. Conc. of Cust Cyl.</b>	<b>Concentration=</b>
	<b>Date:</b> <b>Response Units:</b> Z1=                  R1=                  T1= R2=                  Z2=                  T2= Z3=                  T3=                  R3= <b>Avg. Conc. of Cust Cyl.</b>	<b>Date:</b> <b>Response Units:</b> Z1=                  R1=                  T1= R2=                  Z2=                  T2= Z3=                  T3=                  R3= <b>Avg. Conc. of Cust Cyl.</b>	<b>Concentration=</b>

SPECIAL NOTES: IF THIS PRODUCT IS USED FOR ACID RAIN COMPLIANCE, THE ACID RAIN DATE NOTED ABOVE APPLIES PER 40 CFR PART 75, APPENDIX C. OTHERWISE THE GENERAL EXPIRATION DATE APPLIES.

Analyst 



# Scott Specialty Gases, Inc.

2600 CAJON BOULEVARD, SAN BERNARDINO, CA 92411

(909) 887-2571 FAX: (909) 887-0549

## CERTIFICATE OF ANALYSIS: EPA PROTOCOL GAS RECERTIFICATION

**Customer**  
ACUREX CORPORATION  
CHAD GARRETSON  
4879 E LA PALMA AVE  
SUITE 201  
ANAHEIM CA 92807

**Assay Laboratory**  
Scott Specialty Gases  
2600 Cajon Boulevard  
San Bernardino, CA 92411

**Purchase Order** NV30371SC  
**Scott Project #** 0227883#003

### ANALYTICAL INFORMATION

Certified to exceed the minimum specifications of EPA Protocol 1 Procedure #G1, Section Number 3.0.4

**Cylinder Number** AAL14063  
**Cylinder Pressure** 1400PSIG

**Certification Date** 10-05-93  
**Previous Certification Dates** 12-30-91

**Acid Rain Exp.**  
General Exp. 10-05-95

### ANALYZED CYLINDER

**Components**  
NITRIC OXIDE

**Certified Concentration**  
47.78PPM

**Analytical Uncertainty\***  
±1% NIST Traceable

**Balance Gas: Nitrogen**

**NOX**

47.95PPM

\*Analytical uncertainty is inclusive of usual known error sources which at least includes reference standard error & precision of the measurement processes.

### REFERENCE STANDARD

**Type** GMS  
**Expiration Date** 09-94

**Cylinder Number**  
ALM33883

**Concentration**  
99.20PPM

### INSTRUMENTATION

**Instrument/Model/Serial #**  
TECO / 10AR-38644-258

**Last Date Calibrated**  
07-26-93

**Analytical Principle**  
Chemi-Luminescent

### ANALYZER READINGS (Z=Zero Gas R=Reference Gas T=Test Gas r=Correlation Coefficient)

**Components**

**Previous Certification**

**Third Triad Analysis**

**Calibration Curve**

NITRIC OXIDE

Date: 12-30-91			Response Units: mv		
Z1=	R1=	T1=	Z1=	R1=	T1=
R2=	Z2=	T2=	R2=	Z2=	T2=
Z3=	T3=	R3=	Z3=	T3=	R3=
Avg. Conc. of Cust Cyl.			47.80PPM		

Date: 10-05-93			Response Units: mv		
Z1=	R1=	T1=	Z1=	R1=	T1=
R2=	Z2=	T2=	R2=	Z2=	T2=
Z3=	T3=	R3=	Z3=	T3=	R3=
Avg. Conc. of Cust Cyl.			47.78PPM		

Concentration=		Ax + B
A = 1.026289		
B = -0.328756		

Date:			Response Units:		
Z1=	R1=	T1=	Z1=	R1=	T1=
R2=	Z2=	T2=	R2=	Z2=	T2=
Z3=	T3=	R3=	Z3=	T3=	R3=
Avg. Conc. of Cust Cyl.					

Date:			Response Units:		
Z1=	R1=	T1=	Z1=	R1=	T1=
R2=	Z2=	T2=	R2=	Z2=	T2=
Z3=	T3=	R3=	Z3=	T3=	R3=
Avg. Conc. of Cust Cyl.					

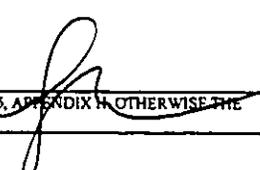
Concentration=		
----------------	--	--

Date:			Response Units:		
Z1=	R1=	T1=	Z1=	R1=	T1=
R2=	Z2=	T2=	R2=	Z2=	T2=
Z3=	T3=	R3=	Z3=	T3=	R3=
Avg. Conc. of Cust Cyl.					

Date:			Response Units:		
Z1=	R1=	T1=	Z1=	R1=	T1=
R2=	Z2=	T2=	R2=	Z2=	T2=
Z3=	T3=	R3=	Z3=	T3=	R3=
Avg. Conc. of Cust Cyl.					

Concentration=		
----------------	--	--

SPECIAL NOTES: IF THIS PRODUCT IS USED FOR ACID RAIN COMPLIANCE, THE ACID RAIN DATE NOTED ABOVE APPLIES PER 40 CFT PART 75, APPENDIX H, OTHERWISE THE GENERAL EXPIRATION DATE APPLIES.

Analyst 

AIR PRODUCTS AND CHEMICALS, INC.  
201 WEST 12TH STREET  
LONG BEACH, CA 90802  
TEL: 407-0441  
PHONE (800) 370-0441

DATE: 10/27/93  
TIME: 11:00  
PAGE: 1

\*\*\*\*\*  
↓ CERTIFICATE OF ANALYSIS ↓  
\*\*\*\*\*

ANALYST: ENVIRONMENTAL DOSE  
O.S. TECHNOLOGY PTIVE SUITE 5210  
IRVINE CA 92718

CUSTOMER ACCOUNT : 75819  
CUSTOMER ORDER NO : NV3037450  
ORDER NO : 235-052029  
ORDER DETAIL SEQ : 3  
SHIPPER NUMBER : 235-6-53499

REMARKS :

SPS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS S  
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS  
(SRM's) - REFERENCE APCI 56D FIELD DIRECTIVE BOOK I PART A-3.

PRIMARY GAS MIXTURE : CARBON MONOXIDE IN NITROGEN

ANALYSIS	BAR	COMPONENT	CONCENTRATION	ANALYTICAL	UNIT OF
DATE	CODE	REQUESTED	REQUESTED	RESULT	MEASURE
10/25/93	PK0551	CARBON MONOXIDE Nitrogen	450	451 BALANCE	MOLAR FPM

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED  
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE  
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

*Eileen Black Rodriguez*  
AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.  
901 WEST 12TH STREET  
LONG BEACH, CA 90813  
(310) 437-0461  
TELEPHONE (800) 350-0461

DATE: 12/21/93  
TIME: 17:38  
PAGE: 1

\*\*\*\*\*  
\* CERTIFICATE OF ANALYSIS \*  
\*\*\*\*\*

ACCUREX ENVIRONMENTAL CORP  
ONE TECHNOLOGY DRIVE SUITE F213  
IRVINE CA 92718

CUSTOMER ACCOUNT : T5819  
CUSTOMER ORDER NO :  
ORDER NO : 235-053976  
ORDER DETAIL SEQ : 1

REMARKS : GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS S  
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS  
(SRM's) - REFERENCE APCI SGD FIELD DIRECTIVE BOOK I PART A-3.

PRIMARY GAS MIXTURE : CARBON MONOXIDE IN NITROGEN

BATCH NO	ANALYSIS DATE	BAR CODE	CYLINDER NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
12295	12/20/93	BGN829	SG860091NB	CARBON MONOXIDE Nitrogen	250	250 BALANCE	MOLAR PPM

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED  
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE  
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

*Eileen Black Rodriguez*  
AUTHORIZED SIGNATURE



# SCOTT-MARRIN, INC.

6531 BOX SPRINGS BLVD. • RIVERSIDE, CA 92507  
TELEPHONE (714) 653-6780 • FAX (714) 653-2430

## REPORT OF ANALYSIS NIST TRACEABLE GAS MIXTURES

ACUR01  
TO: CHAD GARRETTSON  
ACUREX  
4879 E LA PALMA AVE  
SUITE 201  
ANAHEIM, CA 92807-

DATE: 02/19/93

CUSTOMER ORDER NUMBER: EV40239Z

PAGE 1

CYLINDER NUMBER	COMPONENT	CONCENTRATION (v/v)	NIST TRACEABLE REFERENCE STANDARD
CC28992	Carbon Dioxide Nitrogen	17.75 ± 0.18 % Balance	SRM 1675b
CC60241	Carbon Dioxide Nitrogen	9.89 ± 0.10 % Balance	SRM 1675b

ppm = umole/mole

% = mole-%

The above analyses are traceable to the National Institute of Standards and Technology by intercomparison with the reference standards listed above. Where indicated, volumetric and gravimetric reference standards are traceable thru use of our analytical balance, NIST Report No. MMAP 232.09/202491.

Analyst:

M.S. Calhoun

Approved:

J.T. Marrin

The only liability of this company for gas which fails to comply with this analysis shall be replacement or reanalysis thereof by the company without extra cost.

STANDARD CALIBRATION GASES IN ALUMINUM CYLINDERS

AIR PRODUCTS AND CHEMICALS, INC.  
901 WEST 12TH STREET  
LONG BEACH, CA 90813  
(310) 437-0461  
TELEPHONE (800) 350-0461

DATE: 12/27/93  
TIME: 11:16  
PAGE: 1

\*\*\*\*\*  
\* CERTIFICATE OF ANALYSIS \*  
\*\*\*\*\*

ACCUREX ENVIRONMENTAL CORP  
ONE TECHNOLOGY DRIVE SUITE F213  
IRVINE CA 92718

CUSTOMER ACCOUNT : T5819  
CUSTOMER ORDER NO : NV305225C  
235.053726  
ORDER DETAIL SEQ : 1

REMARKS : - GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS 5  
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS  
(SRM's) - REFERENCE APCI-SGD FIELD DIRECTIVE BOOK I PART A-3.

PRIMARY GAS MIXTURE : CARBON MONOXIDE IN NITROGEN

BATCH NO	ANALYSIS DATE	BAR CODE	CYLINDER NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
12303	12/21/93	BJA601	S6881575	CARBON MONOXIDE Nitrogen	90	90 BALANCE	MOLAR PPM

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED  
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE  
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

-----  
AUTHORIZED SIGNATURE

AIR PRODUCTS AND CHEMICALS, INC.  
901 WEST 12TH STREET  
LONG BEACH, CA 90813  
(310) 437-0461  
TELEPHONE (800) 350-0461

DATE: 12/27/93  
TIME: 11:16  
PAGE: 1

\*\*\*\*\*  
# CERTIFICATE OF ANALYSIS #  
\*\*\*\*\*

ACCUREX ENVIRONMENTAL CORP  
ONE TECHNOLOGY DRIVE SUITE F213  
IRVINE CA 92718

CUSTOMER ACCOUNT : T5819  
CUSTOMER ORDER NO : MV305225C  
235 053726  
ORDER DETAIL SEQ : 2

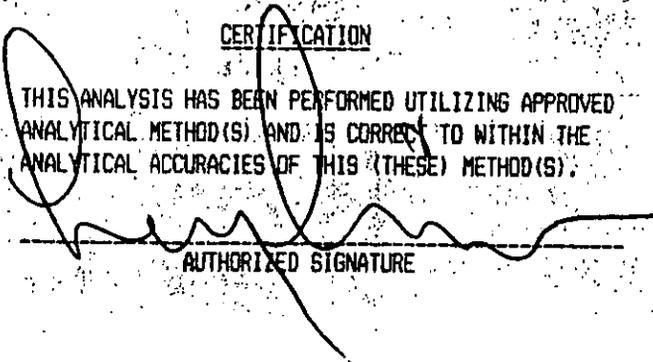
REMARKS : - GAS MIXTURE(S) LISTED BELOW ARE TRACEABLE TO NIST CLASS 5  
WEIGHTS AND/OR NIST GAS MIXTURE STANDARD REFERENCE MATERIALS  
(SRM's) - REFERENCE APCI 56D FIELD DIRECTIVE BOOK I PART A-3.

PRIMARY GAS MIXTURE : CARBON MONOXIDE IN NITROGEN

BATCH NO	ANALYSIS DATE	BAR CODE	CYLINDER NO	COMPONENT REQUESTED	CONCENTRATION REQUESTED	ANALYTICAL RESULT	UNIT OF MEASURE
12296	12/21/93	BNE008	S69103300BAL	CARBON MONOXIDE Nitrogen	50	50 BALANCE	MOLAR PPM

CERTIFICATION

THIS ANALYSIS HAS BEEN PERFORMED UTILIZING APPROVED  
ANALYTICAL METHOD(S) AND IS CORRECT TO WITHIN THE  
ANALYTICAL ACCURACIES OF THIS (THESE) METHOD(S).

  
\_\_\_\_\_  
AUTHORIZED SIGNATURE

**APPENDIX D-2**  
**FIELD TEST DATA SHEETS**



# CEM CALIBRATION SHEET

DATE 3/22/94

PLANT Etiwanda G.S.

LOCATION Unit 3

TEST NUMBER TEST # 1 - FGR on

OPERATOR D. URBY

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14		4.20	0-10%		
CO <sub>2</sub> (%)	17.75		9.89	0-20%		
CO(ppm)	451		250	0-500ppm		
IIC(ppm)						
NO <sub>x</sub> (ppm)	92.18		47.95	0-100ppm		
SO <sub>2</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Strip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	IIC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	IIC as methane	
Pre	High	0754	0754	0754		0754		92.7	44.0	<del>94.8</del> 94.8		95.6		22.0" H <sub>2</sub> O @ 0754
	Mid													22.0" @ 0754
	Low	0707	0707	0707		0707		43.2	54.0	55.3		50.0		
	Zero	0703	0703	0702		0703		2.0	5.1	5.0		1.2		
	External	0813	0809	0818		0815		43.9	53.4	55.0		49.0		System response = 45 seconds
	Zero Bias	0804	0804	0804		0804		2.2	5.3	5.0		1.2		
Post	High	1046	1046	1046		1046		91.9	94.0	94.9		94.7		
	Mid													23.4" H <sub>2</sub> O @ 1034
	Low	1042	1042	1042		1042		42.7	54.0	55.3		49.7		23.2" H <sub>2</sub> O @ 1039
	Zero	1039	1039	1039		1039		1.5	5.0	5.0		1.7		
	External	1024	1027	1032		1029		42.5	53.5	55.2		49.0		
	Zero Bias	1021	1021	1021		1021		1.9	5.4	5.0		2.0		

# CEM CALIBRATION SHEET

DATE 3/22/94  
 PLANT ETIWANDA - SCE  
 LOCATION UNIT 3  
 TEST NUMBER TEST 2 - FGR+UREA  
 OPERATOR D. URPY

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14		4.20	0-10%		
CO <sub>2</sub> (%)	17.75		9.89	0-20%		
CO(ppm)	451		250	0-500ppm		
HIC(ppm)						
NO <sub>x</sub> (ppm)	92.2		48.0	0-100ppm		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Snip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	IIC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	IIC as methane	
Pre	High	1046	1046	1046		1046		91.9	94.0	94.9		94.7		23.4 "HG" 1034
	Mid													23.2 "HG" 1034
	Low	1042	1042	1042		1042		42.7	54.0	55.3		49.7		
	Zero	1039	1039	1039		1039		1.5	5.0	5.0		1.7		
	External	1024	1027	1032		1029		42.5	53.5	55.2		49.0		
Post	High	1244	1244	1244		1244		92.5	93.7	95.0		94.2		21.7 "HG" 1224
	Mid													21.6 "HG" 1234
	Low	1239	1239	1239		1239		43.0	53.7	55.8		49.5		
	Zero	1234	1234	1234		1234		1.6	4.9	5.0		2.0		
	External	1217	1214	1226		1222		42.7	53.3	55.8		49.9		

Bas 1212 1213 1213 1213 5.0 5.1 2.0

# CEM CALIBRATION SHEET

DATE 3/22/94  
 PLANT SE - Etiwanda  
 LOCATION Unit 3  
 TEST NUMBER #3 - FOR TUREA  
 OPERATOR D. URRY

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14		4.20	0-70%		
CO <sub>2</sub> (%)	17.75		9.89	0-20%		
CO(ppm)	451		250	0-500ppm		
HC(ppm)						
NO <sub>x</sub> (ppm)	92.2		41.0	0-100ppm		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Strip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	
Pre	High	1244	1244	1244		1244		92.5	43.7	95.0		94.2		21.7' H <sub>2</sub> O @ 1224
	Mid													21.6" H <sub>2</sub> O @ 1234
	Low	1239	1239	1239		1239		43.0	53.7	55.8		44.5		
	Zero	1234	1234	1234		1234		1.6	4.9	5.0		2.0		
	External	1217	1219	1226		1222		42.7	53.3	55.8		48.9		
	Zero DRY	1212	1213	1213		1213		2.0	5.0	5.1		2.0		
Post	High	1439	1409	1439		1439		94.6	43.6	96.5		94.0		21.1' H <sub>2</sub> O @ 1430
	Mid													21.5' H <sub>2</sub> O @ 1436
	Low	1434	1434	1424		1434		43.0	53.7	55.8		49.4		
	Zero	1430	1430	1430		1430		1.1	4.9	5.0		2.0		
	External	1418	1421	1427		1424		42.7	53.0	55.3		48.7		
		1412	1412	1412		1412		1.7	5.1	5.0		2.0		

# CEM CALIBRATION SHEET

DATE 3/22/94  
 PLANT SCE Etiwanda  
 LOCATION Unit 3  
 TEST NUMBER #4 - Baseline  
 OPERATOR D. Urey

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	91.4		4.20	0-10%		
CO <sub>2</sub> (%)	17.75		9.89	0-20%		
CO(ppm)	451		250	0-500ppm		
HIC(ppm)						
NO <sub>x</sub> (ppm)	92.2		48.0	0-100ppm		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Strip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HIC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HIC as methane	
Pre	High	1434	1434	1434	5	1434		92.6	93.6	96.5		94.0		Leak Check
	Mid													
	Low	1434	1434	1434		1434		43.0	53.7	55.8		49.4		21.8" H <sub>2</sub> O @ 1430
	Zero	1430	1430	1430		1430		1.1	4.9	5.0		2.0		21.5" H <sub>2</sub> O @ 1435
	External	1418	1421	1427		1424		42.7	53.0	55.3		48.7		
	2m DWS	1412	1412	1412		1412		1.7	5.1	5.0		2.0		
Post	High	1639	1639	1639		1639		92.8	93.7	96.5		93.8		
	Mid													23.5" H <sub>2</sub> O @ 1628
	Low	1636	1636	1636		1636		43.0	53.8	55.5		49.3		23.4" H <sub>2</sub> O @ 1633
	Zero	1634	1634	1634		1634		1.3	5.0	6.0		2.0		
	External	1617	1620	1626		1623		42.9	53.1	55.5		48.8		
		1613	1617	1613		1613		7	5.1	5.0		2.0		

TEST VAN D... SHEET

DATE 3/22/94 PLANT Ethwards - SCE OPERATOR D. UREY

LOCATION Unit 3 OPERATING LOAD 320 MW

Time Start/Stop	NI, Slip	Strip Chart measurements						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	CO @3%O <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	NO <sub>x</sub> @3%O <sub>2</sub> (ppm)	
0915/1015		3.1	9.9	220	221	52.0	52.3	TEST 1 - FGR + <del>UREA</del> DU.
1100/1200		3.1	9.9	220	221	44.0	44.2	TEST 2 - FGR + UREA
1301/1401		3.1	9.9	205	206	44.5	44.8	TEST 3 - FGR + UREA
1500								
1530/1600		3.0	9.9	195	195	60.0	60.0	TEST 4 - Baseline

BP. = 29.91

# CEM CALIBRATION SHEET

DATE 3/23/94  
 PLANT SCE Etiwanda  
 LOCATION Unit 3  
 TEST NUMBER #5 - Mid Load Stratification  
 OPERATOR C.84

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	91.4		4.20	0-10%		
CO <sub>2</sub> (%)	17.75		9.89	0-20%		
CO(ppm)	451		250	0-500 ppm		
HC(ppm)						
NO <sub>x</sub> (ppm)	92.2		48.0	0-100 ppm		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements							Snip Chart Measurements (divisions)							COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane			
Pre	High	0705	0705	0705		0711		93.2	94.0	95.0		95.6		21.0 @ 0649		
	Mid	0700	0700	0700		0708		43.6	53.3	55.0		49.8		20.6 @ 0654		
	Low															
	Zero	0655	0655	0655		0706	0706	2.0	5.0	5.0		1.0				
	External	0738	0720	0723		0725		43.5	53.0	55.0		49.0				
	Zero bias	0718	0718	0718		0718		2.6	5.2	5.0		1.0				
Post	High	1011	1011	1011		1011		93.0	95.2	95.7		94.5		24.0 @ 1003		
	Mid	1015	1015	1015		1015		43.5	54.7	55.4		49.3		23.5 @ 1008		
	Low															
	Zero	1006	1006	1006		1006		1.5	5.7	5.0		1.2				
	External	1002	0953	0956		0958		43.8	54.0	55.0		48.6				
		0951	0951	0951		0951		2.2	5.8	5.0		1.5				

# CEM CALIBRATION SHEET

DATE 3/23/94  
 PLANT SCE Etowanda  
 LOCATION Unit # 3  
 TEST NUMBER # 6 Mid-Load Baseline  
 OPERATOR Ced

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14	4.20		0-10%		
CO <sub>2</sub> (%)	17.75	9.89		0-20%		
CO(ppm)	451	250		0-500		
HC(ppm)						
NO <sub>x</sub> (ppm)	92.2	48.0		0-100		
SO <sub>2</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Strip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	
Pre	High	1011	1011	1011		1011		93.0	95.2	95.7		94.5		24.0 @ 1003
	Mid	1015	1015	1015		1015		43.5	54.7	55.4		49.3		23.5 @ 1008
	Low													
	Zero	1006	1006	1006		1006		1.5	5.7	5.0		1.2		
	External	1002	0953	0956		0958		43.1	54.0	55.0		48.6		
	Zero bias	0951	0951	0951		0951		2.2	5.0	5.0		1.5		
Post	High	1159	1158	1158		1158		93.1	95.7	96.2		93.9		
	Mid	1155	1158	1155		1155		49.3	54.8	55.5		49.0		
	Low													
	Zero	1151	1151	1151		1151		1.3	5.6	5.0		1.5		23.7 @ 1149
	External	1147	1140	1142		1144		43.0	54.0	55.2		48.3		23.4 @ 1154
	Zero bias	1139	1138	1136		1138		1.9	5.9	5.0		1.7		

# CEM CALIBRATION SHEET

314 682  
8670

DATE 3/23/94  
 PLANT SEE Ethwanda  
 LOCATION Unit # 3  
 TEST NUMBER #7 D.U.  
 OPERATOR CA

TEST NUMBER #1 Mid-load FGRON

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14	4.20		0-10%		
CO <sub>2</sub> (%)	17.75	9.89		0-20%		
CO(ppm)	451	250		0-500		
HC(ppm)						
NO <sub>x</sub> (ppm)	92.2	48.0		0-100		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements							Simp Chart Measurements (divisions)					COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	
Pre	High	1158	1158	1158		1158		93.1	95.7	96.2		93.9		23.7 @ 1149
	Mid	1155	1155	1155		1155		43.3	54.8	55.5		49.0		23.4 @ 1154
	Low													
	Zero	1151	1151	1151		1151		1.3	5.6	5.0		1.5		
	External	1147	1140	1142		1146		43.0	54.0	55.2		48.3		
	zero bias	1138	1138	1138		1138		1.9	5.7	5.0		1.7		
Post	High	1402	1402	1402		1402		93.3	95.8	96.2		93.0		
	Mid	1358	1358	1358		1358		43.4	55.0	55.7		48.7		
	Low													
	Zero	1354	1354	1354		1354		1.5	5.7	5.0		1.9		23.1 H <sub>2</sub> O @ 1349
	External	1351	1340	1343		1347		43.0	54.5	55.5		48.0		22.6 H <sub>2</sub> O @ 1355
		1337	1337	1337		1337		1.9	5.9	5.0		2.0		

# CEM CALIBRATION SHEET

DATE 3/23/94

PLANT SCE Etowanda

LOCATION Unit #3

TEST NUMBER #8 Mid Load, Fert & UREA ON

OPERATOR CA

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14	4.20		0-10%		
CO <sub>2</sub> (%)	17.75	9.89		0-20%		
CO(ppm)	451	250		0-500		
HC(ppm)						
NO <sub>x</sub> (ppm)	92.2	48.0		0-100		
SO <sub>2</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Strip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO(ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO(ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	
Pre	High	1402	1402	1402		1402		93.3	95.8	96.2		93.0		23.1" @ 1349
	Mid	1358	1358	1358		1358		43.4	55.0	55.7		48.7		22.6" @ 1355
	Low													
	Zero	1354	1354	1354		1354		1.5	5.9	5.0		1.9		
	Mid External	1351	1340	1343		1347		43.0	54.5	55.5		48.0		
	Zero bias	1337	1337	1337		1337		1.9	5.9	5.0		2.0		
Post	High	1543	1543	1543		1543		93.3	96.2	96.5		92.9		23.5" @ 1533
	Mid	1538	1538	1538		1538		43.2	55.2	55.9		48.7		23.0" @ 1534
	Low													
	Zero	1536	1536	1536		1536		1.2	5.9	5.0		2.0		
	Mid External	1532	1525	1527		1529		43.0	54.7	54.3		47.6		
	zero bias	1523	1523	1523		1523		1.8	6.2	5.0		2.0		

TEST VAN DATA SHEET

DATE 3/23/94 PLANT SCE Etowanda OPERATOR CH

LOCATION UNIT NO. 3 OPERATING LOAD Mid-Lead Stratification (Test 5)

Time Start/Stop	NH <sub>3</sub> Slip	Strip Chart measurements					NO <sub>x</sub> @3%O <sub>2</sub> (ppm)	NO <sub>x</sub> @3%O <sub>2</sub> (ppm)	COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	CO @3%O <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)			
0742/0746						43.4		Part A - Reference (center)	
0746/0748						43.4		A-1	
0750/0752						43.5		A-2	
0755/0757						43.5		A-3	
0800/0802						43.1		A-4	
0805/0807						43.4		Part A - Reference (center)	
0814/0816						43.5		Part D - Reference (center)	
0819/0821						43.3		D-1	
0823/0825						43.5		D-2	
0828/0830						43.1		D-3	
0833/0835						43.0		D-4	
0837/0839						43.0		Part D - Reference (center)	
0847/0850						43.4		Part C - Reference (center)	
0852/0854						43.2		C-1	
0857/0859						43.6		C-2	
0901/0903						43.0		C-3	
0906/0908						43.0		C-4	
0911/0913						43.4		Part C - Reference (center)	





# CEM CALIBRATION SHEET

DATE 3/23/94  
 PLANT SCE Etiwanda  
 LOCATION Unit #3  
 TEST NUMBER Low Load, Stratification  
 OPERATOR CEJ

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14	4.20		0-10%		
CO <sub>2</sub> (%)	17.75	9.89		0-20%		
CO(ppm)	451	250		0-500		
HC(ppm)						
NO <sub>x</sub> (ppm)	92.2	48.0		0-100		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Strip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO(ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO(ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	
Pre	High	1954	1956	1954		1958		93.2	93.8	95.0		94.2		23.5" @ 1533
	Mid	1950	1954	1950		1956		43.5	53.5	55.0		49.3		23.0" @ 1539
	Low													
	Zero	1946	1953	1946		1954		2.0	5.0	5.0		1.9		
	External	2028	2022	2025		2020		43.5	53.1	54.8		49.0		
	zero bias	2016	2016	2016		2016		2.3	5.0	5.0		1.7		
Post	High	2250				2250		92.7				95.0		24.7" @ 2243
	Mid	2247				2247		43.0				49.3		24.5" @ 2248
	Low													
	mid bias zero	2241				2239		43.0				49.0		
	zero bias external	2235				2235		2.3				1.5		

zero 2244m low 2244  
 zero 2244m low 2244  
 1.6  
 1.3

# CEM CALIBRATION SHEET

DATE 3/23/94  
 PLANT Edison EGS  
 LOCATION Unit #3  
 TEST NUMBER Test 10 Low Lead, Baseline  
 OPERATOR Colt

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14	4.20		0-10%		
CO <sub>2</sub> (%)	17.75	9.89		0-20%		
CO(ppm)	90	50		0-100		
HC(ppm)						
NO <sub>x</sub> (ppm)	21.0	12.3		0-25		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Simp Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	
Pre	High	2308	2308	2308		2308		93.4	95.0	95.0		86.8		24.7" @ 2243
	Mid	2304	2304	2304		2304		43.3	54.1	54.0		51.6		24.5" @ 2248
	Low													
	Zero	2300	2300	2300		2300		1.4	5.2	5.0		1.8		
	External	2323	2314	2318		2320		43.2	53.7	53.9		86.2		
	Zero bias	2312	2312	2312		2312		2.0	5.4	5.0		1.9		
Post	High	0054	0054	0054		0054		93.4	94.8	90.0		86.5		24.1" @ 0044
	Mid	0050	0050	0050		0050		43.2	54.2	54.0		50.8		23.9" @ 0049
	Low													
	Zero	0046	0046	0046		0046		1.3	5.3	5.0		1.3		
	External	0042	0033	0036		0039		43.1	53.8	53.8		85.8		

Zero bias 0031 0031 0031 0031 9 5.5 5.1 2.0

# CEM CALIBRATION SHEET

DATE 3/23/94  
 PLANT SCE  
 LOCATION UNIT # 3  
 TEST NUMBER #11 Low Load FGR ON  
 OPERATOR Cdf

Constituent	Actual Gas Concentration			Instrument Range	Percent-of-Range	
	High	Mid	Low		High	Low
O <sub>2</sub> (%)	9.14	4.20		0-10%		
CO <sub>2</sub> (%)	17.75	9.89		0-20%		
CO(ppm)	90	50		0-100		
HC(ppm)						
NO <sub>x</sub> (ppm)	21.0	12.3		0-25		
SO <sub>x</sub> (ppm)						

Time	Concentration	Data Logger Measurements						Strip Chart Measurements (divisions)						COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	SO <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)	HC as methane	
Pre	High	0054	0054	0054		0054		93.4	94.8	90.0		86.5		24.1" @ 0044
	Mid	0050	0050	0050		0050		43.2	54.2	54.0		50.8		23.9" @ 0049
	Low													
	Zero	0046	0046	0046		0046		1.3	5.3	5.0		1.3		
	External	0042	0033	0036		0039		43.1	53.8	53.8		85.8		
	zero bias	0031	0031	0031		0031		1.9	5.5	5.1		2.0		
Post	High	0242	0242	0242		0242		93.4	94.6	94.7		86.4		23.8" @
	Mid	0246	0246	0246		0246		43.4	54.1	53.8		50.5		23.5" @
	Low													
	Zero	0238	0238	0238		0238		1.3	5.3	5.1		0.5		
	External	0235	0225	0228		0231		43.3	53.9	53.5		85.8		
								1.8	5.7	5.1				1.1

zero bias 0222 0220 0222 0220 0222

TEST VAN DATA SHEET

DATE 3/23/94 PLANT EGS #3 OPERATOR BA

LOCATION Unit #3 OPERATING LOAD low load Stratification Test # 9

1/11/11

Time Start/Stop	NH <sub>3</sub> Slip	Strip Chart measurements					divisions raw	COMMENTS
		O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	CO @3%O <sub>2</sub> (ppm)	NO <sub>x</sub> (ppm)		
2031/2033							22.0	Port B - Reference (Center)
2035/2037							22.2	B-1
2039/2041							22.2	B-2
2043/2045							22.3	B-3
2047/2049							21.9	B-4
2052/2054							22.4	Port B - Reference (Center)
2058/2101							22.5	Port A - Reference (Center)
2103/2105							22.5	A-1
2108/2110							22.5	A-2
2112/2114							22.6	A-3
2116/2118							22.7	A-4
2120/2122							22.9	Port A - Reference (Center)
2127/2130							22.7	Port D - Reference (Center)
2132/2134							22.8	D-1
2136/2138							23.3	D-2
2140/2143							22.4	D-3
2146/2149							23.2	D-4
2151/2153							23.5	Port D - Reference (Center)

Stack pressure negative believe minor dilution occurred →  
 ↓  
 conc. up.  
 O<sub>2</sub> @ 150

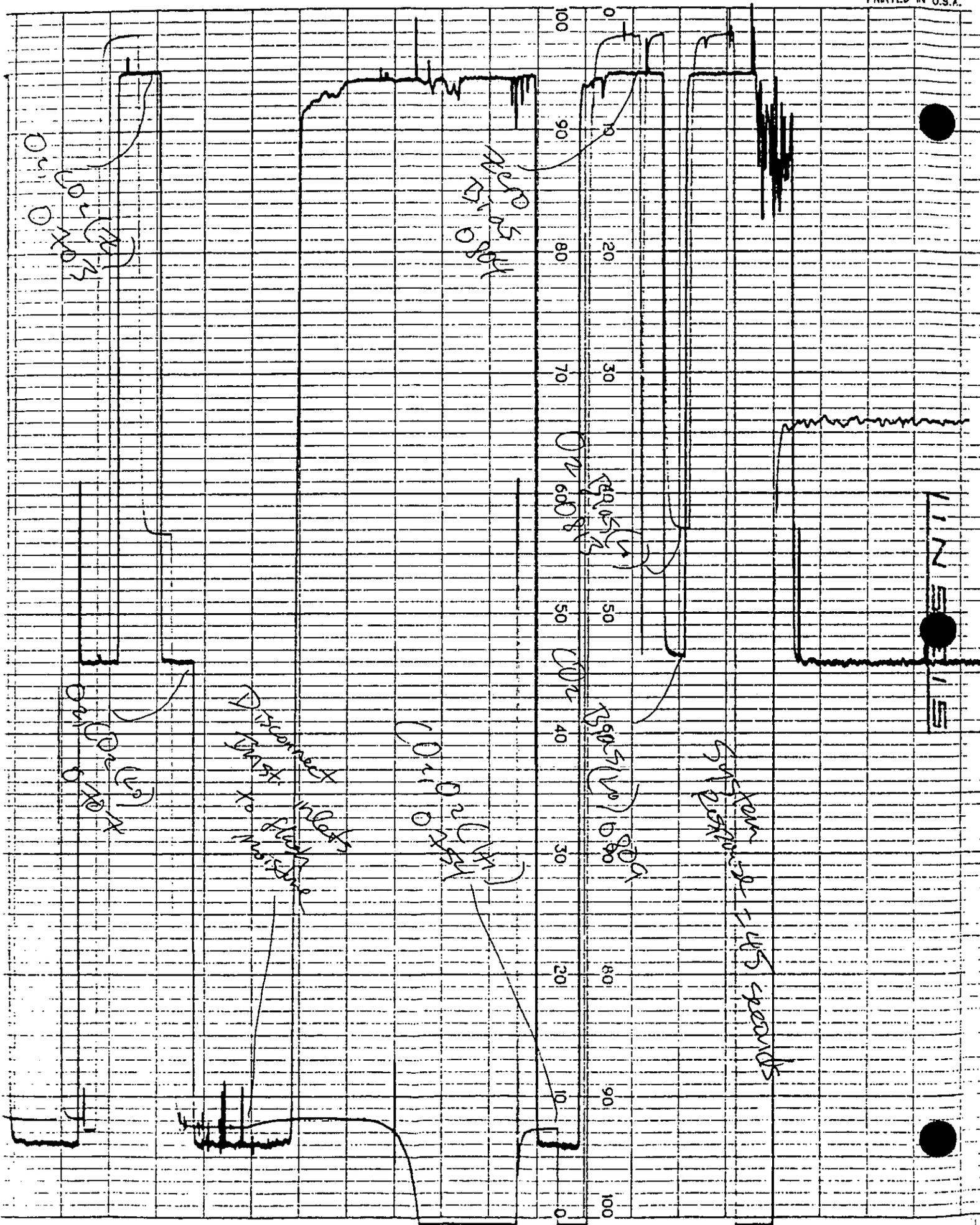


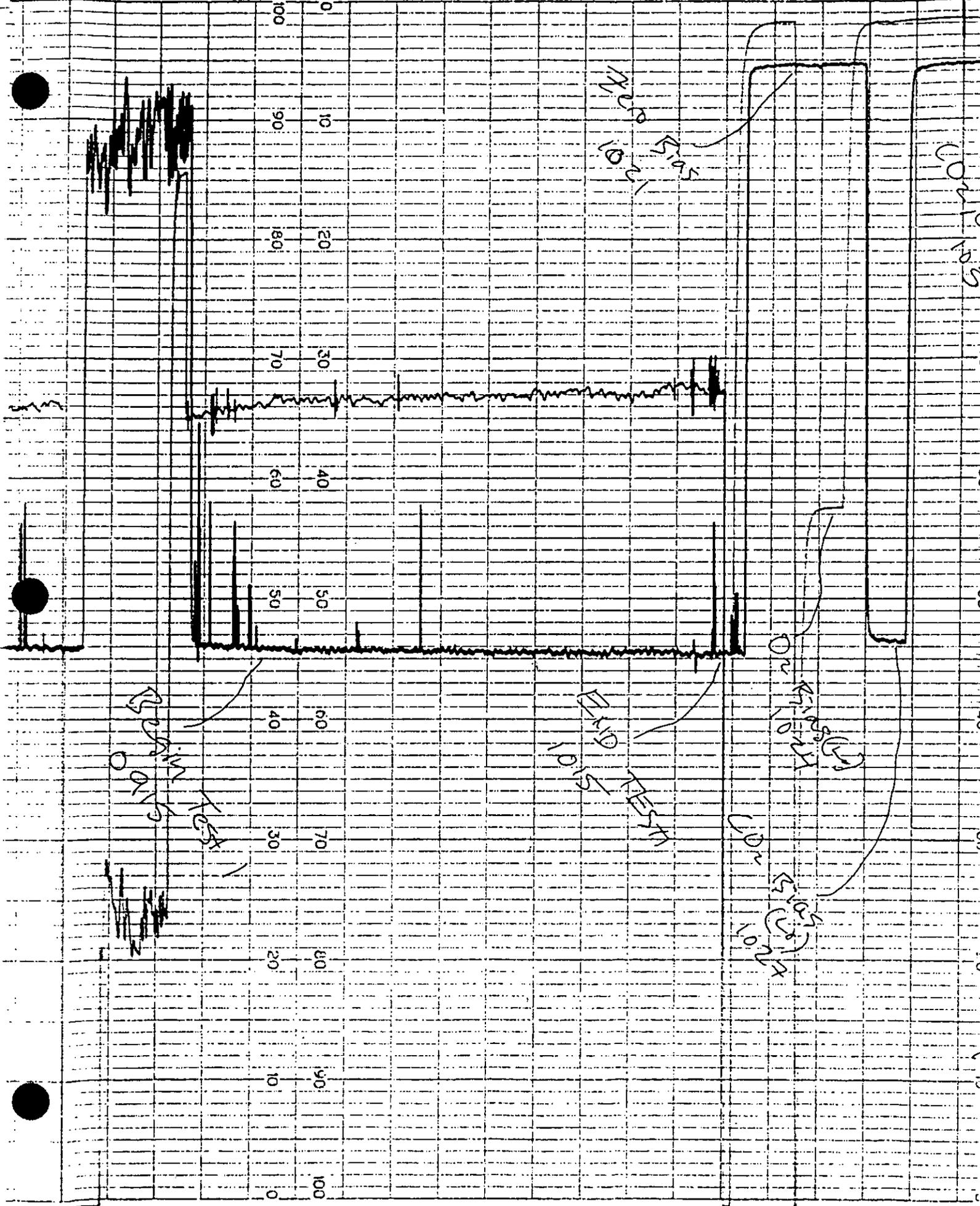


**APPENDIX D-3**  
**STRIP CHART RECORDS**









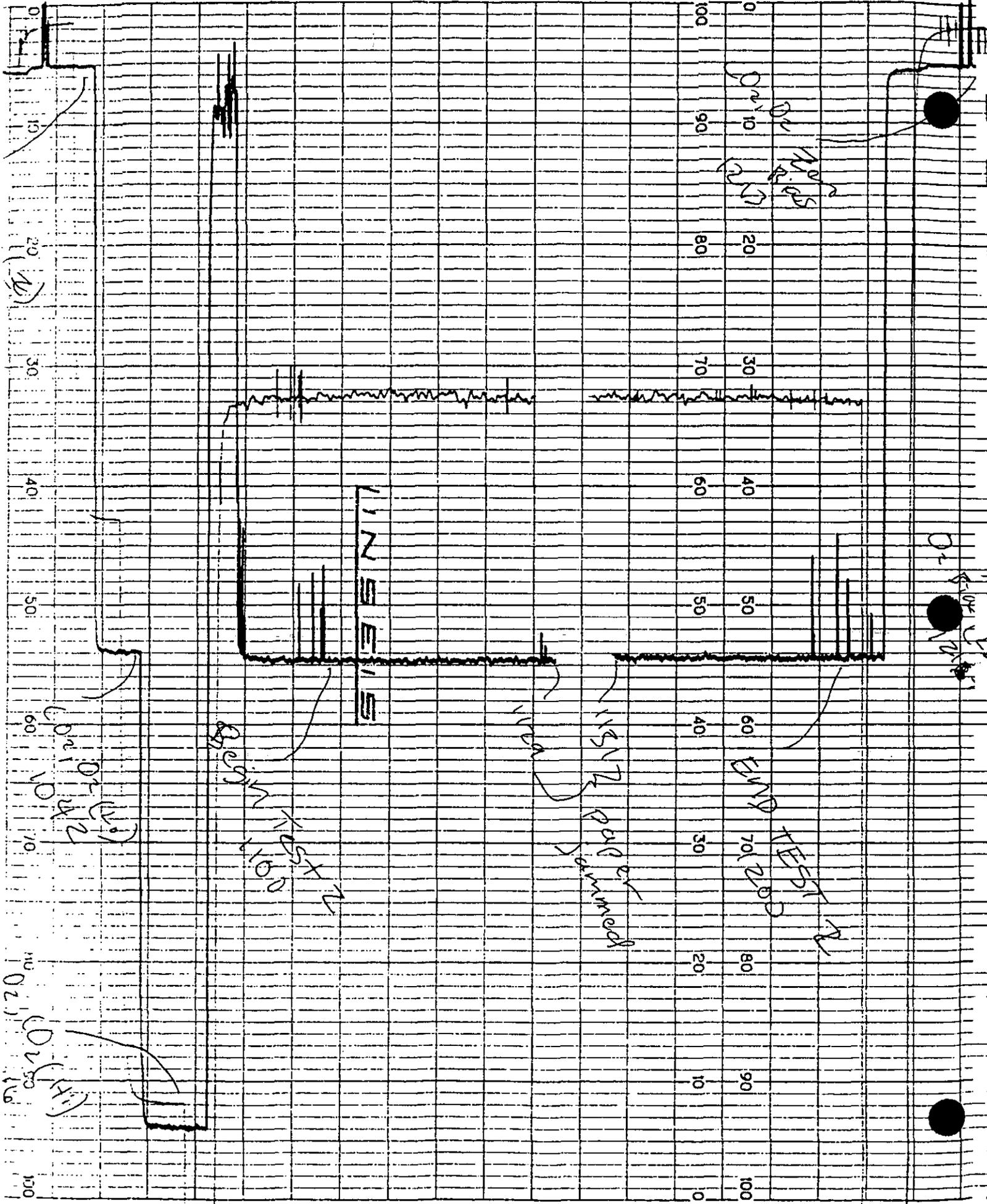
NIP 10/15

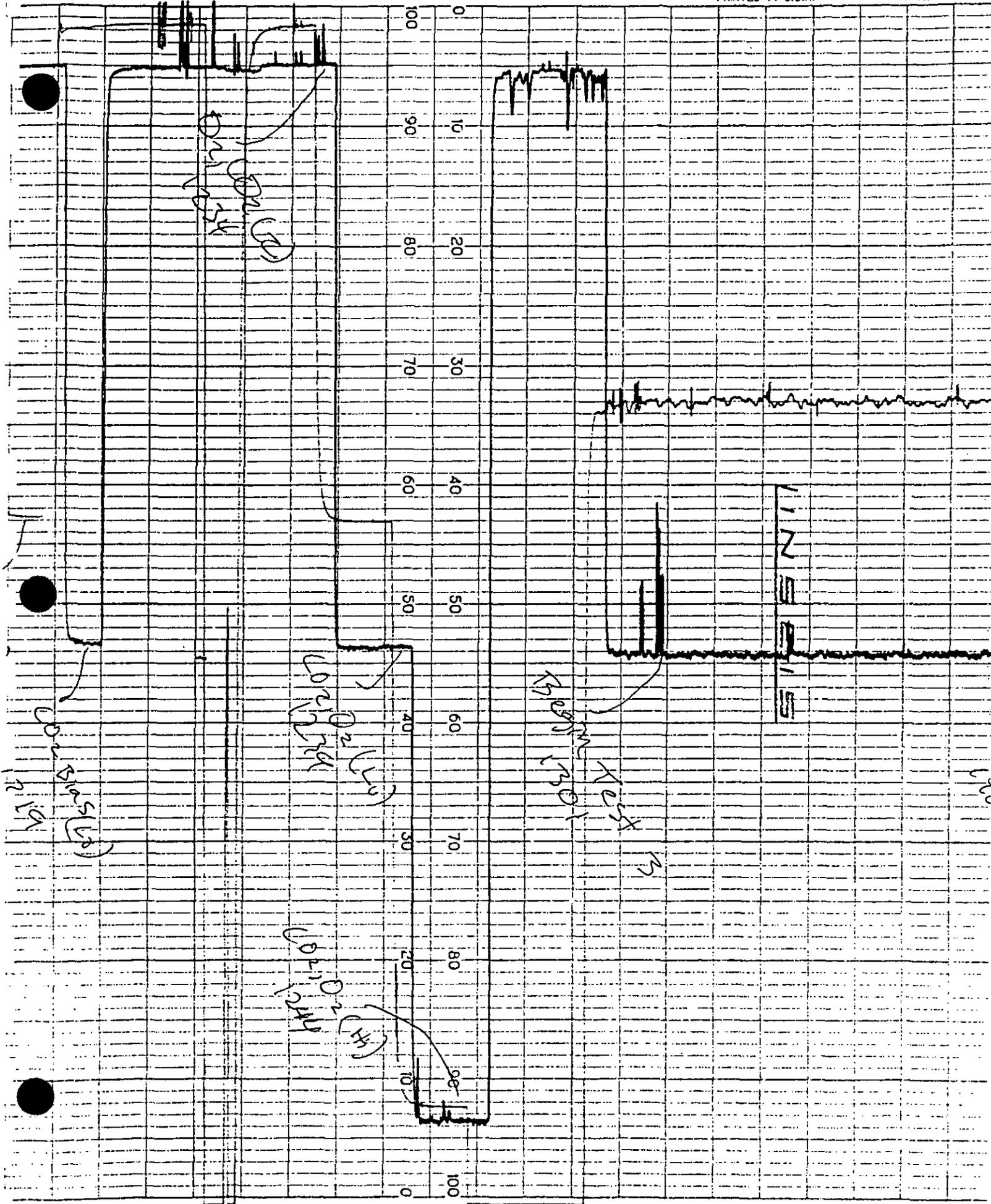
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DOWN 10/15

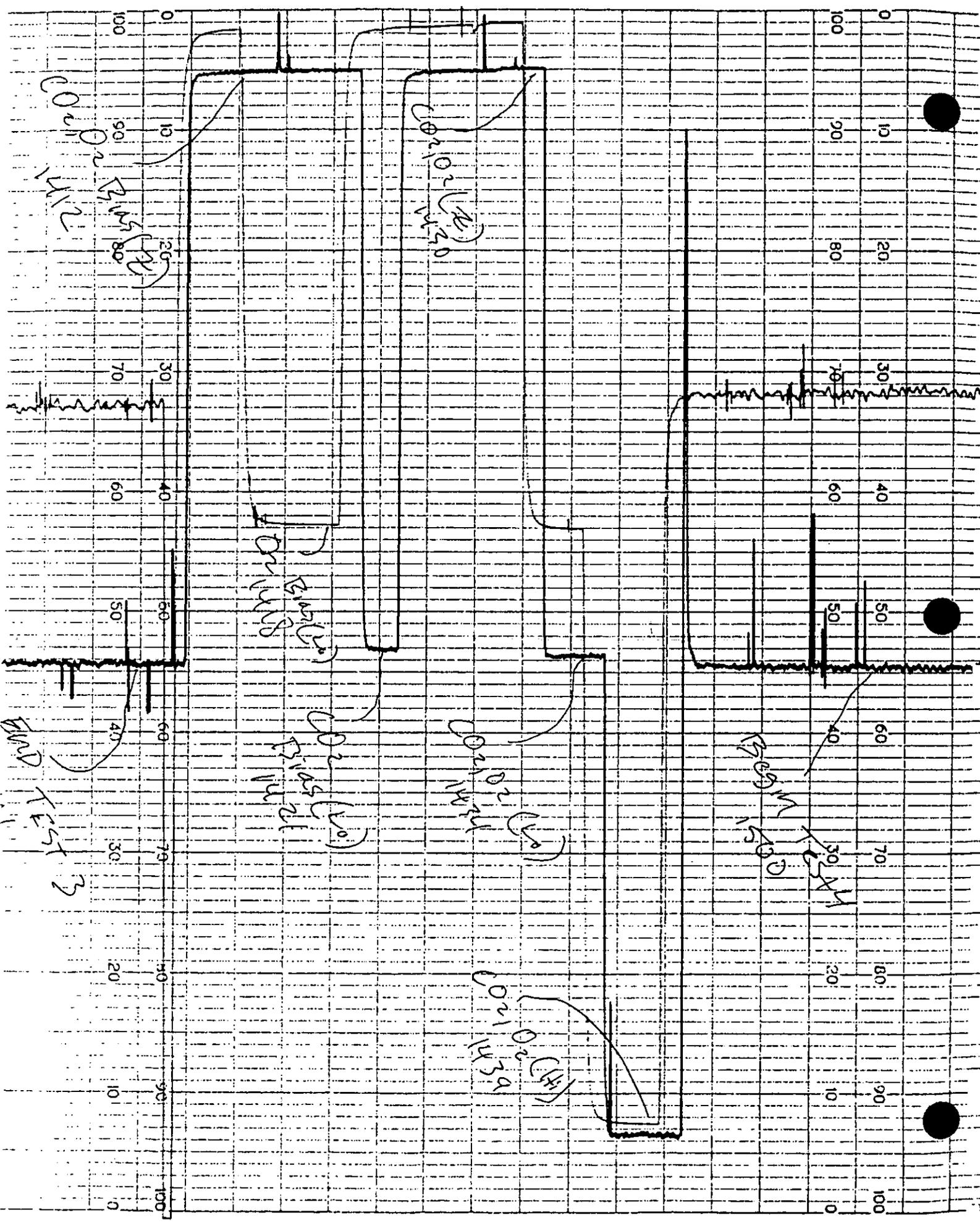
EX 10/15

DOWN 10/15

DOWN 10/15

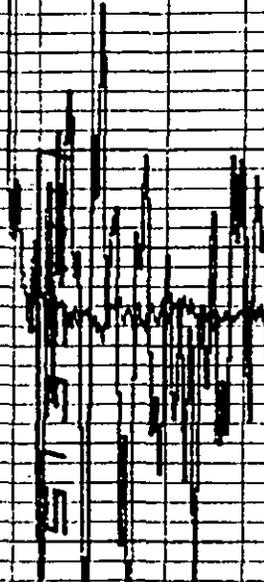
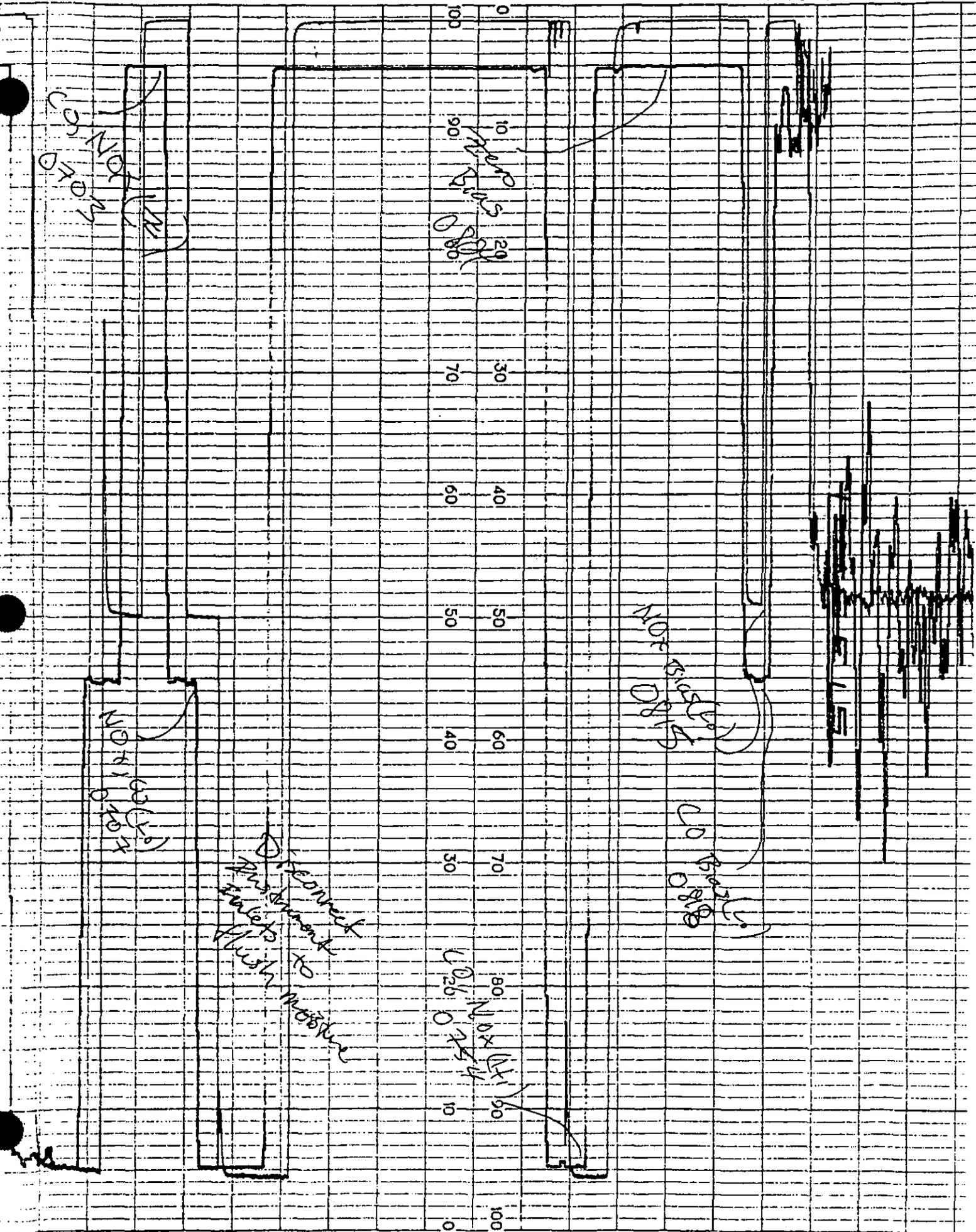








2/22/94  
 SCE EDWARDS  
 Unit 883  
 270 MW  
 O. Pratt  
 -D-880  
 NOx - 100 PPM  
 HI - 92.18  
 Cyl # AAL 5362  
 Exp 10/95  
 LO - 88.95  
 Cyl # AAL 4063  
 Exp 10/95  
 CO - BLUE  
 O - 500 PPM  
 HI - 157.0  
 Cyl # 55C 8077  
 Exp 10/96  
 Cyl # C2786  
 Exp 10/96  
 C.S.  
 3000  
 6000  
 12000  
 24000  
 48000  
 96000  
 192000  
 384000  
 768000  
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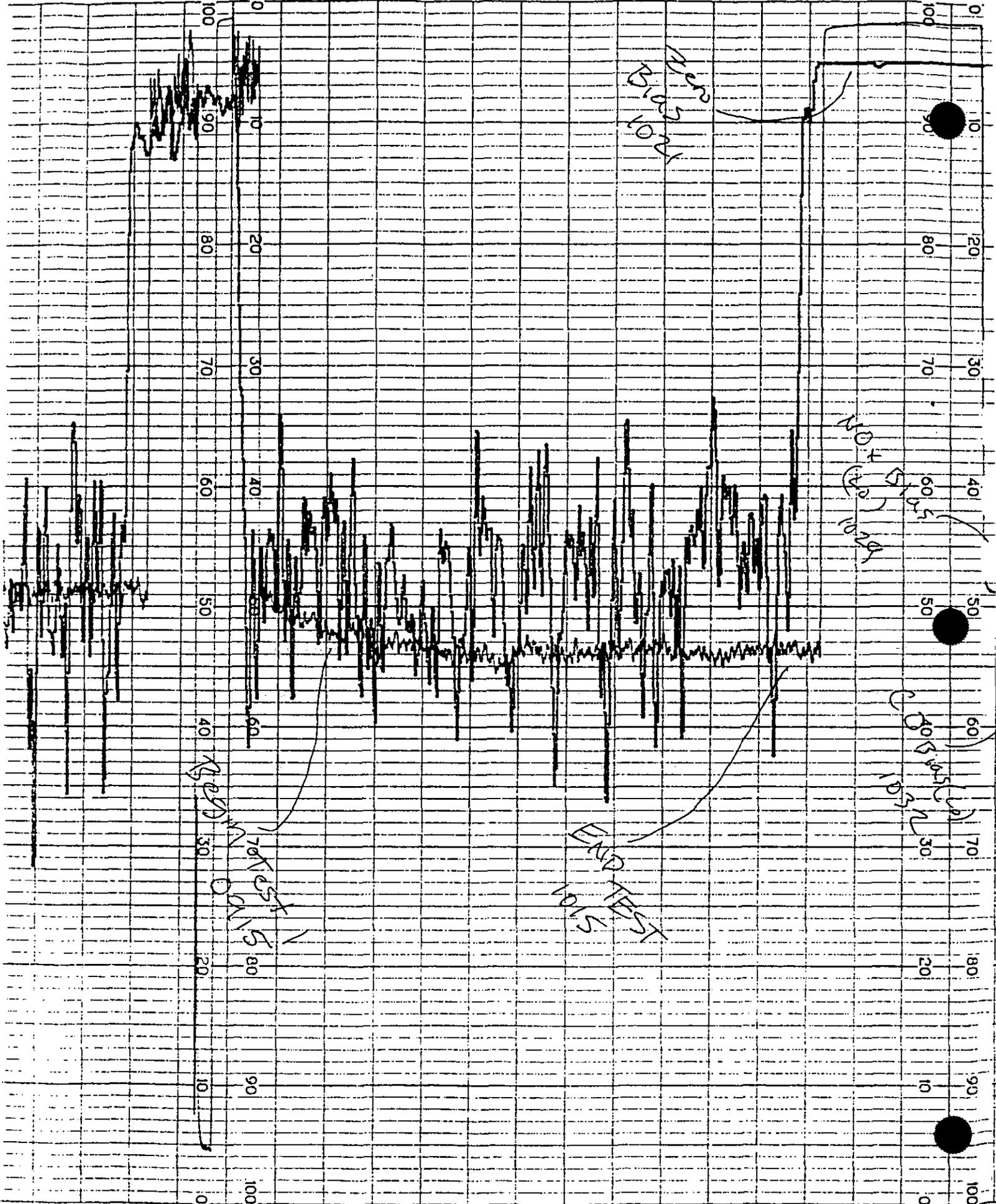
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D. 1515  
D. 1515

NO. 1515  
D. 1515

NO. 1515  
D. 1515

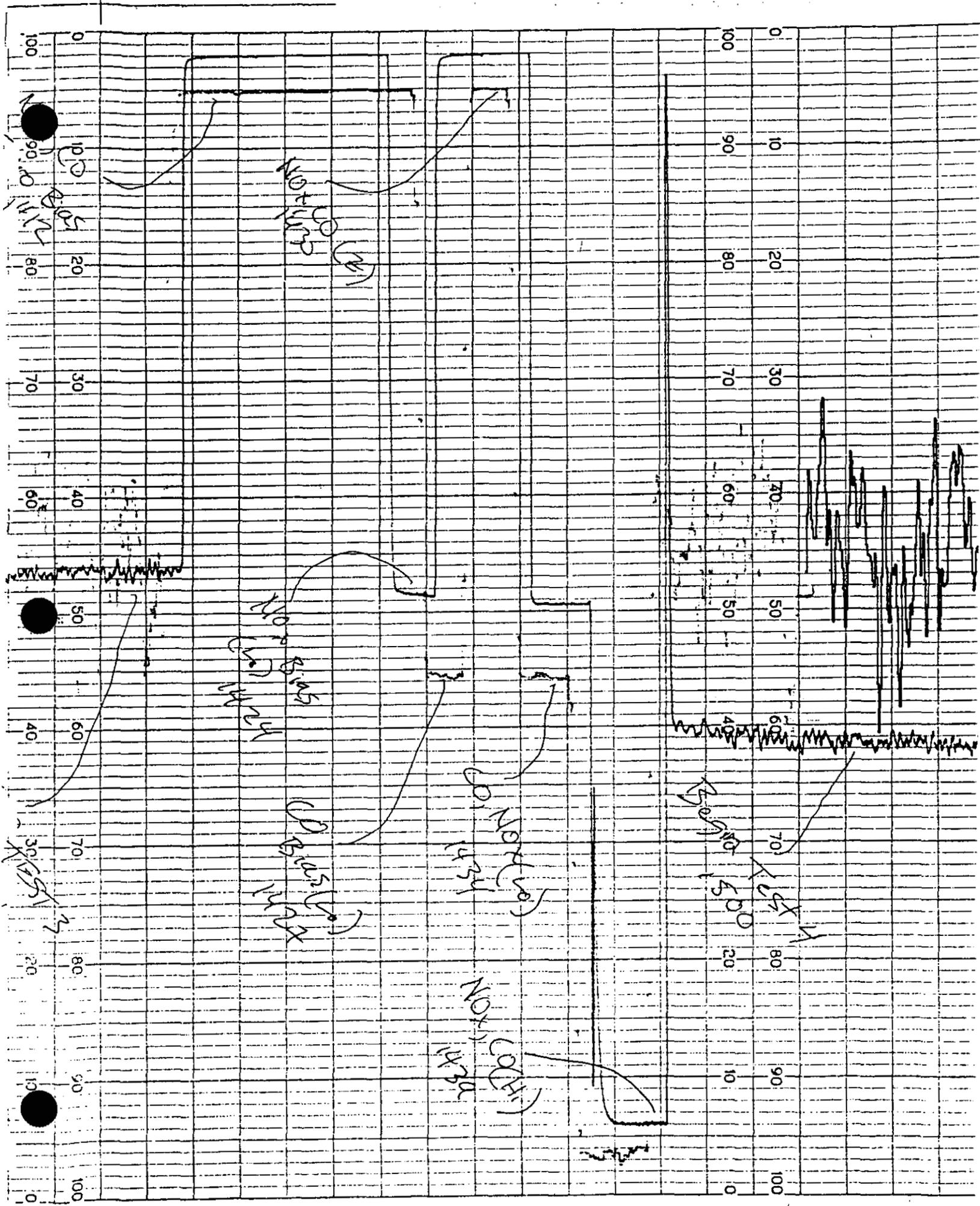
NO. 1515  
D. 1515

NO. 1515  
D. 1515









NO. 1 COAL

NO. 2 COAL

NO. 3 COAL

NO. 4 COAL

NO. 5 COAL

NO. 6 COAL

NO. 7 COAL

NO. 8 COAL

NO. 9 COAL

NO. 10 COAL

NO. 11 COAL

DEPTH

DISTANCE

0 10 20 30 40 50 60 70 80 90 100

0 10 20 30 40 50 60 70 80 90 100

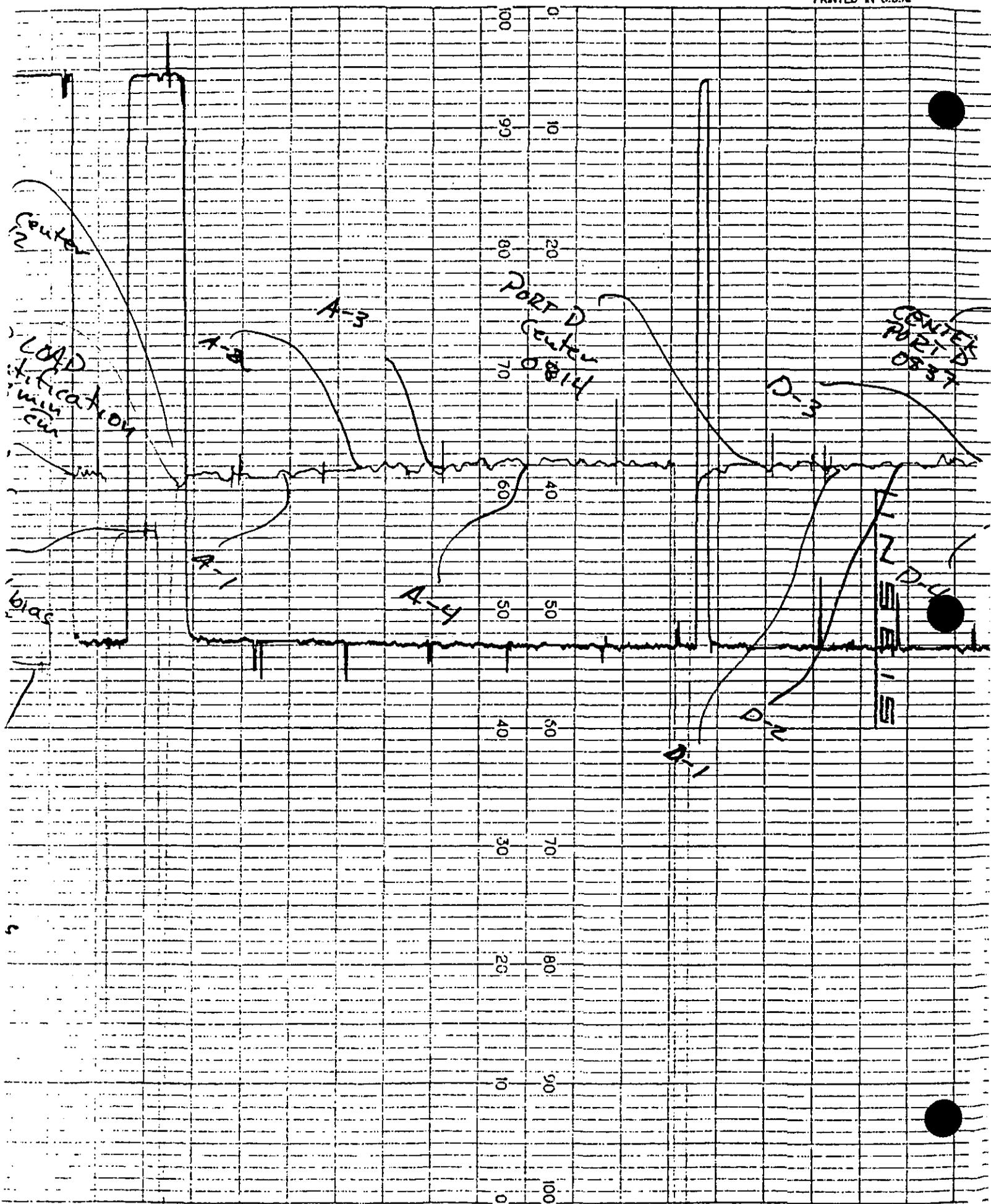
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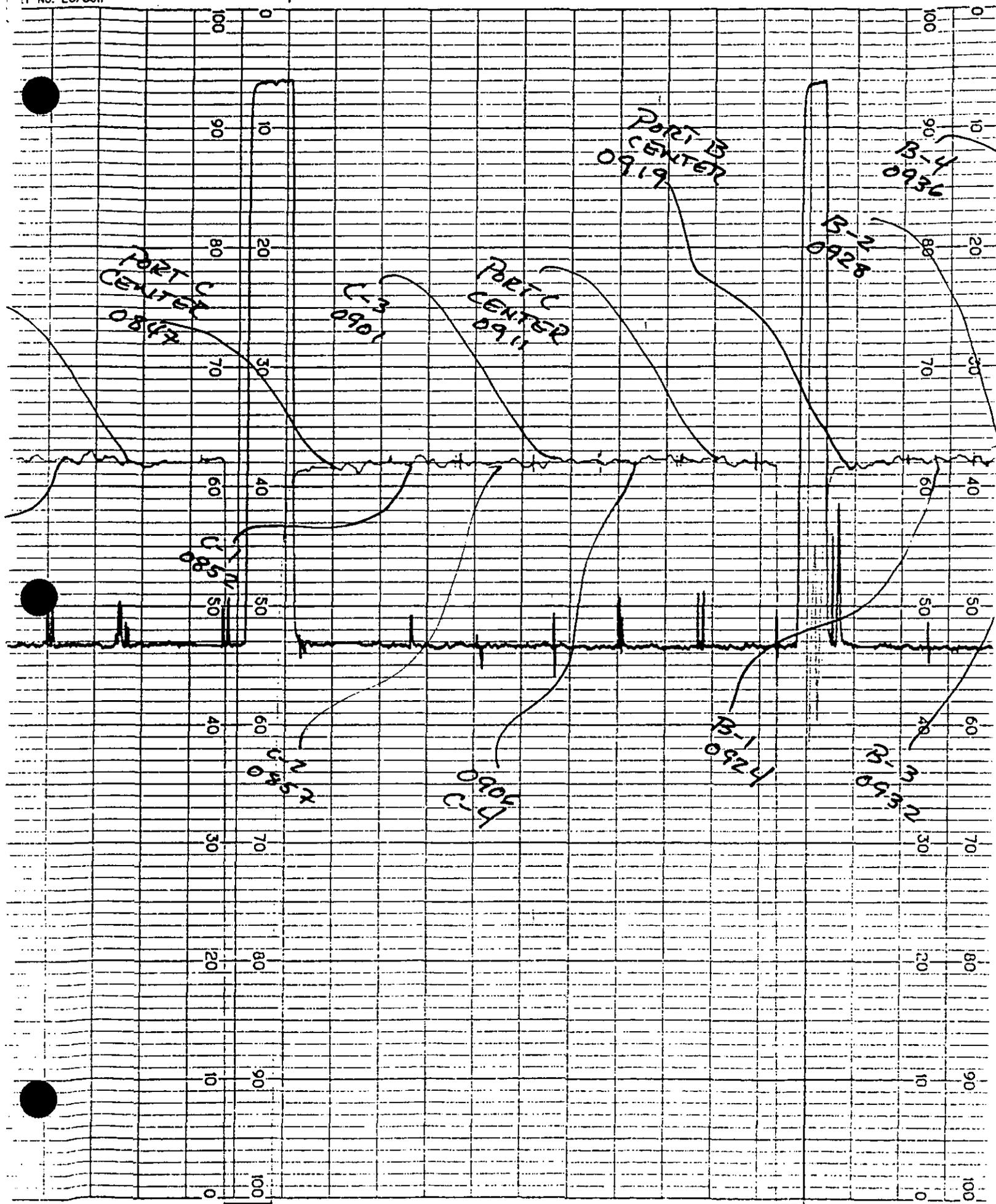
0 10 20 30 40 50 60 70 80 90 100

0 10 20 30 40 50 60 70 80 90 100









PORT CENTER  
0919

B-4  
0934

PORT CENTER  
0847

B-3  
0901

PORT CENTER  
0911

B-1  
0928

N-4  
0847

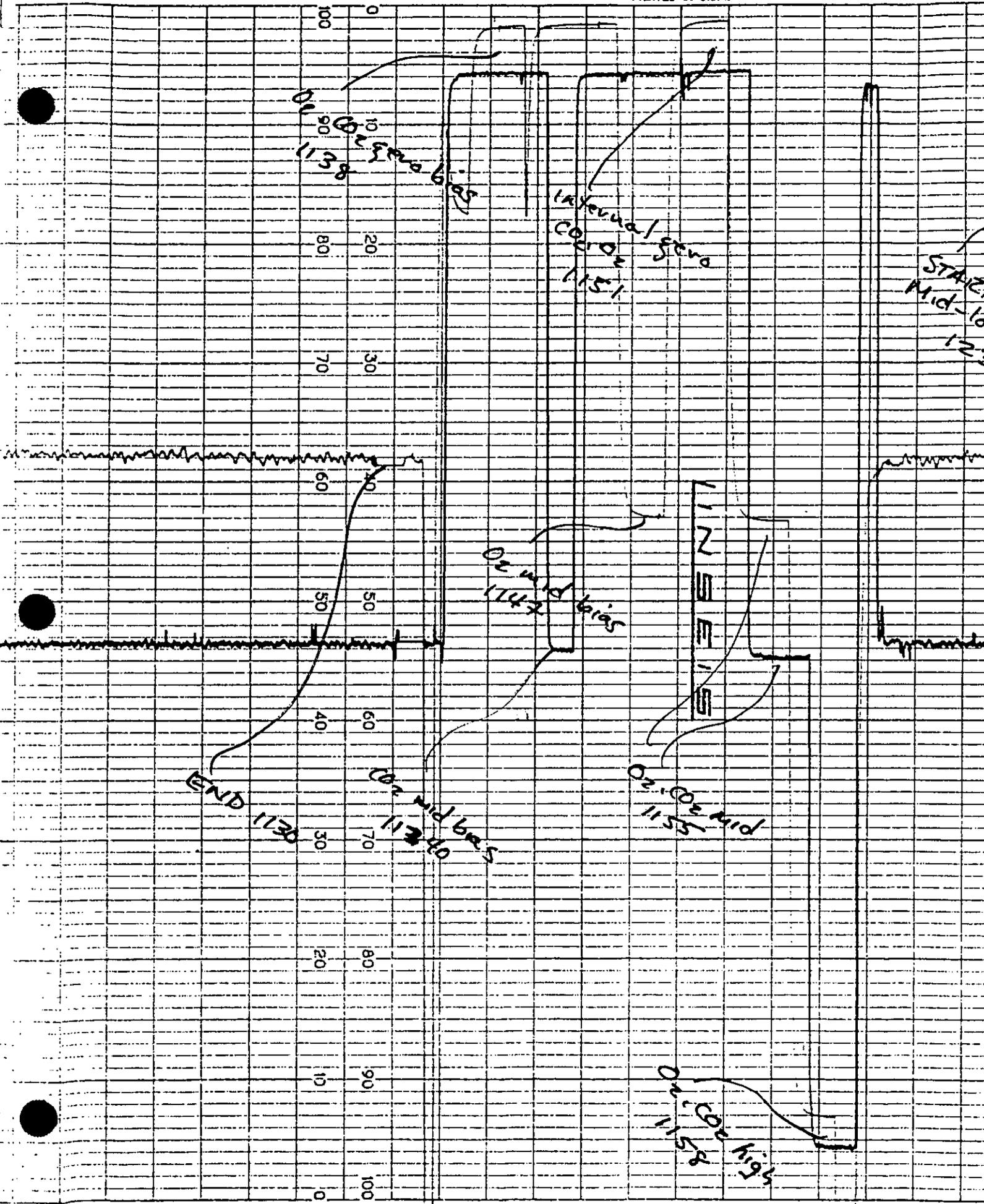
N-5  
0905

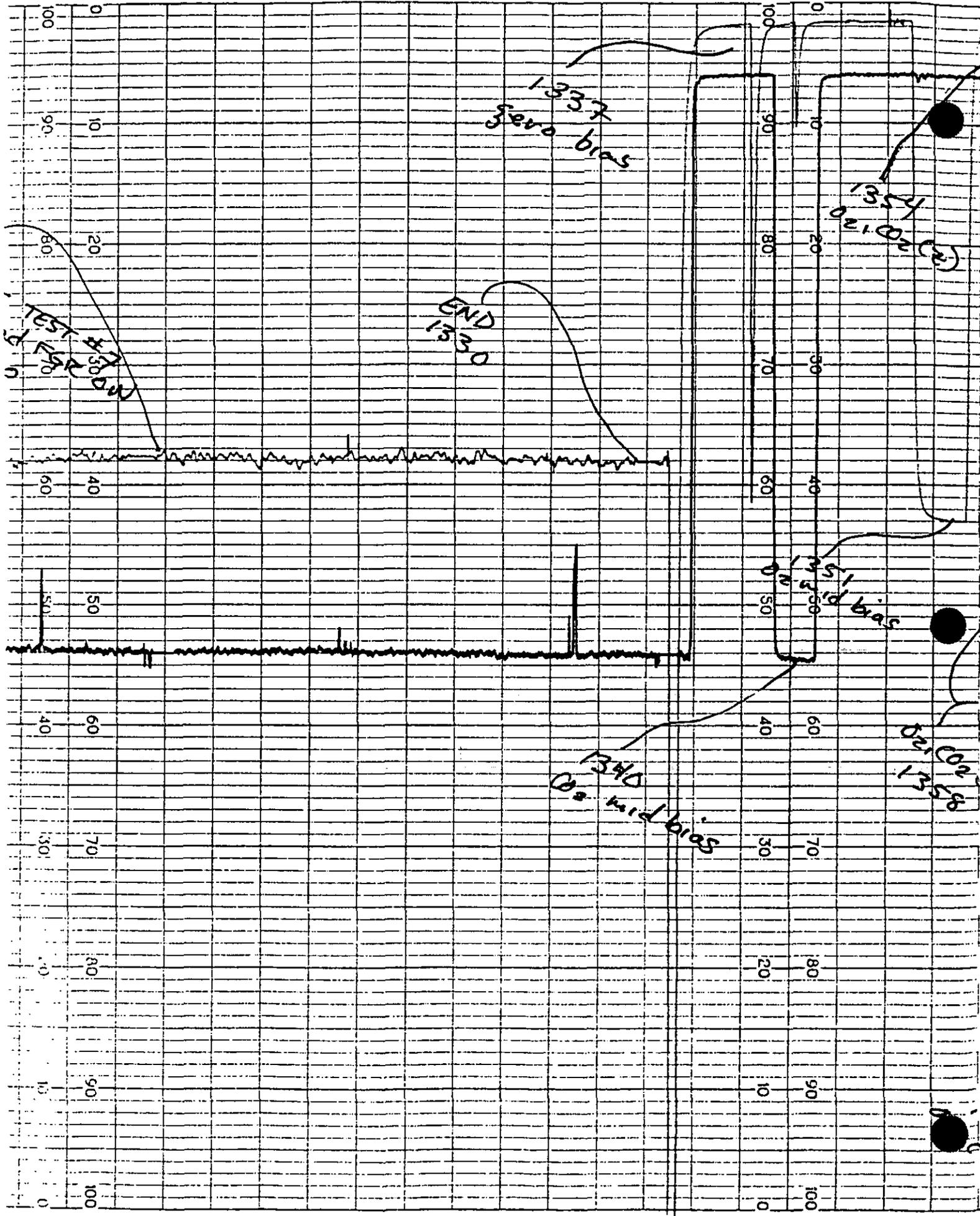
B-C  
0907

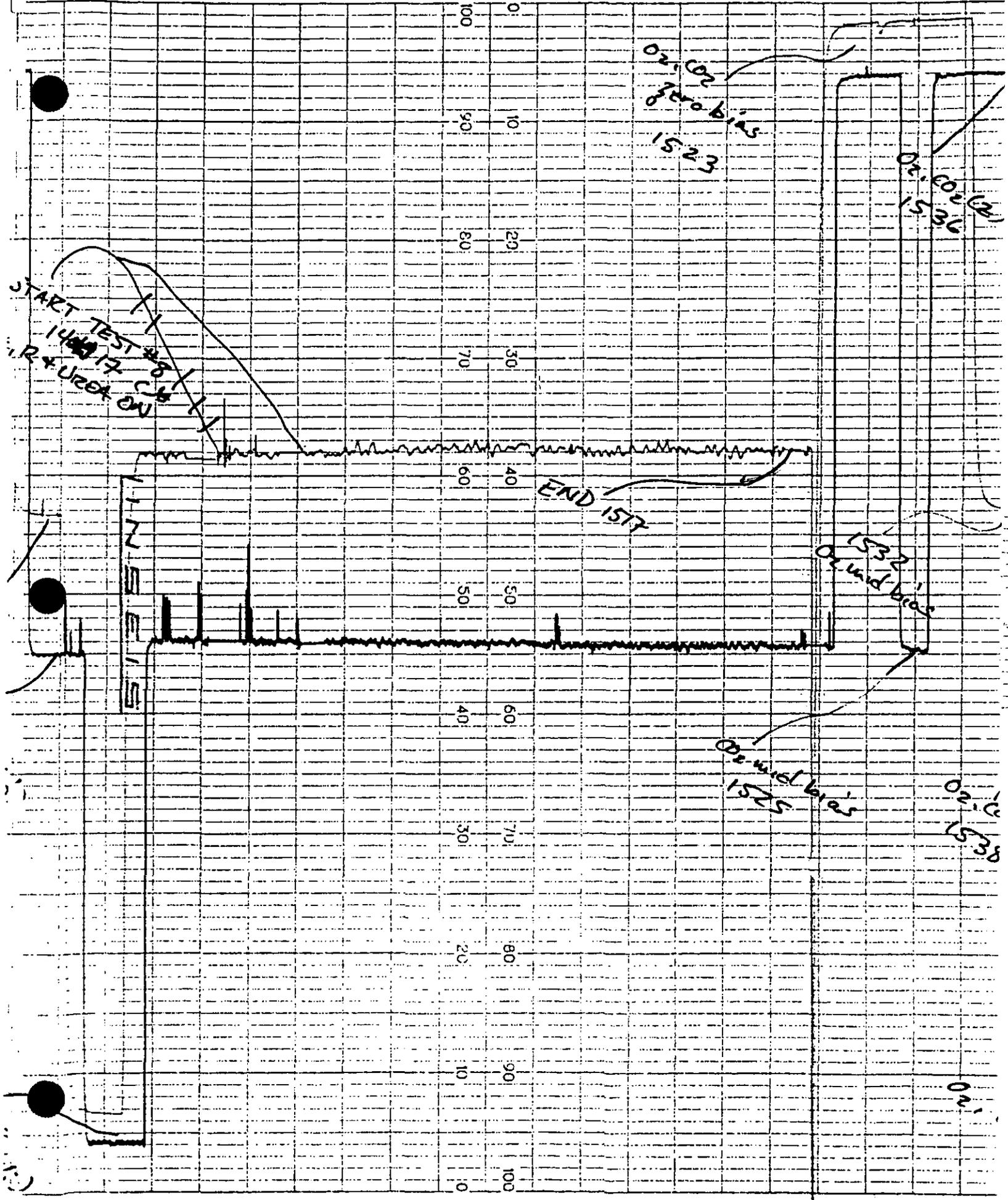
B-1  
0924

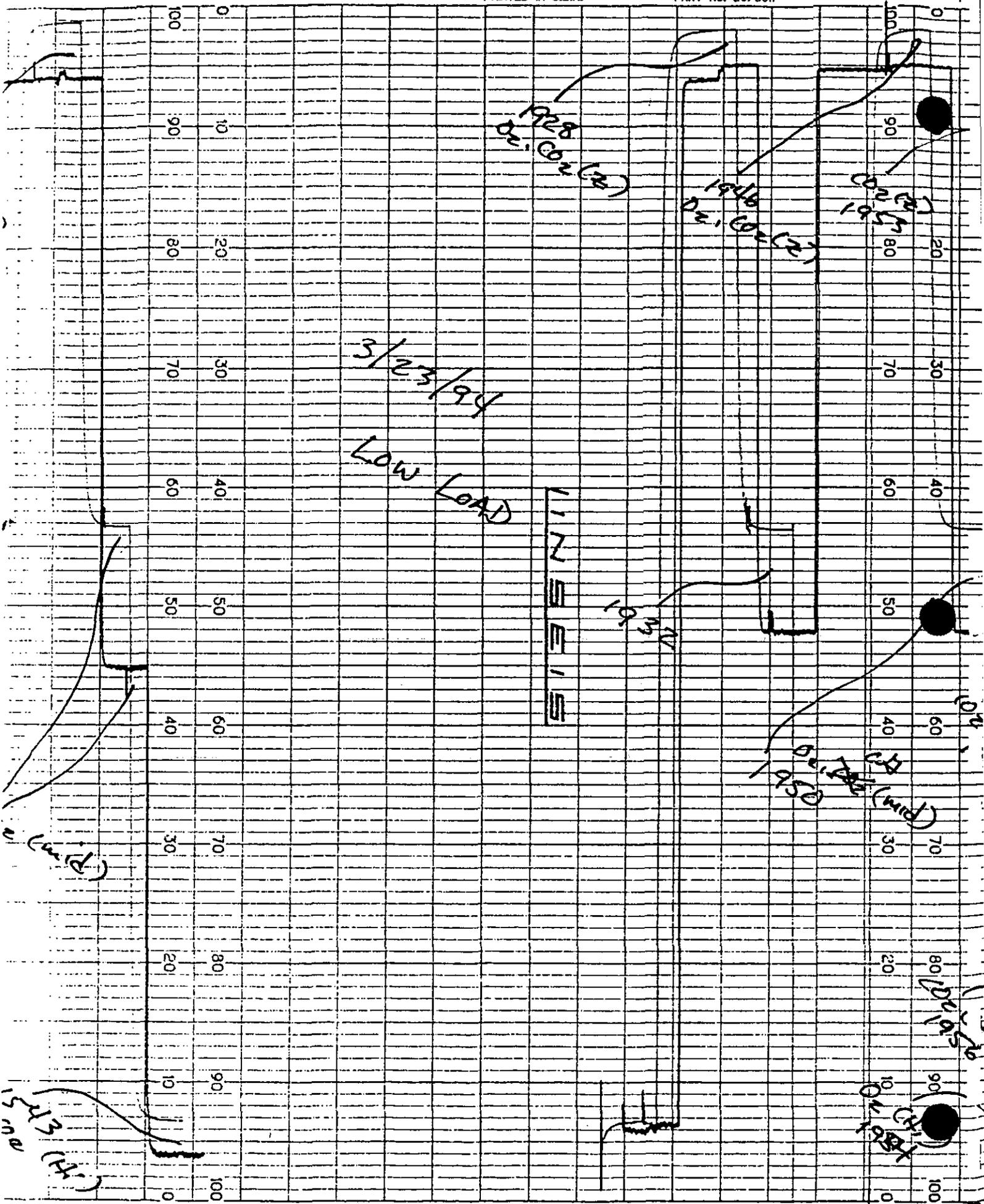
N-6  
0905

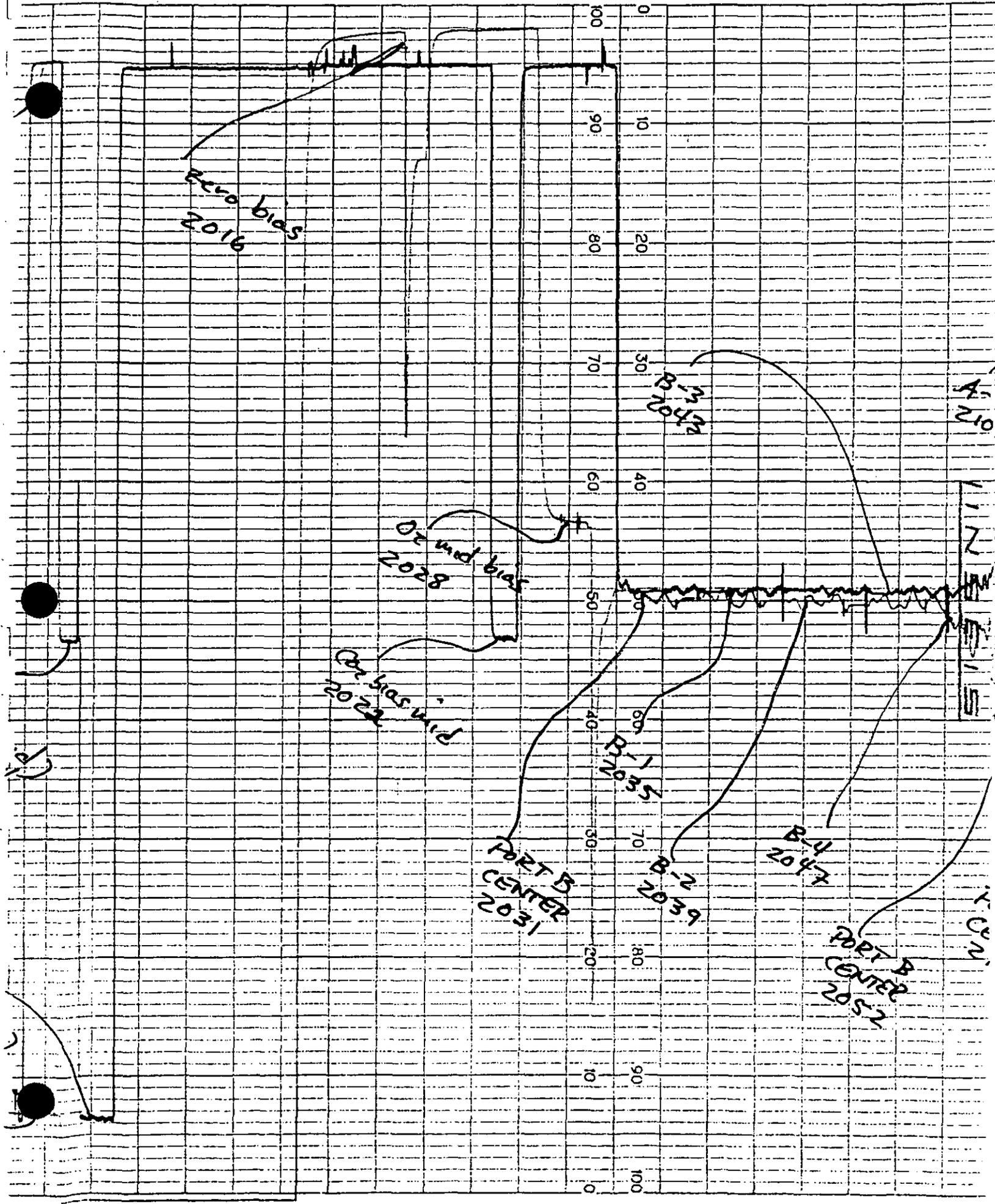


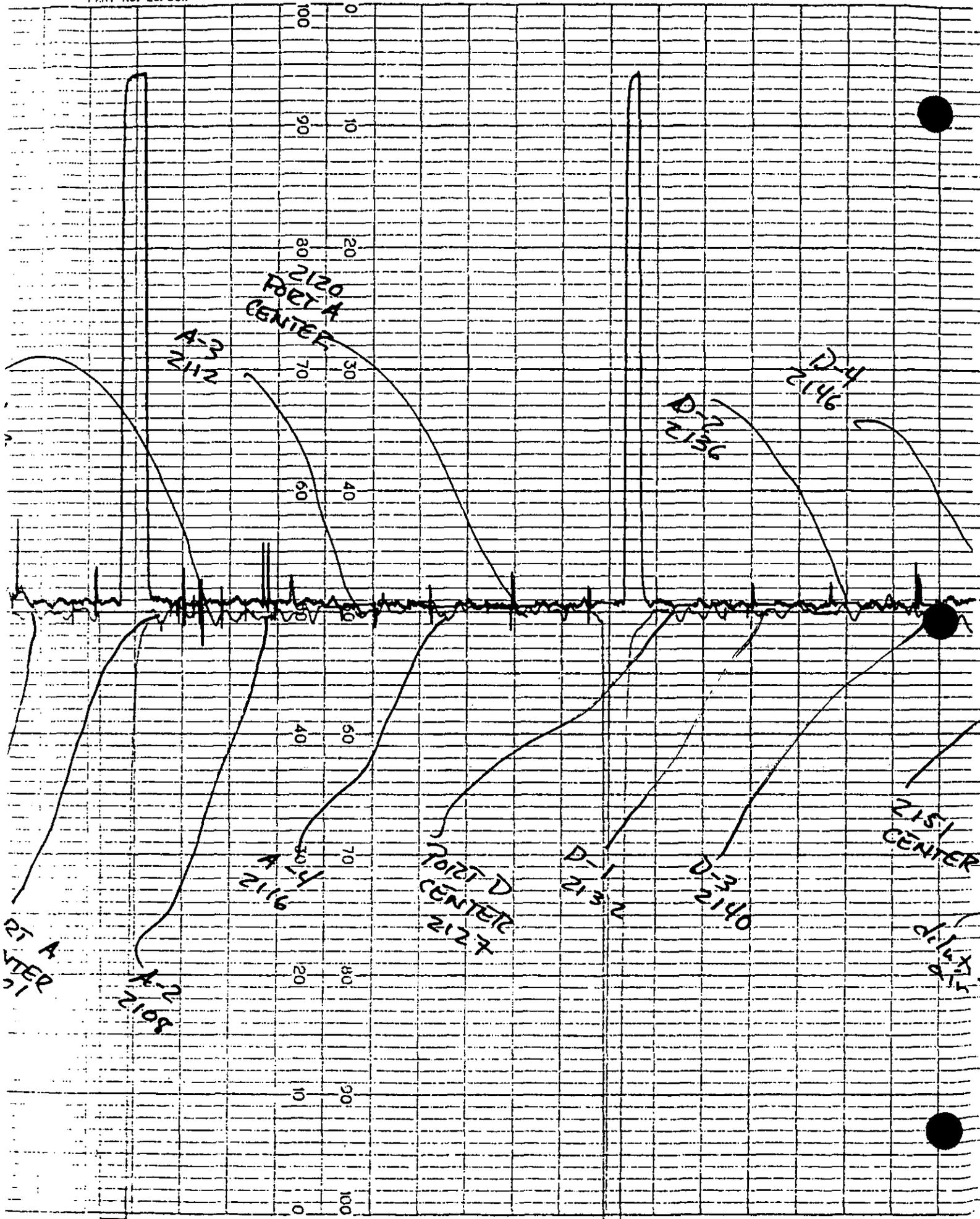






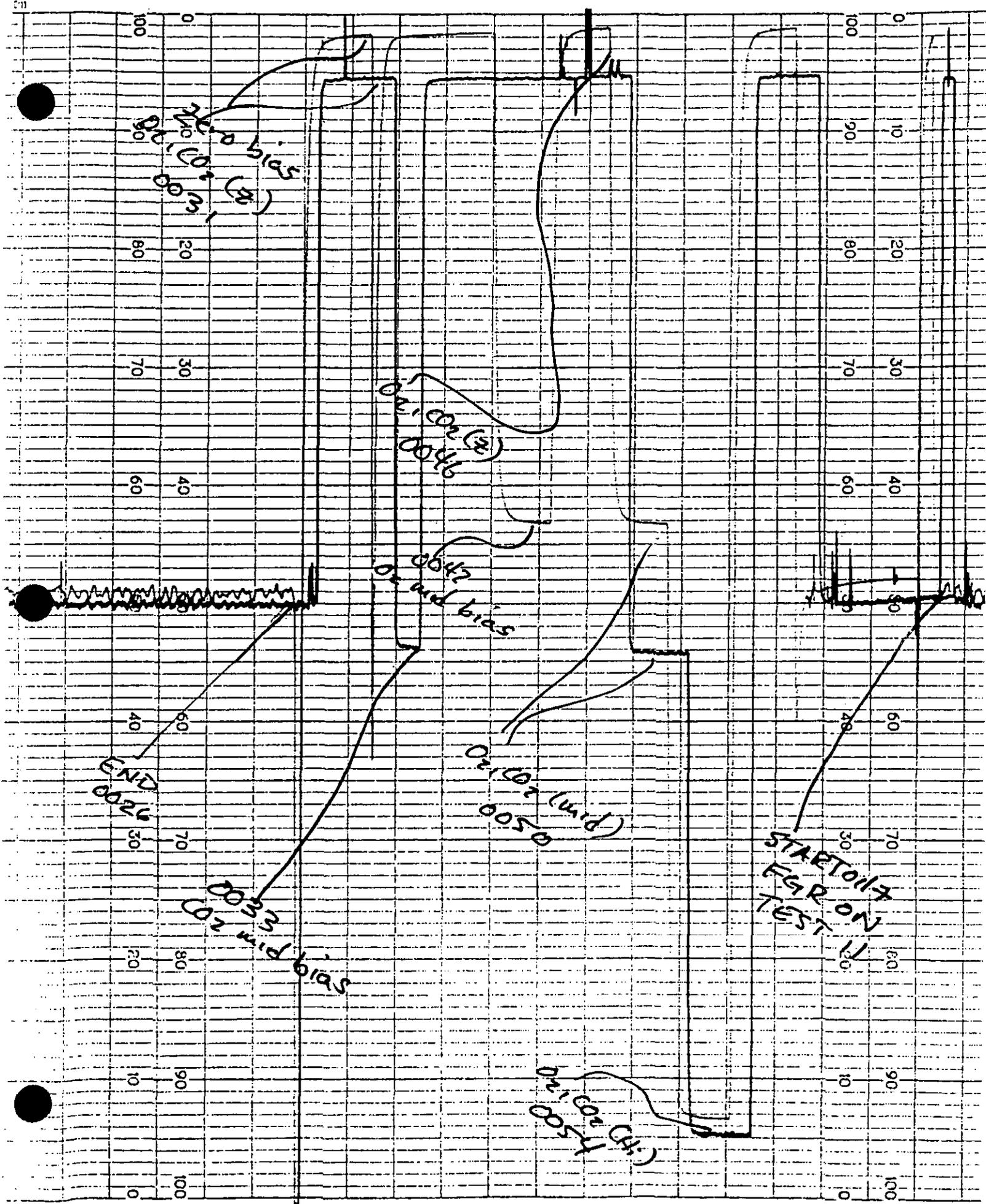


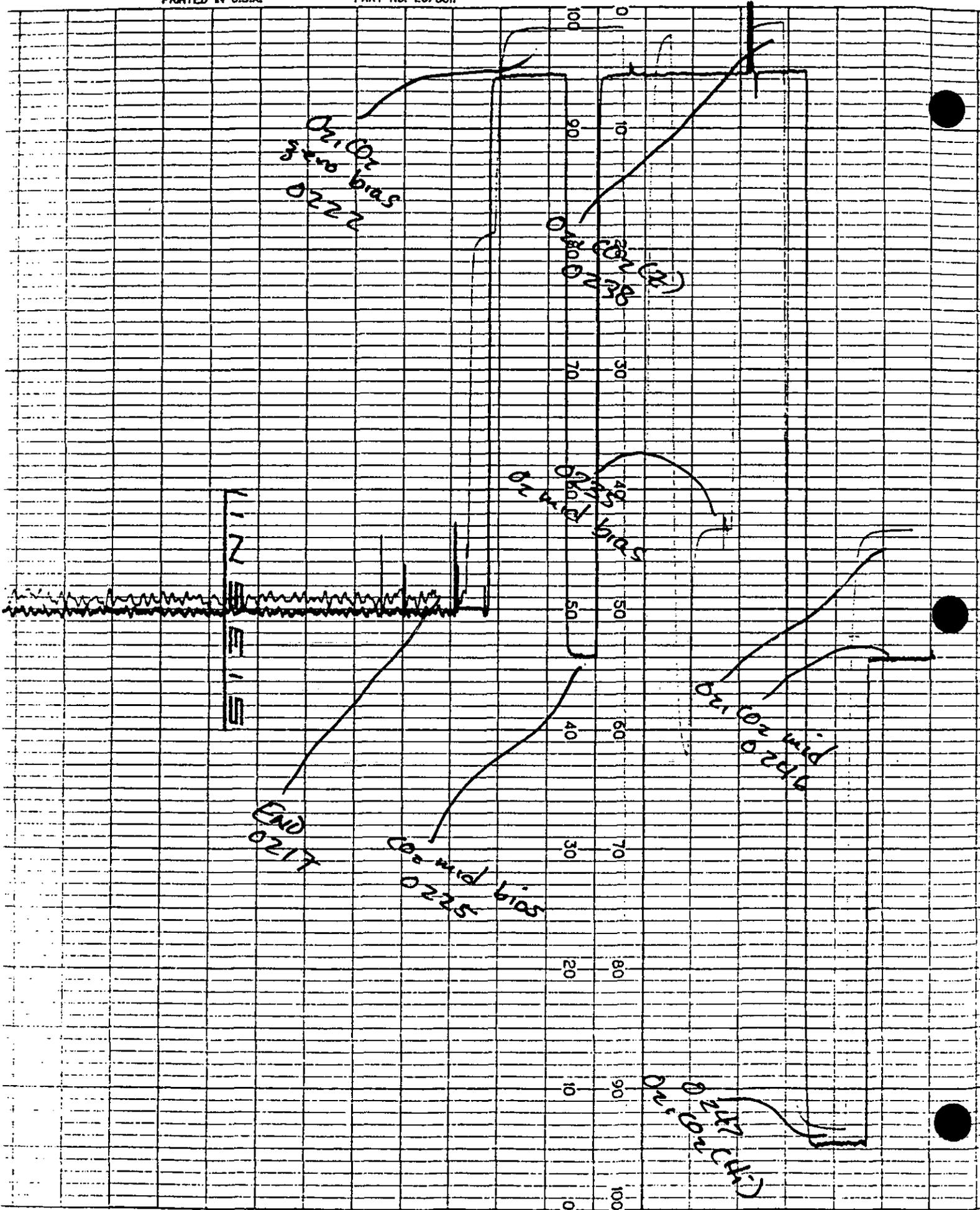












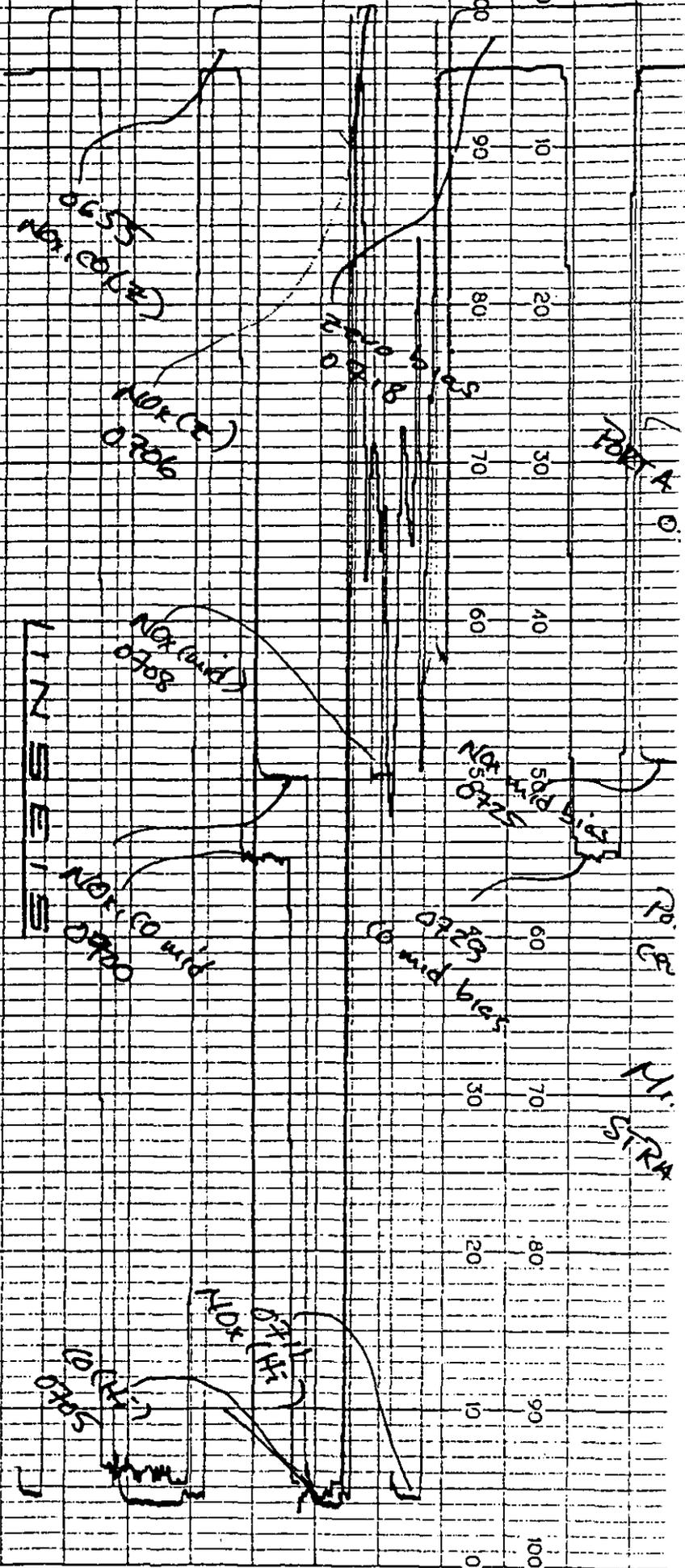
0 10 20 30 40 50 60 70 80 90 100

3/23/94  
SCE-~~XXXX~~ EGS #3  
MID LOAD  
oper. C. Yarnetson

NOR-red  
0-100 ppm  
Hi-92.18 ppm  
Cyl. # AAL5362  
Exp. 10/95  
Mid 47.95  
Cyl. # AAL14063  
Exp. 10/95

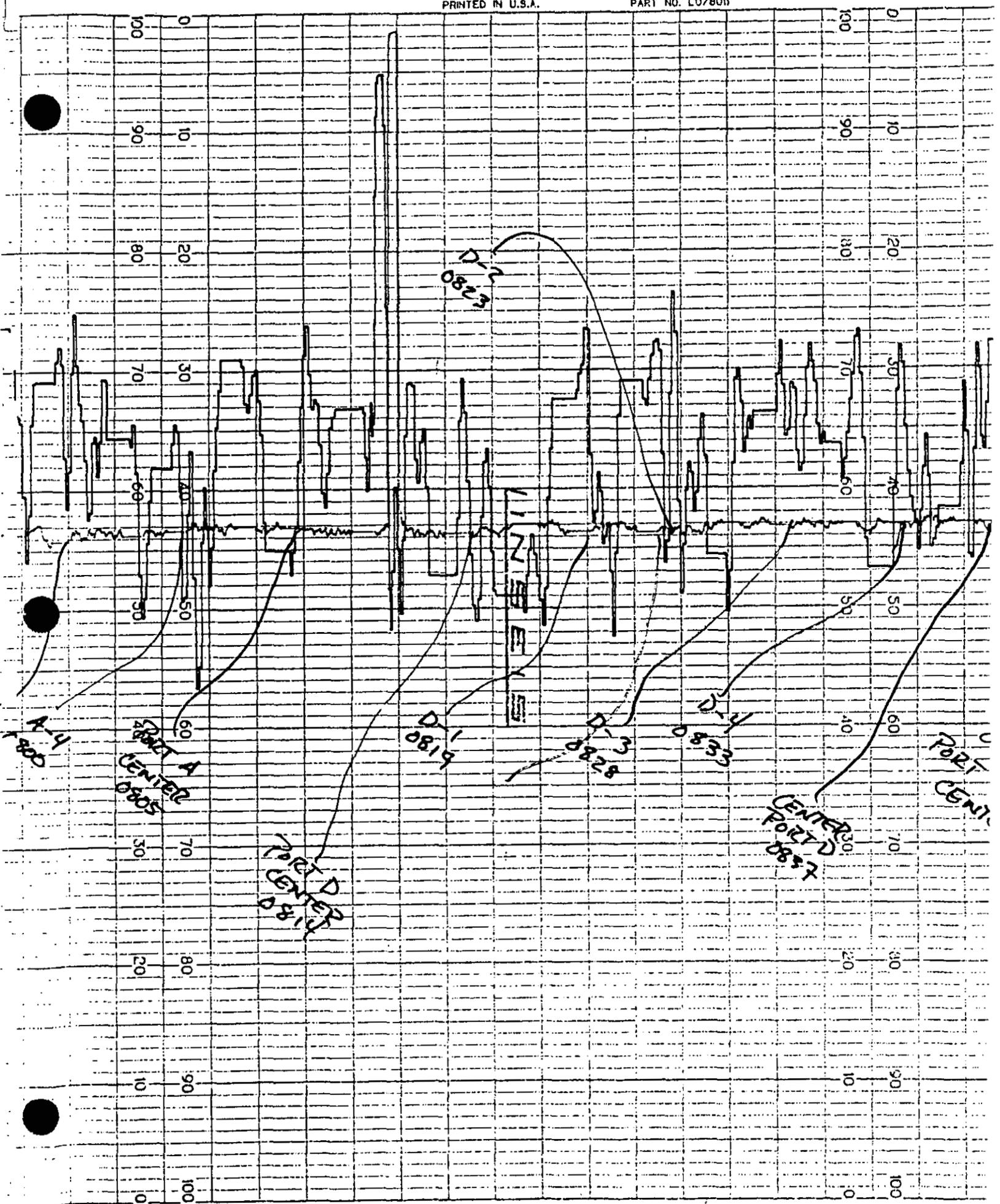
CO-blave  
0-500 ppm  
Hi-451  
Cyl. # S5708 D725  
Exp. 10/96  
Mid-250  
Cyl. # CL27460  
Exp. 10/96

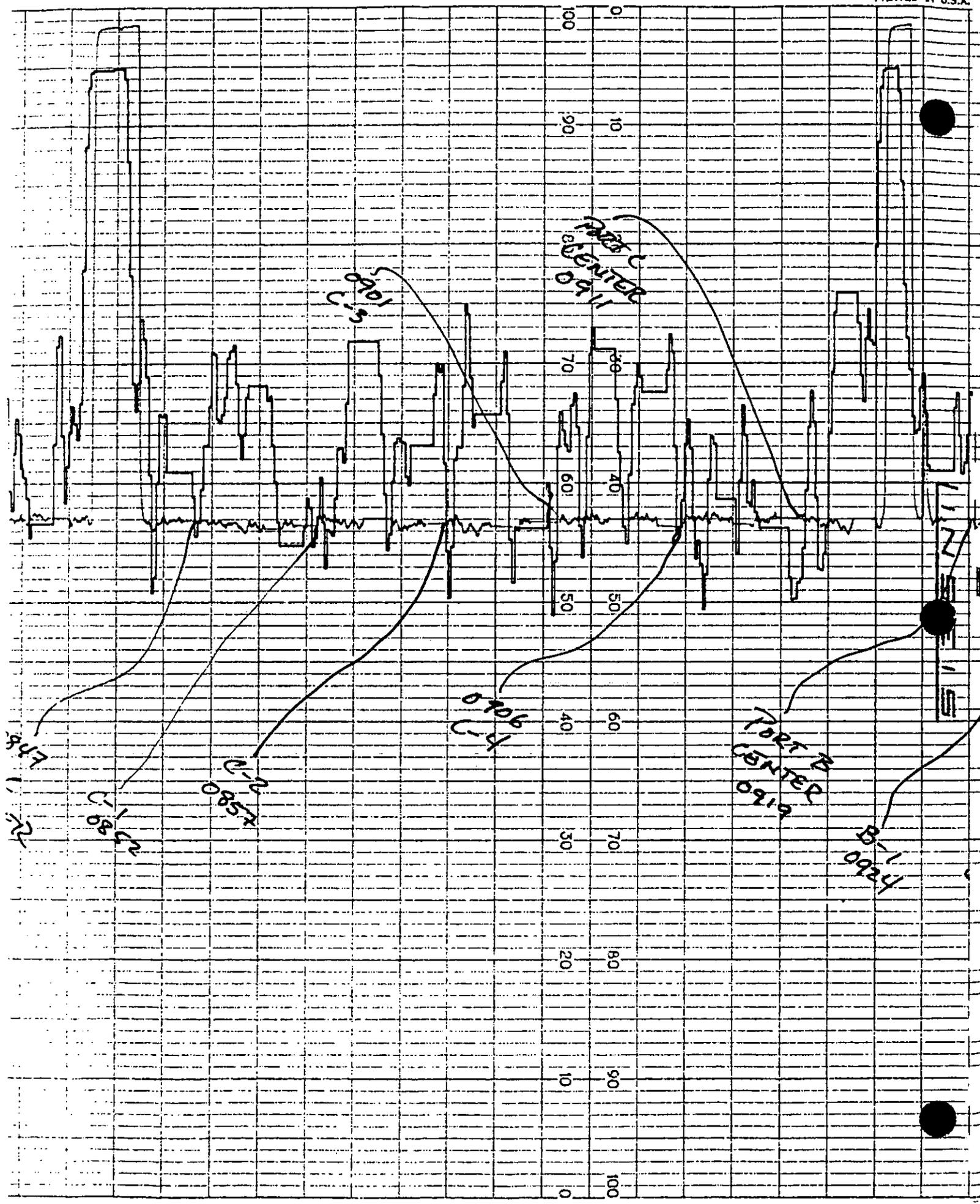
C.S.  
Sachin - calib.  
6 min - test

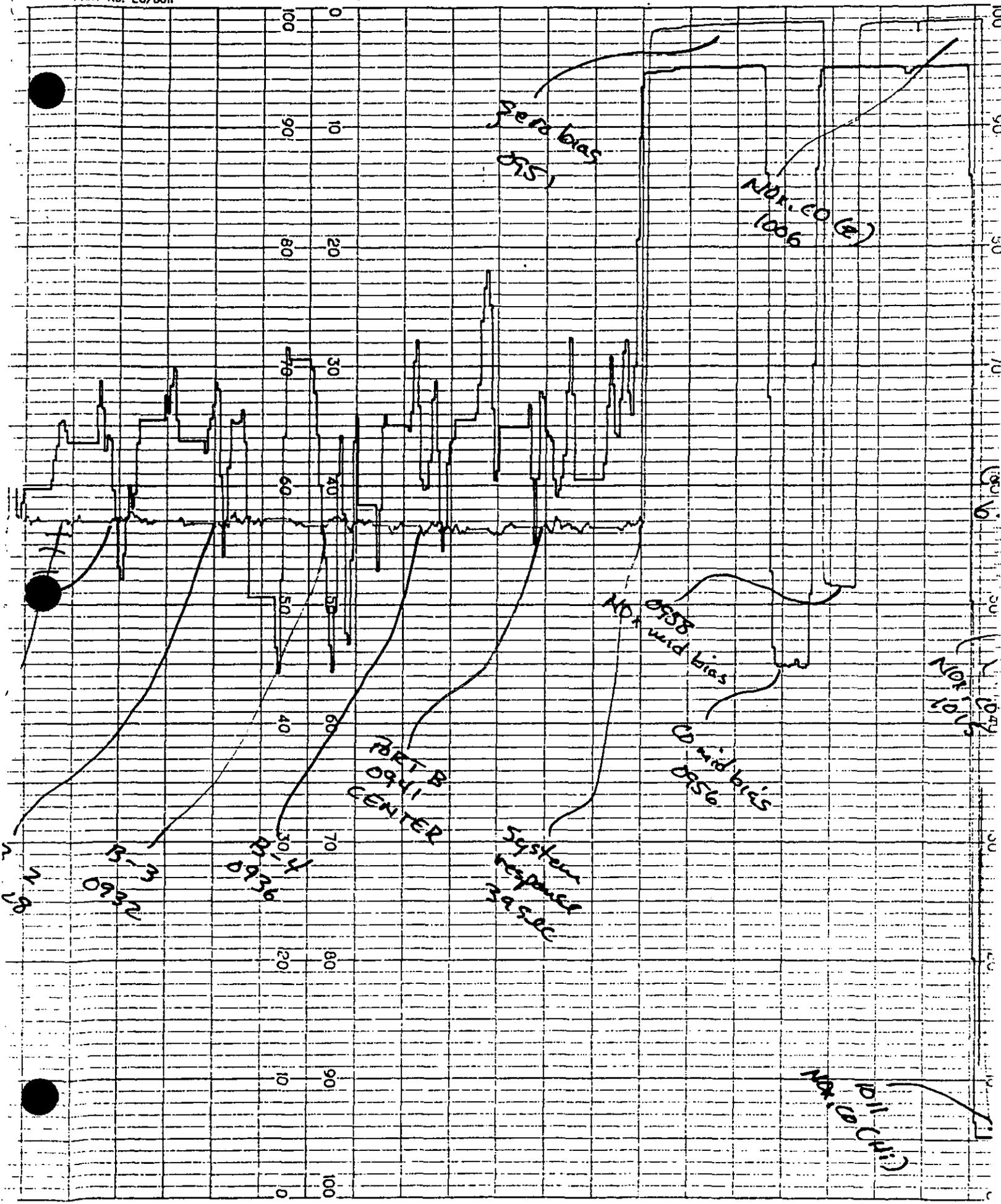


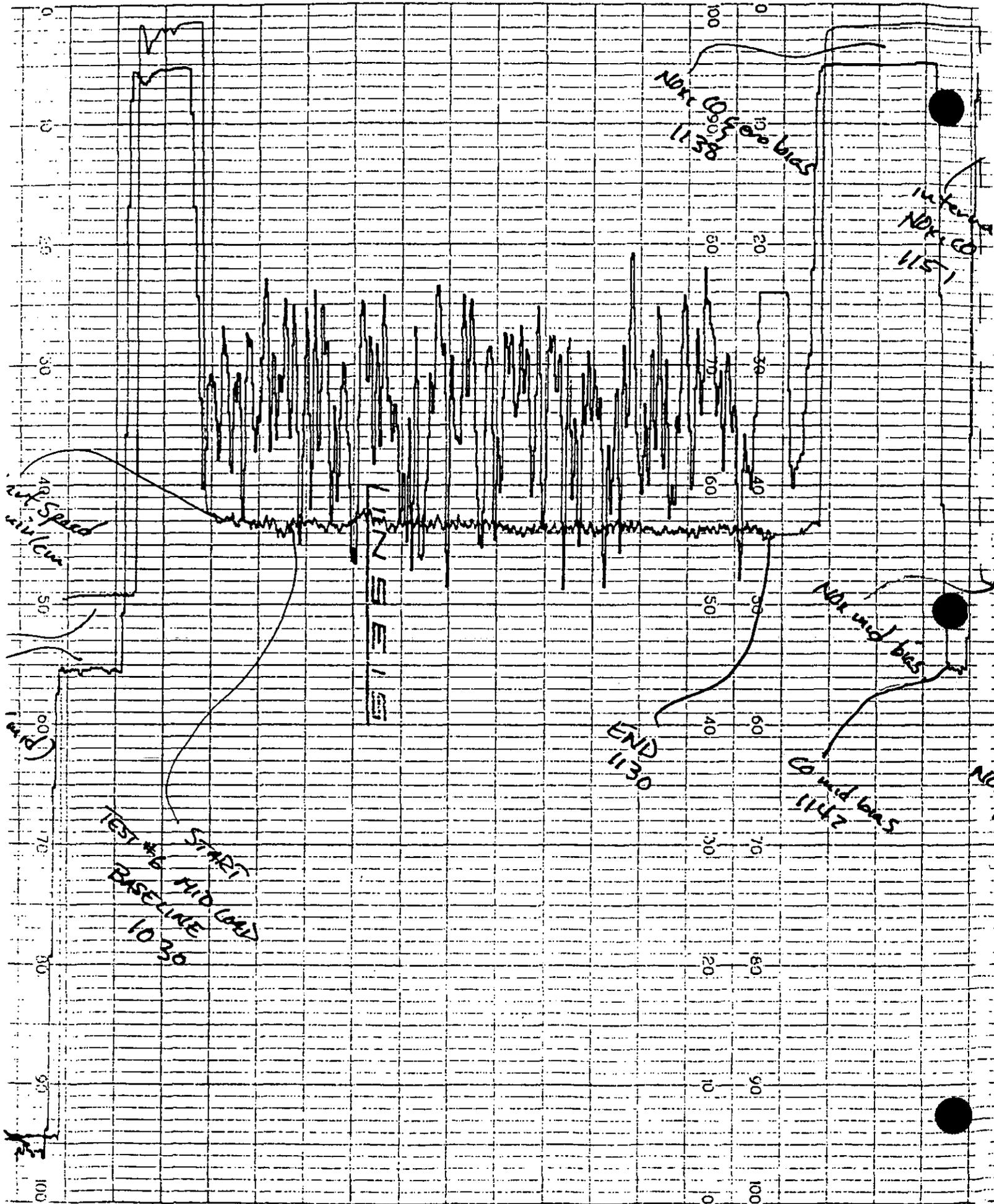
NOX (CE)  
NOX (mid)  
NOX (low)  
NOX (high)  
NOX (total)  
NOX (avg)  
NOX (min)  
NOX (max)  
NOX (std dev)  
NOX (variance)  
NOX (coefficient of variation)  
NOX (skewness)  
NOX (kurtosis)  
NOX (entropy)  
NOX (information content)  
NOX (mutual information)  
NOX (conditional entropy)  
NOX (joint entropy)  
NOX (conditional mutual information)  
NOX (total mutual information)  
NOX (conditional mutual information)  
NOX (joint mutual information)  
NOX (conditional mutual information)  
NOX (joint mutual information)  
NOX (conditional mutual information)  
NOX (joint mutual information)

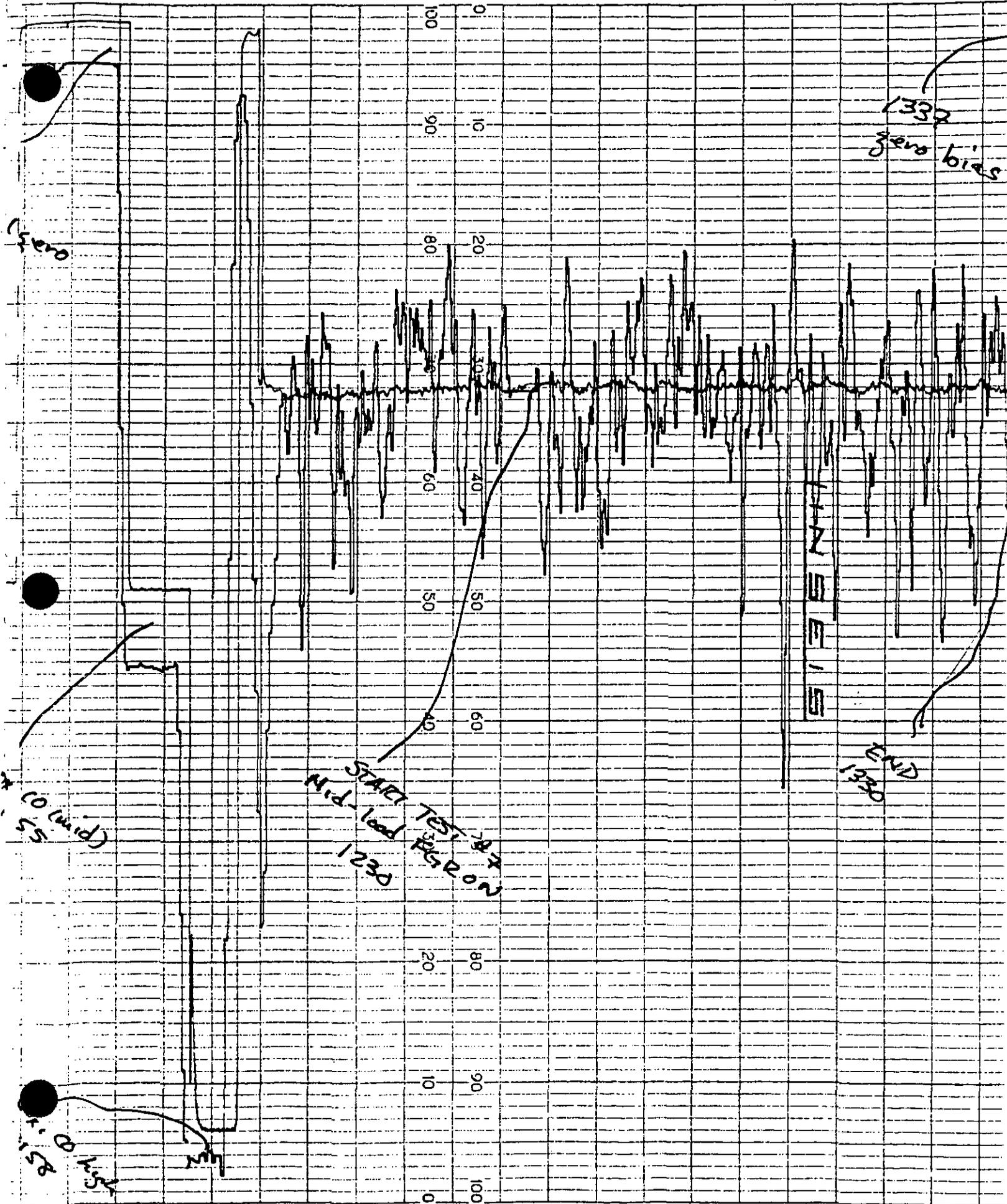


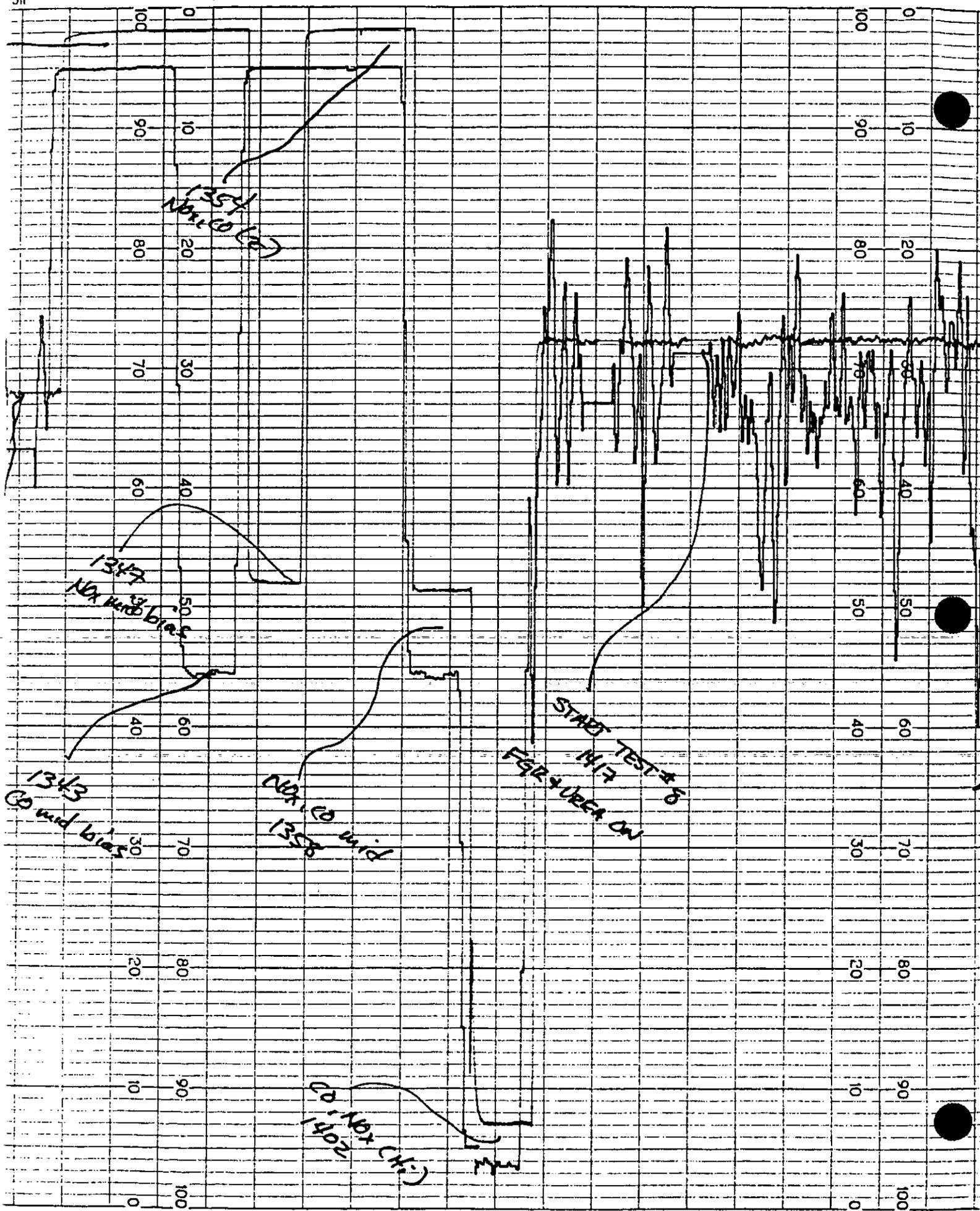


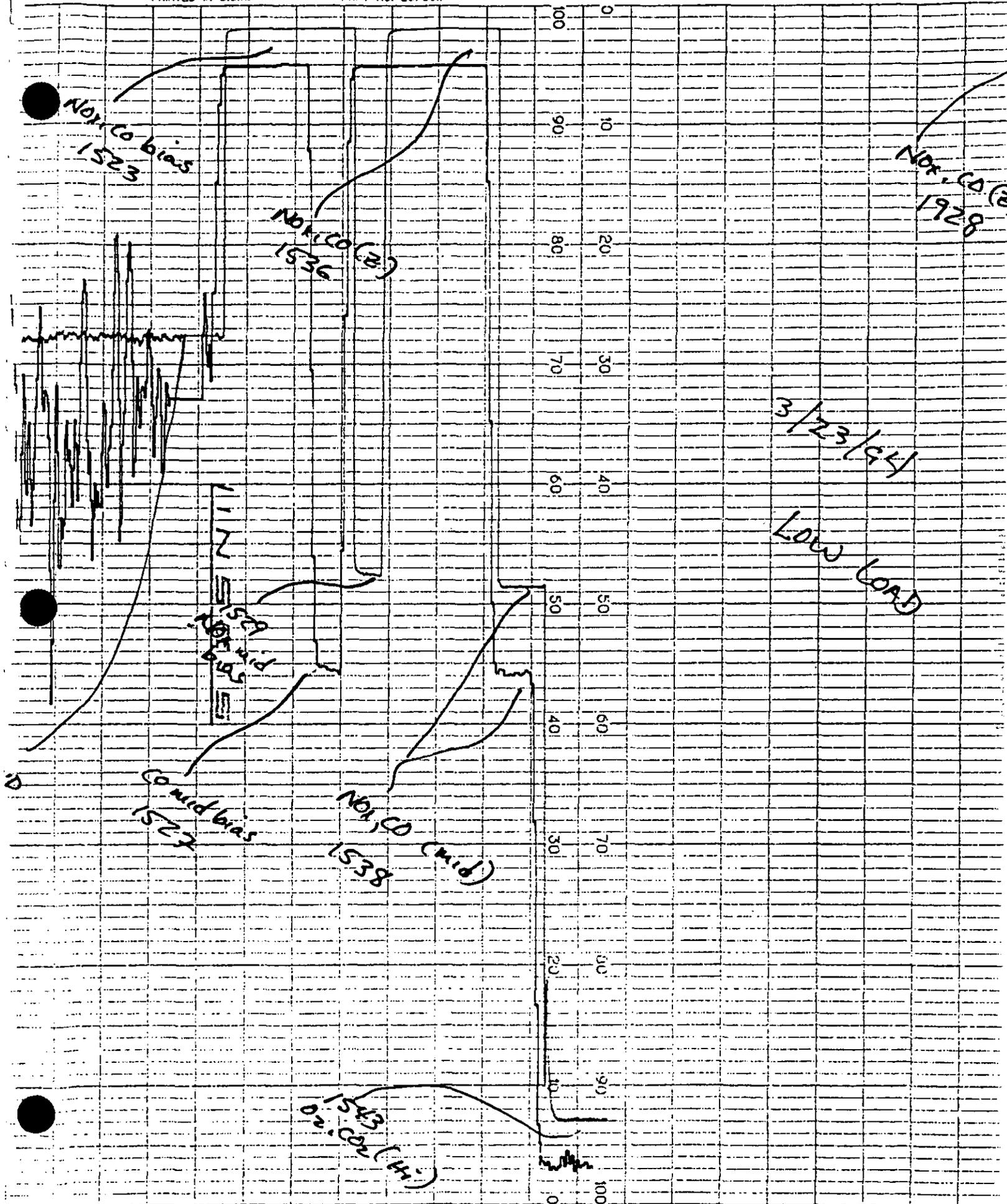




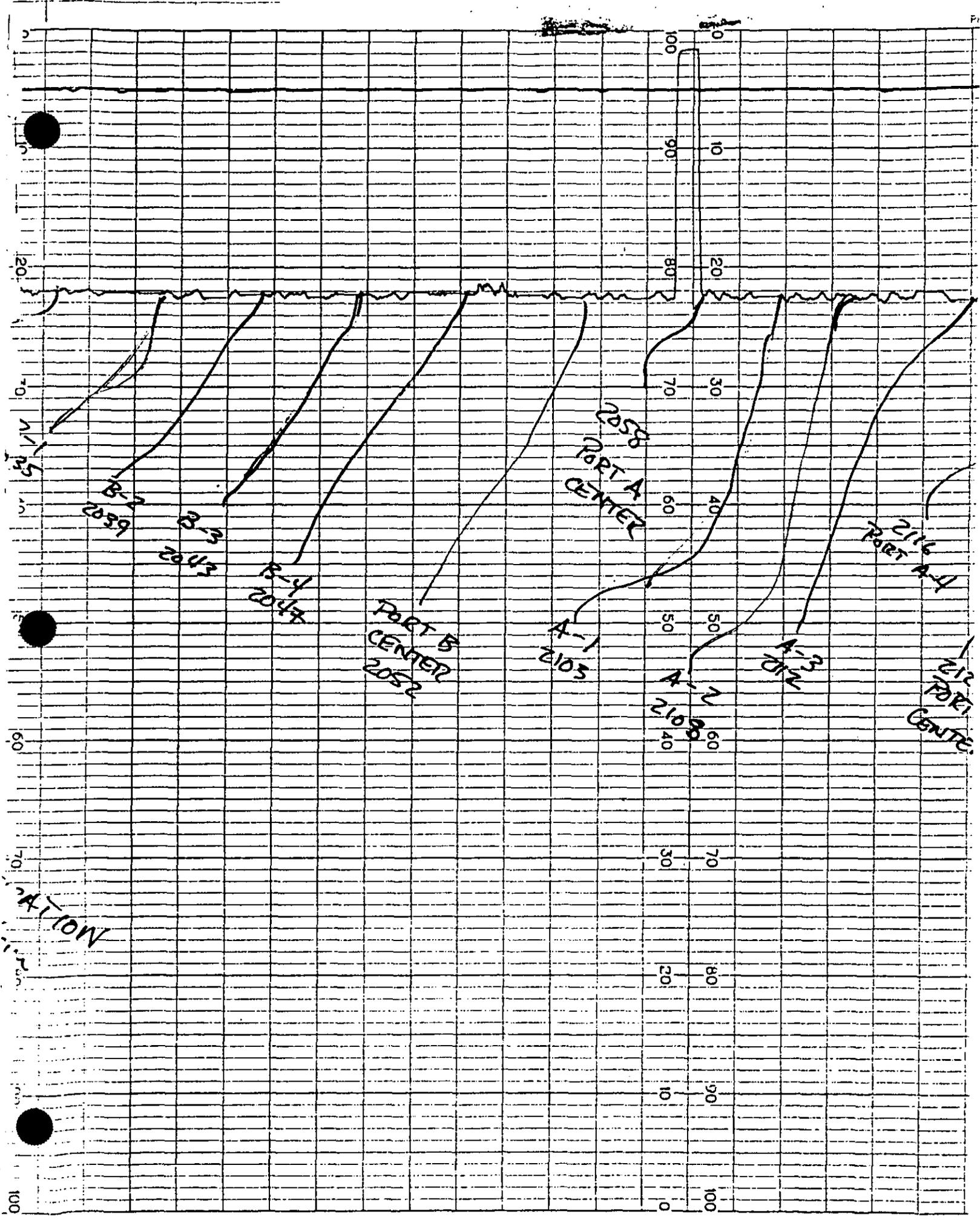


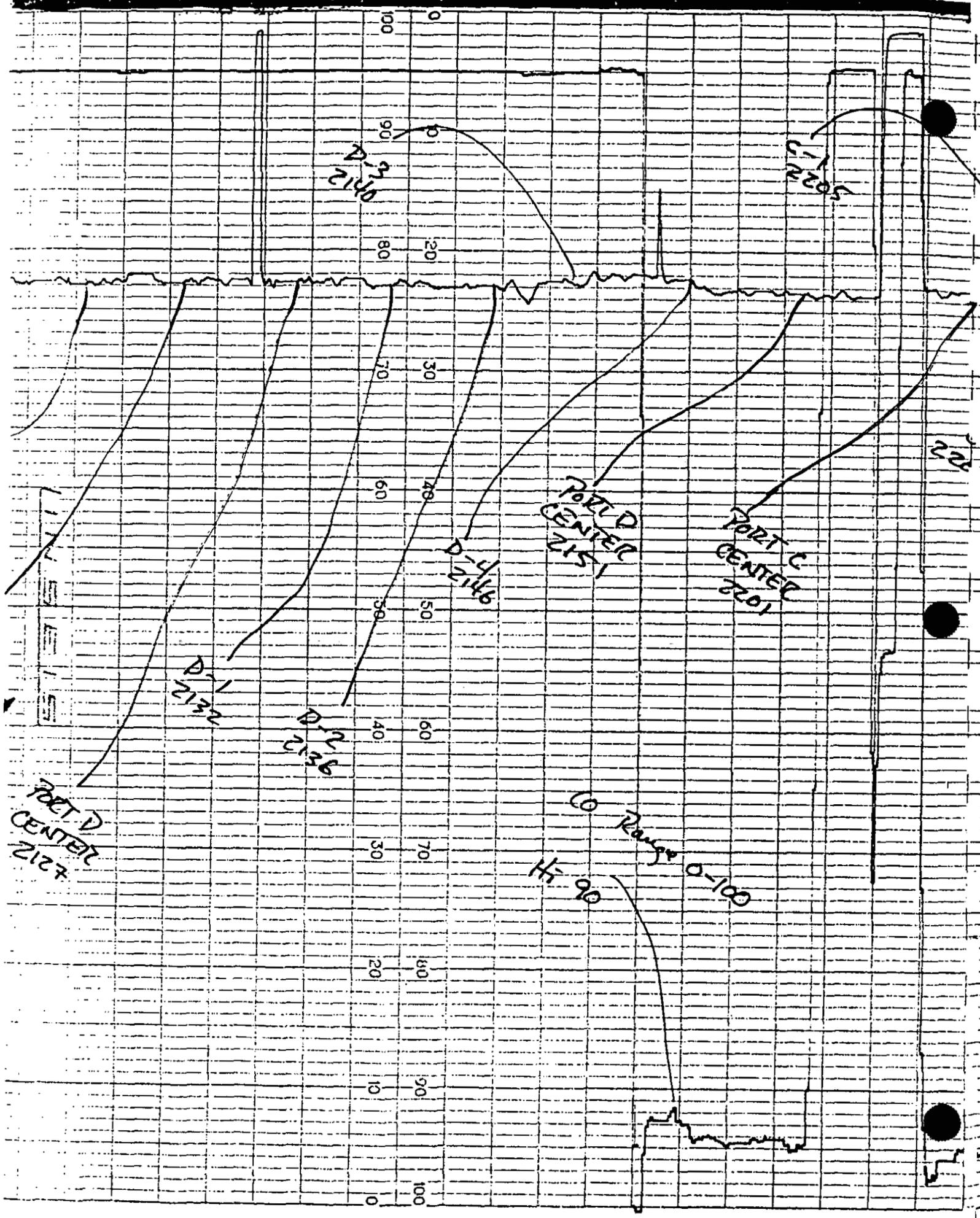


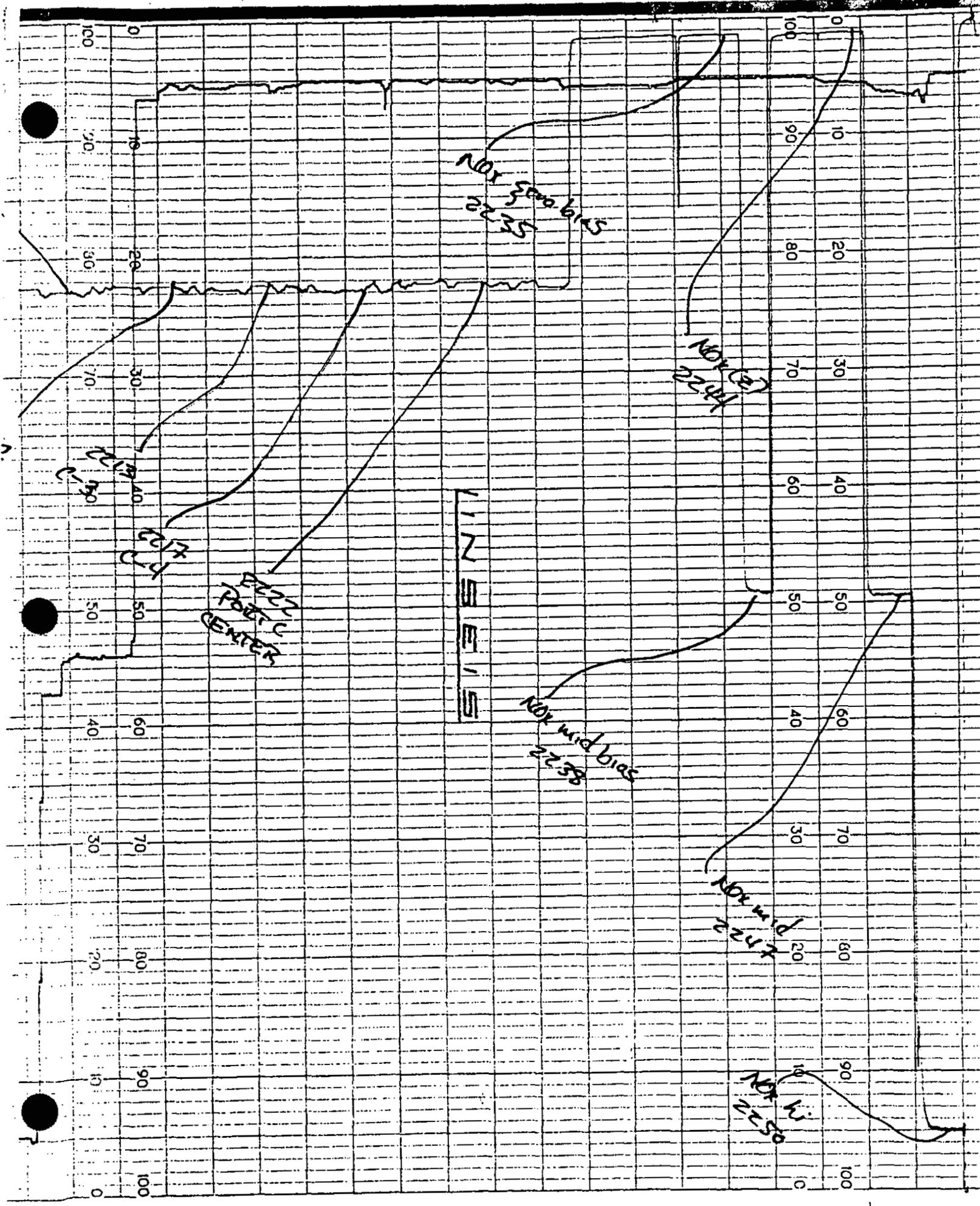




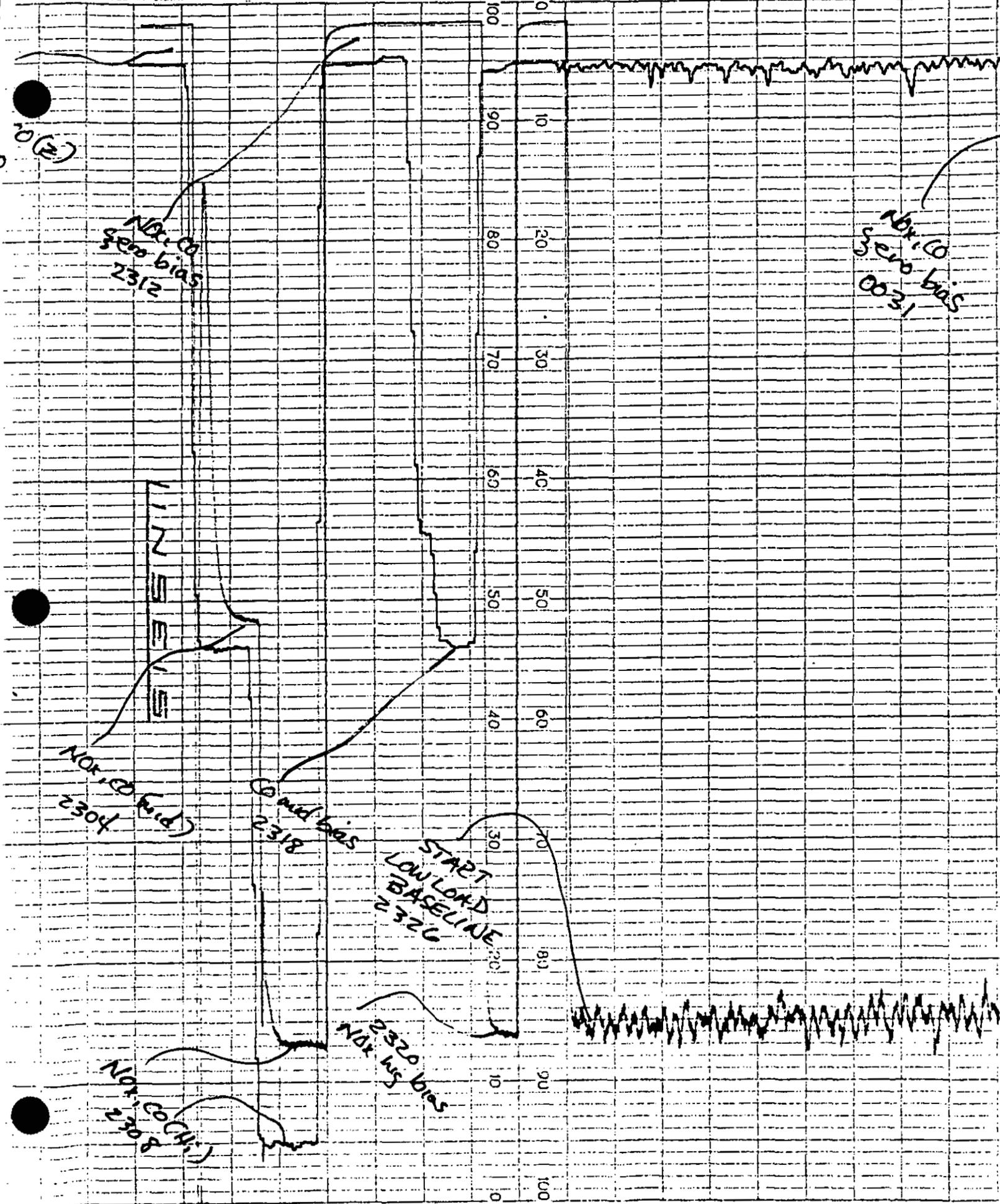












20(2)

NOX CO  
Serv bias  
2312

NOX CO  
Serv bias  
0031

L  
I  
N  
E  
S  
E  
L  
S

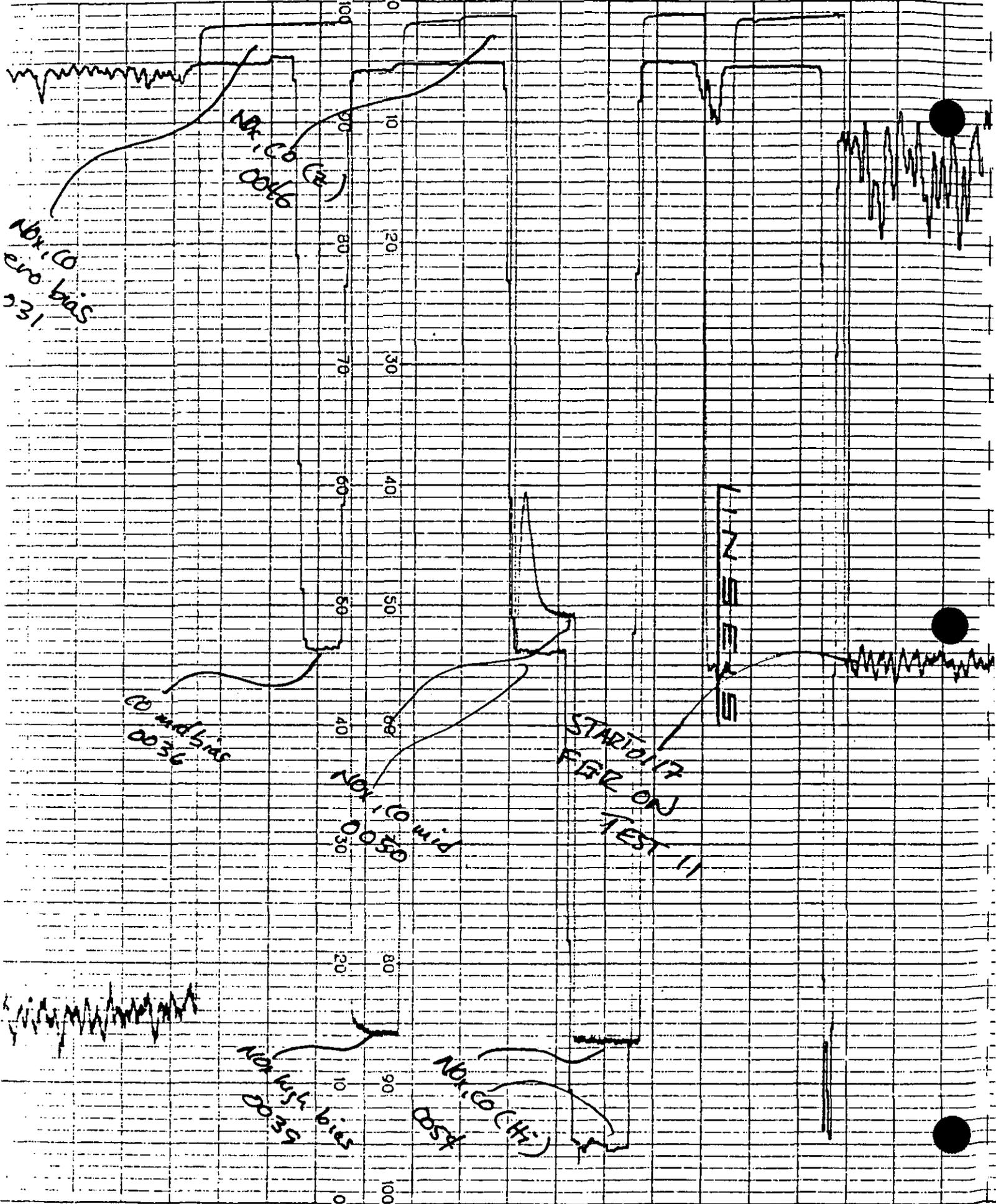
NOX CO Serv bias  
2302  
(PREF. CO)

NOX CO Serv bias  
2318

START  
LOW LOAD  
BASELINE  
2320

NOX MS Serv bias  
0320

NOX CO (Hi)  
8032







**APPENDIX D-4**

**STRATIFICATION TEST TRAVERSE POINT LOCATIONS**

D-80

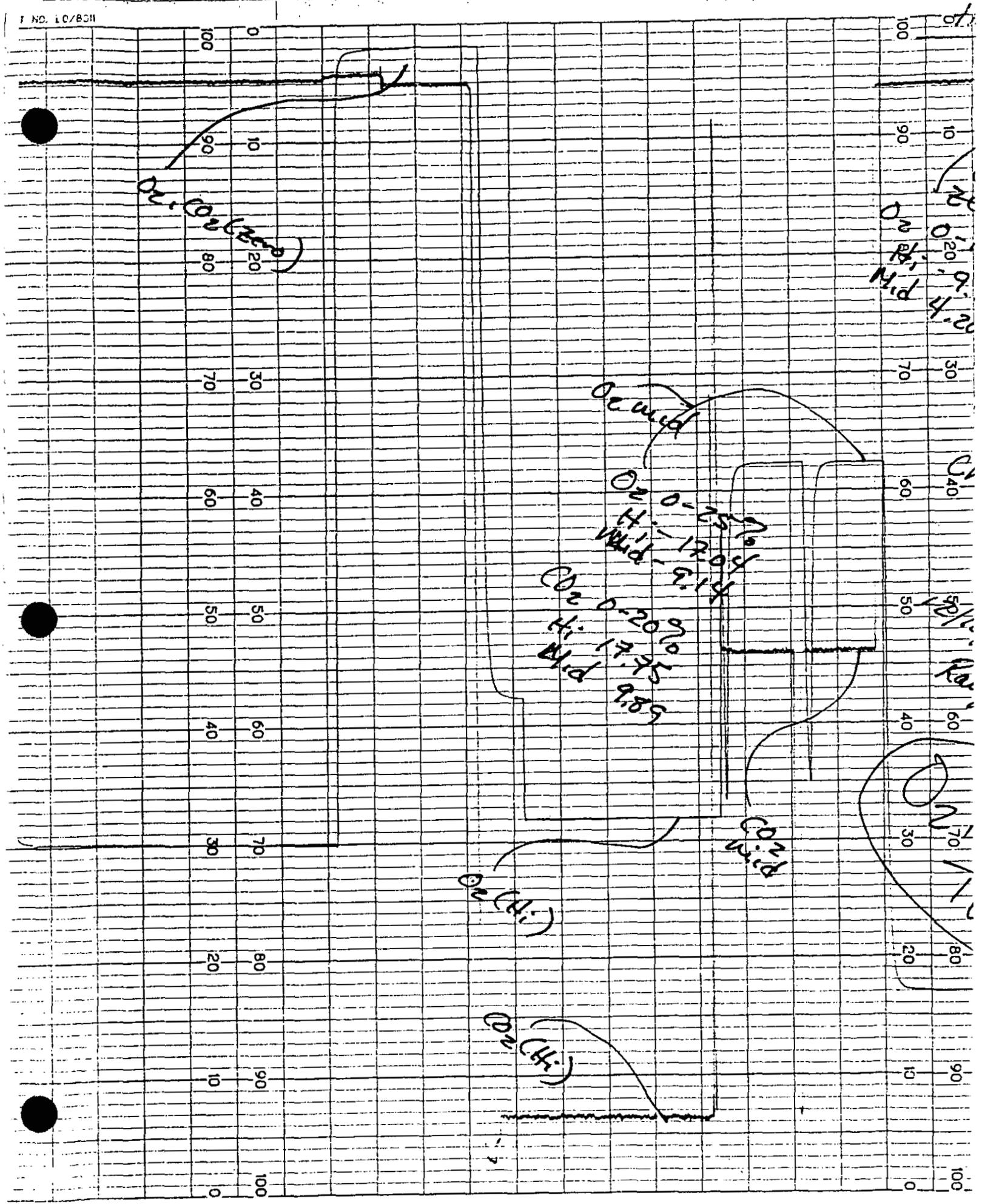




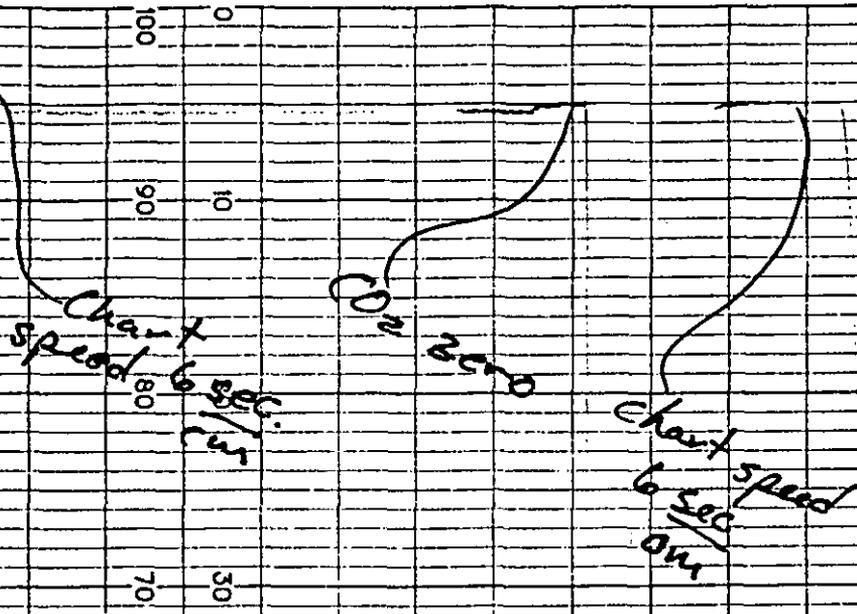
**APPENDIX D-5**

**SEMI-ANNUAL INSTRUMENT CALIBRATION RECORDS**









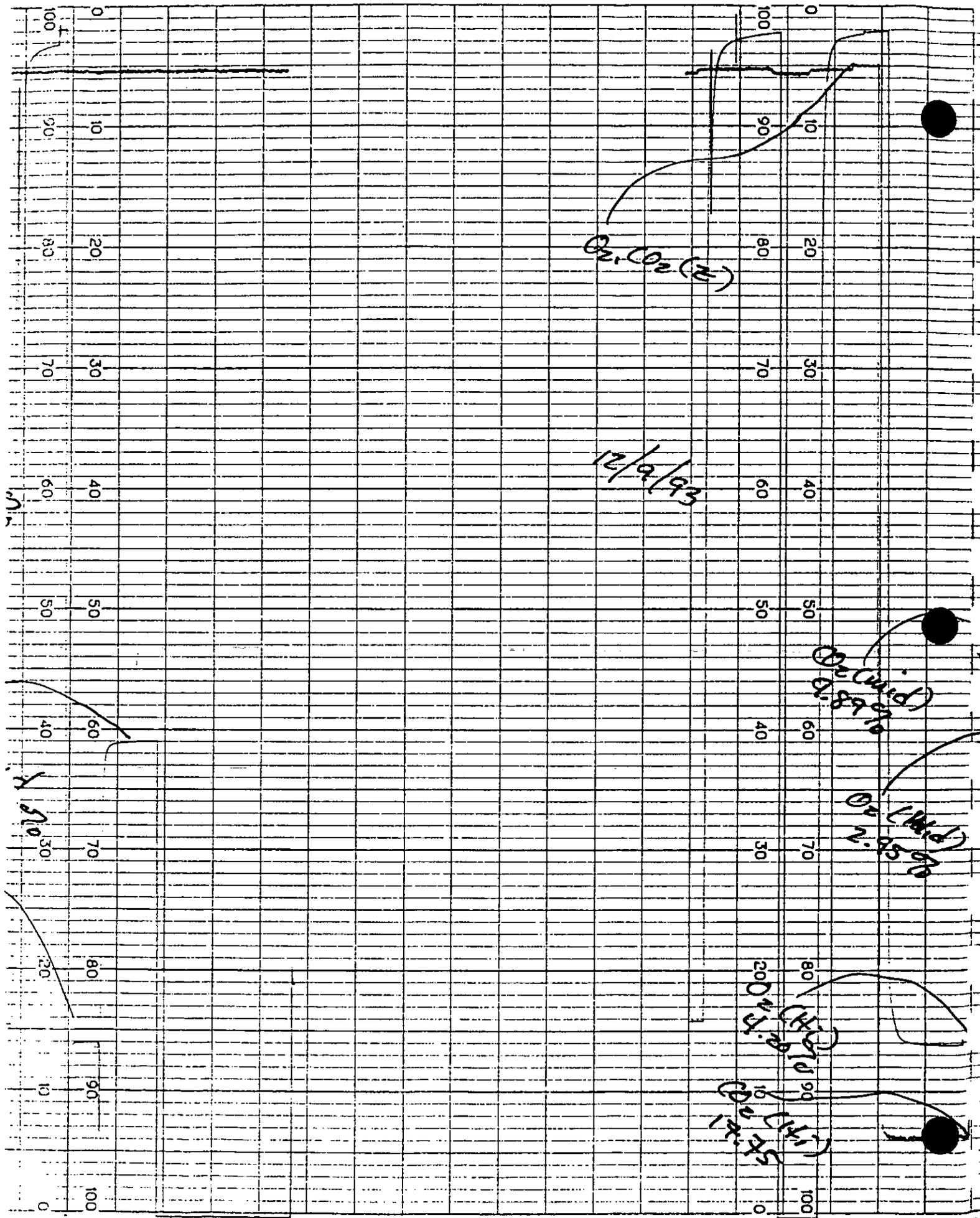
Annotated  
 # 28992  
 # 60241  
 Exp 2/16  
 Exp 2/16  
 # 1775  
 # 989  
 # 2070  
 # 1775  
 # 989  
 # 2070

LINE IS

1.010  
 0.590  
 1.010  
 0.590  
 1.010  
 0.590

0.5  
 0.4  
 0.3  
 0.2  
 0.1  
 0

1.010  
 0.590



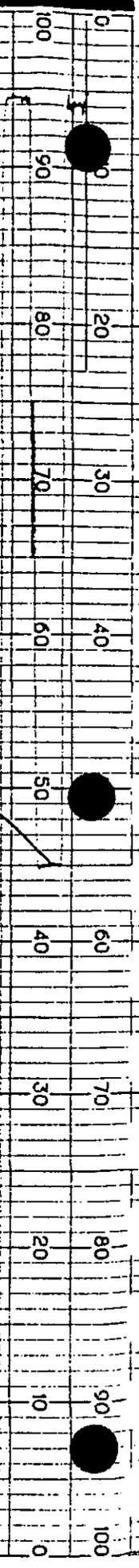
LINE

0 10 20 30 40 50 60 70 80 90 100

NOE (zero)

CO (zero)  
Horiba  
0-500

NOE mid  
0.87

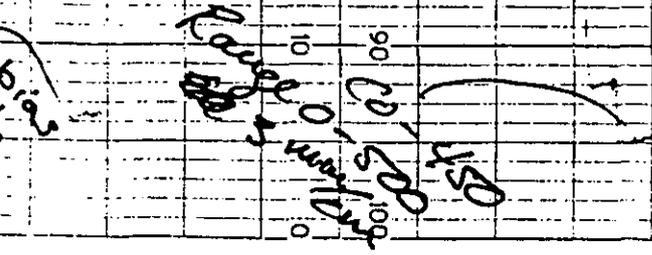
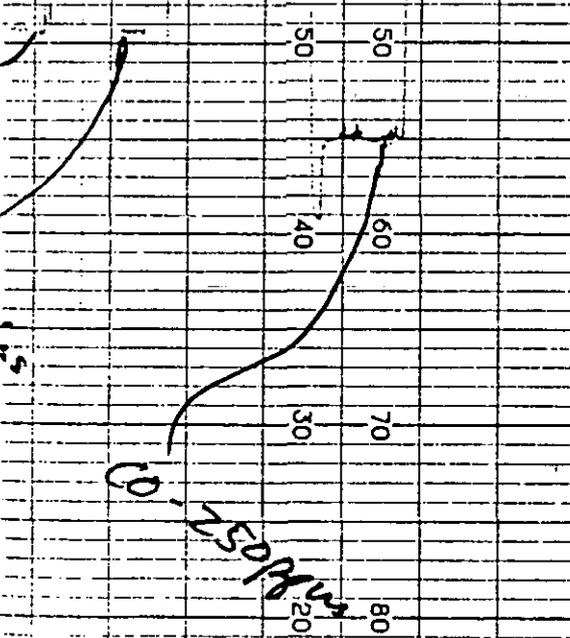
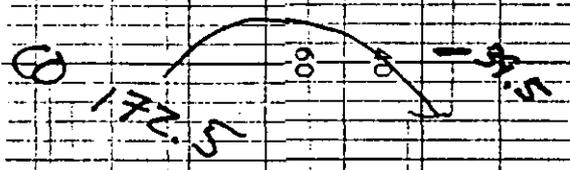
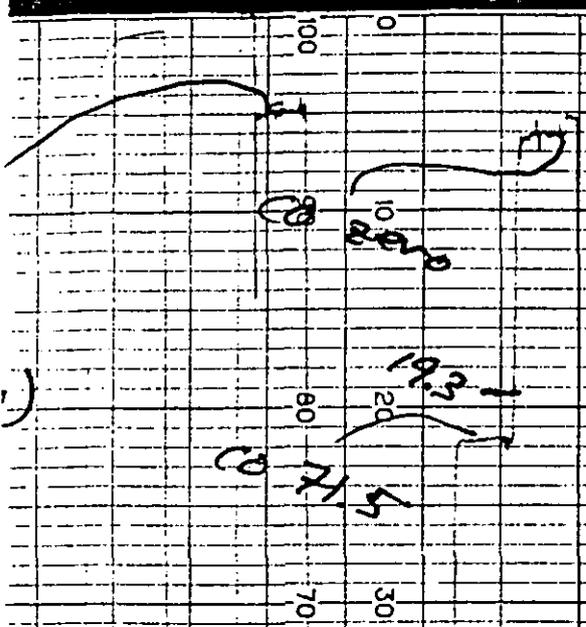


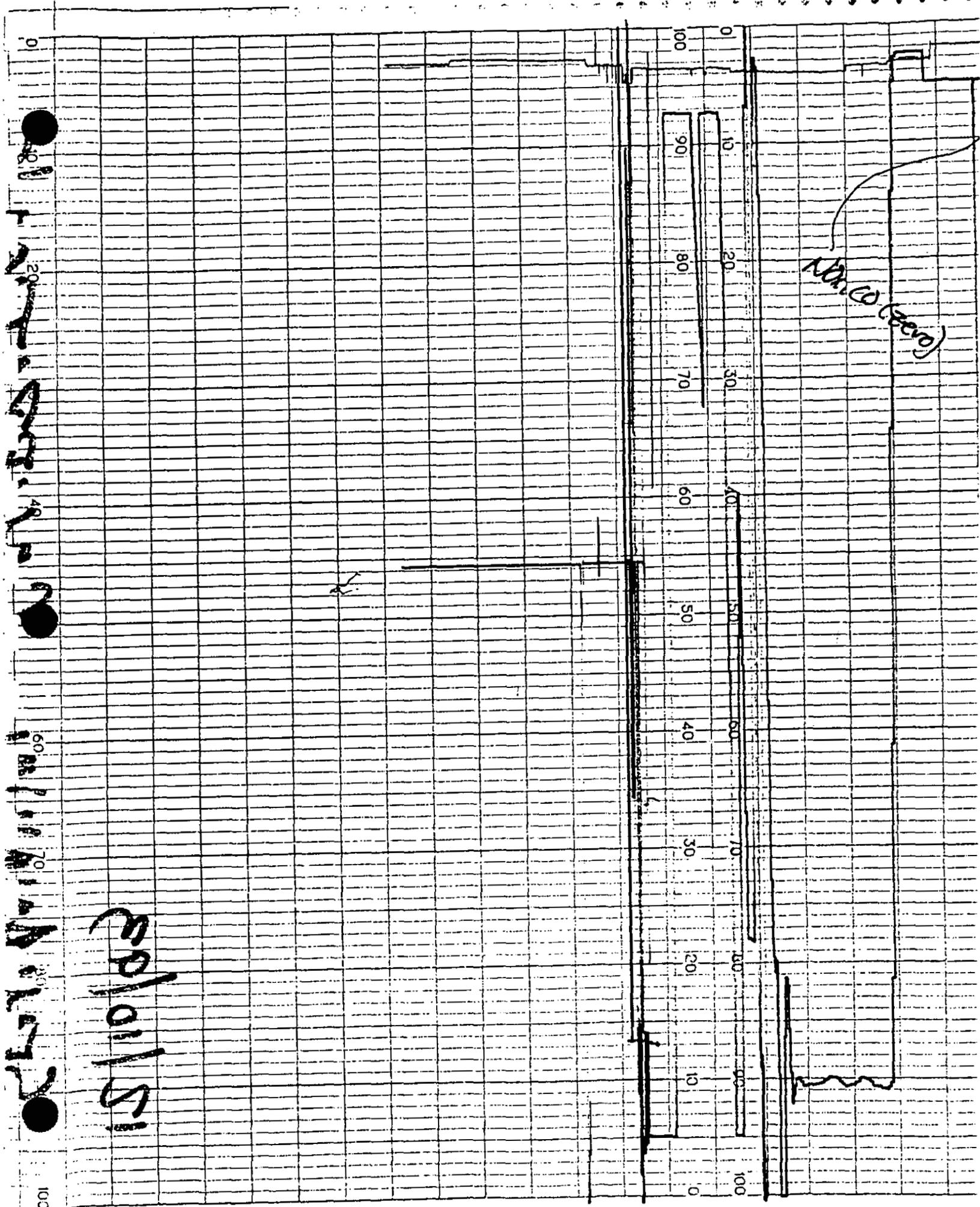
3 sec/cm

LINES

10 sec response time

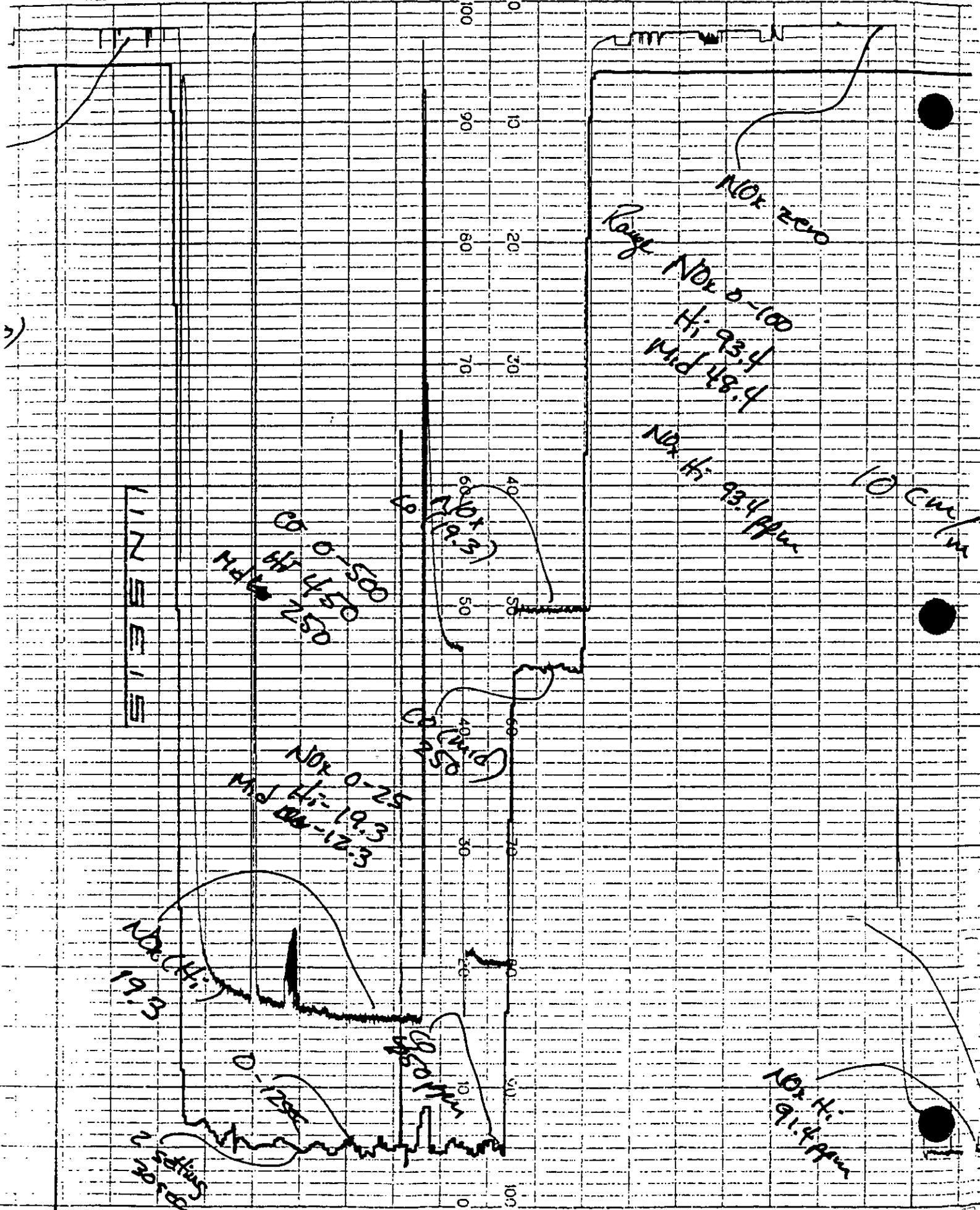
1070

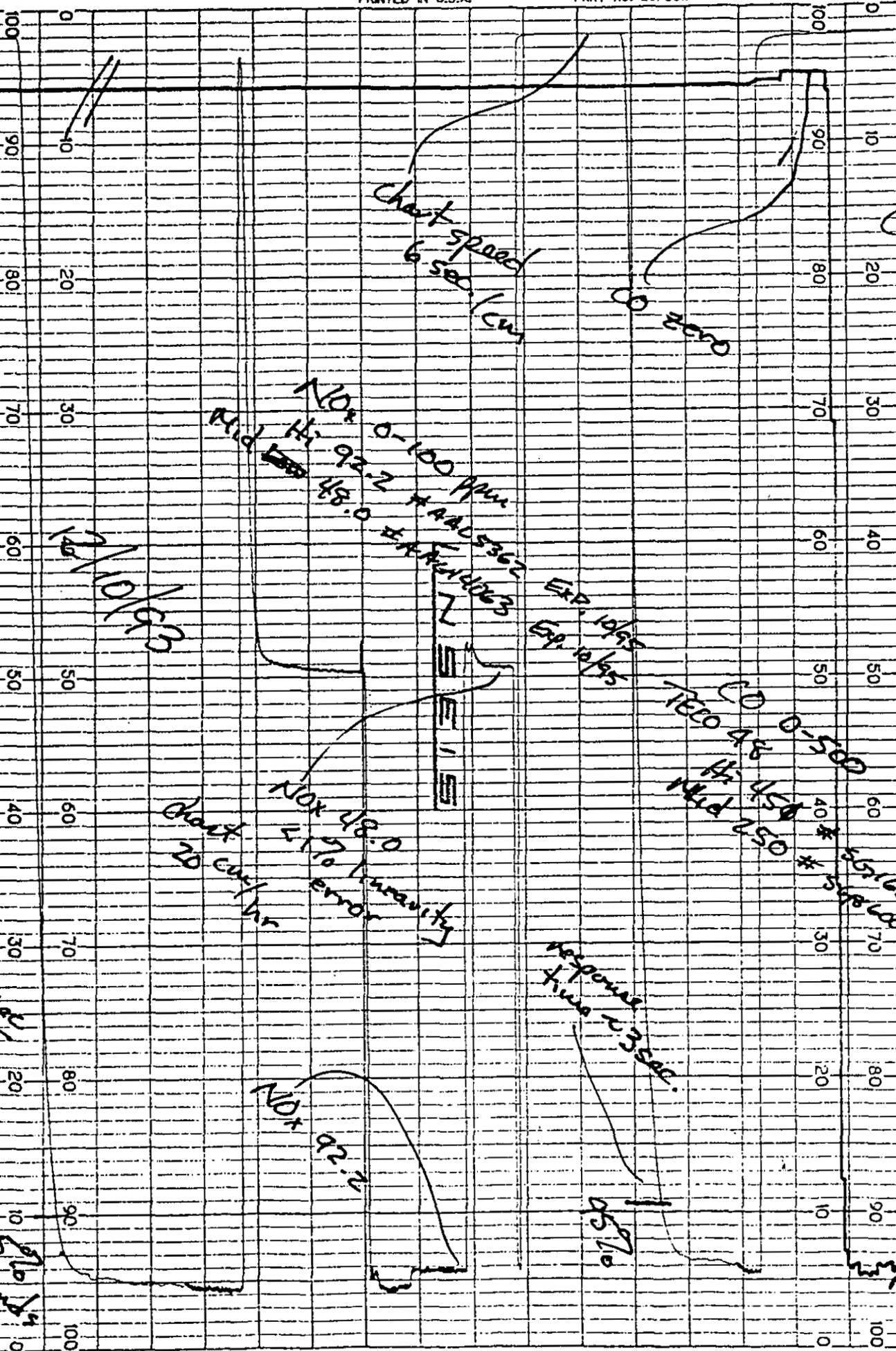




20/01/51

01 20 40 60 80 100





NOx 0-100 ppm  
 Mid Hi 92.2 + AAD 5362  
 48.0 ± 1% linearity error

CO 0-500  
 TECO 48 0-500  
 Hi 450  
 Mid 250  
 # 5362  
 # 5362

Chart 20 cm/hr  
 NOx 48.0  
 +/- 1% linearity error

Response time  $\approx$  3 sec.

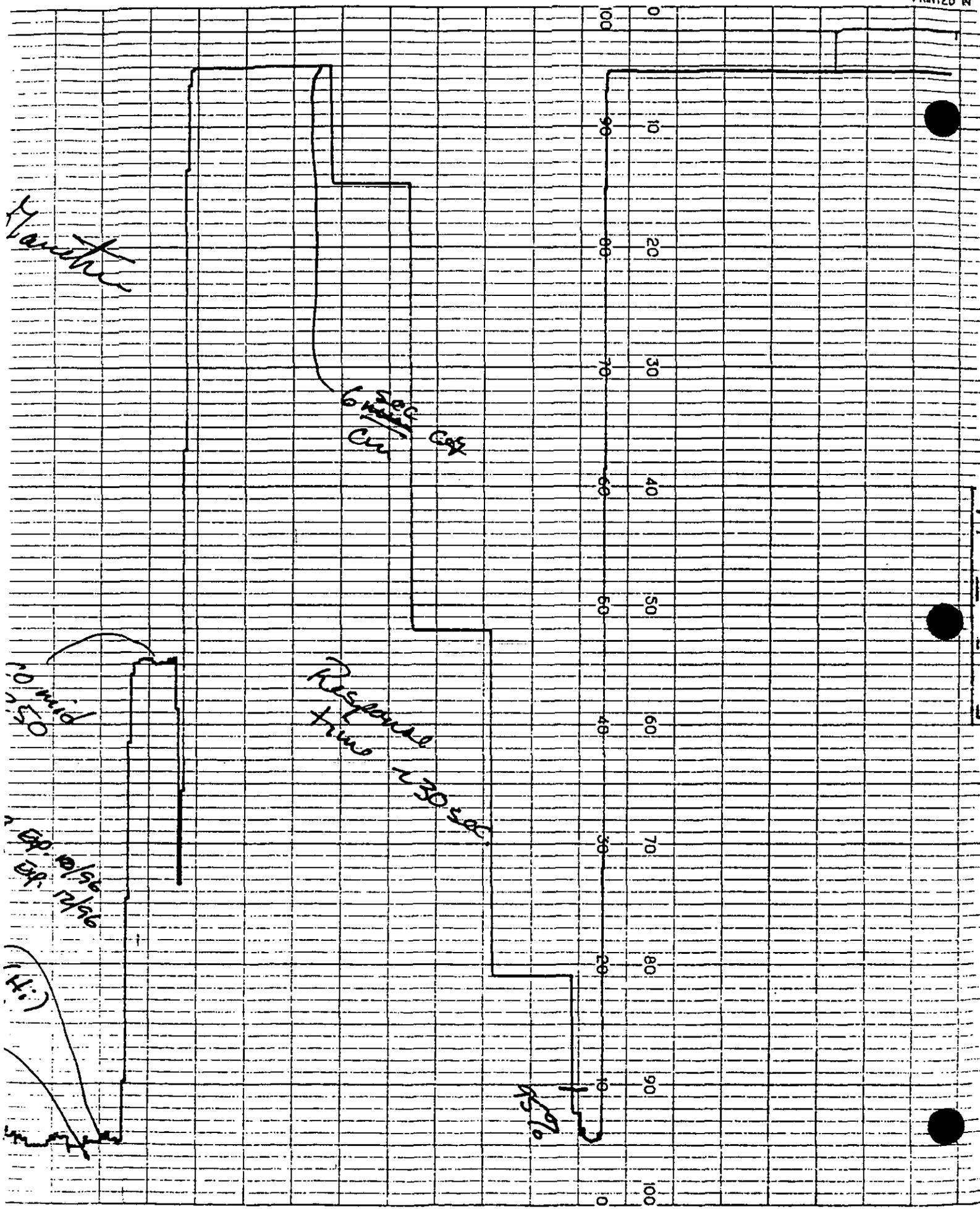
NOx 92.2

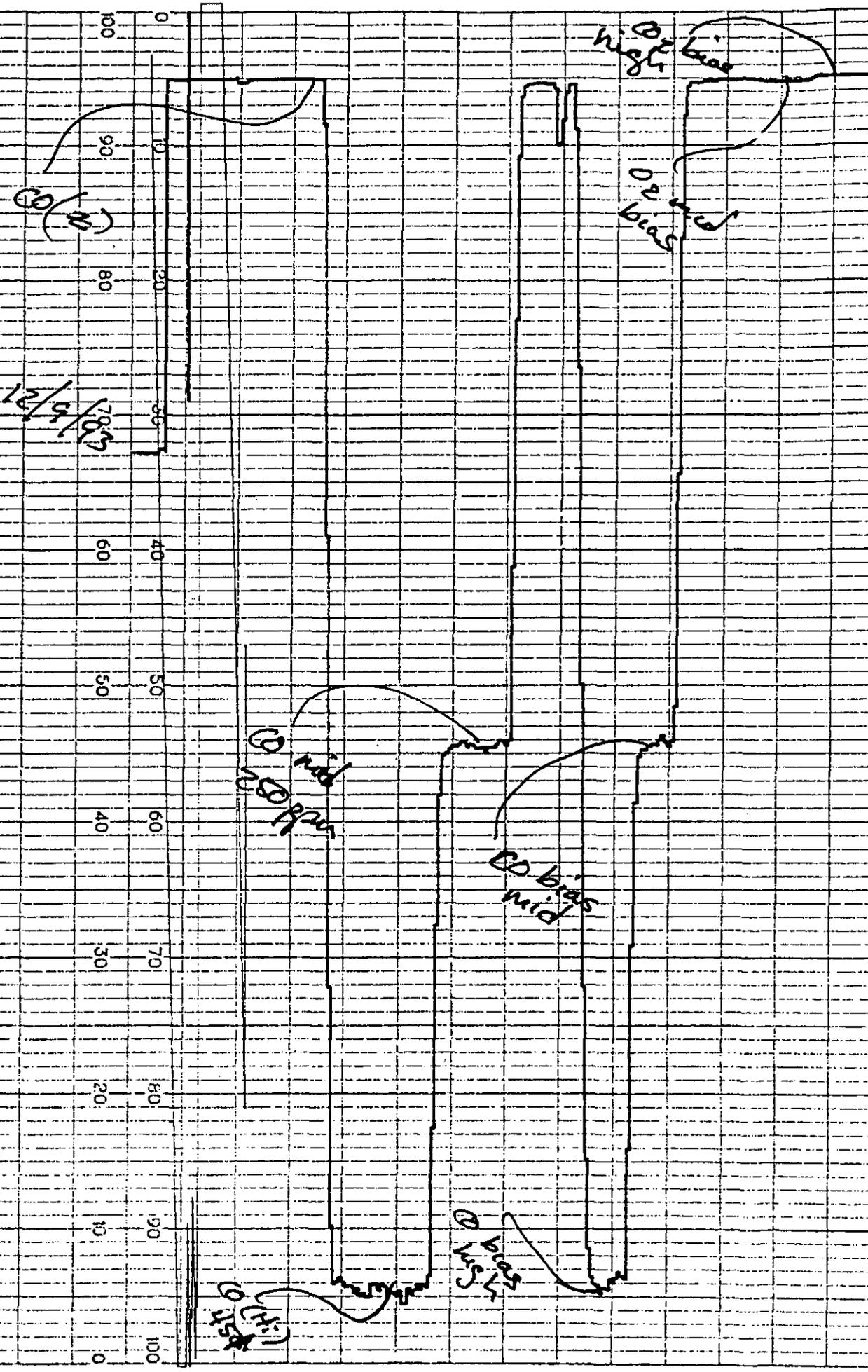
12/10/65

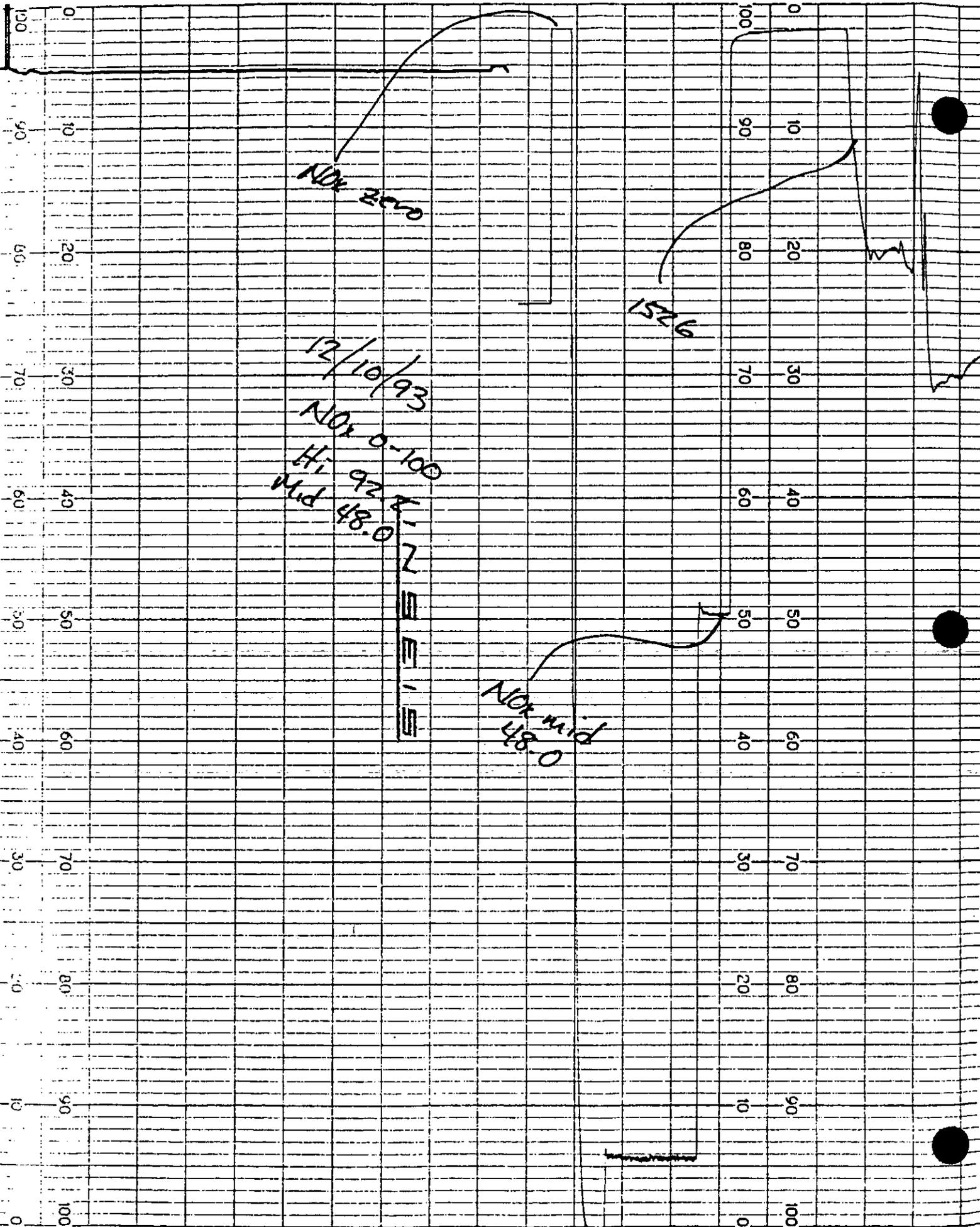
11

cm/hr

Response time  
 1-2 sec







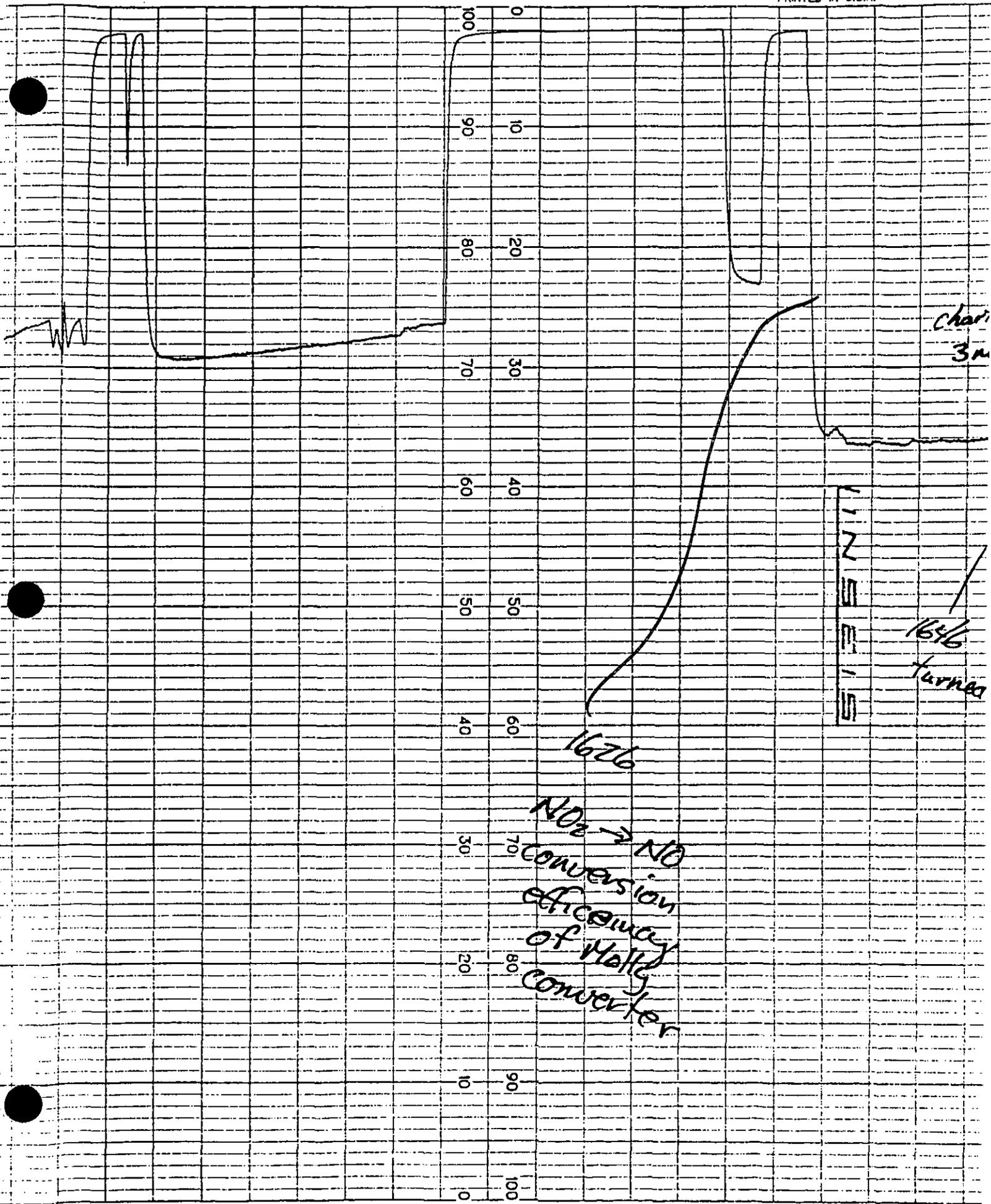
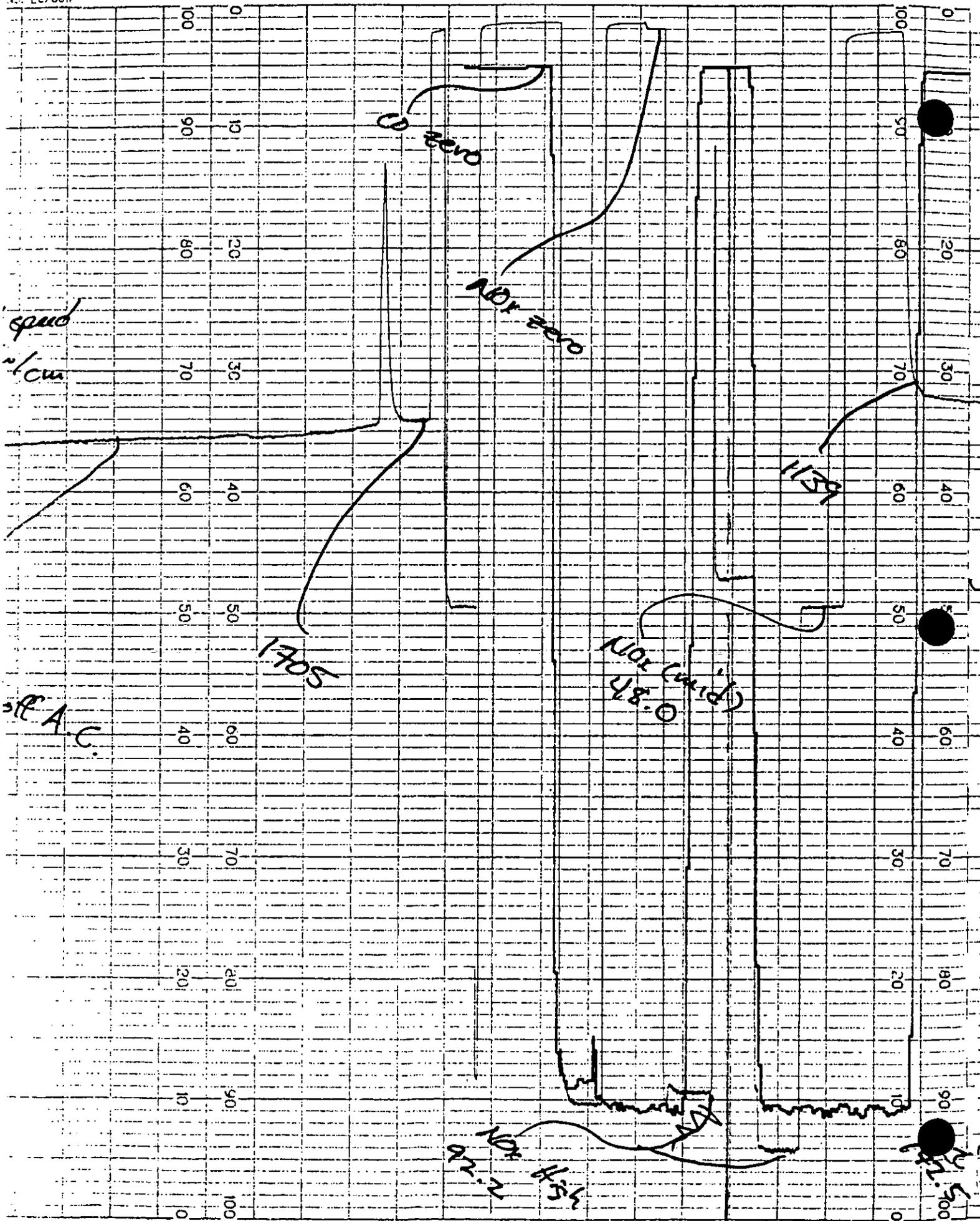
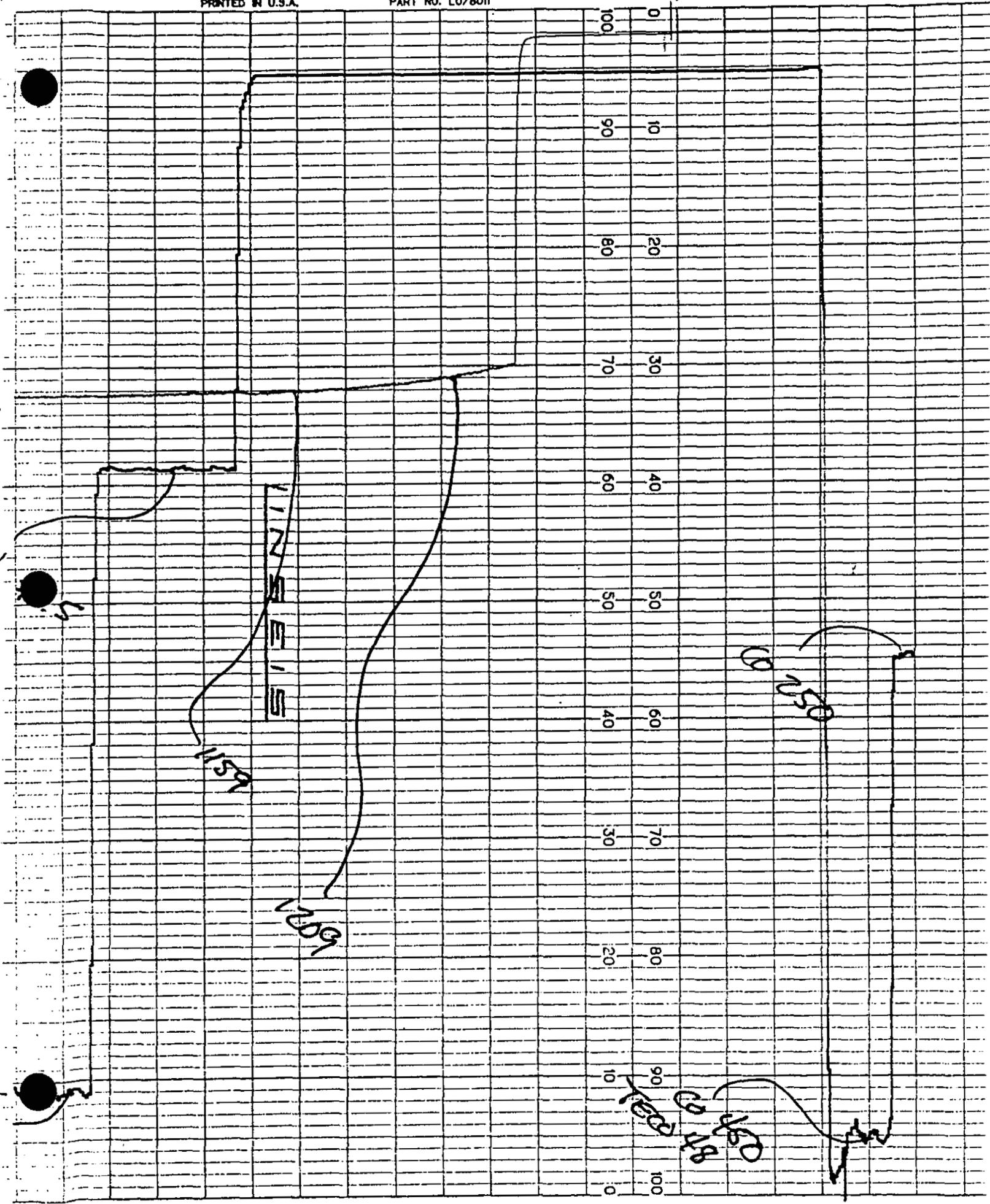
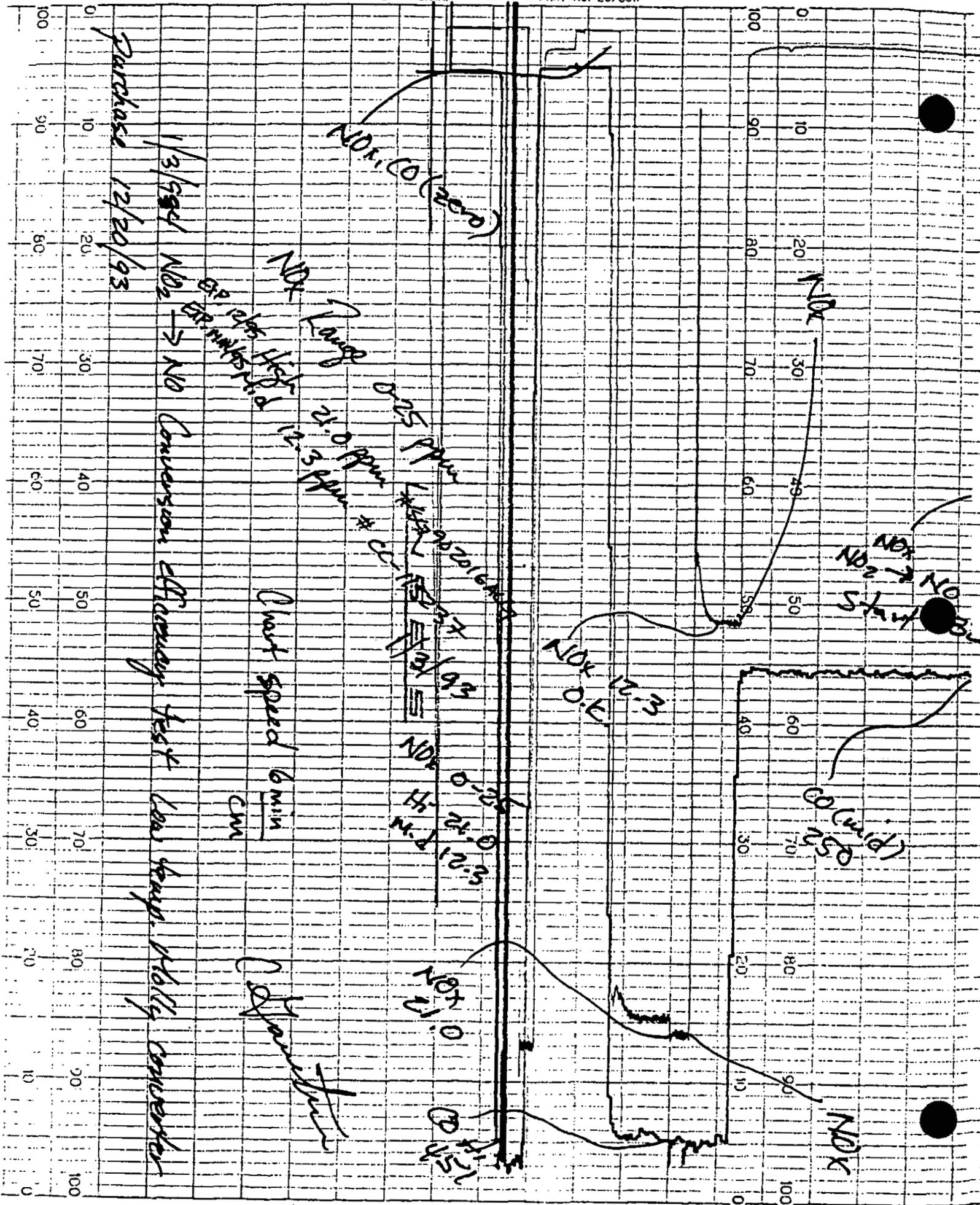
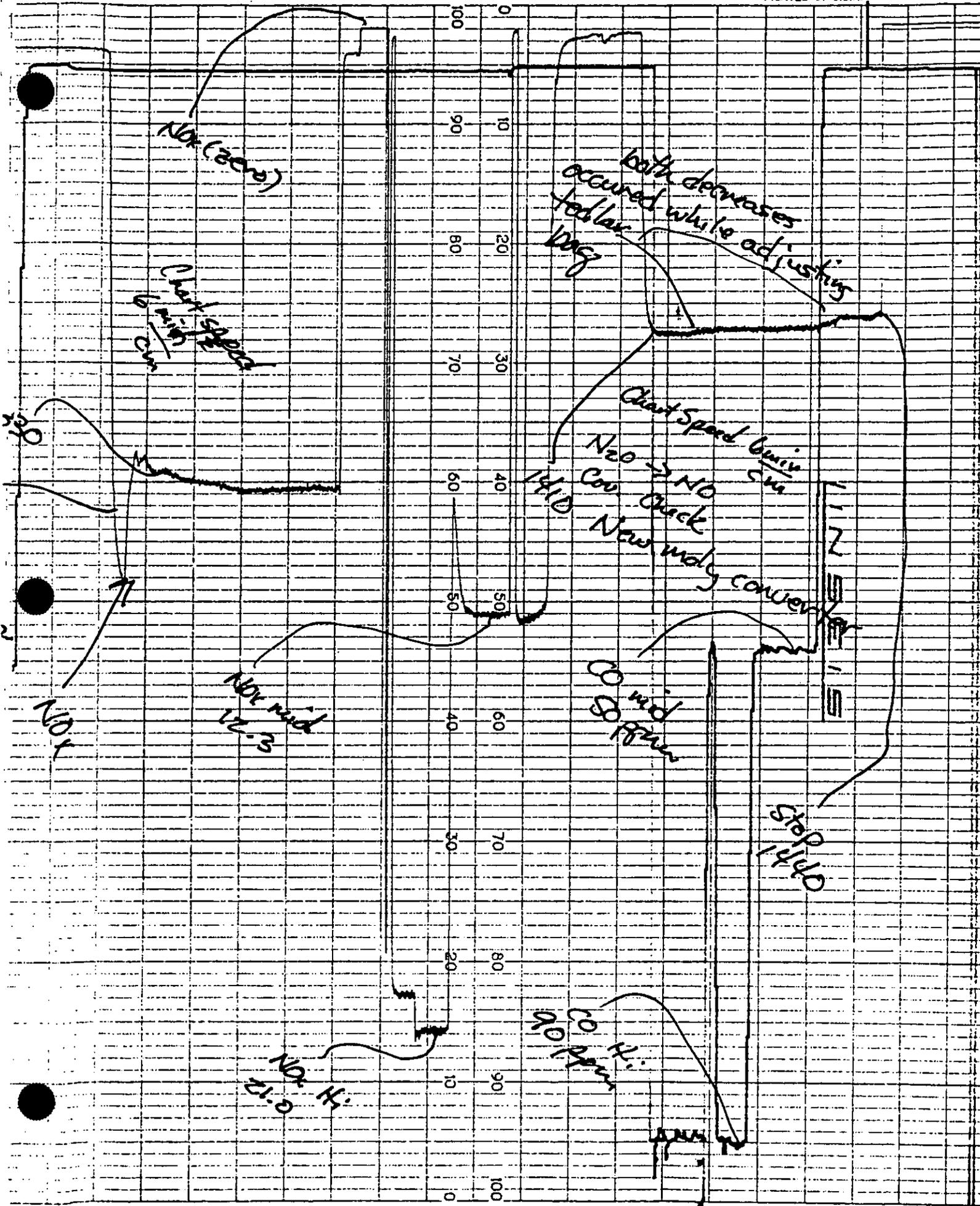


Chart 3m









No. 100

No. 90

both decreases occurred while adjusting

Chart Speed Curve

No. 3 NO COOL Check New mold convert

COOL mid

Drift stops

COOL Hi

No. 11 0-12

No. 12 mid

No. 100

No. 90

0  
10  
20  
30  
40  
50  
60  
70  
80  
90  
100

100  
90  
80  
70  
60  
50  
40  
30  
20  
10  
0

D-102

**APPENDIX D-6**  
**DATA LOGGER OUTPUT**

D-104

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
628	8.1	0.1	-1.1	-0.9	-0.5
629	8.1	0.1	-1.1	-1.5	-0.8
630	8.1	0.1	-1.1	-1.5	-0.8
631	8.1	0.1	-1.1	-1.5	-0.8
632	8.1	0.1	-1.1	-1.5	-1.0
633	8.1	0.1	-1.1	-1.5	-0.9
634	5.5	7.6	30.3	34.7	34.7
635	3.9	9.5	37.3	39.2	92.9
636	1.9	2.7	8.8	9.3	79.6
637	0.1	-0.0	-1.1	-1.0	-1.1
638	0.1	-0.0	-1.1	-1.0	-1.5
639	0.1	-0.1	-1.1	-1.0	-1.5
640	0.1	-0.1	-1.1	-1.0	-1.6
641	0.0	-0.1	-1.2	-1.0	-1.6
642	0.0	-0.1	-1.2	-1.0	-1.5
643	0.0	-0.1	-1.1	-0.9	-1.5
644	0.8	2.6	3.7	3.5	7.9
645	8.5	17.4	74.9	108.7	386.7
646	9.0	17.6	92.5	138.9	443.9
647	9.0	17.7	92.8	139.7	444.5
648	9.0	17.7	92.8	139.9	443.5
649	9.0	17.7	92.9	140.0	444.3
650	9.0	17.7	93.0	140.1	445.8
651	9.0	17.7	93.1	140.3	453.7
652	9.0	17.7	93.2	140.4	450.4
653	8.5	15.0	75.3	111.8	444.9
654	8.2	9.7	46.3	65.3	270.5
655	9.0	9.7	47.9	72.2	250.4
656	9.0	9.7	48.0	72.4	250.8
657	9.1	9.7	48.2	72.9	250.0
658	8.2	7.4	35.1	53.4	244.7
659	0.5	-0.0	-0.7	-0.6	28.7
700	0.1	-0.0	-0.7	-0.6	-1.4
701	0.0	-0.0	-0.7	-0.6	-1.5
702	0.0	-0.0	-0.7	-0.6	-1.6
703	0.0	-0.0	-0.8	-0.6	-1.5
704	2.7	7.7	40.6	40.8	113.1
705	4.1	9.7	48.3	51.6	250.3
706	4.2	9.7	48.3	51.7	249.8
707	4.2	9.7	48.3	51.7	251.4
708	6.5	15.0	77.9	99.5	324.8
709	9.0	17.7	93.3	140.5	454.6
710	9.1	17.7	93.7	141.8	453.1
711	9.1	17.7	93.7	141.9	453.1
712	9.1	17.6	93.7	142.0	452.7
713	9.1	17.7	93.8	142.1	452.5

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
714	9.1	17.7	93.8	142.1	452.2
715	9.1	17.7	93.8	142.2	452.1
716	9.1	17.7	93.8	142.2	451.7
717	9.1	17.7	46.0	69.6	218.7
718	9.1	17.7	-0.4	-0.6	-0.7
719	9.1	17.7	-0.6	-0.9	-0.5
720	9.0	17.3	-0.6	-0.9	-0.4
721	9.0	7.8	-0.7	-1.0	-0.5
722	9.0	0.7	-0.7	-1.0	-0.5
723	9.0	0.5	-0.7	-1.0	-0.4
724	9.0	0.4	-0.6	-1.0	-0.5
725	9.0	0.4	-0.7	-1.0	-0.4
726	9.0	0.4	-0.7	-1.1	-0.4
727	9.0	0.2	-0.7	-1.0	-0.5
728	9.0	0.2	-0.7	-1.0	-0.6
729	9.0	0.1	-0.7	-1.0	-0.6
730	9.0	0.1	-0.7	-1.1	-0.4
731	9.0	0.1	-0.7	-1.0	-0.5
732	9.0	0.1	-0.7	-1.1	-0.5
733	9.0	0.1	-0.7	-1.1	-0.5
734	9.1	0.1	-0.7	-1.0	-0.5
735	9.1	0.1	-0.7	-1.1	-0.4
736	9.1	0.1	-0.7	-1.1	-0.4
737	9.2	0.2	-0.7	-1.1	-0.4
738	9.4	0.2	-0.7	-1.1	-0.5
739	9.8	0.1	-0.7	-1.1	-0.6
740	10.2	0.2	-0.7	-1.2	-0.6
741	10.5	0.3	-0.7	-1.2	-0.5
742	11.0	0.1	-0.7	-1.3	-0.4
743	11.7	0.1	-0.7	-1.4	-0.5
744	12.6	0.1	-0.7	-1.5	-0.6
745	13.3	0.1	-0.7	-1.7	-0.5
746	13.9	0.1	-0.7	-1.9	-0.4
747	14.3	0.1	-0.7	-1.9	-0.5
748	15.5	0.1	-0.7	-2.5	-0.5
749	20.1	0.2	-0.1	-2.6	-0.5
750	20.4	0.1	-0.6	-21.3	0.4
751	17.4	8.2	42.1	362.1	64.7
752	8.2	17.7	92.8	134.6	439.1
753	9.1	17.7	93.8	142.4	451.2
754	9.1	17.7	93.8	142.3	449.4
755	9.1	17.7	93.8	142.3	452.2
756	9.1	17.7	93.8	142.3	450.6
757	13.9	1.6	9.9	15.3	160.2
758	19.6	0.2	-0.1	-2.9	-0.5
759	20.3	0.1	-0.4	-13.1	-0.4

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
800	18.5	0.1	-0.4	-8.0	0.5
801	1.5	0.0	-0.7	-0.6	-1.0
802	0.1	0.0	-0.7	-0.6	-1.2
803	0.1	0.0	-0.7	-0.6	-1.1
804	0.1	0.0	-0.7	-0.6	-1.5
805	0.1	-0.0	-0.7	-0.6	-1.2
806	0.0	0.0	-0.7	-0.6	-1.3
807	1.4	1.6	-0.7	-0.7	-1.1
808	0.6	9.5	-0.7	-0.6	-1.6
809	0.1	9.6	-0.7	-0.6	-1.6
810	0.5	7.0	-0.7	-0.6	-1.6
811	3.9	0.1	-0.7	-0.8	-1.4
812	4.1	0.0	-0.7	-0.8	-1.4
813	4.1	0.0	0.6	-0.6	-1.5
814	1.1	0.0	45.9	41.8	-1.4
815	0.1	0.0	46.1	39.7	-1.3
816	0.1	0.0	-0.1	-0.1	159.3
817	0.0	0.0	-0.6	-0.5	248.9
818	0.0	0.0	-0.7	-0.6	250.3
819	2.4	0.1	0.2	0.8	238.4
820	17.9	1.1	3.5	24.5	46.4
821	18.7	1.2	4.7	39.2	12.2
822	17.6	1.6	6.7	36.9	31.2
823	18.1	1.4	5.2	33.6	21.9
824	11.7	6.7	33.4	87.8	75.8
825	3.5	9.5	46.3	47.7	193.7
826	3.3	9.7	46.7	47.5	210.1
827	3.3	9.7	46.8	47.6	242.7
828	3.3	9.7	46.9	47.7	200.4
829	3.3	9.7	47.3	48.0	182.6
830	3.3	9.7	46.2	46.9	244.3
831	3.2	9.7	46.9	47.6	206.6
832	3.3	9.7	47.1	47.8	179.6
833	3.3	9.7	46.7	47.5	227.4
834	3.2	9.8	46.6	47.2	261.8
835	3.2	9.7	46.5	47.1	192.5
836	3.2	9.7	46.5	47.1	243.9
837	3.3	9.8	46.9	47.5	225.0
838	3.3	9.7	47.1	47.8	235.1
839	3.3	9.7	46.9	47.6	249.9
840	3.3	9.7	46.8	47.5	218.3
841	3.3	9.7	46.7	47.4	231.9
842	3.3	9.7	46.9	47.6	202.6
843	3.3	9.7	47.0	47.7	204.7
844	3.3	9.7	47.1	47.8	194.8
845	3.3	9.7	47.3	48.1	228.8

zero bias

mid bias

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
846	3.3	9.7	47.1	47.9	222.1
847	3.3	9.8	46.9	47.6	203.6
848	3.3	9.7	46.9	47.6	276.0
849	3.2	9.7	47.0	47.7	234.2
850	3.3	9.7	47.2	47.9	207.6
851	3.3	9.7	46.8	47.6	228.6
852	3.3	9.3	46.7	47.4	232.6
853	3.3	9.7	47.1	47.8	214.8
854	3.3	9.7	46.9	47.6	192.4
855	3.3	9.7	47.0	47.7	219.2
856	3.2	9.8	47.0	47.6	203.4
857	3.3	9.7	46.9	47.6	232.6
858	3.2	9.8	46.7	47.3	226.7
859	3.2	9.7	47.4	48.1	225.6
900	10.6	3.9	16.9	25.3	130.7
901	17.9	1.6	6.2	37.9	27.9
902	17.8	1.8	7.2	42.3	32.4
903	17.8	1.5	5.8	32.7	29.7
904	18.4	1.3	4.9	35.6	26.2
905	12.1	1.1	4.0	13.0	16.6
906	7.2	1.5	62.1	81.1	32.5
907	7.5	1.2	93.0	124.0	18.5
908	7.4	1.1	55.4	73.2	19.4
909	7.7	0.7	-0.5	-0.7	14.8
910	7.7	0.9	1.3	1.7	11.1
911	7.4	1.2	4.5	6.0	13.7
912	7.5	1.1	3.8	5.2	17.6
913	7.5	1.2	5.1	6.8	15.8
914	2.8	9.1	46.2	46.6	106.5
908	1.3	9.4	47.5	43.4	206.1
909	2.0	9.6	47.9	45.3	241.2
910	3.3	9.6	48.4	49.4	229.2
911	3.3	9.7	49.2	50.1	207.5
912	3.3	9.7	49.5	50.3	202.4
913	3.3	9.4	49.5	50.4	188.0
914	3.3	9.7	49.4	50.1	228.6
915	3.3	9.6	50.2	51.0	215.8
916	3.3	9.7	50.5	51.3	189.4
917	3.3	9.7	50.7	51.4	204.2
918	3.2	9.7	50.5	51.2	199.7
919	3.2	9.7	50.4	51.1	182.7
920	3.2	9.8	50.4	51.0	208.8
921	3.2	9.8	51.2	51.7	210.5
922	3.2	9.8	52.0	52.5	206.6
923	3.2	9.8	51.5	52.1	229.8
924	3.2	9.8	51.2	51.8	249.1

Start  
FGD ON

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
925	3.2	9.8	51.5	52.1	233.3
926	3.2	9.8	51.5	52.1	207.0
927	3.2	9.8	51.4	52.0	214.4
928	3.2	9.7	52.0	52.7	224.1
929	3.2	9.8	51.9	52.4	236.5
930	3.2	9.8	52.2	52.7	232.0
931	3.2	9.8	52.4	53.0	239.2
932	3.2	9.8	52.2	52.7	237.8
933	3.2	9.8	52.4	53.0	200.1
934	3.2	9.8	52.2	52.8	220.0
935	3.2	9.8	52.1	52.6	253.8
936	3.2	9.7	52.6	53.1	217.4
937	3.2	9.8	53.2	53.7	196.1
938	3.2	9.8	52.8	53.3	190.5
939	3.2	9.8	52.3	52.9	208.2
940	3.2	9.8	51.9	52.4	200.3
941	3.2	9.8	51.5	52.0	247.8
942	3.2	9.8	51.9	52.4	253.2
943	3.2	9.8	52.3	52.8	213.4
944	3.2	9.8	52.3	52.9	193.8
945	3.1	9.8	52.4	52.9	189.5
946	3.2	9.8	52.5	53.1	188.4
947	3.2	9.8	51.9	52.3	270.5
948	3.2	9.8	52.1	52.6	218.2
949	3.2	9.8	52.2	52.7	201.7
950	3.2	9.8	52.0	52.4	199.1
951	3.2	9.8	51.8	52.2	210.4
952	3.2	9.8	52.0	52.5	195.8
953	3.1	9.8	51.8	52.2	257.2
954	3.1	9.8	52.0	52.4	240.9
955	3.1	9.8	51.7	52.2	220.3
956	3.1	9.8	51.9	52.3	170.5
957	3.1	9.8	51.7	52.0	210.9
958	3.1	9.8	51.4	51.7	238.5
959	3.1	9.8	52.2	52.5	204.1
1000	3.1	9.8	51.9	52.2	249.7
1001	3.1	9.8	52.4	52.8	214.0
1002	3.1	9.8	52.0	52.4	225.2
1003	3.1	9.8	52.2	52.6	241.9
1004	3.2	9.8	52.6	53.1	198.2
1005	3.2	9.8	52.5	53.0	188.6
1006	3.2	9.8	52.4	52.9	186.7
1007	3.1	9.8	51.9	52.3	158.0
1008	3.2	9.8	52.1	52.6	190.0
1009	3.1	9.8	52.0	52.3	182.3
1010	3.1	9.8	51.9	52.1	198.0

full load, 22 march, 1994

END  
FGR ON

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1011	3.1	9.8	52.0	52.3	203.8
1012	3.1	9.9	51.7	51.9	196.9
1013	3.1	9.7	51.9	52.2	193.2
1014	3.1 / 3.2	9.8 / 9.8	51.6 / 51.9	51.9	246.1 / 213.4 ← avgs
1015	3.1	9.8	52.2 / 51.9	52.6	207.8
1016	3.1	9.6	52.1	52.3	209.0
1017	3.2	9.2	47.8	48.1	164.5
1018	11.3	0.2	0.6	1.3	41.8
1019	0.4	0.1	0.0	0.0	1.0
1020	0.0	0.1	-0.1	-0.1	-1.1
1021	0.0	0.1	-0.1	-0.1	-1.1
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1022	3.3	0.1	-0.1	-0.1	-1.0
1023	4.6	0.0	-0.2	-0.2	-0.5
1024	4.1	0.0	-0.2	-0.2	-1.2
1025	3.6	2.9	-0.2	-0.3	-1.3
1026	0.2	9.6	-0.3	-0.2	-1.7
1027	0.0	9.6	-0.3	-0.2	-1.7
1028	0.0	3.8	29.7	25.5	-1.6
1029	-0.0	0.1	47.1	40.3	-1.1
1030	-0.0	0.0	23.7	20.3	40.5
1031	-0.0	0.1	-0.2	-0.2	243.9
1032	-0.0	0.0	-0.3	-0.2	250.8
1033	-0.0	-0.1	-0.3	-0.2	229.4
1034	3.3	0.1	-0.2	-0.2	91.9
1035	16.9	0.1	-0.2	-1.1	7.0
1036	2.2	-0.1	-0.4	-0.4	-0.4
1037	0.1	-0.2	-0.4	-0.4	-1.6
1038	-0.0	-0.0	-0.4	-0.4	-1.5
1039	-0.0	-0.1	-0.4	-0.4	-1.6
<hr/>					
1040	2.2	6.9	35.4	35.2	91.9
1041	4.1	9.7	48.0	51.1	251.0
1042	4.1	9.7	48.0	51.2	250.2
<hr/>					
1043	6.8	15.8	75.2	98.2	348.3
1044	9.0	17.7	92.5	138.7	454.3
1045	9.0	17.7	92.8	139.8	457.1
1046	9.0	17.7	92.8	139.9	454.8
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1047	13.3	7.1	31.2	51.8	306.3
1048	19.2	0.7	2.4	25.3	12.8
1049	19.6	0.5	1.7	22.5	8.3
1050	13.8	5.3	27.5	100.2	48.5
1051	3.5	9.7	44.8	46.2	191.5
1052	3.2	9.8	44.5	45.0	238.3
1053	3.2	9.8	44.5	44.9	207.1
1054	3.2	9.8	44.5	44.9	176.6
1055	3.1	9.8	44.1	44.4	159.7
1056	3.1	9.8	44.0	44.4	185.3

zero bias

mid bias

zero

mid

high

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1057	3.1	9.8	43.8	44.0	255.1
1058	3.1	9.8	44.1	44.4	194.3
1059	3.1	9.8	44.5	44.8	223.4
1100	3.1	9.7	44.3	44.6	210.0
1101	3.1	9.7	44.2	44.5	231.9
1102	3.1	9.8	44.5	44.8	186.9
1103	3.1	9.8	44.1	44.4	208.1
1104	3.1	9.8	44.4	44.7	228.7
1105	3.1	9.8	44.9	45.2	197.3
1106	3.1	9.8	44.8	45.1	200.2
1107	3.1	9.8	44.7	44.9	212.5
1108	3.1	9.8	44.5	44.7	222.7
1109	3.1	9.8	44.5	44.7	227.0
1110	3.1	9.8	44.5	44.7	213.2
1111	3.1	9.8	44.5	44.7	206.5
1112	3.1	9.9	44.4	44.6	271.5
1113	3.1	9.8	44.4	44.6	231.6
1114	3.1	9.8	44.2	44.5	207.7
1115	3.1	9.8	44.3	44.5	235.8
1116	3.1	9.8	44.4	44.6	239.8
1117	3.1	9.9	44.5	44.7	220.2
1118	3.1	9.9	44.5	44.7	190.7
1119	3.1	9.8	44.3	44.5	229.8
1120	3.1	9.8	44.2	44.4	229.9
1121	3.1	9.8	44.4	44.8	189.4
1122	3.1	9.8	44.6	44.9	177.2
1123	3.1	9.8	44.6	44.9	213.3
1124	3.1	9.8	44.6	44.9	210.7
1125	3.1	9.8	44.2	44.5	212.8
1126	3.1	9.8	44.3	44.6	215.9
1127	3.1	9.8	44.5	44.8	230.3
1128	3.1	9.8	44.6	44.8	205.8
1129	3.1	9.8	44.3	44.6	195.9
1130	3.1	9.8	44.4	44.7	175.2
1131	3.1	9.8	44.5	44.8	181.1
1132	3.1	9.8	44.5	44.8	194.9
1133	3.1	9.9	44.5	44.7	215.5
1134	3.1	9.9	44.6	44.8	212.1
1135	3.1	9.8	44.2	44.5	221.7
1136	3.1	9.8	44.2	44.4	254.2
1137	3.1	9.8	44.4	44.7	220.5
1138	3.1	9.8	44.5	44.8	197.6
1139	3.1	9.8	44.3	44.5	222.1
1140	3.1	9.8	44.1	44.2	237.1
1141	3.1	9.8	44.3	44.6	201.1
1142	3.1	9.8	44.5	44.7	211.8

START  
GR & UREA  
Run 1

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1143	3.1	9.8	44.6	45.0	203.2
1144	3.1	9.8	44.6	44.9	211.3
1145	3.1	9.9	44.2	44.4	242.0
1146	3.1	9.8	44.6	44.8	262.8
1147	3.1	9.8	44.9	45.2	218.5
1148	3.1	9.8	44.6	44.9	247.3
1149	3.1	9.8	44.5	44.8	189.0
1150	3.1	9.8	44.5	44.7	196.7
1151	3.1	9.8	44.4	44.7	227.2
1152	3.1	9.8	44.4	44.7	231.1
1153	3.1	9.8	44.6	44.8	232.1
1154	3.1	9.8	44.3	44.6	190.4
1155	3.1	9.8	44.8	45.2	206.8
1156	3.1	9.8	44.7	45.1	222.3
1157	3.1	9.8	45.0	45.3	205.2
1158	3.1	9.8	44.6	44.9	239.0
1159	3.1	9.7	44.7	45.1	197.5
1200	3.1	9.8	44.8	45.1	204.7
1201	3.1	9.7	44.8	45.1	213.0
1202	3.1	9.8	44.9	45.3	214.8
1203	3.1	9.8	44.6	44.9	183.4
1204	3.1	9.8	45.0	45.4	207.5
1205	3.2	9.6	41.4	41.8	175.9
1206	16.6	0.7	0.9	2.1	51.1
1207	20.3	0.1	-0.0	-0.4	-0.2
1208	20.4	0.1	-0.1	-2.2	-0.4
1209	14.8	0.1	-0.2	-3.2	3.6
1210	0.5	-0.0	-0.2	-0.2	0.4
1211	0.1	-0.0	-0.2	-0.2	-1.1
1212	0.0	-0.1	-0.2	-0.1	-1.2
1213	0.0	0.0	-0.2	-0.2	-1.1
1214	0.3	0.0	-0.2	-0.1	-1.0
1215	3.8	0.0	-0.2	-0.2	-0.8
1216	4.1	0.0	-0.2	-0.2	-1.2
1217	4.1	0.0	-0.2	-0.2	-1.2
1218	2.4	5.9	-0.2	-0.2	-1.4
1219	0.1	9.6	-0.2	-0.2	-1.6
1220	0.0	8.6	5.3	4.5	-1.5
1221	-0.0	0.2	46.5	39.8	-1.3
1222	-0.0	0.0	47.0	40.2	-1.1
1223	-0.0	0.0	36.9	31.5	3.2
1224	-0.0	0.0	0.1	0.1	213.0
1225	-0.0	-0.2	-0.1	-0.1	250.9
1226	-0.0	-0.0	-0.1	-0.1	252.2
1227	-0.0	-0.1	-0.2	-0.1	251.4
1228	3.6	0.0	-0.1	-0.1	153.8

END

L

3.1

9.8

44.5

215.3

← Averages

zero bias

mid bias

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1229	17.8	0.0	-0.0	-0.2	18.7
1230	9.8	0.0	-0.1	0.0	58.3
1231	0.5	-0.1	-0.2	-0.2	1.9
1232	0.0	-0.1	-0.2	-0.2	-1.6
1233	-0.0	-0.1	-0.2	-0.2	-1.6
1234	-0.0	-0.1	-0.2	-0.2	-1.6
1235	1.0	4.0	20.4	19.4	25.9
1236	4.0	9.7	47.8	50.7	242.1
1237	4.1	9.7	47.8	51.1	252.9
1238	4.2	9.7	47.8	51.1	252.1
1239	4.2	9.7	47.8	51.1	252.9
1240	5.3	13.1	61.4	71.9	288.3
1241	8.9	17.6	90.8	135.6	452.4
1242	9.1	17.6	92.4	139.6	455.5
1243	9.1	17.6	92.5	139.8	456.4
1244	9.1	17.7	92.4	139.9	457.0
1245	12.7	8.6	38.5	59.2	338.4
1246	20.1	0.2	0.7	18.0	4.9
1247	20.3	0.2	0.6	16.8	2.5
1248	20.4	0.1	-0.0	-0.5	1.2
1249	20.5	0.1	0.0	0.0	-0.7
1250	20.3	0.3	0.9	25.6	1.4
1251	20.4	0.1	0.0	1.1	2.7
1252	20.5	0.1	0.2	9.1	-0.1
1253	20.3	0.2	0.5	15.6	2.7
1254	20.3	0.2	0.5	13.7	3.1
1255	18.1	2.9	14.2	124.6	15.8
1256	4.1	9.7	44.1	47.6	245.5
1257	3.2	9.8	44.3	44.9	224.3
1258	3.2	9.8	44.6	45.1	222.2
1259	3.2	9.8	44.4	44.8	224.0
1300	3.2	9.6	44.7	45.1	183.1
1301	3.2	9.8	44.8	45.2	208.2
1302	3.1	9.4	44.3	44.6	255.4
1303	3.1	9.7	44.5	44.9	244.9
1304	3.1	9.8	44.4	44.8	207.2
1305	3.2	9.8	44.5	44.9	204.0
1306	3.1	9.8	44.5	44.9	235.7
1307	3.2	9.8	44.5	44.9	230.8
1308	3.1	9.8	44.4	44.7	221.2
1309	3.2	9.8	44.5	45.0	183.9
1310	3.2	9.8	44.6	45.0	192.3
1311	3.1	9.8	44.3	44.7	208.8
1312	3.1	9.8	44.3	44.6	234.3
1313	3.1	9.8	44.6	45.0	185.9
1314	3.1	9.8	44.5	44.8	240.7

Zero

mid

high

START FGR+  
 LEA ON;  
 UN #2

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1315	3.1	9.8	44.5	44.8	224.5
1316	3.1	9.8	44.4	44.7	209.8
1317	3.2	9.8	44.6	45.0	204.1
1318	3.1	9.8	44.5	44.8	223.2
1319	3.1	9.8	44.8	45.2	223.4
1320	3.2	9.8	44.9	45.3	181.6
1321	3.1	9.8	44.6	45.0	187.4
1322	3.1	9.8	44.6	44.9	180.9
1323	3.2	9.8	44.7	45.1	182.4
1324	3.2	9.8	44.3	44.7	192.6
1325	3.2	9.8	44.4	44.8	189.4
1326	3.1	9.8	44.2	44.6	225.9
1327	3.1	9.8	44.5	44.8	226.2
1328	3.2	9.8	45.1	45.6	164.7
1329	3.2	9.8	44.9	45.3	204.6
1330	3.2	9.8	44.6	45.0	191.2
1331	3.1	9.8	44.8	45.2	211.7
1332	3.1	9.8	45.1	45.5	243.2
1333	3.2	9.8	45.2	45.7	176.0
1334	3.1	9.8	45.1	45.4	188.2
1335	3.1	9.8	44.6	45.0	241.0
1336	3.1	9.8	44.8	45.2	223.3
1337	3.2	9.8	45.1	45.5	208.2
1338	3.2	9.8	45.1	45.6	164.8
1339	3.2	9.8	45.0	45.4	183.2
1340	3.2	9.8	44.9	45.3	203.1
1341	3.2	9.8	44.7	45.1	196.7
1342	3.1	9.8	44.8	45.1	197.9
1343	3.1	9.8	44.6	44.9	214.2
1344	3.2	9.8	45.0	45.5	189.6
1345	3.2	9.8	44.7	45.1	207.6
1346	3.1	9.8	44.8	45.2	191.0
1347	3.1	9.8	44.8	45.1	188.4
1348	3.2	9.8	44.7	45.0	219.3
1349	3.1	9.8	44.6	45.0	218.0
1350	3.1	9.8	44.7	45.0	199.2
1351	3.2	9.8	44.9	45.3	207.3
1352	3.2	9.8	44.9	45.3	195.2
1353	3.1	9.8	44.3	44.7	176.7
1354	3.1	9.8	44.6	45.0	177.7
1355	3.1	9.9	44.5	44.8	213.8
1356	3.1	9.8	44.5	44.9	198.6
1357	3.1	9.8	44.4	44.7	182.3
1358	3.1	9.8	44.5	44.8	233.8
1359	3.2	9.8	45.1	45.5	176.7
1400	3.1/3.1	9.8/9.8	44.4/44.7	44.7	217.4/205.2

D L

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)	
1401	3.1	9.8	44.8	45.1	216.6	
1402	3.1	9.8	44.8	45.2	193.3	
1403	3.1	9.8	44.5	44.8	197.1	
1404	3.1	9.9	44.6	44.9	182.5	
1405	3.1	9.8	44.3	44.6	183.9	
1406	3.2	9.8	44.8	45.2	197.5	
1407	3.1	9.6	44.6	44.9	242.5	
1408	3.1	9.8	44.4	44.7	220.7	
1409	9.6	3.6	15.5	16.1	160.6	
1410	1.4	0.1	0.1	0.1	8.4	
1411	0.0	0.0	0.1	0.1	-1.1	
1412	0.0	0.0	0.0	0.0	-1.1	
1413	-0.0	-0.0	0.0	0.0	-1.2	zero bias
1414	2.9	-0.0	0.1	0.1	-0.7	
1415	4.1	-0.1	0.0	0.0	-1.2	
1416	4.1	0.0	0.0	0.0	-1.2	
1417	4.1	0.0	0.0	0.0	-1.2	
1418	4.1	0.0	0.0	0.0	-1.1	
1419	4.1	0.0	0.0	0.0	-1.2	
1420	2.0	6.9	0.0	0.0	-1.5	
1421	0.0	9.6	0.0	0.0	-1.7	
1422	-0.0	6.1	17.9	15.4	-1.6	
1423	-0.0	0.1	46.6	39.8	-1.1	
1424	-0.0	0.1	46.8	40.0	-1.2	
1425	-0.0	-0.0	27.5	23.5	26.4	
1426	-0.0	0.0	0.2	0.2	240.3	
1427	-0.0	-0.0	0.1	0.1	251.5	mid bias
1428	-0.0	-0.0	0.0	0.0	226.4	
1429	-0.1	-0.1	-0.0	-0.0	9.0	
1430	-0.1	-0.1	-0.0	-0.0	-1.6	
1431	0.5	2.8	14.7	13.5	9.6	zero
1432	4.0	9.7	47.7	50.3	230.3	
1433	4.1	9.7	47.6	50.9	251.8	
1434	4.2	9.7	47.7	50.9	252.6	mid
1435	5.4	13.0	62.1	73.0	288.1	
1436	9.0	17.6	90.5	135.6	453.4	
1437	9.1	17.6	92.0	139.2	458.2	
1438	9.1	17.6	92.1	139.5	457.6	
1439	9.1	17.7	92.0	139.5	456.0	high
1440	6.7	11.6	58.1	78.5	385.8	
1441	3.1	9.8	58.3	58.7	182.3	
1442	3.0	9.8	58.5	58.6	202.7	
1443	3.0	9.8	58.7	58.9	195.0	
1444	3.0	9.8	59.0	59.1	214.8	
1445	3.0	9.8	59.4	59.5	194.4	
1446	3.0	9.7	59.1	59.2	181.9	

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1447	3.0	9.8	58.9	58.9	208.6
1448	3.0	9.8	59.0	59.1	194.5
1449	3.0	9.8	59.4	59.5	174.0
1450	3.0	9.8	59.3	59.4	195.5
1451	3.0	9.8	59.5	59.5	184.2
1452	3.0	9.8	59.6	59.7	177.5
1453	3.0	9.2	60.2	60.3	180.6
1454	3.0	9.8	59.9	60.0	180.6
1455	3.0	9.8	59.1	59.1	258.0
1456	3.0	9.9	59.2	59.3	250.9
1457	3.0	9.9	59.3	59.3	184.8
1458	3.0	9.8	60.1	60.1	176.1
1459	3.0	9.7	59.7	59.8	162.7
1500	3.0	9.7	59.5	59.5	205.3
1501	3.0	9.9	59.2	59.3	197.0
1502	3.0	9.8	59.7	59.8	195.2
1503	3.0	9.8	59.9	59.9	178.4
1504	3.0	9.8	60.0	60.1	177.3
1505	3.0	9.9	59.9	59.9	206.0
1506	3.0	9.9	59.4	59.3	233.6
1507	3.0	9.9	59.7	59.7	202.8
1508	3.0	9.8	59.5	59.5	217.1
1509	3.0	9.9	59.6	59.6	229.4
1510	3.0	9.9	59.8	59.7	230.6
1511	3.0	9.8	59.8	59.8	193.5
1512	3.0	9.8	60.0	60.0	210.7
1513	3.0	9.8	60.1	60.1	165.5
1514	3.0	9.8	59.9	59.9	216.4
1515	3.0	9.8	60.1	60.1	190.1
1516	3.0	9.8	60.3	60.4	161.8
1517	3.0	9.8	59.9	59.9	182.4
1518	3.0	9.8	60.1	60.2	198.3
1519	3.0	9.8	60.2	60.2	191.6
1520	3.0	9.8	60.4	60.4	203.2
1521	3.0	9.9	60.2	60.2	214.4
1522	3.0	9.8	60.1	60.2	204.1
1523	3.0	9.9	59.9	59.9	233.1
1524	3.0	9.9	59.6	59.5	239.8
1525	3.0	9.9	60.2	60.2	233.3
1526	3.0	9.9	60.0	60.0	228.1
1527	3.0	9.8	60.0	60.0	221.4
1528	3.0	9.9	60.1	60.1	216.9
1529	3.0	9.9	60.3	60.3	198.4
1530	3.0	9.9	60.0	60.0	188.9
1531	3.0	9.8	60.2	60.2	194.4
1532	3.0	9.8	60.2	60.2	204.3

START  
BASELINE

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1533	3.0	9.8	60.2	60.2	183.1
1534	3.0	9.8	61.1	61.1	153.2
1535	3.0	9.8	60.9	61.1	161.1
1536	3.0	9.9	60.5	60.6	172.8
1537	3.0	9.8	60.4	60.4	190.3
1538	3.0	9.8	60.5	60.6	165.1
1539	3.0	9.8	60.5	60.5	194.7
1540	3.0	9.8	61.2	61.4	149.7
1541	3.0	9.8	60.6	60.7	186.2
1542	3.0	9.8	60.7	60.6	217.5
1543	3.0	9.8	60.6	60.6	188.6
1544	3.0	9.9	60.2	60.2	219.0
1545	3.0	9.8	60.2	60.2	193.2
1546	3.0	9.8	60.3	60.3	215.0
1547	3.0	9.9	60.3	60.3	215.6
1548	3.0	9.9	60.5	60.5	205.9
1549	3.0	9.9	61.1	61.2	158.6
1550	3.0	9.9	60.2	60.2	205.5
1551	3.0	9.8	60.6	60.6	189.4
1552	3.0	9.9	60.5	60.5	182.0
1553	3.0	9.9	60.5	60.5	192.1
1554	3.0	9.9	61.0	61.0	194.9
1555	3.0	9.9	61.0	61.0	210.1
1556	3.0	9.9	61.1	61.0	178.7
1557	3.0	9.8	61.0	61.1	171.0
1558	3.0	9.8	60.4	60.4	166.8
1559	3.0 / 3.0	9.9 / 9.8	59.9 / 60.2	59.9	208.1 / 197.2
1600	3.0	9.9	59.9	59.9	205.1
1601	3.0	9.8	60.5	60.5	175.2
1602	3.0	9.7	60.2	60.2	172.7
1603	3.1	9.6	54.4	54.4	157.1
1604	16.9	0.7	1.7	9.4	40.1
1605	20.5	0.1	0.6	22.3	-0.4
1606	20.5	0.1	0.5	22.4	-0.5
1607	20.6	0.1	0.4	20.8	-0.9
1608	19.5	0.1	0.3	15.0	0.6
1609	1.8	0.0	0.2	0.2	7.0
1610	0.1	0.0	0.2	0.1	-1.2
1611	0.0	0.0	0.1	0.1	-1.2
1612	0.0	0.0	0.1	0.1	-1.2
1613	-0.0	-0.0	0.1	0.1	-1.1
1614	0.2	0.0	0.1	0.1	-1.2
1615	3.8	-0.0	0.1	0.1	-0.6
1616	4.1	-0.0	0.1	0.1	-1.1
1617	4.1	0.0	0.0	0.1	-1.1
1618	2.8	4.9	0.1	0.1	-1.5

END

zero bias

aid bias

full load, 22 march, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1619	0.1	9.5	0.1	0.1	-1.8
1620	-0.0	9.6	0.1	0.1	-1.8
1621	-0.0	3.6	30.7	26.3	-1.6
1622	-0.0	0.1	46.8	40.0	-1.3
1623	-0.0	0.0	46.9	40.1	-1.3
1624	-0.0	0.0	13.0	11.1	93.6
1625	-0.0	-0.0	0.1	0.1	250.1
1626	-0.0	-0.0	0.1	0.1	251.9
1627	-0.0	-0.0	0.1	0.1	250.9
1628	1.8	0.0	0.1	0.1	150.8
1629	13.9	0.1	0.1	0.6	53.8
1630	7.4	0.0	0.0	0.3	14.8
1631	0.1	-0.0	-0.0	-0.0	-1.6
1632	-0.0	-0.0	-0.0	-0.0	-1.6
1633	-0.0	-0.2	-0.0	-0.0	-1.6
1634	-0.0	-0.1	-0.0	-0.0	-1.6
1635	2.7	8.1	41.0	41.1	126.7
1636	4.1	9.7	47.5	50.7	251.7
1637	5.4	13.3	62.7	73.9	289.3
1638	9.0	17.7	90.7	136.0	451.7
1639	9.1	17.7	91.8	139.2	457.0
1640	10.2	10.2	45.9	69.8	342.9
1641	19.3	0.2	0.8	11.6	23.2
1642	17.5	3.3	22.4	169.2	19.7
1643	3.7	9.8	60.2	63.4	196.9
1644	3.1	9.8	60.3	60.6	196.8
1645	3.0	9.9	60.3	60.3	192.5
1646	3.0	9.9	60.8	60.9	198.1
1647	3.0	9.9	60.7	60.7	181.5
1648	3.0	9.8	61.1	61.2	162.0
1649	3.0	9.8	60.7	60.8	151.1
1650	3.0	9.8	60.5	60.7	169.9
1651	3.0	9.9	60.3	60.3	216.1
1652	3.0	9.9	60.6	60.6	181.5
1653	3.0	9.8	61.1	61.2	157.7
1654	3.0	9.8	61.1	61.1	164.6
1655	3.0	9.8	60.8	60.9	159.1
1656	3.0	9.8	60.4	60.4	193.0
1657	3.0	9.8	60.7	60.8	166.2
1658	3.0	9.9	60.6	60.7	156.2
1659	3.0	9.9	60.7	60.6	166.6
1700	3.0	9.8	61.2	61.3	142.0
1701	3.0	9.8	60.7	60.8	164.8
1702	3.2	9.2	54.6	54.7	173.3
1703	17.8	0.4	1.5	11.3	52.5
1704	20.4	0.1	0.7	22.9	0.6

mid bias

zero

mid

high

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)	
642	8.09	17.11	91.9	78.7	326.6	
643	8.8	17.24	93.6	138.1	438.4	
644	9.06	17.27	94.2	142.3	444.7	
645	9.08	17.29	94.2	142.6	444.4	
646	9.08	17.32	94.2	142.7	444.5	
647	9.09	17.31	94.2	142.8	445.1	
648	9.09	17.3	94.2	142.7	444.8	
649	9.09	17.3	93.8	142.1	445.2	
650	9.08	17.01	93.7	142	449.1	
651	7.51	11.67	57.63	87.1	409.1	
652	0.423	0.002	-1.043	-0.914	18.79	
653	0.065	0	-1.129	-0.97	-1.024	
654	0.04	0.022	-1.151	-0.988	-1.393	
655	0.026	0.136	-1.167	-1.001	-1.067	<del>zero</del>
656	1.964	5.699	37.55	36.4	122.2	
657	4.152	9.59	48.01	51.3	249.4	
658	4.203	11.71	48.02	51.48	250	
659	4.207	14.62	48.16	51.64	248.8	
700	4.207	9.61	48.17	51.65	250.2	mid
701	6.825	16.42	85.4	111	353.6	
702	9.09	17.72	94.2	142.6	453.2	
703	9.14	17.76	94.3	143.5	451.2	
704	9.15	17.74	82.5	125.6	453.1	
705	9.15	17.68	37.18	56.64	451.2	high
706	9.15	17.62	-1.139	-1.734	387.3	<del>zero</del>
707	11.49	4.509	37.99	82.7	20.54	
708	5.736	9.22	47.99	59.96	118.3	mid
709	3.761	9.43	81	84.6	134.6	
710	3.7	9.45	93.8	97.6	187.7	
711	3.669	9.45	93.8	97.5	168.8	high
712	4.629	7.62	43.54	45.29	138.3	
713	9.06	7.74	34.47	61.15	142.6	
714	8.85	4.513	18.97	19.47	105.1	
715	6.9	0.105	-0.866	-2.116	2.264	
716	0.215	0.022	-1.025	-0.887	-1.475	
717	0.082	0.011	-1.083	-0.932	-1.504	
718	0.065	0.018	-1.138	-0.977	-1.523	zero bias
719	4.974	4.907	-1.145	-1.389	-1.147	
720	0.431	9.59	-1.152	-1.011	-2.043	
721	0.077	2.123	-1.152	-0.991	104.9	
722	0.059	0.034	-1.159	-0.996	248.9	
723	0.054	0.036	-1.211	-1.04	248.5	
724	0.063	0.025	41.58	35.72	113.8	
725	0.076	0.022	47.19	40.56	-1.047	Mid Bias
726	3.022	0.031	6.456	5.404	-1.076	
727	5.177	0.022	-1.118	-1.273	-1.149	

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
728	5.28	0.054	-1.152	-1.32	-1.135
729	5.305	0.025	-1.153	-1.324	-1.398
730	5.279	1.329	4.983	5.678	-1.072
731	3.926	9.44	41.47	43.85	95.4
732	3.685	9.47	41.49	43.14	122.5
733	3.697	9.47	41.65	43.33	140.7
734	3.697	9.47	41.77	43.46	137.3
735	3.718	9.42	41.45	43.18	124
736	5.552	0.398	-0.049	-0.14	60.83
737	4.219	0.074	-0.911	-0.977	-0.98
738	4.181	0.063	-1.013	-1.085	-1.474
739	4.779	0.123	-0.873	-0.912	-1.223
740	7.05	8.46	39.08	53.98	65.59
741	3.784	9.44	41.95	43.89	137
742	3.702	9.46	41.43	43.12	154.9
743	3.707	9.46	41.68	43.39	130.2
744	3.732	9.51	41.77	43.55	126.4
745	3.706	9.49	41.33	43.03	117.9
746	3.702	9.46	41.27	42.95	158.9
747	3.682	9.48	41.66	43.31	161.4
748	3.689	9.52	41.75	43.42	109.2
749	3.669	9.48	42.03	43.66	163
750	3.664	9.49	41.98	43.6	125.9
751	3.636	9.49	41.4	42.93	141.6
752	3.642	9.53	41.76	43.31	186
753	3.665	9.51	41.62	43.24	127.4
754	3.653	9.49	42.02	43.61	162.5
755	3.657	9.5	41.89	43.49	143
756	3.639	9.52	41.71	43.26	132.2
757	3.608	9.58	41.76	43.23	166.7
758	3.63	9.55	41.69	43.21	146
759	3.59	9.57	41.73	43.15	200
800	3.601	9.54	41.3	42.73	176
801	3.594	9.57	41.24	42.65	210.1
802	3.615	9.55	41.41	42.88	183.5
803	3.619	9.55	41.51	43	131.7
804	3.619	9.55	41.34	42.82	152.2
805	3.621	9.56	41.57	43.07	173
806	3.621	9.55	41.75	43.25	132.5
807	3.626	9.51	41.75	43.26	160.4
808	3.635	9.56	41.71	43.24	156.9
809	8.98	4.788	17.83	18.15	106.1
810	19.33	1.695	8.1	102.2	3.61
811	5.482	9.46	41.25	50.57	178
812	3.719	9.56	41.88	43.65	173.8
813	3.672	9.55	41.92	43.56	155.7

Mid  
Brow

Part A

Center =

A-1 =

A-2 =

A-3 =

A-4 =

Center =

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
814	3.647	9.57	41.98	43.55	171.7
815	3.637	9.57	41.65	43.2	204.3
816	3.64	9.49	41.58	43.13	187.8
817	3.605	9.57	41.2	42.64	207.8
818	3.653	9.52	41.59	43.16	193
819	3.647	9.56	41.47	43.03	125.2
820	3.622	9.58	41.26	42.75	183.6
821	3.644	9.49	41.45	43	187
822	3.618	9.59	41.77	43.26	125.2
823	3.628	9.58	41.82	43.33	151.6
824	3.639	9.58	41.77	43.32	171.9
825	3.592	9.56	41.35	42.77	164.9
826	3.607	9.59	41.42	42.87	177.2
827	3.612	9.58	41.12	42.57	147.7
828	3.619	9.59	41.31	42.79	134.6
829	3.613	9.59	41.29	42.75	149.2
830	3.614	9.47	41.4	42.87	136.5
831	3.606	9.59	41.61	43.06	151.9
832	3.612	9.59	41.47	42.94	148.3
833	3.629	9.59	41.32	42.82	145.2
834	3.571	9.6	40.88	42.23	184.3
835	3.601	9.42	41.13	42.56	181.7
836	3.632	9.57	41.43	42.94	169.8
837	3.643	9.59	41.31	42.85	135.7
838	3.66	9.58	41.2	42.78	152.9
839	3.633	9.59	40.94	42.44	175.6
840	3.617	9.54	41.27	42.74	149.6
841	6.005	6.79	26.58	27.57	140.6
842	19.61	0.244	-0.432	-9.28	9.3
843	20.51	0.206	-0.499	-22.97	-0.506
844	16.74	3.956	18.71	140.9	18.12
845	4.341	9.57	41.63	45.33	125
846	3.711	9.58	41.28	42.99	178.2
847	3.674	9.58	41.37	42.99	175.7
848	3.684	9.57	41.54	43.19	142.3
849	3.642	9.59	41.78	43.34	132.9
850	3.634	9.56	41.75	43.29	145.7
851	3.648	9.6	41.59	43.15	164.7
852	3.604	9.61	41.16	42.59	191
853	3.643	9.59	41.41	42.95	192.6
854	3.636	9.59	41.54	43.08	156.5
855	3.636	9.62	41.71	43.25	170.5
856	3.642	9.59	41.6	43.15	162.7
857	3.635	9.6	41.36	42.89	140.2
858	3.62	9.6	41.95	43.45	185.3
859	3.659	9.6	41.84	43.44	128

PORT D

Center =

D-1 =

D-2 =

D-3 =

D-4 =

Center =

PORT C

Center =

C-1 =

C-2 =

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)	
900	3.64	9.6	41.49	43.03	165.9	
901	3.608	9.6	41.27	42.72	187.8	
902	3.619	9.6	41.11	42.58	150.3	C-3 =
903	3.614	9.55	41.24	42.71	163.4	
904	3.628	9.59	41.07	42.56	161.6	
905	3.621	9.59	41.16	42.63	141.6	
906	3.617	9.62	41.26	42.74	148.9	C-4 =
907	3.603	9.61	41.12	42.55	173.3	
908	3.601	9.56	41.06	42.48	197.5	
909	3.611	9.56	41.34	42.8	169	
910	3.616	9.61	41.18	42.64	183.7	
911	3.606	9.6	41.25	42.7	215.1	Center =
912	3.647	9.59	41.55	43.11	167.2	
913	3.629	9.6	41.81	43.33	169	
914	3.642	9.6	41.46	43	114.6	
915	13.31	2.364	6.595	5.344	60.94	
916	19.82	1.373	6.714	97.7	0.855	PORT B
917	6.256	9.04	39.15	51.78	108.5	
918	3.907	9.59	41.33	43.66	149	
919	3.659	9.6	41.5	43.09	154.5	
920	3.627	9.6	41.09	42.58	180.4	Center =
921	3.614	9.59	41.33	42.8	219	
922	3.603	9.61	41.08	42.51	178.4	
923	3.62	9.61	41.22	42.7	157.7	
924	3.606	9.61	41.1	42.54	147.1	
925	3.593	9.63	40.83	42.23	189.5	B-1 =
926	3.606	9.63	41.2	42.64	173.1	
927	3.625	9.59	41.32	42.82	139.7	
928	3.617	9.6	41.35	42.83	144.6	B-2 =
929	3.606	9.62	41.02	42.46	170.5	
930	3.602	9.58	41.23	42.67	164.8	
931	3.595	9.63	41.33	42.75	187.1	
932	3.585	9.64	41.16	42.55	161.9	
933	3.578	9.6	41.43	42.8	213.4	B-3 =
934	3.581	9.57	41.23	42.61	195.8	
935	3.609	9.6	41.7	43.17	170.1	
936	3.652	9.61	41.8	43.38	137.2	
937	3.633	9.6	41.75	43.28	159.7	B-4 =
938	3.625	9.6	41.94	43.46	176.8	
939	3.673	9.61	42.1	43.74	131.2	
940	3.672	9.59	41.73	43.36	134	
941	3.645	9.59	41.55	43.11	159.4	
942	3.621	9.61	41.62	43.11	163.4	Center =
943	3.64	9.6	41.75	43.3	148.1	
944	3.62	9.59	41.62	43.11	144.9	
945	4.34	8.31	33.03	34.25	130	

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)	
946	18.67	0.344	-0.172	-3.592	22.18	
947	20.42	0.293	-0.316	-11.8	0.222	
948	9.08	0.15	-0.524	-5.737	-0.556	
949	0.268	0.072	-0.601	-0.522	-1.497	
950	0.071	0.132	-0.673	-0.579	-1.547	
951	0.042	0.143	-0.7	-0.601	-1.598	zero bias
952	1.886	4.734	-0.742	-0.708	-1.619	
953	0.183	9.72	-0.765	-0.661	-1.974	
954	0.037	2.742	-0.801	-0.687	97.1	
955	0.025	0.145	-0.813	-0.697	249.9	
956	0.018	0.134	-0.812	-0.696	249.7	mid bias
957	0.013	0.134	40.61	34.8	115.3	
958	0.003	0.134	46.74	40.04	-1.044	
959	2.11	0.134	12.22	10.42	-1.178	
1000	4.094	0.134	-0.722	-0.769	-1.465	
1001	4.145	0.134	-0.77	-0.823	-1.466	
1002	4.151	0.152	-0.81	-0.865	-1.532	
1003	1.351	0.179	-0.827	-0.76	-0.128	
1004	0.005	0.121	-0.883	-0.757	-1.545	
1005	-0.033	0.119	-0.878	-0.75	-1.599	
1006	-0.044	0.127	-0.879	-0.751	-1.618	zero
1007	5.524	14.69	75.8	94.9	241.1	
1008	9.04	17.96	92.5	139.5	454.4	
1009	9.11	18.05	92.6	140.6	454.6	
1010	9.12	17.94	92.6	140.7	454	
1011	9.13	17.96	92.6	140.8	453.7	high
1012	6.157	11.08	55.24	71.1	354.1	
1013	4.232	9.86	47.52	51.05	251.4	
1014	4.194	9.86	47.46	50.86	251.7	
1015	4.187	9.86	47.43	50.8	250.9	mid
1016	4.21	8.75	44.22	47.36	248.8	
1017	14.8	0.335	0.717	3.142	46.32	
1018	17.88	0.273	0.094	0.41	4.385	
1019	19.59	0.282	-0.216	-3.565	0.743	
1020	19.93	0.268	-0.612	-11.27	-0.071	
1021	10.27	8.11	36.25	114.4	75.7	
1022	3.878	9.6	41.09	43.26	138.6	
1023	3.71	9.63	41.16	42.86	142.4	
1024	3.686	9.46	41.13	42.77	138.3	
1025	3.688	9.6	41.37	43.03	136.6	
1026	3.659	9.65	41.42	43	154	
1027	3.663	9.6	41.38	42.98	129.4	
1028	3.625	9.66	41.54	43.04	137.6	
1029	3.672	9.65	42.23	43.87	117.7	
1030	3.662	9.61	41.69	43.29	134.8	
1031	3.651	9.66	41.13	42.68	118.6	

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baseline

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1032	3.629	9.67	41.3	42.81	126.8
1033	3.635	9.67	41.21	42.73	168.6
1034	3.641	9.66	41.68	43.22	133.6
1035	3.625	9.68	41.6	43.11	137.3
1036	3.622	9.66	41.76	43.26	116
1037	3.593	9.69	41.54	42.96	163.8
1038	3.593	9.71	41.21	42.63	151.5
1039	3.593	9.71	40.69	42.09	155.4
1040	3.562	9.72	40.81	42.14	193.4
1041	3.599	9.7	41.15	42.57	111.2
1042	3.586	9.7	41.48	42.88	137.1
1043	3.593	9.69	41.7	43.12	133.9
1044	3.613	9.67	41.41	42.88	124
1045	3.611	9.69	41.26	42.72	150.7
1046	3.59	9.72	41.26	42.67	182.7
1047	3.604	9.69	41.43	42.88	173.3
1048	3.607	9.71	41.47	42.92	170.3
1049	3.609	9.68	41.33	42.78	173.1
1050	3.622	9.68	41.53	43.02	119.6
1051	3.629	9.69	41.41	42.92	112.2
1052	3.599	9.7	41.49	42.92	165.2
1053	3.607	9.69	41.5	42.95	151.9
1054	3.628	9.68	41.64	43.15	118.7
1055	3.62	9.69	41.47	42.96	123.3
1056	3.614	9.7	41.47	42.95	186
1057	3.629	9.68	41.63	43.14	125.4
1058	3.609	9.7	41.82	43.3	175.1
1059	3.63	9.68	42.09	43.62	131.4
1100	3.63	9.69	41.93	43.46	129.6
1101	3.608	9.69	41.9	43.37	125.6
1102	3.589	9.69	41.65	43.07	146.3
1103	3.61	9.68	41.9	43.37	135.1
1104	3.606	9.71	41.94	43.41	156.1
1105	3.595	9.69	41.84	43.29	123.4
1106	3.595	9.72	41.64	43.08	163.2
1107	3.615	9.69	41.83	43.32	148.1
1108	3.606	9.68	41.88	43.34	173.3
1109	3.639	9.67	41.85	43.4	135.2
1110	3.623	9.7	41.69	43.2	138.4
1111	3.615	9.7	41.57	43.05	174.9
1112	3.61	9.71	41.7	43.17	171.7
1113	3.646	9.69	41.69	43.25	161.9
1114	3.615	9.7	41.67	43.14	134.1
1115	3.633	9.69	41.76	43.3	114.6
1116	3.657	9.67	42.08	43.67	166.2
1117	3.647	9.69	41.97	43.55	147.8

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1118	3.651	9.69	42.06	43.65	128.8
1119	3.639	9.68	41.9	43.46	151.7
1120	3.657	9.65	42.12	43.73	177.1
1121	3.639	9.69	42.13	43.68	126.5
1122	3.636	9.69	41.78	43.33	142.6
1123	3.649	9.67	41.83	43.41	131.7
1124	3.639	9.71	41.88	43.43	110.6
1125	3.63	9.68	41.8	43.32	116
1126	3.648	9.69	41.96	43.54	144.7
1127	3.644	9.7	41.92	43.49	132.3
1128	3.634	9.7	41.76	43.29	166.9
1129	3.632 / 3.6	9.7 / 9.7	41.92 / 41.6	43.45	171.6 / 145.2
1130	3.655	9.72	42.38	43.99	160.1
1131	3.677	9.64	42.24	43.9	119.9
1132	3.665	9.5	40.13	41.66	157.6
1133	10.33	0.588	0.752	1.022	47.01
1134	1.073	0.197	-0.177	-0.16	-1.351
1135	1.469	0.197	-0.243	-0.224	-1.248
1136	0.147	0.197	-0.358	-0.309	-1.565
1137	0.011	0.177	-0.443	-0.379	-1.433
1138	-0.004	0.183	-0.478	-0.409	-1.562
1139	0.433	5.495	-0.483	-0.423	-1.642
1140	0.015	9.79	-0.493	-0.423	-2.049
1141	-0.012	1.956	-0.498	-0.426	119.9
1142	-0.019	0.201	-0.528	-0.452	250.6
1143	-0.017	0.197	38.34	32.81	127.7
1144	-0.019	0.212	46.45	39.75	-0.899
1145	2.554	0.201	6.062	5.151	-1.187
1146	4.097	0.194	-0.458	-0.488	-1.233
1147	4.13	0.206	-0.506	-0.54	-1.484
1148	2.037	0.203	-0.559	-0.534	0.153
1149	0.01	0.17	-0.607	-0.521	-1.531
1150	-0.04	0.145	-0.61	-0.521	-1.558
1151	-0.05	0.134	-0.603	-0.515	-1.631
1152	2.164	7.74	36.2	35.72	104.5
1153	4.122	9.92	47.11	50.25	251
1154	4.164	9.93	47.12	50.39	251.4
1155	4.17	9.93	47.09	50.39	251.7
1156	7.06	16.49	82	108.6	360.5
1157	9.09	18.08	91.9	139.2	455.6
1158	9.13	18.09	91.9	139.8	454.7
1159	13.76	3.791	15.38	24.06	208.1
1200	12.43	6.002	19.09	50.71	70.7
1201	3.87	9.66	30.18	31.76	296.8
1202	3.696	9.73	30.75	32	175.2
1203	3.681	9.69	30.81	32.03	136.4

END

zero bias

mid bias

zero

mid

high

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1204	3.657	9.69	30.53	31.7	186.7
1205	3.647	9.71	30.65	31.8	138.9
1206	3.681	9.68	30.79	32	141.1
1207	3.683	9.67	30.93	32.16	114.9
1208	3.667	9.7	30.56	31.75	167.5
1209	3.66	9.71	30.62	31.8	155.8
1210	3.649	9.69	30.43	31.57	190.4
1211	3.636	9.71	30.42	31.54	155.8
1212	3.655	9.68	30.42	31.57	142.1
1213	3.643	9.71	30.43	31.56	136.7
1214	3.628	9.73	30.03	31.12	169.1
1215	3.65	9.68	30.29	31.43	154.2
1216	3.66	9.59	30.39	31.56	113.7
1217	3.662	9.52	30.44	31.61	116
1218	3.626	9.74	30.23	31.33	107.6
1219	3.649	9.72	30.09	31.22	113.2
1220	3.628	9.72	30.09	31.19	116
1221	3.61	9.75	30.15	31.22	142.5
1222	3.638	9.71	30.1	31.21	99.7
1223	3.615	9.74	29.95	31.02	104
1224	3.587	9.74	29.61	30.62	172.6
1225	3.61	9.73	29.87	30.92	136.2
1226	3.614	9.73	29.69	30.74	129.6
1227	3.623	9.75	30	31.08	175
1228	3.624	9.74	30.35	31.45	128.1
1229	3.618	9.75	30.26	31.34	133
1230	3.606	9.81	29.96	31.01	123.9
1231	3.608	9.73	29.61	30.66	161.9
1232	3.592	9.75	29.94	30.96	169.6
1233	3.6	9.77	29.81	30.84	156.1
1234	3.648	9.72	30.36	31.5	126.3
1235	3.598	9.73	30.05	31.09	127.2
1236	3.605	9.75	30.16	31.21	170.5
1237	3.606	9.74	29.93	30.98	154.5
1238	3.621	9.72	29.68	30.74	149.3
1239	3.601	9.74	29.59	30.62	191.8
1240	3.599	9.76	29.6	30.63	137.5
1241	3.593	9.76	29.76	30.78	149
1242	3.617	9.74	30.17	31.25	120.2
1243	3.642	9.71	30.25	31.37	110.7
1244	3.655	9.73	29.84	30.98	121.9
1245	3.6	9.76	29.63	30.66	147.2
1246	3.629	9.72	29.86	30.94	148.6
1247	3.635	9.73	30.19	31.3	111
1248	3.648	9.71	30.28	31.41	128.2
1249	3.678	9.71	30.41	31.61	100.1

START  
GR ON

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1250	3.628	9.73	30.1	31.19	112.5
1251	3.645	9.69	29.96	31.08	129.5
1252	3.609	9.72	29.97	31.02	138
1253	3.62	9.74	29.91	30.99	140.8
1254	3.609	9.74	29.78	30.83	138
1255	3.576	9.78	29.87	30.87	156.9
1256	3.618	9.76	29.93	31	166.3
1257	3.614	9.74	30.26	31.33	155.8
1258	3.621	9.77	30.02	31.1	126.7
1259	3.606	9.79	30.25	31.31	134
1300	3.631	9.77	30.14	31.24	129.6
1301	3.582	9.77	29.43	30.43	212.9
1302	3.613	9.75	30.14	31.21	145.2
1303	3.615	9.77	29.97	31.04	109.3
1304	3.606	9.77	29.84	30.89	147.2
1305	3.605	9.77	29.5	30.54	156.1
1306	3.579	9.78	29.79	30.79	156.1
1307	3.6	9.77	29.87	30.9	158.9
1308	3.618	9.78	30.32	31.41	182.6
1309	3.633	9.77	30.48	31.59	123.8
1310	3.652	9.78	30.36	31.5	101.2
1311	3.585	9.8	29.9	30.91	149.3
1312	3.573	9.8	29.72	30.7	175.3
1313	3.606	9.79	30.09	31.14	158.5
1314	3.645	9.79	30.34	31.47	123.2
1315	3.628	9.79	30.1	31.19	135.6
1316	3.629	9.78	30.06	31.15	196.6
1317	3.603	9.8	30.13	31.18	139.1
1318	3.636	9.79	30.5	31.62	159.2
1319	3.606	9.8	30.31	31.37	133.8
1320	3.638	9.21	30.38	31.5	142.6
1321	3.635	9.77	29.96	31.07	137.9
1322	3.621	9.79	30.29	31.38	200.6
1323	3.636	9.79	30.1	31.21	135.6
1324	3.649	9.78	30.08	31.21	113.1
1325	3.627	9.79	29.73	30.81	181.7
1326	3.657	9.78	30.2	31.35	195.5
1327	3.656	9.78	30.47	31.63	127.7
1328	3.655	9.78	30.49	31.65	111.8
1329	3.655/3.6	9.79/9.8	30.3/30.0	31.45	121.5/144.4
1330	3.631	9.79	30.17	31.27	175.1
1331	3.645	9.84	30.15	31.27	142.4
1332	3.627	9.8	30.1	31.19	116.4
1333	12.71	2.28	5.151	6.791	73.1
1334	1.765	0.237	0.105	0.115	-0.983
1335	0.052	0.206	-0.073	-0.063	-1.137

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1336	0.003	0.201	-0.146	-0.125	-1.195
1337	-0.01	0.201	-0.19	-0.162	-1.424
1338	1.009	3.929	-0.19	-0.172	-1.402
1339	0.109	9.83	-0.203	-0.175	-1.997
1340	-0.01	9.88	-0.21	-0.18	-1.767
1341	0.216	2.912	-0.203	-0.176	94.6
1342	-0.018	0.237	-0.209	-0.179	251.3
1343	-0.026	0.201	-0.221	-0.189	252.2
1344	-0.028	0.206	-0.24	-0.206	251.3
1345	-0.027	0.201	41.49	35.49	109.5
1346	-0.03	0.203	46.14	39.46	-1.038
1347	-0.031	0.223	46.15	39.47	-1.1
1348	0.993	0.206	25.63	21.92	-1.068
1349	4.006	0.201	-0.071	-0.076	-1.117
1350	4.118	0.201	-0.147	-0.157	-1.422
1351	4.13	0.203	-0.176	-0.188	-1.187
1352	1.427	0.235	-0.214	-0.196	-0.836
1353	-0.013	0.201	-0.263	-0.225	-1.577
1354	-0.046	0.199	-0.254	-0.217	-1.548
1355	1.178	4.635	24.54	23.43	44.92
1356	4.079	9.97	46.8	49.76	248.2
1357	4.165	9.91	46.8	50.06	253
1358	4.173	9.9	46.8	50.08	252.6
1359	6.944	16.13	78.4	103.6	348.3
1400	9.1	18.1	90.9	137.8	457.2
1401	9.14	18.1	90.9	138.4	455.8
1402	9.15	18.1	90.8	138.3	456.4
1403	5.265	10.7	30.92	38.22	290.9
1404	3.668	9.61	25.65	26.66	211.1
1405	3.645	9.57	25.79	26.76	115.9
1406	3.653	9.75	25.75	26.73	93.2
1407	3.661	9.73	25.76	26.74	139.7
1408	3.65	9.75	25.92	26.89	136.3
1409	3.656	9.58	25.88	26.87	112.8
1410	3.665	9.69	25.87	26.86	135.5
1411	3.654	9.64	26.01	27	132.3
1412	3.643	9.73	25.97	26.94	96.1
1413	3.653	9.76	25.89	26.86	140.6
1414	3.643	9.77	25.87	26.84	163.8
1415	3.648	9.7	25.85	26.82	109.1
1416	3.656	9.74	25.96	26.95	144.3
1417	3.669	9.72	25.85	26.86	90.7
1418	3.652	9.77	25.68	26.65	120.7
1419	3.647	9.78	25.72	26.69	130.5
1420	3.634	9.75	26.09	27.04	135.5
1421	3.664	9.76	26.14	27.15	124.9

zero bias

mid bias

zero

mid

high

FGR and Urea OW

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1422	3.661	9.77	25.94	26.93	121.3
1423	3.63	9.78	25.76	26.7	144.7
1424	3.634	9.79	25.53	26.48	159.7
1425	3.616	9.78	25.47	26.38	193.4
1426	3.614	9.78	25.58	26.5	163.1
1427	3.627	9.76	25.64	26.56	152
1428	3.641	9.77	25.93	26.89	136.1
1429	3.634	9.78	25.84	26.79	105.4
1430	3.602	9.79	25.84	26.74	136.1
1431	3.637	9.78	25.75	26.7	145.4
1432	3.616	9.79	25.79	26.71	152.9
1433	3.626	9.78	25.74	26.67	131.2
1434	3.614	9.78	25.73	26.64	128.9
1435	3.593	9.78	25.7	26.58	120.9
1436	3.612	9.78	25.67	26.58	143.7
1437	3.599	9.79	25.61	26.5	146.2
1438	3.621	9.79	25.71	26.64	128.1
1439	3.592	9.79	25.74	26.62	135.3
1440	3.603	9.79	25.67	26.56	162.8
1441	3.6	9.78	25.77	26.66	144.8
1442	3.621	9.77	25.73	26.66	199.7
1443	3.628	9.78	25.78	26.71	120.1
1444	3.605	9.78	25.57	26.46	134.8
1445	3.59	9.81	25.58	26.46	140
1446	3.586	9.81	25.75	26.61	157.9
1447	3.65	9.67	25.83	26.81	90.4
1448	3.611	9.82	25.84	26.76	116.6
1449	3.626	9.81	26.02	26.96	110.6
1450	3.623	9.81	25.89	26.82	120.8
1451	3.623	9.83	25.76	26.68	146.5
1452	3.618	9.82	25.79	26.71	228.3
1453	3.636	9.8	25.96	26.92	146.2
1454	3.648	9.81	26.04	27.02	130.5
1455	3.652	9.79	25.97	26.95	168.9
1456	3.653	9.81	26.03	27.02	97.1
1457	3.636	9.83	26.08	27.05	154.8
1458	3.647	9.8	26.07	27.04	107.5
1459	3.619	9.82	26.04	26.97	173.4
1500	3.646	9.81	26.12	27.1	154.5
1501	3.617	9.82	26.07	27.01	163.4
1502	3.623	9.84	25.83	26.77	124.9
1503	3.6	9.83	25.69	26.58	188.1
1504	3.599	9.83	25.66	26.55	173.9
1505	3.618	9.81	25.8	26.72	175.8
1506	3.627	9.83	25.77	26.7	164.2
1507	3.643	9.83	25.93	26.9	127

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1508	3.646	9.81	25.65	26.61	145.5
1509	3.619	9.83	25.66	26.58	185.3
1510	3.635	9.81	25.64	26.58	162
1511	3.629	9.83	25.85	26.79	130.2
1512	3.639	9.84	25.89	26.85	137.2
1513	3.664	9.79	26.04	27.05	100.6
1514	3.624	9.85	25.74	26.67	142.8
1515	3.625	9.87	25.92	26.86	137.4
1516	3.636	9.87	25.83	26.78	126.2
1517	3.635	9.85	25.9	26.85	142.2
1518	3.64	9.77	25.77	26.72	145
1519	3.64	9.72	25.38	26.32	112.7
1520	3.755	0.501	0.274	0.314	52.14
1521	0.064	0.259	-0.082	-0.071	-1.049
1522	0.006	0.226	-0.104	-0.089	-1.063
1523	-0.008	0.241	-0.104	-0.089	-1.153
1524	0.012	7.85	-0.117	-0.101	-1.75
1525	-0.021	9.92	-0.132	-0.113	-1.593
1526	-0.026	1.455	-0.119	-0.101	133.8
1527	-0.03	0.288	-0.121	-0.103	250.8
1528	-0.028	0.221	33.65	28.78	149.3
1529	-0.031	0.215	45.71	39.09	-0.703
1530	2.602	0.226	6.286	5.388	-1.171
1531	4.101	0.21	-0.046	-0.049	-1.236
1532	4.13	0.217	-0.088	-0.094	-1.166
1533	1.894	0.215	-0.121	-0.115	-1.205
1534	-0.007	0.179	-0.152	-0.13	-1.567
1535	-0.047	0.201	-0.149	-0.127	-1.608
1536	-0.056	0.201	-0.121	-0.103	-1.67
1537	2.213	7.22	35.3	35.04	102.6
1538	4.138	10.06	46.78	49.94	252.7
1539	4.176	10.05	46.8	50.09	253
1540	5.929	16.06	77.6	95	345.2
1541	9.08	18.19	90.9	137.5	457.8
1542	9.15	18.17	90.9	138.5	455.8
1543	9.16	18.18	90.9	138.6	457.9
1544	9.14	17.71	91.9	139.9	454.8
1545	17.66	1.734	3.457	8.14	169.7
1546	20.54	0.333	0.112	5.555	-0.564
1547	20.55	0.337	0.13	6.686	-0.486
1548	20.58	0.333	0.052	2.792	-0.498
1549	20.62	0.311	-0.005	-0.285	-0.565
1550	20.64	0.313	-0.043	-2.98	-1.123
1551	20.65	0.282	-0.05	-3.569	-1.153
1552	20.65	0.295	-0.054	-3.962	-1.17
1553	20.66	0.286	-0.055	-4.037	-1.145

END

3.6

9.8

25.8

142.3

zero bias

mid bias

zero mid

high

mid load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1554	20.66	0.279	-0.042	-3.06	-1.176
1555	20.65	0.288	-0.025	-1.747	-0.763
1556	20.65	0.317	-0.038	-2.743	-0.602
1557	20.66	0.277	-0.05	-3.718	-1.174
1558	20.66	0.259	-0.044	-3.279	-1.182
1559	20.64	0.317	-0.016	-1.029	-0.628
1600	20.66	0.295	-0.054	-4.033	-0.992
1601	20.66	0.317	-0.053	-3.949	-0.896
1602	20.66	0.326	-0.045	-3.352	-0.8
1603	20.66	0.313	-0.059	-4.44	-1.068
1604	20.66	0.328	-0.053	-4.023	-1.1
1605	20.67	0.311	-0.055	-4.237	-1.111
1606	20.63	0.324	0.044	3.147	-0.635
1607	20.66	0.29	-0.024	-1.804	-1.181
1608	20.65	0.326	0.001	0.121	-0.949
1609	20.65	0.317	-0.015	-1.031	-1.069

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
1922	9.16	17.56	92.2	79	453.2
1923	9.16	17.61	92.5	141	450.5
1924	6.232	9.07	38.31	58.66	320
1925	0.208	0.201	-0.13	-0.112	2.463
1926	0.055	0.179	-0.19	-0.163	-1.59
1927	0.036	-0.051	-0.213	-0.183	-1.621
1928	0.026	-0.06	-0.228	-0.196	-1.653
1929	1.937	6.141	32.55	32.06	78.3
1930	4.164	9.32	47.52	50.8	248.6
1931	4.204	9.37	47.5	50.93	249.2
1932	4.206	9.36	47.5	50.93	250
1933	16.37	0.574	0.612	-0.785	87.7
1934	20.64	0.067	-0.191	-13.51	-1.008
1935	20.69	0.06	-0.22	-18.73	-0.992
1936	20.69	0.065	-0.23	-19.83	-0.776
1937	20.69	0.058	-0.256	-22.01	-0.454
1938	20.7	0.067	-0.268	-24.17	-1.09
1939	20.69	0.067	-0.263	-22.93	-0.949
1940	20.7	0.067	-0.278	-24.3	-1.066
1941	20.69	0.009	-0.284	-24.79	-1.144
1942	17.05	0.02	-0.305	-18.04	-1.162
1943	0.771	-0.054	-0.336	-0.302	-1.624
1944	0.084	-0.058	-0.349	-0.3	-1.617
1945	0.042	-0.067	-0.37	-0.318	-1.553
1946	0.027	-0.047	-0.375	-0.321	-1.528
1947	2.692	7.84	41.93	41.92	129.9
1948	4.178	9.37	47.53	50.87	249.2
1949	4.199	9.37	47.55	50.96	249.8
1950	4.201	9.36	47.57	50.99	249
1951	6.799	15.46	81.3	106.2	339.8
1952	9.1	3.768	92.8	140.7	449.6
1953	9.14	-0.065	91.7	139.5	449.5
1954	9.15	6.838	0.053	0.081	450.4
1955	9.15	11.27	26.55	40.45	374.9
1956	18.33	17.63	47.48	1024	10.45
1957	20.69	17.66	80.3	6986	-1.113
1958	20.72	0.784	92.3	6999	-1.062
1959	20.71	0.065	92.2	6999	-1.133
2000	20.69	0.067	0.739	63.82	-1.095
2001	20.69	0.049	-0.345	-29.37	-1.065
2002	20.69	0.065	-0.365	-30.89	-1.114
2003	20.69	0.067	-0.396	-33.61	-1.125
2004	20.69	0.065	-0.424	-35.99	-1.04
2005	20.69	0.063	-0.42	-35.66	-1.118
2006	20.69	0.065	-0.426	-36.15	-1.134
2007	20.69	0.067	-0.435	-37.2	-1.089

zero

mid

high

no: CO2 mid data logger water

mid

high

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
2008	20.63	0.067	-0.461	-32.84	-0.853
2009	20.61	0.063	-0.457	-28.88	-0.964
2010	20.48	0.058	-0.448	-31.89	-1.118
2011	3.198	0.027	-0.478	-0.589	-1.376
2012	0.195	-0.042	-0.494	-0.428	-1.521
2013	0.109	-0.038	-0.494	-0.426	-1.586
2014	0.085	0.022	-0.487	-0.418	-1.616
2015	0.073	0.009	-0.508	-0.437	-1.538
2016	0.068	0.034	-0.508	-0.437	-1.556
2017	0.899	-0.02	11.62	11.52	-1.541
2018	1.26	0.007	44.59	40.73	-1.63
2019	0.259	0.009	47.1	40.92	-1.628
2020	0.054	0	47.17	40.51	-1.638
2021	0.046	2.519	34.3	29.44	-1.555
2022	0.042	9.56	-0.388	-0.333	-1.95
2023	0.041	4.638	-0.478	-0.41	38.72
2024	0.035	0.047	-0.514	-0.441	241.8
2025	0.033	0.022	-0.526	-0.451	247.6
2026	3.12	0.02	-0.536	-0.539	90.2
2027	4.169	0.018	-0.544	-0.582	-1.145
2028	4.194	-0.031	-0.549	-0.588	-1.496
2029	5.451	3.073	7.08	9.27	0.278
2030	5.038	8.7	20.21	22.86	0.297
2031	4.8	8.73	20.11	22.35	-1.065
2032	4.835	8.75	20.07	22.37	-0.826
2033	4.868	8.73	20.25	22.61	-1.215
2034	4.825	8.76	20.17	22.46	-0.584
2035	4.823	8.76	20.25	22.54	-0.827
2036	4.862	8.76	20.46	22.84	-1.277
2037	4.854	8.74	20.24	22.58	-1.415
2038	4.864	8.73	20.23	22.58	-1.088
2039	4.856	8.77	20.27	22.62	-1.033
2040	4.867	8.75	20.35	22.72	-1.477
2041	4.861	8.79	20.27	22.62	-1.27
2042	4.851	8.79	20.44	22.8	-1.486
2043	4.876	8.72	20.34	22.72	-1.459
2044	4.86	8.77	20.48	22.86	-1.415
2045	4.871	8.78	20.43	22.81	-1.624
2046	4.865	8.74	20.22	22.57	-1.306
2047	5.032	8.63	20.14	22.72	-1.501
2048	5.183	8.55	19.72	22.45	-1.127
2049	5.102	8.61	19.95	22.62	-1.53
2050	5.075	8.59	20.43	23.11	-1.623
2051	4.887	8.74	20.43	22.84	-0.919
2052	4.855	8.77	20.35	22.71	-1.424
2053	4.871	8.75	20.48	22.87	-1.461

zero bias

mid bias

PORT B

Center =

B-1 =

B-2 =

B-3 =

B-4 =

Center =

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
2054	4.894	8.74	20.57	23.01	-1.105
2055	4.84	8.7	20.35	22.68	-1.395
2056	6.011	6.931	15.63	17.5	-1.449
2057	19.38	0.154	-0.421	-9.54	-1.14
2058	13.03	6.066	14.48	76.8	-1.271
2059	5.087	8.74	20.43	23.16	-1.378
2100	4.9	8.75	20.59	23.04	-1.452
2101	4.84	8.83	20.46	22.81	-1.555
2102	4.876	8.73	20.6	23.01	-1.169
2103	4.873	8.77	20.56	22.95	-1.574
2104	4.896	8.75	20.55	22.99	-1.535
2105	4.903	8.7	20.59	23.05	-1.477
2106	4.888	8.72	20.43	22.83	-1.249
2107	4.887	8.7	20.71	23.15	-1.426
2108	4.893	8.74	20.59	23.03	-1.627
2109	4.86	8.78	20.44	22.81	-1.23
2110	4.867	8.81	20.58	22.98	-1.188
2111	4.858	8.82	20.56	22.94	-1.301
2112	4.862	8.78	20.74	23.15	-1.546
2113	4.825	8.8	20.58	22.92	-0.951
2114	4.829	8.82	20.84	23.22	-1.439
2115	4.854	8.79	20.65	23.03	-1.594
2116	4.851	8.83	20.9	23.31	-1.558
2117	4.829	8.81	20.72	23.07	-1.509
2118	4.82	8.81	20.48	22.79	-1.39
2119	4.854	8.78	20.62	23	-1.056
2120	4.835	8.81	20.74	23.11	-1.615
2121	4.824	8.82	20.5	22.83	-1.593
2122	4.858	8.79	20.73	23.13	-1.639
2123	5.986	6.952	15.65	17.51	-1.462
2124	17.38	2.687	6.304	47.13	-1.216
2125	5.689	8.75	20.7	24.75	-1.627
2126	4.927	8.77	20.83	23.35	-1.382
2127	4.887	8.78	20.63	23.06	-1.223
2128	4.86	8.79	20.63	23.02	-1.625
2129	4.851	8.81	20.67	23.06	-1.598
2130	4.867	8.77	20.69	23.11	-1.542
2131	4.871	8.77	20.94	23.39	-1.572
2132	4.862	8.77	20.76	23.17	-1.288
2133	4.831	8.83	20.82	23.2	-1.494
2134	<del>4.843</del>	8.79	21.04	23.45	-1.504
2135	<u>4.84</u>	<u>8.81</u>	20.99	23.39	-1.438
2136	4.872	8.81	21	23.46	-1.556
2137	4.82	8.82	21.42	23.84	-1.575
2138	4.778	8.84	21.48	23.86	-0.839
2139	4.854	8.74	20.54	22.9	-0.738

PORT A

Center =

A-1 =

A-2 =

A-3 =

A-4 =

Center =

PORT D

Center =

D-1 =

D-2 =

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)	
2140	4.956	8.73	20.77	23.32	-1.404	
2141	4.956	8.73	20.11	22.57	-1.322	
2141	4.892	8.79	20.16	22.62	-0.863	$\overline{D-3} =$
2142	4.948	8.71	19.94	22.37	-0.997	
2143	4.96	8.67	20.14	22.62	-1.163	
2144	5.537	8.18	18.86	21.91	30.38	
2145	5.4	8.59	20.4	23.73	91.9	
2146	4.904	8.81	20.9	23.39	88.1	$\overline{D-4} =$
2147	4.815	8.84	21.44	23.86	89.6	
2148	4.747	8.86	21.32	23.63	89.9	
2149	4.782	8.81	21.43	23.8	90.5	
2150	4.804	8.84	21.44	23.84	90.2	
2151	4.831	8.82	21.55	24	90.5	$\overline{\text{Center}} =$
2152	4.822	8.83	21.68	24.14	86.8	
2153	4.76	8.78	21.45	23.79	9.32	
2154	4.808	8.84	21.74	24.18	-1.214	
2155	13.54	2.191	4.187	2.745	28.4	
2156	20.46	0.15	-0.571	-24.81	49.37	$\text{PORT C}$
2157	20.61	0.123	-0.611	-38.22	31.14	
2158	18.66	2.645	6.13	47.28	-0.948	
2159	5.866	8.74	21.09	25.58	27.95	
2200	4.979	8.77	21.31	23.97	91.8	
2201	4.922	8.78	21.13	23.67	91.3	
2201	4.906	8.85	21.11	23.64	86.6	
2201	4.892	8.79	21.48	24.02	1128	$\overline{\text{Center}} =$
2201	4.905	8.72	21.17	23.69	89.5	
2202	4.904	8.79	21.19	23.71	89.5	
2202	4.825	8.79	20.97	23.37	90.1	
2203	4.856	8.84	20.77	23.17	89.8	
2204	4.9	8.81	21	23.5	78.5	
2205	4.88	8.81	21.05	23.52	48.65	$\overline{C-1} =$
2206	4.859	8.81	20.79	23.2	48.21	
2207	4.864	8.8	20.62	23.02	48.35	
2208	4.893	8.8	20.64	23.08	35.45	
2209	4.883	8.8	20.53	22.95	-0.179	$\overline{C-2} =$
2210	4.88	8.77	20.67	23.09	-0.765	
2211	4.887	8.69	20.77	23.22	-0.726	
2212	4.865	8.82	20.85	23.28	-0.71	
2213	4.884	8.8	20.71	23.15	-0.832	$\overline{C-3} =$
2214	4.881	8.81	20.57	22.98	-0.494	
2215	4.891	8.77	20.72	23.17	-0.789	
2216	4.932	8.78	21	23.54	-1.091	
2217	4.944	8.74	20.54	23.04	-0.984	$\overline{C-4} =$
2218	4.945	8.77	20.85	23.4	-1.041	
2219	4.94	7.98	20.51	23	-0.729	
2220	4.908	8.69	20.26	22.67	-0.944	

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
2221	4.924	8.79	20.55	23.03	-1.056
2222	4.911	8.78	20.54	23	-0.973
2223	4.892	8.8	20.59	23.02	-1.015
2224	4.865	8.67	20.51	22.9	-0.806
2225	4.892	8.24	20.57	23.01	-1.004
2226	12.98	2.493	4.545	3.205	-0.759
2227	20.44	0.148	-0.526	-21.7	-0.427
2228	20.6	0.121	-0.547	-32.9	-0.432
2229	20.63	0.125	-0.548	-35.72	-0.457
2230	20.63	0.096	-0.559	-37.59	-0.446
2231	20.64	0.083	-0.628	-42.77	-0.443
2232	20.64	0.094	-0.626	-42.72	-0.402
2233	12.19	0.635	0.745	49.67	-0.576
2234	0.438	0.067	-0.629	-0.552	-0.953
2235	0.1	0.065	-0.656	-0.565	-0.916
2236	0.065	0.056	-0.679	-0.583	-0.933
2237	0.679	0.067	39.77	35.42	-0.908
2238	0.07	0.058	47.33	40.68	-0.924
2239	2.819	0.063	2.539	2.115	-0.994
2240	4.142	0.054	-0.628	-0.671	-0.932
2241	4.168	0.058	-0.673	-0.72	-0.943
2242	2.17	0.036	-0.683	-0.658	-0.901
2243	0.042	0.118	-0.745	-0.64	-0.518
2244	-0.005	0.087	-0.749	-0.641	-0.441
2245	1.316	0.083	40.48	37.39	-0.42
2246	4.08	0.094	47.64	50.67	0.014
2247	4.166	0.094	47.68	50.98	0.423
2248	7.35	0.107	86.5	116.1	0.6
2249	9.08	0.094	93	140.8	0.77
2250	9.12	0.092	93.1	141.4	-0.744
2250	9.12	0.067	0.108	0.165	-1.036
2250	9.12	0.134	-0.322	-0.489	-1.044
2251	9.16	0.073	-0.361	-0.55	-1.04
2252	2.869	0.049	2.25	1.869	-1.057
2253	0.047	0.013	19.31	16.6	-1.057
2254	0	-0.157	16.13	13.81	-1.059
2254	-0.012	0	8.26	7.07	-0.954
2254	-0.012	0	20.74	17.75	-0.952
2255	-0.012	0	20.78	17.78	-0.952
2256	-0.016	0.007	10.3	8.82	-1.034
2257	-0.021	0.013	-0.051	-0.044	-1.049
2258	0.492	0.004	-0.066	-0.058	-1.04
2259	-0.006	0.013	-0.081	-0.069	-1.034
2300	-0.031	0.02	-0.089	-0.077	-1.022
2301	2.84	7.61	11.46	10.88	11.79
2302	4.172	9.74	10.11	10.82	47.85

Center =

zero bias

mid bias

zero

mid

high

zero

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
2303	4.201	9.76	12.31	13.19	48.34
2304	4.207	9.74	12.46	13.36	48.21
2305	6.648	16.01	18.9	24.23	68.94
2306	9.14	17.83	21.18	32.21	89.8
2307	9.19	17.85	21.26	32.5	89.7
2308	9.2	17.84	21.27	32.53	89.7
2309	6.745	5.715	6.324	9.67	56.13
2310	0.276	0.067	0	0	-0.791
2311	0.063	0.065	-0.047	-0.041	-0.888
2312	0.041	0.06	-0.068	-0.059	-0.961
2313	0.855	7.44	-0.073	-0.065	-1.197
2314	0.062	9.66	-0.07	-0.06	-1.47
2315	2.818	0.883	-0.068	-0.067	20.25
2316	2.697	0.078	-0.082	-0.081	40.72
2317	0.118	0.065	-0.094	-0.081	47.82
2318	0.035	0.072	-0.095	-0.081	48.22
2319	0.024	0.02	18.33	15.72	22.87
2320	0.018	0.067	21.08	18.07	-0.305
2321	2.622	0.063	2.438	2.091	-0.678
2322	4.149	0.065	-0.056	-0.06	-0.924
2323	4.184	0.011	-0.081	-0.087	-0.959
2324	4.336	4.431	10.49	11.42	-0.829
2325	4.726	8.83	20.78	23	-0.499
2326	4.806	8.88	20.93	23.28	-0.362
2327	4.736	8.93	20.84	23.08	-0.546
2328	4.783	8.9	20.92	23.24	-0.493
2329	4.784	8.87	20.88	23.19	-0.598
2330	4.764	8.93	20.89	23.17	-0.826
2331	4.786	8.92	20.82	23.13	-0.648
2332	4.783	8.88	20.86	23.16	-0.774
2333	4.765	8.93	20.88	23.17	-0.577
2334	4.786	8.89	20.87	23.18	-0.623
2335	4.775	8.92	20.95	23.26	-0.618
2336	4.78	8.91	20.8	23.1	0.032
2337	4.765	8.93	20.94	23.24	-0.461
2338	4.79	8.92	20.9	23.23	-0.401
2339	4.789	8.9	20.79	23.1	-0.549
2340	4.769	8.92	20.88	23.17	-0.673
2341	4.797	8.91	20.84	23.16	0.1
2342	4.783	8.92	20.75	23.05	-0.342
2343	4.769	8.94	21.04	23.35	-0.608
2344	4.785	8.92	20.75	23.04	-0.599
2345	4.763	8.93	20.76	23.03	-0.185
2346	4.773	8.92	20.89	23.19	0.022
2347	4.749	8.95	20.82	23.08	-0.626
2348	4.798	8.89	21.05	23.4	-0.42

*mid*

*high*

*zero bias*

*mid/high bias*

*BASELINE  
START*

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
2349	4.767	8.95	20.72	22.99	-0.142
2350	4.751	8.94	20.54	22.77	-0.23
2351	4.778	8.93	20.64	22.91	0.239
2352	4.775	8.91	20.7	22.98	-0.575
2353	4.807	8.89	20.79	23.13	-0.146
2354	4.773	8.92	21	23.31	0.067
2355	4.792	8.93	20.87	23.19	-0.403
2356	4.751	8.94	20.71	22.96	0
2357	4.739	8.96	20.84	23.08	0.093
2358	4.8	8.93	20.97	23.32	-0.687
2359	4.779	8.91	20.76	23.05	-0.459
2400	4.767	8.93	20.87	23.16	0.116
1	4.773	8.94	20.8	23.09	-0.028
2	4.787	8.9	20.62	22.9	-0.186
3	4.778	8.93	20.57	22.83	-0.153
4	4.78	8.94	20.96	23.28	-0.496
5	4.767	8.92	20.71	22.98	0.006
6	4.775	8.9	20.57	22.83	-0.343
7	4.77	8.95	20.68	22.95	-0.477
8	4.778	8.94	20.62	22.89	0.666
9	4.77	8.92	20.75	23.03	0.622
10	4.81	8.93	21.09	23.47	-0.446
11	4.791	8.92	20.61	22.9	-0.228
12	4.782	8.93	20.73	23.02	-0.408
13	4.788	8.91	20.54	22.82	-0.582
14	4.789	8.94	20.79	23.1	-0.693
15	4.789	8.93	20.93	23.26	-0.56
16	4.785	8.93	20.37	22.62	-0.416
17	4.787	8.94	20.62	22.9	-0.285
18	4.79	8.92	20.68	22.98	-0.521
19	4.78	8.94	20.53	22.79	-0.234
20	4.769	8.96	20.51	22.77	-0.63
21	4.8	8.92	20.54	22.83	-0.071
22	4.76	8.95	20.75	23.01	0.406
23	4.779	8.91	20.54	22.8	-0.12
24	4.749	8.96	20.38	22.59	-0.049
25	4.777 / 4.8	8.94 / 8.9	20.5 / 20.8	22.76	0 / -0.3
26	4.754	8.74	20.23	22.43	0.42
27	10.12	2.207	4.675	5.31	-0.33
28	1.255	0.107	0.016	0.016	-0.937
29	0.072	0.04	-0.005	-0.004	-0.987
30	0.029	0.072	-0.026	-0.022	-0.925
31	0.017	0.069	-0.039	-0.033	-0.927
32	1.832	5.099	-0.04	-0.038	-1.074
33	0.154	9.7	-0.053	-0.046	-1.508
34	0.028	1.992	-0.066	-0.056	19.51

END

zero bias

mid bias

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
35	0.017	0.107	-0.075	-0.064	47.88
36	0.014	0.074	-0.088	-0.076	47.88
37	0.012	0.114	19.19	16.44	20.8
38	0.008	0.076	20.98	17.97	-0.362
39	0.004	0.078	20.99	17.98	-0.406
40	2.605	0.072	2.428	2.076	-0.626
41	4.145	0.081	-0.088	-0.094	-0.914
42	4.183	0.025	-0.11	-0.118	-0.93
43	3.92	0.101	-0.122	-0.129	-0.932
44	0.314	-0.315	-0.2	-0.175	-0.943
45	-0.019	0.034	-0.215	-0.184	-1.023
46	-0.034	-0.038	-0.218	-0.186	-1.048
47	1.68	6.212	6.903	6.722	13.04
48	4.12	9.77	11.02	11.76	47.83
49	4.187	9.8	12.15	13.02	48.14
50	4.196	9.78	12.25	13.13	48.12
51	7.24	16.6	20.41	27.09	70.7
52	9.15	17.88	21.15	32.2	89.6
53	9.19	17.89	21.15	32.31	89.5
54	9.19	17.89	21.15	32.35	89.9
55	3.834	2.451	3.809	5.905	45.3
56	0.061	0.054	-0.226	-0.195	-0.997
57	-0.015	0.029	-0.24	-0.205	-1.051
58	-0.028	0.009	-0.244	-0.209	-1.058
59	4.357	6.977	11.05	12.47	0.367
100	4.8	8.7	13.51	15.02	1.953
101	4.761	8.91	9.48	10.51	3.125
102	4.737	8.82	-0.047	-0.052	-0.379
103	4.719	8.91	-0.154	-0.17	-0.689
104	4.704	8.9	-0.121	-0.134	-0.677
105	4.691	8.89	-0.147	-0.162	-0.687
106	4.682	8.87	-0.154	-0.171	-0.665
107	4.673	8.87	-0.162	-0.178	-0.695
108	4.666	8.86	-0.171	-0.189	-0.681
109	4.66	8.85	-0.181	-0.2	-0.709
110	4.657	8.84	-0.193	-0.212	-0.708
111	4.65	8.99	-0.192	-0.211	-0.665
112	4.652	8.81	-0.192	-0.212	-0.658
113	4.652	8.83	-0.197	-0.217	-0.588
114	2.882	2.277	-0.216	-0.218	31.97
115	0.278	1.454	2.206	1.943	84.8
116	4.208	8.85	13.24	14.14	21.57
117	4.76	8.7	13.33	14.79	5.467
118	4.767	8.9	13.17	14.61	5.932
119	4.758	8.94	13.27	14.72	6.957
120	4.763	8.95	13.21	14.66	9.07

high bias

mid bias

zero

Mid

High

ZR ON  
SRT

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
121	4.799	8.94	13.25	14.73	10.5
122	4.789	8.95	13.47	14.96	7.53
123	4.739	8.96	13.16	14.57	7.91
124	4.773	8.96	13.21	14.66	4.803
125	4.761	8.96	13.29	14.74	7.37
126	4.755	8.96	13.21	14.65	6.455
127	4.722	8.99	13.13	14.52	10.52
128	4.754	8.95	13.2	14.64	9.3
129	4.77	8.96	13.33	14.79	8.86
130	4.767	8.98	13.37	14.84	9.05
131	4.773	8.98	13.28	14.74	9
132	4.778	8.96	13.22	14.68	10.49
133	4.785	8.94	13.28	14.74	7.7
134	4.795	8.94	13.25	14.72	6.147
135	4.791	8.97	13.42	14.92	4.438
136	4.782	8.96	13.33	14.8	6.645
137	4.782	8.99	13.61	15.12	5.65
138	4.785	8.97	13.41	14.89	7.1
139	4.786	8.97	13.49	14.98	4.878
140	4.768	8.96	13.37	14.83	5.343
141	4.813	8.96	13.6	15.13	3.753
142	4.779	8.97	13.52	15.02	4.822
143	4.773	8.94	13.49	14.97	9.87
144	4.749	8.99	13.41	14.86	8.99
145	4.772	8.96	13.47	14.95	8.22
146	4.788	8.97	13.42	14.9	6.39
147	4.761	8.98	13.34	14.8	11.05
148	4.765	8.98	13.34	14.8	10.91
149	4.788	8.95	13.39	14.87	9.22
150	4.805	8.96	13.51	15.03	4.161
151	4.801	8.93	13.37	14.86	7.06
152	4.796	8.95	13.34	14.84	8.42
153	4.801	8.95	13.33	14.82	6.701
154	4.794	8.96	13.32	14.81	8.48
155	4.767	8.97	13.24	14.69	6.469
156	4.79	8.96	13.27	14.75	7.59
157	4.761	8.99	13.17	14.61	7.05
158	4.777	8.97	13.22	14.67	7.12
159	4.772	8.96	13.05	14.49	7.91
200	4.779	8.97	13.3	14.77	6.519
201	4.776	8.96	13.22	14.68	6.409
202	4.773	8.96	13.26	14.71	6.007
203	4.779	8.95	13.41	14.89	8.13
204	4.765	8.96	13.32	14.78	6.05
205	4.797	8.94	13.42	14.91	6.085
206	4.784	8.95	13.41	14.9	9.04

low load, 23 March, 1994

time	O2 (%)	CO2 (%)	NOx (ppm)	NOx 3% (ppm)	CO (ppm)
207	4.765	8.99	13.31	14.76	11.05
208	4.789	8.98	13.41	14.91	7.74
209	4.791	8.96	13.4	14.89	8.79
210	4.778	8.95	13.23	14.69	8.06
211	4.832	8.9	13.47	15	9.41
212	4.791	8.96	13.18	14.64	11.03
213	4.759	9.01	13.16	14.59	12.04
214	4.77	8.96	13.07	14.51	18.71
215	4.776	8.95	13.17	14.62	13.36
216	4.804 / 4.8	8.98 / 9.0	13.31 / 13.3	14.8	8.8 / 8.0
217	4.777	8.99	13.19	14.64	10.5
218	4.767	8.75	13.17	14.61	9.11
219	3.76	3.977	5.846	6.485	11.42
220	1.758	0.134	-0.193	-0.181	0.654
221	0.784	0.128	-0.221	-0.197	-0.918
222	0.039	0.119	-0.243	-0.209	-0.905
223	0.016	0.128	-0.254	-0.218	-0.969
224	0.022	7.72	-0.262	-0.225	-1.056
225	0.022	9.73	-0.272	-0.233	-1.494
226	0.019	1.68	-0.283	-0.243	22.05
227	0.014	0.13	-0.297	-0.254	47.78
228	0.012	0.094	-0.305	-0.261	47.9
229	7.02	0.134	3.838	5.815	24.54
230	7.07	0.119	14.93	19.26	-0.38
231	0.251	0.087	21	18.23	-0.373
232	3.829	0.128	1.968	1.643	-0.684
233	5.168	0.101	-0.306	-0.35	-0.862
234	4.217	0.092	-0.33	-0.354	-0.906
235	4.199	-0.293	-0.325	-0.349	-0.915
236	1.145	0.094	-0.389	-0.356	-0.844
237	0.002	0.029	-0.407	-0.349	-1.014
238	-0.029	0.058	-0.41	-0.35	-1.059
239	5.003	13.5	17.42	21.33	40.48
240	9.08	17.87	21.16	32.04	89.4
241	9.18	17.84	21.17	32.33	89.2
242	9.19	17.85	21.16	32.35	89.6
243	6.406	10.72	14.26	18.7	68.97
244	4.267	9.73	12.16	13.09	48.14
245	4.219	9.74	12.2	13.09	47.92
246	4.213	9.75	12.21	13.09	48.07
247	4.213	9.73	12.19	13.08	48.24

END

zero bias

mid bias

high bias

zero

Hi

Mid

D-142

**APPENDIX D-7**  
**EMISSION RATE CALCULATIONS**



SCE EGS COMPLIANCE

PPM TO LB/HR WORKSHEET

Test #	Load	Condition	Run #	flow rate (dscf/min)	NOx		CO		TGNMO		NH3	
					ppm	lb/hr	ppm	lb/hr	ppm	lb/hr	ppm	lb/hr
1	Full	FGR on	Average:	676063	53.4	263	213	639				
2	Full	FGR + Urea	Average:	665233	45.4	220	214	631			5.5	10
3	Full	FGR + Urea	Tray 1	657293					158	264		
			Tray 2	657293					159	265		
			Average:	657293	45.8	219	204	595	159	265	6.6	12
4	Full	Baseline	Tray 1	660325					142	238		
			Tray 2	660325					117	196		
			Average:	660325	61.7	297	196	574	130	217		
6	Mid	Baseline	Average:	516124	42.9	161	146	334				
7	Mid	FGR on	Average:	517347	31.2	118	144	330				
8	Mid	FGR + Urea	Average:	514175	27.0	101	142	324			4.0	5.5
10	Low	Baseline	Average:	258370	20.8	39	0.7	1				
11	Low	FGR on	Average:	262007	13.3	25	9.1	11				

M = Molecular Weight = | 46.01 | 28.01 | 16.04 | 17.03 |

E = Emission Rate, lb/hr  
 C<sub>g</sub> = Gas Concentration, ppm  
 Q = Stack Gas Flowrate, dscfm

$$E = \frac{C_g \cdot M}{379 \times 10^6} \cdot Q \cdot 60 \frac{\text{min}}{\text{hr}}$$

379 x 10<sup>6</sup> = conversion factor, scf/lb-mole

SCAQMD METHOD 100.1, CORRECTED TEST AVERAGES

Test #/Description	Time Start/Stop	Measurement Parameter	Bias Results				Calibration Bias		Calibration Gas		Constituent Average	
			Zero Bias		Pre	Post	Pre	Post	Actual	Raw	Corrected	
			Pre	Post								
Full Load FGR ON (Test 1)	0915/1014	O2 (%)	0.1	0.0	4.1	4.1	4.1	4.2	3.2	3.3		
		NOx (ppm)	-0.7	-0.1	46.1	47.1	48.0	51.9	53.4			
		CO (ppm)	-1.5	-1.1	250.3	250.8	250.0	213.4	213.1			
		CO2 (%)	0.0	0.1	9.6	9.6	9.8	9.8	10.0			
Full Load FGR and Urea ON Run #1 (Test 2)	1100/1159	O2 (%)	0.0	0.0	4.1	4.1	4.1	4.2	3.1	3.2		
		NOx (ppm)	-0.1	-0.2	47.1	47.0	48.0	44.5	45.4			
		CO (ppm)	-1.1	-1.1	250.8	252.2	250.0	215.3	214.2			
		CO2 (%)	0.1	0.0	9.6	9.6	9.8	9.8	10.0			
Full Load FGR and Urea ON Run #2 (Test 3)	1301/1400	O2 (%)	0.0	0.0	4.1	4.1	4.1	4.2	3.1	3.2		
		NOx (ppm)	-0.2	0.0	47.0	46.8	48.0	44.7	45.8			
		CO (ppm)	-1.1	-1.1	252.2	251.5	250.0	205.2	203.9			
		CO2 (%)	0.0	0.0	9.6	9.6	9.8	9.8	10.0			
Full Load Baseline (Test 4)	1500/1559	O2 (%)	0.0	0.0	4.1	4.1	4.1	4.2	3.0	3.1		
		NOx (ppm)	0.0	0.1	46.8	46.9	48.0	60.2	61.7			
		CO (ppm)	-1.1	-1.1	251.5	251.9	250.0	197.2	196.1			
		CO2 (%)	0.0	0.0	9.6	9.6	9.8	9.8	10.0			
Mid-Load Baseline (Test 6)	1030/1129	O2 (%)	0.0	0.0	4.2	4.1	4.1	4.2	3.6	3.6		
		NOx (ppm)	-0.7	-0.5	46.7	46.5	48.0	41.6	42.9			
		CO (ppm)	-1.6	-1.6	249.7	250.6	250.0	145.2	145.8			
		CO2 (%)	0.1	0.2	9.7	9.8	9.8	9.7	9.7			
Mid-Load FGR ON (Test 7)	1230/1329	O2 (%)	0.0	0.0	4.1	4.1	4.1	4.2	3.6	3.7		
		NOx (ppm)	-0.5	-0.2	46.5	46.2	48.0	30.0	31.2			
		CO (ppm)	-1.6	-1.4	250.6	252.2	250.0	144.4	144.2			
		CO2 (%)	0.2	0.2	9.8	9.9	9.8	9.8	9.7			
Mid-Load FGR and Urea ON (Test 8)	1417/1516	O2 (%)	0.0	0.0	4.1	4.1	4.1	4.2	3.6	3.7		
		NOx (ppm)	-0.2	-0.1	46.2	45.7	48.0	25.8	27.0			
		CO (ppm)	-1.4	-1.2	252.2	250.8	250.0	142.3	142.0			
		CO2 (%)	0.2	0.2	9.9	9.9	9.8	9.8	9.6			

3%

54

21

45

21

46

20

62

19

44

15

32

150

28

148

SCAQMD METHOD 100.1, CORRECTED TEST AVERAGES

Test #/Description	Time Start/Stop	Measurement Parameter	Bias Results						Calibration Gas		Constituent Average Corrected
			Zero Bias		Calibration Bias		Actual	Corrected			
			Pre	Post	Pre	Post					
Low Load Baseline (Test 10)	2326/0025	O2 (%)	0.0	0.0	4.2	4.2	4.2	4.8	4.8	23.0	
		NOx (ppm)	-0.1	0.0	21.1	21.0	21.0	20.8	20.8	0.7	
		CO (ppm)	-1.0	-0.9	48.2	47.9	50.0	-0.3	0.7	0.8	
		CO2 (%)	0.1	0.1	9.7	9.7	9.8	8.9	8.9	10.1	
Low Load FGR ON (Test 11)	0117/0216	O2 (%)	0.0	0.0	4.2	4.2	4.2	4.8	4.8	14.0	
		NOx (ppm)	0.0	-0.2	21.0	21.0	21.0	13.3	13.3	9.1	
		CO (ppm)	-0.9	-0.9	47.9	47.9	50.0	8.0	9.1	9.0	
		CO2 (%)	0.1	0.1	9.7	9.7	9.8	9.0	9.0	9.0	



**APPENDIX D-8**

**QA/QC PERFORMANCE MEASUREMENTS SUMMARY TABLES**

D-150

Table D-8-1. SCAQMD Method 100.1 instrument calibration results, full load, FGR ON, 3/22/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	0.0	-1.5	-0.8
Post-Test Response	0.0	-0.1	-1.6	-0.4
<b>High Range Calibration Response</b>				
Pre-Test Response	9.1	17.7	449.4	93.8
Post-Test Response	9.0	17.7	454.8	92.8
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.7	251.4	48.3
Post-Test Response	4.1	9.7	250.2	48.0
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.1	0.0	-1.5	-0.7
Post-Test Response	0.0	0.1	-1.1	-0.1
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.1	9.6	250.3	46.1
Post-Test Response	4.1	9.6	250.8	47.1
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.4%	0.3%	0.3%	1.6%
Pre-Test Mid	0.0%	1.0%	0.3%	0.3%
Pre-Test Zero	0.0%	0.0%	0.3%	0.8%
Post-Test High	1.4%	0.3%	0.8%	0.6%
Post-Test Mid	1.0%	1.0%	0.0%	0.0%
Post-Test Zero	0.0%	0.5%	0.3%	0.4%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	1.0%	0.5%	0.2%	2.2%
Post-Test	0.0%	0.5%	0.1%	0.9%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.2%	0.8%	0.6%	0.1%
Post-Test	0.4%	0.6%	0.2%	0.1%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Full Load, FGR ON	0.0%	0.5%	0.0%	0.4%
<b>Calibration Drift (criteria: 3%)</b>				
Full Load, FGR ON	1.0%	0.0%	0.2%	0.3%

Table D-8-2. SCAQMD Method 100.1 instrument calibration results, full load FGR and UREA ON, 3/22/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	-0.1	-1.6	-0.2
Post-Test Response	-0.1	-0.1	-1.6	0.0
<b>High Range Calibration Response</b>				
Pre-Test Response	9.1	17.7	457.0	92.4
Post-Test Response	9.1	17.7	456.0	92.0
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.7	252.9	47.8
Post-Test Response	4.2	9.7	252.6	47.7
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.0	0.0	-1.1	-0.2
Post-Test Response	0.0	0.0	-1.1	0.0
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.1	9.6	252.2	47.0
Post-Test Response	4.1	9.6	251.5	46.8
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.4%	0.3%	1.2%	0.2%
Pre-Test Mid	0.0%	1.0%	0.6%	0.2%
Pre-Test Zero	0.0%	0.5%	0.3%	0.2%
Post-Test High	0.4%	0.3%	1.0%	0.2%
Post-Test Mid	0.0%	1.0%	0.5%	0.3%
Post-Test Zero	1.0%	0.5%	0.3%	0.0%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	1.0%	0.5%	0.1%	0.8%
Post-Test	1.0%	0.5%	0.2%	0.9%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.2%	0.6%	0.1%	0.2%
Post-Test	0.7%	0.6%	0.1%	0.2%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Full Load, FGR and UREA ON	1.0%	0.0%	0.0%	0.2%
<b>Calibration Drift (criteria: 3%)</b>				
Full Load, FGR and UREA ON	0.0%	0.0%	0.1%	0.1%

Table D-8-3. SCAQMD Method 100.1 instrument calibration results, full load Baseline, 3/22/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	-0.1	-0.1	-1.6	0.0
Post-Test Response	0.0	-0.1	-1.6	0.0
<b>High Range Calibration Response</b>				
Pre-Test Response	9.1	17.7	456.0	92.0
Post-Test Response	9.1	17.7	457.0	91.8
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.7	252.6	47.7
Post-Test Response	4.1	9.7	251.7	47.5
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.0	0.0	-1.1	0.0
Post-Test Response	0.0	0.0	-1.1	0.1
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.1	9.6	251.5	46.8
Post-Test Response	4.1	9.6	251.9	46.9
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.4%	0.3%	1.0%	0.2%
Pre-Test Mid	0.0%	1.0%	0.5%	0.3%
Pre-Test Zero	1.0%	0.5%	0.3%	0.0%
Post-Test High	0.4%	0.3%	1.2%	0.4%
Post-Test Mid	1.0%	1.0%	0.3%	0.5%
Post-Test Zero	0.0%	0.5%	0.3%	0.0%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	1.0%	0.5%	0.2%	0.9%
Post-Test	0.0%	0.5%	0.0%	0.6%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.7%	0.6%	0.1%	0.2%
Post-Test	0.8%	0.6%	0.2%	0.3%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Full Load, Baseline	1.0%	0.0%	0.0%	0.0%
<b>Calibration Drift (criteria: 3%)</b>				
Full Load, Baseline	1.0%	0.0%	0.2%	0.2%

Table D-8-4. SCAQMD Method 100.1 instrument calibration results, mid load Stratification, 3/23/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	NR	NR	-1.1
Post-Test Response	0.0	NR	NR	-0.9
<b>High Range Calibration Response</b>				
Pre-Test Response	9.2	NR	NR	93.8
Post-Test Response	9.1	NR	NR	92.6
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	NR	NR	48.0
Post-Test Response	4.2	NR	NR	47.4
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.1	NR	NR	-1.1
Post-Test Response	0.0	NR	NR	-0.7
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.2	NR	NR	47.2
Post-Test Response	4.2	NR	NR	46.7
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.1%			1.6%
Pre-Test Mid	0.1%			0.0%
Pre-Test Zero	0.3%			1.1%
Post-Test High	0.1%			0.4%
Post-Test Mid	0.1%			0.6%
Post-Test Zero	0.4%			0.9%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	0.3%			0.8%
Post-Test	0.4%			0.7%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.1%			0.3%
Post-Test	0.2%			0.4%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Mid Load, Stratification	0.7%			0.3%
<b>Calibration Drift (criteria: 3%)</b>				
Mid Load, Stratification	0.2%			0.6%

Table D-8-5. SCAQMD Method 100.1 instrument calibration results, mid load Baseline, 3/23/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	0.1	-1.6	-0.9
Post-Test Response	-0.1	0.1	-1.6	-0.6
<b>High Range Calibration Response</b>				
Pre-Test Response	9.1	18.0	453.7	92.6
Post-Test Response	9.1	18.1	454.7	91.9
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.9	250.9	47.4
Post-Test Response	4.2	9.9	251.7	47.1
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.0	0.1	-1.6	-0.7
Post-Test Response	0.0	0.2	-1.6	-0.5
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.2	9.7	249.7	46.7
Post-Test Response	4.1	9.8	250.6	46.5
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.1%	1.1%	0.5%	0.4%
Pre-Test Mid	0.1%	0.2%	0.2%	0.6%
Pre-Test Zero	0.4%	0.6%	0.3%	0.9%
Post-Test High	0.1%	1.7%	0.7%	0.3%
Post-Test Mid	0.3%	0.2%	0.3%	0.9%
Post-Test Zero	0.5%	0.7%	0.3%	0.6%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	0.4%	0.7%	0.2%	0.7%
Post-Test	0.4%	0.7%	0.2%	0.6%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.2%	1.0%	0.0%	0.4%
Post-Test	0.0%	1.0%	0.1%	0.5%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Mid Load, Baseline	0.1%	0.0%	0.0%	0.3%
<b>Calibration Drift (criteria: 3%)</b>				
Mid Load, Baseline	0.2%	0.4%	0.2%	0.3%

Table D-8-6. SCAQMD Method 100.1 instrument calibration results, mid load FGR ON, 3/23/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	-0.1	0.1	-1.6	-0.6
Post-Test Response	0.0	0.2	-1.5	-0.3
<b>High Range Calibration Response</b>				
Pre-Test Response	9.1	18.1	454.7	91.9
Post-Test Response	9.2	18.1	456.4	90.8
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.9	251.7	47.1
Post-Test Response	4.2	9.9	252.6	46.8
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.0	0.2	-1.6	-0.5
Post-Test Response	0.0	0.2	-1.4	-0.2
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.1	9.8	250.6	46.5
Post-Test Response	4.1	9.9	252.2	46.2
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.1%	1.7%	0.7%	0.3%
Pre-Test Mid	0.3%	0.2%	0.3%	0.9%
Pre-Test Zero	0.5%	0.7%	0.3%	0.6%
Post-Test High	0.1%	1.7%	1.1%	1.4%
Post-Test Mid	0.3%	0.2%	0.5%	1.2%
Post-Test Zero	0.5%	1.0%	0.3%	0.3%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	0.4%	0.7%	0.2%	0.6%
Post-Test	0.4%	0.2%	0.1%	0.6%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.0%	1.0%	0.1%	0.5%
Post-Test	0.1%	1.2%	0.1%	0.3%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Mid Load, FGR ON	0.0%	0.3%	0.0%	0.3%
<b>Calibration Drift (criteria: 3%)</b>				
Mid Load, FGR ON	0.0%	0.0%	0.2%	0.3%

Table D-8-7. SCAQMD Method 100.1 instrument calibration results, mid load FGR and UREA ON, 3/23/94

	O <sub>2</sub> (%)	CO <sub>2</sub> (%)	CO (ppm)	NO <sub>x</sub> (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	0.2	-1.5	-0.3
Post-Test Response	-0.1	0.2	-1.7	-0.1
<b>High Range Calibration Response</b>				
Pre-Test Response	9.2	18.1	456.4	90.8
Post-Test Response	9.2	18.2	457.9	90.9
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.9	252.6	46.8
Post-Test Response	4.1	10.1	252.7	46.8
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.0	0.2	-1.4	-0.2
Post-Test Response	0.0	0.2	-1.2	-0.1
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.1	9.9	252.2	46.2
Post-Test Response	4.1	9.9	250.8	45.7
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.1%	1.7%	1.1%	1.4%
Pre-Test Mid	0.3%	0.2%	0.5%	1.2%
Pre-Test Zero	0.5%	1.0%	0.3%	0.3%
Post-Test High	0.2%	2.1%	1.4%	1.3%
Post-Test Mid	0.6%	0.8%	0.5%	1.2%
Post-Test Zero	0.6%	1.0%	0.3%	0.1%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	0.4%	0.2%	0.1%	0.6%
Post-Test	0.1%	0.7%	0.4%	1.1%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.1%	1.2%	0.1%	0.3%
Post-Test	0.4%	0.8%	0.1%	0.5%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Mid Load, FGR and UREA ON	0.1%	0.0%	0.0%	0.1%
<b>Calibration Drift (criteria: 3%)</b>				
Mid Load, FGR and UREA ON	0.4%	0.7%	0.0%	0.0%

Table D-8-8. SCAQMD Method 100.1 instrument calibration results, low load Stratification, 3/23/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 500	0- 100
High Range	9.14	17.75	451	92.2
Mid Range	4.20	9.89	250	48.0
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	NR	NR	0.1
Post-Test Response	0.0	NR	NR	-0.7
<b>High Range Calibration Response</b>				
Pre-Test Response	9.2	NR	NR	92.3
Post-Test Response	9.1	NR	NR	93.1
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	NR	NR	47.5
Post-Test Response	4.2	NR	NR	47.7
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.1	NR	NR	-0.5
Post-Test Response	0.1	NR	NR	-0.7
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.2	NR	NR	47.2
Post-Test Response	4.2	NR	NR	47.3
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.1%			0.1%
Pre-Test Mid	0.0%			0.5%
Pre-Test Zero	0.3%			0.1%
Post-Test High	0.2%			0.9%
Post-Test Mid	0.3%			0.3%
Post-Test Zero	0.1%			0.7%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	0.1%			0.3%
Post-Test	0.0%			0.3%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.2%			0.6%
Post-Test	0.2%			0.4%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Low Load, Stratification	0.3%			0.8%
<b>Calibration Drift (criteria: 3%)</b>				
Low Load, Stratification	0.3%			0.2%

Table D-8-9. SCAQMD Method 100.1 instrument calibration results, low load, Baseline, 3/23/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 100	0- 25
High Range	9.14	17.75	90	21.0
Mid Range	4.20	9.89	50	12.3
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	0.0	-1.0	-0.1
Post-Test Response	0.0	0.0	-1.0	-0.2
<b>High Range Calibration Response</b>				
Pre-Test Response	9.2	17.8	89.7	21.3
Post-Test Response	9.2	17.9	89.9	21.2
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.7	48.2	12.5
Post-Test Response	4.2	9.8	48.1	12.3
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.0	0.1	-1.0	-0.1
Post-Test Response	0.0	0.1	-0.9	0.0
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.2	9.7	48.2	21.1
Post-Test Response	4.2	9.7	47.9	21.0
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.6%	0.4%	0.3%	1.1%
Pre-Test Mid	0.1%	0.8%	1.8%	0.6%
Pre-Test Zero	0.3%	0.1%	1.0%	0.4%
Post-Test High	0.5%	0.7%	0.1%	0.6%
Post-Test Mid	0.0%	0.6%	1.9%	0.2%
Post-Test Zero	0.3%	0.2%	1.0%	0.9%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	0.2%	0.4%	0.0%	0.8%
Post-Test	0.1%	0.4%	0.2%	0.6%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.0%	1.0%	1.2%	0.2%
Post-Test	0.1%	0.9%	1.4%	0.2%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Low Load, Baseline	0.0%	0.3%	0.0%	0.5%
<b>Calibration Drift (criteria: 3%)</b>				
Low Load, Baseline	0.1%	0.2%	0.1%	0.8%

Table D-8-10. SCAQMD Method 100.1 instrument calibration results, low load, FGR ON, 3/24/94

	O2 (%)	CO2 (%)	CO (ppm)	NOx (ppm)
<b>Calibration Gas Concentration</b>				
Operating Range	0- 10	0- 20	0- 100	0- 25
High Range	9.14	17.75	90	21.0
Mid Range	4.20	9.89	50	12.3
<b>Zero Calibration Response</b>				
Pre-Test Response	0.0	0.0	-1.0	-0.2
Post-Test Response	0.0	0.1	-1.1	-0.4
<b>High Range Calibration Response</b>				
Pre-Test Response	9.2	17.9	89.9	21.2
Post-Test Response	9.2	17.9	89.6	21.2
<b>Mid Range Calibration Response</b>				
Pre-Test Response	4.2	9.8	48.1	12.3
Post-Test Response	4.2	9.8	48.1	12.2
<b>Zero Gas System Bias Response</b>				
Pre-Test Response	0.0	0.1	-0.9	0.0
Post-Test Response	0.0	0.1	-0.9	-0.2
<b>Cal-Gas System Bias Response</b>				
Pre-Test Response	4.2	9.7	47.9	21.0
Post-Test Response	4.2	9.7	47.9	21.0
<b>Analyzer Calibration Error (criteria: 2%)</b>				
Pre-Test High	0.5%	0.7%	0.1%	0.6%
Pre-Test Mid	0.0%	0.6%	1.9%	0.2%
Pre-Test Zero	0.3%	0.2%	1.0%	0.9%
Post-Test High	0.5%	0.5%	0.4%	0.6%
Post-Test Mid	0.1%	0.7%	1.9%	0.4%
Post-Test Zero	0.3%	0.3%	1.1%	1.6%
<b>Sampling System Bias Error (criteria: 5%)</b>				
Pre-Test	0.1%	0.4%	0.2%	0.6%
Post-Test	0.1%	0.1%	0.2%	0.6%
<b>Linearity (criteria: 1%)</b>				
Pre-Test	0.1%	0.9%	1.4%	0.2%
Post-Test	0.1%	1.1%	1.2%	0.1%
<b>Zero Calibration Drift (criteria: 3%)</b>				
Low Load FGR ON	0.1%	0.5%	0.0%	0.8%
<b>Calibration Drift (criteria: 3%)</b>				
Low Load FGR ON	0.2%	0.1%	0.0%	0.2%

**APPENDIX E**  
**RECORDS SUPPORTING SCAQMD METHOD 25.1 MEASUREMENTS**



**APPENDIX E-1**  
**ANALYTICAL REPORTS**





AIR MEASUREMENT SERVICES, INC.

M25-023-FR

April 5, 1994

Mr. Chad Garretson  
Acurex Environmental Coporation  
555 Clyde Avenue  
Mountain View, California 94039

**RE: SCAQMD METHOD 25.1 RESULTS**

Dear Mr. Garretson:

Please find enclosed the corrected results of the SCAQMD Method 25.1 testing you conducted on March 22, 1994.

If you have any questions concerning the results, please call me at (805) 498-8781. HORIZON appreciates the opportunity to provide Acurex Enviornmental with our services and we look forward to working with you again in the future.

Sincerely,

HORIZON AIR MEASUREMENT SERVICES, INC.

A handwritten signature in cursive script, appearing to read "Edward S. Swede".

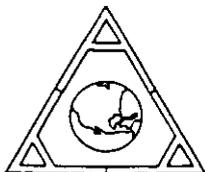
Edward S. Swede  
Air Quality Technician

ES:img

Enclosures

	TOTAL COMBUSTION ANALYSIS RESULTS		TEST #3		
	TEST #4				
Tank #	19	17	76	77	79
Trap #	18	17	13	33	19
Methane in Tank	1.9	1.5	2.2	2.2	<1
TNMHC, Tank (noncond.)	2.3	2.4	2.7	3.1	2.4
TNMHC - condensables	167.1	141.4	182	183	25
TNMHC - Total	169.4	143.9	184.7	186.3	27.2
CO Concentration	195.0	181.0	188.0	190.0	<1
CO2 Concentration	94700	93900	89900	93100	37
Sample Tank Vol.	12.245	12.328	12.211	12.300	12.338
Initial Pressure	1.3	1.3	1.3	1.3	1.3
Initial Temperature	292	292	292	292	292
Final Pressure	652	688	650	637	561
Final Temperature	292	292	292	292	292
Sample Volume	10.52	11.18	10.46	10.33	9.12
Analysis Pressure	800	800	800	800	800
Analysis Temperature	292	292	292	292	292
ICV Volume	2.266	2.266	2.266	2.266	2.266
ICV Final Pressure	800	800	800	800	800
ICV Final Temp.	292	292	292	292	292
CO2 in ICV	776.0	698.0	840.0	835.0	100.0
TNMHC, Trap(cond.)	167	141	182	183	25
Stack Total TNMHC	169	144	185	186	27

NOTE: All hydrocarbon values are in terms of ppm, v/v, as methane.



AtmAA Inc.

23917 Craftsman Rd., Calabasas, CA 91302 • (818) 223-3277 • FAX (818) 223-8250

environmental consultants  
laboratory services

LABORATORY ANALYSIS REPORT

CO, CH4, CO2, & Total Gaseous Non-Methane Organics (TGNMO)  
Analysis in Tanks and Traps by SCAQMD Method 25 (FID/TCA)

Report Date: March 30, 1994  
Client: HorizonAcurex  
P.O. No.: Verbal  
Client Project No.: M25-023  
Source Location: Horizon  
Source ID: Not Given

Date Received: March 25, 1994  
Date Analyzed: March 25, 1994

AtmAA Lab No.	Sample ID			CO	CH4	CO2	TGNMO	CO2 in ICV (Concentration in ppmv)	P1	P2
	Tank	Trap	ICV							
90844-6	19	18	28	195	1.92	94700	2.32	776	652	800
90844-7	17	17	40	181	1.54	93900	2.42	698	688	800
90844-8	76	13	M1	188	2.15	89900	2.74	840	650	800
90844-9	77	33	13	190	2.16	93100	3.06	835	637	800
90844-10	79	19	24	<1	<1	36.8	2.37	100	561	800
90844-11	System blank							12.0		

P1 - Initial Pressure, mm Hg  
P2 - Final Pressure, mm Hg

  
Michael L. Porter  
Laboratory Director

**QUALITY ASSURANCE SUMMARY**  
(Repeat Analysis)

Client Proj. No.: M25-023  
Date Received: March 25, 1994  
Date Analyzed: March 25, 1994

Components	Sample ID	Repeat	Analysis	Mean Conc.	% Diff. From Mean
		Run #1	Run #2		
(Concentration in ppmv)					
CO	TK-19	195	195	195	0.0
	TK-77	190	190	190	0.0
CH4	TK-77	2.13	2.20	2.16	1.6
CO2	No Repeat				
TGNMO	TK-77	2.81	3.30	3.06	8.0
CO2 in ICV (in trap, transfer tanks)	ICV-40	682	713	698	2.2

*A set of 5 TCA samples, laboratory numbers 90844-(6-10) was analyzed for CO, CH4, CO2, & TGNMO. Agreement between repeat analyses is a measure of precision and is shown above in the column "% Difference from Mean." Repeat analyses are an important part of AtmAA's quality assurance program. The average % Difference from Mean for 5 repeat measurements from the sample set of 5 TCA samples is 2.4%.*

*Gas standards (containing CO, CH4, CO2 and propane) used for TCA analyses, were prepared and certified by Scott Specialty Gases.*





CHAIN OF CUSTODY RECORD

Client/Project Name		Project Location		ANALYSES			
Acurex		Horizon					
Project No.		Field Logbook No.					
M25-023							
Sampler: (Signature)		Chain of Custody Tape No.					
<i>Edward S. Sweda</i>							
Sample No./ Identification	Date	Time	Lab Sample Number	Type of Sample	Trap #	Remarks	
ICV# 21	3/25/94		90844-11	Trap Burn	33	System blank	
" 13			" - 9		77		
" M1			" - 8		13	Field Blank	
" 24			" - 10		19		
" 40			" - 7		17		
" 28			" - 10		18		
Relinquished by: (Signature)		Date	Time	Received by: (Signature)		Date	Time
<i>Edward S. Sweda</i>		3/25/94	1200				
Relinquished by: (Signature)		Date	Time	Received by: (Signature)		Date	Time
Relinquished by: (Signature)		Date	Time	Received for Laboratory: (Signature)		Date	Time
				<i>[Signature]</i>		3/25/94	1200
Sample Disposal Method:		Disposed of by: (Signature)				Date	Time
SAMPLE COLLECTOR		ANALYTICAL LABORATORY					
HORIZON AIR MEASUREMENT SERVICES 996 Lawrence Drive, Suite 108 Newbury Park, CA 91320 (805) 498-8781		Atm A.A.					
						No: 2237	



**SCAQMD METHOD 25.1**  
**Rental Equipment Preparation Form**  
**and Packing List**

Client/Contact: <i>Chad Garretson</i>	# of Tanks: <i>7</i>
Shipping Destination:	# of Traps: <i>7</i>
Shipped Via:	# of Rotos: <i>0</i>

Turn Around Requested:

	PAIRS		INITIAL PRESSURE (Torr)		LEAK CHECK		DATE RECONDITIONED	
	TANKS	<i>10</i>	<i>13</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<i>3/16/94</i>
	<i>76</i>	<i>77</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<i>"</i>	<i>"</i>
	<i>17</i>	<i>19</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<i>"</i>	<i>"</i>
	<i>79</i>	<i>80</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<i>"</i>	<i>"</i>
TRAPS	<i>14</i>	<i>12</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<i>"</i>	<i>"</i>
	<i>13</i>	<i>33</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<i>"</i>	<i>"</i>
	<i>17</i>	<i>18</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>	<i>"</i>	<i>"</i>
		<i>19</i>			<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>		<i>"</i>
ROTOS								
MISC	Data Sheets: <i>4</i>							
	Ice Chests: <i>0</i>							
	Dry Ice (lbs.): <i>0</i>							

Prepared by: *Chad Garretson* Date: *3/16/94* Horizon Air Measurement Services, Inc.

**APPENDIX E-2**  
**FIELD TEST DATA SHEETS**



TOTAL COMBUSTION ANALYSIS  
 SCAQMD METHOD 25  
 FIELD SAMPLING DATA SHEET

Job #: 9585  
 Facility: SOE Etiwanda  
 Location: Port C  
 Date: 3/22/94  
 Operator: B. Day

Control Device: \_\_\_\_\_  
 Sample Location: Port C  
 Ambient Temperature: \_\_\_\_\_  
 Barometric Pressure: 29.91

SAMPLE A

Tank #: 76 Trap #: 13  
 Initial Vacuum: 26  
 Final Vacuum: 1.8/17 650  
Roto #2 800

SAMPLE B

Tank #: 77 Trap #: 33  
 Initial Vacuum: 28  
 Final Vacuum: 4" 637"  
Roto #1 800

TIME	VACUUM ("Hg)	FLOW (cc/min)
1301	26	243
1311	26	↓
1321	26	↓
1331	24	↓
1341	18	↓
1351	6.5	↓
1401	3.0	↓

TIME	VACUUM ("Hg)	FLOW (cc/min)
1301	28	245
1311	27	↓
1321	26	↓
1331	24.5	↓
1341	18	↓
1351	6.5	↓
1401	3.0	↓

Leak Rate Pre Test: PASS  
 Post Test: ✓



TOTAL COMBUSTION ANALYSIS  
 SCAQMD METHOD 25  
 FIELD SAMPLING DATA SHEET

Job #: 9585  
 Facility: SCE Etiwanda  
 Location: Unit 3  
 Date: 3/22/94  
 Operator: B. Day

Control Device: \_\_\_\_\_  
 Sample Location: Part C  
 Ambient Temperature: 59°F  
 Barometric Pressure: 29.91

SAMPLE A

SAMPLE B

Tank #: 10 Trap #: 14  
 Initial Vacuum: 25"  
 Final Vacuum: \_\_\_\_\_

Tank #: 13 Trap #: 12  
 Initial Vacuum: 27.5"  
 Final Vacuum: \_\_\_\_\_

Roto #2 243 cc/min = .6

Roto #1 245 cc/min = .6

TIME	VACUUM ("Hg)	FLOW (cc/min)
1100	25"	243
1110	19.5"	
1120	14"	
1130	5.5"	
1140		
1150		
1200		

TIME	VACUUM ("Hg)	FLOW (cc/min)
1100	27.5"	245
1110	26.3	
1120	24.7	
1130	20.0	
1140	12.5	
1150	4.0	
1200	3.0	

Leak Rate Pre Test: Good/Pass

Post Test: \_\_\_\_\_

Reduced Flow @ 1120  
 Roto #2 200 cc/min  
 Roto #1 200 cc/min

TOTAL COMBUSTION ANALYSIS  
 SCAQMD METHOD 25  
 FIELD SAMPLING DATA SHEET

Job #: 9585  
 Facility: SE  
 Location: EGS #3  
 Date: 3/23/94  
 Operator: CAF

Control Device: \_\_\_\_\_  
 Sample Location: \_\_\_\_\_  
 Ambient Temperature: \_\_\_\_\_  
 Barometric Pressure: 29.91

SAMPLE A

Tank #: 71 Trap #: 19  
 Initial Vacuum: 28.0"  
 Final Vacuum: 6.5"

SAMPLE B

Tank #: \_\_\_\_\_ Trap #: \_\_\_\_\_  
 Initial Vacuum: \_\_\_\_\_  
 Final Vacuum: \_\_\_\_\_

Blank was collected by pass N<sub>2</sub> in tank; trap was submitted 29 IS

TIME	VACUUM ("Hg)	FLOW (cc/min)
1310	28.0	250
1317	26.4	↓
1320	22.2	
1330	16.4	
1341	10.8	
1350	6.5	

TIME	VACUUM ("Hg)	FLOW (cc/min)

Leak Rate Pre Test: OK  
 Post Test: ✓

CAF

**APPENDIX F**

**RECORDS SUPPORTING AMMONIA CONCENTRATION MEASUREMENTS**



**APPENDIX F-1**  
**DRAFT METHOD 207.1**



## SCAQMD METHOD 207.1

ANALYTICAL METHOD FOR AMMONIA AND AMMONIUM COMPOUNDS  
FROM STATIONARY SOURCES  
NESSLER COLORIMETRY

## 1. Principle and Applicability

## 1.1 Principle

Free and combined ammonia are withdrawn from the source using a Smith-Greenburg impinger train. The gas or particulate is collected in the train probe and impingers containing sulfuric acid solution. The solution is analyzed for ammonia by colorimetry after reaction with Nessler reagent.

## 1.2 Applicability

This method is applicable for the determination of ammonia and ammonium ion in furnace stacks, catalytic cracking plant regenerator emissions, galvanizing operations, and other stationary sources when approved by the Executive Officer. The recommended range is  $0.4 \text{ mg/m}^3$  to  $20 \text{ mg/m}^3$  for a sample of one cubic meter.

1.3 The range and sensitivity of the method has not been established. Commercially prepared, APHA approved reagent has been found with a response of about  $430 \text{ ug NH}_3$  in a  $50 \text{ mL}$  aliquot per optical density (OD) at  $440 \text{ nm}$  using a  $1 \text{ cm}$  cell. This factor applies from  $20$  to  $160 \text{ ug NH}_3$ . A slightly reduced sensitivity was found at higher concentrations. Very high concentrations shift the absorbance to the  $450$  to  $500 \text{ nm}$  range. Based on the above response and a train recovery volume of  $500 \text{ mL}$ , the estimated sensitivity is approximately  $0.1 \text{ mg NH}_3$ .

## 1.4 Interferences

Calcium, iron, magnesium, and sulfide interfere by causing turbidity after the addition of Nessler reagent. Inherent sample color and suspended matter also interfere with direct Nesslerization. Because direct Nesslerization is subject to a number of possible interferences, at least one sample per set must be checked for color and/or turbidity prior to reagent addition, and by spike and recovery to confirm that no interferences exist. In this case, a set of samples is a sample or series of samples taken from one sampling point during one day of testing.

However, blanking and spike recovery may need to be performed more often if emission characteristics are expected to change frequently during one day.

When interferences exist, distill the sample prior to analysis. (See Standard Methods for the Examination of Water and Wastewater, 17th Edition).

#### 1.5 Precision and Accuracy

Precision and accuracy have not been determined.

### 2. Field Procedures

A copy of the field procedures can be found in the District's Source Test Manual.

### 3. Laboratory Procedures

#### 3.1 Apparatus

3.1.1 A schematic of the sampling train is shown in Figure 207.1L.

##### a. Impinger Train

The train consists of four impingers connected in series with leak-free non-contaminating fittings. The first and second Smith-Greenburg impingers shall have standard tips, the third and fourth impingers shall have a modified tip (one-half in. ID glass tube) extending to about one-half in. from the bottom of the flask. The first two impingers each contain 100 mL of 0.1 N  $\text{H}_2\text{SO}_4$ . The third impinger is empty. The fourth (last) impinger contains silica gel.

##### b. Probe

Probe may be of 316 stainless steel, quartz, or glass. Quartz and glass must be used for corrosive samples.

##### c. Pre-filter (optional)

A pre-filter may be inserted to remove particulate matter from the sampling train.

#### 3.1.2 Sample Recovery

##### a. Wash bottle.

##### b. 500 mL or 1000 mL graduated cylinder, with stopper.

- c. Polyethylene bottles, 500 mL or 1000 mL

### 3.1.3 Sample Analysis

- a. Perkin Elmer 552 Spectrophotometer, or equivalent.
- b. Spectrophotometer cells, 1 cm.
- c. Volumetric flasks, 50 mL, one for each sample, standard and blank.
- d. Pipettes, Class A, 2 mL, 4 mL, 8 mL, 10 mL, 12 mL, and 14 mL, or burette for calibration curve.
- e. Graduated cylinders, 25 mL, 50 mL, 100 mL, and 250 mL.

## 3.2 Reagents

### 3.2.1 Sampling

Unless otherwise indicated, all reagents are to conform to the specifications established by the Committee on Reagents of the American Chemical Society, where such specifications are available. Otherwise, use best available grade.

- a. Water

Deionized or distilled to conform to ASTM specifications D-1193-74, Type 3. At the option of the analyst, the  $\text{KMnO}_4$  test for oxidizable matter may be omitted when high concentrations of organic matter are not expected to be present.

- b. Absorbing Solution

Dilute 2.8 mL of concentrated sulfuric acid (18M) to 1 liter with deionized water to form 0.1 N sulfuric acid.

- c. Silica Gel

Indicating type. Fresh or dried at  $175^\circ\text{C}$  ( $350^\circ\text{F}$ ) for 2 hours, 6 to 16 mesh.

- d. Stopcock grease

### 3.2.2 Sample Recovery

- a. Rinse Solution. See absorbing Solution.

### 3.2.3 Sample analysis

- a. Water. See above.
- b. Nessler Reagent:  
Purchase from a laboratory chemicals supplier (APHA approved) or prepare as follows:

Dissolve 35 grams of mercuric chloride in 500 mL of hot water. Filter and allow to cool. Dissolve 62.5 grams of potassium iodide in 260 mL of cold water. Gradually add the mercuric chloride solution to 250 mL of the iodide solution until a slight permanent red precipitate is formed. Dissolve the precipitate with the remaining iodide solution and again add mercuric chloride slowly until a red precipitate remains.

Dissolve 150 grams of potassium hydroxide in 250 mL of distilled water. Caution: Corrosive. Add solution to the potassium iodide mercuric chloride solution and make up to 1 liter with distilled water. Stir thoroughly and allow to stand a day or so, and decant the clear liquid. Warning: The Nessler reagent should be handled with caution because of its toxicity and corrosive properties.

- c. Stock Standard Ammonium Sulfate Solution:  
Dissolve 0.194 g of ammonium sulfate in absorbing solution and make up to 500 mL with absorbing solution. One mL of this solution contains 100 ug of ammonia. Discard this solution after one month.
- d. Intermediate Standard  
Dilute 10 mL of the stock standard solution to 100 mL with absorbing solution. 1 mL of this solution contains 10 ug of ammonia. Discard after one week.
- e. Stock Absorbing Solution  
Dilute 2.8 mL of concentrated sulfuric acid (19M) to 1 liter with distilled water to form 0.1 N sulfuric acid.

- f. Potassium Iodide.
- g. Mercuric Chloride
- h. Potassium Hydroxide.
- i. Ammonium Sulfate.
- j. Calibration Standards  
Dilute 0 mL, 2 mL, 4 mL, 8 mL, 10 mL, 12 mL and 14 mL of intermediate standard to 50 mL with absorbing solution in a volumetric flask and shake well to mix. This corresponds to 0 ug, 20 ug, 40 ug, 80 ug, 100 ug, 120 ug and 140 ug of ammonia in each flask.

NOTE 1: The calibration standards used in this method are based on experience using an APHA approved Nessler reagent. The prepared Nessler reagent may require calibration standards that differ in concentrations by an order of magnitude.

### 3.3 Pre-Test Preparation

No special pre-test preparation is required.

### 3.4 Sample Collection Train Preparation

During the preparation and assembly, keep all opening covered wherever contamination can occur until just prior to assembly. Assemble the impingers in the tray. Load each of the first two impingers with exactly 100 mL of absorbing solution. Leave the third impinger empty. Load the last impinger with approximately 200 to 300 grams of silica gel. If moisture content is to be performed gravimetrically, weight each impinger plus contents to the nearest 0.5 g and record the weights. Reserve about 200 mL of the absorbing solution as a reagent blank.

### 3.5 Sample Collection Train leak Check

The sample collection train may be leak checked in the Laboratory after assembly using the procedure in the Source Test Manual.

### 3.6 Sample Recovery

Inspect the train for general condition. Note if the silica gel is completely expended, and if the train or its components are sealed. Note anything other than a colorless, odorless, clear impinger catch, and any other condition that may be reflected in the

analysis. Working in a area protected from the wind and free from dust and ammonia, carefully disconnect the probe and the impingers. Weigh each impinger plus contents to the nearest 0.5 g and record these weights.

Transfer the impinger catch to a 500 mL graduated cylinder (1000 mL if necessary). Rinse the inside of the probe, the impingers and all connecting glassware into the graduated cylinder at least three time using the rinse solution. Be sure to contact all interior surfaces with each rinse.

Dilute the sample to 500 mL with the rinse solution (1000 mL if necessary). Stopper the cylinder and mix well. Transfer the sample to a container. Seal it well, mark the level of the liquid and label the container to clearly identify it contents.

Take 200 mL of the reagent blank, and dilute it to the sample volume with rinse solution. Stopper the cylinder, and mix will. Transfer the blank to a container. Seal it well, mark the level of the liquid and label the container to clearly identify it contents.

### 3.7 Sample Analysis

Shake the sample well. Transfer 50.0 mL to a volumetric flask. Add 2.0 mL of Nessler reagent to the flask, mix well, and allow the color to develop for a least 10 minutes. Read the absorbance of the sample in a 1 cm cell at 440 nm. Use water in the reference cell. If the sample exceeds the linear range of the spectrophotometer, use a smaller sample aliquot and dilute it to 50.0 mL. Analyze the reagent blank using the same procedure.

### 3.8 Calculations and Reporting

Using the calibration factor (obtained in Section 3.9), calculate total mg of ammonia as follows:

$$\text{mg} = \text{AF} \times (\text{OD}_{\text{spl}} - \text{OD}_{\text{blank}}) \times \text{M}$$

Where:

AF	= Aliquot factor (sample volume/aliquot volume)
OD <sub>spl</sub>	= Optical density of the sample
OD <sub>blank</sub>	= Optical density of the reagent blank
M	= Nessler response factor, mg per OD.

Report ammonia to the nearest 0.1 mg.

Report moisture gain to the nearest gram or mL.

### 3.9 Calibrations

Each bottle of Nessler reagent must be calibrated on opening.

Dilute 0 mL, 2 mL, 4 mL, 8 mL, 10 mL, 12 mL and 14 mL of intermediate standard solution to 50.0 mL with absorbing solution, and shake well. Add 2.0 mL of Nessler reagent to each, mix well, and allow the color to develop for at least 10 minutes. Read the absorbance of each standard in a 1 cm cell at 440 nm. Use water in the reference cell.

Subtract the blank (0 mL standard) from each reading, and calculate the curve of ug of ammonia vs. the corrected absorbance. Correlation coefficient of this curve should be at least 0.9995. Any standard that is more than 7% from the calculated curve must be remade and rerun. Label the Nessler's reagent with the response factor (mg per OD), blank reading, date of calibration and reference to the calibration data. The Nessler's reagent must be recalibrated when control values indicate a change in response or every six months, whichever occurs first.

### 3.10 Quality Control

Nessler reagent may deteriorate during storage and must be checked frequently. Analyze a 40 ug control solution every set of samples, or every ten samples, whichever occurs first. This control solution must be obtained independently from the calibration standards. Calculate the ammonium content using the corrected absorbance and latest response factor. Measured value should be within  $\pm 5\%$  of theoretical. If control values indicate a change, recalibrate the reagent and recalculate the control results. If the recalculated values are still out of range, void the previous analysis and investigate the procedure until it is under control.

Check the reagent blank against previous blank readings. A significant increase in the blank reading (more than 10%) indicates absorbing solution contamination or Nessler reagent deterioration. Investigate this problem until blank is brought to normal levels.



**APPENDIX F-2**  
**ANALYTICAL RESULTS**



12-Apr-94  
Date

Regression Output:

Absorb. corrected  
Percent Deviation  
Constant  
Std Err of Y Est  
R Squared  
No. of Observations  
Degrees of Freedom  
Degrees of Freedom  
X Coefficient(s)  
Std Err of Coef.  
Std Err of Coef.

0.007087  
0.000873  
0.9997  
6  
4  
5  
0.418552  
0.003529  
0.004978

standard (ml)  
Blank Absorb.  
Absorb.  
Absorb. (-blank)  
Slope (M)  
volume used in analysis (ml)  
sample aliquot (ml)  
volume collected (ml)  
mass collected (mg)

3/19/94  
3/19/94  
3/19/94  
3/19/94  
3/19/94  
3/19/94  
Control (4/4/94)

2  
4  
8  
10  
12  
14  
0.02  
0.04  
0.08  
0.10  
0.12  
0.14  
0.04  
0.005  
0.005  
0.005  
0.005  
0.005  
0.005  
0.006  
0.035  
0.083  
0.180  
0.230  
0.275  
0.320  
0.081  
0.030  
0.078  
0.175  
0.225  
0.270  
0.315  
0.075  
1.8%  
0.7%  
0.4%  
1.2%  
0.1%  
0.8%  
4.0%

Test	Analysis	Blank Absorb.	Absorb.	Absorb. (-blank)	Slope (M)	volume used in analysis (ml)	sample aliquot (ml)	volume collected (ml)	Aliquot Factor	mass collected (mg)
Mid-Load	Run 1	0.003	0.105	0.102	0.42	52	10	500	50	2.13
	Run 2	0.006	0.102	0.096	0.42	52	10	500	50	2.01
									avg:	2.07
Full Load Test 1	Run 1	0.003	0.136	0.133	0.42	52	10	500	50	2.78
	Run 2	0.006	0.139	0.133	0.42	52	10	500	50	2.78
									avg:	2.78
Full Load Test 2	Run 1	0.003	0.16	0.157	0.42	52	10	500	50	3.29
	Run 2	0.006	0.165	0.159	0.42	52	10	500	50	3.33
									avg:	3.31

SUBJECT: SLIP ANALYSES  
 PROJECT: H2G5/EGS Compliance  
 CLIENT/PROJECT NO: Edison 9585

BY: CH DATE: 4/4/94  
 CHKD: DATE:  
 REV: DATE:

SHEET 1

(S1) ⇒ <sup>Stock</sup> Initial Standard mixed 3/19/94 + curve also run on 3/19/94

↳ was mixed from Fisher Brand Ammonium Sulfate

4/4/94 ⇒ mixed Second Standard (S2); also by dissolving 0.194g of VWR Brand Ammonium Sulfate in 500 ml of reagent.

	Aliquot	Absorbance Run 1 / Run 2	Total wg Run 1 / Run 2
blank			
Etiwanda #3, Mid-Load	∅	0.003 / 0.006	
Etiwanda #3, Full Load, Test #1	10ml	0.105 / 0.102	2.13 / 2.01 <u>2.0</u>
Etiwanda #3, Full Load, Test #2	10ml	0.136 / 0.139	2.78 / 2.78 <u>2.78</u>
Etiwanda #3, Full Load, Test #2	10ml	0.160 / 0.165	3.29 / 3.33 <u>3.31</u>

{ Control Sample (S2) 40 µg 0.081 4.07% deviation  
 { Blank → 0.006

**APPENDIX F-3**  
**SPREADSHEETS AND FIELD TEST DATA SHEETS**



AMMONIA SLIP CALCULATIONS

Plant: SCE, EGS  
 Date : 3/22/94  
 Performed by: BD

Sample Location:  
 Test No./Type:  
 Start/Stop Time:

UNIT 3  
 RUN 1/AMMONIA  
 1100/1200

Conditions: FULL LOAD, FGR & UREA

PARAMETER	SYMBOL	VALUE (calc.)
Gas Meter Correction Factor	(gamma)	1.02
Barometric Pressure (in Hg)	P(b)	29.91
# of Sample Points	#	4
Total Sampling Time (min)	(theta)	( 60.0 )
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s)	( 283.5 )
Gas Meter Initial Reading (cu ft)		298.00
Gas Meter Final Reading (cu ft)		322.64
Net Gas Sample Volume (cu ft)	V(m)	( 24.64 )
Vol of Liquid Collected (ml)	VI(c)	102.6
Vol of Liq @ Std. Conds. (scf)	V(w std)	( 4.829 )
Measure O2 Concentration @KVB	(%)	3.2

FIELD DATA AVERAGES

Avg Orifice Meter Reading (in H2O)	dH(avg)	=	0.500
Avg Stack Temperature (degF)	T(s avg)	=	251.3
Average Meter Temperature (degF)	T(m avg)	=	68.1

CALCULATED VALUES

Meter Volume (std, cu. ft.)	V(m std)	=	25.11
Stack Gas Water Vapor Proportion	B(wo)	=	0.161
	Total Mass: (mg NH3)	=	2.78
	NH3 Concentration (ppmv air)	=	5.5
	NH3 Concentration (ppmv air @3.0% O2)	=	5.5

Sample Point	dClock Time	Orifice Meter, dH (in H2O)	Stack Temp (degF)	Gas Meter Temp (degF) in	Gas Meter Temp (degF) out	
1	15	0.50	250	67	67	
2	15	0.50	251	70	68	
3	15	0.50	252	68	67	
4	15	0.50	252	70	68	
TOTALS		60.0	2.00	1005.0	275.0	270.0

AMMONIA SLIP CALCULATIONS

Plant: SCE, EGS  
 Date : 3/22/94  
 Performed by: BD

Sample Location:  
 Test No./Type:  
 Start/Stop Time:

UNIT 3  
 RUN 2/AMMONIA  
 1301/1401

Conditions: 310 MW, FGR, UREA

PARAMETER	SYMBOL	VALUE (calc.)
Gas Meter Correction Factor	(gamma)	1.02
Barometric Pressure (in Hg)	P(b)	29.91
# of Sample Points	#	4
Total Sampling Time (min)	(theta)	( 60.0 )
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(a)	( 283.5 )
Gas Meter Initial Reading (cu ft)		323.16
Gas Meter Final Reading (cu ft)		347.65
Net Gas Sample Volume (cu ft)	V(m)	( 24.49 )
Vol of Liquid Collected (ml)	VI(c)	103.2
Vol of Liq @ Std. Conds. (scf)	V(w std)	( 4.858 )
Measure O2 Concentration @KVB	(%)	3.2

FIELD DATA AVERAGES

Avg Orifice Meter Reading (in H2O)	dH(avg)	=	0.500
Avg Stack Temperature (degF)	T(s avg)	=	251.0
Average Meter Temperature (degF)	T(m avg)	=	70.4

CALCULATED VALUES

Meter Volume (std, cu. ft.)	V(m std)	=	24.85
Stack Gas Water Vapor Proportion	B(wc)	=	0.184
	Total Mass: (mg NH3)	=	3.31
	NH3 Concentration (ppmv air)	=	6.6
	NH3 Concentration (ppmv air @3.0% O2)	=	6.6

Sample Point	dClock Time	Orifice Meter, dH (in H2O)	Stack Temp (degF)	Gas Temp in	Meter Temp (degF) out
1	15	0.50	252	68	68
2	15	0.50	251	71	70
3	15	0.50	251	72	71
4	15	0.50	250	72	71
[[TOTALS]]	60.0	2.00	1004.0	283.0	280.0

AMMONIA SLIP CALCULATIONS

Plant: SCE, EGS  
 Date: 3/23/94  
 Performed by: BD

Sample Location:  
 Test No./Type:  
 Start/Stop Time:

UNIT 3  
 AMMONIA  
 1417/1517

Conditions: MID-LOAD, FGR & UREA ON

PARAMETER	SYMBOL	VALUE (calc.)
Gas Meter Correction Factor	(gamma)	1.02
Barometric Pressure (in Hg)	P(b)	29.91
# of Sample Points	#	4
Total Sampling Time (min)	(theta)	( 60.0 )
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s)	( 283.5 )
Gas Meter Initial Reading (cu ft)		470.21
Gas Meter Final Reading (cu ft)		495.14
Net Gas Sample Volume (cu ft)	V(m)	( 24.93 )
Vol of Liquid Collected (ml)	V(c)	102.2
Vol of Liq @ Std. Conds. (scf)	V(w std)	( 4.811 )
Measure O2 Concentration @KVB	(%)	3.8

FIELD DATA AVERAGES

Avg Orifice Meter Reading (in H2O)	dH(avg)	=	0.500
Avg Stack Temperature (degF)	T(s avg)	=	230.8
Average Meter Temperature (degF)	T(m avg)	=	70.4

CALCULATED VALUES

Meter Volume (std, cu. ft.)	V(m std)	=	25.31
Stack Gas Water Vapor Proportion	B(wo)	=	0.160
	Total Mass: (mg NH3)	=	2.07
NH3 Concentration (ppmv air)		=	4.0
NH3 Concentration (ppmv air @ 3.0% O2)		=	4.2

Sample Point	dClock Time	Orifice Meter, dH (in H2O)	Stack Temp (degF)	Gas Meter Temp (degF) in	Gas Meter Temp (degF) out
1	15	0.50	231	67	68
2	15	0.50	230	70	68
3	15	0.50	231	74	70
4	15	0.50	231	75	71
TOTALS	60.0	2.00	923.0	286.0	277.0







**APPENDIX G**

**RECORDS SUPPORTING VOLUMETRIC FLOW RATE MEASUREMENTS**



**APPENDIX G-1**

**VOLUMETRIC FLOW RATE CALCULATION SHEET**



ISOKINETIC PERFORMANCE WORKSHEET & PARTICULATE CALCULATIONS

Plant \_\_\_\_\_

Performed by \_\_\_\_\_

Date \_\_\_\_\_

Sample Location \_\_\_\_\_

Test No./Type \_\_\_\_\_

Barometric Pressure (in. Hg)	$P_b$	
Meter volume (std), $17.64 \left( \frac{V_m}{\alpha} \right) \left( \frac{P_b + \frac{\Delta H}{13.6}}{T_m + 460} \right)$ $17.64 \left( \frac{(\quad)}{(\quad)} \right) \left( \frac{(\quad) + \frac{(\quad)}{13.6}}{(\quad) + 460} \right)$	$V_{m \text{ std}}$	
Volume of liquid collected (grams)	$V_{l_c}$	
Volume of liquid at standard condition (scf) $V_{l_c} \times 0.04707$	$V_{w \text{ std}}$	
Stack gas proportion of water vapor $\frac{V_{w \text{ std}}}{V_{w \text{ std}} + V_{m \text{ std}}}, \frac{(\quad)}{(\quad) + (\quad)}$	$B_{w_o}$	
Molecular weight, stack gas dry (lb/lb-mole) $(\% \text{ CO}_2 \times 0.44) + (\% \text{ O}_2 \times 0.32) + (\% \text{ N}_2 + \% \text{ CO} \times 0.28)$ $(\quad \times 0.44) + (\quad \times 0.32) + (\quad + \quad \times 0.28)$	$M_d$	
Molecular weight, stack gas wet (lb/lb-mole) $M_d(1-B_{w_o}) + 18(B_{w_o}), (\quad)(1-\quad) + 18(\quad)$	$M_s$	
Absolute stack pressure (in. Hg) $P_b + \frac{P_{\text{stack}} (\text{in. H}_2\text{O})}{13.6}, (\quad) + \frac{(\quad)}{13.6}$	$P_s$	

Temperature stack gas, average (°F)	$T_s$	
Stack velocity (fps) $85.49 (C_p) (\sqrt{\Delta P_s \text{ avg}}) \sqrt{\frac{T_s \text{ avg} + 460}{P_s M_s}}$ $85.49 ( \quad ) (\sqrt{\quad}) \sqrt{\frac{( \quad ) + 460}{( \quad ) ( \quad )}}$	$V_{s(\text{avg})}$	
Total sample time (minutes)	$\theta$	
Nozzle diameter, actual (inches)	$N_d$	
Percent isokinetic (%) $17.33 (T_s + 460)(V_w \text{ std} + V_m \text{ std})$ $\frac{\theta V_s P_s N_d^2}{17.33 ( \quad + 460 ) ( ( \quad ) + ( \quad ) )}$ $\frac{( \quad ) ( \quad ) ( \quad ) ( \quad )}{( \quad ) ( \quad ) ( \quad ) ( \quad )}$	%I	
Area of stack (ft <sup>2</sup> ) $\pi = 3.1416$ $\pi r^2 \div 144, \quad \pi ( \quad )^2 \div 144$	$A_s$	
Stack gas volume at standard conditions (dscfm) $60 (1 - B_{wo}) V_{s \text{ avg}} A_s \left( \frac{528}{T_s \text{ avg} + 460} \right) \left( \frac{P_s}{29.92} \right)$ $60 (1 - \quad) ( \quad ) ( \quad ) \left( \frac{528}{\quad + 460} \right) \left( \frac{( \quad )}{(29.92)} \right)$	$Q_s$	
Particulate matter concentration, dry (gr/dscf) $15.432 \frac{M_p \text{ (grams)}}{V_m \text{ std}}, \quad 15.432 \frac{( \quad )}{( \quad )}$	$C_{s(\text{std})}$	
Emission rate of particulate matter (lb/hr) $0.00857 (Q_s) C_{s(\text{std})}, \quad 0.00857 ( \quad ) ( \quad )$	$E_p$	

**APPENDIX G-2**  
**SPREADSHEETS AND FIELD TEST DATA SHEETS**



## FLOW RATE CALCULATION

Plant: EDISON EGS  
 Date: 3/22/94  
 Sample Location: UNIT 3  
 Performed by: CG/BD

Conditions: FULL LOAD, FGR ON  
 Start/Stop: 0915/1015

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	0.22
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114
Length (if rectangular)	L	
Width (if rectangular)	W	
Area of Stack (sq ft)	A(s)	( 283.53 )
O2 Concentration	% O2	3.3
CO2 Concentration	% CO2	10.0
CO Concentration	% CO	0.213
N2 Concentration (by diff.)	% N2	( 86.49 )

### VELOCITY TRAVERSE AVERAGES

Avg Velocity Head (in H2O)	dP(avg) =	0.921
Avg Stack Temperature (degF)	T(s avg) =	249.0
Avg SQRT(dP)	=	0.958

### CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS

Stack Gas Water Vapor Proportion	B(wo) =	0.159
Mol. Wt., Stack Gas Dry	M(d) =	29.73
Mol. Wt., Stack Gas Wet	M(s) =	27.87
Abs Stack Pressure (in Hg)	P(s) =	29.93
Avg Stack Velocity (ft/sec)	V(s avg) =	63.4
Stack Gas STD Vol Flow (dscfm)	Q(s) =	676063
Actual Stack Gas Vol Flow (acfm)	Q(a) =	1079230

### VELOCITY TRAVERSE MEASUREMENTS

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.85	249	0.92	61.0
2	1.05	249	1.02	67.8
3	1.05	249	1.02	67.8
4	0.95	249	0.97	64.5
5	0.95	249	0.97	64.5
6	0.95	249	0.97	64.5
B-1	0.90	249	0.95	62.8
2	0.85	249	0.92	61.0
3	0.85	249	0.92	61.0
4	0.90	249	0.95	62.8
5	0.85	249	0.92	61.0
6	0.85	249	0.92	61.0
C-1	0.80	249	0.89	59.2
2	0.75	249	0.87	57.3
3	0.80	249	0.89	59.2
4	0.80	249	0.89	59.2
5	0.90	249	0.95	62.8
6	0.90	249	0.95	62.8
D-1	0.90	249	0.95	62.8
2	0.90	249	0.95	62.8
3	1.00	249	1.00	66.2
4	1.10	249	1.05	69.4
5	1.10	249	1.05	69.4
6	1.15	249	1.07	71.0
<b>TOTALS</b>	<b>22.10</b>	<b>5978</b>	<b>22.99</b>	<b>1522.6</b>

## FLOW RATE CALCULATION

Plant: EDISON EGS  
 Date: 3/22/94  
 Sample Location: UNIT 3  
 Performed by: CG/BD

Conditions: FULL LOAD, FGR AND UREA ON, RUN 1  
 Start/Stop: 1100/1200

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	0.22
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114
Length (if rectangular)	L	
Width (if rectangular)	W	
Area of Stack (sq ft)	A(s)	( 283.53 )
O2 Concentration	% O2	3.2
CO2 Concentration	% CO2	10.0
CO Concentration	% CO	0.214
N2 Concentration (by diff.)	% N2	( 86.59 )

### VELOCITY TRAVERSE AVERAGES

Avg Velocity Head (in H2O)	dP(avg) =	0.896
Avg Stack Temperature (degF)	T(s avg) =	251.0
Avg SORT(dP)	=	0.946

### CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS

Stack Gas Water Vapor Proportion	B(wo) =	0.161
Mol. Wt., Stack Gas Dry	M(d) =	29.73
Mol. Wt., Stack Gas Wet	M(s) =	27.84
Abs Stack Pressure (in Hg)	P(s) =	29.93
Avg Stack Velocity (ft/sec)	V(s avg) =	62.7
Stack Gas STD Vol Flow (dsctm)	Q(s) =	665233
Actual Stack Gas Vol Flow (acfm)	Q(a) =	1067476

### VELOCITY TRAVERSE MEASUREMENTS

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.90	251	0.95	62.9
2	0.95	251	0.97	64.7
3	0.95	251	0.97	64.7
4	0.90	251	0.95	62.9
5	0.95	251	0.97	64.7
6	0.95	251	0.97	64.7
B-1	0.85	251	0.92	61.2
2	0.85	251	0.92	61.2
3	0.85	251	0.92	61.2
4	0.90	251	0.95	62.9
5	0.85	251	0.92	61.2
6	0.85	251	0.92	61.2
C-1	0.85	251	0.92	61.2
2	0.80	251	0.89	59.3
3	0.85	251	0.92	61.2
4	0.85	251	0.92	61.2
5	0.80	251	0.89	59.3
6	0.85	251	0.92	61.2
D-1	0.85	251	0.92	61.2
2	0.95	251	0.97	64.7
3	0.90	251	0.95	62.9
4	1.00	251	1.00	66.3
5	1.00	251	1.00	66.3
6	1.05	251	1.02	68.0
<b>TOTALS</b>	<b>21.50</b>	<b>6024</b>	<b>22.70</b>	<b>1508.0</b>



## FLOW RATE CALCULATION

Plant: EDISON EGS  
 Date : 3/22/94  
 Sample Location: UNIT 3  
 Performed by: CG/BD

Conditions: FULL LOAD, BASLINE  
 Start/Stop: 1500/1455

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	0.22
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114
Length (if rectangular)	L	
Width (if rectangular)	W	
Area of Stack (sq ft)	A(s)	( 283.53 )
O2 Concentration	% O2	3.1
CO2 Concentration	% CO2	10.0
CO Concentration	% CO	0.198
N2 Concentration (by diff.)	% N2	( 86.70 )

### VELOCITY TRAVERSE AVERAGES

Avg Velocity Head (in H2O)	dP(avg) =	0.873
Avg Stack Temperature (degF)	T(s avg) =	250.0
Avg SQRT(dP)	=	0.934

### CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS

Stack Gas Water Vapor Proportion	B(wo) =	0.156
Mol. Wt., Stack Gas Dry	M(d) =	29.72
Mol. Wt., Stack Gas Wet	M(s) =	27.90
Abs Stack Pressure (in Hg)	P(s) =	29.93
Avg Stack Velocity (ft/sec)	V(s avg) =	61.8
Stack Gas STD Vol Flow (dsctm)	Q(s) =	680325
Actual Stack Gas Vol Flow (acfm)	Q(a) =	1051841

### VELOCITY TRAVERSE MEASUREMENTS

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.90	250	0.95	62.8
2	0.85	250	0.92	61.1
3	0.90	250	0.95	62.8
4	0.85	250	0.92	61.1
5	0.90	250	0.95	62.8
6	0.90	250	0.95	62.8
B-1	0.85	250	0.92	61.1
2	0.90	250	0.95	62.8
3	0.80	250	0.89	59.2
4	0.85	250	0.92	61.1
5	0.85	250	0.92	61.1
6	0.90	250	0.95	62.8
C-1	0.80	250	0.89	59.2
2	0.80	250	0.89	59.2
3	0.75	250	0.87	57.4
4	0.80	250	0.89	59.2
5	0.85	250	0.92	61.1
6	0.80	250	0.89	59.2
D-1	0.85	250	0.92	61.1
2	0.95	250	0.97	64.6
3	0.90	250	0.95	62.8
4	1.00	250	1.00	66.2
5	0.95	250	0.97	64.6
6	1.05	250	1.02	67.9
<hr/>				
TOTALS	20.95	6000	22.41	1483.9

FLOWRATE CALCULATIONS - CYCLONIC

Plant: SCE, ETIWANDA GENERATING STATION  
 Date: 3/23/94  
 Sample Location: UNIT NO. 3  
 Performed by: ROBERT M.

Condition: Mid-load Baseline

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.81
Barometric Pressure (in Hg)	P(b)	29.91
Stack Pressure (in H2O)	P(stack)	0.050
# of Sample Points	#	20
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114
Length (if rectangular)	L	
Width (if rectangular)	W	
Area of Stack (sq ft)	A(s)	( 283.53 )
O2 Concentration	% O2	3.6
CO2 Concentration	% CO2	9.7
CO Concentration	% CO	0.146
N2 Concentration (by diff.)	% N2	( 86.55 )

FIELD DATA AVERAGES	
Avg Velocity Head (in H2O)	dP(avg) = 0.514
Avg Stack Temperature (degF)	T(s avg) = 229.6
Avg SQRT(dP)	= 0.715
Avg Yaw Angle (degrees)	= 7.9

CALCULATED VALUES	
Stack Gas Water Vapor Proportion	B(wo) = 0.153
Mol. Wt., Stack Gas Dry	M(d) = 29.70
Mol. Wt., Stack Gas Wet	M(s) = 27.91
Abs Stack Pressure (in Hg)	P(s) = 29.91
Avg Stack Velocity (ft/sec)	V(s avg) = 45.0
Stack Gas STD Vol Flow (dscfm)	Q(s) = 496281
Actual Stack Gas Vol Flow (acfm)	Q(a) = 765419

Sample Point	Angle of Cyclonic Flow	Velocity Head, dP (in H2O)	Cyclonic Velocity Head	Stack Temp (degF)	SQRT(dP)	Cyclonic SQRT(dP)
D-6	-7	0.50	0.50	230	0.7071	0.7045
5	-5	0.51	0.51	229	0.7141	0.7128
4	0	0.65	0.65	229	0.8062	0.8062
3	4	0.65	0.65	230	0.8062	0.8052
2	10	0.59	0.58	230	0.7681	0.7623
					0.0000	0.0000
C-6	-22	0.48	0.45	228	0.6928	0.6671
5	-10	0.40	0.39	231	0.6325	0.6276
4	-15	0.45	0.43	229	0.6708	0.6593
3	-8	0.51	0.51	229	0.7141	0.7107
2	5	0.48	0.48	230	0.6928	0.6915
					0.0000	0.0000
B-6	2	0.50	0.50	230	0.7071	0.7069
5	5	0.45	0.45	230	0.6708	0.6695
4	5	0.45	0.45	229	0.6708	0.6695
3	5	0.54	0.54	230	0.7348	0.7334
2	25	0.39	0.35	228	0.6245	0.5945
					0.0000	0.0000
A-6	0	0.51	0.51	230	0.7141	0.7141
5	5	0.59	0.59	230	0.7681	0.7667
4	0	0.48	0.48	230	0.6928	0.6928
3	8	0.59	0.58	230	0.7681	0.7644
2	17	0.55	0.53	230	0.7416	0.7252
					0.0000	0.0000
TOTALS	158	10.27	10.12	4592	14.2978	14.1844

CYCLONIC FLOW CALCULATIONS	
Avg Velocity Head (in H2O)	dP(avg) = 0.506
Avg SQRT (dP)	= 0.709
Avg Stack Velocity (ft/sec)	V(s avg) = 44.6
Stack Gas STD Vol Flow (dscfm)	Q(s) = 492345
Actual Stack Gas Vol Flow (acfm)	Q(a) = 759349

FLOWRATE CALCULATIONS - CYCLONIC

Plant: SCE, ETIWANDA GENERATING STATION  
 Date: 3/23/94  
 Sample Location: UNIT NO. 3  
 Performed by: ROBERT M.

Condition: Low Load Baseline

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.81
Barometric Pressure (in Hg)	P(b)	29.91
Stack Pressure (in H2O)	P(stack)	-0.24
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114
Length (if rectangular)	L	
Width (if rectangular)	W	
Area of Stack (sq ft)	A(s)	( 283.53 )
O2 Concentration	% O2	4.8
CO2 Concentration	% CO2	8.9
CO Concentration	% CO	0.000
N2 Concentration (by diff.)	% N2	( 86.30 )

FIELD DATA AVERAGES

Avg Velocity Head (in H2O)	dP(avg)	=	0.152
Avg Stack Temperature (degF)	T(s avg)	=	184.7
Avg SQRT(dP)		=	0.390
Avg Yaw Angle (degrees)		=	0.0

CALCULATED VALUES

Stack Gas Water Vapor Proportion	B(w)	=	0.153
Mol. Wt., Stack Gas Dry	M(d)	=	29.62
Mol. Wt., Stack Gas Wet	M(s)	=	27.84
Abs Stack Pressure (in Hg)	P(s)	=	29.89
Avg Stack Velocity (ft/sec)	V(s avg)	=	23.7
Stack Gas STD Vol Flow (dscfm)	Q(s)	=	279946
Actual Stack Gas Vol Flow (acfm)	Q(a)	=	403919

Sample Point	Angle of Cyclonic Flow	Velocity Head, dP (in H2O)	Cyclonic Velocity Head	Stack Temp (degF)	SQRT(dP)	Cyclonic SQRT(dP)
D-6	0	0.14	0.14	185	0.3742	0.3742
5	0	0.16	0.16	187	0.4000	0.4000
4	0	0.16	0.16	187	0.4000	0.4000
3	0	0.18	0.18	186	0.4243	0.4243
2	0	0.15	0.15	185	0.3873	0.3873
1	0	0.12	0.12	183	0.3464	0.3464
C-6	0	0.16	0.16	183	0.4000	0.4000
5	0	0.15	0.15	183	0.3873	0.3873
4	0	0.16	0.16	185	0.4000	0.4000
3	0	0.16	0.16	183	0.4000	0.4000
2	0	0.14	0.14	184	0.3795	0.3795
1	0	0.13	0.13	179	0.3606	0.3606
B-6	0	0.16	0.16	183	0.4000	0.4000
5	0	0.14	0.14	184	0.3742	0.3742
4	0	0.16	0.16	185	0.4000	0.4000
3	0	0.14	0.14	187	0.3742	0.3742
2	0	0.14	0.14	186	0.3742	0.3742
1	0	0.12	0.12	183	0.3464	0.3464
A-6	0	0.14	0.14	185	0.3742	0.3742
5	0	0.15	0.15	186	0.3873	0.3873
4	0	0.18	0.18	186	0.4243	0.4243
3	0	0.19	0.19	185	0.4359	0.4359
2	0	0.17	0.17	187	0.4123	0.4123
1	0	0.15	0.15	185	0.3873	0.3873
TOTALS	0	3.65	3.65	4432	9.3496	9.3496

CYCLONIC FLOW CALCULATIONS

Avg Velocity Head (in H2O)	dP(avg)	=	0.152
Avg SQRT (dP)		=	0.390
Avg Stack Velocity (ft/sec)	V(s avg)	=	23.7
Stack Gas STD Vol Flow (dscfm)	Q(s)	=	279946
Actual Stack Gas Vol Flow (acfm)	Q(a)	=	403919

**FLOW RATE CALCULATION USING FLUE FACTOR METHOD**

Plant: EDISON EGS  
 Date: 3/23/84  
 Sample Location: UNIT 3  
 Performed by: RM/BD

Conditions: MID LOAD, BASELINE  
 Start/Stop: 1100/1200

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	0.05
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s)	( 283.53 )
O2 Concentration	% O2	3.6
CO2 Concentration	% CO2	9.7
CO Concentration	% CO	0.146
N2 Concentration (by diff.)	% N2	( 86.55 )

**VELOCITY TRAVERSE AVERAGES**

Avg Velocity Head (in H2O)	dP (avg) =	0.513
Avg Stack Temperature (degF)	T(s avg) =	225.0
Avg SQRT(dP)	=	0.715

**CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS**

Stack Gas Water Vapor Proportion	B(wo) =	0.153
Mol. Wt., Stack Gas Dry	M(d) =	29.70
Mol. Wt., Stack Gas Wet	M(s) =	27.91
Abs Stack Pressure (in Hg)	P(s) =	29.91
Avg Stack Velocity (ft/sec)	V(s avg) =	46.5
Stack Gas STD Vol Flow (dscfm)	Q(s) =	516124
Actual Stack Gas Vol Flow (acfm)	Q(a) =	790713

**VELOCITY TRAVERSE MEASUREMENTS**

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.45	225	0.67	43.6
2	0.50	225	0.71	46.0
3	0.55	225	0.74	48.2
4	0.60	225	0.77	50.4
5	0.50	225	0.71	46.0
6	0.50	225	0.71	46.0
B-1	0.50	225	0.71	46.0
2	0.50	225	0.71	46.0
3	0.55	225	0.74	48.2
4	0.50	225	0.71	46.0
5	0.50	225	0.71	46.0
6	0.45	225	0.67	43.6
C-1	0.40	225	0.63	41.1
2	0.55	225	0.74	48.2
3	0.50	225	0.71	46.0
4	0.55	225	0.74	48.2
5	0.50	225	0.71	46.0
6	0.35	225	0.59	38.5
D-1	0.45	225	0.67	43.6
2	0.55	225	0.74	48.2
3	0.60	225	0.77	50.4
4	0.60	225	0.77	50.4
5	0.60	225	0.77	50.4
6	0.55	225	0.74	48.2
<b>TOTALS</b>	<b>12.30</b>	<b>5400</b>	<b>17.15</b>	<b>1115.5</b>

## FLOW RATE CALCULATION

Plant: EDISON EGS  
 Date: 3/23/04  
 Sample Location: UNIT 3  
 Performed by: RM/BD

Conditions: MID LOAD, FGR ON  
 Start/Stop: 1245/1345

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	0.05
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s)	( 283.5 )
O2 Concentration	% O2	3.7
CO2 Concentration	% CO2	9.7
CO Concentration	% CO	0.144
N2 Concentration (by diff.)	% N2	( 86.46 )

### VELOCITY TRAVERSE AVERAGES

Avg Velocity Head (in H2O)	dP(avg) =	0.521
Avg Stack Temperature (degF)	T(s avg) =	228.5
Avg SQRT(dP)	=	0.720

### CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS

Stack Gas Water Vapor Proportion	B(wo) =	0.158
Mol. Wt., Stack Gas Dry	M(d) =	29.70
Mol. Wt., Stack Gas Wet	M(s) =	27.87
Abs Stack Pressure (in Hg)	P(s) =	29.91
Avg Stack Velocity (ft/sec)	V(s avg) =	47.0
Stack Gas STD Vol Flow (dscfm)	Q(s) =	517347
Actual Stack Gas Vol Flow (acfm)	Q(a) =	799469

### VELOCITY TRAVERSE MEASUREMENTS

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.50	229	0.71	46.2
2	0.55	229	0.74	48.4
3	0.55	229	0.74	48.4
4	0.55	229	0.74	48.4
5	0.60	229	0.77	50.6
6	0.50	229	0.71	46.2
B-1	0.60	229	0.77	50.6
2	0.45	229	0.67	43.8
3	0.45	229	0.67	43.8
4	0.50	229	0.71	46.2
5	0.50	229	0.71	46.2
6	0.45	229	0.67	43.8
C-1	0.50	228	0.71	46.1
2	0.45	228	0.67	43.8
3	0.50	228	0.71	46.1
4	0.50	228	0.71	46.1
5	0.55	228	0.74	48.4
6	0.35	228	0.59	38.6
D-1	0.50	228	0.71	46.1
2	0.50	228	0.71	46.1
3	0.60	228	0.77	50.5
4	0.65	228	0.81	52.6
5	0.60	228	0.77	50.5
6	0.60	228	0.77	50.5
<b>TOTALS</b>	<b>12.50</b>	<b>5484</b>	<b>17.28</b>	<b>1127.9</b>

## FLOW RATE CALCULATION

Plant: EDISON EGS  
 Date: 3/23/94  
 Sample Location: UNIT 3  
 Performed by: RM/BD

Conditions: MID LOAD, FGR & UREA ON  
 Start/Stop: 1435/1530

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	0.05
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s)	( 283.5 )
O2 Concentration	% O2	3.7
CO2 Concentration	% CO2	9.6
CO Concentration	% CO	0.142
N2 Concentration (by diff.)	% N2	( 86.56 )

### VELOCITY TRAVERSE AVERAGES

Avg Velocity Head (in H2O)	dP (avg) =	0.519
Avg Stack Temperature (degF)	T(s avg) =	230.0
Avg SQRT(dP)	=	0.719

### CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS

Stack Gas Water Vapor Proportion	B(wc) =	0.160
Mol. Wt., Stack Gas Dry	M(d) =	29.68
Mol. Wt., Stack Gas Wet	M(s) =	27.81
Abs Stack Pressure (in Hg)	P(s) =	29.91
Avg Stack Velocity (ft/sec)	V(s avg) =	47.0
Stack Gas STD Vol Flow (dscfm)	Q(s) =	514175
Actual Stack Gas Vol Flow (acfm)	Q(a) =	800090

### VELOCITY TRAVERSE MEASUREMENTS

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.55	230	0.74	48.5
2	0.50	230	0.71	48.2
3	0.55	230	0.74	48.5
4	0.60	230	0.77	50.7
5	0.50	230	0.71	46.2
6	0.50	230	0.71	46.2
B-1	0.50	230	0.71	46.2
2	0.40	230	0.63	41.4
3	0.50	230	0.71	46.2
4	0.50	230	0.71	46.2
5	0.50	230	0.71	46.2
6	0.45	230	0.67	43.9
C-1	0.50	230	0.71	46.2
2	0.50	230	0.71	46.2
3	0.50	230	0.71	46.2
4	0.60	230	0.77	50.7
5	0.50	230	0.71	46.2
6	0.40	230	0.63	41.4
D-1	0.50	230	0.71	46.2
2	0.55	230	0.74	48.5
3	0.60	230	0.77	50.7
4	0.60	230	0.77	50.7
5	0.60	230	0.77	50.7
6	0.55	230	0.74	48.5
TOTALS	12.45	5520	17.26	1128.8

## FLOW RATE CALCULATION

Plant: EDISON EGS  
 Date: 3/23/94  
 Sample Location: UNIT 3  
 Performed by: BD

Conditions: LOW LOAD, BASELINE  
 Start/Stop: 2330/2415

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	-0.25
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s)	( 283.5 )
O2 Concentration	% O2	4.8
CO2 Concentration	% CO2	8.9
CO Concentration	% CO	0.001
N2 Concentration (by diff.)	% N2	( 86.30 )

### VELOCITY TRAVERSE AVERAGES

Avg Velocity Head (in H2O)	dP(avg) =	0.120
Avg Stack Temperature (degF)	T(s avg) =	181.5
Avg SQRT(dP)	=	0.344

### CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS

Stack Gas Water Vapor Proportion	B(wo) =	0.147
Mol. Wt., Stack Gas Dry	M(d) =	29.62
Mol. Wt., Stack Gas Wet	M(s) =	27.91
Abs Stack Pressure (in Hg)	P(s) =	29.89
Avg Stack Velocity (ft/sec)	V(s avg) =	21.7
Stack Gas STD Vol Flow (dscfm)	Q(s) =	258370
Actual Stack Gas Vol Flow (acfm)	Q(a) =	368357

### VELOCITY TRAVERSE MEASUREMENTS

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.13	183	0.36	22.7
2	0.13	183	0.36	22.7
3	0.14	183	0.37	23.6
4	0.13	183	0.36	22.7
5	0.12	183	0.35	21.8
6	0.07	183	0.26	16.7
B-1	0.15	183	0.39	24.4
2	0.10	183	0.32	19.9
3	0.10	183	0.32	19.9
4	0.11	183	0.33	20.9
5	0.09	183	0.30	18.9
6	0.07	183	0.26	16.7
C-1	0.13	180	0.36	22.7
2	0.13	180	0.36	22.7
3	0.11	180	0.33	20.9
4	0.10	180	0.32	19.9
5	0.11	180	0.33	20.9
6	0.10	180	0.32	19.9
D-1	0.13	180	0.36	22.7
2	0.13	180	0.36	22.7
3	0.12	180	0.35	21.8
4	0.17	180	0.41	25.9
5	0.17	180	0.41	25.9
6	0.13	180	0.36	22.7
<b>TOTALS</b>	<b>2.87</b>	<b>4356</b>	<b>8.25</b>	<b>519.7</b>

## FLOW RATE CALCULATION

Plant: EDISON EGS  
 Date: 3/24/04  
 Sample Location: UNIT 3  
 Performed by: BD

Conditions: LOW LOAD, FGR ON  
 Start/Stop: 0117/0210

PARAMETER	SYMBOL	VALUE (calc.)
Pitot Tube Correction Factor	C(p)	0.84
Barometric Pressure (in Hg)	P(b)	29.91
Static Pressure (in H2O)	P(stack)	-0.25
# of Sample Points	#	24
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s)	( 283.5 )
O2 Concentration	% O2	4.8
CO2 Concentration	% CO2	9.0
CO Concentration	% CO	0.009
N2 Concentration (by diff.)	% N2	( 86.19 )

### VELOCITY TRAVERSE AVERAGES

Avg Velocity Head (in H2O)	dP(avg) =	0.124
Avg Stack Temperature (degF)	T(s avg) =	182.0
Avg SQRT(dP)	=	0.350

### CALCULATED VALUES FROM VELOCITY TRAVERSE AND MOISTURE MEASUREMENTS

Stack Gas Water Vapor Proportion	B(wo) =	0.150
Mol. Wt., Stack Gas Dry	M(d) =	29.63
Mol. Wt., Stack Gas Wet	M(s) =	27.89
Abs Stack Pressure (in Hg)	P(s) =	29.89
Avg Stack Velocity (ft/sec)	V(s avg) =	22.1
Stack Gas STD Vol Flow (dscfm)	Q(s) =	262007
Actual Stack Gas Vol Flow (acfm)	Q(a) =	375152

### VELOCITY TRAVERSE MEASUREMENTS

Sample Point	Velocity Head, dP (in H2O)	Stack Temp (degF)	SQRT(dP)	Stack Velocity (ft/sec)
A-1	0.14	182	0.37	23.6
2	0.15	182	0.39	24.4
3	0.14	182	0.37	23.6
4	0.13	182	0.36	22.7
5	0.12	182	0.35	21.8
6	0.07	182	0.26	16.7
B-1	0.15	182	0.39	24.4
2	0.12	182	0.35	21.8
3	0.14	182	0.37	23.6
4	0.12	182	0.35	21.8
5	0.10	182	0.32	19.9
6	0.05	182	0.22	14.1
C-1	0.12	182	0.35	21.8
2	0.13	182	0.36	22.7
3	0.11	182	0.33	20.9
4	0.12	182	0.35	21.8
5	0.12	182	0.35	21.8
6	0.08	182	0.28	17.8
D-1	0.13	182	0.36	22.7
2	0.14	182	0.37	23.6
3	0.16	182	0.40	25.2
4	0.16	182	0.40	25.2
5	0.15	182	0.39	24.4
6	0.13	182	0.36	22.7
<b>TOTALS</b>	<b>2.08</b>	<b>4368</b>	<b>8.40</b>	<b>529.3</b>

## MOISTURE AND VOLUME CALCULATIONS

Plant: EDISON, EGS  
 Date : 3/22/94  
 Performed by: CG/BD

Sample Location: UNIT 3  
 Test No./Type: MOISTURE/FGR ON  
 Start/Stop Time: 0915/1015

CONDITIONS: FULL LOAD, FGR ON

PARAMETER	SYMBOL	VALUE (calc.)
Gas Meter Correction Factor	(gamma)	1.019
Barometric Pressure (in Hg)	P(b)	29.91
# of Sample Points	#	6
Total Sampling Time (min)	(theta) (	60.00 )
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s) (	283.5 )
Gas Meter Initial Reading (cu ft)		263.49
Gas Meter Final Reading (cu ft)		296.72
Net Gas Sample Volume (cu ft)	V(m) (	33.23 )
Vol of Liquid Collected (ml)	VI(c)	137.5
Vol of Liq @ Std. Conds. (scf)	V(w std)(	6.472 )

FIELD DATA AVERAGES

Avg Orifice Meter Reading (in H2O)	dH(avg) =	1.000
Avg Stack Temperature (degF)	T(s avg) =	249.2
Average Meter Temperature (degF)	T(m avg) =	64.6

### CALCULATED VALUES

Meter Volume (std, cu. ft.)	V(m std) =	34.14
Stack Gas Water Vapor Proportion	B(wo) =	0.159

Sample Point	dClock Time	Orifice Meter dH (in H2O)	Stack Temp (degF)	Gas Temp in	Meter (degF) out
1	10	1.00	249	62	63
2	10	1.00	248	64	63
3	10	1.00	248	65	64
4	10	1.00	250	66	64
5	10	1.00	249	67	64
6	10	1.00	251	68	65
<b>TOTALS</b>	60	6.0000	1495.0	392	383

## MOISTURE AND VOLUME CALCULATIONS

Plant: EDISON, EGS  
 Date: 3/22/94  
 Performed by: CG/BD

Sample Location: UNIT 3  
 Test No./Type: MOISTURE/BASELINE  
 Start/Stop Time: 1500/1600

CONDITIONS: FULL LOAD, BASELINE

PARAMETER	SYMBOL	VALUE (calc.)	FIELD DATA AVERAGES
Gas Meter Correction Factor	(gamma)	1.019	Avg Orifice Meter Reading (in H2O) dH(avg) = 1.500
Barometric Pressure (in Hg)	P(b)	29.91	Avg Stack Temperature (degF) T(s avg) = 250.0
# of Sample Points	#	4	Average Meter Temperature (degF) T(m avg) = 67.6
Total Sampling Time (min)	(theta) (	60.00 )	
Stack (Duct) Dimensions (in):			
Radius (if round)	R	114.0	
Length (if rectangular)	L	0.0	
Width (if rectangular)	W	0.0	
Area of Stack (sq ft)	A(s) (	283.5 )	
Gas Meter Initial Reading (cu ft)		348.17	
Gas Meter Final Reading (cu ft)		387.40	
Net Gas Sample Volume (cu ft)	V(m) (	39.23 )	
Vol of Liquid Collected (ml)	VI(c)	157.9	
Vol of Liq @ Std. Conds. (scf)	V(w std)(	7.432 )	
			CALCULATED VALUES
			Meter Volume (std, cu. ft.) V(m std) = 40.12
			Stack Gas Water Vapor Proportion B(wo) = 0.156

Sample Point	dClock Time	Orifice Meter dH (in H2O)	Stack Temp (degF)	Gas Temp in	Meter (degF) out
1	15	1.50	250	67	67
2	15	1.50	250	70	67
3	15	1.50	250	70	65
4	15	1.50	250	70	65
<b>TOTALS</b>	60	6.0000	1000.0	277	264

## MOISTURE AND VOLUME CALCULATIONS

Plant: EDISON, EGS  
 Date : 3/23/94  
 Performed by: CG/BD

Sample Location: UNIT 1  
 Test No./Type: MOISTURE/BASELINE  
 Start/Stop Time: 1030/1130

CONDITIONS: MID LOAD, BASELINE

PARAMETER	SYMBOL	VALUE (calc.)	FIELD DATA AVERAGES
Gas Meter Correction Factor	(gamma)	1.019	Avg Orifice Meter Reading (in H2O) dH(avg) = 1.500
Barometric Pressure (in Hg)	P(b)	29.91	Avg Stack Temperature (degF) T(s avg) = 225.3
# of Sample Points	#	4	Average Meter Temperature (degF) T(m avg) = 69.9
Total Sampling Time (min)	(theta) (	60.00 )	
Stack (Duct) Dimensions (in):			
Radius (if round)	R	114.0	
Length (if rectangular)	L	0.0	
Width (if rectangular)	W	0.0	
Area of Stack (sq ft)	A(s) (	330.1 )	<b>CALCULATED VALUES</b>
Gas Meter Initial Reading (cu ft)		387.80	Meter Volume (std, cu. ft.) V(m std) = 41.86
Gas Meter Final Reading (cu ft)		428.90	Stack Gas Water Vapor Proportion B(wo) = 0.153
Net Gas Sample Volume (cu ft)	V(m) (	41.10 )	
Vol of Liquid Collected (ml)	VI(c)	160.2	
Vol of Liq @ Std. Conds. (scf)	V(w std)(	7.541 )	

Sample Point	dClock Time	Orifice Meter dH (in H2O)	Stack Temp (degF)	Gas Temp in	Meter (degF) out
1	15	1.50	225	67	67
2	15	1.50	225	71	68
3	15	1.50	226	73	71
4	15	1.50	225	71	71
<b>TOTALS</b>	60	6.0000	901.0	282	277

## MOISTURE AND VOLUME CALCULATIONS

Plant: EDISON, EGS  
 Date: 3/23/94  
 Performed by: CG/BD

Sample Location: UNIT 1  
 Test No./Type: MOISTURE/FGR ON  
 Start/Stop Time: 1245/1345

CONDITIONS: MID LOAD, FGR ON

PARAMETER	SYMBOL	VALUE (calc.)	FIELD DATA AVERAGES
Gas Meter Correction Factor	(gamma)	1.019	Avg Orifice Meter Reading (in H2O) dH(avg) = 1.500
Barometric Pressure (in Hg)	P(b)	29.91	Avg Stack Temperature (degF) T(s avg) = 228.5
# of Sample Points	#	4	Average Meter Temperature (degF) T(m avg) = 71.9
Total Sampling Time (min)	(theta) (	60.00 )	
Stack (Duct) Dimensions (in):			
Radius (if round)	R	114.0	
Length (if rectangular)	L	0.0	
Width (if rectangular)	W	0.0	
Area of Stack (sq ft)	A(s) (	283.5 )	
Gas Meter Initial Reading (cu ft)		429.22	
Gas Meter Final Reading (cu ft)		469.26	
Net Gas Sample Volume (cu ft)	V(m) (	40.04 )	
Vol of Liquid Collected (ml)	VI(c)	159.6	
Vol of Liq @ Std. Conds. (scf)	V(w std)(	7.512 )	
			<b>CALCULATED VALUES</b>
			Meter Volume (std, cu. ft.) V(m std) = 40.62
			Stack Gas Water Vapor Proportion B(wo) = 0.156

Sample Point	dClock Time	Orifice Meter dH (in H2O)	Stack Temp (degF)	Gas Temp in	Meter (degF) out
1	15	1.50	227	71	71
2	15	1.50	230	72	72
3	15	1.50	228	73	71
4	15	1.50	229	73	72
<b>TOTALS</b>	60	6.0000	914.0	289	286

## MOISTURE AND VOLUME CALCULATIONS

Plant: EDISON, EGS  
 Date : 3/23/94  
 Performed by: CG/BD

Sample Location: UNIT 1  
 Test No./Type: MOISTURE/BASELINE  
 Start/Stop Time: 2325/2425

CONDITIONS:      LOW LOAD, BASELINE

PARAMETER	SYMBOL	VALUE (calc.)	FIELD DATA AVERAGES
Gas Meter Correction Factor	(gamma)	1.019	Avg Orifice Meter Reading (in H2O)    dH(avg) = 1.500
Barometric Pressure (in Hg)	P(b)	29.91	Avg Stack Temperature (degF)        T(s avg) = 182.3
# of Sample Points	#	4	Average Meter Temperature (degF)    T(m avg) = 53.3
Total Sampling Time (min)	(theta) (	60.00 )	
 Stack (Duct) Dimensions (in):			
Radius (if round)	R	114.0	
Length (if rectangular)	L	0.0	
Width (if rectangular)	W	0.0	
Area of Stack (sq ft)	A(s) (	283.5 )	 CALCULATED VALUES
Gas Meter Initial Reading (cu ft)		495.38	Meter Volume (std, cu. ft.)            V(m std) = 40.73
Gas Meter Final Reading (cu ft)		534.12	Stack Gas Water Vapor Proportion    B(wo) = 0.147
Net Gas Sample Volume (cu ft)	V(m) (	38.74 )	
Vol of Liquid Collected (ml)	VI(c)	148.9	
Vol of Liq @ Std. Conds. (scf)	V(w std)(	7.009 )	

Sample Point	dClock Time	Orifice Meter dH (in H2O)	Stack Temp (degF)	Gas Temp in	Meter (degF) out
1	15	1.50	183	52	54
2	15	1.50	182	54	53
3	15	1.50	182	56	53
4	15	1.50	182	53	51
<b>TOTALS</b>	60	6.0000	729.0	215	211

## MOISTURE AND VOLUME CALCULATIONS

Plant: EDISON, EGS  
 Date : 3/24/94  
 Performed by: CG/BD

Sample Location: UNIT 1  
 Test No./Type: MOISTURE/FGR ON  
 Start/Stop Time: 0117/0217

CONDITIONS:    LOW LOAD, FGR ON

PARAMETER	SYMBOL	VALUE (calc.)
Gas Meter Correction Factor	(gamma)	1.019
Barometric Pressure (in Hg)	P(b)	29.91
# of Sample Points	#	4
Total Sampling Time (min)	(theta) (	60.00 )
Stack (Duct) Dimensions (in):		
Radius (if round)	R	114.0
Length (if rectangular)	L	0.0
Width (if rectangular)	W	0.0
Area of Stack (sq ft)	A(s) (	283.5 )
Gas Meter Initial Reading (cu ft) :		534.38
Gas Meter Final Reading (cu ft)		570.97
Net Gas Sample Volume (cu ft)	V(m) (	36.59 )
Vol of Liquid Collected (ml)	Vl(c)	144.7
Vol of Liq @ Std. Conds. (scf)	V(w std)	6.811 )

### FIELD DATA AVERAGES

Avg Orifice Meter Reading (in H2O)	dH(avg) =	1.150
Avg Stack Temperature (degF)	T(s avg) =	181.5
Average Meter Temperature (degF)	T(m avg) =	49.8

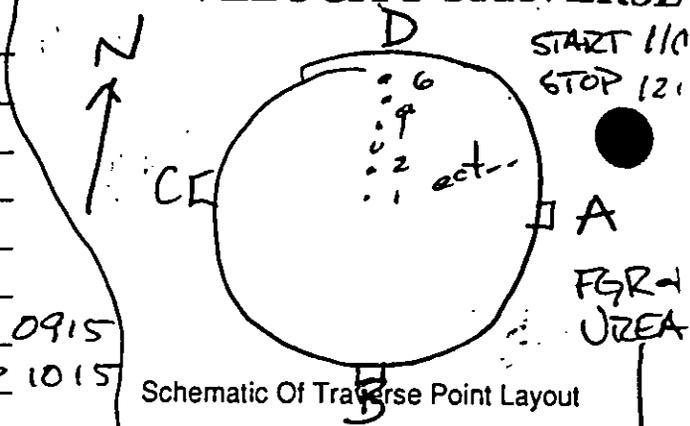
### CALCULATED VALUES

Meter Volume (std, cu. ft.)	V(m std) =	38.70
Stack Gas Water Vapor Proportion	B(wo) =	0.150

Sample Point	dClock Time	Orifice Meter dH (in H2O)	Stack Temp (degF)	Gas Temp in	Meter (degF) out
1	15	1.20	182	49	49
2	15	1.20	181	51	49
3	15	1.10	182	51	49
4	15	1.10	181	51	49
<b>TOTALS</b>	60	4.6000	726.0	202	196

# Full Load, FGR ON PRELIMINARY VELOCITY TRAVERSE

Plant SCE  
 Date 3/22/94  
 Location SCE Etiwanda  
 Stack I.D. 19'  
 Barometric Pressure, in. Hg 29.91  
 Static Pressure, in. H<sub>2</sub>O 0.22  
 Cp 0.84  
 Operators B.D. C.G. Time 0915  
 STOP 1015  
 FGR ON 2 to leak dc, OK

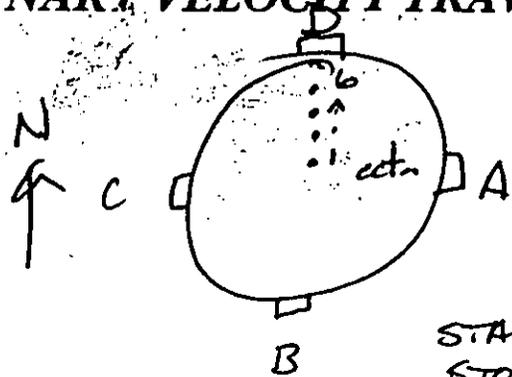


TRAVERSE POINT NUMBER	VELOCITY HEAD (Δps), in. H <sub>2</sub> O	STACK TEMPERATURE (T <sub>s</sub> ), °F
B-1	0.90	249
-2	0.85	
-3	0.85	
-4	0.90	
-5	0.85	
-6	0.85	
D-1	0.90	
-2	0.90	
-3	1.00	
-4	1.10	
-5	1.10	
-6	1.15	
B-1	0.80	
-2	0.75	
-3	0.90	
-4	0.80	
-5	0.90	
-6	0.90 <del>0.85</del> cda	
A-1	0.85	
-2	1.05	
-3	1.05	
-4	0.95	
-5	0.95	
-6	0.95	
AVERAGE		

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δps), in. H <sub>2</sub> O	STACK TEMPERATURE (T <sub>s</sub> ), °F
C-1	0.85	251
2	0.90	
3	0.85	
4	0.85	
5	0.80	
6	0.85	
B-1	0.85	
-2	0.85	
-3	0.85	
-4	0.90	
-5	0.85	
-6	0.85	
D-1	0.85	
-2	0.95	
-3	0.90	
-4	1.00	
-5	1.00	
-6	1.05	
A-1	0.90	
-2	0.95	
-3	0.95	
-4	0.90	
-5	0.95	
-6	0.95	
AVERAGE		

# PRELIMINARY VELOCITY TRAVERSE

Plant Edison EGS  
 Date 3/22/94  
 Location UNIT 3  
 Stack I.D. 19'  
 Barometric Pressure, in. Hg 29.91  
 Static Pressure, in. H<sub>2</sub>O 0.22  
 Cp 0.84  
 Operators CH  
EGR & Urea On - Run 2



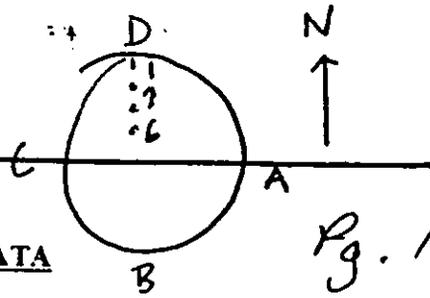
START 1500  
 STOP 1455

START 1301

STOP 1400

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δps), in. H <sub>2</sub> O	STACK TEMPERATURE (T <sub>s</sub> ), °F
A-1	0.85	250
-2	0.90	
-3	0.90	
-4	0.90	
-5	0.95	
-6	0.85	
B-1	0.85	
-2	0.85	
-3	0.85	
-4	0.85	
-5	0.85	
-6	0.90	
C-1	0.80	
-2	0.80	
-3	0.75	
-4	0.80	
-5	0.80	
-6	0.80	
D-1	0.85	
-2	0.90	
-3	1.00	
-4	1.00	
-5	1.00	
-6	1.10	
AVERAGE		

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δps), in. H <sub>2</sub> O	STACK TEMPERATURE (T <sub>s</sub> ), °F
A-1	0.90	250
-2	0.85	
-3	0.90	
-4	0.85	
-5	0.90	
-6	0.90	
B-1	0.85	
-2	0.90	
-3	0.80	
-4	0.85	
-5	0.85	
-6	0.90	
C-1	0.80	
C-2	0.80	
-3	0.75	
-4	0.80	
-5	0.85	
-6	0.80	
D-1	0.85	
-2	0.95	
-3	0.90	
-4	1.00	
-5	0.95	
-6	1.05	
AVERAGE		



Pg. 1 of 2

**VELOCITY DATA**

Client/Location SCE-Etiwanda  
 Sample Location: Stack  
 Unit No: 3  
 Test No: Mid/Cyclonic Flow  
 Barometric Pressure (in Hg): 29.91  
 Static Pressure in Stack (inwg): + 0.05

Date: 3-23-94  
 Data Taken By: Robt. M.  
 Test Description: Velocity  
 Pitot I.D. No.: 0.81 (Coefficient)  
 Pre-Test Leak Check   
 Post-Test Leak Check:

Time	Port	Point	Yaw Angle (Degrees)	Velocity (P1-P2)	Pitch (P4-P5)	Temperature (F)	
0759	D	6	-7	0.50	Z	230	
		5	-5	0.51		229	
		4	0	0.65		229	
		3	+4	0.65		230	
		2	+10	0.59		230	
		1	0	0.52		228	
0803	C	6	-22	0.48		Z	228
		5	-10	0.40			231
		4	-15	0.45			229
		3	-8	0.51			229
		2	+5	0.48			230
		1	+20	0.41			231
0825	B	6	+2	0.50	Z		230
		5	+5	0.45			230
		4	+5	0.45			229
		3	+5	0.54			230
		2	+25	0.39			228
		1	+45	0.30			228

Note: Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.

Mid-load, Cyclonic Flow

Pg. 2 of 2

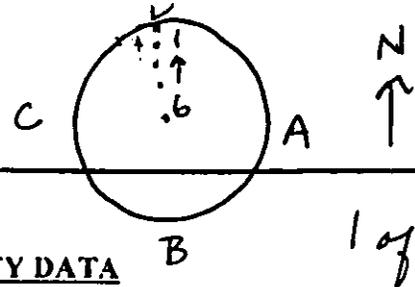
VELOCITY DATA

Client/Location \_\_\_\_\_ Date: \_\_\_\_\_  
 Sample Location: \_\_\_\_\_ Data Taken By: \_\_\_\_\_  
 Unit No: \_\_\_\_\_ Test Description: \_\_\_\_\_  
 Test No: \_\_\_\_\_ Pitot I.D. No.: *RB*  
 Barometric Pressure (in Hg): \_\_\_\_\_ Pre-Test Leak Check: *(circle with slash)*  
 Static Pressure in Stack (iwg): \_\_\_\_\_ Post-Test Leak Check: \_\_\_\_\_

*See*

Time	Port	Point	Yaw Angle (Degrees)	Velocity (P1-P2)	Pitch (P4-P5)	Temperature (F)
12845	A	6	0	0.51	<i>(wavy line)</i>	230
		5	+5	0.59		230
		4	0	0.58		230
		3	+8	0.59		230
		2	+17	0.55		230
		1	+40	0.37		229
		<del>6</del>				
		<del>5</del>				
		<del>4</del>				
		<del>3</del>				
		<del>2</del>				
		<del>1</del>				

~~Note:~~ Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.



**VELOCITY DATA**

Client/Location SCE/Etiwanda 3 Date: 3-23-94  
 Sample Location: Stack Data Taken By: Robt. M.  
 Unit No: 3 Test Description: Velocity  
 Test No: Mid load Baseline Pitot I.D. No.: 0.84 (Coefficient)  
 Barometric Pressure (in Hg): 29.91 Pre-Test Leak Check: ✓  
 Static Pressure in Stack (inwg): +0.05 Post-Test Leak Check: .  
 # P12-02

Time	Port	Point	Yaw Angle Velocity (Degrees)	Velocity (P1-P2)	<del>P4-P5</del> (P4-P5)	Temperature (F)
1100	B	1 <del>AD</del>	0.50			225
		2 <del>S</del>	0.50			
		3 <del>V</del>	0.55			
		4 <del>B</del>	0.50			
		5 <del>R</del>	0.50			
	↓	6 <del>V</del>	0.45			
1110	A	1 <del>AD</del>	0.45			
		2 <del>S</del>	0.50			
		3 <del>V</del>	0.55			
		4 <del>B</del>	0.60			
		5 <del>R</del>	0.50			
	↓	6 <del>V</del>	0.50			

~~Positive~~ rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.

Mid Load, Baseline

VELOCITY DATA

2 of 2

Client/Location \_\_\_\_\_

Date: \_\_\_\_\_

Sample Location: \_\_\_\_\_

Data Taken By: \_\_\_\_\_

Unit No: \_\_\_\_\_

Test Description: \_\_\_\_\_

Test No: \_\_\_\_\_

Pitot I.D. No.: \_\_\_\_\_

Barometric Pressure (in Hg): \_\_\_\_\_

Pre-Test Leak Check \_\_\_\_\_

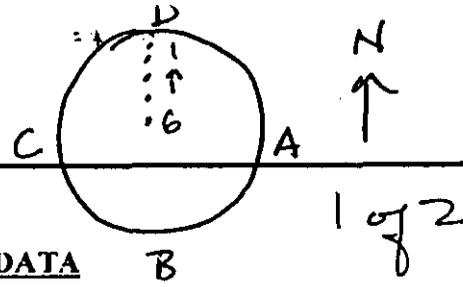
Static Pressure in Stack (iwg): \_\_\_\_\_

Post-Test Leak Check: \_\_\_\_\_

See [circled scribble]

Time	Port	Point	Yaw Angle velocity (Degrees)	Velocity (P1-P2)	<del>Velocity</del> (P4-P5)	Temperature (F)
1120	D	60 1	0.45			225
		5 2	0.55		[wavy line]	
		4 3	0.60			
		3 4	0.60			
		2 5	0.60			
		1 6	0.55			
1145	C	6 1	0.40			
		5 2	0.55			
		4 3	0.50			
		3 4	0.55			
		2 5	0.50			
		1 6	0.35			

Note: Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.



[REDACTED]  
[REDACTED] VELOCITY DATA

Client/Location SCF Etiwanda  
 Sample Location: Unit 3  
 Unit No: 3  
 Test No: Mid load FGR ON  
 Barometric Pressure (in Hg): 29.91  
 Static Pressure in Stack (inwg): +0.05

Date: 3/23/94  
 Data Taken By: B. Day Robt. M  
 Test Description: Velocity  
 Pilot I.D. No.: 0.84  
 Pre-Test Leak Check   
 Post-Test Leak Check:

→ #P12-02

Time	Port	Point	Yaw Angle (Degrees)	Velocity (P1-P2)	Pitch (P4-P5)	Temperature (F)
1245	C ↓	16	—	0.50		228 ↓
		29	—	0.45		
		34	—	0.50		
		43	—	0.50		
		52	—	0.55		
		61	—	0.35		
1300	D ↓	16	—	0.50		
		29	—	0.50		
		37	—	0.60		
		43	—	0.65		
		52	—	0.60		
		61	—	0.60		

Note: Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.

Mid-load / FGZ ON

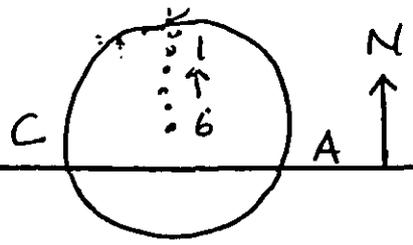
2 of 2

VELOCITY DATA

Client/Location \_\_\_\_\_ Date: \_\_\_\_\_  
 Sample Location: \_\_\_\_\_ Data Taken By: \_\_\_\_\_  
 Unit No: \_\_\_\_\_ Test Description: *Page 1*  
 Test No: *See* Pitot I.D. No.: \_\_\_\_\_  
 Barometric Pressure (in Hg): \_\_\_\_\_ Pre-Test Leak Check \_\_\_\_\_  
 Static Pressure in Stack (iwg): \_\_\_\_\_ Post-Test Leak Check: \_\_\_\_\_

Time	Port	Point	Yaw Angle (Degrees)	Velocity (P1-P2)	Pitch (P4-P5)	Temperature (F)
1315	A	6 1	—	0.50		229
		5 2	—	0.55		↓
		4 3	—	0.55		
		3 4	—	0.55		
		2 5	—	0.60		
		1 6	—	0.50		
1340	B	6 1	—	0.60		
		5 2	—	0.45		
		4 3	—	0.45		
		3 4	—	0.50		
		2 5	—	0.50		
		1 6	—	0.45		

Note: Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.



**VELOCITY DATA**

Client/Location SCE Etiwanda  
 Sample Location: ~~A~~  
 Unit No: 3  
 Test No: Mid load Force on  
 Barometric Pressure (in Hg): 29.91  
 Static Pressure in Stack (iwg): +0.05

Date: 3/23/94  
 Data Taken By: B. Day Robt. M  
 Test Description: Velocity  
 Pitot I.D. No.: 0.84 (coefficient)  
 Pre-Test Leak Check   
 Post-Test Leak Check: \_\_\_\_\_  
 → #P12-02

Time	Port	Point	Yaw Angle (Degrees)	Velocity (P1-P2)	Pitch (P4-P5)	Temperature (F)
1435	B	1 6 80	—	0.50		230
		2 5	—	0.40		
		3 4	—	0.50		
		4 3	—	0.50		
		5 2	—	0.50		
		6 1	—	0.45		
1440	A	1 6	—	0.55		
		2 5	—	0.50		
		3 4	—	0.55		
		4 3	—	0.60		
		5 2	—	0.50		
		6 1	—	0.50		

Note: Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.

Mid-Load, FGZ + UREA ON

**VELOCITY DATA**

Client/Location \_\_\_\_\_

Date: \_\_\_\_\_

Sample Location: \_\_\_\_\_

Data Taken By: \_\_\_\_\_

Unit No: \_\_\_\_\_

Test Description: \_\_\_\_\_

Test No: \_\_\_\_\_

Pitot I.D. No.: \_\_\_\_\_

Barometric Pressure (in Hg): \_\_\_\_\_

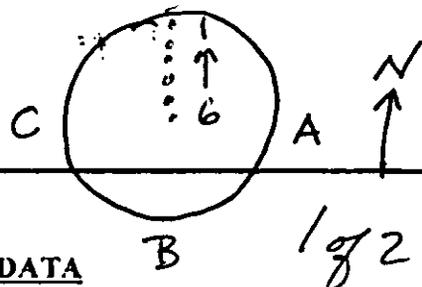
Pre-Test Leak Check \_\_\_\_\_

Static Pressure in Stack (iwg): \_\_\_\_\_

Post-Test Leak Check: \_\_\_\_\_

Time	Port	Point	Yaw Angle Velocity (Degrees)	Velocity (P1-P2)	Pitch (P4-P5)	Temperature (F)
1455	D	1 6 90	0.50			230
		2 4	0.55			
		3 4	0.60			
		4 7	0.60			
		5 2	0.60			
	↓	6 1	0.55			
1530	C	1 6 90	0.50			
		2 4	0.50			
		3 4	0.50			
		4 7	0.60			
		5 2	0.50			
	↓	6 1	0.40			

Note: Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.



Low Load, Cyclonic Flow

VELOCITY DATA

Client/Location SC E Etiwanda  
 Sample Location: Unit 3  
 Unit No: 3  
 Test No: Baseline low load  
 Barometric Pressure (in Hg): 29.91  
 Static Pressure in Stack (inwg): -0.24

Date: 3/23/94  
 Data Taken By: B. Day Rofit M  
 Test Description: velocity  
 Pilot I.D. No.: 0.81 coefficient  
 Pre-Test Leak Check   
 Post-Test Leak Check: \_\_\_\_\_

Time	Port	Point	Yaw Angle (Degrees)	Velocity (P1-P2)	<del>Pitch (P1-P2)</del>	Temperature (F)
2110	D	6	0	0.14		185
		5		0.16		187
		4		0.16		187
		3		0.18		186
		2		0.15		185
		1		0.12		183
	C	6		0.16		183
		5		0.15		183
		4		0.16		185
		3		0.16		183
		2		0.14		184
		1		0.13 → 0.13		179

Note: Clockwise rotation of the probe corresponds to a positive yaw angle: > 0 or > 90 degrees.



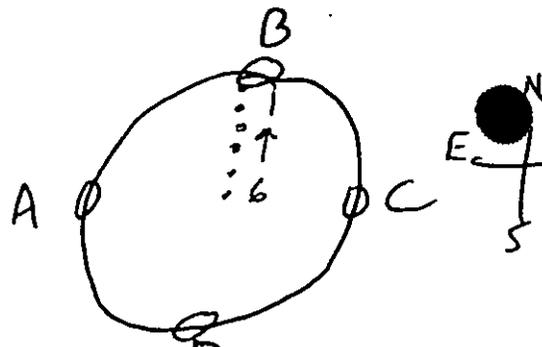




LOW LOAD, FG2 ON

PRELIMINARY VELOCITY TRAVERSE

Plant SCE Etiwanda  
 Date 3/24/94  
 Location Unit 3  
 Stack I.D. 19"  
 Barometric Pressure, in. Hg 29.91  
 Static Pressure, in. H<sub>2</sub>O -0.25  
 Cp 0.84  
 Operators B. Day



Schematic Of Traverse Point Layout

start: 0117  
 stop: 0210

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δps), in. H <sub>2</sub> O	STACK TEMPERATURE (T <sub>s</sub> ), °F
A-6	0.14	182
5	0.15	↓
4	0.14	
3	0.13	
2	0.12	
1	0.07	
B-6	0.15	
5	0.12	
4	0.14	
3	0.12	
2	0.10	
1	0.05	
AVERAGE		

TRAVERSE POINT NUMBER	VELOCITY HEAD (Δps), in. H <sub>2</sub> O	STACK TEMPERATURE (T <sub>s</sub> ), °F
C-6 1	0.12	182
5 2	0.13	↓
4 3	0.11	
3 4	0.12	
2 5	0.12	
1 6	0.08	
D-6 1	0.13	
5 2	0.14	
4 3	0.10	
3 4	0.16	
2 5	0.15	
1 6	0.13	
AVERAGE		













**APPENDIX H**  
**SAMPLING EQUIPMENT CALIBRATION RECORDS**



**APPENDIX H-1**  
**DRY GAS METER CALIBRATION RECORDS**



# CONSOLE METER POST-CALIBRATION

Client SCE Project No. 9585011 Calibrated By B. Dany Date 3/30/94  
 Barometric Pressure, P<sub>b</sub> 29.50 in. Hg Pre-Test Meter Correction Factor 0.996 Date Calib. \_\_\_\_\_  
 Ambient Temperature 67 °F Post-Test Meter Correction Factor 0.997  
 Primary Test Meter No. 259453 Console No. 20151 Percent Difference  $\left( \frac{\text{Pre} - \text{Post}}{\text{Pre}} \times 100 = \right)$  0.1

Orifice Manometer Setting, (ΔH), in. H <sub>2</sub> O	Gas Volume		Temperature				Vacuum Setting, in. Hg	Y	K <sub>o</sub>	ΔH@
	Primary Meter (V <sub>p</sub> ), ft <sup>3</sup>	Dry Gas Meter (V <sub>d</sub> ), ft <sup>3</sup>	Primary Meter (t <sub>p</sub> ), °F	Dry Gas Volume		Time (Θ), min				
				Inlet (t <sub>i</sub> ), °F	Outlet (t <sub>o</sub> ), °F					
0.83	10.754	10.712	65 66	67 74	62 64	21	5"	0.996	0.716	1.783
2.00	9.220	9.229	60 60	71 79	65 67	12	5	0.997	0.689	1.899
							Average	0.997	0.703	1.841

	Primary Meter	Total	Dry Gas Meter	Total
Stop	745.240		585.462	
Start	734.486	10.754	574.750	10.712
Stop	756.505		596.729	
Start	747.285	9.220	587.500	9.229
Stop				
Start				

**Calculations**

$$Y = \frac{V_p(P_b)(t_d + 460)}{V_d \left( P_b + \frac{\Delta H}{13.6} \right) (t_p + 460)}$$

$$K_o = \frac{V_p}{\theta \sqrt{\frac{\Delta H (t_d + 460)}{P_b (28.96)}}}$$

$$\Delta H@ = \frac{0.0317 \Delta H}{P_b (t_o + 460)} \left[ \frac{(t_p + 460) \theta}{V_p} \right]^2$$



**APPENDIX H-2**  
**MAGNEHELIC CALIBRATION RECORDS**



DATA SHEET FOR MAGNETIC GAGE  
(<10" H<sub>2</sub>O) CALIBRATION WITH INCLINED MANOMETER

Magnetic Gauge I.D.# R80927  
Reference Gauge I.D.# IM-1

Date 3/31/94  
Calibrated by B. Day  
Calibration for:  
Semiannual   
Bimonthly \_\_\_\_\_  
Other \_\_\_\_\_

Full Scale of Magnetic Gauge 0-10 "H<sub>2</sub>O

System Leak Test (Pass-Fail) <input type="radio"/> or F: <u>10</u> " H <sub>2</sub> O Press. <u>10</u> " H <sub>2</sub> O Vac.						
Leak Test ~90% F.S. (Pass-Fail) <input type="radio"/> or F: " H <sub>2</sub> O Press. " H <sub>2</sub> O Vac.						
Full Scale %	Magne. H <sub>1</sub> in. H <sub>2</sub> O	Standard H <sub>2</sub> in. H <sub>2</sub> O	H <sub>2</sub> - H <sub>1</sub> x px	Differ. H = H <sub>2</sub> - H <sub>1</sub>	Deviation 100ΔH/H <sub>2</sub> %	Remarks**
20	2.0	1.96		0.04	2.0	
40	4.0	3.94		0.06	1.5	
60	6.0	5.98		0.02	0.3	
80						
100						
20	2.0	1.96		0.04	2.0	
40	4.0	3.98		0.02	0.5	
60	6.0	5.99		0.01	0.2	
80						
100						
20	2.0	1.96		0.04	2.0	
40	4.0	3.96		0.04	1.0	
60	6.0	5.98		0.02	0.3	
80						
100						
50	5.0					Vacuum

1.0 in. for H<sub>2</sub>O and Oil Manometer. 13.55 in. for Hg. Manometer  
 \*\* Average Deviation, 95% CI. Correction Factor (0.95 F 1.05). Precision (± 3%)  
 Can only go to 6000 of scale. Calibration above 6000 will be done when dealing w a source over 6 inches of water is tested  
 Figure III-13  
 Example Data Sheet for Differential Pressure Gauge



DATA SHEET FOR MAGNETIC GAGE  
(<10" H<sub>2</sub>O) CALIBRATION WITH INCLINED MANOMETER

Magnetic Gauge I.D.# R910911EUIP  
Reference Gauge I.D.# EM-1

Date 3/31/94  
Calibrated by B. Day  
Calibration for:  
Semiannual   
Bimonthly   
Other

Full Scale of Magnetic Gauge 2.0 "H<sub>2</sub>O

System Leak Test (Pass-Fail) <input checked="" type="radio"/> or F: <input type="radio"/>		6" H <sub>2</sub> O Press.		6" H <sub>2</sub> O Vac.		
Leak Test -90°F.S. (Pass-Fail) <input checked="" type="radio"/> or F: <input type="radio"/>		1.8" H <sub>2</sub> O Press.		1.8" H <sub>2</sub> O Vac.		
Full Scale %	Magne. H <sub>1</sub> in. H <sub>2</sub> O	Standard H <sub>2</sub> in. H <sub>2</sub> O	H <sub>2</sub> - H <sub>1</sub> x 100	Differ. H = H <sub>2</sub> - H <sub>1</sub>	Deviation 100   H <sub>2</sub> - H <sub>1</sub>   %	Remarks**
20	0.4	0.38		0.02	5	
40	0.8	0.78		0.02	2.6	
60	1.2	1.17		0.03	2.6	
80	1.6	1.56		0.04	2.6	
100	2.0	1.95		0.05	2.6	
20	0.4	0.38		0.02	5	
40	0.8	0.78		0.02	2.6	
60	1.2	1.16		0.04	3.5	
80	1.6	1.56		0.04	2.6	
100	2.0	1.95		0.05	2.6	
20	0.4	0.38		0.02	5	
40	0.8	0.78		0.02	2.6	
60	1.2	1.15		0.05	4.3	
80	1.6	1.56		0.04	2.6	
100	2.0	1.95		0.05	2.6	
50	1.0	0.96		0.04	4.2	vacuum

\* 1.0 in. for H<sub>2</sub>O and Oil Manometer. 13.55 in. for Hg. Manometer  
\*\* Average Deviation, 95% CI. Correction Factor (0.95 F 1.05). Precision (± 3%)

Figure III-13  
Example Data Sheet for Differential Pressure Gauge Calibration (English Units)



**APPENDIX H-3**  
**THERMOCOUPLE CALIBRATION RECORDS**



STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

ROG Sampling Probe  
stack temp.

Date 3/30/94 Thermocouple number ROG P-1  
 Ambient temperature 67° F Barometric pressure 29.50 in. Hg  
 Calibrator B. Day Reference: mercury in glass  
 other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, °F
	Simulator	0	0	0
	↓	100	100	0
		200	201	0.5
		300	300	0
		400	399	0.25
		500	500	0

<sup>a</sup> type of calibration system used.

<sup>b</sup> 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{C} + \frac{160}{273}) - (\text{test thermom temp, } ^\circ\text{C} + \frac{160}{273})}{\text{ref temp, } ^\circ\text{C} + \frac{160}{273}} \right] \times 100 = \%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Cold Box #1

Date 3/30/94

Thermocouple number CB1

Ambient temperature 67° F

Barometric pressure 29.50 in. Hg

Calibrator B. Day

Reference: mercury in glass

other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference Thermometer Temperature, °F	Thermocouple potentiometer Temperature, °F	Temperature difference, °F
	Simulator	0	0	0
		100	100	0
		200	202	1
		300	300	0
		400	399	0.25
		500	500	0

a. type of calibration system used.

b. 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{C} + \frac{273}{100})}{\text{ref temp, } ^\circ\text{C} + \frac{273}{100}} = \frac{(\text{test thermom. temp, } ^\circ\text{C} + \frac{273}{100})}{\text{ref temp, } ^\circ\text{C} + \frac{273}{100}} \right] \times 100 = 1.02$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Cold Box #2

Date 3/30/94 Thermocouple number CB2  
 Ambient temperature 71°F Barometric pressure 29.50 in. Hg  
 Calibrator B. Day Reference: mercury-in-glass \_\_\_\_\_  
 other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, % <sup>b</sup>
	Simulator	0	0	0
	↓	100	100	0
		200	202	1
		300	301	0.3
		400	399	0.25
		500	500	0

<sup>a</sup> type of calibration system used.

<sup>b</sup> 
$$\left| \frac{(\text{ref temp, } ^\circ\text{F} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right| \times 100 < 1.5\%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Cold Box #1

Date 3/30/94

Thermocouple number CB4

Ambient temperature 67°F

Barometric pressure 29.50 in. Hg

Calibrator B. Day

Reference: mercury in glass

other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference Thermometer Temperature, °F	Thermocouple potential/temperature, °F	Temperature difference, °F
	↓ Simulator	0	0	0
		100	100	0
		200	201	0.5
		300	301	0.3
		400	399	0.25
		500	500	0

<sup>a</sup> type of calibration system used.

<sup>b</sup> 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] \times 100 = 1.5\%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

umbilical #1  
stack temp male end

Date 3/30/94 Thermocouple number U12A  
 Ambient temperature 67° F Barometric pressure 29.50  
 Calibrator B. Day Reference: mercury in glass  
 other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, °F
	↓ Simulator	0	0	0
		100	98	2
		200	200	0
		300	299	0.3
		400	397	0.8
		500	496	0.8

<sup>a</sup> Type of calibration system used.

<sup>b</sup> 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{F} + \frac{460}{273}) - (\text{test thermom temp, } ^\circ\text{F} + \frac{460}{273})}{\text{ref temp, } ^\circ\text{C} + \frac{273}{1}} \right] \times 100 \text{ (in \%)}$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Umbilical #1  
Stack temp female end

Date 3/30/94

Thermocouple number U12B

Ambient temperature 67° F

Barometric pressure 29.50 in. Hg

Calibrator B. Day

Reference mercury in glass

other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference Thermometer Temperature, °F	Thermocouple output (mV) or Temperature, °F	Temperature difference, °F
	Simulator	0	0	0
		100	98	2
		200	200	0
		300	299	0.3
		400	397	0.8
		500	496	0.8

<sup>a</sup> type of calibration system used.

<sup>b</sup> 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{F} + \frac{460}{2.73})}{\text{ref temp, } ^\circ\text{C} + 273} - \frac{(\text{test thermom temp, } ^\circ\text{C} + \frac{460}{2.73})}{\text{test temp, } ^\circ\text{C} + 273} \right] \times 100 = \%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

umbilical #1  
exit temp male end

Date 3/30/94

Thermocouple number U14A

Ambient temperature 67°F

Barometric pressure 29.50

Calibrator B. Day

Reference: mercury-in-glass

other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, °F
	Simulator	0	0	0.00
	↓	100	98	2
		200	200	0
		300	299	0.3
		400	397	0.8
		500	496	0.8

<sup>a</sup> type of calibration system used.

<sup>b</sup> 
$$\left| \frac{(\text{ref temp, } ^\circ\text{F} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right| \times 100 \leq 1.5\%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

umbilical #1 exit to  
FEMALE

Date 3/30/94

Thermocouple number U14B

Ambient temperature 67°F

Barometric pressure 29.50 in. Hg

Calibrator B. Day

Reference: mercury-in-glass

other Simulator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, % <sup>b</sup>
	Simulator	0	0	0.010
	↓	100	98	2.010
		200	200	0.010
		300	299	0.3010
		400	397	0.8010
		500	496	0.8010

<sup>a</sup> Type of calibration system used.

<sup>b</sup> 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{F} + 460) - (\text{test thermom temp, } ^\circ\text{C} + 460)}{\text{ref temp, } ^\circ\text{C} + 273} \right] \times 100 \pm 1.5\%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

console # 201151  
stack temp

Date 3/30/94

Thermocouple number C27

Ambient temperature 67° F

Barometric pressure 29.50 in. Hg

Calibrator B. Day

Reference: in-glass

other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference Thermometer Temperature, °F	Thermocouple packet/element Temperature, °F	Temperature difference, °F
	↓ Simulator	0	0	0.070
		100	98	2.070
		200	200	0.070
		300	299	0.370
		400	397	0.870
		500	496	0.870

<sup>a</sup> type of calibration system used.

<sup>b</sup> 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{F} + 460)}{\text{ref temp, } ^\circ\text{C} + 273} - \frac{(\text{test thermom temp, } ^\circ\text{C} + 273)}{T + 460} \right] \times 100 = \%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

console # 20151  
exit temp.

Date 3/30/94 Thermocouple number C47  
Ambient temperature 67° F Barometric pressure 29.50 in. Hg  
Calibrator B. Day Reference: mercury-in-glass  
other: Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, °F
	Simulator	0	0	0.076
	↓	100	98	2.020
		200	200	0.020
		300	299	0.3020
		400	397	0.8020
		500	496	0.8020

<sup>a</sup> type of calibration system used.

<sup>b</sup> 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{C} + 273) - (\text{test thermom temp, } ^\circ\text{C} + 273)}{\text{ref temp, } ^\circ\text{C} + 273} \right] \times 100 \leq 1.5\%$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Gas meter In  
console 20151

Date 3/30/94

Thermocouple number C67

Ambient temperature 67°F

Barometric pressure 29.50 in. Hg

Calibrator B. Day

Reference: mercury in glass

other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potentiometer temperature, °F	Temperature difference, °F
	Simulator	0	0	0.000
	↓	100	98	2.000
		200	200	0.000
		300	299	0.300
		400	397	0.800
		500	497	0.6000

<sup>a</sup>Type of calibration system used.

<sup>b</sup>
$$\left[ \frac{(\text{ref temp, } ^\circ\text{C} + \frac{160}{273}) - (\text{test thermom temp, } ^\circ\text{C} + \frac{160}{273})}{\text{ref temp, } ^\circ\text{C} + \frac{160}{273}} \right] \times 100 \text{ (in \%)}$$

STACK TEMPERATURE SENSOR CALIBRATION DATA FORM

Gas Meter Out  
console 20151  
C 77

Date 3/30/94

Thermocouple number

Ambient temperature 67° F

Barometric pressure 29.50 in. Hg

Calibrator B. Day

Reference: mercury-in-glass

other Simulator/calibrator

Reference point number	Source <sup>a</sup> (specify)	Reference thermometer temperature, °F	Thermocouple potential/temperature, °F	Temperature difference, °F
	↓ Simulator	0	0	0.000
		100	98	2.00
		200	200	0
		300	299	0.300
		400	397	0.800
		500	496	0.800

a. Type of calibration system used.

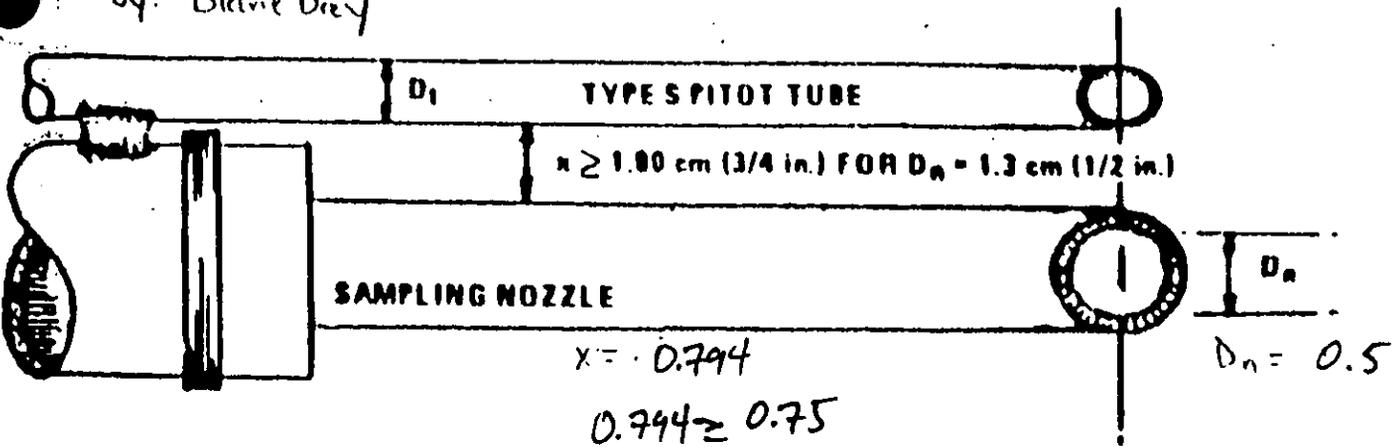
b. 
$$\left[ \frac{(\text{ref temp, } ^\circ\text{F} + \frac{460}{1.8}) - (\text{test thermom temp, } ^\circ\text{F} + \frac{460}{1.8})}{\text{ref temp, } ^\circ\text{C} + 273} \right] \times 100$$

**APPENDIX H-4**  
**PITOT CALIBRATION RECORDS**

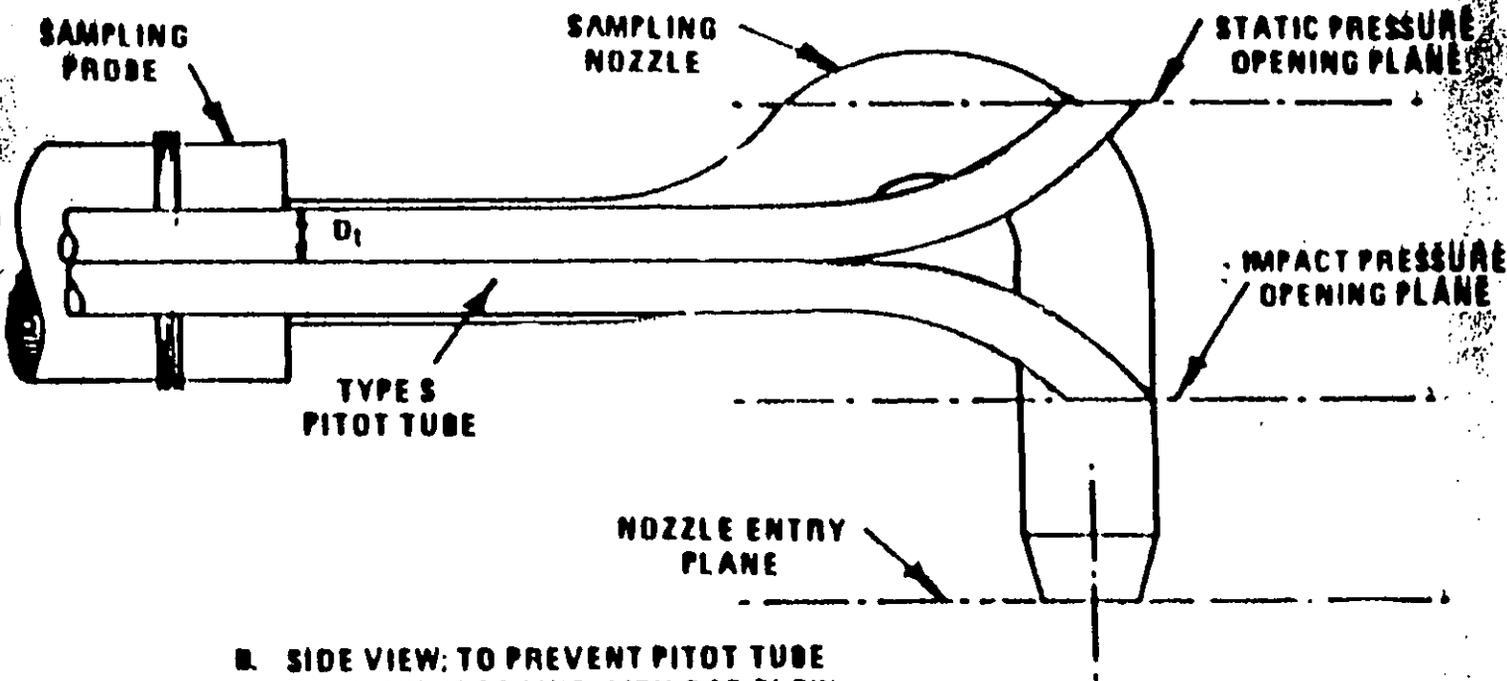


Pitot # S 1202  
 Calibrated 12/13/93  
 by: Blake Drey

Semiannual cal.  
 required



A. BOTTOM VIEW: SHOWING MINIMUM PITOT NOZZLE SEPARATION.

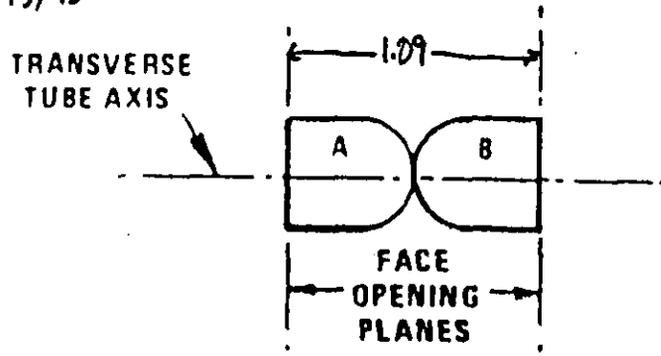


B. SIDE VIEW: TO PREVENT PITOT TUBE FROM INTERFERING WITH GAS FLOW STREAMLINES APPROACHING THE NOZZLE, THE IMPACT PRESSURE OPENING PLANE OF THE PITOT TUBE SHALL BE EVEN WITH OR ABOVE THE NOZZLE ENTRY PLANE.

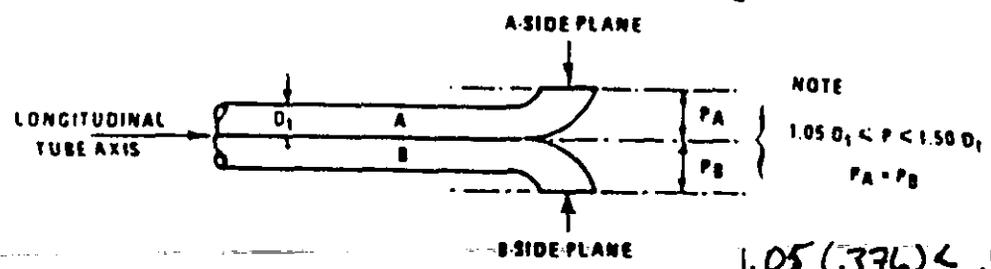
Figure 2-6. Proper pitot tube-sampling nozzle configuration to prevent aerodynamic interference. Hook-type nozzle; centers of nozzle and pitot opening aligned;  $D_1$  between 0.48 and 0.95 cm (1/8 and 3/8 in.).

[Figure 2-6 amended by 52 FR 34639, September 14, 1987]

Pitot # 51202  
 calibrated 12/13/93  
 by: B. Day

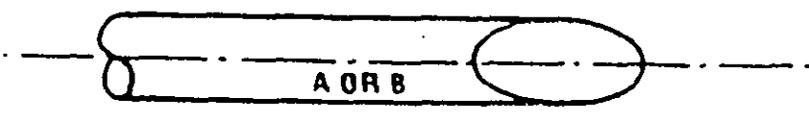


(a)  $D_1 = 0.776$   
 $P_A = .545$   
 $P_B = .545$



NOTE  
 $1.05 D_1 < P < 1.50 D_1$   
 $P_A = P_B$

$1.05 (.776) < .545 < 1.5(.776)$   
 $.395 < .545 < .564$

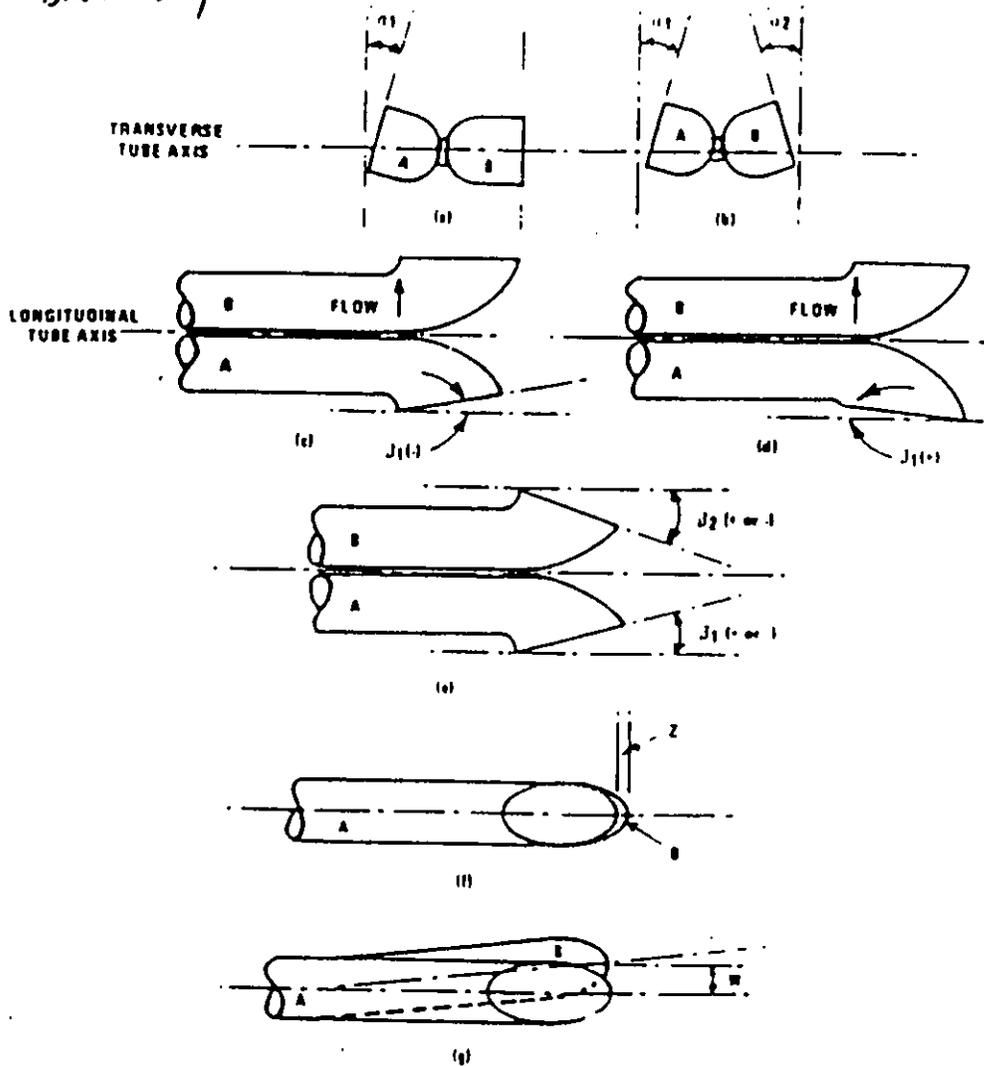


(c)

Properly constructed Type S pitot tube, shown in: (a) end view; face opening planes perpendicular to transverse axis; (b) top view; face opening planes parallel to longitudinal axis; (c) side view; both legs of equal length and centerlines coincident, when viewed from both sides. Baseline coefficient values of 0.84 may be assigned to pitot tubes constructed this way.

Figure III-2  
 Proper Pitot Tube Configuration

Pitot # S 1202  
 calibrated 12/13/99  
 by: Blane Day



Types of face-opening misalignment that can result from field use or improper construction of Type S pitot tubes. These will not affect the baseline value of  $C_0(s)$  so long as  $\alpha_1$  and  $\alpha_2 < 10^\circ$ ,  $\beta_1$  and  $\beta_2 < 5^\circ$ ,  $z < 0.32$  cm (1/8 in.) and  $w < 0.08$  cm (1/32 in.) (criterion 11 in Section 6).

$$\begin{aligned} \alpha_1 &= 0^\circ & \beta_1 &= 0^\circ & z &= 0^\circ \\ \alpha_2 &= 0^\circ & \beta_2 &= 0^\circ & w &= 0^\circ \end{aligned}$$

Figure III-3  
 Improper Pitot Tube Configuration

Pitot # S1202  
 calibrated 12/13/93  
 by: Brent Dwyer

separation calc.  
 required

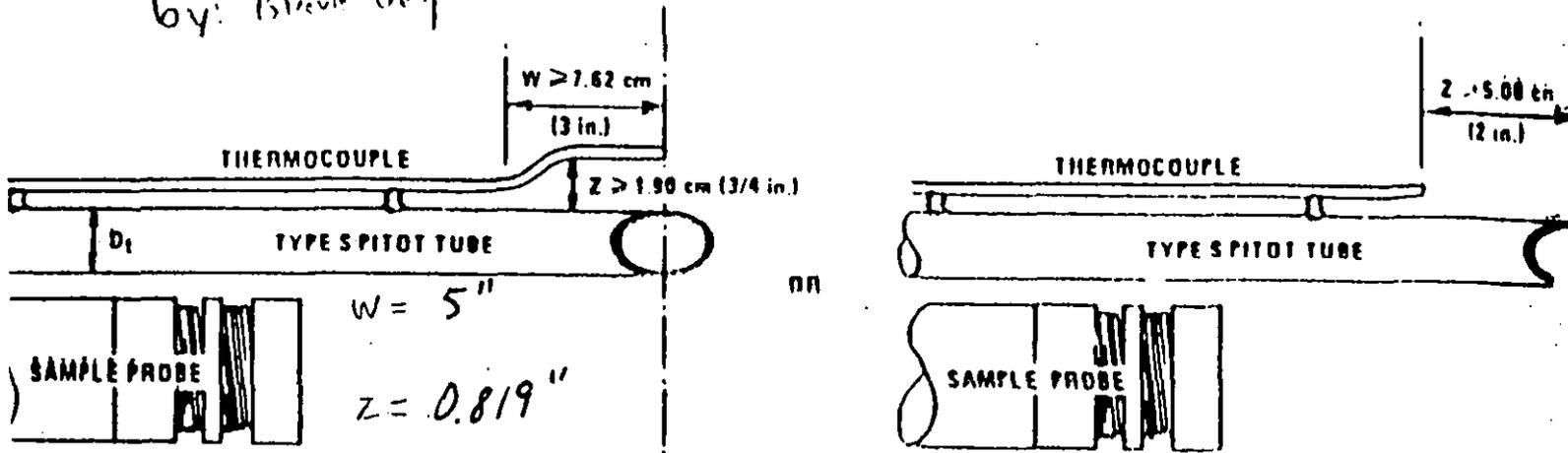


Figure 2.7. Proper thermocouple placement to prevent interference;  $D_t$  between 0.48 and 0.95 cm (3/16 and 3/8 in.).

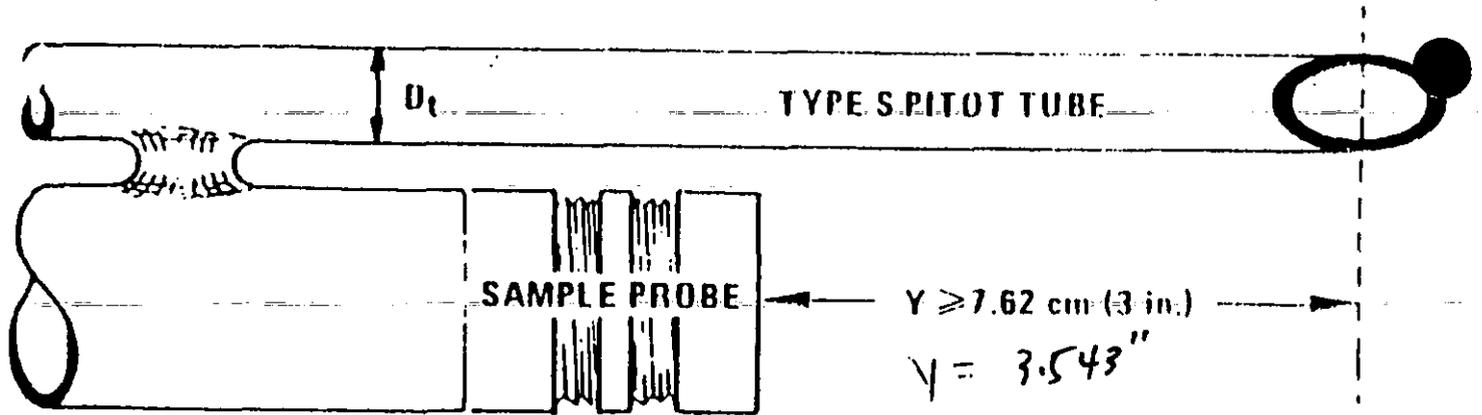


Figure 2.8. Minimum pitot-sample probe separation needed to prevent interference;  $D_t$  between 0.48 and 0.95 cm (3/16 and 3/8 in.).

Pitot # 5 S1201  
 calibrated 12/13/93  
 by: Blaine Day

Measurement not required

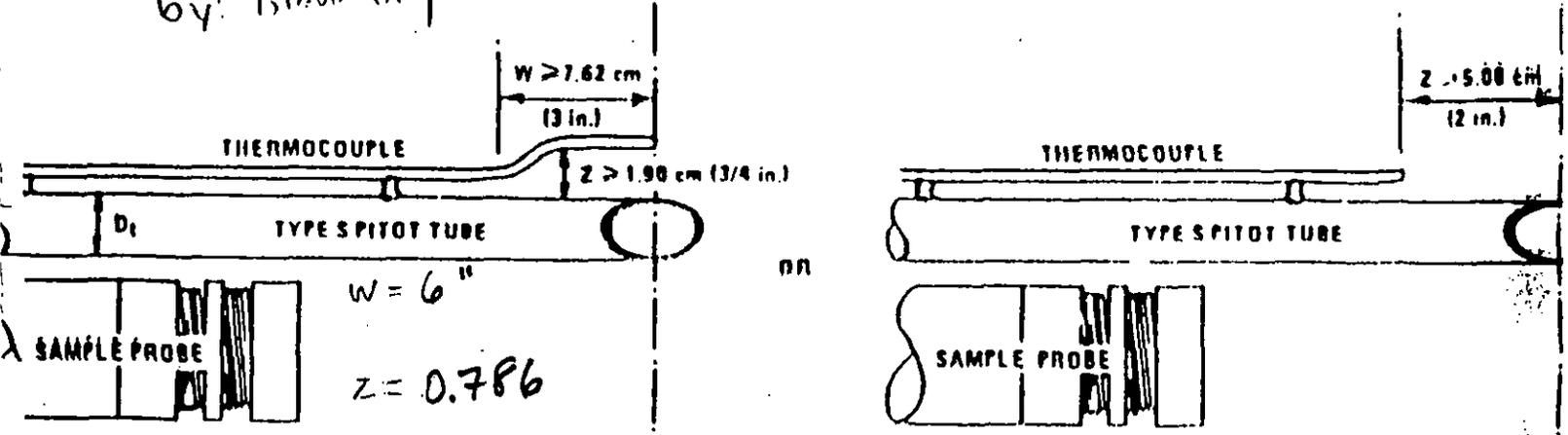


Figure 2.7. Proper thermocouple placement to prevent interference;  $D_1$  between 0.48 and 0.95 cm (3/16 and 3/8 in.).

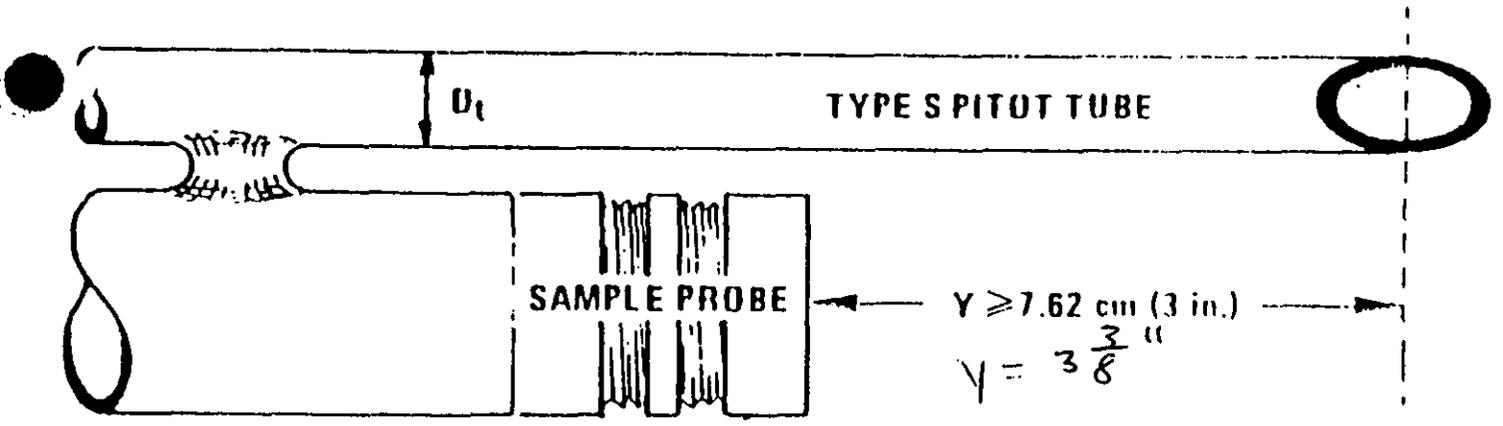
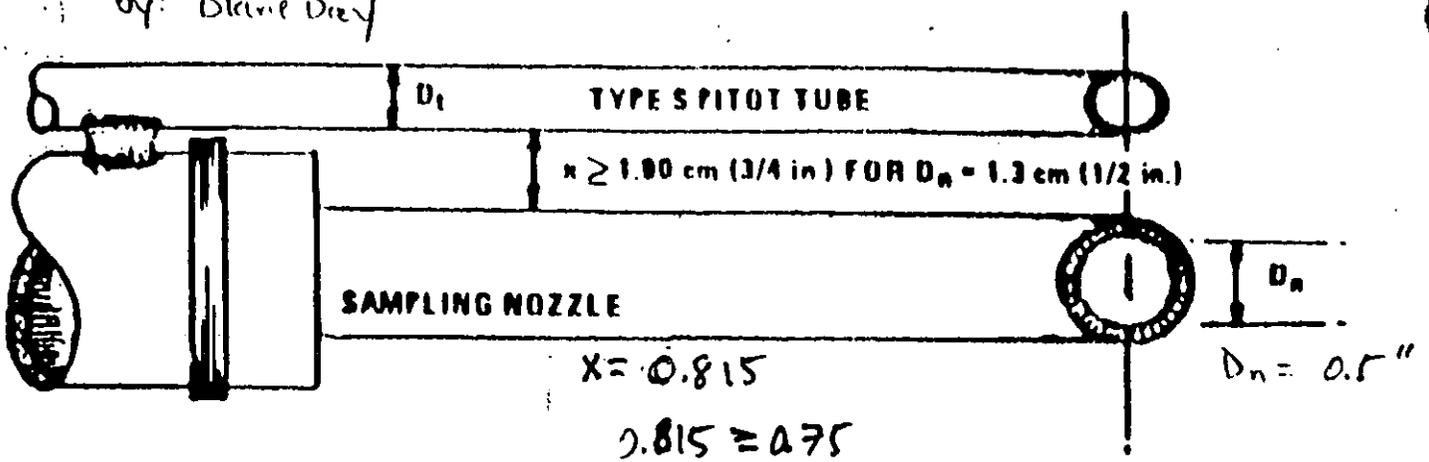


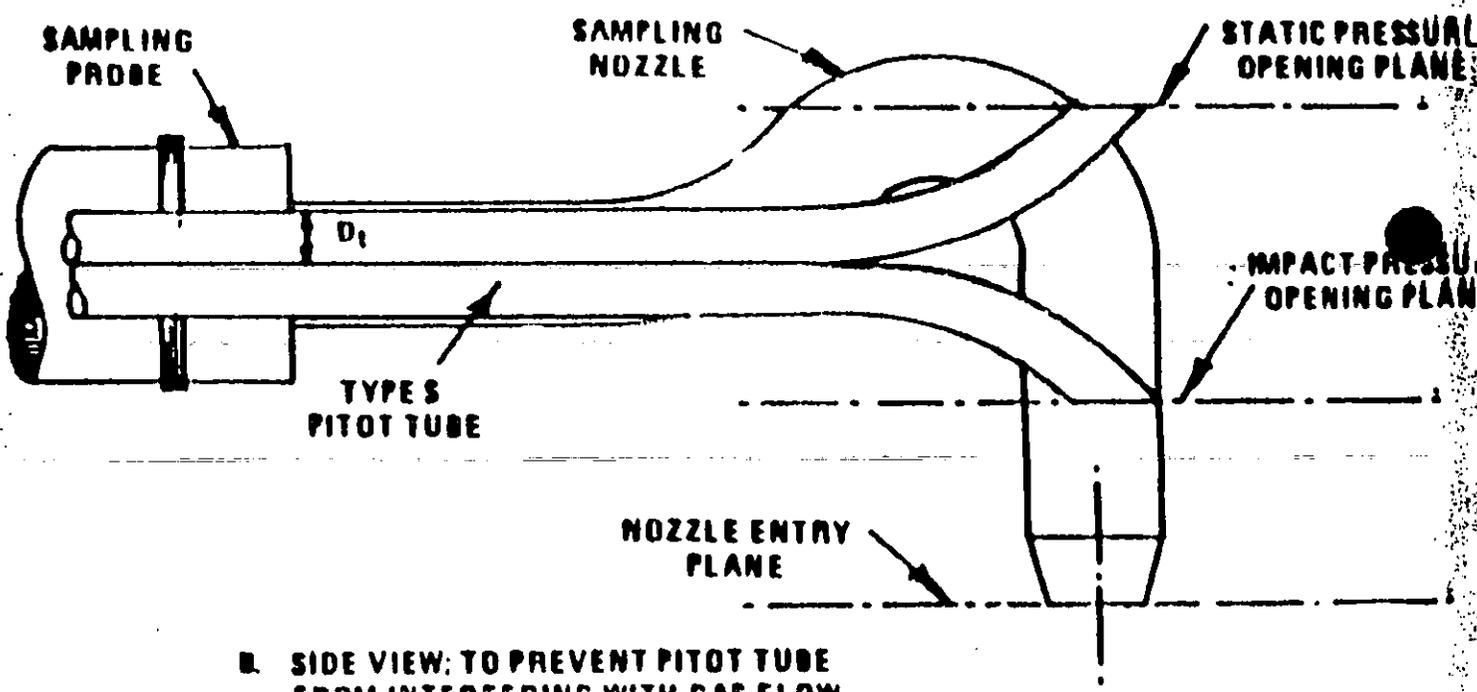
Figure 2.8. Minimum pitot-sample probe separation needed to prevent interference between 0.48 and 0.95 cm (3/16 and 3/8 in.).

Pitot # 51201  
 Calibrated 12/13/93  
 by: Blake Drey

semiannual cal.  
 required



A. BOTTOM VIEW; SHOWING MINIMUM PITOT-NOZZLE SEPARATION.



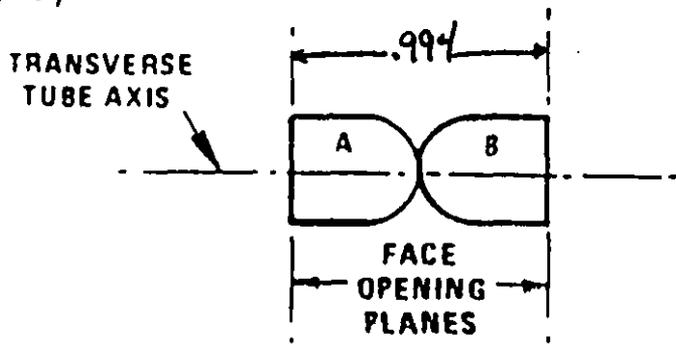
B. SIDE VIEW; TO PREVENT PITOT TUBE FROM INTERFERING WITH GAS FLOW STREAMLINES APPROACHING THE NOZZLE, THE IMPACT PRESSURE OPENING PLANE OF THE PITOT TUBE SHALL BE EVEN WITH OR ABOVE THE NOZZLE ENTRY PLANE.

Figure 2-6. Proper pitot tube-sampling nozzle configuration to prevent aerodynamic interference with hook-type nozzle; centers of nozzle and pitot opening aligned;  $D_t$  between 0.48 and 0.63 in. (3/8 and 3/8 in.).

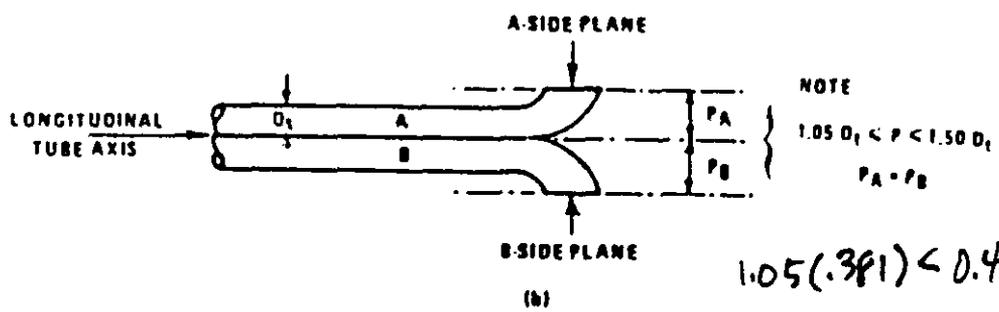
[Figure 2-6 amended by 52 FR 34639, September 14, 1987]

Pitot # 51201  
 calibrated 12/13/93  
 by: B. Day

$D_t =$



(a)  $D_t = 0.381$   
 $P_A = 0.497$   
 $P_B = 0.497$



$1.05(.381) < 0.497 < 1.50(.381)$   
 $0.4 < 0.497 < 0.572$

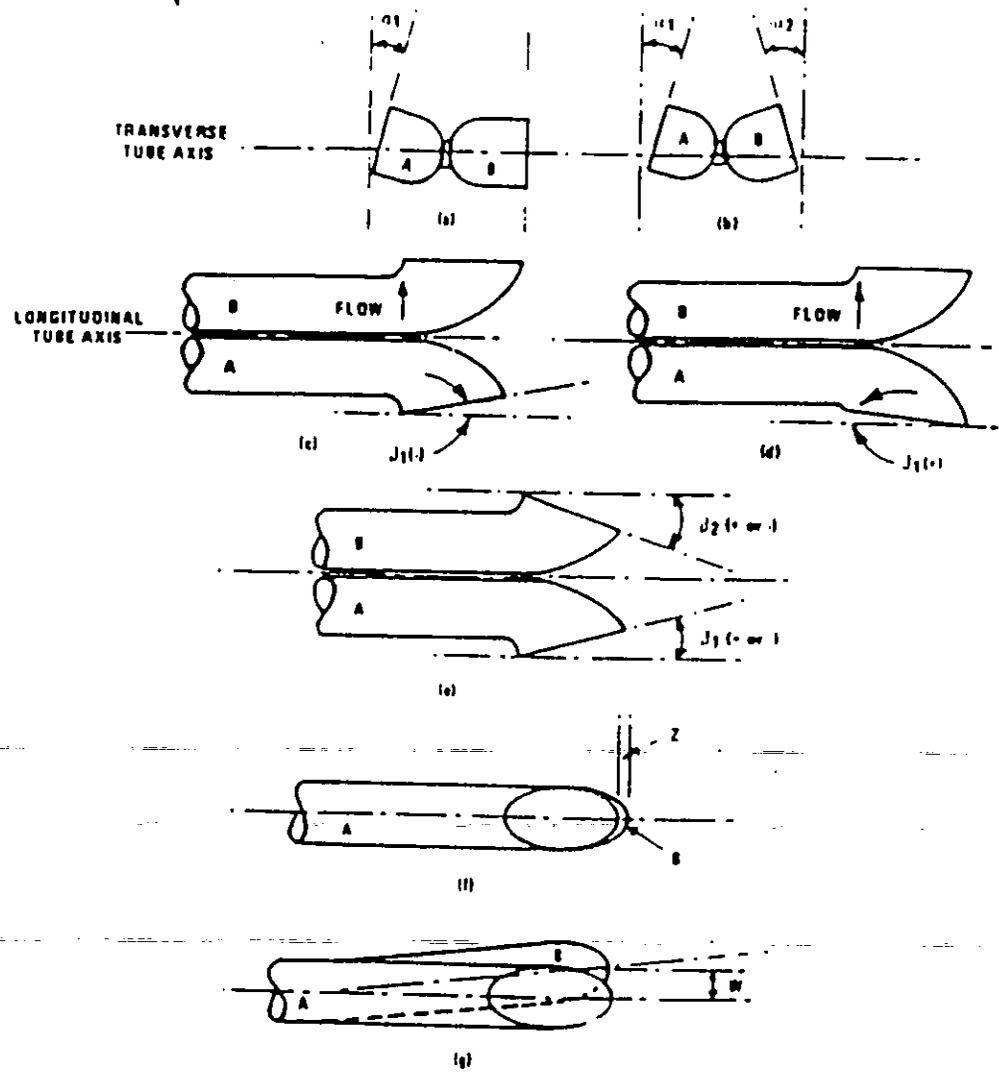


(c)

Properly constructed Type S pitot tube, shown in: (a) end view; face opening planes perpendicular to transverse axis; (b) top view; face opening planes parallel to longitudinal axis; (c) side view; both legs of equal length and centerlines coincident, when viewed from both sides. Baseline coefficient values of 0.84 may be assigned to pitot tubes constructed this way.

Figure III-2  
 Proper Pitot Tube Configuration

Pitot # 51201  
 calibrated 12/13/93  
 by: Blane Day



Types of face-opening misalignment that can result from field use or improper construction of Type S pitot tubes. These will not affect the baseline value of  $C_p(s)$  so long as  $a_1$  and  $a_2 \leq 10^\circ$ ,  $\beta_1$  and  $\beta_2 \leq 5^\circ$ ,  $z \leq 0.32$  cm (1/8 in.) and  $w \leq 0.08$  cm (1/32 in.) (criterion 11 in Section 6).

$$\begin{aligned}
 a_1 &= 0^\circ & \beta_1 &= 1^\circ & z &= 0^\circ \\
 a_2 &= 0^\circ & \beta_2 &= 0^\circ & w &= 0^\circ
 \end{aligned}$$

Figure III-3  
 Improper Pitot Tube Configuration

**APPENDIX I**

**CALIFORNIA ARB CONTRACTORS PROGRAM CERTIFICATION CERTIFICATE**



State of California  
Air Resources Board  
Approved Independent Contractor  
Acurex Environmental Corporation

This is to certify that the company listed above has been approved by the Air Resources Board to conduct compliance testing pursuant to Section 91207, Title 17, California Code of Regulations, until June 30, 1994, for those test methods listed below:

ARB Source Test Methods:  
1, 2, 3, 4, 5, 10, 100(CO<sub>2</sub>, NO<sub>x</sub>, O<sub>2</sub>, SO<sub>2</sub>, THC)  
Visible Emissions Evaluation

  
James J. Morgester, Chief  
Compliance Division

  
Laura McKinney, Manager  
Investigation and Certification Section